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control systems. In [8], a three-area thermal system under deregulated environment is considered with GRC which is modeled as “open loop” method; a name that we use hereafter for one of two methods employed in papers for modeling of GRC. In [9], automatic generation control (AGC) of a multi-area hydrothermal system with GRC modeled in open loop method are investigated. In [5], a three-area reheat thermal units are examined taking into account GDB and GRC nonlinearities in which the GRC is modeled in open loop method. GRCs of both hydro and thermal units are modeled by the open loop method. In [10], GRCs of an interconnected hydrothermal system are simulated by the open loop model.

In [11], a nonlinear thermal turbine model with GRC is utilized which we name as the “closed loop” GRC model. In order to take effect of the GRC in the simulations, most of papers replace linear model of thermal turbine with a nonlinear closed loop model [2, 12, 13]. In [7], LFC of interconnected reheat thermal power system considering GDB and GRC nonlinearities is investigated in which the GRC is simulated by the closed loop model. The authors in [14], adopt an anti-GRC structure to overcome the negative effects of GRC on frequency stability where the GRC of the thermal unit is simulated by closed loop model. In [15], GRC is taken into theoretical consideration in the LFC design procedure. In doing so, nonlinear turbine model is used in which the closed loop model of GRC is applied in simulations to emulate the practical limit on the response of the turbine. In [16], GDB and GRC nonlinearities are taken into account simultaneously for a two-area reheat thermal units.

Above literature survey reveals that investigation on an appropriate GRC modeling method for LFC can be a major concern. In this paper, appropriate GRC modeling for reheat thermal plants of a two-area realistic interconnected power system is investigated by dynamic simulations. Proportional-integral-differential (PID) controller is adjusted by an improved particle swarm optimization (IPSO) algorithm in presence of the GDB and GRC physical constraints because ignoring these lead to nonrealistic results.

II. POWER SYSTEM STUDIES

A. Realistic interconnected power system

Fig. 1 shows the transfer function model of interconnected reheat thermal system including GDB and GRC constraints. The block descriptions of reheat thermal plants are shown on Fig. 1. The system parameters are given in TABLE I. The GRC of thermal units can be modeled in either closed loop or open loop method. Here, the value of GRC for reheat thermal units is considered as 10%/min, i.e.:

$$|\Delta \dot{P}_{th}| = 0.1 \left(\frac{pu}{min} \right) = 0.0017 \left(\frac{pu}{sec} \right) \quad (1)$$

Hence, The GRC for the units can be taken into account by adding two limiters, bounded by ± 0.0017 within the turbines in the closed loop or open loop method as shown in Fig. 2 to restrict the generation ramp rate for the thermal plants [6, 17].

