



A model-based greenhouse design method

Bram Vanthoor

Propositions

1. Since results from the past do not provide guarantees for the future, one should focus on the harvest rate instead of cumulative yield when using sensitivity analysis techniques. (this thesis)
2. Optimal greenhouse design requires optimal climate control. (this thesis)
3. Not-field-related publications stimulates the scientist's creativity better than field-related publications.
4. Just like horticultural crops, the health of human beings will benefit by regular analysis of their drain, for example following each visit to the toilet.
5. People will develop better sensors if they are not influenced by their own senses.
- 6 .The human race does not have a shortage of energy, only an energy conversion problem; energy can simply not be lost.
7. The increase in communication means results in a more individualistic society.
8. According to Johan Cruijff simple soccer is the most difficult to play, and unfortunately, this also applies to simple modelling.

Propositions belonging to the PhD thesis of B.H.E. Vanthoor entitled: '*A model-based greenhouse design method*'.

Wageningen, June 17, 2011

Stellingen

1. Aangezien resultaten uit het verleden geen garanties bieden voor de toekomst, moet men bij gevoeligheidsanalyses focussen op de oogstsnelheid in plaats van op de cumulatieve oogst. (dit proefschrift)
2. Optimaal kasontwerp vereist een optimale klimaatregeling. (dit proefschrift)
3. Niet-vakgerelateerde publicaties stimuleren de creativiteit van een wetenschapper beter dan vakgerelateerde publicaties.
4. Net zoals bij kasplanten zal de gezondheid van mensen verbeteren als hun drain regelmatig wordt geanalyseerd, bijvoorbeeld bij ieder toiletbezoek.
5. Mensen ontwikkelen betere sensoren als ze zich niet laten beïnvloeden door eigen zintuigen.
6. De mensheid heeft geen energietekort, maar een energieconversie probleem; energie kan immers niet verloren gaan.
7. De toename van communicatiemiddelen leidt tot meer individualisme in de maatschappij.
8. Volgens Johan Cruijff is simpel voetballen het moeilijkst, dit geldt helaas ook voor simpel modelleren.

Stellingen behorende bij het proefschrift: '*A model-based greenhouse design method*', van B.H.E Vanthoor.

Wageningen, 17 juni 2011

A model-based greenhouse design method

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A model-based greenhouse design method

Bram H.E. Vanthoor

Thesis

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Chapter 1

General introduction and outline of the thesis

1.1 Background and motivation

Large greenhouse areas can be found all over the world, as presented in Table 1.1. This worldwide spread of greenhouses was caused by several beneficial reasons. A greenhouse protects the crop against pests, insects and extreme climate conditions such as heavy precipitation and wind. Moreover, the shelter around the crop enables an aerial environment somewhat independent from the outdoor climate. In high-technology greenhouses, one can adapt the light level, temperature, CO₂ concentration and relative humidity to the needs of the crop. These advantages result in higher crop yields, higher quality and longer production periods than field production. In addition, compared to open field production, the resource use efficiency of a greenhouse is higher. For example, water use efficiency is several times higher thanks to the combination of a much higher productivity and a lower transpiration rate. Moreover, fewer nutrients are leached if a recirculation irrigation system is installed.

Table 1.1 The production area of plastic greenhouses and glasshouses all over the world (source: Giacomelli et al., 2008).

Location	Plastic greenhouses (Ha)	Glasshouses (Ha)	Total (Ha)
Western Europe	140,000	29,000	169,000
Eastern Europe	25,000	1,800	26,800
Africa	27,000	600	27,600
Middle East	28,000	13,000	41,000
North America	9,850	1,350	11,200
Central/South America	12,500	0	12,500
Asia/Oceania	450,000	2,500	452,500
Total area	692,350	48,250	740,600

An enormous variety of protected cultivation systems can be found throughout the world (Fig. 1.1). They range from fully passive “solar greenhouses” with thick energy storage walls as found in China (Sun *et al.*, 2006) to the high-tech “closed greenhouses” without ventilation openings in Western Europe (Heuvelink *et al.*, 2008).



Fig. 1.1 Different greenhouses in China (a), The Netherlands (b), Spain (c) and Saudi Arabia (d).

The particular choice of a protected cultivation system depends on many factors, as demonstrated by Hanan (1998) and Van Heurn and Van der Post (2004). Van Henten *et al.* (2006) combined and extended their list of factors to: (1) market size and regional infrastructure which determines the opportunity to sell products as well as the costs associated with transportation; (2) local climate; (3) availability, type and costs of fuels and electric power; (4) availability and quality of water; (5) soil quality; (6) availability and cost of land; (7) availability of capital; (8) the availability and cost of labour as well as the level of education; (9) the availability of materials, equipment and service level; (10) legislation in terms of food safety, residuals of chemicals, the use and emission of chemicals to soil, water and air. In line with these factors, Von Elsner *et al.* (2000) stated that the variety of greenhouses is caused by the adaption of greenhouses to climatic, economic and social conditions. An example of the impact of the temperature and the global radiation on climate modification techniques is presented in Fig. 1.2 for Beijing China, De Bilt The Netherlands, and Almeria Spain. This figure shows that in the relatively dark and cold Dutch climate artificial photosynthetic lighting and a heating system might be useful whereas in the relatively sunny and hot climate in Spain an appropriate cooling technique might be beneficial.

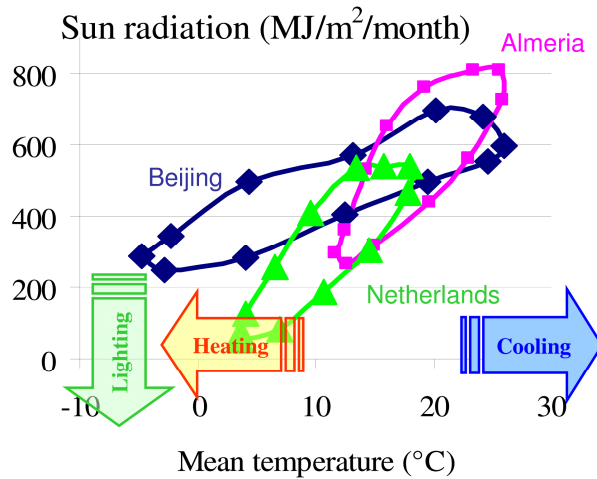


Fig. 1.2 The monthly mean outdoor temperature (x-axis) and the global radiation sum (y-axis) for three different climate zones, i.e. Beijing China, De Bilt The Netherlands and Almeria, Spain. The arrows indicate when a specific climate modification technique might be beneficial.

The fast development of commercial greenhouse horticulture has resulted in many techniques to modify the indoor climate (Berenschot, 2004) as presented for Dutch conditions in Fig. 1.3.

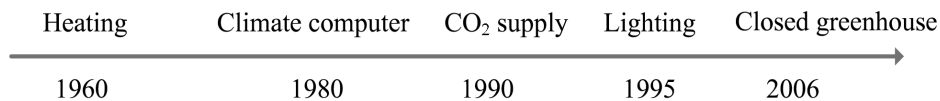


Fig. 1.3 Timing of the introduction of climate modification techniques in Dutch greenhouses.

The enormous variety of boundary conditions and design elements makes greenhouse design a complex task. Von Elsner *et al.* (2000) concluded that optimisation of a greenhouse design with respect to local climatic and economic conditions still remains a challenge for the designer. As suggested by Baille (1999) a systematic approach that integrates physical, biological and economical models is the most promising way for strategic decision making on greenhouse configurations given the wide variety of climate conditions on a worldwide scale. Such a method would be beneficial for several reasons.

First, a designer is unable to take into account all relevant boundary conditions and design elements which results often in sub-optimal designs. For areas where greenhouse horticulture is less developed, the systematic approach could support the design process so

that suitable greenhouses for the given local conditions are produced. For areas where greenhouse horticulture is more developed, the systematic approach can re-evaluate existing greenhouse designs to check whether and how they might be improved further. In addition, a systematic design procedure might indicate how greenhouses might evolve in the face of future changes in economic conditions, such as product and resources prices.

Second, sensitivity analysis applied in such a systematic approach might pinpoint the key factors for greenhouse design which increases our understanding of the design process. In addition, the properties of greenhouse materials that should be modified so that growers gain extra revenues could be revealed. The manufacturers then would know which properties should be optimised and what would be the economic margin for this modification. Additionally, this systematic approach might even identify whether adjustable design parameters over time as proposed by e.g. Sonneveld *et al.* (2011) would be beneficial.

Third, the systematic approach might indicate the decisive factors why greenhouses have evolved to totally different designs at different locations. Furthermore, the impact of uncertain boundary conditions on greenhouse design can be evaluated.

However, when the current state in greenhouse design is considered, most studies have focused on optimising the design for a specific location, or they considered only a single design parameter (Zaragoza *et al.*, 2007; Campen, 2005; Sonneveld *et al.*, 2006; Kacira *et al.*, 2004; Engel, 1984; Amir & Hasegawa, 1989). To the best of our knowledge, a model-based methodology to design protected cultivation systems for the wide variety of conditions that exist around the world is thus not yet available.

1.2 Research objective

The objective of this thesis is to develop a method that produces a greenhouse design suitable for the given local climatic and economic conditions. In principle, this methodology should work for the wide variety of conditions that can be found throughout the world.

1.3 Scope of the research

As described before, the particular choice of a protected cultivation system depends on many factors. Therefore, to keep this research manageable, we focus on the following aspects. The climatic and economic conditions are used as boundary conditions and the design problem is narrowed down to techniques that influence the aerial climate. In particular, this study focuses on the following eight design elements: the type of greenhouse structure, the cover type, the outdoor shade screen, the whitewash, the thermal screen, the heating system, the cooling system and the CO₂ enrichment system. Tomato is selected as model crop since it is one of the most widely produced greenhouse vegetables in the world and knowledge about tomato yield modelling is well established.

1.4 Model-based design approach

According to Van Henten *et al.* (2006) greenhouse design can be addressed as a multi-factorial optimisation problem. Such an approach relies on a quantitative trade-off between the economic return of the crop and the costs associated with construction, maintenance and operation of the greenhouse facility. Design optimisation has been used intensively to solve complex problems in other application domains e.g. aerospace engineering (William Begg & Liu, 2000; Anthony & Keane, 2003), automobile design (Yildiz *et al.*, 2004), electronics (Abido, 2002) and cold stores design (Lukasse *et al.*, 2009). Using optimisation techniques to solve the multi-factorial greenhouse design problem thus seems promising. Therefore, a model-based greenhouse design method as presented in Fig. 1.4 was developed. The key components of the method are a greenhouse climate model, a tomato yield model, an economic model and an optimisation algorithm. The three models are used to determine the net financial result as a function of outdoor climate, greenhouse design, climate management and economic variables. The optimisation algorithm adjusts the greenhouse in such a way that a maximum net financial result will be obtained. Since our aim is to develop a design method that focuses on the optimisation of the set of design elements, aspects that might be relevant for other design aspects will be neglected or simplified. Due to the generic nature of the model-based design method, new modules can easily be implemented whenever they become available.

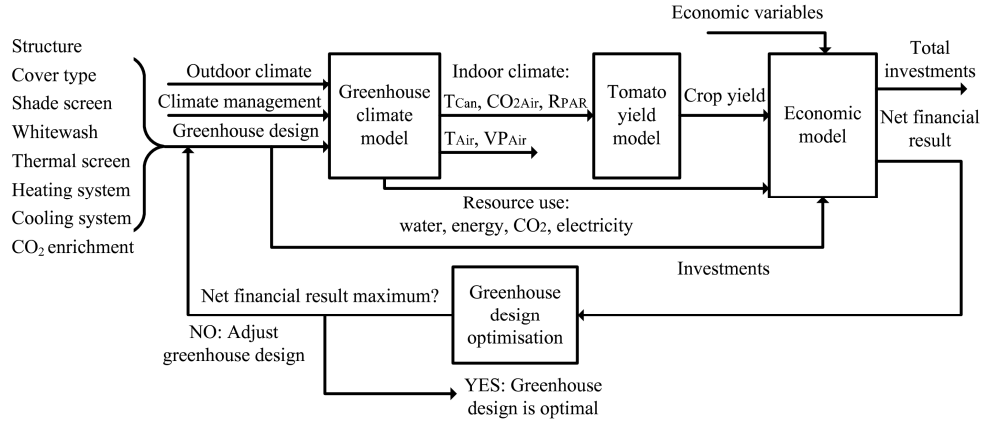


Fig. 1.4 An overview of the model-based greenhouse design method. This method selects the set of alternatives to fulfil the eight design elements presented at the left-hand side to yield the largest annual net financial result. The method consists of four key components, i.e. the greenhouse climate model, the tomato yield model, the economic model and the design optimisation algorithm. The applied performance measure is the annual net financial result.

1.5 Thesis outline

The four key components of the model-based design method (Fig. 1.4) and a sensitivity analysis are each described in a chapter. In **Chapter 2**, the greenhouse climate model that determines the indoor climate as a function of outdoor climate, climate management and greenhouse design is presented. Requirements related to the model formalism are presented and the design elements that are sufficiently generic for worldwide greenhouse design are selected and described in model equations. The dynamic model is validated for four different greenhouse designs under three climate conditions: a temperate marine climate, a Mediterranean climate and a semi-arid climate to assure that it is sufficiently accurate and generic to be incorporated in the model-based design method.

Chapter 3 describes the model to calculate the tomato yield as a function of the predicted indoor climate. Requirements related to the model formalism are presented and relevant yield model aspects are revealed in view of the model-based design method. Temperature effects on tomato yield are reviewed and are implemented in the model. The model is then validated for four different temperature regimes.

In **Chapter 4** three sensitivity analysis techniques are applied to the combined greenhouse climate-tomato yield model to indicate the most relevant design aspects and to increase our understanding of the design process. The sensitivity analysis quantifies the impact of parameters on the harvest rate, resource consumption and indoor climate for a low-tech greenhouse in Almeria, Spain and a high-tech greenhouse in Texas, USA. The single-variate sensitivity analysis pinpoints design parameters that are candidates for improvement. The multi-variate sensitivity analysis reveals the parameters that will have a joint effect on crop yield. The analysis of the seasonal impact of parameters indicates whether adjustable design properties might increase greenhouse performance.

Chapter 5 presents the economic model that determines the annual net financial result as a function of crop yield, the resource use and the depreciation and maintenance of the construction. The economic model is joined with the greenhouse climate-tomato yield model to identify – among a predefined set of design alternatives – the greenhouse with the highest annual net financial result for tomato production under South-Spanish conditions. This analysis reveals which greenhouse technology level will perform best in South Spain. This procedure is repeated for different outdoor climate trajectories and tomato price trajectories to demonstrate how the best design will change with changing local conditions. A sensitivity analysis presents the extra revenue of a grower caused by a modification of a specific design parameter. In addition, the impact of uncertainty in input parameters, i.e. economic parameters and climate set-points on net financial result is determined to analyse their impact on greenhouse design.

Chapter 6 presents an optimisation algorithm to solve the multi-factorial design problem. Requirements of the algorithm are described. The controlled random search algorithm of Price (1977) using parallel computing, optimises the greenhouse design in order to maximise the financial result. To demonstrate that the model-based design method is able to modify the design to local condition, the greenhouse is optimised for Southern Spanish and Dutch conditions. Subsequently, two techniques evaluate the population of designs that would give similar returns so that the most relevant design elements are revealed.

In **Chapter 7**, the results of this work are evaluated and discussed in view of the initial objective. Recommendations to improve the performance and generality of the method are presented and future opportunities of the model-based design method are given.

Chapter 2

A greenhouse climate model for a broad range of designs and climates

The contents of this chapter are accepted for publication in Biosystems Engineering as a paper entitled: *A methodology for model-based greenhouse design: Part 1, A greenhouse climate model for a broad range of designs and climates.*

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2.1 Abstract

With the aim of developing a model-based method to design greenhouses for a broad range of climatic and economic conditions, a greenhouse climate model was developed and validated. This model describes the effects of the outdoor climate and greenhouse design on the indoor greenhouse climate. For use in a greenhouse design method that focused on the optimisation of a set of design elements, the model should fulfil the following three requirements: 1) predict the temperature, vapour pressure and CO₂ concentration of the greenhouse air, with sufficient accuracy for a wide variety of greenhouse designs under varying climate conditions, 2) include the commonly used greenhouse construction parameters and climate conditioning equipment, and 3) the model should consist of a set of differential equations to assure that it can be combined with a tomato yield model (of a similar structure) and to allow the use of ordinary differential equation solvers. The dynamic model was validated for four different greenhouse designs under three climatic conditions: a temperate marine climate, a Mediterranean climate and a semi-arid climate. For these conditions, the model accurately predicted the greenhouse climate for all four designs without modification of the model parameters (except for one case). In more than 78% of the cases, comparison of simulations and measurements of the indoor climate yielded a relative root mean square error of less than 10%. Given these results, the model is considered to be sufficiently accurate and sufficiently generic to be used for developing a model-based greenhouse design method.

2.2 Introduction

This chapter contains a description and validation of the greenhouse climate model. This model describes the effects of outdoor climate and the greenhouse design, including the above mentioned design elements, on the indoor greenhouse climate. The estimated indoor climate will be used as input for the tomato yield model. For use in a model-based greenhouse design method, the model should fulfil the following three requirements: (i) it should predict the greenhouse climate: temperature, vapour pressure and CO₂ concentration of the air with sufficient accuracy for a wide variety of greenhouse designs under varying climate conditions, without modification of model parameters, (ii) it should include the commonly used greenhouse design elements to control the indoor climate, so that it can be used to design greenhouses for worldwide conditions, (iii) the model should consist of a set of differential equations since it will be combined with a tomato yield model consisting of a set of differential equations and to allow the use of ordinary differential equation solvers. In addition, the right-hand sides must be continuously differentiable to speed up the simulation and to assure that gradient-based dynamic optimisation algorithms can be applied to the model.

Greenhouse climate models have received considerable attention in the literature in recent decades (Bot, 1983; Luo *et al.*, 2005; Impron *et al.*, 2007; De Zwart, 1996; Ooteghem, 2007; De Halleux *et al.*, 1991; Baptista, 2007), but all these authors focused on a single location and a limited and specific set of construction and climate modification elements. Recently, Fitz-Rodríguez *et al.* (2010) developed a greenhouse environmental model for educational purposes which was applicable to different design configurations and geographic locations. However, this model was not validated and some model fluxes relevant for the present purpose of greenhouse design were missing. Therefore, by building on the work of Bot (1983) and De Zwart (1996), in our study a more generic greenhouse model was developed and validated for a wide range of greenhouse designs and climates. The following climates were selected to validate the model: a temperate marine climate (northwest part of The Netherlands); a Mediterranean climate, (Sicily, Italy); and a semi-arid climate (Arizona and Texas, USA).

2.3 Model description

Section 2.3.1 presents the design elements included in the greenhouse climate model. A concise model description is presented in the section 2.3.2. A detailed description of the greenhouse climate model with all the individual mass and energy flows can be found in chapter 8.

2.3.1 Greenhouse design elements

Since the focus of the design method is on optimisation of a set of design elements, the selected functions and techniques presented in Fig. 2.1 were incorporated in the greenhouse climate model. In this model, the greenhouse functions heating, insulation, shading, cooling, CO₂ enrichment, humidification and de-humidification are fulfilled by one or more techniques. For example, the function heating might be fulfilled by the following techniques: a direct air heater, a boiler, an industrial heat source, a geothermal source and a passive buffer.

For the development of a model-based design method, these techniques are considered to be sufficiently generic for a wide range of locations all over the world. Specific local solutions for energy production, energy conversion or climate modification, such as co-generation of heat and electricity, artificial photosynthetic lighting, an active heat buffer, a heat pump and a solar heat collector, lie outside the scope of this study.

2.3.1.1 Notational conventions

All the state variables, fluxes, inputs, superscripts and subscripts are listed in the Nomenclature in section 2.8. Following the notational conventions of De Zwart (1996), the state variables of the model are denoted by names with capital letters followed by one subscript, e.g. T_{Air} . The model fluxes start with a capital letter and are followed by two subscripts. The first subscript represents the source of the flux and the second subscript represents the destination of the flux, e.g. H_{CanAir} . The radiation fluxes start with a capital letter R followed with the type of radiation and then two subscripts to represent the source and sink of the specific radiation, i.e. R_{PAR_SunCan} .

2.3.2 Model overview and state variables

2.3.2.1 Model overview and assumptions

An overview of the state variables and the energy and mass fluxes of the greenhouse model are shown in Fig. 2.2. The model was based on the following assumptions: 1) the greenhouse air is considered to be a “perfectly stirred tank”, which means that there are no spatial differences in temperature, vapour pressure and the CO₂ concentration; therefore, all the model fluxes were described per square metre of greenhouse floor; 2) to describe the effect of the thermal screen on the indoor climate, the greenhouse air was divided into two compartments: one below and one above the thermal screen.

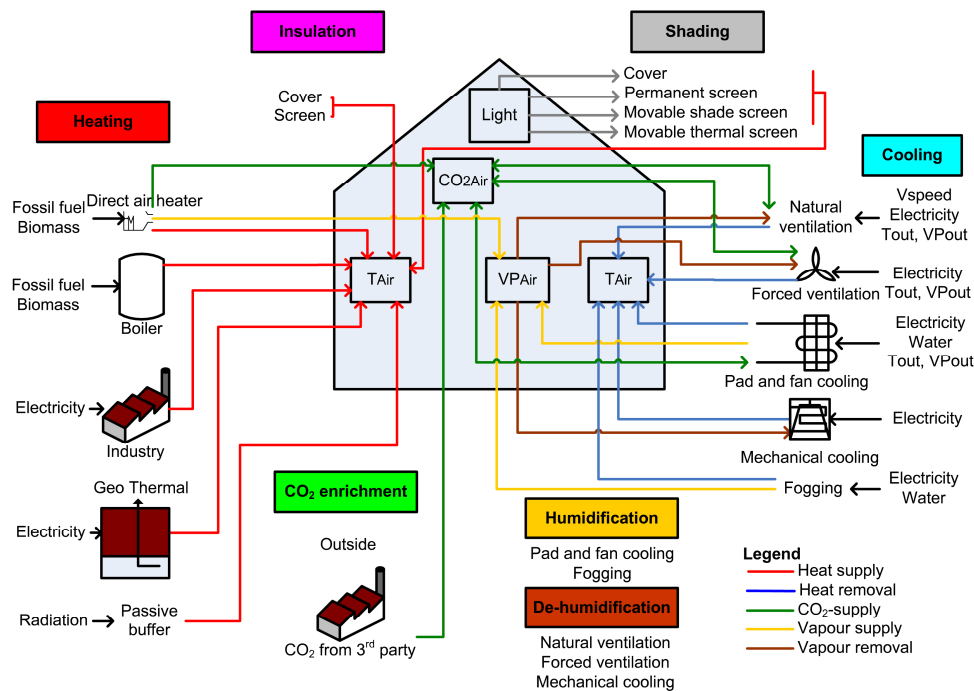


Fig. 2.1 Selected functions (coloured boxes), and design elements (text blocks and pictures below the accompanying functions), needed for the greenhouse design method to manage the greenhouse climate (transparent boxes inside the greenhouse). The coloured arrows represent the various energy and mass fluxes (legend at the bottom right).

This model was based on the greenhouse climate modelling study of De Zwart (1996). For the current purpose of greenhouse design, extra model elements were added and some

model parts were simplified. The following model elements were implemented: the design elements presented in Fig. 2.1; a lumped cover description to combine the impact of different cover layers on indoor climate; the internal and external cover temperature are state variables of the model to describe the impact of cover insulation on indoor climate; a description of the far infrared radiation (FIR) transmission through the cover, which is needed for films that partially transmit FIR; a description of both roof and side ventilation; a description of the impact of insect screens on ventilation rate; and a description of the near infrared radiation (NIR) absorption of both canopy and floor, which depend on the optical properties of the cover and floor. Since optimisation of the properties of the greenhouse structure i.e. dimensions of the greenhouse, roof slope and orientation and location of the vents, exceeded the purpose of our design method, the model was simplified by making no distinction between diffuse and direct solar radiation and by assuming that the transmission coefficient of the greenhouse cover did not depend on solar angle.

Because of space limitations, the model fluxes are described in detail in the detailed model description as presented in Chapter 8. A brief description of some relevant fluxes is given here. Assuming a non-limiting irrigation strategy, the transpiration rate of a tomato crop was determined based on the transpiration and stomata model of Stanghellini (1987). The CO₂ fluxes caused by canopy activity, i.e. photosynthesis rate, maintenance and growth respiration, were described in chapter 3. The ventilation rate function was based on equations of Boulard and Bailie (1995) and Kittas *et al.* (1997).

2.3.2.2 State variables of the model

The state variables of the model are all described by differential equations. The derivatives of the state variables to time are indicated by a dot above the state symbol.

2.3.2.2.1 Temperature of different greenhouse components

Canopy temperature T_{Can} is described by:

$$cap_{Can} \dot{T}_{Can} = R_{PAR_SunCan} + R_{NIR_SunCan} + R_{PipeCan} - H_{CanAir} - L_{CanAir} - R_{CanCov,in} - R_{CanFlr} - R_{CanSky} - R_{CanThScr} \quad [W m^{-2}] \quad (2.1)$$

where cap_{Can} is the heat capacity of the canopy, R_{PAR_SunCan} is the PAR absorbed by the canopy, R_{NIR_SunCan} is the NIR absorbed by the canopy. FIR is exchanged between the canopy and surrounding elements i.e. the heating pipes $R_{PipeCan}$, the internal cover layer $R_{CanCov,in}$, the floor R_{CanFlr} , the sky R_{CanSky} , and the thermal screen $R_{CanThScr}$. H_{CanAir} is the sensible heat exchange between canopy and greenhouse air and L_{CanAir} is the latent heat flux caused by transpiration.

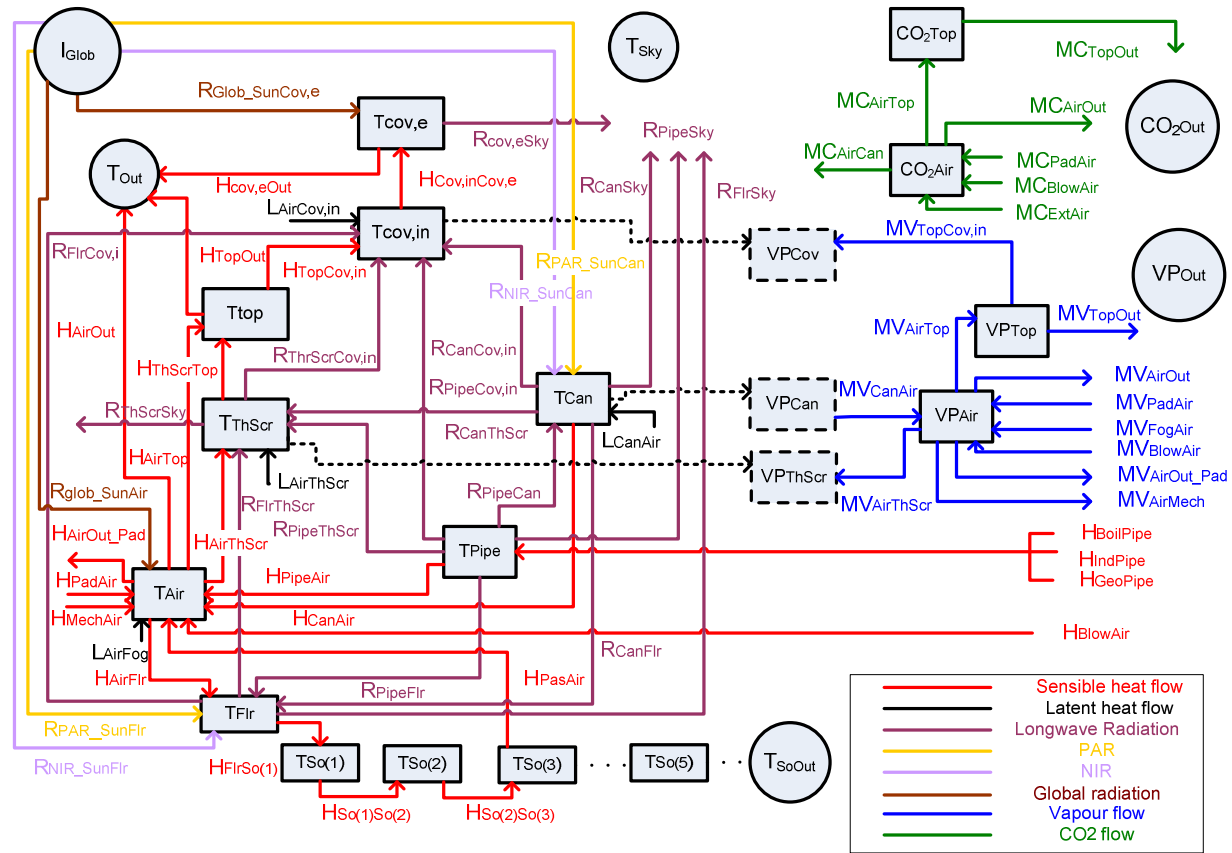


Fig. 2.2 Overview of the state variables (blocks), semi-state variables (dotted blocks), external climate inputs (circles) and fluxes (arrows) of the greenhouse model. Coloured arrows represent the various energy and mass fluxes (legend at the bottom right). Abbreviations and their definitions are listed in the Nomenclature in section 2.8, and the underlying equations are presented in section 2.3.2.2.

The greenhouse air temperature T_{Air} is described by:

$$\begin{aligned} cap_{Air} \dot{T}_{Air} = & H_{CanAir} + H_{PadAir} + H_{MechAir} + H_{PipeAir} + H_{PasAir} + H_{BlowAir} + R_{Glob_SunAir} \\ & - H_{AirFlr} - H_{AirThScr} - H_{AirOut} - H_{AirTop} - H_{AirOut_Pad} - L_{AirFog} \end{aligned} \quad [W \ m^{-2}] \quad (2.2)$$

where cap_{Air} is the heat capacity of the greenhouse air. Sensible heat is exchanged between the greenhouse air and the surrounding elements i.e. the canopy H_{CanAir} , the outlet air of a cooling pad H_{PadAir} , the mechanical cooling system $H_{MechAir}$, the heating pipes $H_{PipeAir}$, the passive energy buffer H_{PasAir} , the direct air heater $H_{BlowAir}$, the floor H_{AirFlr} , the thermal screen $H_{AirThScr}$, the outdoor air H_{AirOut} , the air of the top compartment which is located above the thermal screen H_{AirTop} , and the outdoor air due to the air exchange caused by the pad and fan system H_{AirOut_Pad} . R_{Glob_SunAir} is the global radiation which is absorbed by the construction elements and which is released to the air and L_{AirFog} is the latent heat needed to evaporate the water droplets added by a fogging system.

The floor layer is the first layer of the greenhouse underground and its temperature T_{Flr} is described by:

$$\begin{aligned} cap_{Flr} \dot{T}_{Flr} = & H_{AirFlr} + R_{PAR_SunFlr} + R_{NIR_SunFlr} + R_{CanFlr} + R_{PipeFlr} \\ & - H_{FlrSol} - R_{FlrCov,in} - R_{FlrSky} - R_{FlrThScr} \end{aligned} \quad [W \ m^{-2}] \quad (2.3)$$

where cap_{Flr} is the heat capacity of the floor; R_{PAR_SunFlr} is the PAR absorbed by the floor; R_{NIR_SunFlr} is the NIR absorbed by the floor; $R_{PipeFlr}$, $R_{FlrCov,in}$, R_{FlrSky} and $R_{FlrThScr}$ are the FIR fluxes between the floor and heating pipes, internal cover layer, sky and thermal screen respectively; and H_{FlrSol} is the sensible heat flux from the floor to soil layer 1.

Because of the high thermal capacity, the soil was divided into five layers with an increasing thickness with increasing depth. The soil temperature $T_{So(j)}$ of layer 'j' is described by:

$$cap_{So(j)} \dot{T}_{So(j)} = H_{So(j-1)So(j)} - H_{So(j)So(j+1)} \quad j = 1, 2, \dots, 5 \quad [W \ m^{-2}] \quad (2.4)$$

where $cap_{So(j)}$ is the heat capacity of each soil layer, $H_{So(j-1)So(j)}$ is the conductive heat flux from layer 'j-1' to 'j' and $H_{So(j)So(j+1)}$ is the conductive heat flux from layer 'j' to 'j+1'. For the first soil layer, $H_{So(j-1)So(j)}$ is equivalent to H_{FlrSol} and for the last soil layer, $H_{So(j)So(j+1)}$ is equivalent to the conductive heat flux from the 5th soil layer to the external soil temperature $H_{So5SoOut}$.

Temperature of the thermal screen T_{ThScr} is described by:

$$cap_{ThScr} \dot{T}_{ThScr} = H_{AirThScr} + L_{AirThScr} + R_{CanThScr} + R_{FlrThScr} + R_{PipeThScr} - H_{ThScrTop} - R_{ThScrCov,in} - R_{ThScrSky} \quad [W m^{-2}] \quad (2.5)$$

where cap_{ThScr} is the heat capacity of the thermal screen; $L_{AirThScr}$ is the latent heat flux caused by condensation on the thermal screen; $R_{PipeThScr}$, $R_{ThScrCov,in}$ and $R_{ThScrSky}$ are the FIR fluxes between the thermal screen and the heating pipes, internal cover layer and sky respectively; and $H_{ThScrTop}$ is the heat exchange between the thermal screen and the top compartment air.

The air temperature of the compartment above the thermal screen T_{Top} , in this study denoted as the ‘top compartment’, is described by:

$$cap_{Top} \dot{T}_{Top} = H_{ThScrTop} + H_{AirTop} - H_{TopCov,in} - H_{TopOut} \quad [W m^{-2}] \quad (2.6)$$

where cap_{Top} is the heat capacity of the top compartment air, $H_{TopCov,in}$ is the heat exchange between the top compartment air and the internal cover layer and H_{TopOut} is the heat exchange between the top compartment and the outside air.

The thermal heat conductivity of the greenhouse cover is a greenhouse design parameter which can induce a significant temperature gradient over the cover. Therefore, both the internal cover temperature and external cover temperature have been modelled. Assuming that the heat capacity of the internal and external cover layer each constitute 10% of the heat capacity of the total cover construction, and assuming that conduction of energy is the dominant mode of energy transport between the internal and the external cover, the internal cover temperature $T_{Cov,in}$ and external cover temperature $T_{Cov,e}$ are described by:

$$cap_{Cov,in} \dot{T}_{Cov,in} = H_{TopCov,in} + L_{TopCov,in} + R_{CanCov,in} + R_{FlrCov,in} + R_{PipeCov,in} + R_{ThScrCov,in} - H_{Cov,inCov,e} \quad [W m^{-2}] \quad (2.7)$$

$$cap_{Cov,e} \dot{T}_{Cov,e} = R_{Glob_SunCov} + H_{Cov,inCov,e} - H_{Cov,eOut} - R_{Cov,eSky} \quad [W m^{-2}] \quad (2.8)$$

where $cap_{Cov,in}$ and $cap_{Cov,e}$ are the heat capacities of the internal and external cover layer respectively, $L_{TopCov,in}$ is the latent heat flux caused by condensation on the greenhouse cover, $R_{PipeCov,in}$ is the FIR exchange between the heating pipes and internal cover layer, $H_{Cov,inCov,e}$ is the heat flux between the internal and external cover layer, R_{Glob_SunCov} is the absorbed global solar radiation by the cover, $H_{Cov,eOut}$ is the sensible heat flux from the external cover layer to the outside air and $R_{Cov,eSky}$ is the FIR exchange between the cover and the sky.

In this model, besides using a direct air heater, heat energy can be added to the greenhouse air using hot water heating pipes (Fig. 2.2). The surface temperature of the heating pipe system T_{Pipe} is described by:

$$\begin{aligned} cap_{Pipe} \dot{T}_{Pipe} = & H_{BoilPipe} + H_{IndPipe} + H_{GeoPipe} - R_{PipeSky} - R_{PipeCov,in} \\ & - R_{PipeCan} - R_{PipeFlr} - R_{PipeThScr} - H_{PipeAir} \end{aligned} \quad [W m^{-2}] \quad (2.9)$$

where cap_{Pipe} is the heat capacity of the heating pipes, $H_{BoilPipe}$ is the boiler heat flux to the pipes, $H_{IndPipe}$ is the industrial heat flux to the pipes, $H_{GeoPipe}$ is the geothermal heat flux to the pipes and $R_{PipeSky}$, is the FIR exchange between the pipes and sky.

2.3.2.2.2 Vapour pressure of the greenhouse air and the air in the top compartment

The vapour pressure of the greenhouse air VP_{Air} is described by:

$$\begin{aligned} cap_{VP_{Air}} \dot{VP}_{Air} = & MV_{CanAir} + MV_{PadAir} + MV_{FogAir} + MV_{BlowAir} - MV_{AirThScr} \\ & - MV_{AirTop} - MV_{AirOut} - MV_{AirOut_Pad} - MV_{AirMech} \end{aligned} \quad [kg m^{-2} s^{-1}] \quad (2.10)$$

where $cap_{VP_{Air}}$ is the capacity of the air to store water vapour. Vapour is exchanged between the air and surrounding elements i.e. the canopy MV_{CanAir} , the outlet air of the pad MV_{PadAir} , the fogging system MV_{FogAir} , the direct air heater $MV_{BlowAir}$, the thermal screen $MV_{AirThScr}$, the top compartment air MV_{AirTop} , the outdoor air MV_{AirOut} , the outdoor air due to the air exchange caused by the pad and fan system MV_{AirOut_Pad} , and the mechanical cooling system $MV_{AirMech}$.

The vapour pressure of the air in the top compartment VP_{Top} is described by:

$$cap_{VP_{Top}} \dot{VP}_{Top} = MV_{AirTop} - MV_{TopCov,in} - MV_{TopOut} \quad [kg m^{-2} s^{-1}] \quad (2.11)$$

where $cap_{VP_{Top}}$ is the capacity of the top compartment to store water vapour, $MV_{TopCov,in}$ is the vapour exchange between the top compartment and the internal cover layer and MV_{TopOut} is the vapour exchange between the top compartment and the outside air.

2.3.2.2.3 CO₂ concentration of the greenhouse air and the air in the top compartment

The greenhouse air CO₂ concentration CO_{2Air} is described by:

$$\begin{aligned} cap_{CO_{2Air}} \dot{CO}_{2Air} = & MC_{BlowAir} + MC_{ExtAir} + MC_{PadAir} \\ & - MC_{AirCan} - MC_{AirTop} - MC_{AirOut} \end{aligned} \quad [mg m^{-2} s^{-1}] \quad (2.12)$$

where $cap_{CO_{2Air}}$ is the capacity of the air to store CO₂. Carbon dioxide is exchanged between the greenhouse air and surrounding elements i.e. the direct air heater $MC_{BlowAir}$, the external CO₂ source MC_{ExtAir} , the pad and fan system MC_{PadAir} , the top compartment air MC_{AirTop} and

the outdoor air MC_{AirOut} . MC_{AirCan} is the CO_2 flux between the greenhouse air and the canopy as described in chapter 3.

The CO_2 concentration of the top compartment air CO_{2Top} is described by:

$$cap_{CO_{2Top}} \dot{CO}_{2Top} = MC_{AirTop} - MC_{TopOut} \quad [mg \ m^{-2} \ s^{-1}] \quad (2.13)$$

where $cap_{CO_{2Top}}$ is the capacity of the top compartment air to store CO_2 , MC_{TopOut} is the CO_2 exchange between the top compartment air and the outside air.

2.4 Model validation

The model could be used for model-based greenhouse design if it is able to predict the temperature, vapour pressure and CO_2 concentration of the air with sufficient accuracy for a wide range of greenhouse designs under varying climate conditions. Therefore, four greenhouse designs located in different climate regions were selected to validate the model. The model equations were solved with a stiff ODE solver (ode15s) of MatlabTM (Release 14; The MathWorks Inc., Natick, MA, USA). Measured data of outdoor climate conditions and settings of control valves were used as model inputs. A quantitative criterion was defined to evaluate the model performance.

2.4.1 Greenhouse design overview

The four greenhouse designs were located in three climatic regions: a temperate marine climate, northwest Netherlands; a Mediterranean climate, Sicily, Italy; and a semi-arid climate, Texas and Arizona, USA. The general details of the individual greenhouses, i.e. location, greenhouse characteristics and climate modification techniques, are listed in Table 2.1. The presented design elements cover the entire range of functions as listed in Fig. 2.1: cooling, heating, CO_2 enrichment, insulating, shading, humidification and de-humidification. A detailed overview of the parameters belonging to these design elements, i.e. physical properties to describe the greenhouse structure; ventilation characteristics; cover; whitewash; thermal screen; floor; soil and the capacities of the active climate modification techniques, can be found in the detailed model description as presented in chapter 8. In all four greenhouses tomatoes were grown. The validation periods of the associated greenhouse designs and the leaf area index (LAI) during validation are shown in Table 2.2.

Chapter 2

Table 2.1 Greenhouse characteristics and climate modification techniques used in the four greenhouses located in Sicily, The Netherlands, and Texas and Arizona, USA. Crosses denote the installed equipment for which data was used during the validation. Circles denote equipment that was installed, but for which no data was available.

Location	Sicily, Italy	Northwest part of The Netherlands	Texas, USA	Arizona, USA ⁺
Geographical coordinates	36°57'N, 14°26'E	53°12'N, 5°29'E	30°21'N, 104°00'W	32°16'N, 110°56'W
Elevation (m above sea level)	104	0	1470	715
Greenhouse type	Arch shape multi-tunnel	Venlo-type	Venlo-type	Arch-shaped single tunnel
Cover type	A double inflated PE layer	A single glass layer	A single glass layer	Polycarbonate sidewalls and an inflated double PE layer
A_Fur Floor area (m ²)	1.3·10 ⁴	1.4·10 ⁴	7.8·10 ⁴	278
Natural ventilation characteristics	Continuous roof ventilation on one side of each span, covered with insect netting	Ventilation windows on both wind and leese side of the roof	Ventilation windows on both wind and leese side of the roof	Ventilation windows were closed
Pad and fan cooling				X
Pipe heating		X	X	
CO ₂ enrichment		X	O	
Movable thermal screen		X	X	
Movable shade screen			X	X
Whitewash	X [*]		X ⁻	

⁺ See Sabeh et al. (2006) for details about the pad and fan cooled greenhouse design.

^{*} Whitewash was only applied to the greenhouse in the first validation period.

⁻ Whitewash was only applied to the greenhouse in the summer period.

Table 2.2 Averages of the outdoor climate conditions for the greenhouses located in Sicily, The Netherlands and Texas and Arizona, USA. Numbers between the brackets represent the standard deviations. An ANOVA revealed that the outdoor climate differed considerably between the first three location because for all outdoor climate variables $F_{prob} < 0.001$. For the pad and fan cooled greenhouse in Arizona, the model was validated for different ventilation fluxes applied to the greenhouse between 8.00 – 17.00h for a sunny day in May 2005.

Location	DOY	Flux* ($\text{m}^3 \text{m}^{-2} \text{s}^{-1}$)	LAI ($\text{m}^2 \text{m}^{-2}$)	I_{Glob_sum} ($\text{MJ m}^{-2} \text{day}^{-1}$)	T_{Out} ($^{\circ}\text{C}$)	VP_{Out} (kPa)	RH_{Out} (%)	V_{Speed} (m s^{-1})
Sicily	267-272	-	1.5	11.6 (2.5)	22.5 (3.4)	2.1 (0.2)	79 (12)	2.5 (2.7)
Sicily	293-298	-	2.5	8.5 (1.7)	15.2 (3.4)	1.2 (0.3)	69 (13)	2.9 (2.9)
Netherlands	38-43	-	2	6.5 (1.9)	5.9 (2.7)	0.7 (0.1)	80 (11)	2.4 (1.0)
Netherlands	200-205	-	3	15.5 (3.0)	15.2 (1.5)	1.5 (0.2)	85 (9.0)	4.6 (1.4)
Texas	3-8	-	2.5	10.1 (5.9)	5.4 (5.6)	0.6 (0.1)	66 (25)	3.5 (2.8)
Texas	157-162	-	2	25.5 (2.5)	23.9 (5.4)	1.3 (0.5)	46 (24)	3.5 (2.4)
Arizona	139	0.016	2.5	25.2	34.2 (2.8)	0.7 (0.0)	13 (2.3)	3.4 (1.2)
Arizona	151	0.034	2.5	26.3	34.2 (3.2)	0.5 (0.0)	9 (2.1)	1.8 (0.9)
Arizona	131	0.047	2.5	24.3	33.5 (3.1)	0.5 (0.1)	10 (3.3)	1.9 (0.9)
Arizona	132	0.060	2.5	23.8	33.5 (2.9)	0.5 (0.0)	10 (2.2)	2.3 (1.1)

The * indicates the ventilation flux of the pad and fan cooling system.

2.4.2 Climate data collection

The climate data of the commercial greenhouses, i.e. Sicily, The Netherlands and Texas, were obtained from weather stations (I_{Glob} , T_{Out} , RH_{Out} and V_{Wind}) and measurement boxes (T_{Air} , RH_{Air} and CO_{2Air} if available), and these data were recorded by the central climate computer. The climate data of the pad and fan cooled greenhouse in Arizona were obtained from a commercial weather station (T_{Out} , RH_{Out} and V_{Wind}), pyranometers (I_{Glob}), thermocouples (T_{Air}) and relative humidity sensors (RH_{Air}). These climate data were recorded using a data logger.

The vapour pressures of the greenhouse air (VP_{Air}) and outside air (VP_{Out}) for all locations were calculated from their psychrometric relationship to the air temperature and air relative humidity. For the missing outdoor climate variables: the outdoor CO_2 concentration (CO_{2Out}) was assumed to be constant at 668 mg m^{-3} (370 ppm); the sky temperature (T_{Sky}) and the temperature of the outer soil layer (T_{SoOut}) were estimated using the equations presented in the detailed model description. The energy flow into the heating pipes for the greenhouses located in The Netherlands and in Texas was not measured. For

these validation cases the measured pipe temperature was used as an input of the model. The CO₂ injection rate and/or CO₂ concentration of the greenhouse air were measured in the greenhouse in Sicily throughout the year and during the summer in the greenhouse in The Netherlands. Therefore, the CO₂ concentration was only validated for these two cases.

2.4.3 Outdoor climate comparison

For all four locations, Table 2.2 lists the average values and standard deviations of the global radiation and the outdoor temperature, humidity and windspeed during the validation experiments. An analysis of variance (ANOVA) using GenStat (Release 12.1 of VSN International Ltd, Hemel Hempstead, UK) revealed that the outdoor climate differed significantly amongst the first three locations, because for all outdoor climate variables $F_{prob} < 0.001$. For the Arizona location, no ANOVA was performed because the time series of this location were not equal to the other three time series. However, the high ambient temperatures in Arizona ensured that these climate data sets differed from the climate data sets at the other locations.

2.4.4 Determination of model performance

Model performance was evaluated in quantitative terms using the relative root mean square error (RRMSE) according to Kobayashi and Salam (2000):

$$RRMSE = \frac{100}{\bar{y}_{Data}} \sqrt{\frac{1}{n} \sum_{i=1}^n (y_{Mod,i} - y_{Data,i})^2} \quad [\%] \quad (2.14)$$

where \bar{y}_{Data} is the mean of measured data over the total time span, n is the number of measurements, $y_{Mod,i}$ is the simulated climate value at time instant ' i ' and $y_{Data,i}$ is the measured climate value at time instant ' i '. For developing the methodology of optimal greenhouse design, it was assumed that an RRMSE of 10% or less would be sufficient. As demonstrated by Baptista (2007), the performance of most greenhouse climate models is around this value.

2.5 Results

2.5.1 A passive multi-tunnel greenhouse in Sicily, Italy

The model correctly predicted the temperature (Fig. 2.3a,b) and the vapour pressure (Fig. 2.3c,d) for a cold and a hot period in the 'low-tech' greenhouse in Sicily. The CO₂

concentration of the greenhouse air was predicted with fair accuracy (Fig. 2.3e,f). Although the simulated CO_2 trend was in agreement with the measurements, especially at night, the absolute predicted CO_2 concentrations differed from the measured CO_2 concentrations.

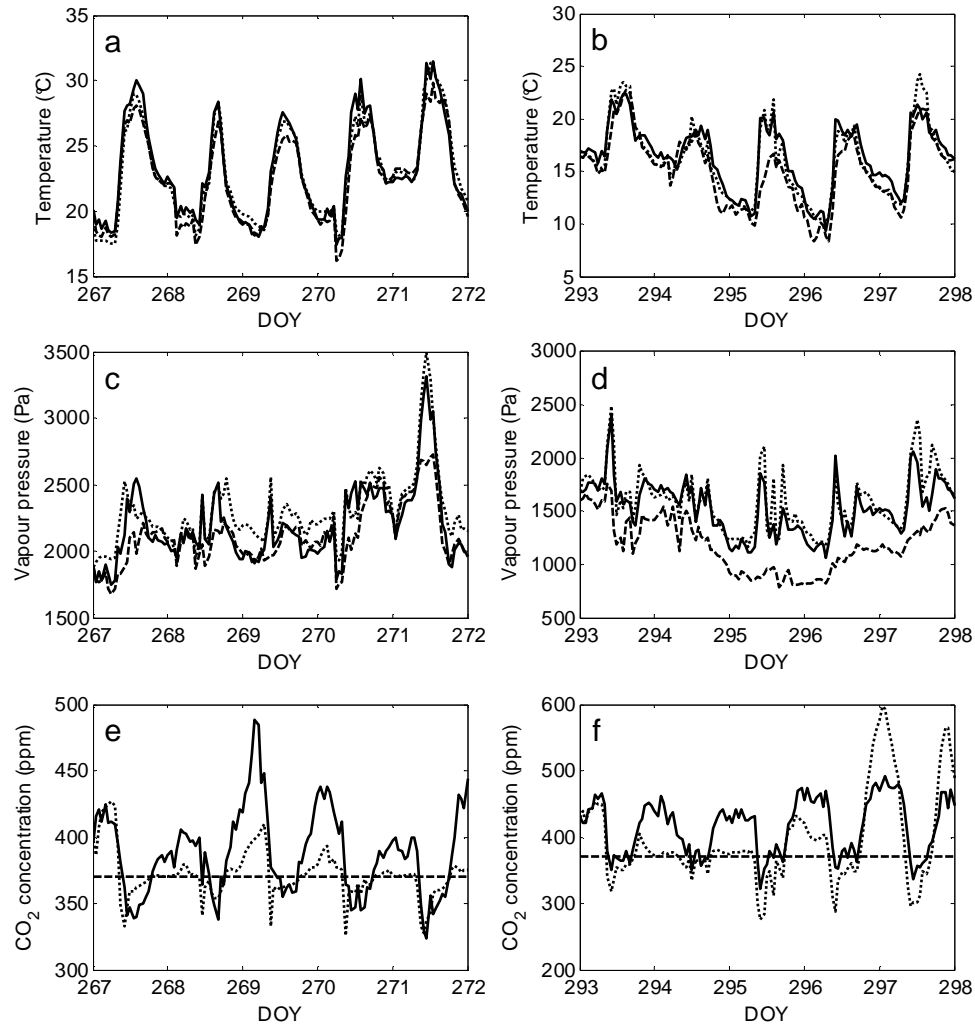


Fig. 2.3 Temperature (a, b), vapour pressure (c, d) and the CO_2 concentration (e, f) of measured greenhouse air (solid line), simulated air (dotted line) and outdoor air (dashed line) for the hot period (DOY 267 - 272) and for the cold period (DOY 293 - 298) in Sicily.

2.5.2 A climate-controlled greenhouse in The Netherlands

The model correctly predicted the temperature (Fig. 2.4a,b) and the vapour pressure (Fig. 2.4c,d) during the winter and summer period in The Netherlands, even with large differences between indoor and outdoor climate. The CO_2 concentration of the greenhouse air was correctly predicted during the summer period (Fig. 2.4e).

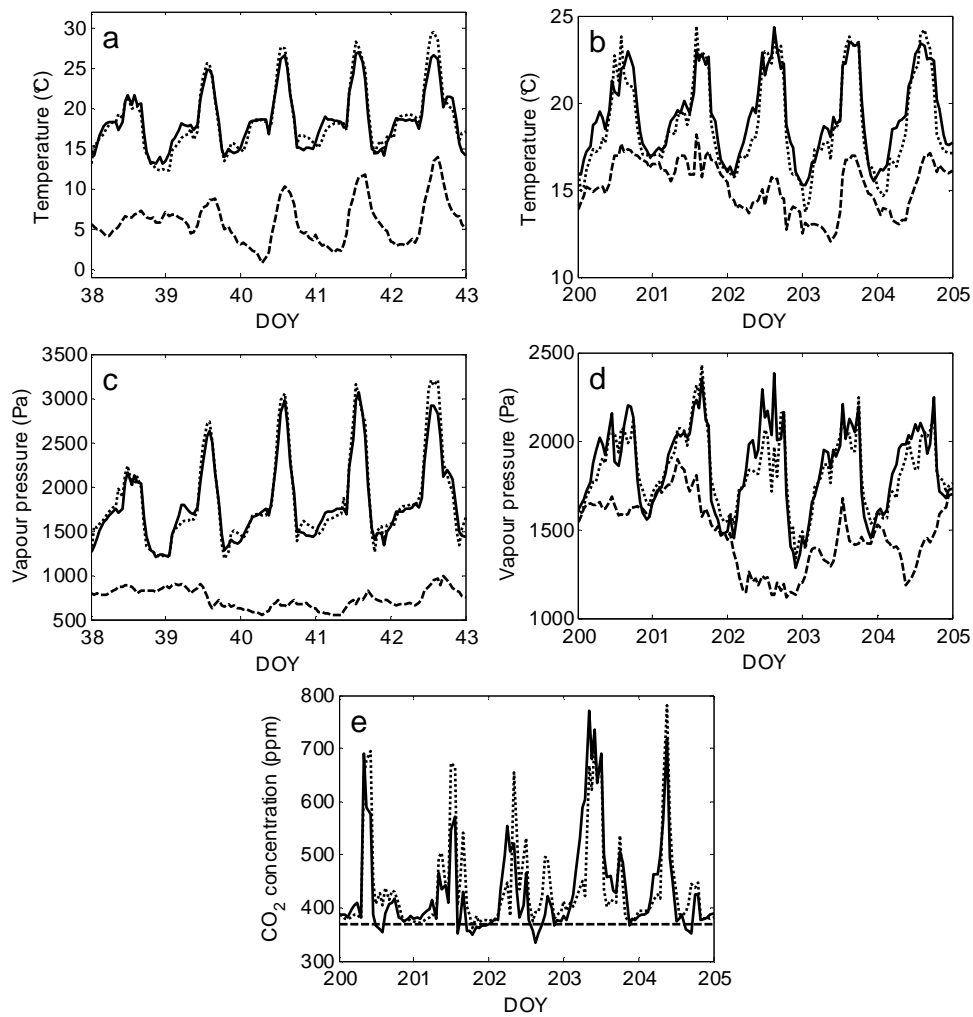


Fig. 2.4 Temperature (a,b), vapour pressure (c,d) and the CO_2 concentration (e) of the measured greenhouse air (solid line), simulated air (dotted line) and outdoor air (dashed line) for the winter period (DOY 38 - 43) and for the summer period (DOY 200 - 205) in The Netherlands.

The simulated temperature (Fig. 2.4a) and vapour pressure (Fig. 2.4c) were overestimated only at day-of-the-year (DOY) 42 during the daytime. This was caused by an underestimated simulated ventilation rate. This underestimation took place because the effect of the vapour pressure difference on ventilation rate was not described in the ventilation rate equation (see detailed model description), and this vapour pressure difference between greenhouse air and outdoor air was large at that time. To improve the model performance, the impact of the vapour pressure difference between greenhouse air and outdoor air on ventilation rate should be incorporated in the ventilation rate equation.

2.5.3 A climate-controlled greenhouse in Texas, USA

The model correctly predicted the temperature and the vapour pressure for both a winter and a summer period in Texas (Fig. 2.5). During the winter period, the temperature and vapour pressure were predicted in close agreement with the measurements, even when temperature and vapour differences between indoor air and outdoor air were large (Fig. 2.5a,c). During summer period, the temperature and vapour pressure were predicted in close agreement with the measurements (Fig. 2.5b,d). However, at some points in time small deviations between the measured and simulated greenhouse climate occurred. The daytime temperatures on DOY 160 and DOY 161 were underestimated at most by 3°C.

Using the parameters of the stomatal resistance model of Stanghellini (1987), the simulated transpiration rate was underestimated with respect to the measured transpiration rate during daytime in the summer. Those parameters, however, were determined empirically for vapour pressure differences between leaf and air up to 0.9 kPa. The vapour pressure differences in Texas, however, could reach 4.0 kPa, a value where extrapolation of Stanghellini's (1987) function would have a considerable impact (see Eq. (8.50) in chapter 8). Therefore the parameter of the stomatal resistance model describing stomatal reaction to vapour pressure difference, i.e. C_{evap4}^{day} was reduced to 10% of its original value, which yielded better results for crop transpiration. We did not investigate whether other models of stomatal conductance, such as Blonquist Jr *et al.* (2009) would perform better.

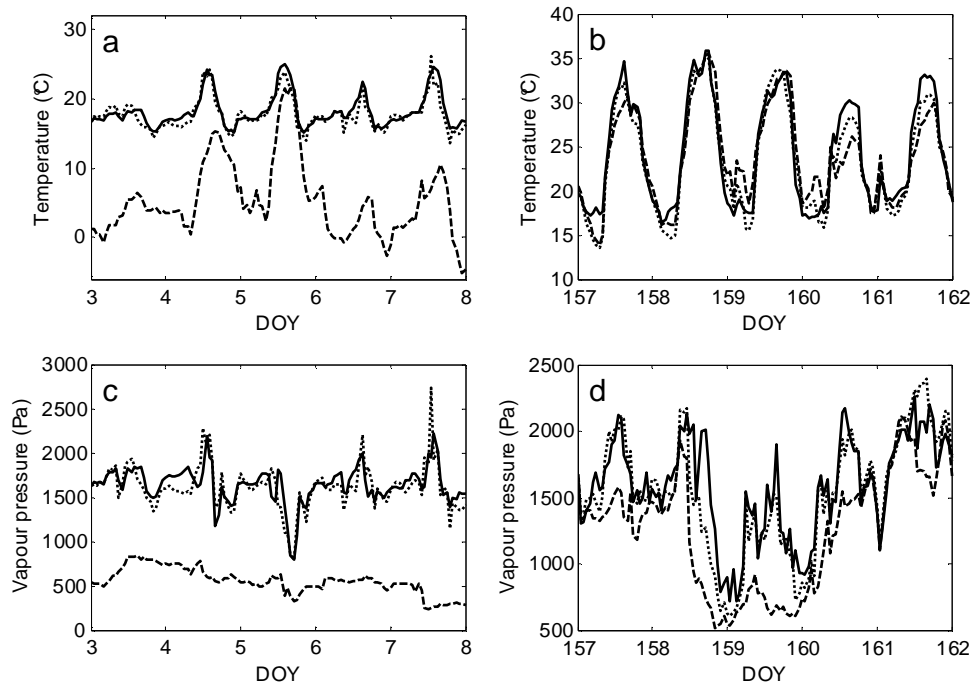


Fig. 2.5 Temperature (a,b) and the vapour pressure (c,d) of measured greenhouse air (solid line), simulated air (dotted line) and outdoor air (dashed line) for the winter period (DOY 3 - 8) and for the summer period (DOY 157 - 162) in Texas, USA.

2.5.4 A pad and fan cooled greenhouse in Arizona, USA

The model correctly predicted the temperature and vapour pressure for a pad cooled greenhouse in Arizona for various ventilation rates during the day in the summer period (Fig. 2.6). The model slightly underestimated the temperature and the vapour pressure of the greenhouse air (Fig. 2.6a) only for the lowest ventilation rate. This underestimation could have been caused by assuming that the greenhouse was a perfectly stirred tank, which is not the case when a pad and fan system is used. Specifically, a pad and fan cooling system causes horizontal temperature and vapour pressure gradients (Sabeh *et al.*, 2006).

Furthermore, the underestimation of the vapour pressure at the lowest ventilation rate might have been caused by an underestimated transpiration rate. The transpiration rate was simulated using a constant boundary layer resistance, which was valid for naturally ventilated greenhouses with an indoor wind speed around 0.10 m s^{-1} (detailed model description). By using this constant boundary layer resistance in a pad and fan cooled

greenhouse with a considerably higher indoor wind speed, the impact of higher wind speeds on boundary layer resistance was not taken into account, which would ultimately result in an underestimated transpiration rate. However, the underestimation of the transpiration rate negatively affected the simulated indoor climate only at the lowest ventilation rate (Fig. 2.6a). At higher ventilation rates, the impact of the pad and fan system on energy and vapour balance became dominant with respect to transpiration rate, which resulted in an accurate prediction of temperature and vapour pressure (Fig. 2.6b-d).

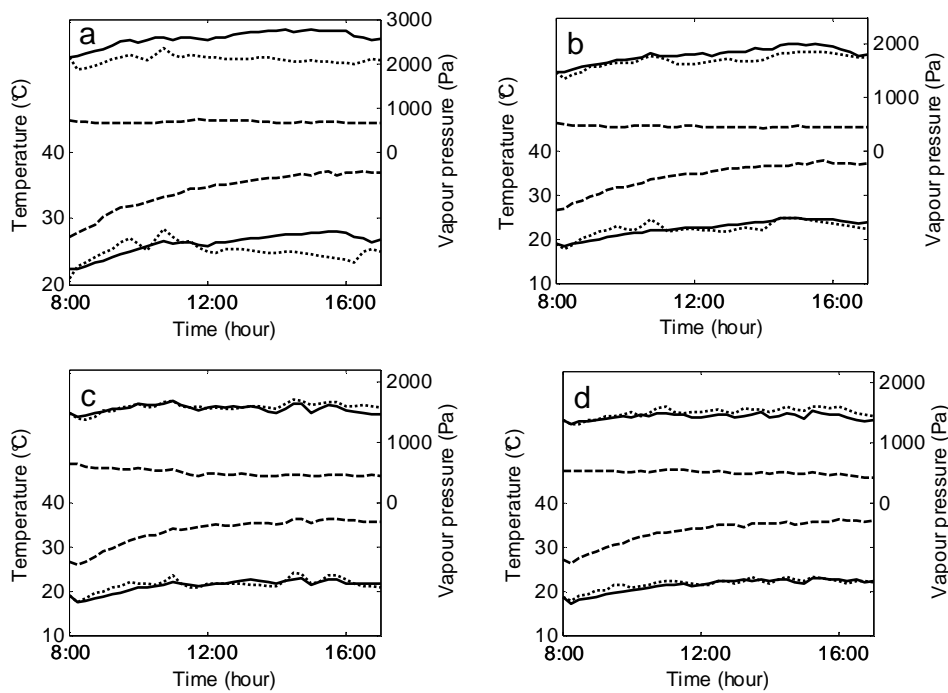


Fig. 2.6 Temperature and the vapour pressure of the measured greenhouse air (solid line), simulated air (dotted line) and of outdoor air (dashed line) for data obtained with four ventilation rates through the pad: $0.016 \text{ m}^3 \text{ m}^{-2} \text{ s}^{-1}$ (a), $0.034 \text{ m}^3 \text{ m}^{-2} \text{ s}^{-1}$ (b), $0.047 \text{ m}^3 \text{ m}^{-2} \text{ s}^{-1}$ (c) and $0.060 \text{ m}^3 \text{ m}^{-2} \text{ s}^{-1}$ (d) in Arizona, USA.

2.5.5 Overall model performance

The model performance in terms of RRMSE is shown in Table 2.3. Additional to the qualitative model evaluation, the more quantitative model performance evaluation, based on the RRMSE, clearly indicates the ability of the model to describe the greenhouse indoor climate for different designs, locations and outdoor climate conditions. In almost all cases,

the RRMSE was well below the required threshold of 10%. Exceptions were the vapour pressure of the air in Texas during the winter and summer periods (10.0% and 12.8% respectively), in Arizona at the lowest ventilation rate (19.8%) and the CO₂ concentration in both Sicily in the autumn period (11.7%) and in The Netherlands in the winter period (12.3%).

Table 2.3 Relative root mean square error (RRMSE) values used to evaluate the ability of the model to describe the air temperature, the humidity and the CO₂ concentration in the four greenhouses located in Sicily, The Netherlands, and in Texas and Arizona in the USA. The crosses indicate that measurements of the associated variables were not available.

Location	DOY	Flux* (m ³ m ⁻² s ⁻¹)	Relative Root Mean Square Error (RRMSE) (%)		
			T_{air}	VP_{air}	CO_{2air}
Sicily, Italy	267-272	-	3.5	7.0	7.1
Sicily, Italy	293-298	-	6.6	8.9	11.7
The Netherlands	38-43	-	6.2	6.4	x
The Netherlands	200 -205	-	5.3	5.7	12.3
Texas, USA	3-8	-	6.0	10.0	x
Texas, USA	157-162	-	6.8	12.8	x
Arizona, USA	139	0.016	8.0	19.8	x
Arizona, USA	151	0.034	4.5	6.8	x
Arizona, USA	131	0.047	4.1	3.9	x
Arizona, USA	132	0.060	3.3	5.9	x

*The * indicates the ventilation flux of the pad and fan cooling system.*

For large differences between the indoor climate and the outdoor climate, which occurred during the winter in The Netherlands and in Texas, and during sunny summer days in Arizona, the model correctly predicted the indoor climate. This means that the physical properties and the design elements had properly been modelled. The calculated errors could be decreased by reducing the measurement errors of the measurement boxes. These measurements contained errors due to measurement inaccuracy and because one measurement box was unable to represent the climate of the whole greenhouse section, because a greenhouse is not as assumed a perfectly stirred tank. Specifically, Bontsema *et al.* (2008) measured the relative errors of commercial measurement boxes for the air

temperature, relative humidity and CO₂ concentration, which were 1.4%, 2.8% and 7.2% respectively. Although the measurement boxes were calibrated and placed at the centre of a greenhouse section, more accurate and randomly placed measurement boxes would reflect the overall indoor climate better. More accurately measuring indoor climate could in turn decrease the RRMSE.

Model performance was measured at a time interval of one hour. This time interval was sufficiently small to describe the daily greenhouse climate fluctuations needed for greenhouse design optimisation. Therefore, the model accuracy for smaller time intervals was not analysed. However, the model performance will probably not decline significantly with smaller time intervals because the model is described using differential equations and solved with a solver with a variable time step.

2.6 Discussion

To design and optimise protected cultivation systems for the wide variety of climate conditions that can be expected around the world, it is essential to have a model that correctly predicts the indoor climate, not only as a function of a wide range of outdoor climate conditions, but also as a function of a wide range of construction elements and climate conditioning equipment.

Accordingly, the model developed here, fulfilling the requirement of using differentiable equations, was validated for a variety of greenhouse designs and outdoor climate conditions. Without calibration (except in one case), the model accurately described the greenhouse climate, both in terms of dynamic responses and absolute values. Quantitative evaluation of the model performance using an RRMSE criterion supported these findings. In more than 78% of the cases, comparison of simulations and measurements of the indoor climate yielded an RRMSE of less than 10%. This model performance, in terms of RRMSE, corresponds with values obtained by other climate modelling studies as reported by Baptista (2007). Given these results, the model is considered to be sufficiently accurate and generic to be used as a key component for developing a model-based greenhouse design method. In particular, our model includes relevant processes for greenhouse design, such as FIR radiation fluxes, CO₂ fluxes and a detailed transpiration module, that are not present in other models, such as the educational climate simulation model of Fitz-Rodríguez *et al.* (2010). However, since our aim was to develop a design method that focussed on the optimisation of a set of design elements, model aspects that might be relevant may have been neglected or too much simplified.

Therefore, whenever better or new modules are available, they can be easily incorporated into the design method. Some issues that might improve the generality of the model-based design method are discussed in more detail here. In particular, a module that describes the light transmission as a function of season, latitude, orientation, shape, gutter and ridge height and type of cover material might enable the optimisation of the greenhouse height and the roof slope. Since radiation diffusing materials seem promising in areas with high solar radiation, differentiation between direct and diffuse radiation would allow diffuse properties of cover materials to be optimised also in relation to diffusion. Additionally, modules of other climate modification techniques such as co-generation of heat and electricity, artificial photosynthetic lighting, an active heat buffer, a heat pump and a solar heat collector might be incorporated.

To systematically quantify the impact of uncertain model aspects on indoor climate prediction, sensitivity analysis techniques can be used (Chalabi & Bailey, 1991; Nijskens *et al.*, 1991). Although a sensitivity analysis was not performed in this chapter, our results allow for some possible model improvements to be indicated. Firstly, according to Campen and Bot (2003), the ventilation rate may depend strongly on wind direction, whereas the modelled ventilation rate was not which, could explain some of the deviations. The ventilation rate influences in turn the indoor temperature, vapour pressure and CO₂ concentration. Although the sky temperature and the external soil temperature were not measured but estimated, the indoor temperature was accurately predicted by the model because all the associated RRMSE values were lower than 10%. Apparently, the small impact of these estimated values on temperature prediction was caused either by accurate calculations or by the negative feedback mechanisms implemented in the model, such as the canopy transpiration and the capacity of the soil to store heat. Nevertheless, the sky temperature and external soil temperature should be measured in future research to increase the model performance. Additionally, pipe temperature was considered as a model input, whereas for greenhouse design optimisation the input must be energy and the pipe temperature must be a state variable as described in this study. Using the pipe temperature as a model input did not undermine our validation results because in the long term the heat input supplied to the heating pipes equals the heat output.

The vapour pressure of the air was predicted with reasonable accuracy; the associated RRMSE was higher than 10% for only three validation experiments. This attests to the ability of the model of Stanghellini (1987) to predict crop transpiration rate with fair accuracy under quite extreme climate conditions (VPD up to 2.0 kPa), as shown by Jolliet and Bailey (1992) and Prenger *et al.* (2002). In addition, the negative feedback between

canopy transpiration and air vapour pressure ensures a reduced sensitivity of the vapour pressure to errors in the estimate of transpiration. Indeed, even for extreme climate conditions (temperature of 35°C and VPD of 4.0 kPa), the air temperature was predicted with fair accuracy (RRMSE < 10%). Nevertheless, the prediction of the transpiration rate could be improved further, by improving the empirical description of the stomatal resistance. In addition, making the boundary layer resistance wind-speed dependent rather than constant might improve the simulation of the transpiration rate under higher wind speeds caused by e.g. pad and fan cooling.

The CO₂ concentration prediction was validated for only the two greenhouse designs for which the indoor data were available. The CO₂ concentration was predicted reasonably well for a greenhouse with and without CO₂ injection. The RRMSE of two out of three validation experiments was slightly higher than the requirement of 10%. CO₂ concentration prediction might be improved if the outdoor CO₂ concentration data were available. A secondary factor is the improvement of the prediction of the maintenance and photosynthesis fluxes. Insight into these CO₂ fluxes would improve if greenhouse growers would measure the indoor and outdoor CO₂ concentration and the CO₂ supply. The lack of a strong negative feedback mechanism for the CO₂ concentration (Fig. 2.2) ensures that these sources of uncertainty might have a relatively large impact on the prediction of CO₂ concentration. For greenhouse design purposes, deviations between simulated and measured CO₂ concentration at night are not important, because then the CO₂ concentration does not influence photosynthesis rate and crop yield. During day, these deviations do influence the photosynthesis rate, which in turn influence crop yield and the optimal greenhouse design problem. The impact of these deviations on optimal greenhouse design should be analysed with a sensitivity analysis of the optimal greenhouse design problem.

