

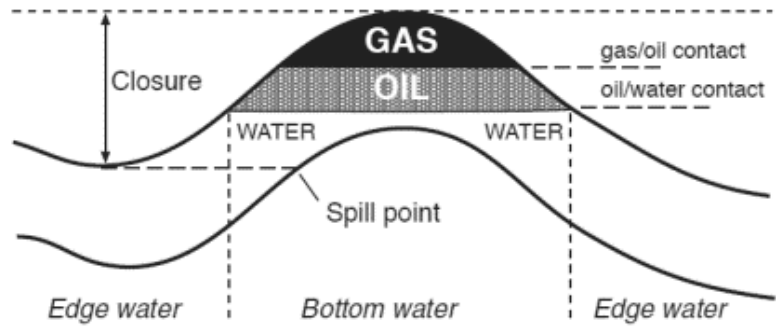
# Reservoir Engineering Fact Sheet

Mazen Nagib

"The art of developing and producing oil and gas fluids in such a manner as to obtain a high economic recovery" (Calhoun, 1960)

- A **Reservoir** is a subsurface accumulation of hydrocarbons, contained in **porous rock** formations, bounded by a barrier of **impermeable rock (seal)**, characterised by **natural pressure**.

Variable	Oilfield Unit	SI Unit	Conversion (Multiply SI Unit)
Area	acre	m <sup>2</sup>	$2.475 \times 10^{-4}$
Length	ft	m	3.28
Permeability	md	m <sup>2</sup>	$1.01 \times 10^{-15}$
Pressure	psi	Pa	$1.45 \times 10^{-4}$
Rate (oil)	STB/d	m <sup>3</sup> /s	$5.434 \times 10^{-5}$
Rate (gas)	Mscf/d	m <sup>3</sup> /s	3049



## Porosity $\phi$

A measure of the rock storage capacity (pore volume) that can hold fluids.



$$\phi = \frac{\text{pore volume}}{\text{bulk volume}}$$

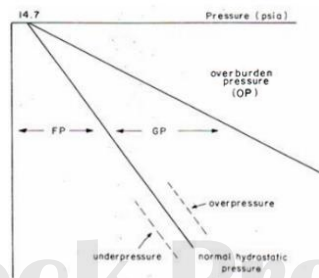
**Absolute  $\phi$** : total pore space in a rock.

**Effective  $\phi$** : interconnected pore space.

Recent sands (loosely packed)	35 - 45%
Sandstones (more consolidated)	20 - 35%
Tight/well cemented sandstones	15 - 20%
Limestones (e.g. Middle East)	5 - 20%
Dolomites (e.g. Middle East)	10 - 30%
Chalk (e.g. North Sea)	5 - 40%

## Formation Pressure

**Pressure Gradient**: The total pressure at any depth resulting from the combined weight of formation rock and fluids, whether water oil or gas is known as **overburden pressure**.



- Overburden pressure increases linearly with depth & typically has a pressure gradient of 1 psi/ft.

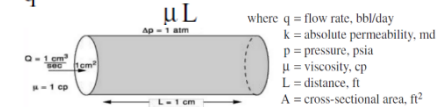
$$\begin{aligned} OB &= FP + GP \\ &= p + p_{eff} \\ p_{eff} &= OB - p \\ p &= \text{internal pressure} \\ p_{eff} &= \text{effective pressure} \end{aligned}$$

## Permeability $k$

A measure of a porous medium's (rock's) ability to transmit or conduct a fluid.

**Darcy's Law**:

$$q = \frac{0.001127 k A (p_1 - p_2)}{\mu L}$$



**Absolute  $k$** : 100% saturation of single fluid

**Effective  $k$** : a particular fluid in the presence of another.  $k_{ro}$ ,  $k_{gr}$ ,  $k_{rw}$ .

**Relative  $k$** : ratio of Effective  $k$  to Absolute  $k$  for each fluid.  $k_{ro} = k_o/k$ ,  $k_{rg} = k_g/k$ ,  $k_{rw} = k_w/k$

## Resistivity

The resistivity of a porous material is defined by:

$$R = \frac{rA}{L}$$

where  $r$  = resistance,  $\Omega$   
 $A$  = cross-sectional area, m<sup>2</sup>  
 $L$  = length, m  
 resistivity is expressed in Ohm-meter ( $\Omega m$ )

Resistivity of the reservoir is therefore related to the amount of **water occupying** a pore space. This gives a means of calculating  $S_w$

**True resistivity  $R_t$** : depends upon  $\phi$ ,  $S_w$  and the resistivity of the formation water  $R_w$ .

**Tortuosity** is usually estimated from electrical resistivity measurements. The tortuosity is in the range of 2 to 5 for most reservoir rocks.

## Saturation

Saturation is defined as that fraction of the pore volume occupied by a particular fluid:

$$\text{fluid saturation} = \frac{\text{total volume of the fluid}}{\text{pore volume}}$$

$$S_o = \frac{\text{volume of oil}}{\text{pore volume}}$$

$$S_g = \frac{\text{volume of gas}}{\text{pore volume}}$$

$$S_w = \frac{\text{volume of water}}{\text{pore volume}}$$

All saturation values are based on pore volume. Saturations range from 0 to 1 (or 0 to 100%) where the **sum** of the saturations is equal to **1.0** (100%).

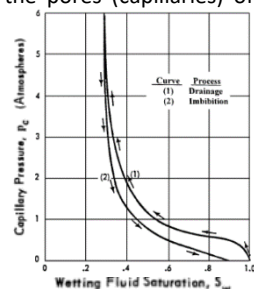
$$S_o + S_g + S_w = 1.0$$

where  $S_o$  = oil saturation  
 $S_g$  = gas saturation  
 $S_w$  = water saturation

## Capillary Pressure

Capillary pressure is the **difference** in pressure which exists at the **interface** between two immiscible fluids in the pores (capillaries) of the reservoir rock.

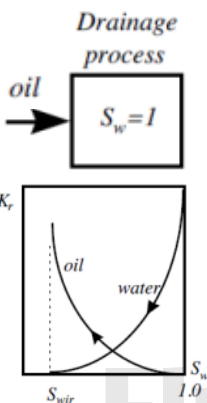
The displacement of one fluid by another is either **aided** or **opposed** by capillary pressure. It can **influence** the **distribution** of fluids in the reservoir.



## Drainage

Drainage describes the **displacement** of the **wetting** phase from the porous medium by a **non-wetting** phase.

Starting with the porous rock filled with water, and **displacing** this **water** by **oil**, the drainage relative permeability curves can be illustrated:



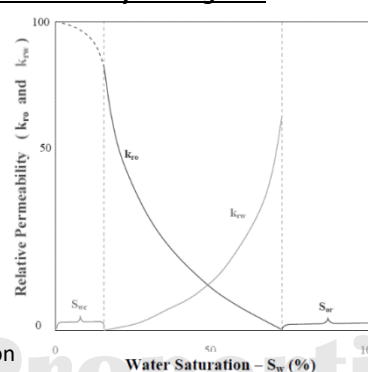
## Relative Permeability $k_{ro}$ , $k_{rg}$ , $k_{rw}$

$$\begin{aligned} k_{ro} &= k_o/k \text{ (Oil)} \\ k_{rg} &= k_g/k \text{ (Gas)} \\ k_{rw} &= k_w/k \text{ (Water)} \end{aligned}$$

$S_{or}$  = Residual oil saturation  
 $S_{wc}$  = Connate water saturation

Estimated using:

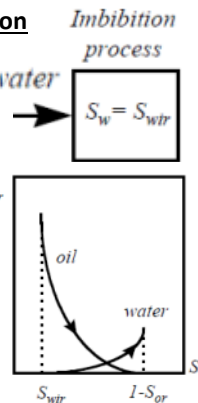
- Corey function
- Buckley and Leverett function



## Imbibition

Imbibition is process in which the **wetting** phase saturation increases, and the **non-wetting** phase saturation decreases.