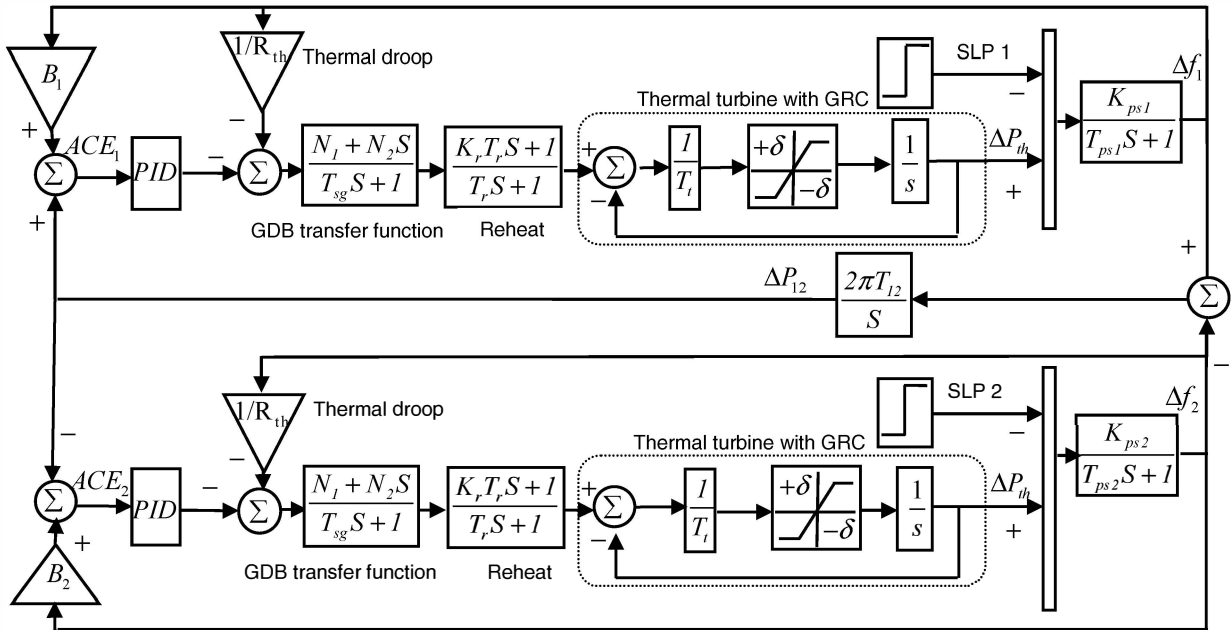


Fig. 1. Transfer function model of interconnected thermal power system considering GDB and GRC in closed loop model

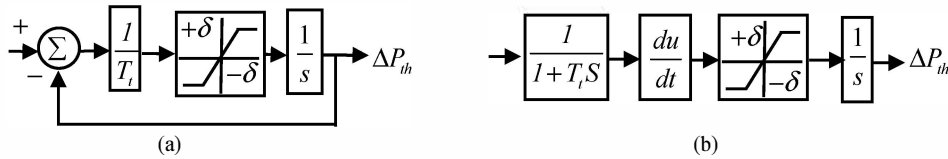


Fig. 2. GRC models: (a) Closed loop modeling (b) Open loop modeling

The GDB is defined as the total magnitude of a sustained speed change within which there is no change in valve position of the turbine. The GDB of the 0.06% backlash type can be linearized in terms of change and the rate of change in the speed. In this paper, following most recent paper [18], N_1 and N_2 in the GDB transfer function model are $N_1=0.8$ and $N_2=-0.2/\pi$, respectively. Droop of thermal units is set at 4%.

TABLE I. PARAMETERS OF THE INTERCONNECTED POWER SYSTEM

Parameter	Value	Description
f	50 Hz	System frequency
R_{th}	2	Speed regulation parameter (Hz/puMW)
T_{sg}	0.06 sec	Governor time constant of steam turbine
T_i	0.3 sec	Steam turbine time constant
K_r	0.3	Steam turbine reheat constant
T_r	10.2 sec	Steam turbine reheat time constant
T_{ps1}, T_{ps2}	11.49 sec	Power system time constants
K_{ps1}, K_{ps2}	68.9655	Power system gains (Hz/puMW)
T_{12}	0.0433	Synchronizing coefficient
B_1, B_2	0.4312	Frequency bias coefficients
$\pm\delta$	± 0.0005	Positive and negative ramp rates
$\Delta f_1, \Delta f_2$		Area frequency deviations
ΔP_{12}		Tie-line power deviation
$N_1=0.8, N_2=-0.2/\pi$		Fourier coefficients of GDB transfer function

B. Objective function for controller design

In order to damp effectively the oscillations, considering a suitable objective function is very important to find the controller parameters. In this work, the integral of time multiplied squared error (ITSE) performance index is considered as the objective function as following:

$$ITSE = \int_0^{T_{sim}} t [\Delta f_1^2 + \Delta f_2^2 + \Delta P_{12}^2] dt \quad (2)$$

where T_{sim} denotes the simulation time. The ITSE index uses advantages of both integral of squared error (ISE) and integral of time multiplied absolute error (ITAE) indices, as it utilizes squared error and time multiplication to weight large oscillations and penalize long settling time. The ITSE performance index has been employed recently in [18, 19] to design AGC of interconnected power systems. In order to design LFC, an optimization problem is solved by improved particle swarm optimization (IPSO) algorithm to minimize the ITSE index to obtain the optimal parameters of the PID controllers, subject to following constraints:

