

Binary limits of ternary systems

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1 Introduction

This memo discusses the binary limit of diffusion- and thermal diffusion coefficients in ternary systems, i.e. the behaviour of the coefficients when the mole fraction of one species in the system approaches zero. As an initial remark, please note that if one of the mole fractions is exactly zero, the solutions to Eq. (6), (8) and (10) in [1] are ill-defined, such that we cannot model a binary system as a ternary system where one mole fraction is exactly zero. We can, however, investigate the behaviour when one mole fraction approaches zero.

The purpose of this memo is to give some insight into which ternary coefficients approach various binary coefficients in the binary limit, as well as showing how the formulation of the force-flux relations in the respective binary and ternary systems effects these relations.

Finally, the current memo serves as a consistency check for the ternary coefficients computed using the KineticGas package.

2 Diffusion

This section discusses the binary limit of the diffusion coefficients in a ternary system. The purpose of the section is to give insight into how the force-flux in a binary system relate to those in a ternary, how to interpret the diffusion coefficients in a ternary system, and raise awareness regarding potential pitfalls when attempting to model a ternary system as a pseudo-binary system.

2.1 Notation

In the following text, $D_{ii}^{(b)}$ is used to denote the diffusion coefficient of a binary system, where component i is the independent component. $D_{ii}^{(k)}$ denotes the diagonal elements of the Fick diffusion matrix

in a ternary system, where component k is the dependent component. D_{ij} denotes the non-diagonal elements of the Fick diffusion matrix in a ternary system, where components i and j are the independent components.

In section 2.3, $\tilde{D}_{ij}^{(t)}$ and $\tilde{D}_{ij}^{(b)}$ are used to denote the diffusion coefficients corresponding to the linearly dependent formulations of Fick's law.

2.2 Independent Fluxes

For a ternary system (1, 2, 3), we can formulate Fick's law for a set of independent fluxes as either

$$\begin{pmatrix} J_1 \\ J_2 \end{pmatrix} = \begin{bmatrix} D_{11}^{(3)} & D_{12} \\ D_{21} & D_{22}^{(3)} \end{bmatrix} \begin{pmatrix} \nabla c_1 \\ \nabla c_2 \end{pmatrix}, \quad (1)$$

$$\begin{pmatrix} J_1 \\ J_3 \end{pmatrix} = \begin{bmatrix} D_{11}^{(2)} & D_{13} \\ D_{31} & D_{33}^{(2)} \end{bmatrix} \begin{pmatrix} \nabla c_1 \\ \nabla c_3 \end{pmatrix}, \quad (2)$$

or

$$\begin{pmatrix} J_2 \\ J_3 \end{pmatrix} = \begin{bmatrix} D_{22}^{(1)} & D_{23} \\ D_{32} & D_{33}^{(1)} \end{bmatrix} \begin{pmatrix} \nabla c_2 \\ \nabla c_3 \end{pmatrix}. \quad (3)$$

Where the superscript on the diffusion coefficients indicates which component is the dependent component.

For a binary system (1, 2), we can choose between

$$J_1^{(b)} = D_{11}^{(b)} \nabla c_1 \quad (4)$$

and

$$J_2^{(b)} = D_{22}^{(b)} \nabla c_2. \quad (5)$$

Now we can examine the question: "When $x_3 \rightarrow 0$, and (necessarily) $\nabla c_3 \rightarrow 0$ and $J_3 \rightarrow 0$, do the ternary coefficients reduce to the corresponding binary coefficients?"

To answer that question, we must be clear about which ternary formulation reduces to which binary formulation.

In the ternary formulation (2), J_2 is the dependent flux, so if $x_3 = \nabla c_3 = 0$ (something we are free to demand, as ∇c_1 and ∇c_3 are independent), $J_1 = D_{11}^{(2)} \nabla c_1$. Thus, we expect that formulation (2) should reduce to formulation (4) when $x_3 = \nabla c_3 = 0$. Therefore, we expect

$$D_{11}^{(2)}(x_3 = 0) = D_{11}^{(b)}. \quad (6)$$

By similar argument, it's formulation (3) that reduces to formulation (5), so

$$D_{22}^{(1)}(x_3 = 0) = D_{22}^{(b)}. \quad (7)$$

Note that formulation (1) does not immediately reduce to one of the binary formulations when $x_3 \rightarrow 0$; this is because in this formulation, we cannot demand $\nabla c_3 = 0$ because component 3 is the dependent component in this formulation. Therefore, the coefficients in formulation (1) cannot be expected to reduce to the binary coefficients when $x_3 \rightarrow 0$.

Figure 1 shows how the ternary coefficients expected to reduce to the corresponding binary coefficients behave as a function of x_3 .

