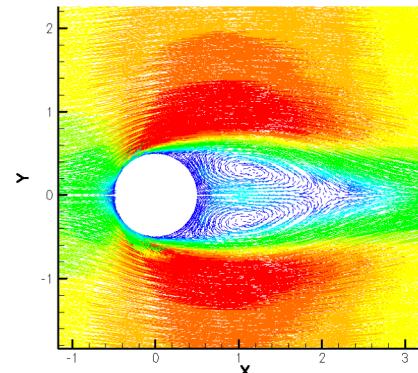
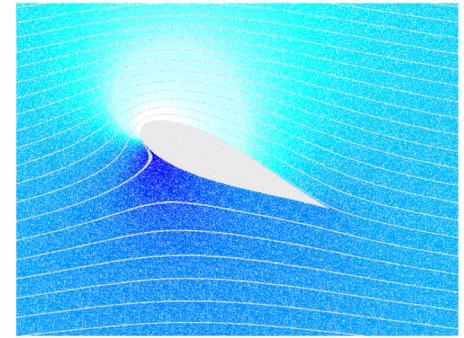


# Lecture X: Fluid Physics

# Fluid Motion

- Describes object with no fixed topology
  - Air flow
  - Viscous fluids
  - Smoke, etc.
- Key descriptor: **flow velocity**
$$\vec{u} = u(x, t)$$
- Describing the velocity of a “fluid parcel” passing at position  $x$  in time  $t$ .
- Eulerian description
  - How come?



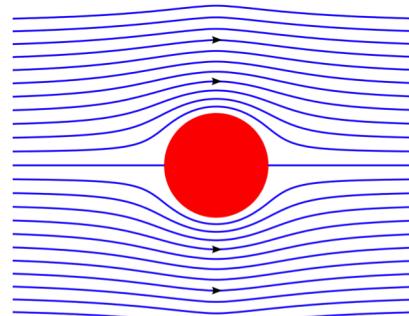
<http://cfd.solvcon.net/old/research/cylinder2.gif>

# Flow Velocity

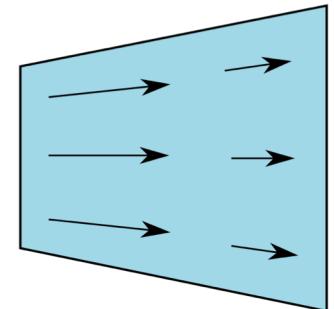
- Vector field describing motion
- Steady field:  $\frac{\partial u}{\partial t} = 0$
- Incompressible:  $\nabla \cdot u = 0$ .
- Irrotational (no vortices):  $\nabla \times u = 0$



Turbulent with a vortex



Incompressible,  
irrotational flow



Steady field

# Incompressibility Assumption

- No fluid is incompressible
  - Otherwise, no soundwaves!
- Fluid is a non-solid “rigid body”.
- Explicit condition:

$$\iint_{\partial\Omega} \vec{u} \cdot \hat{n} = 0$$

- For every (sub) domain  $\Omega$  with boundary  $\partial\Omega$ .
- “volume in = volume out”.

# Incompressibility

- The divergence theorem:

$$\iint_{\partial\Omega} \vec{u} \cdot \hat{n} = \iiint_{\Omega} \nabla \cdot \vec{u} = 0$$

- Since  $\Omega$  is arbitrary, we have:

$$\nabla \cdot \vec{u} = 0$$

**everywhere** as our condition for incompressibility!

# (Incompressible) Navier-Stokes Equations

- Representing the **conservation of mass** and momentum for an **incompressible** fluid ( $\nabla \cdot \vec{u} = 0$ ):

$$\frac{D\vec{u}}{Dt} = \rho(\vec{u}_t + \vec{u} \cdot \nabla \vec{u}) = \underbrace{\nu \nabla \cdot (\nabla \vec{u})}_{\text{Viscosity}} - \underbrace{\nabla p}_{\text{Pressure gradient}} + \underbrace{\vec{f}}_{\text{External body forces}}$$

*Material Derivative*      *Divergence of stress*

*Unsteady acceleration*      *Convective acceleration*

*Viscosity*      *Pressure gradient*      *External body forces*

- $p$ : pressure field
- $\nu$ : kinematic viscosity.
- $f$ : body force per density (usually just gravity  $\rho g$ ).

# Material Derivative

- A particle with mass  $m$  has velocity  $\vec{u}$ .

- Newton's 2<sup>nd</sup> law:

$$m \frac{D\vec{u}}{Dt} = \vec{F}$$

- What are the forces acting on the particle?
- Simplest component: **gravity**  $\vec{F}_g = m\vec{g}$ .