Regarding the design of the validation study, all the greenhouse functions were fulfilled by at least one design element (Table 2.1). Validation on function level was sufficient because it did not matter where a model flux came from, but it did matter how the model reacted to it. Consequently, the model was not validated for all the design elements shown in Fig. 2.1. It is, of course, advisable to validate the model aspects related to these design elements with data. Differentiable switch functions were implemented instead of conditional “if/else” statements, due to the requirement that the model should consist of differentiable equations. Although the steep flanks of the switch function approached the conditional “if/else” statements, these functions might have an impact on model behaviour. Nevertheless, no discrepancies in model output between these approaches were shown, which support the feasibility of this approach.

2.7 Conclusion

A greenhouse climate model that describes the effect of outdoor climate and greenhouse design, including construction parameters and climate conditioning equipment on indoor greenhouse climate, was developed and validated. The aim is to use this model in a method to design greenhouses for the wide variety of climate conditions that can be expected around the world. To enable our findings to be implemented and reproduced, all model equations are presented in this chapter and in the detailed model description.

For a broad range of greenhouse designs under varying climate conditions, the model predicted the greenhouse climate with reasonable accuracy. In our study, the greenhouse climate consisted of the temperature, vapour pressure and the CO₂ concentration. With the exception of one case, model parameters were not modified. In more than 78% of the cases, comparison of simulations and measurements of the indoor climate yielded an RRMSE of less than 10%. Additionally, the model fulfilled the requirements of containing the design elements that are sufficiently generic for a wide range of climate conditions and of being differentiable.

Given these results, the model is considered to be sufficiently accurate and sufficiently generic to be used for developing a model-based greenhouse design method. Therefore, the greenhouse climate model will be integrated into a model-based greenhouse design method, where it will be combined with a crop yield model and an economic model. An optimisation algorithm will then select the best design elements under the given climatic and economic conditions in order to maximize the profit of the grower.

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2.8 Nomenclature

State variables

CO_2	Carbon dioxide concentration	$mg\ m^{-3}$
T	Temperature	$^{\circ}C$
VP	Vapour pressure	Pa

Flux densities

H	Sensible heat flux density	$W\ m^{-2}$
L	Latent heat flux density	$W\ m^{-2}$
MC	Mass CO_2 -flux density	$mg\ m^{-2}\ s^{-1}$
MV	Mass vapour flux density	$kg\ m^{-2}\ s^{-1}$
R	Far infrared radiation (FIR) flux density	$W\ m^{-2}$
R_{NIR}	Near infrared radiation (NIR) flux density	$W\ m^{-2}$
R_{PAR}	Photosynthetically active radiation (PAR) flux density	$W\ m^{-2}$
R_{Glob}	Global radiation flux density	$W\ m^{-2}$

External Climate Inputs

$CO_{2\ Out}$	Outdoor CO_2 concentration	$mg\ m^{-3}$
I_{Glob}	The outside global radiation	$W\ m^{-2}$
T_{Out}	Outdoor temperature	$^{\circ}C$
T_{Sky}	Sky temperature	$^{\circ}C$
T_{SoOut}	Soil temperature of outer soil layer	$^{\circ}C$
VP_{Out}	Outdoor vapour pressure	Pa
v_{Wind}	Outdoor wind speed	$m\ s^{-1}$

Remaining symbol

cap	Capacity of the associated state
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Chapter 2

Subscripts

<i>Air</i>	Greenhouse air compartment below thermal screen
<i>Blow</i>	Direct air heater
<i>Boil</i>	Boiler
<i>Can</i>	Canopy
<i>Cov</i>	Cover
<i>e</i>	External side
<i>Ext</i>	External CO ₂ source
<i>Flr</i>	Floor
<i>Fog</i>	Fogging system
<i>Geo</i>	Geothermal heat
<i>Glob</i>	Global radiation
<i>Ind</i>	Industrial source
<i>Mech</i>	Mechanical cooling
<i>Out</i>	Outside air
<i>Pad</i>	Pad and fan system
<i>Pas</i>	Passive heat storage facility
<i>Pipe</i>	Pipe heating system
<i>Sky</i>	Sky
<i>So(j)</i>	The 'j' th the soil layer
<i>Sun</i>	The sun
<i>Top</i>	Compartment above the thermal screen
<i>ThScr</i>	Thermal screen

Chapter 3

Description and validation of a tomato yield model

The contents of this chapter have been submitted to Biosystems Engineering as a paper entitled: *A methodology for model-based greenhouse design: Part 2, Description and validation of a tomato yield model.*

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3.1 Abstract

With the aim of developing a model-based method to design greenhouses for a broad range of climatic and economic conditions, a tomato yield model that describes the effects of greenhouse climate on yield was described and validated. A literature survey of temperature effects on tomato yield was performed and the main temperature effects were implemented in the model. Subsequently, the yield model was validated for four temperature regimes. Results demonstrated that the tomato yield was simulated accurately for both near-optimal and non-optimal temperature conditions in respectively The Netherlands and Southern Spain with varying light and CO₂ concentrations. In addition, the adverse effects of extremely low as well as high mean temperatures on yield and moment of first fruit harvest were simulated with fair accuracy. The simulated yield response to extreme diurnal temperature oscillations were in agreement with literature values. In addition, the model consisted of a set of differential equations with continuous differentiable right-hand sides. Given these results, the model is considered to be sufficiently accurate to be used for developing a model-based greenhouse design method. Therefore, the presented model will be integrated in the model-based design method with the aim to design the best greenhouse for local climate and economic conditions.

3.2 Introduction

This chapter contains a description and validation of the tomato yield model. Since greenhouse design affects crop yield through its effect on indoor climate, a model is presented that describes the tomato (*Lycopersicon esculentum*) yield as a function of indoor climate. For use in design and optimisation studies, the model should fulfil three requirements: (i) describe the effects of the indoor temperature, light, and CO₂-concentration on tomato yield; (ii) describe adverse effects of extremely low as well as high temperatures on tomato yield since the solution of a greenhouse design optimisation problem is expected to allow these extreme temperatures in order to save energy and investments; (iii) the model should consist of a set of differential equations since it will be combined with a greenhouse climate model consisting of a set of differential equations and to allow the use of ordinary differential equation solvers. In addition, the right-hand sides must be continuously differentiable to speed up the simulation and to assure that gradient-based dynamic optimisation algorithms can be applied to the model.

In the literature, several models can be found that describe the influence of light, temperature and CO₂-concentration on tomato yield. However, these models are mostly valid for relatively small temperature ranges (Seginer *et al.*, 1994; Tap, 2000; Ooteghem, 2007) and are not fully differentiable e.g. TOMGRO (Jones *et al.*, 1991; Dayan *et al.*, 1993), TOMSIM (Heuvelink, 1996), and the tomato yield model of De Koning (1994). In conclusion, the literature review revealed that a tomato yield model satisfying the predefined requirements is still missing and therefore the aim of this work was to describe and validate such a tomato yield model. Due to the aim of the model – to use it in a model-based greenhouse design method –, the primary focus of this chapter is to describe the extreme temperature effects on tomato dry matter yield.

The outline of this chapter is as follows. Firstly, since the model should deal with extreme temperatures, a literature survey of temperature effects on tomato yield is presented. Secondly, the model implementation of these main temperature effects is described. Subsequently, the simulated tomato yield is validated with the measured tomato yield for the following three temperature regimes: 1) mild temperatures with varying light and CO₂ conditions in two Dutch greenhouses; 2) extreme temperature conditions with varying light and CO₂ conditions in a low-tech greenhouse and a high-tech greenhouse in southeast Spain and 3) four constant temperature trajectories varying from sub-optimal to supra-optimal temperatures conducted in growth chambers. In addition, the effect of extreme temperature regimes is evaluated and compared with data found in the literature.

3.3 Temperature effects on tomato yield

Temperature influences different aspects of tomato growth (e.g., production rate and partitioning, dry matter content) and development (e.g., leaf and truss appearance, fruit growth period, abortion and fruit quality) (De Koning, 1994; Van Der Ploeg & Heuvelink, 2005). Photosynthesis, which depends on light, CO₂ and temperature, produces carbohydrates needed for crop growth. These carbohydrates are distributed to fruits, leaves, stems and roots and are converted to dry matter (such as sugars, amino acids and organic acids). The sugars fulfil the energy requirement for maintenance processes and growth processes. Finally, fruit set, fruit growth and abortion rates determine how much of the potentially available carbohydrates are allocated to the fruits.

In this section, a literature study of the effects of sub-optimal, supra-optimal and (large) differences between day and night temperature on growth, development and ultimately on tomato yield is presented. Being not exhaustive, this survey is only considered to capture the main trends. Although the impact of temperature depends on the associated solar radiation, CO₂ concentration and humidity levels, the focus of this survey was to capture the main temperature trends based on temperature experiments with naturally varying levels of the other climatic factors. The impact of supra-optimal temperature on growth implicitly comprises the negative effect of high vapour pressure deficit (VPD) on growth. Specifically, a high VPD is strongly correlated to a high temperature so that uncoupling both factors seemed superfluous. Results of this survey are summarized in Table 3.1.

3.3.1 Effect of sub-optimal temperatures on fruit fresh weight yield

Chilling temperatures may affect negatively photosynthesis, respiration, membrane integrity, water relations, the hormone balance of the plants and fruit set (Van Der Ploeg & Heuvelink, 2005; Adams *et al.*, 2001; Brüggemann *et al.*, 1992; Yakir *et al.*, 1986). Additionally, the fruit growth period increases with decreasing temperatures (De Koning, 1994). These unfavourable processes decrease the total fruit fresh weight as shown hereafter.

Below a mean temperature of 12°C, Criddle *et al.* (1997) observed no significant growth and tomato yield. Khayat *et al.* (1985) found that with similar solar radiation levels, the cultivar Moneymaker, grown at a night temperature of 12°C, yielded only 76% of the yield observed at 18°C. However, the same treatment for the cultivar Cherry did not affect

growth. These results indicate that the impact of low temperature on crop yield is cultivar dependent. According to Baytorun *et al.* (1999), yield levels of plants exposed for 3 months to a minimum mean night temperature of 8.2°C decreased to 46% compared to levels observed at a minimum mean night temperature of 11.5°C with similar solar radiation levels. Furthermore, Adams *et al.* (2001) observed at a mean temperature of 14°C, a yield decrease to 21% of the crop yield observed at 22°C with other climatic factors remained similar. Additionally, Adams *et al.* (2001) found that fruits grown at a mean temperature of 14°C were parthenocarpic, small, hard and without economical value. In contrast to the above-mentioned results, Martínez Mirón (2008) observed under relatively low light conditions (mean global radiation sum of 7.6 MJ m⁻² day⁻¹) at a mean minimum night temperature of 13.2°C, a yield increase to 108% of the yield observed at 15.2°C. At higher light levels (9.4 MJ m⁻² day⁻¹) no positive effect of a low mean night temperature on crop yield was observed. These results indicate that under low light conditions, low rather than high mean night temperature may favour crop growth. However, the general trend observed in the literature was that yield decreased with decreasing night temperatures.

3.3.2 Effects of supra-optimal temperatures on fruit fresh weight yield

At supra-optimal levels, the instantaneous temperature decreased photosynthesis and the mean temperature caused a lower fruit set, shorter fruit growth period and smaller fruits (Heckathorn *et al.*, 1998; Camejo *et al.*, 2005; De Koning, 1994; Adams *et al.*, 2001; Peet *et al.*, 1997; Sato *et al.*, 2000). These unfavourable processes decreased the total fruit fresh weight as shown hereafter. Adams *et al.* (2001) reported at a mean temperature of 26°C, 18% of the crop yield observed at 22°C and Peet *et al.* (1997) found at a mean temperature of 29°C, 17% of the crop yield observed at 25°C with similar radiation levels. Zhang *et al.* (2008) observed at a day temperature of 35°C a crop yield decrease to 46.1% compared to a day temperature of 25°C.

Table 3.1 A summary of effects of low and high temperatures on crop growth processes and crop yield levels based on a literature review.

Period	Temperature	Results	Author
<i>Photosynthesis</i>			
14 days	10°C at photoperiod	2-5% of initial photosynthesis	Yakir <i>et al.</i> (1986)
3 days after 14 days treatment	10°C at photoperiod	Recovering to 50% of initial photosynthesis	Yakir <i>et al.</i> (1986)
3 hour	43 °C	Significant decrease compared to 25°C	Heckathorn <i>et al.</i> (1998)
2 hours	40 °C	Reduced to 30%	Camejo <i>et al.</i> (2005)
<i>Fruit development time</i>			
Total period ⁺	14 °C mean	94.8 days, 205% of 22 °C mean	Adams <i>et al.</i> (2001)
Total period ⁺	26 °C mean	41.5 days, 89.6% of 22 °C mean	Adams <i>et al.</i> (2001)
Total period	Between 17°C and 26°C	Development rate is linearly related to temperature	De Koning (1994)
<i>Fruit size</i>			
Total period ⁺	14 °C mean	18.3 g, 36 % of 22 °C mean	Adams <i>et al.</i> (2001)
Total period ⁺	26 °C mean	23.9 g, 47% compared to 22 °C mean	Adams <i>et al.</i> (2001)
<i>Fruit set/abortion</i>			
3 weeks	6°C constant	irreversible damage	Brüggemann <i>et al.</i> (1992)
Total period ⁺	14 °C mean	59 % compared to 22 °C mean	Adams <i>et al.</i> (2001)
Production period	28/22°C	>75% (for all cultivars)	Sato <i>et al.</i> (2000)
Production period	32/26°C	0% (for 4 out 5 cultivars)	Sato <i>et al.</i> (2000)
Production period	25 °C mean	48%	Peet <i>et al.</i> (1997)
Production period	29 °C mean	11%	Peet <i>et al.</i> (1997)
Total period ⁺	26 °C mean	40 % compared to 22 °C mean	Adams <i>et al.</i> (2001)
<i>Crop production</i>			
Continuous	12°C mean	0%	Criddle <i>et al.</i> (1997)
During night	8.2°C mean	46% compared to 11.5°C mean	Baytorun <i>et al.</i> (1999)
During night	13.2°C mean	108% compared to 15.2°C mean	Martínez Mirón (2008)
During night	12 °C	1571 g / plant, 76% of 18°C night	Khayat <i>et al.</i> (1985)
Total period ⁺	14, 18, 22, 26 °C mean	See Table 3.4	Adams <i>et al.</i> (2001)
Production period	29 °C mean	117.32 g/plant 17% compared to 25°C mean	Peet <i>et al.</i> (1997)
Day time	35°C	46,1% compared to 25°C	Zhang <i>et al.</i> (2008)
Daily	DIF=-6°C (D=18°C,N=24°C)	Reduced plant growth and development	Heuvelink (1989)
Daily	DIF=10°C (D=26°C, N=16°C)	Same growth and development as DIF=2°C(D=22°C,N=20°C)	Heuvelink (1989)
Production period	DIF = 14°C	Higher production compared to 5°C DIF	Gent and Ma (1998)
Production period	DIF = 18°C	Similar production to a DIF is 6°C	Mavrogianopoulos and Kyritis (1989)

The ⁺ indicates that the treatment started after 21 days after sowing.

3.3.3 Effects of both short term and long term temperature differences

The difference between day and night temperature (DIF) also affects crop growth processes. For young tomato plants, Heuvelink (1989) found that for similar mean temperatures, a lower day than night temperature (DIF = -6 °C) reduced plant growth and development (number of leaves and number of trusses) with respect to a treatment with a DIF of 2°C with similar radiation levels. Yet, for a large positive DIF of 10°C, Heuvelink (1989) observed a growth rate and development rate similar to a DIF of 2°C. Gent and Ma (1998) observed that crops grown at a DIF of 14°C yielded more fruit fresh weight than those grown under 5°C DIF with similar radiation levels whereas Mavrogianopoulos and Kyritis (1989) observed at a DIF of 6°C and 18°C similar crop yield levels in warm climates. The negative effects of a large positive DIF on crop yield should be seen as a result of non-optimal temperature levels (i.e. caused by sub-optimal night temperature and/or supra-optimal day temperature) rather than day-night differences per se.

3.3.4 Temperature dependent growth rate responses and model implementation

Summarizing, the literature survey indicated that a) both instantaneous and mean temperatures affect crop yield, b) both sub-and supra-optimal temperatures affect several growth processes, resulting in lower yield, c) it is difficult to identify one single growth process causing crop stress because growth processes influence each other, d) stress sensitivity is cultivar dependent and, e) a negative DIF and a large positive DIF negatively affect crop yield due to sub-or supra-optimal temperatures.

Since the crop yield model will be integrated in a model-based design method, detailed modelling of the effects of non-optimal temperatures on individual crop growth processes was beyond the scope of this research. In contrast, a model was developed that captures the temperature dependency of various processes by means of two lumped temperature-dependent growth inhibition functions. These inhibition functions capture the instantaneous and the mean temperature effects on overall tomato yield by multiplying the potential tomato growth rate with these inhibition functions ($0 \leq \text{inhibition function} \leq 1$). These growth inhibition functions will implicitly take into account also the impact of large VPD on growth processes because a large VPD mainly occurs at a supra-optimal temperature. Abortion processes were already captured by the two lumped temperature-dependent growth inhibition functions and were therefore not modelled explicitly.

3.4 Model overview and states

3.4.1 Notational conventions

To describe the states and the flows of the tomato yield model the notational conventions of De Zwart (1996) are used. The states of the model are denoted by names with capital letters followed by one subscript (see the Nomenclature in section 3.8). The flows are denoted by a capital letter followed by two subscripts. The first subscript represents the source of the flow and the second subscript represents the destination of the flow. For example, MC_{AirBuf} denotes the carbon flow from air to the carbon buffer. The surface unit is m^2 of greenhouse floor, unless specified otherwise. As presented in the Nomenclature, the carbohydrates are expressed in $mg \{CH_2O\} m^{-2}$.

3.4.2 Model overview

The model structure, with a common carbohydrate buffer and carbohydrate distribution to plant organs as presented in Fig. 3.1, was essentially based on earlier crop yield models (Marcelis *et al.*, 1998; Heuvelink, 1996; Dayan *et al.*, 1993; Seginer *et al.*, 1994; Linker *et al.*, 2004) and extended with the two lumped temperature-dependent growth inhibition functions.

Photosynthesis MC_{AirBuf} depends mainly on the canopy temperature, the photosynthetically active radiation (PAR) absorbed by the canopy and the CO_2 -concentration in the greenhouse. When relating crop growth directly to photosynthesis without using a carbohydrate buffer, the impact of night temperature on growth would be neglected in the absence of photosynthesis. However, night temperatures play an important role in crop growth and development. To model the effects of night temperature on growth and development, the photosynthesised carbohydrates are stored in a buffer, C_{Buf} , whose outflow is affected by temperature. The buffer distributes the carbohydrates ($MC_{BufFruit}$, $MC_{BufLeaf}$, $MC_{BufStem}$) to the plant organs (C_{Fruit} , C_{Leaf} , C_{Stem}) even when no photosynthesis occurs. These carbohydrate flows are influenced by the availability of carbohydrates in the buffer, the organ growth rate coefficients, two temperature dependent growth inhibition functions (each described as a function of the instantaneous temperature, T_{Can} , and the 24 hour mean temperature, T_{Can}^{24}) and the temperature sum, T_{Can}^{Sum} , representing the development stage of the crop.

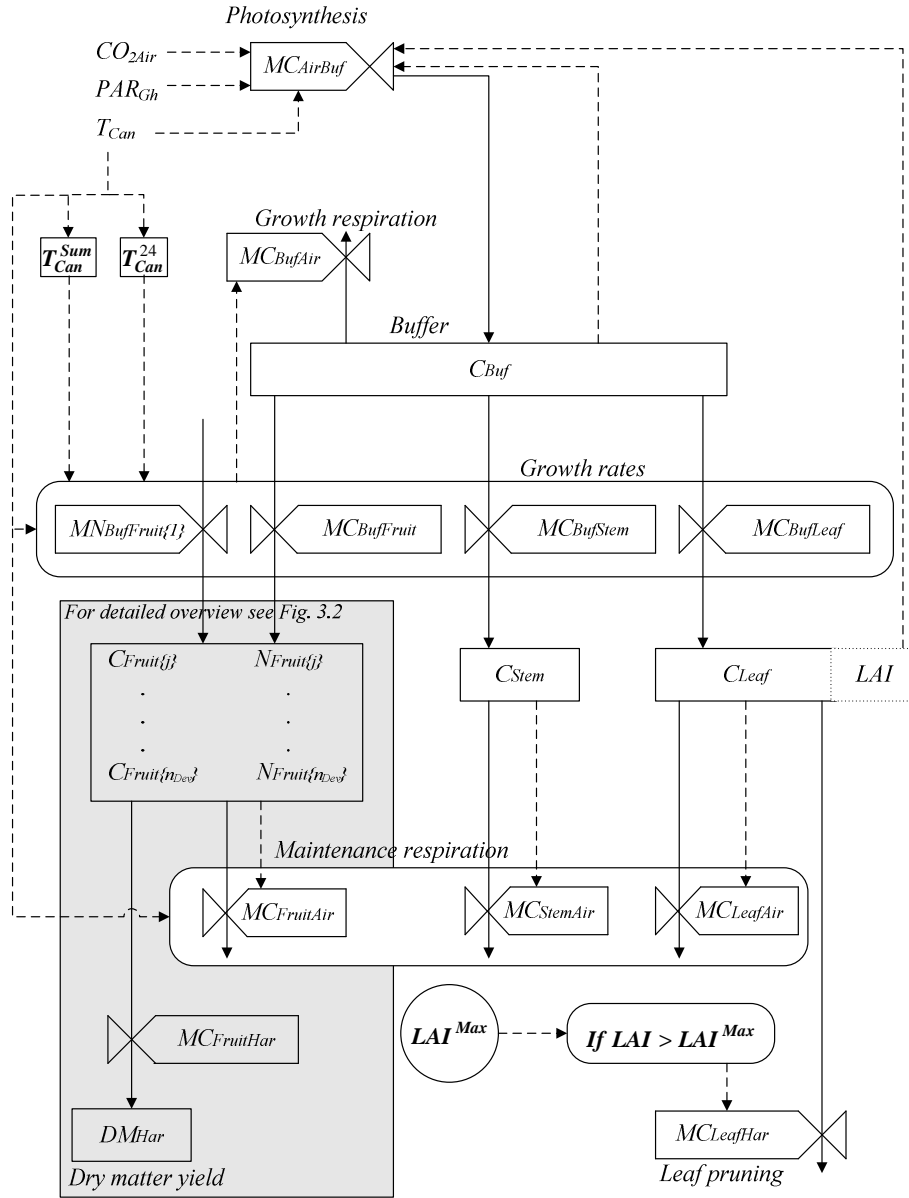


Fig. 3.1 Schematic diagram of the tomato yield model using a modelling formalism of Forrester (1962). The boxes represent the state variables of the model, valves are rate variables. The dashed lines are information flows and the solid lines represent mass flows. The box representing the fruit weight, $C_{fruit[j]}$, and the number of fruits, $N_{fruit[j]}$, is described in more detail in Fig. 3.2. The dotted box represents a semi-state variable of the model

The plant organ C_{Stem} represents the carbohydrates which are stored in both stem and root. To take into account the time delay between fruit set and fruit harvest, the model simulates for each fruit development stage, j , the fruit weight $C_{Fruit[j]}$ and the fruit numbers $N_{Fruit[j]}$. A part of the carbohydrates in the organs is used for maintenance respiration ($MC_{FruitAir}$, $MC_{LeafAir}$, $MC_{StemAir}$). When the leaf area index (LAI) exceeds a maximum value, LAI^{Max} , the leaves are pruned back to this value, resulting in the mass flow $MC_{LeafHar}$. The accumulated harvested tomato dry matter is determined by integrating the carbohydrate outflow of the last fruit development stage.

The state variable equations and the carbohydrate flow to the individual plant organs with special interest for the two lumped temperature-dependent growth inhibition functions are presented in this chapter. Because of space limitations the remaining model processes are presented in the detailed description of the tomato yield with which can be found in chapter 9. A brief description of these model processes is given here. The PAR absorbed by the canopy is described by a negative exponential decay of light with LAI in a homogeneous row crop as described by Ross (1975). The canopy photosynthesis is based on the leaf photosynthesis model of Farquhar and Von Caemmerer (1982), Farquhar *et al.* (1980) and Farquhar (1988) which is scaled up to canopy photosynthesis by multiplying the maximal rate of electron transport for a leaf with the LAI as described by Evans and Farquhar (1991). Even though VPD strongly affects stomatal conductance, photosynthesis is not sensitive to VPD (Stanghellini & Bunce, 1993). Therefore, VPD effects on canopy photosynthesis rate were not incorporated in the model. For the purpose of model-based greenhouse design, the crop yield model will be combined with a greenhouse climate model (see chapter 2) that calculates the canopy temperature. This state variable depends on the transpiration and stomatal model of Stanghellini (1987). Consequently, the modelled thermal and hydraulic feedback systems ensure that VPD affects the temperature dependent growth inhibition functions and crop growth through its effect on canopy temperature. The fruit flow and carbohydrate flow to fruit development stages and the daily potential growth rate per fruit for different fruit development stages are based on De Koning (1994). The growth and maintenance respiration are based on Heuvelink (1996). The model parameters are listed in Table 3.2.

Table 3.2 List of model parameters and symbols. If not specified, the mass units are expressed in $\{CH_2O\}$.

Parameter	Symbol and value	Unit	Reference
Conversion factor from carbohydrate to dry matter	$\eta_{C_DM} = 1$	mg {DM} mg^{-1}	No lignification assumed
The time constant to calculate the 24 hour mean temperature	$\tau = 86400$	s	See section 9.7.1
Maximum buffer capacity	$C_{Buf}^{Max} = 20 \cdot 10^3$	mg m^{-2}	See section 9.5.1
Minimum amount of carbohydrates in the buffer	$C_{Buf}^{Min} = 1 \cdot 10^3$	mg m^{-2}	See section 9.5.2
The gain of the process to calculate the 24 hour mean temperature	$k = 1$	-	See section 9.7.1
Potential fruit growth rate coefficient at 20°C	$rg_{Fruit} = 0.328$	mg $m^{-2} s^{-1}$	See section 9.7.3 (De Koning, 1994)
Potential leaf growth rate coefficient at 20°C	$rg_{Leaf} = 0.095$	mg $m^{-2} s^{-1}$	See section 9.7.3. (Heuvelink, 1996)
Potential stem growth rate coefficient	$rg_{Stem} = 0.074$	mg $m^{-2} s^{-1}$	See section 9.7.3 (Heuvelink, 1996)
Specific leaf area index	$SLA = 2.66 \cdot 10^{-5}$	$m^2 \{leaf\} mg^{-1}$	Based on Heuvelink (1996)
Temperature sum when fruit growth rate is at full potential	$T_{End}^{Sum} = 1035$	°C	Based upon Eq. (9.32)
Base temperature for 24 hour mean crop growth inhibition	$T_{Base_24} = 12$	°C	See section 9.7.3
1 st optimal temperature for 24 hour crop growth inhibition	$T_{Opt1_24} = 18$	°C	See section 9.7.3
2 nd optimal temperature for 24 hour crop growth inhibition	$T_{Opt2_24} = 22$	°C	See section 9.7.3
Maximum temperature for 24 hour crop growth inhibition	$T_{Max_24} = 27$	°C	See section 9.7.3
Base temperature for instantaneous crop growth inhibition	$T_{Base_Inst} = 6$	°C	See section 9.7.3
1 st optimal temperature for instantaneous crop growth inhibition	$T_{Opt1_Inst} = 14$	°C	See section 9.7.3
2 nd optimal temperature for instantaneous crop growth inhibition	$T_{Opt2_Inst} = 28$	°C	See section 9.7.3
Maximum temperature for instantaneous crop growth inhibition	$T_{Max_Inst} = 40$	°C	See section 9.7.3

3.4.3 State variables of the model

The state variables of the model are all described by differential equations. The derivatives of the state variables to time are indicated by a dot above the state symbol.

The evolution of the carbohydrates in the buffer, C_{Buf} , in time is described by:

$$\dot{C}_{Buf} = MC_{AirBuf} - MC_{BufFruit} - MC_{BufLeaf} - MC_{BufStem} - MC_{BufAir} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (3.1)$$

where MC_{AirBuf} is the photosynthesis rate, $MC_{BufFruit}$, $MC_{BufLeaf}$, $MC_{BufStem}$ are the carbohydrate flows to fruits, leaves and stems respectively, and MC_{BufAir} is the growth respiration of the plant. During the light period carbohydrates produced by the photosynthesis are stored in the buffer and, whenever carbohydrates are available in the buffer, carbohydrates flow to the plant organs. This carbohydrate flow stops when the buffer approaches its lower limit. When the buffer approaches its upper limit, carbohydrates can not be stored anymore in the buffer and the photosynthesis will be inhibited.

The time between fruit set and fruit harvest is the fruit growth period which is modelled using a “fixed boxcar train” method of Leffelaar and Ferrari (1989). This method implies that carbohydrates and the number of fruits flow from one fruit development stage to the next with a specific development rate (Fig. 3.2). When the plant shifts from the vegetative stage to the generative stage, carbohydrates are stored in the fruit development stage j , $C_{Fruit\{j\}}$, as described by:

$$\dot{C}_{Fruit\{j\}} = MC_{BufFruit\{j\}} + MC_{Fruit\{j-1\}Fruit\{j\}} - MC_{Fruit\{j\}Fruit\{j+1\}} - MC_{FruitAir\{j\}} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (3.2)$$

with $j = 1, 2, \dots, n_{Dev}$

where $MC_{BufFruit\{j\}}$ is the carbohydrate flow from the buffer to fruit development stage j , $MC_{Fruit\{j-1\}Fruit\{j\}}$ and $MC_{Fruit\{j\}Fruit\{j+1\}}$ represent the carbohydrate inflow from the previous development stage and the outflow to the next stage respectively, $MC_{FruitAir\{j\}}$ is the fruit maintenance respiration of development stage j , and n_{Dev} is the total number of fruit development stages. For the first fruit development stage, the carbohydrate inflow from the previous stage is zero. For the last development stage, the carbohydrate outflow to the next stage is described by $MC_{FruitHar}$.

The number of fruits in the fruit development stage j , $N_{Fruit\{j\}}$, affects the carbohydrate distribution to the fruits and is therefore described by:

$$\dot{N}_{Fruit\{j\}} = MN_{Fruit\{j-1\}Fruit\{j\}} - MN_{Fruit\{j\}Fruit\{j+1\}}, \quad j = 1, 2, \dots, n_{Dev} \quad [\text{fruits m}^{-2} \text{s}^{-1}] \quad (3.3)$$

where $MN_{Fruit\{j-1\}Fruit\{j\}}$ is the fruit number flow from fruit development stage $j-1$ to stage j

and $MN_{Fruit\{j\}Fruit\{j+1\}}$ is the fruit number flow from fruit development stage j to stage $j+1$. For the first fruit development stage $MN_{Fruit\{j-1\}Fruit\{j\}}$ is replaced by $MN_{BufFruit\{1\}}$.

The fruit number flow to the first fruit development stage depends on carbohydrates available for fruit growth and on the truss appearance rate. The carbohydrates stored in the leaves, C_{Leaf} , are described by:

$$\dot{C}_{Leaf} = MC_{BufLeaf} - MC_{LeafAir} - MC_{LeafHar} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (3.4)$$

where $MC_{BufLeaf}$ is the carbohydrate flow from the buffer to leaves, $MC_{LeafAir}$ is the maintenance respiration of the leaves and $MC_{LeafHar}$ is the leaf pruning.

The LAI is a semi-state of the model and is calculated by:

$$LAI = SLA \cdot C_{Leaf} \quad [\text{m}^2 \{\text{leaf}\} \text{ m}^{-2}] \quad (3.5)$$

where SLA is the specific leaf area ($\text{m}^2 \{\text{leaf}\} \text{ mg}^{-1} \{\text{CH}_2\text{O}\}$).

The carbohydrates stored in the stem and roots, C_{Stem} , are described by:

$$\dot{C}_{Stem} = MC_{BufStem} - MC_{StemAir} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (3.6)$$

where $MC_{BufStem}$ is the carbohydrate flow from the buffer to stems and roots, $MC_{StemAir}$ is the maintenance respiration of the stems and roots.

For sake of simplicity a continuous harvest rate was assumed. Consequently, the accumulated harvested tomato dry matter (DM), DM_{Har} , equals the outflow of dry matter from the last fruit development stage and is described by:

$$\dot{DM}_{Har} = \eta_{C_DM} \cdot MC_{FruitHar} \quad [\text{mg}\{\text{DM}\} \text{ m}^{-2} \text{ s}^{-1}] \quad (3.7)$$

where η_{C_DM} is the conversion factor from carbohydrate to dry matter. Since growth respiration was incorporated into the model, this conversion factor is $1 \text{ mg}\{\text{DM}\} \text{ mg}^{-1} \{\text{CH}_2\text{O}\}$.

The development stage of the plant, required to describe the transition from the vegetative to the generative stage, is expressed by the temperature sum:

$$\dot{T}_{Can}^{Sum} = \frac{1}{86400} T_{Can} \quad [^{\circ}\text{C s}^{-1}] \quad (3.8)$$

where T_{Can} is the simulated canopy temperature. By definition, the start of the generative period T_{Can}^{Sum} is zero.

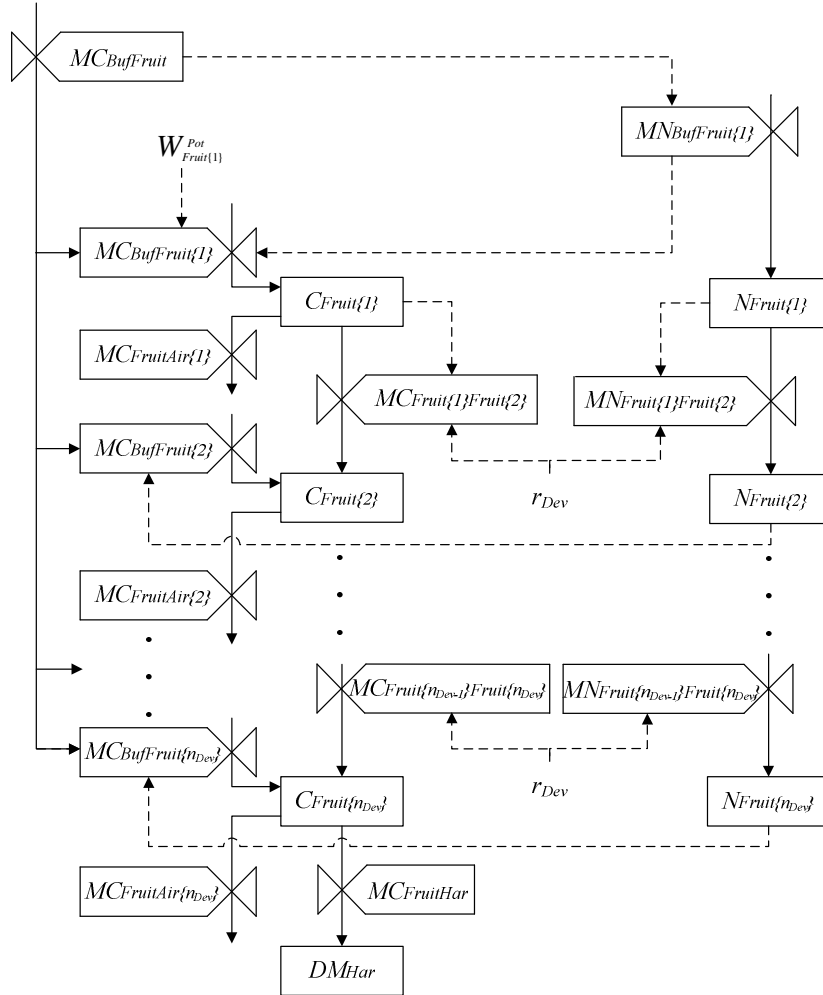


Fig. 3.2 Fruit development is modelled by describing for each fruit development stage the number of fruits, $N_{Fruit\{j\}}$ and the amount of carbohydrates, $C_{Fruit\{j\}}$. As in Fig. 3.1, the boxes represent the state variables of the model, valves are rate variables. The dashed lines are information flows and the solid lines represent the carbon and fruit flows. The carbohydrates available for fruit growth, $MC_{BufFruit}$ are distributed to the different fruit development stages $C_{Fruit\{j\}}$. The carbohydrate flow to the first development stage $MC_{BufFruit\{1\}}$ is affected by the fruit set $MN_{BufFruit\{1\}}$ which in turn is influenced by the carbohydrates available for fruit growth $MC_{BufFruit}$ and the potential fruit growth rate $W_{Fruit\{1\}}^{Pot}$ as described in Eq.(9.35). The carbohydrate flow to the remaining fruit development stages is influenced by the available carbohydrates $MC_{BufFruit}$, the number of fruits $N_{Fruit\{j\}}$ and by a development stage dependent fruit growth rate as described by Eq. (9.38).

The 24 hour mean canopy temperature was approached by a 1st order approach:

$$\dot{T}_{Can}^{24} = \frac{1}{\tau} (kT_{Can} - T_{Can}^{24}) \quad [^{\circ}\text{C s}^{-1}] \quad (3.9)$$

where τ , represents the time constant of the process and k is the gain of the process. When integrated in the model-based design method, the greenhouse climate model calculates the canopy temperature as a state variable. Therefore, the canopy temperature and the 24 hour mean canopy temperature could not be calculated beforehand. To approximate the 24 hour mean canopy anyway, the first order approach of Eq. (3.9) as derived in section 9.7.1 was incorporated into the model.

3.4.4 The carbohydrate flow to the individual plant organs

The carbohydrate flow from buffer to the fruits is determined by multiplying the potential fruit growth coefficient rg_{Fruit} , by the inhibition factors h :

$$MC_{BufFruit} = h_{C_{Buf}}^{MC_{BufOrg}} \cdot h_{Tcan} \cdot h_{Tcan24} \cdot h_{TcanSum} \cdot g_{Tcan24} \cdot rg_{Fruit} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (3.10)$$

where the inhibition factors ($0 < h < 1$): are: $h_{C_{Buf}}^{MC_{BufOrg}}$ (-), insufficient carbohydrates in the buffer; h_{Tcan} (-), non-optimal instantaneous temperature; h_{Tcan24} (-), non-optimal 24 hour mean canopy temperatures; and $h_{TcanSum}$ (-), crop development stage. The effect of the 24 hour mean temperature on the carbohydrate flow to fruits is described by g_{Tcan24} (-) and rg_{Fruit} ($\text{mg } \{\text{CH}_2\text{O}\} \text{ m}^{-2} \text{ s}^{-1}$) is the potential fruit growth rate coefficient at 20°C.

The carbohydrate flow to the first fruit development stage is influenced by the available carbohydrates for fruit growth, fruit set and potential fruit growth rate (Fig. 3.2 and Eq. (9.35) in chapter 9). The carbohydrate flow to the remaining fruit development stages depends on the available carbohydrates, the number of fruits and the fruit growth rate as a function of fruit development stage (Fig. 3.2 and Eq. (9.36)).

The carbohydrate flow from buffer to the leaves and stem is described by:

$$MC_{BufOrg(i)} = h_{C_{Buf}}^{MC_{BufOrg}} \cdot h_{Tcan24} \cdot g_{Tcan24} \cdot rg_{Org(i)} \quad i = 2,3 \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (3.11)$$

where i represents the plant organ code for *Leaf* and *Stem*, $rg_{Org(i)}$ ($\text{mg } \{\text{CH}_2\text{O}\} \text{ m}^{-2} \text{ s}^{-1}$) is the organ growth rate coefficient at 20°C. As in agreement with Table 3.1, these carbohydrate flows are not influenced by instantaneous temperature. The two lumped temperature-dependent growth inhibition functions of Eqs. (3.10) and (3.11) are described in more detail in this section.

The literature review revealed that crop growth was inhibited by non-optimal levels of the instantaneous and 24 hour mean temperature which was described by two trapezoid growth inhibition functions, $h_{T_{can}}$ and $h_{T_{can24}}$, respectively. Each inhibition function was based on Boote and Scholberg (2006) and was described by four cardinal temperatures (Fig. 3.3).

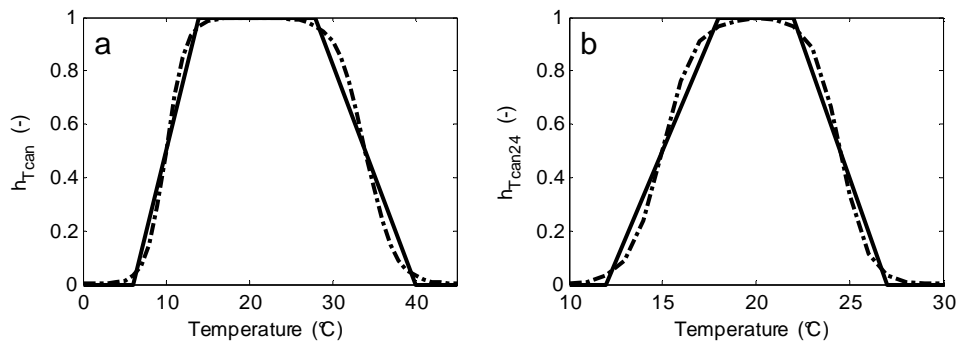


Fig. 3.3 The growth inhibition by the instantaneous temperature (a) and by the 24 hour mean canopy temperature (b). The solid lines represent the non-differentiable inhibition functions and the dashed dotted lines represent the differentiable inhibition functions. The non-differentiable inhibition functions were each smoothed by multiplying two smoothed conditional “if/else” statements as described in section 9.7.2. The cardinal temperatures for both inhibition functions are presented in Table 3.2.

Below a certain base temperature T_{Base} no carbohydrate flow to organs is expected ($h=0$), between T_{Opt1} and T_{Opt2} the carbon flow is maximal ($h=1$) and above T_{Max} no carbohydrate flow is expected ($h=0$). Between T_{Base} and T_{Opt1} and between T_{Opt2} and T_{Max} a linear relationship between inhibition and temperature is assumed. The growth inhibition function of Boote and Scholberg (2006) is not differentiable and therefore not suitable for dynamic optimisation purposes. Therefore, the non-differentiable inhibition functions were each smoothed by multiplying two smoothed conditional “if/else” statements as described in section 9.7.2. Based on the temperature effects on crop growth presented in Table 3.1, the cardinal temperatures presented in Table 3.2 were determined as described in section 9.7.3

3.5 Model validation

For all four temperature regimes, the yield model was validated using the same model parameters (Table 3.2). Since most of these parameters were extracted from literature, model parameters were not calibrated on data. Therefore, all simulations presented in Fig. 3.5 to Fig. 3.7 can be considered as model validations. The model was first validated for mild temperatures commonly encountered under Dutch greenhouse conditions and second for extreme temperatures encountered under southeast Spanish greenhouse conditions. Third, the model was validated for non-optimal temperature conditions. Fourth, the tomato harvest rate for long-term diurnal temperature oscillations was determined and compared with data obtained from literature.

To simulate crop yield, the differential equations were solved with an ODE solver of Matlab 7.1[®]. Hourly greenhouse climate data, i.e. greenhouse air temperature, CO₂-concentration and outside global radiation were used as model inputs. Since the canopy temperature was not measured, it was assumed to be equal to the greenhouse air temperature. An overview of the data needed to run the model for the Dutch and Spanish greenhouses is presented in Table 3.3. For the Dutch and Spanish validation studies, solely the LAI was measured as initial crop condition. Therefore, the initial leaf carbohydrates were calculated based on the LAI and the specific leaf area (Eq. 3.5). The initial stem and root carbohydrates were determined by multiplying the leaf carbohydrates with a ratio that depends on the vegetative development. Since the initial temperature sum was unknown for the Spanish studies, this parameter was fitted to the data to assure that the moment of the simulated first tomato harvest was equal to the measured first tomato harvest.

3.5.1 Model validation for mild temperature conditions

The model was validated with measured tomato yield—obtained under mild temperature conditions—of two Dutch greenhouse growers in different production years. In both cases tomatoes were grown in a Venlo-type greenhouse which was equipped with CO₂-enrichment and a heating system. Tomatoes were grown close to the optimal 24 hour mean canopy temperature interval of 18°C-22°C with varying CO₂-concentrations and PAR levels commonly encountered in the Dutch greenhouses (Table 3.3).

Table 3.3 The location, crop production data, initial conditions, the mean greenhouse climate conditions for the Dutch growers A and B and for the low-tech and high-tech located in Southern Spain. Some initial crop conditions were not measured but calculated as described in section 3.5.

	Grower A	Grower B	Low-tech Spain	High-tech Spain
<i>Location</i>				
Latitude	52°0'N	52°0'N	36°57'N	36°48'N
Longitud	4°3'E	4°3'E	2°00'W	2.43'W
Elevation (m)	-3	-3	180	151
<i>Crop production data</i>				
Start growing cycle	10-12- 1999	8-12-1997	1-8-2009	26-9-2003
End growing cycle	2-10-2000	23-9-1998	5-05-2010	9-07-2004
Cultivar	Aromata	Rapsodie	Atletico	Pitenza
Greenhouse transmission	78%	78%	55%	40%
LAI^{Max}	3.0	2.85	3.5	3.5
<i>Initial conditions</i>				
Start simulation	6-1-2000*	6-1-1998*	1-8-2009	26-9-2003
$T_{CanSum0}$ (°C)	0	0	-900	-650
LAI_0 (m ² m ⁻²)	1.06	1.25	0.4	0.1
C_{Leaf0} (mg {CH ₂ O} m ⁻²)	40·10 ³	47·10 ³	15·10 ³	3.8·10 ³
C_{Stem0} (mg {CH ₂ O} m ⁻²)	30·10 ³	31·10 ³	15·10 ³	3.8·10 ³
<i>Indoor climate</i>				
Mean canopy temperature (°C)	18.2 (2.7)	19.1 (2.1)	17.5 (7.0)	19.7 (3.2)
Daily global outside radiation (MJ m ⁻² day ⁻¹)	12.2 (7.4)	9.7 (5.6)	12.9 (5.6)	15.9 (7.7)
Mean CO ₂ concentration at daylight (μmol mol ⁻¹)	677 (301)	659 (253)	355 (15)	476 (81)

The * indicates that the simulation started at onset generative phase.

3.5.2 Model validation for Spanish temperature conditions

The model was validated with measured tomato yield obtained for Southern Spanish climate conditions for a low tech “raspa y amagdo” greenhouse (LT) with only natural ventilation and a high tech greenhouse arch shape multi-tunnel (HT) equipped with natural

ventilation, a heating system, a thermal screen, an external shade screen, a fogging system and CO₂ enrichment. In the LT greenhouse tomatoes were imposed to strongly fluctuating temperatures being frequently non-optimal (Table 3.3). In contrast, in the HT greenhouse tomatoes were grown closer to the optimal 24 hour mean canopy temperature interval.

3.5.3 Model validation for extreme temperature conditions

The simulated tomato yield for four different mean temperature levels was compared with yield measurements of the cultivar Liberto conducted in growth chambers by Adams *et al.* (2001). Until 26 weeks after sowing, Adams *et al.* determined the yield for four constant temperature regimes of 14°C, 18°C, 22°C and 26°C with the following climate set-points: a daylight period of 12 hours with 315 µmol photons m⁻² s⁻¹ PAR above the canopy and a CO₂-concentration of 1000 µmol CO₂ mol⁻¹ air. Subsequently the model simulated tomato yield using the climate set-points of Adams as model inputs.

The simulated temperature treatment started similarly to Adams *et al.* (2001) – 21 days after sowing – when plants were still in the vegetative stage. Since destructive crop measurements were not performed, the following initial conditions were estimated for the 21 days old tomato crop: LAI_0 was 0.1, C_{Leaf0} was $3.8 \cdot 10^3$ mg {CH₂O} m⁻², C_{Stem0} was $2.5 \cdot 10^3$ mg {CH₂O} m⁻². The temperature sum for onset of the generative stage was determined from the observations of the first fruit harvest for the different temperature treatments, which resulted in a mean temperature sum, T_{Can}^{Sum} , of -550 °C. As a best estimate of LAI^{Max} , the mean of the measured LAI (2.5) of a full grown commercial tomato crop was used.

To make a fair comparison between the measured and simulated crop yield results, the measured fresh tomato yield per plant obtained by Adams *et al.* (2001) was expressed in dry matter tomato yield (g {DM} m⁻²). For this re-calculation, the plant density of each growth chamber was set to 2.2 plants m⁻² and the average dry matter content of the fruits for the treatments 14°C, 18°C, 22°C and 26°C were set at 10.7%, 6.2%, 5.6% and 6.2%, respectively according to Adams (personal communication, 2008).

3.5.4 Model evaluation of effects of diurnal temperature oscillations

The effect of diurnal temperature oscillations on crop yield was investigated for four temperature trajectories, namely: low night temperatures (T_{night}), high day temperatures (T_{day}), mean temperature (T_{mean}) and the difference between day and night temperature (DIF) (T_{DIF}) as shown in Fig. 3.4. The temperature trajectories of T_{night} , T_{day} and T_{DIF} were described by a sine function with a mean temperature of 20°C and a different day and night

amplitude. The temperature trajectory of T_{mean} , was described by a variable mean temperature (14°C, 18°C, 22°C and 26°C) with a fixed day and night amplitude of 3°C.

The tomato harvest rate for the four temperature scenarios was simulated under the following conditions: the plant was totally in the generative stage with a LAI^{Max} of 2.5 and the simulation period was 100 days. The PAR absorbed by the crop during the light period of 12 hours was described by a sinus function. To investigate how the harvest rate response to temperature depends on PAR, two PAR amplitudes were used: 460 $\mu\text{mol photons m}^{-2} \text{ s}^{-1}$ and 920 $\mu\text{mol photons s}^{-1} \text{ m}^{-2}$. The CO_2 level in the greenhouse was 370 $\mu\text{mol CO}_2 \text{ mol}^{-1}$ air. The tomato harvest rates were determined for the last seven days of the total production period of 100 days to prevent the influence of the initial conditions on the results.

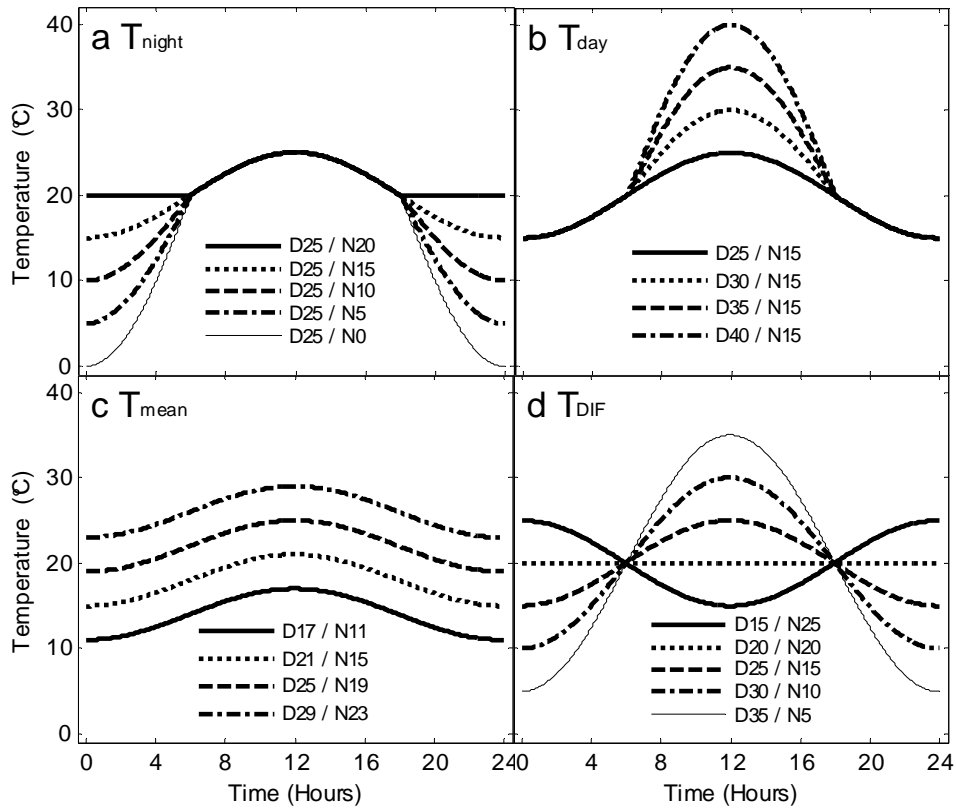


Fig. 3.4 The temperature trajectories for the four temperature sensitivity studies: a) different night temperatures (T_{night}); b) different high day temperatures (T_{day}); c) different mean temperatures (T_{mean}); and d) difference between day and night temperature (T_{DIF}).

3.6 Results and discussion

In section 3.6.1 to 3.6.4 the validation results are presented and discussed with respect to model performance on the tomato yield (g DM m^{-2}). In section 3.6.5 the model is discussed with respect to other tomato yield models and relevant yield model aspects for greenhouse design optimisation are discussed as well. All tomato yield simulations were performed with the same set of model parameters.

3.6.1 Model validation for mild temperature conditions

For two commercial Dutch greenhouses, with mild temperature conditions and varying global radiation levels and CO_2 -concentrations (Table 3.3), the model simulated the tomato yield very well (Fig. 3.5). Only the tomato yield of grower B was slightly overestimated at the end of the production period. The higher crop yield of greenhouse A compared to greenhouse B was caused by its higher outside global radiation.

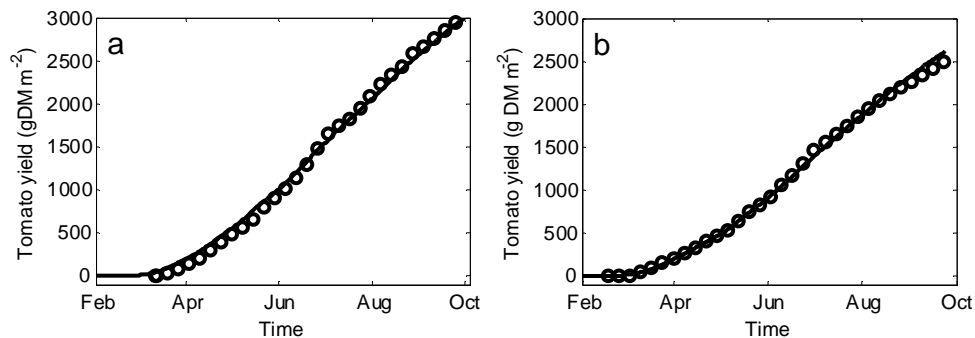


Fig. 3.5 The simulated tomato yield compared with measurements for grower A (a) and for grower B (b) under mild temperatures in Dutch greenhouses. Solid lines represent the simulations and the circles represent the measurements.

3.6.2 Model validation for Southern Spanish temperature conditions

The impact of non-optimal temperatures on model performance was evaluated using Southern Spanish climate conditions. The tomato yield of the LT greenhouse was simulated with fair accuracy (Fig. 3.6a). The cumulative measured tomato yield of 922 g DM m^{-2} was underestimated by the model with 97 g DM m^{-2} . This difference will not be a problem for greenhouse design because the error will be located in model uncertainty. The

trend of the simulated yield differed from the measured yield which might be caused by errors introduced due to the conversion from measured tomato fresh tomato yield to calculated dry matter yield. For this conversion a constant dry matter content (DMC) was used since time variant measurements were missing. However, according to Segura *et al.* (2009) the dry matter content varies along the production period with a relatively low DMC in winter and a relatively high DMC in summer under South Spanish conditions. Using a time dependent DMC would improve the trend of the measured dry matter yield. Additionally, the underestimation of the measured crop yield might be caused by applying generic cardinal temperatures for the growth inhibition functions to a cultivar bred to withstand low temperatures. To improve the simulation result further, an option is to calibrate these cardinal temperatures for each cultivar.

For the HT greenhouse, the model predicted accurately the tomato yield (Fig. 3.6b). Only at the end of the production period the crop yield was underestimated slightly due to harvest simulation of the dry matter outflow from the last fruit development stage (Eq. 3.7) whereas in practise all marketable tomatoes on the plant were harvested.

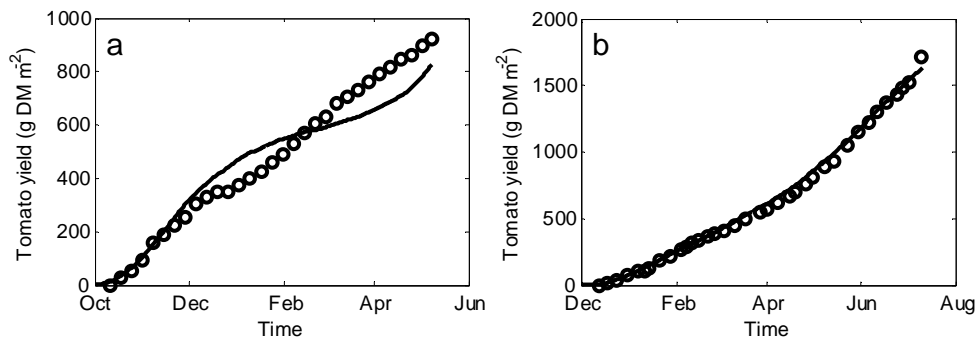


Fig. 3.6 The simulated tomato yield compared with measurements in a low-tech greenhouse (a) and a high-tech greenhouse (b) located in South Spain. Solid lines represent the simulations and the circles represent the measurements.

3.6.3 Model validation for extreme temperature conditions

Comparing simulated yield with yield measured by Adams *et al.* (2001), it can be observed that the model simulated with fair accuracy the effect of the mean temperature regimes of 14°C, 18°C, 22°C and 26°C on yield (Fig. 3.7a, b).

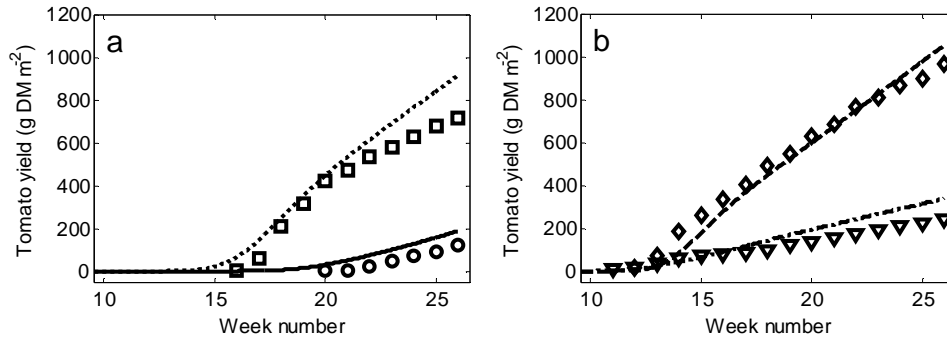


Fig. 3.7 The simulated tomato yield for four different mean temperature treatments between week number 10 and 26 after sowing. Fig.3.7a presents the crop yield at 14°C (solid line represents the simulation and circles the measurements) and at 18°C (dotted line represents the simulation and squares the measurements). Fig. 3.7b presents the crop yield at 22°C (dashed line represents the simulation and diamonds the measurements) and at 26°C (dashed dotted line represents the simulation and triangles the measurements). Source of the measured data was Adams et al. (2001).

The model correctly captured a reduction in yield at non-optimal mean temperatures of 14°C and 26°C. Specifically, the simulated relative decrease in crop yield at non-optimal temperatures was almost equal to the measured relative reduction in yield (Table 3.4) as caused by the growth inhibition due to temperature (Eq. (3.10) and Fig. 3.3). However, the model tended to overestimate the yield at the end of the growing period by on average 33% (Table 3.4). This overestimation might be caused by growth chamber conditions not equal to those in the greenhouse for which the model was developed.

Table 3.4 Simulated and measured production values for four temperature treatments.

	Temperature (°C)			
	14	18	22	26
<i>Production (g {DM} m⁻²)</i>				
Measured	123	720	970	241
Simulated	188	919	1057	340
<i>Relative production compared to maximum (%)</i>				
Measured	13	74	100	25
Simulated	18	87	100	32
Difference between simulations and measurements (%)	53	28	9	41

Temperature effects on first fruit harvest were simulated in close agreement to the measured first fruit harvest. Specifically, low mean temperature resulted in a delayed simulated first fruit harvest which was caused by the temperature effect on both vegetative development rate and generative development rate. However, for low mean temperatures (14°C and 18°C) the simulated first fruit harvest was earlier than the measured first fruit harvest whereas for high mean temperatures (22°C and 26°C) the simulated first fruit harvest was later than the measured values. The moment of simulated first fruit harvest at 14°C and 26°C differed 5 weeks whereas 10 weeks were measured. This underestimation was caused by processes both in the vegetative and generative period as explained hereafter.

Regarding vegetative development, a linear relationship with temperature was modelled using Eq. (9.27) of the detailed model description. However, measurements indicated that at sub-optimal temperatures the crop needs a higher temperature sum to fulfil the vegetative development period (Adams, personal communication 2009). To improve the simulation of the vegetative period, a base temperature should be introduced in the temperature sum description of Eq. (3.8).

The temperature sum needed for the generative period was based on the fruit development rate of Eq. (9.32) as determined by De Koning (1994), being different from the temperature sum of Adams *et al.* (2001) for the measurements under consideration. The underestimation of the fruit growth period at lower temperatures is due to the lower temperature sum from De Koning (1994) which resulted in a 24 days shorter growing period at 14°C than the observed fruit growth period of Adams *et al.* (2001).

3.6.4 Model evaluation for diurnal temperature oscillations

To evaluate the model for its response to diurnal temperature oscillations, the trends of the simulated crop harvest responses to four extreme temperature treatments (Fig. 3.4, Fig. 3.8 and Fig. 3.9) were compared with harvest responses obtained from literature (Table 3.1). The impact of a low night temperature on harvest rate (Fig. 3.8a) shows that the model reproduced the expected interaction between radiation and temperature on harvest rate. In agreement with Martínez Mirón (2008), the optimum night temperature increased with increasing PAR level. Specifically, at a low PAR level the optimum night temperature was 5°C whereas at a high PAR level the optimum night temperature was 10-15°C. In addition, the positive impact of PAR on harvest rate at moderate temperature trajectories was demonstrated. For instance, for the day/night treatment of 25°C/15°C, the harvest rate at a low PAR level was 55.2 % of the harvest rate at a high PAR level (123.1 g m⁻² week⁻¹).

Although negative effects of low night temperatures on tomato harvest rate were incorporated in the model, at low PAR levels the simulated tomato harvest rate increased slightly with decreasing night temperature. This result was in agreement with Martínez Mirón (2008) who measured under constant shading in the autumn and winter season in Southern Spain a higher yield at a mean night-time temperature of 13.2°C than at 15.2°C. This effect was caused by lower maintenance respiration losses at low night temperature. It seems that the model was not valid for extremely low night temperatures because at 0°C and 5°C still a reasonable crop yield was simulated. This overestimation was caused by not modelling lethal damage or hormonal misbalances at low temperature. Nevertheless, extremely low temperatures will decrease tomato yield rate through the effect of mean temperature on tomato yield (Fig. 3.9a).

Fig. 3.8b shows that too high day temperatures lowered the harvest rate for both PAR levels. Under high PAR levels, the harvest rate at a maximum day temperature of 40°C was 54.5 % of the harvest rate at a maximum day temperature of 25°C. This result was in agreement with a measured tomato yield decrease of 46.1% at 35°C compared to the 25°C treatment which was observed by Zhang *et al.* (2008).

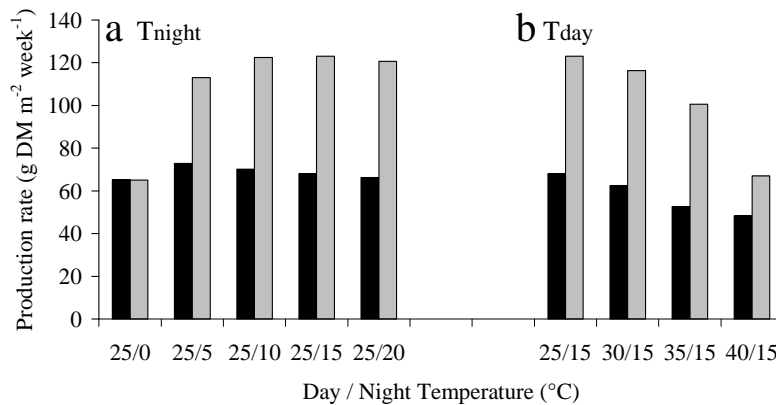


Fig. 3.8 The effect of daily fluctuations of the night temperature T_{night} (a) and the day temperature T_{day} (b) on production rate for two levels of PAR: 460 $\mu\text{mol photons m}^{-2} \text{s}^{-1}$ (the black bar) and 920 $\mu\text{mol photons m}^{-2} \text{s}^{-1}$ (the grey bar).

In agreement with the crop yield measurements of Adams *et al.* (2001), Fig. 3.9a shows that non-optimal mean temperature affected negatively the harvest rate at both PAR levels. Specifically, the harvest rate under high PAR levels at a mean temperature of 14°C was 32.0 % of the harvest rate at the mean temperature of 18°C ($129.1 \text{ g m}^{-2} \text{ week}^{-1}$) whereas the harvest rate at a mean temperature of 26 °C was 19.6 % of the harvest rate at the mean temperature of 18°C. These results agreed well with crop yield reductions at non-optimal mean temperatures shown in Table 3.1. The tomato harvest rate at non-optimal mean temperatures was equal for both PAR levels. Specifically, at non-optimal temperatures the carbon outflow from buffer to fruits was reduced due to the temperature dependent growth inhibition functions (Eq. (3.10) and Fig. 3.3) whereas the inflow of carbon produced by photosynthesis sustained until buffer saturation. At buffer saturation, the photosynthesis was inhibited which resulted in lower crop yield values. Not PAR but temperature was thus the limiting factor for crop growth.

A DIF lower than 20°C influenced only slightly the harvest rate (Fig. 3.9b) which was in close agreement with Mavrogianopoulos and Kyritis (1989) who found a similar crop yield at a DIF of 6°C and 18°C. In contrast, a large DIF of 30°C did negatively affect the crop harvest rate. Specifically, for high PAR levels, the treatment of 35/ 5°C resulted in 70.5 % of the harvest rate obtained in the treatment of 20/ 20°C ($124.4 \text{ g m}^{-2} \text{ week}^{-1}$). The simulated harvest reduction was caused by both a sub-optimal night temperature of 5°C and a supra-optimal day temperature of 35°C. Although the effect of an extremely high DIF on tomato harvest rate was not explicitly described by the model, its impact on tomato harvest rate was properly simulated.

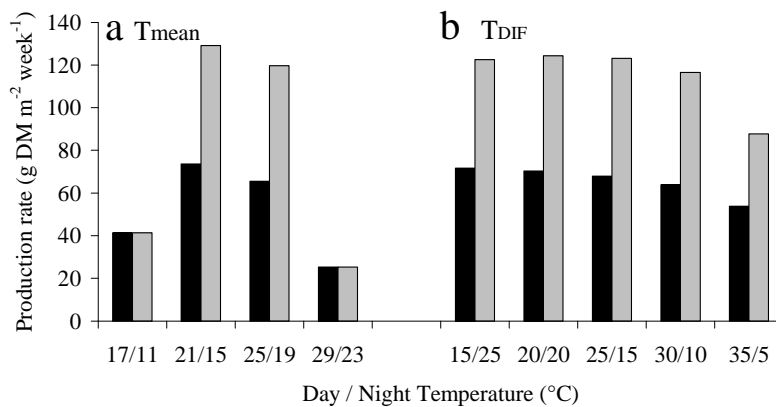


Fig. 3.9 The effect of daily fluctuations of the 24 hour mean temperature T_{mean} (a) and the difference between day and night temperature T_{DIF} (b) on production rate for two levels of PAR: $460 \mu\text{mol photons m}^{-2} \text{ floor s}^{-1}$ (the black bar) and $920 \mu\text{mol photons m}^{-2} \text{ floor s}^{-1}$ (the grey bar).

3.6.5 Discussion of model performance in view of greenhouse design

In horticultural research a considerable number of tomato yield models have been developed. For the aim of greenhouse design optimisation, the presented yield model has two advantages compared to, for example, the TOMGRO model (Jones *et al.*, 1991; Dayan *et al.*, 1993): 1) the crop response to extreme values for both instantaneous and diurnal mean temperature effects are modelled implying that the model can be used within a model-based greenhouse design method, 2) the model is described in differential equations with continuous differentiable right hand sides enabling us to combine the yield model with the greenhouse climate model presented in chapter 2 to solve differential equations with an existing ordinary differential equations solver and to use gradient based-optimisation algorithms to optimise greenhouse design. Furthermore, the model describes, based on crop physiological processes, the most important effects of extreme temperatures on tomato yield. These crop physiological processes were lacking in related studies. Specifically, Ioslovich and Seginer (1998) bounded the minimum and maximum temperature and Ooteghem (2007) penalized extreme temperatures by introducing a term in the cost criterion.

Given these results, obtained for a broad range of temperature conditions, the model is considered to be sufficiently accurate to be used for developing a model-based greenhouse design method. However, since our aim was to develop a design method that focussed on the optimisation of a set of design elements, model aspects that might be relevant may have been neglected or too much simplified. Therefore, whenever better or new modules are available, they can be easily incorporated into the design method. Some issues that might improve the generality of the model-based design method are discussed in more detail here.

To enhance the generality, yield models of other crops than tomatoes should be developed that fulfil the same requirements as demanded for the tomato yield model. Additionally, the transpiration module of the greenhouse climate model (see section 8.9) should then be adjusted to this crop as well. Performance of the tomato yield model might be improved by describing the impact of temperature and other climate variables on each growth and development process such as fruit set, fruit abortion and membrane integrity. Since modules of these processes were not available, two lumped temperature dependent growth inhibition functions were used in this study. Growth inhibition functions were based on literature values and therefore photosynthesis effects might have been captured in these functions. Since the simulated photosynthesis depended already on temperature, effects of non-optimal temperatures on photosynthesis might have been overestimated by the model.

However, first analysis of the crop yield prediction for non-optimal temperature conditions revealed that the incorporation of photosynthesis effects in the inhibition functions did not play an important role as can be seen in Fig. 3.7 and Fig. 3.8 due to the plant's ability to store carbohydrates in the buffer.

To solve a greenhouse design problem, the economic benefits of crop yield must be determined. Since the presented model described dry matter yield as a function of greenhouse climate, the impact of dry matter content on fresh tomato yield should be integrated into the model. In addition, this DMC should then be described as a function of electrical conductivity of the growing medium, on outdoor climate variations (Segura *et al.*, 2009) and on non-optimal temperatures (Adams *et al.*, 2001). Subsequently, the quality of the tomatoes must be incorporated into the model since they determine the economic yield. According to Adams *et al.* (2001) the quality of the tomatoes and marketable ratio depends on temperature and air humidity. Therefore, when using the model for optimal greenhouse design, it would be better to describe the impact of humidity on quality and yield. To do this, the tomato quality model of Liu *et al.* (2007) can be used as a starting point. No direct effects of a large VPD on photosynthesis were modelled. However, when integrated in de model-based design method, a large VPD will indirectly affect growth through its effect on transpiration and canopy temperature. Additionally, fertigation was assumed to be non-limiting for crop growth whereas in practise it might occasionally be non-optimal. The impact of fertigation on crop yield can be described by the nutrient model of Van Straten *et al.* (2006).

Since temperature effects on crop yield are cultivar dependent (Camejo *et al.*, 2005; Khayat *et al.*, 1985; Adams *et al.*, 2001; De Koning, 1994), the model performance can be increased by calibration of the parameters related to the growth inhibition functions, photosynthesis functions and fruit growth period. Furthermore, instead of using a constant SLA, a seasonal dependent SLA based on Heuvelink (1996) might improve the model performance. Additionally, the estimation of the vegetative growth period might be improved by introducing a base temperature in the temperature sum calculation. No long term effects of extreme temperatures on crop yield were modelled, whereas in practice extreme temperatures indeed affect crop yield on the long term (Yakir *et al.*, 1986). Consequently, the simulated crop could, erroneously, totally recover from extreme temperatures. To avoid that the resulting overestimated yields affect the greenhouse design optimisation problem, the greenhouse air temperature must not go beyond these extreme temperature values.