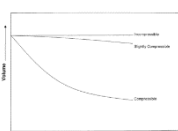
Reversing the process when all mobile **water** has been displaced, **injecting water** to displace the **oil**, imbibition curves defined:



## Reservoir Fluid Types

### 1. Incompressible fluids:

A fluid whose **volume** (or **density**) does **not** change with **pressure**.



### 2. Slightly compressible fluids:

These "slightly" compressible fluids exhibit small changes in volume, or density, with changes in pressure. Crude oil and water systems fit into this category.

### 3. Compressible fluids:

Are fluids that experience large changes in volume as a function of pressure. All gases are considered compressible fluids.

## Reservoir Flow Regimes

### 1. Steady-state flow

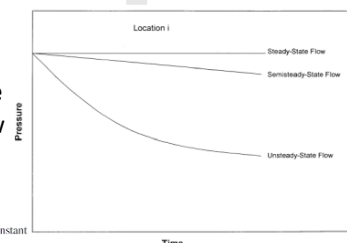
$$\left( \frac{\partial p}{\partial t} \right)_i = 0$$

### 2. Unsteady-state (Transient) flow

$$\left( \frac{\partial p}{\partial t} \right) = f(i, t)$$

### 3. Pseudosteady-state flow

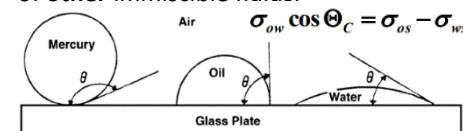
$$\left( \frac{\partial p}{\partial t} \right) = \text{constant}$$



There are **three** types of flow regimes that must be recognized in order to describe the fluid flow behaviour and **reservoir pressure distribution** as a function of **time**.

## Wettability

The tendency of one fluid to spread on or **adhere** to a solid **surface** in the presence of **other** immiscible fluids.



By measuring the angle of contact at the liquid-solid surface, the angle, which is always measured through the liquid to the solid, is called the **contact angle  $\theta$** .

## Viscosity

A measure of a fluid's internal **resistance** to flow and can be measured as the proportionality of **shear rate** to **shear stress**, which is a form of **internal friction**.

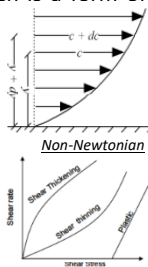
### Dynamic Viscosity (poise):

Expressed in the metric CGS  
[N s/m<sup>2</sup>, Pa.s or kg/m.s]

### Kinematic Viscosity (stoke):

The ratio of absolute or dynamic viscosity to density.  $\nu = \mu / \rho$   
[m<sup>2</sup>/s or Stoke St]

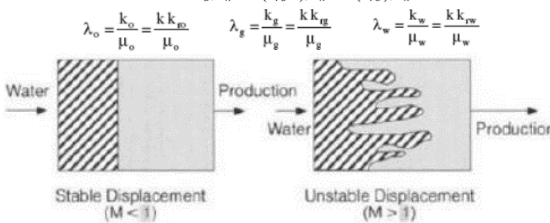
$$1 \text{ St (Stokes)} = 10^{-4} \text{ m}^2/\text{s} = 1 \text{ cm}^2/\text{s}$$



## Mobility Ratio

The mobility ratio **M** is defined as the mobility of the **displacing** fluid to the mobility of the **displaced** fluid.

$$M = \frac{k_w \mu_o}{k_o \mu_w} = \frac{(k_{rw}/k) \mu_o}{(k_{ro}/k) \mu_w} = \frac{(k_{rw}) \mu_o}{(k_{ro}) \mu_w}$$



## Tension

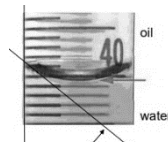
### Surface Tension



$$\sigma = \frac{F}{l}$$

$$w + T = F = 2\sigma l$$

### Interfacial Tension



$$\sigma_{ow} \cos \theta = \sigma_{os} - \sigma_{ws}$$

$$F = l \sigma_{ow} \cos \theta = 2\pi \sigma_{ow} \cos \theta$$

$$p = \frac{F}{A} = \frac{2\pi \sigma_{ow} \cos \theta}{\pi r^2} = \frac{2\sigma_{ow} \cos \theta}{r}$$

## Compressibility

A measure of the relative **volume change** of a **fluid** or **solid** as a response to a **pressure change**.

### Isothermal Compressibility c

$$c = -\frac{1}{V} \left( \frac{\partial V}{\partial p} \right)_T$$

Typical values:

Oil: 5 to 20  $\times 10^{-6}$  psi<sup>-1</sup> ( $p > p_b$ )  
30 to 200  $\times 10^{-6}$  psi<sup>-1</sup> ( $p < p_b$ )  
Gas: 50 to 1000  $\times 10^{-6}$  psi<sup>-1</sup>  
Water: 3 to 5  $\times 10^{-6}$  psi<sup>-1</sup>

### Formation Compressibility c<sub>f</sub>

$$c_f = \frac{1}{\phi} \frac{d\phi}{dp}$$

Typical values:

Normal: 2 to 10  $\times 10^{-6}$  psi<sup>-1</sup>  
Abnormal: 10 to 100  $\times 10^{-6}$  psi<sup>-1</sup>

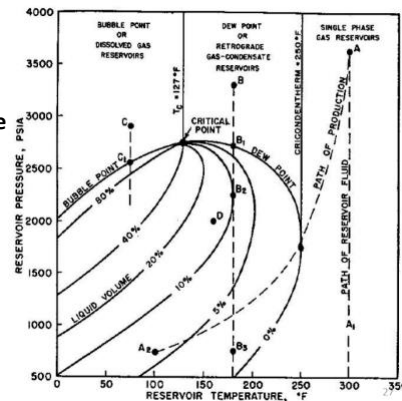
Undersaturated  
vs Saturated

### Phases:

- Solid
- Compressible Liquid
- Vapour
- Gaseous
- Supercritical Fluid

Isothermal  
conditions in the  
reservoir

## Phase Diagrams



## API Gravity

API gravity is related to the density of the crude oil and is the preferred method for classifying crude systems.

$$^{\circ}\text{API} = \frac{141.5}{\gamma_o} - 131.5$$

- where  $\gamma_o$  = the specific gravity of the oil

light	$^{\circ}\text{API} > 31.1$	$\rho_o < 870$
medium	$31.1 > ^{\circ}\text{API} > 22.3$	$870 < \rho_o < 920$
heavy	$22.3 > ^{\circ}\text{API} > 10.0$	$920 < \rho_o < 1000$

## Gas Specific Gravity $\gamma_g$

The specific gravity is defined as the **ratio** of the **gas density** to that of the **air**. Both densities are measured or expressed at the same pressure and temperature.

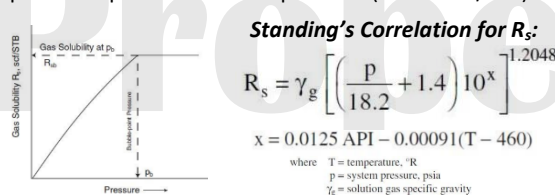
$$\gamma_{gas} = \frac{\rho_{gas}}{\rho_{air}}$$

Commonly, the **standard pressure**  $p_{sc}$  and **standard temperature**  $T_{sc}$  are used in defining the gas specific gravity.

