

Model Predictive Control of a Sewer System

June 14, 2018

Group 1030

Jacob Naundrup Pedersen

Thomas Holm Pilgaard

Department of Electronic Systems

Aalborg University

Denmark



AALBORG UNIVERSITY
DENMARK



Agenda

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

Introduction

Implementation

Control

Results

Discussion

Conclusion



Introduction

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

2

► slide 1 hello world



Overview

Jacob Naundrup Pedersen

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

3

- ▶ Implementation
- ▶ Control
- ▶ Results
- ▶ Discussion
- ▶ Conclusion

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

4

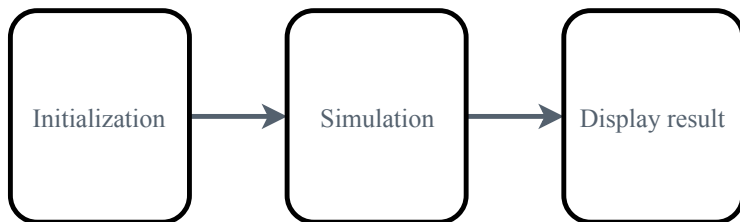


Figure: Chosen structure of simulation environment.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

5

1. Pipe

- ▶ Length [m]
- ▶ Sections (Number of sections the pipe should be split in to)
- ▶ S_b (Slope) [‰]
- ▶ $\Delta x = \text{Length} / \text{Sections}$ [m]
- ▶ Diameter [meter]
- ▶ Theta (parameter used in Preissmann scheme)
- ▶ $Q_f [\text{m}^3/\text{s}]$
- ▶ Side/lateral inflow present
- ▶ Section location in data

2. Tank

- ▶ Size [m^3]
- ▶ Height [m]
- ▶ Area = Size / Height [m^2]
- ▶ Maximum outflow [m^3/s]
- ▶ Section location in data

Table: List of parameters for pipe and tank.

Agenda

Group 1030

6

Introduction

Implementation

Control

Results

Discussion

Conclusion

Fields	length	sections	Dx	Sb	d	Theta	Qf	side_inflow	data_location
1	700	35	20	0.0030	0.9000	0.6500	0.9730	0	1
2	303	15	20.2000	0.0030	0.9000	0.6500	0.9730	0	3
3	27	2	13.5000	0.0030	1	0.6500	1.2843	1	4
4	155	8	19.3750	0.0041	1	0.6500	1.5014	0	5
5	295	14	21.0714	0.0122	0.8000	0.6500	1.4386	0	6
6	318	15	21.2000	0.0053	0.9000	0.6500	1.2932	1	7
7	110	5	22	0.0036	0.9000	0.6500	1.0658	1	8
8	38	2	19	0.0024	1	0.6500	1.1487	1	9
9	665	30	22.1667	0.0030	1	0.6500	1.2843	1	10
10	155	7	22.1429	8.0000e-04	1	0.6500	0.6632	0	11
11	955	47	20.3191	0.0029	1.2000	0.6500	2.0415	1	12
12	304	15	20.2667	0.0030	1.2000	0.6500	2.0764	0	13
13	116	5	23.2000	0.0021	1.2000	0.6500	1.7373	1	14
14	283	12	23.5833	0.0017	1.4000	0.6500	2.3463	1	15
15	31	2	15.5000	0.0019	1.4000	0.6500	2.4805	1	16
16	125	6	20.8333	0.0021	1.6000	0.6500	3.7075	0	17
17	94	4	23.5000	0.0013	1.5000	0.6500	2.4609	0	18
18	360	18	20	0.0046	1.6000	0.6500	5.4872	1	19
19	736	38	19.3684	0.0012	1.6000	0.6500	2.8026	0	20

Figure: Setup in MATLAB of pipe specification of the main line in Fredericia.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

7

Field ▲	Value
size	90
height	10
area	9
Q_out_max	0.9730
data_location	2

Figure: Setup in MATLAB of tank specifications.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

8




Fields	 type	 component	 sections
1	'Pipe'	1	35
2	'Tank'	1	1
3	'Pipe'	18	245
4	'Total'	20	281

Figure: Display of structure showing system setup information in MATLAB.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

9

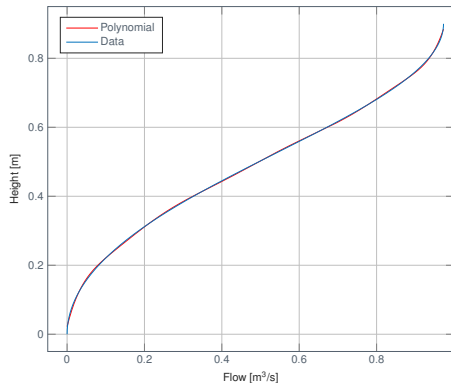


Figure: Comparison between data obtained by equation ?? and the same data curve fitted to a ninth order polynomial.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

