# Fluid effect on hydraulic fracture propagation behavior: a comparison between water and supercritical CO<sub>2</sub>-like fluid

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### **ABSTRACT**

The initiation of hydraulic fractures during fluid injection in deep formations can be either engineered or induced unintentionally. Upon injection of  $CO_2$ , the pore fluids in deep formations can be changed from oil/saline water to  $CO_2$  or  $CO_2$  dominated. The type of fluid is important not only because the fluid must fracture the rock, but also because rocks saturated with different pore fluids behave differently. We investigated the influence of fluid properties on fracture propagation behavior by using the cohesive zone model in conjunction with a poroelasticity model. Simulation results indicate that the pore pressure fields are very different for different pore fluids even when the initial field conditions and injection schemes (rate and time) are kept the same. Low viscosity fluids with properties of supercritical  $CO_2$  will create relatively thin and much shorter fractures in comparison with fluids exhibiting properties of water under similar injection schemes. Two significant times are recognized during fracture propagation: the time at which a crack ceases opening and the later time point at which a crack ceases propagating. These times are very different for different fluids. Both fluid compressibility and viscosity influence fracture propagation, with viscosity being the more important property. Viscosity can greatly affect hydraulic conductivity and the leak-off coefficient. This analysis assumes the in-situ pore fluid and injected fluid are the same and the pore space is 100% saturated by that fluid at the beginning of the simulation.

Key words: cohesive finite element method, cohesive zone model, fracture propagation, hydraulic fracture, pore fluid

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## INTRODUCTION

A particular class of fractures in the earth develops as a result of internal pressurization by a fluid (Detournay 2004). Dykes and sills are natural examples of hydraulically induced fractures (Pollard 1976; Spence & Turcotte 1985), whereas hydraulic fractures designed to increase oil/gas production are man-made and have been used to stimulate over 70% of gas wells and 50% of oil wells in North America in the last half-century (Economides & Nolte 2000). Other applications include preconditioning of ore bodies, disposal of waste drill cuttings, remediation of contaminated land, and measurement of in-situ stress (Haimson & Fairhurst 1969; Sun 1969; Zoback *et al.* 1977; Evans *et al.* 1999; Murdoch & Slack 2002; Haimson & Cornet 2003; Frank & Barkley 2005; Legarth *et al.* 2005; Adachi & Detournay 2008).

Carbon dioxide has been used as a liquefied gas in oil and gas field stimulation since the early 1960s because it eliminates formation damage and residual fluids (Harris et al. 1984; Sinal & Lancaster 1987). Carbon dioxide injection is considered one of the most effective technologies for improving oil recovery from hard-to-extract oil reserves because CO<sub>2</sub> is effective in penetrating the formation due to its high diffusivity, and the rock associated with petroleum-containing formations is generally porous (Fink 2011). Field experience in petroleum engineering indicates that different fracturing fluids can result in different patterns of fracture creation and propagation. Viscous fluids tend to generate thick and planar cracks with few branches, while thin or low viscosity fluids tend to generate narrow and wavelike cracks with many secondary branches (Ishida et al. 1998, 2004). Even liquid CO<sub>2</sub> and supercritical CO<sub>2</sub> show different fracturing features in a recent laboratory test, with supercritical CO<sub>2</sub> generating cracks that extend much more three-dimensionally (Ishida et al. 2012). Some field experiences also show that when other normally used hydraulic fluids can fracture the formation at a comparable injection flow rate, CO<sub>2</sub> cannot (Yao 2012).

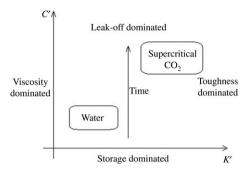
Two energy dissipation mechanisms and two fluid storage mechanisms compete during hydraulic fracturing. The energy dissipation mechanisms are mainly related to viscous flow and the creation of fracture area in solid host rock. The fluid storage mechanisms are storage of fluid in the fracture and leak-off of fluid into the permeable solid. These two sets of mechanisms are associated with four combined asymptotic regimes: storage-toughness (Garagash 2006), storage-viscosity (Savitski & Detournay 2002), leak-off-toughness (Bunger et al. 2005), and leak-off-viscosity (Adachi & Detournay 2008). For example, the toughness-dominated regime refers to a condition of large toughness or, equivalently, a low fracturing fluid viscosity. Here, toughness refers to how easy or difficult it is for a fracture to be initiated and/or propagated within a formation. In such a regime, the energy dissipated by viscous fluid flow inside the fracture is negligibly small compared to the energy expended in fracturing the solid medium. On the vertex of storage-viscosity-dominated regime, fluid leak-off is negligible compared to fluid storage in the fracture and the energy expended in fracturing the rock is negligible compared to viscous dissipation (Garagash 2006; Peirce & Detournay 2008a,b).

The relative magnitude of the dissipation processes on one hand, and of the storage processes on the other hand, can be described by a dimensionless toughness K' and a dimensionless leak-off coefficient C' (Adachi & Detournay 2008; Carrier & Granet 2012), respectively:

$$K' = \frac{4K_{IC}}{\sqrt{\pi}} \left( \frac{1}{3Q_0 E'^3 \mu} \right)^{1/4}; C' \approx 2 \frac{\kappa}{\mu} \frac{\sigma_0}{\sqrt{\pi c}} \left( \frac{E't}{12\mu Q_0^3} \right)^{1/6} \quad (1)$$

where  $K_{IC}$  is fracture toughness, E' is dimensionless Young's modulus,  $\epsilon$  is diffusivity coefficient,  $Q_0$  is injection rate,  $\mu$  is fluid viscosity,  $\sigma_0$  is the confining stress,  $\kappa$  is the intrinsic permeability and related with the hydraulic conductivity k by  $\kappa = k\mu/\rho_f g$ ,  $\rho_f$  is fluid density. Here, viscosity (or a power of it) is inversely related to K' and C' in both equations. Figure 1 shows the two-dimensional parameter space of dimensionless toughness K' and dimensionless leak-off coefficient C'. Each edge of this space represents an asymptotic regime. During the injection of fluid into a plane strain fracture, the propagation regime evolves from storage-dominated to leak-off-dominated with time (Carrier & Granet 2012).

