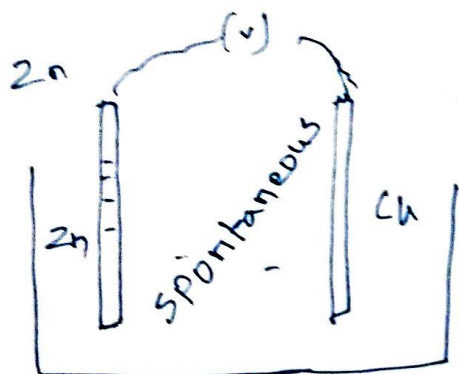


9, 18, 32
25, 28, 32, 34

Electrochem cell

Chem Energy \downarrow
Electrical Energy

Battery, Daniel cell



Anode

Zn - oxidation $\rightarrow e^-$

(-) ve sign

Cathode

Cu - Reduction - (+)

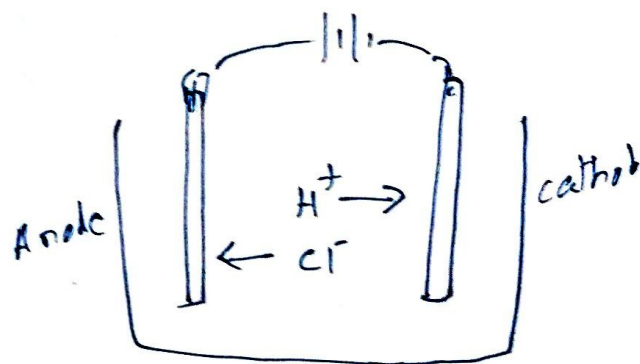
(+) ve sign

Electrolytic cell

Electrical Energy
 \downarrow

Chemical Energy

Electroplating etc..



Anode - oxidation

(+) ve electrode.



Cathode - Reduction

e^- -rich



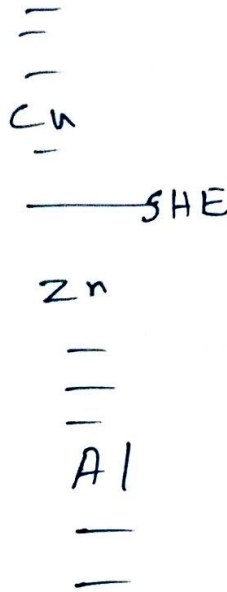
Factors influencing Corrosion rate

(1) Potential difference between the metals

EMF

Cu - Zn - less
Corrosion

Cu - Al - More
Corrosion



(2) Area Effect

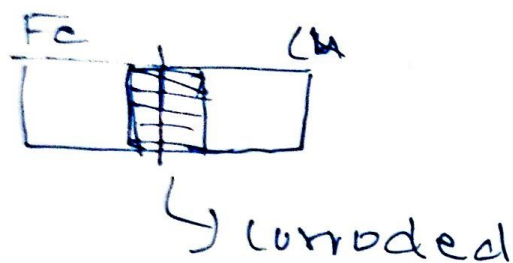
$$\text{Corr. Rate} \propto \frac{\text{Area of Cathode}}{\text{Area of Anode}}$$

$$\text{Rate} = \frac{\text{M.I.P. Per Year}}{\text{M.P.Y}}$$

Cathode - e^- demanding

Anode - e^- donating

3. Distance Effect



4. Purity

Homogeneous - Zn \rightarrow no corrosion

Heterogeneous - Zn / trace Cu

\rightarrow corrosion high

5. Corrosion product

soluble - more corrosion

Insoluble - less corrosion

oxide layer \rightarrow

Corrosion Control

① Material selection

noble metals, Pure Metals

Suitable Alloy

Al - Fe

↓
corrodes $\rightarrow v = 0.8v$

Al - Cr - Fe

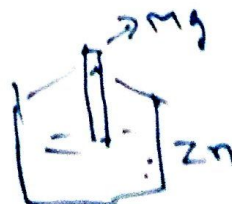
↓ \rightarrow less difference

less corrosion

② Sacrificial Anode

metal - even more oxidative

Zn - corrodes.



