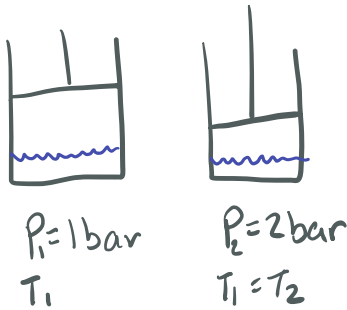


1.

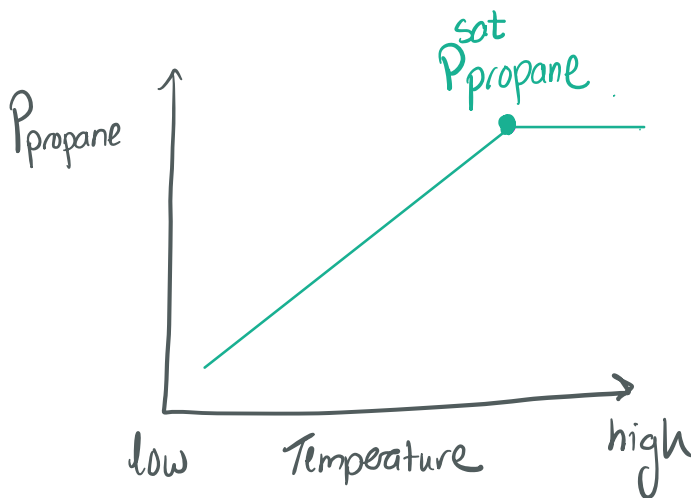


at the new equilibrium, the partial pressure of the water

b. Remains the same

The partial pressure of a saturated vapor is the p^{sat} . p^{sat} only depends on temperature (look at the Antoine Equation)

2.



The partial pressure describes how much of the total pressure comes from the propane.

$$y_i P = P_i^o$$

The partial pressure of the propane describes how much of the total pressure comes from the propane $y_i P = P_i^o$ for an ideal gas. When it is superheated, the propane stays in the gas phase (constant $P_{propane}$) until it hits the $p_{propane}^{sat}$. After this, the $p_{propane}^{sat} = P_{propane}$. We know that the $p_{propane}^{sat}$ decreases with temperature (Antoine Equation). This will continue until the p^{sat} is ≈ 0 .

3. If $T=80^\circ\text{C}$, use Antoine Equation to calculate p_A^{sat}

$$p_A^{\text{sat}} = 10^{\left[A - \frac{B}{T+C}\right]} \quad \text{where } \begin{aligned} A &= 4.42448 \\ B &= 1312.253 \\ C &= -32.445 \\ T &= 353\text{K} \end{aligned}$$

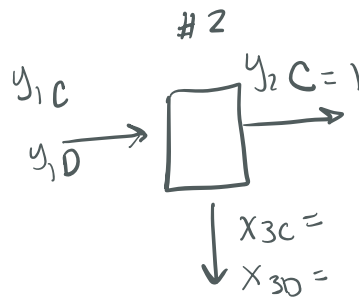
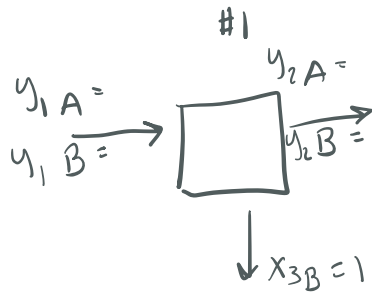
OR

$$p_A^{\text{sat}} = 2.1 \text{ bar}$$

$$p_A^{\text{sat}} = 1600 \text{ mmHg}$$

Taken from
NIST chemical
webbook, $T \equiv \text{K}$
 $P \equiv \text{bar}$

4.



write Raoult's law for both systems.