10

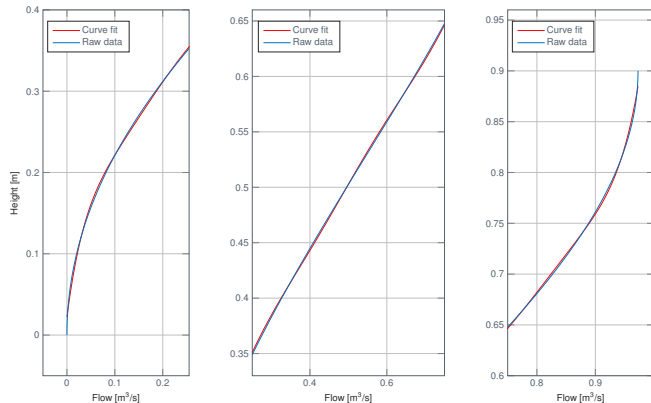


Figure: Comparison between data obtained by equation ?? and the same data curve fitted to a ninth order polynomial.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

11

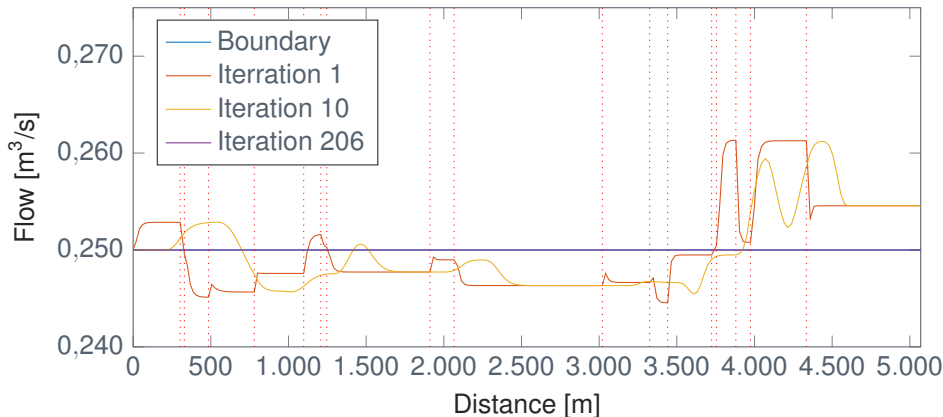


Figure: Height and flow of pipe setup from part of Fredericia where boundary conditions is found by fitted polynomial. Various amount of iterations, with constant flow input of $0,25 \text{ m}^3/\text{s}$, is performed. The dotted line indicates pipe intersections.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

12

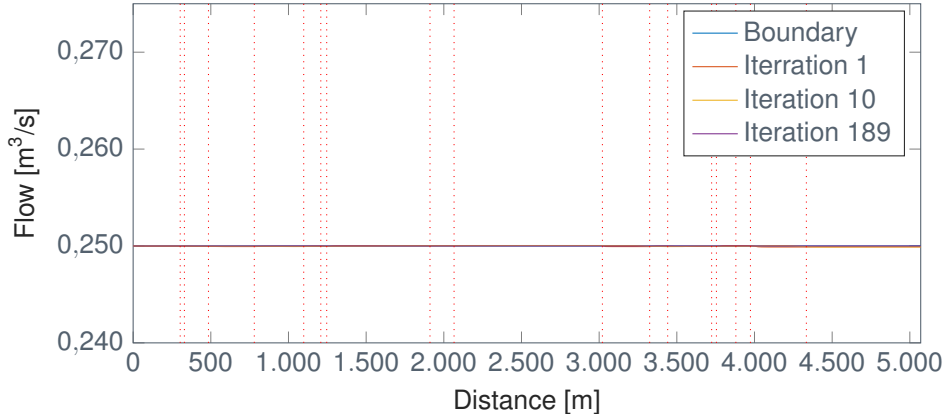


Figure: Height and flow of pipe setup from part of Fredericia where boundary conditions is found by lookup table. Various amount of iterations, with constant flow input of $0,25 \text{ m}^3/\text{s}$, is performed. The dotted line indicates pipe intersections.



