

Sequence Specific Modeling of *E. coli* Cell-Free Protein Synthesis

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Abstract

Cell-free protein expression has become a widely used research tool in systems and synthetic biology, and a promising technology for personalized medicine. In this study, we used sequence specific constraint based modeling to evaluate the performance of an *E. coli* cell-free protein synthesis system. A core *E. coli* metabolic model, describing glycolysis, the pentose phosphate pathway, amino acid biosynthesis and degradation and energy metabolism, was augmented with sequence specific descriptions of transcription and translation processes, and effective models of promoter function. Thus, sequence specific constraint based modeling explicitly couples transcription and translation processes, and the regulation of gene expression, with the availability of metabolic resources. We tested this approach by simulating the expression of two model proteins chloramphenicol acetyltransferase and dual emission green fluorescent protein for which we have training data sets; we then expanded the simulations

to a range of therapeutically relevant proteins. Protein expression simulations were consistent with measurements for a variety of cases. Further, global sensitivity analysis identified the key metabolic processes that controlled the productivity, energy efficiency, and carbon yield of the process. Taken together, sequence specific constraint based modeling offers a novel means to *a priori* estimate the performance of cell-free synthetic circuits.

Keywords

Synthetic biology, constraints based modeling, cell-free protein synthesis

1 Introduction

Cell-free protein expression has become a widely used research tool in systems and synthetic biology, and a promising technology for personalized protein production. From the perspective of research, cell-free systems offer many advantages for the study, manipulation and modeling of metabolism compared to *in vivo* processes. Central amongst these, is direct access to metabolites and the biosynthetic machinery without the interference of a cell wall, or complications associated with cell growth. This allows us to interrogate the chemical environment while the biosynthetic machinery is operating, potentially at a fine time resolution. Cell-free protein synthesis (CFPS) systems are arguably the most prominent examples of cell-free systems used today (1). However, CFPS is not new; CFPS in crude *E. coli* extracts has been used since the 1960s to explore fundamental biological mechanisms (2, 3). Today, cell-free systems are used in a variety of applications ranging from therapeutic protein production (4) to synthetic biology (5). However, if CFPS is to become a mainstream technology for advanced applications such as point of care manufacturing (6), we must first understand the performance limits and cost of these systems (1). One tool to address these questions is mathematical modeling.

Stoichiometric reconstructions of microbial metabolism, popularized by constraint based approaches such as flux balance analysis (FBA), have become standard tools to interrogate metabolism (7). Constraint based methods such as FBA, metabolic flux analysis (MFA) (8), and convex network decomposition approaches such as elementary modes (9) or extreme pathways (10) model intracellular metabolism using biochemical stoichiometry and other constraints such as thermodynamical feasibility (11, 12) under pseudo steady state conditions. Constraint based approaches have predicted productivity (13, 14), yield (13), mutant behavior (15), and growth phenotypes (16) for biochemical networks of arbitrary complexity, including genome scale networks, using linear programming (17). Since the first genome scale stoichiometric model of *E. coli* (18), stoichiometric reconstructions of hundreds of organisms, including industrially important prokaryotes such as *E. coli* (19) or *B. subtilis* (20), are now available (21). Stoichiometric reconstructions have been expanded to include the integration of metabolism with detailed descriptions of gene expression (ME-Model) (16, 22), and protein structures (GEM-PRO) (23, 24). These expansions have greatly increased the scope of questions these models can explore. Constraint based methods are powerful tools to estimate the performance of metabolic networks with very few adjustable parameters. However, constraint based methods are typically used to model *in vivo* processes, and have not yet been applied to cell-free metabolism.

In this study, we used sequence specific constraint based modeling to evaluate the performance of *E. coli* cell-free protein synthesis (CFPS). A core *E. coli* cell-free metabolic model was developed from literature (19). This model, which described glycolysis, pentose phosphate pathway, amino acid biosynthesis and degradation and energy metabolism, was then augmented with sequence specific descriptions of promoter function, transcription and translation processes. Thus, sequence specific constraints based modeling explicitly coupled transcription and translation with the availability of metabolic resources. We tested this approach by simulating the production of two model proteins, and then investigated the productivity, energy efficiency, and carbon yield for eight different proteins.

From this, higher carbon number proteins typically had lower productivity rates, energy efficiency, and carbon yields than that of the lower carbon number proteins. Further, global sensitivity analysis identified the key metabolic processes that controlled circuit performance, showing oxidative phosphorylation as instrumental for maintaining a high energy efficiency and carbon yield and the translation rate for productivity. Taken together, sequence specific constraints based modeling offers a novel means to *a priori* estimate the performance of cell-free synthetic circuits.

2 Results and discussion

2.1 Model derivation and validation

The cell-free stoichiometric network was constructed by removing growth associated reactions from the *iAF1260* reconstruction of K-12 MG1655 *E. coli* (19), and adding deletions associated with the specific cell-free system (see materials and methods). We then added the transcription and translation template reactions of Allen and Palsson for the specific proteins of interest (22). A schematic of the metabolic network, which consisted of 264 reactions and 146 species, is shown in Fig. 1A. The network described the major carbon and energy pathways, as well as amino acid biosynthesis and degradation pathways. Using this network, in combination with effective promoter models taken from Moon et al. (25), and literature values for cell-free culture parameters (Table 2), we simulated the sequence specific production of two model proteins, chloramphenicol acetyltransferase (CAT) and dual emission green fluorescent protein (deGFP) using different *E. coli* cell-free extracts. The cell-free metabolic network, along with all model code and parameters, can be downloaded under an MIT software license from the Varnerlab website (26).

Cell-free simulations of the time evolution of CAT and deGFP production were consistent with experimental measurements (Fig. 1B and C). Chloramphenicol acetyltransferase (CAT), was produced under a T7 promoter in a glucose/NMP cell-free system (27) using glucose as a carbon and energy source (Fig. 1B). With the exception of the first 10-15 min, the cell-free prediction of CAT abundance was consistent with the measured values (coefficient of determination, $R^2 = 0.86$). On the other hand, deGFP was produced under a P70a promoter in TXTL 2.0 *E. coli* extract for eight hours using maltose as a carbon and energy source (Fig. 1C). The cell-free simulation captured the overall trend of deGFP abundance, but failed to capture saturation at the end of the CFPS culture ($R^2 = 0.84$). Uncertainty in experimental factors such as the concentration of RNA polymerase, ribosomes, transcription and translation elongation rates or the upper bounds for oxygen and glucose consumption

rates (modeled as being normally distributed around the parameter values shown in Table 2) did not qualitatively alter the performance of the model (blue region, 95% confidence estimate). Together, these simulations suggested the description of transcription and translation, and its integration with metabolism encoded in the cell-free metabolic model, were consistent with experimental measurements. However, these simulations were conducted at a single plasmid concentration of 5 nM. Thus, it was unclear if the model could capture cell-free protein synthesis for a range of plasmid concentrations.

Cell-free simulations of the deGFP titer for a range of plasmid concentrations were consistent with experimental measurements (Fig. 1D). The cell-free deGFP titer at each plasmid concentration was calculated by multiplying the flux of deGFP synthesis by the active time of production, approximately 8 hours in TXTL 2.0 (28). The mean of the ensemble (calculated by sampling the uncertainty in the model parameters) captured the saturation of deGFP production as a function of plasmid concentration ($R^2 = 0.97$). However, while the mean and 95% confidence estimate of the ensemble were consistent with measured deGFP levels, the model under predicted the deGFP titer at the saturating point of 5 nM of plasmid concentration. These results, in combination with the time-dependent CAT and deGFP simulations, validated our CFPS modeling approach which required very few adjustable parameters. It also showed that the sequence specific template reactions and metabolic network were sufficient to predict the production of different proteins under different promoters, and cell-free systems. Next, we used our modeling approach to better understand the theoretical performance limits of CFPS.

2.2 Analysis of CFPS performance

To better understand the performance of CFPS reactions, we analyzed the productivity, energy efficiency and carbon yield for the cell-free production of eight model proteins with and without amino acid supplementation (Fig. 2). The expression of each of these proteins was under a P70a promoter, with the exception of CAT which was expressed

using a T7 promoter. In all cases, the CFPS reaction was supplied with glucose; however, we considered different scenarios for amino acid supplementation. First, the CFPS reaction was supplied with amino acids, and simultaneously was also allowed to synthesize amino acids from glucose (AAs supplied and *de novo* synthesis). Next, the CFPS reaction was supplied with both glucose and amino acids, but *de novo* amino acid biosynthesis was not allowed (AAs supplied w/o *de novo* synthesis). This scenario was consistent with common cell-free extract preparation protocols which often involve amino acid supplementation; thus, we expect the enzymes responsible for amino acid biosynthesis to be largely absent from the CFPS reaction in these cases. Lastly, the cell-free reaction was given glucose but not supplemented with amino acids, and was forced to synthesize them *de novo* from glucose (*de novo* synthesis only). Eight proteins, ranging in size, were selected to evaluate CFPS performance: bone morphogenetic protein 10 (BMP10), chloramphenicol acetyltransferase (CAT), caspase 9 (CASP9), dual emission green fluorescent protein (deGFP), prothrombin (FII), coagulation factor X (FX), fibroblast growth factor 21 (FGF21), and single chain variable fragment R4 (scFvR4). An additional case was considered for CAT, where central metabolic fluxes were constrained by experimental metabolic measurements of glucose, organic and amino acid consumption/production rates (see supplemental materials). Using these model proteins, we developed effective correlation models that predicted the productivity, energy efficiency and carbon yield given the carbon number of the model protein. Finally, we independently validated the effective correlations with a protein not in our original data set, maltose binding protein (MBP).