A supercritical fluid exhibits physiochemical properties intermediate between those of liquids and gases. Mass transfer is rapid with supercritical fluids because their



**Fig. 1.** Schematic hydraulic fracture parametric space with respect to different fluids (water and supercritical CO<sub>2</sub>).

dynamic viscosities are nearer to those of normal gaseous states. The K' and C' values when supercritical  $CO_2$  is injected will be much larger than those of water because supercritical  $CO_2$  has a much smaller viscosity than water;  $\mu_{CO_2}$  is in the range of 0.02~0.16 cp (Fenghour *et al.* 1998; Heidaryana *et al.* 2011), while  $\mu_{HO_2}$  is about 1 cp. The relatively large K' and C' values will tend to put injection of supercritical  $CO_2$  closer to the leak-off-toughness-dominated regime than injection of water.

The pore fluids in deep formations will be changed from one type of fluid to another after consistent fluid injection, and rock formations saturated with such different pore fluids will behave very differently. Water-/oil-saturated rock and CO<sub>2</sub>-saturated rock will have very different pore pressure change curves because of their different Skempton's *B* values, and consequently, the fractures may propagate very differently (Berryman 2012). The objective of this paper is to investigate the effect of fluid properties on hydraulically induced fracture propagation behavior by using the cohesive finite element method (CFEM) or cohesive zone modeling approach.

In this paper, we focus on the effect of a fluid's hydromechanical properties on the hydraulic fracture's propagation behavior and assume single-phase flow conditions, that is, the in-situ pore fluid and the injected fluid are the same and the pore space is 100% saturated by that fluid at the beginning of the simulation. A single phase analysis using either supercritical CO2 or water allows us to make an end-member comparison of the hydro-mechanical effects of these fluids on the fracture initiation/propagation behavior during fluid injection.

### THE COHESIVE ZONE MODEL

Due to the difficulty of making accurate measurements of the fracture geometry during and after the hydraulic fracturing, modeling of the process assumes special importance (Adachi 2001). However, hydraulic fracturing is not a trivial process to model as it involves the coupling of several physical processes with singular behavior at the fracture tip (Sarris & Papanastasiou 2011). The cohesive zone model allows explicit modeling of fracturing in monolithic and composite material systems. The cohesive zone model in its infancy was described by Barenblatt's 'cohesive force' model (1959, 1962), Dugdale's 'strip-yield' model (1960), and Hillerborg's 'fictitious crack model' (Hillerborg et al. 1976). Cohesive zone elements do not represent any physical material, but describe the cohesive forces that occur when materials are being pulled apart. A series of investigations have been conducted dealing with the development of computational fracture mechanics (Camacho & Ortiz 1996; Needleman 1987; Falk et al. 2001; etc.) and hydraulic fracturing (Boone et al. 1986; Boone & Ingraffea 1990; Papanastasiou & Thiercelin 1993; etc.).

In classic linear elastic fracture mechanics (LEFM), an elastic crack tip region has an infinite stress at the sharp crack tip. The cohesive zone model assumes a fracture process zone characterized by a traction–separation law to avoid the singularity in the crack tip stress field that is present in classic fracture mechanics. The ability of a cohesive zone model to simulate a hydraulic fracture in different propagation regimes, such as the toughness-dominated and viscosity-dominated regimes, has been demonstrated by the work of Chen *et al.* (2009), Carrier & Granet (2012) and Chen (2012), etc.

The success of this approach may lie in the assumption that the stress-intensity factors at the crack tip are extremely small, and the limit of zero is perhaps the most common case (Spence & Sharp 1985; Spence & Turcotte 1985). Laboratory tests have also found that the viscositydominated regime prevails during hydraulically driven crack propagation in many real world conditions, with the crack tip effect extremely small in comparison with the dimension of the crack (Bunger & Detournay 2008). The cohesive zone model is more suitable for crack problems than LEFM for cemented materials because the size of the nonlinear zone is not negligible, due for instance to plasticity or micro-cracking. In fact, many hydraulic fracturing operations are performed in relatively 'soft' formations, such as porous sedimentary rocks (limestone or sandstone) or shale (impermeable but weak rock) instead of hard igneous rocks (granite) that are prone to nonlinear failures, which differ from LEFM (Elices et al. 2002; Adachi et al. 2007).

Figure 2 shows a cohesive zone model under tension failure due to a forced incoming fluid. The fluid flows in the cohesive zone with leak-off into the surrounding porous formation. The fluids can be separated into tangential flow and normal flow, and the fluid leak-off effect is defined by a permeable layer (Fig. 2). Leak-off from the fracture into the formation and pore pressure diffusion may change effective stresses in the formation and hence the size of the plastic zones (Papanastasiou 1999). The influence of fluid leak-off and pore pressure in a stationary

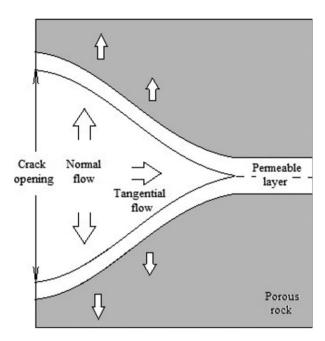


Fig. 2. Fluid flow in a cohesive zone with leak-off.

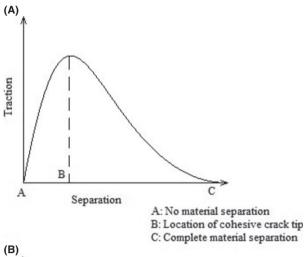
hydraulic fracture in a poroelastic medium has been investigated by Detournay & Cheng (1991).

Figure 3 shows the schematic constitutive cohesive law for a typical cohesive traction–separation curve (Shet & Chandra 2002) and its linear and exponential approximations. The constitutive behavior of the cohesive zone is based on laboratory tests. The traction–separation constitutive relation for the surface is such that with increasing separation, the traction across a pair of cohesive surfaces reaches a peak and then decreases (either linearly or exponentially) and eventually vanishes to permit a complete separation.

# **GOVERNING EQUATIONS**

The consideration of hydraulically induced fractures is at the juncture of four classical disciplines: lubrication theory, filtration theory, fracture mechanics, and poroelasticity. This type of problem involves the coupling of four distinct processes: (i) the relationship between fracture opening and the incoming fluid; (ii) the flow of fluid within the fracture; (iii) the propagation of the fracture; and (iv) leak-off of the fracturing fluid into the permeable medium, which is a time-dependent process (Bunger *et al.* 2005; Adachi & Detournay 2008). The equations governing the propagation of a hydraulic fracture in a reservoir have to account for these four dominant physical processes in addition to the deformation of the rock, the creation of new fracture surfaces, and fluid diffusion in the reservoir (Peirce & Detournay 2008b).