3.7 Conclusion

In this research, a yield model that describes the effect of greenhouse climate on tomato yield was developed and validated. The ultimate aim is to use this model in a model-based method to design greenhouses for the wide variety of climate and economic conditions that can be expected around the world. A literature survey of temperature effects on tomato yield was performed and the main temperature effects were implemented in the crop yield model.

Validations results showed that the model fulfilled the three predefined requirements. Specially, the model covers the effects of indoor climate and non-optimal temperature conditions on crop yield (requirements 1 and 2). Without calibration of model parameters, the crop yield model predicted with fair accuracy the crop yield levels for four temperature regimes. In more detail, the tomato yield was simulated accurately for both near-optimal and non-optimal temperature conditions in respectively The Netherlands and Southern Spain, given the varying light levels and CO₂ concentrations. In addition, the adverse effects of extremely low as well as high mean temperatures on tomato yield and moment of first fruit harvest was simulated with fair accuracy. The simulated yield response to extreme diurnal temperature oscillations were in agreement with literature values. Since the presented model consisted of a set of differential equations with continuous differentiable right-hand sides, requirement 3 was fulfilled as well. All model equations are presented in this chapter and in the detailed model description to assure that our colleagues are able to implement and reproduce our findings.

Given these results, obtained for a broad range of temperature conditions, the model is considered to be sufficiently accurate to be used for developing a model-based greenhouse design method. Therefore, the presented model will be integrated in the design method with the aim to design the best greenhouse design for local climate and economic conditions.

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3.8 Nomenclature

States

<i>C</i>	Carbohydrate amount	mg {CH ₂ O} m ⁻²
<i>DM</i>	Dry matter	mg {DM} m ⁻²
<i>N</i>	Number	fruits m ⁻²
<i>T</i>	Temperature	°C

Semi-state

<i>LAI</i>	Leaf Area Index	m ² {leaf} m ⁻²
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Flow

<i>MC</i>	Carbohydrate mass flow	mg {CH ₂ O} m ⁻² s ⁻¹
<i>MN</i>	Number flow	fruits m ⁻² s ⁻¹

Subscripts

<i>24</i>	Mean of 24 hour
<i>Air</i>	Air
<i>Buf</i>	The carbon buffer
<i>Can</i>	Canopy
<i>End</i>	End of period
<i>Fruit</i>	Fruit
<i>Har</i>	Harvest
<i>Inst</i>	Instantaneous temperature effect
<i>j</i>	Fruit development stage
<i>Leaf</i>	Leaves
<i>Start</i>	Start of period
<i>Stem</i>	Stem and roots

Superscripts

<i>Max</i>	Maximum
<i>Min</i>	Minimum
<i>Sum</i>	Summation

Chapter 4

Sensitivity analysis of a combined greenhouse climate-crop yield model

The contents of this chapter have been submitted to Biosystems Engineering as a paper entitled: *A methodology for model-based greenhouse design: Part 3, Sensitivity analysis of a combined greenhouse climate-crop yield model.*

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4.1 Abstract

Greenhouse design is an optimisation problem that could be solved by a model-based greenhouse design method. Since the number of optimisation factors is very large, the objective of this research was to identify those parameters that most strongly influence a greenhouse design. For that purpose a sensitivity analysis was applied to a combined greenhouse climate crop yield model of tomato. The analysis was performed for a low-tech greenhouse in Almeria, Spain and a high-tech greenhouse in Texas, USA. Simulations indicated that the model produced realistic data of the indoor climate and crop yield. Single variate sensitivity results showed that outdoor climate has the strongest impact on the performance of the greenhouse system, followed by the greenhouse design parameters and the greenhouse climate set-points. The selection of a proper greenhouse location is thus of utmost importance. Concerning the design parameters, PAR remains the main limiting factor for greenhouse production systems. To increase crop yield, structures with a higher PAR transmission and a NIR selective whitewash must be used. Furthermore, results indicated whether sufficient climate control capacities were installed and which greenhouse design parameters can be adjusted to save resources. In addition, clear seasonal patterns in the model sensitivity suggested the need of adjustable cover parameters. The multi-variate sensitivity analysis revealed strong joint effects of the PAR transmission and temperature set-point for ventilation on crop yield. The presented SA techniques were thus able to quantify the single, combined and seasonal impact of parameters on the harvest rate, resource consumption and indoor climate.

4.2 Introduction

Optimal design of protected cultivation systems for the wide variety of conditions that exist around the world can be addressed as a multi-factorial optimisation problem (Van Henten *et al.*, 2006) that relies on a quantitative trade-off between economic return of the crop and the costs associated with construction, maintenance and operation of the greenhouse facility. As the number of factors involved in this design optimisation problem is very large, it is beneficial to identify those parameters that most strongly influence the economic trade-off and consequently the greenhouse design. A model sensitivity analysis (SA) is an appropriate technique for that purpose.

In horticultural science, several researchers applied a sensitivity analysis to greenhouse climate models and crop yield models (Nijskens *et al.* (1991), Chalabi & Bailey (1991), Nava *et al.* (1998), Cooman & Schrevens (2007), Van Henten & Van Straten (1994), Van Henten (2003)). However, none of them analyzed a combined greenhouse climate and crop yield model and none of them performed the analysis specifically in view of greenhouse design. Therefore, the goal of this study was to address both these topics in an integral fashion using sensitivity analysis techniques.

Some preliminary studies already gave directions for investigation. Vanthoor *et al.* (2008b) revealed that the sensitivity of tomato yield to a single greenhouse design parameter depends on the absolute values of the other parameters. Additionally, it was found that the sensitivity of the crop yield with respect to the cover design parameters changed over time. In another paper Vanthoor *et al.* (2008a) showed that the design and climate management are mutually dependent. Based on these preliminary findings, in this study it was decided to analyse the sensitivity of some key performance indicators to variations in the input parameters i.e. design parameters, the outdoor climate and the indoor climate setpoints. Attention was paid to seasonal effects in the sensitivity. Additionally, further to a single variate parameter sensitivity analysis as commonly implemented in various studies, in this study, also a multi-variate analysis was implemented to identify the impact of joint variations in input parameters.

The chapter is organized as follows. Firstly, the greenhouse climate-crop yield model to be used for greenhouse design is presented briefly and key performance indicators are identified. Secondly, two SA techniques are described: a single-variate analysis that determines local sensitivities to indicate relevant input parameters at an individual basis and a multi-variate analysis to reveal the combined effect of two input parameters. Thirdly, to

show how the results of the SA depend on greenhouse design and climate conditions, the SA was performed for two different greenhouse designs used under different climate conditions: a low-tech greenhouse in Almeria, Spain and a high-tech greenhouse in Texas, USA. Results of these two cases will be presented and discussed.

4.3 Materials and methods

4.3.1 Model description and analysed input parameters and model outputs

A model that describes tomato yield as a function of greenhouse climate (see chapter 3) was embedded into a model that describes greenhouse climate and resource consumption as a function of outdoor climate and greenhouse design parameters (see chapter 2).

The combined model consists of a set of ordinary differential equations:

$$\dot{X} = f(X, U, D, P, t) \quad [-] \quad (4.1)$$

where X is the state vector containing the indoor climate variables, the crop variables and resource consumption variables, \dot{X} denotes the derivatives of the states to time, U is the climate set-point vector, D is the outdoor climate vector, P is the model parameter vector including the design parameter vector P_d , and t (s) is the time.

To focus the sensitivity analysis, key performance indicators were identified for greenhouse design and operation. These indicators were the crop yield and the consumption of energy, water and carbon dioxide. In this research, the impact of various parameters on these performance indicators was determined (Fig. 4.1). Results obtained will give directions for greenhouse design, since ultimately, in greenhouse design, these performance indicators will be combined into a cost criterion to be optimised. This cost criterion reads:

$$\max_{P_d} J(X, U, D, P, t) = -Investments + \int_{t_0}^{t_f} q_{Yield} \dot{Yield} - q_E \dot{E} - q_W \dot{W} - q_{CO_2} \dot{CO_2} dt \quad [€ m^{-2}] \quad (4.2)$$

where $Investments$ (€ m⁻²) are the costs related to greenhouse design investments, t_0 (s) and t_f (s) are the start and the end, respectively, of the simulation period, q is the price coefficient of the associated cost aspect, $Yield$ (kg m⁻²) is the cumulative crop yield, W is the water consumption (kg m⁻²) needed for canopy transpiration, CO_2 is the CO₂ consumption (mg m⁻²) and E is the energy consumption (W m⁻²). The variables $Yield$, W ,

CO_2 and E are a member of the set of state variables X . In this approach labour, logistics, maintenance of the greenhouse facility and fertigation, to mention a few, are not taken into account.

As indicated by Eq. (4.2) and Fig. 4.1, the greenhouse design parameters P_d , the climate set-points U and the outdoor climate variables D affect the evolution of the state variables of the greenhouse system and consequently the performance indicators mentioned above. Therefore, it was decided to analyse, not only, the impact of P_d , U and D on the crop yield and consumption of energy, water and CO_2 , but also their impact on the intermediate greenhouse state variables influencing these performance indicators, i.e. the canopy temperature (T_{Can}), greenhouse air temperature (T_{Air}), CO_2 concentration of the air (CO_{2Air}) and the vapour pressure of the air (VP_{Air}).

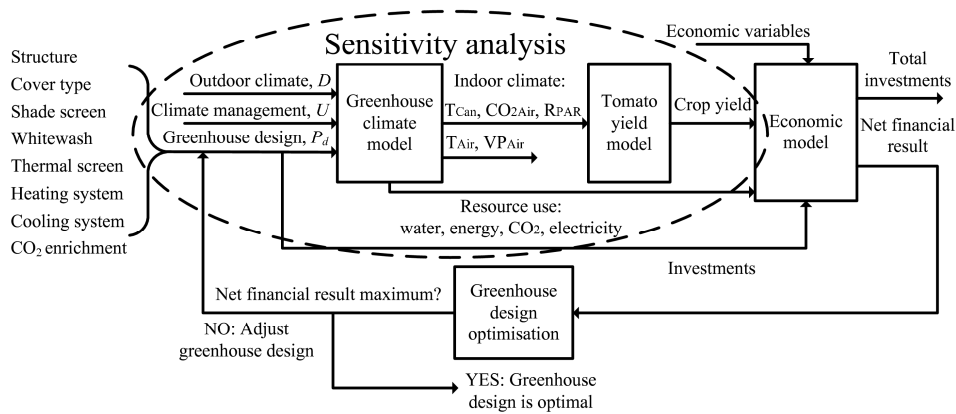


Fig. 4.1 An overview of the model-based greenhouse design method. In this study, the sensitivity of the model outputs, i.e. indoor climate, resource consumption and yield to the input parameters i.e. outdoor climate, climate management and greenhouse design is determined.

4.3.2 Sensitivity analysis techniques

The impact of a parameter on model output was determined using a single-variate analysis as described in section 4.3.2.1. Using this method the mean impact and the time dependent impact of the parameters could be revealed. Section 4.3.2.2 describes a multi-variate analysis to assess the joint impact of two greenhouse parameters.

4.3.2.1 A single-variate sensitivity analysis

In this research, a normalized relative sensitivity measure based on Chalabi and Bailey (1991) was used. This measure is defined in discrete time form as:

$$S_z^X(t_k) = \frac{X_{z_{Nom} + \Delta z}(t_k) - X_{z_{Nom}}(t_k)}{\Delta z} \frac{z_{Nom}}{\bar{X}_{z_{Nom}}}$$

$$t_k = k \cdot \Delta t; k = 0, 1, \dots, N \text{ and } N = (t_f - t_0) / \Delta t \quad [-] \quad (4.3)$$

where S_z^X is the normalised relative sensitivity of state variable X to input parameter z , t_k (s) is the time, z_{Nom} is the nominal input parameter value, Δz is the input parameter deviation, $X_{z_{Nom} + \Delta z}$ is the state value at input parameter deviation, $X_{z_{Nom}}$ is the state value after the nominal input parameter value, and $\bar{X}_{z_{Nom}}$ is the mean value of the state evaluated over the whole simulation horizon, Δt (s) is the simulation output interval, N is the total number of time instants at which the sensitivity is determined. A relative sensitivity measure is preferred over an absolute measure, to compensate for the large differences in scale size of the various input parameters and model outputs. The relative sensitivity of the model output can be interpreted as the relative increase of the model output at time instant t_k , with respect to its mean value evaluated over the whole simulation horizon, expressed in %, caused by an increase of 1% of the nominal value of the associated input parameter.

Additional to the impact of the parameters on the states, the impact of the parameters on the time derivatives of the states were determined through a modification of Eq. (4.3):

$$S_z^{\dot{X}}(t_k) = \frac{\dot{X}_{z_{Nom} + \Delta z}(t_k) - \dot{X}_{z_{Nom}}(t_k)}{\Delta z} \frac{z_{Nom}}{\bar{\dot{X}}_{z_{Nom}}} \quad [-] \quad (4.4)$$

This approach was implemented, because as indicated by Eq. (4.2), the net return of the greenhouse design is determined by the time derivatives of some state variables and not by their current absolute values. Therefore analysing the impact of the parameters on the time

derivatives of these states offers valuable information about the seasonal effects of parameters. Appendix A presented in section 4.6.1 contains some details offering support for this approach.

In Eqs. (4.3) and (4.4), input parameter z includes the greenhouse design parameters P_d , the climate set-points U and the outdoor climate variables D :

$$z = \{P_d, U, D\} \quad (4.5)$$

In the current research these parameters were deviated using a fixed perturbation factor, $h=0.10$ for all input parameters, resulting in an absolute increase of the input parameters:

$$\begin{aligned} \Delta P_d &= h \cdot P_{d_Nom} \\ \Delta U &= h \cdot U_{Nom} \\ \Delta D &= h \cdot \overline{D_{Nom}} \end{aligned} \quad (4.6)$$

Since time invariant deviations of input parameters were preferred, the outdoor climate variables, D , were deviated with the average of the absolute values of the outdoor climate variables. Since global radiation is always zero during night time, radiation was only deviated during the day time period. To determine the relative sensitivities, the model was simulated once with the nominal input parameters and thereafter each selected input parameter was deviated with a perturbation factor h and the model was simulated again. The resulting evolution of the states and their time derivatives were used to calculate the sensitivity measures of Eqs. (4.3) and (4.4).

In this study, time invariant scaling factors $\frac{z_{Nom}}{\bar{X}_{z_{Nom}}}$ and $\frac{z_{Nom}}{\dot{\bar{X}}_{z_{Nom}}}$ were used in Eqs.

(4.3) and (4.4) in stead of time variant scaling factors as was done by Chalabi and Bailey (1991) and Van Henten (2003). Essentially, this was done to avoid the situation that the relative sensitivity approaches infinity when a state value approaches zero, which would make the interpretation of the relative sensitivity ambiguous. The reason for the large relative sensitivity might be caused by a high impact of the associated parameter or by a very small value of the state or its derivative. Additionally, this was done to assure that the mean relative sensitivity of the time derivative of a state equals the relative sensitivity of the state value at the end of the production period (see Appendix B in section 4.6.2), a property that was used during the interpretation of the results. To simplify the interpretation of the results, the relative sensitivity measures of Eqs. (4.3) and (4.4) were modified. Due to similarity between these measures, only the modifications of Eq. (4.3) will be described.

For first analysis of the sensitivity results, a mean relative sensitivity was introduced:

$$\bar{S}_Z^X = \frac{1}{N+1} \sum_{k=0}^{k=N} S_Z^X(t_k) \quad [-] \quad (4.7)$$

As clarified in section 4.6.2, the mean relative sensitivity of the time derivative of a state equals the relative sensitivity of the similar state at time instant t_f . A mean relative sensitivity of the energy consumption rate of 2 indicates that the total energy consumption for the total simulation horizon increases with 2% when the input parameter increases with 1%. This property is only valid if the relative sensitivity equations contain time invariant scaling factors as in Eqs. (4.3) and (4.4).

Clearly, a mean relative sensitivity measure as in Eq. (4.7) might result in small values around zero although considerable positive and negative variations in sensitivity might exist in the time period considered. Therefore, Eq. (4.7) was modified to an absolute relative sensitivity measure:

$$|S_Z^X| = \frac{1}{N+1} \sum_{k=0}^{k=N} |S_Z^X(t_k)| \quad [-] \quad (4.8)$$

As demonstrated by Chalabi and Bailey (1991) and Van Henten and Van Straten (1994), the relative sensitivity of the model outputs may fluctuate strongly on a daily base. These variations are of interest in this analysis. To make the seasonal impact readily visible Eqs. (4.3) and (4.4) were smoothed:

$$S_Z^{X,Smooth}(t_k) = \frac{1}{2N_{Smooth} + 1} \sum_{j=-N_{Smooth}}^{j=N_{Smooth}} S_Z^X(t_j), \quad t_j = t_k + j \cdot \Delta t, \quad [-] \quad (4.9)$$

$$j = -N_{Smooth}, -N_{Smooth} + 1, \dots, N_{Smooth}$$

where N_{Smooth} is the integer part of:

$$N_{Smooth} = t_{Smooth} / 2\Delta t \quad [-] \quad (4.10)$$

where t_{Smooth} (s) is the smoothing period.

4.3.2.2 A multi-variate sensitivity analysis

A multi-variate sensitivity analysis was used to identify the combined effect of input parameters on model output. In this study, “a combined effect” means that a simultaneous increase of two parameters has a different impact on model output than the sum of their individual impacts on model output. For this purpose, the multi-variate sensitivity analysis according to Abusam *et al.* (2001) was implemented. Essentially, this approach approximates the sensitivity response surface with a linear regression meta model. Potentially, the parameters of this meta model reveal cross correlations in the parameter sensitivity. The approach consists of the following steps.

Firstly, model output was generated for a range of values of the selected set of input parameters. To limit the number of simulations needed to determine the regression coefficients of the linear regression model, a normalised second-order composite design around the nominal parameter vector was used (Box & Draper, 1987). For 2 input parameters, this design requires 9 simulation runs ($2^n + 2n + 1$ with n the number of evaluated input parameters).

Then, the following linear regression meta-model was fitted on the simulated model output and the associated input parameters values:

$$y(t_f) = b_0 + b_1 p_1 + b_2 p_2 + b_{11} p_1^2 + b_{22} p_2^2 + b_{12} p_1 p_2 \quad [-] \quad (4.11)$$

where $y(t_f)$ is the model output at the end of the simulation horizon t_f , b are the regression coefficients, p_1 and p_2 are the scaled parameters for the input parameters as listed in Table 4.1. To determine the regression coefficients, Eq. (4.11) was reformulated in vector-matrix notation as:

$$Y = C\theta, \quad Y = \begin{pmatrix} y_1 \\ y_2 \\ \vdots \\ y_n \end{pmatrix}, \quad C = \begin{pmatrix} 1 & p_{1,1} & p_{2,1} & p_{1,1}^2 & p_{2,1}^2 & (p_1 p_2)_1 \\ 1 & p_{1,2} & p_{2,2} & p_{1,2}^2 & p_{2,2}^2 & (p_1 p_2)_2 \\ \vdots & \vdots & \vdots & \vdots & \vdots & \vdots \\ 1 & p_{1,n} & p_{2,n} & p_{1,n}^2 & p_{2,n}^2 & (p_1 p_2)_n \end{pmatrix}, \quad \theta = \begin{pmatrix} b_0 \\ b_1 \\ b_2 \\ b_{11} \\ b_{22} \\ b_{12} \end{pmatrix} \quad (4.12)$$

where n is the total number of simulation runs. Subsequently, the regression coefficient vector θ was estimated by:

$$\hat{\theta} = (C^T C)^{-1} C^T Y \quad (4.13)$$

The significance ($p < 0.10$) of the regression coefficients was calculated with the T-test as described by Montgomery and Peck (1992). Finally, the significant regression coefficients of this meta-model were analysed because they contain information about the impact of both single and combined input parameters on the model output. For example, a significant regression coefficient b_{12} indicates a combined effect of the scaled input parameters p_1 and p_2 on model output.

Table 4.1 The original parameter levels and the normalised parameter values for the combined sensitivity of the final crop yield towards some model inputs for the greenhouse in Almeria and Texas. The coded levels accompanying the original parameter values were based on the normalised second-order composite design around the nominal parameter vector of Box and Draper (1987).

Coded level	Original parameter values					Normalised parameter values
	$x = -\sqrt{2}$	$x = -1$	$x = 0$	$x = 1$	$x = \sqrt{2}$	
τ_{RfPAR}	0.3272	0.41	0.61	0.81	0.8928	$p = (\tau_{RfPAR} - 0.61)/0.2$
τ_{RfNIR}	0.3272	0.41	0.61	0.81	0.8928	$p = (\tau_{RfNIR} - 0.61)/0.2$
τ_{RfFIR}	0.1172	0.2	0.4	0.6	0.6828	$p = (\tau_{RfFIR} - 0.61)/0.2$
CO_{2Out}	299.3	320	370	420	440.7	$p = (CO_{2Out} - 370)/50$
T_{Air_VentOn}	20.17	21	23	25	25.83	$p = (T_{Air_VentOn} - 23)/2$
<i>Texas</i>						
τ_{RfPAR}	0.7793	0.8	0.85	0.9	0.9207	$p = (\tau_{RfPAR} - 0.85)/0.05$
CO_{2Air_ExtOn}	517.16	600	800	1000	1082.84	$p = (CO_{2Air_ExtOn} - 800)/200$
T_{Air_VentOn}	20.17	21	23	25	25.83	$p = (T_{Air_VentOn} - 23)/2$

4.3.3 Two case studies: Almeria, Spain and Texas, USA

To show how the sensitivity results depend on greenhouse design and climate conditions, the SA was performed for two different greenhouse designs under different climate conditions: a low-tech greenhouse in Almeria, Spain and a high-tech greenhouse in Texas, USA. These different designs were caused by local climate conditions and represent the current state of greenhouse production systems in Almeria and Texas. In this section the assumptions concerning the sensitivity analysis study are presented. This includes the greenhouse parameters, outdoor climate, greenhouse climate management and the crop conditions as well as the parameters studied in the sensitivity analysis.

4.3.3.1 Greenhouse design in Almeria and Texas

The low-tech greenhouse was located in Almeria, Spain (36°47'N, 2°43'W and 150 m above sea level). The 3-span multi-tunnel greenhouse was covered with a PE foil. Sole means for greenhouse climate management were roof and side ventilators and seasonal whitewash. The high-tech greenhouse was located in Texas, USA (30°21'N, 104°00'W and 1470 m a.s.l.). The Venlo-type greenhouse was covered with a single glass layer and was equipped with pipe heating, CO₂ injection, roof ventilation and with a thermal screen. Details of the two greenhouse designs are presented in Appendix C (see section 4.6.3).

4.3.3.2 Outdoor climate, greenhouse climate management and crop conditions

Details of the outdoor climate, the greenhouse climate management and the crop conditions for both greenhouses are presented in Table 4.2. For both locations the same growing period (August 1st to July 1st) and climate set-points were used to assure that differences between sensitivity results of both locations were only caused by greenhouse design and outdoor climate. However, the seasonal whitewash was applied earlier in Almeria than in Texas based on real data. The climate control strategy is described in Fig. 4.2.

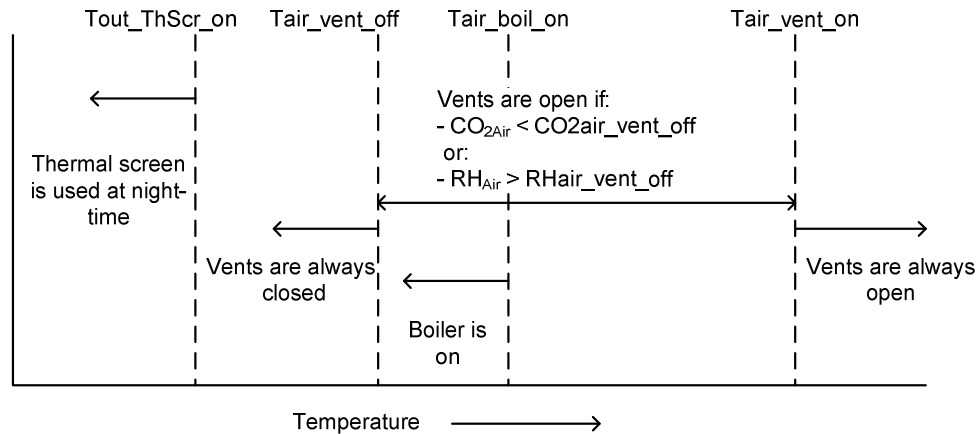


Fig. 4.2 The climate control strategy based upon climate set-points for both greenhouses. CO₂ was supplied whenever the CO₂ concentration in the greenhouse was below the CO₂ concentration set-point for enrichment. Values of the climate set-points are listed in Table 4.2.

Table 4.2 Overview of the average outdoor climate, the greenhouse climate management and the crop conditions for the greenhouses in Almeria and Texas. The last column presents if a Sensitivity Analysis was performed on the presented measures. The values between the brackets represent the standard deviation. The dots indicate that the accompanying climate control techniques were not used in the greenhouse.

	Almeria, Spain	Texas, USA	Sensitivity Analysis
<i>Outdoor climate (D)</i>			
I_{glob_sum} (MJ m ⁻² day ⁻¹)	17.3 (7.1)	17.8 (6.0)	+
T_{out} (°C)	17.6 (5.3)	15.7 (9.4)	+
VP_{out} (kPa)	1.3 (0.4)	1.0 (0.6)	+
RH_{out} (%)	65.4 (17.7)	52.6 (25.6)	+
T_{sky} (°C)	-0.4 (7.6)	-4.7 (12.6)	+
T_{SoOut} (°C)	18.0 (2.6)	16.2 (3.7)	+
v_{wind} (m s ⁻¹)	3.0 (2.3)	2.9 (2.1)	+
<i>Greenhouse climate management (U)</i>			
<i>Whitewash</i>	August 1 st – September 15 th April 16 th – July 1 st	August 1 st – September 15 th May 16 th – July 1 st	-
$T_{air_vent_on}$	23	23	+
$T_{air_vent_off}$	17	17	+
$RH_{air_vent_on}$	90	90	+
$CO_{2air_vent_off}$	200	200	+
$T_{air_boil_on}$	*	18	+
$T_{out_ThScr_on}$	*	10	+
$CO_{2air_ExtCO2_on}$	*	800	+
<i>Crop conditions</i>			
LAI_start	0.3	0.3	-
LAI_max	2.5	2.5	-
Start growing period	August 1 st 2002	August 1 st 2007	-
End growing period	July 1 st 2003	July 1 st 2008	-

4.3.3.3 Simulation of the model

The model was simulated by solving the differential equations with a variable time step ODE solver of Matlab 7.1[®]. The output interval of the simulation Δt , was 3600 s and the smoothing period, t_{Smooth} , was chosen pragmatically to be 7 days which equals $6.0 \cdot 10^5$ s.

4.3.3.4 Sensitivity analysis

Both cases were investigated with the following three step procedure. First the model was simulated with the outdoor climate data. Not intended to be an in depth validation, evaluation of the produced output offered valuable insight into the ability of the model to produce at least realistic output. Secondly, a single-variate sensitivity analysis was performed. Followed, thirdly, with the multi-variate sensitivity analysis.

The parameters evaluated in the single-variate sensitivity analysis are listed in the last column of Table 4.2 and in the last column of the table presented in Appendix C (see section 4.6.3). For some greenhouse design parameters no sensitivity analysis was performed since they were related to other greenhouse design parameters. Specifically, since the sum of the transmission, reflection and absorption coefficients must always be one, the following assumptions for all the cover layers, i.e. the roof, whitewash and thermal screen, were made: a) when analyzing the impact of the photosynthetically active radiation (PAR) and the near infrared radiation (NIR) transmission coefficient, the absorption coefficient for NIR and PAR remained the same; consequently a change in the PAR and NIR transmission coefficient resulted only in a change of the PAR and NIR reflection coefficient, b) when analyzing the impact of the far infrared radiation (FIR) emission coefficient, the FIR transmission coefficient remained the same, and c) when analyzing the impact of the FIR transmission coefficient, the FIR emission coefficient remained the same.

For the multi-variate sensitivity analysis the ranges and normalised values of the selected parameters are presented in Table 4.1 together with the accompanying coded levels based on the composite design procedure of Box and Draper (1987). To reduce the number of potential parameter combinations, only a limited set of parameters was selected for analysis. Only those combinations were selected for which a combined effect on final crop yield was expected. Solar radiation, temperature and CO₂ concentration mutually influence the photosynthesis rate. Since a combined impact of these climate variables on crop yield was expected, the PAR transmission of the cover, temperature set-point for ventilation, the outdoor CO₂-concentration in Almeria and the CO₂ concentration set-point for CO₂ enrichment in Texas were selected as input parameters. Cooman and Schrevens (2007) revealed that solar radiation intensity and air temperature had a combined effect on fruit

weight. Therefore, for the greenhouse in Almeria, the input parameters influencing the solar radiation and air temperature were selected, namely: the PAR, NIR and FIR transmission of the greenhouse cover.

4.4 Results and discussion

In section 3.1 results are presented of the nominal model simulations for both cases. Then, results are presented of the single and multi-variate sensitivity analysis of the model in sections 3.2 to 3.6. Results are discussed in view of information available from literature and implications for greenhouse design are presented. In section 4.4.7 the applied sensitivity analysis is discussed.

4.4.1 Nominal simulation results

Obviously, the value of a sensitivity analysis depends on the quality of the model to which the analysis is applied. For a detailed description and validation of the greenhouse climate model and crop yield model, see chapter 2 and 3 respectively. Additionally, in this research we checked that the order of magnitude of the simulated crop yield (Fig. 4.3a, b) and the indoor climate (Fig. 4.3c-f) of both greenhouses were representative for the conditions observed in Almeria, Spain and Texas, USA.

As might be expected, the final crop yield in the high-tech greenhouse in Texas was considerably higher than in the low-tech greenhouse in Almeria which had a much more growth-limiting climate management (Fig. 4.3c-e). Specifically, the indoor temperature, global radiation and CO₂ concentration were more favourable for crop growth in the high-tech greenhouse than in the low-tech greenhouse. The low harvest rate in winter in Almeria was caused by the negative effect of sub-optimal mean temperatures on simulated tomato yield and low light levels as described in chapter 3.

The final simulated tomato yield in Texas (68 kg fresh weight per m²) was in agreement with the grower's observation. The final simulated tomato yield in Almeria (24 kg fresh weight per m²) overestimated slightly the measured production of 18.5 – 20.8 kg m⁻² obtained in a 'raspa y amagado' greenhouse under Southern Spanish conditions (Callejón-Ferre *et al.*, 2009). This overestimation was caused by the better ventilation performance of the simulated greenhouse compared to the limited ventilation of a 'raspa y amagado' greenhouse and because the simulation considered a longer growing period than used in Spanish practice.

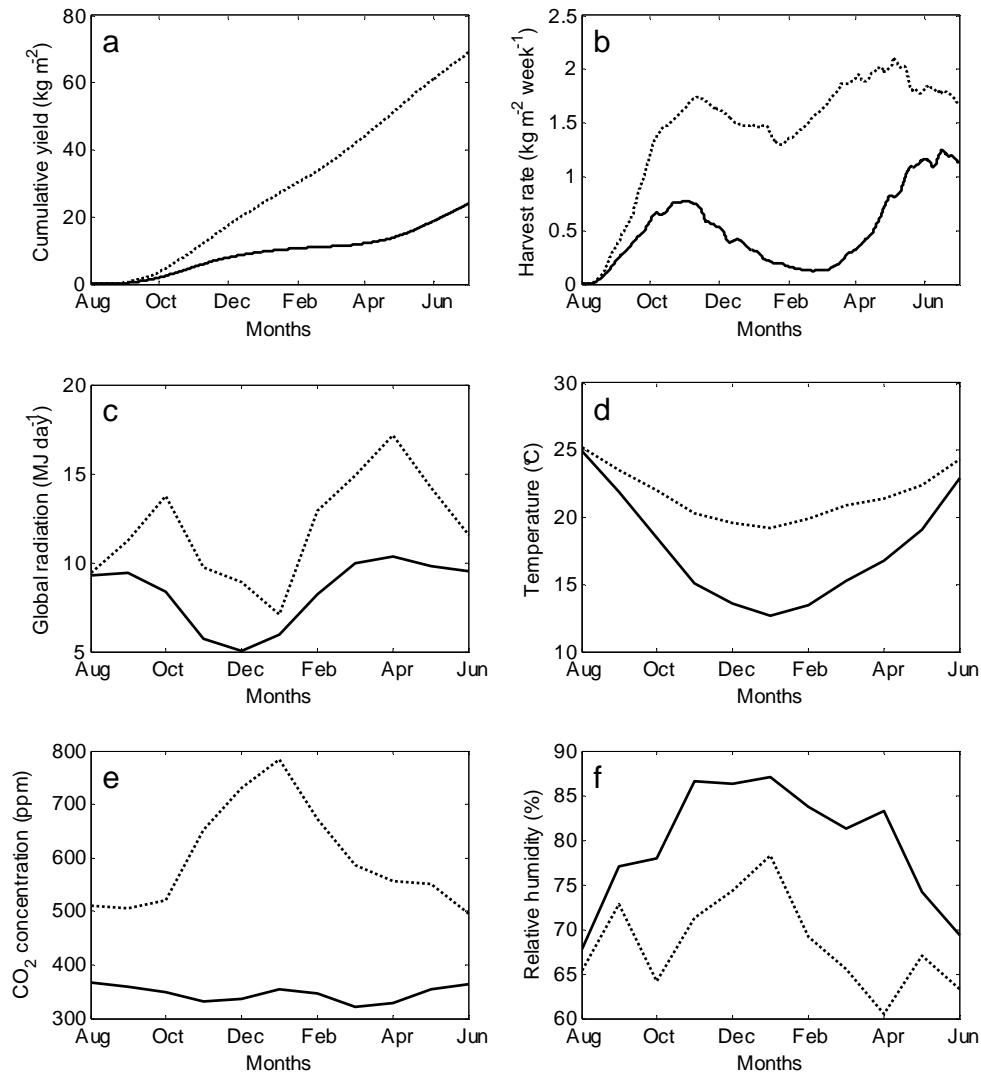


Fig. 4.3 Simulated crop yield (a), harvest rate (b), and the simulated monthly mean indoor values of the global indoor radiation (c), greenhouse air temperature (d), CO_2 concentration during day period (e) and the relative humidity (f) in the low-tech greenhouse in Spain (solid line) and in the high-tech greenhouse in Texas, USA (dotted line) from August 1st to July 1st.

4.4.2 Impact of greenhouse design parameters

The calculated mean relative sensitivities were ordered in Table 4.3 – Table 4.8 based on their impact on harvest rate. These tables present an enormous amount of relevant information about the impact of parameters on greenhouse performance. In this chapter only the most relevant findings will be discussed. For both greenhouses, the spectral properties of the greenhouse roof and the seasonal whitewash had the highest impact on the harvest rate (Table 4.3 and Table 4.4), even at 2 locations with relatively high outside global radiation levels.

Table 4.3 The mean relative sensitivity of the harvest rate, water use rate and indoor climate variables towards the greenhouse design parameters, P_{a} , with the highest impact on harvest rate for the low-tech greenhouse in Almeria. The "0" indicates that the mean relative sensitivity was lower than 0.005. Only the 10 design parameters with the highest impact on harvest rate are presented. Note that the presented mean relative sensitivities of the harvest rate, energy use, water use and CO_2 use, equal the relative sensitivities of the states at the end of the production period.

	Harvest rate	Water use	T_{Can}	T_{Air}	$\text{CO}_{2\text{Air}}$	VP_{Air}
τ_{RfPAR}	0.77	0.44	0.07	0.04	0.02	0.03
$\tau_{\text{ShScrPerPAR}}$	0.27	0.15	0.02	0.01	0.01	0.01
τ_{RfFIR}	-0.24	-0.18	-0.06	-0.04	-0.01	-0.04
τ_{RfNIR}	0.1	0.19	0.06	0.04	0.02	0.03
ρ_{FlrPAR}	0.09	0.05	0	0	0	0
ϵ_{RfFIR}	-0.08	-0.05	-0.02	-0.02	-0.01	-0.02
$\rho_{\text{ShScrPerPAR}}$	0.06	0.02	-0.01	0	0	0
$\eta_{\text{Glob_Air}}$	-0.04	-0.02	0.	0	0	0
$\tau_{\text{ShScrPerNIR}}$	-0.03	0.03	0.02	0.01	0.01	0.01
ρ_{FlrNIR}	-0.03	0	-0.02	-0.01	-0.01	-0.01

Particularly, the PAR transmission of the roof and the whitewash were the most important greenhouse design parameter to improve the harvest rate: in Almeria a year-round increase of the PAR transmission of the roof with 1% resulted in a harvest rate increase of 0.77% whereas in Texas the same PAR transmission increase resulted in a harvest rate increase of 0.34%. Such a positive impact of PAR on crop yield was also described by Marcelis *et al.*

(2006). However, increasing the PAR transmission might also result in a higher fruit temperature which then could negatively affect the fruit quality. This quality aspect was not included in the model used in this study.

Table 4.4 The mean relative sensitivity of the harvest rate, resource use rate and indoor climate variables towards the greenhouse design parameters, P_d , with the highest impact on harvest rate for the high-tech greenhouse in Texas. Only the 10 design parameters with the highest impact on harvest rate are presented.

	Harvest rate	Energy use	Water use	CO ₂ use	T_{Can}	T_{Air}	CO ₂ Air	VP _{Air}
τ_{RfPAR}	0.34	-0.14	0.24	0.09	0.07	0.03	0.12	0
$\tau_{ShScrPerPAR}$	0.07	-0.02	0.04	0.01	0.02	0.01	0.03	0.01
η_{Glob_Air}	-0.06	0.01	-0.01	0.01	-0.01	0	-0.03	-0.01
ϕ_{ExtCO_2}	0.06	0	0	0.86	0	0	0.1	0
ρ_{FIRPAR}	0.05	0.04	0.02	0.01	0	0	0.01	0
τ_{RfNIR}	-0.05	-0.16	0.11	0.04	0.04	0.02	0	0
$h_{Elevation}$	-0.02	-0.05	-0.1	0	0.02	0.01	0	-0.03
$\tau_{ShScrPerNIR}$	-0.02	-0.03	0	0	0.02	0.01	0	0
\mathcal{E}_{RfFIR}	0.01	0.58	-0.06	-0.04	-0.05	-0.03	-0.01	-0.08
$\mathcal{E}_{ShScrPerFIR}$	0.01	0.06	0.01	-0.01	-0.01	-0.01	0	-0.01

Reasons for the higher impact of the PAR transmission on harvest rate in Almeria were : 1) the indoor global radiation of the greenhouse in Almeria was lower than in Texas (Fig. 4.3c) and due to the non-linear response of the photosynthesis to PAR, the increase of the PAR transmission at the lower PAR levels in Almeria affected the photosynthesis rate relatively more than at the higher PAR levels in Texas and 2) in Almeria an increase of PAR transmission favoured both the growing factors light and temperature whereas in Texas an increase of PAR favoured only the amount of growing light because heating already ensured the desired temperature.

Besides cover materials and whitewash with a higher PAR transmission also other greenhouse design parameters might be adjusted to improve the harvest rate. In the low-tech greenhouse both an increase of the transmission and emission coefficient for FIR decreased the harvest rate considerably (-0.24 and -0.08, respectively). This was caused by

a lower night time temperature. This result was in agreement with Nijskens *et al.* (1991) who demonstrated that in an unheated greenhouse these parameters had the largest impact on greenhouse air temperature.

Furthermore, the potential advantage of a NIR-selective whitewash over a conventional whitewash (with equal transmission values for PAR and NIR) was clearly demonstrated. At both locations, an increase of the PAR transmission coefficient of the whitewash favoured harvest rate (0.27 in Almeria and 0.07 in Texas) whereas a similar decrease of the NIR transmission coefficient of the whitewash favoured harvest rate (-0.03 in Almeria and -0.02 in Texas) as well. Therefore, the same reduction of solar radiation in the greenhouse can be achieved by means of a NIR-selective whitewash and a conventional whitewash whilst additionally, the NIR-selective whitewash would increase crop yield. This was confirmed by López-Marín *et al.* (2008) who observed under a NIR-selective whitewash a higher sweet pepper yield than under a conventional whitewash in Southern Spain from half May to August.

Design parameters that decrease PAR transmissivity decreased in all cases the harvest rate. For instance, the harvest rate decreased with increasing radiation intercepting construction elements demonstrated by the associated mean relative sensitivity of -0.04 under low-tech and -0.06 under high-tech conditions. This result indicates the need for “light” structures even in places where light is not perceived to be limiting production. Furthermore, an increase of the PAR reflection coefficient of the floor favoured the harvest rate (0.09 in the low-tech and 0.05 in the high-tech) considerably. In contrast to this result, Lorenzo *et al.* (2005) revealed that increasing the PAR and NIR reflection coefficient of the floor by using mulching decreased the cucumber yield in an unheated plastic greenhouse in Almeria. Specifically, they started their experiment in a relative cold period (autumn and spring) which resulted, due to less heat storage in the soil, in lower temperatures. These low temperatures slowed down plant development and LAI development resulting in lower crop yield. With respect to this mechanism, the simulated crop yield was affected oppositely because lower temperatures favoured crop yield under high temperature conditions which occurred at the beginning of the growth period (August).

The sensitivity analysis gave clear indications about whether or not sufficient climate control systems with sufficient capacity had been installed. Enough boiler capacity was installed because an increase of the boiler capacity did not benefit harvest rate (0, not shown). However, an increase of the CO₂ enrichment capacity did favour the harvest rate (0.06). Yet, increasing the CO₂ enrichment capacity would simultaneously increase the CO₂ consumption (0.86). This indicates an economic trade-off between extra yield and extra

resource use costs. This result clearly supports the need for multi-factorial optimisation.

Greenhouse design parameters that are candidates for reduction of resource use without compromising the harvest rate were clearly indicated in the analysis of the high-tech greenhouse. For example, energy might be saved by a variety of options including decreasing the FIR emission coefficient of the roof (0.58), increasing the NIR transmission of the roof (-0.16), increasing the gutter height (-0.08, not presented), decreasing the gutter to ridge height (0.18, not presented), decreasing the NIR reflection coefficient of the greenhouse floor (0.13, not presented) and decreasing the boiler capacity (0.20, not presented). The processes behind some of these energy saving measures are explained briefly here.

The large impact of the FIR emission coefficient of the roof on energy use was in agreement with results reported by Nijskens *et al.* (1991). Particularly, decreasing the FIR emission coefficient resulted in an increase of the reflection coefficient for FIR which in turn decreased the radiation emitted to the sky resulting in a lower heating demand.

Increasing the gutter height induced a more stable indoor climate, due to a larger buffer capacity of the greenhouse, and therefore less ventilation for humidity control was needed resulting in less energy consumption. Similar observations have been reported by Raya *et al.* (2006) for Canarian screenhouses. In contrast, increasing the height from gutter to ridge results in a higher convective heat loss and more energy consumption due to a larger surface of the greenhouse cover. This is in agreement with the results of Chalabi and Bailey (1991) who demonstrated that an increase of the glass to ground relative surface indeed decreased indoor air temperature due to a higher heat loss. The large difference of the impact of both gutter and gutter to ridge height on energy consumption was caused by the ratio between the greenhouse volume (V) and the greenhouse cover area (A). An increase of the gutter height increases the ratio V/A which in turn favours the buffer effect, whereas, an increase of the height from gutter to roof decreases the ratio V/A which in turn favours the convective heat loss.

Decreasing the height from gutter to ridge in real world conditions will negatively influence the transmission of the cover and thus the harvest rate. The angular transmissivity of the cover was not modelled, and could possibly cancel out the observed positive impact of a lower gutter height on resource consumption.

Decreasing the NIR reflection coefficient of the greenhouse floor might decrease the energy consumption because it would allow more use of daily thermal storage in the soil. This is in agreement with (Nijskens *et al.*, 1991) who also demonstrated the large impact of solar absorption coefficient of the floor on energy use.

4.4.3 Impact of outdoor climate

For both greenhouses, the global radiation, the CO₂-concentration and the temperature had the largest impact on the mean harvest rate (Table 4.5 and Table 4.6). The harvest rate was positively influenced by an increase of the global radiation (1.35 in Almeria and 0.59 in Texas) and CO₂ concentration (0.62 in Almeria and 0.17 in Texas) whereas an increase of outdoor temperature favoured the harvest rate in Almeria (0.36) and decreased the harvest rate in Texas (-0.37).

Table 4.5 The mean relative sensitivity of the harvest rate, water use rate and indoor climate variables towards the outdoor climate variables, D , for the low-tech greenhouse in Almeria.

	Harvest rate	Water use	T_{Can}	T_{Air}	CO_{2Air}	VP_{Air}
I_{glob}	1.35	0.81	0.21	0.14	-0.01	0.19
CO_{2out}	0.62	0.14	-0.01	-0.01	1.02	0.01
T_{out}	0.36	1.03	0.54	0.70	-0.09	-0.14
VP_{out}	0.22	-0.69	0.13	0.06	0.03	0.52
T_{sky}	0.10	0.05	0.04	0.03	0.02	0.03
T_{soe}	0.07	0.05	0.03	0.02	0.02	0.03
V_{speed}	0.05	0.08	0.01	0.01	0.01	-0.02

Table 4.6 The mean relative sensitivity of the harvest rate, resource use rate and indoor climate variables towards the outdoor climate variables, D , for the high-tech greenhouse in Texas.

	Harvest rate	Energy use	Water use	CO ₂ use	T_{Can}	T_{Air}	CO_{2Air}	VP_{Air}
I_{glob}	0.59	-0.68	0.48	0.29	0.15	0.08	0.14	0.06
T_{out}	-0.37	-0.54	0.15	0.30	0.18	0.24	-0.45	-0.18
CO_{2out}	0.17	0	0	-0.11	0	0	0.46	0
VP_{out}	-0.03	-0.07	-0.15	0.05	0.03	0.01	-0.02	0.22
V_{speed}	-0.02	0.04	0.04	0.04	-0.01	-0.01	-0.28	-0.06
T_{sky}	-0.02	-0.26	-0.01	0.03	0.03	0.02	-0.01	0.05
T_{soe}	-0.01	-0.15	0.01	0.01	0.01	0.01	0.01	0.01

The positive crop yield response to an increased light level was demonstrated by Marcelis *et al.* (2006) who found 0.7 to 1% yield increase for 1% light increase for fruit vegetables under temperate greenhouse climate conditions. The large impact of global radiation on harvest rate can be explained in a similar way as was stated above for cover transmissivity. The climate control of the high-tech greenhouse ensured a lower sensitivity to the outdoor climate than the low-tech greenhouse. This result is in agreement with Castilla and Montero (2008) who observed that an advantage of enhanced technology in the Mediterranean was to add security and stability to extreme outdoor conditions.

In agreement with Stanghellini *et al.* (2008), the potential of CO₂ enrichment in Mediterranean greenhouses was demonstrated because an increase of the mean indoor CO₂ concentration with 1.02 % would favour an harvest rate increase of 0.62 % in Almeria (Table 4.5). However an economic evaluation including investment costs must be carried out to confirm the true potential of CO₂ enrichment.

Additionally, in agreement with Nijsskens *et al.* (1991), the impact of outdoor climate variables on model outputs was considerable higher than the impact of design parameters on model outputs (Table 4.3-Table 4.6). This result demonstrates the importance of selecting an appropriate greenhouse location with respect to outdoor climate.

4.4.4 Impact of climate set-points

In Almeria, increasing both the relative humidity set-point for ventilation ($RH_{air_vent_on}$) and the temperature set-point above which the vents may be opened ($T_{air_vent_off}$) would increase the harvest rate (0.12 and 0.07, respectively) through their positive effect on canopy temperature at low (night) temperatures (Table 4.7). Obviously, one has to keep in mind that the possible effect of high humidity on pathologies was not modelled.

Table 4.7 The mean relative sensitivity of the harvest rate, water use rate and indoor climate variables towards the greenhouse climate set-points, U , for the low-tech greenhouse in Almeria.

	Harvest rate	Water use	T_{Can}	T_{Air}	CO_{2Air}	VP_{Air}
$RH_{air_vent_on}$	0.12	-0.13	0.08	0.07	-0.10	0.16
$T_{air_vent_off}$	0.07	-0.05	0.03	0.03	-0.04	0.06
$T_{air_vent_on}$	-0.07	-0.35	0.14	0.12	-0.11	0.44
$CO_{2air_vent_off}$	0	0	0	0	0	0

In Texas, the impact of set-points on resource use was considerably higher than on harvest rate (Table 4.8). Particularly, an increase of the heating set-point ($T_{air_boil_on}$) increased drastically energy use (2.77). An increase of the temperature set-point for ventilation ($T_{air_vent_on}$) increased harvest rate and decreased the use of all resources (-0.43 for energy, -0.32 for water and -0.71 for CO_2).

Table 4.8 The mean relative sensitivity of the harvest rate, resource use rate and indoor climate variables towards the greenhouse climate set-points, U , for the high-tech greenhouse in Texas.

	Harvest rate	Energy use	Water use	CO_2 use	T_{Can}	T_{Air}	CO_{2Air}	VP_{Air}
$T_{air_vent_on}$	0.15	-0.43	-0.32	-0.71	0.19	0.16	0.34	0.55
$T_{air_boil_on}$	-0.08	2.77	0.15	0.14	0.39	0.39	0.16	0.27
$CO_{2air_Ext}CO_{2_on}$	0.04	0	0	0.20	0	0	0.31	0
$RH_{air_vent_on}$	0	-0.07	-0.02	-0.09	0.01	0.01	0.10	0.02
$T_{out_ThScr_on}$	0	-0.20	0	0	0.01	0.01	0.01	0.03
$T_{air_vent_off}$	0	-0.02	-0.01	-0.03	0	0	0.02	0.01
$CO_{2air_vent_off}$	0	0	0	0	0	0	0	0

This demonstrates the possible advantage of a semi-closed greenhouse equipped with active cooling techniques. De Zwart (2008) found that in a semi-closed greenhouse under Dutch and Mediterranean conditions indeed less resources would be used and crop yield would increase. However, to judge if such a system will be profitable one should perform an economic evaluation for the local climate conditions and price variables.

Regarding optimal greenhouse design, the impact of climate set-points has a tremendous impact on resource use and therefore these set-points should be optimised as well because resource costs are part of the cost criterion of the greenhouse optimisation problem. As demonstrated by Vanthoor *et al.* (2008a), climate set-points affects even the optimised greenhouse design.

4.4.5 Time effect of greenhouse design parameters

The impact of the roof design parameters on harvest rate was time dependent because the mean sensitivity differed with the absolute sensitivity (Table 4.9). In addition, the upper and lower percentile values showed that the impact of these design parameters on harvest rate varied considerably over time.

Table 4.9 The mean relative sensitivity and the absolute relative sensitivity of the harvest rate in Almeria and Texas towards the PAR transmission, NIR transmission and the FIR emission coefficient of the roof. The percentile values describe the spreading of the relative sensitivity: 10% of the data is located below the presented value (<10%) or above the presented value (> 90%). The time dependent relative sensitivities related to these design parameters are shown in Fig. 4.4.

Almeria	Mean relative sensitivity	Absolute relative sensitivity	Lower percentile (< 10%) of relative sensitivity	Higher percentile (> 90%) of relative sensitivity
$\tau_{R/PAR}$	0.77	0.77	0.305	1.265
$\tau_{R/NIR}$	0.10	0.18	-0.127	0.401
$\epsilon_{R/FIR}$	-0.08	0.09	-0.221	0.000
Texas				
$\tau_{R/PAR}$	0.34	0.34	0.033	0.539
$\tau_{R/NIR}$	-0.05	0.05	-0.119	-0.002
$\epsilon_{R/FIR}$	0.01	0.02	-0.014	0.043

This time dependency is shown in more detail in Fig. 4.4, in which the smoothed relative sensitivity of the harvest rate towards these roof design parameters is presented. In Almeria, the impact of PAR transmission on the harvest rate fluctuated strongly during the growing period, with a relatively low impact in winter time. In Texas the impact of PAR transmission on the harvest rate did not decrease during winter time (Fig. 4.4).

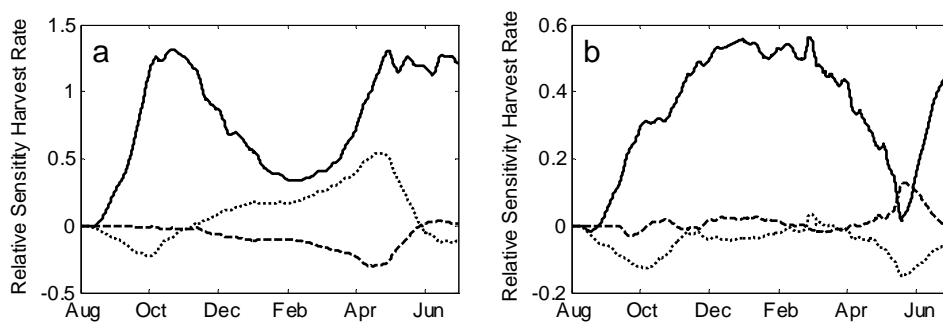


Fig. 4.4 The relative sensitivity of the harvest rate towards: the PAR transmission coefficient (solid line), NIR transmission coefficient (dotted line) and the FIR emission coefficient (dashed line) of the roof from August 1st to July 1st in Almeria (a) and Texas (b). Note that by definition the mean values of the trajectories of the relative sensitivities correspond with the mean relative sensitivities presented in Table 4.9.

The low impact of PAR transmission in Almeria during winter time seems counterintuitive because in winter the inside global radiation is very low (Fig. 4.3c) and consequently an increase of PAR inside the greenhouse would favour crop growth in winter time like in Texas. However, Fig. 4.3c demonstrates that in wintertime canopy temperature is sub-optimal with respect to crop production in an unheated greenhouse in Almeria. Consequently, due to these low temperatures the crop did not benefit efficiently an increase of PAR. This reasoning is in agreement with Marcelis *et al.* (2006) who revealed that the relative positive effect of radiation on crop yield decreases at low temperatures. In Texas, where temperature was near optimal for crop growth, the impact of PAR remained high during the winter time.

The impact of some design parameters switched between positive and negative values which indicates that selection of these design parameters is a trade-off along the production horizon (Fig. 4.4). For example, a higher NIR transmission would favour harvest rate in winter time (higher temperature) whereas it would decrease harvest rate at the beginning and end of the production period (too high temperature). This result suggests that cover materials with adjustable instead of fixed properties are needed so that for each season the best cover properties can be implemented.

4.4.6 Combined effect of two model inputs on crop yield

Combined effects of input parameters on crop yield were revealed by analysing the regression coefficients of the derived linear regression meta-model (Table 4.10). As quantified by the regression coefficients b_{12} of Eq. (4.11), results showed that crop yield was significantly affected by a combined increase of: a) the PAR and FIR transmission coefficient of the roof in Almeria (-0.83), b) the PAR transmission coefficient of the roof and the temperature set-point for ventilation (0.43 in Almeria and -0.06 in Texas) and c) the temperature set-point for ventilation and CO₂ concentration set-point for CO₂ enrichment in Texas (0.27). For both greenhouses no combined effect of the PAR transmission and CO₂ concentration on crop yield was found.

Table 4.10 The regression coefficients, b , of Eq. (4.11) to determine the combined effect of model inputs on crop yield for the greenhouse in Almeria and Texas. Bold numbers indicate that the regression coefficients are significant ($p < 0.10$).

Parameters		Regression coefficients				
p_1	p_2	b_1	b_2	b_{11}	b_{22}	b_{12}
<i>Almeria</i> , $b_0 = 32.08$						
τ_{RfPAR}	τ_{RfNIR}	9.06	0.83	-1.55	-0.13	0.01
τ_{RfPAR}	τ_{RfFIR}	9.17	-4.10	-1.55	0.66	-0.83
τ_{RfPAR}	$T_{air_vent_on}$	8.72	0.31	-1.45	-0.42	0.43
τ_{RfPAR}	CO_{2Out}	8.70	3.38	-1.44	-0.79	0.01
$T_{air_vent_on}$	CO_{2Out}	0.32	3.44	-0.43	-0.81	0.20
<i>Texas</i> , $b_0 = 68.48$						
τ_{RfPAR}	$T_{air_vent_on}$	1.60	0.96	-0.14	-0.07	-0.06
τ_{RfPAR}	CO_{2Air_ExtOn}	1.62	0.98	-0.13	-0.36	-0.06
$T_{air_vent_on}$	CO_{2Air_ExtOn}	0.92	0.98	-0.06	-0.36	0.27

Surprisingly, the combined impact of the PAR transmission coefficient of the roof and the temperature set-point for ventilation on crop yield was positive in Almeria and negative in Texas. It seems that at relative lower radiation and temperature levels (like in Almeria) a combined increase favours crop yield. The positive combined impact of radiation and temperature on crop yield in Almeria was in agreement with results reported by Cooman and Schrevers (2007) for a greenhouse without CO₂ enrichment located at the Bogota Plateau, Colombia. The saturating impact of an increase of PAR on crop yield was clearly demonstrated by the associated negative regression coefficients b_{11} . The impact of the temperature set-point for ventilation and the CO₂-concentration set-point for CO₂ enrichment on crop yield in Texas was simulated for 10x10 input parameter combinations (Fig. 4.5).

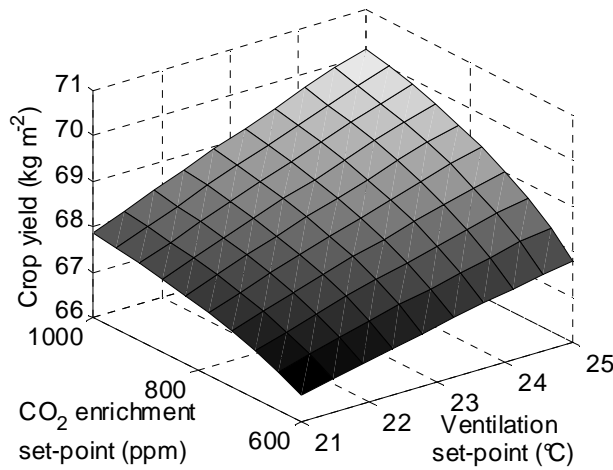


Fig. 4.5 The combined effect of the temperature set-point for ventilation ($T_{air_vent_on}$) and the CO_2 concentration set-point for CO_2 enrichment ($CO_{2air_Ext_CO_{2on}}$) on crop yield in Texas.

The standard deviation between the crop yield estimated by the linear regression model and the simulated crop yield presented in Fig. 4.5 was 0.08. This small standard deviation showed that a normalised second-order composite design around the nominal parameter vector was very efficient to determine the regression coefficients accurately.

Note that, the combined effects of input parameters on crop yield were only analysed for several sets of parameter combinations for which a combined effect on crop yield was expected. Consequently, selecting these combinations beforehand implied that unexpected combined effects would not be revealed.

4.4.7 The methodology used for the sensitivity analysis

In contrast to other sensitivity studies (Van Henten & Van Straten, 1994; Cooman & Schrevers, 2007; Nijsskens *et al.*, 1991; Chalabi & Bailey, 1991; Nava *et al.*, 1998; Van Henten, 2003; Vanthoor *et al.*, 2008b), the impact of input parameters on crop yield, resource use and indoor climate was analysed simultaneously using a combined greenhouse climate crop yield model. This enables the selection of greenhouse parameters relevant for design optimisation. Additionally, the sensitivity of the time derivatives of the states was evaluated which produced valuable information about the seasonal effects of the greenhouse design.

As a first approach, this study focused on the impact of greenhouse design parameters and climate modification techniques on crop yield and resource consumption.

However, to increase the insight in relevant design aspects for greenhouse optimisation even further, the sensitivity of the net profit of the greenhouse grower to input parameters should be determined as well. Therefore, we are currently incorporating an economic model into the combined greenhouse climate-crop yield model in order to determine the net profit as a function of crop yield, investments, resource consumption and labour.

The significance of the mean relative sensitivity values with respect to model accuracy and simulation accuracy is discussed briefly here. The combined greenhouse climate-crop yield model predicted the indoor climate and crop yield with fair accuracy as described in chapter 2 and 3. Furthermore, since the presented sensitivities are based on changes in state values, the impact of absolute simulation errors reduced which in turn further reduced the sensitivity errors. Simulation accuracy was ensured because the selection of a low maximum relative error of the ODE solver resulted that model precision did not influence the sensitivity results.

Although the impact of seasonal effects on sensitivities and combined sensitivities were analysed, the evolution of the combined sensitivities in time was not analysed in this study. However, we think it might be possible to evaluate the combined sensitivities in time as well by performing the following steps. Firstly, the time derivatives of the cumulative crop yield must be determined for the normalised second-order composite design. Subsequently, the regression coefficients of Eq. (4.11) have to be calculated for the time derivatives of the cumulative crop yield at each time instant. Subsequently, the evolution in time can be analysed by plotting these time variant regression coefficients.

This study analysed the sensitivities around the nominal greenhouse design parameters values. This local SA was suitable to select the most relevant greenhouse design parameters for design optimisation. However, to determine the sensitivities for a broader range of design parameter values sampling-based sensitivity analysis of Helton *et al.* (2006) or the average local sensitivity evaluated over a wide range of parameter values should be used as performed Chalabi and Bailey (1991).

4.5 Conclusion

Greenhouse design is an optimization problem that relies on a quantitative trade-off between the economic return of the crop and the costs associated with construction, maintenance and operation of the greenhouse facility. To solve this optimisation problem, we developed a model-based greenhouse design method. Since the number of factors involved in this optimisation problem is very large, it is beneficial to identify those parameters that most strongly influence the economic trade-off and consequently the greenhouse design. A model sensitivity analysis (SA) is an appropriate technique for that purpose.

The objective of this research was to identify those parameters that most strongly influence a greenhouse design. For that purpose a sensitivity analysis was applied to the combined greenhouse climate-tomato yield model which is a key component of the model-based design method. To show that the results of the SA depend on the greenhouse design and the local climate conditions, the analysis was performed for a low-tech greenhouse under conditions encountered in Almeria, Spain and a high-tech greenhouse under conditions encountered in Texas, USA. Additional to earlier validation experiments, simulations with real climate data from Almeria and Texas indicated that the model was able to produce realistic data of the indoor climate and crop yield. Then, a single variate and a multi-variate sensitivity analysis were implemented. Results showed that the outdoor climate had the strongest impact on the performance of the greenhouse system, followed by the greenhouse design parameters and finally, the greenhouse climate set-points. This indicates that the selection of a proper location for the greenhouse is of utmost importance.

Concerning the design parameters, PAR remains the main limiting factor for greenhouse production systems. For both locations the crop yield can be increased using: a higher PAR transmission of both the cover and the whitewash; a higher PAR reflection coefficient of the greenhouse floor and by less light-absorbing greenhouse construction elements. Since the impact of the NIR transmission of the whitewash on crop yield is opposite to the impact of its PAR transmission, a NIR selective whitewash would increase crop yield for both locations. For the low-tech greenhouse without a heating system, a decrease of the FIR transmission coefficient and an increase of the NIR transmission coefficient of the cover would favour crop yield due to their positive impact on the canopy temperature. Furthermore, the single variate sensitivity analysis indicated whether sufficient climate control capacities were installed and which greenhouse design parameters must be

adjusted to save resources. Specifically, for the high-tech greenhouse, an increase of the CO₂ enrichment capacity would favour crop yield and a decrease of the FIR emission coefficient of the cover would considerably lower the energy consumption. The research revealed clear seasonal patterns in the model sensitivity for instance for the PAR transmission, NIR transmission and FIR emission coefficient of the cover material. This suggests that a greenhouse design with adjustable cover parameters will be advantageous over a design with fixed greenhouse cover parameters. The multi-variate analysis revealed strong joint effects of parameters on crop yield. A joint increase of PAR transmission and temperature set-point for ventilation favoured the crop yield for both greenhouses.

The presented SA techniques were able to quantify and compare the single, combined and seasonal impact of input parameters on the harvest rate, resource consumption and indoor climate. The results presented in this study will be used to further develop the model-based design method which aims to design the best greenhouse with respect to local climate and economic conditions for each location on earth.

Acknowledgement

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4.6 Appendices

4.6.1 Appendix A

Appendix A explains why, in some cases, the sensitivity of the time derivatives of states had to be determined instead of the sensitivity of the associated states. An example is presented for the state “cumulative crop yield”.

Fictive values of the cumulative crop yield and the harvest rate are presented respectively in Fig. A1.a and Fig. A1.b. Subsequently, the relative sensitivity of both the cumulative crop yield and the harvest rate at time instants 50 and 80 was calculated using Eq. (4.3) and (4.4) assuming $z_{nom} = 1$ and $\Delta z = 0.1$:

Relative sensitivity cumulative crop yield:

$$t_k = 50: S_Z^x(t_k) = \frac{200 - 100}{0.1} \frac{1}{100} = 10$$

$$t_k = 80: S_Z^x(t_k) = \frac{280 - 160}{0.1} \frac{1}{100} = 12$$

Relative sensitivity harvest rate:

$$t_k = 50: S_Z^{\dot{x}}(t_k) = \frac{4 - 2}{0.1} \frac{1}{2} = 10$$

$$t_k = 80: S_Z^{\dot{x}}(t_k) = \frac{2 - 2}{0.1} \frac{1}{2} = 0$$

Now it is remarkable that at time instant t_k is 80 the crop yield is sensitive to a parameter disturbance ($S_Z^x(t_k)=12$) whereas the harvest rate was not influenced by this parameter (Fig. A1.b) which was presented well by the relative sensitivity of the harvest rate ($S_Z^{\dot{x}}(t_k)=0$). Therefore, we used in this study the harvest rate sensitivity instead of the cumulative crop yield sensitivity to reveal the seasonal effect of input parameter impact.

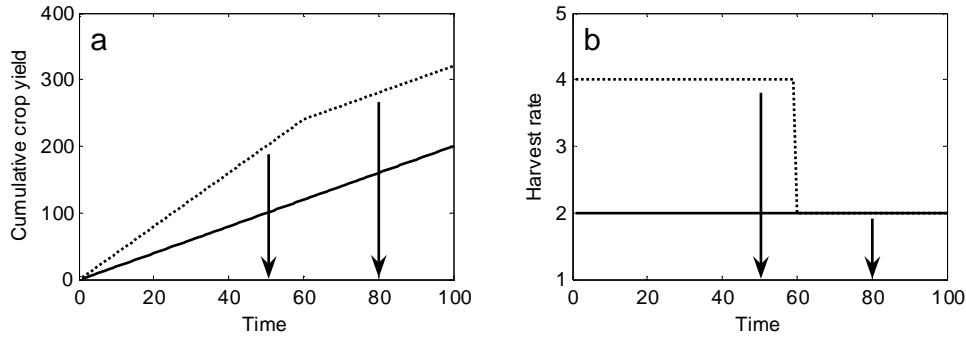


Fig. A1 The cumulative crop yield (a) and the accompanying harvest rate (b) for a simulation with a nominal input parameter (solid line) and for the deviated input parameter (dotted line). Fictive values were presented here to simplify the explanation.

4.6.2 Appendix B

Appendix B proves that the mean relative sensitivity of the time derivative of a state, $\bar{S}_Z^{\dot{X}}$, equals the relative sensitivity of a state value at the end of the production period, $S_Z^X(t_f)$:

$$\bar{S}_Z^{\dot{X}} = S_Z^X(t_f) \quad [-] \quad (\text{B.1})$$

with:

$$\dot{X}(t_k) = \frac{dX(t_k)}{dt} \rightarrow X(t_0) + \sum_{k=0}^{k=N} \dot{X}(t_k) \cdot \Delta t = X(t_f) \quad [-] \quad (\text{B.2})$$

Since all initial conditions of the state variables for which the mean relative sensitivity of the time derivatives was determined were zero, Eq. (B.2) can be rewritten into:

$$\sum_{k=0}^{k=N} \dot{X}(t_k) = \frac{1}{\Delta t} (X(t_f)) \quad [-] \quad (\text{B.3})$$

By definition:

$$\bar{\dot{X}}_{Z_{Nom}} = \frac{1}{N+1} \sum_{k=0}^{k=N} \dot{X}_{Z_{Nom}}(t_k) \quad [-] \quad (\text{B.4})$$

According to the relative sensitivity definition of Chalabi and Bailey (1991):

$$S_z^X(t_f) = \frac{X_{z_{Nom}+\Delta z}(t_f) - X_{z_{Nom}}(t_f)}{\Delta z} \frac{z_{Nom}}{X_{z_{Nom}}(t_f)} \quad [-] \quad (\text{B.5})$$

The relative sensitivity of the time derivate of a state is described by:

$$S_z^{\dot{X}}(t_k) = \frac{\dot{X}_{z_{Nom}+\Delta z}(t_k) - \dot{X}_{z_{Nom}}(t_k)}{\Delta z} \frac{z_{Nom}}{\dot{X}_{z_{Nom}}(t_k)} \quad [-] \quad (\text{B.6})$$

Based on Eq. (4.7) of section 4.3.2.1, the mean relative sensitivity of the time derivate of a state is described by:

$$\bar{S}_Z^{\dot{X}} = \frac{1}{N+1} \sum_{k=0}^{k=N} S_Z^{\dot{X}}(t_k) \quad [-] \quad (\text{B.7})$$

Combining Eqs. (B.6) and (B.7):

$$\bar{S}_Z^{\dot{X}} = \frac{1}{N+1} \sum_{k=0}^{k=N} \frac{\dot{X}_{z_{Nom}+\Delta z}(t_k) - \dot{X}_{z_{Nom}}(t_k)}{\Delta z} \frac{z_{Nom}}{\dot{X}_{z_{Nom}}(t_k)} \quad [-] \quad (\text{B.8})$$

Re-arrangement of Eq. (B.8):

$$\bar{S}_Z^{\dot{X}} = \frac{1}{N+1} \frac{1}{\bar{\dot{X}}_{z_{Nom}}} \frac{z_{Nom}}{\Delta z} \left(\sum_{k=0}^{k=N} \dot{X}_{z_{Nom}+\Delta z}(t_k) - \dot{X}_{z_{Nom}}(t_k) \right) \quad [-] \quad (\text{B.9})$$

Combining Eqs. (B.4) and (B.9) results in:

$$\bar{S}_Z^{\dot{X}} = \frac{1}{N+1} \frac{1}{\sum_{k=0}^{k=N} \dot{X}_{z_{Nom}}(t_k)} \frac{z_{Nom}}{\Delta z} \left(\sum_{k=0}^{k=N} \dot{X}_{z_{Nom}+\Delta z}(t_k) - \sum_{k=0}^{k=N} \dot{X}_{z_{Nom}}(t_k) \right) \quad [-] \quad (\text{B.10})$$

Eq. (B.10) is rewritten using Eq. (B.3), so that the statement of Eq. (B.1) is proven:

$$\bar{S}_Z^{\dot{X}} = \frac{X_{z_{Nom}+\Delta z}(t_f) - X_{z_{Nom}}(t_f)}{\Delta z} \frac{z_{Nom}}{X_{z_{Nom}}(t_f)} \quad [-] \quad (\text{B.11})$$

4.6.3 Appendix C

The greenhouse design parameters for the low-tech greenhouse in Almeria, Spain and for the high-tech greenhouse in Texas, USA. The column sensitivity analysis (SA) presents which greenhouse design parameters were evaluated during the sensitivity analysis study. The dots indicate that the greenhouse design did not contain the accompanying design parameter.