2.2.1 Productivity

The theoretical maximum productivity for proteins expressed using a P70a promoter ($\mu\text{M}/\text{h}$) was inversely proportional to the carbon number (C_{POI}) and varied between 1 and 12 $\mu\text{M}/\text{h}$ for the proteins sampled (Fig. 2A-B). The theoretical maximum productivity was within a standard deviation with and without amino acid supplementation for each

protein, but varied significantly between proteins. Productivity was a non-linear function of protein length; for instance, BMP10 (424 aa) had a optimal productivity of approximately $2.5 \mu\text{M}/\text{h}$ whereas the optimal productivity of deGFP (229 aa) was approximately $8.4 \mu\text{M}/\text{h}$. To examine the influence of protein length, the mean optimal productivity was plotted against the carbon number of each protein (Fig. 2B). The optimal productivity and protein length were related by the power-law relationship $\alpha \times (C_{POI})^\beta$, where $\alpha = 6.02 \times 10^6 \mu\text{M}/(\text{h} \cdot \text{carbon number})$ and $\beta = -1.93$ for a P70a promoter. Interestingly, CAT did not obey the P70a power-law relationship; the relatively high productivity of CAT was due to its T7 promoter. The higher transcription rate of the T7 promoter led to a 34% higher mRNA steady state level, resulting in a higher productivity. However, CAT expressed under a P70a promoter followed the P70a power-law correlation with a productivity of approximately $8.2 \pm 2.2 \mu\text{M}/\text{h}$ (predicted to be $7.2 \mu\text{M}/\text{h}$ by the optimal productivity correlation).

We independently validated the productivity correlation by calculating the optimal productivity of MBP using the full model and the effective correlation model (Fig. 2B). The prediction error was less than 8% for an *a priori* prediction of CFPS productivity using the effective correlation. Thus, the effective productivity correlation could be used as a parameter free method to estimate optimal productivity for cell free protein production using a P70a promoter. For CFPS using other promoters, a similar correlation model could be developed. For example, maximal transcription occurs when the promoter model coefficient $u(\kappa) = 1$; the theoretical maximum productivity correlation for maximum promoter activity also followed a power-law distribution ($\alpha = 1.39 \times 10^7 \mu\text{M}/(\text{h} \cdot \text{carbon number})$ and $\beta = -1.99$) (Fig. 2B, gray). The CAT value under a T7 promoter was similar to the maximal possible productivity as $u_{T7}(\kappa) \simeq 0.95$ given the T7 promoter model parameters used in this study (Table 2). Taken together, the maximum optimal productivity of a cell-free reaction was found to be inversely proportional to protein size, following a power-law relationship for proteins expressed under a P70a promoter.

2.2.2 Energy efficiency

The optimal energy efficiency of protein synthesis was independent of protein length, with and without amino acid supplementation (Fig. 2C-D). The optimal energy efficiency was approximately 86% for the model proteins sampled. The optimal energy efficiency was independent of the protein length; $m_Y \times (C_{POI}) + b_Y$ where $m_Y = -4.01 \times 10^{-4}$ energy efficiency (%) / carbon number with supplementation, and $m_Y = 3.03 \times 10^{-3}$ energy efficiency (%) / carbon number without supplementation. The y-intercept $b_Y = 86.20$ energy efficiency (%) with supplementation, and $b_Y = 67.40$ energy efficiency (%) without supplementation. In the presence of amino acids, energy was utilized to power CFPS instead of synthesizing amino acids, thus a constant level of energy efficiency was observed regardless of the protein size. In the absence of supplementation, there was a drop in energy efficiency, ranging from 68% to 76%. In this case, glucose consumption more than doubled (64% increase for CAT) compared to cases supplemented with amino acids, meanwhile the productivity was similar for each protein (Fig. 2D). Therefore, the energy burden required for synthesizing each amino acid, and powering CFPS, lowered the energy efficiency. Surprisingly, without amino acid supplementation, proteins with a higher carbon number had a marginally higher energy efficiency; however, this linear trend was mostly independent of protein size ($R^2 = 0.65$). MBP showed good agreement with the linear efficiency model with and without amino acid supplementation. The estimated MBP energy efficiency had a maximum error of 5% without supplementation, and an error of 1% - 3% in the presence of amino acid.

Experimentally constrained CAT simulations showed suboptimal energy efficiency (Fig. 2D, dagger). CAT production was simulated using the constraint based model in combination with experimental measurements of glucose consumption, organic and amino acid consumption and production rates (Fig. 1B). The experimentally constrained energy efficiency was $13.3 \pm 5.0\%$ compared to the theoretical maximum of approximately $84 \pm 0.1\%$. Given that the CAT productivity was similar between the simulated and measured

systems, differences in the glucose consumption rate and the ATP yield per glucose were likely responsible for the difference between the optimal and experimental systems. The glucose consumption rate was approximately 30 - 40 mM/h in the experimental system (even in the presence of amino acids). On the other hand, the constraint based simulation suggested the optimal glucose consumption rate was significantly less than the observed rate, approximately 1 - 7 mM/h (depending upon amino acid supplementation). In the constraint based simulation, the CFPS reaction produced only acetate as a by-product, but in the experimental system acetate, lactate, pyruvate, succinate and malate accumulated during the first hour of production. Thus, the constraint based simulation was more carbon efficient. Next, the energy produced per unit glucose was different between the optimal and experimental constrained system. In the optimal simulation, 12 ATPs were produced per glucose (the theoretical maximum for this network was 21), while the experimentally constrained simulation produced only 4 ATPs per glucose. Thus, approximately 120 - 160 mM ATP/hr was produced in the experimental system, in contrast to 12 - 84 mM ATP/hr for the optimal simulations. We know from measurements that ATP did not accumulate in the experimental system, rather it was consumed by a variety of pathways that were not active in the optimal simulation. This suggested that CFPS retained a growth like operational memory that led to over consumption of glucose, and the over production of ATP.

2.2.3 Carbon Yield

The theoretical maximum carbon yield was inversely proportional to protein length and varied between 40% to 64% for the proteins sampled (Fig. 2E-F). The relationship between the optimal carbon yield and carbon number was linear; $m_Y \times (C_{POI}) + b_Y$ where $m_Y = -8.03 \times 10^{-3}$ carbon yield (%) / carbon number with supplementation, and $m_Y = -6.98 \times 10^{-3}$ carbon yield (%) / carbon number without supplementation. The y-intercept $b_Y = 63.83$ carbon yield (%) with supplementation, and $b_Y = 58.86$ carbon yield (%) without

supplementation. The linear yield models showed good predictability for estimating the optimal carbon yield for a range of carbon numbers ($R^2 = 0.95$ with amino acids and $R^2 = 0.90$ without supplementation), irrespective of the promoter used to control protein expression. The MBP prediction also showed good agreement with the constraint based model, with a prediction error between 3% to 4% with and without amino acid supplementation. The effective yield models were approximately parallel, with a drop in carbon yield of approximately 7% without amino acids. The difference between the cases was associated with glucose consumption. In the absence of amino acids, glucose consumption increased, with the change in the carbon yield being largely accounted for by increased CO_2 production with supplementation.

The carbon yield for experimentally constrained CAT production was 6.2% compared to the theoretical maximum of 58% (Fig. 2F, dagger). Given that the CAT productivity was similar between the simulated and measured systems, differences in the glucose consumption rate and byproduct accumulation were likely responsible for the difference between the optimal and experimental systems. The translation rate has been identified as the rate-limiting step for cell-free protein synthesis (29, 30), thus increased glucose consumption only hindered the carbon yield of CAT. The experimental system was not as energy efficient as the optimal system which resulted in the increased glucose consumption. Since CAT productivity could not be improved, the increased carbon consumption accumulated in byproducts such as pyruvate, acetate, lactate, succinate and malate. The accumulation of acetate and lactate also indicated that oxidative phosphorylation activity was limited. Thus to improve carbon yield for CFPS, energy efficiency should be improved to lower the glucose consumption rate, or the translation rate should be improved for increased protein productivity. However, it may also be hypothesized that only the amino acids supplied contribute to the carbon yield of the protein of interest, while glucose is used to energize CFPS. In this case, the carbon yield for the optimal and experimental systems was approximately 100%. Therefore, the energy efficiency of CFPS is left to be improved.