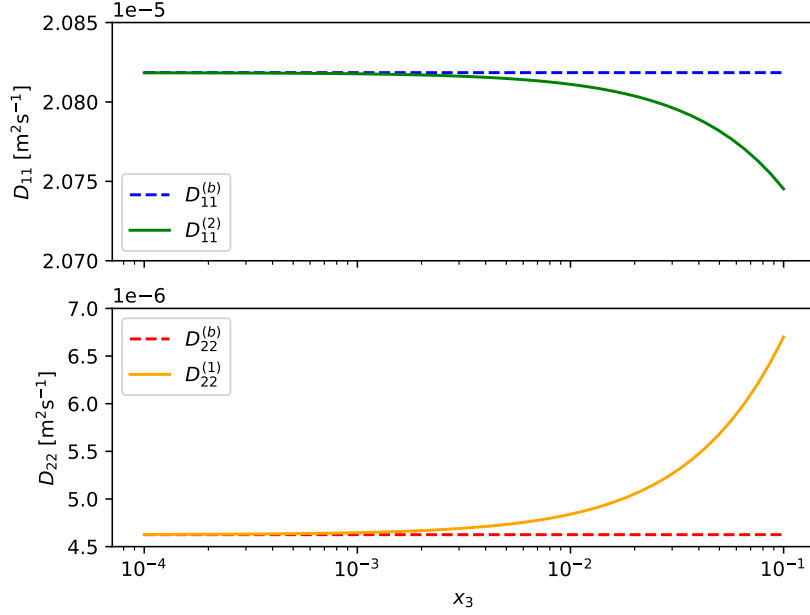


Figure 1: The ternary diffusion coefficients reduce to the corresponding binary coefficients when $x_3 \rightarrow 0$.

2.3 Dependent Fluxes

An alternative flux-force formulation for the ternary system is through a set of *dependent* fluxes and forces; thus, we can formulate Fick's law as

$$\begin{pmatrix} J_1 \\ J_2 \\ J_3 \end{pmatrix} = \begin{bmatrix} \tilde{D}_{11}^{(t)} & \tilde{D}_{12}^{(t)} & \tilde{D}_{13}^{(t)} \\ \tilde{D}_{21}^{(t)} & \tilde{D}_{22}^{(t)} & \tilde{D}_{23}^{(t)} \\ \tilde{D}_{31}^{(t)} & \tilde{D}_{32}^{(t)} & \tilde{D}_{33}^{(t)} \end{bmatrix} \begin{pmatrix} \nabla c_1 \\ \nabla c_2 \\ \nabla c_3 \end{pmatrix}, \quad (8)$$

and correspondingly for the binary system:

$$\begin{pmatrix} J_1 \\ J_2 \end{pmatrix} = \begin{bmatrix} \tilde{D}_{11}^{(b)} & \tilde{D}_{12}^{(b)} \\ \tilde{D}_{21}^{(b)} & \tilde{D}_{22}^{(b)} \end{bmatrix} \begin{pmatrix} \nabla c_1 \\ \nabla c_2 \end{pmatrix}. \quad (9)$$

Note that these two matrices are not invertible because they implicitly contain the dependency $J_1 + J_2 + J_3 = 0$. However, this formulation can be useful for consistency checking because when $x_3 \rightarrow 0$, Equation (10) should hold:

$$\begin{bmatrix} \tilde{D}_{11}^{(t)} & \tilde{D}_{12}^{(t)} \\ \tilde{D}_{21}^{(t)} & \tilde{D}_{22}^{(t)} \end{bmatrix} = \begin{bmatrix} \tilde{D}_{11}^{(b)} & \tilde{D}_{12}^{(b)} \\ \tilde{D}_{21}^{(b)} & \tilde{D}_{22}^{(b)} \end{bmatrix}. \quad (10)$$

This equality should hold precisely because the matrices contain the dependence between the fluxes and forces, and when $x_3 = \nabla c_3 = 0$, $J_1 + J_2 = 0$, and we should obtain the same fluxes as from the binary matrix.

Figure 2 demonstrates that Equation (10) is satisfied when $x_3 \rightarrow 0$.

Finally, for the ternary matrix, we can observe that

$$\tilde{D}_{13} - \tilde{D}_{23} = 0 \quad (11)$$

when $x_3 = 0$ because when $x_3 = \nabla c_3 = 0$, $\nabla c_2 = -\nabla c_1$, and J_3 should vanish. Figure 3 demonstrates that this condition is met.

