

Purely elastic self sustaining process

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1. Introduction

2. Methods

2.1. Streaky profile

We use a Chebyshev-Fourier decomposition, with Chebyshev polynomials in the wall-normal (y) direction and Fourier modes in the spanwise (z) direction. We then solve for the velocity in the streamwise (x) direction, subject to forcing in the y and z directions, via a Newton-Raphson iteration of the governing Navier-Stokes and Oldroyd-B equations,

$$Re \left[\frac{d\mathbf{v}}{dt} + \mathbf{v} \cdot \nabla \mathbf{v} \right] = -\nabla p + \beta \nabla^2 \mathbf{v} + \frac{1-\beta}{Wi} \nabla \cdot \boldsymbol{\tau} \quad (2.1)$$

$$\nabla \cdot \mathbf{v} = 0 \quad (2.2)$$

$$\dot{\boldsymbol{\tau}}/Wi + \overset{\nabla}{\boldsymbol{\tau}} = (\nabla \mathbf{v})^T + \nabla \mathbf{v} \quad (2.3)$$

where Re is the Reynold's number, Wi is the Weissenberg number, ∇ is the gradient operator, ∇^2 is the Laplacian and $\overset{\nabla}{\boldsymbol{\tau}}$ is the upper convected derivative of the stress tensor. In order to decompose the system onto the computational grid, we take a Fourier and Chebyshev transform of the variables,

$$\tilde{G}(y, z) = \sum_{n=-N}^N \sum_{m=0}^{M+1} G_{m,n} e^{i\gamma z} T_m(y) \quad (2.4)$$

where g stands for any of the base profile variables (U, V, W, τ_{ij}) in the problem and $T_m(y)$ is the m th Chebyshev polynomial of the first kind.

Given that the base profile is independent of the streamwise direction and time, we reduce the Navier-Stokes and Oldroyd-B equations and then solve them using a simple Newton-Raphson iteration for the base Streamwise velocity U . The system is driven by

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the standard no-slip boundary conditions on the streamwise velocity at the walls,

$$U(\pm 1) = 1 \quad (2.5)$$

$$(2.6)$$

and forcing terms introduced via fixing of the wall-normal and spanwise base profile velocities,

$$V(y, z) = V_0 \hat{v}(y) \cos(\gamma z) \quad (2.7)$$

$$W(y, z) = \frac{V_0}{\gamma} \frac{\partial \hat{v}}{\partial y} \sin(\gamma z) \quad (2.8)$$

Where,

$$\hat{v}(y) = \frac{\cos(py)}{\cos(p)} - \frac{\cosh(\gamma y)}{\cosh(\gamma)} \quad (2.9)$$

p is given by solutions to $p \tan p + \gamma \tanh \gamma = 0$ and governs the number of rolls in the wall-normal direction. These velocities are a guess for the rolls derived from the lowest order eigenmode of the operator ∇^4 , precisely the same rolls used in ?. This provides us with the streaky profile shown below.

2.2. Linear Stability Analysis

Having obtained the full base profile of the problem, we then performed a linear stability analysis, to look for instabilities that might produce waviness in the streaks. These wavy instabilities are responsible for sustaining the exact coherent state in the Newtonian version of the process.

We decompose the disturbance velocities in a similar way to above (equation 2.4), but include streamwise dependence

$$\check{g}(x, y, z, t) = \sum_{n=-N}^N \sum_{m=0}^{M+1} g_{m,n}(k_x) e^{i(k_x x + \gamma z)} T_m(y) e^{i\lambda t} \quad (2.10)$$

where g can be any of the disturbance variables (u, v, w, p, τ_{ij}) . To increase the numerical stability of the problem, we use free slip boundary conditions on the disturbance velocities, $\frac{\partial w}{\partial y}(\pm 1) = v(\pm 1) = \frac{\partial w}{\partial y}(\pm 1) = 0$.

