

CHEME 3130: Macroscopic energy balances and the First Law of Thermodynamics

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Introduction

Thermodynamics is the study of the physical and energetic properties of pure materials and mixtures of materials, and how we can exploit these properties for technological or societal benefit. Thermodynamics is at the heart of chemical engineering applications ranging from traditional process engineering to biology and medicine. In this class, we will learn the theoretical basis of thermodynamics, and will apply this understanding to practical problems in chemical and biomolecular engineering.

Student outcomes

At the end of this lecture module, students will be able to:

- O₁ Describe the total energy balance equation and first law of thermodynamics for an open and closed system
- O₂ Describe the constant pressure and constant volume heat capacity
- O₃ Describe the thermodynamic state function called enthalpy H :

$$H \equiv U + PV \quad (1)$$

where U denotes the internal energy, P denotes the pressure and V denotes the volume.

Introduction

Imagine that we could decompose a chemical engineering process into a *system* and its *surroundings*. The *system* e.g., a reactor or downstream processing unit such as distillation column can exchange mass and energy with its *surroundings*. Collectively the *system* and its *surroundings* is called a *universe*. Total energy (E) is neither created nor destroyed in a *universe*; instead, it is converted from one form to another, leading to the principle of conservation of energy:

$$\Delta E_{\text{universe}} = \Delta E_{\text{system}} + \Delta E_{\text{surroundings}} = 0 \quad (2)$$

The first law of thermodynamics, which can be derived from the conservation of energy principle, governs the pathways by which these energy conversions can occur. Suppose we have a general thermodynamic system separated from its surroundings by a permeable boundary (Fig. 1). Energy (and mass) can accumulate inside the system, or can be transferred into and from the system by passing across this boundary. Putting these ideas together we can write *differential* energy and

Universe

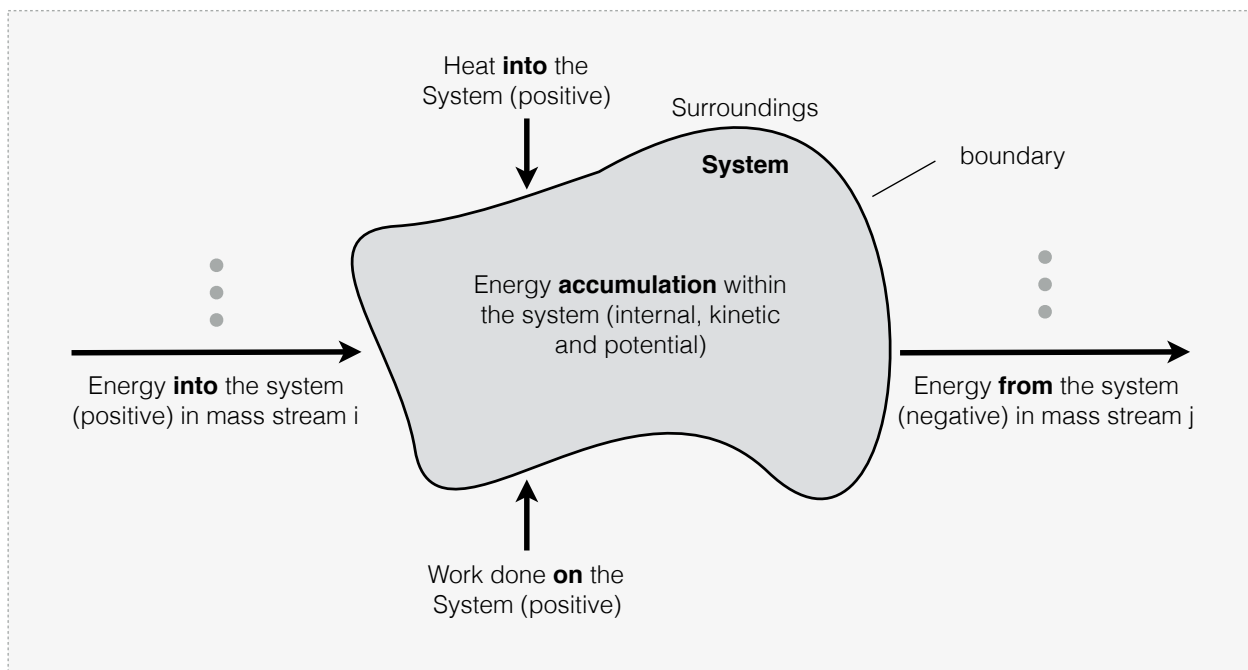


Fig. 1: Schematic of a general system and its surroundings. \mathcal{S} streams enter or exit from the system which can transfer both energy and mass with the surroundings. \mathcal{R} chemical reactions occurring inside the system can act a source or sink of energy for the system.

