Lecture 7: The Substantial Derivative and Conservation of Momentum

ENAE311H Aerodynamics I

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QUIZ

5.11 At cruise conditions, air flows into a jet engine at a steady rate of 65 lbm/s. Fuel enters the engine at a steady rate of 0.60 lbm/s. The average velocity of the exhaust gases is 1500 ft/s relative to the engine. If the engine exhaust effective cross section area is 3.5 ft², estimate the density of the exhaust gases in lbm/ft³.

The substantial derivative

Consider again the differential form of the continuity equation:

 $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0.$

We can expand out the second term to give:

$$\nabla \cdot (\rho \mathbf{v}) = \mathbf{v} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{v}$$

Our original equation thus becomes

$$\frac{\partial \rho}{\partial t} + \mathbf{v} \cdot \nabla \rho = -\rho \nabla \cdot \mathbf{v}$$

We can expand out the LHS to give

$$\frac{\partial \rho}{\partial t} + v_x \frac{\partial \rho}{\partial x} + v_y \frac{\partial \rho}{\partial y} + v_z \frac{\partial \rho}{\partial z} \equiv \frac{D\rho}{Dt}.$$

The derivative D/Dt is known as the total, substantial, or material derivative. It describes the rate of change of a property of a fluid element moving with the flow.

To see this, imagine we have a fluid element of density ρ , at position (x, y, z) at time t, i.e., $\rho(x, y, z, t)$.

At time $t + \Delta t$, it will have moved to $(x + \Delta x, y + \Delta y, z + \Delta z)$ and its density will be:

$$\rho|_{t+\Delta t} = \rho(x + \Delta x, y + \Delta y, z + \Delta z, t + \Delta t)$$

$$= \rho(x, y, z, t) + \frac{\partial \rho}{\partial x} dx + \frac{\partial \rho}{\partial y} dy + \frac{\partial \rho}{\partial z} dz + \frac{\partial \rho}{\partial t} dt$$

+H.O.T.

The change in density is then

$$d\rho = \frac{\partial \rho}{\partial x}dx + \frac{\partial \rho}{\partial y}dy + \frac{\partial \rho}{\partial z}dz + \frac{\partial \rho}{\partial t}dt$$

and thus

$$\frac{d\rho}{dt} = \frac{\partial\rho}{\partial x}\frac{dx}{dt} + \frac{\partial\rho}{\partial y}\frac{dy}{dt} + \frac{\partial\rho}{\partial z}\frac{dz}{dt} + \frac{\partial\rho}{\partial t}$$

$$= v_x\frac{\partial\rho}{\partial x} + v_y\frac{\partial\rho}{\partial y} + v_z\frac{\partial\rho}{\partial z} + \frac{\partial\rho}{\partial t}$$

$$= \frac{D\rho}{Dt}.$$
 Applies to any intrinsic property of the flow!

Conservation of momentum

Let us return now to the Reynolds Transport Theorem:

$$\frac{dN_s}{dt} = \frac{\partial}{\partial t} \iiint_{CV} \eta \rho dV + \iint_{CS} \eta \rho \mathbf{v} \cdot \mathbf{dA},$$

Let us now consider the case of $N_s = P$, i.e., the momentum of the fluid system. We have seen already that the corresponding intensive variable is the fluid velocity, i.e, $\eta = v$.

From Newton's second law, the rate of change of momentum is equal to the sum of applied forces, i.e.,

$$\frac{d\mathbf{P_s}}{dt} = \sum \mathbf{F}$$

Applying the RTT, we thus have

$$\frac{\partial}{\partial t} \iiint_{CV} \rho \mathbf{v} dV + \iint_{CS} \mathbf{v} (\rho \mathbf{v} \cdot \mathbf{dA}) = \sum \mathbf{F}$$
Rate of change of Net momentum Applied forces momentum flux through CV within CV boundaries

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Note that this is a vector equation with three components. The x-component, for example, is

$$\frac{\partial}{\partial t} \iiint_{CV} \rho v_x dV + \iint_{CS} v_x \rho \mathbf{v} \cdot \mathbf{dA} = \sum F_x$$

Conservation of momentum (integral form)

The forces relevant here are of two types:

1. Surface forces (pressure and shear stress), for which we can write

$$\sum \mathbf{F_s} = -\iint_{CS} p \mathbf{dA} + \iint_{CS} \bar{\bar{\tau}} \cdot \mathbf{dA}$$

2. The gravity body force:

$$\sum \mathbf{F_b} = \iiint_{CV} \rho \mathbf{f} \, dV,$$

where $f = -g\hat{j}$ is the gravitational acceleration (assumed in the y direction).