$$y_{2B}P = x_{3B}^1 P_B^{\text{sat}}$$

$$y_{2B}P = P_B^{\text{sat}}$$

$$P_B = P_B^{\text{sat}}$$

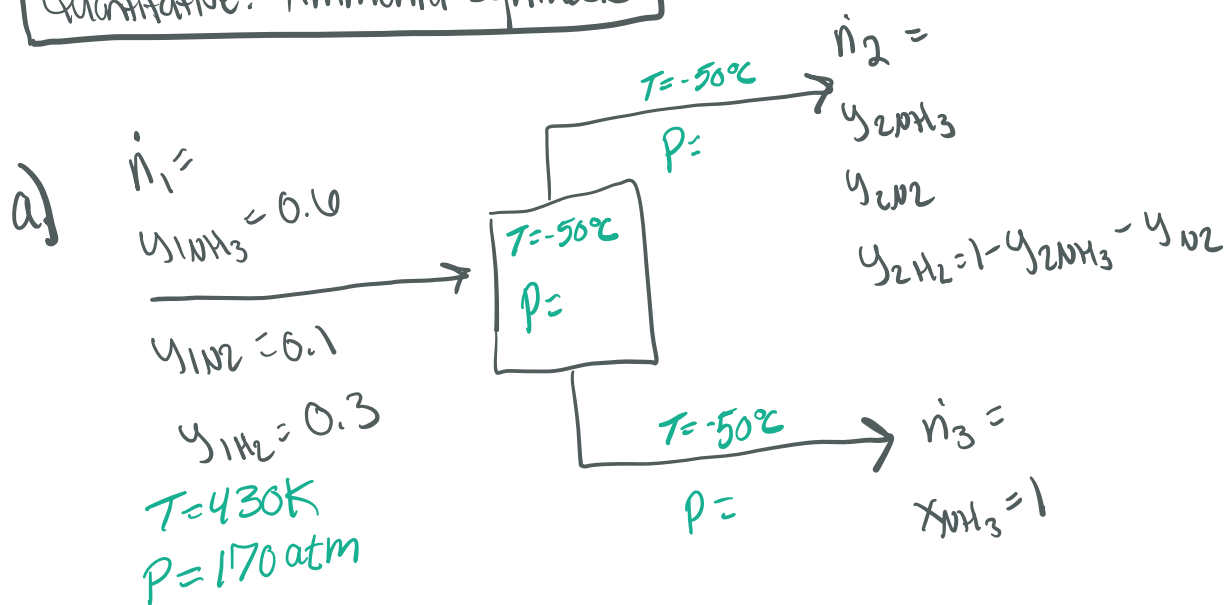
$$y_{2C}P = x_{3C}^1 P_C^{\text{sat}}$$

$$P_C = x_{3C} P_C^{\text{sat}}$$

$$P_C = x_{3C} P_C^{\text{sat}}$$

So only a) $P_B = P_B^{\text{sat}}$

Quantitative: Ammonia Synthesis



Extra Info

20% NH_3 fed is condensed $\rightarrow \frac{\dot{n}_3}{\dot{n}_1 y_{\text{NH}_3}} = 0.20$

$$\dot{V}_1 = 1.4 \text{ L/s}$$

Want to know

Condenser

$$y_{2\text{NH}_3} \quad y_{2\text{N}_2} \quad y_{2\text{H}_2} \quad \dot{V}_3$$

I won't consider \dot{n}_1 an unknown because we can calculate it from an EOS

b.)

DOF

5 unknowns (\dot{n}_2 \dot{n}_3 P $y_{2\text{N}_2}$ $y_{2\text{NH}_3}$)

- 3 mat. balances (NH_3 N_2 H_2)

- 2 Add. eq's (2 Raoult/Antoine + 20% condensed)

0 DOF! we can get to work ~

First, I will use an EOS to solve for \dot{n}_1
Then I'll have enough info to work through
Raoult's + the material balances.

c) EOS to solve for \dot{n}_1 . We have high pressure (14.7 atm)
so I will use the compressibility factor EOS.

$$P\dot{V} = \dot{n}_1 RT_1 z$$

To solve for \dot{n}_1 we need to calculate z .