mass balance equations which describe the energy (or mass) inputs and outputs shown in Fig. 1:

$$d(me)\Big|_{sys} = \delta Q + \delta W + \sum_{s=1}^S \nu_s e_s \delta m_s + \sum_{r=1}^{\mathcal{R}} \delta E_r \quad (3)$$

$$dm = \sum_{s=1}^S \nu_s \delta m_s \quad (4)$$

The symbol e denotes the *total* energy in the system per unit mass (or mol), e_s denotes the *total* energy of stream s (of S possible streams) per unit mass (or mol), m and m_s denote the system mass, and the mass of stream s respectively, while δE_r denotes the heat liberated or consumed by chemical reaction r (of \mathcal{R} possible chemical reactions). Lastly, the quantity ν_s denotes a direction parameter for stream s ; $\nu_s = 1$ if stream s enters the system, while $\nu_s = -1$ if stream s exits the system.

The differential energy and mass balance equations can be converted to the more familiar rate based balances by dividing both sides by a time window Δt and allowing the window to shrink to zero ($\Delta t \rightarrow 0$):

$$\frac{d}{dt}(me)\Big|_{sys} = \dot{Q} + \dot{W} + \sum_{s=1}^S \nu_s e_s \dot{m}_s + \sum_{r=1}^{\mathcal{R}} \dot{E}_r \quad (5)$$

$$\frac{dm}{dt} = \sum_{s=1}^S \nu_s \dot{m}_s \quad (6)$$

where \dot{Q} , \dot{W} , \dot{m}_s denote the *rate* of heat, work and mass transferred to/from the system in stream s . The left-hand side describes the rate of accumulation of total energy (or mass) in the system, while the right-hand side describes the various sources and sinks of total energy (or mass). For most chemical engineering systems, we'll formulate the specific total energy (total energy per unit mass or mol) as the sum of the internal u , kinetic $e_K = (1/2)mv_j^2$ and potential energies $e_P = gz$:

$$e = u + \frac{1}{2}v_j^2 + gz \quad (7)$$

The specific total energy of any stream can also be represented as the sum of the internal, kinetic and potential energies of the molecules in that stream. Putting these ideas together, we can write the general time-dependent macroscopic energy and mass balances as:

$$\frac{d}{dt}\left[m(u + e_K + e_P)\right]\Big|_{sys} = \dot{Q} + \dot{W} + \sum_{s=1}^S \nu_s \left(u_s + gz_s + \frac{1}{2}v_s^2\right) \dot{m}_s + \sum_{r=1}^{\mathcal{R}} \dot{E}_r \quad (8)$$

$$\frac{dm}{dt} = \sum_{s=1}^S \nu_s \dot{m}_s \quad (9)$$

We'll study how to apply these equations to practical chemical engineering problems for the rest of the semester.

What is thermodynamic work?

Let's begin by discussing expansion work in a *closed* system (no exchange of material between the system and the surroundings). In physics, a force does work if, when acting on a body, there is a displacement of the point of application in the direction of the force. Work can be expressed by the relationship:

$$\delta W = \mathbf{F} \cdot d\mathbf{s} \quad (10)$$

where \mathbf{F} denotes a force vector, and $d\mathbf{s}$ denotes a displacement vector. To calculate work using Eqn (10), we must take the scalar (dot or inner) product between the force vector and the displacement vector. We can rewrite the force vector (and similarly the displacement vector) in terms of unit vectors \mathbf{e}_i or:

$$\mathbf{F} = \sum_i F_i \mathbf{e}_i \quad (11)$$

where our unit vectors are *orthonormal* to each other:

$$\mathbf{e}_i \cdot \mathbf{e}_j = (\mathbf{e}_i, \mathbf{e}_j) = \begin{cases} 1 & : i = j \\ 0 & : i \neq j \end{cases} \quad (12)$$

If we substitute the force and displacement vectors into Eqn (10) (our definition of work) we arrive at:

$$\delta W = \sum_i \sum_j F_i ds_j (\mathbf{e}_i, \mathbf{e}_j) \quad (13)$$

which simplifies to:

$$\delta W = \sum_i F_i ds_i \quad (14)$$

because $(\mathbf{e}_i, \mathbf{e}_i) = 1$, and all other cases equal zero.