Substituting into the momentum equation, we have

inviscid gravity negligible
$$\frac{\partial}{\partial t} \iiint_{CV} \rho \mathbf{v} dV + \iint_{CS} \mathbf{v} (\rho \mathbf{v} \cdot \mathbf{dA}) = -\iint_{CS} p \mathbf{dA} + \iiint_{CS} \bar{\tau} \cdot \mathbf{dA} + \iiint_{CV} \rho \mathbf{f} dV$$

Or, in x-direction (inviscid, no body force):

$$\frac{\partial}{\partial t} \iiint_{CV} \rho v_x dV + \iint_{CS} \rho v_x (\mathbf{v} \cdot \mathbf{dA}) = -\iint_{CS} p dA_x$$

Conservation of momentum (differential form)

We can derive a corresponding differential form by using similar arguments as in the continuity case.

Since the CV is spatially fixed, we have

$$\frac{\partial}{\partial t} \iiint_{CV} \rho \mathbf{v} dV = \iiint_{CV} \frac{\partial}{\partial t} (\rho \mathbf{v}) dV.$$

From the divergence theorem:

$$\iint_{CS} \mathbf{v}(\rho \mathbf{v} \cdot \mathbf{dA}) = \iiint_{CV} \nabla \cdot (\rho \mathbf{v} \mathbf{v}) dV$$
$$\iint_{CS} \bar{\bar{\tau}} \cdot \mathbf{dA} = \iiint_{CV} \nabla \cdot \bar{\bar{\tau}} dV,$$

And from the gradient theorem:

$$\iint_{CS} p \mathbf{dA} = \iiint_{CV} \nabla p dV.$$

Substituting into the integral momentum equation:

$$\iiint_{CV} \left[\frac{\partial}{\partial t} (\rho \mathbf{v}) + \nabla \cdot (\rho \mathbf{v} \mathbf{v}) + \nabla p - \nabla \cdot \bar{\bar{\tau}} - \rho \mathbf{f} \right] dV = 0.$$

We argue, as before, that since the CV is arbitrary, the term in [] must be identically zero, i.e.,

$$\frac{\partial}{\partial t}(\rho \mathbf{v}) + \nabla \cdot (\rho \mathbf{v} \mathbf{v}) + \nabla p - \nabla \cdot \bar{\bar{\tau}} - \rho \mathbf{f} = 0.$$

A more useful form of this results if we expand the first two terms and use the continuity equation:

$$\left[\rho \frac{\partial \mathbf{v}}{\partial t} + \rho(\mathbf{v} \cdot \nabla)\mathbf{v} + \nabla p - \nabla \cdot \bar{\bar{\tau}} - \rho \mathbf{f} = 0.\right]$$

Or alternatively

$$\rho \frac{D\mathbf{v}}{Dt} + \nabla p - \nabla \cdot \bar{\bar{\tau}} - \rho \mathbf{f} = 0.$$

Conservation of momentum (differential form)

We can derive a corresponding differential form by using similar arguments as in the continuity case.

Often we will have the case that the flow is (approximately) inviscid and the body forces are negligible, in which case these equations simplify to:

$$\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla)\mathbf{v} + \frac{1}{\rho}\nabla p = 0$$

and

$$\frac{D\mathbf{v}}{Dt} + \frac{1}{\rho}\nabla p = 0$$

The x-component of this equation is

$$\frac{\partial v_x}{\partial t} + (\mathbf{v} \cdot \nabla)v_x + \frac{1}{\rho} \frac{\partial p}{\partial x} = 0$$

or

$$\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} + \frac{1}{\rho} \frac{\partial p}{\partial x} = 0.$$

Substituting into the integral momentum equation:

$$\iiint_{CV} \left[\frac{\partial}{\partial t} (\rho \mathbf{v}) + \nabla \cdot (\rho \mathbf{v} \mathbf{v}) + \nabla p - \nabla \cdot \bar{\bar{\tau}} - \rho \mathbf{f} \right] dV = 0.$$