Implementation

Simulation

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

13

► Preissmann scheme

30

Implementation Display

Agenda

Group 1030

Introduction

Implementation

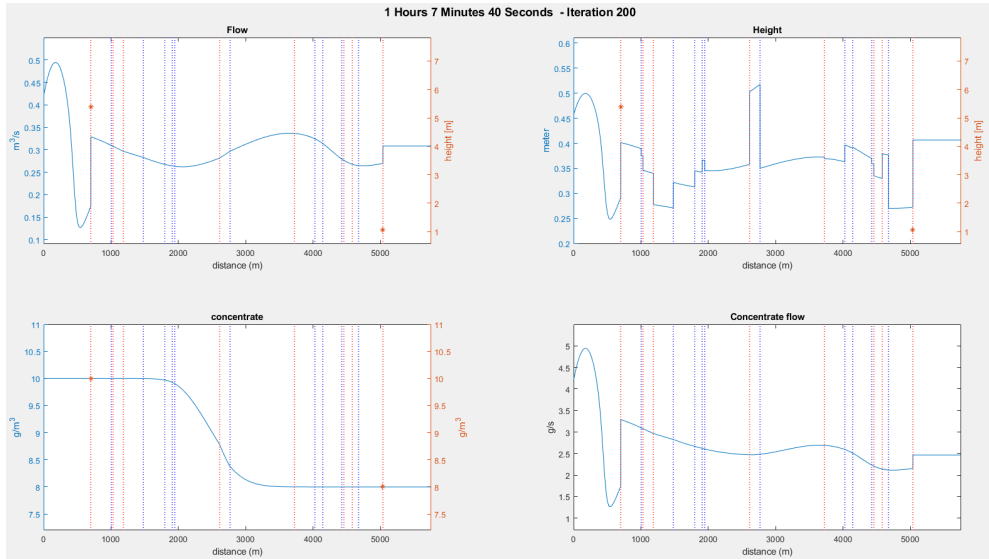
Control

Results

Discussion

Conclusion

14



Figure



Control

Linearization

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

15

30



Control

Linearization

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

16

30



Control

Linearization

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

17

- ▶ Sinus
- ▶ Flow profiles

30

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

18

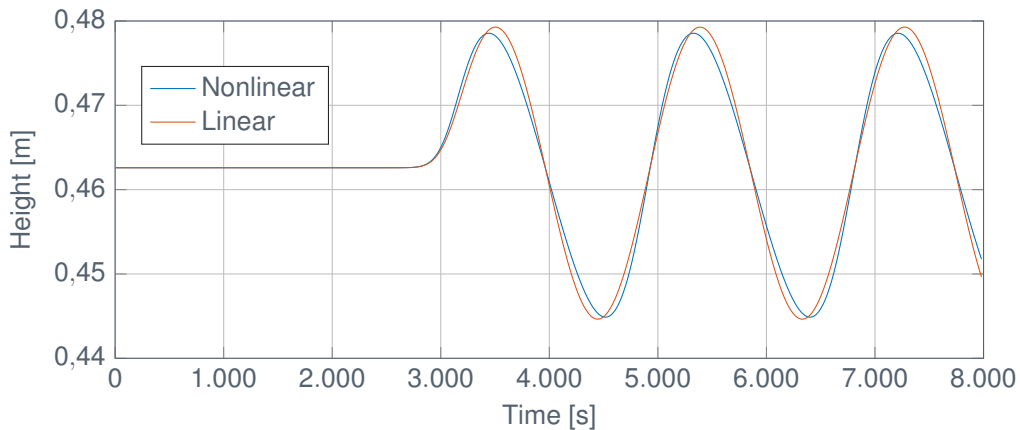


Figure: Comparison of the nonlinear and linear model at the last pipe in the setup.



Control MPC

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

19

- ▶ Cost function
- ▶ Constraints
- ▶ Linear model

30

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

20

- ▶ Bestemmelse af Prediction horizon
 - ▶ Flow profiler
 - ▶ Industri
- ▶ Begrænsning af Prediction horizon

