Model Predictive Control of a Sewer System

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Group 1030

Jacob Naundrup Pedersen Thomas Holm Pilgaard

Department of Electronic Systems Aalborg University Denmark





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Circup 100

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Lineariseri

Resultat

Diskussion/Konklusion

Implementering

Kontrol

Linearisering MPC

Resultat

Diskussion/Konklusion



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Implementering

Kontrol Linearisering

Resultat

Diskussion/Konklus

- ► Implementation
- ► Kontrol
- ► Resultater
- ▶ Diskussion
- ► Konklusion



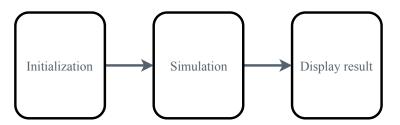
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Kontrol Linearisering

Resultat

Diskussion/Konklusion





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Implementering

Kontro

Lineariseri

Resultat

Diskussion/Konklusion

1. Pipe

- Længde [m]
- Sektioner
- ► S_b (Hældning) [‰]
- ▶ ∆x = Længde/Sektioner [m]
- ▶ Diameter [m]
- ► Theta
- ▶ Q_f[m³/s]
- ► Side inflow
- ► Placering i data

2. Tank

- ► Størrelse [m³]
- ► Højde [m]
- ► Areal = Size / Height [m²]
- ► Maximum outflow [m³/s]
- Placering i data



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Resultat

Diskussion/Konklusi

► Rør specifikationer

Fields	length	⊞ sections	⊞ Dx	⊞ Sb	⊞ d	H Theta	■ Qf		data_location
1	700	35	20	0.0030	0.9000	0.6500	0.9730	0	1
2	303	15	20.2000	0.0030	0.9000	0.6500	0.9730	0	3
3	27	2	13.5000	0.0030	1	0.6500	1.2843	1	4
4	155	8	19.3750	0.0041	1	0.6500	1.5014	0	5
5	295	14	21.0714	0.0122	0.8000	0.6500	1.4386	0	6
6	318	15	21.2000	0.0053	0.9000	0.6500	1.2932	1	8



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Implementering

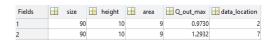
Kontrol

Linearisering MPC

Resultat

Diekussien/Kenklusie

▶ Tank specifikationer





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Resultat

Diskussion/Konklusio

► System specifikationer

Fields	type type	component	sections
1	'Pipe'	1	35
2	'Tank'	1	1
3	'Pipe'	4	39
4	'Tank'	1	1
5	'Pipe'	14	206
6	'Total'	21	282



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Implementering

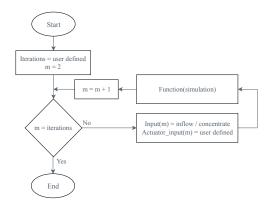
Lineariseri

Lineariserin MPC

Resulta

Diskussion/Konklusio

► Itererer igennem rør og tank for hvert tidsskridt





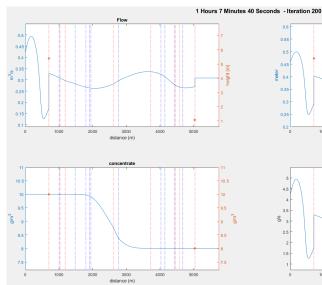
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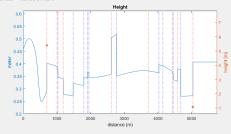
Implementering

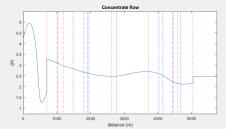
Kontrol Lineariseri

Resultat

Diskussion/Konklusion







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Implementer

Kontro

Linearisering

Resulta

Diskussion/Konklusio

- ► Linearisering af ulineær model
- ► Opstilles på state space form

$$\frac{\partial A(x,t)}{\partial t} + \frac{\partial Q(x,t)}{\partial x} = 0$$

$$\frac{\partial A(h)}{\partial h} \frac{\partial h(x,t)}{\partial t} + \frac{\partial Q(h)}{\partial h} \frac{\partial h(x,t)}{\partial x} = 0$$