We'll typically focus on *reversible* pressure-volume expansion work (Fig. 2). Imagine we have an isothermal chamber filled with an ideal gas at temperature T_1 that is being compressed by a weightless, frictionless piston loaded with total mass M . At equilibrium, the gravitational external force pushing down on the piston F_e will be counterbalanced by the force of the gas molecules hitting the piston, F_{sys} . Force is related to pressure through an area, in this case the cross sectional area of the piston A_\perp :

$$F_{sys}/A_\perp - F_e/A_\perp = 0 \quad (15)$$

or $P_{sys} = P_e$ at equilibrium. Substituting the pressure into the differential work expression Eqn (14) gives:

$$\delta W = -P_e A_\perp ds_2 \quad (16)$$

where we have no displacement in the x (s_1) or z (s_3) directions. However, the product $A_\perp ds_2$ describes the displacement of an area, which is volume, thus Eqn. (16) becomes:

$$\delta W = -P_e dV \quad (17)$$

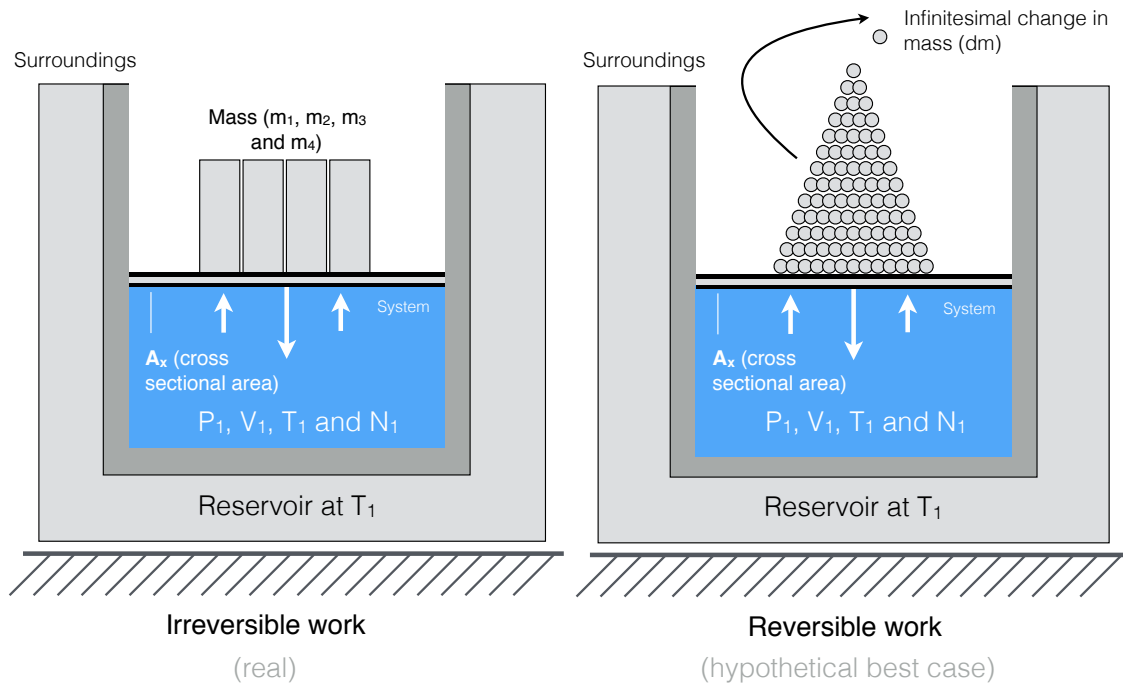


Fig. 2: Schematic of isothermal expansion work for a closed system for finite (irreversible) and hypothetically infinitesimal (reversible) changes in the external pressure.

or after integration of the inexact differential:

$$W = - \int P_e dV \quad (18)$$

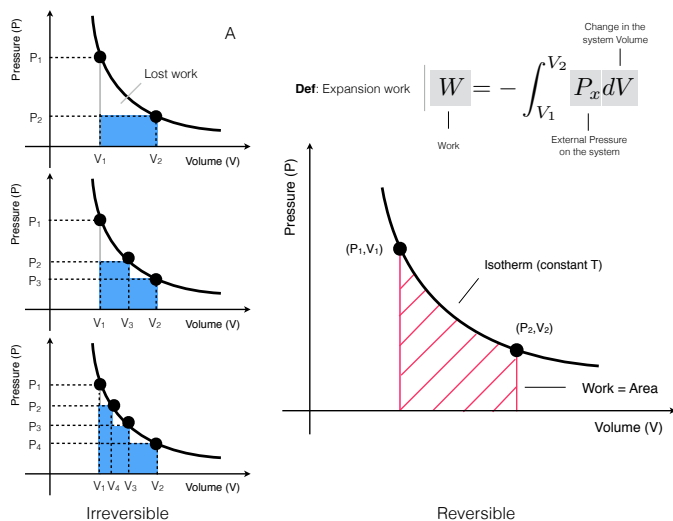


Fig. 3: Schematic of the work generated by irreversible (left) and reversible (right) isothermal expansion of an ideal gas. Reversible work generates the maximum possible work, but is a hypothetical upper bound.