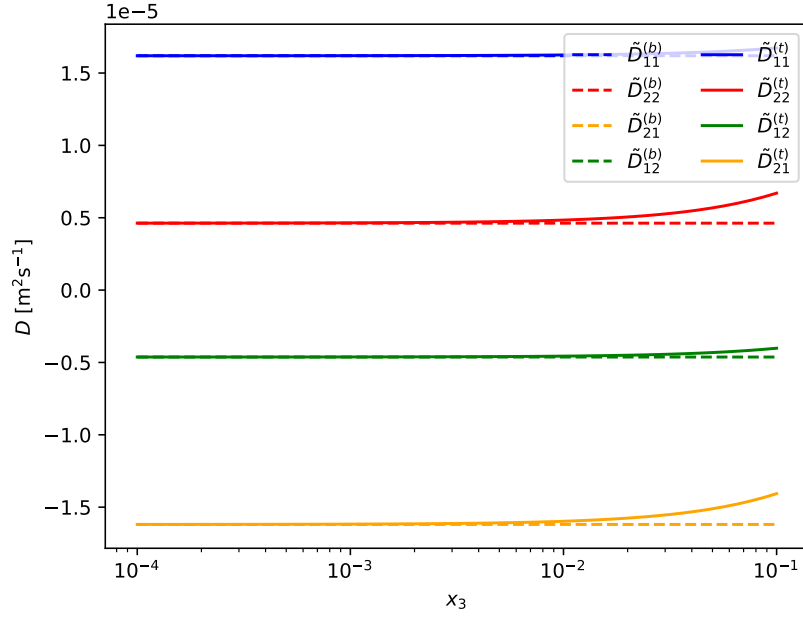


Figure 2: The coefficients in the singular, ternary Fick matrix reduce to the corresponding coefficients in the singular, binary Fick matrix when $x_3 \rightarrow 0$.

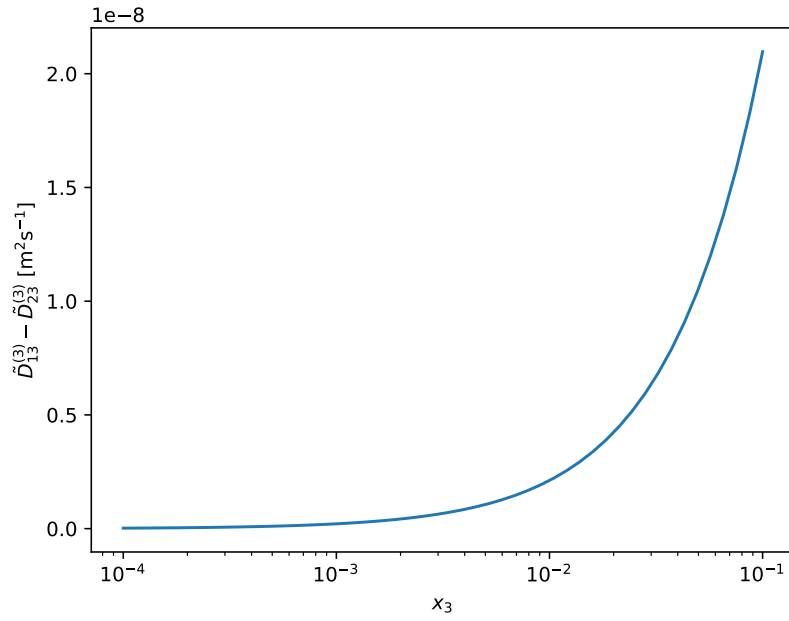


Figure 3: The flux J_3 vanishes when $x_3 \rightarrow 0$ and $\nabla c_3 = 0$.

3 Thermal diffusion

This section shows how the thermal diffusion coefficients relate to those in a binary system in the binary limit. The section also gives some insight into different definitions of the thermal diffusion coefficient, with the aim of showing that the definition is not arbitrary if one wishes to relate the ternary coefficients to the respective binary coefficients.

3.1 Notation

For fluxes the superscript (i, j) is used, where i is the basis (m for mass-based, n for mole based) and j is the frame of reference. Thermal diffusion coefficients are denoted $D_{T,i}$, the superscript (z) denotes thermal diffusion coefficients as defined by Ortiz de Zárate [2], while superscripts (m) and (n) denote the independent thermal diffusion coefficients in the centre of mass, and centre of moles FoR, as defined in ref. [1].

Similarly, diffusion matrices are superscripted with (x) and (w) to denote those defined by Ortiz de Zárate using the same notation, while superscripts (m) and (n) are used for the independent diffusion matrices in the CoM and CoN FoR as defined in ref. [1].

The notation $D_{T,i}^{(z,tj)}$ denotes the thermal diffusion coefficient of species i in a ternary mixture with species j taken to be the dependent species, as defined in ref. [2] while $D_{T,i}^{(z,bj)}$ denotes the thermal diffusion coefficient of species i in a binary mixture, with species j taken to be the dependent species.

Boldface roman font (\mathbf{v}) is used to indicate vectors, and slanted underlined boldface figures ($\underline{\mathbf{D}}$) are used to indicate matrices. The notation $\nabla \mathbf{v}$, should be understood not as a dot product, but as a vector of gradients (i.e. $\nabla \mathbf{v} \equiv (\nabla v_1, \nabla v_2, \dots)^\top$, in which case the equations should be understood to hold componentwise for these gradients.

