

problem 1

(a) n-pentane

$$f^L(T, P) = p^{\text{sat}} \phi^{\text{sat}} \exp \left[ \frac{1}{RT} \int_{p^{\text{sat}}}^P v^L dp \right]$$

find  $T = T^{\text{boil}} (P = 1 \text{ bar})$

use Antoine eq:  $\ln(P[\text{bar}]) = A - \frac{B}{T+C}$

$$\frac{B}{T+C} = A - \ln P$$

$$T = \frac{B}{A - \ln P} - C$$

$$T = \frac{2477.07}{9.2131 - \ln(1)} - (-39.94)$$

(coefficients from  
Koretsky  
Table A1-1)

use this  
T

$$T^{\text{boil}} = 309 \text{ K}$$

for  $T = 309 \text{ K}$ ,  $p^{\text{sat}} = 1 \text{ bar}$

low pressure,  
vapour  $\approx$  ideal

$$\phi^{\text{sat}}(T = 309 \text{ K}, P = 1 \text{ bar}) \approx 1$$

$$F^L(T, P) = p^{\text{sat}} \exp \left[ \underbrace{\frac{v_m^L}{RT} (P - p^{\text{sat}})}_{\text{assume } v_m^L = \text{const.}} \right]$$

(1)

from NIST (pure Chem)  
 $\rho = 630 \text{ kg/m}^3$

$$v_m^L = \frac{m_w}{\rho} = \frac{72.15 \times 10^{-3} \text{ kg/mol}}{630 \text{ kg/m}^3} = 0.000115 \text{ m}^3/\text{mol}$$

$$F^L = (1 \text{ bar}) \exp \left[ \frac{0.000115 \text{ m}^3/\text{mol}}{(8.314 \text{ J/mol}\cdot\text{K})(309\text{K})} (200 \text{ kPa} - 1 \text{ kPa}) \times 10^5 \frac{\text{Pa}}{\text{bar}} \right]$$

$$F^L = 2.4 \text{ bar}$$

(6) From NIST Chemistry Webbook:

(use diff units)  $\log_{10}(P[\text{bar}]) = A - \frac{B}{T+C}$

$$T = \frac{B}{A - \log_{10} P} - C$$

$$T = \frac{1099.207}{4.24696 - \underbrace{\log_{10}(1)}_{=0}} - (-8.256)$$

$$T = 267 \text{ K}$$

$$F^L = p^{\text{sat}} \exp \left[ \frac{v_m^L}{RT} (P - p^{\text{sat}}) \right]$$

$$\rho = 0.626 \text{ g/mL} = 626 \text{ kg/m}^3 \text{ (NIST)}$$

$$v_m^L = \frac{56.108 \times 10^{-3} \text{ kg/mol}}{626 \text{ kg/m}^3} = 8.96 \times 10^{-5} \text{ m}^3/\text{mol}$$

$$F^L = 2.2 \text{ bar}$$

(2)

2)

$$g_m^E = x_a x_b [A + B(x_a - x_b)]$$

$$\gamma_{H_2O}^\infty = \gamma_a^\infty = 2.62$$

$$G^E = \frac{n_a n_b}{n_a + n_b} \left[ A + B \left( \frac{n_a - n_b}{n_a + n_b} \right) \right]$$

$$\gamma_{EtOH}^\infty = \gamma_b^\infty = 7.24$$

$$\bar{G}_a^E = \left( \frac{\partial G^E}{\partial n_a} \right)_{T,P,n_b} = \frac{2}{2n_a} \left[ A \left( \frac{n_a n_b}{n_a + n_b} \right) + B \frac{n_a n_b (n_a - n_b)}{(n_a + n_b)^2} \right]$$

$$= A \left[ \frac{n_b (n_a + n_b) - n_a n_b}{(n_a + n_b)^2} \right]$$

$$+ B \left[ \frac{(2n_a n_b - n_b^2)(n_a + n_b)^2 - 2(n_a + n_b)n_a n_b (n_a - n_b)}{(n_a + n_b)^4} \right]$$

$$= A(x_b - x_a x_b)$$

$$+ B \left[ (2x_a x_b - x_b^2) - 2x_a x_b (x_a - x_b) \right]$$

$$= Ax_b^2 + B \left[ x_b^2 (2x_a - 1) + 2x_a x_b \underbrace{(1 - x_a)}_{x_b} \right]$$

$$= Ax_b^2 + Bx_b^2 [2x_a - 1 + 2x_a]$$

$$= Ax_b^2 + Bx_b^2 [4(1 - x_b) - 1]$$

$$= Ax_b^2 + 3Bx_b^2 - 4Bx_b^3$$

$$\bar{G}_a^E = RT \ln \gamma_a = (A + 3B)x_b^2 - 4Bx_b^3$$

← equivalent to result in Table 7.2

Similarly,

$$\bar{G}_b^E = RT \ln \gamma_b = (A - 3B) x_a^2 + 4B x_a^3 \quad (\text{also in Table 7.2})$$