Greenhouse design parameters, P_d	Parameter	Unit	Almeria, Spain	Texas, USA	SA
Construction					
The ratio of the global radiation which is absorbed by the greenhouse construction elements	η_{Glob_Air}	-	0.05	0.1	+
Mean greenhouse cover slope	ψ	°	Arch shaped greenhouse	22	-
Surface of the cover including side-walls	A_{Cov}	m ²	$1.15 \cdot 10^3$	$9.0 \cdot 10^4$	-
Surface of the greenhouse floor	A_{Flr}	m ²	$0.63 \cdot 10^3$	$7.8 \cdot 10^4$	+
Convective heat exchange parameter between cover and outdoor air that depends on the greenhouse shape	C_{HECin}	W m ⁻² K ⁻²	2.21	1.86	+
Convective heat exchange variables between cover and outdoor air which depend on the greenhouse shape	C_{HECout_1}	W m ⁻² cover K ⁻¹	0.95	2.8	+
	C_{HECout_2}	J m ⁻³ K ⁻¹	6.76	1.2	
	C_{HECout_3}	-	0.49	1	
Height of the greenhouse compartment below the thermal screen	h_{Air}	m	3	4.65	+
The altitude of the greenhouse	$h_{Elevation}$	m	150	1470	+
Mean height of the greenhouse	h_{Gh}	m	4.37	5.06	+
Ventilation properties					
The porosity of the insect screens	ζ_{InsScr}	-	0.33	*	+
The specific roof ventilation area	A_{Roof}/A_{Flr}	m ²	0.13	0.18	+
The side ventilation area	A_{Side}/A_{Flr}	m ²	0.09	*	+

Greenhouse design parameters, P_d	Parameter	Unit	Almeria, Spain	Texas, USA	SA
Ventilation discharge coefficient depends on greenhouse shape	C_d^{Gh}	-	0.65	0.65	+
Greenhouse leakage coefficient which depends on the greenhouse type	$c_{leakage}$	-	$1 \cdot 10^{-4}$	$1 \cdot 10^{-4}$	+
Ventilation global wind pressure coefficient depends on greenhouse shape	C_w^{Gh}	-	0.07	0.09	+
Vertical distance between mid-points of side wall and roof ventilation openings	$h_{SideRoof}$	m	3	*	+
Vertical dimension of a single ventilation opening	h_{Vent}	m	*	0.97	+
Roof					
The FIR emission coefficient of the roof	ϵ_{RfFIR}	-	0.5	0.85	+
Density of the roof layer	ρ_{Rf}	kg m^{-3}	$0.93 \cdot 10^3$	$2.6 \cdot 10^3$	-
The NIR reflection coefficient of the roof	ρ_{RfNIR}	-	0.34	0.13	-
The PAR reflection coefficient of the roof	ρ_{RfPAR}	-	0.34	0.13	-
The FIR reflection coefficient of the roof	ρ_{RfFIR}	-	0.1	0.15	-
The NIR transmission coefficient of the roof	τ_{RfNIR}	-	0.61	0.85	+
The PAR transmission coefficient of the roof	τ_{RfPAR}	-	0.61	0.85	+
FIR transmission coefficient of the roof	τ_{RfFIR}	-	0.4	0	+
Thermal heat conductivity of greenhouse roof	λ_{Rf}	$\text{W m}^{-1} \text{K}^{-1}$	0.2	1.05	+
The specific heat capacity of the roof layer	$c_{p,Rf}$	$\text{J K}^{-1} \text{kg}^{-1}$	$2.5 \cdot 10^3$	$0.84 \cdot 10^3$	+
Thickness of the roof layer	h_{Rf}	m	$0.25 \cdot 10^{-3}$	$4 \cdot 10^{-3}$	-
Whitewash					
The FIR emission coefficient of the whitewash	$\epsilon_{ShScrPerFIR}$	-	0.9	0.9	+
Density of the whitewash	$\rho_{ShScrPer}$	kg m^{-3}	$1 \cdot 10^3$	$1 \cdot 10^3$	-
NIR reflection coefficient of the whitewash	$\rho_{ShScrPerNIR}$	-	0.3	0.3	+

Greenhouse design parameters, P_d	Parameter	Unit	Almeria, Spain	Texas, USA	SA
PAR reflection coefficient of the whitewash	$\rho_{ShScrPerPAR}$	-	0.3	0.3	+
FIR reflection coefficient of the whitewash	$\rho_{ShScrPerFIR}$	-	0.05	0.05	-
NIR transmission coefficient of the whitewash	$\tau_{ShScrPerNIR}$	-	0.6	0.6	+
PAR transmission coefficient of the whitewash	$\tau_{ShScrPerPAR}$	-	0.6	0.6	+
FIR transmission coefficient of the whitewash	$\tau_{ShScrPerFIR}$	-	0.05	0.05	+
Specific heat capacity of the whitewash	$c_{p,ShScrPer}$	J K ⁻¹ kg ⁻¹	$4.18 \cdot 10^3$	$4.18 \cdot 10^3$	+
Thickness of the whitewash	$h_{ShScrPer}$	m	$0.2 \cdot 10^{-3}$	$0.2 \cdot 10^{-3}$	-
Thermal screen					
The FIR emission coefficient of the thermal screen	$\varepsilon_{ThScrFIR}$	-	*	0.44	+
Density of the thermal screen	ρ_{ThScr}	kg m ⁻³	*	$0.2 \cdot 10^3$	-
The NIR reflection coefficient of the thermal screen	$\rho_{ThScrNIR}$	-	*	0.7	+
The PAR reflection coefficient of the thermal screen	$\rho_{ThScrPAR}$	-	*	0.7	+
The FIR reflection coefficient of the thermal screen	$\rho_{ThScrFIR}$	-	*	0.45	-
The NIR transmission coefficient of the thermal screen	$\tau_{ThScrNIR}$	-	*	0.25	+
PAR transmission coefficient of the thermal screen	$\tau_{ThScrPAR}$	-	*	0.25	+
FIR transmission coefficient of the thermal screen	$\tau_{ThScrFIR}$	-	*	0.11	+
Specific heat capacity of the thermal screen	$c_{p,ThScr}$	J kg ⁻¹ K ⁻¹	*	$1.8 \cdot 10^3$	+
Thickness of the thermal screen	h_{ThScr}	m	*	$0.35 \cdot 10^{-3}$	-
The thermal screen flux coefficient	K_{ThScr}	m ³ m ⁻² K ^{-0.66} s ⁻¹	*	$0.25 \cdot 10^{-3}$	+
Floor					
FIR emission coefficient of the greenhouse floor	ε_{Flr}	-	1	1	+
Density of the floor	ρ_{Flr}	kg m ⁻³	2300	2300	-
NIR reflection coefficient of the floor	ρ_{FlrNIR}	-	0.5	0.5	+
PAR reflection coefficient of the greenhouse floor	ρ_{FlrPAR}	-	0.65	0.65	+

Greenhouse design parameters, P_d		Parameter	Unit	Almeria, Spain	Texas, USA	SA
Thermal heat conductivity of the floor		λ_{Flr}	$\text{W m}^{-1} \text{K}^{-1}$	1.7	1.7	+
Specific heat capacity of the floor		$c_{p,Flr}$	$\text{J K}^{-1} \text{kg}^{-1}$	$0.88 \cdot 10^3$	$0.88 \cdot 10^3$	+
Thickness of the greenhouse floor		h_{Flr}	m	0.02	0.02	-
Soil properties						
The volumetric heat capacity of the soil		$\rho c_{p,So}$	$\text{J m}^{-3} \text{K}^{-1}$	$1.73 \cdot 10^6$	$1.73 \cdot 10^6$	+
Thermal heat conductivity of the soil layers.		λ_{So}	$\text{W m}^{-1} \text{K}^{-1}$	0.85	0.85	+
Heating system						
FIR emission coefficient of the heating pipes		ε_{Pipe}	-	*	0.88	+
External diameter of the heating pipe		$\phi_{Pipe,e}$	m	*	$51 \cdot 10^{-3}$	-
Internal diameter of the heating pipe		$\phi_{Pipe,i}$	m	*	$47 \cdot 10^{-3}$	-
Length of the heating pipe per square meter greenhouse		l_{Pipe}	m m^{-2}	*	1.25	+
Active climate control						
Capacity of the external CO_2 source		$\phi_{Ext\text{CO}_2}$	mg s^{-1}	*	$4.3 \cdot 10^5$	+
Thermal heat capacity of the boiler		P_{Boil}	W	*	$13.9 \cdot 10^6$	+

Chapter 5

An economic model to evaluate different greenhouses under Spanish conditions

The contents of this chapter have been submitted to Biosystems Engineering as a paper entitled: *A methodology for model-based greenhouse design: Part 4, An economic model to evaluate different greenhouses under Spanish conditions.*

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5.1 Abstract

An economic model was developed as a key component of a model-based method to design greenhouses for a broad range of climatic and economic conditions. This economic model was joined with an existing greenhouse climate-crop yield model to calculate the annual Net Financial Result (NFR) of a greenhouse. The aim of this study was to identify—among ten predefined design alternatives—the greenhouse with the highest annual NFR for tomato production under South-Spanish conditions. The basic designs were either the parral greenhouse, or a multi-tunnel, possibly fitted with any combination of heating, fogging and CO₂ enrichment. Results demonstrated that the multi-tunnel, fitted with only a fogging system was most profitable, followed by the multi-tunnel with heating, CO₂ enrichment and fogging. However, the difference in NFR between such a design and a simple parral was small with respect to the difference in investment. A sensitivity analysis of the NFR of the two technology extremes shows that tomato price, the fraction of marketable yield and the photosynthetically active radiation transmission of the cover had the largest bearing on NFR. With increasing technology level, the NFR depended less on outdoor climate and more on tomato price. This indicates that a low-tech greenhouse diminishes the risk of variations among price paths in different years, whereas a high-tech greenhouse covers better the “weather risk”. The best design was also affected by climate management and the joint impact of climate modification techniques. These results demonstrated that a model-based design approach can cope with multi-factorial design aspects.

5.2 Introduction

This chapter contains a description of the economic model. This model describes the annual Net Financial Result (NFR) as a function of the crop yield, the variable costs and the depreciation and maintenance of the construction. To demonstrate the feasibility of a model-based design approach, the economic model is joined with the greenhouse climate-tomato yield model to evaluate the economic performance of different tomato producing greenhouses under South-Spanish conditions.

In the South-Spanish province Almería there are about 27000 Ha greenhouses of which 99% are low-cost structures, covered with plastic and manual regulation of openings as the one mean of climate control (Magán *et al.*, 2008). The low productivity of such greenhouses is often attributed to the limited means for climate control (Castilla & Montero, 2008). Possible improvements of one design factor have been researched extensively: for instance, air tightness of the greenhouse (López *et al.*, 2001), increase of the ventilation rate (Pérez-Parra *et al.*, 2004), increase of the cover slope (Soriano *et al.*, 2004), cover type (Magán *et al.*, 2008), heating system (López *et al.*, 2008), cooling system (Gázquez *et al.*, 2008; Meca *et al.*, 2007; Antón *et al.*, 2006), ventilation design (Pérez-Parra *et al.*, 2004; Baeza *et al.*, 2009) and CO₂ enrichment (Stanghellini *et al.*, 2008). However, most studies determined the effect on productivity, rather than the improvement of economical performance. In addition, an objective comparison between different greenhouse designs cannot be done by analysing one factor at a time, since an “optimal” modification may require concurrent adaptation of several design factors.

Therefore, the aims of this work were first to identify the greenhouse with the highest annual NFR, among a predefined set of ten design alternatives: a low-tech Spanish parral and a multi-tunnel fitted with various combinations of climate management tools and then to select promising design improvements, by means of a sensitivity analysis applied to the combined greenhouse climate-crop yield model and economic model. As starting point for the predefined set of greenhouses, a parral with only natural ventilation was selected, because this greenhouse represents the current state. Contributing factors to the low productivity of this type of greenhouse have been identified as: a) the very open structure enables insects to enter and decreases the resource efficiency (López *et al.*, 2001), b) insufficient ventilation rate (Pérez-Parra *et al.*, 2004) and c) the low cover slope decreases light transmission in winter time (Soriano *et al.*, 2004) and may enable falling of the condensate droplets on the canopy which in turn increases the incidence of diseases. The

first step to improve a greenhouse design is to optimise the structure rather than to implement expensive climate modification techniques (Castilla & Montero, 2008). Therefore, as a second alternative, a multitunnel arch-roof greenhouse with only natural ventilation was selected because this type of greenhouse meets most of the shortcomings mentioned above. The second step to improve a greenhouse design is to select a “greenhouse technological design package” that suits the local climate, in order to comply with the demand for year-round supply of high quality products (Castilla & Hernandez, 2007). Therefore, the multitunnel with natural ventilation was gradually equipped with more (combined) climate modification techniques such as CO₂ enrichment, fogging system and a heating system.

Previous works have shown that the aspects influencing the NFR are affected by several factors, such as outdoor climate conditions (Vanthoor *et al.*, 2009), greenhouse climate set-points (Vanthoor *et al.*, 2008a) and the combined impact of design parameters (chapter 4). Therefore, we wanted to demonstrate in this study that optimal greenhouse design is indeed a multi-factorial optimisation problem. This was done by analysing the impact of the uncertainty in yearly variations of outdoor climate conditions and tomato price trajectories on greenhouse design. The chapter is organised as follows. An economic model to determine the annual NFR and the investments is described. Then the applied sensitivity analysis technique is presented, followed by the set of design alternatives that ranges from low-tech to high-tech greenhouses. Subsequently, the three evaluation studies, i.e. the NFR evaluation of different designs, a sensitivity analysis of a low-tech and a high-tech greenhouse, and the uncertainty analysis are described. Results of the best greenhouse design and design improvements are presented. Finally, the multi-factorial character of the design problem is presented and implications on the model-based greenhouse design method are discussed.

5.3 Materials and method

5.3.1 Description of the economic model

The overall description of the model-based design method is presented in chapter 1. A greenhouse climate-crop yield model relates the inputs of the method to the economic indicators of the greenhouse. Specifically, from the hourly outdoor climate; climate set-points and selected greenhouse design, the greenhouse climate model (see chapter 2) determines the hourly indoor climate and resource consumption. Subsequently, the tomato production is calculated by the yield model (see chapter 3) as a function of the calculated indoor climate. Here the economic model to determine the net financial result (NFR) and total investments, as a function of the crop yield, variable costs and the selected greenhouse design is described.

The economic state variables needed to describe the NFR are added to the combined greenhouse climate-crop yield. The time derivatives of these state variables are presented by a dot above the state symbol and the related economic parameter values are presented in Table 5.1. To compare the different greenhouse designs, the annual net financial result, Q_{NFR} ($\text{€ m}^{-2} \text{ year}^{-1}$) was used:

$$Q_{NFR}(t_f) = -Q_{Fixed} + \int_{t=t_0}^{t=t_f} \dot{Q}_{CropYield} - \dot{Q}_{Var} dt \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.1)$$

where t_0 (s) and t_f (s) are the beginning and the end of the production period respectively, Q_{Fixed} ($\text{€ m}^{-2} \text{ year}^{-1}$) are the costs related to the tangible assets, $Q_{CropYield}$ ($\text{€ m}^{-2} \text{ year}^{-1}$) is the economic value of crop yield, Q_{Var} ($\text{€ m}^{-2} \text{ year}^{-1}$) are the costs related to the crop (i.e. plant material, fertilizers, crop protection and other crop assets), resource use (in this study defined as water, fossil energy and CO_2) and labour. An overview of the cost aspects is presented in Fig. 5.1. The individual cost aspects are explained in more detail hereafter.

Table 5.1 An overview of the costs-related variables used in this study

Parameter explanation	Parameter	Unit	Value	Source
Average conversion factor from tomato dry matter to fresh matter	η_{DMFM}	$\text{kg}\{\text{FM}\} \text{mg}\{\text{DM}\}^{-1}$	$15.95 \cdot 10^{-6}$	Based on (Magán <i>et al.</i> , 2008)
Fraction of crop transpiration needs to assure sufficient irrigation	η_{Drain}	%	30	Based on practice
Marketable fraction of harvest	η_{FMsold}	-	-	See Table 5.2
Energy content of gas	η_{Fuel}	J m^{-3}	$31.65 \cdot 10^6$	Known
Interest rate	$\eta_{Interest}$	%	3.5	Cajamar
Cost of short-term borrowing	$\eta_{Interest_Short}$	%	1	Cajamar
Labour cost coefficient that describes impact of the production level on labour cost	η_{Labour_kg}	$\text{h kg}^{-1}\{\text{FM}\}$	0.01	Based on (Pérez <i>et al.</i> , 2003)
Labour cost coefficient that describes the impact of plant related labour on variable labour cost	η_{Labour_m2}	h m^{-2}	0.27	Based on (Pérez <i>et al.</i> , 2003)
Annual maintenance cost coefficient of construction element i ,	$\eta_{Maintenance,i}$	% year ⁻¹	-	See Table 5.5
Annual depreciation coefficient of construction element i .	$\eta_{Depreciation,i}$	% year ⁻¹	-	See Table 5.5
Unaccounted fraction of greenhouse construction costs	η_{Rem}	%	2.5	Assumed
Sales cost coefficient for sorting and selling the tomatoes	η_{Sales}	%	9	Cajamar
Fraction of first class tomatoes in marketable yield	η_{Tom1}	%	-	See Table 5.2
Transport cost per kg tomatoes	$\eta_{Transport}$	€ kg ⁻¹	0.02	Cajamar
Greenhouse floor area	A_{Flr}	m ²	10000	Assumed
Harvest rate of tomatoes expressed in dry matter	\dot{DM}_{Har}	$\text{mg}\{\text{DM}\} \text{s}^{-1}$	-	Output tomato yield model
Heat supply to the greenhouse air	$H_{BlowAir}$	W m^{-2}	-	Output climate model

Heat supply to heating pipes	$H_{BoilPipe}$	$W\ m^{-2}$	-	Output climate model
CO ₂ supply rate	MC_{ExtAir}	$mg\ m^{-2}\ s^{-1}$	-	Output climate model
Transpiration rate	MV_{CanAir}	$kg\ m^{-2}\ s^{-1}$	-	Output climate model
Fog supply	MV_{FogAir}	$kg\ m^{-2}\ s^{-1}$	-	Output of climate model
CO ₂ costs	q_{CO2}	$€\ kg^{-1}$	0.15	Cajamar
Gas costs	q_{Fuel}	$€\ m^{-3}$	0.38	Cajamar
Initial investment of construction element i	$q_{Invest,i}$	€	-	See Table 5.5
Labour costs	q_{Labour}	$€\ h^{-1}$	5.4	Cajamar
First class tomato price which is time dependent	q_{Tom1}	$€\ kg^{-1}$	-	Cajamar
Second class tomato price which is time dependent	q_{Tom2}	$€\ kg^{-1}$	-	Cajamar
Water costs	q_{Water}	$€\ m^{-3}$	0.25	Cajamar
Plant material		$€\ plant^{-1}$	0.25	Cajamar
Plant density		m^{-2}	2.5	Based on practice
Fertilizer		$€\ m^{-2}\ year^{-1}$	0.6	Cajamar
Crop protection		$€\ m^{-2}\ year^{-1}$	0.35	Cajamar
Waste treatment		$€\ m^{-2}\ year^{-1}$	0.36	Cajamar
Remaining materials		$€\ m^{-2}\ year^{-1}$	0.3	Cajamar

5.3.1.1 Economic crop yield

The economic tomato yield is described by:

$$\dot{Q}_{CropYield} = \eta_{FMsold} \eta_{DMFM} q_{Tom}(t) \dot{DM}_{Har}(t) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (5.2)$$

where η_{FMsold} (-) is the marketable fraction of harvest, η_{DMFM} is the conversion factor from dry matter to fresh matter ($\text{kg}\{\text{FM}\} \text{ mg}\{\text{DM}\}^{-1}$), q_{Tom} (€ kg^{-1}) is the price of tomatoes, \dot{DM}_{Har} ($\text{mg}\{\text{DM}\} \text{ m}^{-2} \text{ s}^{-1}$) is the harvest rate of tomatoes expressed in dry matter, which is an output of the tomato yield model.

The tomato price q_{Tom} (€ kg^{-1}) depends on the ratio between first class and second class tomatoes and is time-variant due to changing price trajectories throughout the production period:

$$q_{Tom}(t) = \frac{\eta_{Tom1} q_{Tom1}(t) + (100 - \eta_{Tom1}) q_{Tom2}(t)}{100} \quad [\text{€ kg}^{-1}] \quad (5.3)$$

where q_{Tom1} (€ kg^{-1}) and q_{Tom2} (€ kg^{-1}) are respectively the price of the first and second class tomatoes, and η_{Tom1} (%) is the ratio of first class tomatoes which depends on the greenhouse design and which was assumed to be time invariant in this study.

To calculate the costs related to the harvested amount of tomatoes the mass crop yield is described by:

$$\dot{Yield} = \eta_{DMFM} \dot{DM}_{Har}(t) \quad [\text{kg}\{\text{FM}\} \text{ m}^{-2} \text{ s}^{-1}] \quad (5.4)$$

5.3.1.2 The fixed costs

The annual fixed costs, Q_{Fixed} ($\text{€ m}^{-2} \text{ year}^{-1}$) are described by:

$$Q_{Fixed} = Q_{Interest} + \sum_{i=1}^{i=N} Q_{Constr,i} + Q_{Rem} \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.5)$$

where $Q_{Interest}$ ($\text{€ m}^{-2} \text{ year}^{-1}$) is the annual average interest payment of the total investment, i (-) represents the greenhouse construction element, N (-) is the total number of greenhouse construction elements, $Q_{Constr,i}$ ($\text{€ m}^{-2} \text{ year}^{-1}$) are the costs related to the maintenance and depreciation of construction element i , and the Q_{Rem} ($\text{€ m}^{-2} \text{ year}^{-1}$) are limited remaining costs related to the greenhouse construction.

The annual average interest payment of the total investment is based on a linear depreciation of the greenhouse with no rest value at the end of the economic lifespan, and is therefore described by:

$$Q_{Interest} = \frac{\eta_{Interest}}{100A_{Flr}} \sum_{i=1}^{i=N} \frac{q_{Invest,i}}{2} \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.6)$$

where $\eta_{Interest}$ (% year⁻¹) is the interest rate, A_{Flr} (m²) is the greenhouse floor area, and $q_{Invest,i}$ (€) is the initial investment of construction element i .

The annual costs of the maintenance and depreciation of the construction elements is described by:

$$Q_{Constr,i} = \frac{\eta_{Maintenance,i} + \eta_{Depreciation,i}}{100A_{Flr}} \cdot q_{Invest,i} \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.7)$$

where $\eta_{Maintenance,i}$ (% year⁻¹) determines the annual maintenance costs of construction element i , $\eta_{Depreciation,i}$ (% year⁻¹) determines the annual depreciation of construction element i . The remaining costs related to the greenhouse construction are described by:

$$Q_{Rem} = \eta_{Rem} \sum_{i=1}^{i=N} Q_{Constr,i} \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.8)$$

where η_{Rem} (%) is the unaccounted fraction of greenhouse construction costs. In view of the huge variability among conditions, costs related to the rent or purchase of the greenhouse area were not taken into account here.

5.3.1.3 The variable costs

The variable costs presented in Fig. 5.1 are described by:

$$\dot{Q}_{Var} = \dot{Q}_{Plant} + \dot{Q}_{Water} + \dot{Q}_{CO2} + \dot{Q}_{Fuel} \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (5.9)$$

where \dot{Q}_{Plant} (€ m⁻² s⁻¹) are plant costs that depend on crop yield, \dot{Q}_{Water} , \dot{Q}_{CO2} and \dot{Q}_{Fuel} (€ m⁻² s⁻¹) are the costs related to the consumption of water, carbon dioxide supply and fossil fuel, respectively, denoted in this study as ‘resource costs’. The electricity costs were not taken into account because they are negligible for the greenhouse designs under consideration (Magán *et al.*, 2008). Obviously,

$$Q_{Var}(t_0) = Q_{Plant}(t_0) \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.10)$$

where $Q_{Plant}(t_0)$ are the plant costs that do not depend on crop yield, i.e. plant material, fertilizers, crop protection, waste treatment and remaining materials which are presented in Table 5.1.

The plant costs that depend on the crop yield i.e. labour, transport, sales, and short term interest are described by:

$$\begin{aligned} \dot{Q}_{Plant} = & q_{Labour} \left(\eta_{Labour_kg} Yield + \eta_{Labour_m2} \right) \\ & + \eta_{Transport} \eta_{FMsold} Yield + \frac{\eta_{Sales} + \eta_{Interest_Short}}{100} \dot{Q}_{CropYield} \end{aligned} \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (5.11)$$

where q_{Labour} (€ h⁻¹) is the labour costs, η_{Labour_kg} (h kg⁻¹{FM}) is the labour cost coefficient that describes the impact of the production level on labour cost, η_{Labour_m2} (h m⁻²) is the labour cost coefficient that describes the impact of plant related labour (no harvest) on labour cost, $\eta_{Transport}$ (€ kg⁻¹) is the transport cost per kg tomatoes, η_{Sales} (%) is the sales cost coefficient describing the costs of sorting and selling the tomatoes, and $\eta_{Interest_Short}$ (%) is the cost of short term borrowing.

The cost of the use of individual resources is calculated with:

$$\dot{Q}_{Water} = 10^{-3} q_{Water} \left(\left(1 + \frac{\eta_{Drain}}{100} \right) MV_{CanAir} + MV_{FogAir} \right) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (5.12)$$

$$\dot{Q}_{CO2} = 10^{-6} q_{CO2} MC_{ExtAir} \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (5.13)$$

$$\dot{Q}_{Fuel} = \frac{q_{Fuel}}{\eta_{Fuel}} (H_{BoilPipe} + H_{BlowAir}) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (5.14)$$

where q_{Water} (€ m⁻³) is the water price, η_{Drain} (%) is a fraction of crop transpiration needs to assure sufficient irrigation, MV_{CanAir} (kg m⁻² s⁻¹) is the transpiration rate of the crop, MV_{FogAir} (kg m⁻² s⁻¹) is the fogging rate, q_{CO2} (€ kg⁻¹) is the CO₂ price, MC_{ExtAir} (mg m⁻² s⁻¹) is the CO₂ enrichment rate, q_{Fuel} (€ m⁻³) is the fuel price, η_{Fuel} (J m⁻³) is the energy efficiency of the fuel, $H_{BoilPipe}$ (W m⁻²) is the heat supply to the heating pipes and $H_{BlowAir}$ (W m⁻²) is the heat supply from the indirect air heater to the greenhouse air.

The total investment for a greenhouse is described by:

$$Q_{Invest} = \sum_{i=1}^{i=N} q_{Invest,i} \quad [\text{€ m}^{-2}] \quad (5.15)$$

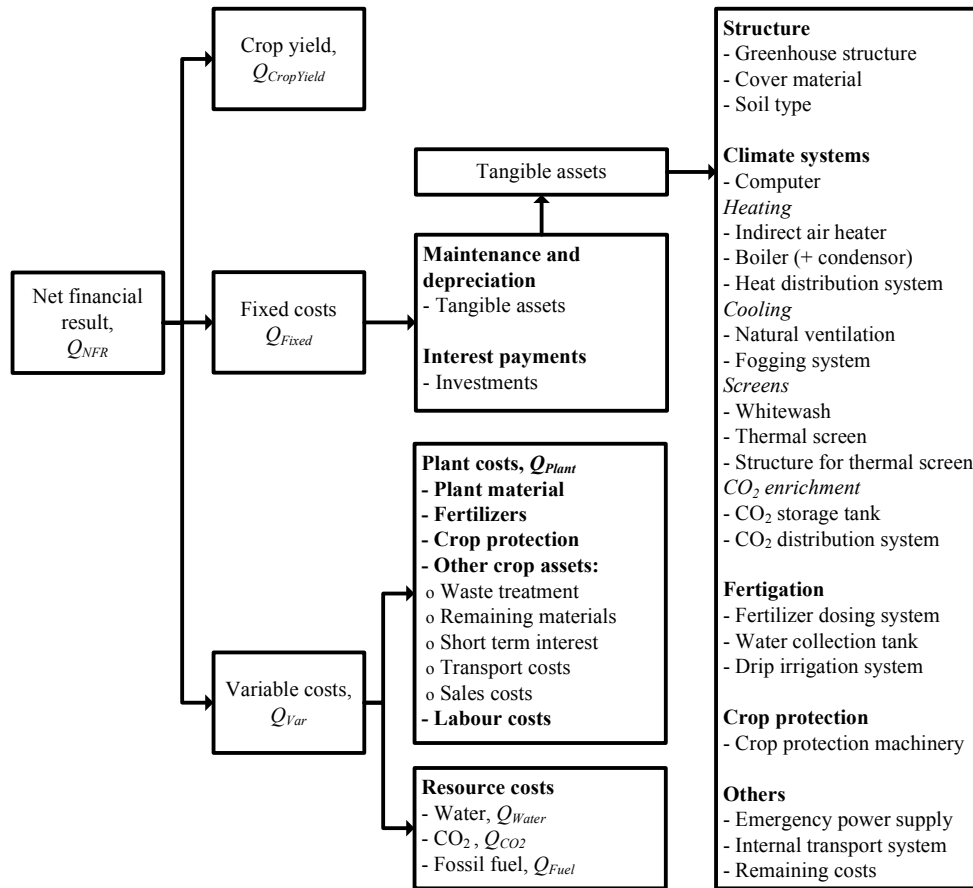


Fig. 5.1 An overview of the costs aspects related to the net financial result, Q_{NFR} , of the grower. The costs aspects are divided in economic crop yield, $Q_{CropYield}$, the fixed costs, Q_{Fixed} and the variable costs, Q_{Var} .

5.3.2 Sensitivity analysis of the economic model states

The economic relative sensitivity is described by:

$$S_z^X(t_f) = \frac{X_{z_{Nom}+\Delta z}(t_f) - X_{z_{Nom}}(t_f)}{\Delta z} \frac{z_{Nom}}{100} \quad [\text{€ m}^{-2} \text{ year}^{-1} \%^{-1}] \quad (5.16)$$

where X are the economic states: Q_{NFR} , $Q_{CropYield}$, Q_{Water} , Q_{CO2} , Q_{Fuel} and Q_{Plant} , z_{Nom} is the nominal input parameter value, Δz is the input parameter deviation, $X_{z_{nom}+\Delta z}$ is the economic state value at input parameter deviation and $X_{z_{nom}}$ is the state value after the nominal input parameter value. This is an adjustment of the relative sensitivity equation presented in chapter 4 in view of the need to express the sensitivity of the economic states to the input parameters in $\text{€ m}^{-2} \text{ year}^{-1} \%^{-1}$. The economic relative sensitivity can be interpreted as the change of the value of the economic model state when an input parameter increases with 1%.

The input parameter z includes the greenhouse design parameters P_d , the climate set-points U and economic parameter values Q :

$$z = P_d \vee U \vee Q \quad [-] \quad (5.17)$$

The input parameters were deviated using a fixed perturbation factor, $h=0.01$, resulting in an absolute increase of the input parameters:

$$\begin{aligned} \Delta P_d &= h \cdot P_{d_Nom} \\ \Delta U &= h \cdot U_{Nom} \\ \Delta Q &= h \cdot \overline{Q_{Nom}} \end{aligned} \quad [-] \quad (5.18)$$

Since time invariant deviations of the input parameters were preferred, the time variant economic parameters, Q , such as the tomato price, were deviated with a fixed fraction of the mean value.

5.3.3 Different greenhouse design and climate management

5.3.3.1 Simulated different greenhouse designs

The ten different configurations that were simulated are described in Table 5.2. All simulated greenhouse designs were covered with a single PE layer (Triplast) and were of rectangular shape of 200 x 50 m resulting in a floor area of $1.0 \cdot 10^4 \text{ m}^2$. The average cover transmission without a thermal screen was 57% and with a thermal screen was 54%. Plants were grown in the soil—a typically artificial layered soil called ‘enarenado’ (Fernández *et al.*, 2005)—and irrigated by a drip irrigation system.

Table 5.2 The different greenhouse technological design packages studied here. The parral represents the current situation. The standard multitunnel design with whitewash (W) was extended with various combinations of CO₂ enrichment (C); fogging (F); air heating (H₋) and boiler-pipe heating (H). All greenhouses were equipped with natural roof and side ventilation.

	Multi-tunnel									
	Parral	W	WC	WF	WFC	WH ₋	WH	WHC	WHF	WHFC
<i>Heating</i>										
Indirect air heater						x				
Pipe heating							x	x	x	x
Thermal screen							x	x	x	x
<i>Cooling</i>										
Whitewash	x	x	x	x	x	x	x	x	x	x
Fog system				x	x				x	x
<i>CO₂-supply</i>										
Pure CO ₂			x		x			x		x
<i>Economic parameters</i>										
Marketable fraction $\eta_{FM\text{sold}}$ (%)	90	95	95	95	95	95	95	95	95	95
1st class tomatoes η_{Tom1} (%)	65	70	70	80	80	80	90	95	95	95

The parral had side ventilation in the 2 long sides (8 % of floor area) and continuous roof ventilation in one side of each span (5 %), resulting in a total ventilation area of 13% of the floor area, which is approximately the mean ventilation area of this type of greenhouse in

Almería (Céspedes *et al.*, 2009). The multi-tunnel had side ventilation in the 2 long sides (6%) and continuous roof ventilation in one side of each span (22.5%) resulting in a total ventilation area of 28.5 % of the floor area. The ventilation openings of both greenhouses were covered with insect nets, which reduced the calculated ventilation by 45%.

The designs evaluated in this study as presented in Table 5.2 were described with a combination of letters each denoting a climate modification technique i.e. whitewash (W), CO₂ enrichment (C), fogging (F), indirect air heater (H₋) and a boiler heating system (H). Two types of heating systems were evaluated: a indirect heating system with a relative low heat capacity of 50 W m⁻² ($P_{Blow} = 0.50$ MW) and a heating set-point of 12°C; and a boiler heating system with a heat capacity of 116 W m⁻² ($P_{Boil} = 1.16$ MW) and a heating set-point of 16°C, the heat distribution system being metallic pipes filled with hot water. A 100% aluminium thermal screen was in all cases associated with this type of heating. The capacity of the CO₂ enrichment system was 50 kg CO₂ ha⁻¹ h⁻¹ ($\phi_{ExtCO2} = 1.39 \cdot 10^4$ mg s⁻¹) and the capacity of the fogging system was 0.5 l m⁻² h⁻¹ ($\phi_{Fog} = 1.39$ kg water s⁻¹).

5.3.3.2 Greenhouse climate control

The control strategy for air temperature is presented in Fig. 5.2, and the related climate set-points are given in Table 5.3. The set point for CO₂ enrichment was a function increasing with outside global radiation and decreasing with window aperture (Magán *et al.*, 2008), see section 5.7 for a detailed description. The vapour pressure deficit of the greenhouse air was controlled by the fogging system, which was switched on whenever the vapour pressure deficit inside, $VP_{Def_Fog_On}$ (kPa), was larger than 1.5 kPa (Gázquez *et al.*, 2010).

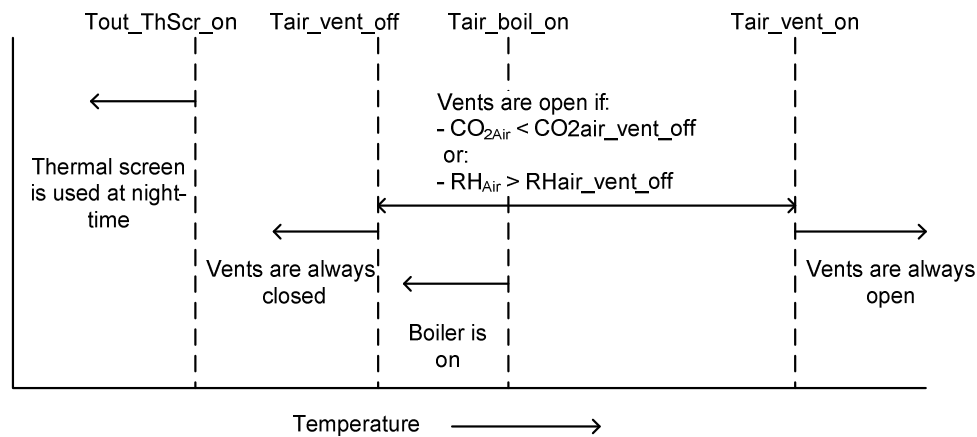


Fig. 5.2 The greenhouse temperature control strategy based upon climate set-points. Values of the climate set-points are listed in Table 5.3

Whitewash was applied in all cases at the beginning of the production period till 15 September (50% decrease of the global transmission), 1 March (25% decrease of the global transmission) and 15 April (50% decrease of the global transmission) which is a commonly used approach in Almería by growers. In the presence of a fogging system growers tend to use a lighter whitewash (Gázquez *et al.*, 2008). Accordingly the fraction of radiation intercepted by the whitewash was reduced in this case to 50% of the values given above.

Table 5.3 Overview of the greenhouse climate management and the crop conditions used for the economic analysis of the different greenhouse designs.

Parameter	Value
<i>Greenhouse climate management</i>	
<i>Whitewash</i>	August 1 st – September 15 th (50% decrease)
	March 1 st – April 15 th (25% decrease)
	April 16 th – June 30 th (50% decrease)
$T_{air_vent_on}$ (°C)	23
$T_{air_vent_off}$ (°C)	20
$RH_{air_vent_off}$ (%)	90
$CO_{2air_vent_off}$ (ppm)	200
$T_{air_boil_on}$ (°C)	12 [*] / 16
$T_{out_ThScr_on}$ (°C)	18
CO_{2Air_ExtMax} (ppm)	850
CO_{2Air_ExtMin} (ppm)	365
I_{Glob_Max} (W m ⁻²)	500
U_{Vent_Max} (-)	0.1
$VP_{Def_Fog_On}$ (kPa)	1.5
<i>Crop conditions</i>	
LAI_start	0.3
LAI_max	2.5
Start growing period, t_0	August 1 st 2008
End growing period, t_f	July 1 th 2009

The ^{*} indicates that this climate set-point was applied for the heating system H_- .

5.3.4 Three design evaluation studies

Three simulation studies were performed: 1) an economic evaluation based on one climate period and average price trajectories; 2) a sensitivity analysis of the economic states to selected input parameters and 3) an uncertainty analysis of NFR to outdoor climate and price trajectories.

The climate data used here were recorded from 2006 to 2009 in Almería (36°48'N, 2°43'W and 151 m above sea level) and the price trajectories for the same years are from the Fundación Cajamar (Anonymous, 2009). For all three simulation studies, the economic crop yield depends on the marketable fraction ($\eta_{FM_{sold}}$) and on the fraction of first class tomatoes (η_{Tom1}). Based on experience and on experimental results of Magán, López, Escudero, Pérez-Parra (2007), both fractions were made dependent on greenhouse design, see Table 5.2. The economic parameters needed to determine the annual costs are presented in Table 5.5. The remaining information needed to perform each simulation study is presented briefly in this section.

5.3.4.1 Economic evaluation based on one climate period and average price trajectories

The NFR was determined for the growing period from August 1st 2006 to July 1st 2007, since the outdoor climate was slightly more moderate than the other two (see Table 5.4).

Table 5.4 Overview of the average outdoor climate and tomato price in Almería from August 1st to July 1st for three successive growing periods. “ $T_{out} < 5\%$ ” is the lower 5th percentiles (the measured temperature is 5% of the time lower than this value) and “ $T_{out} > 95\%$ ” is the upper 5th percentile (the measured temperature is 5% of the time higher than this value).

Period	T_{out} (°C)	$T_{out} < 5\%$ (°C)	$T_{out} > 95\%$ (°C)	Global radiation (MJ m ⁻² day ⁻¹)	RH (%)	Vwind (m s ⁻¹)	q_{Tom1} (€ kg ⁻¹)	q_{Tom2} (€ kg ⁻¹)
2006-2007	17.7	9.1	27.4	16.9	69.7	2.9	0.60	0.33
2007-2008	17.8	10.2	27.7	17.1	67.7	3.3	0.54	0.29
2008-2009	17.2	8.3	28.1	17.2	67.9	3.3	0.51	0.28

The weekly tomato price of the first and second class long life tomatoes were averaged over the three considered production years to determine the time variant tomato price of Eq. (5.3) as presented in Fig. 5.3.

Table 5.5 The economic parameters needed to determine the annual costs of the maintenance and depreciation for all construction elements $Q_{Constr,i}$ of Eq. (5.7): the investments $q_{Invest,i}$ the depreciation $\eta_{Depreciation,i}$ and the maintenance $\eta_{Maintenance,i}$

Construction element	$q_{Invest,i}$ (€ m ⁻²)	$q_{Invest,i}$ (€)	$\eta_{Depreciation,i}$ (% year ⁻¹)	$\eta_{Maintenance,i}$ (% year ⁻¹)	$Q_{Constr,i}$ (€ m ⁻² year ⁻¹)
<i>Construction</i>					
Parral structure	8		6.67	2	0.69
Multi-tunnel structure	18		6.67	2	1.56
Soil type: Enarenado	0.69		33.33	0	0.23
Simple climate computer		8000	15	8	0.18
<i>Cover and screens</i>					
Triplast cover	1.38		33.33	5	0.53
Whitewash	0.09		100	0	0.09
Thermal screen XLS	2		20	5	0.50
Structure for thermal screen	3		10	5	0.45
<i>Heating system</i>					
Boiler heating: 1.16 MW		82000	7	1	0.66
Indirect air heater: 0.5 MW		40000	15	2	0.68
Metalic pipe heating Spain	6		7	0.5	0.45
<i>Fogging system</i>					
System air-water: 500 g m ⁻² h ⁻¹	3		10	5	0.45
<i>CO₂ enrichment system</i>					
Pure CO ₂ : 50 kg Ha ⁻¹ h ⁻¹		3120	100	0	0.31
CO ₂ delivering system	0.34		10	5	0.05
<i>Irrigation</i>					
Fertilizer dosing system		30000	10	5	0.45
Water collection tank		13500	5	1	0.08
Drip irrigation system	1.4		10	5	0.21
<i>Crop protection</i>					
Crop protection machinery		1500	15	5	0.03
Emergency power		9000	5	5	0.09
<i>Remaining</i>					
Internal transport system		26580	10	5	0.40

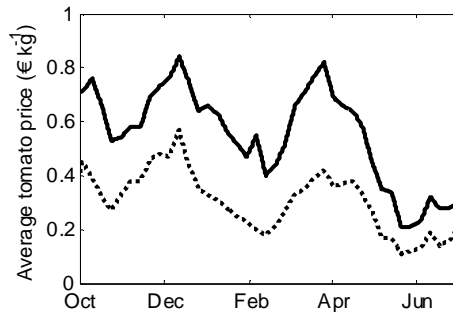


Fig. 5.3 The weekly price of the first class (solid line) and second class (dotted line) long life tomatoes averaged over the three successive production cycles between 2006 and 2009 (Source: Anonymous, 2009)

5.3.4.2 Sensitivity of analysis of economic states to input parameters

The sensitivity of the economic states to some input parameters was determined for the parral and for the high-tech multitunnel (equipped with all climate modification techniques, WHFC) for the climate period and price trajectories as above.

As the economic crop yield is the only revenue, the economic parameters of Eqs. (5.2) and (5.3) might have a large impact on the economic states; therefore the sensitivity of the results to these parameters needs to be evaluated. With respect to the greenhouse design parameters and climate parameters set-points, we relied on results presented in chapter 4 showing that transmission of the cover and whitewash for photosynthetically active radiation (PAR); near infrared (NIR) and far infrared (FIR) radiation; the ventilation area and temperature set-point for ventilation have a large impact on yield. Therefore the sensitivity of the NFR to all these parameters was evaluated. Finally, for the multi-tunnel the sensitivity to all capacities of the climate modification techniques and corresponding climate management set-points were evaluated as well.

5.3.4.3 Uncertainty analysis of NFR to outdoor climate and price trajectories

The impact of the uncertainty in yearly variations of outdoor climate and tomato price on the NFR was analysed for all greenhouse designs by: 1) determining the NFR for three different years (2006 – 2007, 2007 – 2008 and 2008 – 2009, Table 5.4), each combined with the average price trajectory, 2) determining the NFR for one year (2006 – 2007), and the three price trajectories (2006-2009), 3) determining the NFR for the three different climate periods and related price trajectories and 4) determining the NFR for one year (2006 – 2007), and three constant tomato prices of 0.50 €/kg⁻¹, 1 €/kg⁻¹ and 1.50 €/kg⁻¹.

5.4 Results and discussion

In this chapter the NFR of the different designs is evaluated, the evolution of the NFR along the production period is analysed and design improvements are suggested based on the sensitivity analysis. Subsequently, the impact of the uncertainty in yearly variations of outdoor climate and tomato price on NFR and greenhouse design is presented.

5.4.1 Evaluation of different greenhouse designs

5.4.1.1 NFR evaluation of different designs

The crop yield model has been successfully validated in chapter 3 for both the parral and the multitunnel with all means of climate modification, under Spanish conditions. The total simulated water and CO₂ consumption agree with measurements of Magán *et al.* (2008) in a multi-tunnel. The fact that their gas consumption was higher than the simulated one can be explained by their higher heating set-point. The economic analysis of the different greenhouse designs is presented in Table 5.6. The costs components presented there, i.e. the economic crop yield, fixed costs, variable costs and NFR are discussed in this section. Some strict assumptions related to the depreciation, maintenance, the unaccounted fraction of greenhouse construction and the short term borrowing costs, have resulted in negative NFR values. Be aware that this will not influence the results because this study focussed on the comparison between greenhouse designs rather than on absolute NFR values.

Table 5.6 Economic analysis of the different greenhouse designs determined for the growing period 2006-2007 with a mean weekly price over the years 2006-2009. The parral with whitewash (W) represents the most common current situation. The standard multi-tunnel design with whitewash (W) was extended with various combinations of CO₂ enrichment (C); fogging (F); air heating (H₋) and pipe heating (H). All greenhouses were equipped with natural roof and side ventilation.

	Parral	Multi-tunnel								
		W	WC	WF	WFC	WH ₋	WH	WHC	WHF	WHFC
Crop Yield (kg m ⁻²)	21.88	23.99	25.78	26.45	28.15	27.71	28.35	31.89	31.34	35.03
Crop Yield (€m ⁻² year ⁻¹)	9.77	11.01	11.86	12.33	13.15	13.65	14.89	17.22	16.42	18.47
Total investments (€m ⁻²)	21.54	31.79	32.46	34.86	35.53	35.89	51.47	52.14	54.54	55.21
Fixed costs (€m ⁻² year ⁻¹)	3.43	4.50	4.88	5.01	5.39	5.26	6.95	7.33	7.46	7.85
Variable costs (€m ⁻² year ⁻¹)	6.59	6.82	7.82	7.17	8.25	9.31	8.88	10.18	9.28	10.65
Water costs	0.17	0.18	0.18	0.21	0.21	0.18	0.19	0.19	0.22	0.22
CO ₂ costs	0	0	0.78	0	0.87	0	0	0.78	0	0.88
Fossil fuel	0	0	0	0	0	1.94	1.34	1.34	1.32	1.32
Labour costs	2.77	2.82	2.92	2.96	3.06	3.03	3.07	3.27	3.24	3.45
Remaining plant costs	3.65	3.82	3.94	4.00	4.11	4.16	4.28	4.60	4.50	4.78
Net financial result (€m ⁻² year ⁻¹)	-0.25	-0.31	-0.84	0.15	-0.49	-0.92	-0.94	-0.29	-0.32	-0.03
Mean tomato price (€kg ⁻¹)	0.45	0.46	0.46	0.47	0.47	0.49	0.53	0.54	0.52	0.53
Marginal tomato price (€kg ⁻¹)	0.46	0.47	0.49	0.46	0.48	0.53	0.56	0.55	0.53	0.53
Water use crop (l m ⁻²)	670.7	716.1	717.1	759.4	759.9	727.3	743.0	743.8	786.9	787.1
Water use fogging system (l m ⁻²)	0	0	0	93.4	93.3	0	0	0	101.5	101.5
Energy use (m ³ m ⁻²)	0	0	0	0	0	5.10	3.52	3.53	3.47	3.47
CO ₂ use (kg m ⁻²)	0	0	5.23	0	5.77	0	0	5.23	0	5.85

Economic crop yield

The simulated economic crop yield increased considerably with increasing technology from $9.77 \text{ € m}^{-2} \text{ year}^{-1}$ for the parral to $18.47 \text{ € m}^{-2} \text{ year}^{-1}$ for the multi-tunnel equipped with all climate modification techniques. Starting from the simple multitunnel (revenue $11.01 \text{ € m}^{-2} \text{ year}^{-1}$) the economic crop yield increased $0.85 \text{ € m}^{-2} \text{ year}^{-1}$ by using CO_2 enrichment and $3.88 \text{ € m}^{-2} \text{ year}^{-1}$ by using a heating system. The joint effect, $6.21 \text{ € m}^{-2} \text{ year}^{-1}$, would be some 30% more than the sum of the two, which follows from the fact that when using only one climate modification technique, either temperature or CO_2 concentration became the limiting factor for crop growth. Using a multivariate sensitivity analysis, results in chapter 4 have shown such a positive combined impact of a higher CO_2 concentration and air temperature for a climate-controlled glasshouse in Texas.

Fig. 5.4a presents the trend in time of the effect of the climate modification techniques on crop yield. During winter, harvest was maximal in a heated multi-tunnel with CO_2 enrichment, followed by a heated multi-tunnel and the unheated one. The CO_2 enrichment system enhanced the harvest rate mainly from December to May, since the relatively small ventilation requirement resulted in a higher CO_2 set-point (see section 5.7) and CO_2 concentration inside. On the other hand, the fogging system boosted crop yield from March through June, mainly thanks to the higher light transmission (milder whitewash) and the lower air temperature.

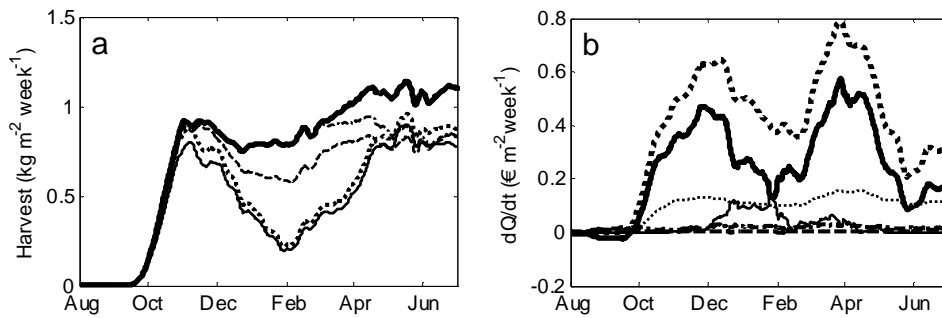


Fig. 5.4 The seasonal impact on the harvest rate (a) and the economic state variables (b). Fig 5.4a The harvest rate for the six different greenhouse designs: the parral (thin solid line), the W (dotted line), the WH (dashed line), the WHC (dashed dotted line) and the WHFC multi-tunnel. Fig. 5.4b The time derivatives of the economic states for the WHC multi-tunnel: the net financial result, (thick solid line); the economic crop yield (thick dotted line); the water costs, (dashed line); the CO_2 costs (dashed dotted line); the fuel costs (thin solid line); and the plant costs (thin dotted line).

The fixed costs

The fixed costs and total investment costs augmented considerably with increasing greenhouse technology level (Table 5.6). Two investments “jumps” occurred: 1) the change from parral to multi-tunnel costs 10.25 € m^{-2} and 2) fitting heating into a multi-tunnel (including thermal screens and metallic heating pipes) costs 19.01 € m^{-2} . The extra annual fixed costs caused by CO₂ enrichment system ($0.38 \text{ € m}^{-2} \text{ year}^{-1}$) or a fogging system ($0.51 \text{ € m}^{-2} \text{ year}^{-1}$) are relatively small, which entails a smaller risk than a heating system ($2.45 \text{ € m}^{-2} \text{ year}^{-1}$).

The variable costs

The variable costs increased with technology level mainly due to a higher resource costs (Table 5.6). Labour and remaining plant costs amount to 44.5% of the total annual costs of the multi-tunnel with whitewash, heating, fogging and CO₂ supply (WHFC), whereas resource consumption accounts for a relatively small fraction: heating (7.1%); CO₂ (4.8%) and water (1.2 %).

The NFR

Table 5.6 shows that the multi-tunnel with only fogging system, WF, was the most profitable ($0.15 \text{ € m}^{-2} \text{ year}^{-1}$), followed by the multi-tunnel with all climate modification techniques, WHFC, ($-0.03 \text{ € m}^{-2} \text{ year}^{-1}$), the parral, ($-0.25 \text{ € m}^{-2} \text{ year}^{-1}$), the multi-tunnel with CO₂ enrichment and heating, WHC, ($-0.29 \text{ € m}^{-2} \text{ year}^{-1}$) and the multi-tunnel without climate modification techniques, W, ($-0.31 \text{ € m}^{-2} \text{ year}^{-1}$). Fogging was most profitable, since the yield increase thanks to the application of a thinner whitewash and to a lower incidence of extreme air temperatures, easily offset the relatively low costs of a fogging system.

According to Table 5.6, the differences in NFR between the parral and a multi-tunnel structure equipped with a fogging system is $0.40 \text{ € m}^{-2} \text{ year}^{-1}$, which may seem small with respect to the daunting difference in investment of 13.32 € m^{-2} . The investment pay-back time does indeed exceed the planning horizon of most growers. In addition, Table 5.6 shows that if one is prepared to invest in a heating system for a multi-tunnel, then it would be certainly worthwhile to fit a CO₂ enrichment system as well. Specifically, the NFR of a greenhouse with a CO₂ enrichment and heating system (WHC, $-0.29 \text{ € m}^{-2} \text{ year}^{-1}$) was considerably higher than a greenhouse with either CO₂ enrichment (WC, $-0.84 \text{ € m}^{-2} \text{ year}^{-1}$) or a heating system (WH, $-0.94 \text{ € m}^{-2} \text{ year}^{-1}$).

The time derivatives of the economic states determine the profitable periods (Fig. 5.4b). For the multi-tunnel equipped with all climate modification techniques, the time derivative of the NFR had two local maxima: the income per week was high at the beginning of December and highest at the beginning of April. The two peaks were caused by a higher tomato price and not by a higher harvest rate, as shown by the similarity with the price trajectory (Fig. 5.3), whereas the harvest rate of the WHFC multi-tunnel (Fig. 5.4a) was rather stable. The weekly income at the end of the production period was small, which explains why most growers stop cultivating even earlier than assumed here.

5.4.1.2 Improvements of low-tech and high tech greenhouse to increase NFR

A sensitivity analysis of the economic states was carried out to demonstrate how the parral (Table 5.7) and the multi-tunnel with heating, CO₂ enrichment and fogging (Table 5.8) could be improved to increase the NFR. For both greenhouses the tomato price and the marketable fraction had the largest impact on NFR. This result indicates that a small change in price trajectories will influence the NFR considerably, which demonstrates the need for negotiating a good tomato price. In addition, the NFR of a high-tech multi-tunnel (WHFC) is twice as sensitive to changes in prices than that of the parral (1668 € Ha⁻¹ year⁻¹ %⁻¹ versus 892 € Ha⁻¹ year⁻¹ %⁻¹, respectively). Consequently, a high tech greenhouse will be more profitable when tomato prices are high and vice versa.

The parral greenhouse

The economic parameters and the PAR transmission of both cover and whitewash had the largest impact on the NFR followed by the NIR and FIR transmission of the cover and the temperature set-point for ventilation (Table 5.7). Based on these results the following recommendations to improve the NFR of the parral– which are in agreement with experimental results – are given: 1) increase the fraction of marketable crop yield and of first class tomatoes, which can be done by making the greenhouse more airtight (López *et al.*, 2001), 2) increase the PAR and NIR transmission of the greenhouse, which can be done by incrementing the cover slope (Soriano *et al.*, 2004) and by washing the greenhouse cover frequently (Montero *et al.*, 1985), 3) use whitewash with a higher PAR transmission and a lower NIR transmission, 4) decrease the FIR transmission of the cover which will increase the plant temperature during night and give a higher crop yield, and 5) increase the temperature set-point for ventilation.

The impact of the side and roof ventilation on NFR was relatively low compared to other design parameters. However, as these parameters can be adjusted more easily than

others, they might be good candidates for adjustment. Perez-Parra *et al.* (2004) already suggested that an increase of the ventilation capacity of a parral would favour crop production, thanks to lower air temperature, higher CO₂ concentration and a lower relative humidity.

Table 5.7 The sensitivity analysis of the economic model states to some economic crop yield parameters, greenhouse design parameters and climate-set-points for the parral greenhouse. The sensitivity values are expressed in € Ha⁻¹ year⁻¹ %⁻¹.

<i>Economic parameter values, Q</i>	Q_{NFR}	$Q_{CropYield}$	Q_{Water}	Q_{Plant}
q_{Tom}	892	991	0	99
η_{FMsold}	837	978	0	141
η_{Tom1}	295	328	0	33
<i>Greenhouse design parameters, P_d</i>				
τ_{RfPAR}	586	811	6	219
$\tau_{ShScrPerPAR}$	107	170	3	60
τ_{RfNIR}	84	116	3	29
τ_{RfFIR}	-70	-94	-1	-23
A_{Side}/A_{Flr}	17	24	1	6
$\tau_{ShScrPerNIR}$	-8	-11	1	-4
A_{Roof}/A_{Flr}	6	9	0	3
<i>Greenhouse climate set-points, U</i>				
$T_{air_vent_on}$	86	100	-4	18

The multitunnel with heating, CO₂ enrichment and fogging

For the WHFC multi-tunnel, the economic parameter inputs, the PAR transmission of the cover and the climate set-points for heating and ventilation had the largest impact on NFR (Table 5.8). Accordingly, the NFR of the WHFC multi-tunnel can be improved by: 1) increasing the PAR transmission of the cover, as described for the parral and 2) decreasing the heating set-point and increasing the ventilation set-point. Furthermore, the NFR was insensitive to the capacities for the heating system, CO₂ enrichment systems and fogging systems indicating that these capacities were sufficient.

Table 5.8 The sensitivity analysis of the economic model states to some economic crop yield parameters, greenhouse design parameters and climate-set-points for the high-tech, WHFC, multi-tunnel. Sensitivity values are in $\text{€ Ha}^{-1} \text{ year}^{-1} \%^{-1}$.

Economic parameter values, Q	Q_{NFR}	$Q_{CropYield}$	Q_{Water}	Q_{CO2}	Q_{Fuel}	Q_{Plant}
q_{Tom}	1668	1854	0	0	0	186
η_{FMsold}	1593	1848	0	0	0	255
η_{TomI}	728	809	0	0	0	81
Greenhouse design parameters, P_d						
τ_{RfPAR}	1067	1422	7	48	-46	346
τ_{RfNIR}	35	-45	4	-16	-57	-11
P_{Boil}	-31	-2	0	0	30	-1
$\tau_{ShScrPerPAR}$	30	55	1	5	0	19
A_{Side}/A_{Flr}	15	35	1	11	0	8
$\tau_{ShScrPerNIR}$	7	7	1	-1	-1	1
A_{Roof}/A_{Flr}	7	9	1	-2	0	3
τ_{RfFIR}	-4	7	-1	3	7	2
ϕ_{ExtCO2}	4	26	0	16	0	6
ϕ_{Fog}	-1	-1	0	0	0	0
Greenhouse climate set-points, U						
$T_{air_boil_on}$	-830	-45	3	-12	808	-14
$T_{air_vent_on}$	339	485	-7	158	-115	110
$T_{out_ThScr_on}$	71	32	0	-3	-44	8
CO_{2Air_ExtMax}	41	95	0	32	0	22
$VP_{Def_Fog_On}$	18	11	-7	-2	0	2
U_{Vent_Max}	14	44	0	19	0	11

The sensitivity results can increase our understanding of the factors influencing the NFR. For instance, an increase of the PAR transmission of the cover by 1% from 54% to 54.54% resulted in a NFR increase of 1067 $\text{€ Ha}^{-1} \text{ year}^{-1}$ which was mainly caused by the extra revenue (1422 $\text{€ Ha}^{-1} \text{ year}^{-1}$) thanks to the effect of an increased photosynthesis rate. This causes plant related variable costs to increase (346 $\text{€ Ha}^{-1} \text{ year}^{-1}$) and the consumption of CO_2 and water (48 and 7 $\text{€ Ha}^{-1} \text{ year}^{-1}$, respectively) as well. In addition, more solar radiation decreased the heating requirement resulting in less fuel costs (-46 $\text{€ Ha}^{-1} \text{ year}^{-1}$). Additionally, the potential of a semi-closed greenhouse under Spanish conditions was demonstrated, since an increase by 1% of the temperature set-point for ventilation resulted in a higher NFR (339 $\text{€ Ha}^{-1} \text{ year}^{-1}$) caused by higher revenue (485 $\text{€ Ha}^{-1} \text{ year}^{-1}$), lower

heating costs ($-115 \text{ € Ha}^{-1} \text{ year}^{-1}$) and lower water costs ($-7 \text{ € Ha}^{-1} \text{ year}^{-1}$). The main cause of the increase in crop yield was the higher CO_2 concentration that could be maintained in the greenhouse.

5.4.2 Impact of outdoor climate and price trajectory on NFR

A change of outdoor climate resulted in another best greenhouse design (Fig. 5.5a), which demonstrates that greenhouse design is a multi-factorial optimisation problem. In more detail, for the ‘cold’ growing cycle of 2008-2009 the best greenhouse design was equipped with all climate modification techniques (WHFC multi-tunnel) whereas for the ‘temperate’ cycles 2006-2007 and 2007-2008 the multi-tunnel equipped with only a fogging system was most profitable. This dependency is expressed by the NFR variance between these different outdoor climate periods which decreased from 1.14 for the parral to 0.08 for the WHFC multi-tunnel. Indeed, it is obvious that the ability to manipulate the inner climate, causes the NFR to be less affected by outdoor conditions, as observed by Castilla and Montero (2008), who suggested that the main advantage of enhanced greenhouse technology could be to add security and stability to the greenhouse production in the Mediterranean area. It was already discussed that the parral can compete with a high-tech multi-tunnel. However, the NFR of a parral depends strongly on outdoor climate (Fig. 5.5), which increases the economic risk of the grower. The sole point of a heating system, therefore, would be to decrease the “weather” risk, and the related chance of negotiating better prices. Similarly, also a change of price trajectory resulted in another best greenhouse design (Fig. 5.5b). In particular, with relatively low tomato prices (2007 – 2008 and 2008 – 2009) the best performing greenhouse was equipped with only a fogging system whereas with relatively high tomato prices (2006-2007) the best greenhouse was equipped with all climate modification techniques. With increasing technology level, the NFR depended thus more on price trajectories, as shown by the NFR variance that increased from 0.18 for the parral to 3.15 for the WHFC multi-tunnel, a trend reflecting the increase in yield. Consequently, a higher price will benefit the NFR of a high-tech greenhouse more than the NFR of a low-tech greenhouse, as shown by Fig. 5.5d. Therefore, in a regime of high price uncertainty a low-tech greenhouse is the best bet, since the NFR depends less on tomato price trajectories than that of a high-tech greenhouse. Finally, a change of both the yearly outdoor climate conditions and price trajectories resulted in even another best design (Fig. 5.5c). In particular, the dependence of NFR on yearly outdoor climate conditions and price trajectories went up with the technology level, which was mainly caused by the high tomato prices in 2006-2007.

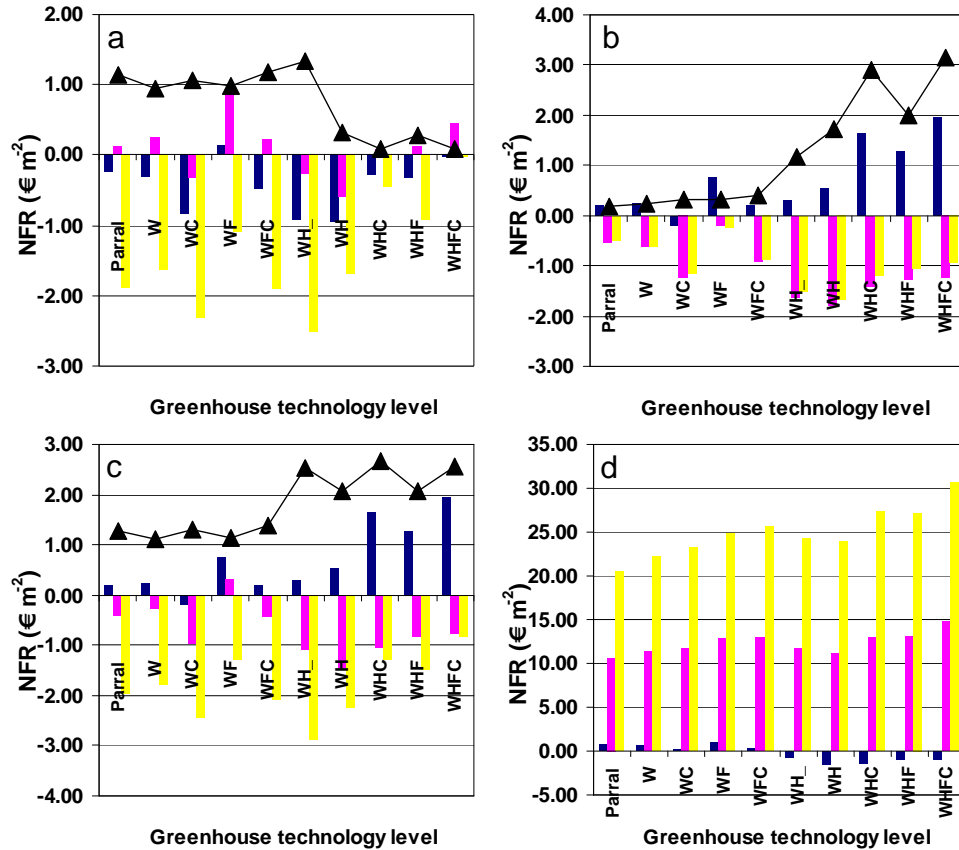


Fig. 5.5 The impact of yearly variations of the outdoor climate (a), the tomato price (b), both the climate and the tomato price (c) and the impact of different constant price trajectories (d) on the net financial result and optimal design.

Fig 5.5a The impact of different outdoor climate periods: 2006 – 2007 (blue), 2007 – 2008 (purple), 2008-2009 (yellow) and the accompanying NFR variance between these different outdoor climate (black line with triangles). The applied price trajectory was the weekly prices averaged over the period 2006-2009.

Fig. 5.5b The impact of different price trajectories: 2006 – 2007 (blue), 2007 – 2008 (purple), 2008-2009 (yellow) and the accompanying NFR variance between these different price trajectories (black line with triangles). The applied outdoor climate was 2006 – 2007.

Fig. 5.5c The impact of different production periods with related outdoor climate and price trajectories: 2006 – 2007 (blue), 2007 – 2008 (purple), 2008-2009 (yellow) and the accompanying NFR variance between these different production periods (black line with triangles).

Fig. 5.5d The impact of different constant price trajectories: 0.50 € kg⁻¹ (blue), 1.00 € kg⁻¹ (purple) and 1.50 € kg⁻¹ (yellow). The applied outdoor climate was 2006 – 2007.

5.5 General discussion

The presented results are discussed with respect to their impact on the development of the model-based greenhouse design method. First the effect on model description is presented, followed by the effect on the greenhouse design optimisation.

5.5.1 Model description

The combined greenhouse climate-crop yield model was already validated in previous studies and demonstrated in this study to predict with fair accuracy the crop yield and resource consumption for Southern Spanish conditions. This combined model was extended here with an economic model and was able to select the most profitable greenhouse design for such conditions. The advantage of this design tool instead of practical experiments is that the NFR of different greenhouse designs can be determined quickly, for different climate years and different price trajectories, with the same assumptions.

However, using a design tool implied that several assumptions had to be made to calculate the NFR for the different greenhouse designs under consideration. Firstly, the fractions of marketable and of first class yield (η_{FMSold} and η_{Tom1} respectively) depend on greenhouse design (Table 5.2) and have a large impact on NFR (Table 5.7 and Table 5.8). The values chosen for these parameters were based on grower experience and on experimental results (Magán *et al.*, 2007) and were assumed to be time invariant, which may be too optimistic. In practice, such fractions depend on diseases, such as blossom end rot (Gázquez *et al.*, 2008) or phytophthora incidence, and extreme fruit temperatures which in turn depend on indoor climate, which follows from weather as much as from greenhouse design. Making these parameters functions of the inner climate would be an improvement, but unfortunately the present knowledge body is far from adequate.

In addition, costs related to the irrigation system, climate computer, emergency power and internal transport system were assumed to be equal for all greenhouse designs in order to compare objectively the impact of greenhouse structure and climate modification techniques on NFR. However, in practice some greenhouses may be equipped with less or cheaper construction elements than others.

5.5.2 Greenhouse design optimisation

In order to limit this study to a “manual design optimisation”, ten alternative designs were selected. However, an enormous amount of greenhouse design and climate management alternatives exists, which demonstrates the need for a more efficient optimisation algorithm. When solving this problem using the model-based design method, four aspects will affect the optimisation result. How to cope with these aspects is discussed shortly hereafter.

First, regarding the large impact of the climate year on the best design, it would be preferable to use one reference climate year that contains the dynamic pattern of climate variables averaged over a long period, as was done by Breuer and Van de Braak (1989) for the Dutch climate. Such a reference year would dispose of the need for calculations with climate data of several years. Second, similarly to the climate reference year, a “reference price trajectory” would be helpful. A word of caution is needed, since the life-span of the optimised greenhouse is in all cases several years. Therefore a good reference period should span much more than one year. As this does not seem feasible, a sensitivity analysis of the NFR of the greenhouse designs to these uncertain input parameters is required. Such an analysis tells how robust the optimal greenhouse design is with respect to uncertain factors such as prices and weather. Third, the combined impact of climate modification techniques on NFR might be larger than the sum of their individual impact as revealed by the joint affect of CO₂ enrichment and heating on NFR (section 5.4.1.1). This result stresses the need to optimise the set of climate modification techniques simultaneously instead of sequentially. Fourth, the sensitivity analysis revealed the considerable impact of climate set-points on NFR (Table 5.8), indicating an effect on the optimal design as well. In a previous study, Vanthoor *et al.* (2008a) indeed have shown that a change in climate management would result in a different optimal greenhouse design which in turn indicates the relevance to select appropriate climate-set-points.

5.6 Conclusion

We have shown that a greenhouse climate-crop yield model, extended with an economic module can be used to select the greenhouse with the highest annual NFR among a predefined set of design alternatives for Southern Spanish conditions and to evaluate possible design improvements of existing greenhouses. Results demonstrated that for the given climatic and economic conditions, a multi-tunnel with only a fogging system would be most profitable ($0.15 \text{ € m}^{-2} \text{ year}^{-1}$). However, the difference in annual NFR between such a structure and a simple parral structure is small ($0.40 \text{ € m}^{-2} \text{ year}^{-1}$) with respect to the big difference in investment (13.32 € m^{-2}), so that the investment pay-back time would exceed the planning horizon of most growers. In addition, it was shown that if one is prepared to invest in a heating system for a multi-tunnel, then it would be certainly worthwhile to fit CO_2 enrichment as well.

A sensitivity analysis of the NFR and related cost factors was carried out to find the factors with the largest bearing on profit at the two extremes: the parral and the multi-tunnel with heating, CO_2 enrichment and fogging. In both cases the tomato price, the fraction of marketable yield and the PAR transmission of the cover had the largest impact on NFR. In addition, the NFR of the low-tech greenhouse would grow with NIR transmission of the cover, with a decrease of the FIR transmission of the cover and with an increase of the temperature set-point for ventilation. On the other hand, the NFR of the high-tech greenhouse would gain by lowering the heating set-point and raising the ventilation set-point.

With respect to sensitivity to uncertain factors, such as weather and prices, we have shown that with increasing technology level, the annual NFR depends less on outdoor climate and more on tomato price. These results indicate that 1) to diminish the risk to fluctuating price trajectories one should operate a low-tech greenhouse with low investments, whereas 2) a high-tech greenhouse would cover better the “weather risk”, which should in turn allow for a higher tomato price. Finally, 3) a high tech greenhouse would be more beneficial at high tomato prices but would suffer more at low price levels.