2.3 Global sensitivity analysis

To better understand the effect of substrate utilization and the transcription/translation parameters on CFPS performance, we performed global sensitivity analysis on the productivity, energy efficiency and carbon yield for the CAT protein (Fig. 3 and Fig. 1 in supporting information). Surprisingly, RNAP and ribosome abundance had only a modest effect; the translation elongation rate had the largest effect on protein productivity. On the other hand, oxygen followed by substrate consumption had the largest influence on the energy efficiency and carbon yield, respectively. The significance of transcription/translation parameters was robust to amino acid supplementation, with the translation rate being the most sensitive across all cases (Fig. 3A). This suggested that the translation elongation rate, and not transcriptional parameters, controlled productivity. Underwood and coworkers showed that an increase in ribosome levels did not significantly increase protein yields or rates; however, adding elongation factors increased protein synthesis rates by 27% (29). In addition, Li et al. increased the productivity by 5-fold of firefly luciferase in PURE CFPS by first improving the rate-limiting step, translation, followed by transcription by adjusting elongation factors, ribosome recycling factor, release factors, chaperones, BSA, and tRNAs (30). In examining substrate utilization, glucose consumption was not important for productivity in the presence of amino acid supplementation. However, its importance increased significantly when amino acids were not available. On the other hand, amino acid consumption was only sensitive when amino acids synthesis reactions were blocked, as it was the only source of amino acids for CAT synthesis. The oxygen consumption rate was the most important factor controlling the energy efficiency of cell-free protein synthesis (Fig. 3B). In the model, we assumed that ATP could be produced by both substrate level and oxidative phosphorylation. Jewett and coworkers reported that oxidative phosphorylation still operated in cell-free systems, and that the protein titer decreased from 1.5-fold to 4-fold when oxidative phosphorylation reactions were inhibited in pyruvate-powered CFPS (1). However, it is unknown how active oxidative phosphorylation is for a glucose

powered cell-free system. Moreover, the connection between oxidative phosphorylation activity and other performance metrics, such as the carbon yield, is also unclear.

To investigate the connection between carbon yield and oxidative phosphorylation further, we calculated the optimal CAT carbon yield as a function of the oxidative phosphorylation flux (Fig. 5). Oxidative phosphorylation had a strong effect on the carbon yield, both with and without amino acid supplementation. In the presence of amino acid supplementation, the carbon yield ranged from 20% to approximately 60%, depending upon the oxidative phosphorylation flux. However, without amino acid supplementation, the carbon yield dropped to approximately 10%, and reached a maximum of 50%. In the absence of supplementation, a lower carbon yield was expected for the same oxidative phosphorylation flux, as glucose was utilized for both energy generation and amino acid biosynthesis. In all cases, whenever the carbon yield was below its theoretical maximum, there was an accumulation of both acetate and lactate. The experimental dataset exhibited a mixture of acetate and lactate accumulation during CAT synthesis, which suggested the CFPS reaction was not operating with optimal oxidative phosphorylation activity. Oxidative phosphorylation is a membrane associated process, however CFPS has no cell membrane. Jewett et al. hypothesized that membrane vesicles present in the CFPS reaction carry out oxidative phosphorylation (1). In addition, they were able to enhance the production yields of CAT by 33% when the reaction was augmented with 10mM phosphate. However, it is unclear why the additional phosphate increased the CAT yield. Jewett et al. believe it either enhanced oxidative phosphorylation activity or inhibited phosphatase reactions. The number, size, protein loading and lifetime of these vesicles remains an open area of study. Thus, we expect CFPS will have suboptimal oxidative phosphorylation capacity and remains an important area to optimize for improved CFPS performance.

2.4 Optimal Metabolic Flux Distribution

Amino acid supplementation altered the optimal metabolic flux distribution predicted for CAT production (Fig. 4). To investigate the influence of amino acid supplementation, we compared the simulated metabolic flux distributions for CAT production with and without external amino acids. In the presence of amino acid supplementation, and *de novo* amino acid synthesis, there was an incomplete TCA cycle, where a combination of glucose and amino acids powered protein expression (Fig. 4A). Glucose was consumed to produce acetyl-coenzyme A, and associated by-products, while glutamate was converted to alpha-ketoglutarate which traveled to oxaloacetic acid and pyruvate for additional amino acid biosynthesis. On the other hand, in the presence of amino acid supplementation, but without *de novo* amino acid biosynthesis, there was no TCA cycle flux. In this case, ATP was produced by a combination of substrate level and oxidative phosphorylation, where ubiquinone was regenerated via *nuo* activity, without relying on succinate dehydrogenase in the TCA cycle (Fig. 4B). These first two cases where amino acids were available had similar performance, and their respective metabolic flux distributions had a 99% correlation for all proteins. In the absence of amino acid supplementation (where all amino acids were synthesized *de novo* from glucose), the energy efficiency and carbon yield decreased; in this case the TCA cycle was largely complete and there was diversion of metabolic flux into the Entner-Doudoroff pathway to produce NADPH (Fig. 4C). However, these simulations represent the theoretical optimum under different conditions. To more accurately describe system performance, we constrained the feasible solution space with experimental measurements and estimated the optimal CAT flux distribution.

The experimentally constrained optimal flux distribution had a 52% similarity with the theoretically optimal flux distribution (Fig. 6). Metabolic fluxes were constrained by experimental measurements of glucose, amino and organic acid consumption and production rates for the first hour of the reaction (supporting information). The low similarity suggested several differences between the solutions which could be exploited to

improve CFPS performance. The largest discrepancy was in oxidative phosphorylation reactions, where the experimental system relied heavily on *cyd* rather than *cyo* which was less efficient for energy generation. In addition, the *pnt1* reaction, which interconverts NADPH to NADH, was active in the experimental system and not in the optimal systems; this suggests CFPS may be limited by NADH. The next largest discrepancy was in folate, purine and pyrimidine metabolism which were inactive in the optimum systems followed by amino acid biosynthesis. The experimentally constrained system had a high flux for alanine and glutamine biosynthesis which accumulated in the media, whereas in the optimum cases there was no accumulation of amino acids. The central carbon organic acids showed good agreement with the data with a coefficient of determination of $R^2=0.92$ (Fig. 6B). Only certain amino acid synthesis reactions were blocked, since during the growth of *E. coli* not all amino acids were supplied (see Materials and Methods). During the cell-free reaction all amino acids were supplied, however glucose still traveled through all the major pathways, and the same metabolic precursors were still utilized for amino acid biosynthesis. In this case, it is unclear which substrate (glucose or amino acids) is used to power CFPS and may in fact be a combination of both. The optimum solutions only produced the required amount of amino acids necessary; however, in examining the measurements there was an accumulation of alanine and glutamine which may explain some of the differences in the correlations of the flux distributions. Accumulation of pyruvate, lactate, acetate, and other organic acids can be seen (Fig. 6B) and may contribute to the inefficiency of carbon utilization.

2.4.1 Potential Alternative Metabolic Optima

Optimal flux distributions predicted using constraint based approaches may not always be unique. Alternative optimal solutions have the same objective value, e.g., productivity, but different metabolic flux distributions. Several techniques, e.g., flux variability analysis (FVA) (31, 32) or mixed-integer approaches (33) can estimate alternative optima. In this

study, we used flux variability analysis to estimate potential alternative optimal solutions for CAT production constrained by experimental measurements (Fig. 7). FVA identified pathways required for CAT production; for example, deletion of the glycolysis/gluconeoogenesis or oxidative phosphorylation pathways resulted in no CAT production. Likewise, there were pathway knockouts that had no effect on productivity or the metabolic flux distribution, such as removal of isoleucine, leucine, histidine and valine biosynthesis. Globally, the constraint based simulation reached the same optimal CAT productivity for 40% of the pairwise knockouts, but had different flux distributions compared with the absence of knockouts. For example, one of the features of the predicted optimal metabolic flux distribution was a high flux through the Entner-Doudoroff (ED) pathway. Removal of the ED pathway had no effect on the CAT productivity compared to the absence of knockouts (Fig. 7A). Pairwise knockouts of the ED pathway and other subgroups (i.e. pentose phosphate pathway, cofactors, folate metabolism, etc.) also resulted in the same optimal CAT productivity. However, there was a difference in the flux distribution with these knockouts (Fig. 7B); thus, alternative optimal metabolic flux distributions exist for CAT production, despite experimental constraints. In addition, knockouts of amino acid biosynthesis reactions had no effect on the productivity with the exception of alanine, aspartate, asparagine, glutamate and glutamine biosynthesis reactions, since amino acids were available in the media. Ultimately, to determine the metabolic flux distribution occurring in CFPS, we need to add additional constraints to the flux estimation calculation. For example, thermodynamic feasibility constraints may result in a better depiction of the flux distribution (11, 12), and ^{13}C labeling in CFPS could provide significant insight. However, while ^{13}C labeling techniques are well established for *in vivo* processes (34), application of these techniques to CFPS remains an active area of research.