Determine  $A$  &  $B$  using  $\gamma_a^\infty, \gamma_b^\infty$  data

$$RT \ln \gamma_a^\infty = \bar{G}_a^E (x_a \approx 0) = A + 3B - 4B$$

$\uparrow$   
 $x_b \approx 1$   
dilute conditions

$$RT \ln \gamma_a^\infty = A - B$$

and:  $RT \ln \gamma_b^\infty = \bar{G}_b^E (x_a = 1) = A - 3B + 4B = A + B$

$$RT \ln (\gamma_a^\infty \gamma_b^\infty) = 2A$$

$$A = \frac{RT}{2} \ln (\gamma_a^\infty \gamma_b^\infty)$$

$$T = 70 + 273 \text{ K}$$

$$\rightarrow \boxed{A = 4195 \text{ J/mol}}$$

$$B = A - RT \ln \gamma_a^\infty$$

$$\boxed{B = 1449 \text{ J/mol}}$$

$$\hat{f}_a (x_a = 0.4) ?$$

$$\hat{f}_a = f_a^L x_a \gamma_a$$

$\uparrow$   
 pure liquid

Note:  $P_a^{\text{sat}}(70^\circ\text{C}) = 31.2 \text{ kPa} \ll 1 \text{ bar} \rightarrow \phi_a^v \approx 1$

If  $P = 1 \text{ bar}$ , ignore  $\exp\left[\frac{v_m^L}{RT}(P - P_a^{\text{sat}})\right] \approx 1$

$$\text{Thus, } f_a^L(T, P) = P_a^{\text{sat}} \underbrace{\phi_a^v}_{\approx 1} \underbrace{\exp\left[\frac{1}{RT} \int_{P_a^{\text{sat}}}^P v_m^L dP\right]}_{\approx 1}$$

$$f_a^L(T, P) \approx P_a^{\text{sat}}(70^\circ\text{C}) = 31.2 \text{ kPa}$$

$$\hat{f}_a = P_a^{\text{sat}} \underbrace{x_a}_{0.4} \exp\left[\frac{1}{RT} \left( (A+3B) \underbrace{x_b^2}_{\uparrow} - 4B \underbrace{x_b^3}_{\uparrow} \right)\right]$$

$\uparrow$   
 $x_b = 1 - x_a = 0.6$

$\hat{f}_a = 23.65 \text{ kPa}$

i) both Lewis

$$\ln \gamma_a \rightarrow 0$$

$$(\gamma_a \rightarrow 1) \text{ as } x_a \rightarrow 1$$

$$\ln \gamma_b \rightarrow 0$$

$$(\gamma_b \rightarrow 1) \text{ as } x_b \rightarrow 1$$

(b)

G-D eqn:

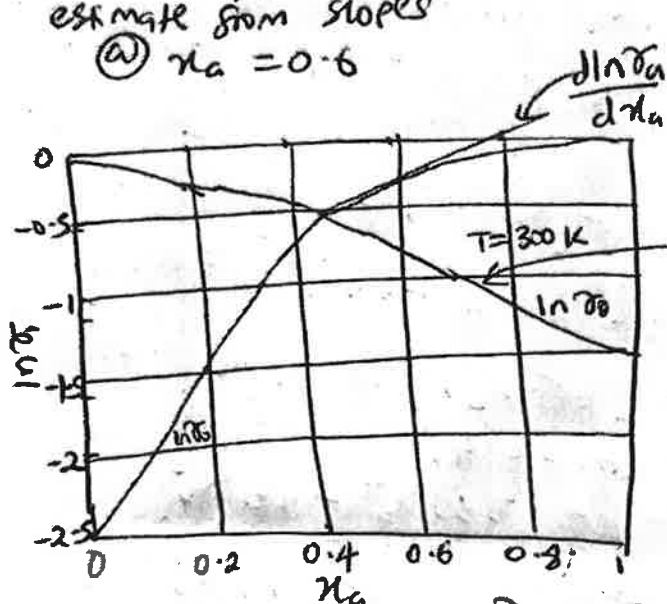
$$\sum x_i d \ln \gamma_i = 0$$

$$x_a d \ln \gamma_a + x_b d \ln \gamma_b = 0$$

$$x_a \frac{d \ln \gamma_a}{d x_a} + x_b \frac{d \ln \gamma_b}{d x_a} = 0$$

estimate from slopes

$$(a) x_a = 0.6$$



$$\left. \frac{d \ln \gamma_a}{d x_a} \right|_{x_a=0.6} \approx \frac{0.25}{0.175}$$

$$\approx 1.43$$

$$\left. \frac{d \ln \gamma_b}{d x_a} \right|_{x_a=0.6}$$

$$\approx \frac{-0.2}{0.1}$$

$$\approx -2$$

$$\rightarrow (0.6)(1.43) + (0.4)(-2) = 0.06 \approx 0$$

(c) cannot use two-suffix Margules:

$$\gamma_a = \exp \left[ \frac{A}{RT} x_b^2 \right], \gamma_b = \exp \left[ \frac{A}{RT} x_a^2 \right]$$

because the  $g_m^E$  model requires the  $\gamma_i$ 's to be symmetric with  $x_a$