Since stream 1 is a mixture, we know to calculate
the P'_c and T'_c using Kay's Rule.

$$T'_c = \sum y_i T_{c,i} = y_{\text{NH}_3} T_{c,\text{NH}_3} + y_{\text{N}_2} T_{c,\text{N}_2} + y_{\text{H}_2} T_{c,\text{H}_2}$$

$$P'_c = \sum y_i P_{c,i} = y_{\text{NH}_3} P_{c,\text{NH}_3} + y_{\text{N}_2} P_{c,\text{N}_2} + y_{\text{H}_2} P_{c,\text{H}_2}$$

* all T'_c and P'_c are found in Table B.1
Calc, T_r and P_r

Then, use the compressibility charts to find z .

Then calculate \dot{n}_1

Use material balances + Raoult's to calculate vapor phase composition.

$$\begin{array}{lcl}
 \text{N}_2: & \dot{n}_1 y_{1\text{N}_2} = \dot{n}_2 y_{2\text{N}_2} & \text{and } 0.20 = \frac{\dot{n}_3}{\dot{n}_1 y_{1\text{NH}_3}} \\
 \text{H}_2: & \dot{n}_1 y_{1\text{H}_2} = \dot{n}_2 y_{2\text{H}_2} & \\
 \text{NH}_3: & \dot{n}_1 y_{1\text{NH}_3} = \dot{n}_2 y_{2\text{NH}_3} + \dot{n}_3 & \\
 \text{total:} & \dot{n}_1 = \dot{n}_2 + \dot{n}_3 & y_{2\text{NH}_3} P = P_{\text{NH}_3}^{\text{sat}} \text{ where } P_{\text{NH}_3}^{\text{sat}} = f(T)
 \end{array}$$

We want to know P which comes from Raoult's so we need to find a way to solve for $y_{2\text{NH}_3}$ first!

1. calculate \dot{n}_3 using % condensed ratio
2. total balance to get $\dot{n}_1 \neq \dot{n}_2 + \dot{n}_3 \Rightarrow \dot{n}_2$
3. solve NH_3 balance for $y_{2\text{NH}_3}$
4. use Antoine to calc. $P_{\text{NH}_3}^{\text{sat}}$
5. use $P_{\text{NH}_3}^{\text{sat}}$ and $y_{2\text{NH}_3}$ in Raoult's to calc P !
6. use H_2 balance to calc $y_{2\text{H}_2}$
7. $1 - y_{2\text{NH}_3} - y_{2\text{H}_2} = y_{2\text{N}_2}$

Calculate \dot{V}_3 from \dot{n}_3

$$\dot{V}_3 = \dot{n}_3 \left(\frac{\text{mol}}{\text{s}} \right) M_w \left(\frac{\text{g}}{\text{mol}} \right) \cdot \frac{1}{\rho} \left(\frac{\text{L}}{\text{g}} \right)$$

✖ ✖ Up until this point is what I would expect on a quiz or a midterm ✖ ✖

d) Now that we've laid out the process - let's crunch some numbers! I did mine in excel

EOS to solve for \dot{n}_1

$$\begin{aligned} T'_c &= \sum y_i T_{c,i} = y_{\text{NH}_3} T_{c,\text{NH}_3} + y_{\text{N}_2} T_{c,\text{N}_2} + y_{\text{H}_2} T_{c,\text{H}_2} \\ &= 0.6(405.5 \text{ K}) + 0.1(121 \text{ K}) + 0.3(184.9 \text{ K}) \\ \underline{T'_c} &= \underline{301.9 \text{ K}} \end{aligned}$$

$$\begin{aligned} P'_c &= \sum y_i P_{c,i} = y_{\text{NH}_3} P_{c,\text{NH}_3} + y_{\text{N}_2} P_{c,\text{N}_2} + y_{\text{H}_2} P_{c,\text{H}_2} \\ &= 0.6(111.5) + 0.1(33.5) + 0.3(50.2) \text{ atm} \\ \underline{P'_c} &= \underline{111.5 \text{ atm}} \end{aligned}$$

$$\left. \begin{aligned} T_r &= \frac{450 \text{ K}}{301.9 \text{ K}} = 1.5 \\ P_r &= \frac{170 \text{ atm}}{85.4 \text{ atm}} = 2 \end{aligned} \right\} \text{ using the compressibility charts}$$