The linearised system of equations now gives an eigenvalue problem for the growth rate of the instability λ at every streamwise wavenumber of the disturbance.

The solution to the eigenvalue problem provides spectra for which eigenmodes with positive growth rates are unstable.

3. Results

3.1. Streaks

After using the above Newton-Raphson method we obtain a streaky profile in the fluid. At high Re we find streaks in the streamwise velocity similar to those in ?. However, as we decrease the Reynold's number for constant and large Weissenberg number, we find that the streaks in the streamwise velocity become less pronounced. This can be explained by considering that at low Reynold's number the fluid has a higher inertia, so it is more difficult for the lift up effect to produce streaks in the streamwise velocity.

Although we do not see streaks in the streamwise velocity, we do see them in the first normal stress difference, $N_1 = T_{xx} - T_{yy}$ (figure ??). These streaks appear in much the same place as the streamwise velocity streaks appear in the Newtonian self-sustaining

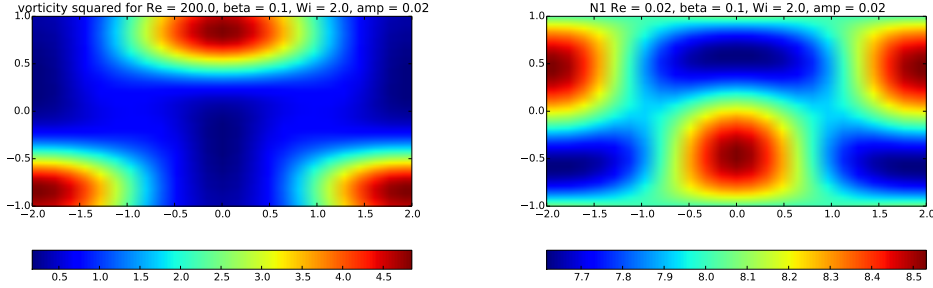


Figure 1: a) The magnitude of the vorticity of the fluid at $Re = 200$, $Wi = 2.0$, $amp=0.02$. b) The first normal stress difference in the polymeric fluid at $Re = 0.02$, $Wi = 2$, $amp=0.02$. The Newtonian vorticity and purely elastic first normal stress difference have large gradients in similar regions. However, the first normal stress difference also shows large gradients next to the wall.

process. As noted earlier, instabilities in viscoelastic fluids are brought about by large changes in the first normal stress difference, since this brings about polymer stretching of the kind seen in the Weissenberg effect. It is important to note that the purely elastic 1st normal stress difference shows very large gradients near the wall, suggesting that resolving the instability in this base profile will be more difficult than in the Newtonian case.

3.2. Dispersion relations

As the Reynold's number is decreased, we find that the base profile becomes more stable. The dispersion relation is reduced in height and moves to lower streamwise wavenumbers. By about $Re = 100$ the base profile has become completely stable. The Newtonian instability is no longer present at this Reynold's number. However, once the Reynolds number becomes negligible in comparison to the Weissenberg number, we begin to see a purely elastic instability arise at very low streamwise wavenumber 2. This purely elastic instability is hugely amplified by further reductions in the Reynold's number.

We can further examine how the purely elastic instability changes with changing Weissenberg number. We find that it grows as the Weissenberg number increases, and saturates by around $Wi = 20$. Doubling the amplitude of the rolls increases the width of the instability by about a third and the height, 3 fold.

3.3. eigenmodes

In Fabian Waleffe's treatment of the Newtonian version of this self-sustaining process [?](#), he found that the feedback on the original rolls was provided by the eigenmode of the instability. The eigenmodes of the viscoelastic instability is quite different to that of the Newtonian instability. Although the components of the instability are large at the walls, the velocity is less important for the instability of the purely elastic fluid than the first normal stress difference. We find that N_1 is large away from the walls, another encouraging sign for a viscoelastic self-sustaining process [\(4\)](#).