Our results prove that the best greenhouse design is strongly affected by four factors: weather, price trajectories, joint impact of climate modification techniques, and greenhouse climate management. A model-based design method can cope with these multi-factorial design aspects and is therefore a suitable approach to solve the resulting multi-factorial design problem. Obviously, such design a problem becomes unmanageable as

soon as more alternatives are considered. Therefore, to be more general, the design method must rely on a more efficient algorithm which will be presented in chapter 6.

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5.7 Appendix

Appendix A The calculation of the CO₂ set-point for CO₂ enrichment

The CO₂ set-point increases linearly with global radiation, I_{Glob} , until a defined maximum CO₂ set-point, CO_{2Air_ExtMax} , is reached and, simultaneously, the CO₂ set-point decreases linearly with the aperture of the ventilation openings, U_{Vent}

$$CO_{2Air_ExtOn} = f(I_{Glob}) \cdot g(U_{Vent}) \cdot (CO_{2Air_ExtMax} - CO_{2Air_ExtMin}) + CO_{2Air_ExtMin} \quad [\text{ppm}] \quad (\text{A.1})$$

$$f(I_{Glob}) = \begin{cases} \frac{I_{Glob}}{I_{Glob_Max}}, & I_{Glob} < I_{Glob_Max} \\ 1, & I_{Glob} \geq I_{Glob_Max} \end{cases} \quad [-] \quad (\text{A.2})$$

$$g(U_{Vent}) = \begin{cases} 1 - \frac{U_{Vent}}{U_{Vent_Max}}, & U_{Vent} < U_{Vent_Max} \\ 0, & U_{Vent} \geq U_{Vent_Max} \end{cases} \quad [-] \quad (\text{A.3})$$

where I_{Glob} (W m⁻²) is the outdoor global radiation, U_{Vent} (-) is the window aperture, CO_{2Air_ExtMax} (ppm) is the maximum CO₂ concentration set-point, CO_{2Air_ExtMin} is the minimum CO₂ concentration set-point (ppm), I_{Glob_Max} (W m⁻²) is the outdoor global radiation at which the maximum CO₂ concentration set-point could be reached and U_{Vent_Max} (-) is the window aperture at which the CO₂ concentration set-point equals the minimum CO₂ concentration set-point (ppm).

Chapter 6

Greenhouse design optimisation for Southern-Spanish and Dutch conditions

The contents of this chapter have been submitted to Biosystems Engineering as a paper entitled: *A methodology for model-based greenhouse design: Part 5, Greenhouse design optimisation for Southern-Spanish and Dutch conditions.*

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6.1 Abstract

An optimisation algorithm, as an essential part of a model-based method to design greenhouses for a broad range of climatic and economic conditions was described. This algorithm—a modified controlled random search using parallel computing—maximised the annual Net Financial Return (NFR) of a tomato grower by selecting the best alternative to fulfil the following eight design elements: type of greenhouse structure, material of the cover, outdoor shade screen, whitewash properties, thermal screen, heating system, cooling system and a CO₂ enrichment system. As an example, the algorithm was applied to two locations with different climatic and economic conditions, i.e. Almeria and The Netherlands. Due to the warm climate with high radiation levels in Almeria, a greenhouse with a relatively large specific ventilation area (20% compared to 14% for Dutch conditions), seasonal whitewash and a low-capacity direct air heater (50 W m⁻² compared to 200 W m⁻² for Dutch conditions) was selected. In contrast, for the relatively cold climate with low radiation levels of The Netherlands, a 100% aluminium thermal screen and no whitewash would give the best result. The design method produced realistic greenhouses and related annual NFR, indicating that the method performs well. An analysis of the close-to-best greenhouses showed that for both locations a structure with high light transmissivity considerably enhanced the greenhouse performance whereas an outdoor shade screen, geothermal heating and mechanical cooling would be not economical. These results demonstrate the feasibility of a model-based design approach that produces suitable greenhouse designs for given climatic and economic conditions.

6.2 Introduction

When the current state in greenhouse design is considered, most studies have focused on optimising the design for a specific location, or they considered only a single design parameter. Specifically, Engel (1984) has optimised step by step the roof geometry, insulation level and the size of the heat storage of an energy passive greenhouse for use in the Southern California area; Amir and Hasegawa (1989) optimised the structural design of a greenhouse with respect to mechanical properties and Kacira *et al.* (2004) have optimised the vent configuration. However, for strategic decision making of greenhouse configuration for world-wide climate conditions, a systematic approach that integrates physical, biological and economical models is the most promising way as suggested by Baille (1999). Therefore, we describe in this study an optimisation algorithm, as an essential part of a model-based method to design greenhouses. The optimisation aims to maximise the annual net financial result by modifying the greenhouse design. The design method focuses to select the best alternative to fulfil the following eight design elements: (i) the type of a greenhouse structure, (ii) the material of the cover, (iii) the presence and type of an outdoor shading screen, (iv) the presence of a whitewash and its properties, (v) the presence and type of a thermal screen, (vi) the type of a heating system and its capacity, (vii) the type of a cooling system and its capacity and (viii) the type of a CO₂ enrichment system and its capacity.

The aim of this study is to integrate an optimisation algorithm into the model-based design method to select the best set of greenhouse design elements from of a large number of alternatives. To demonstrate the feasibility of this approach, the greenhouse design is optimised for two different locations: Almeria, Spain and De Bilt, The Netherlands. The chapter is organised as follows. First, a description of the optimisation problem is presented. Second, an optimisation algorithm is selected and briefly discussed. Third, the assumptions for the Spanish and Dutch optimisation studies are presented. Fourth, the optimisation results are presented and discussed with respect to literature results.

6.3 Material and method

6.3.1 Description of the optimisation problem

6.3.1.1 Model overview

An overview of the design method is shown in chapter 1. The greenhouse climate model is described in chapter 2, the crop yield model in chapter 3, and the economical model in chapter 5. Therefore only a concise description of these models is presented here.

The various models consist of a set of differential equations:

$$\dot{X} = f(X, U, D, P, t) \quad [-] \quad (6.1)$$

where X is the state vector containing the indoor climate variables, the crop variables and the resource consumption variables, \dot{X} denotes the derivative of the state vector with respect to time, U is the climate control vector containing the climate control valve settings, D is the outdoor climate vector, P is the model parameter vector and t (s) is time.

6.3.1.2 The integer greenhouse design vector

This optimisation focuses on the following eight design elements: (i) the type of a greenhouse structure, (ii) the material of the cover, (iii) the presence and type of an outdoor shading screen, (iv) the presence of a whitewash and its properties, (v) the presence and type of a thermal screen, (vi) the type of a heating system and its capacity, (vii) the type of a cooling system and its capacity and (viii) the type of a CO₂ enrichment system and its capacity (Fig. 6.1).

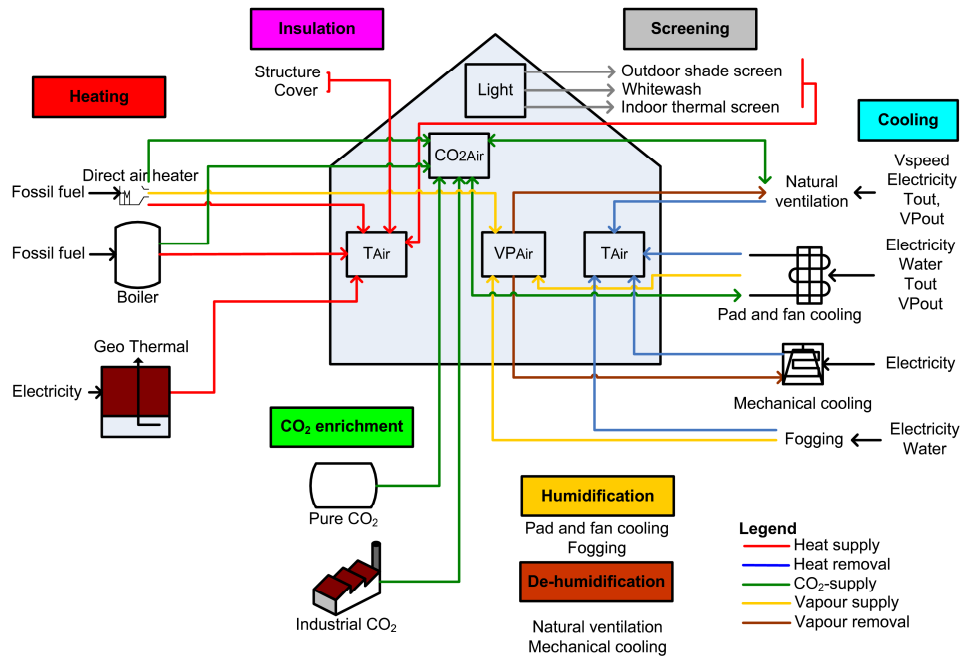


Fig. 6.1 Functions (coloured boxes) and design elements (text blocks and pictures below the accompanying functions) used to manage the greenhouse climate (transparent boxes inside the greenhouse). The coloured arrows represent the various energy and mass fluxes (legend at the bottom right). The selection of alternatives to fulfil the following eight design elements: the type of greenhouse structure, the cover type, the outdoor shade screen, the whitewash, the thermal screen, the heating system, the cooling system and the CO₂ enrichment system.

To optimise this set of design elements, an integer greenhouse design vector as shown in Fig. 6.2a was defined, which consists of eight design elements:

$$I = \{e_1, e_2, \dots, e_8\} \quad \text{with } 1 \leq e_j \leq n_e^j \text{ and } j = 1, 2, \dots, 8 \quad [-] \quad (6.2)$$

where each design element is denoted by an integer design variable e_j that can be fulfilled by n_e^j alternatives as described in Table 6.1. For example, the particular realisation of the integer greenhouse design vector as presented in Fig. 6.2b is thus represented as:

$$I = \{2, 1, 1, 2, 5, 3, 4, 1\} \quad [-] \quad (6.3)$$

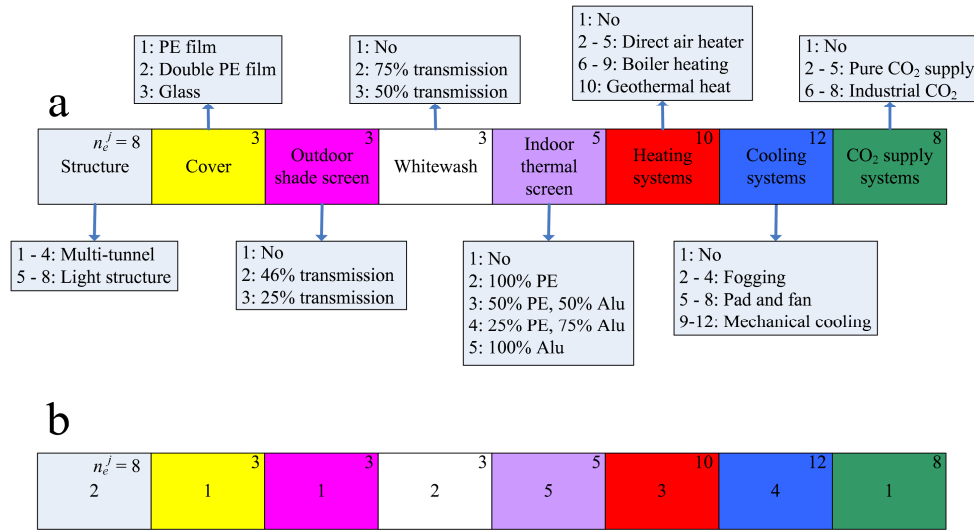


Fig. 6.2 An overview of the integer greenhouse design vector (a) with an example (b). Fig. 6.2a Each coloured box represents a design element that could be executed by several alternatives as presented in the light-blue boxes. The number of alternatives to fulfil a design element n_e^j , is presented in the upright corner of coloured boxes. Fig. 6.2b An example of a integer greenhouse vector which can be interpreted using Table 6.1 and represents: a multi-tunnel structure type 2 covered with a PE film and equipped with: no outdoor shade screen, a seasonable whitewash with a transmission of 75%, a 100% aluminium thermal screen, a direct air heater with a capacity of 1.0 MW, a fogging system with a capacity of 600 g m⁻² h⁻¹ and no CO₂ enrichment. Detailed information about the specific properties and/or capacities of the design elements is presented in Table 6.1.

From Fig. 6.2 and Table 6.1 it can be inferred that this integer vector presents a multi-tunnel structure type 2 covered with a PE film and equipped with: no outdoor shade screen, a seasonal whitewash with a transmission of 75%, a 100% aluminium thermal screen, a direct air heater with a capacity of 1.0 MW (equivalent to 100 W m⁻²), a fogging system with a capacity of 600 g m⁻² h⁻¹ and no CO₂ enrichment.

Table 6.1 The economic parameters needed to determine the annual costs of the maintenance and depreciation for all design elements as described in chapter 5: the investments $q_{Invest,i}$ the depreciation $\eta_{Depreciation,i}$ and the maintenance $\eta_{Maintenance,i}$

Design element	e_j	$q_{Invest,i}$ € m ⁻²	$q_{Invest,i}$ €	$\eta_{Depreciation,i}$ % year ⁻¹	$\eta_{Maintenance,i}$ % year ⁻¹	$Q_{Constr,i}$ € m ⁻² year ⁻¹
<i>Structure (j=1)</i>						
Multi-tunnel 1Ha, 0% Vent	1	15.00		7.0	2.0	1.35
Multi-tunnel 1Ha, 29% Vent	2	18.00		7.0	2.0	1.62
Multi-tunnel 1Ha, 45% Vent	3	21.30		7.0	2.0	1.92
Multi-tunnel 1Ha, 77% Vent	4	30.14		7.0	2.0	2.71
Venlo 1Ha, 0% Vent	5	29.00		7.0	0.5	2.18
Venlo 1Ha, 14% Vent	6	32.00		7.0	0.5	2.40
Venlo 1Ha, 20% Vent	7	33.25		7.0	0.5	2.49
Venlo 1Ha, 38% Vent	8	47.50		7.0	0.5	3.56
<i>Covers (j=2)</i>						
PE Film, Spain	1	1.38		33.3	5.0	0.53
PE Film, Netherlands	1	4.00		12.5	5.0	0.70
Double PE film, Spain	2	2.38		33.3	5.0	0.91
Double PE film, Netherlands	2	5.00		12.5	5.0	0.88
Glass	3	5.00		7.0	0.5	0.38
<i>Outdoor shade screen (j=3)</i>						
No	1	0.00		0	0	0
OLS 50 Abri, 46% transmission	2	3.81		20.0	5.0	0.95
OLS 70 Abri, 25% transmission	3	3.97		20.0	5.0	0.99
Structure shade screen		13.30		10.0	5.0	2.00
<i>Whitewash (j=4)</i>						
No	1	0.00		0	0	0
Whitewash 75% tr Spain	2	0.07		100.0	0	0.07
Whitewash 75% tr Neth	2	0.80		100.0	0	0.80
Whitewash 50% tr Spain	3	0.09		100.0	0	0.09
Whitewash 50% tr Neth	3	0.82		100.0	0	0.82
<i>Indoor thermal screen (j=5)</i>						
No	1	0.00		0	0	0
100 % PE	2	1.50		20.0	5.0	0.38
50% Aluminium/50 % PE	3	4.06		20.0	5.0	1.02
75% Aluminium/25 % PE	4	4.24		20.0	5.0	1.06
100% Aluminum	5	5.58		20.0	5.0	1.40
Structure thermal screen		2.97		10.0	5.0	0.45
<i>Heating systems (j=6)</i>						
No	1		0	0	0	0

Design element	e_j	$q_{Invest,i}$ € m ⁻²	$q_{Invest,i}$ €	$\eta_{Depreciation,i}$ % year ⁻¹	$\eta_{Maintenance,i}$ % year ⁻¹	$Q_{Constr,i}$ € m ⁻² year ⁻¹
Direct air heater: 0.5 MW	2		16725	15.0	2.5	0.29
Direct air heater: 1 MW	3		29225	15.0	2.5	0.51
Direct air heater: 1.5 MW	4		44850	15.0	2.5	0.78
Direct air heater: 2 MW	5		57350	15.0	2.5	1.00
Boiler: 1.16 MW	6		60000	7.0	1.0	0.48
Boiler: 1.74 MW	7		66000	7.0	1.0	0.53
Boiler: 2.32 MW	8		80400	7.0	1.0	0.64
Boiler: 3.48 MW	9		92400	7.0	1.0	0.74
Geothermal 7 MW	10		6000000	4.0	5.0	54.00
Heating pipes, 1 pipe per m		5.45		7.0	0.5	0.41
<i>Cooling systems (j=7)</i>						
No	1			0	0	0
Fogging: 200 g m ⁻² h ⁻¹	2	5.50		10.0	5	0.83
Fogging: 400 g m ⁻² h ⁻¹	3	7.00		10.0	5.0	1.05
Fogging: 600 g m ⁻² h ⁻¹	4	10.00		10.0	5.0	1.50
Pad and fan: 50 m ³ m ⁻² h ⁻¹	5	3.54		10.0	5.0	0.53
Pad and fan: 100 m ³ m ⁻² h ⁻¹	6	5.07		10.0	5.0	0.76
Pad and fan: 150 m ³ m ⁻² h ⁻¹	7	6.60		10.0	5.0	0.99
Pad and fan: 200 m ³ m ⁻² h ⁻¹	8	8.14		10.0	5.0	1.22
Mechanical cool: 0.5 MWe/unit	9		240000	7.0	2.0	2.16
Mechanical cool: 1 MWe/unit	10		480000	7.0	2.0	4.32
Mechanical cool: 1.5 MWe/unit	11		720000	7.0	2.0	6.48
Mechanical cool: 2 MWe/unit	12		960000	7.0	2.0	8.64
<i>CO₂ supply (j=8)</i>						
No	1		0	0.0	0	0
Pure supply: 50 kg Ha ⁻¹ h ⁻¹	2		3120	10.0	0	0.03
Pure supply: 100 kg Ha ⁻¹ h ⁻¹	3		3120	10.0	0	0.03
Pure supply: 150 kg Ha ⁻¹ h ⁻¹	4		4320	10.0	0	0.04
Pure supply: 200 kg Ha ⁻¹ h ⁻¹	5		4320	10.0	0	0.04
Industrial CO ₂ : 100 kg Ha ⁻¹ h ⁻¹	6		20000	6.7	2.0	0.17
Industrial CO ₂ : 150 kg Ha ⁻¹ h ⁻¹	7		21000	6.7	2.0	0.18
Industrial CO ₂ : 200 kg Ha ⁻¹ h ⁻¹	8		22000	6.7	2.0	0.19
CO ₂ distribution system		0.34		10.0	5.0	0.05
Remaining costs for irrigation, crop protection, internal transport, sorting, packaging etc.						
Spain		11.13		10.0	5.0	1.67
The Netherlands		38.73		10.0	5.0	5.81

6.3.1.3 Performance measure

The performance measure to be maximised is the expected annual net financial result (NFR) of the grower, described by:

$$\max_t J(t_f) = -Q_{Fixed} + \int_{t=t_0}^{t=t_f} \dot{Q}_{CropYield} - \dot{Q}_{Var} dt \quad [\text{€ m}^{-2} \text{ year}^{-1}] \quad (6.4)$$

where J ($\text{€ m}^{-2} \text{ year}^{-1}$) is the annual net financial result of the grower, t_0 (s) and t_f (s) are the beginning and the end of the production period respectively, Q_{Fixed} ($\text{€ m}^{-2} \text{ year}^{-1}$) are the fixed costs related to the tangible assets, $Q_{CropYield}$ ($\text{€ m}^{-2} \text{ year}^{-1}$) is the economic value of crop yield, Q_{Var} ($\text{€ m}^{-2} \text{ year}^{-1}$) are the costs related to the crop (i.e. plant material, fertilisers, crop protection and other crop assets), resource use (in this study defined as water, CO₂, fossil fuel and electricity) and labour. A more detailed description of the individual cost elements can be found in chapter 5. Labour costs consisted of fixed cost related to crop maintenance plus a fraction that was linearly related to crop yield. The cost of the use of individual resources was calculated with:

$$\dot{Q}_{Water} = 10^{-3} q_{Water} \left(\left(1 + \frac{\eta_{Drain}}{100} \right) MV_{CanAir} + MV_{FogAir} + MV_{PadAirNet} \right) [\text{€ m}^{-2} \text{ s}^{-1}] \quad (6.5)$$

$$\dot{Q}_{CO_2} = 10^{-6} (q_{CO_2_Ext} MC_{ExtAir} + q_{CO_2_Ind} MC_{IndAir}) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (6.6)$$

$$\dot{Q}_{Fuel} = \frac{q_{Fuel}}{\eta_{Fuel}} (H_{BoilPipe} + H_{BlowAir}) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (6.7)$$

$$\dot{Q}_{Elec} = \frac{q_{Elec}}{3.6 \cdot 10^6} (P_{Pad} + P_{Fog} + P_{Geo} + P_{Mech}) \quad [\text{€ m}^{-2} \text{ s}^{-1}] \quad (6.8)$$

where q_{Water} (€ m^{-3}) is the water price, η_{Drain} (%) is a fraction of crop transpiration needs to assure sufficient irrigation, MV_{CanAir} ($\text{kg m}^{-2} \text{ s}^{-1}$) is the transpiration rate of the crop, MV_{FogAir} ($\text{kg m}^{-2} \text{ s}^{-1}$) is the fogging rate, $MV_{PadAirNet}$ ($\text{kg m}^{-2} \text{ s}^{-1}$) is the water added to the inlet air of the pad and fan system, $q_{CO_2_Ext}$ (€ kg^{-1}) is the price of pure CO₂, MC_{ExtAir} ($\text{mg m}^{-2} \text{ s}^{-1}$) is the CO₂ enrichment rate of pure CO₂, $q_{CO_2_Ind}$ (€ kg^{-1}) is the price of industrial CO₂, MC_{IndAir} ($\text{mg m}^{-2} \text{ s}^{-1}$) is the CO₂ enrichment rate of industrial CO₂, q_{Fuel} (€ m^{-3}) is the fuel price, η_{Fuel} (J m^{-3}) is the energy efficiency of the fuel, $H_{BoilPipe}$ (W m^{-2}) is the heat supply to the heating pipes, $H_{BlowAir}$ (W m^{-2}) is the heat supply from the indirect air heater to the greenhouse air, q_{Elec} is the electricity price (€ kWh^{-1}), P_{Pad} , P_{Fog} , P_{Geo} and

P_{Mech} , is the electricity consumption of the pad and fan system, the fogging system, the pump of the geothermal source and the mechanical cooling system respectively. Calculation of electricity consumption rates is presented in section 6.6.1.

6.3.1.4 Impact of extreme humidity levels on tomato quality parameters

As presented in chapter 5 the economic crop yield is described as a function of crop yield mass and two quality parameters i.e. the fraction of first class tomatoes and the marketable fraction. A description of the impact of indoor climate on these quality parameters was not integrated in the design method. Therefore, as a first approach two quality filters were developed to describe the impact of humidity on the marketable fraction and fraction of first class tomatoes. These quality filters were based on real climate data and quality parameters as described in section 6.6.2.

6.3.2 The controlled random search optimisation algorithm

6.3.2.1 Description and implementation of the algorithm

The controlled random search (CRS) method of Price (1977) was used to solve the optimisation problem. Such a derivative-free global optimisation method was required because the performance measure will have many local maxima and its gradient is not continuous. In addition, the CRS allows efficient parallel computing, it is easy to implement, it is a robust optimisation method and there is no need to fine-tune many algorithm parameters. Because of the time needed to solve the optimisation problem (Table 6.2), a solution based on parallel computing is needed to achieve manageable CPU times. Furthermore, due to its population-based nature, the output of the CRS method produces valuable information about the close-to-best designs.

Table 6.2 The number of design alternatives, time needed to evaluate all design alternatives and the time needed for design optimisation under constrained and unconstrained conditions.

Location	Number of design alternatives	Years needed to evaluate all design alternatives by one computer ⁺	Days needed for parallel optimisation [*]
Spain	$5.40 \cdot 10^5$	26	2
Netherland	$8.64 \cdot 10^5$	41	3

The ⁺ indicates that a single simulation time of 25 minutes was assumed.

The ^{*} indicates parallel optimisation with 50 computers and an optimisation algorithm that evaluates at most 1% of all design alternatives to come up with a solution. For the Spanish case fewer designs were evaluated because the CO₂ supply from industry was not optimised.

The original CRS method of Price (1977) iteratively improves a candidate population A of best guesses for a number of continuous design parameters. This population consists of N continuous design vectors constituting each of n continuous design variables and the accompanying performance measure values. After each iteration, a new design vector I , is created based on A and the performance measure J_I is evaluated. If J_I is higher than the lowest performance measure value in A , the design vector associated to the lowest performance measure is replaced by I and the lowest performance measure value is replaced by J_I .

The original CRS was developed for continuous optimisation problems whereas the greenhouse design optimisation is approached as an integer based problem. However, according to Lampinen and Zelinka (1999), population-based methods developed for continuous problems could solve discrete optimisation problems provided that the discrete parameters are represented as floating point values even when the problem is inherently discrete. The performance measure is thus evaluated once the floating-point parameter values are rounded to, but not overwritten by, their nearest allowable discrete values (Price *et al.*, 2005). The original CRS algorithm was thus modified to assure that the integer design problem was efficiently solved. In addition, to speed up the optimisation process, a new design vector could only be evaluated once by the model. Specifically, only design vectors which are not stored in population A , nor in the memory stack B will be evaluated. A detailed description of the modified CRS algorithm is presented as software steps below:

Steps 1 to 3 are performed to initialise the optimisation parameters

1. Define N , the number of design vectors. Price (1983) proposed N as a function of the total number of $n=8$ design variables: $N=25n$.
2. Choose randomly N sets of n design variables over the search domain V and store the design vectors in the first n columns of the $N \times (n+1)$ population matrix A .
3. Initialise $Counter = 0$ and the memory stack B as an empty $1 \times (n+1)$ vector. The memory stack B is used to store the evaluated design vectors and accompanying performance measures.
4. Initialise the maximum number of iterations $Counter_{Max}$.

Steps 4 to 8 determine the performance measure value for each individual in the population A .

5. Update the variable counter: $Counter = Counter + 1$
6. If $Counter \leq N$, proceed with step 7. If $Counter > N$, go to step 8.

7. Obtain the design vector I , located at row number $Counter$ of matrix A . Determine J_I , the value of the performance measure of I and store J_I in the common matrix A at row number $Counter$ and column number $n+1$. Proceed with step 5.

These steps are performed to improve the population A

8. Choose randomly $n + 1$ distinct sets of the design vectors R_1, R_2, \dots, R_{n+1} from the population A. Determine the centroid G of the points R_1, \dots, R_n . Then determine the next design vector I such that $\bar{I} = 2\bar{G} - \bar{R}_{n+1}$. Where $\bar{I}, \bar{G}, \bar{R}_{n+1}$ represent the position vectors in the n -space.
9. Round I to the nearest allowed integer values so that the quantified I_q is obtained. Keep the original I in the floating-point parameter domain.
10. Is I_q consistent with the constraints? If not go to step 8, if so, proceed with step 11.
11. Update the variable counter: $Counter = Counter + 1$
12. Exist I_q in the quantified population matrix A_q or in the memory stack B ? If not, proceed with step 13, if so, obtain J_{I_q} from A or B and go to step 14.
13. Evaluate the performance measure to determine J_{I_q} , the value of the performance measure at I_q .
14. Determine from A the design vector, L , which has the lowest performance measure value J_L .
15. If $J_{I_q} \leq J_L$, proceed with step 16. If $J_{I_q} > J_L$, go to step 17.
16. Store I_q and J_{I_q} in the B matrix. Is $Counter \geq Counter_{Max}$? If so, maximum number of iterations reached and exit optimisation algorithm. If not, go to step 8.
17. Replace in A , the design vector L by I and the performance measure J_L by J_{I_q} . Thus I and not I_q is stored in A as recommended by Lampinen and Zelinka (1999) and Price *et al.* (2005). Store the quantified design vector I_q and its performance measure J_L in B .
18. Is $Counter \geq Counter_{Max}$? If so, maximum number of iterations reached. If not, go to step 8.

This modified CRS algorithm was implemented in a parallel processing program that used 50 personal computers (each equipped with a 3000 MHz Intel core 2 DUO processor with 2 GB internal memory). These computers could simultaneously: read N and $Counter_{Max}$; read and write the matrices A , B and the $Counter$ variable. Each computer evaluated a particular performance measure by solving the differential equations of the model with a variable time step ODE solver as included in Matlab 7.1[®]. After each evaluation, the common variables and matrices were modified, a new greenhouse design was determined as described by the modified CRS algorithm and this design was evaluated. All greenhouse design evaluations in the parallel computation process were synchronised in time as to guarantee an objective search. The number of integer design vectors in the population matrix A was set to $N = 250$ which was larger than Price's (1983) proposition of $N=25 \cdot 8=200$ as to increase the probability that a global maximum was found. Based on the consistent convergence of the performance measure during optimisation, the maximum number of iterations $Counter_{Max}$ was set to 7500.

6.3.2.2 Analysis of the results of an optimisation run

As the CRS method is a population-based optimisation method, the exit-population offers interesting additional insights. The population of greenhouse designs can be evaluated using distribution curves and sensitivity analysis techniques.

The distribution curves show for the set of close-to-best greenhouse designs the frequency of all alternatives to fulfil each design element. In this study, the set of close-to-best greenhouse designs consisted of greenhouses for which the NFR differed less than $X \text{ € m}^{-2} \text{ year}^{-1}$ compared to the NFR of the best greenhouse (in this chapter denoted with $\Delta NFR < X \text{ € m}^{-2} \text{ year}^{-1}$). The frequency of each alternative was expressed in % of the resulting population size. In this study the distribution curves of the design elements were determined for two sets of best greenhouses, i.e. $\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$ and $\Delta NFR < 1.50 \text{ € m}^{-2} \text{ year}^{-1}$.

The sensitivity analysis shows the impact of all alternatives to fulfil each design element. The sensitivity was defined as follows. For each alternative, a sub-population was created that existed of only designs equipped with this specific alternative. Subsequently, the mean of the NFR of this sub-population was determined and shown in the sensitivity analysis. When evaluating the impact of one alternative, the other alternatives to fulfil the remaining seven design elements were thus allowed to vary. This single-variate analysis was used to reduce complexity when analysing the optimisation results.

6.3.3 Two cases: Almeria, Spain and De Bilt, The Netherlands

To demonstrate how the optimised design depends on local climate and economic conditions, two locations were selected: Almeria, Spain and De Bilt, The Netherlands. In this section, the assumptions underlying the optimisation study are presented. This includes the greenhouse design elements, crop conditions, outdoor climate, climate management and economic parameters.

6.3.3.1 Greenhouse design description

A long tomato growing period was used for both locations: in Almeria from August 1st to July 1st and in De Bilt from December 15th to December 1st. For both locations the standard climate year was used as described in section 6.3.3.2 and the crop conditions are described in Table 6.3. Both greenhouses were assumed to have a rectangular shape of 200 x 50 m resulting in a floor area of 1Ha.

An overview of the set of eight greenhouse design elements to be optimised and their accompanying economic parameters are presented in Table 6.1. For both locations, the same possible design alternatives were considered with the exception that CO₂ enrichment from an industrial source was not considered possible in Spain. The two possible greenhouse structures were: a cheap structure with a relatively low light transmissivity of 71% (such as an iron arch-shaped multitunnel) and a more expensive structure with a higher light transmissivity of 95% (such as a Venlo-type structure). Note that the overall greenhouse transmission depends also on cover type, whitewash, and light absorbing design elements such as structures to mount the indoor and outdoor screen. Both structures could be coupled to four different specific ventilation areas. The structure with the low light-transmissivity had side ventilation in the 2 long sides and continuous roof ventilation in one side of each span. This structure could only be covered with a film. The structure with the high light-transmissivity had only roof ventilation.

The possible greenhouse cover materials were: a single PE film, a double PE film and a single glass cover. For the movable outdoor shade screen and for the whitewash, several alternatives with different light transmission could be selected. For the movable indoor thermal screen there were several alternatives with different ratios of aluminium and PE (influencing the far infrared radiation fluxes). For the heating system, a number of capacities, including zero, of a direct air heater, a boiler and geothermal heat could be selected. A direct air heater supplies heat, CO₂ and the water vapour directly to the greenhouse air, whereas a boiler and a geothermal source both supply heat to the heating pipes, which, in turn, heat up the greenhouse air by convective heat exchange and radiation.

The boiler system had lower investment costs and higher variable costs compared to the geothermal source. The CO₂ produced by the boiler is also supplied to the greenhouse air. The source to supply CO₂ to the greenhouse could be selected between pure CO₂ from a tank and industrial waste CO₂, all with a number of capacities. At equal capacity, pure CO₂ supply had lower investments cost and higher variable costs than industrial CO₂. The possible cooling systems were: high-pressure fogging; pad and fan and mechanical cooling, all possible with a number of capacities.

A commonly encountered growing system was selected for each location. In Almeria, plants were assumed to grow in soil whereas in The Netherlands plants were grown in substrate above a white foil. Therefore, the reflection coefficient for visible light of the floor layer was higher in The Netherlands than in Spain. A closed irrigation system with disinfection unit was used in The Netherlands which resulted, compared to Spain, in a lower fraction of crop transpiration needs to assure sufficient irrigation.

6.3.3.2 Local climate

Variations between different outdoor climate years have a significant impact on the NFR as demonstrated in chapter 5. Therefore, a standard climate year representing long term climate data was created using the algorithm based on Breuer and Van de Braak (1989) as presented in section 6.6.3. This algorithm selects from the long term series climate data, each single month with the closest match to the mean monthly values of temperature and global radiation sums. Spanish climate data of the period 2004 – 2009 and Dutch climate data of the period 1989 – 2009 were used to determine such standard climate years. Fig. 6.3 presents the monthly mean values of the daily global radiation as a function of monthly mean outdoor temperature for Almeria and for De Bilt.

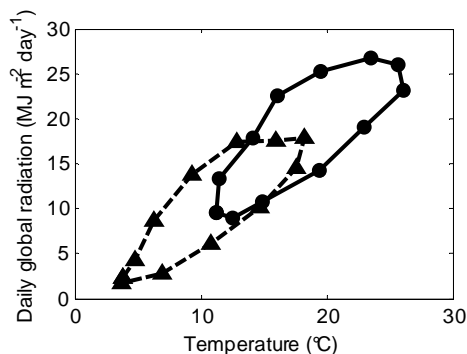


Fig. 6.3 The monthly mean values of the daily global radiation as a function of the monthly mean outdoor temperature for Almeria (solid line with circles) and for De Bilt (dashed line with triangles).

6.3.3.3 Greenhouse climate management

The climate control valve settings are determined as a function of the climate control strategy and the applied climate set-points. For both locations the same greenhouse climate set-points were used, as presented in Table 6.3, to ensure that differences between optimisation results were only caused by climatic and economic conditions. However, the period for which a seasonal whitewash could be applied was longer in Spain than in The Netherlands. The strategy for controlling the air temperature is presented in Fig. 6.4. The set point for CO₂ enrichment CO_{2Air_ExtOn} , increased with increasing outside global radiation and decreased with increasing ventilation rate which was based on Magán *et al.* (2008) as described in section 6.6.4. The outdoor shade screen was used when the outdoor global radiation was higher than $I_{glob_ShScr_on}$.

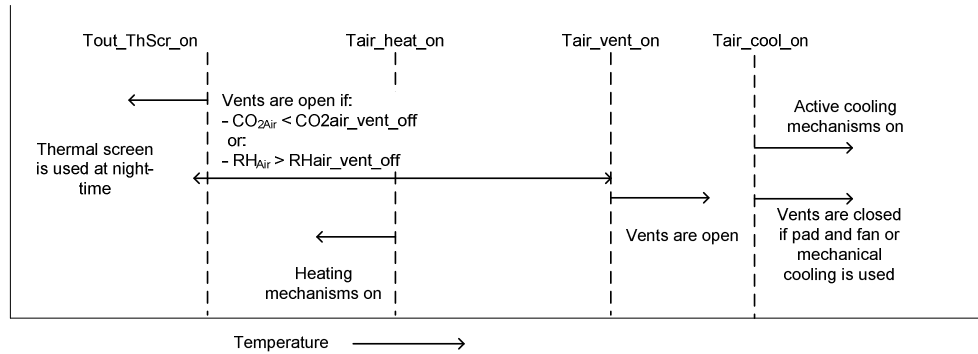


Fig. 6.4 The greenhouse temperature control strategy based upon climate set-points. Values of the climate set-points are listed in Table 6.3.

6.3.3.4 Economic conditions

The performance measure was calculated using the equations presented in chapter 5 and section 6.3.1.3. The economic parameters needed to determine the annual fixed costs related to the tangible assets are presented in Table 6.1. Similar costs for the tangible assets were used for the two locations, except for the films and the whitewash, for which the investments costs were higher in The Netherlands than in Spain. Since different growing systems were used, each location had different remaining costs. The economic parameters to determine the variable costs are presented in Table 6.4. For Almeria, the weekly tomato price of the first and second class long life tomatoes (Anonymous, 2009) were averaged over four successive production periods between 2006 and 2010. For Dutch conditions, the 4 week period price of the first and second class truss tomatoes of Vermeulen (2010) were averaged over four successive years i.e. 2006 – 2009.

Table 6.3 Overview of the outdoor climate, the greenhouse climate management and the crop conditions used for the greenhouse design optimisation.

	Almeria, Spain	De Bilt, The Netherlands
<i>Greenhouse climate management</i>		
	August 1 st – September 15 th (full whitewash)	June 1 st – August 15 th (50 % whitewash)
<i>Whitewash</i>	March 1 st – April 15 th (50 % whitewash)	
	April 16 th – June 30 th (full whitewash)	
$I_{glob_ShScr_on}$ ($W\ m^{-2}$)	650	650
$T_{air_vent_on}$ ($^{\circ}C$)	24	24
$RH_{air_vent_on}$ (%)	85	85
$CO_{2air_vent_min}$ (ppm)	200	200
$CO_{2air_vent_max}$ (ppm)	3000	3000
$T_{air_heat_on}$ ($^{\circ}C$) (night/day)	17/19	17/19
$T_{air_cool_on}$ ($^{\circ}C$)	26	26
$T_{out_ThScr_on}$ ($^{\circ}C$)	14	14
CO_{2Air_ExtMax} (ppm)	1000	1000
CO_{2Air_ExtMin} (ppm)	390	390
I_{Glob_Max} ($W\ m^{-2}$)	500	500
$f_{VentExtCO2_Max}$ ($m^3\ m^{-2}\ s^{-1}$)	$6.95 \cdot 10^{-3}$	$6.95 \cdot 10^{-3}$
$CO_{2air_ExtCO2_on}$ (ppm)	Function of global radiation and ventilation rate	Function of global radiation and ventilation rate
<i>Crop conditions</i>		
LAI_start	0.3	0.3
LAI_max	2.5	2.5
Start growing period, t_0	August 1 st	December 15 th
End growing period, t_f	July 1 th	December 1 st

Table 6.4 An overview of the costs-related variables used in this study

Parameter explanation	Parameter	Unit	Almeria	Source	De Bilt	Source
The average conversion factor from tomato dry matter to fresh matter	η_{DMFM}	kg mg ⁻¹	15.95·10 ⁻⁶	Based on Magán <i>et al.</i> (2008)	18.18·10 ⁻⁶	Based on practice
A fraction of crop transpiration needs to assure sufficient irrigation	η_{Drain}	%	30	Based on practice	0	Closed system
Marketable fraction of harvest	η_{FMsold}	-	-	Function of indoor climate	-	Function of indoor climate
Energy content of gas	η_{Fuel}	J m ⁻³	31.65·10 ⁶	Known	31.65·10 ⁶	Known
Interest rate	$\eta_{Interest}$	%	3.5	Cajamar	5	Vermeulen (2008)
The cost of short-term borrowing	$\eta_{Interest_Short}$	%	1	Cajamar	1	Vermeulen (2008)
The labour cost coefficient that describes impact of the production level on labour cost	η_{Labour_kg}	h kg ⁻¹ FM	0.010	Based on Pérez <i>et al.</i> (2003)	0.0043	Vermeulen (2008)
The labour cost coefficient that describes the impact of plant related labour (no harvest) on variable labour cost	η_{Labour_m2}	h m ⁻²	0.270	Based on Pérez <i>et al.</i> (2003)	0.825	Vermeulen (2008)
The annual maintenance cost coefficient of design element <i>i</i>	$\eta_{Maintenance,i}$	% year ⁻¹	-	See Table 6.1	-	See Table 6.1
The annual depreciation coefficient of design element <i>i</i> .	$\eta_{Depreciation,i}$	% year ⁻¹	-	See Table 6.1	-	See Table 6.1
The material costs for packaging	$\eta_{Package}$	€ kg ⁻¹	0	Part of sales cost	0.009	Vermeulen (2008)
The unaccounted fraction of greenhouse construction costs	η_{Rem}	%	2.5	Assumed	2.5	Vermeulen (2008)
The sales cost coefficient for sorting and selling the tomatoes	η_{Sales}	%	9	Cajamar	2.75	Vermeulen (2008)
The fraction of first class tomatoes in	η_{Tom1}	%	-	Depends on indoor	-	Depends on indoor

marketable yield				climate		climate
The transport cost per kg tomatoes	$\eta_{Transport}$	€ kg ⁻¹	0.02	Cajamar	0	Included in sales costs
Greenhouse floor area	A_{Flr}	m ²	10000	Assumed	10000	Assumed
Pure CO ₂ costs	q_{CO2_Ext}	€ kg ⁻¹	0.20	Cajamar	0.10	Vermeulen (2008)
Industrial CO ₂ costs	q_{CO2_Ind}	€ kg ⁻¹	-	Not selected	0.06	OCAP
Electricity costs	q_{Elec}	€ kWh ⁻¹	0.13	Cajamar	0.07	Vermeulen (2008)
Gas costs	q_{Fuel}	€ m ⁻³	0.38	Cajamar	0.25	Vermeulen (2008)
Initial investment of design element i	$q_{Invest,i}$	€	-	See Table 6.1	-	See Table 6.1
The labour costs	q_{Labour}	€ h ⁻¹	5.4	Cajamar	16.0	Vermeulen (2008)
Time variant first class tomato price	q_{Tom1}	€ kg ⁻¹	-	Cajamar	-	Vermeulen (2008)
Time variant second class tomato price	q_{Tom2}	€ kg ⁻¹	-	Cajamar	-	Vermeulen (2008)
Water costs	q_{Water}	€ m ⁻³	0.25	Cajamar	0	Rain water is used
Plant material		€ plant ⁻¹	0.45	Cajamar	0.65	Vermeulen (2008)
Plant density		m ⁻²	2.5	Practice	2.5	Practice
Fertiliser		€ m ⁻² year ⁻¹	0.6	Cajamar	0.9	Vermeulen (2008)
Crop protection		€ m ⁻² year ⁻¹	0.35	Cajamar	1	Vermeulen (2008)
Waste treatment		€ m ⁻² year ⁻¹	0.36	Cajamar	0.75	Vermeulen (2008)
Remaining materials		€ m ⁻² year ⁻¹	0.3	Cajamar	1.15	Vermeulen (2008)
Substrate		€ m ⁻² year ⁻¹	0	Not used	1.3	Vermeulen (2008)

6.4 Results and discussion

For each location, the evolution of the two design populations *A* are presented in section 6.4.1. Then, in section 6.4.2 the best designs are discussed and relevant economic aspects are described. The close-to-best designs are analysed in section 6.4.3 using distribution curves and sensitivity analysis. In section 6.4.4 the performance of the model-based design-method is discussed.

6.4.1 Evaluation of the performance measure during optimisation

For both locations, the CRS algorithm was able to solve the multi-factorial greenhouse design optimisation problem. Specifically, with increasing iteration number, the performance (NFR) of the design population *A* increased (Fig. 6.5). Two different start design populations yielded the same maximum NFR with similar end design populations and each time the mean NFR of the design population converged to the same maximum NFR. Therefore we can claim with some confidence that a global maximum NFR was found. The highest NFR was reached after 3000 iterations for the Spanish case, whereas the Dutch one required some 5000 since there were more design alternatives, as presented in Table 6.2. These numbers indicate that the evaluation of less than 1% of all design alternatives was sufficient to come up with the greenhouse with the highest performance in both cases. The optimisation was stopped after 7500 iterations because it was expected that, due to the flat trajectory of the NFR, the design could not be improved much further.

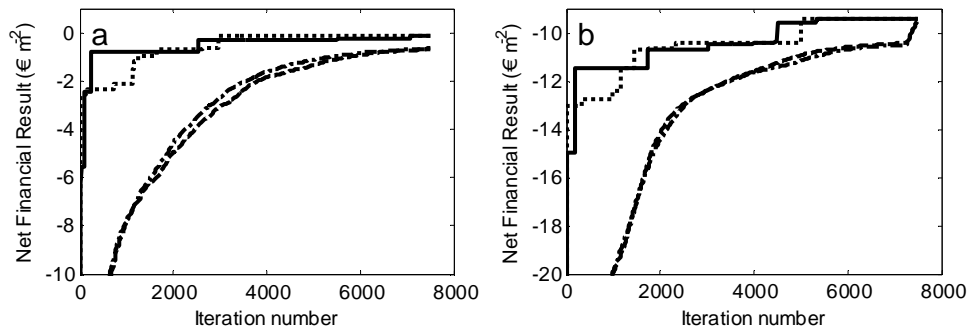


Fig. 6.5 The evolution of the net financial result of the design population 'A' in Almeria (a) and in The Netherlands (b). For both figures, the solid line represents the maximum NFR of the first optimisation run, the dotted line represents the maximum NFR of the second optimisation run, the dashed line represents the mean NFR of the first optimisation run and the dashed-dotted line represents the mean NFR of the second optimisation run.

6.4.2 Evaluation of the best greenhouse design for both conditions

6.4.2.1 The best design as a function of local conditions

Table 6.5 shows that the best greenhouses were adapted to Spanish and Dutch climate conditions as presented in Fig. 6.3. For the relatively warm climate with high radiation levels in Almeria, a greenhouse with a relatively large ventilation area (20% compared to 14% for Dutch conditions), with seasonal whitewash to reduce the indoor temperature and fitted with a direct air heating of small capacity (0.5 MW compared to 2.0 MW for Dutch conditions) was selected. In contrast, whitewash was not selected in view of the low radiation levels in The Netherlands, and a thermal screen was selected to increase the heating efficiency for the relatively cold climate. For both conditions, a structure of high light transmissivity was selected to benefit as much as possible from outdoor radiation. CO₂ application was worthwhile only for Dutch conditions, thanks to the lower ventilation requirement (and thus a higher CO₂ supply set-point, see section 6.6.4) and the larger difference between the average tomato price and the variable CO₂ price in The Netherlands. Specifically, this difference was in The Netherlands $0.73 - 0.06 = 0.67 \text{ € kg}^{-1}$ and in Spain $0.56 - 0.20 = 0.36 \text{ € kg}^{-1}$.

Table 6.5 The optimised greenhouse design in Almeria and The Netherlands.

Location	Structure	Cover	Outdoor screen	White wash	Indoor screen	Heating MW	Cooling	CO ₂ supply kg Ha ⁻¹ h ⁻¹	NFR € m ⁻² year ⁻¹
Almeria	Light, 20%*	Glass	No	50% tr	No	Dirair: 0.5	No	No	-0.11
Netherlands	Light, 14%*	Glass	No	No	100% Alu	Dirair: 2.0	No	Ind 200	-9.41

The * indicates the specific ventilation area of the greenhouse.

For Spanish conditions the annual NFR was $-0.11 \text{ € m}^{-2} \text{ year}^{-1}$ and for Dutch conditions the annual NFR was $-9.41 \text{ € m}^{-2} \text{ year}^{-1}$, which agreed reasonably well with Vermeulen (2008) who determined an annual NFR of $-11.06 \text{ € m}^{-2} \text{ year}^{-1}$ for a similar greenhouse. These negative values indicate that growers, under the economic conditions considered, could not make a living at both locations. For Spain, some assumptions related to the depreciation, maintenance and the short term borrowing costs might have resulted in negative NFR values. For The Netherlands, it is known that only growers with a co-generator to sell electricity (not considered in this study) have earned money in spite of the relatively low tomato prices of the last years. However, these negative values will not have affected the optimisation outcome, since in this study the annual NFR was maximised.

The selected best greenhouse for Almeria agrees reasonably with the greenhouses encountered in practice. Whitewash (and not other cooling means) was selected, which

agrees with an economic analysis of Gázquez *et al.* (2008) who demonstrated that whitewash in combination with sufficient ventilation area was the most cost-efficient cooling treatment for sweet peppers under Southern Spanish conditions. Moreover an outdoor shade screen, an indoor thermal screen and CO₂ supply were not selected, and they seldom are found in Almeria greenhouses. However, our results suggest that the performance of the commonly encountered parral greenhouses might be improved by; (i) using a high-light transmissivity structure, covered with glass, which would increase light transmissivity from 57% to 75%; (ii) increasing the mean ventilation area from 13% to 20%; and (iii) by installing a low-investment heating system with a limited capacity. The use of a higher light transmission (Soriano *et al.*, 2004) and higher specific ventilation area (Pérez-Parra *et al.*, 2004) to increase crop yield was already demonstrated. As cover material glass (rather than the much more widely applied single PE film) was selected, mainly for its lower annual costs (0.38 € m⁻² year⁻¹ compared to 0.53 € m⁻² year⁻¹) and for the slightly higher light transmission (82% compared to 81%). This result indicates that a greenhouse with more advanced technology might be feasible provided that enough funds are available for the required additional investment. Specifically, the investment cost of the selected design is 52.44 € m⁻² which is much higher than the 21.54 € m⁻² required for a common parral greenhouse. This large difference in investment cost was probably caused by our choice of not constraining the investment potential.

For Dutch conditions the optimised greenhouse design was quite similar to the common greenhouses, with exception of the heating system. The design method suggests that a direct air heater would give a higher NFR, whereas a boiler with pipe heating system is used in practice. Simulations revealed that a direct air heater had a higher heat efficiency than a boiler-pipe heating system. The lower heat efficiency of the boiler-pipe heating system was caused by higher heat losses from the cover to outside (due to the far infrared radiation (FIR) from pipes to cover) and because of the higher ventilation demand due to higher humidity levels caused by a higher transpiration rate (due to the FIR from pipes to canopy resulting in a higher canopy temperature). However, in reality, the boiler-pipe heating system has several advantages: the pipes can be used as internal transportation system; the heat can be buffered enabling a smaller boiler capacity and higher CO₂ efficiency of exhaust gasses. In addition, the direct air heater might exhaust flue gasses and increases spatial climate differences which both might negatively affect crop growth. Since these processes were not described by the model, the results of the design optimisation are not surprising.

6.4.2.2 Relevant cost aspects that determine the NFR

Both locations had the same four main costs aspects i.e. fixed costs, labour, energy and plant related costs (Table 6.6). The contribution of water, electricity and CO₂ to the total costs was small. Although the greenhouse climate model and tomato yield model were both successfully validated in chapters 2 and 3 to assure reliable NFR values the crop yield value, labour costs and energy were compared with values described in literature.

Table 6.6 The simulated economic costs that determine the NFR of the optimised greenhouse in Spain and in The Netherlands.

Location	Spain (€ m ⁻² year ⁻¹)	Netherland (€ m ⁻² year ⁻¹)
Crop Yield	22.50	41.73
Fixed costs	6.43	14.57
Variable costs		
Labour	3.63	17.73
Energy	6.54	9.48
Water	0.21	0.00
Electricity	0.00	0.21
CO ₂	0.00	0.34
Plant related costs	5.80	8.81
Net financial result	-0.11	-9.41

In Spain, the calculated marketable tomato yield of 40.3 kg m⁻² was considerably higher than the marketable tomato yield of 23.8 kg m⁻² measured in a high tech greenhouse by Magán *et al.* (2007). The higher simulated crop yield was caused by a 50 days longer simulated production period (using a simulated production period similar to the measured one would have resulted in a simulated crop tomato yield of 32.1 kg m⁻²) and by the higher light transmission of the optimised greenhouse since it had less light absorption design elements i.e. no shading screen and no thermal screen. To check the order of magnitude, simulation results were compared with values obtained for a sweet pepper crop by Magán, López *et al.* (2008). They found similar amounts for labour costs (2.3 € m⁻² year⁻¹ versus the simulated labour of 3.63 € m⁻² year⁻¹) and energy costs (4.56 € m⁻² year⁻¹ versus the simulated gas consumption of 6.54 € m⁻² year⁻¹). The simulated labour costs were higher because of the higher production and simulated gas costs were higher because no thermal screen was used. These results indicate that for Spanish conditions the method produced realistic model output. In The Netherlands, the simulated costs agreed with fair accuracy

with the national greenhouse statistics of Vermeulen (2008) indicating that for Dutch conditions the method produced realistic model outputs as well. In particular: the crop yield (56.5 kg m^{-2} and 57.5 kg m^{-2} , measured and simulated, respectively), labour ($16.74 \text{ € m}^{-2} \text{ year}^{-1}$ and $17.73 \text{ € m}^{-2} \text{ year}^{-1}$) and energy use (43.4 m^3 , 37.9 m^3 gas). Consequently, as described before, the negative simulated NFR agreed reasonably well with the NFR presented by Vermeulen (2008). The higher economic crop yield in The Netherlands was caused by the higher average tomato price of 0.73 € kg^{-1} compared to 0.56 € kg^{-1} in Spain, and by the higher marketable yield of $57.5 \text{ kg m}^{-2} \text{ year}^{-1}$ compared to $40.3 \text{ kg m}^{-2} \text{ year}^{-1}$ in Spain. The lower crop yield in Spain was caused by the lower light transmission of the greenhouse due to the appliance of seasonal whitewash and by not applying CO_2 enrichment.

6.4.3 Evaluation of the close-to-best greenhouses

For this analysis we combined the population of greenhouse designs obtained during the two optimisations runs for each case.

6.4.3.1 Southern Spanish conditions

For Spanish conditions, the distribution of the design elements alternatives of the greenhouses for which the NFR differed less than $€ 0.25 \text{ m}^{-2} \text{ year}^{-1}$ from the NFR of the best greenhouse ($\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$) is presented in Fig. 6.6. This figure shows that there were only minimal differences among the close-to-best greenhouses which indicates that the optimisation converged to an optimum.

Allowing for larger differences ($\Delta NFR < 1.50 \text{ € m}^{-2} \text{ year}^{-1}$) resulted obviously in a broader spectrum of design elements (Fig. 6.7). Specifically, compared to $\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$, a light structure with a specific ventilation area of 14%, a single PE film, no appliance of whitewash and a direct air heater with a capacity of 1.0 MW were also feasible designs solutions. In addition, the broad spectrum of the alternatives related to the indoor screen and the CO_2 supply, indicated that the effect of these factor was marginal. The sensitivity analysis presented in Fig. 6.8 shows the impact of all alternatives to fulfil each design element on the NFR. Alternatives for which the accompanying mean NFR was high indicate that these individual alternatives enhanced the overall performance of a greenhouse significantly. Since the design element alternatives with a high NFR were present as well in the set of close-to-best greenhouse designs (Fig. 6.6 and Fig. 6.7), it is expected that a global maximum was found.

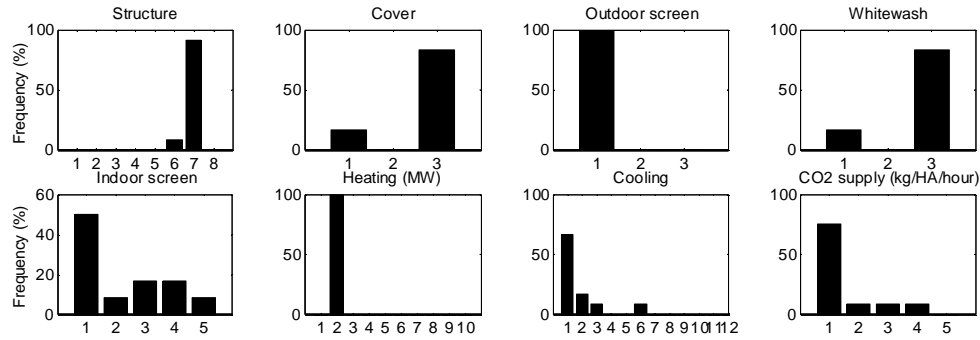


Fig. 6.6 The frequency of the design element alternatives expressed in % of the best 12 designs for which the $\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$ (i.e. all greenhouses for which the net financial result differed less than 0.25 € m^{-2} with respect to the best greenhouse) for Spanish conditions. The indices on the x-axis correspond with the design element alternatives presented in Table 6.1.

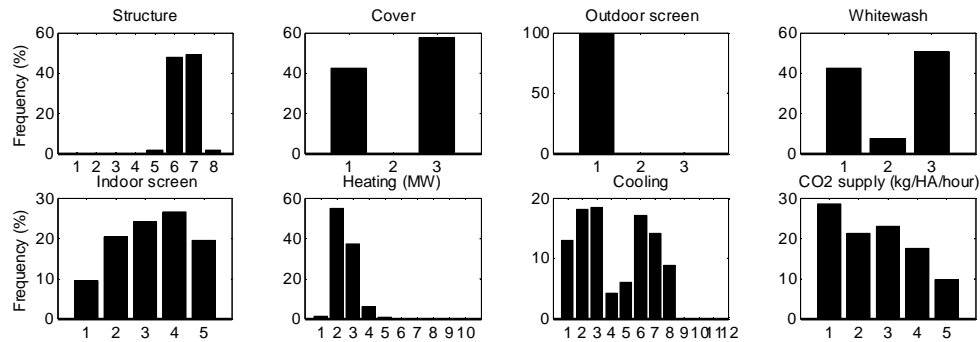


Fig. 6.7. The frequency of the design element alternatives expressed in % of the best 781 designs for which the $\Delta NFR < 1.50 \text{ € m}^{-2} \text{ year}^{-1}$ for Spanish conditions.

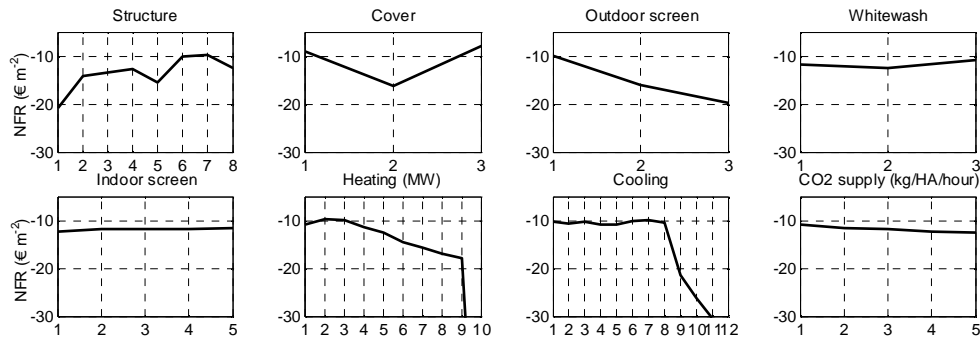


Fig. 6.8 For all 8 design elements and associated alternatives individually, the mean average of the NFR belonging to the greenhouse designs that were equipped with a particular alternative for Spanish conditions. All designs evaluated by the CRS algorithm were used for this analysis.

As follows from the observation above, the NFR was not sensitive to the selection of an alternative to fulfil the indoor screen and CO₂ supply as demonstrated by the relatively flat response of the NFR to these alternatives. Therefore, focussing first on the optimisation of the design elements for which the NFR is sensitive to changes in the selected alternatives, would in this case mean focusing on the greenhouse structure, cover, whitewash and a heating system. Given the applied assumptions on greenhouse floor area and economics, techniques with an extreme low NFR, i.e. geothermal heating and mechanical cooling should be discarded from the alternatives to be optimised under the given conditions.

Additionally, a high light transmissivity structure rather than a low light transmissivity structure was preferable (Fig. 6.8). The large positive impact of a higher light transmission on yield and resulting NFR was already demonstrated by the sensitivity analysis of a Spanish greenhouse performed in chapter 5. However, as indicated by the selection of a whitewash with a transmission of 50%, a higher greenhouse transmission was not favourable in summer conditions to increase the NFR. This result indicates that the impact of the cover transmission on NFR varies with seasons, which was already pointed out in chapter 4.

6.4.3.2 Dutch conditions

For Dutch conditions, the design element distribution of $\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$ revealed that also a thermal screen constituting of 75% aluminium and 25% PE, a direct air heater of capacity 1.5 MW and several capacities of CO₂ supply from the tank or industry were feasible alternatives as well (Fig. 6.9). The design element distribution of $\Delta NFR < 1.50 \text{ € m}^{-2} \text{ year}^{-1}$ demonstrated that cooling and CO₂ supply could be fulfilled by several feasible alternatives (Fig. 6.10). Although these cooling techniques did not have a significant impact on simulated crop yield and variable costs, their selection resulted from their low annual fixed cost (Table 6.1).

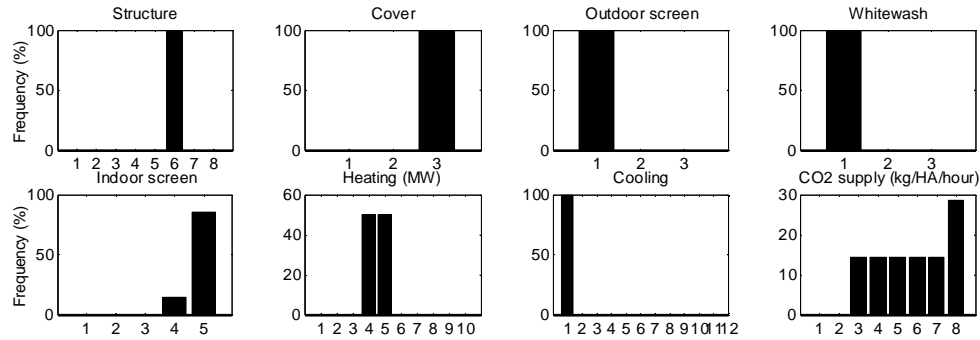


Fig. 6.9 The frequency of the design element alternatives expressed in % of the best 14 designs for which the $\Delta NFR < 0.25 \text{ € m}^{-2} \text{ year}^{-1}$ for Dutch conditions. The indices on the x-axis correspond with the design element alternatives presented in Table 6.1

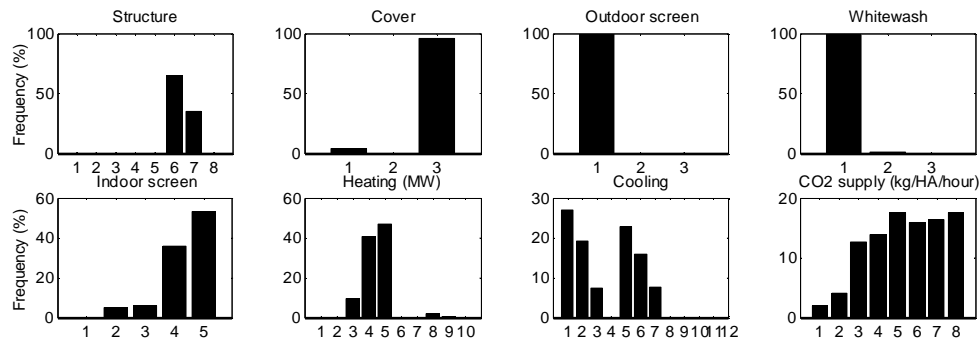


Fig. 6.10 The frequency of the design element alternatives expressed in % of the best 245 designs for which the $\Delta NFR < 1.50 \text{ € m}^{-2} \text{ year}^{-1}$ for Dutch conditions.

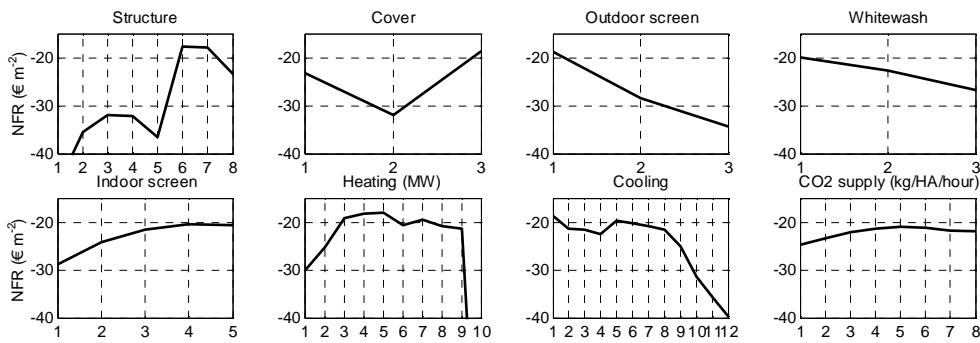


Fig. 6.11 For all 8 design elements and associated alternatives individually, the mean average of the NFR belonging to the greenhouse designs that were equipped with a particular alternative for Dutch conditions. All designs evaluated by the CRS algorithm were used for this analysis.

Since the impact of design element alternatives on NFR differed considerably between Spanish (Fig. 6.8) and Dutch conditions (Fig. 6.11) the need to adjust greenhouses to local conditions is demonstrated once again. Specifically, the different trajectories of the mean NFR for the indoor screen and heating system indicates that in the relatively cold Netherlands an indoor thermal screen and a large heating capacity are more relevant than in Spain. As presented before, for both locations a high light transmissivity structure was obviously the best. However, the NFR difference between a high light and a low light structure is much larger in The Netherlands than in Spain which in turn indicates that light in the Netherlands is a much more limiting growth factor, as expected

6.4.4 Discussion of the model-based design method

In contrast to chapter 5 and other greenhouse design studies (Engel, 1984; Amir & Hasegawa, 1989; Kacira *et al.*, 2004), a broad set of design elements were optimised using a model-based greenhouse design method. For Spanish and Dutch conditions, this method adjusted the greenhouse designs to the local climate and economic conditions in order to obtain a maximum NFR. Additionally, the distribution curves and sensitivity analysis revealed the impact of design elements on greenhouse design and related NFR. Although, the design method was able to optimise greenhouse designs for different climatic and economic conditions, several issues need to be addressed to improve the performance and generality of the model-based design method. The modified CRS algorithm was able to solve efficiently the multi-factorial greenhouse design optimisation problem as demonstrated in Fig. 6.5. Although the CRS was developed for continuous design variables, the modified CRS could solve the integer greenhouse design problem because the discrete optimisation parameters were represented as floating point values as proposed by Lampinen and Zelinka (1999). It might be expected that other population-based optimisation methods like simulated annealing and a genetic algorithm could be used as well (Dréo *et al.*, 2006). Provided that these more elegant optimisation algorithms also may benefit from parallel computing, these methods might decrease optimisation time compared to the modified CRS algorithm. Even though two optimisation runs with different start sets found the same optimised greenhouse, like all other optimisation methods, the CRS could not guarantee a global maximum.

The performance of an optimisation depends mainly on three factors. First, the optimisation takes into account only processes which are included in the models. In our project, the focus was to optimise a limited set of design elements. Therefore, optimisation of the structural design, climate control, heat buffers, fertigation systems, labour and logistics was not carried out. Consequently, for example the positive effects of a boiler-pipe

heating system on heat storage, labour and logistics were not incorporated and therefore these advantages of this heating system could not be optimised by the design method. The generic nature of the design method allows that design elements, key components and model aspects can easily be adjusted or added. Second, the accuracy of the models determines the confidence limits of the NFR and consequently the performance of the optimisation. In spite of the validation, the greenhouse climate model and tomato yield model might be improved as discussed in chapter 2 and 3 respectively, which might also influence the optimised design. Furthermore, since tomato quality aspects are not only affected by humidity levels but also by other climatic variables (Adams *et al.*, 2001), model performance might be improved by replacing the tomato quality filter described in section 6.6.2 by a more detailed description of the quality aspects.

Third, the selection of the performance measure and boundary conditions have an impact on the optimised design. In this study, greenhouses were optimised by maximising the annual NFR per square meter ($\text{€ m}^{-2} \text{ year}^{-1}$) under the boundary condition of a fixed greenhouse area (1 Ha). The investment potential was not constrained, because in this way we were able to find out the best performing greenhouses in given market and climate conditions. In this way, for instance, local authorities could find out whether productivity in a region could be improved through subsidies or other financial stimuli. Results demonstrated that the investment cost of the best greenhouse was higher than for the local commercial parallel greenhouses which indicates that these financial stimuli might be beneficial under these conditions. It might be interesting as well to optimise both the surface and greenhouse design by maximising the annual NFR (€ year^{-1}) with a limited investment potential as boundary condition. Because of the modular structure of the design method, the performance measure and boundary conditions can be adjusted easily to the demands of the designer.

As demonstrated in chapters 4 and 5 the greenhouse climate set-points, economic input parameters and outdoor climate have a significant impact on NFR. In addition, Vanthoor *et al.* (2008a) have shown that the choice of climate set-points even affected some optimal design parameters. These results indicate that changes of economic input parameters, outdoor climate data and climate set-point parameter might influence the optimised design. The design optimisation horizon was one year whereas the optimised greenhouse will have a lifespan of approximately 15 years. Therefore, these input parameters should be determined in such a way that they represent, with the currently known information, the future input parameters at best.

6.5 Conclusion

The aim of this study was to integrate an optimisation algorithm into the model-based design method to select the greenhouse design that would yield the largest annual Net Financial Return for a tomato greenhouse for different climatic and economic conditions. This aim was fulfilled. A modified CRS optimisation algorithm using parallel computing was able to select the best set of alternatives to fulfil the design elements for Almeria and Dutch conditions.

Specifically, due to the relatively warm climate with high radiation levels in Almeria, a greenhouse with a relatively large ventilation area (20% compared to 14% for Dutch conditions), seasonal whitewash and a relatively low capacity of the direct air heating (0.5 MW compared to 2.0 MW for Dutch conditions) was selected. In contrast, for the relatively cold climate with low radiation levels in The Netherlands, whitewash was not selected and a 100% aluminium thermal screen was applied. Only for Dutch conditions CO₂ enrichment was applied. The design method produced realistic designs and related annual NFR which indicates that a robust and reliable design method was developed.

A population-based optimisation method offers the opportunity to analyse the close-to-best greenhouses. The distribution curves of the close-to-best greenhouse designs and a sensitivity analysis of the mean NFR to the design element alternatives revealed: a) the relevant design elements and associated alternatives for optimisation and b) whether there are many different greenhouses with an almost similar NFR. For both locations, the selection of a high-light transmissivity structure with sufficient ventilation area was important and an outdoor shade screen, geothermal heating and mechanic cooling were not feasible for the given conditions. Additionally, for Spanish conditions, one should also focus on the optimisation of the cover material, whitewash and heating system to increase the NFR whereas for Dutch conditions, the indoor screen and heating system have a large impact on performance.

With these results, all four key components of the model-based design method i.e. the greenhouse climate model, the tomato yield model, the economic model and an optimisation algorithm were successfully integrated. This design method is able to describe the economic performance of a greenhouse as a function of outdoor climate, climate management and greenhouse design. The modified CRS algorithm adapts the greenhouse to given conditions so that the maximum net financial result will be obtained. To the best of our knowledge, it is the first time that this multi-factorial optimisation problem is addressed

and a partial solution of the more complex problem is obtained. These results demonstrate the feasibility of a model-based approach towards greenhouse design for a wide variety of climatic and economic conditions.