2.5 Summary and conclusions

In this study, we developed a sequence specific constraint based modeling approach to predict the performance of cell-free protein synthesis reactions for a range of proteins. We showed first principle predictions for protein production of deGFP and CAT which were in agreement with experimental measurements, under two different promoters and two different cell-free extract systems. We are currently working on expanding our library of promoters that can provide good estimates of performance for different proteins. Different promoter will help design *de novo* circuits for optimal functionality and performance. This modeling approach suggested correlations for productivity, energy efficiency and carbon yield as a function of the size of the protein. Maltose binding protein showed good agreement with these performance metrics with the established model correlations. Furthermore, global sensitivity analysis identified oxygen uptake as being instrumental for maintaining a high energy efficiency and carbon yield. The translation rate was identified as the rate limiting step for productivity. The model also suggested that cell-free systems can simultaneously operate aerobically and anaerobically, which can lead to inefficient production and should be addressed to optimize energy efficiency and carbon yield. In addition, our modeling approach could be expanded with a more detailed description of gene expression that has been utilized in a *E. coli* genome scale model (16). We would also like to expand our model to include post translation modifications that proteins would require for proper folding and functionality. In conclusion, sequence specific constraint based modeling offers a novel means to *a priori* estimate the performance of cell-free synthetic circuits.

Materials and Methods

Glucose/NMP cell-free protein synthesis.

The glucose/NMP cell-free protein synthesis reaction was performed using the S30 extract in 1.5-mL Eppendorf tubes (working volume of 15 μ L) and incubated in a humidified incubator. The S30 extract was prepared from *E. coli* strain KC6 (A19 Δ tonA Δ tnaA Δ speA Δ endA Δ sdaA Δ sdaB Δ gshA met+). This K12-derivative has several gene deletions to stabilize amino acid concentrations during the cell-free reaction. The KC6 strain was grown to approximately 3.0 OD₅₉₅ in a 10-L fermenter (B. Braun, Allentown PA) on defined media with glucose as the carbon source and with the addition of 13 amino acids (alanine, arginine, cysteine, serine, aspartate, glutamate, and glutamine were excluded) (35). Crude S30 extract was prepared as described previously (36). Plasmid pK7CAT was used as the DNA template for chloramphenicol acetyl transferase (CAT) expression by placing the *cat* gene between the T7 promoter and the T7 terminator (37). The plasmid was isolated and purified using a Plasmid Maxi Kit (Qiagen, Valencia CA). Cell-free CAT synthesis was performed at 37 °C.

The protein synthesis reaction was conducted using the PANOxSP protocol with slight modifications from that described previously (38). Unless otherwise noted, all reagents were purchased from Sigma (St. Louis, MO). The initial mixture included 1.2 mM ATP; 0.85 mM each of GTP, UTP, and CTP; 30 mM phosphoenolpyruvate (Roche, Indianapolis IN); 130 mM potassium glutamate; 10 mM ammonium glutamate; 16 mM magnesium glutamate; 50 mM HEPES-KOH buffer (pH 7.5); 1.5 mM spermidine; 1.0 mM putrescine; 34 μ g/mL folinic acid; 170.6 μ g/mL *E. coli* tRNA mixture (Roche, Indianapolis IN); 13.3 μ g/mL pK7CAT plasmid; 100 μ g/mL T7 RNA polymerase; 20 unlabeled amino acids at 2-3 mM each; 5 μ M l-[U-¹⁴C]-leucine (Amersham Pharmacia, Uppsala Sweden); 0.33 mM nicotinamide adenine dinucleotide (NAD); 0.26 mM coenzyme A (CoA); 2.7 mM sodium oxalate; and 0.24 volumes of *E. coli* S30 extract. This reaction was modified for the energy

source used such that glucose reactions have 30-40 mM glucose in place of PEP. Sodium oxalate was not added since it has a detrimental effect on protein synthesis and ATP concentrations when using glucose or other early glycolytic intermediate energy sources (39). The HEPES buffer (pKa \sim 7.5) was replaced with Bis-Tris (pKa \sim 6.5). In addition, the magnesium glutamate concentration was reduced to 8 mM for the glucose reaction since a lower magnesium optimum was found when using a nonphosphorylated energy source (38). Finally, 10 mM phosphate was added in the form of potassium phosphate dibasic adjusted to pH 7.2 with acetic acid.

Protein product and metabolite measurements.

Cell-free reaction samples were quenched at specific timepoints with equal volumes of ice-cold 150 mM sulfuric acid to precipitate proteins. Protein synthesis of CAT was determined from the total amount of ^{14}C -leucine-labeled product by trichloroacetic acid precipitation followed by scintillation counting as described previously (27). Samples were centrifuged for 10 min at 12,000g and 4°C. The supernatant was collected for high performance liquid chromatography (HPLC) analysis. HPLC analysis (Agilent 1100 HPLC, Palo Alto CA) was used to separate nucleotides and organic acids, including glucose. Compounds were identified and quantified by comparison to known standards for retention time and UV absorbance (260 nm for nucleotides and 210 nm for organic acids) as described previously (27). The standard compounds quantified with a refractive index detector included inorganic phosphate, glucose, and acetate. Pyruvate, malate, succinate, and lactate were quantified with the UV detector. The stability of the amino acids in the cell extract was determined using a Dionex Amino Acid Analysis (AAA) HPLC System (Sunnyvale, CA) that separates amino acids by gradient anion exchange (AminoPac PA10 column). Compounds were identified with pulsed amperometric electrochemical detection and by comparison to known standards.

Formulation and solution of the model equations.

The sequence-specific flux balance analysis problem was formulated as a linear program:

$$\begin{aligned} & \max_w \left(w_X = \boldsymbol{\theta}^T \mathbf{w} \right) \\ & \text{Subject to : } \mathbf{S}\mathbf{w} = \mathbf{0} \\ & \mathcal{L}_i \leq w_i \leq \mathcal{U}_i \quad i = 1, 2, \dots, \mathcal{R} \end{aligned} \tag{1}$$

where \mathbf{S} denotes the stoichiometric matrix, \mathbf{w} denotes the unknown flux vector, $\boldsymbol{\theta}$ denotes the objective cost vector and \mathcal{L}_i and \mathcal{U}_i denote the lower and upper bounds on flux w_i , respectively. The transcription (T) and translation (X) stoichiometry was modeled based upon the template reactions of Allen and Palsson (22) (Table 1). The objective of the sequence specific flux balance calculation was to maximize the rate of protein translation, w_X . The total glucose uptake rate was bounded by [0,40 mM/h] according to experimental data, while the amino acid uptake rates were bounded by [0,30 mM/h], but did not reach the maximum flux. Gene and protein sequences were taken from literature and are available in the Supporting Information. The sequence specific flux balance linear program was solved using the GNU Linear Programming Kit (GLPK) v4.55 (40). For all cases, amino acid degradation reactions were blocked as these enzymes were knocked out during the cell-free extract preparation (27, 28). In the second case, all amino acid synthesis reactions were set to 0 mM/hr since *E. coli* was grown in the presence of amino acids, thus these enzymes would not be present in the cell-free extract media. In the third case, amino acid uptake reactions were set to 0 mM/hr. In the experimental constrained case, *E. coli* was grown in the presence of 13 amino acids (alanine, arginine, cysteine, serine, aspartate, glutamate, and glutamine were excluded) (35), thus the synthesis reactions responsible for those 13 amino acid were set to 0 mM/hr.