Suppose we remove one of the finite weights on top of the piston (Fig. 2A). Initially, the system is at rest and the internal and external pressures are equal. However, when we remove a finite weight, there will be a mismatch between the system and surrounding pressure ($P_{sys} > P_e$) causing the piston to accelerate upwards. Eventually the pressures will equilibrate, and the piston will come to rest. This type of expansion work is called *irreversible* (perhaps a better term would be non-static or non-equilibrium work). When we were at equilibrium we knew P_{sys} , however, in between the equilibrium states for an irreversible expansion we do not know the system pressure. Imagine instead that

we do a hypothetical expansion in which we break the same weight M into tiny particles of size dM , and remove a single particle at a time. This type of expansion is called *reversible* (perhaps a better name would equilibrium or static work). In this case, the equilibrium assumption remains approximately true, and at each hypothetical stage of the expansion $P_{sys} \simeq P_e$. If the working fluid in the system were an ideal gas (a simple equation of state) valid for only low pressures, the work expression becomes:

$$W = - \int_1^2 \frac{nRT}{V} dV = -nRT_1 \ln \frac{V_2}{V_1} \quad (19)$$

where we used the the ideal gas law $P_e V = nRT$. Expansion work can also be thought of as the area under the curve in the P-V plane (Fig 3). Thus, finite changes in the opposing pressure (no longer in equilibrium with the surroundings) leads to jumps in the P-V plane (and lost work). On the other hand, infinitesimally small changes in the surrounding pressure leads to a smooth expansion and the maximum possible work. Reversible expansions are not real, yet we'll often assume reversible behavior the upper bound of system performance.

Work in an open system The rate of total work in an open system (an open system can exchange both energy and mass with the surroundings) is the sum of two types of work, *shaft* and *flow* work:

$$\dot{W} = \dot{W}_{sh} + \dot{W}_f \quad (20)$$

Shaft work \dot{W}_{sh} is the rate of generation of mechanically useful work, while flow work \dot{W}_f is the energy required to push fluid into or from the system. Thus, for an open system the total rate of work is given by:

$$\dot{W} = \dot{W}_{sh} + \sum_{s=1}^S \nu_s (Pv)_s \dot{m}_s \quad (21)$$

where P_s denotes the pressure of stream s, and v_s denotes specific volume (e.g., L/kg or L/mol) of stream s. Substituting Eqn. (21) into the energy balance Eqn. (8) gives:

$$\left. \frac{d}{dt} [m(u + e_K + e_P)] \right|_{sys} = \dot{Q} + \dot{W}_{sh} + \sum_{s=1}^S \nu_s \{ (Pv)_s + e_s \} \dot{m}_s + \sum_{r=1}^{\mathcal{R}} \dot{E}_r \quad (22)$$

If we collect terms and define a new thermodynamic quantity called the specific enthalpy h ([J/mol] or [J/mass]) for stream j:

$$h_j \equiv u_j + (Pv)_j \quad (23)$$

we arrive at the total macroscopic energy balance for an open system:

$$\left. \frac{d}{dt} [m(u + e_K + e_P)] \right|_{sys} = \dot{Q} + \dot{W}_{sh} + \sum_{s=1}^S \nu_s (h + e_K + e_P)_s \dot{m}_s + \sum_{r=1}^{\mathcal{R}} \dot{E}_r \quad (24)$$

$$\frac{dm}{dt} = \sum_{s=1}^S \nu_s \dot{m}_s \quad (25)$$

Aside: What is $d(\cdot)$ versus $\delta(\cdot)$? A curious feature of Eqn (3) and (4) is the $d(\cdot)$ versus the $\delta(\cdot)$ operators; the $d(\cdot)$ operator denotes an *exact* differential, while $\delta(\cdot)$ denotes an *inexact* differential. We'll talk more about this later, but an easy way to think about the difference between these operators is that exact differentials describe changes in system quantities, while inexact differentials describes actions taken on the system (adding mass, adding heat etc). Mathematically, integrals of exact differentials take the form:

$$\Delta x = \int_{x_1}^{x_2} dx \quad (26)$$

while integrals of inexact differentials are given by:

$$x = \int \delta x \quad (27)$$

The first law of thermodynamics for a closed system.