$$0 \leq K_{p1}, K_{I1}, K_{D1}, K_{p2}, K_{I2}, K_{D2} \leq 5 \quad (3)$$

C. Improved particle swarm optimization (IPSO) algorithm

Particle swarm optimization (PSO) is a member of wide category of swarm intelligence-based optimization algorithms. PSO is one of most well-known heuristic evolutionary algorithms that has found many applications in solving of engineering optimization problems. In the case of populations with large diversity, improved PSO (IPSO) algorithm recently introduced in [20], employs crossover operator so that the search space can be successfully surveyed. This helps in finding the global optimal solution more precisely. The IPSO is employed here to minimize the proposed objective functions due to its great effectiveness in optimizing of the parameters. To find optimal parameters of the PID controller, IPSO should explore in three-

dimensional search space. To start optimization process, initially some executions have been performed with different values of the IPSO parameters to assess if IPSO will find satisfactory results or not. The parameters of IPSO algorithm should be selected carefully to provide high performance. The parameters of our written MATLAB-based IPSO program are selected as: $n=30$; $m=3$; $\omega_{min}=0.4$; $\omega_{max}=0.9$; $c_1=c_2=2$; $\gamma=0.1$; $t_{max}=30$; CR=0.6, where n is the population size; m is total number of parameters to be optimized; $\omega_{max}, \omega_{min}$ are the initial and final inertia weights; c_1, c_2 are acceleration coefficients; γ is a chosen number in interval (0, 1) to control the maximum velocity vector; t_{max} is total number of the iterations; and CR is crossover rate.

III. SIMULATION RESULTS AND DISCUSSES

A. Simulation of reheat thermal power system considering open loop and closed loop models of GRC

In this case, the time domain simulations are realized for 0.01pu SLP in area 1 applying GRC in the open loop model. The proposed IPSO algorithm is repeated many times to solve the optimization problem. Some near optimal solutions for nominal system parameters obtained after numerous runs are shown in TABLE II. The solution with minimum value of the ITSE index is chosen as final optimized parameters of the controller which is highlighted in TABLE II. It is noteworthy to say that the running time of the IPSO algorithm with application of the open loop GRC model is very longer than the simulation time for the closed loop GRC model. The damping measures such as settling time (T_s) with 5% criterion, system oscillatory modes and damping ratios (ζ) corresponding to the open loop and closed loop models of the GRCs are presented in TABLE III. These damping indices are very important in evaluating the LFC dynamic performance. Fig. 3 shows the frequencies and tie-line power oscillation responses.

TABLE II. SOME NEAR OPTIMAL PID CONTROLLERS IN DIFFERENT GRC MODELING METHODS

	K_{P1}	K_{I1}	K_{D1}	K_{P2}	K_{I2}	K_{D2}	ITSE
Open loop	3.5517	2.1053	2.6671	1.5975	1.0933	0.2780	0.0936
	4.2658	0.9839	2.0164	5.0000	2.8834	2.0512	0.0947
	4.4303	0.6949	0.0925	1.7326	2.1834	2.1972	0.0789
	2.4579	0.7529	0.9707	2.7274	2.1482	0.9876	0.0832
Closed loop	0.1146	0.0766	2.8878	2.0251	0.1745	2.2962	0.0734
	0.0902	0.0618	3.0861	2.7809	0.1062	2.5285	0.0763
	0.0837	0.0691	2.0957	1.1408	0.2644	0.9304	0.0795
	0.5334	0.0563	3.3569	1.9686	0.3821	1.4893	0.1212

TABLE III. SYSTEM DAMPING CHARACTERISTICS WITH OPEN LOOP AND CLOSED LOOP MODELS OF GRC

	oscillatory mode	ζ	Signal	T_s
Open loop			Δf_1	>50
	-0.0435 ± 1.8063i	0.0241	Δf_2	>50
			ΔP_{12}	>50
Closed loop	-0.2418 ± 2.5228i	0.0954	Δf_1	27.7025
	-1.0492 ± 1.2064i	0.6562	Δf_2	29.8534
	-0.0728 ± 0.0422i	0.8654	ΔP_{12}	30.9709