## Gas Solubility $R_s$

The **solubility** of natural gas in crude oil is dependent upon **pressure**, **temperature**, and **composition** of both the gas and oil.

$R_s$  Defined as the number of standard [cu ft] of natural gas which will dissolve in one [stock tank bbl] of oil at a particular pressure and temperature (units = scf/STB)



### Standing's Correlation for $R_s$ :

$$R_s = \gamma_g \left[ \left( \frac{p}{18.2} + 1.4 \right) 10^x \right]^{1.2048}$$

$$x = 0.0125 \text{ API} - 0.00091(T - 460)$$

where  $T$  = temperature, °R  
 $p$  = system pressure, psia  
 $\gamma_g$  = solution gas specific gravity

## Oil Specific Gravity $\gamma_o$

Fluid gravity or specific gravity of oil is the **ratio** of the density of the oil to the density of water (where both densities are measured at atmospheric pressure 60F)

$$\gamma_o = \frac{\rho_o}{\rho_w}$$

where  $\gamma_o$  = specific gravity of the oil  
 $\rho_o$  = density of the crude oil, lb/ft<sup>3</sup>  
 $\rho_w$  = density of the water, lb/ft<sup>3</sup>

## Bubble-point Pressure $p_b$

The bubble-point pressure  $p_b$  of a is defined as the **highest pressure** at which a **bubble** of gas is **first liberated** from the **oil**.

### Standing's Correlation for $p_b$ :

$$p_b = 18.2 [(R_s/\gamma_g)^{0.83} (10)^a - 1.4]$$

$$a = 0.00091 (T - 460) - 0.0125 (\text{API})$$

where  $p_b$  = bubble-point pressure, psia  
 $T$  = system temperature, °R

A **central aspect** of PVT analysis is understanding how gas **evolves** from oil when the pressure falls below the bubble-point.

## Gas Formation Volume Factor $B_g$

$B_g$  is used to relate the volume of gas measured at reservoir conditions to the volume of gas measured at standard conditions (60F, 14.7 psi)

$$B_g = \frac{\text{Volume of gas at reservoir conditions}}{\text{Volume of gas at standard conditions}} = \frac{(V_g)_{p,T}}{(V_g)_{sc}}$$

### Standing's Correlation for $B_g$ :

$$B_g = 0.02827 \frac{zT}{p}$$

where  $B_g$  = gas formation volume factor, ft<sup>3</sup>/scf  
 $z$  = gas compressibility factor  
 $T$  = temperature, °R

$$\text{Oil field units } B_g = 0.005035 \frac{zT}{p} \quad [\text{bbl/scf}]$$

## Oil Formation Volume Factor $B_o$

$B_o$  is defined as the ratio of the **volume** of **oil** (plus the gas in solution) at the prevailing **reservoir temperature** and **pressure** to the volume of oil at **standard conditions**.

$$B_o = \frac{\text{Volume of oil at reservoir conditions}}{\text{Volume of oil at standard conditions}} = \frac{(V_o)_{p,T}}{(V_o)_{sc}}$$

### Standing's Correlation for $B_o$ :

$$B_o = 0.9759 + 0.000120 \left[ R_s \left( \frac{\gamma_g}{\gamma_o} \right)^{0.5} + 1.25(T - 460) \right]^{1.2}$$

where  $T$  = temperature, °R  
 $\gamma_o$  = specific gravity of the stock-tank oil  
 $\gamma_g$  = specific gravity of the solution gas

## Water Formation Volume Factor $B_w$

$B_w$  is used to relate the volume of produced water measured at reservoir conditions to the volume of water measured at standard conditions (60F, 14.7 psi)

$$B_w = \frac{\text{Water Volume at reservoir conditions}}{\text{Water Volume at standard conditions}} \quad [\text{bbl/scf}]$$

$B_w$  is generally taken to be equivalent to 1  
( $B_w \sim 1$ )

$$B_o = B_t - (R_{si} - R_s) B_g$$

$B_t$  is defined as the **volume** in **bbl's** of one STB and its initial dissolved gas.

## Ideal Gas Law

Assuming that the **behaviour** of both the gas and air can be described the ideal gas equation:

$$pV = nRT$$

where

- $p$  = absolute pressure [psia]
- $V$  = volume [ft<sup>3</sup>]
- $T$  = absolute temperature [°R]
- $n$  = number of moles of gas [lb-mol]
- $R$  = universal gas constant [10.73 psia.ft<sup>3</sup>/lb-mol.°R]
- $m$  = mass [lb]
- $M$  = molecular weight [lb/lb-mol]

$$n = \frac{m}{M}$$

The number of moles ( $n$ ) is related to the mass of gas under consideration ( $m$ ) and its molecular weight ( $M$ )

## Density $\rho$

Gas density  $\rho$  is defined as the **mass** of the **gas** occupying a **certain volume** at **specified pressure** and **temperature**. The density is usually represented in units of [lbm/ft<sup>3</sup>].

$$\rho_{g,sc} = \frac{M}{23.645} \text{ kgm}^{-3} \quad \rho_{g,sc} = \frac{M}{380} \text{ lbft}^{-3}$$

$$pV = znRT \quad \rho_g(p, T) = \frac{\rho_{g,sc}}{B_g}$$

where  $z$  is a dimensionless quantity and is defined as the **ratio** of the **actual volume** of **n-moles** of gas at  $T$  and  $p$  to the **ideal volume** of the same number of moles at the same  $T$  and  $p$



The external (drainage) radius is usually determined by equating the area of the well spacing with that of a circle.

# Material Balance

Initial Mass		Final Mass
		Pore volume occupied by the remaining oil at $p$ $(N - N_p)B_o$
Pore volume occupied by the oil initially in place at $p_i$ $NB_{oi}$		Pore volume occupied by the gas in the gas cap at $p$ $GB_g = \left(\frac{mNB_{gi}}{B_{gi}}\right)B_g$
		Pore volume occupied by the evolved solution gas at $p$ $(NR_p - (N - N_p)R_s - N_p R_p)B_g$
	=	Pore volume occupied by the net water influx at $p$ $W_e = W_p B_w$
+ Pore volume occupied by the gas in the gas cap at $p_i$ $GB_{oi} = mNB_{oi}$		Change in P.V due to connate water expansion and pore volume reduction due to rock expansion $(PV)S_{wi}c_w\Delta p + (PV)c_f\Delta p$ $= \frac{(1+m)NB_{oi}}{(1-S_{wi})}(S_{wi}c_w + c_f)\Delta p$
		Pore volume occupied by the injected gas at $p$ $G_{inj}B_{gi}$
		Pore volume occupied by the injected water at $p$ $W_{inj}B_w$

$$N = \frac{N_p [B_o + (R_p - R_s)B_g] - (W_e - W_p B_w) - G_{inj}B_{gi} - W_{inj}B_{wi}}{(B_o - B_{oi}) + (R_{si} - R_s)B_g + mB_{oi} \left[ \frac{B_g}{B_{gi}} - 1 \right] + B_{oi}(1+m) \left[ \frac{S_{wi}c_w + c_f}{1 - S_{wi}} \right] \Delta p}$$

$$m = \frac{\text{initial volume of gas cap}}{\text{initial volume of oil in place}} = \frac{GB_{gi}}{NB_{oi}} \quad R_{si} = \frac{G_{dissolved}}{N} \left[ \frac{scf}{STB} \right] \therefore G_{dissolved} = NR_{si}$$