Let's try 3-suffix Margules:

$$g_m^E = x_a x_b [A + B(x_a - x_b)]$$

find A & B

Table 7.2:

$$RT \ln \gamma_a = (A + 3B) x_b^2 - 4B x_b^3$$

$$RT \ln \gamma_b = (A - 3B) x_a^2 + 4B x_a^3$$

Use data at infinite dilution.

$$\rightarrow RT \ln \gamma_a^\infty = RT \ln \gamma_a (x_a \rightarrow 0) = -2.5RT = A + 3B - 4B$$

$$A - B = -2.5RT$$

$$\rightarrow RT \ln \phi_b = RT \ln \phi_b (\chi_b \rightarrow 0) = -1.5RT = -4988.4$$

$$A+B = -1.5RT$$

↓ SUM eqns

$$(A-B) + (A+B) = -4RT$$

$$2A = -4RT$$

$$A = -2RT$$

$$A = -4988.4 \text{ J/mol}$$

$$B = 1247.1 \text{ J/mol}$$

$$\text{for } g_m^E = \chi_a \chi_b [A + B(\chi_a - \chi_b)]$$

(d) It will not separate into two liq phases.

-  $\chi_a$  and  $\chi_b$  are always  $< 1$

So system is more stable as a mixture

- note:

$$g_m^E = \chi_a \chi_b [A + B(\chi_a - \chi_b)]$$

$$= -4988.4$$

max: 1247 (when  $\chi_a \rightarrow 1$ )  
min: -1247 (when  $\chi_a \rightarrow 0$ )

$g_m^E < 0$  always.

and

$\Delta g_{m, \text{min}} < 0$  always

$\rightarrow$  stable as a mixture (1 liq phase)

$$g_m^E = \left[ \frac{1}{A\chi_a} + \frac{1}{B\chi_b} \right]^{-1} + C \chi_a \chi_b (\chi_a - \chi_b)^2 \quad (4)$$

$$g_m^E = \left[ \frac{n}{A n_a} + \frac{n}{B n_b} \right]^{-1} + \frac{C n_a n_b}{n^4} (n_a - n_b)^2$$

$$G^E = \frac{n}{A \left( \frac{1}{A n_a} + \frac{1}{B n_b} \right)} + \frac{C n_a n_b (n_a - n_b)^2}{n^3}$$

$$G^E = \frac{1}{\left( \frac{1}{A n_a} + \frac{1}{B n_b} \right)} + \frac{C n_a n_b (n_a - n_b)^2}{n^3}$$

$$\bar{G}_a^E = \left( \frac{\partial G^E}{\partial n_a} \right)_{T, P, n_b} = \frac{-\left( -\frac{1}{A n_a^2} \right)}{\left( \frac{1}{A n_a} + \frac{1}{B n_b} \right)^2} + \frac{C n^3 (n_b (n_a - n_b)^2 + 2 n_a n_b (n_a - n_b))}{n^6} - \frac{3 C n_a n_b (n_a - n_b)^2 n^2}{n^6}$$

$$\bar{G}_a^E = \frac{1}{A n^2 \left( \frac{1}{A n_a} + \frac{1}{B n_b} \right)^2} + C \left[ \frac{n^3 n_b - 3 n_a n_b n^2}{n^6} (n_a - n_b)^2 + \frac{2 n_a n_b (n_a - n_b)}{n^3} \right]$$

$$\bar{G}_a^E = \frac{1}{A \left( \frac{1}{A \chi_a} + \frac{1}{B \chi_b} \right)^2} + C \left[ (\chi_b - 3 \chi_a \chi_b) (\chi_a - \chi_b)^2 + 2 \chi_a \chi_b (\chi_a - \chi_b) \right]$$

$$RT \ln \gamma_a = \frac{1}{A \left( \frac{1}{A \chi_a} + \frac{1}{B \chi_b} \right)^2} + C \left[ (\chi_b - 3 \chi_a \chi_b) (\chi_a - \chi_b)^2 + 2 \chi_a \chi_b (\chi_a - \chi_b) \right]$$

$$RT \ln \gamma_a = A \left( \frac{B \chi_b}{A \chi_a + B \chi_b} \right)^2 + \chi_b \left[ (1 - 3 \chi_a) (\chi_a - \chi_b)^2 + 2 \chi_a (\chi_a - \chi_b) \right]$$

$$\bar{G}_b^E = \left( \frac{\partial G^E}{\partial n_b} \right)_{T, P, n_a} = \frac{1}{B n^2 \left( \frac{1}{A n_a} + \frac{1}{B n_b} \right)^2}$$

$$+ C \left[ \frac{n^3 n_a - 3 n^2 n_a n_b}{n^6} (n_a - n_b)^2 + \frac{2 n_a n_b (n_a - n_b)}{n^3} \right]$$

$$RT \ln \gamma_b = B \left( \frac{A \chi_a}{A \chi_a + B \chi_b} \right)^2 + \chi_a \left[ (1 - 3 \chi_b) (\chi_a - \chi_b)^2 + 2 \chi_b (\chi_a - \chi_b) \right]$$