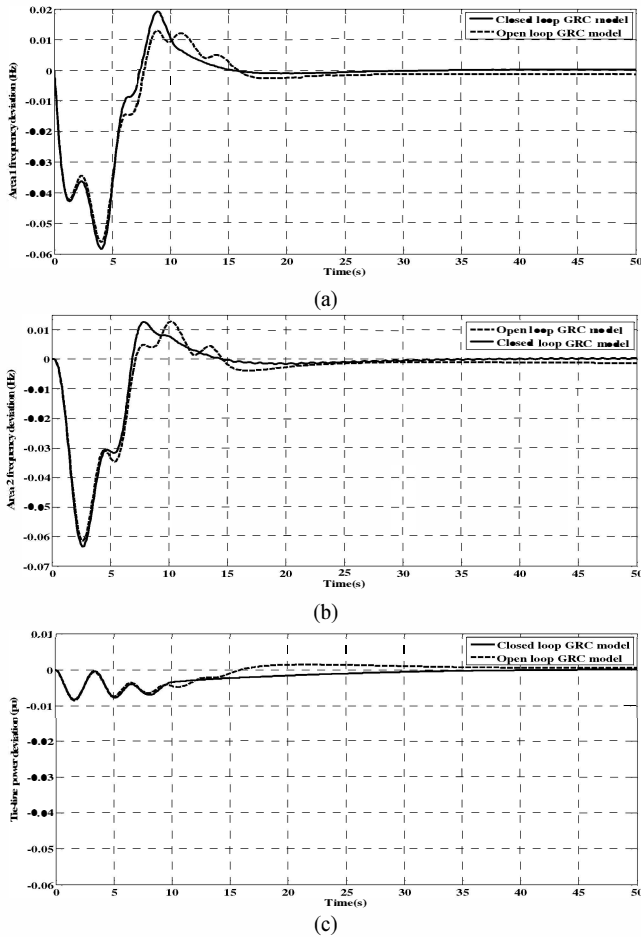


Fig. 3. Dynamic responses: (a) Δf_1 , (b) Δf_2 , and (c) ΔP_{12}

It is clear from TABLE III that the T_s in closed loop model is significantly smaller than that of obtained from the open loop modeling method. Also, the minimum damping ratios of the system with closed loop GRC is very larger than the open loop counterpart. It can be seen from Fig. 3 that with the open loop GRC model, the area frequencies and the tie-line power deviations regulate to zero with difficulty. As it is obvious, even with the optimized PIDs, the oscillations persist for a long time and a small steady state error remains considering the open loop GRC model. I. e., the LFC system can no longer suppress the oscillations to drive back them to zero, effectively. With application of the closed loop GRC model, the area frequencies and tie-line power oscillations are damped to zero fully.

B. Robustness analysis against uncertainties in system loading condition and parameters

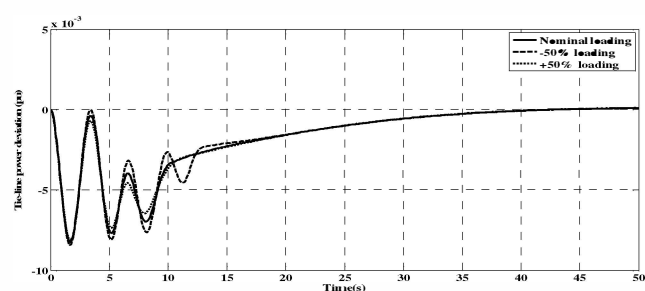
The sensitivity analysis is carried out to investigate the robustness of the GRC models to wide variations in the system loading condition and parameters. The loading condition, steam turbine time constant T_b , and the synchronizing torque T_{12} are varied in the range of $\pm 50\%$ from nominal values, individually. The simulation results with these conditions for 0.01pu SLP in area 1 are summarized in TABLE IV. It can be observed that even with consideration of $\pm 50\%$ uncertainty in loading

condition, T_b or T_{12} , the ITSE index and minimum damping ratios of the system with closed loop GRC model are better than the other. Increase (or decrease) of ITSE index can be interpreted as decrease (or increase) of system damping performance. The damping ratios with closed loop GRC are larger than with the open loop GRC. Also, the T_s of the area frequencies and tie-line power responses with closed loop GRC model are smaller than open loop model, considerably.