Let's begin by simplifying the differential energy and mass balances; consider a *closed* system, with no chemical reactions consisting of a pure working fluid that obeys the general equation of state:

$$\mathcal{F}(P, V, T, n) = 0 \quad (28)$$

Lets also assume we can ignore changes in the potential and kinetic energy. In a closed system, $\delta m_s = 0$ for all streams ($\forall s$), and no chemical reactions says that $\sum_{r=1}^{\mathcal{R}} \delta E_r = 0$. Thus, our energy and material balances reduce to:

$$d(mu) \Big|_{sys} = \delta Q + \delta W \quad (29)$$

$$dm = 0 \quad (30)$$

Expanding the differential on the left hand side of the energy balance leads to:

$$md(u) \Big|_{sys} + ud(m) \Big|_{sys} = \delta Q + \delta W \quad (31)$$

However, we know that $dm = 0$ (closed system), so the energy balance further reduces to:

$$dU = \delta Q + \delta W \quad (32)$$

where we have dropped the explicit system reference and absorbed the mass. Solving for δQ and substituting our definition of PV-work

$$\delta W = -PdV \quad (33)$$

yields:

$$\delta Q = dU + PdV \quad (34)$$

where P denotes the system pressure (assumed to be equilibrium with the surroundings) and V denotes the volume of the system. Eqn (34) is the differential form of the *first law of thermodynamics* for a closed system.

The first law of thermodynamics for an open system.

Let's begin by simplifying the open time-dependent mass and energy balance equations; assume no chemical reactions, and the change in kinetic and potential energy in the system and all streams is negligible. These assumptions applied to the mass and energy balances give:

$$\left. \frac{d}{dt} [mu] \right|_{sys} = \dot{Q} + \dot{W}_s + \sum_{s=1}^S \nu_s h_s \dot{m}_s \quad (35)$$

$$\frac{dm}{dt} = \sum_{s=1}^S \nu_s \dot{m}_s \quad (36)$$

This system of equations is the time dependent first law of thermodynamics (in the absence of chemical reactions). However, often we are concerned with processes at steady state; if the system is at steady state, the time derivatives vanish leaving the steady state open first law of thermodynamics:

$$\dot{Q} + \dot{W}_{sh} + \sum_{s=1}^S \nu_s h_s \dot{m}_s = 0 \quad (37)$$

$$\sum_{s=1}^S \nu_s \dot{m}_s = 0 \quad (38)$$

Example: Consider a steady-state two stage flow calorimeter with a resistance heating element stage 1 (inlet) connected with a measurement unit in stage 2 (outlet). Liquid water enters the heater stage at $T_1 = 0^\circ\text{C}$ and exists the measurement unit (as a vapor) at $T_2 = 300^\circ\text{C}$. The following data were taken from the inlet and outlet of the calorimeter: $\dot{m}_1 = 4.15 \text{ g s}^{-1}$, $P_2 = 3 \text{ bar}$ and $\dot{Q} = 12,740 \text{ W}$. The liquid water is completely vaporized in this process. Calculate the specific enthalpy of steam at the outlet of the measurement unit h_2 . Assume no shaft work, insulated pipes and process units, and negligible changes in the kinetic and potential energy.

Solution: Starting from the steady-state open first law equation:

$$\dot{Q} + \dot{W}_{sh} + \sum_{s=1}^S \nu_s h_s \dot{m}_s = 0 \quad (39)$$

we can begin throwing out terms. First, $\dot{W}_{sh} = 0$ (from the problem statement). Next, we have two streams, so $S = 2$ with $\nu_1 = 1$ and $\nu_2 = -1$ from the process diagram. Thus, the open first law equation for this problem is given by:

$$\dot{Q} + h_1 \dot{m}_1 - h_2 \dot{m}_2 = 0 \quad (40)$$

However, we know the calorimeter unit is at steady-state, which implies $\dot{m}_1 = \dot{m}_2 \equiv \dot{m}$, thus:

$$\dot{Q} = \dot{m} (h_2 - h_1) \quad (41)$$

Solving for the enthalpy at the outlet gives:

$$h_2 = h_1 + \frac{\dot{Q}}{\dot{m}} \quad (42)$$

From the steam tables, $h_1 = 0$, which leaves:

$$h_2 = (12,740 \text{ J s}^{-1}) / (4.15 \text{ g s}^{-1}) = 3,070 \text{ J g}^{-1} \quad (43)$$

Derivation of general heat capacity relationships.