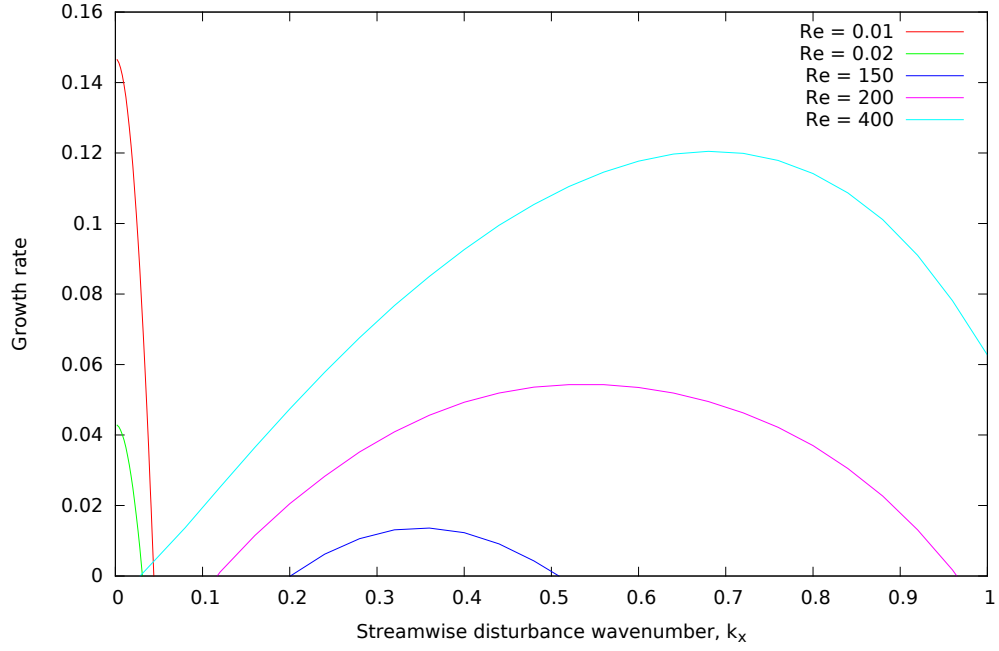


Figure 2: Dispersion relations as the Reynold's number is decreased at $Wi = 2$, $\beta = 0.1$ and $amp = 0.02$. A clear instability can be seen at low k_x in the purely elastic regime.