TABLE IV. ROBUST ANALYSIS OF GRC MODELS AGAINST VARIOUS UNCERTAINTY SCENARIOS

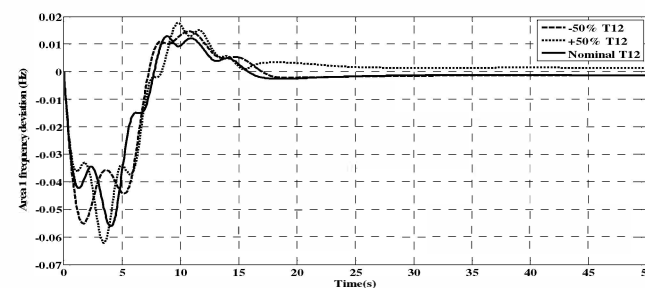
% change	GRC model	oscillatory Modes	ζ	ITSE	signal	T_s
+50% in loading	open loop	$-0.0652 \pm 1.8057i$	0.0361	0.0573	Δf_1	>50
					Δf_2	>50
	Closed loop	$-0.2725 \pm 2.5347i$	0.1069		Δf_1	28.5075
		$-1.0704 \pm 1.2459i$	0.6516	0.0564	Δf_2	29.9483
-50% in loading	Open loop	$-0.0217 \pm 1.8067i$	0.0120	0.1243	ΔP_{12}	30.6714
					Δf_1	>50
	Closed loop	$-0.2113 \pm 2.5111i$	0.0838		Δf_2	>50
		$-1.0265 \pm 1.1640i$	0.6614	0.1150	Δf_1	27.3392
+50% in T_1	open loop	$-0.0435 \pm 1.8063i$	0.0241	0.0789	Δf_2	29.4890
					ΔP_{12}	30.9290
	Closed loop	$-0.0730 \pm 0.0421i$	0.8664		Δf_1	>50
					Δf_2	>50
-50% in T_1	open loop	$-0.0774 \pm 2.3969i$	0.0323		Δf_1	>50
		$-0.7345 \pm 1.1700i$	0.5317	0.0743	Δf_2	>50
	Closed loop	$-0.0728 \pm 0.0427i$	0.8625		ΔP_{12}	26.9940
					Δf_1	29.9638
+50% in T_{12}	open loop	$-0.0435 \pm 1.8063i$	0.0241	0.0789	Δf_2	31.0314
					ΔP_{12}	>50
	Closed loop	$-0.6367 \pm 2.5181i$	0.2451		Δf_1	>50
		$-1.8126 \pm 1.0041i$	0.8748	0.0741	Δf_2	28.4601
-50% in T_{12}	open loop	$-0.0729 \pm 0.0416i$	0.8682		Δf_1	31.8648
					Δf_2	31.0902
	Closed loop	$-0.0435 \pm 2.2125i$	0.0197	0.1015	ΔP_{12}	>50
		$-0.0870 \pm 2.8701i$	0.0303		Δf_1	>50
+50% in T_{12}	open loop	$-1.1412 \pm 1.2119i$	0.6856	0.1058	Δf_2	28.9176
		$-0.0738 \pm 0.0424i$	0.8667		Δf_1	30.1953
	Closed loop	$-0.0435 \pm 1.2769i$	0.0340	0.0976	ΔP_{12}	29.2244
		$-0.5698 \pm 2.1238i$	0.2591		Δf_1	>50
-50% in T_{12}	open loop	$-0.8101 \pm 1.1409i$	0.5789	0.0726	Δf_2	27.1840
		$-0.0703 \pm 0.0413i$	0.8622		Δf_1	32.9511
	Closed loop				ΔP_{12}	32.9511
					Δf_2	>50