This paper considers the plane strain problem of a hydraulic fracture propagating in a permeable and linear



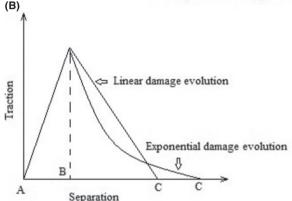


Fig. 3. Constitutive cohesive law (A) a typical cohesive traction–separation curve under stain control (B) linear and exponential approximations.

elastic medium. The particular problem of interest is conceptualized in plane strain and is usually referred to as a KGD fracture (in honor of Khristianovitch, Geertsma and de Klerk) (Geertsma & de Klerk 1969). The symmetry of the problem allows us to model only half of the space. The *x*-axis coincides with the fracture path with its origin at the injection point (Fig. 4).

# Fracture propagation theory based on cohesive law

The cohesive zone represents a region ahead of the crack tip and is characterized by microcracking along the crack path (Sarris & Papanastasiou 2011). The progressive damage and failure in cohesive layers is defined in terms of traction–separation law, in which a cohesive potential function  $\psi$  can be expressed as a function of the traction tensor T and the displacement jump  $\Omega$  across a pair of cohesive surfaces (Chen 2012):

$$\partial \psi = T \bullet \partial \Omega \tag{2}$$

The cohesive zone model implies that normal stress continues to be transferred across a discontinuity and is a

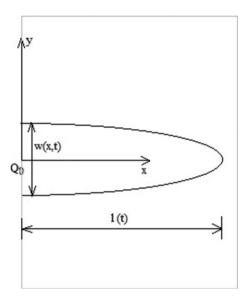


Fig. 4. KGD fracture problem.

function of the separation, falling to zero at a critical opening at which point the fracture propagates. During hydraulic fracturing, the fluid pressure is considered as traction acting on the open surfaces of the fracture and is balanced by the far-field stress and by the cohesive tractions acting across the cohesive zone. The traction tensor T relates to the field pore pressure  $(p_{\infty})$  (the pore pressure with enough distance from the fracture thus can be considered as a reference state without the disturbance of fluid injection), injection pressure inside of the fracture  $(p_i)$ , and confining stress tensor  $\sigma_{ij}$  for a tensile failure criterion in the normal direction:

$$T = \sigma_{ij} - \delta_{ij}(p_{\infty} + \Delta p_i), \quad T \le T_{\text{max}}; \quad \Delta p_i = p_i - p_{\infty}$$
 (3)

where  $\delta_{ij}$  is the Kronecker delta. This equation shows that the traction will decrease when pore pressure increases within the cohesive zone during fluid injection. The tensile strength comes into play once the injection pressure is higher than the confining stress, and tensile failure will be initiated once a tensile threshold is exceeded. The traction will eventually recover to equal to the far-field effective stress after pumping stops, and the fracture will finally close except where the opening is sustained by particles introduced during the fracturing process.

Hydraulic fracture modeling based on cohesive zone model requires fracture toughness as the fracture initiation criterion, which is a quadratic nominal stress criterion of the cohesive finite element method used in this paper (Hibbitt, Karlsson & Sorensen, Inc. 1998). In this criterion, damage is assumed to initiate when a quadratic interaction function involving the nominal stress ratios reaches

$$\left[\frac{t_n}{t_n^{\max}}\right]^2 + \left[\frac{t_{s1}}{t_{s1}^{\max}}\right]^2 + \left[\frac{t_{s2}}{t_{s2}^{\max}}\right]^2 = 1 \tag{4}$$

where  $t_n$  and  $t_{s1}$ ,  $t_{s2}$  are the normal, the first and second shear tractions, respectively. Because shear tractions are very small in our hydraulic fracturing problem configuration, fracture initiation will mainly be determined by the normal traction maximum  $t_n^{\max}$ . Note that the maximum cohesive traction tensor  $T_{max}$  is related to these tractions by  $T_{\max} = t_n^{\max}$ ,  $t_{s1}^{\max}$ ,  $t_{s2}^{\max}$ . Various types of traction–separation relations for the cohesive zone model have been proposed for fracture propagation, and the bilinear model is generally considered a good choice due to its straightforward physical background (Tomar *et al.* 2004). For a pure normal deformation mode, the cohesive energy  $G_c$ , the maximum cohesive traction tensor  $T_{max}$ , and the critical separation at complete failure  $\Omega_f$  are related through the following function (Chen 2012):

$$G_C = \frac{1}{2} T_{\text{max}} \Omega_f \tag{5}$$

### Fluid flow in the fracture

The injection rate of an incompressible fluid into a fracture in a plane strain configuration having an infinite permeable medium is assumed to be a constant  $Q_0$ . Note that at very high pore pressures, even supercritical  $CO_2$  can be so-considered for purposes of this problem. The mathematical model that describes the propagation of a fracture of half-length l(t) and aperture w(x,t) (Fig. 4) through an infinite poroelastic medium begins with global conservation of fluid injected at the crack inlet  $V_{inject}$  (Bunger *et al.* 2005):

$$V_{inject} = \frac{Q_0 t}{2} = V_{crack} + V_{leak} \tag{6}$$

The volumes of the fluid stored in the crack  $V_{crack}$  and leaked into the porous solid  $V_{leak}$  are correspondingly:

$$V_{crack} = \int_{0}^{l(t)} w(x, t) dx, t > 0$$

$$V_{leak} = \int_{0}^{t} dt' \int_{0}^{l(t')} \frac{2C}{\sqrt{t - t_0(x)}} dx, t - t_0(x) > 0$$
(7)

where C is the leak-off parameter characterizing the loss of fluid into the solid material,  $t_0$  is the lapse time since the exposure of the fracture surface to the fluid. The local fluid flux  $Q(t)\delta(x,y)$  is the summation of the tangential flux  $\nabla \cdot q_T$  and the normal flux  $\nabla \cdot q_N$  with the consideration of aperture change based on local mass conservation (Savitski & Detournay 2002; Peirce & Detournay 2008a).

$$Q(t)\delta(x,y) = \frac{\delta_w}{\delta_t} + \nabla \cdot q_T + \nabla \cdot q_N$$
 (8)

Lubrication theory is used to model the flow of fluid within the crack. If the fluid is assumed to have Newtonian rheology within the crack and the crack is such that  $w/l \ll 1$ , then the tangential flow  $q_T$  in the fluid-filled part of the fracture is governed by Poiseuille's law:

$$q_T = -\frac{w^3}{12\mu} \nabla p \tag{9}$$

where  $\mu$  is fluid viscosity, and  $\nabla p$  is the pore fluid gradient along the central line of the fracture. The normal flow  $q_N$  can be defined as:

$$q_N = 2C(p_C - p_b) \tag{10}$$

where  $p_c$  is the pore pressure on the central line of the fracture with  $p_c \approx p_i$  because the pressure gradient of fluid within the fracture is much smaller than the difference between  $p_c$  and  $p_b$ . Here,  $p_b$  is the pore pressure on the fracture boundary, assuming a symmetric configuration such that the upper and the lower boundary conditions do not differ.