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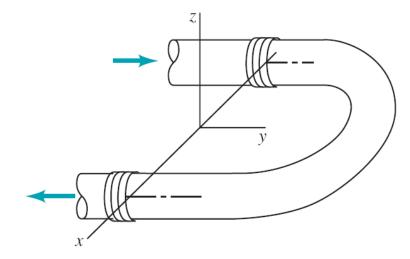
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Or alternatively

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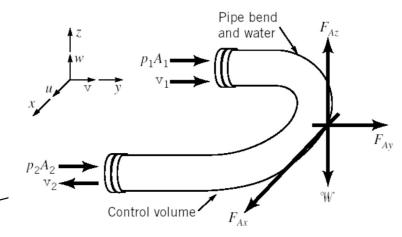
5.28 Water flows through a horizontal, 180° pipe bend as is illustrated in Fig. P5.28. The flow cross section area is constant at a value of 9000 mm^2 . The flow velocity everywhere in the bend is 15 m/s. The pressures at the entrance and exit of the bend are 210 and 165 kPa, respectively. Calculate the horizontal (x and y) components of the anchoring force needed to hold the bend in place.



5.28 Water flows through a horizontal, 180° pipe bend as is illustrated in Fig. P5.28. The flow cross section area is constant at a value of 9000 mm². The flow velocity everywhere in the bend is 15 m/s. The pressures at the entrance and exit of the bend are 210 and 165 kPa, respectively. Calculate the horizontal (x and y) components of the anchoring force needed to hold the bend in place.



Step. 2 Find all forces acting on the CV (Free-body diagram)



 $n_1 \cdot v_1 < 0$

 n_1

Then,
$$\frac{\partial}{\partial t} \int_{CV} \vec{V} \rho dV + \int_{CS} \vec{V} \rho \vec{V} \cdot \hat{n} dA = \sum_{i} \vec{F}_{CV}$$
 (Steady flow) at the side wall

1.
$$x - \text{comp.}: \int_{CS} u \rho \vec{V} \cdot \hat{n} dA = \int_{(1)} u_1 \rho \vec{V} \cdot \hat{n} dA + \int_{\text{Side}} u \rho \vec{V} \cdot \hat{n} dA + \int_{(2)} u_2 \rho \vec{V} \cdot \hat{n} dA = F_{Ax}$$

No x component of fluid velocity at sections (1) and (2), $(u_1 = u_2 = 0)$

$$\therefore \int_{CS} u \rho \vec{V} \cdot \hat{n} dA = F_{Ax} = 0$$

2.
$$y - \text{comp.}: \int_{CS} v \rho \vec{V} \cdot \hat{n} dA = v_1 \int_{(1)} \rho \vec{V} \cdot \hat{n} dA + v_2 \int_{(2)} \rho \vec{V} \cdot \hat{n} dA = F_{Ay} + p_1 A_1 + p_2 A_2$$

or
$$(v_1)(-\dot{m}_1) + (-v_2)(\dot{m}_2) = F_{Ay} + p_1 A_1 + p_2 A_2$$

$$\therefore F_{Ay} = -\dot{m}(v_1 + v_2) - p_1 A_1 - p_2 A_2$$

$$\rho \vec{V} \cdot \hat{n} dA = v_1 \int_{(1)} \rho \vec{V} \cdot \hat{n} dA + v_2 \int_{(2)} \rho \vec{V} \cdot \hat{n} dA = F_{Ay} + p_1 A_1 + p_2 A_2$$