Imagine that we have a function that describes how the internal energy of a system $U(\cdot)$ varies with other thermodynamic states x_1, x_2, \dots, x_N :

$$U(x_1, x_2, \dots, x_N) = 0 \quad (44)$$

We can take the *total differential* of the internal energy equation:

$$dU = \sum_{j=1}^N \left(\frac{\partial U}{\partial x_j} \right)_{x_1, x_2, \dots, x_N, j} dx_j \quad (45)$$

and substitute this into Eqn. (34) to arrive at:

$$\delta Q = \sum_{j=1}^N \left(\frac{\partial U}{\partial x_j} \right)_{x_1, x_2, \dots, x_N, j} dx_j + PdV \quad (46)$$

Equation (46) is a completely general equation that relates the change in heat δQ to the internal energy of the system. For single component systems, the states x_1, x_2, \dots, x_N are combinations of four variables, temperature, pressure, volume and abundance (the number of particles in the system). However, since we have a closed system with no chemical reactions, our state variables are simply the temperature, pressure and volume. If we specify two of these variables we can calculate the third from the state equation. This leads to three possible system configurations (for a constant abundance system):

- (T, V) systems: If the independent state variables are temperature T and volume V , we can write dU as:

$$dU = \left(\frac{\partial U}{\partial T} \right)_V dT + \left(\frac{\partial U}{\partial V} \right)_T dV \quad (47)$$

which yields a differential energy balance of the form:

$$\delta Q = \left(\frac{\partial U}{\partial T} \right)_V dT + \left[\left(\frac{\partial U}{\partial V} \right)_T + P \right] dV \quad (48)$$

- (T, P) systems: If the independent state variables are pressure P and temperature T , we can write dU as:

$$dU = \left(\frac{\partial U}{\partial T} \right)_P dT + \left(\frac{\partial U}{\partial P} \right)_T dP \quad (49)$$

which yields a differential energy balance of the form:

$$\delta Q = \left[\left(\frac{\partial U}{\partial T} \right)_P + P \left(\frac{\partial V}{\partial T} \right)_P \right] dT + \left[\left(\frac{\partial U}{\partial P} \right)_T + P \left(\frac{\partial V}{\partial P} \right)_T \right] dP \quad (50)$$

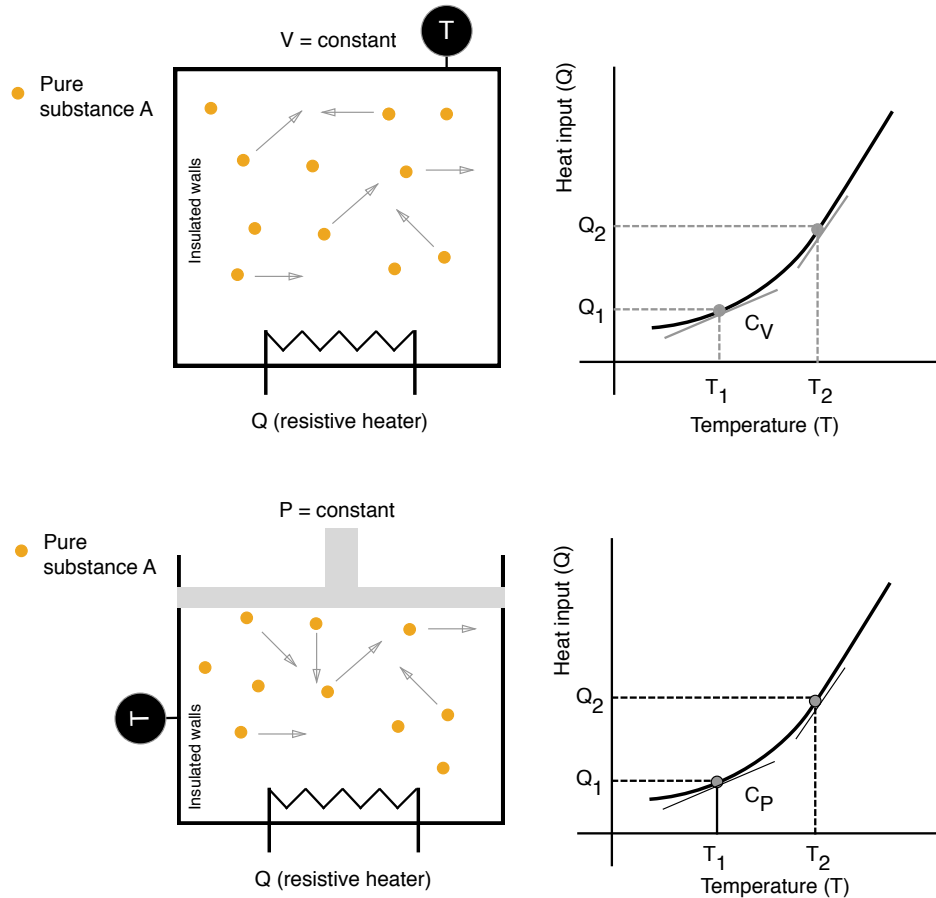


Fig. 4: Schematic of the experimental setup for a constant volume (top) and a constant pressure (bottom) heat capacity experiment for a pure substance A.