# Poroelasticity field equations

Poroelastic effects have been ignored when modeling hydraulic fractures in many works in the past. However, poroelastic effects can be significant if the rock is considered to be porous. Modeling the poroelastic effect in hydraulic fracturing was pioneered by Cleary in the form of a back-stress (Cheng et al. 1993; Cheng & Detournay 1998). A hydraulic fracture in a poroelastic medium represents a (changing) surface across which the solid displacement and the normal fluid flux are discontinuous (Detournay et al. 1990; Detournay & Cheng 1991). As a starting point, the general constitutive equations for a continuous porous field govern both the deformation of the elastic porous medium and the diffusion of fluid through the pore space of the material (Rice & Cleary 1976; Berryman & Milton 1991):

$$\sigma_{ij} = 2G\left(\varepsilon_{ij} + \frac{v}{1 - v}\varepsilon_{ij}\delta_{ij}\right) - 2\eta \frac{1 - v}{1 - 2v}p_{\infty}\delta_{ij} \tag{11}$$

$$\Delta m_f = \frac{\rho_f(1-\nu)}{G(1+\nu)} \eta \left(\sigma_{kk} + \frac{3}{B} p_{\infty}\right) \tag{12}$$

$$\eta = \frac{3(\nu_u - \nu)}{2B(1 - \nu)(1 + \nu_u)} \tag{13}$$

$$B = \frac{\frac{1}{K} - \frac{1}{K_s}}{\frac{1}{K} - \frac{1}{K_s} + n\left(\frac{1}{K_f} - \frac{1}{K_n}\right)}$$
(14)

where  $\eta$  is an intermediate parameter as defined by Eqn. 13. B is Skempton's B coefficient and is defined by Eqn. 14,  $\sigma_{ij}$  and  $\varepsilon_{ij}$  are stress and strain tensors, respectively,  $v_u$  and v are undrained and drained Poisson's ratio, respectively, n is porosity, G is shear modulus,  $p_{\infty}$  is field

pore pressure,  $\rho_f$  is fluid density, K is drained bulk modulus,  $K_s$  is bulk modulus of the solid grains,  $1/K_n$  is the unjacketed pore compressibility, and  $K_f$  is the pore fluid bulk modulus. Pore fluid mass change  $\Delta m_f$  in the porous formation is related to the normal flow through the fracture by the equation:

$$\Delta m_f = \rho_f V_{leak} = \rho_f \int_0^t dt' \int_0^{t} \frac{2C}{\sqrt{t - t_0(x)}} dx, t - t_0(x) > 0$$
(15)

where  $\rho_f$  is fluid density,  $V_{leak}$  refers to the fluid volume that leaked into the porous solid, C is leak-off coefficient. Next, consider fluid flow field outside of the fracture where the behavior of the fluid leaking off into the porous formation is controlled by the pore pressure gradient and the compressibility of fluid as well as the mobility of the fluid. Due to the pore pressure gradient between the fracture zone and the far-field, a groundwater flow equation can be written with the addition of a term that incorporates stress effects on the pore pressure (Renshaw & Harvey 1994). The fundamental governing equation for transient flow is derived by combining Darcy's Law and the conservation of fluid mass (Green & Wang 1990):

$$\nabla^2 h = \frac{S_s}{k} \frac{\partial h}{\partial t}; \quad S_s = g \frac{\partial m_f}{\partial p}; \quad \frac{\partial m_f}{\partial t} = \rho_f S_s \frac{\partial h}{\partial t}$$
 (16)

where b is hydraulic head,  $S_s$  is the specific storage coefficient, k is the hydraulic conductivity ( $k = \kappa \rho_s g / \mu$ ),  $m_f$  is the fluid mass, and dp refers to the differential pressure between  $p_{\infty}$  (field pore pressure) and  $p_b$  (fluid pressure at fracture boundary). For the commonly applied boundary conditions of constant horizontal aquifer strain  $\Delta \varepsilon_{11} = \Delta \varepsilon_{22} = 0$  and constant overburden ( $\Delta \sigma_{33} = 0$ ), specific storage coefficient can be derived as (Green & Wang 1990):

$$\begin{split} S_s &= g \frac{dm_f}{dP} \bigg|_{\Delta \sigma_{33} = 0; \Delta \varepsilon_{11} = \Delta \varepsilon_{22} = 0} \\ &= \rho_f g \left\{ \left[ \left( \frac{1}{K} - \frac{1}{K_s} \right) + n \left( \frac{1}{K_f} - \frac{1}{K_s} \right) \right] - \frac{4\alpha}{3} G \left( 1 - \frac{K}{K_s} \right) \left( \frac{1}{K} - \frac{1}{K_s} \right) \right\} \end{split}$$

$$\tag{17}$$

where K is drained bulk modulus of the porous material,  $K_r$  is bulk modulus of the solid grains,  $K_f$  is bulk modulus of the pore fluid, G is shear modulus,  $\alpha$  is the compressibility along the vertical direction.

The fluid leak-off into the formation is dependent on the fracturing pressure, with the leak-off velocity  $v_l$  expressed as (Abousleiman 1991):

$$v_{l} = \frac{\kappa}{\mu\sqrt{\pi c}} \left( \frac{\sigma_{0} - p_{\infty}}{\sqrt{t_{0}}} + \int_{0}^{t_{0}} \frac{\partial p_{i}}{\partial t} \frac{1}{\sqrt{t_{0} - t}} dt \right)$$
 (18)

$$c = \frac{2\kappa B^2 G(1 - \nu)(1 + \nu_u)^2}{9\mu(1 - \nu_u)(\nu_u - \nu)}$$
(19)

where  $t_0$  is the lapse time since the exposure of the fracture surface to the fluid,  $\kappa$  is intrinsic permeability, G is shear modulus, B is Skempton's B coefficient, and c is the diffusivity coefficient. It has been demonstrated that the time scale of the diffusional process in poroelasticity is controlled by the diffusivity coefficient (Green & Wang 1990; Cheng  $et\ al.\ 1993$ ). The effects of fluid properties can be demonstrated by the parameters  $\mu$ , B,  $K_\beta$ , c,  $\rho_f$  in these equations.