The dynamic responses considering aforementioned uncertainties are depicted in Figs. 4 - 6. One can infer from these figures that there is insignificant impact of the changes in the system loading condition and parameters on the obtained results with closed loop GRC, in that, the frequencies and tie-line power oscillations are suppressed as well. Moreover, by employing closed loop GRC model, the steady state error can be eliminated effectively. One important point is that as we know from the linear control theory, the negative-feedback closed loop system usually tends to increase the system stability rather than the open loop. Moreover, since the derivative operator is sensitive to discontinuity, the sudden changes in loads or system parameters of direct path (in open loop GRC model) can degrade the system performance significantly. Our robustness analysis reveals that the closed loop GRC model is quite robust. Hence, the parameters of optimal PID controllers once set for nominal condition need not to be reset for $\pm 50\%$ variations in the system parameters and loading condition from their nominal values.

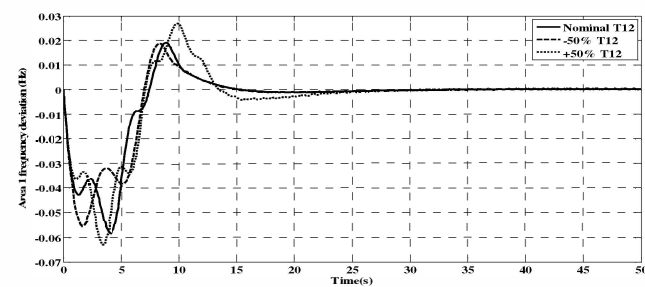


(b2) ΔP_{12} with closed loop GRC model

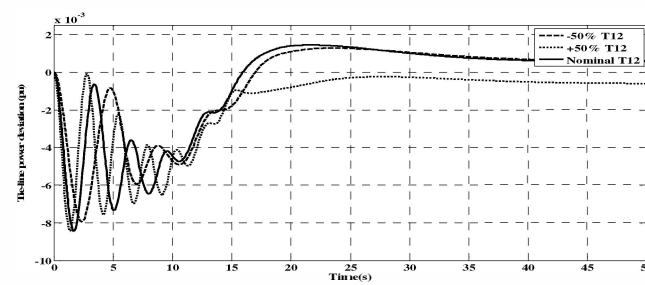
Fig. 4. Robustness analysis against uncertainty in loading condition