Acknowledgement

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6.6 Appendices

6.6.1 Appendix A: Calculation of electric consumption of climate modification techniques

$$P_{Fog} = \frac{p_{Fog} MV_{FogAir}}{1000 \eta_{FogPump}} \quad [\text{W m}^{-2}] \quad (\text{A.1})$$

$$P_{Geo} = \eta_{Geo} H_{GeoPipe} \quad [\text{W m}^{-2}] \quad (\text{A.2})$$

$$P_{Mech} = U_{MechCool} (1 + \eta_{MechCool}) P_{MechCool} / A_{Flr} \quad [\text{W m}^{-2}] \quad (\text{A.3})$$

$$P_{Pad} = c_{Pad} f_{Pad}^2 \quad [\text{W m}^{-2}] \quad (\text{A.4})$$

where

$$c_{Pad} = \frac{P_{PadMax}}{f_{PadMax}^2} \quad [\text{W s}^2 \text{ m}^{-4}] \quad (\text{A.5})$$

$$P_{PadMax} = \frac{n_{Vents} P_{VentMax}}{A_{Flr}} \quad [\text{W m}^{-2}] \quad (\text{A.6})$$

$$f_{PadMax} = \frac{n_{Vents} f_{VentMax}}{A_{Flr}} \quad [\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}] \quad (\text{A.7})$$

where p_{Fog} (Pa) is the static pressure of the fogging system, $\eta_{FogPump}$ (-) is the efficiency of the fogging pump, η_{Geo} (J J^{-1}) is the electrical energy needed to pump the geothermal heat, $U_{MechCool}$ (-) is the control valve of the mechanical cooling mechanism, $\eta_{MechCool}$ (-) is a fraction to account for pump costs of the mechanical cooling system, $P_{MechCool}$ (W) is the electric power of the mechanical cooling system, A_{Flr} (m^2) is the greenhouse floor area, c_{Pad} ($\text{W s}^2 \text{ m}^{-4}$) is the fan characteristic in terms of electricity consumption, f_{Pad} ($\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}$) is the ventilation flux due to the pad and fan system, P_{PadMax} (W m^{-2}) is the maximum electric consumption of the fans expressed per square meter greenhouse, f_{PadMax} ($\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}$) is the maximum air flow of the fans, n_{Vents} (-) is the total number of fans, $P_{VentMax}$ (W m^{-2}) is the maximum electric power of one fan, and $f_{VentMax}$ ($\text{m}^3 \text{ s}^{-1} \text{ fan}^{-1}$) is the maximum air flux of one fan.

6.6.2 Appendix B: Determination of the fraction of first class tomatoes and marketable fraction as a function of humidity

Körner and Challa (2003) indicated that the crop growth and development is affected by the 24 hour running mean value of the vapour pressure difference (VPD_{24}) and that botrytis is affected by the 48 hour running mean value of the relative humidity of the greenhouse air (RH_{48}). Based on these data, we assumed that the fraction of first class tomatoes can be described as a function of VPD_{24} and that the marketable fraction can be described as a function of RH_{48} . These two functions are each described by a trapezoid function as presented in Fig. B1

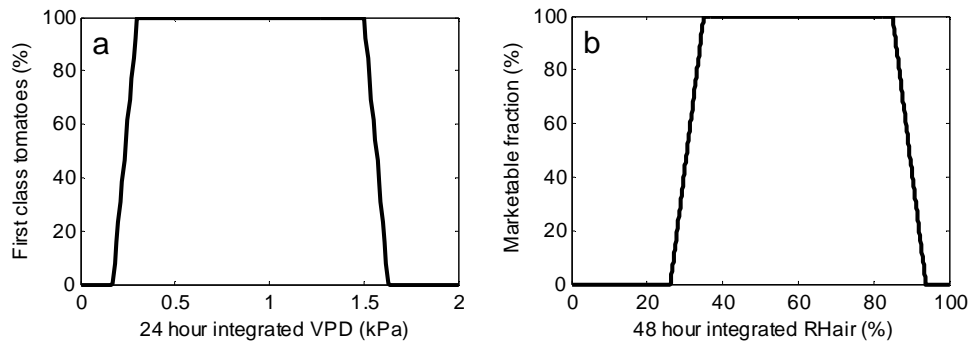


Fig. B.1a The fraction of first class tomatoes as a function of the 24 hour running mean value of the vapour pressure difference (VPD_{24}). Fig. B.1b The marketable fraction as a function of the 48 hour running mean value of the relative humidity (RH_{48}).

The boundary conditions at which the quality parameters were still maximal were: $VPD_{min} = 0.3$ kPa (Körner & Challa, 2003); $VPD_{max} = 1.5$ kPa Las Palmerillas Cajamar; $RH_{air_{min}} = 35\%$ greenhouse grower A and $RH_{air_{max}} = 85\%$ greenhouse grower B. The slopes of these functions were estimated by fitting the estimated quality parameters on the measured values as a function of the measured indoor climate in a low-tech and high-tech greenhouse. It was assumed that for the current approach, these quality filters estimated sufficiently accurate the fraction of first class tomatoes and marketable fraction (Table A1).

Table A1 The estimated quality parameters and the measured quality parameters (between brackets) for two greenhouses located in South Spain

Quality parameters	Low-tech greenhouse	High-tech greenhouse
First class tomatoes, η_{Tom1} (%)	69.9 (65)	92.5 (95)
Marketable fraction η_{FMsold} (%)	90.1 (90)	95.2 (95)

6.6.3 Appendix C: The algorithm to calculate a standard climate year

The algorithm to generate a standard climate year was based on Breuer and Van de Braak (1989) and adjusted to produce a standard year that has a close match with the mean monthly values of temperature and global radiation sums. To produce the standard year the following steps were performed:

1. Determine the monthly mean values of temperature and global radiation averaged over all the climate years, $\bar{x}_{i,j}$, where i denotes the month indices and j denotes the climate variables under consideration.
2. Determine for each climate year, k , the monthly mean values of temperature and global radiation, $x_{i,j,k}$
3. Determine for each month, i , for each climate variable, j and for each climate year,

$$k \text{ the normalised deviation: } S_{i,j,k} = \left| \frac{\bar{x}_{i,j} - x_{i,j,k}}{std(x_{i,j})} \right|$$

4. Determine for each month, the year with the smallest summed standardised deviation for all climate variables: $Year_i = \min_k \sum_{j=1}^{j=Nj} S_{i,j,k}$
5. Create the standard year by appending the years with the smallest monthly standardised deviation

:

$$STDyear = (January(Year_1), February(Year_2), \dots, December(Year_{12}))$$

6.6.4 Appendix D: The calculation of the CO₂ set-point for CO₂ enrichment

The CO₂ set-point increases linearly with global radiation, I_{Glob} , until a defined maximum CO₂ set-point, CO_{2Air_ExtMax} , is reached and, simultaneously, the CO₂ set-point decreases linearly with the total ventilation rate of the greenhouse, $f_{VentTot}$:

$$CO_{2Air_ExtOn} = f(I_{Glob}) \cdot g(f_{VentTot}) \cdot (CO_{2Air_ExtMax} - CO_{2Air_ExtMin}) + CO_{2Air_ExtMin} \quad [\text{ppm}] \quad (\text{D.1})$$

$$f(I_{Glob}) = \begin{cases} \frac{I_{Glob}}{I_{Glob_Max}}, & I_{Glob} < I_{Glob_Max} \\ 1, & I_{Glob} \geq I_{Glob_Max} \end{cases} \quad [-] \quad (\text{D.2})$$

$$g(f_{VentTot}) = \begin{cases} 1 - \frac{f_{VentTot}}{f_{VentExtCO2_Max}}, & f_{VentTot} < f_{VentExtCO2_Max} \\ 0, & f_{VentTot} \geq f_{VentExtCO2_Max} \end{cases} \quad [-] \quad (\text{D.3})$$

where I_{Glob} (W m⁻²) is the outdoor global radiation, $f_{VentTot}$ (m³ m⁻² s⁻¹) is the total ventilation rate, CO_{2Air_ExtMax} (ppm) is the maximum CO₂ concentration set-point, CO_{2Air_ExtMin} is the minimum CO₂ concentration set-point (ppm), I_{Glob_Max} (W m⁻²) is the outdoor global radiation at which the maximum CO₂ concentration set-point could be reached and $f_{VentExtCO2_Max}$ (m³ m⁻² s⁻¹) is the total ventilation rate at which the CO₂ concentration set-point equals the minimum CO₂ concentration set-point (ppm).

Chapter 7

Conclusion, discussion, recommendations and
future perspectives

7.1.1 Conclusion

To design greenhouses that are adapted to local climatic and economic conditions, the model-based greenhouse design method presented in Fig. 7.1 was developed. This method determined the greenhouse performance as a function of multiple design factors using a greenhouse climate model, a tomato yield model and an economic model.

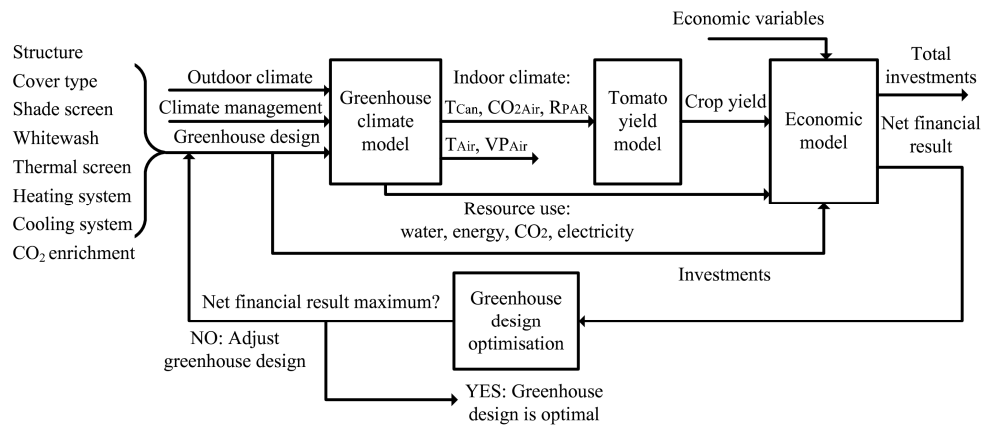


Fig. 7.1 An overview of the model-based greenhouse design method. This method selects the set of alternatives to fulfil the eight design elements presented at the left-hand side that would yield the largest annual net financial result. The method consists of four key components, i.e. the greenhouse climate model, the tomato yield model, the economic model and the design optimisation algorithm. The applied performance measure is the annual net financial result.

To the best of our knowledge, it is the first time that this multi-factorial optimisation problem is addressed in detail and partly solved. The presented method selected the best greenhouse under given local climatic and economic conditions, as demonstrated by two cases i.e. South Spain and The Netherlands (Chapter 6). The best greenhouse for Almeria (South Spain) had seasonal whitewash and was equipped with a relatively large ventilation area, whereas for Dutch conditions a greenhouse with a lower ventilation area, a higher heating capacity and thermal screen was found to be the best.

In both cases, the derived greenhouse designs represented reasonably well the current greenhouse state-of-the-art, which increases our confidence in the robustness and reliability of the design method. Furthermore, results demonstrated that for a wide range of climatic conditions the models used were sufficiently accurate to be incorporated in the

model-based design method. In particular, the greenhouse climate model predicted the indoor climate with reasonable accuracy for four different greenhouse designs, under three climatic conditions: a temperate marine climate, a Mediterranean climate and a semi-arid climate, as shown in Chapter 2. The tomato yield model simulated the tomato yield with fair accuracy for a wide variety of temperature regimes, as shown in Chapter 3. Calculation of the annual net financial result gave reliable estimates of current economics as shown in Chapters 5 and 6.

Given these results, the objective of this thesis was fulfilled. A design method for protected cultivation systems has been developed that produces greenhouse designs adapted to local climatic and economic conditions. As demonstrated for South Spain and The Netherlands, this method produces very different reliable greenhouses for both locations. As the underlying models were validated thoroughly for a wide variety of climatic conditions, the design method might be expected to produce reliable greenhouse designs for other locations as well. Since the focus was on climatic and economic conditions and techniques that influence the aerial climate, a partial solution of the greenhouse design problem was obtained. Consequences of this approach as well as other aspects of the design method will be discussed hereafter.

7.1.2 Discussion and recommendations

7.1.2.1 Adaptation of greenhouses to local conditions

Results generated by the design method gave indications why and how the optimised greenhouses were adapted to local climate and economic conditions. The outdoor climate - particularly the global radiation, temperature and CO₂ concentration - affected the crop yield and resource consumption enormously for a low-tech greenhouse in Spain and a high-tech greenhouse in Texas (Table 4.5 and 4.6) which indicates that these climate variables will affect greenhouse design as well. Indeed, the greenhouse designs were adapted to these climate conditions as demonstrated for South Spain and The Netherlands in Chapter 6. The relatively low radiation levels and temperature in The Netherlands (Fig. 6.3) resulted in a greenhouse with a structure of high light transmissivity, without whitewash, a heater capacity of 2.0 MW and a thermal screen. In contrast, the relatively high radiation levels and high temperature in Spain resulted in a greenhouse covered with seasonal whitewash (but high transmissivity of the cover, for the winter months) and equipped with a larger specific ventilation area (20% against 14% in The Netherlands) to reduce greenhouse air temperature. In addition, to avoid low night temperatures, this greenhouse was equipped

with a heater capacity of 0.5 MW, although a thermal screen did not prove economical.

Economic conditions strongly affected the greenhouse design as well. Changing tomato price trajectories resulted in another “best” greenhouse as indicated in Fig. 5.5b. In particular, or Southern Spanish conditions, a high tech greenhouse would be beneficial at high tomato prices but not for low prices. In agreement with this, the higher tomato prices in The Netherlands (0.73 € kg^{-1} compared to 0.56 € kg^{-1} in Spain) yielded a greenhouse with more technology than in Spain.

7.1.2.2 Definition of a greenhouse design optimisation problem

In this research, the performance of a greenhouse design was expressed in terms of maximisation of the expected annual net financial result. Given the generic nature of the design method, this performance measure can be easily replaced. Alternatives might be another economic performance measure, minimisation of the resource consumption or maximisation of the yield.

Since an economic performance measure was selected in this study, the design parameters could not be optimised. Specifically, a greenhouse design can be considered to exist of as a set of design elements that each consist of one or more design parameters. For example, the design element ‘cover material’ consists of the following set of design parameters: the transmission-and absorption coefficients for PAR, NIR and FIR, the thickness, thermal heat conductivity, the specific heat capacity and the density of the cover. It might be interesting to search for optimal values of these design parameters. Yet, allocating costs to individual design parameters is rather complex especially when the accompanying design element does not exist (e.g. a cover material with a high PAR transmission coefficient and low NIR transmission coefficient). Consequently, these costs should be estimated based on rough assumptions which result in a huge price uncertainty. Therefore, since the costs of design elements are known (Table 6.1), this study focussed on optimisation of the set of alternatives to fulfil these design elements. However, if another performance measure would be selected e.g. yield maximisation, the set of design parameters can be optimised as well since then no costs need to be allocated to design parameter changes. In this way the “net worth” of a given modification of a design parameters is determined, which is useful information for producers of greenhouses to indicate the potential additional revenue of the grower. The economic potential of adjustable parameters over time can be determined as well if the greenhouse design is defined as a set of adjustable parameters. For example, the resulting extra revenues of an adjustable NIR transmission coefficient of the cover can be calculated then.

Besides the selection of a limited set of design elements, and fixing the greenhouse area to 1 Ha, no other constraints were used in this study. Whenever needed, other relevant optimisation constraints such as maximum levels of investments, greenhouse area or resource use can easily be applied to the design method. Design solutions that violate these constraints will then be discarded from the best set of greenhouse designs.

The impact of the performance measure and optimisation constraints on the greenhouse design optimisation was discussed in Chapter 6. For the Spanish optimisation case, the selected greenhouse had higher investments and a higher technology level compared to the commonly encountered ones. This difference was probably caused by the applied performance measure that maximises the annual net financial result (NFR) per square meter and by using an unlimited investment potential. In practice investment levels will be limited. Therefore, it might be interesting to evaluate how the best greenhouse design will be affected by: (i) another economic performance measure, for instance minimisation of the payback period or maximisation of the return on investment; (ii) a constraint on the investment level; and (iii) optimisation of the greenhouse area. Performing such an evaluation might answer the following two interesting design questions. Would another economic performance measure result in a totally different “optimal” greenhouse? And, should a grower under particular conditions invest in a small high-tech greenhouse or in a large low-tech one? These are questions that need to be addressed in a follow-up to this project. The design method can answer these questions provided that the effects of economy of scale on investment costs and a calculations of the pay-back period and return on investment will be integrated in the economic model.

7.1.2.3 Different ways to solve the greenhouse design problem

As discussed in the previous section greenhouse design can be defined in three ways: as a set of design elements; as a set of fixed design parameters and as a set of adjustable design parameters. In this section, optimisation techniques are discussed to solve these different design problems.

The present method focused on finding the optimal combination of possible alternatives to fulfil the eight design elements. In Chapter 6, this discrete design optimisation was defined as an integer optimisation problem and was solved with, a gradient-free global optimisation method that could cope with the discontinuous design parameters. For this purpose, the population-based controlled random search (CRS) method of Price (1977) was modified and applied to the design method. Selecting the best optimisation algorithm for this problem was outside the scope of this research. It might be

expected, that other population-based optimisation methods like simulated annealing and genetic algorithms can solve this problem as well (Dréo *et al.*, 2006). Provided that these more elegant optimisation algorithms allow parallel computing as well they might decrease optimisation time compared to the modified CRS algorithm.

The design method can also optimise individual design parameters. This continuous optimisation problem can efficiently be solved by gradient-based optimisation algorithms. Since these algorithms require differential equations with continuously differentiable right-hand sides, the models have been developed in this format. By joining the set of differential equations, the models were easily combined with each other. These differential equations were solved by an ordinary differential equation solver of MatlabTM. To implement these equations in software code, no rewriting or linearization was needed. Additionally, evaluation of the model performance revealed that the differentiable right-hand sides speeded up the simulation compared to non-differentiable ones (results not shown).

To optimise the adjustable design parameters over time and to determine their economic potential, these parameters should be considered as dynamic parameters. This optimisation problem can thus be considered as a dynamic optimisation problem. This problem can be solved using a dynamic optimisation algorithm in a similar way as the dynamic climate control optimisation described by Van Straten *et al.* (2010).

7.1.2.4 How to reveal relevant design aspects?

The applied population based optimisation algorithm produces insight into the set of greenhouses most suitable for the local conditions and reveals the most relevant design elements for that specific location. For instance, a structure with a high light transmissivity and sufficient ventilation area is of importance to increase the performance of a greenhouse both in South Spain and The Netherlands (Fig. 6.6– 6.11). In addition, for both locations, applying a geothermal heat source and mechanical cooling is not economic for a 1 Ha greenhouse.

The impact of the individual design parameters was analysed as well. A single-variate sensitivity analysis pinpointed the design parameters that were candidates for adjustment to increase the net financial result. Specifically, Table 5.8 shows that for a high tech greenhouse in Almeria Spain, the PAR transmission coefficient had the largest impact on net financial result: if the cover PAR transmission coefficient would increase by 1%, the annual NFR would increase € 1067 per Ha. For both a low-tech and a high-tech

greenhouse, the optical properties of the cover and whitewash, and the ventilation rate had the largest impact on the net financial result. No costs were allocated to design parameter modifications due to its complexity (see section 7.1.2.2), and therefore the single-variate analysis indicated only the extra gross revenues of a parameter modification and not the accompanying costs. The impact that some parameters can be modified easier than others (resulting in lower costs of a specific parameter modification) was thus not captured by this approach.

Sensitivity results also demonstrated that the impact of the cover properties on tomato yield varies with the season (Fig. 4.4), which indicates that, at least for some parameters, adjustable properties might give better results than fixed design parameters. Sonneveld *et al.* (2011) already indicated that adjustable cover properties might be beneficial for greenhouse performance. Nevertheless, more research is needed to identify the most promising parameters and to develop materials with dynamic properties.

The impact of economic parameters, outdoor climate conditions and climate set-points on NFR was revealed by the single-variate sensitivity analysis. Table 5.8 shows that for the conditions of Almeria, the NFR of a high-tech greenhouse was highly sensitive to economic input parameters, i.e. tomato price, marketable tomato fraction, ratio of first class tomatoes, and the heating and ventilation set-points. In addition, Table 4.5 and 4.6 demonstrate that the crop yield and the resource consumption were most sensitive to outdoor climate conditions both for a low-tech greenhouse in Almeria and a high-tech greenhouse in Texas. The impact of the uncertainty in yearly variations of outdoor climate and tomato price on the NFR was analysed (Fig. 5.5) and revealed that the selection of a specific year affected the “best” design for Almeria conditions.

7.1.2.5 Design optimisation under uncertainty of input parameters

Results presented in the previous section indicate that changes of economic input parameters, outdoor climate data and climate set-point parameters might considerably influence the optimised design. Since the lifespan of a greenhouse is much larger than the design optimisation horizon of one year, the selection of the input parameters is of utmost importance. These input parameters must be determined in such a way that they represent as best as possible the future input parameters with the currently known information. The most common approach to solve design optimisation under uncertainty of input parameters is to apply stochastic optimisation algorithms (Sahinidis, 2004). These algorithms would solve the optimisation problem for many different sets of stochastic price trajectories,

climate trajectories and climate set-points. This type of algorithms will thus come up with the best greenhouse design under input uncertainty. However, applying stochastic optimisation algorithms to the model-based design method will result in huge CPU times. Therefore a less time consuming approach to diminish the impact of price trajectories, outdoor climate and climate management on best design is proposed.

Averaging the tomato price over the last four successive production periods as was done in Chapter 6, reduced its uncertainty. However, since future price trajectories are uncertain, it would be better to repeat the optimisation procedure for a worst case and best case price scenario. Then, the greenhouse that performs best for these different levels should be selected. A standard climate year based on a longer climate period was applied to the design method (Chapter 6). To create a 'mean' standard year, extreme climate months were not selected which might influence the optimisation procedure. Therefore, it would be better to incorporate extreme events in a statistically sound fashion in the standard climate year, or to use an optimisation time span and outdoor climate for several years.

In this study, the climate control valves settings were determined as a function of the control strategy and climate set-points. To make the optimised design independently of the applied climate management strategy, these valves settings should be optimised simultaneously with the design. Research on the design of cold storage facilities (Lukasse *et al.*, 2009), elevators and car suspension systems (Fathy, 2003) has shown the feasibility of this approach. Though dynamic optimisation of climate control was already researched intensively (Seginer, 1989; Ooteghem, 2007; Van Henten, 1994; Van Straten *et al.*, 2010), a combined control and design optimisation problem for greenhouses has not been addressed. If the climate management will significantly affect the optimised greenhouse design, greenhouse design must be considered as a combined design and control optimisation problem. Solving such an optimisation problem will require an enormous CPU time. Another approach to limit the impact of the chosen climate management is to optimise the static climate set-points instead of the actual control actions and treat them in a similar way as the design elements. These climate set-points can then be added to the integer design vector (Fig. 6.2) and optimised in a similar way. This static optimisation approach will solve the optimisation problem faster than the combined design and control optimisation approach because the static climate-set-points do not vary in time whereas the dynamic control valve settings do. However, when optimising the climate-set-points, the selected control strategy undesirably would still affect the greenhouse design.

7.1.2.6 How to improve the reliability of the design method?

In this section the reliability of the method is first discussed in terms of accuracy of the used models and then in terms of the generality of the design method. Due to the generic nature of the design method, the proposed improvements or adjustments can easily be integrated into the method. Since our aim was to develop a design method that focussed on the optimisation of a set of elements, aspects that might be relevant may have been simplified or on purpose neglected. Since the accuracy of the models influences the confidence limits of the NFR and hence the optimisation procedure, some issues that might improve the accuracy of the models are discussed here.

The greenhouse climate model and crop yield model were validated separately, because data to validate them simultaneously were not available. However, as presented in Fig. 7.1, there are several input-output interactions between both models. Specifically, the crop yield model used the calculated indoor climate as input and crop growth processes affected the indoor CO₂ concentration, temperature and humidity of the greenhouse air. Therefore, it would have been better to jointly validate these models. A more thorough validation might improve the model confidence even further. Since crop yield is strongly affected by the canopy temperature, it would be beneficial to validate the canopy temperature and related variables such as the transpiration rate, and the temperatures of the cover and of the soil. Since photosynthesis and resource use have a major impact on the annual net financial result they should be validated as well.

The greenhouse climate model predicted the air temperature with fair accuracy even for extreme climate conditions by using the transpiration and stomata model of Stanghellini (1987) that was validated for a moderate vapour pressure differences. To come up with realistic transpiration rates under stress conditions, one parameter affecting the stomatal reaction to vapour pressure difference was adjusted. The good model performance was probably caused by the negative feedback between canopy transpiration and air vapour pressure. Since this approach is not fully-generic, the performance of the transpiration model might be improved by either adjusting the empirical description or by using a more generic stomatal model such as the model of Blonquist Jr. *et al.* (2009).

Modules to relate climate variables to each tomato growth and development process such as fruit set, fruit growth, fruit abortion and membrane integrity were not available and thus not integrated in the yield model. The literature review shown in chapter 3, indicated that extremely low and high temperatures considerably affect the crop yield. Therefore, to approximate non-optimal temperature effects on tomato growth and development processes, two lumped temperature-dependent growth inhibition functions

were used. To improve the model accuracy and performance these two functions should be replaced by modules that relate climate variables to each tomato growth and development process based on principles of plant physiology. Incorporation of these growth and development processes into the empirical tomato yield model will be a complex task. According to Yin and Struik (2010), combining physiological modelling and genetic mapping into gene-based modelling could be a powerful method to resolve these complex environment-dependent processes. They suggested that for further progress, crop models must be upgraded based on understanding of these complicated phenomena at lower organisational levels.

The yield model predicted the dry matter tomato yield and to transform this into fresh matter yield, a constant dry matter content was used. Since the dry matter content of tomatoes is affected by many factors such as electrical conductivity of the growing medium (Van Straten *et al.*, 2006), outdoor climate variations (Segura *et al.*, 2009) and non-optimal temperatures (Adams *et al.*, 2001), model performance can be improved by integrating these effects. To relate fresh matter yield to economic crop yield, a simple humidity-dependent quality filter that determined the marketable tomato fraction and the ratio of first class tomatoes was used. This approach gave a reasonable prediction of economic crop yield, as discussed in chapters 5 and 6. Nevertheless, such a filter had a considerable impact on economic crop yield as shown in Table 5.7 and 5.8. Therefore, uncertainty in the quality parameters will influence the determination of NFR and might affect the optimisation result as well. Therefore, a better description of the quality of fruits and tomato plants as a function of (extreme) climatic conditions (Adams *et al.*, 2001) and diseases should be incorporated into the method. The impact of fertigation on yield was not integrated in the yield model but was assumed to be non-limiting for crop growth. To describe this impact, the nutrient model of Van Straten *et al.* (2006) might be used.

A simple function that described labour costs as a function of crop maintenance and tomato harvest was applied. Although, labour optimisation was outside the scope of this research, a more detailed description of labour costs would be beneficial since it significantly contributes to the annual NFR

Factors that were not incorporated in the model-based design method and which might improve its generality are described hereafter. To keep this study manageable we focussed on: (i) the impact of climate and economic conditions on greenhouse design; (ii) the design elements that influence the aerial climate, i.e. the type of greenhouse structure, the cover type, the outdoor shade screen, the whitewash, the thermal screen, the heating system, the cooling system and the CO₂ enrichment system; and (iii) tomato as model crop.

However, the particular choice of the protected cultivation system depends on more factors according to Van Henten *et al.* (2006) as described in the list presented in the introduction section. Some factors of this list were incorporated in the model-based-design method. Specifically, tomato price, transportation costs and climate were input parameters of the method and the scarcity of resources, i.e. fuels, electricity, water, labour and materials was discounted in the associated prices.

The design method did not take into account social conditions. According to Von Elsner *et al.* (2000), these conditions do influence the adoption rate of greenhouses. For instance, a greenhouse grower with insufficient system knowledge will probably not adopt successfully a high-technology greenhouse. Although not incorporated, the design method could partly deal with the knowledge level of the grower. Generally, with increasing knowledge level, the technology level and maximum investment level of a grower will increase. Using the maximum investment level as optimisation constraint, it might be expected that the optimal greenhouse will match with the technology level of the grower.

The influence of legislation on greenhouse design in terms of food safety, residuals of chemicals, the use and emission of chemicals to soil, water and air were not integrated into the design method. Provided that these aspects are modelled, the current design method could cope with legislation aspects by considering them as optimisation constraints.

Integration of irrigation systems, labour systems and logistics systems would increase the generality of the design method. An example of the consequence of ignoring labour aspects on greenhouse design optimisation was discussed in Chapter 6. Specifically, since beneficial effects of a pipe heating system on labour and some negative effects of a direct air heater were not incorporated, the design method selected for Dutch conditions a direct air heater and not the much more common boiler-pipe rail heating.

To extend the set of eight design elements, several modules should be integrated in the greenhouse climate model. A module that describes the light transmission as a function of season, latitude, orientation, shape, greenhouse dimensions and type of cover material might enable the optimisation of the greenhouse shape and dimensions in more detail. Such a module might be based on models developed by Kozai *et al.* (1978), Critten (1983; 1988) and De Zwart (1993). Since radiation-diffusing materials seem promising in areas with high solar radiation, differentiation between direct and diffuse radiation would allow diffuse properties of cover materials to be optimised. To enable this, the cover transmission module and photosynthesis module must be modified and both the direct and diffuse component of the global radiation should be measured. To describe direct and diffuse indoor radiation as a function of outdoor radiation values, the research of Cabrera *et al.* (2009) can be used as

starting point.

Modules of other climate modification techniques such as co-generation of heat and electricity, application of assimilation light, an active heat buffer, a heat pump and a solar heat collector might be incorporated as well. For optimisation purposes, there is no need to integrate the effects of extreme outdoor conditions such as earthquakes, heavy precipitation and wind on greenhouse design if only greenhouse structures are selected that comply with the local construction norms.

The climate model considers the greenhouse air as a “perfectly stirred tank”. This will limit the evaluation of design elements and processes that are affected by or affect spatial climate differences. Particularly, optimisation of the location of the ventilation openings and the evaluation of undesirable spatial climate differences caused by a pad and fan system, a thermal screen and side ventilation could not be analysed. To analyse and optimise these design aspects, one should apply computational fluid dynamic models as was done by Campen and Bot (2003) and Baeza *et al.* (2009).

The present method can obviously be applied also to other horticultural crops than tomatoes. The yield model and the transpiration model must then be adjusted to the characteristics of the desired crop. Since there is a strong analogy between algae and horticultural crops - both organisms need light, temperature and CO₂ to grow (Norsker *et al.*, 2011; Slegers *et al.*, 2011) - the presented model-based design approach might support the development of an algae producing system as well.

7.1.2.7 Model-based design versus methodical design approach

Greenhouse design can also be approached by the methodical design procedure of Van den Kroonenberg and Siers (1999), which consist of the following steps: (1) definition of design objective; (2) a description of the brief of requirements; (3) a system analysis revealing the required functions; (4) derivation of alternative working principles for each function; (5) concept development stage; (6) design evaluation and bottle-neck assessment; (7) detailed description of the selected designs and (8) the design prototype is built.

The feasibility of this approach was demonstrated by Van 't Ooster *et al.* (2008a) who adjusted the greenhouse designs to different climate zones in Mexico and by Van 't Ooster *et al.* (2008b) who developed a concept for a zero-fossil-energy greenhouse for Dutch conditions. This approach relies on expert knowledge because in step 4 and 5 of this design procedure experts derive alternative working principles and propose a limited set of potential greenhouse designs. Since most experts are not able to take into account all

aspects of the complex design process, their decisions will result in a biased greenhouse design. To avoid this, the developed design method fully relied on objective mathematical models. However, the current design method does not tackle all relevant greenhouse design aspects and therefore a synergy with methodical design will offer opportunities for greenhouse design. Specifically, the design objective in step 1 and the brief of requirements of step 2 can be applied to the model-based design method by considering them as the performance measure and the optimisation constraints respectively. In step 3, experts select the list of design elements that are expected to be beneficial for the given conditions and steps 4 and 5 of the methodical design approach are replaced by the design optimisation, as performed by the model-based design method. Since the design method does not cover all design aspects, experts can evaluate and select the best greenhouse based on the optimisation output.

7.1.3 Future perspectives

The present method can support the development of greenhouses for worldwide conditions, which will improve the productivity of greenhouse horticulture. On the other hand, the model-based design tool could be used as well to select the best location, among a limited number of options, to construct a greenhouse. This is an advantage for both policy makers and growers to pinpoint beneficial locations for protected horticultural production systems. Greenhouses for other crops than tomatoes can be designed as well, provided that suitable yield models are available. The design method can indicate which properties of greenhouse design elements must be adjusted by the industry and what the resulting extra grower's revenue will be. A step further is that the extra revenues of adjustable design parameters are determined. To design greenhouses independently of the applied climate management strategy, the design and climate control should be optimised simultaneously. Such an optimisation approach will theoretically result in the absolute best design. In view of the current evolution to a more sustainable agriculture, it is important to observe that the present design method can also be used to select greenhouse modifications which would reduce the resource consumption of a greenhouse. In addition, the impact of changing economic parameters on the net financial result and on the best greenhouse design can be evaluated as well, which gives an indication how greenhouses should be adjusted to changing price input parameters

Chapter 8

Detailed description of the greenhouse climate model

This model description has been submitted to Biosystems Engineering as an electronic appendix belonging to: *A methodology for model-based greenhouse design: Part 1, A greenhouse climate model for a broad range of designs and climates*

B.H.E. Vanthoor, C. Stanghellini, E.J. van Henten, P.H.B. de Visser

8.1 Introduction

Section 8.2 presents the design elements needed for the greenhouse climate model. The overview and states of the greenhouse climate model are described in section 8.3 and the lumped cover model is described in section 8.4. The model capacities are described in section 8.5. The heat fluxes are described in section 8.6, the vapour fluxes in section 8.7 and the CO₂- fluxes in Section 8.8. The canopy transpiration model is presented in section 8.9. Section 8.10 presents the model equations of the implemented design elements and section 8.11 describes the calculation of unknown outdoor climate inputs. The Nomenclature is presented in section 8.12 and the tables in section 8.13.

8.2 Greenhouse design elements

The selected functions and design elements for the greenhouse design model are presented in Fig. 2.1 in chapter 2. The greenhouse design functions: heating, insulation, shading, cooling, CO₂ enrichment, humidification and de-humidification were fulfilled by one or more design elements. For example, the function heating could thus be fulfilled by the following design elements: the direct air heater, boiler, industrial heat source, geo-thermal source, and a passive buffer. In view of design of protected cultivation systems, the presented design elements are considered to be sufficiently generic for a wide range of locations all over the world. Local particular solutions for energy production, energy conversion or climate modification such as a co-generator, artificial light, an active heat buffer, a heat pump and a solar heat collector lie outside the scope of the current study.

8.3 Model overview and state equations

8.3.1 Notational conventions

All the state variables, fluxes, inputs, superscripts and subscripts are listed in the Nomenclature. All the model parameters and greenhouse design parameters are listed in Table 8.1 and Table 8.2, respectively. For the description of the state variables and the fluxes of the greenhouse climate model, the notational conventions of De Zwart (1996) are used. The state variables of the model are denoted by names with capital letters followed by one subscript, i.e. T_{Air} . The model fluxes start with a capital letter and are followed by two subscripts. The first subscript represents the source of the flux and the second subscript

represents the destination of the flux, i.e. H_{CanAir} . The radiation fluxes start with a capital letter R followed with the type of radiation and then two subscripts to represent the source and sink of the specific radiation, i.e. R_{PAR_SunCan} .

8.3.2 Model overview and assumptions

An overview of the states and the energy and mass fluxes of the greenhouse model is presented in Fig. 2.2. The model is based on the following assumptions:

- greenhouse air is considered to be a “perfectly stirred tank” which means that no spatial differences in temperature, vapour pressure and the CO_2 -concentration occur. Therefore all the model fluxes are described per square metre of greenhouse floor.
- to describe the effect of the thermal screen on the indoor climate, the greenhouse air is divided into two compartments: one below and one above the thermal screen.

8.3.3 States of the model

The states of the model are all described by differential equations. The time derivatives of the states to time are presented by a dot above the state symbol. All symbols are defined in the Nomenclature.

8.3.3.1 Temperature of different greenhouse objects

Canopy temperature T_{Can} is described by:

$$cap_{Can} \dot{T}_{Can} = R_{PAR_SunCan} + R_{NIR_SunCan} + R_{PipeCan} - H_{CanAir} - L_{CanAir} - R_{CanCov,in} - R_{CanFlr} - R_{CanSky} - R_{CanThScr} \quad [W\ m^{-2}] \quad (8.1)$$

where cap_{Can} is the heat capacity of the canopy, R_{PAR_SunCan} is the PAR absorbed by the canopy, R_{NIR_SunCan} is the NIR absorbed by the canopy. FIR is exchanged between the canopy and surrounding elements i.e. the heating pipes $R_{PipeCan}$, the internal cover layer $R_{CanCov,in}$, the floor R_{CanFlr} , the sky R_{CanSky} , and the thermal screen $R_{CanThScr}$. H_{CanAir} is the sensible heat exchange between canopy and greenhouse air and L_{CanAir} is the latent heat flux caused by transpiration.

Greenhouse air temperature T_{Air} is described by:

$$cap_{Air} \dot{T}_{Air} = H_{CanAir} + H_{PadAir} + H_{MechAir} + H_{PipeAir} + H_{PasAir} + H_{BlowAir} + R_{Glob_SunAir} - H_{AirFlr} - H_{AirThScr} - H_{AirOut} - H_{AirTop} - H_{AirOut_Pad} - L_{AirFog} \quad [W\ m^{-2}] \quad (8.2)$$

where cap_{Air} is the heat capacity of the greenhouse air. Sensible heat is exchanged between the greenhouse air and the surrounding elements i.e. the canopy H_{CanAir} , the outlet air of a

cooling pad H_{PadAir} , the mechanical cooling system $H_{MechAir}$, the heating pipes $H_{PipeAir}$, the passive energy buffer H_{PasAir} , the direct air heater $H_{BlowAir}$, the floor H_{AirFlr} , the thermal screen $H_{AirThScr}$, the outdoor air H_{AirOut} , the air of the top compartment which is located above the thermal screen H_{AirTop} , and the outdoor air due to the air exchange caused by the pad and fan system H_{AirOut_Pad} . R_{Glob_SunAir} is the global radiation which is absorbed by the construction elements and which is released to the air and L_{AirFog} is the latent heat needed to evaporate the water droplets added by a fogging system.

The floor layer is the first layer of the greenhouse underground and its temperature T_{Flr} is described by:

$$cap_{Flr} \dot{T}_{Flr} = H_{AirFlr} + R_{PAR_SunFlr} + R_{NIR_SunFlr} + R_{CanFlr} + R_{PipeFlr} - H_{FlrSo1} - R_{FlrCov,in} - R_{FlrSky} - R_{FlrThScr} \quad [W m^{-2}] \quad (8.3)$$

where cap_{Flr} is the heat capacity of the floor; R_{PAR_SunFlr} is the PAR absorbed by the floor; R_{NIR_SunFlr} is the NIR absorbed by the floor; $R_{PipeFlr}$, $R_{FlrCov,in}$, R_{FlrSky} and $R_{FlrThScr}$ are the FIR fluxes between the floor and heating pipes, internal cover layer, sky and thermal screen respectively; and H_{FlrSo1} is the sensible heat flux from the floor to soil layer 1.

Because of the high thermal capacity, the soil was divided into five layers with an increasing thickness with increasing soil depth. The soil temperature $T_{So(j)}$ of layer 'j' is described by:

$$cap_{So(j)} \dot{T}_{So(j)} = H_{So(j-1)So(j)} - H_{So(j)So(j+1)} \quad j = 1, 2, \dots, 5 \quad [W m^{-2}] \quad (8.4)$$

where $cap_{So(j)}$ is the heat capacity of each soil layer, $H_{So(j-1)So(j)}$ is the conductive heat flux from layer 'j-1' to 'j' and $H_{So(j)So(j+1)}$ is the conductive heat flux from layer 'j' to 'j+1'. For the first soil layer, $H_{So(j-1)So(j)}$ is equivalent to H_{FlrSo1} and for the last soil layer, $H_{So(j)So(j+1)}$ is equivalent to the conductive heat flux from the 5th soil layer to the constant external soil temperature $H_{So5SoOut}$ which is described by Eq. (8.78).

Temperature of the thermal screen T_{ThScr} is described by:

$$cap_{ThScr} \dot{T}_{ThScr} = H_{AirThScr} + L_{AirThScr} + R_{CanThScr} + R_{FlrThScr} + R_{PipeThScr} - H_{ThScrTop} - R_{ThScrCov,in} - R_{ThScrSky} \quad [W m^{-2}] \quad (8.5)$$

where cap_{ThScr} is the heat capacity of the thermal screen; $L_{AirThScr}$ is the latent heat flux caused by condensation on the thermal screen; $R_{PipeThScr}$, $R_{ThScrCov,in}$ and $R_{ThScrSky}$ are the FIR fluxes between the thermal screen and the heating pipes, internal cover layer and sky respectively; and $H_{ThScrTop}$ is the heat exchange between the thermal screen and the top

compartment air.

The air temperature of the compartment above the thermal screen T_{Top} , in this study denoted as the ‘top compartment’, is described by:

$$cap_{Top} \dot{T}_{Top} = H_{ThScrTop} + H_{AirTop} - H_{TopCov,in} - H_{TopOut} \quad [W \ m^{-2}] \quad (8.6)$$

where cap_{Top} is the heat capacity of the top compartment air, $H_{TopCov,in}$ is the heat exchange between the top compartment air and the internal cover layer and H_{TopOut} is the heat exchange between the top compartment and the outside air.

The thermal heat conductivity of the greenhouse cover is a greenhouse design parameter which can induce a significant temperature gradient over the cover. Therefore, both the internal cover temperature and external cover temperature have been modelled. Assuming that the heat capacity of the internal and external cover layer each constitute 10% of the heat capacity of the total cover construction, and assuming that conduction of energy is the dominant mode of energy transport between the internal and the external cover, the internal cover temperature $T_{Cov,in}$ and external cover temperature $T_{Cov,e}$ are described by:

$$cap_{Cov,in} \dot{T}_{Cov,in} = H_{TopCov,in} + L_{TopCov,in} + R_{CanCov,in} + R_{FlrCov,in} + R_{PipeCov,in} + R_{ThScrCov,in} - H_{Cov,inCov,e} \quad [W \ m^{-2}] \quad (8.7)$$

$$cap_{Cov,e} \dot{T}_{Cov,e} = R_{Glob_SunCov,e} + H_{Cov,inCov,e} - H_{Cov,eOut} - R_{Cov,eSky} \quad [W \ m^{-2}] \quad (8.8)$$

where $cap_{Cov,in}$ and $cap_{Cov,e}$ are the heat capacities of the internal and external cover layer respectively, $L_{TopCov,in}$ is the latent heat flux caused by condensation on the greenhouse cover, $R_{PipeCov,in}$ is the FIR exchange between the heating pipes and internal cover layer, $H_{Cov,inCov,e}$ is the heat flux between the internal and external cover layer, $R_{Glob_SunCov,e}$ is the absorbed global solar radiation by the cover, $H_{Cov,eOut}$ is the sensible heat flux from the external cover layer to the outside air and $R_{Cov,eSky}$ is the FIR exchange between the cover and the sky.

In this model, besides using a direct air heater, heat energy can be added to the greenhouse air using hot water heating pipes (Fig. 2.2). The surface temperature of the heating pipe system T_{Pipe} is described by:

$$cap_{Pipe} \dot{T}_{Pipe} = H_{BoilPipe} + H_{IndPipe} + H_{GeoPipe} - R_{PipeSky} - R_{PipeCov,in} - R_{PipeCan} - R_{PipeFlr} - R_{PipeThScr} - H_{PipeAir} \quad [W \ m^{-2}] \quad (8.9)$$

where cap_{Pipe} is the heat capacity of the heating pipes, $H_{BoilPipe}$ is the boiler heat flux to the pipes, $H_{IndPipe}$ is the industrial heat flux to the pipes, $H_{GeoPipe}$ is the geothermal heat flux to the pipes and $R_{PipeSky}$, is the FIR exchange between the pipes and sky.

8.3.3.2 Vapour pressure of the greenhouse air and the air in the top compartment

The vapour pressure of the greenhouse air VP_{Air} is described by:

$$cap_{VP_{Air}} \dot{VP}_{Air} = MV_{CanAir} + MV_{PadAir} + MV_{FogAir} + MV_{BlowAir} - MV_{AirThScr} - MV_{AirTop} - MV_{AirOut} - MV_{AirOut_Pad} - MV_{AirMech} \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.10)$$

where $cap_{VP_{Air}}$ is the capacity of the air to store water vapour. Vapour is exchanged between the air and surrounding elements i.e. the canopy MV_{CanAir} , the outlet air of the pad MV_{PadAir} , the fogging system MV_{FogAir} , the direct air heater $MV_{BlowAir}$, the thermal screen $MV_{AirThScr}$, the top compartment air MV_{AirTop} , the outdoor air MV_{AirOut} , the outdoor air due to the air exchange caused by the pad and fan system MV_{AirOut_Pad} , and the mechanical cooling system $MV_{AirMech}$.

The vapour pressure of the air in the top compartment VP_{Top} is described by:

$$cap_{VP_{Top}} \dot{VP}_{Top} = MV_{AirTop} - MV_{TopCov,in} - MV_{TopOut} \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.11)$$

where $cap_{VP_{Top}}$ is the capacity of the top compartment to store water vapour, $MV_{TopCov,in}$ is the vapour exchange between the top compartment and the internal cover layer and MV_{TopOut} is the vapour exchange between the top compartment and the outside air.

8.3.3.3 CO₂-concentration of the greenhouse air and the air in the top compartment

The greenhouse air CO₂ concentration CO_{2Air} is described by:

$$cap_{CO_{2Air}} \dot{CO}_{2Air} = MC_{BlowAir} + MC_{ExtAir} + MC_{PadAir} - MC_{AirCan} - MC_{AirTop} - MC_{AirOut} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.12)$$

where $cap_{CO_{2Air}}$ is the capacity of the air to store CO₂. Carbon dioxide is exchanged between the greenhouse air and surrounding elements i.e. the direct air heater $MC_{BlowAir}$, the external CO₂ source MC_{ExtAir} , the pad and fan system MC_{PadAir} , the top compartment air MC_{AirTop} and the outdoor air MC_{AirOut} . MC_{AirCan} is the CO₂ flux between the greenhouse air and the canopy as described in chapter 3.

The CO₂ concentration of the top compartment air CO_{2Top} is described by:

$$cap_{CO_{2Top}} \dot{CO}_{2Top} = MC_{AirTop} - MC_{TopOut} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.13)$$

where cap_{CO_2Top} is the capacity of the top compartment air to store CO_2 , MC_{TopOut} is the CO_2 exchange between the top compartment air and the outside air.

8.4 Lumped cover layers

The model contains four cover layers, i.e. a movable outdoor shading screen, a semi-permanent shading screen, the greenhouse roof and a movable indoor thermal screen. These cover layers have a combined influence on the overall optical properties, i.e. transmission, reflection and absorption coefficients of the cover. To simplify the model, individual properties of the four cover layers are lumped together. Assumptions concerning the lumped cover are:

- All four cover layers influence the transmission, reflection and absorption of PAR, NIR and FIR of the greenhouse
- The semi-permanent shading screen is a coating on the roof and therefore it influences the thermal heat conductance and the heat capacity of the cover
- The movable outdoor shading screen has generally an open structure and consequently the temperature below the shading screen equals the outdoor temperature. Therefore the movable outdoor shading screen does not influence the thermal heat conductance and the heat capacity of the lumped cover.
- The use of an outdoor shading screen will influence the ventilation discharge coefficients.
- The convective heat exchange coefficients of the cover are not influenced by the use of one or more screens.

These assumptions imply that the optical properties of PAR, NIR and FIR of all four cover layers must be lumped together. Furthermore, the thermal heat conductance and the heat capacity of the lumped cover depend on the thermal heat conductance and the heat capacity of both the roof as well as the semi-permanent shading screen.

The PAR and NIR transmission of the cover is a combined transmission of the four cover layers. The total cover PAR and NIR transmission is calculated according to the EN 410 standard (Anonymous, 1998) by determining first the transmission and reflection coefficient of the first 2 layers and subsequently the last 2 layers. Secondly, for these 2 combined layers the overall cover transmission is calculated.

The transmission coefficient τ_{12} (-) and the reflection coefficient ρ_{12} (-) of a double layer cover are determined according the EN 410 standard (Anonymous, 1998):

$$\tau_{12} = \frac{\tau_1 \tau_2}{1 - \rho_1 \rho_2} \quad [-] \quad (8.14)$$

$$\rho_{12} = \rho_1 + \frac{\tau_1^2 \rho_2}{1 - \rho_1 \rho_2} \quad [-] \quad (8.15)$$

where τ_1 (-) and τ_2 (-) are the transmission coefficients of the first and second layer respectively, ρ_1 (-) and ρ_2 (-) are the reflection coefficients of the first and second layer respectively.

An example of the calculation of the optical properties of PAR for the lumped cover is presented. The optical properties for NIR are calculated in a similar way. Firstly, the transmission coefficient and the reflection coefficient of the first 2 cover layers are calculated in order to determine the PAR transmission coefficient and PAR reflection coefficient of the total greenhouse cover.

The first two layers can be controlled and therefore the transmission coefficient, $\tau_{ShScr_ShScrPer}$ and the reflection coefficient $\rho_{ShScr_ShScrPer}$ of the movable shading screen and the semi-permanent shading screen are determined by:

$$\tau_{ShScr_ShScrPerPAR} = \frac{(1 - U_{ShScr}(1 - \tau_{ShScrPAR}))(1 - U_{ShScrPer}(1 - \tau_{ShScrPerPAR}))}{1 - U_{ShScr}\rho_{ShScrPAR}U_{ShScrPer}\rho_{ShScrPerPAR}} \quad [-] \quad (8.16)$$

$$\rho_{ShScr_ShScrPerPAR} = U_{ShScr}\rho_{ShScrPAR} + \frac{(1 - U_{ShScr}(1 - \tau_{ShScrPAR}))^2 U_{ShScrPer}\rho_{ShScrPerPAR}}{1 - U_{ShScr}\rho_{ShScrPAR}U_{ShScrPer}\rho_{ShScrPerPAR}} \quad [-] \quad (8.17)$$

where U_{ShScr} (-) is the control of the movable shading screen, $U_{ShScrPer}$ (-) is the control of the semi-permanent shading screen, $\tau_{ShScrPAR}$ (-) is the PAR transmission coefficient of the movable shading screen, $\tau_{ShScrPerPAR}$ (-) is the PAR transmission coefficient of the semi-permanent shading screen, $\rho_{ShScrPAR}$ (-) is the reflection coefficient of the movable shading screen and $\rho_{ShScrPerPAR}$ (-) is the reflection coefficient of the semi permanent shading screen. Secondly, the transmission coefficient and the reflection coefficient of the last 2 cover layers, i.e. the greenhouse roof and the thermal screen, are calculated analogously to

Eqs. (8.16) and (8.17). Thirdly, the transmission coefficient τ_{CovPAR} and the reflection coefficient ρ_{CovPAR} of the lumped cover are determined using Eqs. (8.14) and (8.15) by filling in the transmission and reflection coefficients of the two combined layers. The absorption coefficient of the lumped cover, a_{GhPAR} , is one minus the sum of the transmission and reflection coefficient.

The optical properties of FIR for the lumped cover depend on the optical properties of FIR of the semi-permanent shading screen, the movable shading screen and the roof and they are calculated analogously to the optical properties of PAR. The FIR emission coefficient of the lumped cover, ϵ_{CovFIR} (-), equals the FIR absorption coefficient a_{CovFIR} .

The heat capacity of the lumped cover is described by:

$$cap_{Cov} = \cos(\psi) \left(U_{ShScrPer} h_{ShScrPer} \rho_{ShScrPer} c_{p,ShScrPer} + h_{Rf} \rho_{Rf} c_{p,Rf} \right) \quad [\text{J K}^{-1} \text{m}^{-2}] \quad (8.18)$$

where ψ is the mean greenhouse cover slope ($^{\circ}$), $U_{ShScrPer}$ (-) is the control of the semi permanent shading screen, $h_{ShScrPer}$ (m) is the thickness, $\rho_{ShScrPer}$ (kg m^{-3}) is the density and $c_{p,ShScrPer}$ ($\text{J K}^{-1} \text{kg}^{-1}$) is the specific heat capacity of the semi permanent shading screen, h_{Rf} (m) is the thickness, ρ_{Rf} (kg m^{-3}) is the density and $c_{p,Rf}$ ($\text{J K}^{-1} \text{kg}^{-1}$) is the specific heat capacity of the roof layer.

The conductive heat flux through the lumped cover depends on the thickness and the thermal heat conductivity of both the semi permanent shading screen and the roof :

$$HEC_{Cov,inCov,e} = \frac{1}{\frac{h_{Rf}}{\lambda_{Rf}} + U_{ShScrPer} \frac{h_{ShScrPer}}{\lambda_{ShScrPer}}} \quad [\text{W m}^{-2} \text{K}^{-1}] \quad (8.19)$$

where λ_{Rf} ($\text{W m}^{-1} \text{K}^{-1}$) is the thermal heat conductivity of the roof and $\lambda_{ShScrPer}$ ($\text{W m}^{-1} \text{K}^{-1}$) is the thermal heat conductivity of semi permanent shading screen.

8.5 Capacities

The heat capacity of the canopy, cap_{Can} , is described by:

$$cap_{Can} = cap_{Leaf} \cdot LAI \quad [J K^{-1} m^{-2}] \quad (8.20)$$

where cap_{Leaf} ($J K^{-1} m^{-2}$ leaf) is the heat capacity of a square meter of canopy and LAI is the leaf area index (m^2 leaf m^{-2}).

The heat capacity of the external and internal cover is assumed to be 10% of the total heat capacity of the lumped cover and is therefore described by:

$$cap_{Cov,e} = cap_{Cov,in} = 0.1 cap_{Cov} \quad [J K^{-1} m^{-2}] \quad (8.21)$$

where cap_{Cov} ($J K^{-1} m^{-2}$) is the heat capacity of the lumped cover.

The heat capacity of the heating pipes is an aggregated heat capacity combining the heat capacity of the steel pipe and of the water inside the pipe:

$$cap_{Pipe} = 0.25\pi l_{Pipe} \left((\phi_{Pipe,e}^2 - \phi_{Pipe,i}^2) \rho_{Steel} c_{p,Steel} + \phi_{Pipe,i}^2 \rho_{Water} c_{p,Water} \right) \quad [J K^{-1} m^{-2}] \quad (8.22)$$

where l_{Pipe} ($m m^{-2}$) is the length of the heating pipe per square meter greenhouse,

$\phi_{Pipe,e}$ (m) is the external diameter of the heating pipe, $\phi_{Pipe,i}$ (m) is the internal diameter of the heating pipe, ρ_{Steel} ($kg m^{-3}$) is the density of steel, $c_{p,Steel}$ ($J K^{-1} kg^{-1}$) is the specific heat capacity of steel, ρ_{Water} is the density of water ($kg m^{-3}$) and $c_{p,Water}$ ($J K^{-1} kg^{-1}$) is the specific heat capacity of water.

The heat capacity of the remaining greenhouse objects is described by

$$cap_{Obj} = h_{Obj} \rho_{Obj} c_{p,Obj} \quad [J K^{-1} m^{-2}] \quad (8.23)$$

where h_{Obj} (m) is the mean height of the greenhouse object, ρ_{Obj} ($kg m^{-3}$) is the density of the greenhouse object and $c_{p,Obj}$ ($J K^{-1} kg^{-1}$) is the specific heat capacity of the object. The capacity of the objects, cap_{Air} , cap_{Flr} , $cap_{So(j)}$, cap_{ThScr} and cap_{Top} are described in an similar way as Eq. (8.23).

The density of the air is elevation dependent and by assuming a mean air temperature of 20 °C the density of the air is calculated by:

$$\rho_{Air} = \rho_{Air0} \exp\left(\frac{g M_{Air} h_{Elevation}}{293.15 R}\right) \quad [kg m^{-3}] \quad (8.24)$$

where ρ_{Air0} (kg m^{-3}) is the air density at sea level, g (m s^{-2}), is the acceleration of gravity, M_{Air} (kg kmol^{-1}) is the molar mass of air, $h_{Elevation}$ (m) is the altitude of the greenhouse above sea level and R ($\text{J kmol}^{-1} \text{K}^{-1}$) is the molar gas constant.

The conversion factor from the water vapour pressure to the water vapour mass per square meter greenhouse of the air compartment below the thermal screen is described by a water vapour capacity of the air compartment:

$$cap_{VP_{Air}} = \frac{M_{Water} h_{Air}}{R(T_{Air} + 273.15)} \quad [\text{kg m}^3 \text{J}^{-1}] \quad (8.25)$$

where M_{Water} (kg kmol^{-1}) is the molar mass of water, h_{Air} (m) is the height from the floor to the thermal screen, R ($\text{J kmol}^{-1} \text{K}^{-1}$) is the molar gas constant. The water vapour capacity of the top compartment, $cap_{VP_{Top}}$, is described with a similar equation as Eq. (8.25).

The conversion factor from the CO_2 concentration of the air compartment below the thermal screen to the CO_2 mass per square meter greenhouse, $cap_{CO_2_{Air}}$ (m), equals the height from the floor to the thermal screen, h_{Air} . The conversion factor from the CO_2 concentration of the top compartment to the CO_2 mass per square metre greenhouse, $cap_{CO_2_{Top}}$ (m), equals the mean height of the greenhouse minus the height from the floor to the thermal screen.

8.6 Heat fluxes

8.6.1 Global, PAR and NIR heat fluxes

The PAR absorbed by the canopy (R_{PAR_SunCan}) is the sum of the PAR transmitted by the greenhouse cover that is directly absorbed by the canopy ($R_{PAR_SunCan\downarrow}$), and the PAR that is first reflected by the greenhouse floor and then is absorbed by the canopy ($R_{PAR_FlrCan\uparrow}$):

$$R_{PAR_SunCan} = R_{PAR_SunCan\downarrow} + R_{PAR_FlrCan\uparrow} \quad [\text{W m}^{-2}] \quad (8.26)$$

The PAR which is directly absorbed by the canopy is described by a negative exponential decay of light with LAI in a homogeneous crop (Ross, 1975):

$$R_{PAR_SunCan\downarrow} = R_{PAR_Gh} \cdot (1 - \rho_{CanPAR}) \cdot \left(1 - e^{-K_{l_PAR} \cdot LAI}\right) \quad [\text{W m}^{-2}] \quad (8.27)$$

where R_{PAR_Gh} (W m^{-2}) is the PAR above the canopy, ρ_{CanPAR} (-) is the reflection coefficient of the canopy for PAR and K_{L_PAR} (-) is the extinction coefficient of the canopy for PAR.

The PAR above the canopy is described by:

$$R_{PAR_Gh} = (1 - \eta_{Glob_Air}) \cdot \tau_{CovPAR} \cdot \eta_{Glob_PAR} \cdot I_{Glob} \quad [\text{W m}^{-2}] \quad (8.28)$$

where η_{Glob_Air} (-) is the ratio of the global radiation which is absorbed by the greenhouse construction elements, τ_{CovPAR} (-) is the PAR transmission coefficient of the greenhouse cover, η_{Glob_PAR} is the ratio between PAR and the global radiation and I_{Glob} (W m^{-2}) is the outside global radiation. The PAR transmission of the cover depends on the PAR transmission of the following design elements: the roof, a semi-permanent cover additive, the movable shading screen and the movable thermal screen (Section 8.4).

The PAR that is absorbed by the canopy after reflection by the greenhouse floor is described by:

$$R_{PAR_FlrCan\uparrow} = R_{PAR_Gh} \cdot e^{-K_{1_PAR} \cdot LAI} \cdot \rho_{FlrPAR} \cdot (1 - \rho_{CanPAR}) \cdot (1 - e^{-K_{2_PAR} \cdot LAI}) \quad [\text{W m}^{-2}] \quad (8.29)$$

where ρ_{FlrPAR} (-) is the reflection coefficient of the greenhouse floor for PAR and K_{2_PAR} (-) is the extinction coefficient for PAR that is reflected from the floor to the canopy.

The NIR reflection coefficient of the canopy is considerably higher than the PAR reflection coefficient. Consequently, a large amount of the NIR is either reflected by the canopy back to the greenhouse cover or is scattered through the canopy to the greenhouse floor. The greenhouse cover and greenhouse floor may reflect the NIR back into the greenhouse again leading to a considerable scattering of NIR in the greenhouse. Because the NIR reflection coefficient of both the cover and floor are greenhouse design parameters, the NIR fluxes in the greenhouses model account for all these reflections.

The NIR absorbed by the canopy and by the floor was determined by considering the lumped cover, the canopy and the floor as a multiple layer model. To assure that the NIR absorption coefficient determined by this multiple-layer model equals the overall NIR absorption coefficient of the canopy, virtual NIR transmission coefficients of the lumped cover and floor were used:

$$\begin{aligned} \hat{\tau}_{CovNIR} &= 1 - \rho_{CovNIR} \\ \hat{\tau}_{FlrNIR} &= 1 - \rho_{FlrNIR} \end{aligned} \quad [-] \quad (8.30)$$

To solve the multiple-layer model, first the transmission and reflection coefficient for NIR of the canopy must be determined. Using the relationship between the LAI and the diffuse NIR absorption by the canopy of De Zwart (1996), the NIR transmission coefficient of the canopy is described by:

$$\hat{\tau}_{CanNir} = e^{-K_{NIR} \cdot LAI} \quad [-] \quad (8.31)$$

where $\hat{\tau}_{CanNir}$ (-) is the NIR transmission coefficient of the canopy and K_{NIR} is the extinction coefficient of the canopy for NIR (-). The NIR reflection coefficient of the canopy depends on the LAI which is described by:

$$\hat{\rho}_{CanNIR} = \rho_{CanNIR} (1 - \hat{\tau}_{CanNir}) \quad [-] \quad (8.32)$$

The NIR transmission, reflection and absorption coefficients of the multiple-layers are determined by implementing the NIR transmission and reflection coefficients of the individual layers in the multiple-layer model in a similar way as Eqs. (8.14)-(8.17). Subsequently, the calculated absorption coefficient of the multiple-layers equals the overall NIR absorption coefficient of the canopy a_{CanNIR} and the calculated transmission coefficient of the multiple-layers equals the overall NIR absorption coefficient of the floor, a_{FlrNIR} .

The NIR absorbed by the canopy and by the floor is described by:

$$R_{NIR_SunCan} = (1 - \eta_{Glob_Air}) \cdot a_{CanNIR} \cdot \eta_{Glob_NIR} \cdot I_{Glob} \quad [W\ m^{-2}] \quad (8.33)$$

$$R_{NIR_SunFlr} = (1 - \eta_{Glob_Air}) \cdot a_{FlrNIR} \cdot \eta_{Glob_NIR} \cdot I_{Glob} \quad [W\ m^{-2}] \quad (8.34)$$

The PAR absorbed by the greenhouse floor is described by:

$$R_{PAR_SunFlr} = (1 - \rho_{FlrPAR}) \cdot e^{-K_{1_PAR} \cdot LAI} \cdot R_{PAR_Gh} \quad [W\ m^{-2}] \quad (8.35)$$

It was assumed that the global radiation which is absorbed by the greenhouse construction elements is directly released to the greenhouse air:

$$R_{Glob_SunAir} = \eta_{Glob_Air} I_{Glob} (\tau_{CovPAR} \eta_{Glob_PAR} + (a_{CanNIR} + a_{FlrNIR}) \eta_{Glob_NIR}) [W\ m^{-2}] \quad (8.36)$$

The global solar radiation that is absorbed by the cover, $R_{Glob_SunCov,e}$, is described by:

$$R_{Glob_SunCov,e} = (a_{GhPAR} \cdot \eta_{Glob_PAR} + a_{GhNIR} \cdot \eta_{Glob_NIR}) I_{Glob} \quad [W\ m^{-2}] \quad (8.37)$$

where a_{GhPAR} (-) is the PAR absorption coefficient of the greenhouse cover, a_{GhNIR} (-) is the NIR absorption coefficient of the greenhouse cover. Both absorption coefficients are determined in Section 8.4.

8.6.2 FIR heat fluxes

The net far infrared radiation fluxes from surface 'i' to 'j', FIR_{ij} are described by:

$$FIR_{ij} = A_i \varepsilon_i \varepsilon_j F_{ij} \sigma \left((T_i + 273.15)^4 - (T_j + 273.15)^4 \right) \quad [\text{W m}^{-2}] \quad (8.38)$$

where A_i ($\text{m}^2 \text{ m}^{-2}$) is the surface of object 'i' per square meter greenhouse soil, ε_i (-) and ε_j (-) are the thermal infrared emission coefficients for object 'i' and 'j' respectively, F_{ij} (-) is the view factor from object 'i' to 'j', σ ($\text{W m}^{-2} \text{ K}^{-4}$) is the Stefan Boltzmann constant, T_i ($^{\circ}\text{C}$) and T_j ($^{\circ}\text{C}$) are the temperatures of object 'i' and 'j' respectively. Table 8.3 shows the equations of A_i and F_{ij} for all the FIR fluxes based upon De Zwart (1996). These FIR fluxes are only valid in a greenhouse where the heating pipes are located below the canopy.

The accompanying emission coefficients are shown in Table 8.1. Some cover materials are partly transparent for FIR. Therefore, the FIR fluxes from the greenhouse objects (canopy, heating pipe and floor) to the sky are described. To describe the effect of the thermal screen on the FIR fluxes, FIR transmission coefficient is used which depends on the control of the thermal screen and on the physical properties of the thermal screen:

$$\tau_{ThScrTIR}^U = 1 - U_{ThScr} (1 - \tau_{ThScrTIR}) \quad [-] \quad (8.39)$$

8.6.3 Convection and conduction

Convective and conductive heat fluxes are described by:

$$H_{12} = HEC_{12} (T_1 - T_2) \quad [\text{W m}^{-2}] \quad (8.40)$$

where H_{12} (W m^{-2}) is the heat flow from object 1 to object 2, HEC_{12} ($\text{W m}^{-2} \text{ K}^{-1}$) is the heat exchange coefficient between object 1 and 2, T_1 is the temperature of object 1 and T_2 is the temperature of object 2. All the convective and conductive heat fluxes and their heat exchange coefficients are presented in Table 8.4.

The natural ventilation flows $f_{VentSide}$ and $f_{VentRoof}$ presented in Table 8.4 are described in Section 8.10.7 and the forced ventilation flow $f_{VentForced}$, is described in Section 8.10.8. The air flux rate through the thermal screen f_{ThScr} ($\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}$) is based on (De Zwart, 1996) and is described by:

$$f_{ThScr} = U_{ThScr} K_{ThScr} |T_{Air} - T_{out}|^{0.66} + \frac{1 - U_{ThScr}}{\rho_{Air}^{Mean}} \left(0.5 \rho_{Air}^{Mean} (1 - U_{ThScr}) g |\rho_{Air} - \rho_{Out}| \right)^{0.5} \quad [\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}] \quad (8.41)$$

where K_{ThScr} ($\text{m}^3 \text{ m}^{-2} \text{ K}^{-0.66} \text{ s}^{-1}$) is the screen flux coefficient which determines the permeability of the screen, g (m s^{-2}) is the gravitational acceleration, ρ_{Air} (kg m^{-3}) is the density of the greenhouse air, ρ_{Out} (kg m^{-3}) is the density of the outdoor air and ρ_{Air}^{Mean} (kg m^{-3}) is the mean density of the greenhouse and the outdoor air.

8.6.4 Latent heat fluxes

The latent heat flux is the energy which is exchanged when water becomes water vapour (canopy transpiration) or when water vapour becomes water (condensation). The latent heat flux is linearly related with its associated vapour flux:

$$L_{12} = \Delta H \cdot MV_{12} \quad [\text{W m}^{-2}] \quad (8.42)$$

where L_{12} (W m^{-2}) is the latent heat flux from object 1 to object 2, ΔH (J kg^{-1} water) is the heat of evaporation and MV_{12} ($\text{kg m}^{-2} \text{ s}^{-1}$) is the vapour flux from object 1 to object 2.

The latent heat fluxes, L_{CanAir} , $L_{AirThScr}$ and $L_{TopCov,in}$ are described analogously to Eq. (8.42), their accompanying vapour fluxes are described in Section 8.7 and 8.9.

8.7 Vapour fluxes

The vapour exchange coefficient between the air and an object is linearly related to the convective heat exchange coefficient between the air and the object. Therefore, the vapour flux from the air to an object by condensation is described by:

$$MV_{12} = \begin{cases} 0 & VP_1 < VP_2 \\ 6.4 \cdot 10^{-9} HEC_{12} (VP_1 - VP_2) & VP_1 > VP_2 \end{cases} \quad [\text{kg m}^{-2} \text{ s}^{-1}] \quad (8.43)$$

where MV_{12} ($\text{kg m}^{-2} \text{ s}^{-1}$) is the vapour flux from air of location 1 to object 2, $6.4 \cdot 10^{-9}$ is the conversion factor relating the heat exchange coefficient ($\text{W m}^{-2} \text{ K}^{-1}$) to the vapour exchange coefficient ($\text{kg m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1}$), HEC_{12} ($\text{W m}^{-2} \text{ K}^{-1}$) is the heat exchange coefficient between the air of location 1 to object 2 and VP_1 (Pa) is the vapour pressure of the air of location 1 and VP_2 (Pa) is the saturated vapour pressure of object 2 at its temperature.

Because the model should consist of only differentiable equations, Eq. (8.43) was smoothed using a differentiable ‘switch function’ to yield:

$$MV_{12} = \frac{1}{1 + \exp(s_{MV_{12}}(VP_1 - VP_2))} 6.4 \cdot 10^{-9} HEC_{12}(VP_1 - VP_2) \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.44)$$

where $s_{MV_{12}}(-)$ is the slope of the differentiable switch function for vapour pressure differences.

The vapour flux from the greenhouse air compartment to the thermal screen, $MV_{AirThScr}$ and the vapour flux from the top compartment to the internal cover layer, $MV_{TopCov,in}$, are described analogously to Eq. (8.43). Their associated heat exchange coefficients are listed in Table 8.4.

The general form of a vapour flux accompanying an air flux is described by:

$$MV_{12} = \frac{M_{Water}}{R} f_{12} \left(\frac{VP_1}{T_1 + 273.15} - \frac{VP_2}{T_2 + 273.15} \right) \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.45)$$

where MV_{12} is the vapour flux from location 1 to location 2, $f_{12} (\text{m}^3 \text{m}^{-2} \text{s}^{-1})$ is the air flux from location 1 to location 2, T_1 (°C) is the temperature at location 1 and T_2 (°C) is the temperature at location 2.

The vapour fluxes, MV_{AirTop} , MV_{AirOut} and MV_{TopOut} are described analogously to Eq. (8.45) whereby their accompanying air fluxes are f_{ThScr} (the flux through the thermal screen), $f_{VentSide} + f_{VentForced}$ (the flux due to natural ventilation through the side windows or forced ventilation) and $f_{VentRoof}$ (flux due to roof ventilation) respectively.

8.8 CO₂ fluxes

The general form of a CO₂ flux accompanying an air flux is described by:

$$MC_{12} = f_{12}(CO_{2,1} - CO_{2,2}) \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.46)$$

where MC_{12} is the CO₂ flux from location 1 to location 2, $f_{12} (\text{m}^3 \text{m}^{-2} \text{s}^{-1})$ is the air flux from location 1 to location 2, $CO_{2,1} (\text{mg m}^{-3})$ is the CO₂-concentration at location 1 and $CO_{2,2} (\text{mg m}^{-3})$ is the CO₂-concentration at location 2. The CO₂ fluxes, MC_{AirTop} , MC_{AirOut} and MC_{TopOut} are described analogously to Eq. (8.46) whereby their related air

fluxes are f_{ThScr} , $f_{VentSide} + f_{VentForced}$ and $f_{VentRoof}$ respectively.