The bounds on the transcription rate ($\mathcal{L}_T = w_T = \mathcal{U}_T$) were modeled as:

$$w_T = V_T^{max} \left(\frac{G_P}{K_T + G_P} \right) \quad (2)$$

where G_P denotes the gene concentration of the protein of interest, and K_T denotes a transcription saturation coefficient. The maximum transcription rate V_T^{max} was formulated as:

$$V_T^{max} \equiv \left[R_T \left(\frac{\dot{v}_T}{l_G} \right) u(\kappa) \right] \quad (3)$$

The term R_T denotes the RNA polymerase concentration (nM), \dot{v}_T denotes the RNA polymerase elongation rate (nt/h), l_G denotes the gene length in nucleotides (nt). The term $u(\kappa)$ (dimensionless, $0 \leq u(\kappa) \leq 1$) is an effective model of promoter activity, where κ denotes promoter specific parameters. The general form for the promoter models was taken from Moon *et al.* (25). In this study, we considered two promoters: T7 and P70a. The promoter function for the T7 promoter, u_{T7} , was given by:

$$u_{T7} = \frac{K_{T7}}{1 + K_{T7}} \quad (4)$$

where K_{T7} denotes a T7 RNA polymerase binding constant. The P70a promoter function u_{P70a} (which was used for all other proteins) was formulated as:

$$u_{P70a} = \frac{K_1 + K_2 f_{\sigma_{70}}}{1 + K_1 + K_2 f_{\sigma_{70}}} \quad (5)$$

where K_1 denotes the weight of RNA polymerase binding alone, K_2 denotes the weight of RNAP- σ_{70} bound to the promoter, and $f_{\sigma_{70}}$ denotes the fraction of the σ_{70} transcription factor bound to RNAP, modeled as a Hill function:

$$f_{\sigma_{70}} = \frac{\sigma_{70}^n}{K_D^n + \sigma_{70}^n} \quad (6)$$

where σ_{70} denotes the sigma-factor 70 concentration, K_D denotes the dissociation constant, and n denotes a cooperativity coefficient. The values for all promoter parameters are given in Table 2.

The translation rate (w_X) was bounded by:

$$0 \leq w_X \leq V_X^{max} \left(\frac{mRNA^*}{K_X + mRNA^*} \right) \quad (7)$$

where $mRNA^*$ denotes the steady state mRNA abundance and K_X denotes a translation saturation constant. The maximum translation rate V_X^{max} was formulated as:

$$V_X^{max} \equiv \left[K_P R_X \left(\frac{\dot{v}_X}{l_P} \right) \right] \quad (8)$$

The term K_P denotes the polysome amplification constant, \dot{v}_X denotes the ribosome elongation rate (amino acids per hour), l_P denotes the number of amino acids in the protein of interest. The steady-state mRNA abundance $mRNA^*$ was estimated as:

$$mRNA^* \simeq \frac{w_T}{\lambda} \quad (9)$$

where λ denotes the rate constant controlling the mRNA degradation rate (hr^{-1}). All translation parameters are given in Table 2.

Calculation of energy efficiency.

Energy efficiency (\mathcal{E}) was calculated as the ratio of protein production to glucose consumption, written in terms of equivalent ATP molecules:

$$\mathcal{E} \equiv \frac{w_X (2 \cdot \text{ATP}_X + \text{GTP}_X) + w_T (2 \times (\text{ATP}_T + \text{CTP}_T + \text{GTP}_T + \text{UTP}_T))}{q_{GLC} \cdot \text{ATP}_{GLC}} \quad (10)$$

where ATP_T , CTP_T , GTP_T , UTP_T denote the stoichiometric coefficients of each energy species for the transcription of the protein of interest, ATP_X , GTP_X denote the stoichiometric coefficients of ATP and GTP for the translation of the protein of interest, $q_{GLC} = w_{GLC}$ denotes the glucose uptake rate, and ATP_{GLC} denotes the equivalent ATP number produced per glucose. The energy species stoichiometric coefficients are available in the Supporting Information.

Calculation of the carbon yield.

The carbon yield (Y_C^{POI}) was calculated as the ratio of carbon produced as the protein of interest divided by the carbon consumed as reactants (glucose and amino acids):

$$Y_C^{POI} \equiv \frac{q_{POI} \cdot C_{POI}}{\sum_{i=1}^{\mathcal{R}} q_{m_i} \cdot C_{m_i}} \quad (11)$$

where q_{POI} denotes the flux of the protein of interest produced, C_{POI} denotes carbon number of the protein of interest, \mathcal{R} denotes the number of reactants, q_{m_i} denotes the uptake flux of the i^{th} reactant, and C_{m_i} denotes the carbon number of the i^{th} reactant.

Quantification of uncertainty.

Experimental factors taken from literature, for example macromolecular concentrations or elongation rates, have uncertainty associated with their values. To quantify the influence of this uncertainty on model performance, we randomly sampled the expected physiological ranges for these parameters as determined from literature. An ensemble of $N = 100$ flux distributions was calculated for the three different cases we considered: control (with amino acid synthesis and uptake), amino acid uptake without synthesis, and amino acid synthesis without uptake. The flux ensemble was calculated by randomly sampling the maximum glucose consumption rate within a range of 0 to 30 mM/h, (determined from

experimental data) and randomly sampling RNA polymerase levels, ribosome levels, and elongation rates in a physiological range determined from literature. RNA polymerase levels were sampled between 60 and 80 nM, ribosome levels between 12 and 18 μ M, the RNA polymerase elongation rate between 20 and 30 nt/sec, and the ribosome elongation rate between 1.5 and 3 aa/s (28, 29).

Global sensitivity analysis.

We conducted a global sensitivity analysis using the variance-based method of Sobol to estimate which parameters controlled the performance of the cell-free protein synthesis reaction (41). We computed the total sensitivity index of each parameter relative to three performance objectives: productivity of the protein of interest, energy efficiency and carbon yield. We established the sampling bounds for each parameter from literature. We used the sampling method of Saltelli *et al.* (42) to compute a family of $N(2d + 2)$ parameter sets which obeyed our parameter ranges, where N was a parameter proportional to the desired number of model evaluations and d was the number of parameters in the model. In our case, $N = 1000$ and $d = 7$, so the total sensitivity indices were computed from 16,000 model evaluations. The variance-based sensitivity analysis was conducted using the SALib module encoded in the Python programming language (43).

Potential alternative optimal metabolic flux solutions.

We identified potential alternative optimal metabolic flux distributions by performing single and pairwise reaction group knockout simulations [TODO:REF]. Reaction group knockouts were simulated by setting the flux bounds for all the reactions involved in a group to zero. We grouped reactions in the cell-free network into 19 subgroups (available in Supporting Information). We computed the difference (l^2 -norm) for CAT productivity in the presence and absence of pairwise reaction knockouts. Simultaneously, we computed

the difference in the flux distribution (l^2 -norm) for each pairwise reaction knockout compared to the flux distribution with no knockouts. Those solutions with the same or similar productivity but large changes in the metabolic flux distribution represent alternative optimal solutions.

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Supporting Information Available

The following files are available free of charge.

- Protein Sequences: DNA and protein sequences of each protein of interest.
- Supporting Information: Performance trendlines as a function of carbon number, transcription/translation stoichiometric coefficients of energy species, and experimental measurements of CAT production.
- Carbon Yield Sensitivity Analysis: Global sensitivity analysis on deGFP carbon yield.
- Metabolites and reactions of the cell-free stoichiometric network.

This material is available free of charge via the Internet at <http://pubs.acs.org/>.

Table 1: Transcription and translation template reactions for protein production. The symbol $G_{\mathcal{P}}$ denotes the gene encoding protein product \mathcal{P} , R_T denotes the concentration of RNA polymerase, $G_{\mathcal{P}}^*$ denotes the gene bounded by the RNA polymerase (open complex), η_i and α_j denote the stoichiometric coefficients for nucleotide and amino acid, respectively, Pi denotes inorganic phosphate, R_X denotes the ribosome concentration, R_X^* denotes bound ribosome, and AA_j denotes j^{th} amino acid.

Description	Template reaction
Transcription initiation	$G_{\mathcal{P}} + R_T \longrightarrow G_{\mathcal{P}}^*$
Transcription (w_T)	$G_{\mathcal{P}}^* + \sum_{k \in \{A,C,G,U\}} \eta_k \cdot (\{k\} TP + H_2O) \longrightarrow mRNA + G_{\mathcal{P}} + R_T + \sum_{k \in \{A,C,G,U\}} \eta_k \cdot PPi$
mRNA degradation	$mRNA \longrightarrow \sum_{k \in \{A,C,G,U\}} \eta_k \cdot \{k\} MP$
Translation initiation	$mRNA + R_X \longrightarrow R_X^*$
tRNA charging	$\alpha_j \cdot (AA_j + tRNA + ATP + H_2O) \longrightarrow \alpha_j \cdot (AA_j-tRNA_j + AMP + PPi)$ $j = 1, 2, \dots, 20$
Translation (w_X)	$R_X^* + \sum_{j \in \{AA\}} \alpha_j \cdot (AA_j-tRNA_j + 2GTP + 2H_2O) \longrightarrow \mathcal{P} + R_X + mRNA$ $+ \sum_{j \in \{AA\}} \alpha_j \cdot (tRNA + 2GDP + 2Pi)$

