

System - Cumene

Critical Temperature - 631K

Critical Pressure - 32.09 bar

Acentric factor (ω) - 0.3274

Source - Perry's Chemical Engineers Handbook.

Equation of State - Peng Robinson

$$P = \frac{RT}{V_m - b} - \frac{a\alpha}{V_m^2 + 2bV_m - b^2}$$

$$a = \frac{0.45724R^2T_c^2}{P_c}$$

$$b = \frac{0.07780RT_c}{P_c}$$

$$\alpha = \left(1 + \left(0.37464 + 1.54226\omega - 0.26992\omega^2\right) \left(1 - T_r^{0.5}\right)\right)^2$$

$$T_r = \frac{T}{T_c}$$

Here, T_c is the critical temperature in Kelvin.

V_m is the molar volume.

T_r is the reduced temperature.

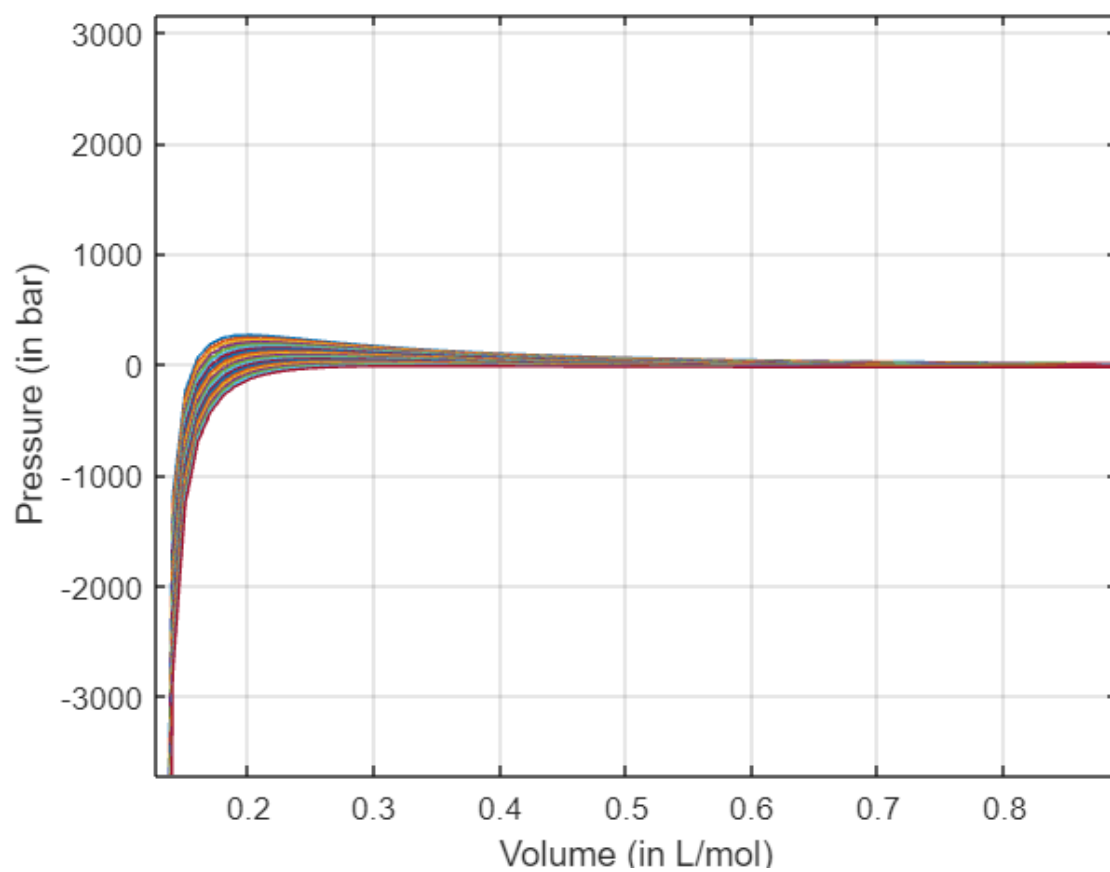
Antoine Coefficients

$\log(P) = A - B/(T+C)$ where P is in mmHg and T is in Celsius

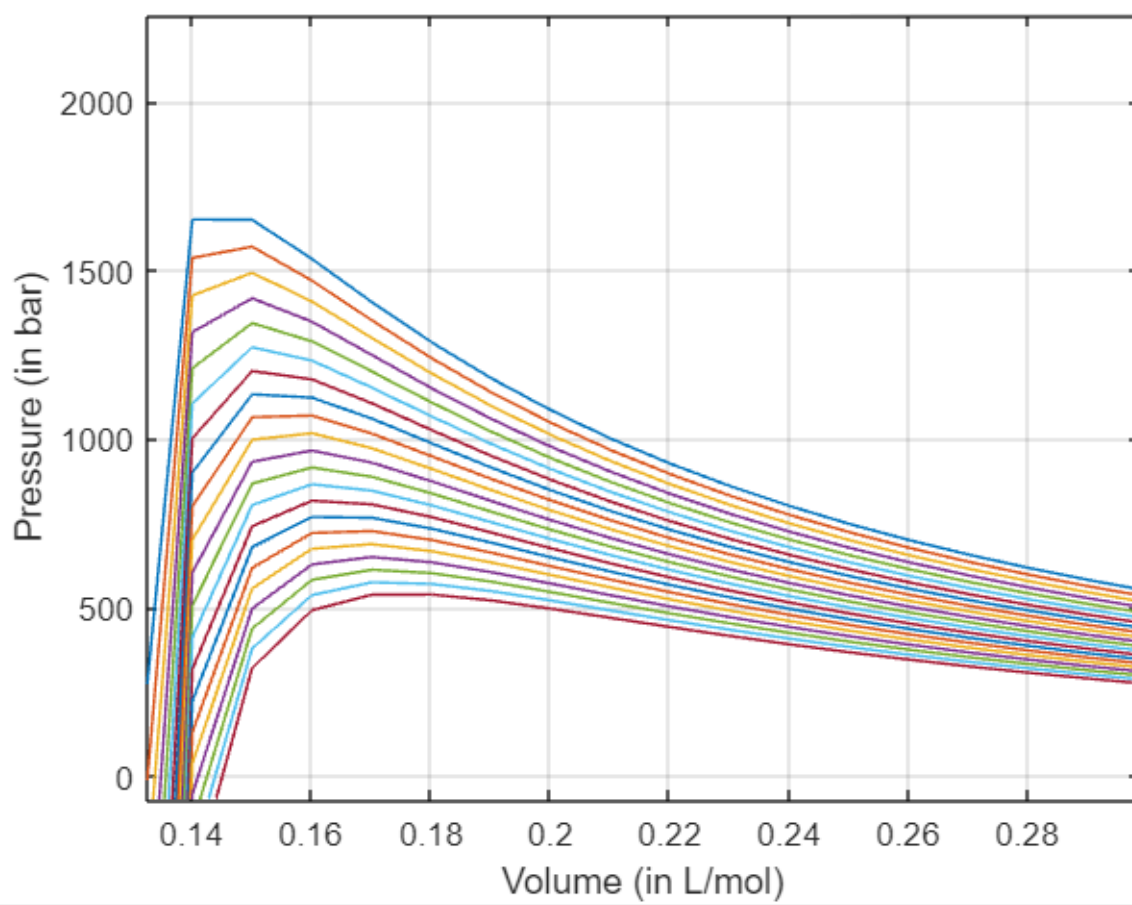
Source of data: Yaws and Yang (Yaws, C. L. and Yang, H. C.