The net CO₂ flux from the air to the canopy MC_{AirCan} depends on the canopy photosynthesis rate and respiration processes which were described in chapter 3.

8.9 Canopy transpiration

The canopy transpiration is described by:

$$MV_{CanAir} = VEC_{CanAir} (VP_{Can} - VP_{Air}) \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.47)$$

where VEC_{CanAir} (kg Pa s⁻¹) is the vapour exchange coefficient between the canopy and air, VP_{Can} is the saturated vapour pressure at canopy temperature. According to Stanghellini (1987) the vapour transfer coefficient of the canopy transpiration can be calculated by:

$$VEC_{CanAir} = \frac{2\rho_{Air}c_{p,Air}LAI}{\Delta H\gamma(r_b + r_s)} \quad [\text{kg m}^{-2} \text{Pa}^{-1} \text{s}^{-1}] \quad (8.48)$$

where ρ_{Air} (kg m⁻³) is the density of the greenhouse air, $c_{p,Air}$ (J K⁻¹ kg⁻¹) is the specific heat capacity of the greenhouse air, LAI (m² m⁻²) is the leaf area index, ΔH (J kg⁻¹) is the latent heat of evaporation of water, γ (Pa K⁻¹) is the psychometric constant, r_b (s m⁻¹) is the boundary layer resistance of the canopy for vapour transport and r_s (s m⁻¹) is the stomatal resistance of the canopy for vapour transport.

The boundary layer resistance for vapour transport depends on the wind speed in the greenhouse and the temperature difference between the canopy and surrounding air (Stanghellini, 1987). However, the wind speed in the greenhouse is not measured nor simulated and therefore a constant boundary layer resistance was used. The stomatal resistance of the canopy is described by a simplification of the stomatal resistance model of Stanghellini (1987) :

$$r_s = r_{s,min} \cdot rf(R_{Can}) \cdot rf(CO_{2,Air_ppm}) \cdot rf(VP_{Can} - VP_{Air}) \quad [\text{s m}^{-1}] \quad (8.49)$$

where $r_{s,min}$ (s m⁻¹) is the minimum canopy resistance and rf is the resistance factor for high radiation levels, high CO₂ levels and large vapour pressure differences. The resistance factors are described according to Stanghellini (1987):

$$\begin{aligned}
rf(R_{Can}) &= \frac{R_{Can} + c_{evap1}}{R_{Can} + c_{evap2}} \\
rf(CO_{2Air}) &= 1 + c_{evap3} (\eta_{mg_ppm} CO_{2Air} - 200)^2 \\
rf(VP_{Can} - VP_{Air}) &= 1 + c_{evap4} (VP_{Can} - VP_{Air})^2
\end{aligned}
\quad [-] \quad (8.50)$$

where R_{Can} ($W\ m^{-2}$) is the global radiation above the canopy, c_{evap1} ($W\ m^{-2}$), c_{evap2} ($W\ m^{-2}$), c_{evap3} (ppm^{-2}) c_{evap4} (Pa^{-2}) are empirically determined parameters and η_{mg_ppm} ($ppm\ mg^{-1}\ m^3$) is the conversion factor from $mg\ m^{-3}\ CO_2$ to ppm. Stanghellini limited the resistance factor for high CO_2 levels to 1.5 and the resistance factor for large vapour pressure differences to 5.8 and determined the transpiration variables c_{evap3} and c_{evap4} for day time and night time. The values of the transpiration parameters c_{evap3} and c_{evap4} differed between the night period and day period which means that the accompanying equations are not differentiable at sunrise and sunset. Therefore the parameters c_{evap3} and c_{evap4} were smoothed to make Eq. (8.50) differentiable using the differentiable switch function:

$$S_{r_s} = \frac{1}{1 + \exp(s_{r_s} (R_{Can} - R_{Can_SP}))} \quad [-] \quad (8.51)$$

where S_{r_s} (-) is the value of the differentiable switch, s_{r_s} ($m\ W^{-2}$) is the slope of the differentiable switch for the stomatal resistance model and R_{Can_SP} ($W\ m^{-2}$) is the radiation value above the canopy to define sunrise and sunset. Using the differential switch, the smoothed transpiration parameters were described by:

$$c_{evap3} = c_{evap3}^{night} (1 - S_{r_s}) + c_{evap3}^{day} S_{r_s} \quad [-] \quad (8.52)$$

The parameter c_{evap4} was described analogously to parameter c_{evap3} .

8.10 Greenhouse design elements

The design elements presented in Fig. 2.1 in chapter 2 are described in this section. All the control inputs, U , have a control range from zero to one.

8.10.1 Direct air heater

The heat flux from the direct air heater to the greenhouse air is described by:

$$H_{BlowAir} = U_{Blow} P_{Blow} / A_{Flr} \quad [\text{W m}^{-2}] \quad (8.53)$$

where U_{Blow} is the control valve of the direct air heater (-), P_{Blow} (W) is the heat capacity of the direct air heaters and A_{Flr} (m²) is the surface of the greenhouse floor.

The CO₂ flux from the heat blower to the greenhouse air is proportional to the heat flux:

$$MC_{BlowAir} = \eta_{HeatCO_2} H_{BlowAir} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.54)$$

where η_{HeatCO_2} (mg CO₂ J⁻¹) is the amount of CO₂ which is released when 1 Joule of sensible energy is produced by the direct air heater.

The vapour flux from the heat blower to the greenhouse air is proportional to the heat flux:

$$MV_{BlowAir} = \eta_{HeatVap} H_{BlowAir} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.55)$$

where $\eta_{HeatVap}$ (kg vapour J⁻¹) is the amount of vapour which is released when 1 Joule of sensible energy is produced by the direct air heater.

8.10.2 Heat from a boiler and from industrial and/or geothermal sources

The heat flux from the boiler to the heating pipe is described by:

$$H_{BoilPipe} = U_{Boil} P_{Boil} / A_{Flr} \quad [\text{W m}^{-2}] \quad (8.56)$$

where U_{Boil} is the control valve of the heat boiler (-), P_{Boil} (W) is the heat capacity of the boiler and A_{Flr} (m²) is the surface of the greenhouse floor. The heat flux to the heating pipes from an industrial source $H_{IndPipe}$ and the geothermal source $H_{GeoPipe}$ are described analogously to Eq. (8.56).

8.10.3 Passive heat storage

In this study, passive heat storage was considered to be a facility that could store durable heat coming from the sun. The most important design parameters of such a passive heat storage mechanisms are modelled by assuming that a soil layer represents the passive heat buffer. The heat flux from the buffer to the greenhouse air, H_{PasAir} , depends on the heat exchange coefficient of the passive heat storage facility and the temperature difference between the passive heat buffer and the greenhouse air:

$$H_{PasAir} = HEC_{PasAir} (T_{So3} - T_{Air}) \quad [\text{W m}^{-2}] \quad (8.57)$$

where HEC_{PasAir} is the convective heat exchange coefficient between soil layer three and the greenhouse air temperature, T_{So3} is the temperature of the third soil layer and T_{Air} is the greenhouse air temperature. Soil layer three was selected as a passive heat buffer because the temperature of this layer has a time delay of about 12 hours with respect to the greenhouse air, due to temperature oscillations in the soil on a 24 hour base, which favours the efficiency of the passive heat storage.

8.10.4 Pad and fan cooling

The vapour flux from the pad and fan to the greenhouse air is described by:

$$MV_{PadAir} = \rho_{Air} f_{Pad} (\eta_{Pad} (x_{Pad} - x_{Out}) + x_{Out}) \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.58)$$

where f_{Pad} ($\text{m}^3 \text{m}^{-2} \text{s}^{-1}$) is the ventilation flux due to the pad and fan system, η_{Pad} (-) is the efficiency of the pad and fan system, x_{Pad} ($\text{kg water kg}^{-1} \text{air}$) is the water vapour content of the pad and x_{Out} ($\text{kg water kg}^{-1} \text{air}$) is the water vapour content of the outdoor air. The ventilation flux due to the pad and fan system is described by:

$$f_{Pad} = U_{Pad} \phi_{Pad} / A_{Flr} \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.59)$$

where U_{Pad} (-) is the control valve of the pad and fan system and ϕ_{Pad} ($\text{m}^3 \text{s}^{-1}$) is the capacity of the air flux through the pad.

The latent energy added to the inlet air equals the sensible heat loss of the outdoor air. Consequently, the sensible heat flux from the pad to the greenhouse air is described by:

$$H_{PadAir} = f_{Pad} (\rho_{Air} c_{p,Air} T_{Out} - \Delta H \rho_{Air} (\eta_{Pad} (x_{Pad} - x_{Out}))) \quad [\text{W m}^{-2}] \quad (8.60)$$

The sensible heat flux from the greenhouse air to the outside air H_{AirOut_Pad} , when using the pad and fan system is described by:

$$H_{AirOut_Pad} = f_{Pad} (\rho_{Air} c_{p,Air} T_{Air}) \quad [\text{W m}^{-2}] \quad (8.61)$$

The vapour flux from the greenhouse air to the outside air MV_{AirOut_Pad} , when using the pad and fan system is described by:

$$MV_{AirOut_Pad} = f_{Pad} \frac{M_{Water}}{R} \left(\frac{VP_{Air}}{T_{Air} + 273.15} \right) \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.62)$$

The net CO₂ flux from the outside air to the greenhouse air MC_{PadAir} , when using the pad and fan system is described analogously to the general form of the CO₂ flux caused by an air flux (Eq. (8.46)).

8.10.5 Mechanical cooling

A mechanical cooling system can be used to decrease both the sensible and latent heat in the greenhouse. It was assumed that the temperature of the surface of the mechanical cooling unit is an input of the system and that the total cooling capacity of the mechanical cooling installation (used for heat and vapour removal) depends on the coefficient of performance (COP) and the installed electrical capacity. Therefore, to determine the heat and vapour flux between the mechanical cooling unit and the greenhouse air, the heat exchange coefficient between the surface of the mechanical cooling unit and the greenhouse air is determined by:

$$HEC_{MechAir} = \frac{(U_{MechCool} COP_{MechCool} P_{MechCool} / A_{Flr})}{T_{Air} - T_{MechCool} + 6.4 \cdot 10^{-9} \Delta H (VP_{Air} - VP_{MechCool})} \quad [\text{W m}^{-2} \text{K}^{-1}] \quad (8.63)$$

where $U_{MechCool}(-)$ is the control valve of the mechanical cooling mechanism, $COP_{MechCool}(-)$ is the coefficient of performance of the mechanical cooling system and $P_{MechCool}$ (W) is the electrical capacity of the mechanical cooling system, $T_{MechCool}$ (°C) is the temperature of the cooling surface which is an input of the model, and $VP_{MechCool}$ (Pa) is the saturated vapour pressure of the mechanical cooling mechanism.

The heat flux from the mechanical cooling to the greenhouse air, $H_{MechAir}$, is described analogously to the general form of convective heat flux (Eq. (8.40)). The vapour flux from the greenhouse air to the surface of mechanical cooling system, $MV_{AirMech}$, is described analogously to the general form of the vapour flux (Eq. (8.43)).

8.10.6 Fogging

The latent heat flux from the greenhouse air depends on the vapour flux from the fogging system to the greenhouse air which is described by:

$$MV_{FogAir} = U_{Fog} \phi_{Fog} / A_{Flr} \quad [\text{kg m}^{-2} \text{s}^{-1}] \quad (8.64)$$

where U_{Fog} (-) is the control valve of the fogging system and ϕ_{Fog} (kg water s^{-1}) is the capacity of the fogging system. The heat flux of the air needed to evaporate the fog L_{AirFog} , is described in a similar way as Eq. (8.42).

8.10.7 Natural ventilation

Three natural ventilation mechanisms are implemented in this model: ventilation through roof openings, ventilation through openings in the side walls and ventilation through both openings in the side walls and the roof. The natural ventilation rate due to roof ventilation is described by Boulard and Baille (1995):

$$f_{VentRoof}'' = \frac{U_{Roof} A_{Roof} C_d}{2 A_{Flr}} \sqrt{\frac{g h_{Vent}}{2} \frac{T_{Air} - T_{Out}}{\bar{T} + 273.15} + C_w v_{Wind}^2} \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.65)$$

where U_{Roof} (-) is the control of the aperture of the roof vents A_{Roof} (m^2) is the maximum roof ventilation area, A_{Flr} (m^2) is the greenhouse floor area, C_d (-) is the discharge coefficient which depends on the greenhouse shape and on the use of an outdoor thermal screen, g (m s^{-2}), is the acceleration of gravity, h_{Vent} (m) is the vertical dimension of a single ventilation opening, \bar{T} ($^{\circ}\text{C}$) is the mean temperature of the greenhouse air and the outside air, C_w (-) is the global wind pressure coefficient which depends on the greenhouse shape and on the use of an outdoor thermal screen and v_{Wind} (m s^{-1}) is the wind speed.

The ventilation rate through both the roof and side vents is described by Kittas *et al.* (1997):

$$f_{VentRoofSide}'' = \frac{C_d}{A_{Flr}} \sqrt{\left(\frac{A_{Roof}^U A_{Side}^U}{\sqrt{A_{Roof}^U{}^2 + A_{Side}^U{}^2}} \right)^2 \left(2g h_{SideRoof} \frac{T_{Air} - T_{Out}}{\bar{T} + 273.15} \right) + \left(\frac{A_{Roof}^U + A_{Side}^U}{2} \right)^2 C_w v_{Wind}^2} \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.66)$$

where A_{Roof}^U (m^2) is the aperture of roof vents, A_{Side}^U (m^2) is the aperture of the side vents and $h_{SideRoof}$ (m) is the vertical distance between mid-points of side wall and roof ventilation openings.

The ventilation rate function for sidewall ventilation only, was determined using

Eq. (8.66), because then the aperture of roof vents becomes zero which results in:

$$f_{VentSide}'' = \frac{C_d A_{Side}^U v_{Wind}}{2 A_{Flr}} \sqrt{C_w} \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.67)$$

The apertures of the roof and sidewall vents depend on the control of the aperture of both vents:

$$A_{Roof}^U = U_{Roof} A_{Roof} \quad [\text{m}^2] \quad (8.68)$$

$$A_{Side}^U = U_{Side} A_{Side} \quad [\text{m}^2] \quad (8.69)$$

where U_{Roof} (-) is the control of the aperture of the roof vents and A_{Roof} (m^2) is the maximum roof ventilation area, U_{Side} (-) is the control of the sidewall vents and A_{Roof} (m^2) is the maximum sidewall ventilation area.

According to Perez Parra *et al.* (2004) insect screens reduce the potential ventilation rate by a factor:

$$\eta_{InsScr} = \zeta_{InsScr} (2 - \zeta_{InsScr}) \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.70)$$

where ζ_{InsScr} (-) the screen porosity which is the area of holes per unit area of screen.

Furthermore the ventilation rate of the greenhouse is influenced by the greenhouse leakage rate which depends on wind speed and is described by:

$$f_{leakage} = \begin{cases} 0.25 c_{leakage}, & v_{wind} < 0.25 \\ c_{leakage} \cdot v_{Wind}, & v_{wind} \geq 0.25 \end{cases} \quad [\text{m}^3 \text{m}^{-2} \text{s}^{-1}] \quad (8.71)$$

where $c_{leakage}$ (-) is the leakage coefficient which depends on the greenhouse type.

To calculate the ventilation rate though both the roof and side vents, the roof ventilation rates and side ventilations rates of Eqs. (8.65) and (8.67) respectively may not be added because then the chimney effect as described by Eq. (8.66) is neglected. Additionally, this chimney effect is also influenced by using a thermal screen. A thermal screen will decrease the ventilation rate when roof and side vents are used because then the chimney effect disappears and then the total ventilation equals the sum of Eqs. (8.65) and (8.67).

The total ventilation rate of the top compartment and greenhouse air compartment depends thus on: the net roof and side ventilation rates, the chimney effect, the thermal screen, the insect screens and the leakage rate of the greenhouse. Taking into account these processes and assuming that above a certain ratio between roof vent area and total vent

area, the chimney effect becomes negligible, the total ventilation rates for roof and side vents are calculated by:

$$f_{VentRoof} = \begin{cases} \eta_{InsScr} f_{VentRoof}'' + 0.5 f_{leakage} & \text{if } \eta_{Roof} \geq \eta_{Roof_Thr} \\ \eta_{InsScr} (U_{ThScr} f_{VentRoof}'' + (1 - U_{ThScr}) f_{VentRoofSide}'' \eta_{Roof}) + 0.5 f_{leakage} & \text{if } \eta_{Roof} < \eta_{Roof_Thr} \end{cases} \quad [\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}] \quad (8.72)$$

$$f_{VentSide} = \begin{cases} \eta_{InsScr} f_{VentSide}'' + 0.5 f_{leakage} & \text{if } \eta_{Roof} \geq \eta_{Roof_Thr} \\ \eta_{InsScr} (U_{ThScr} f_{VentSide}'' + (1 - U_{ThScr}) f_{VentRoofSide}'' \eta_{Side}) + 0.5 f_{leakage} & \text{if } \eta_{Roof} < \eta_{Roof_Thr} \end{cases} \quad [\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}] \quad (8.73)$$

where η_{Roof} is the ratio between the roof vent area and total ventilation area, η_{Side} is the ratio between the side vents area and total ventilation area and η_{Roof_Thr} is the threshold value above which no chimney effect is assumed to occur. Implicitly, it was assumed that the leak ventilation is equally distributed over the top compartment and greenhouse air compartment.

The discharge coefficients, C_d and C_w depend on the use of an external shading screen. A linear relationship between the use of an external shading screen and the ventilation discharge coefficients was assumed for a greenhouse without an external shading screen:

$$C_d = C_d^{Gh} (1 - \eta_{ShScrC_d} U_{ShSc}) \quad [-] \quad (8.74)$$

$$C_w = C_w^{Gh} (1 - \eta_{ShScrC_w} U_{ShSc}) \quad [-] \quad (8.75)$$

where C_d^{Gh} is the discharge coefficient determined for a greenhouse without an external shading screen, η_{ShScrC_d} is a parameter that determines the effect of the shading screen on the discharge coefficient, C_w^{Gh} is the global wind pressure coefficient for a greenhouse without an external shading screen and η_{ShScrC_w} is a parameter that determines the effect of the shading screen on the global wind pressure coefficient.

8.10.8 Forced ventilation

The forced ventilation is described by:

$$f_{VentForced}'' = U_{VentForced} \phi_{VentForced} / A_{Flr} \quad [\text{m}^3 \text{ m}^{-2} \text{ s}^{-1}] \quad (8.76)$$

where $U_{VentForced}$ (-) is the control of the forced ventilation and $\phi_{VentForced}$ ($\text{m}^3 \text{ s}^{-1}$) is the air

flow capacity of the forced ventilation system. The effect of the insect screens on the forced ventilation flow is determined using Eq. (8.70).

8.10.9 External CO₂ source

The CO₂ added to the green greenhouse by an external CO₂-source is described by:

$$MC_{ExtAir} = U_{ExtCO_2} \phi_{ExtCO_2} / A_{Flr} \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (8.77)$$

where U_{ExtCO_2} (-) is the control valve of the external CO₂ source, ϕ_{ExtCO_2} (mg s⁻¹) is the capacity of the external CO₂ source.

8.11 Calculated climate inputs

Usually, measurements of the following outdoor climate conditions are not available: the sky temperature T_{sky} , the soil temperature at a certain depth T_{SoOut} , and the CO₂-concentration of the outside air CO_{2Out} . An approach to calculate these climate inputs based on the available outside climate data is presented here.

The soil temperature at a certain depth is calculated using the yearly soil temperature variation determined by Van Wijk (1963):

$$T_{So(d,t)} = \bar{T}_{So} + a_0 e^{-d_{Soil}/D} \sin(\omega t - d_{Soil}/D + \beta) \quad [^{\circ}\text{C}] \quad (8.78)$$

where \bar{T}_{So} (°C) is the mean soil temperature, a_0 (°C) is the amplitude of the temperature at surface level, d_{Soil} (m) is the soil depth, D (m) is the damping depth, t is the time (s), ω is the yearly frequency (s⁻¹) and β (-) is the time shift of the sine function. The mean soil temperature equals the yearly mean outdoor temperature; the amplitude of the temperature at surface level equals the yearly outdoor temperature amplitude. The parameters \bar{T}_{So} , a_0 and β are location dependent and determined using a sinus fitting function. The damping depth is described by:

$$D = \sqrt{\frac{2\lambda_{Soil}}{\rho_{Soil} c_{pSoil}}} \quad [\text{m}] \quad (8.79)$$

where λ_{Soil} (W m⁻¹ K⁻¹) is the thermal heat conductivity of the soil, ρ_{Soil} (kg m⁻³) is the density of the soil and c_{pSoil} (J kg⁻¹ K⁻¹) is the specific heat capacity of the soil.

The sky temperature is calculated according Monteith (1973):

$$T_{Sky} = \left((1 - fr_{cloud}) \varepsilon_{Sky,Clear} (T_{Out} + 273.15)^4 + fr_{cloud} \left((T_{Out} + 273.15)^4 - 9 / \sigma \right) \right)^{0.25} - 273.15 \quad [^{\circ}\text{C}] \quad (8.80)$$

where fr_{cloud} is the fraction of clouds, $\varepsilon_{Sky,Clear}$ is the FIR emission coefficient of a clear sky, T_{Out} is the outdoor temperature and σ is the Stefan Boltzmann constant. The fraction clouds during day time is averaged for the day period and calculated by:

$$fr_{Cloud_Day(DOY)} = \frac{\sum I_{Glob}}{\sum I_{Sol}} \quad [-] \quad (8.81)$$

where I_{Sol} (W m^{-2}) is the calculated solar radiation under clear sky conditions. During the night there is no solar radiation and therefore the fraction of clouds during the night is calculated by interpolating the fraction of clouds of the preceding day with the fraction of clouds of the next day.

The FIR emission coefficient of a clear sky is calculated by:

$$\varepsilon_{sky,clear} = 0.53 + 6 \cdot 10^{-3} VP_{Out}^{0.5} \quad [-] \quad (8.82)$$

When not measured, the outdoor CO_2 concentration was assumed to have a constant value of 370 ppm throughout the day.

8.12 Nomenclature

States	Name	Unit	
CO_2	Carbon dioxide concentration	mg m^{-3}	
T	Temperature	$^{\circ}\text{C}$	
VP	Vapour pressure	Pa	
Flux densities			
H	Sensible heat flux density	W m^{-2}	
L	latent heat flux density	W m^{-2}	
MC	mass CO_2 -flux density	$\text{mg m}^{-2} \text{s}^{-1}$	
MV	mass vapour flux density	$\text{kg m}^{-2} \text{s}^{-1}$	
R	FIR flux density	W m^{-2}	
R_{NIR}	NIR flux density	W m^{-2}	
R_{PAR}	PAR flux density	W m^{-2}	
R_{Glob}	Global radiation flux density	W m^{-2}	
Superscripts	Name	Subscripts	Name
Day	Day period	$Leakage$	Leak ventilation through cracks
$Night$	Night period	$Mech$	Mechanical cooling
$Mean$	Mean value	NIR	Near infrared radiation
		Obj	Different greenhouse objects
Subscripts		Out	Outside air
Air	Greenhouse air compartment below thermal screen	PAR	Photosynthetically active radiation
b	Boundary	Pad	Pad and fan system
$Blow$	Direct air heater.	Pas	Passive heat storage facility
$Boil$	Boiler	$Pipe$	Pipe heating system
Can	Canopy	Rf	Roof of the greenhouse
$Clear$	Clear sky conditions	$Roof$	Roof ventilation
$Cloud$	Cloudy sky conditions	s	Stomata
Cov	Cover	$Side$	Side ventilation
e	External side	Sky	Sky
Ext	External CO_2 source	$So(j)$	The ‘j’ th the soil layer
FIR	Far infrared radiation	$Soil$	The soil
Flr	Floor	Sun	The sun

Chapter 8

<i>Fog</i>	Fogging system	<i>ShScr</i>	Shading screen
<i>Geo</i>	Geothermal heat	<i>ShScrPer</i>	Semi permanent screen
<i>Gh</i>	Greenhouse	<i>Top</i>	Compartment above the thermal screen
<i>Glob</i>	Global radiation	<i>ThScr</i>	Thermal screen
<i>in</i>	Internal side	<i>Vent</i>	Natural ventilation
<i>Ind</i>	Industrial source	<i>Ventforced</i>	Forced ventilation
<i>Leaf</i>	Canopy leaf	<i>Wind</i>	Wind

External climate inputs

CO_{2Out}	Outdoor CO ₂ concentration	mg m ⁻³
I_{Glob}	The outside global radiation	W m ⁻²
T_{Out}	Outdoor temperature	°C
T_{Sky}	Sky temperature	°C
T_{SoOut}	Soil temperature of outer soil layer	°C
VP_{Out}	Outdoor vapour pressure	Pa
v_{Wind}	Outdoor wind speed	m s ⁻¹

Remaining inputs

LAI	The leaf area index	m ² m ⁻²
MC_{AirCan}	The net CO ₂ flux from the air to the canopy	mg m ⁻³ s ⁻¹
$T_{MechCool}$	The temperature of the cool surface of the mechanical cooling system	°C

Climate control variables

U_{Blow}	Heat blower control
U_{Boil}	Boiler control
$U_{HeatInd}$	Control of the heat input from industry
$U_{HeatGeo}$	Control of the heat input from geothermal source
U_{Pad}	Pad and fan control
$U_{MechCool}$	Control of the mechanical cooling
U_{Fog}	Control of fogging system
U_{Roof}	Control of the roof ventilators
U_{Side}	Control of the side ventilators
$U_{VentForced}$	Control of the forced ventilation
U_{ExtCO2}	Control of the CO ₂ -input from an external source
U_{ShScr}	Control of the external shading screen
$U_{ShScrPer}$	Control of the semi-permanent shading screen
U_{ThScr}	Control of the thermal screen

Remaining symbols

β	Time shift of sine function	-
ϕ	Diameter	m
ε	FIR emission coefficient	-
η	Conversion coefficient	-
ρ	Density or reflection coefficient	kg m ⁻³ , -
λ	Thermal heat conductivity	W m ⁻¹ K ⁻¹
τ	Transmission coefficient	-
a	Amplitude or absorption coefficient	-
A	Area	m ²
c_p	Specific heat capacity	J kg ⁻¹ K ⁻¹
cap	Capacity of the associated state	
d	Depth	m
D	Damping depth	-
fr	Fraction	-
f	Flux	m ³ m ⁻² s ⁻¹
F	View factor	-
h	Thickness	m
HEC	Heat exchange coefficient	W m ⁻² K ⁻¹
l	Length	m m ⁻²
r	Resistance	s m ⁻¹
rf	Resistance factor for transpiration	-
S	Value of the differentiable switch	
t	Time	s
v	Speed	m s ⁻¹
VEC	Vapour exchange coefficient	kg m ⁻² Pa ⁻¹ s ⁻¹
x	Water vapour content	kg water kg ⁻¹ air

8.13 Tables

Table 8.1 List of model parameters and symbols

Fixed model parameters	Symbol and value	Unit	Reference
Convective heat exchange coefficient from the canopy leaf to the greenhouse air	$\alpha_{LeafAir} = 5$	$\text{W m}^{-2} \text{K}^{-1}$	De Zwart (1996)
Latent heat of evaporation	$\Delta H = 2.45 \cdot 10^6$	$\text{J kg}^{-1} \text{water}$	
Stefan Boltzmann constant	$\sigma = 5.670 \cdot 10^{-8}$	$\text{W m}^{-2} \text{K}^{-4}$	
FIR emission coefficient of the canopy	$\mathcal{E}_{Can} = 1$	-	Stanghellini (1987): leaves are considered as black bodies
FIR emission coefficient of the sky	$\mathcal{E}_{Sky} = 1$	-	By definition
Ratio between NIR and the outside global radiation	$\eta_{Glob_NIR} = 0.5$	-	Monteith (1973): UV is attributed to NIR.
Ratio between PAR and the outside global radiation	$\eta_{Glob_PAR} = 0.5$	-	Monteith (1973)
Amount of CO_2 which is released when 1 Joule of sensible energy is produced by the heat blower	$\eta_{HeatCO_2} = 0.057$	$\text{mg CO}_2 \text{J}^{-1}$	
Amount of vapour which is released when 1 Joule of sensible energy is produced by the heat blower	$\eta_{HeatVap} = 4.43 \cdot 10^{-8}$	kg vapour J^{-1}	
CO_2 conversion factor from mg m^{-3} to ppm.	$\eta_{mg_ppm} = 0.554$	$\text{ppm mg}^{-1} \text{m}^3$	
The ratio between the roof vent area and total ventilation area above no chimney effect was assumed	$\eta_{Roof_Thr} = 0.9$		Assumed
Density of the air at sea level	$\rho_{Air0} = 1.20$	kg m^{-3}	

Fixed model parameters	Symbol and value	Unit	Reference
The PAR reflection coefficient	$\rho_{CanPAR} = 0.07$	-	Marcelis <i>et al.</i> (1998).
The NIR reflection coefficient of the top of the canopy	$\rho_{CanNIR} = 0.35$	-	De Zwart (1996): based on absorption of diffuse NIR of
Density of steel	$\rho_{Steel} = 7850$	kg m ⁻³	
Density of water	$\rho_{Water} = 1 \cdot 10^3$	kg m ⁻³	
Psychrometric constant	$\gamma = 65.8$	Pa K ⁻¹	
The yearly frequency to calculate the soil temperature	$\omega = 1.99 \cdot 10^{-7}$	s ⁻¹	
Heat capacity of a square meter canopy leaves	$cap_{Leaf} = 1.2 \cdot 10^3$	J K ⁻¹ m ⁻² leaf	Stanghellini (1987):
Coefficient of the stomatal resistance model to account for radiation effect	$c_{evap1} = 4.30$	W m ⁻²	Stanghellini (1987):
Coefficient of the stomatal resistance model to account for radiation effect	$c_{evap2} = 0.54$	W m ⁻²	Stanghellini (1987):
Coefficient of the stomatal resistance model to account CO ₂ effect	$c_{evap3}^{day} = 6.1 \cdot 10^{-7}$ (day) $c_{evap3}^{night} = 1.1 \cdot 10^{-11}$ (night)	ppm ⁻²	Stanghellini (1987):
Coefficient of the stomatal resistance model to account for vapor pressure difference	$c_{evap4}^{day} = 4.3 \cdot 10^{-6}$ (day) $c_{evap4}^{night} = 5.2 \cdot 10^{-6}$ (night)	Pa ⁻²	Stanghellini (1987):
Specific heat capacity of the air	$c_{p,Air} = 1 \cdot 10^3$	J K ⁻¹ kg ⁻¹	
Specific heat capacity of steel	$c_{p,Steel} = 0.64 \cdot 10^3$	J K ⁻¹ kg ⁻¹	
Specific heat capacity of water	$c_{p,Water} = 4.18 \cdot 10^3$	J K ⁻¹ kg ⁻¹	

Fixed model parameters	Symbol and value	Unit	Reference
The acceleration of gravity	$g = 9.81$	m s^{-2}	
The thickness of the soil layers	$h_{So,j} = [0.04 \ 0.08 \ 0.16 \ 0.32 \ 0.64]$ $j = 1, 2, \dots, 5$	m	Based on De Zwart (1996)
PAR extinction coefficient of the canopy	$K_{I_PAR} = 0.7$	-	Marcelis <i>et al.</i> (1998)
PAR extinction coefficient of the canopy when PAR is reflected from the floor	$K_{2_PAR} = 0.7$	-	Assumed, similar to K_I
Extinction coefficient of the canopy for NIR	$K_{NIR} = 0.27$	-	Based on absorption of diffuse NIR of De Zwart (1996)
Extinction coefficient of the canopy for FIR	$K_{FIR} = 0.94$		Based on De Zwart (1996)
Molar mass of air	$M_{Air} = 28.96$	kg kmol^{-1}	
Molar mass of water	$M_{Water} = 18$	kg kmol^{-1}	
Molar gas constant	$R = 8.314 \cdot 10^3$	$\text{J kmol}^{-1} \text{K}^{-1}$	
The radiation value above the canopy when the night becomes day and vice versa.	$R_{Can_SP} = 5$	W m^{-2}	
Boundary layer resistance of the canopy for vapour transport	$r_b = 275$	s m^{-1}	Mean value based on Stanghellini (Stanghellini, 1987)
The minimum canopy resistance for transpiration	$r_{s,min} = 82.0$	s m^{-1}	Stanghellini (Stanghellini, 1987)
The slope of the differentiable switch for the stomatal resistance model	$s_{r_s} = -1$	m W^{-2}	
The slope of the differentiable switch function for vapour pressure differences	$s_{MV12} = -0.1$	Pa^{-1}	

Table 8.2 The greenhouse design parameters for the four different greenhouse designs in Sicily, The Netherlands, Texas and Arizona. The greenhouse design elements which were not used during the validation experiments are denoted with a cross.

Greenhouse design parameters	Parameter	Unit	Sicily	Netherland	Texas	Arizona
<i>Construction</i>						
The ratio of the global radiation which is absorbed by the greenhouse construction elements	η_{Glob_Air}	-	0.1	0.1	0.1	0.1
Mean greenhouse cover slope	ψ	°	Arch shaped	25	22	Arch shaped
Surface of the cover including side-walls	A_{Cov}	m ²	$1.7 \cdot 10^4$	$1.8 \cdot 10^4$	$9.0 \cdot 10^4$	730
Surface of the greenhouse floor	A_{Flr}	m ²	$1.3 \cdot 10^4$	$1.4 \cdot 10^4$	$7.8 \cdot 10^4$	278
Convective heat exchange parameter between cover and outdoor air that depends on the greenhouse shape	c_{HECin}	W m ⁻² K ⁻¹	2.21	1.86	1.86	2.21
Convective heat exchange variables between cover and outdoor air which depend on the greenhouse shape	c_{HECout_1}	W m ⁻² cover K ⁻¹	0.95	2.8	2.8	0.95
	c_{HECout_2}	J m ⁻³ K ⁻¹	6.76	1.2	1.2	6.76
	c_{HECout_3}	-	0.49	1	1	0.49
Height of the greenhouse compartment below the thermal screen	h_{Air}	m	4.0	3.8	4.7	5.9
The altitude of the greenhouse	$h_{Elevation}$	m (a.s.l)	104	0	1470	715
Mean height of the greenhouse	h_{Gh}	m	4.8	4.2	5.1	6.1
<i>Ventilation properties</i>						
Parameter that determines the effect of the movable shading screen on the discharge coefficient	η_{ShScrC_d}	-	x	x	x	x

Greenhouse design parameters	Parameter	Unit	Sicily	Netherland	Texas	Arizona
Parameter that determines the effect of the movable shading screen on the global wind pressure coefficient	η_{ShScrC_w}	-	x	x	x	x
The porosity of the insect screens	ζ_{InsScr}	-	0.33	1	1	x
The specific roof ventilation area	A_{Roof}/A_{Flr}	m ²	0.20	0.10	0.18	x
The side ventilation area	A_{Side}/A_{Flr}	m ²	0	0	0	x
Ventilation discharge coefficient depends on greenhouse shape	C_d^{Gh}	-	0.75	0.75	0.65	x
Greenhouse leakage coefficient	$c_{leakage}$	-	$1 \cdot 10^{-4}$	$1 \cdot 10^{-4}$	$1 \cdot 10^{-4}$	$1 \cdot 10^{-4}$
Ventilation global wind pressure coefficient depends on greenhouse shape	C_w^{Gh}	-	0.12	0.09	0.09	x
The vertical distance between mid-points of side wall and roof ventilation openings	$h_{SideRoof}$	m	x	x	x	x
The vertical dimension of a single ventilation opening	h_{Vent}	m	1.6	0.68	0.97	x
<i>Roof</i>						
The FIR emission coefficient of the roof	ϵ_{RfFIR}	-	0.9	0.85	0.85	0.9
Density of the roof layer	ρ_{Rf}	kg m ⁻³	35	$2.6 \cdot 10^3$	$2.6 \cdot 10^3$	35
The NIR reflection coefficient of the roof	ρ_{RfNIR}	-	0.21	0.13	0.13	0.20
The PAR reflection coefficient of the roof	ρ_{RfPAR}	-	0.21	0.13	0.13	0.20
The FIR reflection coefficient of the roof	ρ_{RfFIR}	-	0	0.15	0.15	0
The NIR transmission coefficient of the roof	τ_{RfNIR}	-	0.77	0.85	0.85	0.78
The PAR transmission coefficient of the roof	τ_{RfPAR}	-	0.77	0.85	0.85	0.78
FIR transmission coefficient of the roof	τ_{RfFIR}	-	0.1	0	0	0.1

Greenhouse design parameters	Parameter	Unit	Sicily	Netherland	Texas	Arizona
Thermal heat conductivity of the roof	λ_{Rf}	$\text{W m}^{-1} \text{K}^{-1}$	0.018	1.05	1.05	0.018
The specific heat capacity of the roof layer	$c_{p,Rf}$	$\text{J K}^{-1} \text{kg}^{-1}$	$2.5 \cdot 10^3$	$0.84 \cdot 10^3$	$0.84 \cdot 10^3$	$2.5 \cdot 10^3$
Thickness of the roof layer	h_{Rf}	m	0.01	$4 \cdot 10^{-3}$	$4 \cdot 10^{-3}$	0.01
<i>Whitewash</i>						
FIR emission coefficient of the whitewash	$\varepsilon_{ShScrPerFIR}$	-	0.9	x	0.9	x
Density of the semi permanent shading screen	$\rho_{ShScrPer}$	kg m^{-3}	$1 \cdot 10^3$	x	$1 \cdot 10^3$	x
NIR reflection coefficient of the whitewash	$\rho_{ShScrPerNIR}$	-	0.2	x	0.3	x
PAR reflection coefficient of the whitewash	$\rho_{ShScrPerPAR}$	-	0.2	x	0.3	x
FIR reflection coefficient of the whitewash	$\rho_{ShScrPerFIR}$	-	0	x	0	x
NIR transmission coefficient of the whitewash	$\tau_{ShScrPerNIR}$	-	0.7	x	0.6	x
PAR transmission coefficient of the whitewash	$\tau_{ShScrPerPAR}$	-	0.7	x	0.6	x
FIR transmission coefficient of the whitewash	$\tau_{ShScrPerFIR}$	-	0.1	x	0.1	x
Thermal heat conductivity of the whitewash	$\lambda_{ShScrPer}$	$\text{W m}^{-1} \text{K}^{-1}$	∞	x	∞	x
Specific heat capacity of the whitewash	$c_{p,ShScrPer}$	$\text{J K}^{-1} \text{kg}^{-1}$	$4.18 \cdot 10^3$	x	$4.18 \cdot 10^3$	x
Thickness of the whitewash	$h_{ShScrPer}$	m	$0.2 \cdot 10^{-3}$	x	$0.2 \cdot 10^{-3}$	x
<i>Thermal screen</i>						
The FIR emission coefficient of the thermal screen	$\varepsilon_{ThScrFIR}$	-	x	0.67	0.44	0.8
Density of the thermal screen	ρ_{ThScr}	kg m^{-3}	x	$0.2 \cdot 10^3$	$0.2 \cdot 10^3$	$0.2 \cdot 10^3$
The NIR reflection coefficient of the thermal screen	$\rho_{ThScrNIR}$	-	x	0.35	0.7	0.5
The PAR reflection coefficient of the thermal screen	$\rho_{ThScrPAR}$	-	x	0.35	0.7	0.5
The FIR reflection coefficient of the thermal screen	$\rho_{ThScrFIR}$	-	x	0.18	0.45	0

Greenhouse design parameters	Parameter	Unit	Sicily	Netherland	Texas	Arizona
The NIR transmission coefficient of the thermal screen	$\tau_{ThScrNIR}$	-	x	0.6	0.25	0.4
The PAR transmission coefficient of the thermal screen	$\tau_{ThScrPAR}$	-	x	0.6	0.25	0.4
FIR transmission coefficient of the thermal screen	$\tau_{ThScrFIR}$	-	x	0.15	0.11	0.2
Specific heat capacity of the thermal screen	$c_{p,ThScr}$	$J\ kg^{-1}\ K^{-1}$	x	$1.8 \cdot 10^3$	$1.8 \cdot 10^3$	$1.8 \cdot 10^3$
Thickness of the thermal screen	h_{ThScr}	m	x	$0.35 \cdot 10^{-3}$	$0.35 \cdot 10^{-3}$	$0.35 \cdot 10^{-3}$
The thermal screen flux coefficient	K_{ThScr}	$m^3\ m^{-2}\ K^{-0.66}\ s^{-1}$	x	$0.05 \cdot 10^{-3}$	$0.25 \cdot 10^{-3}$	$1 \cdot 10^{-3}$
<i>Floor</i>						
FIR emission coefficient of the floor	ε_{Flr}	-	1	1	1	1
Density of the floor	ρ_{Flr}	$kg\ m^{-3}$	2300	2300	2300	2300
NIR reflection coefficient of the floor	ρ_{FlrNIR}	-	0.5	0.5	0.5	0.5
PAR reflection coefficient of the floor	ρ_{FlrPAR}	-	0.65	0.65	0.65	0.65
Thermal heat conductivity of the floor	λ_{Flr}	$W\ m^{-1}\ K^{-1}$	1.7	1.7	1.7	1.7
Specific heat capacity of the floor	$c_{p,Flr}$	$J\ K^{-1}\ kg^{-1}$	$0.88 \cdot 10^3$	$0.88 \cdot 10^3$	$0.88 \cdot 10^3$	$0.88 \cdot 10^3$
Thickness of the greenhouse floor	h_{Flr}	m	0.02	0.02	0.02	0.02
<i>Soil properties</i>						
The volumetric heat capacity of the soil	$\rho c_{p,So}$	$J\ m^{-3}\ K^{-1}$	$1.73 \cdot 10^6$	$1.73 \cdot 10^6$	$1.73 \cdot 10^6$	$1.73 \cdot 10^6$
Thermal heat conductivity of the soil layers.	λ_{So}	$W\ m^{-1}\ K^{-1}$	0.85	0.85	0.85	0.85
<i>Heating system</i>						
FIR emission coefficient of the heating pipes	ε_{Pipe}	-	0.88	0.88	0.88	x
External diameter of the heating pipe	$\phi_{Pipe,e}$	m	$51 \cdot 10^{-3}$	$51 \cdot 10^{-3}$	$51 \cdot 10^{-3}$	x
Internal diameter of the heating pipe	$\phi_{Pipe,i}$	m	$47 \cdot 10^{-3}$	$47 \cdot 10^{-3}$	$47 \cdot 10^{-3}$	x

Greenhouse design parameters	Parameter	Unit	Sicily	Netherland	Texas	Arizona
Length of the heating pipes per square meter greenhouse	l_{Pipe}	m m ⁻²	1.25	1.875	1.25	x
<i>Active climate control</i>						
Efficiency of the pad and fan system	η_{Pad}	-	x	x	x	Function of the air flux through the pad
Capacity of the fogging system	ϕ_{Fog}	kg water s ⁻¹	x	x	x	0
Capacity of the air flux through the pad and fan system	ϕ_{Pad}	m ³ s ⁻¹	x	x	x	16.7
Air flow capacity of the forced ventilation system	$\phi_{VentForced}$	m ³ s ⁻¹	x	x	x	0
Capacity of the external CO ₂ source	ϕ_{ExtCO2}	mg s ⁻¹	x	7.2·10 ⁴	4.3·10 ⁵	x
Coefficient of performance of the mechanical cooling system	$COP_{MechCool}$	-	x	x	x	x
The convective heat exchange coefficient between the passive heat storage facility and the greenhouse air temperature	HEC_{PasAir}	W m ⁻² K ⁻¹	x	x	x	x
Heat capacity of the heat blowers	P_{Blow}	W	x	x	x	x
Thermal heat capacity of the boiler	P_{Boil}	W	x	T_{Pipe} was input	T_{Pipe} was input	x
Heat capacity of the geothermal heat source	P_{Geo}	W	x	x	x	x
Heat capacity of the industrial heat source	P_{Ind}	W	x	x	x	x
Electrical capacity of the mechanical cooling system	$P_{MechCool}$	W	x	x	x	x

Table 8.3 The equations of A_i and F_{ij} used to calculate the FIR model fluxes.

FIR_{ij}	A_i	F_{ij}
$R_{CanCov,in}$	$A_{Can} = 1 - e^{-K_{FIR}LAI}$	$F_{CanCov,in} = \tau_{ThScrFIR}^U$
R_{CanSky}	$A_{Can} = 1 - e^{-K_{FIR}LAI}$	$F_{CanSky} = \tau_{CovFIR} \cdot \tau_{ThScrFIR}^U$
$R_{CanThScr}$	$A_{Can} = 1 - e^{-K_{FIR}LAI}$	$F_{CanThScr} = U_{ThScr}$
R_{CanFlr}	$A_{Can} = 1 - e^{-K_{FIR}LAI}$	$F_{CanFlr} = 1 - 0.49\pi_{Pipe}\phi_{Pipe,e}$
$R_{PipeCov,in}$	$A_{Pipe} = \pi_{Pipe}\phi_{Pipe,e}$	$F_{PipeCov,in} = \tau_{ThScrFIR}^U 0.49e^{-K_{FIR}LAI}$
$R_{PipeSky}$	$A_{Pipe} = \pi_{Pipe}\phi_{Pipe,e}$	$F_{PipeSky} = \tau_{CovFIR} \cdot \tau_{ThScrFIR}^U 0.49e^{-K_{FIR}LAI}$
$R_{PipeThScr}$	$A_{Pipe} = \pi_{Pipe}\phi_{Pipe,e}$	$F_{PipeThScr} = U_{ThScr} 0.49e^{-K_{FIR}LAI}$
$R_{PipeFlr}$	$A_{Pipe} = \pi_{Pipe}\phi_{Pipe,e}$	$F_{PipeFlr} = 0.49$
$R_{PipeCan}$	$A_{Pipe} = \pi_{Pipe}\phi_{Pipe,e}$	$F_{PipeCan} = 0.49(1 - e^{-K_{FIR}LAI})$
$R_{FlrCov,in}$	$A_{Flr} = 1$	$F_{FlrCov,in} = \tau_{ThScrFIR}^U (1 - 0.49\pi_{Pipe}\phi_{Pipe,e})e^{-K_{FIR}LAI}$
R_{FlrSky}	$A_{Flr} = 1$	$F_{FlrSky} = \tau_{CovFIR} \tau_{ThScrFIR}^U (1 - 0.49\pi_{Pipe}\phi_{Pipe,e})e^{-K_{FIR}LAI}$
$R_{FlrThScr}$	$A_{Flr} = 1$	$F_{FlrThScr} = U_{ThScr} (1 - 0.49\pi_{Pipe}\phi_{Pipe,e})e^{-K_{FIR}LAI}$
$R_{ThScrCov,in}$	$A_{ThScr} = 1$	$F_{ThScrCov,in} = U_{ThScr}$
$R_{ThScrSky}$	$A_{ThScr} = 1$	$F_{ThScrSky} = \tau_{CovFIR} U_{ThScr}$
$R_{Cov,eSky}$	$A_{Cov,e} = 1$	$F_{Cov,eSky} = 1$

Table 8.4 The convective and conductive heat fluxes and their heat exchange coefficients

H (W m^{-2})	HEC ($\text{W m}^{-2} \text{ K}^{-1}$)	Source
H_{CanAir}	$HEC_{CanAir} = 2\alpha_{LeafAir} LAI$	De Zwart (1996)
H_{AirFlr}	$HEC_{AirFlr} = \begin{cases} 1.7(T_{Flr} - T_{Air})^{0.33} & \text{if } T_{Flr} > T_{Air} \\ 1.3(T_{Air} - T_{Flr})^{0.25} & \text{if } T_{Flr} \leq T_{Air} \end{cases}$	De Zwart (1996)
$H_{AirThScr}$	$HEC_{AirThScr} = 1.7U_{ThScr} T_{Air} - T_{ThScr} ^{0.33}$	De Zwart (1996)
H_{AirOut}	$HEC_{AirOut} = \rho_{Air} c_{p,Air} (f_{VentSide} + f_{VentForced})$	
H_{AirTop}	$HEC_{AirTop} = \rho_{Air} c_{p,Air} f_{ThScr}$	De Zwart (1996)
$H_{ThScrTop}$	$HEC_{ThScrTop} = 1.7U_{ThScr} T_{ThScr} - T_{Top} ^{0.33}$	De Zwart (1996)
$H_{TopCov,in}$	$HEC_{TopCov,in} = c_{HECin} (T_{Top} - T_{Cov,in})^{0.33} \frac{A_{Cov}}{A_{Flr}}$	Roy <i>et al.</i> (2002)
H_{TopOut}	$HEC_{TopOut} = \rho_{Air} c_{p,Air} f_{VentRoof}$	
$H_{Cov,eOut}$	$HEC_{Cov,eOut} = \frac{A_{Cov}}{A_{Flr}} (c_{HECout_1} + c_{HECout_2} v_{Wind}^{c_{HECout3}})$	Roy <i>et al.</i> (2002)
$H_{PipeAir}$	$HEC_{PipeAir} = 1.99\pi \phi_{Pipe,e} l_{Pipe} T_{Pipe} - T_{Air} ^{0.32}$	De Zwart (1996)
H_{FlrSo1}	$HEC_{FlrSo1} = \frac{2}{h_{Flr} / \lambda_{Flr} + h_{So1} / \lambda_{So}}$	
$H_{So(j-1)So(j)}$	$HEC_{So(j-1)So(j)} = \frac{2\lambda_{So}}{(h_{So(j-1)} + h_{So(j)})}$	

Chapter 9

Detailed description of the tomato yield model

This model description has been submitted to Biosystems Engineering as an electronic appendix belonging to: *A methodology for model-based greenhouse design: Part 2, Description and validation of a tomato yield model*

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9.1 Introduction

In this document all the equations of the tomato yield model are presented to assure that our colleagues are able to implement and reproduce the model. Section 9.2 presents the notational conventions used in this document. Section 9.3 shows the model overview and Section 9.4 presents the state variable equations. In Section 9.5 the following model flows are presented: canopy photosynthesis, the carbohydrate flow to individual plant organs, the fruit number and carbohydrate flow to the fruit development stages, growth and maintenance respiration and leaf pruning. Section 9.6 contains the appendices.

9.2 Notational conventions

To describe the states and the flows of the tomato yield model the notational conventions of De Zwart (1996) are used. The states of the model are denoted by names with capital letters followed by one subscript (see Nomenclature in section 9.6). The flows are denoted by a capital letter followed by two subscripts. The first subscript represents the source of the flow and the second subscript represents the destination of the flow. For example, MC_{AirBuf} denotes the carbon flow from air to the carbon buffer. The surface unit is m^2 of greenhouse floor, unless otherwise specified. As presented in the Nomenclature the carbohydrates are expressed in $mg \{CH_2O\} m^{-2}$.

9.3 Model overview

The model structure, with a common carbohydrate buffer and carbohydrate distribution to plant organs as presented in Fig. 3.1, was essentially based on earlier crop yield models (Marcelis *et al.*, 1998; Heuvelink, 1996; Dayan *et al.*, 1993; Seginer *et al.*, 1994; Linker *et al.*, 2004) and extended with the two lumped temperature-dependent growth inhibition functions.

Photosynthesis MC_{AirBuf} depends mainly on the canopy temperature, the PAR absorbed by the canopy and the CO_2 -concentration in the greenhouse. Models that relate crop growth directly to photosynthesis neglect temperature effects on growth in the absence of photosynthesis during the night. However, night temperatures play an important role in crop growth and development. To model the effects of night temperature on growth and development, the produced carbohydrates are stored in a buffer, C_{Buf} , whose outflow is

affected by temperature. The buffer distributes the carbohydrates ($MC_{BufFruit}$, $MC_{BufLeaf}$, $MC_{BufStem}$) to the plant organs (C_{Fruit} , C_{Leaf} , C_{Stem}) even when no photosynthesis occurs. These carbohydrate flows are mainly influenced by the instantaneous temperature (T_{Can}), the 24 hour mean temperature (T_{Can}^{24}), the temperature sum (T_{Can}^{Sum}) and the availability of carbohydrates in the buffer. The plant organ C_{Stem} represents the carbohydrates which are stored in both stem and root. To take into account the time delay between fruit set and fruit harvest, the model simulates for each fruit development stage, j , the fruit weight $C_{Fruit\{j\}}$ and the fruit numbers $N_{Fruit\{j\}}$. A part of the carbohydrates in the organs is used for maintenance respiration ($MC_{FruitAir}$, $MC_{LeafAir}$, $MC_{StemAir}$). When the LAI exceeds a maximum value, LAI^{Max} , the leaves are pruned back to this value, resulting in the mass flow $MC_{LeafHar}$. The accumulated harvested tomato dry matter is determined by integrating the carbohydrate outflow of the last fruit development stage.

The state equations and the carbohydrate flow to the individual plant organs are presented in this section. The model parameters are listed in Table 9.1.

9.4 State variables of the model

The state variables of the model are all described by differential equations. The derivatives of the state variables to time are shown by a dot above the state symbol.

The evolution of the carbohydrates in the buffer, C_{Buf} , in time is described by:

$$\dot{C}_{Buf} = MC_{AirBuf} - MC_{BufFruit} - MC_{BufLeaf} - MC_{BufStem} - MC_{BufAir} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.1)$$

where MC_{AirBuf} is the photosynthesis rate, $MC_{BufFruit}$, $MC_{BufLeaf}$, $MC_{BufStem}$ are the carbohydrate flows to fruits, leaves and stems respectively, and MC_{BufAir} is the growth respiration of the plant. During the light period carbohydrates produced by the photosynthesis are stored in the buffer and, whenever carbohydrates are available in the buffer, carbohydrates flow to the plant organs. This carbohydrate flow stops when the buffer approaches its lower limit. When the buffer approaches its upper limit, carbohydrates can not be stored anymore in the buffer and the photosynthesis will be inhibited.

The time between fruit set and fruit harvest is the fruit growth period which is modelled using a “fixed boxcar train” method of Leffelaar and Ferrari (1989). This method implies that carbohydrates and the number of fruits flow from one fruit development stage to the next with a specific development rate (Fig. 3.2).

When the plant shifts from the vegetative stage to the generative stage, carbohydrates are stored in the fruit development stage j , $C_{Fruit[j]}$, as described by:

$$\dot{C}_{Fruit\{j\}} = MC_{BufFruit\{j\}} + MC_{Fruit\{j-1\}Fruit\{j\}} - MC_{Fruit\{j\}Fruit\{j+1\}} - MC_{FruitAir\{j\}} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.2)$$

with $j = 1, 2, \dots, n_{Dev}$

where $MC_{BufFruit\{j\}}$ is the carbohydrate flow from the buffer to fruit development stage j , $MC_{Fruit\{j-1\}Fruit\{j\}}$ and $MC_{Fruit\{j\}Fruit\{j+1\}}$ represent the carbohydrate inflow from the previous development stage and the outflow to the next stage respectively, $MC_{FruitAir\{j\}}$ is the fruit maintenance respiration of development stage j , and n_{Dev} is the total number of fruit development stages. For the first fruit development stage, the carbohydrate inflow from the previous stage is zero. For the last development stage, the carbohydrate outflow to the next stage is described by $MC_{FruitHar}$.

The number of fruits in the fruit development stage j , $N_{Fruit[j]}$, affects the carbohydrate distribution to the fruits and is therefore described by:

$$\dot{N}_{Fruit\{j\}} = MN_{Fruit\{j-1\}Fruit\{j\}} - MN_{Fruit\{j\}Fruit\{j+1\}}, \quad j = 1, 2 \dots n_{Dev} \quad [\text{fruits m}^{-2} \text{ s}^{-1}] \quad (9.3)$$

where $MN_{Fruit\{j-1\}Fruit\{j\}}$ is the fruit number flow from fruit development stage $j-1$ to stage j and $MN_{Fruit\{j\}Fruit\{j+1\}}$ is the fruit number flow from fruit development stage j to stage $j+1$. For the first fruit development stage $MN_{Fruit\{j-1\}Fruit\{j\}}$ is replaced by $MN_{BufFruit\{1\}}$. The fruit number flow to the first fruit development stage depends on carbohydrates available for fruit growth and on the truss appearance rate.

The carbohydrates stored in the leaves, C_{Leaf} , are described by:

$$\dot{C}_{Leaf} = MC_{BufLeaf} - MC_{LeafAir} - MC_{LeafHar} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.4)$$

where $MC_{BufLeaf}$ is the carbohydrate flow from the buffer to leaves, $MC_{LeafAir}$ is the maintenance respiration of the leaves and $MC_{LeafHar}$ is the leaf pruning. The LAI is a semi-state of the model and is calculated by:

$$LAI = SLA \cdot C_{Leaf} \quad [\text{m}^2 \{\text{leaf}\} \text{ m}^{-2}] \quad (9.5)$$

where SLA is the specific leaf area ($\text{m}^2 \{\text{leaf}\} \text{ mg}^{-1} \{\text{CH}_2\text{O}\}$).

The carbohydrates stored in the stem and roots, C_{Stem} , are described by:

$$\dot{C}_{Stem} = MC_{BufStem} - MC_{StemAir} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.6)$$

where $MC_{BufStem}$ is the carbohydrate flow from the buffer to stems and roots, $MC_{StemAir}$ is the maintenance respiration of the stems and roots.

For sake of simplicity a continuous harvest rate was assumed. Consequently, the accumulated harvested tomato dry matter (DM), DM_{Har} , equals the outflow of dry matter from the last fruit development stage and is described by:

$$\dot{DM}_{Har} = \eta_{C_DM} \cdot MC_{FruitHar} \quad [\text{mg}\{\text{DM}\} \text{ m}^{-2} \text{ s}^{-1}] \quad (9.7)$$

where η_{C_DM} is the conversion factor from carbohydrate to dry matter. Since growth respiration was incorporated into the model, this conversion factor was $1 \text{ mg}\{\text{DM}\} \text{ mg}^{-1} \{\text{CH}_2\text{O}\}$.

The development stage of the plant, required to describe the transition from the vegetative to the generative stage (Eqs. 9.24 and 9.27), is expressed by the temperature sum:

$$\dot{T}_{Can}^{Sum} = \frac{1}{86400} T_{Can} \quad [^{\circ}\text{C s}^{-1}] \quad (9.8)$$

where T_{Can} is the simulated canopy temperature. By definition, the start of the generative

period T_{Can}^{Sum} is zero.

The 24 hour mean canopy temperature was approached by a 1st order approach:

$$\dot{T}_{Can}^{24} = \frac{1}{\tau} (kT_{Can} - T_{Can}^{24}) \quad [^{\circ}\text{C s}^{-1}] \quad (9.9)$$

where τ , represents the time constant of the process and k is the gain of the process. When integrated in the model-based design method, the greenhouse climate model (see chapter 2) calculates the canopy temperature as a state variable. Therefore, the canopy temperature and the 24 hour mean canopy temperature could not be calculated beforehand. To approximate the 24 hour mean canopy anyway, the first order approach of Eq. (9.9) as derived in section 9.7.1 was incorporated into the model.

9.5 Model flows

9.5.1 Canopy photosynthesis

The canopy photosynthesis calculation is based on the canopy photosynthesis model of Farquhar and Von Caemmerer (1982) and by up-scaling the leaf based photosynthesis model of Farquhar (1980, 1988) to canopy level.

9.5.1.1 The net photosynthesis rate

The net photosynthesis rate equals the gross photosynthesis rate minus photorespiration (Farquhar & Von Caemmerer, 1982):

$$MC_{AirBuf} = M_{CH_2O} \cdot h_{C_{Buf}}^{MC_{AirBuf}} (P - R) \quad [\text{mg m}^{-2} \text{s}^{-1}] \quad (9.10)$$

where M_{CH_2O} ($\text{mg } \mu\text{mol}^{-1}$) is the molar mass of CH_2O , $h_{C_{Buf}}^{MC_{AirBuf}}$ (-) is the inhibition of the photosynthesis rate by saturation of the leaves with carbohydrates, P ($\mu\text{mol}^{-1} \{CO_2\} \text{m}^{-2} \text{s}^{-1}$) is the gross canopy photosynthesis rate and R ($\mu\text{mol}^{-1} \{CO_2\} \text{m}^{-2} \text{s}^{-1}$) is the photorespiration during the photosynthesis process.

When the carbohydrate amount in the buffer exceeds its maximum storage capacity, then the photosynthesis is inhibited. This inhibition is described by:

$$h_{C_{Buf}}^{MC_{AirBuf}} = \begin{cases} 0, & C_{Buf} > C_{Buf}^{Max} \\ 1, & C_{Buf} \leq C_{Buf}^{Max} \end{cases} \quad [-] \quad (9.11)$$

where C_{Buf}^{Max} ($\text{mg}\{\text{CH}_2\text{O}\}\text{m}^{-2}$) is the maximum buffer capacity which was assumed to be equal to the sum of carbohydrates produced at potential photosynthesis capacity on a daily basis. To enhance readability the conditional “if/else” statements are presented here. However, a differentiable form of these statements are modelled and given in Appendix B in section 9.7.2 (Eq. (B.1) and Table 9.2).

Photosynthesis rate at canopy level, P , is described by (Farquhar, 1988):

$$P = \frac{J \cdot (CO2_{Stom} - \Gamma)}{4 \cdot (CO2_{Stom} + 2\Gamma)} \quad [\mu\text{mol}\{\text{CO}_2\}\text{m}^{-2}\text{s}^{-1}] \quad (9.12)$$

where J ($\mu\text{mol}\text{e}^{-}\text{m}^{-2}\text{s}^{-1}$) is the electron transport rate, 4 ($\mu\text{mol}\{\text{e}^{-}\}\mu\text{mol}^{-1}\{\text{CO}_2\}$) is the number of electrons per fixed CO_2 molecule, $CO2_{Stom}$ ($\mu\text{mol}\{\text{CO}_2\}\text{mol}^{-1}\{\text{air}\}$) is the CO_2 -concentration in the stomata and Γ ($\mu\text{mol}\{\text{CO}_2\}\text{mol}^{-1}\{\text{air}\}$) is the CO_2 compensation point.

The photorespiration, R , is described by (Farquhar & Von Caemmerer, 1982):

$$R = P \cdot \frac{\Gamma}{CO2_{Stom}} \quad [\mu\text{mol}\{\text{CO}_2\}\text{m}^{-2}\text{s}^{-1}] \quad (9.13)$$

9.5.1.2 The electron transport rate

The electron transport rate, J , is a function of the potential rate of electron transport and of the absorbed PAR by the canopy (Farquhar, 1988; Evans & Farquhar, 1991):

$$J = \frac{J^{POT} + \alpha PAR_{Can} - \sqrt{(J^{POT} + \alpha PAR_{Can})^2 - 4\Theta \cdot J^{POT} \cdot \alpha PAR_{Can}}}{2\Theta} \quad [\mu\text{mol}\text{e}^{-}\text{m}^{-2}\text{s}^{-1}] \quad (9.14)$$

where J^{POT} ($\mu\text{mol}\{\text{e}^{-}\}\text{m}^{-2}\text{s}^{-1}$) is the potential rate of electron transport, PAR_{Can} ($\mu\text{mol}\{\text{photons}\}\text{m}^{-2}\text{s}^{-1}$) is the absorbed PAR, α ($\mu\text{mol}\{\text{e}^{-}\}\mu\text{mol}^{-1}\{\text{photons}\}$) is the conversion factor from photons to electrons, including an efficiency term, and Θ (-) is the degree of curvature of the electron transport rate.

The potential rate of electron transport J^{POT} , depends on temperature (Farquhar *et al.*, 1980):

$$J^{POT} = J_{25,Can}^{MAX} \cdot e^{\frac{E_j}{R \cdot T_{Can,K}} \cdot \frac{T_{Can,K} - T_{25,K}}{T_{25,K}}} \cdot \frac{1 + e^{\frac{S \cdot T_{25,K} - H}{R \cdot T_{25,K}}}}{1 + e^{\frac{S \cdot T_{Can,K} - H}{R \cdot T_{Can,K}}}} \quad [\mu\text{mol e}^- \text{ m}^{-2} \text{ s}^{-1}] \quad (9.15)$$

where $J_{25,Can}^{MAX}$ ($\mu\text{mol e}^- \text{ m}^{-2} \text{ s}^{-1}$) is the maximum rate of electron transport at 25°C for the canopy, E_j (J mol^{-1}) is the activation energy for J^{POT} , $T_{Can,K}$ (K) is the canopy temperature, $T_{25,K}$ (K) is the reference temperature at 25°C, R_g ($\text{J mol}^{-1} \text{ K}^{-1}$) is the molar gas constant, S ($\text{J mol}^{-1} \text{ K}^{-1}$) is the entropy term and H (J mol^{-1}) is the deactivation energy

The maximum rate of electron transport at 25°C for the canopy is calculated by (Evans & Farquhar, 1991):

$$J_{25,Can}^{MAX} = LAI \cdot J_{25,Leaf}^{MAX} \quad [\mu\text{mol e}^- \text{ m}^{-2} \text{ s}^{-1}] \quad (9.16)$$

where $J_{25,Leaf}^{MAX}$ ($\mu\text{mol e}^- \text{ m}^{-2} \text{ {leaf}} \text{ s}^{-1}$) is the maximum rate of electron transport for the leaf at 25°C (Farquhar *et al.*, 1980).

9.5.1.3 The absorbed PAR by the canopy

The total PAR absorbed by the canopy is the sum of the PAR transmitted by the greenhouse cover that is directly absorbed, and the PAR reflected by the greenhouse floor that is indirectly absorbed:

$$PAR_{Can} = PAR_{GhCan} + PAR_{FlrCan} \quad [\mu\text{mol {photons}} \text{ m}^{-2} \text{ s}^{-1}] \quad (9.17)$$

The PAR which is directly absorbed by the canopy is described by a negative exponential decay of light with LAI in a homogeneous crop (Ross, 1975):

$$PAR_{GhCan} = PAR_{Gh} \cdot (1 - \rho_{Can}) \cdot (1 - \exp\{-K_1 \cdot LAI\}) \quad [\mu\text{mol {photons}} \text{ m}^{-2} \text{ s}^{-1}] \quad (9.18)$$

where PAR_{Gh} ($\mu\text{mol {photons}} \text{ m}^{-2} \text{ s}^{-1}$) is the PAR above the canopy, ρ_{Can} (-) is the reflection coefficient of the canopy for PAR and K_1 is the extinction coefficient of the canopy for PAR (-).

The PAR above the canopy is described by:

$$PAR_{Gh} = \tau_{Gh} \cdot \eta_{Glob_PAR} \cdot I_{Glob} \quad [\mu\text{mol {photons}} \text{ m}^{-2} \text{ s}^{-1}] \quad (9.19)$$

where τ_{Gh} (-) is the light transmission of the greenhouse cover and η_{Glob_PAR} ($\mu\text{mol$

{photons} J⁻¹) is a conversion factor from global radiation to PAR and I_{Glob} (W m⁻²) is the outside global radiation.

Absorption of PAR reflected by the greenhouse floor is described by:

$$PAR_{FlrCan} = \rho_{Flr} PAR_{Gh} \cdot (1 - \rho_{Can}) \cdot \exp(-K_1 \cdot LAI) \cdot (1 - \exp\{-K_2 \cdot LAI\})$$

[μmol {photons} m⁻² s⁻¹] (9.20)

where ρ_{Flr} (-) is the reflection coefficient of the greenhouse floor and K_2 (-) is the extinction coefficient of the canopy when PAR is reflected from the floor to the canopy. We assumed K_2 to be equal to K_1 .

9.5.1.4 CO₂-relationships in the photosynthetic tissue

The CO₂-concentration inside the stomata, CO_{2Stom} depends on the stomatal and mesophyll conductance, boundary layer resistance, the photosynthesis rate and the difference between the CO₂-concentration in the stomata and the CO₂-concentration of the greenhouse air. However, the CO₂-concentration in the stomata is assumed to be a fixed fraction of the CO₂-concentration in the greenhouse air (Evans & Farquhar, 1991):

$$CO_{2Stom} = \eta_{CO_2Air_Stom} \cdot CO_{2Air}$$

[μmol {CO₂} mol⁻¹ {air}] (9.21)

where $\eta_{CO_2Air_Stom}$ (-) is conversion factor from the CO₂-concentration of the greenhouse air, CO_{2Air} , to the CO₂-concentration in the stomata (Evans & Farquhar, 1991).

The CO₂ compensation point (Γ) affects the leaf photosynthesis rate and depends on temperature (Farquhar, 1988):

$$\Gamma = c_{\Gamma} T_{Can}$$

[μmol {CO₂} mol⁻¹ {air}] (9.22)

where c_{Γ} (μmol {CO₂} mol⁻¹ {air} K⁻¹) determines the effect of canopy temperature on the CO₂ compensation point.

The relation between the canopy temperature and CO₂-compensation point is valid for leaf photosynthesis rate calculations. However, applying Eq. (9.22) to canopy level results in unrealistically low optimal canopy temperature for canopy photosynthesis rate at low light and CO₂-levels, because for canopy photosynthesis calculation a higher $J_{25,Can}^{MAX}$ compared to $J_{25,Leaf}^{MAX}$ was used as described by Eq. (9.16). To avoid these unrealistically low optimal canopy temperatures, the sensitivity of the compensation point to temperature was adjusted by making the slope of Eq. (9.22) dependent of the ratio of $J_{25,Leaf}^{MAX}$ and $J_{25,Can}^{MAX}$:

$$\Gamma = \frac{J_{25,Leaf}^{MAX}}{J_{25,Can}^{MAX}} c_{\Gamma} T_{Can} + 20 c_{\Gamma} \left(1 - \frac{J_{25,Leaf}^{MAX}}{J_{25,Can}^{MAX}} \right) \quad [\mu\text{mol } \{\text{CO}_2\} \text{ mol}^{-1} \{\text{air}\}] \quad (9.23)$$

The right term of Eq. (9.23) is introduced to assure that, for all values of $J_{25,Can}^{MAX}$ at a temperature of 20°C, the compensation point calculated by Eq. (9.23) equals the compensation point calculated by Eq. (9.22).

9.5.2 The carbohydrate flow to the individual plant organs

The carbohydrate flow from buffer to the fruits is determined by multiplying the potential fruit growth coefficient by the inhibition factors h

$$MC_{BufFruit} = h_{C_{Buf}}^{MC_{BufOrg}} \cdot h_{Tcan} \cdot h_{Tcan24} \cdot h_{TcanSum} \cdot g_{Tcan24} \cdot rg_{Fruit} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.24)$$

where the inhibition factors ($0 < h < 1$): are: $h_{C_{Buf}}^{MC_{BufOrg}}$ (-), insufficient carbohydrates in the buffer; h_{Tcan} (-), non-optimal instantaneous temperature; h_{Tcan24} (-), non-optimal 24 hour canopy temperatures; and $h_{TcanSum}$ (-), crop development stage. The effect of temperature on the carbohydrate flow to fruits is described by g_{Tcan24} (-) and rg_{Fruit} ($\text{mg m}^{-2} \text{ s}^{-1}$) is the potential fruit growth rate coefficient at 20°C.

The carbohydrate flow from buffer to the leaves and stem is described by:

$$MC_{BufOrg(i)} = h_{C_{Buf}}^{MC_{BufOrg}} \cdot h_{Tcan24} \cdot g_{Tcan24} \cdot rg_{Org(i)} \quad i = 2,3 \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.25)$$

where i represents the plant organ code for *Leaf* and *Stem*, $rg_{Org(i)}$ ($\text{mg } \{\text{CH}_2\text{O}\} \text{ m}^{-2} \text{ s}^{-1}$) is the organ growth rate coefficient at 20°C. As in agreement with Table 3.1 in chapter 3, these carbohydrate flows are not influenced by instantaneous temperature. The individual processes of Eqs. (9.24) and (9.25) are described in more detail in this section.