$p_i$	Initial reservoir pressure, psi	$B_{gi}$	Initial gas formation volume factor, bbl/scf
$p$	Volumetric average reservoir pressure	$B_g$	Gas formation volume factor, bbl/scf
$\Delta p$	Change in reservoir pressure = $p_i - p$ , psi	$W_{inj}$	Cumulative water injected, STB
$p_b$	Bubble point pressure, psi	$G_{inj}$	Cumulative gas injected, scf
$N$	Initial (original) oil in place, STB	$W_e$	Cumulative water influx, bbl
$N_p$	Cumulative oil produced, STB	$m$	Ratio of initial gas-cap-gas reservoir volume to initial reservoir oil volume, bbl/bbl
$G_p$	Cumulative gas produced, scf	$G$	Initial gas-cap gas, scf
$W_p$	Cumulative water produced, bbl	$P.V$	Pore volume, bbl
$R_p$	Cumulative gas-oil ratio, scf/STB	$c_w$	Water compressibility, $\text{psi}^{-1}$
$GOR$	Instantaneous gas-oil ratio, scf/STB	$c_f$	Formation (rock) compressibility, $\text{psi}^{-1}$
$R_{si}$	Initial gas solubility, scf/STB		
$R_s$	Gas solubility, scf/STB		
$B_{oi}$	Initial oil formation volume factor, bbl/STB		
$B_o$	Oil formation volume factor, bbl/STB		

## Havlena-Odeh Method

$$N = \frac{F - W_e}{[rb] \left( E_o + mE_g + E_{fw} \right)}$$

$F$  = Underground Withdrawal  
= oil prod. + gas prod. + water prod.  
=  $N_p B_o + N_p (R_p - R_s) B_g + W_p$

$E_o$  = Oil Expansion

$$= (B_o - B_{oi}) + (R_{si} - R_s) B_g = B_t - B_{oi}$$

$$E_g = \text{Gas Expansion} = B_{oi} \left( \frac{B_g}{B_{gi}} - 1 \right)$$

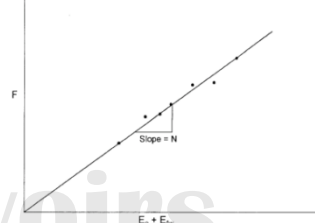
$$E_{fw} = (1+m)B_{oi} \left[ \frac{c_w S_{wi} + c_f}{1 - S_{wi}} \right] \Delta p$$

where  $\Delta p = p_i - p$

### Case 1: Undersaturated, No Gas Cap

$W_e$  is neglected

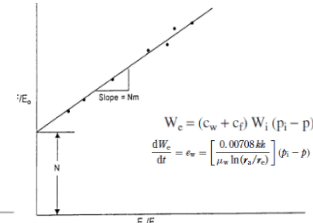
$$F = N(E_o + E_{fw})$$



### Case 2: Saturated, Gas Cap

$W_e$  and  $W_p$  is neglected

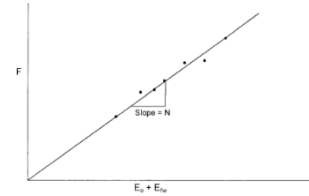
$$F/E_o = N + mN(E_g/E_o)$$



### Case 3: Saturated, At Bubble Point

$W_e$  and  $W_p$  is neglected

$$N = \frac{F}{E_o} \rightarrow F = NE_o$$



### Cumulative GOR

$$R_p = \frac{\text{Volume of gas produced}}{\text{Volume of oil produced}} = \frac{G_p}{N_p}$$

### Instantaneous GOR

$$GOR = R_s + \left( \frac{k_{rg}}{k_{ro}} \right) \left( \frac{\mu_o B_o}{\mu_g B_g} \right)$$

where GOR = instantaneous gas-oil ratio, scf/STB  
 $R_s$  = gas solubility, scf/STB  
 $k_{rg}$  = relative permeability to gas  
 $k_{ro}$  = relative permeability to oil  
 $B_o$  = oil formation volume factor, bbl/scf  
 $B_g$  = gas formation volume factor, bbl/scf  
 $\mu_o$  = oil viscosity, cp  
 $\mu_g$  = gas viscosity, cp

### Case 4: Water Drive Reservoirs

No initial gas cap  $m = 0$

$$\frac{F}{E_o} = N + \frac{W_e}{E_o}$$

Initial gas cap  $E_{fw} = 0$

$$\frac{F}{E_o + mE_g} = N + \frac{W_e}{E_o + mE_g}$$

### Water Influx $W_e$ Pot Aquifer Model

- Water influx (water encroachment,  $W_e$ )
  - offsets pressure decline
  - changes the position of the OWC
- Affected by
  - degree of pressure maintenance
  - outer boundary conditions
  - flow geometries
  - flow regimes

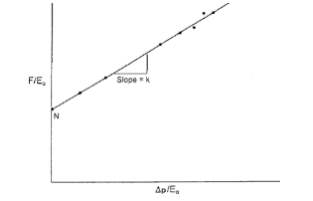
### Active Water Drive

$$c_w = \frac{dW_e}{dt} = B_o \frac{dN_p}{dt} + (GOR - R_s) \frac{dN_p}{dt} B_g + \frac{dW_p}{dt} B_w$$

where  $W_e$  = cumulative water influx, bbl  
 $t$  = time, days  
 $N_p$  = cumulative oil production, STB  
 $GOR$  = current gas-oil ratio, scf/STB  
 $R_s$  = current gas solubility, scf/STB  
 $B_o$  = gas formation volume factor, bbl/scf  
 $B_g$  = cumulative gas production, STB  
 $(dN_p/dt)$  = daily oil flow rate  $Q_o$ , STB/day  
 $(dW_e/dt)$  = daily water flow rate  $Q_w$ , STB/day  
 $(dW_p/dt)$  = daily water influx rate  $c_w$ , bbl/day  
 $(GOR - R_s)(dN_p/dt)$  = daily free gas flow rate, scf/day

### Steady State Pot Aquifer

$$W_e = K \Delta p \quad \frac{F}{E_o} = N + K \left( \frac{\Delta p}{E_o} \right)$$



# Gas Reservoirs

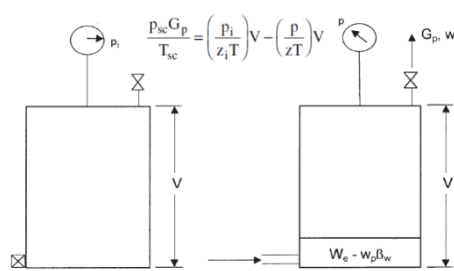
$$\frac{p_{sc} G_p}{R T_{sc}} = \frac{p_i V}{z_i R T} - \frac{p[V - (W_e - W_p)]}{z R T}$$

where  $p_i$  = initial reservoir pressure  
 $G_p$  = cumulative gas production, scf  
 $p$  = current reservoir pressure  
 $V$  = original gas volume,  $\text{ft}^3$   
 $z_i$  = gas deviation factor at  $p_i$   
 $z$  = gas deviation factor at  $p$   
 $T$  = temperature,  $^{\circ}\text{R}$   
 $W_e$  = cumulative water influx,  $\text{ft}^3$   
 $W_p$  = cumulative water production,  $\text{ft}^3$

no. of moles

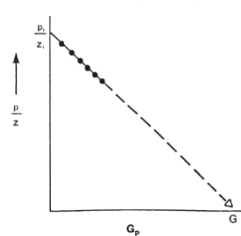
$n_p = n_i - n_f$  where  $n_p$  = moles of gas produced  
 $n_i$  = moles of gas initially in the reservoir  
 $n_f$  = moles of gas remaining in the reservoir