A multiphase flow condition arises if the injected fluid is different from the pore fluid, and new equations such as the Buckley-Leverett equation may be introduced (Pinder & Gray 2008), which is beyond the scope of this paper.

### NUMERICAL SIMULATION

In this paper, calculations were carried out using the software platform Abaqus, a finite element code with a cohesive element function. Abaqus is also capable of simulating poroelasticity problems where the drained bulk moduli of both solid matrix and saturated pore fluid are dependent on the pore pressure (Schoenball *et al.* 2010).

# The model for evaluating fracture formation and propagation

Figure 5 shows the discretized domain area of  $100 \times 100$  m. The cohesive finite element is generally taken as a very thin layer (on the order of 0.1 mm or even less). The element spacing adjacent to a cohesive element should also be very fine in order to accurately simulate the

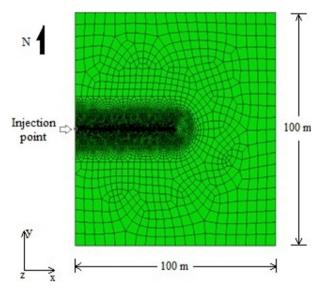


Fig. 5. Mesh layout of the model.

fracture propagation profile. Consequently, an extremely large number of elements are required for a model of significant size because of the intention to also consider the far-field effects. Eight nodes are required for a normal cubic element, and for a cohesive element, 12 nodes are required because four nodes are needed in the middle for the fluid flow calculation. The z-dimension thickness of the model is 1 m. The cohesive zone representing the predefined path of the fracture is 50 m long and the mesh in that region is very fine. Close to the cohesive zone, meshes with similar sizes are preferable as they can minimize mesh-induced dispersion effects in stress wave propagation (Falk *et al.* 2001). The input parameters for the model are listed in Table 1.

The simulated rock possesses the mechanical properties of Indiana limestone, which is mainly composed of calcite (98%); thus, the bulk modulus of the solid part was determined to be 74 GPa (Hart & Wang 1995). Fluid A and Fluid C resemble water and supercritical CO<sub>2</sub>, respectively; Fluid B is an artificial fluid with a property between these end members, which may be considered a mixture of A and C. Even a multiphase (or two phase) flow condition is beyond the scope of this paper, we expect this fluid can provide further understanding of the behavior of intermediate fluids (between water and supercritical CO<sub>2</sub>-like fluid) on the pore pressure distribution and fracture propagation.

Three parameters are required in Abaqus to represent a pore fluid: specific weight (density), bulk modulus and

Table 1 Input parameters for the numerical model.

Rock properties	
Variable	Value
Density (kg m $^{-3}$ ) $\rho$	2600
Young's modulus (GPa) E	33
Poisson ratio v	0.26
Grain bulk modulus (GPa) Ks	74
Void ratio $e$ ( $e = n/(1-n)$ , $n$ is porosity)	0.14

# Pore fluid properties

Variable	Fluid A	Fluid B	Fluid C
Density (kg m <sup>-3</sup> ) $\rho_f$	1000	880	660
Bulk modulus (GPa) $K_f$	2.2	0.22	0.058
Viscosity (cp) $\mu$	1.0	0.30	0.06
Phase 1			
Hydraulic conductivity (m s $^{-1}$ ) $k$	2.40E-8	2.40E-8	2.40E-8
Leak-off coefficient (m $s^{-1}$ ) C	5.80E-10	5.80E-10	5.80E-10
Phase 2			
Hydraulic conductivity (m s $^{-1}$ ) $k$	2.18E-8	6.40E-8	2.40E-7
Leak-off coefficient (m s $^{-1}$ ) C	5.80E-10	1.93E-9	9.67E-9

In-situ stress field	
Maximum, $\sigma_H$ (MPa) (x-axis)	23.8
Intermediate, $\sigma_v$ (MPa) (z-axis)	21.8
Minimum, $\sigma_h$ (MPa) (y-axis)	17.8
Field pore pressure (MPa)	8.8

viscosity. For supercritical CO2, these parameters will vary with temperature and pressure (Law & Bachu 1996; Span & Wagner 1996). The bulk modulus (0.058 GPa) and density (660 kg m<sup>-3</sup>) of CO<sub>2</sub> in its supercritical condition (>7.4 MPa and >31.1°C) are much smaller than that of water under similar conditions. Such a temperature and pressure condition generally implies a minimum depth of 800 m to 1000 m in a sedimentary basin. Thus, an initial in-situ stress appropriate to a depth of about 900 m is used here, with the intermediate stress estimated on the basis of the weight of the overburden. The in-situ stress regime is typically a strike-slip regime  $(\sigma_H > \sigma_v > \sigma_h)$  for a cratonic basin such as the Williston basin or the Illinois basin (Zoback & Zoback 1980). Fractures in such basins at great depths are generally developed vertically and perpendicular to the minimum stress (Begnaud & Claiborne 1985), in which a plane strain condition may apply (or at least to some degree). Knowledge of the in-situ stress field is important, as the propagation axes of subsurface hydraulic fractures can be predicted on this basis (Bell & Grasby 2011).

Hydraulically induced fractures may be more likely to involve multiphase flows, with the injected fluid different from the in-situ pore fluid. To avoid the difficulty of handling a multiphase flow problem, we only consider cases with injected fluid similar to the in-situ pore fluid. In fact, the in-situ fluid and injected fluid will tend to become more alike after a period of injection, especially in the region close to the injection well. The normal traction and shear tractions in the cohesive zone were assigned to be 7.0 GPa and 8.0 GPa for all cases. The injection rate was kept at  $1.50 \times 10^{-4}$  m $^3$  s $^{-1}$  and the injection time lasted for a total of 450 seconds.

Other parameters influenced by fluid properties are hydraulic conductivity and leak-off coefficient. Hydraulic fracture propagation behavior is very sensitive to these two parameters. To evaluate the importance of fluid compressibility (or fluid bulk modulus), hydraulic conductivity and leak-off coefficient, we conduct two phases of tests. In the Phase 1 test, hydraulic conductivity and leak-off coefficient are assigned similar values for all the three cases; thus the fracture propagation behavior will be mainly influenced by the fluid compressibility. We further assume that the permeable layers adjacent to fracture boundaries and the porous formation have the same hydraulic characteristics with respect to all fluids.

