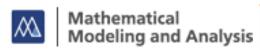


ENTWICKLUNG UND ANWENDUNG EINER METHODE ZUR DIREKTEN NUMERISCHEN SIMULATION REAKTIVER TRANSPORTPROZESSE IN BLASENSYSTEMEN

Dennis Hillenbrand, Holger Marschall







STRUCTURE SPP 1740

	complexity	SuperFocusMixer Coordination: S. Schindler	Taylor Flow coordination: G. Rinke	Bubble Swarms Coordination: H. Marschall	Bubbly Flows coordination: U. Hampel
A	Experiments coordination: M. Schlüter	M. Schlüter G. Rinke/W. Simon	U. Hampel G. Rinke/W. Simon M. Schlüter	M. Kraume M. Schlüter G. Rinke/W. Simon	C. Brücker U. Hampel C. Kähler J. Thöming
В	Simulation and modeling coordination: D. Bothe	S. Turek	D. Bothe H. Marschall S. Turek	D. Bothe H. Marschall	R. Rzehak M. Hlawitschka
С	Chemistry reaction networks coordination: S. Herres-Pawlis	S. Herres-Pawlis P. Klüfers G. Rinke/W. Simon S. Schindler	G. Rinke/W. Simon S. Schindler S. Herres-Pawlis D. Ziegenbalg	S. Schindler S. Herres-Pawlis	P. Klüfers
D	Transfer to selective reactions in bubbly flows coordination: U. Nieken			M. Hlawitschka	M. Hlawitschka U. Nieken U. Tuttlies K. Zähringer



SCIENTIFIC RELEVANCE



Contents lists available at ScienceDirect

Chemical Engineering Research and Design



journal homepage: www.elsevier.com/locate/cherd

Review Article

Review on hydrodynamics and mass transfer in minichannel wall reactors with gas-liquid Taylor flow



Stefan Haase a,b,*, Dmitry Yu. Murzinb, Tapio Salmib

Dedicated to Prof. Dr.-Ing. habil. Rüdiger Lange on the occasion of his 65th birthday.

"The reviewed literature identifies no clear window of operating conditions and hydrodynamic parameters at which Taylor flow offers the highest mass transfer"

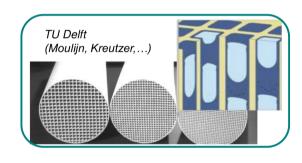
^a Faculty of Mechanical Science and Engineering, Chair of Chemical Reaction Engineering and Process Plant, Technische Universität Dresden, D-01062 Dresden, Germany

^b Faculty of Science and Engineering, Laboratory of Industrial Chemistry and Reaction Engineering, Åbo Akademi University, Biskopsgatan 8, FI-20500 Turku (Åbo), Finland



INDUSTRIAL RELEVANCE

- Used for microfluidic applications
- High mass and heat transfer rates
- High mixing rates within liquid slugs
- Controllable flow characteristics





NUMERICAL CHALLENGES

• Bubble deformation



NUMERICAL CHALLENGES

- Bubble deformation
- Resolution of very thin film region
- Resolution of species boundary layer
- Resolution of wake structures

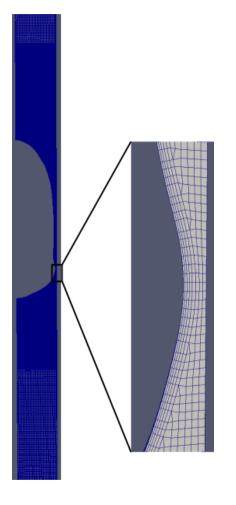




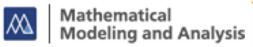
NUMERICAL CHALLENGES

- Bubble deformation
- Resolution of very thin film region
- Resolution of species boundary layer
- Resolution of wake structures

Results in very fine meshes with many cells!