3.2 Definitions of the thermal diffusion coefficient

The default definition of the thermal diffusion coefficient in a multicomponent mixture in the KineticGas package is

$$J_i^{(n,m)} = D_{T,i}^{(m)} \nabla \ln T - \sum_{j \neq \ell} D_{ij}^{(m)} \nabla c_j \quad (12)$$

where the superscript (n, m) indicates that the flux is on a molar basis in the centre of mass (CoM) frame of reference (FoR), and the superscripts (m) indicate that the coefficients apply to the CoM FoR. Component ℓ is the dependent component, which defaults to the last component in the mixture. For later convenience, we rewrite this for a ternary system as

$$\begin{aligned} \begin{pmatrix} J_1^{(n,m)} \\ J_1^{(n,m)} \end{pmatrix} &= -\underline{\mathbf{D}}^{(m)} \begin{pmatrix} \nabla c_1 \\ \nabla c_1 \end{pmatrix} + \begin{pmatrix} D_{T,1}^{(m)} \\ D_{T,2}^{(m)} \end{pmatrix} \nabla \ln T \\ \mathbf{J}^{(n,m)} &= -\underline{\mathbf{D}}^{(m)} \nabla \mathbf{c} + \mathbf{D}_T^{(m)} \nabla \ln T \end{aligned} \quad (13)$$

In the centre of moles frame of reference, the diffusion- and thermal diffusion coefficients are defined by

$$\mathbf{J}^{(n,n)} = -\underline{\mathbf{D}}^{(n)} \nabla \mathbf{c} + \mathbf{D}_T^{(n)} \nabla \ln T. \quad (14)$$

and they are related by

$$\underline{\mathbf{D}}^{(n)} = \underline{\Psi}^{n \leftarrow m} \underline{\mathbf{D}}^{(m)}, \quad \mathbf{D}_T^{(n)} = \underline{\Psi}^{n \leftarrow m} \mathbf{D}_T^{(m)}, \quad (15)$$

with $\underline{\Psi}^{n \leftarrow m}$ being the transformation matrix given in the supporting information of [1], adapted to a $(N_c - 1) \times (N_c - 1)$ matrix, rather than the original $N_c \times N_c$ matrix, by using the linear dependence of the fluxes.

In 2019 Ortiz de Zárate [2] showed that one can define thermal diffusion coefficients that are equivalent in the centre of mass and centre of moles frames of reference, if one defines them through either

$$\begin{aligned}\mathbf{J}^{(n,n)} &= -c \left(\underline{\mathbf{D}}^{(x)} \nabla \mathbf{x} + \underline{\mathbf{X}} \mathbf{D}_T^{(z)} \nabla T \right), \quad \text{or} \\ \mathbf{J}^{(m,m)} &= -\rho \left(\underline{\mathbf{D}}^{(w)} \nabla \mathbf{w} + \underline{\mathbf{W}} \mathbf{D}_T^{(z)} \nabla T \right)\end{aligned}\tag{16}$$

where the matrices $\underline{\mathbf{X}}$ and $\underline{\mathbf{W}}$ are given by

$$X_{ij} = \delta_{ij} x_i - x_i x_j, \quad W_{ij} = \delta_{ij} w_i - w_i w_j.\tag{17}$$

The superscripts (x) and (w) indicate diffusion matrices that apply in the centre of moles and centre of mass FoR respectively, when using these definitions. The superscript (z) marks the thermal diffusion coefficients as defined by Eq. (16). When using this definition of the thermal diffusion coefficient, Ortiz de Zárate shows that

$$\lim_{x_2 \rightarrow 0} D_{T,1}^{(z,t3)} = D_{T,1}^{(z,b3)},\tag{18}$$

where $D_{T,1}^{(z,t)}$ is the thermal diffusion coefficient of species 1 in a ternary mixture, and $D_{T,1}^{(z,b3)}$ is the thermal diffusion coefficient of species 1 in a binary mixture with species 3, both as defined by Eq. (16). that is: For a ternary system (1, 2, 3), when the mole fraction of species 2 tends to zero, the thermal diffusion coefficient of species 1 approaches the thermal diffusion coefficient of species 1 in the binary mixture (1, 3). This relation follows from an argument analogous to that in section 2.2.

