

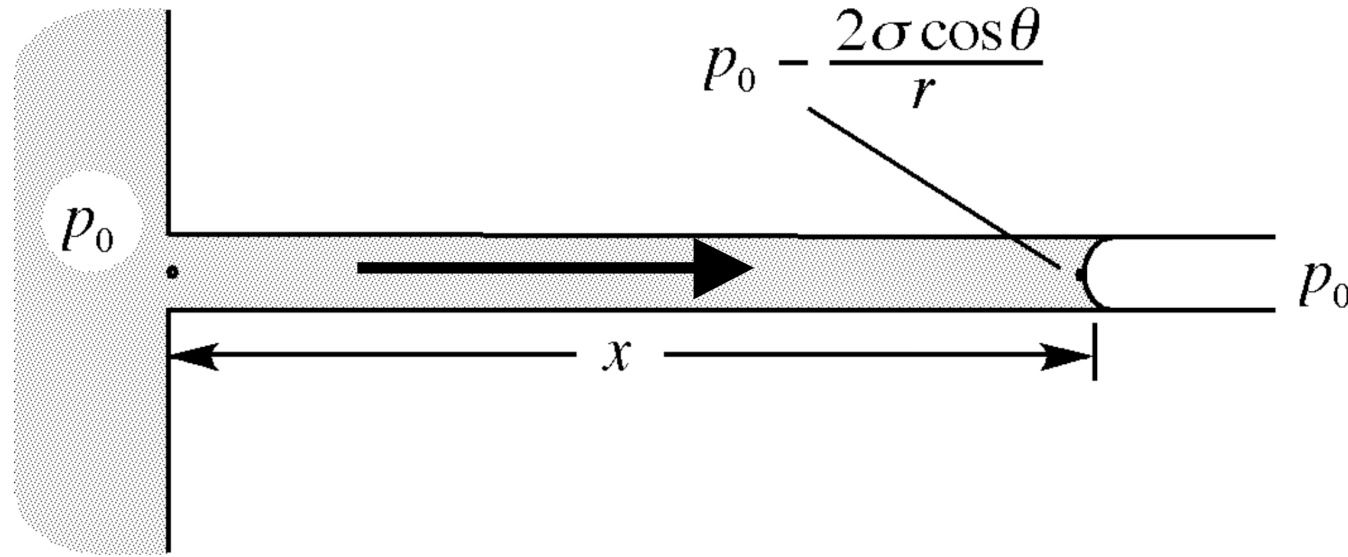
Wicking Flow in Porous Media

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Surface and Colloid Science

Wicking flow in a horizontal tube is driven by Young-Laplace pressure gradient



- Young-Laplace equation

$$\Delta p_c = \frac{2\sigma}{R_m}$$

- Part-of-sphere approx

$$R_m = \frac{r}{\cos \theta}$$

Washburn equation is derived from Hagen-Poiseuille equation

- Hagen-Poiseuille equation

$$v = \frac{r^2}{8\mu} \frac{dp}{dx}$$

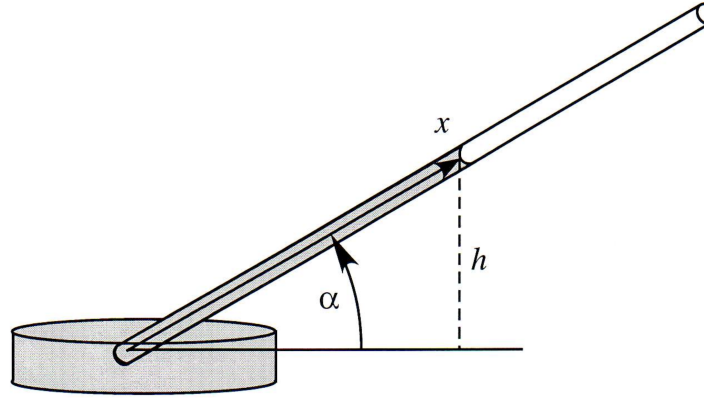
- Washburn equation

$$x = k_W \sqrt{t}$$

- Washburn constant

$$k_W = \sqrt{\frac{r \sigma \cos \theta}{2\mu}}$$

Wicking flow in an inclined tube is affected by gravity



- Pressure drop

$$\Delta p = \Delta p_c - \rho g h$$

- Rise height

$$H = \frac{2\sigma \cos \theta}{\rho g r}$$

- Wicking distance

$$X = \frac{H}{\sin \alpha} = \frac{2\sigma \cos \theta}{\rho g r \sin \alpha}$$

Wicking distance with respect to time in an inclined tube

- Hagen-Poiseuille equation

$$v = \frac{r^2}{8\mu} \frac{dp}{dx}$$

- Integrate

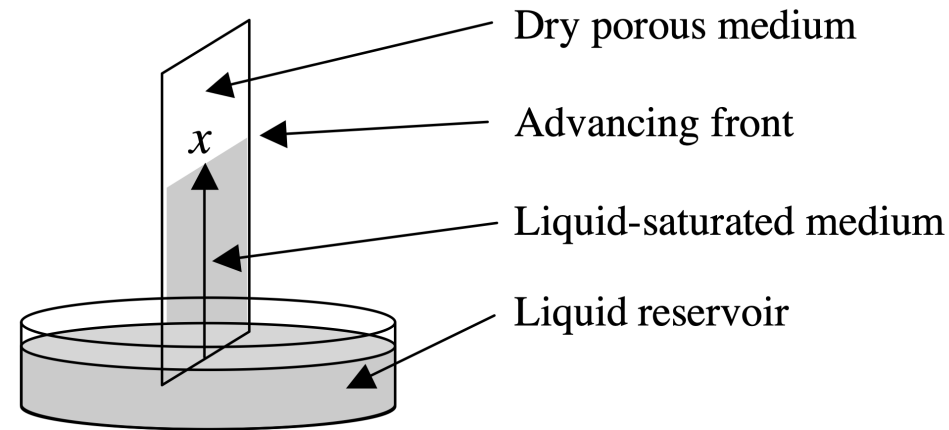