9.5.2.1 Insufficient carbohydrates in the buffer

The inhibition of the carbohydrate flow to the plant organs caused by insufficient carbohydrates in the buffer is described by:

$$h_{C_{Buf}}^{MC_{BufOrg}} = \begin{cases} 0, & C_{Buf} \leq C_{Buf}^{Min} \\ 1, & C_{Buf} > C_{Buf}^{Min} \end{cases} \quad [-] \quad (9.26)$$

where C_{Buf}^{Min} ($\text{CH}_2\text{O m}^{-2}$) is the minimum amount of carbohydrates in the buffer. It was

assumed that the buffer is never totally empty and therefore C_{Buf}^{Min} is 5 % of C_{Buf}^{Max} . A differentiable form of Eq. (9.26) is given in 9.7.2.

9.5.2.2 Non-optimal instantaneous and 24 hour mean temperature

The literature review revealed that crop growth was inhibited by non-optimal levels of the instantaneous and 24 hour mean temperature which was described by two trapezoid growth inhibition functions, h_{Tcan} and h_{Tcan24} , respectively. Each inhibition function was based on Boote and Scholberg (2006) and was described by four cardinal temperatures as shown in Fig. 3.3 in chapter 3. Below a certain base temperature T_{Base} no carbohydrate flow to organs is expected ($h=0$), between T_{Opt1} and T_{Opt2} the carbon flow is maximal ($h=1$) and above T_{Max} no carbohydrate flow is expected ($h=0$). Between T_{Base} and T_{Opt1} and between T_{Opt2} and T_{Max} a linear relationship between inhibition and temperature is assumed. The growth inhibition function of Boote and Scholberg (2006) is not differentiable and therefore not suitable for dynamic optimisation purposes. The differentiable approximation of the inhibition function is listed in section 9.7.2.

9.5.2.3 Start of the generative phase

The first development stage is vegetative and all carbohydrates are used for leaf and stem growth. When a given temperature sum is reached, the generative stage starts and the carbohydrates are divided over the fruits, leafs and stems (root is part of the stem). It was assumed that the fruit growth rate starts at zero and increases linearly to full potential with increasing temperature sum. The gradual increase in fruit growth rate, depending on tomato development stage, $h_{TcanSum}$, is described by:

$$h_{TcanSum} = \begin{cases} 0 & \text{if } T_{Can}^{Sum} \leq T_{Start}^{Sum} \\ \frac{T_{Can}^{Sum} - T_{Start}^{Sum}}{T_{End}^{Sum} - T_{Start}^{Sum}} & \text{if } T_{Start}^{Sum} < T_{Can}^{Sum} \leq T_{End}^{Sum} \\ 1 & \text{if } T_{Can}^{Sum} > T_{End}^{Sum} \end{cases} \quad [-] \quad (9.27)$$

where T_{Can}^{Sum} (°C) is the temperature sum, T_{Start}^{Sum} (°C) is the temperature sum when the generative stage starts, T_{End}^{Sum} (°C) is the temperature sum when the fruit growth rate is at full potential. By definition, T_{Start}^{Sum} is zero because at the start of the generative stage T_{Can}^{Sum}

is zero. Furthermore, it was assumed that the fruit growth rate is maximal after one fruit growth period, which result based upon Eq. (9.32) in T_{End}^{Sum} of 1035 °C. A differentiable form of Eq. (9.27) is described in section 9.7.2.

9.5.2.4 The temperature effect on structural carbon flow to organs

The growth rate coefficients (rg_{Fruit} , rg_{Leaf} and rg_{Stem}) are temperature independent. However in biology, growth rate increases with increasing temperature. Growth dependency on temperature was assumed to be related to flowering rate dependency on temperature. According to the De Koning, (1994), flowering rate per unit time of tomato was linearly related to temperature for temperatures ranging between 17°C and 23°C. Based upon this relation, the growth rate dependency to temperature, g_{Tcan24} , is described by:

$$g_{Tcan24} = 0.047 \cdot T_{Can}^{24} + 0.060 \quad [-] \quad (9.28)$$

The coefficients were determined by converting the flowering rate dependency on temperature (De Koning, 1994) to growth dependency on temperature by demanding that g_{Tcan24} is 1 at 20°C, because the growth rate coefficients (rg_{Fruit} , rg_{Leaf} and rg_{Stem}) were defined at 20°C. Although Eq. (9.28) was only validated for the temperature range 17°C-23°C, this relation was applied for temperature ranges outside this range. Outside this range, temperature effects are described by the growth inhibition functions.

9.5.3 The fruit number and carbohydrate flows to fruit development stages

Fruit development is modelled by describing the number of fruits and the amount of carbohydrates for each fruit development stage (Fig. 3.2 in chapter 3). Fruits and carbohydrates flow through different fruit development stages are represented by a series of pools. Fruit numbers are modelled to determine for each fruit development stage the carbohydrate demand. The fruit number and carbohydrate flows to different fruit development stages are described in this section.

9.5.3.1 The fruit flow to different the fruit development stages

The number of fruits in the development stages, $N_{Fruit\{j\}}$, depend on the fruit set in the first development stage, $MN_{BufFruit\{1\}}$, and on the fruit flow to the remaining development stages, $MN_{Fruit\{j\}Fruit\{j+1\}}$ based on the fixed boxcar train" method. The fruit set of the first

development stage depends on the carbohydrate flow from buffer to fruits and on the maximum fruit set. It was assumed that above a certain carbohydrate flow from buffer to the fruits, fruit set is maximal. Below this carbohydrate flow, fruit set decreases linearly with a decreasing carbohydrate flow from buffer to the fruits:

$$MN_{BufFruit\{1\}} = \begin{cases} \frac{MC_{BufFruit}}{r_{BufFruit}^{Max, FrtSet}} \cdot MN_{BufFruit\{1\}}^{Max}, & MC_{BufFruit} \leq r_{BufFruit}^{Max, FrtSet} \\ MN_{BufFruit\{1\}}^{Max}, & MC_{BufFruit} > r_{BufFruit}^{Max, FrtSet} \end{cases} \quad [\text{fruits m}^{-2} \text{ s}^{-1}] \quad (9.29)$$

where $MC_{BufFruit}$ is the total carbohydrate flow from buffer to fruits, $MN_{BufFruit\{1\}}^{Max}$ is the maximum fruit set and $r_{BufFruit}^{Max, FrtSet}$ ($\text{mg } \{\text{CH}_2\text{O}\} \text{ m}^{-2} \text{ s}^{-1}$) is the carbohydrate flow from buffer to the fruits above which fruit set is maximal. A differentiable form of Eq. (9.29) is given in section 9.7.2.

Truss appearance is linearly related to the mean canopy temperature (De Koning, 1994). The maximum fruit set dependency on temperature, $MN_{BufFruit\{1\}}^{Max}$, is obtained by up-scaling the truss appearance rate:

$$MN_{BufFruit\{1\}}^{Max} = n_{Plants} \cdot \left(c_{BufFruit_1}^{Max} + c_{BufFruit_2}^{Max} \cdot T_{Can}^{24} \right) \quad [\text{fruits m}^{-2} \text{ s}^{-1}] \quad (9.30)$$

where n_{Plants} (plant m^{-2}) is the plant density in the greenhouse and $c_{BufFruit_1}^{Max}$ ($\text{fruits plant}^{-1} \text{ s}^{-1}$) and $c_{BufFruit_2}^{Max}$ ($\text{fruits plant}^{-1} \text{ s}^{-1} \text{ } ^\circ\text{C}^{-1}$) are regression coefficients. The regression coefficients of the truss appearance according to De Koning (1994) were adjusted to maximum fruit set coefficients by assuming nine fruits per truss.

The fruit flow through the fruit development stages is based upon “the fixed boxcar train mechanism” of Leffelaar and Ferrari (1989) and depends on the fruit growth period and on the number of fruits in the development stage:

$$MN_{Fruit\{j\}Fruit\{j+1\}} = r_{Dev} \cdot n_{Dev} \cdot h_{T_{Can}^{Sum}}^{MN_{Fruit}} \cdot N_{Fruit\{j\}} \quad j = 1, 2, \dots, n_{Dev} \quad [\text{fruits m}^{-2} \text{ s}^{-1}] \quad (9.31)$$

where, r_{Dev} (s^{-1}) is the fruit development rate, n_{Dev} (-) is the number of development stages and $h_{T_{Can}^{Sum}}^{MN_{Fruit}}$ (-) assures that tomatoes flow through the fruit development stages when the plant is in the generative phase.

The fruit development rate is linearly related to temperature and is described by (De Koning, 1994):

$$r_{Dev} = c_{Dev1} + c_{Dev2} \cdot T_{Can}^{24} \quad [s^{-1}] \quad (9.32)$$

where the coefficients c_{Dev1} (s^{-1}) and c_{Dev2} ($s^{-1} \text{ } ^\circ\text{C}^{-1}$) were determined by De Koning for a temperature range between 17°C and 27°C .

To assure the onset of fruits, the fruit number allocated to the first development stage at initial simulation conditions was set larger than zero. To assure that fruits stay in this first development stage at vegetative stage, the fruit flow inhibition as a function of temperature sum is described by:

$$h_{T_{Can}^{Sum}}^{MN_{Fruit}} = \begin{cases} 0 & \text{if } T_{Can}^{Sum} \leq T_{Start}^{Sum} \\ 1 & \text{if } T_{Can}^{Sum} > T_{Start}^{Sum} \end{cases} \quad [s^{-1}] \quad (9.33)$$

A differentiable form of Eq. (9.33) is described in section 9.7.2.

9.5.3.2 The carbohydrate flow from carbohydrate buffer to different fruit development stages

The amount of fruit carbohydrates in the development stages, $C_{Fruit\{j\}}$, depends on two carbohydrate inflow processes: the carbohydrate flow through the development stages, $MC_{Fruit\{j\}Fruit\{j+1\}}$ and the carbohydrate flow from the carbohydrate buffer to a specific fruit development stage $MC_{BufFruit\{j\}}$.

The fruit carbohydrates flow from one development stage to the next development stage is described by:

$$MC_{Fruit\{j\}Fruit\{j+1\}} = r_{Dev} \cdot n_{Dev} \cdot C_{Fruit\{j\}} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.34)$$

The available carbohydrates for fruit growth $MC_{BufFruit}$, are distributed to the different fruit development stages, $C_{BufFruit\{j\}}$. The carbohydrate flow to the first fruit development stage, $MC_{BufFruit\{1\}}$, depends on the fruit set of Eq. (9.29) and is described by:

$$MC_{BufFruit\{1\}} = W_{Fruit\{1\}}^{Pot} \cdot MN_{BufFruit\{1\}} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.35)$$

where $W_{Fruit\{1\}}^{Pot}$ ($\text{mg } \{\text{CH}_2\text{O}\} \text{ fruit}^{-1}$) is the potential dry matter per fruit in fruit development stage one, which is determined by integration of the Gompertz growth rate function as described in Eq. (9.38).

The carbohydrate flow from the carbohydrate buffer into the remaining fruit development stages $MC_{BufFruit\{j\}}$ depends on: the number of fruits, the fruit growth rate, and on the carbohydrates available for fruit growth:

$$MC_{BufFruit\{j\}} = \eta_{BufFruit} \cdot N_{Fruit\{j\}} \cdot GR\{j\} \cdot (MC_{BufFruit} - MC_{BufFruit\{1\}}) \quad [mg \ m^{-2} \ s^{-1}] \quad (9.36)$$

$j = 2, 3, \dots, n_{Dev}$

where $\eta_{BufFruit}$ ($d \ m^2 \ mg^{-1} \ CH_2O$) is a conversion factor to ensure that $MC_{BufFruit}$ equals the sum of the carbohydrates that flow to the different fruit development stages, $N_{Fruit\{j\}}$ (fruit m^{-2}) is the number of fruits in a fruit development stage and $GR\{j\}$ ($mg\{CH_2O\} \ fruit^{-1} \ d^{-1}$) is the daily potential growth rate per fruit in development stage j .

The conversion factor, $\eta_{BufFruit}$, is defined by:

$$\eta_{BufFruit} = \frac{1}{\sum_{j=1}^{j=n_{Dev}} N_{Fruit\{j\}} \cdot GR\{j\}} \quad j = 2, 3, \dots, n_{Dev} \quad [d \ m^2 \ mg^{-1} \ \{CH_2O\}] \quad (9.37)$$

The fruit growth rate depends on the fruit development stage and is described by the first derivative of the Gompertz equation to time (De Koning, 1994):

$$GR\{j\} = G^{Max} \exp\left[-\exp\left[-B\left(t_j^{FGP} - M\right)\right]\right] \cdot B \exp\left[-B\left(t_j^{FGP} - M\right)\right] \quad [mg \ \{CH_2O\} \ fruit^{-1} \ d^{-1}] \quad (9.38)$$

where $GR\{j\}$ ($mg \ \{CH_2O\} \ fruit^{-1} \ d^{-1}$) is the daily potential growth rate per fruit in fruit development stage j , G^{Max} ($mg \ \{CH_2O\} \ fruit^{-1}$) is the potential fruit weight, B (d^{-1}) represents the steepness of the curve, t_j^{FGP} (d) is the number of days after fruit set for development stage j and M (d) is the fruit development time in days where GR is maximal. Parameters B and M depend on the fruit growth period, FGP , and are described by (De Koning, 1994):

$$FGP = \frac{1}{r_{Dev} \cdot 86400} \quad [d] \quad (9.39)$$

$$M = -4.93 + 0.548 \cdot FGP \quad [d] \quad (9.40)$$

$$B = 1 / (2.44 + 0.403 \cdot M) \quad [d^{-1}] \quad (9.41)$$

The number of days after fruit set for development stage j , t_j^{FGP} , depends on the total fruit growth period:

$$t_j^{FGP} = \frac{(j-1)+0.5}{n_{Dev}} FGP \quad [d] \quad (9.42)$$

9.5.4 Growth and maintenance respiration

The growth respiration of the total plant which is released by the carbon buffer (MC_{BufAir}) is determined by adding the growth respiration of the individual plant organs:

$$MC_{BufAir} = \sum_{i=1}^{i=3} MC_{Org(i)Air-g} \quad [mg \ m^{-2} \ s^{-1}] \quad (9.43)$$

where i represents the plant organ code and $MC_{Org(i)Air-g}$ is the growth respiration of the individual plant organ which is linearly related to the carbohydrate flow to the plant organ:

$$MC_{Org(i)Air-g} = c_{Org(i)-g} MC_{BufOrg(i)} \quad i = 1,2,3 \quad [mg \ m^{-2} \ s^{-1}] \quad (9.44)$$

where $c_{Org(i)-g}$ (-) is the growth respiration coefficient of plant organ i . The growth respiration coefficients were calculated based on the assimilate requirements for formation of fruits, leaves, stems and roots (Heuvelink, 1996).

The maintenance respiration of the individual plant organs, $MC_{Org(i)Air}$, is described by (Heuvelink, 1996):

$$MC_{Org(i)Air} = c_{Org(i)-m} \cdot Q_{10-m}^{0.1(T_{can24-25})} \cdot C_{Org(i)} \cdot (1 - e^{-c_{RGR} \cdot RGR}) \quad i = 1,2,3 \quad [mg \ m^{-2} \ s^{-1}] \quad (9.45)$$

where $c_{Org(i)-m}$ ($mg\{CH_2O\}mg^{-1}\{CH_2O\}s^{-1}$) is the maintenance respiration coefficient of the plant organ, Q_{10-m} (-) is the Q_{10} value for temperature effect on maintenance respiration, $C_{Org(i)}$ is the carbohydrate weight of plant organ, RGR (s^{-1}) is the net relative growth rate and c_{RGR} (s) is the regression coefficient for maintenance respiration.

9.5.5 Leaf pruning

Leaf pruning depends on the management of the grower. To deal with this uncertainty, it was assumed that leafs were pruned if the simulated LAI exceeds the maximum allowed LAI.

The maximum allowed carbohydrates stored in the leaves C_{Leaf}^{Max} , is determined by:

$$C_{Leaf}^{Max} = \frac{LAI^{Max}}{SLA} \quad [\text{mg m}^{-2}] \quad (9.46)$$

The leaf harvest rate $MC_{LeafHar}$ is determined by:

$$MC_{LeafHar} = \begin{cases} 0 & \text{if } C_{Leaf} < C_{Leaf}^{Max} \\ C_{Leaf} - C_{Leaf}^{Max} & \text{if } C_{Leaf} \geq C_{Leaf}^{Max} \end{cases} \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (9.47)$$

A differentiable form of Eq. (9.47) is given in section 9.7.2.

9.6 Nomenclature

States	Name	Unit	
<i>C</i>	Carbohydrate amount	mg {CH ₂ O} m ⁻²	
<i>DM</i>	Dry matter	mg {DM} m ⁻²	
<i>N</i>	Number	fruits m ⁻²	
<i>T</i>	Temperature	°C	
Semi-state			
<i>LAI</i>	Leaf Area Index	m ² {leaf} m ⁻²	
Flow			
<i>MC</i>	Carbohydrate mass flow	mg {CH ₂ O} m ⁻² s ⁻¹	
<i>MN</i>	Number flow	fruits m ⁻² s ⁻¹	
Subscripts	Name	Subscripts	Name
<i>_g</i>	Growth respiration	<i>K</i>	Temperature in Kelvin
<i>_m</i>	Maintenance respiration	<i>Leaf</i>	Leaves
<i>24</i>	Mean of 24 hour	<i>Org</i>	Plant organ (fruit, leaves, stem and roots)
<i>Air</i>	Air	<i>Plants</i>	Plants
<i>Buf</i>	The carbon buffer	<i>Start</i>	Start of period
<i>Can</i>	Canopy	<i>Stem</i>	Stem and roots
<i>Dev</i>	Development	<i>Stom</i>	Stomata
<i>End</i>	End of period		
<i>Flr</i>	Floor	Superscripts	Name
<i>Fruit</i>	Fruit	<i>Max</i>	Maximum
<i>Gh</i>	Greenhouse	<i>Min</i>	Minimum
<i>Har</i>	Harvest	<i>Pot</i>	Potential
<i>i</i>	Organ code: i=1, fruits; i=2, leaves; and i= 3, stem and roots	<i>Sum</i>	Summation
<i>Inst</i>	Instantaneous temperature effect	<i>FrtSet</i>	Fruit set
<i>j</i>	Fruit development stage	<i>FGP</i>	Fruit Growth Period

Remaining symbols	Symbol	Unit
CO ₂ compensation point	Γ	$\mu\text{mol } \{\text{CO}_2\} \text{ mol}^{-1} \{\text{air}\}$
Conversion factor for fruit dry matter distribution	η_{BufFruit}	$\text{d m}^2 \text{ mg}^{-1} \{\text{CH}_2\text{O}\}$
Inhibition of process 1 by process 2	h_2^1	-
Steepness of the Gompertz growth rate curve	B	d^{-1}
Carbon dioxide concentration	CO_2	$\mu\text{mol } \{\text{CO}_2\} \text{ mol}^{-1} \{\text{air}\}$
Daily potential growth rate per fruit	GR	$\text{mg } \{\text{CH}_2\text{O}\} \text{ fruit}^{-1} \text{ d}^{-1}$
Outside global radiation	I_{Glob}	W m^{-2}
The electron transport rate	J	$\mu\text{mol } \{\text{e}^-\} \text{ m}^{-2} \text{ s}^{-1}$
The state or flow that determines S	k	
The value of k where S_k^l is 0.5	k_{Switch}	
The process that is influenced by the differentiable switch	l	
Leaves are pruned back to this LAI	LAI^{Max}	$\text{m}^2 \text{ m}^{-2}$
The fruit development time where fruit growth rate is maximal	M	d
Canopy photosynthesis rate	P	$\mu\text{mol}^{-1} \{\text{CO}_2\} \text{ m}^{-2} \text{ s}^{-1}$
Photosynthetic active radiation	PAR	$\mu\text{mol } \{\text{photons}\} \text{ m}^{-2} \text{ s}^{-1}$
Fruit development rate	r_{Dev}	s^{-1}
Photorespiration during photosynthesis processes	R	$\mu\text{mol}^{-1} \{\text{CO}_2\} \text{ m}^{-2} \text{ s}^{-1}$
Relative Growth Rate	RGR	s^{-1}
The slope at k_{Switch}	s	
Value of the differentiable switch	S_k^l	
Time	t	s
Days after fruit set for development stage j	t_j^{FGP}	d
Temperature	T	$^{\circ}\text{C}$
Dry matter per unit	W	$\text{mg } \{\text{CH}_2\text{O}\} \text{ unit}^{-1}$

9.7 Appendices

9.7.1 Appendix A Calculation of the 24 hour mean temperature

Several growth processes are influenced by the 24 hour mean canopy temperature. To calculate the 24 hour mean canopy temperature in a state space format is rather complicated because the state space format assumes that the future states could be predicted by using only the values of the current states and inputs. In other words, the 24 hour mean canopy temperature should be described without information from the past. The 24 hour mean canopy temperature was approached by a 1st order approach according to Van Straten (personal communication, 2008):

$$\tau \frac{dT_{Can}^{24}}{dt} + T_{Can}^{24} = kT_{Can} \quad [^{\circ}\text{C}] \quad (\text{A.1})$$

This can be re-written and becomes a state of the model:

$$\frac{dT_{Can}^{24}}{dt} = \frac{1}{\tau} (kT_{Can} - T_{Can}^{24}) \quad [^{\circ}\text{C s}^{-1}] \quad (\text{A.2})$$

where τ , represents the time constant of the process and k is the gain of the process. This is a typical first order system (Stephanopoulos, 1984) with a time constant, τ , of 86400 s and a gain, k , of 1.

9.7.2 Appendix B Differentiable representation of conditional model statements

The conditional “if/else” statements, in which output values are zero or one depending on the process condition, are not differentiable and therefore these statements were replaced in the model by smoothed conditional “if/else” statements:

$$S_k^l = \frac{1}{1 + e^{(s_k^l (k - k_{Switch} \cdot l))}} \quad [-] \quad (B.1)$$

where S_k^l is the value of the differentiable switch, k is the state or flow that determines S , l is the process that is influenced by the differentiable switch, k_{Switch} is the value of k where S is 0.5 and s is the slope at k_{Switch} . The sign of s determines if the differentiable switch value increases ($s < 0$) or decreases ($s > 0$) with increasing state value. The following non-differential model equations were smoothed using the smoothed conditional “if/else” statement (Eq. (B.1)) and the parameters shown Table 9.2.

The photosynthesis inhibition by buffer saturation, $h_{C_{Buf}}^{MC_{AirBuf}}$, described in Eq. (9.11), the inhibition of the carbohydrate flow to plant organs by insufficient carbohydrates in the buffer, $h_{C_{Buf}}^{MC_{BufOrg}}$, described by Eq. (9.26) and the fruit flow inhibition as a function of temperature sum, $h_{T_{Sum}}^{MN_{Fruit}}$, described by described by Eq. (9.33) were smoothed using only the smoothed conditional “if/else” statement of Eq. (B.1).

The growth inhibition functions by: instantaneous temperature, (h_{Tcan}), and 24 hour mean temperature (h_{Tcan24}) described in Fig. 3.3 were each approximated by multiplying two smoothed conditional “if/else” statement:

$$h_{Tcan} = S_{Tcan}^{Min} \cdot S_{Tcan}^{Max} \quad [-] \quad (B.2)$$

$$h_{Tcan24} = S_{Tcan24}^{Min} \cdot S_{Tcan24}^{Max} \quad [-] \quad (B.3)$$

The values of s shown in Table 9.2 were determined by demanding that the deviation between the smoothed function and the trapezoid growth inhibition functions at the cardinal temperatures should be less than 3%.

The fruit set dependency on carbohydrate flow from buffer to the fruits, $MN_{BufFruit\{1\}}$, described in Eq. (9.29) was smoothed by:

$$MN_{BufFruit\{1\}} = S_{MC_{BufFruit}}^{MN_{BufFruit\{1\}}} \cdot MN_{BufFruit\{1\}}^{Max} \quad [\text{fruits m}^{-2} \text{ s}^{-1}] \quad (\text{B.4})$$

The leaf pruning, $MC_{LeafHar}$, described in Eq. (9.47) was smoothed by

$$MC_{LeafHar} = S_{C_{Leaf}}^{MC_{LeafHar}} \cdot (C_{Leaf} - C_{Leaf}^{Max}) \quad [\text{mg m}^{-2} \text{ s}^{-1}] \quad (\text{B.5})$$

The non-differential gradual increase in fruit growth rate, depending on tomato development stage, $h_{TcanSum}$, described in Eq. (9.27) could not be smoothed by Eq. (B.1) because the gradual increase in fruit growth rate was linearly related to the temperature sum. Two smoothed functions to describe a bounded linear relationship (Ooteghem, 2007) were combined to make Eq. (9.27) differentiable:

$$h_{TcanSum} = 0.5 \cdot \left(\frac{1}{T_{End}^{Sum}} T_{Can}^{Sum} + \sqrt{\left| \frac{1}{T_{End}^{Sum}} T_{Can}^{Sum} \right|^2 + 1 \cdot 10^{-4}} \right) - 0.5 \cdot \left(\frac{1}{T_{End}^{Sum}} (T_{Can}^{Sum} - T_{End}^{Sum}) + \sqrt{\left| \frac{1}{T_{End}^{Sum}} (T_{Can}^{Sum} - T_{End}^{Sum}) \right|^2 + 1 \cdot 10^{-4}} \right) \quad [-] \quad (\text{B.6})$$

9.7.3 Appendix C Determination of some model parameters

Potential growth coefficients

The potential fruit growth coefficient is the sum of the net potential fruit growth rate coefficient and the maintenance respiration coefficient. The daily potential net fruit growth rate was determined by using the Gompertz equation of Eq. (9.38) which resulted in 26 gram $\{CH_2O\} d^{-1} m^{-2}$ which equals $0.301 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$. Furthermore, the fruit maintenance respiration was calculated using Eq. (9.45). Assuming a mean dry matter weight for all fruits during the generative stage resulted in a maintenance respiration of $0.027 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$. Consequently, the potential fruit growth coefficient, rg_{Fruit} , was $0.328 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$.

The potential growth rate coefficients of the leaves and stems (roots included) were calculated as follows. According to Heuvelink (1996), when tomato plants were fully generative, 74% of the carbohydrates was distributed to the fruits and 26% to the vegetative parts at a ratio of 7:3:1.5 for leaves stems and roots respectively. Thus 15.8% of the available carbohydrates were distributed to the leaves and 10.2% to the stem and roots. By applying these values, the net leaf growth rate was $0.064 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$ and the stem growth rate was $0.042 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$. Adding these net growth rates with maintenance respiration resulted in a potential leaf growth rate coefficient rg_{Leaf} of $0.095 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$ and a potential stem growth rate coefficient rg_{Stem} of $0.074 \text{ mg } \{CH_2O\} m^{-2} s^{-1}$.

Cardinal temperatures

The cardinal temperatures of the crop growth inhibition function for the instantaneous and 24 hour mean canopy were based upon the literature review of which results were summarized in Table 3.1 in chapter 3. According to Brüggemann *et al.* (1992) the base temperature for instantaneous crop growth inhibition, T_{Base_Inst} , was 6°C. Extrapolation of the 75% production level obtained at a night temperature of 12°C (Khayat *et al.*, 1985) resulted in a T_{Opt1_Inst} of 14°C. According to Sato *et al.* (2000) at a day temperature of 28°C almost no loss in fruit set occurred and therefore no crop production loss was assumed which resulted in T_{Opt2_Inst} of 28°C. At 40°C fruit set was inhibited and therefore T_{Max_Inst} was assumed to be 40°C. With the latter two cardinal temperatures, the growth inhibition of 50% at 35°C obtained by Zhang *et al.* (2008) approached the inhibition value obtained by the inhibition filter at 35°C. According to Criddle *et al.* (1997) below a mean temperature of 12°C no crop growth was expected and therefore the base temperature for crop growth

inhibition by the 24 hour mean temperature, T_{Base_24} , was 12°C. According to Adams *et al.* (2001) plants grown at a mean temperature of 18°C and 22°C produced normal fruits and had a normal canopy structure. Therefore T_{Opt1_24} and T_{Opt2_24} were respectively 18°C and 22°C. By extrapolating the production values of Adams *et al.* (2001) at a mean temperature of 22°C and 26°C, a maximum cardinal mean temperature, T_{Max_24} , of 27°C was assumed. Smooth and non-smooth representations of the two inhibition functions are shown in Fig. 3.3.

9.8 Tables

Table 9.1 List of model parameters and symbols

Parameter	Symbol and value	Unit	Reference
The conversion factor from photons to electrons including an efficiency term	$\alpha = 0.385$	$\mu\text{mol } \{e^-\} \mu\text{mol}^{-1} \{\text{photons}\}$	Farquhar <i>et al.</i> (1980)
PAR reflection coefficient of the canopy	$\rho_{Can} = 0.07$	-	Marcelis <i>et al.</i> (1998)
PAR reflection coefficient of the floor	$\rho_{Flr} = 0.5$	-	Assumed for white mulching
Degree of curvature of the electron transport rate	$\Theta = 0.7$	-	Farquhar (1988)
Conversion factor from carbohydrate to dry matter	$\eta_{C_DM} = 1$	$\text{mg } \{\text{DM}\} \text{mg}^{-1} \{\text{CH}_2\text{O}\}$	No lignification assumed
Conversion factor from the greenhouse air CO ₂ -concentration to the CO ₂ -concentration in the stomata	$\eta_{CO2Air_Stom} = 0.67$	$\mu\text{mol } \{\text{CO}_2\} \text{mol}^{-1} \{\text{air}\}$	Evans and Farquhar (1991)
Conversion factor from global radiation to PAR	$\eta_{Glob_PAR} = 2.3$	$\mu\text{mol } \{\text{photons}\} \text{J}^{-1}$	Based upon De Zwart (1996)
The time constant to calculate the 24 hour mean temperature	$\tau = 86400$	s	See section 9.7.1
Light transmission of the greenhouse cover	$\tau_{Gh} = 0.78$	-	Measured for Dutch growers
The effect of canopy temperature on the CO ₂ compensation point.	$C_\Gamma = 1.7$	$\mu\text{mol } \{\text{CO}_2\} \text{mol}^{-1} \{\text{air}\} \text{K}^{-1}$	Farquhar (1988)
Maximum fruit set regression coefficient 1	$C_{Buffruit_1}^{Max} = -1.71 \cdot 10^{-7}$	$\text{fruits plant}^{-1} \text{s}^{-1}$	Based upon De Koning (1994).

Parameter	Symbol and value	Unit	Reference
Maximum fruit set regression coefficient 2	$C_{BufFruit_2}^{Max} = 7.31 \cdot 10^{-7}$	fruits plant ⁻¹ s ⁻¹ °C ⁻¹	Based upon De Koning (1994)
Fruit development rate coefficient 1	$c_{Dev1} = -7.64 \cdot 10^{-9}$	s ⁻¹	Based upon De Koning (1994)
Fruit development rate coefficient 2	$c_{Dev2} = 1.16 \cdot 10^{-8}$	s ⁻¹ °C ⁻¹	Based upon De Koning (1994)
Fruit maintenance respiration coefficient	$c_{Fruit_m} = 1.16 \cdot 10^{-7}$	mg {CH ₂ O} mg ⁻¹ {CH ₂ O} s ⁻¹	Heuvelink (1996)
Fruit growth respiration coefficient	$c_{Fruit_g} = 0.27$	-	Based upon Heuvelink (1996)
Leaf maintenance respiration coefficient	$c_{Leaf_m} = 3.47 \cdot 10^{-7}$	mg {CH ₂ O} mg ⁻¹ {CH ₂ O} s ⁻¹	Heuvelink (1996)
Leaf growth respiration coefficient	$c_{Leaf_g} = 0.28$	-	Based upon Heuvelink (1996)
Stem maintenance respiration coefficient	$c_{Stem_m} = 1.47 \cdot 10^{-7}$	mg {CH ₂ O} mg ⁻¹ {CH ₂ O} s ⁻¹	Heuvelink (1996)
Stem growth respiration coefficient	$c_{Stem_g} = 0.30$	-	Based upon Heuvelink (1996)
Regression coefficient in maintenance respiration function	$c_{RGR} = 2.85 \cdot 10^6$	s	Heuvelink (1996)
Maximum buffer capacity	$C_{Buf}^{Max} = 20 \cdot 10^3$	mg {CH ₂ O} m ⁻²	Assumed, see text
Minimum amount of carbohydrates in the buffer	$C_{Buf}^{Min} = 1 \cdot 10^3$	mg {CH ₂ O} m ⁻²	Assumed, see text
Activation energy for J^{POT} calculation	$E_j = 37 \cdot 10^3$	J mol ⁻¹	Farquhar <i>et al.</i> (1980)
Potential fruit dry weight at harvest	$G^{Max} = 1 \cdot 10^4$	mg {CH ₂ O} fruit ⁻¹	Based upon De Koning (1994)
Deactivation energy for J^{POT} calculation	$H = 22 \cdot 10^4$	J mol ⁻¹	Farquhar <i>et al.</i> (1980)
Maximal rate of electron transport at 25°C for the leaf	$J_{25,Leaf}^{MAX} = 210$	μmol {e ⁻ } m ⁻² {leaf} s ⁻¹	Farquhar <i>et al.</i> (1980)
The gain of the process to calculate the 24	$k = 1$	-	See section 9.7.1

Parameter	Symbol and value	Unit	Reference
hour mean temperature			
The extinction coefficient of the canopy for PAR	$K_1 = 0.7$	-	Marcelis <i>et al.</i> (1998)
The extinction coefficient of the canopy for PAR when PAR is reflected from the floor	$K_2 = 0.7$	-	Assumed, similar to K_1
Molar mass of CH ₂ O	$M_{CH_2O} = 30 \cdot 10^{-3}$	mg {CH ₂ O} μmol^{-1} {CH ₂ O}	-
Plant density in the greenhouse	$n_{Plants} = 2.5$	plants m ⁻²	Measured for Dutch growers
Number of fruit development stages	$n_{Dev} = 50$	-	Assumption
Carbohydrate flow from buffer to the fruits above which fruit set is maximal	$r_{BufFruit}^{Max, FritSet} = 0.1$	mg {CH ₂ O} m ⁻² s ⁻¹	Assumption
Potential fruit growth rate coefficient at 20°C	$rg_{Fruit} = 0.328$	mg {CH ₂ O} m ⁻² s ⁻¹	See section 9.7.3
Potential leaf growth rate coefficient at 20°C	$rg_{Leaf} = 0.095$	mg {CH ₂ O} m ⁻² s ⁻¹	See section 9.7.3
Potential stem growth rate coefficient	$rg_{Stem} = 0.074$	mg {CH ₂ O} m ⁻² s ⁻¹	See section 9.7.3
Molar gas constant	$R = 8.314$	J mol ⁻¹ K ⁻¹	-
Entropy term for J^{POT} calculation	$S = 710$	J mol ⁻¹ K ⁻¹	Farquhar <i>et al.</i> (1980)
Specific leaf area index	$SLA = 2.66 \cdot 10^{-5}$	m ² {leaf} mg ⁻¹ {CH ₂ O}	Assumed to be constant, Heuvelink (1996)
Reference temperature for J^{POT} calculation	$T_{25,K} = 298.15$	K	
Temperature sum when fruit growth rate is at full potential	$T_{End}^{Sum} = 1035$	°C	Based upon Eq. (9.32)

Parameter	Symbol and value	Unit	Reference
Base temperature for 24 hour mean crop growth inhibition	$T_{Base_24} = 12$	°C	See section 9.7.3
First optimal temperature for 24 hour mean crop growth inhibition	$T_{Opt1_24} = 18$	°C	See section 9.7.3
Second optimal temperature for 24 hour mean crop growth inhibition	$T_{Opt2_24} = 22$	°C	See section 9.7.3
Maximum temperature for 24 hour mean crop growth inhibition	$T_{Max_24} = 27$	°C	See section 9.7.3
Base temperature for instantaneous crop growth inhibition	$T_{Base_Inst} = 6$	°C	See section 9.7.3
First optimal temperature for instantaneous crop growth inhibition	$T_{Opt1_Inst} = 14$	°C	See section 9.7.3
Second optimal temperature for instantaneous crop growth inhibition	$T_{Opt2_Inst} = 28$	°C	See section 9.7.3
Maximum temperature for instantaneous crop growth inhibition	$T_{Max_Inst} = 40$	°C	See section 9.7.3
Q_{10} value of temperature effect on maintenace respiration	$Q_{10_m} = 2$	-	Heuvelink (1996)

Table 9.2 Parameter values of the differential switch functions described by Eq. (B1) in section 9.7.2 for different model equations.

S_k^l	Related to the non differentiable function	s_k^l	k	k_{Switch}
$h_{C_{Buf}}^{MC_{AirBuf}}$	Eq. (9.11)	$s_{C_{Buf}}^{MC_{AirBuf}} = 5 \cdot 10^{-4}$	C_{Buf}	$C_{Buf}^{Max} = 20 \cdot 10^3 \text{ mg m}^{-2}$
$h_{C_{Buf}}^{MC_{BufOrg}}$	Eq. (9.26)	$s_{C_{Buf}}^{MC_{BufOrg}} = -5 \cdot 10^{-3}$	C_{Buf}	$C_{Buf}^{Min} = 1 \cdot 10^3 \text{ mg m}^{-2}$
$h_{T_{Can}^{Sum}}^{MN_{Fruit}}$	Eq. (9.33)	$s_{T_{Can}^{Sum}}^{MN_{Fruit}} = -5 \cdot 10^{-2}$	T_{Can}^{Sum}	$T_{Can}^{Sum} = 0 \text{ }^\circ\text{C}$
$S_{T_{Can}}^{Min}$	Fig. 3.3	$s_{T_{Can}}^{Min} = -0.8690$	T_{Can}	$\bar{T}_{Can}^{Min} = 10 \text{ }^\circ\text{C}$
$S_{T_{Can}}^{Max}$	Fig. 3.3	$s_{T_{Can}}^{Max} = 0.5793$	T_{Can}	$\bar{T}_{Can}^{Max} = 34 \text{ }^\circ\text{C}$
$S_{T_{Can24}}^{Min}$	Fig. 3.3	$s_{T_{Can24}}^{Min} = -1.1587$	T_{Can24}	$\bar{T}_{Can24}^{Min} = 15 \text{ }^\circ\text{C}$
$S_{T_{Can24}}^{Max}$	Fig. 3.3	$s_{T_{Can24}}^{Max} = 1.3904$	T_{Can24}	$\bar{T}_{Can24}^{Max} = 24.5 \text{ }^\circ\text{C}$
$S_{MC_{BufFruit}}^{MN_{BufFruit}\{1\}}$	Eq. (9.29)	$s_{MC_{BufFruit}}^{MN_{BufFruit}\{1\}} = -58.9$	$MC_{BufFruit}$	$MC_{BufFruit}^{Switch} = 0.05 \text{ mg m}^{-2} \text{ s}^{-1}$
$S_{C_{Leaf}}^{MC_{LeafHar}}$	Eq. (9.47)	$s_{C_{Leaf}}^{MC_{LeafHar}} = -5 \cdot 10^{-5}$	C_{Leaf}	$C_{Leaf}^{Max} = \frac{LAI^{Max}}{SLA}$

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Summary

An enormous variety of protected cultivation systems can be found throughout the world. Prevailing local conditions, such as climate, economy, social aspects, availability of resources and legislation are the main causes. The diversity of local boundary conditions and greenhouse elements complicate the design process and may result in sub-optimal designs. A systematic approach that integrates physical, biological and economical models is a promising way for strategic decision making on greenhouse configurations. This approach might adapt greenhouses better to local conditions and it can suggest design improvements for existing greenhouses.

The objective of this thesis was therefore to develop a method that produces a greenhouse design suitable for the given local climatic and economic conditions, and that can cope with the diversity of conditions that can be found throughout the world. Since this is obviously a multi-factorial optimisation problem, a model-based greenhouse design method was developed that adjusts the design in such a way that the maximum net financial result (NFR) will be obtained. To focus this research, the climatic and economic conditions were regarded as boundary conditions, tomato was selected as model crop and the design problem was narrowed down to design elements that influence the aerial climate.

A greenhouse climate model was developed to determine the indoor climate (temperature, vapour pressure and CO₂ concentration of the air), as a function of outdoor climate, climate management, greenhouse design and crop condition (**Chapter 2**). The model contained design elements that are sufficiently generic for a wide range of climate conditions. Furthermore, the model consisted of a set of differential equations, so that it could easily be combined with the tomato yield model of a similar structure. The model was validated for four different greenhouse designs under three climatic conditions: a temperate marine climate, a Mediterranean climate and a semi-arid climate. In all cases, the model accurately predicted the greenhouse climate for all four designs, without modification of the pre-selected model parameters (except for one case). In particular, in more than 78% of the cases, comparison of simulations and measurements of the indoor climate yielded a relative root mean square error of less than 10%.

Chapter 3 describes the model to calculate the tomato yield as a function of the simulated canopy temperature, photosynthetically active radiation (PAR) and CO₂-concentration of the indoor air. Since the solution of a greenhouse design optimisation problem was expected to allow extremely low and high temperatures in order to save

energy and investments, temperature effects on tomato yield were integrated in the model. A review of existing knowledge on this matter indicated that both sub-and supra-optimal temperatures can affect, both instantaneously and on daily average base, several growth and development processes resulting in lower yield. Such temperature effects were captured in the model by means of two lumped temperature-dependent growth inhibition functions, describing the instantaneous and the mean temperature effects on tomato growth, respectively. Without calibration of pre-selected model parameters, the tomato yield model predicted with accuracy the crop yield levels for four temperature regimes: near-optimal temperatures in the Netherlands; non-optimal temperatures in South Spain; extremely low as well as high mean temperatures, and extreme diurnal temperature oscillations.

In **Chapter 4**, three sensitivity analysis techniques were applied to the combined greenhouse climate-tomato yield model, to identify the parameters that most strongly influence greenhouse design, and to increase our understanding of the design process. The analysis was performed for a low-tech greenhouse in Almeria, Spain and a high-tech greenhouse in Texas, USA. Simulations indicated that the model produced realistic data for both the indoor climate and crop yield. Single-variate sensitivity results showed that outdoor climate had the strongest impact on the performance of the greenhouse system, followed by the greenhouse design parameters and the greenhouse climate set-points. The selection of a proper greenhouse location is thus of utmost importance. Concerning the design parameters, PAR was the main limiting factor for greenhouse production systems. To increase crop yield, structures with a higher PAR transmission and a near infrared radiation (NIR)-selective whitewash/screens must be used. Results can also be used to determine whether sufficient climate control capacities are installed, and which greenhouse design parameters can be adjusted to save resources. In addition, obvious seasonal patterns in the model sensitivity suggested the advantage of adjustable cover parameters. The multi-variate sensitivity analysis revealed strong joint effects of the PAR transmission and ventilation set-point on crop yield. Sensitivity analysis techniques were thus able to quantify the single, combined and seasonal impact of parameters on the harvest rate, resource consumption and indoor climate. However, to increase the insight in relevant design aspects for greenhouse optimisation even further, the sensitivity of the net profit of the greenhouse grower to input parameters had to be determined next.

The economic model to evaluate the annual NFR as a function of crop yield, the resource use and the depreciation and maintenance of the construction is described in **Chapter 5**. The economic model was joined with the greenhouse climate-crop yield model to identify—among ten predefined design alternatives—the greenhouse with the highest

annual NFR for tomato production under South-Spanish conditions. The basic designs were either the parral greenhouse, or a multi-tunnel, possibly fitted with any combination of heating, fogging and CO₂ enrichment. Results demonstrated that the multi-tunnel, fitted with only a fogging system, was most profitable, followed by the multi-tunnel with heating, CO₂ enrichment and fogging. However, the difference in NFR between such a design and a simple parral was small with respect to the difference in investment. A sensitivity analysis of the NFR of the two technology extremes showed that tomato price, the fraction of marketable yield and the PAR transmission of the cover had the largest bearing on NFR. Results proved that the best greenhouse design was strongly affected by four factors: weather, price trajectories, joint impact of climate modification techniques, and greenhouse climate management. With increasing technology level, the NFR depended less on outdoor climate and more on tomato price. This indicates that a low-tech greenhouse diminishes the risk of variations among price paths in different years, whereas a high-tech greenhouse covers better the “weather risk”.

To cope with a larger numbers of design alternatives, an efficient optimisation algorithm was integrated in the design method (**Chapter 6**). The algorithm maximised the annual NFR by optimising the selection of alternatives to fulfil the following eight design elements: (i) the type of greenhouse structure, (ii) the material of the cover, (iii) the presence and type of outdoor shade screen, (iv) the whitewash properties, (v) the presence and type of thermal screen, (vi) the type of heating system and its capacity, (vii) the type of cooling system and its capacity and (viii) the type of CO₂ enrichment system and its capacity. A modified controlled random search algorithm, using parallel computing adapted the greenhouse design to local climatic and economic conditions of two locations (Almeria and The Netherlands), taken as example. A greenhouse with a relatively large specific ventilation area (20% compared to 14% for Dutch conditions), seasonal whitewash and a low-capacity direct air heater (50 W m⁻² compared to 200 W m⁻² for Dutch conditions) was selected as optimal for the warm climate with high radiation levels of Almeria. In contrast, for the relatively cold climate with low radiation levels of The Netherlands, whitewash was not selected and a 100% aluminium thermal screen was applied. The design method produced realistic greenhouses and related annual NFR, indicating that a robust and reliable design method was developed. An analysis of the close-to-best greenhouses showed that for both locations a high-light transmissivity-structure considerably enhanced the greenhouse performance whereas an outdoor shade screen, geothermal heating and mechanical cooling were not economic.

Given the results presented so far, we concluded in **Chapter 7** that the objective of this thesis was fulfilled, since the design method produced different greenhouse designs, each suitable for given climatic and economic conditions in Spain and The Netherlands. As the underlying models were validated thoroughly for a wide variety of climatic conditions, the design method might be expected to produce reliable greenhouse designs for other locations as well. Furthermore, techniques were developed to pinpoint the most relevant design parameters and design elements, which in turn increased our understanding of the design process. To the best of our knowledge, it is the first time that such a multi-factorial optimisation problem was addressed in detail and partly solved. To optimise the total design, the impact of social aspects, labour and logistics on greenhouse design should be incorporated in the design method. Other aspects that would improve the reliability and generality of the three models are discussed as well. Due to the generic nature of the design method, more aspects could easily be integrated. The impact of the uncertainty in weather and prices on greenhouse design is discussed, and measures that would reduce this impact are proposed. Last, several future perspectives of the design method are presented.

Resumen

Alrededor del mundo se encuentran diferentes tipos de invernaderos. Estas diferencias se deben a las condiciones locales como la meteorología, la economía, las condiciones sociales, la legislación y la presencia de fuentes como de agua, de energía y de CO₂. También porque existe una gran variedad de elementos de diseño, como por ejemplo cubiertas, sistemas de calefacción y de refrigeración, el diseño de invernaderos es muy complicado. Esto es la razón por la que se diseñan invernaderos que no se adaptan bien a las condiciones locales y por lo tanto no ofrecen un rendimiento óptimo. Un trabajo sistemático basado en modelos físicos, biológicos y económicos es una forma de diseñar invernaderos que ofrece grandes expectativas. Esto hará posible una mayor adaptación a las condiciones locales e indicará mejoras para invernaderos existentes.

El objetivo de esta tesis ha sido el desarrollo de un método generador de diseños de invernaderos, adaptados a las condiciones climáticas y económicas locales. Este método debe funcionar para las diferentes condiciones a nivel mundial. Ya que el diseño de invernaderos es un complicado problema de optimización que depende de diferentes factores, hemos desarrollado un método de diseño que utiliza modelos de ordenador. Este método maximiza el resultado financiero del invernadero, adaptándolo a las condiciones locales. El resultado financiero del invernadero es la diferencia entre los rendimientos económicos de por ejemplo tomates y los gastos fijos y variables del invernadero. En esta investigación nos hemos concentrado en el cultivo del tomate y el clima y las condiciones económicas se han seleccionado como condiciones previas. Además se ha reducido el problema de diseño a elementos que influyen sobre el clima del invernadero.

Se ha desarrollado un modelo de clima de invernadero para predecir el clima en el interior del invernadero (temperatura, humedad y concentración de CO₂ del aire y la temperatura del cultivo) (**Capítulo 2**). Se han incluido las siguientes variables en el modelo: el clima exterior (p.e. radiación solar, temperatura, humedad, velocidad del viento y concentración de CO₂), el control de clima, el diseño de invernadero y el cultivo. El modelo contenía elementos genéricos de diseño de invernadero para poder diseñar invernaderos para diferentes climas. La predicción del clima se ha comparado con el clima medido para cuatro invernaderos diferentes y tres climas diferentes: un clima templado marítimo, un clima mediterráneo y un clima semidesértico. El modelo predijo con precisión el clima interior del invernadero en todos estos casos. En más del 78% de los casos la diferencia entre las simulaciones y las mediciones era menos de un 10%.

En el **Capítulo 3** se describe el modelo que predice el rendimiento de tomates dependiendo de la temperatura del cultivo, la radiación fotosintéticamente activa (PAR, la parte de la luz solar que utiliza la planta para su crecimiento) y la concentración de CO₂ del aire interior (una mayor concentración de CO₂ estimula el crecimiento). La solución del diseño de invernadero tenderá a invernaderos que permiten tanto temperaturas extremadamente altas como extremadamente bajas con el fin de mantener los gastos energéticos a un mínimo. Por esta razón es muy importante que estén bien descritos estos efectos de temperaturas sobre el rendimiento de tomates. Un estudio de literatura muestra con claridad que tanto las temperaturas altas como las bajas, ejercen una influencia negativa sobre diferentes procesos de crecimiento y de desarrollo de la planta, resultando en un menor rendimiento. Tanto efectos de temperatura directos como medios, influyen sobre el crecimiento del tomate y estos efectos han sido implementado de manera sencilla en el modelo. Sin la adaptación de parámetros determinados con antelación, el modelo desarrollado fue capaz de predecir con precisión el rendimiento de tomate para cuatro trayectos de temperatura diferentes, que son: temperaturas casi óptimas para condiciones de clima de invernadero holandeses; temperaturas no óptimas para condiciones de clima de invernadero del sur de España; temperaturas medias extremadamente altas y bajas y variaciones extremas diarias de temperaturas.

Capítulo 4 describe un análisis de sensibilidad para descubrir los parámetros de mayor influencia sobre el diseño de invernadero y para aumentar nuestro entendimiento del proceso de diseño. Se han aplicado tres técnicas de análisis de sensibilidad al modelo combinado de clima de invernadero-rendimiento de tomates, con el fin de determinar las sensibilidades para un invernadero con un bajo nivel de tecnificación en Almería en el sur de España y para un invernadero con un alto nivel de tecnificación en Texas, Estados Unidos. El modelo predijo de forma realista el clima interior y el rendimiento de tomates. Los resultados del análisis de sensibilidad enfocado al efecto de uno de los parámetros, demostraban que el clima exterior ejercía la mayor influencia sobre el rendimiento del invernadero, seguido por los parámetros de diseño y los ajustes de regulación del clima interior. Por lo tanto resulta muy importante la elección correcta de la ubicación para la construcción del invernadero. Referente a los parámetros de del invernadero, la luz PAR resultaba el factor más importante para el rendimiento de los invernaderos. Para aumentar el rendimiento de tomates será necesario diseñar estructuras con mayor permeabilidad para esta luz de crecimiento y los invernaderos deberán ser equipados con pantalla o blanqueo que permitan que pase la radiación cercano-infrarrojo (NIR, la parte de la radiación solar que funciona como fuente de calor para el invernadero) de forma selectiva. Los resultados

de este análisis de sensibilidad mostraron si la capacidad del sistema de calefacción y la inyección de CO₂ era suficiente. También se revelaron parámetros de invernadero que deberían ser adaptados para el ahorro de agua, energía y CO₂. El impacto de la luz sobre el rendimiento de tomates variaba a lo largo de la temporada, lo cual sugiere que tiene preferencia una cubierta de invernadero de características variables sobre características fijas de la cubierta de invernadero. Los resultados del análisis de sensibilidad enfocado en efectos combinados de parámetros, demuestran fuertes efectos combinados de la transmisión PAR y los ajustes de ventilación sobre el rendimiento de tomates. Las técnicas utilizadas de análisis de sensibilidad, son capaces de cuantificar tanto el impacto de un solo parámetro, como de parámetros combinados y su dependencia del tiempo sobre el rendimiento de tomates, el clima interior y sobre el consumo de fuentes. Sin embargo, para mejorar el entendimiento de aspectos importantes del diseño de invernaderos, será necesario determinar el impacto sobre el resultado financiero neto del invernadero.

El modelo económico que calcula el resultado financiero neto (NFR) como función del rendimiento de tomates, el consumo de fuentes y la amortización y el mantenimiento del invernadero, se describe en el **Capítulo 5**. El modelo económico fue combinado con el modelo clima de invernadero-rendimiento de tomates para determinar, entre diez diseños diferentes de invernadero – todos con diferente nivel de tecnificación - el invernadero de tomates con el mayor resultado financiero neto para las condiciones en el sur de España. Los diseños de invernadero eran un invernadero de plástico típico de parral con una baja inclinación de techo o un invernadero de arcos equipado con diferentes combinaciones de técnicas para el control climático como sistemas de calefacción, nebulización (para la refrigeración) y dosificación de CO₂. Los resultados indicaban que un invernadero de arcos con solamente nebulización era el más rentable, seguido por un invernadero de arcos con calefacción, nebulización y dosificación de CO₂. La diferencia de resultado financiero entre un invernadero de este tipo y un invernadero relativamente barato de parral, sin embargo era pequeña en comparación con la diferencia en la inversión. Un análisis de sensibilidad del resultado financiero neto para los dos extremos de tecnología, revelaba que el precio del tomate, la parte de tomates para la venta y la permeabilidad PAR de la cubierta del invernadero, tenían el mayor impacto sobre el resultado financiero neto. Los resultados demostraron que el rendimiento financiero del invernadero se veía fuertemente influenciado por cuatro factores: la meteorología, los precios del tomate, impacto combinado de técnicas de control climático y la regulación del clima aplicado. El rendimiento financiero neto en el caso de mayor tecnificación, dependía en menor grado de las variaciones anuales en el clima y más de las variaciones anuales de los precios del

tomate. Esto indica que un invernadero de bajo nivel de tecnificación depende en menor grado de las variaciones en los precios del tomate y que el invernadero con alto nivel de tecnificación depende en menor grado de las variaciones climáticas.

Para poder elegir de forma rápida y sencilla el mejor invernadero entre muchas alternativas, hemos integrado un algoritmo de optimización en el método de diseño (**Capítulo 6**). Este algoritmo maximiza el rendimiento financiero neto, optimizando la selección de alternativas para la realización de los siguientes ocho elementos de diseño: (i) el tipo de construcción de invernadero, (ii) el material de cubierta de invernadero, (iii) la presencia y el tipo de pantalla de sombreo exterior (iv), las propiedades de blanqueo para la disminución de la entrada de radiación, (v) la presencia y el tipo de pantalla térmica, (vi) la capacidad y el tipo de sistema de calefacción, (vii) la capacidad y el tipo de sistema de refrigeración, y (viii) la capacidad y el tipo de sistema de dosificación de CO₂. Un algoritmo de búsqueda controlado y variable (controlled random search algorithm) se aplicaba sobre 50 PC's veloces y adaptaba el diseño de invernadero al clima y las condiciones económicas locales para dos ubicaciones diferentes, Almería y Holanda. El modelo seleccionó un invernadero con una superficie relativamente grande de ventilación (la superficie de ventilación era igual al 20% de la superficie de suelo, mientras que esto era de un 14% para las condiciones holandesas), blanqueo para disminuir la temperatura del aire en el interior del invernadero y una capacidad relativamente baja de calefactor de aire (50 W/m² en comparación con 200 W/m² para las condiciones holandesas) para el clima soleado y cálido en Almería. Para el clima relativamente frío y oscuro en Holanda, el blanqueo no era necesario y el invernadero estaba equipado con una pantalla energética de un 100% de aluminio. Para ambas ubicaciones el método de diseño seleccionó invernaderos realistas y resultados financieros netos correspondientes, lo que indica que ha sido desarrollado un método fiable y robusto. Un análisis de los mejores invernaderos mostró que para ambas ubicaciones una construcción de invernadero con alta permeabilidad a la luz, mejoraba el rendimiento económico del invernadero mientras que una pantalla de sombreo exterior, calefacción geotérmica y refrigeración mecánica empeoraban el rendimiento del invernadero.

En el **Capítulo 7** se discute el método de diseño basado en modelos desarrollado. Basándonos en los resultados presentados podemos concluir que el objetivo de esta tesis se ha cumplido. El método de diseño de invernaderos generó dos invernaderos diferentes adaptados a las condiciones climáticas y económicas locales en España y en Holanda. Es de esperar que el método de diseño genere igualmente invernaderos fiables para otras ubicaciones ya que los modelos de su base han sido validados profundamente para una

amplia gama de climas. Hasta donde sabemos, es la primera vez que se describe en detalle y se soluciona en su mayor parte, un problema de optimización de diseño de invernadero. Para seguir optimizando el problema de diseño en su totalidad será necesario integrar en el método de diseño de invernadero la influencia de aspectos sociales, mano de obra y logística sobre el diseño de invernaderos. Se discuten aspectos para la mejora de la fiabilidad de los tres modelos. Dado el hecho que el método de diseño ha sido construido de forma genérica, estos aspectos se podrán integrar de forma sencilla en el método. La influencia de la inseguridad del clima y de los precios sobre el diseño de invernadero ha sido descrita y se han propuesto medidas para limitar su influencia. Finalmente se presentan perspectivas futuras del método de diseño.

Samenvatting

Wereldwijd kom je verschillende soorten kassen tegen. Deze verschillen worden veroorzaakt door lokale omstandigheden zoals het weer, economie, sociale condities, de wetgeving en de aanwezigheid van bronnen zoals water, energie en CO₂. Omdat er ook nog eens veel verschillende ontwerp elementen - bijvoorbeeld constructies, kasdekken, verwarmingssystemen en koelsystemen - beschikbaar zijn is het ontwerpen van kassen erg moeilijk. Daardoor worden er kassen ontworpen die niet goed zijn aangepast aan de lokale omstandigheden, waardoor deze financieel niet optimaal presteren. Een systematische aanpak die gebruik maakt van fysische, biologische en economische modellen is een veelbelovende manier om kassen te ontwerpen. Deze aanpak kan het mogelijk maken om kassen beter aan te passen aan lokale omstandigheden en om verbeteringen voor bestaande kassen aan te wijzen.

Het doel van dit proefschrift was het ontwikkelen van een methode die kasontwerpen genereert die geschikt zijn voor de lokale klimaat en economische condities. Deze methode moet functioneren voor de verschillende condities die men wereldwijd tegen kan komen. Omdat kasontwerp een ingewikkeld optimalisatieprobleem is, hebben we een ontwerp methode ontwikkeld die gebruik maakt van computermodellen. Deze methode maximaliseert het financiële resultaat van de kas door deze aan de lokale omstandigheden aan te passen. Het financiële resultaat van een kas is het verschil tussen de economische opbrengsten van bijvoorbeeld tomaten en de variabele en vaste kosten van de kas. In dit onderzoek hebben we ons gericht op tomaat als gewas, en het klimaat en economische condities zijn geselecteerd als randvoorwaarden. Tevens is het ontwerp probleem teruggebracht tot elementen die het kasklimaat beïnvloeden.

Een kasklimaatmodel is ontwikkeld om het klimaat in de kas (temperatuur, vochtigheid en de CO₂ concentratie van de lucht en de gewastemperatuur) te voorspellen (**Hoofdstuk 2**). De volgende variabelen zijn meegenomen in het model: het buitenklimaat (bv. zoninstraling, temperatuur, vochtigheid, windsnelheid en CO₂ concentratie), de klimaatregeling, het kasontwerp en het gewas. Om kassen te kunnen ontwerpen voor verschillende klimaten bevatte het model generieke kasontwerp elementen. Het voorspelde klimaat was vergeleken met het gemeten klimaat voor vier verschillende kassen en drie verschillende klimaten: een gematigd zeeklimaat, een Mediterraan klimaat en een semiwoestijn klimaat. Het model voorspelde voor al deze gevallen het kasklimaat nauwkeurig. In meer dan 78% van de gevallen was de afwijking tussen de simulaties en

metingen kleiner dan 10%.

In **Hoofdstuk 3** is het model beschreven dat de tomatenopbrengst voorspelt afhankelijk van de gewastemperatuur, de fotosynthetische actieve straling (PAR, het gedeelte van het zonlicht dat de plant gebruikt voor groei) en de CO₂ concentratie van de kaslucht (een hogere CO₂ concentratie stimuleert de groei). De oplossing van het kasontwerp probleem zal neigen naar kassen die zowel extreem lage als hoge temperaturen toestaan om investeringen en energiekosten zo laag mogelijk te houden. Daarom is het erg belangrijk dat deze temperatuureffecten op tomaten opbrengst goed beschreven zijn. Een literatuurstudie maakte duidelijk dat zowel lage als hoge temperaturen een negatieve invloed hebben op verschillende groei en ontwikkelingsprocessen van de plant wat vervolgens resulteert in een lagere tomatenopbrengst. Zowel directe en gemiddelde temperatuur effecten beïnvloeden de tomatengroei en deze effecten zijn op een simpele manier geïmplementeerd in het model. Zonder aanpassing van vooraf vastgestelde modelparameters was het ontwikkelde model in staat om de tomatenopbrengst nauwkeurig te voorspellen voor vier verschillende temperatuur trajecten, namelijk voor: bijna optimale temperaturen voor Nederlandse kasklimaat condities; niet-optimale temperaturen voor Zuid Spaanse kasklimaat condities; extreem lage en hoge gemiddelde temperaturen en extreme dagelijkse temperatuur schommelingen.

Hoofdstuk 4 beschrijft een gevoeligheidsanalyse om de parameters te onthullen die de meeste invloed hebben op het kasontwerp en om ons begrip van het ontwerpproces te vergroten. Drie gevoeligheidsanalyse technieken zijn toegepast op het gecombineerde kasklimaat-tomatenopbrengst model om de gevoeligheden te bepalen voor een kas met een laag technologieniveau in Almeria, Zuid-Spanje en voor een kas met een hoog technologieniveau in Texas, Verenigde Staten. Het model voorspelde voor beide locaties het binnenklimaat en de tomatenopbrengst realistisch. Resultaten van de gevoeligheidsanalyse gericht op het effect van één parameter toonden aan dat het buitenklimaat de meeste invloed had op de prestaties van de kas, gevolgd door de ontwerpparameters en de setpoints om het binnenklimaat te regelen. Het kiezen van een juiste locatie om een kas te bouwen is dus erg belangrijk. Wat betreft de kasparameters, PAR was de belangrijkste factor voor de prestatie van kassen. Om de tomatenopbrengst te verhogen moeten structuren met een hogere doorlaatbaarheid voor het groeilicht ontworpen worden, tevens moeten de kassen uitgerust worden met kalk of een scherm die de nabij-infrarode straling (NIR, het gedeelte van het zonlicht dat als warmtebron voor de kas fungeert) selectief doorlaat. Resultaten van deze gevoeligheidsanalyse lieten zien of de capaciteit van het verwarmingssysteem en de CO₂ toediening voldoende was. Ook werden

kasparameters onthuld die aangepast moeten worden om water, energie en CO₂ te besparen. De impact van licht op tomatenopbrengst varieerde gedurende de seizoenen wat suggereert dat aanpasbare kasdek eigenschappen een voordeel hebben ten opzichte van vaste kasdek eigenschappen. Resultaten van de gevoeligheidsanalyse gericht op gecombineerde effecten van parameters onthulde sterke gecombineerde effecten van de PAR transmissie en ventilatie setpoint op tomatenopbrengst. De gebruikte gevoeligheidsanalyse technieken zijn in staat om de impact van zowel één parameter, gecombineerde parameters als hun tijdsafhankelijkheid op tomatenopbrengst, het binnenklimaat en op de consumptie van bronnen te kwantificeren. Echter, om het inzicht in belangrijke kasontwerp aspecten te verbeteren moet de impact op het netto financiële resultaat van de kas worden bepaald.

Het economische model dat het netto financiële resultaat (NFR) berekent als functie van de tomatenopbrengst, het verbruik van de bronnen en de afschrijving en onderhoud van de kas is beschreven in **Hoofdstuk 5**. Het economisch model was samengevoegd met het kasklimaat-tomatenopbrengst model zodat uit tien verschillende kasontwerpen – allemaal variërend in technologieniveau - de tomatenkas met het hoogste netto financiële resultaat voor Zuid Spaanse condities kon worden bepaald. De kasontwerpen waren een typische plastic parral kas met een lage dakhelling of een boogkas uitgerust met verschillende combinaties van technieken om het kasklimaat te beïnvloeden zoals systemen om te verwarmen, vocht te vernevelen (om de lucht te koelen) en om CO₂ te doseren. Resultaten toonden aan dat een boogkas met alleen verneveling het meest rendabel was, gevolgd door een boogkas uitgerust met verwarming, verneveling en CO₂ dosering. Het verschil in financieel resultaat tussen een dergelijke kas en een relatief goedkope parral kas was echter klein in vergelijking met het verschil in investering. Een gevoeligheidsanalyse van het netto financiële resultaat voor de twee technologie extremen onthulde dat de tomatenprijs, de fractie van de verkoopbare tomaten en de PAR doorlaatbaarheid van het kasdek de grootste impact hadden op het NFR. De resultaten toonden aan dat de financiële prestatie van de kas sterk beïnvloed werd door vier factoren: het weer, de tomaten prijzen, gecombineerde impact van technieken om het klimaat te regelen en de toegepaste klimaatbesturing. Het netto financiële resultaat hing met toenemend technologieniveau minder af van jaarlijkse variaties in het buitenklimaat en meer af van jaarlijkse variaties in tomatenprijzen. Dit geeft aan dat een kas met een laag technologieniveau minder afhankelijk is van variaties in tomatenprijs en dat een kas met een hoog technologieniveau minder afhankelijk is van variaties in het klimaat.

Om relatief snel en gemakkelijk de beste kas uit een heleboel alternatieven te kunnen kiezen, hebben we een optimalisatie algoritme geïntegreerd in de ontwerp methode

(Hoofdstuk 6). Dit algoritme maximaliseert het netto financiële resultaat door het optimaliseren van de selectie van alternatieven om de volgende acht ontwerpelementen te vervullen: (i) het type kasconstructie, (ii) het kasdekmetaal, (iii) de aanwezigheid en het type buiten schaduw scherm (iv), de eigenschappen van kalk om de zoninstraling te verminderen, (v) de aanwezigheid en het type thermisch scherm, (vi) de capaciteit en het type verwarmingssysteem en capaciteit, (vii) de capaciteit en het type koelsysteem, en (viii) de capaciteit en het type CO₂ toedieningsysteem. Een gecontroleerd variabel zoekalgoritme (controlled random search algorithm) was toegepast op 50 snelle PC's en paste het kasontwerp aan op het lokale klimaat en economische omstandigheden voor twee verschillende locaties, Almeria en Nederland. Het model selecteerde een kas met een relatief groot ventilatie oppervlak (het ventilatie oppervlak was net zo groot als 20% van het grondoppervlak terwijl dit voor Nederlandse omstandigheden 14% was), kalk om de kaslucht temperatuur te verlagen en een relatief lage capaciteit hete-lucht kanon (50 W/m² vergeleken met 200 W/m² voor Nederlandse omstandigheden) voor het zonnige en warme klimaat in Almeria. Voor het relatieve koude en donkere klimaat in Nederland, was kalk niet nodig en was de kas uitgerust met een energiescherm van 100% aluminium. Voor beide locaties selecteerde de ontwerp methode realistische kassen en bijbehorende netto financiële resultaten wat aangeeft dat een robuuste en betrouwbare methode was ontwikkeld. Een analyse van de beste kassen liet zien dat voor beide locaties een kasconstructie met een hoge lichtdoorlaatbaarheid de economische prestatie van de kas verbeterde terwijl een buiten schaduw scherm, geothermische verwarming en mechanische koeling de prestatie van de kas verslechterde.

In **Hoofdstuk 7** wordt de ontwikkelde modelgebaseerde ontwerp methode bediscussieerd. Gebaseerd op de gepresenteerde resultaten kunnen we concluderen dat het doel van dit proefschrift is vervuld. De kasontwerpmethode genereerde namelijk twee verschillende kassen die geschikt waren voor de lokale klimaat en economische condities in Spanje en Nederland. Het mag worden verwacht dat de ontwerp methode ook voor andere locaties betrouwbare kassen genereert omdat de onderliggende modellen grondig zijn gevalideerd voor een breed scala aan klimaten. Voor zover wij weten, is het de eerste keer dat een kasontwerp optimalisatie probleem gedetailleerd is beschreven en gedeeltelijk is opgelost. Om het hele ontwerp probleem verder te optimaliseren, moet de invloed van sociale aspecten, arbeid en logistiek op het kasontwerp worden geïntegreerd in de kasontwerpmethode. Aspecten om de betrouwbaarheid van de drie modellen te verbeteren worden bediscussieerd. Omdat de ontwerp methode generiek is opgezet kunnen deze aspecten eenvoudig geïntegreerd worden in de methode. De invloed van onzekerheid in

klimaat en prijzen op het kasontwerp is beschreven en maatregelen om hun invloed te beperken zijn voorgesteld. Tenslotte worden de toekomstige perspectieven van de ontwerpmethode gepresenteerd.

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Bram

Curriculum Vitae

Bram Henricus Emanuel Vanthoor was born on November 7th 1980 in Mariaheide, The Netherlands. He attended secondary school at the Fioretti College in Veghel. After receiving his VWO diploma in 1999 he started his studies in Agricultural Engineering at Wageningen University. In his major thesis he modelled and optimised the nutrient supply to tomatoes. This research was executed at the System and Control group of Wageningen University. For his six months internship Bram went to La Universidad Autónoma Chapingo in Mexico. He measured and modelled the greenhouse climate of a passive naturally ventilated greenhouse at the central highland of Mexico. After graduating in November 2005 he started his PhD project that focussed on the development of a model-based greenhouse design method for worldwide conditions. This project was executed at the institute Wageningen UR Greenhouse Horticulture and at the Farm Technology Group of Wageningen University. Since March 2011 Bram lives in Santiago de Querétaro, Mexico and works there as Business Developer for HortiMaX.

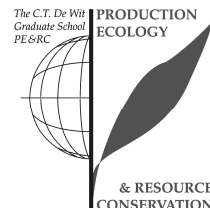


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- Systematic Integral Design in Protected Cultivation Systems; presented at Priva B.V. (2006)

Writing of project proposal (2.5 ECTS)

- Systematic Integral Design of Protected Cultivation Systems (2006)

Post-graduate courses (4 ECTS)

- Uncertainty modelling and analysis (2008)

Laboratory training and working visits (4.5 ECTS)

- Economic evaluation of different Spanish greenhouse designs; Fundación Cajamar, Las Palmerillas, Almería, Spain (2010)

Invited review of (unpublished) journal (1 ECTS)

- Biosystems Engineering: greenhouse climate modelling (2007)

Deficiency, refresh, brush-up courses (1.6 ECTS)

- Information literacy (2006)
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- Maths & Stats (2006-2010)
- PhD Discussion group of the Farm Technology Group (2007-2009)
- Kick off meeting EU project Euphoros (2008)

International symposia, workshops and conferences (6.3 ECTS)

- International symposium on high technology for greenhouse system management; Naples, Italy (2007)
- Strategies towards sustainability of protected cultivation in mild winter climate; Antalya, Turkey (2008)
- Model-IT: applications of modeling as an innovative technology in the agri-food chain; Madrid, Spain (2008)

Lecturing / supervision of practical 's / tutorials (4.5 ECTS)

- MSc. Course: greenhouse technology; 15 days (2007-2008)

Supervision of 1 MSc student; 10 days (3 ECTS)

- Optimization of greenhouse design in Ethiopia (2008)

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