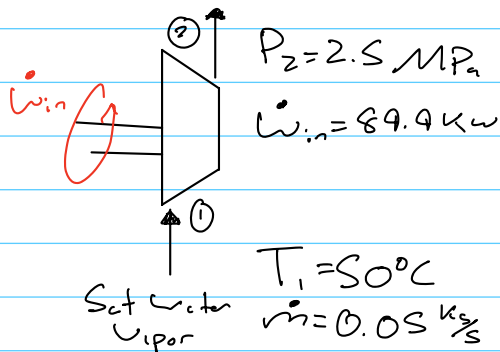


3-6) Adiabatic Compressor

3) Find Outlet °C T_2

$$T_1 = 50^\circ\text{C} \quad \left. \begin{array}{l} \text{Sat} \\ \text{water} \end{array} \right\} \xrightarrow{\text{vapor}} P_1 = 12.352$$

$$h_g = h_1 = 2541.3$$

$$s_g = s_1 = 8.0748$$

$$1^{st} \text{ Law: } Q_{in} - Q_{out} = W_{in} - W_{out} = \dot{m}(h_2 - h_1)$$

$$\dot{W}_{in} = \dot{m}(h_2 - h_1)$$

$$h_2 = \frac{\dot{W}_{in}}{\dot{m}} + h_1 = \frac{89.4 \text{ kW}}{0.05 \text{ kg/s}} + 2541.30$$

$$h_2 = 4384.30$$

$$\left. \begin{array}{l} P_2 = 2.5 \text{ MPa} \\ h_2 = 4384.30 \end{array} \right\} \Rightarrow h_f < h_g < h_2 \Rightarrow \text{superheated vapor} \Rightarrow T_2 = 400^\circ\text{C} \quad \boxed{T_2 = 400^\circ\text{C}}$$

Exit state at $P = 2.5 \text{ MPa}$, non-pelt4) Phase change fluid: isentropic $\rightarrow s_1 = s_2$

$$T_1 = 50^\circ\text{C} \quad \left. \begin{array}{l} \text{Sat} \\ \text{water} \end{array} \right\} s_1 = 8.0748 \frac{\text{kJ}}{\text{kg K}}$$

$$\boxed{s_2 = 8.0748 \frac{\text{kJ}}{\text{kg K}}}$$

5) Entropy = $4149.2 \frac{\text{kJ}}{\text{kg}}$? Enthalpy is in units $\frac{\text{kJ}}{\text{kg}}$, will assume enthalpy

$$\dot{W}_{ideal} = \dot{m}(h_{2s} - h_1) = 0.05(4149.2 - 2541.3) = 77.895 \text{ kW}$$

$$\boxed{\dot{W}_{ideal} = 77.895 \text{ kW}}$$

Assume
Typo
made

$$6) \eta_c = \frac{h_{2s} - h_1}{h_{2A} - h_1} = \frac{\dot{W}_{ideal}}{\dot{W}_{actual}} = \frac{4149.2 \frac{\text{kJ}}{\text{kg}} - 2541.30 \frac{\text{kJ}}{\text{kg}}}{4384.30 \frac{\text{kJ}}{\text{kg}} - 2541.30 \frac{\text{kJ}}{\text{kg}}} = 0.866$$