Table 2: Parameters for sequence specific flux balance analysis

Description	Parameter	Value	Units	Reference
RNA polymerase concentration	R_T	75	nM	(28)
Ribosome concentration	R_X	1.6	μ M	(28, 29)
Transcription elongation rate	\dot{v}_T	25	nt/sec	(28)
Translation elongation rate	\dot{v}_X	2	aa/sec	(28, 29)
Transcription saturation coefficient	K_T	3.5	nM	estimated
Translation saturation coefficient	K_X	45.0	μ M	estimated
Polysome amplification constant	K_P	10	constant	estimated
mRNA degradation rate	λ	5.2	hr ⁻¹	(28)
T7 promoter	K_{T7}	10	constant	estimated
Weight RNA polymerase binding alone P70a	K_1	0.014	constant	estimated
Weight bound RNAP- σ_{70} P70a	K_2	10	constant	estimated
σ_{70} concentration	σ_{70}	35	nM	(28)
σ_{70} dissociation constant	K_D	130	nM	(44)
σ_{70} hill coefficient	n	1	constant	(44)
Gene concentration	G_P	5	nM	(28)

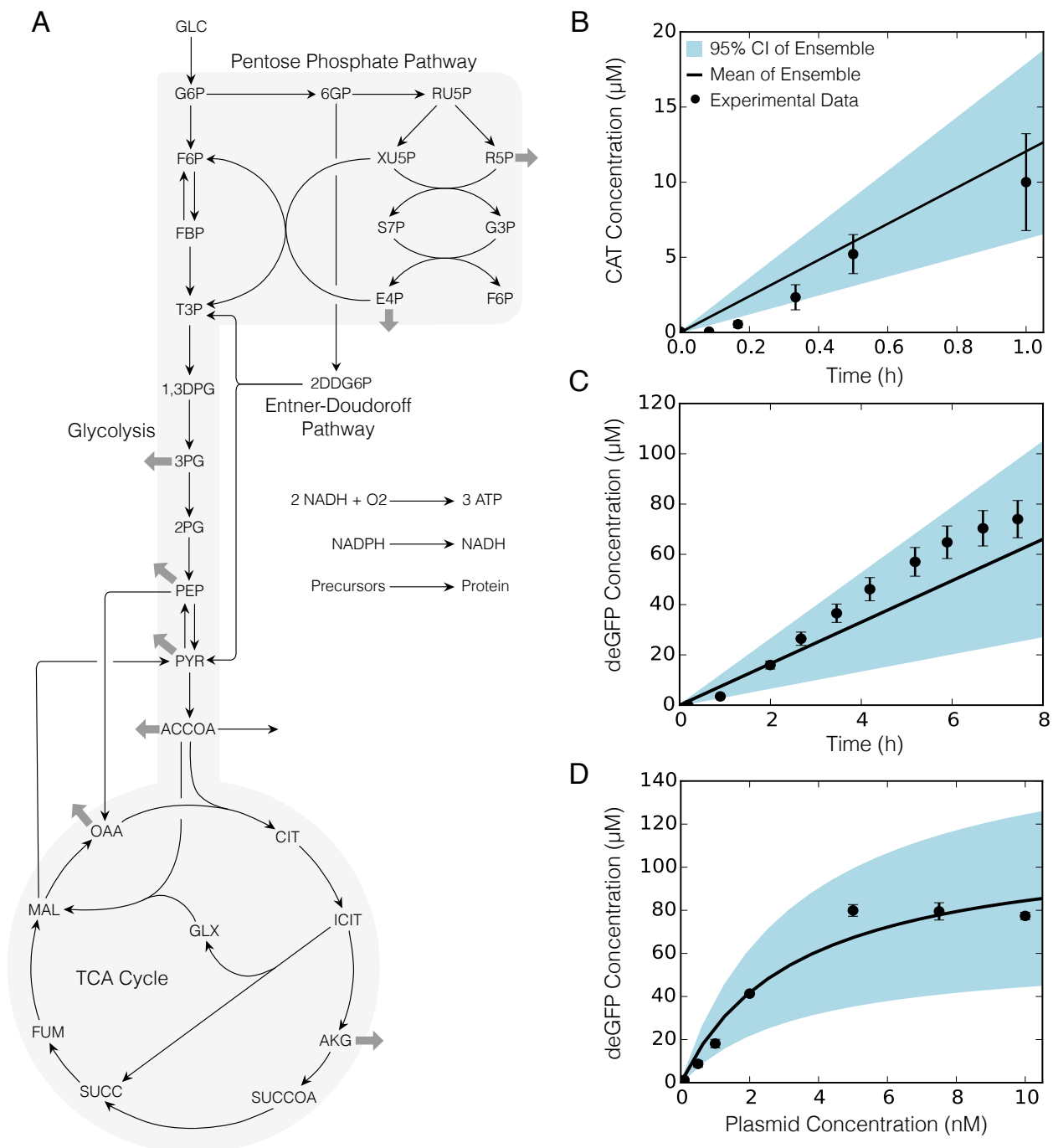


Figure 1: Sequence specific flux balance analysis. **A.** Core metabolic network with glycolysis, pentose phosphate pathway, TCA cycle, Entner-Doudoroff pathway. Thick gray arrows indicate withdrawal of precursors for amino acid synthesis. **B.** CAT production under a T7 promoter in CFPS *E. coli* extract for 1 h under glucose consumption. Error bars denote the standard deviation of experimental measurements. **C.** deGFP production under a P70 promoter in TXTL 2.0 *E. coli* extract for 8 h under maltose consumption. Error bars denote a 10% coefficient of variation. **D.** Predicted deGFP concentration at different plasmid concentrations versus measurements of deGFP synthesized in TXTL 2.0. 95% CI (blue region) over the ensemble of 100 sets, mean of the ensemble (black line), and experimental measurements (dots).