For an ideal gas can relate the thermal diffusion coefficients $\mathbf{D}_T^{(n)}$ to the $\mathbf{D}_T^{(z)}$, by rewriting Eq. (14) as

$$\begin{aligned}\mathbf{J}^{(n,n)} &= -\underline{\mathbf{D}}^{(n)} (c \nabla \mathbf{x} + \mathbf{x} \nabla c) + \mathbf{D}_T^{(n)} \nabla \ln T \\ &= -\underline{\mathbf{D}}^{(n)} (c \nabla \mathbf{x} - \mathbf{x} c \nabla \ln T) + \mathbf{D}_T^{(n)} \nabla \ln T \\ &= -c \underline{\mathbf{D}}^{(n)} \nabla \mathbf{x} + \frac{1}{T} \left(\mathbf{D}_T^{(n)} + c \underline{\mathbf{D}}^{(n)} \mathbf{x} \right) \nabla T\end{aligned}\tag{19}$$

such that $\mathbf{D}_T^{(z)}$ is given by the solution to

$$-c \underline{\mathbf{X}} \mathbf{D}_T^{(z)} = \frac{1}{T} \left(\mathbf{D}_T^{(n)} + c \underline{\mathbf{D}}^{(n)} \mathbf{x} \right), \quad \text{Ideal gas}\tag{20}$$

where we have made use of $\nabla c = c \nabla \ln T$ for an ideal gas. For a non-ideal gas the corresponding expression is

$$\begin{aligned}\mathbf{J}^{(n,n)} &= -\underline{\mathbf{D}}^{(n)} \left[\left(\frac{\partial \mathbf{c}}{\partial T} \right)_{\mathbf{x},p} \nabla T + \underline{\mathbf{\Gamma}}_c \nabla \mathbf{x} \right] + \frac{1}{T} \mathbf{D}_T^{(n)} \nabla T \\ &= -\underline{\mathbf{D}}^{(n)} \underline{\mathbf{\Gamma}}_c \nabla \mathbf{x} + \left[\frac{1}{T} \mathbf{D}_T^{(n)} - \underline{\mathbf{D}}^{(n)} \left(\frac{\partial \mathbf{c}}{\partial T} \right)_{\mathbf{x},p} \right] \nabla T,\end{aligned}\tag{21}$$

where

$$[\underline{\mathbf{\Gamma}}_c]_{ij} = \left(\frac{\partial c_i}{\partial x_j} \right)_{T,p,x_{k \neq j}},\tag{22}$$

and it can be useful to note that

$$\begin{aligned}c_i = \frac{x_i}{v} &\implies \\ \left(\frac{\partial c_i}{\partial T} \right)_{p,\mathbf{x}} &= -\frac{x_i}{v^2} \left(\frac{\partial v}{\partial T} \right)_{p,\mathbf{x}}, \\ \left(\frac{\partial c_i}{\partial x_j} \right)_{T,p,x_{k \neq j}} &= \frac{\delta_{ij}}{v} - \frac{c_i v_j}{v},\end{aligned}\tag{23}$$

and to keep in mind that these matrices and vectors are in \mathbb{R}^{s-1} , because the dependent component is excluded. **Note:** At the time of writing, the expressions for non-ideal gas have not been implemented.

Returning to an ideal gas, using $\nabla c = c \nabla \ln T$, and noting that we can write $\nabla \mathbf{x} = \underline{\mathbf{T}}^{x \leftarrow w} \nabla \mathbf{w}$, we can rewrite equation (13) as

$$\begin{aligned} \mathbf{J}^{(n,m)} &= -\underline{\mathbf{D}}^{(m)} \nabla c + \mathbf{D}_T^{(m)} \nabla \ln T \\ &= -c \underline{\mathbf{D}}^{(m)} \nabla \mathbf{x} + \frac{1}{T} \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) \nabla T \\ &= -c \underline{\mathbf{D}}^{(m)} \underline{\mathbf{T}}^{x \leftarrow w} \nabla \mathbf{w} + \frac{1}{T} \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) \nabla T \\ \mathbf{J}^{(m,m)} &= -\text{diag}(\mathbf{M}) c \underline{\mathbf{D}}^{(m)} \underline{\mathbf{T}}^{x \leftarrow w} \nabla \mathbf{w} + \frac{1}{T} \text{diag}(\mathbf{M}) \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) \nabla T \end{aligned} \quad (24)$$

where $\mathbf{M} = (M_1, M_2, \dots)^\top$ is the vector of molar masses, such that $\mathbf{D}_T^{(z)}$ is given by the solution to

$$-\rho \underline{\mathbf{W}} \mathbf{D}_T^{(z)} = \frac{1}{T} \text{diag}(\mathbf{M}) \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right). \quad (25)$$