$$(v_1)(-\dot{m}_1) + (-v_2)(\dot{m}_2) = F_{Ay} + p_1 A_1 + p_2 A_2$$

$$v_2$$

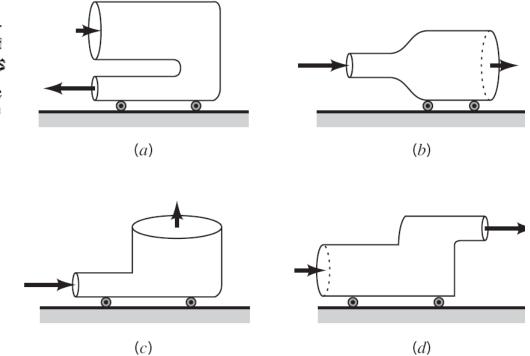
$$v_1$$

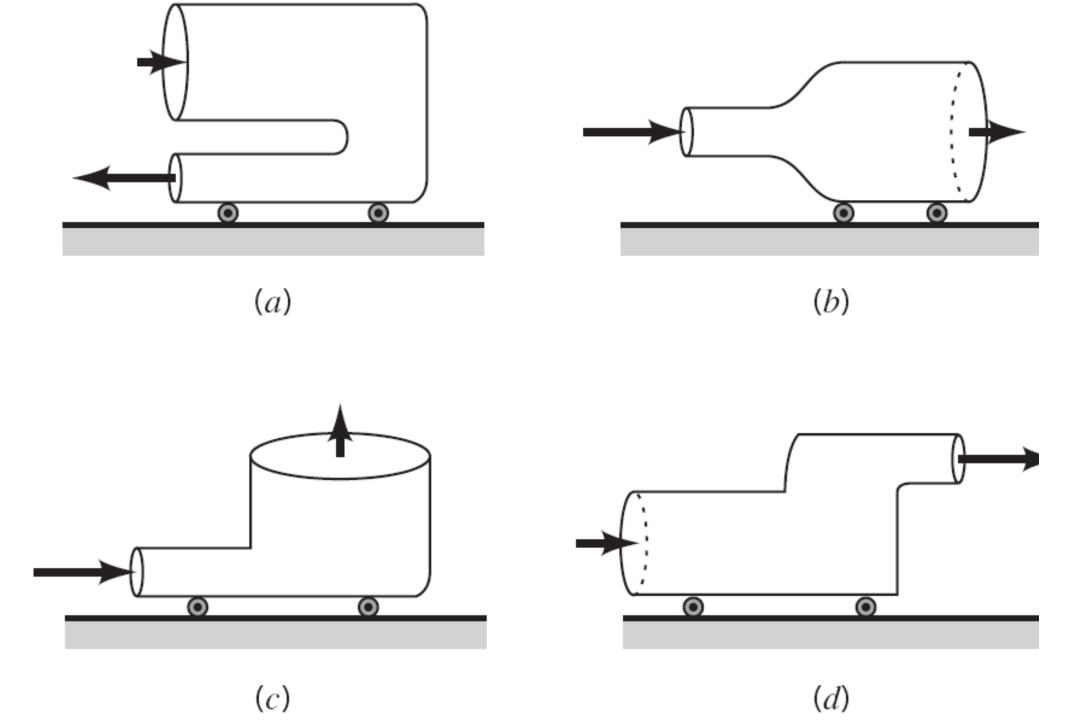
$$F_{Ay} = -\dot{m}(v_1 + v_2) - p_1 A_1 - p_2 A_2$$

where
$$\dot{m} = \rho A_1 v_1 = (1.94)(0.1)(50) = 9.70 \text{ slug/s}$$

 $p_1 = 30 \text{ psia}$, $p_2 = 24 \text{ psia}$, and $A_1 = A_2 = 0.1 \text{ ft}^2 (144 \text{ in}^2 / \text{ft}^2) = 14.4 \text{ in}^2$

5.58 The four devices shown in Fig. P5.58 rest on friction-less wheels, are restricted to move in the x direction only and are initially held stationary. The pressure at the inlets and outlets of each is atmospheric, and the flow is incompressible. The contents of each device is not known. When released, which devices will move to the right and which to the left? Explain.

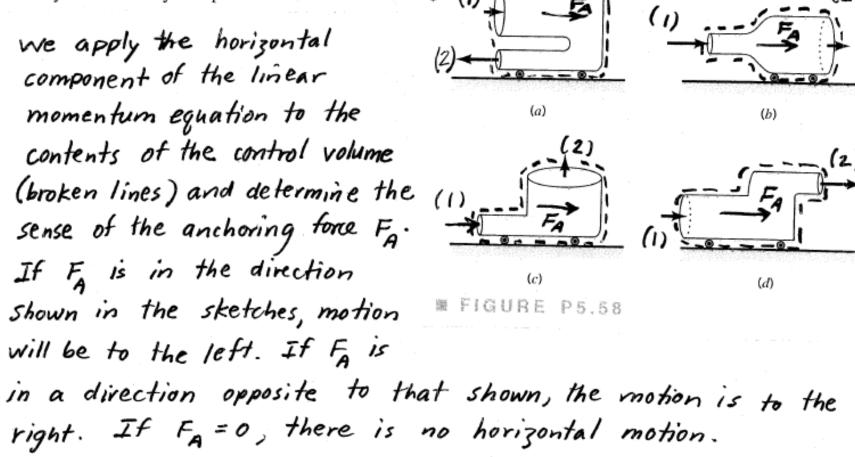




5.58 The four devices shown in Fig. P5.58 rest on frictionless wheels, are restricted to move in the x direction only and are initially held stationary. The pressure at the inlets and outlet\$

For sketch(a)

The four devices shown in Fig. P5.58 rest on frictionelse are restricted to move in the x direction only and



-V, QV, A, - V_2 QV, $A_2 = F_A$ Since F_A is to the left, motion is to the right.