compound name	A	B	C	Tmin	Tmax	??	?
cumene	6.93666	1460.793	207.777	38	181	Y3	0

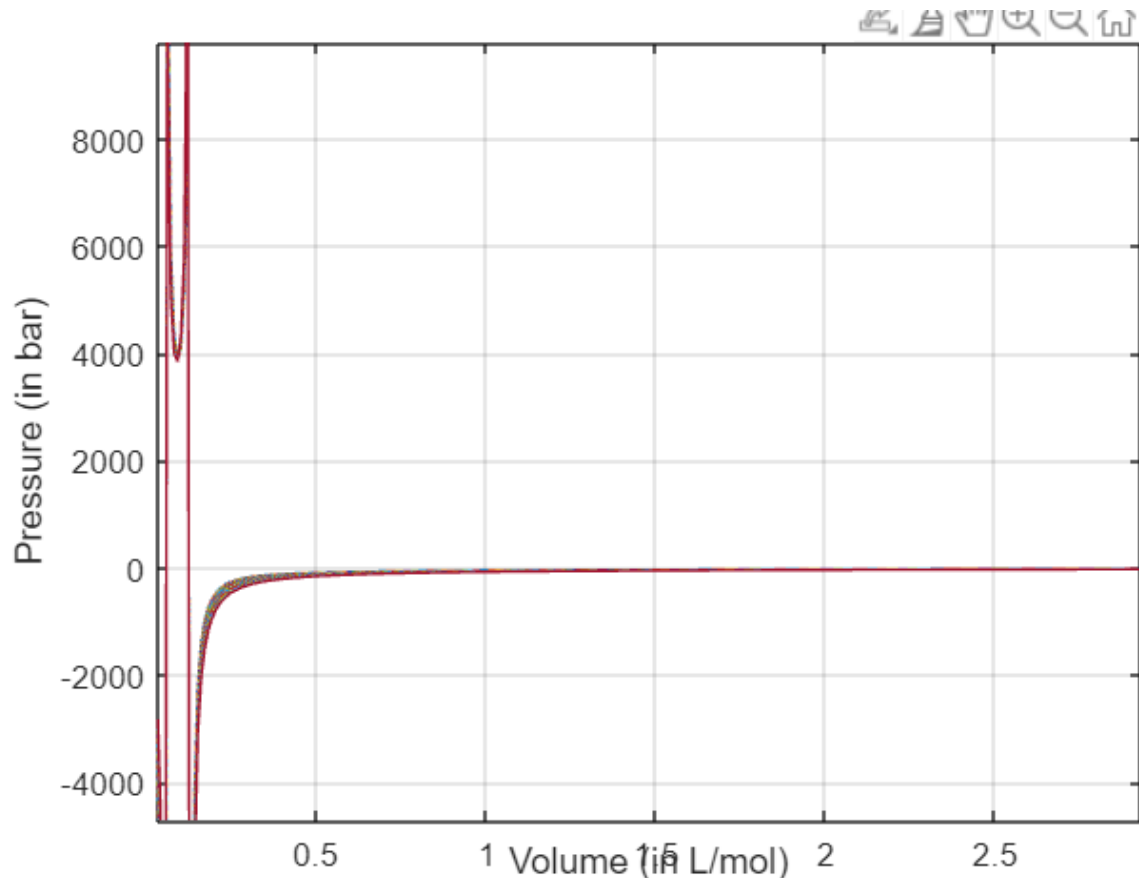
For $400 < T < 600$



For $100 < T < 300$



For $800 < T < 1000$



Algorithm:-

First estimate saturation pressure using antoine equation.

Then substitute values in Peng Robinson EOS to find minimum and maximum values. Store in an array.

Use eqn 1 to find the roots.

$$Pv^3 + (Pb - RT)v^2 + (-3Pb^2 - 2bRT + a\alpha)v + (Pb^3 - a\alpha b + RTb^2) = 0 \quad \text{--- Eqn 1}$$

Using $\mu_g - \mu_l = 0$, we get

$$\log(v_{min}/(v_{min} - b)) - a\alpha/(bRT * (\sigma - \epsilon)) \log((b\sigma + v_{min})/(b\epsilon + v_{min})) + \log(1/v_{min}) + Pv_{min}/RT - [\log(v_{max}/(v_{max} - b)) - a\alpha/(bRT * (\sigma - \epsilon)) \log((b\sigma + v_{max})/(b\epsilon + v_{max})) + \log(1/v_{max}) + Pv_{max}/RT] = 0$$

----- Eqn 2

Substituting v_{min}, v_{max} in Eqn 1 and solving simultaneously with eqn 2 using fsolve, gives 3 values corresponding to saturation pressure, maximum volume and minimum volume

Using spline to fit the curve.