In the Phase 2 test, the effects of viscosity on hydraulic conductivity and leak-off coefficient are taken into account. Differences due to the nature of the different fluids are fully captured at this stage. Assuming the intrinsic permeability of the rock is the same for all the cases, the hydraulic conductivities k to the fluids are related by:  $k_A\mu_A/\rho_A = k_B\mu_B/\rho_B = k_C\mu_C/\rho_C$ . Therefore, the hydraulic conductivities assigned to each fluid are proportioned based on these relationships. The fluid leak-off coefficient

is a very complicated parameter that is influenced by fluid viscosity, hydraulic conductivity, diffusivity, and even time (Warpinski 1991). Here, it is assumed that the leak-off coefficient is inversely proportional to the viscosity, instead of being a complicated function involving higher powers of the viscosity as in Eqn. 1, based on the assumption that the intrinsic permeability of the cohesive zone is the same for all the cases. Thus, the results can be considered as relatively conservative in the sense that the differences in behavior for different fluids are less than they could be. The input parameters for Fluid A are almost the same for Phase 1 and Phase 2, establishing a bridge for comparison between these two phases.

#### Phase 1 test results

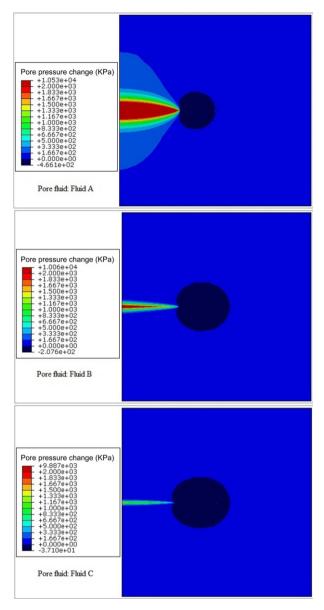
Figure 6 shows the contour maps of pore pressure changes after fluid injection for all three cases of the Phase 1 test. The impacts of fluid composition on the pore pressure fields are obvious. In each case, a region of pore pressure decline occurs ahead of the fracture tip, indicating rock dilation immediately before fracturing. The simulation using pore Fluid A (water) shows a much larger pressure disturbance than that with Fluid C (supercritical CO<sub>2</sub>) in terms of both magnitude and areal extent; Fluid B is intermediate.

Figure 7 shows pore pressure along the upper boundary of the created fracture; the lower boundary would be the same because of the symmetry. Pore pressure increases over time for all three cases. However, case A shows a much higher pore pressure level than B and C for all time steps. The pore pressures drop below the field pore pressure (88 MPa) at the fracture tip regions but finally converge to that pressure for all three cases. The regions of pore pressure decline correspond to rock dilations, and case A has the highest level of rock dilation.

Figure 8 shows the accumulated fluid leak-off volume for all three cases, and the results reveal that more compressive fluids (Fluid C) leak off more readily than less compressive fluids. The leak-off potential for fluid with a larger bulk modulus (such as Fluid A) is considerably lower, even when a higher pore pressure gradient exists in the field.

Figures 9–11 show fracture propagation curves for all three Phase 1 cases. The fracture lengths grow with injection time for each case; however, the fracture openings increase only at earlier times and then tend to stabilize or even experience a minor reduction at large injection times. These phenomena are more obvious for thin fluids, such as Fluids B and C. Fracture tip advancing rates are almost constant for Fluid A and B, but show a gradual slowing trend for the very thin fluid (Fluid C).

Figure 12 shows the fracture opening curves as measured along the upper boundaries for all three cases at the end of the simulation period (t = 450 s). The fracture



**Fig. 6.** Contour maps of simulated pore pressure changes after fluid injection for a similar injection rate and period for three different pore fluids (Phase 1 test).

associated with Fluid A has the largest crack opening and the longest propagation path under a similar injection flow rate and time (thus total injection quantity). Because less fluid has leaked off into the surrounding formation from the fracture for case A, more fluid is retained within the fracture to create a thicker and larger fracture. Over time, this differential behavior would become even more pronounced.

#### Phase 2 test results

The effect of fluid viscosity on hydraulic conductivity and leak-off coefficient are also taken into account in the Phase

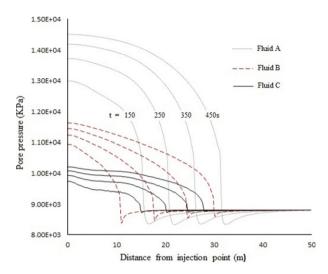


Fig. 7. Pore pressure measured along the upper boundary of the fracture (Phase 1 test).

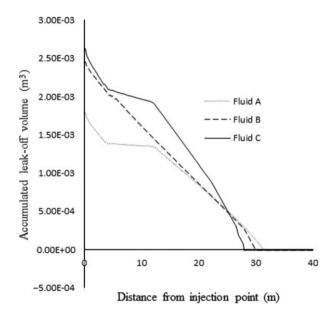


Fig. 8. Accumulated fluid leak-off volume for all cases (Phase 1 test).

2 test. Thus, Fluid C differs more from Fluid A, and the difference approaches the actual difference between water and supercritical CO<sub>2</sub>. Figure 13 shows the contour maps of pore pressure changes after fluid injection for all three cases for the Phase 2 test. The impacts of pore fluids on the pressure fields are even more pronounced (Compare with Fig. 6). The differences in terms of fracture length are large, particularly for Fluid C, which exhibits an extremely short fracture. In addition, the rock dilation regions differ, especially in the case of Fluid C.

Figure 14 shows pore pressure measured along the upper boundary of the created fractures. The pore pressure behaviors depicted in this figure are very different from

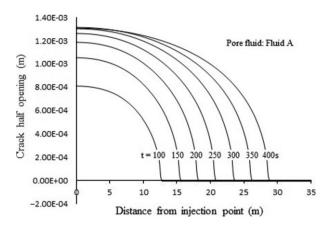


Fig. 9. Fracture propagation curves at quasi-static stages for Fluid A at different times (Phase 1 test).

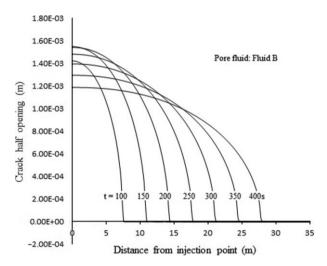


Fig. 10. Fracture propagation curves at quasi-static stages for Fluid B at different times (Phase 1 test).

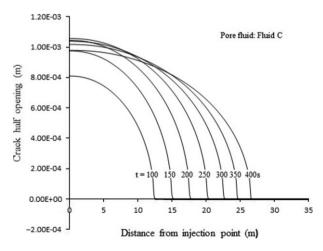


Fig. 11. Fracture propagation curves at quasi-static stages for Fluid C at different times (Phase 1 test).