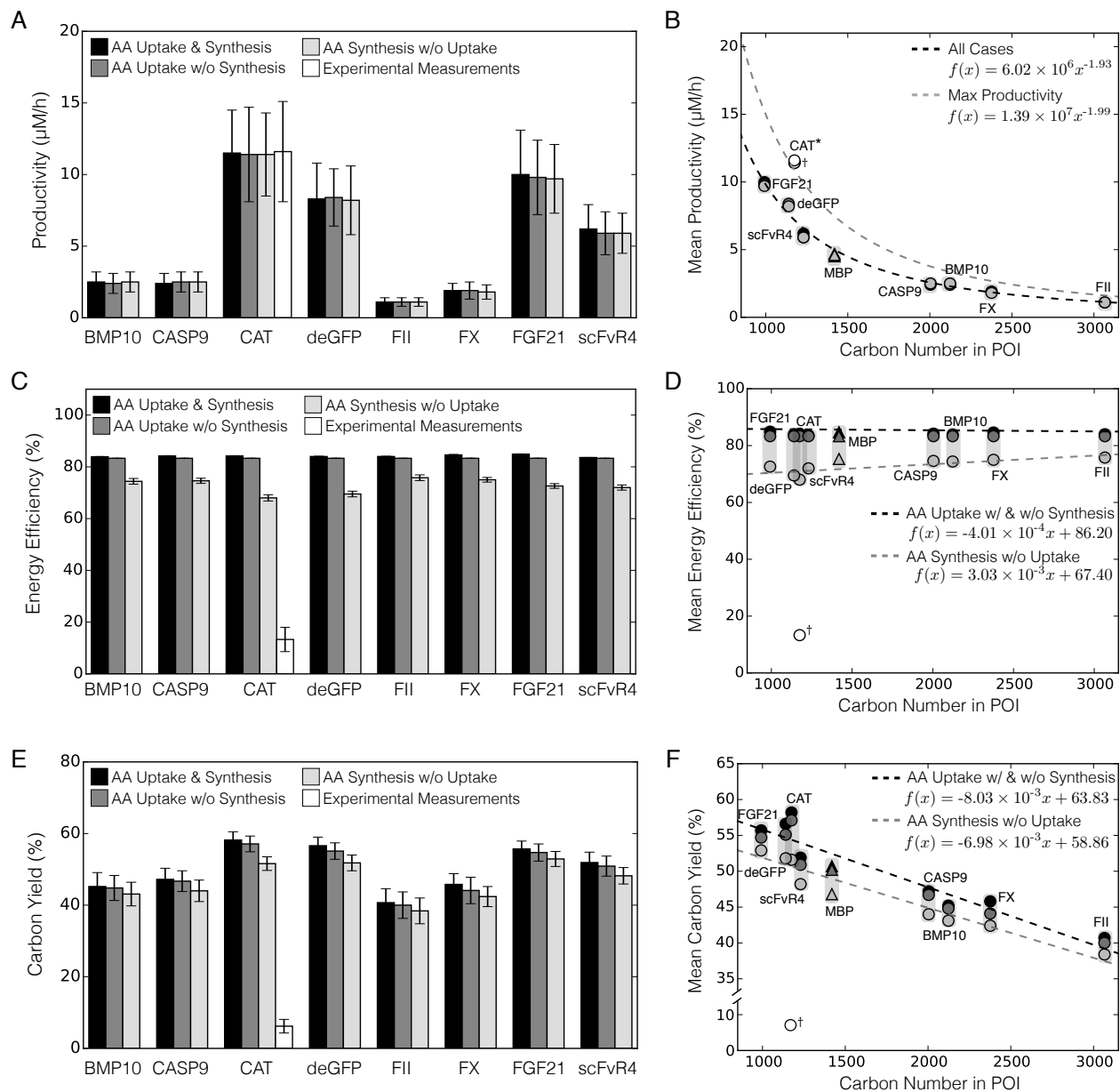


Figure 2: The CFPS performance for eight model proteins with and without amino acid supplementation. A. Mean CFPS productivity for a panel of model proteins with and without amino acid supplementation. B. Mean CFPS productivity versus carbon number for a panel of model proteins with and without amino acid supplementation. Trendline (black dotted line) was calculated across all cases for a P70a promoter ($R^2 = 0.99$) and maximum productivity trendline assumed $u(\kappa) = 1$ (grey dotted line; $R^2 = 0.99$). C. Mean CFPS energy efficiency for a panel of model proteins with and without amino acid supplementation. D. Mean CFPS energy efficiency versus carbon number for a panel of model proteins with and without amino acid supplementation. Trendline for cases with amino acids (black dotted line) and trendline for without amino acids (grey dotted line; $R^2 = 0.65$). E. Mean CFPS carbon yield for a panel of model proteins with and without amino acid supplementation. F. Mean CFPS carbon yield versus carbon number. Trendline for cases with amino acids (black dotted line; $R^2 = 0.95$) and trendline for without amino acids (grey dotted line; $R^2 = 0.90$). Error bars: 95% CI calculated by sampling; asterisk: protein excluded from trendline; dagger: constrained by experimental measurements and excluded from trendline; triangles: first principle prediction and excluded from formulating trendline.

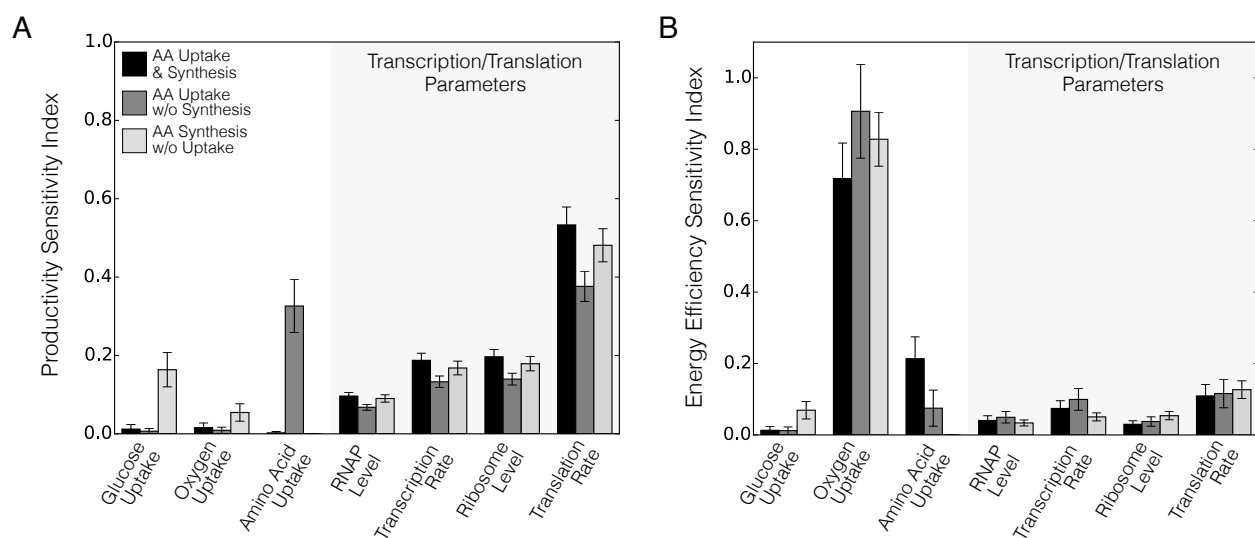


Figure 3: Total order sensitivity analysis of CFPS. A. Total order sensitivity of the optimal CAT productivity with respect to metabolic and transcription/translation parameters. B. Total order sensitivity of the optimal CAT energy efficiency. Metabolic and transcription/translation parameters were varied for amino acid supplementation and synthesis (black), amino acid supplementation without synthesis (dark grey) and amino acid synthesis without supplementation (light gray). Error bars represent a 95% CI on the total-order sensitivity index.

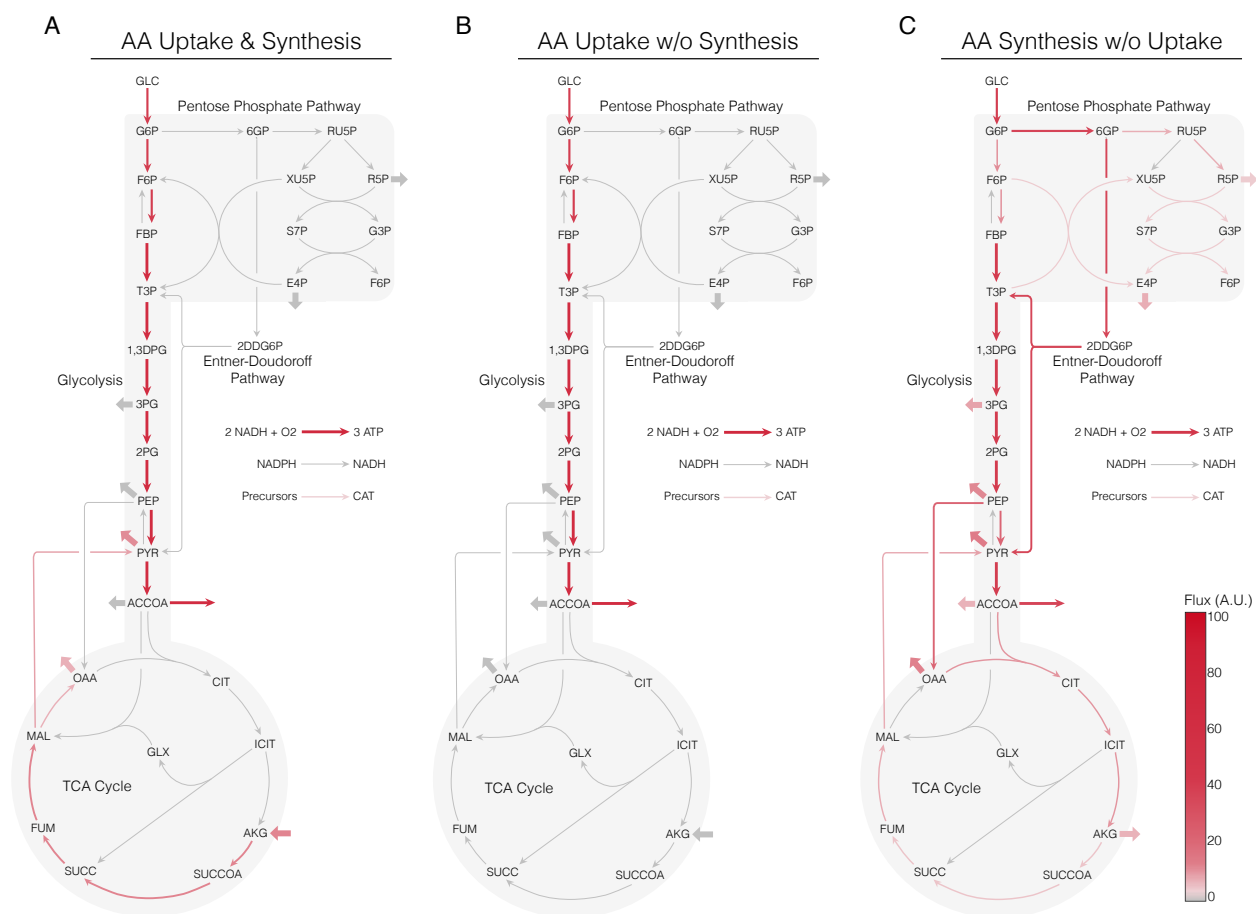


Figure 4: Flux profile for glycolysis, pentose phosphate pathway, Entner-Doudoroff pathway, TCA cycle, and oxidative phosphorylation, for three different cases: (A) amino acid uptake and synthesis, (B) amino acid uptake without synthesis, and (C) amino acid synthesis without uptake. Mean flux across the ensemble, normalized to glucose uptake flux. Thick arrows indicate flux to or from amino acids.