30

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

21

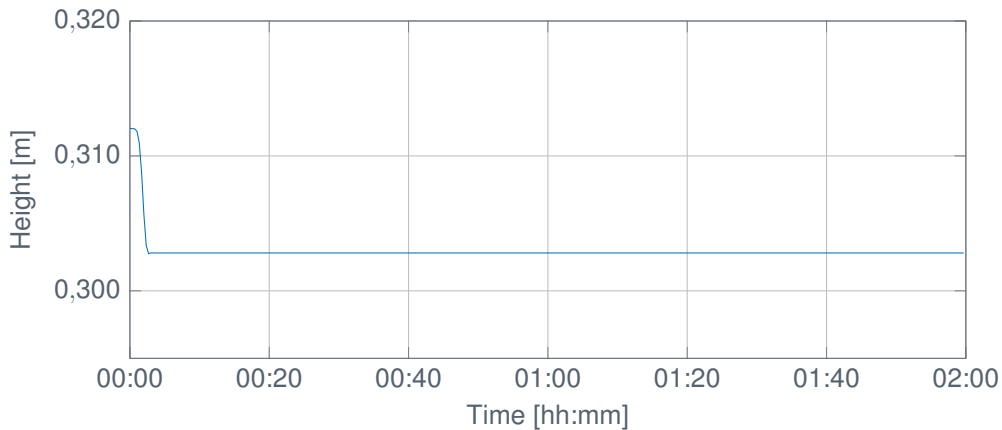


Figure: Output of the last pipe.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

22

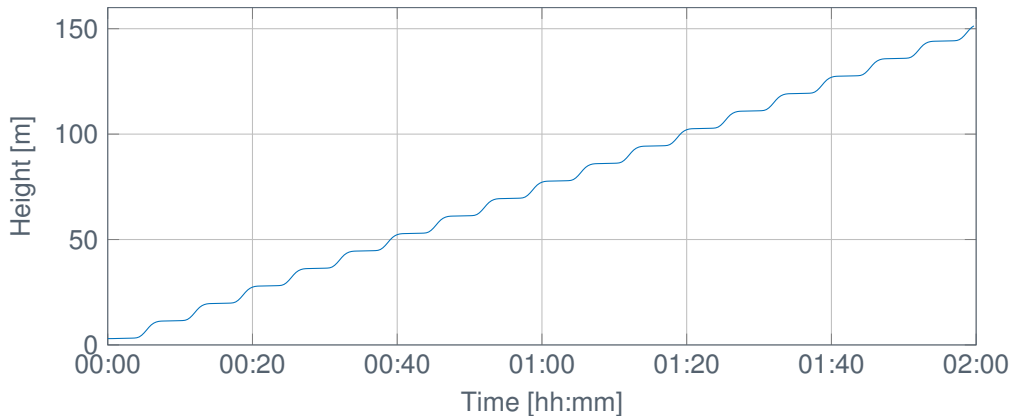


Figure: Height in the tank.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

23

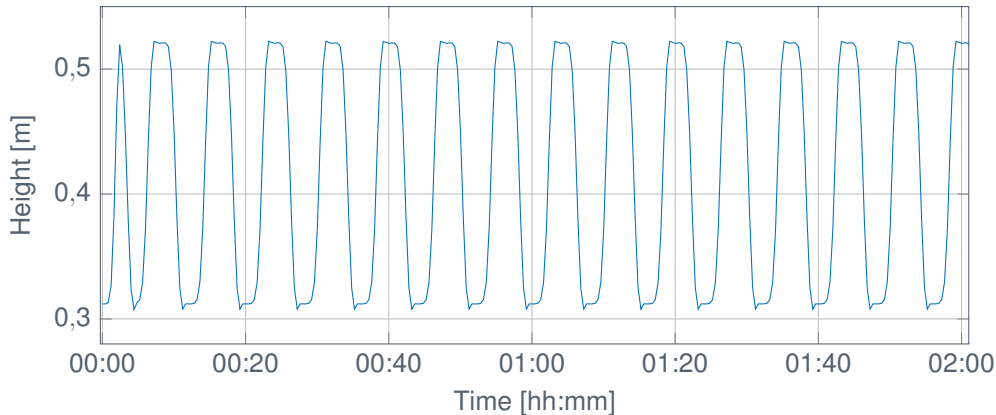


Figure: Output of the last pipe in the second simulation run.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

24

- System setup
- Flow profiles

Type	Component	Sections
Pipe	1	35
Tank	1	1
Pipe	17	207
Tank	1	1
Pipe	1	38
Total	21	282

Table: System setup.