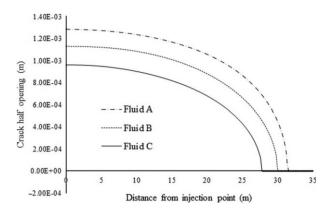


Fig. 12. Fracture opening curve as measured along upper boundaries for all the cases (Phase 1 test).

those of Figure 7, particularly for Fluids B and C. Curves for case C and case B at late times are clustered, indicating the stagnation of fracturing for these fluids.

Figure 15 shows accumulated fluid leak-off volumes for all the three cases for the Phase 2 test and reveals extremely large differences in leak-off conditions. The fracture associated with Fluid C is very short, while the leak-off is very high; and fracture associated with Fluid A is very long, while the leak-off is very low. The curves in Fig. 8 are all similar to the curve for Fluid A in Fig. 15, and the differences seen in Fig. 8 are minor in comparison to those between Figs 8 and 15. The fracture associated with Fluid C is clearly in a leak-off dominated regime. The effects of fluid viscosity are much stronger than those of fluid compressibility and can even mask the effects of the latter if tests were not conducted in two separate phases.

Figure 16 shows fracture propagation curves for all three cases for times from 50 s to 450 s. The fracture propagation behaviors associated with different fluids are very different in terms of fracture lengths, openings and propagation rates. To capture the fracture propagation behavior more clearly, Fig. 17 shows the changes of fracture lengths and openings over time.

For all three cases, both fracture lengths and openings increased during early time. This phenomenon has also been demonstrated by previous work (e.g., Bunger et al. 2005; Chen et al. 2009; Chen 2012). However, a fracture in a porous medium cannot be continuously propagated by an injection of a constant flow rate, nor can it be continuously opened by constant injection. A balancing point is reached in which the incoming fluids are completely leaked off into the adjacent porous medium, so that no fluid is left to propagate the fracture further. This phenomenon may not be captured if the test is too short and/or the domain is not large enough. There are actually two key time points; one at which a fracture ceases opening and the other at which a fracture stops extending. For all the cases simulated here, the fracture opening stops before

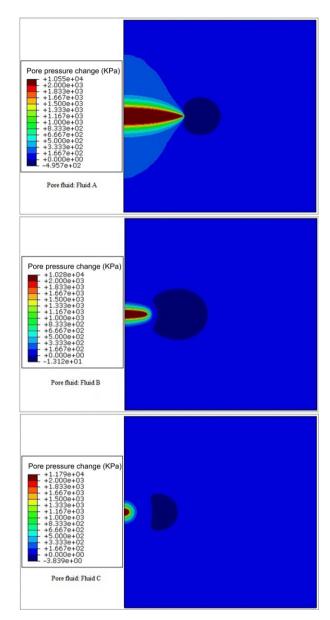


Fig. 13. Contour maps of pore pressure changes after fluid injection for three different fluids under a similar injection rate and period (Phase 2 test).

fracture propagation. Fracture propagation rates are very different for all the cases, with much slower rates for thin fluids.

In the Phase 1 test, the time at which fracture opening ceases was reached for all three cases, but the time at which fracture propagation ends was not reached for any of the cases. In the Phase 2 test, the time at which fracture opening ceases was reached for all three cases, and the time at which fracture propagation ends was reached for cases B and C, but not for A. The fracture stops opening at very early times for thin fluids (50 s for Fluid C) and fracture propagation stops after 100s, with only a minor fluctuation of fracture openings at large times. For Fluid B, the

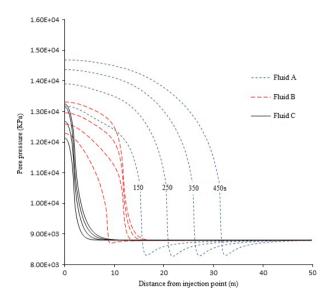


Fig. 14. Pore pressures measured along the upper boundary of the fracture (Phase 2 test).

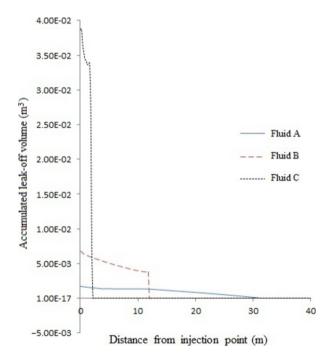


Fig. 15. Accumulated fluid leak-off volume for all the cases (Phase 2 test).

fracture stops opening after about 100s and stops propagating after about 200s. For a relatively thick fluid, such as Fluid A, the time at which the fracture ceases to open is about 300s, but the time at which fracture propagation ceases was not reached within 450s.

# **DISCUSSION AND CONCLUDING REMARKS**

The crust behaves not as a dry medium but as a multiphase fluid-saturated porous medium (Roeloffs 1996). Fluid-

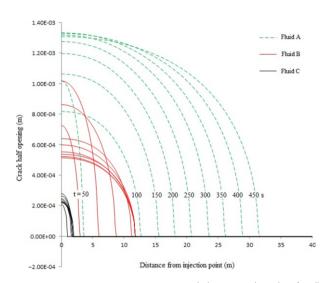


Fig. 16. Fracture opening curves as measured along upper boundary for all three cases at different times (Phase 2 test).

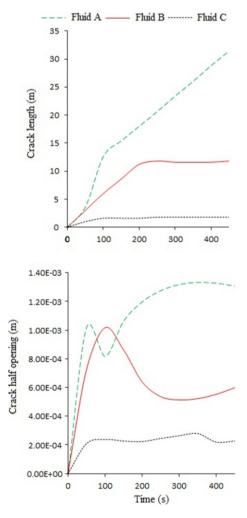


Fig. 17. Fracture length and opening as a function of time (Phase 2 test).

induced fracture propagation is essentially a problem of fluid–structure interaction. The type of fluid is important not only because the fluid that must fracture the rock, but also because rocks saturated with different pore fluids behave differently (Zhou & Burbey 2012). Therefore, when modeling the hydraulic fracturing process, one must account for the mechanics of the various fluids, as well as the mechanics of the rock, and their interaction (Sousa et al. 1993).

Hydraulically induced fractures are controlled to a large degree by the depth of penetration of the fracture system. Loss of fluid to the formation adjacent the fracture governs the fracture extent, which depends on the fluid viscosity and the permeability of the formation relative to the fracturing fluid, wall-building properties, and compressibility of the reservoir fluid (Howard & Fast 1957). The wall-building is envisioned as a continuous buildup of a thin layer (the filter cake) which manifests an ever increasing resistance to flow through the fracture face during fluid injection (Valko & Ecomomides 1995). Effective stress field variations due to fluid injection depend on diffusion through the poroelastic rock mass as well as diffusion in preferential directions or through fresh shear zones or other hydraulically induced fractures (Cornet 2012).