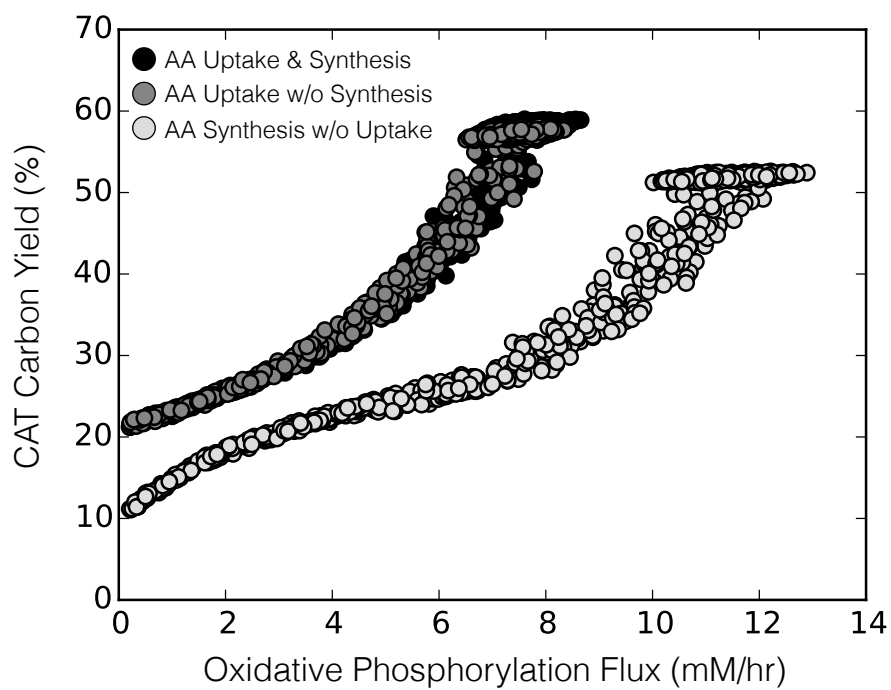


Figure 5: The deGFP carbon yield versus oxidative phosphorylation flux, across an ensemble of 1000 flux balance solutions, for amino acid uptake and synthesis (black), amino acid uptake without synthesis (dark grey), and amino acid synthesis without uptake (light gray).

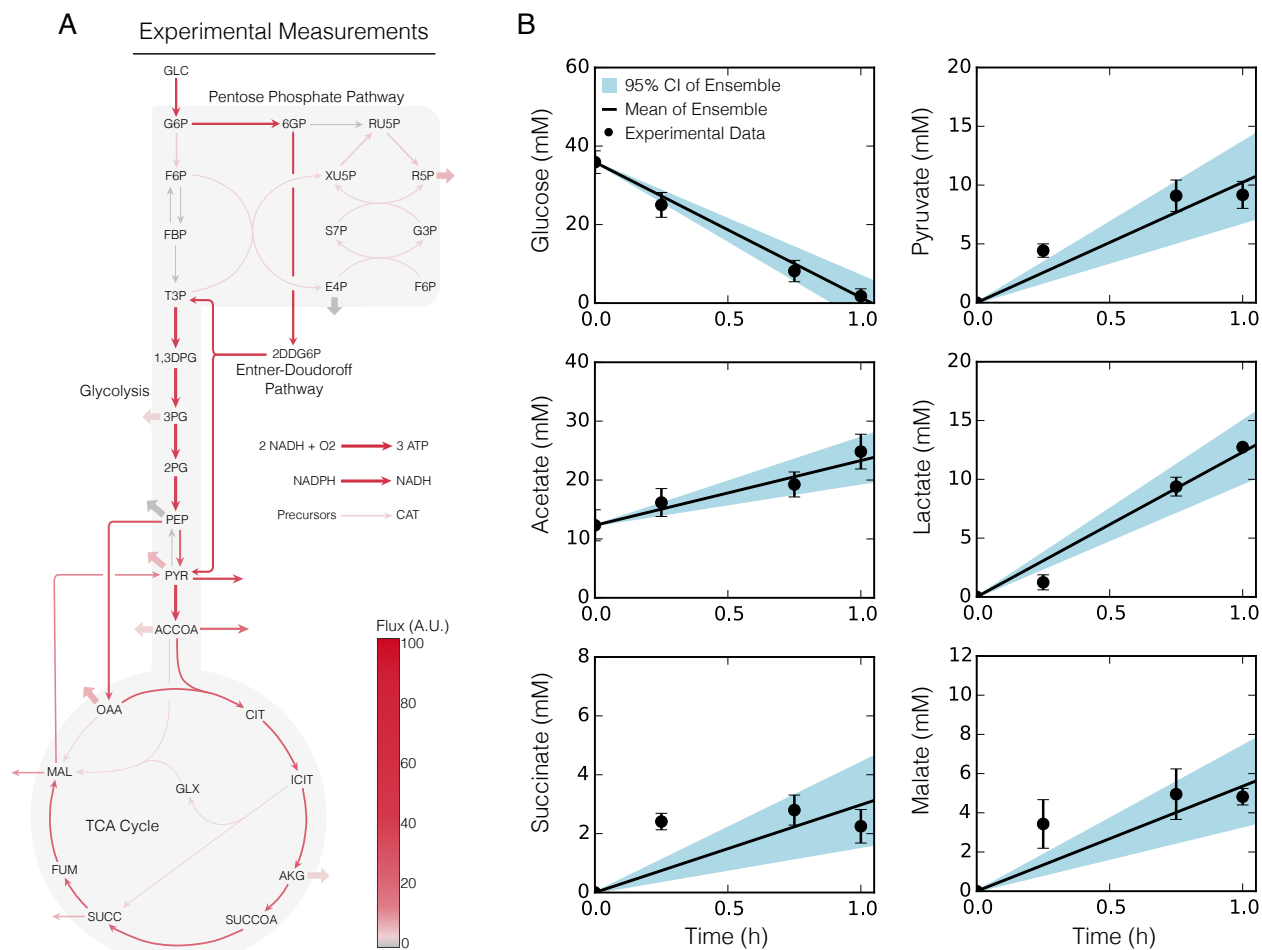


Figure 6: Constraint based simulation of CAT production for an experimentally constrained case. (A) Flux profile for glycolysis, pentose phosphate pathway, Entner-Doudoroff pathway, TCA cycle, and oxidative phosphorylation. Mean flux across the ensemble, normalized to glucose uptake flux. Thick arrows indicate flux to or from amino acids. (B) Central carbon metabolite measurements versus simulations over a one hour time course.

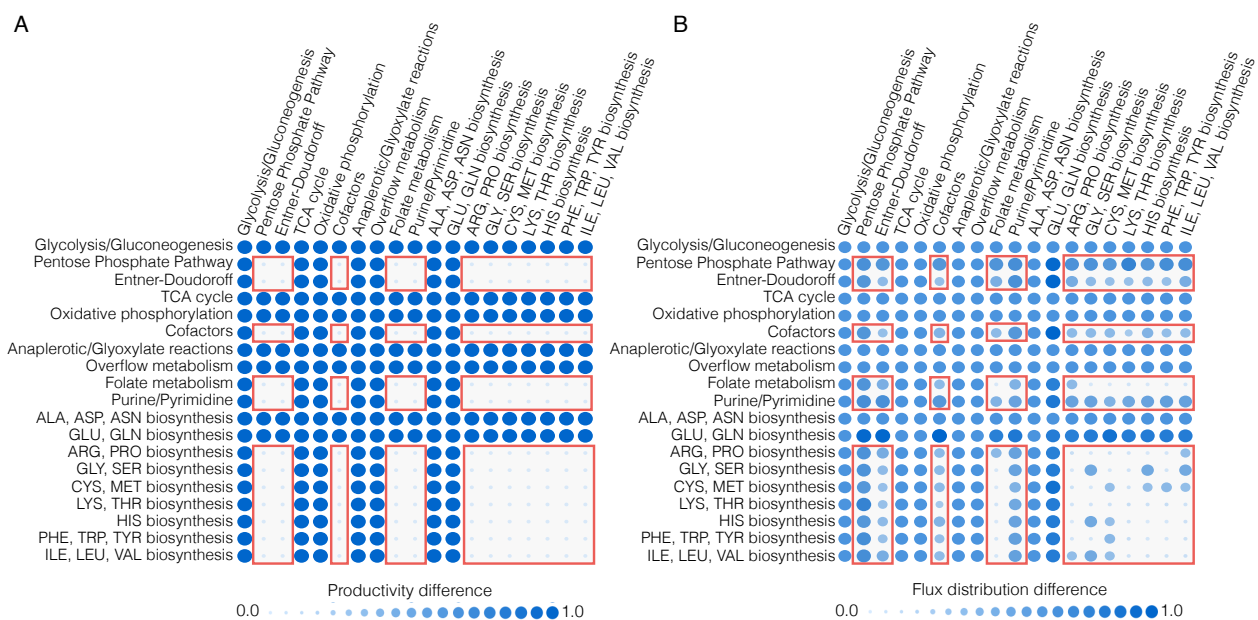


Figure 7: The norm effect of pairwise knockouts of subgroups in the cell-free network. (A) CAT productivity norm compared to no knockouts in the experimentally constrained case. (B) Flux distribution norm compared to no knockouts in the experimentally constrained case.

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