For sketch (6)

-V,PV,A, + SPSA = F and from conservation of mass PV,A, = PV2 A3

and since v, > v, then Fa is to the left and motion is to the right. For sketch (c) (note: flow is into cvat (1)

- VPV, A. = F and Fo is to the left so motion is to the right.

For sketch (d)

- V, PV, A + V2 PV, A, = FA and from conservation of mass PV, A, = PV2 A2

and $V_1 < V_2$

so Fo is to the right and motion is to the left.

5.36 The thrust developed to propel the jet ski shown in Video V9.7 and Fig. P5.36 is a result of water pumped through the vehicle and exiting as a high-speed water jet. For the conditions shown in the figure, what flowrate is needed to produce a 300-lb thrust? Assume the inlet and outlet jets of water are free jets.



For the control volume indicated the x-component of the momentum equation

$$\int_{CS} u \rho \vec{V} \cdot \hat{n} dA = \sum_{x} F_{x} becomes$$

$$R_{x} = 300lb$$

$$V_{1} = 300lb$$

$$V_{1} = 300lb$$

$$V_{2} = 0$$

$$V_{30} = 0$$

$$V_{30} = 0$$

$$V_{30} = 0$$

$$V_{30} = 0$$

$$V_{2} = 0$$

$$V_{30} = 0$$

(1)
$$(V_1 \cos 30^\circ) \rho (-V_1) A_1 + V_2 \rho (+V_2) A_2 = R_X$$

where we have assumed that p=0 on the entire control surface and that the exiting water jet is horizontal.

With
$$\dot{m} = \rho A_1 V_1 = \rho A_2 V_2$$
 Eq. (1) becomes

$$R_{x} = \dot{m} (V_{2} - V_{1} \cos \theta) = \rho V_{1} A_{1} (V_{2} - V_{1} \cos 30^{\circ})$$
 (1)

$$V_2 = \frac{A_1 V_1}{A_2} = \frac{25 \text{ in.}^2}{\frac{T}{4} (3.5 \text{ in.})^2} V_1 = 2.60 \text{ V}_1$$
 (2)

By combining Eqs. (1) and (2):

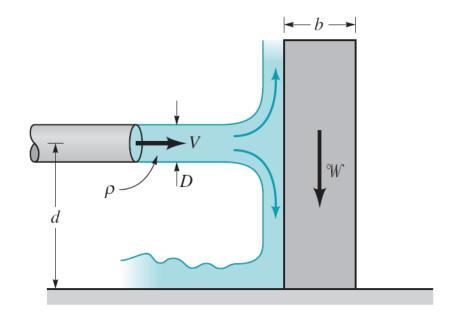
$$R_{x} = \rho V_{i}^{2} A_{i} (2.60 - \cos 30^{\circ})$$

or
$$V_1 = \left[\frac{300 \text{ /b}}{(1.94 \text{ slvgs})(\frac{25}{\text{ft}^3})(2.60 - \cos 30^\circ)} \right]^2 = 22.7 \frac{\text{ft}}{\text{s}}$$

Thus,

$$Q = A_1 V_1 = \left(\frac{25}{144} \text{ft}^2\right) (22.7 \frac{\text{ft}}{5}) = 3.94 \frac{\text{ft}^3}{5}$$

7.14 As shown in Fig. P7.14 and Video V5.4, a jet of liquid directed against a block can tip over the block. Assume that the velocity, V, needed to tip over the block is a function of the fluid density, ρ , the diameter of the jet, D, the weight of the block, W, the width of the block, b, and the distance, d, between the jet and the bottom of the block. (a) Determine a set of dimensionless parameters for this problem. Form the dimensionless parameters by inspection. (b) Use the momentum equation to determine an equation for V in terms of the other variables. (c) Compare the results of parts (a) and (b).