where $V(T, P)$ gives:

$$dV = \left(\frac{\partial V}{\partial T} \right)_P dT + \left(\frac{\partial V}{\partial P} \right)_T dP \quad (51)$$

- (P, V) systems: If the independent state variables are pressure P and volume V , we can write dU as:

$$dU = \left(\frac{\partial U}{\partial P} \right)_V dP + \left(\frac{\partial U}{\partial V} \right)_P dV \quad (52)$$

which yields a differential energy balance of the form:

$$\delta Q = \left(\frac{\partial U}{\partial P} \right)_V dP + \left[\left(\frac{\partial U}{\partial V} \right)_P + P \right] dV \quad (53)$$

Changes in internal energy at constant volume. Definition of C_V . Let's suppose we have a (T, V) system with a pure substance. When we supply heat at a constant volume (Fig. 4, top), Eqn (48)

reduces to:

$$\delta Q_V = \left(\frac{\partial U}{\partial T} \right)_V dT \quad (54)$$

where $dV = 0$. If we divide both sides by dT , we arrive at an expression which describes how the internal energy changes with temperature:

$$C_V \equiv \frac{\delta Q_V}{dT} = \left(\frac{\partial U}{\partial T} \right)_V \quad (55)$$

where the subscript V denotes the derivatives are calculated at constant volume. The quantity C_V is called the constant volume heat capacity. The term $\delta Q/dT$ (and hence the heat capacity) can easily be measured experimentally (Fig 4). If we integrate both sides of Eqn. (55) with respect to temperature, we arrive at:

$$\Delta U = \int_{T_1}^{T_2} C_V dT \quad (56)$$

Note that C_V is typically a strong function of temperature, so if T_1 and T_2 span a large temperature range, we *cannot* pull C_V out the integral. Instead, we have to estimate how C_V varies with temperature, for example estimating C_V at many different temperatures and then fitting the results to function of temperature.

Changes in internal energy at constant pressure. Definition of C_P . For a constant pressure system, let's start with Eqn. (50). When we supply heat at a constant pressure (Fig. 4, bottom) $dP = 0$, which reduces Eqn. (50) to:

$$\delta Q_P = \left[\left(\frac{\partial U}{\partial T} \right)_P + P \left(\frac{\partial V}{\partial T} \right)_P \right] dT \quad (57)$$

If we divide both sides of the constant pressure δQ_P expression by dT we arrive at:

$$\frac{\delta Q_P}{dT} = \left(\frac{\partial U}{\partial T} \right)_P + P \left(\frac{\partial V}{\partial T} \right)_P \quad (58)$$

The right-hand side of Eqn. (58) is the sum of an internal energy term and a constant pressure expansion term, which is similar to the definition of enthalpy from the open energy balance:

$$H \equiv U + PV \quad (59)$$

Computing the total differential of H gives:

$$dH = dU + PdV + VdP \quad (60)$$

However, we are at constant pressure ($dP = 0$), which reduces the enthalpy differential to:

$$dH = dU + PdV \quad (61)$$

Differentiating both sides of Eqn. (61) with respect to temperature (at constant pressure) gives the expression:

$$\left(\frac{\partial H}{\partial T}\right)_P = \left(\frac{\partial U}{\partial T}\right)_P + P \left(\frac{\partial V}{\partial T}\right)_P \quad (62)$$

Thus, the change in the internal energy of a material as a function of temperature, when measured at constant pressure, is equal to the change in enthalpy:

$$C_P \equiv \frac{\delta Q_P}{dT} = \left(\frac{\partial H}{\partial T}\right)_P \quad (63)$$

Similar to the constant volume heat capacity, we can decompose Eqn. (63) to solve for the change in enthalpy resulting from a change in temperature (at a constant pressure):

$$\Delta H = \int_{T_1}^{T_2} C_P dT \quad (64)$$

Also like the constant volume heat capacity, C_P can be a strong function of T ; thus, we typically cannot pull it out the temperature integral for large changes in temperature.