30

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

25

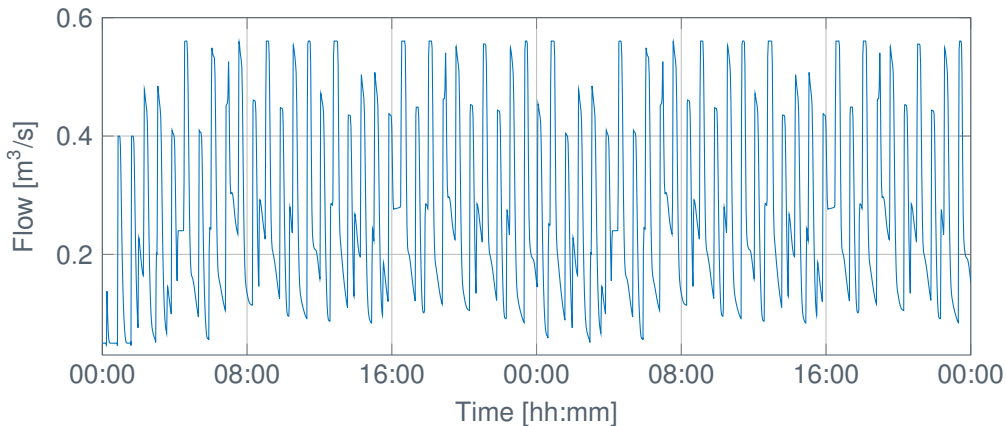


Figure: Output of the last pipe into the WWTP.

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

26

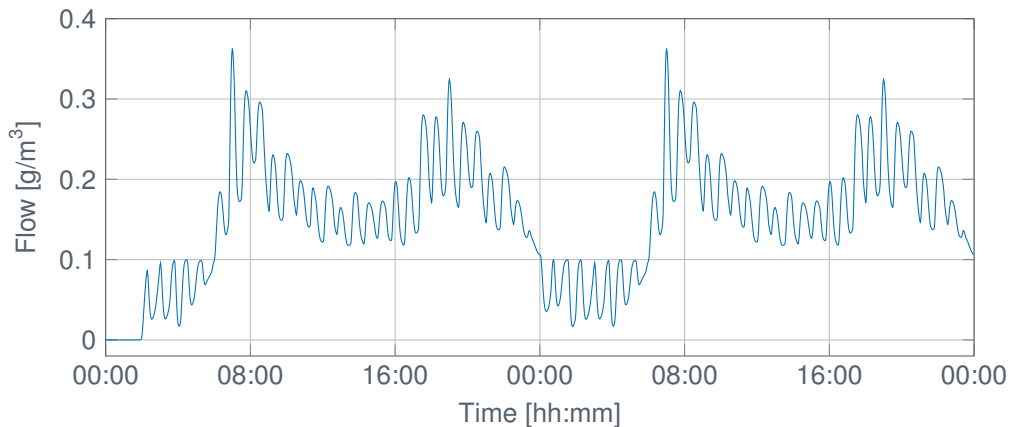


Figure: Simulation of COD output of the last pipe into the WWTP.



Results

Second test

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

27

- ▶ Over dimensioneret tank
- ▶ Konstant output af tank

30

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

28

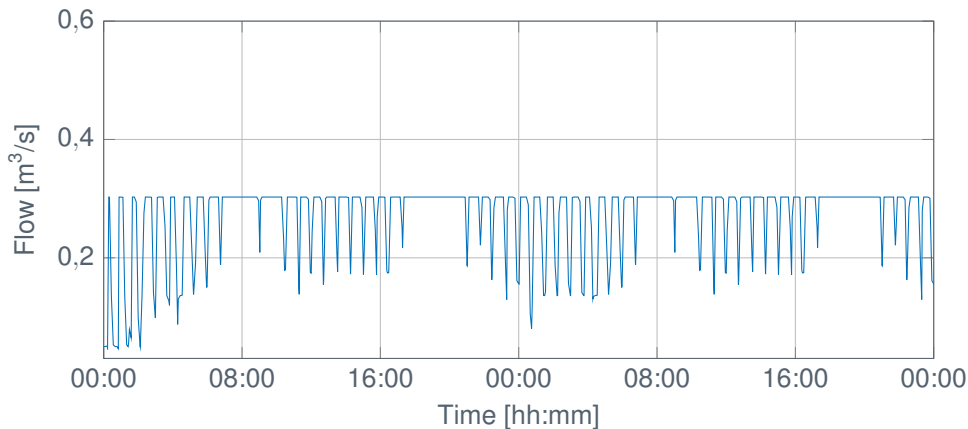


Figure: Output of the last pipe in to the WWTP, where a tank has been placed in front to reduce variation in flow into WWTP.

30



Discussion

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

- ▶ Courant's number
- ▶ Model reduction

29

30



Conclusion

Agenda

Group 1030

Introduction

Implementation

Control

Results

Discussion

Conclusion

- ▶ Simulation
- ▶ MPC

30

30