$Z = 0.84$

$$P_1 \dot{V}_1 = \dot{n}_1 R T_1 Z$$

$$\dot{n}_1 = \frac{P_1 \dot{V}_1}{R T_1 Z} = \frac{(170 \text{ atm}) \left(1.4 \frac{\text{L}}{\text{s}}\right)}{0.0821 \frac{\text{L atm}}{\text{mol} \cdot \text{K}} (450 \text{ K}) (0.84)} = \underline{\underline{9.7 \frac{\text{mol}}{\text{s}}}}$$

Material balances + Raoult's to calc y_i 's

1. Calc $\dot{n}_3 \rightarrow \frac{\dot{n}_3}{\dot{n}_1 y_{1NH_3}} = 0.20$, $\dot{n}_3 = 0.2 \left(7.7 \frac{\text{mol}}{\text{s}} \right) (0.6)$
 $\dot{n}_3 = 0.92 \text{ mol/s}$

2. Use \dot{n}_3 to calc \dot{n}_2
 $\dot{n}_1 = \dot{n}_2 + \dot{n}_3 \rightarrow \dot{n}_2 = 7.7 \text{ mol/s} - 0.92 \text{ mol/s}$
 $\dot{n}_2 = 6.7 \text{ mol/s}$

3. Solve NH_3 balance for y_{2NH_3}

$$\dot{n}_1 y_{1NH_3} = \dot{n}_2 y_{2NH_3} + \dot{n}_3$$

$$y_{2NH_3} = \frac{\dot{n}_1 y_{1NH_3} - \dot{n}_3}{\dot{n}_2}$$

$$y_{2NH_3} = \frac{7.7 \frac{\text{mol}}{\text{s}} (0.6) - 0.92 \frac{\text{mol}}{\text{s}}}{6.7 \text{ mol/s}}$$

$$y_{2NH_3} = 0.54$$

4.5. Antoine Equation + Raoult's

$$\log_{10} P_{NH_3}^{\text{sat}} = A - \frac{B}{T+C}$$

$$A = 7.55466$$

$$B = 1002.711$$

$$C = 247.883$$

$$P_{NH_3}^{\text{sat}} = 307 \text{ mmHg}$$

$$y_{2NH_3} P = P_{NH_3}^{\text{sat}}$$

$$P = \frac{P_{NH_3}^{\text{sat}}}{y_{2NH_3}} = \frac{307 \text{ mmHg}}{0.54} = P = 563 \text{ mmHg}$$

$$P = 0.74 \text{ atm}$$

6. H₂ balance to calc y_{2H₂}

$$\dot{n}_1 y_{1H_2} = \dot{n}_2 y_{2H_2} \quad y_{2H_2} = \frac{\dot{n}_1 y_{1H_2}}{\dot{n}_2} = y_{2H_2} = 0.34$$

7. 1 - y_{2H₂} - y_{2NH₃} = y_{2N₂}

$$y_{2N_2} = 1 - 0.34 - 0.54$$

$$y_{2N_2} = 0.11$$

8. Finally! We can calculate \dot{V}_3 ... last one!

$$\dot{V}_3 = \dot{n}_3 \left(\frac{\text{mol}}{\text{s}} \right) M_w \left(\frac{\text{g}}{\text{mol}} \right) \cdot \frac{1}{\rho} \left(\frac{\text{L}}{\text{g}} \right)$$

$$\dot{V}_3 = 0.92 \frac{\text{mol}}{\text{s}} \left(17.03 \frac{\text{g}}{\text{mol}} \right) \left(\frac{1 \text{ m}^3}{0.73 \text{ kg}} \right) \left(\frac{1000 \text{ L}}{1 \text{ m}^3} \right) \left(\frac{1 \text{ kg}}{1000 \text{ g}} \right)$$

$$\dot{V}_3 = 21 \text{ L/s}$$

Remember how long this took when you ask for numerical answers in class - my hand is cramping up! We would spend a full 50 minutes doing algebra!