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Kontrol

Linearisering

Result

Diskussion/Konklusio

► Priessmann scheme

► Opsat på matrix og vektor form

$$\left[\underbrace{\frac{1}{2\Delta t}\frac{\partial A}{\partial h} - \frac{\theta}{\Delta x}\frac{\partial Q}{\partial h}}_{a} \underbrace{\frac{1}{2\Delta t}\frac{\partial A}{\partial h} + \frac{\theta}{\Delta x}\frac{\partial Q}{\partial h}}_{b}\right] \begin{bmatrix} h_{j+1}^{i+1} \\ h_{j+1}^{i+1} \end{bmatrix} =$$

$$- \left[\underbrace{\frac{-1}{2\Delta t}\frac{\partial A}{\partial h} - \frac{(1-\theta)}{\Delta x}\frac{\partial Q}{\partial h}}_{c} \underbrace{\frac{-1}{2\Delta t}\frac{\partial A}{\partial h} + \frac{(1-\theta)}{\Delta x}\frac{\partial Q}{\partial h}}_{d} \right] \begin{bmatrix} h_{j+1}^{i} \\ h_{j+1}^{i} \end{bmatrix} =$$



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Kontrol

Linearisering

Resultat

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 $\begin{bmatrix}
1 & 0 & 0 & \cdots & 0 \\
0 & b_1 & 0 & \cdots & 0 \\
0 & a_1 & b_2 & \ddots & \vdots \\
\vdots & \vdots & \ddots & \ddots & 0 \\
0 & 0 & 0 & a_{m-1} & b_m
\end{bmatrix}$

x(k+1)

$$= \underbrace{\begin{bmatrix} 0 & 0 & 0 & \cdots & 0 \\ c_0 & d_1 & 0 & \cdots & 0 \\ 0 & c_1 & d_2 & \cdots & 0 \\ \vdots & \vdots & \ddots & \ddots & \vdots \\ 0 & 0 & 0 & c_{m-1} & d_m \end{bmatrix}}_{A} \underbrace{\begin{bmatrix} h_0^i \\ h_1^i \\ h_2^i \\ \vdots \\ h_m^i \end{bmatrix}}_{x(k)} +$$

$$\begin{bmatrix}
1 \\
-a_0 \\
0 \\
\vdots \\
0
\end{bmatrix}
h_0^{i+1} + \begin{bmatrix}
\frac{dh}{dQ} \\
0 \\
0 \\
\vdots \\
0
\end{bmatrix}
d_0^{i+1}$$

$$\vdots$$

$$\vdots$$

$$\vdots$$

$$\vdots$$

$$\vdots$$

$$\vdots$$

$$\vdots$$



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Linearisering

MPC

Resultat

Diskussion/Konklusio

- ► e Forøgelse af højde i tank(inflow)
- ► f Reducering af højde i tank(Outflow)
- g Inflow i efterfølgende rør

$$\begin{bmatrix} b_{1,2} & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & 0 \\ 0 & 0 & a_{2,1} & b_{2,2} \end{bmatrix} \underbrace{\begin{bmatrix} h_{1,2}^{l+1} \\ h_{tank}^{l+1} \\ h_{2,0}^{l+1} \\ h_{2,1}^{l+1} \end{bmatrix}}_{\chi(k+1)}$$

$$= \underbrace{\begin{bmatrix} d_{1,2} & 0 & 0 & 0 \\ e & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 \\ 0 & 0 & c_{2,0} & d_{2,1} \end{bmatrix}}_{A} \underbrace{\begin{bmatrix} h_{1,2}^{l} \\ h_{2,0}^{l} \\ h_{2,0}^{l} \\ h_{2,1}^{l} \end{bmatrix}}_{\chi(k)} + \underbrace{\begin{bmatrix} 0 & 0 \\ 0 & -f \\ 0 & g \\ 0 & 0 \end{bmatrix}}_{B} \begin{bmatrix} h_{0}^{l+1} \\ u_{tank} \end{bmatrix}$$