(a) $V = f(\rho, D, 2\omega, b, a)$

(a)
$$V = f(\rho, D, 20, b, d)$$

 $V = LT^{-1} \rho = FL^{-1}T^{2} D = L 20 = F b = L d = L$

(a)
$$V = f(\rho, D, 20, b, d)$$
 $V = LT^{-1} \rho = FL^{-4}T^{2} D = L 20 = Fb = L d = L$

From the ρ i theorem, $b-3=3$ ρ i terms regulared.

By inspection for $t1$, (containing V)

 $t1 = VDVP = (LT^{-1})(L)(VFL^{-4}T^{2}) = F^{0}L^{0}T^{0}$

(a)
$$V = f(\rho, D, 2\omega, b, d)$$
 $V = LT^{-1} \quad \rho = FL^{-4}T^2 \quad D = L \quad 2\omega = F \quad b = L \quad d = L$

From the pi theorem, $b - 3 = 3$ pi terms required.

By inspection for ti, (containing V)

 $TT_i = VDVP' = (LT^{-1})(L)(\sqrt{FL^{-4}T^2}) = F^0L^0T^0$

Check using MLT:

 $VDVP' = (LT^{-1})(L)(\sqrt{ML^{-3}}) = M^0L^0T^0$: OK

(a)
$$V = f(\rho, D, 2\omega, b, d)$$
 $V = LT^{-1} \rho = FL^{-4}T^{2} D = L 2\omega = F b = L d = L$

From the pi theorem, $b - 3 = 3$ pi terms required.

By inspection for π , (containing Y)

 $TT_{i} = VDVP_{2\omega} = (LT^{-1})(L)(\sqrt{FL^{-4}T^{2}}) = F^{0}L^{0}T^{0}$

Check using MLT :

 $VDVP_{2\omega} = (LT^{-1})(L)(\sqrt{ML^{-3}}) = M^{0}L^{0}T^{0} = 0$

For TT_{2} let

 $TT_{2} = \frac{b}{d}$

(a)
$$V = f(\rho, D, W, b, d)$$
 $V = LT^{-1} \quad \rho = FL^{-4}T^2 \quad D = L \quad W = F \quad b = L \quad d = L$

From the pi theorem, $b - 3 = 3$ pi terms required.

By inspection for Π_1 (containing V)

 $\Pi_1 = VD \mid P \mid = (LT^{-1})(L) \left(\sqrt{\frac{FL^{-4}T^2}{F}}\right) = F^0L^0T^0$

Check using MLT :

 $VD \mid P \mid = (LT^{-1})(L) \left(\sqrt{\frac{ML^{-3}}{FL}}\right) = M^0L^0T^0$: ok

For Π_2 let

 $\Pi_3 = \frac{d}{D}$

and

 $\Pi_3 = \frac{d}{D}$

(a)
$$V = f(\rho, D, 2W, b, d)$$
 $V = LT^{-1} \rho = FL^{-4}T^2 D = L 2W = F b = L d = L$

From the pi theorem, $b - 3 = 3$ pi terms required.

By inspection for TI , (containing V)

 $TI_1 = VDVL^2 = (LT^{-1})(L)(\sqrt{\frac{FL^{-4}T^2}{F}}) = F^0L^0T^0$

Check using $MLT:$
 $VDVL^2 = (LT^{-1})(L)(\sqrt{\frac{ML^{-3}}{KL}}) = M^0L^0T^0 : OK$

For TI_2 let

 $TI_2 = \frac{b}{d}$

and for TI_3
 $TI_3 = \frac{d}{D}$

and both TI_2 and TI_3 are obviously dimensionless.

Thus,

 $VDVL^2 = \frac{b}{d} \frac{d}{d} \frac{d}{D}$

(a)
$$V = f(\rho, D, W, b, d)$$
 $V = LT^{-1} \rho = FL^{-4}T^{-2} D = L W = F b = L d = L$

From the pi theorem, $b - 3 = 3$ pi terms required.

By inspection for TI , (containing V)

 $TI_1 = V D \sqrt{\frac{P}{2W}} = (LT^{-1})(L) \left(\sqrt{\frac{FL^{-4}T^2}{F}}\right) = F^0L^0T^0$

Check using MLT :

 $VD \sqrt{\frac{P}{2W}} = (LT^{-1})(L) \left(\sqrt{\frac{ML^{-3}}{F}}\right) = M^0L^0T^0 : OK$

For TI_2 let

 $TI_2 = b$

and for TI_3
 $TI_3 = \frac{d}{D}$

and both TI_2 and TI_3 are obviously dimensionless.