Mesh resolution for Taylor bubble



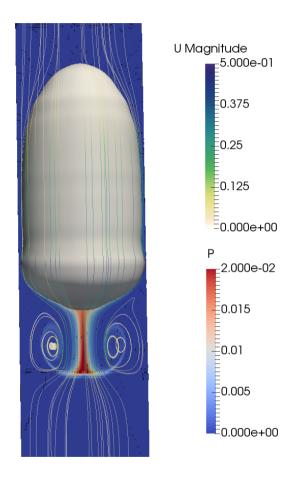




Experiments and simulations show rotational symmetric hydrodynamics for Re < 200 Highly resolved simulations possible for quasi-2D domains



Experiments and simulations show rotational symmetric hydrodynamics for Re < 200 Highly resolved simulations possible for quasi-2D domains

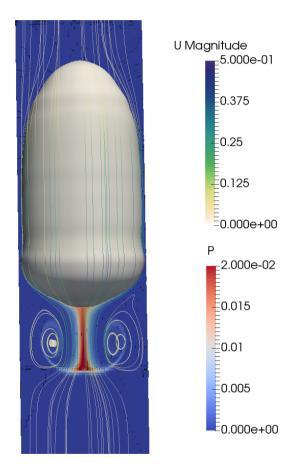


3D study of mass transfer around Taylor bubble



Experiments and simulations show rotational symmetric hydrodynamics for Re < 200 Highly resolved simulations possible for quasi-2D domains

BUT: Rotational symmetry not accessible in interface tracking simulations!

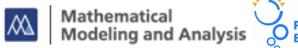


3D study of mass transfer around Taylor bubble



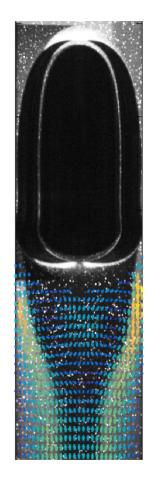
THREE GOALS FOR TAYLOR BUBBLES

- 1. VALIDATION AGAINST EXPERIMENTS
- 2. INVESTIGATION OF LOCAL SELECTIVITY
 - 3. MASS TRANSFER CORRELATIONS





1. EXPERIMENTAL VALIDATION



Experimental results, TUHH



bubble shape



rise velocity and flow patterns



Numerical simulation

2. LOCAL SELECTIVITY

Competitive consecutive schemes

$$A+B \xrightarrow{k_1} P$$

$$A + P \xrightarrow{k_2} S$$

Realistic and important parameter ranges for reaction ratios $\kappa = \frac{k_2}{k_1}$

2. LOCAL SELECTIVITY

Competitive consecutive schemes

$$A+B \xrightarrow{k_1} P$$

$$A + P \xrightarrow{k_2} S$$

Realistic and important parameter ranges for reaction ratios $\kappa = \frac{k_2}{k_1}$

Important parameter: local selectivity

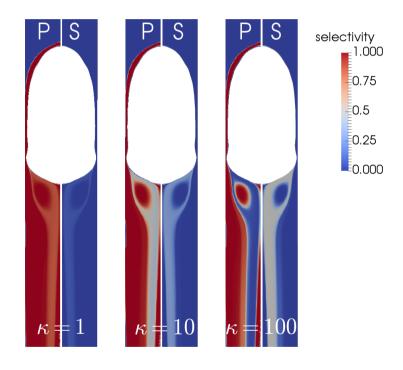
$$Sel_{P,A} = \frac{r_1-r_2}{r_1+r_2} = \frac{c_B-\kappa c_P}{c_B+\kappa c_P}$$
 Dennis Hillenbrand | SPP 1740 annual meeting Hamburg, 28.09.2019 | MMA, TO Darmstadt



2. LOCAL SELECTIVITY

Influence of wake structure on local selectivity

Side product mainly produced along vortex structure
Product selectivity reduced along vortex structures



Selectivity for $Da_1 = 1$



3. MASS TRANSFER CORRELATIONS

• Correlations available in literature for physisorption

3. MASS TRANSFER CORRELATIONS

- Correlations available in literature for physisorption
 - Mainly for smaller channels $d \leq 2mm$
 - Mainly applicable in a short range of characteristic parameters
 - Taylor flow can reduce mass transfer due to saturation in the film between bubble and wall

3. MASS TRANSFER CORRELATIONS

- Correlations available in literature for physisorption
 - Mainly for smaller channels $d \leq 2mm$
 - Mainly applicable in a short range of characteristic parameters
 - Taylor flow can reduce mass transfer due to saturation in the film between bubble and wall
- No correlation for enhancement by reaction in bulk phase found

NEXT STEPS

- Validate hydrodynamics against experimental results (TUHH)
- Estimate parameter range with simplified setup
- Two-phase simulations with
 - highly resolved meshes
 - maschine learning SGS model
- Gain insight into local selectivity fields
- Obtain mass transfer correlations including reactions



THANK YOU FOR YOUR ATTENTION!

REMAINING QUESTIONS?