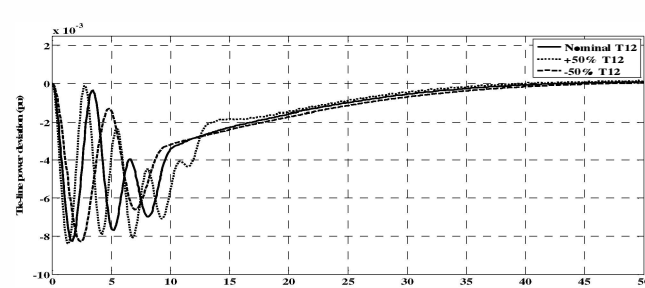
(a1) Δf_1 with open loop GRC model



(a2) Δf_1 with closed loop GRC model

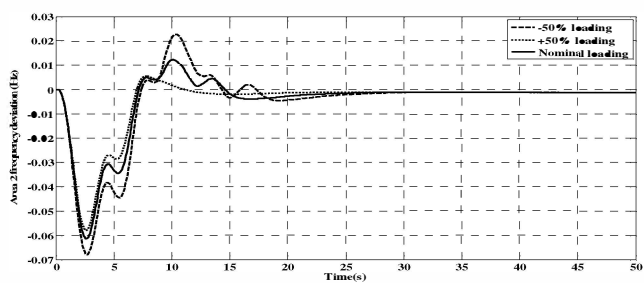


(b1) ΔP_{12} with open loop GRC model

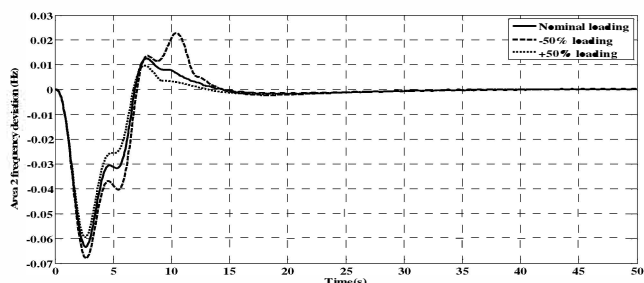


(b2) ΔP_{12} with closed loop GRC model

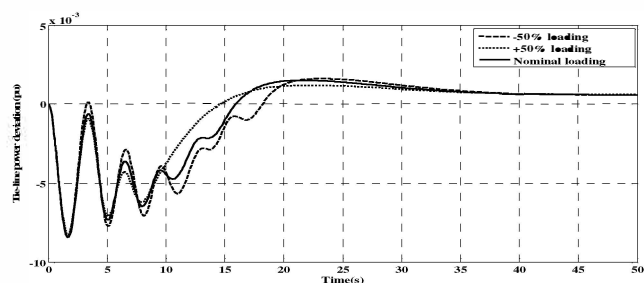
Fig. 5. Robustness analysis against uncertainty in T_{12}



(a1) Δf_2 with open loop GRC model



(a2) Δf_2 with closed loop GRC model



(b1) ΔP_{12} with open loop GRC model

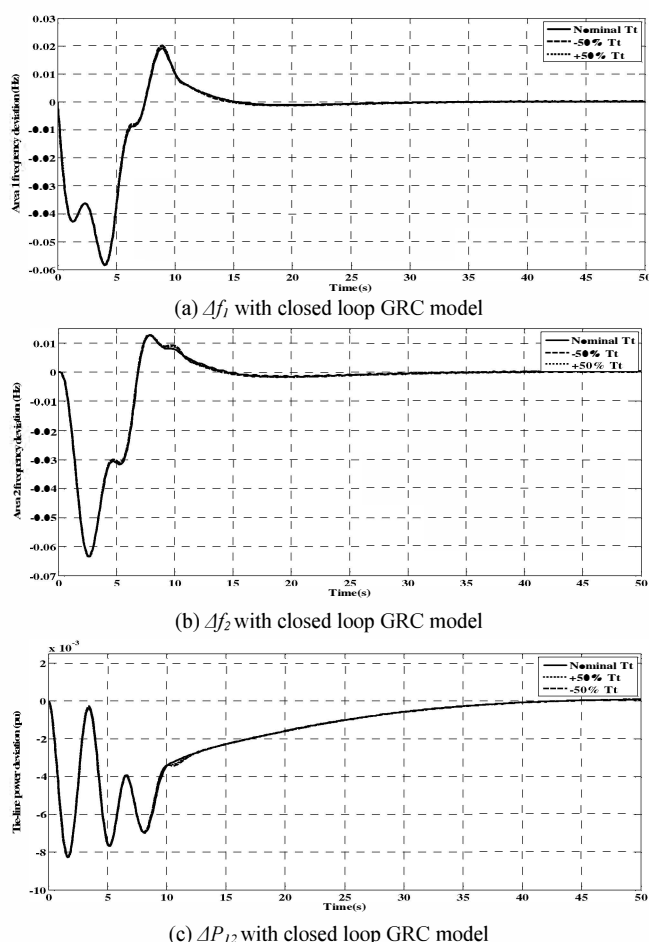


Fig. 6. Robustness analysis against uncertainty in T_l

IV. CONCLUSION

In this paper an effort has been made to choose the appropriate SIMULINK model of GRC in reheat thermal units using dynamic simulations to obtain optimal LFC. The dynamic performance of the interconnected thermal power system considering GRC and GDB nonlinearities has been evaluated by applying the open loop and closed loop models of the GRC, individually. The effectiveness of both models in damping of the area frequencies and tie-line power oscillations has been examined. The eigenvalue analysis and time domain dynamic simulation results show that with the closed loop model of GRC, greater dynamic performance can be attained. Also, the robustness of the power system equipped with the different GRC models has been investigated by sensitivity analyses considering uncertainty scenarios in system loading condition and parameters. These analyses exhibit that the optimized PID controllers are quite robust and performs satisfactorily under uncertainty conditions when the closed loop GRC model is applied. Hence, clearly this paper suggests the closed loop model of GRC for dynamic simulations of reheat thermal units in LFC studies.

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