### No water production



### In terms p/z

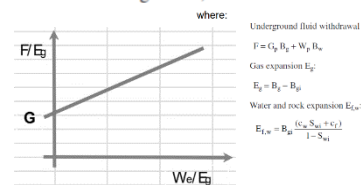
$$\frac{p}{z} = \frac{p_i}{z_i} - \left( \frac{p_{sc} T}{R T_{sc} V} \right) G_p$$



### In terms $B_g$

$$G_p B_g + W_p B_w = G(B_g - B_{gi}) + G B_{gi} \frac{(c_w S_{wi} + c_f)}{1 - S_{wi}} \Delta p + W_e B_w$$

$$F = G(E_g + E_{f,w}) + W_e B_w$$



### Natural Decline, D

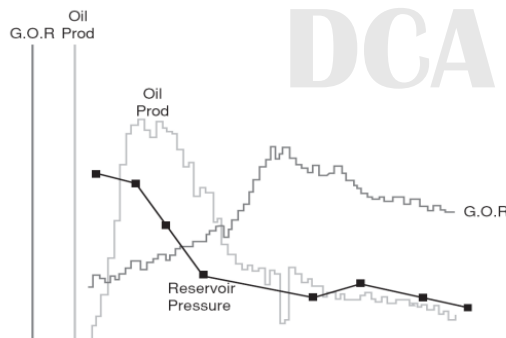
$$D = -\frac{dq/dt}{q} = -\lim_{\Delta t \rightarrow 0} \frac{\Delta q / \Delta t}{q}$$

### Cumulative $N_p$

$$N_p = \int_0^t q(t) dt = \int_{q_i}^q q \frac{dt}{dq} dq$$

### Cumulative $N_p$ as a function of $q$

$$N_p = \int_{q_i}^q \frac{1}{D_i} \left( \frac{q_i}{q} \right)^n dq$$



Reservoir Pressure

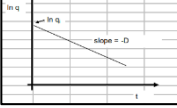
$$\Rightarrow t = \frac{-\ln \left( \frac{q}{q_i} \right)}{D}$$

$$\Rightarrow N_p = \frac{q_i - q}{D}$$

$$\ln q = \ln q_i + \ln e^{-Dt}$$

$$\Rightarrow \ln q = \ln q_i - Dt$$

$$\Rightarrow \ln q = (-D)t + \ln q_i$$



Decline Exponent	Type of Decline	Rate-Time Relationship	Rate: Cumulative relationship	$Dt$
0	Exponential	$q(t) = q_i \exp(-D_i t)$	$N_p = \frac{q_i - q}{D_i}$	$Dt = \ln \left( \frac{q_i}{q} \right)$
1	Harmonic	$q(t) = \frac{q_i}{(1 + D_i t)}$	$N_p = \frac{q_i}{D_i} \ln(q_i / q)$	$Dt = \left( \frac{q_i}{q} \right) - 1$
$0 < n < 1$	Hiperbolic	$q(t) = \frac{q_i}{(1 + n D_i t)^{1/n}}$	$N_p = \frac{q_i^n}{D_i (1 - n)} \left( \frac{1}{q_i^{n-1}} - \frac{1}{q^{n-1}} \right)$	$Dt = \frac{\left( \frac{q_i}{q} \right)^n - 1}{n}$

Natural decline trend is dictated by:

Natural drive, Rock and fluid properties and well completion.

When the average reservoir pressure decreases with time due to oil and gas production, this causes the well and field production rates to decrease yielding a rate time relation similar to that in the following figure.



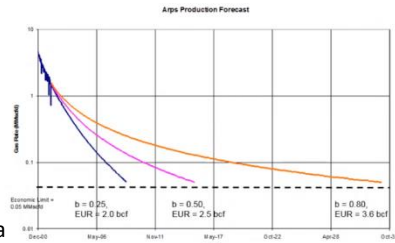
- **Production rate only**
- **Using historical data to predict**
- **Production rate only**

- **Deliverables:**

Production forecast  
Recoverable reserves under current conditions.

- **Limitations:**

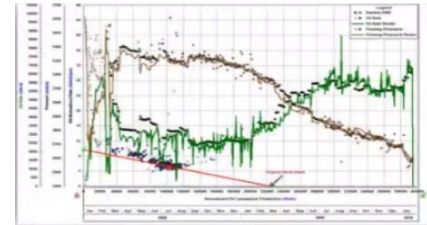
Assume constant opt cond.  
Requires decline in prod rate  
Can be uncertainly limited data



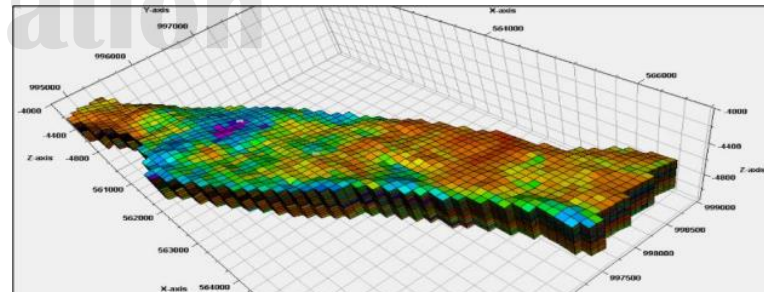
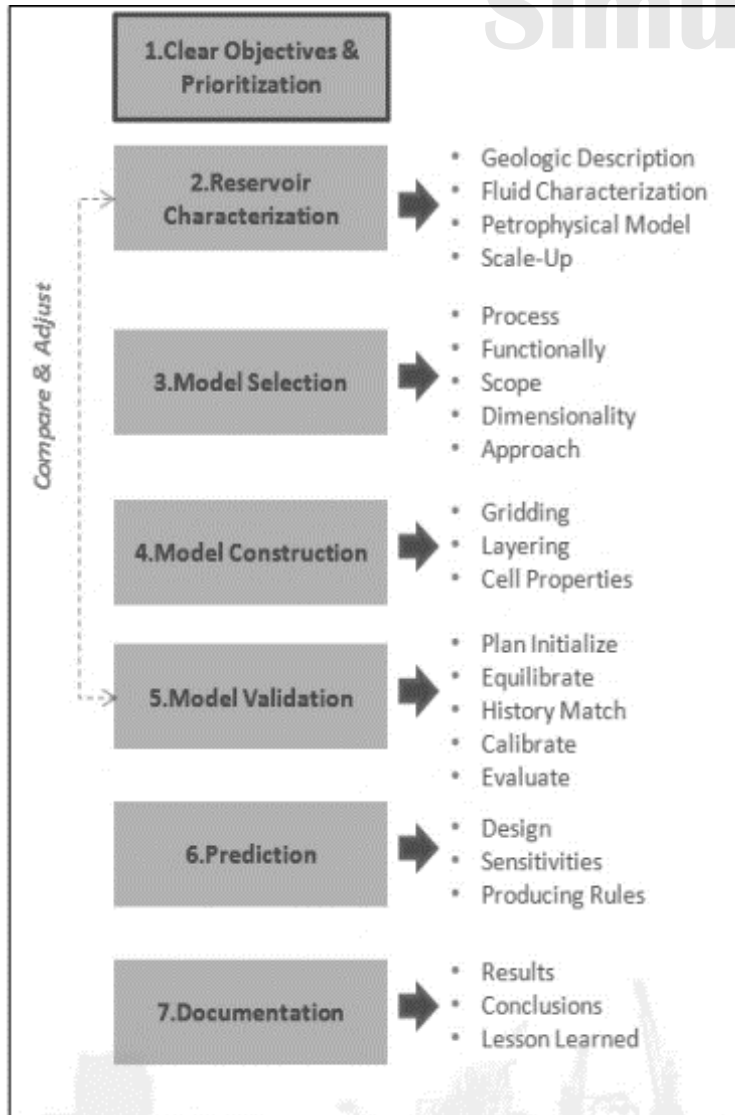
- Does not require wells to be shut in
- Uses rates & flowing pressure, applicable to variable operating cond.
- Based on physics and developed from PTA
- Reservoir signal extraction and characterization