Is there a relationship between C_V and C_P ? Intuitively, given the same pure substance and the same heat input, you would expect that there is a relationship between C_V and C_P . To explore this question, let's consider the first-law written for a (T, V) system held at a constant pressure P :

$$\delta Q_P = \left(\frac{\partial U}{\partial T}\right)_V dT + \left[\left(\frac{\partial U}{\partial V}\right)_T + P\right] dV \quad (65)$$

Using our definition of the constant volume heat capacity, we can rewrite Eqn. (65) as:

$$\delta Q_P = C_V dT + \left[\left(\frac{\partial U}{\partial V}\right)_T + P\right] dV \quad (66)$$

which, after differentiating with respect to temperature at a constant pressure becomes:

$$\frac{\delta Q_P}{dT} = C_V + \left[\left(\frac{\partial U}{\partial V}\right)_T + P\right] \frac{\partial V}{\partial T}_P \quad (67)$$

Again, using our definition of constant pressure heat capacity this time, Eqn. (67) reduces to:

$$C_P - C_V = \left[\left(\frac{\partial U}{\partial V}\right)_T + P\right] \left(\frac{\partial V}{\partial T}\right)_P \quad (68)$$

Equation (68) governs the general relationship between C_P and C_V for an arbitrary pure material. Although we have not (yet) explicitly shown it, the quantity of the right-hand side of Eqn. (68) is always greater than zero, thus $C_P > C_V$. To work out the exact difference between the heat capacities, we need an *equation of state* for the material we are exploring.

Example: Derive the difference between the constant volume and constant pressure heat capacities assuming an ideal gas as the working fluid.

Solution: The internal energy of an ideal gas can be calculated from statistical mechanics and is given by:

$$U = \frac{3}{2}Nk_B T \quad (69)$$

Thus, the first term on the right side of Eqn. (68) vanishes i.e., $(\partial U / \partial V)_T = 0$ because U is only a function of T for an ideal gas. This leaves us with the volume expansion term:

$$C_P - C_V = P \left(\frac{\partial V}{\partial T} \right)_P \quad (70)$$

Rearranging the ideal gas law for V , and differentiating with respect to temperature T yields:

$$\left(\frac{\partial V}{\partial T} \right)_P = \frac{nR}{P} \quad (71)$$

which, when substituted into Eqn. (70), yields:

$$C_P - C_V = nR \quad (72)$$

where n denotes the number of mols of ideal gas, and R denotes the ideal gas constant.

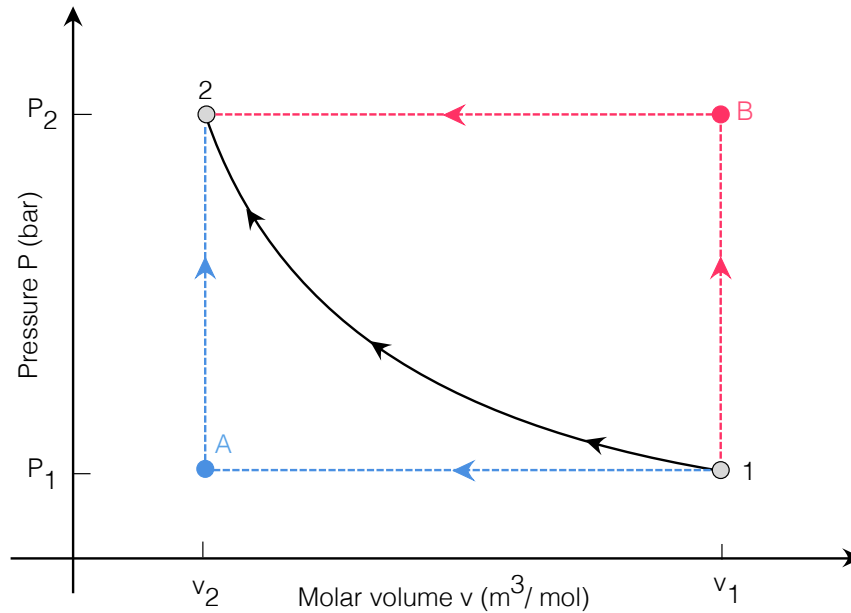


Fig. 5: Thermodynamic paths for the compression of air.

Challenge example: 1 mol of air at $P = 1$ bar and $T = 298.15\text{K}$ is compressed to 5 bar and 298.15K by two different mechanically reversible processes:

- (a) Cooling at constant pressure followed by heating at constant volume
- (b) Heating at constant volume followed by cooling at constant pressure

The overall compression process, and the two hypothetical reversible pathways to accomplish the compression are shown in Fig. 5. Calculate the heat and work requirements, ΔU and ΔH of the air for each path. The heat capacities for air: $C_V = 20.78 \text{ J mol}^{-1} \text{ K}^{-1}$ and $C_P = 29.10 \text{ J mol}^{-1} \text{ K}^{-1}$. Assume both C_V and C_P are independent of temperature. Also assume air is an ideal gas, with a molar volume $v = 0.02479 \text{ m}^3 \text{ mol}^{-1}$ at $T = 298.15\text{K}$ and $P = 1$ bar.