Together, Eqs. (20) and (25) allow for a consistency check on the transformation matrices $\underline{\Psi}^{m \leftarrow n}$ and $\underline{\Psi}^{n \leftarrow m}$, as we should have

$$\begin{aligned} \frac{1}{c} \underline{\mathbf{X}}^{-1} \left(\mathbf{D}_T^{(n)} + c \underline{\mathbf{D}}^{(n)} \mathbf{x} \right) &= \frac{1}{\rho} \underline{\mathbf{W}}^{-1} \text{diag}(\mathbf{M}) \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) \\ &= \frac{1}{\rho} \underline{\mathbf{W}}^{-1} \text{diag}(\mathbf{M}) \underline{\Psi}^{m \leftarrow n} \left(\mathbf{D}_T^{(n)} + c \underline{\mathbf{D}}^{(n)} \mathbf{x} \right) \\ \underline{\mathbf{I}} &= \frac{c}{\rho} \underline{\mathbf{X}} \underline{\mathbf{W}}^{-1} \text{diag}(\mathbf{M}) \underline{\Psi}^{m \leftarrow n}, \quad \text{and} \\ \frac{1}{c} \underline{\mathbf{X}}^{-1} \underline{\Psi}^{n \leftarrow m} \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) &= \frac{1}{\rho} \underline{\mathbf{W}}^{-1} \text{diag}(\mathbf{M}) \left(\mathbf{D}_T^{(m)} + c \underline{\mathbf{D}}^{(m)} \mathbf{x} \right) \\ \frac{\rho}{c} \text{diag}(\mathbf{M}^{-1}) \underline{\mathbf{W}} \underline{\mathbf{X}}^{-1} \underline{\Psi}^{n \leftarrow m} &= \underline{\mathbf{I}} \end{aligned} \quad (26)$$

As a second side-effect of this procedure, we can relate the diffusion matrices (for an ideal gas), as defined by Eqs. (16) to $\underline{\mathbf{D}}^{(m)}$ and $\underline{\mathbf{D}}^{(n)}$ as

$$\begin{aligned} \underline{\mathbf{D}}^{(x)} &= \underline{\mathbf{D}}^{(n)} \\ \underline{\mathbf{D}}^{(w)} &= \frac{c}{\rho} \text{diag}(\mathbf{M}) \underline{\mathbf{D}}^{(m)} \underline{\mathbf{T}}^{x \leftarrow w} \end{aligned} \quad (27)$$

and remark that Ortiz de Zárate gives the relation

$$\underline{\mathbf{W}}^{-1} \underline{\mathbf{D}}^{(w)} \underline{\mathbf{W}} = \underline{\mathbf{X}}^{-1} \underline{\mathbf{D}}^{(x)} \underline{\mathbf{X}} \equiv \underline{\mathbf{D}}^{(z)}, \quad (28)$$

which can serve as a second consistency check.

All the consistency checks mentioned above have been carried out numerically and been found to pass.

In light of Eq. (27), the simplest way to implement these diffusion matrices is likely to implement $\underline{\mathbf{D}}^{(n)}$, and to compute $\underline{\mathbf{D}}^{(w)}$ and $\underline{\mathbf{D}}^{(z)}$ using the relations in Eq. (28). This is the approach taken in the KineticGas package.

3.2.1 The binary case

For convenience, the binary transformations are given explicitly as

$$\begin{aligned} D_{T,1}^{(z,b3)} &= -\frac{D_{T,1}^{(n,b3)} + c_1 D_{11}^{(n,b3)}}{c_1 (1 - x_1) T} \\ &= -\frac{D_{T,1}^{(m,b3)} + c_1 D_{11}^{(m,b3)}}{c_1 (1 - w_1) T} \end{aligned} \quad (29)$$

3.3 The binary limit

With the path to obtaining $\mathbf{D}_T^{(z)}$ established, we can now investigate the binary limit of a ternary system. The ternary system investigated consists of species (1, 2, 3) and has the molar composition $\mathbf{x}_t = (x_1(1 - x_2), x_2, (1 - x_1)(1 - x_2))$. We are comparing it to a binary system of species (1, 3) with composition $\mathbf{x}_b = (x_1, 1 - x_1)$, such that the systems are exactly equivalent when $x_2 = 0$. In both systems we take species 3 to be the dependent species.

The results are shown in Figs. 4 and 5.

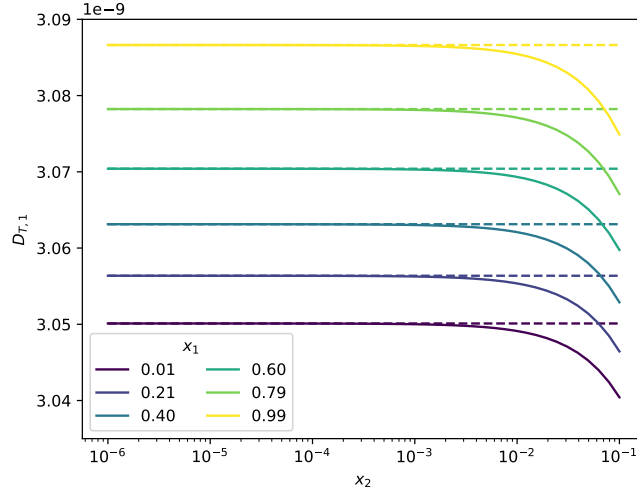


Figure 4: The thermal diffusion coefficient $D_{T,1}^{(z,t)}$ in the ternary mixture (1, 2, 3) (solid lines), and the thermal diffusion coefficient $D_{T,1}^{z,b3}$ in the binary mixture (1, 3) (dashed lines), at different mole fractions of species 1 (colors). x_1 indicates the mole fraction of species 1 in the binary, i.e. $x_1 = n_1/(n_1 + n_3)$, such that the composition of the ternary is $\mathbf{x}_t = (x_1(1 - x_2), x_2, (1 - x_1)(1 - x_2))$.