- **Deliverables:**

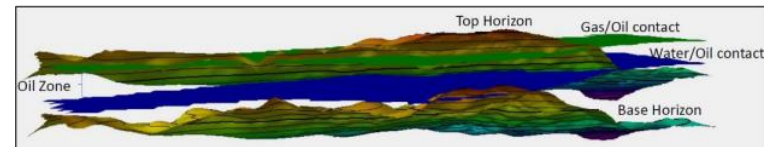
OGIP/OOIP and Reserves  
Production optimization  
Drainage area  
Infill potential  
Permeability and skin



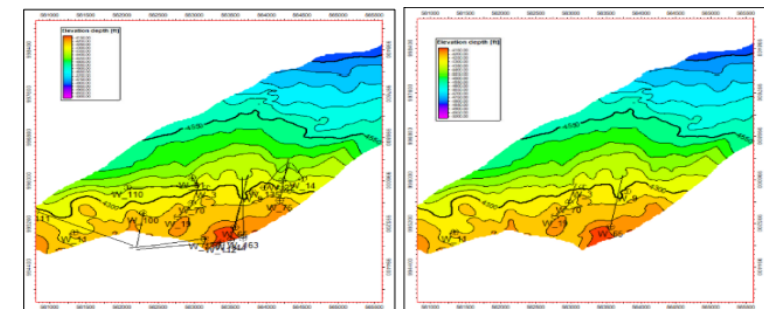
- **Reservoir Simulation Fundamentals**



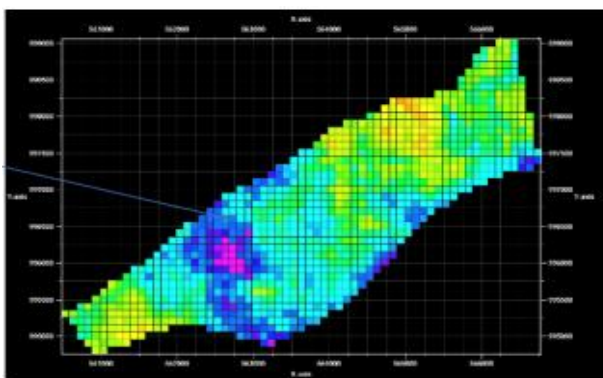
The reservoir formation 3D grid was divided at an optimum of 100m2 blocks. This qualifies the grid as Coarse Grid, thus enabling a fast and efficient simulation run as a result of the reduced volume in calculations required to complete the simulation. The target reservoir formation was evaluated from depth 4000m to 5200m.



It is vital to identify the relevant Water Oil Contact (WOC) and Gas Oil Contact (GOC) with regards to the Top and Base Horizons created using Petrel thus resulting in the outstanding Oil Zone. The relevant zones and contacts are vital to utilize when establishing development plans of the asset due to the constant threat of developing water and gas Coning because of increased production. Such parameters are key to identify due to the optimization of oil recovery as the development of water Coning immediately results in an increase of water invasion, thus reducing the efficiency of production because of an increased Water Cut.

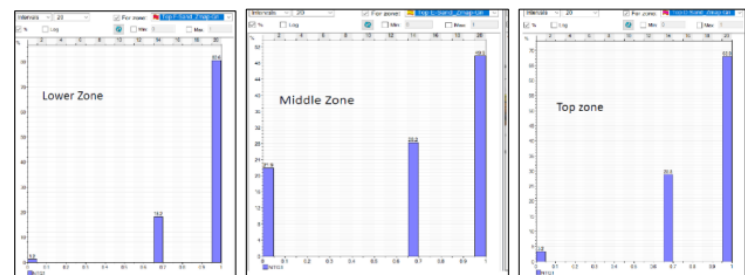


- **Reservoir 3D Model**

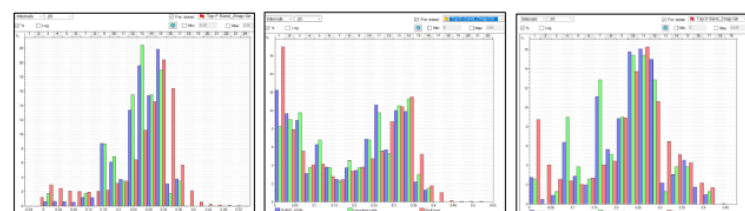


Reservoir simulation requires a precise balance between performance and simulation time duration. Due to the massive demand in calculations of material balance being carried out by the simulator a grid is created in order to breakdown the relevant reservoir formation area in blocks. The variation in size of blocks results in a simultaneous variation in uncertainty of simulation results. The larger the size of grid blocks results in a faster run time, however results in an increased uncertainty regarding the results due to a smaller amount of calculations taking place.

- **Porosity distribution**



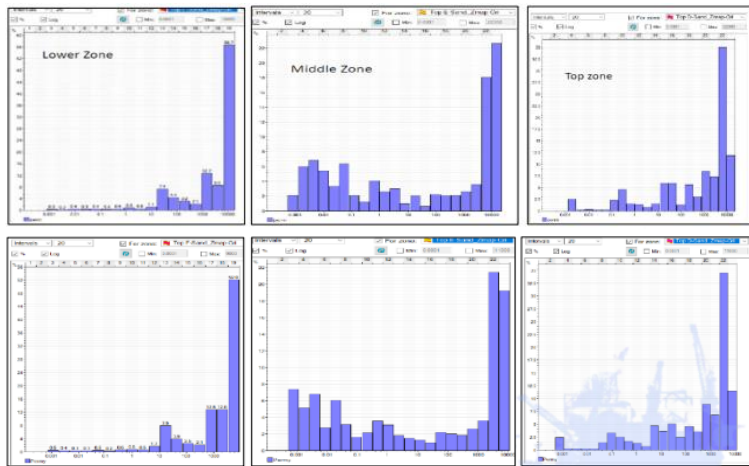
- **Net-to-Gross**



- **Permeability Distribution**

Permeability of a 3D Reservoir Model can be identified in all three directional axis X, Y and Z. As Z is a function of Perm X and Y these will be the focus of interpretation. The distribution of Permeability was established upon the relationships connecting Porosity and Permeability carried out via laboratory tests on formation samples (core analysis).