Mg - placed - Zn protected

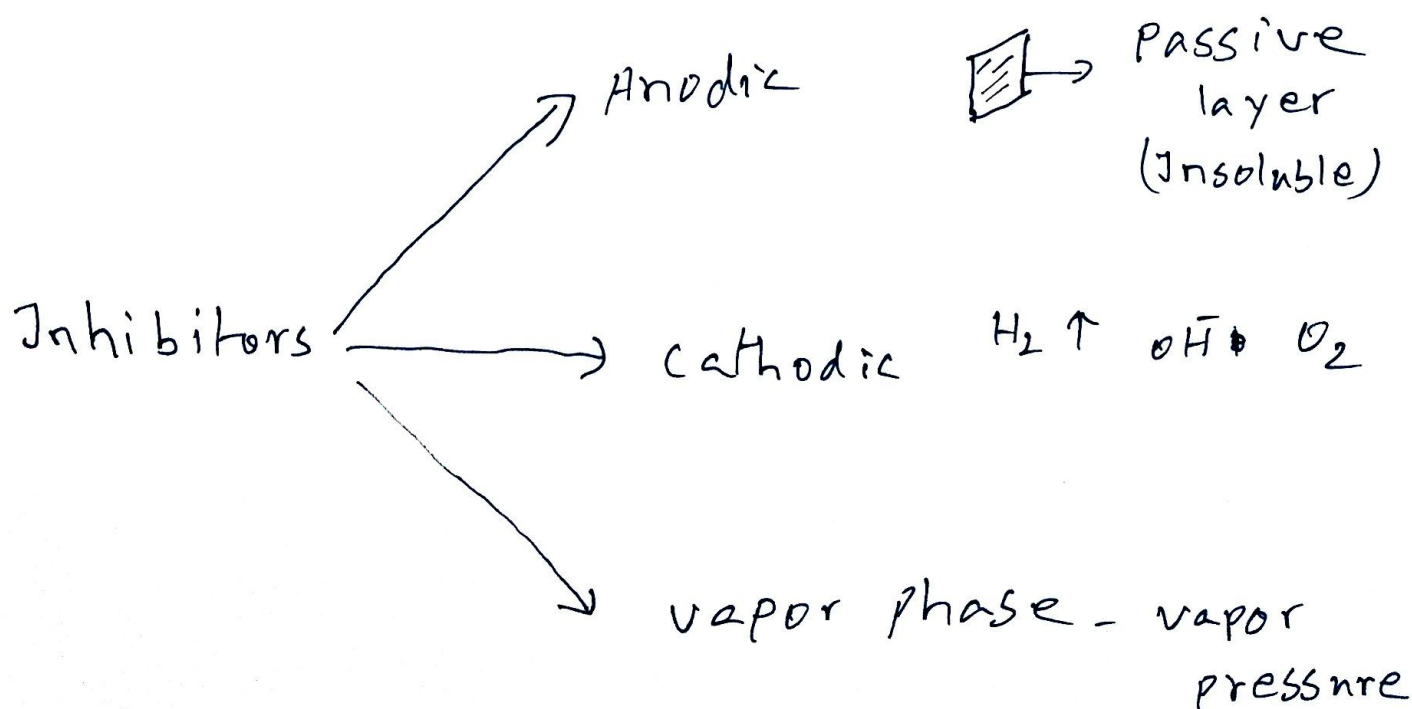
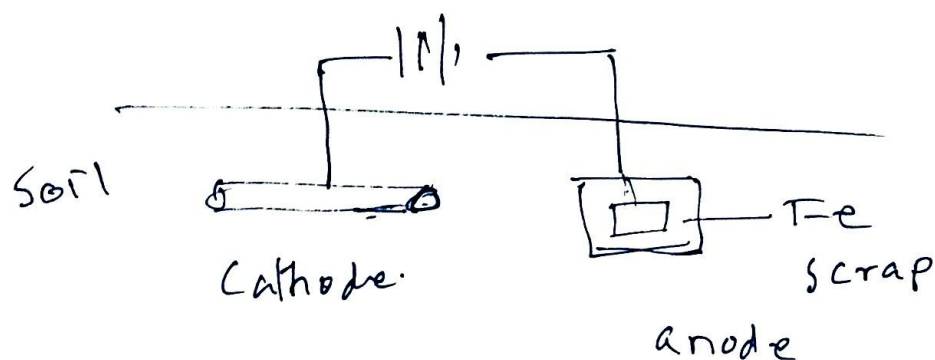


② External current impression

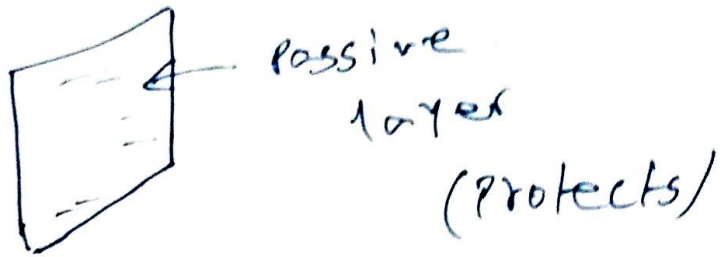
Electrolytic cell approach

Corroding metal \rightarrow made as cathode

Scrap iron/graphite \rightarrow Anode.



Anodic inhibitor



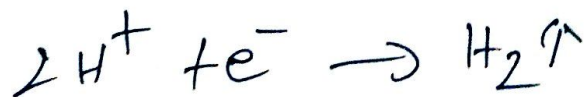
If any breaking



entire quantity of e^-
would be from smaller
area

Cathodic

Acidic



Diffusion of H^+ - controlled

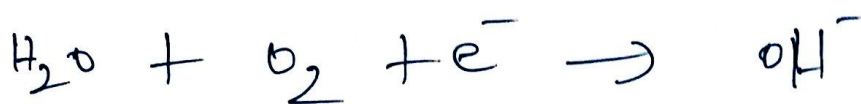
Power voltage - increased

Forming layer \leftarrow 

Over voltage \rightarrow H_2 evolution potential

\downarrow
vary metal to metal

Neutral / Alkaline



How controlled?

\swarrow elimination

(or)

retarding the
diffusion

Elimination