# Pressure

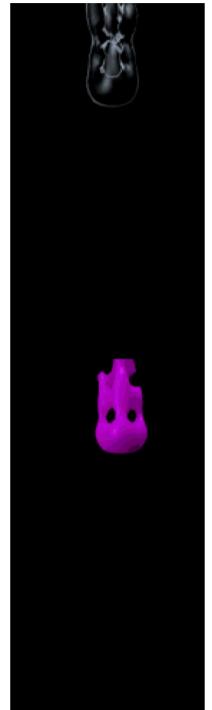
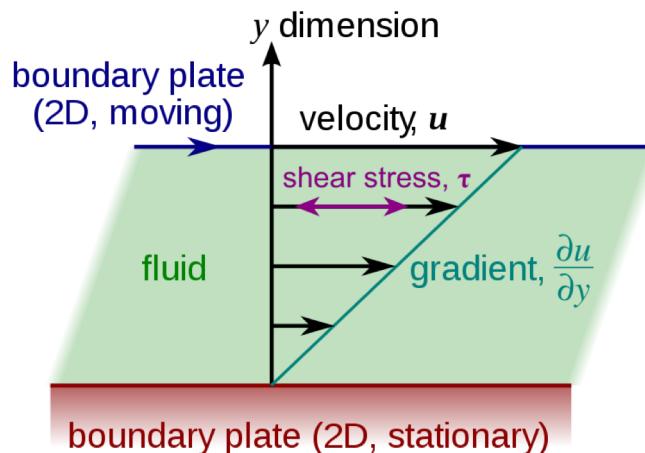
- The particle receives **pressure** from all directions in a fluid.
- What causes pressure? Incompressibility!
  - Pressure balances flow that creates compression.
- Algebraically:
  - $\nabla \cdot \vec{u} = 0$  is a constraint
  - Pressure is the **Lagrange multiplier**  $\lambda$ !
- Suppose particle volume  $V$ .
- Integrated (scalar!) pressures over particle :  $p$ .
- Net force enacted by pressure:  $\vec{F}_{pre} = -V\nabla p$ .

# Viscosity

- Resistance to deformation by **shear stress**.
- Expressed by coefficient  $\nu$ :

$$\frac{F}{A} = \nu \frac{\partial u}{\partial y}$$

- Higher  $\nu$ : **more pressure** required for shearing!
  - Viscid fluids.



# Viscosity

- Another interpretation: how much the flow of a particle different from the flow of its neighbors.
- Laplacian:  $\nu \nabla \cdot (\nabla \vec{u}) = \nu \Delta \vec{u}$ .
  - $\nu$ : dynamic viscosity.
- $\nu$  is defined per volume unit, so to get force:
- $\vec{F}_{vis} = V \cdot [\nu \nabla \cdot (\nabla \vec{u})]$
- What is the Laplacian of a vector?
  - For each coordinate independently.

# Putting it All Together

- The **Navier-Stokes equation** in particle form:

$$m \frac{D\vec{u}}{Dt} = \vec{F}_{vis} + \vec{F}_{pre} + \vec{F}_{ext} = V\nu\nabla \cdot (\nabla\vec{u}) - V\nabla p + m\vec{g}$$

- In the limit (infinitesimal particles):  $\frac{m}{V} \rightarrow \rho$ .
- dividing by  $V$  we get:

$$\rho \frac{D\vec{u}}{Dt} = \nu\nabla \cdot (\nabla\vec{u}) - \nabla p + \rho\vec{g}$$

- What is the **material derivative**  $\frac{D\vec{u}}{Dt}$ ?

# Material Derivative

- The connecting thread between **Lagrangian** and **Eulerian** approaches.
- Reminder:
  - Lagrangian: tracking elements as they move (particles, mesh vertices).
  - Eulerian: tracking movement in a fixed point in space (temperature on grid, amount of material in a cell).
- **Lagrangian description:**
  - Suppose a set of particles, each with quantity  $q$ .
  - The particle is moving with velocity  $\vec{u}(t) = \frac{d\vec{x}(t)}{dt}$
- **Eulerian description:**
  - $q(t, \vec{x})$ : the quantity of the particle that passes through **fixed point**  $\vec{x}$  at time  $t$ .
- How to tie both narratives?

# Material Derivative

- Material (or total) derivative:

$$\frac{Dq}{Dt} = \frac{d}{dt} q(t, \vec{x}(t))$$

- How much  $q$  changes for the moving particle.

$$\frac{\partial}{\partial t} q(t, \vec{x})$$

- How much  $q$  changes at a fixed point  $\vec{x}$ .