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MPC

Resultat

Distance in a fixed blood

- ► Samligning af ulineær og linear model
- ► System setup
- ► Sinus input

Туре	Components	Sections
Pipe	1	35
Tank	1	1
Pipe	18	227
Total	20	263





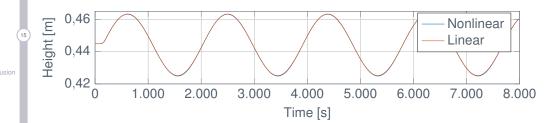
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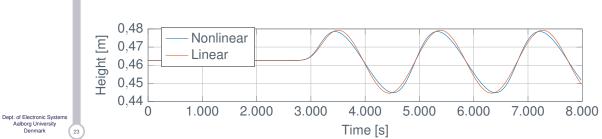
Implemente

Linearisering

Resultat

Diskuss







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Kontrol

Lineariserin MPC

Resultat

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- ► Cost function
 - ► Afgrænset til at minimiere output variationer
- ▶ Constraints
 - ► Højde
 - ► Kontrol input
- ► Prediction model



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Kontrol

MPC

- Bestemmelse af Prediction horizon
 - Flow profiler
 - ► Industri
- ► Begrænsning af Prediction horizon
- System setup
- ► Forstyrrelses input

Fields	type type	⊞ component	⊞ sections
1	'Pipe'	1	5
2	'Tank'	1	1
3	'Pipe'	1	5
4	'Total'	3	11





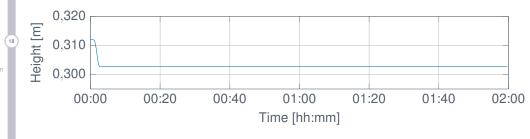
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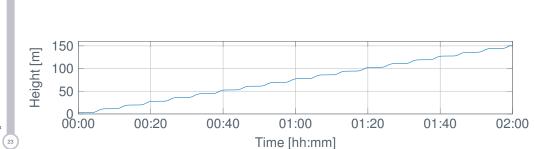
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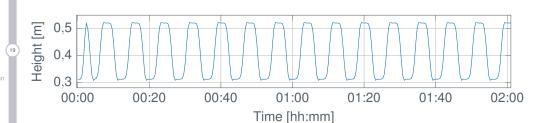
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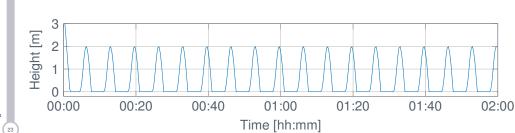
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Diskussion/Konklusio





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Diskussion/Konklusion

 System setup, efterligning af Fredericia

► Flow profiler

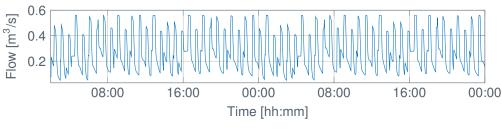
Type	Component	Sections
Pipe	1	35
Tank	1	1
Pipe	17	207
Tank	1	1
Pipe	1	38
Total	21	282

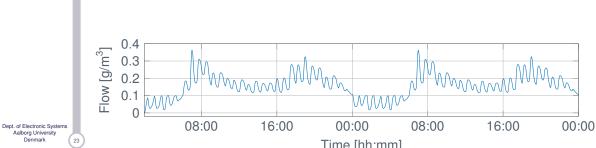




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Linearisering MPC

Resultat

Diskussion/Konklusion (22)

- ▶ Courant's tal
- ► Model reduction



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Diskussion/Konklusion 23

► Simulering

► MPC