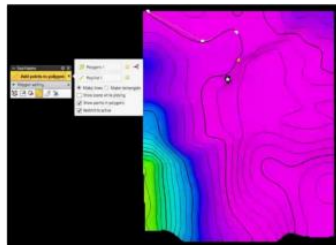
<b>Permeability</b>	<b>X</b>	<b>= Permeability</b>
	<b>Y</b>	<b>= Permeability X</b>
	<b>Z</b>	<b>= 0.5 * Permeability X</b>



- *Schematic Workflow Initial Volume Calculation*

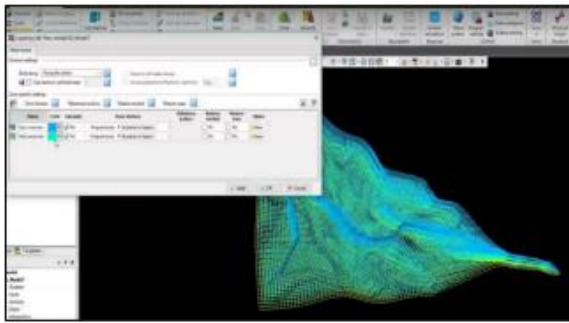
## 5. Import Data Polygon

Upon starting a new Petrel project, field units must be selected. This is followed by importing relevant assorted data regarding Well Logs, Well Deviations and Well Heads. Along with Well data, relevant surface maps of Top and Bottom sands must be imported. After the relevant data has been imported to the project, analyses of Logs must be interpreted in order to locate potentially commercial reservoirs. In order to obtain hydrocarbon volumes in place, various stages of Petrel workflow must take place following the standard steps when setting up the Petrel model. To begin with, potential reservoir zones of clean sands are identified by creating boundaries from closed Polygons, this sets the boundaries of the Reservoir.



#### 4. Gridding

A 3D grid is then created regarding the Reservoir formation, by completing the workflow procedure as follows. Select Make Simple Grid and insert surfaces, insert boundary values regarding the Geometry and increment in which the Grid will be created allocating value of nodes in the 3D Grid. In this case 100m2 increments were selected. By creating the 3D grid, the skeleton of the grid can be seen in a 3D window which also enables models of the fault to be viewed. Then, zones must be created in order to populate regions between the horizons. The zones will cover from Top-Mid and Mid-Base horizons. Layering is essential in order to select the amount of layers required to populate the 3D Skeleton.



### 3. Facies Workflow

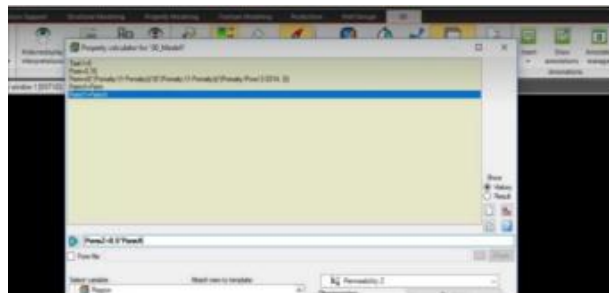
Now that the 3D grid has been created, Petrel Property Calculator must be utilized in order to populate relevant model properties to be modelled. The porosity can be populated by inputting value of porosity (e.g. Pore=0.18). This will generalise the 3D grid with this porosity value. In order to accurately interpret any model, contacts of Gas and Oil along with Oil and Water must be interpreted from Well log readings. By making a contact, proceed to contact set and input interpreted depths at which contacts will be set regarding GOC and WOC. After establishing relevant contacts of Gas, Oil and Water the properties calculator is employed in order to generate the facies logs. The format in which the cut-off's must be listed is as follows: [Facies= If(Porosity < 0.13, 3, 0)]. This is required in order to distribute the facies with regards to available porosity cut offs.



- **Schematic Workflow Initial Volume Calculation**

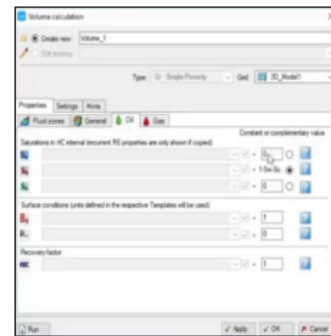
### 1. Property Calculator

Upscaling the well logs into the grid is necessary in order to populate the remainder of the 3D grid with petrophysical properties such as porosity. By utilizing the well log upscaling function in Petrel, you can select Wells and relevant Logs in order to upscale properties to complete the 3D grid model with properties. By upscaling the facies and the porosity you can move forward towards populating the permeability properties by utilizing the properties calculator. After selecting Permeability, the calculation of Permeability inputted to the calculator must be in a similar format as follows: Perm= (6\*(Porosity/(1-Porosity))) \* (6\*(Porosity/(1-Porosity))) \* (Porosity/Pow(0.0314, 2)). After populating Permeability, the remaining Perm Y, Perm X and Perm Z must be populated.



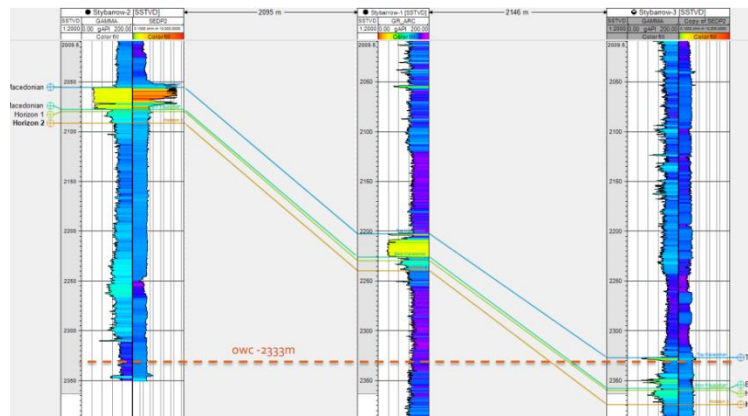
## 2. Volume workflow

Having populated all relevant data regarding the 3D Grid, it is now possible to begin with initial volume calculations as no dynamic fluid properties have yet been utilized. Starting by selecting the Volume section under the Property modelling tab, name the Case. In the fluid contacts tab select the GOC and WOC set previously, and then move to the general tab. In the general tab the Net-ToGross and Porosity cut-off points can be detailed, as given previously in section 3.1.5 regarding NTG cut-offs. Then, the fluid properties can be detailed in the Oil window regarding the saturation of water ( $S_w$ ), saturation of gas ( $S_g$ ) and saturation of oil ( $S_o$ ), including values regarding Bo and Rs. Refer to Figure 3.2E. After all data is confirmed, it is possible to run the case in order to calculate the initial Volume calculation regarding the base case. Figure 3.2A presents the results obtained regarding the initial volume calculation obtained.

[illegible]

- **Schematic Workflow Subsurface Storage Sleipner**

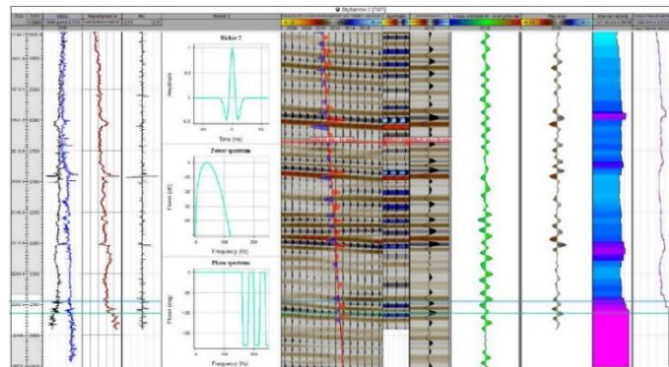
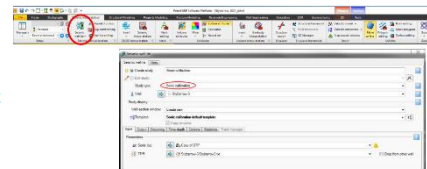
## 1. Seismic Well Ties



### Synergistic Seismograms

- Velocity ( $V$ ) and density( $\rho$ ) logs are required to calculate acoustic impedance:

