## Natural convective flow

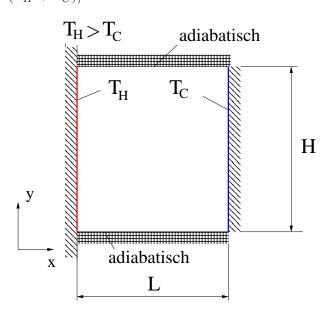
Consider the incompressible laminar flow inside an infinitely long cavity with rectangular cross section. The motion is driven by buoyancy, due to temperature-dependent change of density met with the considered non-isothermal flow conditions. The cooled right side wall is kept at given constant wall temperature  $T_C$ , while the heated left wall is kept on constant wall temperature  $T_H$ . The upper and lower walls are thermally isolated (adiabatic). All material properties, such as kinematic viscosity  $\nu$ , thermal diffusivity a, and thermal expansion coeffficient  $\beta = -\frac{1}{\bar{\rho}} \frac{\partial \rho}{\partial T}\Big|_p$  are assumed constant and given. The aspect ratio be H/L = 2. Assuming the so called Boussinesqu approximation, the problem is governed by the following equations:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\bar{\rho}} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\bar{\rho}} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + g\beta(T - T_M)$$

$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = a \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$
with  $T_M = (T_H + T_C)/2$ 



## Tasks:

• Nondimensionalize the equations using L,  $V_C = \sqrt{g\beta(T_H - T_C)L}$ ,  $\bar{\rho}V_C^2$ , and  $T_H - T_C$  as reference quantities for length, velocity, pressure, and temperature, respectively. The obtained non-dimensional formulation should solely depend on the parameters

$$Re = V_C L/\nu$$
,  $Pr = \nu/a$ 

- Finite-Volume-Discretization second order in space and time. For enforcing continuity the Poisson equation for the pressure should be solved with an indirect (iterative) solver.
- Simulate the following cases until a converged (stationary) state is reached:

i) 
$$Re = 100, Pr = 1$$

ii) 
$$Re = 100, Pr = 10$$

iii) 
$$Re = 200, Pr = 1$$

• Evaluate the Nusselts number for all cases:

$$Nu = \frac{Q_w L}{\lambda (T_H - T_C) H}, \text{ with } Q_w = -\int_0^H \lambda \left. \frac{\partial T}{\partial x} \right|_{x=0} dy$$

• Documentation of the work in a report. As for the results, show streamlines, contours of u, v and T.