As seen immediately from Fig. 4, the ternary coefficient (solid lines) approaches the expected binary coefficient as $x_2 \rightarrow 0$. Note also the logarithmic scale, and that even at mole fractions of species 2 as small as $x_2 = 10^{-2}$, there is an appreciable difference in $D_{T,1}$ in the ternary compared to the corresponding binary. As seen more clearly in Fig. 5, the effect of increasing x_2 on $D_{T,1}$ is largest when x_1 is large. This could indicate that, contrary to intuition, if one wishes to model a ternary system with $x_1 > x_2 \gg x_3$ as a binary, neglecting the presence of species 3, a better estimate for thermal diffusion is obtained by taking species 2 as the independent species.

Explicitly: For a ternary system consisting of a trace component in air, the best estimate for thermal diffusion appears to be obtained if one models this as a binary mixture of nitrogen with the tracer *taking the tracer to be the independent species*.

4 Soret coefficients

The Soret coefficient is a measure of the steady state separation in a mixture induced by a temperature gradient. Ortiz de Zárate [2] defines the Soret coefficients of a multicomponent mixture (s components) through

$$\begin{bmatrix} x_1(1 - x_1) & x_1x_2 & \cdots & x_1x_{s-1} \\ x_2x_1 & x_2(1 - x_2) & \cdots & x_2x_{s-1} \\ \vdots & & \ddots & \vdots \\ x_{s-1}x_1 & & & x_{s-1}(1 - x_{s-1}) \end{bmatrix} \begin{pmatrix} S_{T,1} \\ S_{T,2} \\ \vdots \\ S_{T,s-1} \end{pmatrix} = -\frac{1}{\nabla T} \begin{pmatrix} \nabla x_1 \\ \nabla x_2 \\ \vdots \\ \nabla x_{s-1} \end{pmatrix}, \quad (30)$$

or more compactly,

$$\underline{\mathbf{X}}\mathbf{S}_T = -\frac{\nabla \mathbf{x}}{\nabla T}. \quad (31)$$

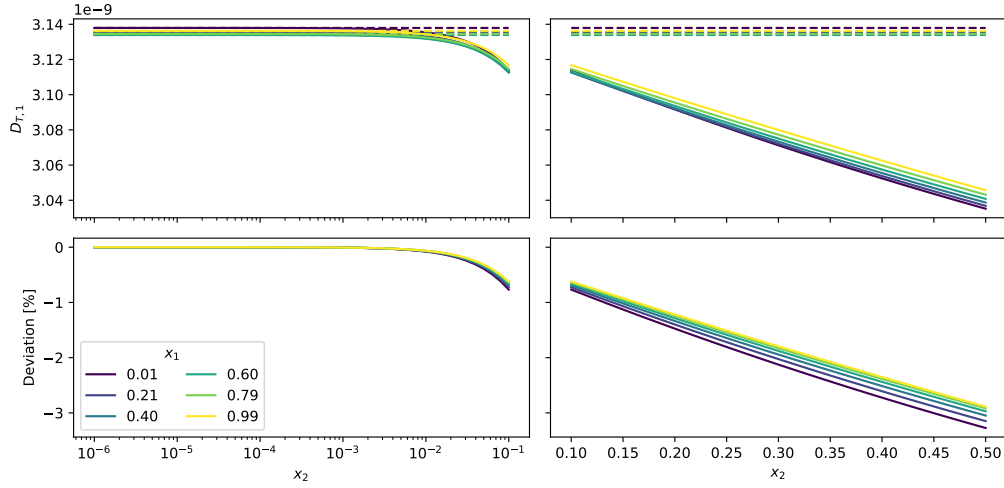


Figure 5: The same thermal diffusion coefficients as in Fig. 4, with deviations and for a larger composition span.

Similarly to the thermal diffusion coefficients, this definition carries the advantage that

$$\underline{\mathbf{X}}\mathbf{S}_T = -\frac{\nabla \mathbf{x}}{\nabla T} \iff \underline{\mathbf{W}}\mathbf{S}_T = -\frac{\nabla \mathbf{w}}{\nabla T}, \quad (32)$$

such that mole- and mass fractions can be used interchangeably with the same Soret coefficients.