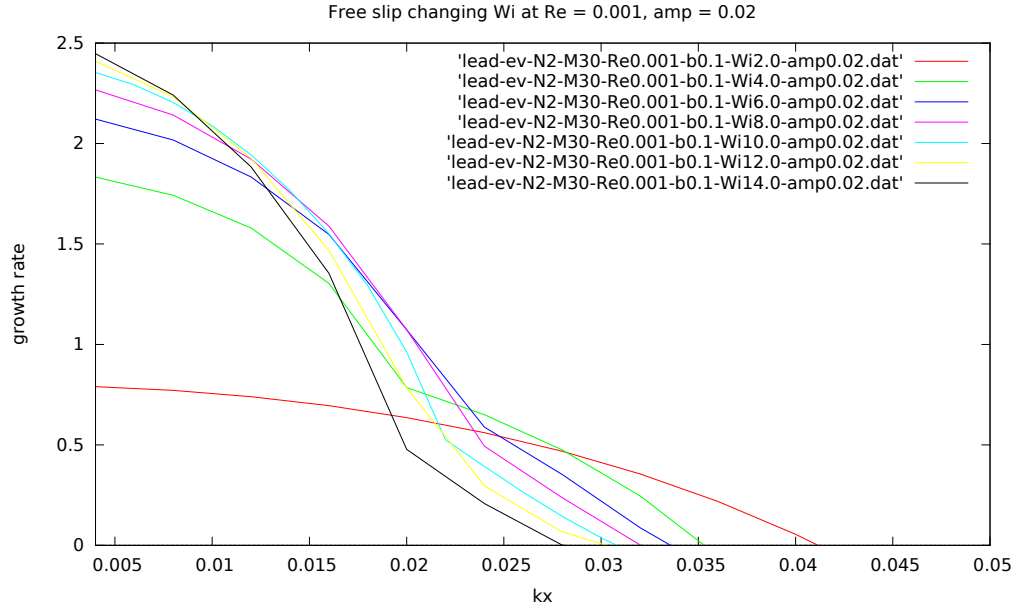


Figure 3: Dispersion relations as the Wi is decreased at $Re = 0.001$, $\beta = 0.1$ and $amp = 0.02$. The instability grows and then saturates.

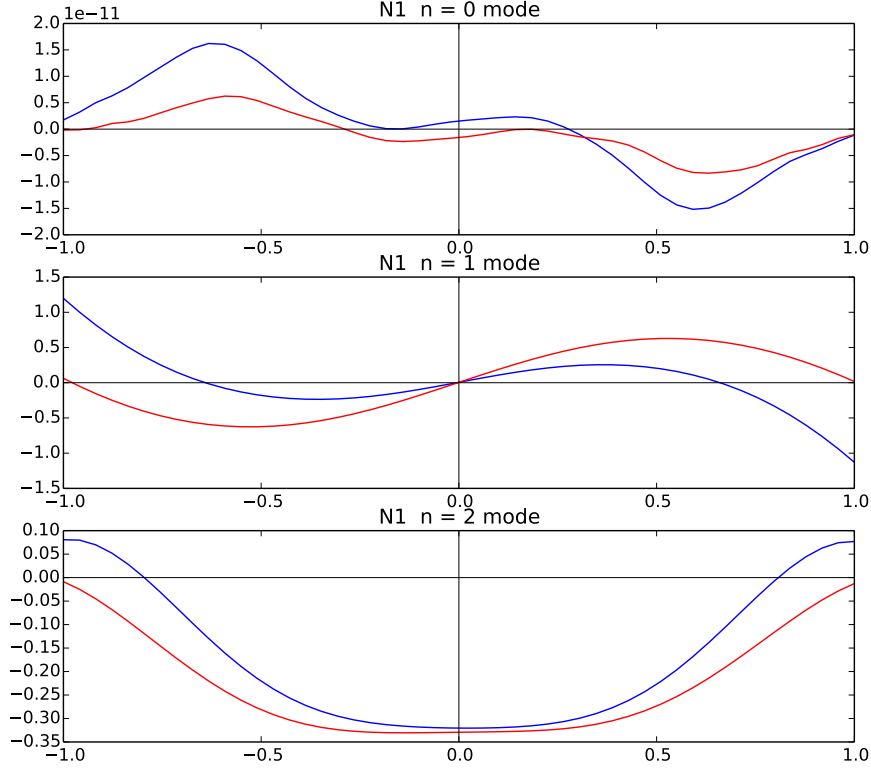


Figure 4: Eigenmodes of the first normal stress difference of the viscoelastic instability at $Wi = 2.0$, $Re = 0.02$, $\beta = 0.1$, $amp=0.02$ and $k_x = 0.01$.

3.4. Cauchy boundary conditions

To investigate the affect of free slip boundary conditions on linear stability analysis, we implemented Cauchy boundary conditions,

$$\alpha \left. \frac{\partial u}{\partial y} \right|_{y=\pm 1} + (1 - \alpha)u(y = \pm 1) = 0 \quad (3.1)$$

$$v(y = \pm 1) = 0 \quad (3.2)$$

$$\alpha \left. \frac{\partial w}{\partial y} \right|_{y=\pm 1} + (1 - \alpha)w(y = \pm 1) = 0 \quad (3.3)$$

Where α is a control parameter which controls the relative strength of the free slip to no-slip conditions. (Slip length?)

We found that on decreasing α the instability grows in strength and broadens. It appears that the no-slip system is infinitely unstable (figure ??).