$$t = \frac{8\mu X}{\rho g r^2 \sin \alpha} \left[-\ln \left(1 - \frac{x}{X} \right) - \frac{x}{X} \right]$$

- Taylor series approximation

$$t \approx \frac{8\mu X}{\rho g r^2 \sin \alpha} \left[\frac{1}{2} \left(\frac{x}{X} \right)^2 + \mathcal{O} \left(\frac{x}{X} \right)^3 \right]$$

Reduces to Washburn equation when x/X is small

Wicking flow in porous media can be approximated by Washburn analysis



- Δp_c varies point to point, but Washburn analysis is good approx

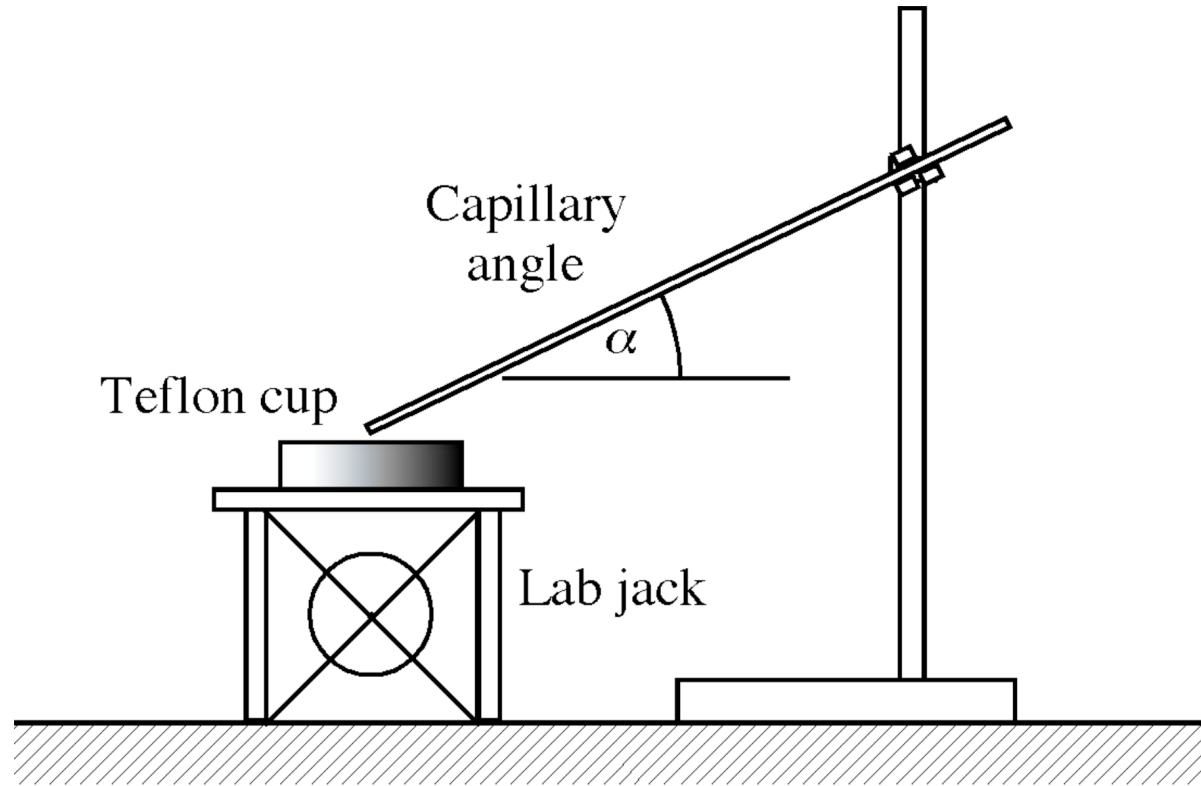
$$k_W = \sqrt{\frac{r_W \sigma \cos \theta}{2\mu}}$$

- r_W - Wicking equivalent radius, effective cylindrical pore radius for Washburn analysis
 - One order of magnitude smaller than actual pore radius
 - Tortuosity correction - replace x as τx

$$x = \sqrt{\frac{r \sigma \cos \theta}{2\tau\mu}} t = \sqrt{\frac{r_W \sigma \cos \theta}{2\mu}} t \implies r_W = \frac{r}{\tau}$$

- Gravity effect negligible due to small pore radius

Experimental setup



- **Wear safety goggles at all times!**
- Variables: liquid, capillary radius, tilt angle