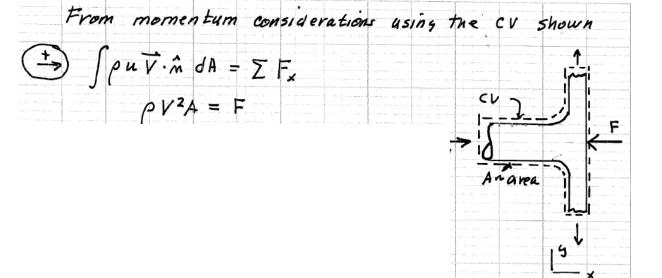
Thus,

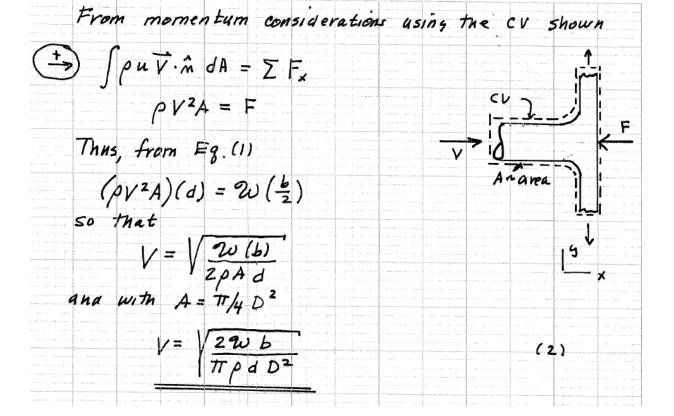
 $VD \sqrt{\frac{P}{2W}} = \oint \left(\frac{b}{d}\right) \frac{d}{D}$
 $VD \sqrt{\frac{P}{2W}} = \frac{d}{D}$

(b) For impending tipping around D
 $TD = D$

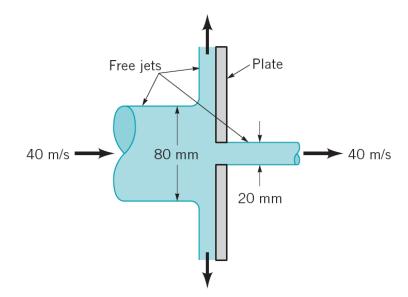
So that

 $TD = D$
 TD



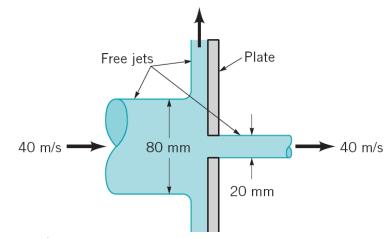


5.38 A circular plate having a diameter of 300 mm is held perpendicular to an axisymmetric horizontal jet of air having a velocity of 40 m/s and a diameter of 80 mm as shown in Fig. P5.38. A hole at the center of the plate results in a discharge jet of air having a velocity of 40 m/s and a diameter of 20 mm. Determine the horizontal component of force required to hold the plate stationary.



$$\int_{cs} -p$$

5.38 A circular plate having a diameter of 300 mm is held perpendicular to an axisymmetric horizontal jet of air having a velocity of 40 m/s and a diameter of 80 mm as shown in Fig. P5.38. A hole at the center of the plate results in a discharge jet of air having a velocity of 40 m/s and a diameter of 20 mm. Determine the horizontal component of force required to hold the plate stationary.



The control volume contains the plate and flowing air as indicated in the sketch above. Application of the hovizontal or X direction component of the linear momentum equation yields

$$-u_{1} \rho u_{1} A_{1} + u_{2} \rho u_{2} A_{2} = -F_{A, X}$$
or
$$F_{A, X} = u_{1}^{2} \rho \frac{m D_{1}^{2}}{4} - u_{2}^{2} \rho \frac{m D_{2}^{2}}{4} = u_{1}^{2} \rho \frac{m}{4} \left(D_{1}^{2} - D_{2}^{2}\right)$$
Thus
$$F_{A, X} = \left(\frac{40 \text{ m}}{5}\right) \left(\frac{1.23 \text{ kg}}{m^{3}}\right) \frac{\pi}{4} \left[\frac{(80 \text{ mm})^{2} - (20 \text{ mm})^{2}}{(1000 \text{ mm})^{2}}\right] \left(\frac{N}{\text{kg.m}}\right)$$
and
$$F_{A, X} = \frac{9.27 \text{ N}}{4}$$