Crack openings are essentially controlled by fluid pressure declines in the fracture, as well as fluid leak-off potential if the formation is porous. Operating conditions which cause high pressure declines along the crack (such as a high injection rate and highly viscous fluids) will result in relatively wide cracks. Conversely, conditions that cause low pressure declines (low injection rates and thin fluids) will result in relatively narrow cracks (Perkins & Kern 1961). Decreased viscosity can lead to undesirable flow characteristics. It has been shown that the use of a non-Newtonian hydraulic fracturing fluid may change the velocity of hydraulic fracture crack propagation (Tagirova 2009). The opening of a fracture is a transient phenomenon and undrained conditions apply, that is, the injected fluid will 'instantly' occupy the entire fracture and we can expect 100% saturation of a thin fracture with the injected fluid if this fracture is freshly initiated.

We studied the influence of fluid properties on fracture propagation behavior by using the cohesive zone model in conjunction with a poroelasticity model. We simulate fracture propagation due to the effects of a thin fluid having the properties of supercritical CO<sub>2</sub> by conducting two phases of numerical tests, with a normal fluid (water) as the basis for comparison. Our findings can be summarized as follows:

(1) A pore fluid is characterized in terms of its compressibility and viscosity, and both of these parameters have impacts on the behavior of fracture propagation. However, fluid viscosity is the most significant property, as it greatly affects the hydraulic conductivity and

- leak-off coefficient. The effect of viscosity can dominate and mask the effect of compressibility in numerical tests
- (2) Relatively large time periods and spatial domains are required to capture the hydraulically induced fracture propagation behavior. Two important times have been identified during a fracturing process in a porous medium: the time at which a crack ceases to open further, and the time at which a crack ceases propagating, with the former occurring before the latter for all tested cases.
- (3) The pore pressure fields are very different for different fluids even when the initial field conditions and injection schemes (rate and time) are the same. Thin fluids will create thinner and much shorter fractures relative to thick fluids. This agrees with laboratory observations that viscous fluids tend to generate thick cracks and thin fluids tend to generate thin cracks. This result agrees with field observations that injected CO<sub>2</sub> may not even fracture the formation if the injection rate is not high enough.
- (4) Crack propagation rates associated with thick fluids are much higher than those associated with thin fluids, and these rates can only be considered constant within intermediate time ranges. The rate is a quasi-logarithmic type function of time, with an initial sharp increase followed by level-off at large times. The crack width can fluctuate after the initial opening stage, and the opening of a fracture by a thin fluid tends to be less stable than one created by a thick fluid.

Fluid properties have significant impact on the behavior of fracture propagation in porous media, and the differences in fracture opening and propagation associated with different fluids can be extremely large. The very short fractures associated with thin fluids do not necessarily mean that the fracturing is inconsequential, because the rock dilation region is far from the crack tip (Fig. 13). This suggests that an abnormal pressure front can advance far ahead of an obvious crack. The actual fractures created by thin fluids can be extremely narrow. Further research is needed in this area, as the impact of fluid properties is also complicated by chemo-thermo-hydro-mechanical coupling.

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NOMENCLATURE		
C	diffusivity coefficient	
е	void ratio of rock formation $(e = n/(1-n))$	
h	hydraulic head	
1	fracture length as measured from injection point	
	to fracture tip	
k	hydraulic conductivity	
$m_f/\Delta m_f$	fluid mass/fluid mass change	
n	porosity of rock formation	
$p_{\infty}$	field pore pressure: pore pressure with enough	
	distance from the fracture thus can be	
	considered as a reference state without the	
	disturbance of fluid injection.	
$p_b$	pore pressure on the fracture boundary	
$p_c$	pore pressure on the fracture center line	
$p_i$	fluid injection pressure	
q	fracturing fluid flow inside the fracture	
$q_T$	fracturing fluid tangential flow inside the fracture	
<i>a</i>	fracturing fluid normal flow inside the fracture	
$q_N \ t/t_0$	time/lapse time since the exposure of the	
ν/ ν0	fracture surface to the fluid	
$t_n/t_s$	normal traction/shear traction	
$v_l$	Leak-off velocity	
w/w(x,t)	•	
. ( ) /	position and time during fluid injection	
B	Skempton's B coefficient (the ratio of the	
	induced pore pressure to the change in	
	confining stress under undrained condition)	
C/C'	leak-off coefficient/dimensionless leak-off	
	coefficient	
E	Young's modulus (stiffness of rock)	
E'	dimensionless Young's modulus	
G	shear modulus (the ratio of shear stress to shear	
0	strain)	
$G_c$	cohesive energy	
K'	dimensionless toughness	
$K_{IC}$	fracture toughness (resistance offered by material	
K	against crack propagation) bulk modulus (the ratio of stress and volumetric	
K	strain at constant pore pressure, and $1/K$ is the	
	compressibility of the material)	
$K_s$	solid grain's bulk modulus (the ratio of	
3	confining stress and volumetric strain, $K_s = K$	
	for material without pores)	
$1/K_n$	unjacketed pore compressibility $(K_n)$ : the	

unjacketed pore bulk modulus) (change in pore

volume over pore pressure change with confining

pressure required to track with the pore pressure)

pore fluid bulk modulus (definition is the same

to *K* but with respect to fluid)

 $Q(t)\delta(x,y)$  local fluid flux in a fracture

injection rate

 $K_f$ 

 $Q_0$ 

$S_s$	specific storage coefficient (a correlation between
	stored fluid mass and pore pressure).
$T/T_{max}$	traction tensor/the maximum
$V_{inject}$	injected fluid volume
$V_{inject}$	volume of the injected fluid stored in the crack
$V_{leak}$	volume of the injected fluid leaked into the
	porous formation
α	compressibility of the formation along the
	vertical direction.
$\delta_{ij}$	Kronecker delta
$oldsymbol{arepsilon}_{ij}$	strain tensor
η	an intermediate poroelastic parameter as defined
	by Eqn. 13.
$\kappa$	intrinsic permeability
$\mu$	fluid viscosity
$v/v_u$	drained Poisson's ratio/undrained Poisson's
	ratio
ρ	bulk density
$ ho_f$	fluid density
$\sigma_0/\sigma_{ij}$	confining stress/confining stress tensor
$\psi$	cohesive potential function
$\Omega/\Omega_f$	displacement jump across a pair of cohesive
	surfaces/the critical separation at complete
	failure of cohesive zone

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