In the state with vanishing mass fluxes ($\mathbf{J} = \mathbf{0}$). From the condition of vanishing mass fluxes, we find that we can compute the Soret coefficients asⁱ

$$\begin{aligned} \mathbf{J} &= -c \left(\underline{\mathbf{X}} \mathbf{D}_T^{(z)} \nabla T + \underline{\mathbf{X}} \underline{\mathbf{D}}^{(z)} \underline{\mathbf{X}}^{-1} \nabla \mathbf{x} \right) = \mathbf{0} \\ -\frac{\nabla \mathbf{x}}{\nabla T} &= \underline{\mathbf{X}} \left(\underline{\mathbf{D}}^{(z)} \right)^{-1} \mathbf{D}_T^{(z)} \\ \mathbf{S}_T &= \left(\underline{\mathbf{D}}^{(z)} \right)^{-1} \mathbf{D}_T^{(z)}. \end{aligned} \quad (33)$$

For a binary system (1, 2), this definition thus yields

$$S_{T,1}^{(b)} = \frac{D_{T,1}^{(z,b)}}{D_{11}^{(z,b)}}. \quad (34)$$

From the preceding relations it is possible to show that when using this definition of the Soret coefficient [2],

$$\begin{aligned} \lim_{x_1 \rightarrow 0} S_{T,2} &= S_{T,2}^{(b,3)} \\ \lim_{x_2 \rightarrow 0} S_{T,1} &= S_{T,1}^{(b,3)} \\ \lim_{x_3 \rightarrow 0} S_{T,1} - S_{T,2} &= S_{T,1}^{(b,2)}, \end{aligned} \quad (35)$$

where $S_{T,i}^{b,j}$ denotes the Soret coefficient of component i in a binary mixture with j , with species j being the dependent species. Figure 6 shows how this convergence behaviour is obeyed.

ⁱSee the memo on definitions of the diffusion coefficient for notes on $\underline{\mathbf{D}}^{(z)}$.

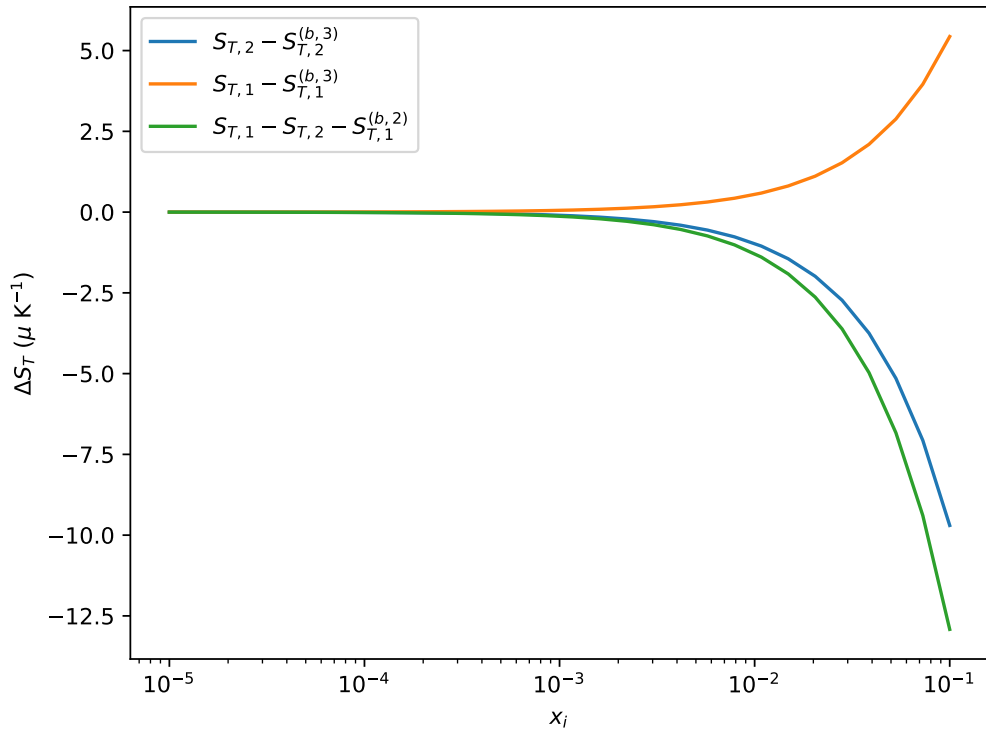


Figure 6: The convergence of the ternary Soret coefficient to the corresponding binaries as indicated in Eq. (35).

References

- [1] V. G. Jervell and O. Wilhelmsen, “Revised Enskog theory for Mie fluids: Prediction of diffusion coefficients, thermal diffusion coefficients, viscosities, and thermal conductivities,” *The Journal of Chemical Physics*, vol. 158, p. 224101, 06 2023.
- [2] J. M. Ortiz de Zárate, “Definition of frame-invariant thermodiffusion and soret coefficients for ternary mixtures,” *The European Physical Journal E*, vol. 42, no. 4, pp. 1–8, 2019.