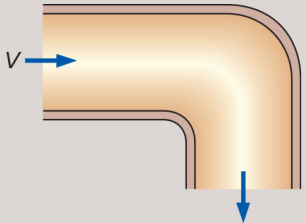
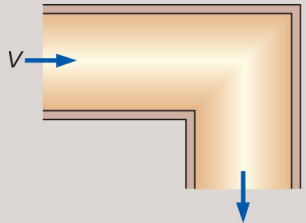
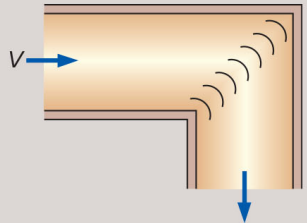
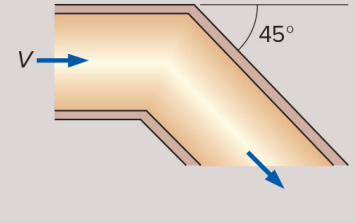


FIGURE A-27

The Moody chart for the friction factor for fully developed flow in circular pipes for use in the head loss relation $\Delta P_L = f \frac{L}{D} \frac{\rho V^2}{2}$. Friction factors in the turbulent flow are evaluated from the Colebrook equation $\frac{1}{\sqrt{f}} = -2 \log_{10} \left(\frac{\epsilon/D}{3.7} + \frac{2.51}{Re\sqrt{f}} \right)$.

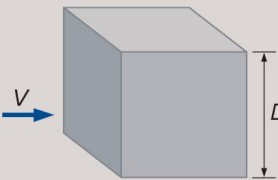
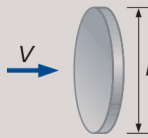
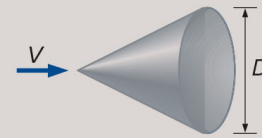
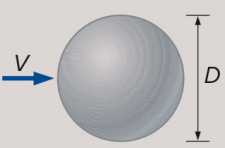
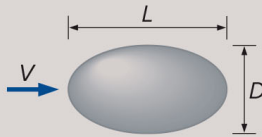
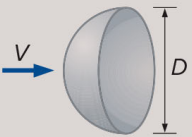
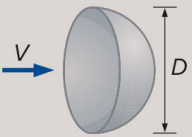
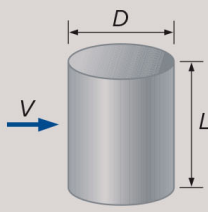
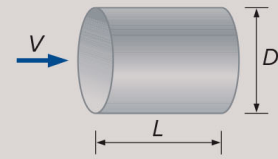
TABLE 14-4 (CONCLUDED)

<p><i>Bends and Branches</i> 90° smooth bend: Flanged: $K_L = 0.3$ Threaded: $K_L = 0.9$</p> 	<p>90° miter bend (without vanes): $K_L = 1.1$</p> 	<p>90° miter bend (with vanes): $K_L = 0.2$</p> 	<p>45° threaded elbow: $K_L = 0.4$</p> 
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TABLE 15-2

Representative drag coefficients C_D for various three-dimensional bodies based on the frontal area for $Re > 10^4$ unless stated otherwise (for use in the drag force relation $F_D = C_D A \rho V^2 / 2$ where V is the upstream velocity)

<p>Cube, $A = D^2$</p>  <p>$C_D = 1.05$</p>	<p>Thin circular disk, $A = \pi D^2/4$</p>  <p>$C_D = 1.1$</p>	<p>Cone (for $\theta = 30^\circ$), $A = \pi D^2/4$</p>  <p>$C_D = 0.5$</p>																										
<p>Sphere, $A = \pi D^2/4$</p>  <p>Laminar: $Re \lesssim 2 \times 10^5$ $C_D = 0.5$ Turbulent: $Re \gtrsim 2 \times 10^6$ $C_D = 0.2$</p> <p>See Fig. 11–36 for C_D vs. Re for smooth and rough spheres.</p>	<p>Ellipsoid, $A = \pi D^2/4$</p>  <table><tr><th rowspan="2">L/D</th><th colspan="2">C_D</th></tr><tr><th>Laminar $Re \lesssim 2 \times 10^5$</th><th>Turbulent $Re \gtrsim 2 \times 10^6$</th></tr><tr><td>0.75</td><td>0.5</td><td>0.2</td></tr><tr><td>1</td><td>0.5</td><td>0.2</td></tr><tr><td>2</td><td>0.3</td><td>0.1</td></tr><tr><td>4</td><td>0.3</td><td>0.1</td></tr><tr><td>8</td><td>0.2</td><td>0.1</td></tr></table>		L/D	C_D		Laminar $Re \lesssim 2 \times 10^5$	Turbulent $Re \gtrsim 2 \times 10^6$	0.75	0.5	0.2	1	0.5	0.2	2	0.3	0.1	4	0.3	0.1	8	0.2	0.1						
L/D	C_D																											
	Laminar $Re \lesssim 2 \times 10^5$	Turbulent $Re \gtrsim 2 \times 10^6$																										
0.75	0.5	0.2																										
1	0.5	0.2																										
2	0.3	0.1																										
4	0.3	0.1																										
8	0.2	0.1																										
<p>Hemisphere, $A = \pi D^2/4$</p>  <p>$C_D = 0.4$</p>  <p>$C_D = 1.2$</p>	<p>Finite cylinder, vertical, $A = LD$</p>  <table><tr><th>L/D</th><th>C_D</th></tr><tr><td>1</td><td>0.6</td></tr><tr><td>2</td><td>0.7</td></tr><tr><td>5</td><td>0.8</td></tr><tr><td>10</td><td>0.9</td></tr><tr><td>40</td><td>1.0</td></tr><tr><td>∞</td><td>1.2</td></tr></table> <p>Values are for laminar flow ($Re \lesssim 2 \times 10^5$)</p>	L/D	C_D	1	0.6	2	0.7	5	0.8	10	0.9	40	1.0	∞	1.2	<p>Finite cylinder, horizontal, $A = \pi D^2/4$</p>  <table><tr><th>L/D</th><th>C_D</th></tr><tr><td>0.5</td><td>1.1</td></tr><tr><td>1</td><td>0.9</td></tr><tr><td>2</td><td>0.9</td></tr><tr><td>4</td><td>0.9</td></tr><tr><td>8</td><td>1.0</td></tr></table>	L/D	C_D	0.5	1.1	1	0.9	2	0.9	4	0.9	8	1.0
L/D	C_D																											
1	0.6																											
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L/D	C_D																											
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