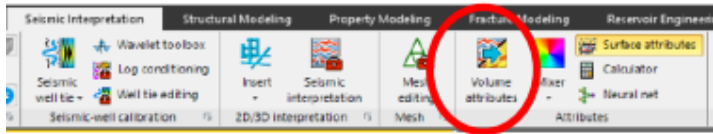
$$\text{Acoustic Impedance} = V\rho$$



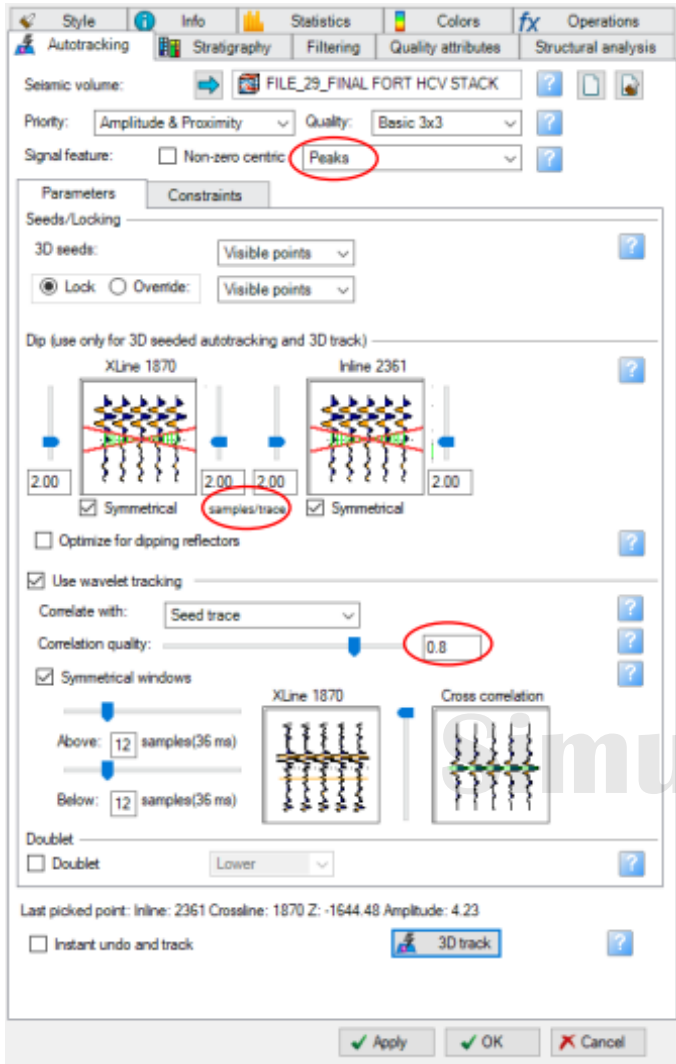


## Schematic Workflow Subsurface Storage Sleipner

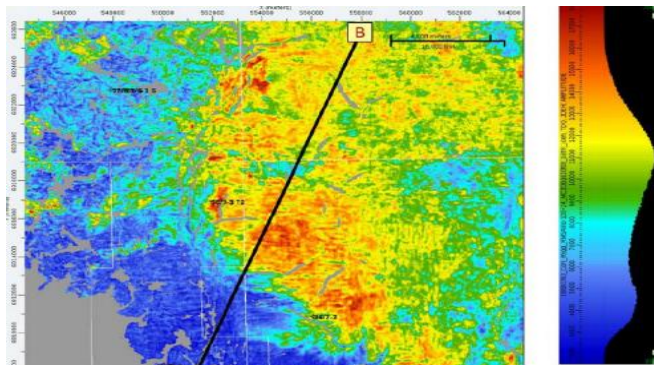
### Volume attributes



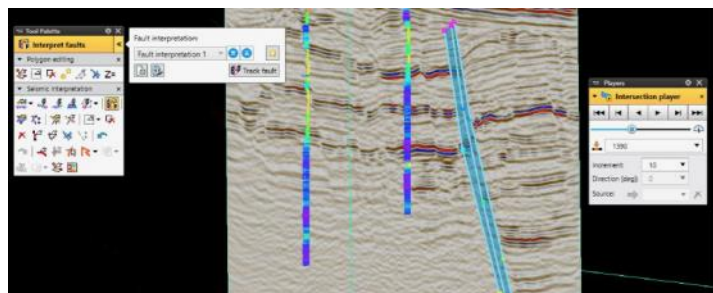
### Reservoir Mapping Auto Tracking Amplitude Extractions



### Amplitude Extractions

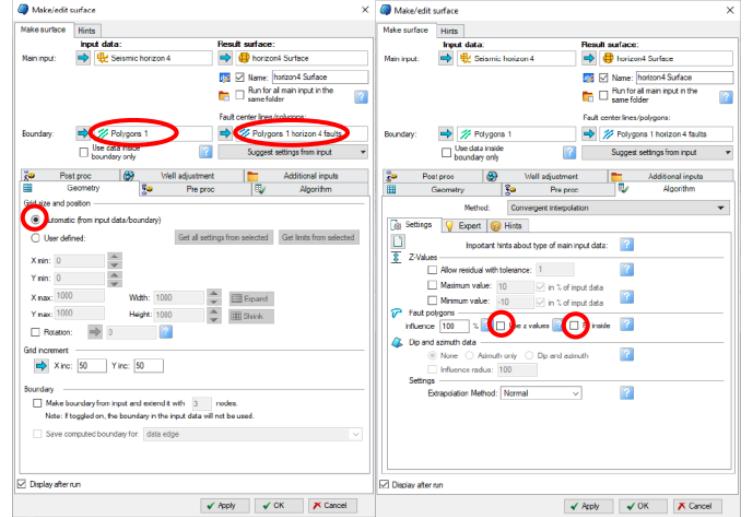


### Fault Interpretation

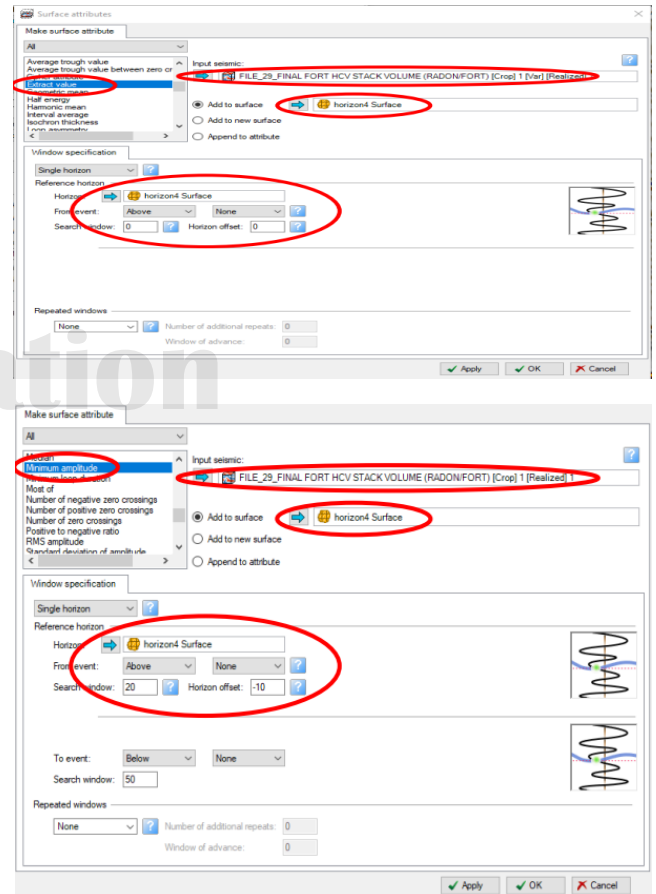


## Schematic Workflow Subsurface Storage Sleipner

### Create Surfaces



### Amplitude Extraction



### Storage Plume Volume