# Material Derivative

- The **chain rule**:

$$\frac{Dq}{Dt} = \frac{d}{dt} q(t, \vec{x}(t)) = \frac{\partial q}{\partial t} + \nabla q \cdot \frac{d\vec{x}}{dt} = \frac{\partial q}{\partial t} + \nabla q \cdot \vec{u}$$

- $\frac{\partial q}{\partial t}$ : How much  $q$  changes at the **fixed point**  $\vec{x}$ .
- $\nabla q \cdot \vec{u}$ : how much of the change is due to **advection** (transfer of material).
  - Also: convection, transport.
- When  $q$  doesn't change for a particle, we get the advection equation:

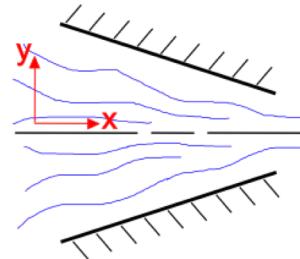
$$\frac{\partial q}{\partial t} + \nabla q \cdot \vec{u} = 0$$

# Material Derivative

- The change in the velocity of the fluid parcel passing at position  $x$  in time  $t$ .

$$\frac{D\vec{u}}{dt} = \vec{u}_t + \vec{u} \cdot \nabla \vec{u}$$

- $\vec{u}_t$ : unsteady acceleration.
  - How much velocity changes in fixed  $x$  over time.
- $\vec{u} \cdot \nabla \vec{u}$ : **convective** acceleration.
  - How much velocity changes due to **movement along trajectory**.



# Inviscid Flow

- We often drop viscosity altogether.
- Getting the Euler equations:

$$m \frac{D\vec{u}}{Dt} = \vec{F}_{pre} + \vec{F}_{ext} = -V\nabla p + m\vec{g}$$

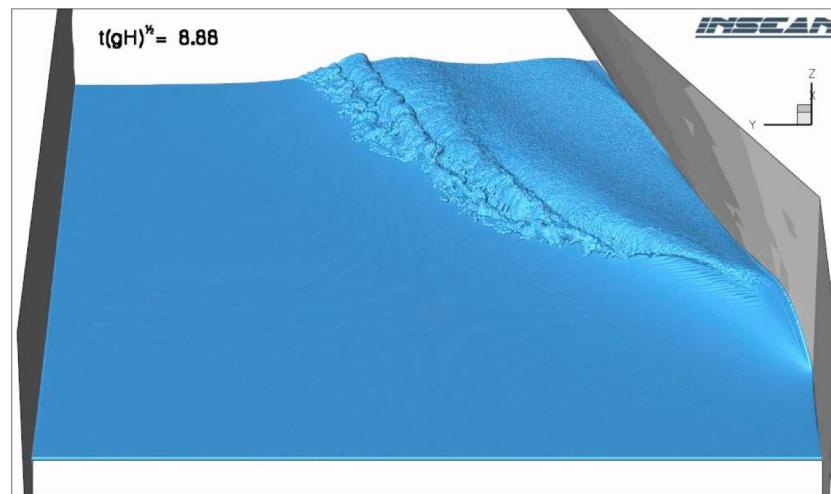
- “numerical dissipation”: errors that mimic physical viscosity enough for the visual effect.
  - Numerical dissipation often  $\gg$  true physical viscosity!

# Boundary Conditions

- Solid walls: no velocity through:

$$\vec{u} \cdot \hat{n} = 0$$

- What about pressure?
- For viscous fluid, there is also tangential “stick”.
  - “no-slip” conditions:  $\vec{u} = 0$



<https://i.ytimg.com/vi/7tAoJ4RarAw/maxresdefault.jpg>

# Water Surface

- Actually a meeting between two fluids (water and air).
- We can assume  $p_{AIR} = 0$
- **Model:** water tries to minimize surface area.



[https://abm-website-assets.s3.amazonaws.com/laboratoryequipment.com/s3fs-public/legacyimages/061813\\_loW.jpg](https://abm-website-assets.s3.amazonaws.com/laboratoryequipment.com/s3fs-public/legacyimages/061813_loW.jpg)

# Water Surface

- Pressure jump:  $[p] = \gamma\kappa$
- $\gamma$ : surface tension coefficient
- $\kappa$ : surface mean curvature.
- Mean curvature: measure of area gradient.

$$2\kappa\hat{n} = \lim_{A \rightarrow 0} \frac{\nabla A}{A}$$