

### UNIVERSITÀ POLITECNICA Delle Marche

Numerical Heat Transfer for Applications

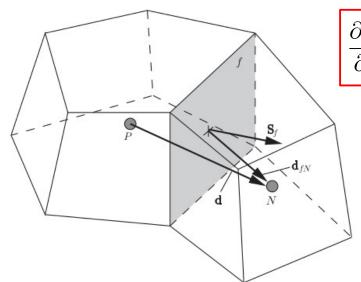
FVM for unsteady state heat conduction

Dr Valerio D'Alessandro

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### Finite volume discretization of Fourier equation

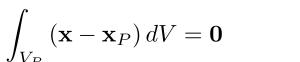
Fourier equation is discretized its integral form over each control volume:



$$\frac{\partial T}{\partial t} - \alpha \nabla^2 T = 0 \Longrightarrow \int_{V_P} \frac{\partial T}{\partial t} dV - \int_{V_P} \alpha \nabla^2 T dV = 0$$

$$\int_{V_P} \frac{\partial T}{\partial t} dV - \int_{V_P} \alpha \nabla \cdot (\nabla T) \, dV = 0$$

$$\int_{V_P} \frac{\partial T}{\partial t} dV - \int_{\partial V_P} \alpha \nabla T \cdot d\mathbf{S} = 0$$

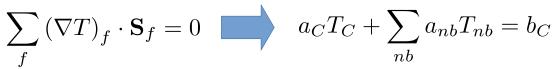


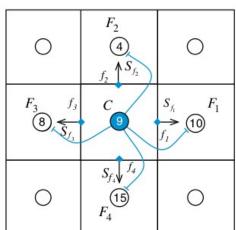


$$V_{P}\frac{dT_{P}}{dt} - \sum_{f} \alpha \left(\nabla T\right)_{f} \cdot \mathbf{S}_{f} = 0$$

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### Finite volume discretization of Fourier equation





$$a_9T_9 + a_{10}T_{10} + a_4T_4 + a_8T_8 + a_{15}T_{15} = 0$$

$$V_P \frac{dT_C}{dt} - \sum_f \alpha \left( \nabla T \right)_f \cdot \mathbf{S}_f = 0 \blacktriangleleft$$

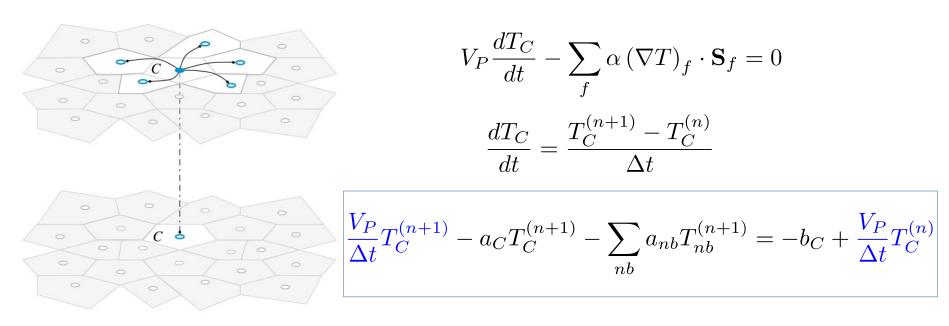
$$V_P \frac{T_C^{(n+1)} - T_C^{(n)}}{\Delta t} - \sum_{f} \alpha \left( \nabla T \right)_f \cdot \mathbf{S}_f = 0$$
Implicit or explicit?

$$\frac{V_P}{\Delta t} T_C^{(n+1)} - a_C T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = -b_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

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### Finite volume discretization of Fourier equation - implicit method



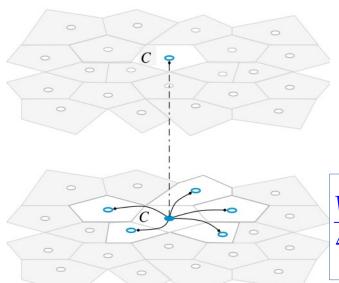
It is possible to use also different time integration schemes rather than backward Euler. A possible alternative is the following one:

$$\frac{dT_C}{dt} = \frac{3T_C^{(n+1)} - 4T_C^{(n)} + T_C^{(n-1)}}{2\Delta t} + O\left(\Delta t^2\right)$$

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### Finite volume discretization of Fourier equation - explicit method



$$V_P \frac{dT_C}{dt} - \sum_f \alpha (\nabla T)_f \cdot \mathbf{S}_f = 0$$
$$\frac{dT_C}{dt} = \frac{T_C^{(n+1)} - T_C^{(n)}}{\Delta t}$$

$$\frac{V_P}{\Delta t} T_C^{(n+1)} - a_C T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = -b_C + \frac{V_P}{\Delta t} T_C^{(n)}$$



$$T_C^{(n+1)} = T_C^{(n)} + \frac{\Delta t}{V_P} \left( a_C T_C^{(n)} + \sum_{nb} a_{nb} T_{nb}^{(n)} + b_C \right)$$

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### **Ex3\_FVM** - Unsteady state heat conduction

#### Matlab code

```
format long e
alpha= 1e-2;
    = 0.01;
Time = 50;
caseName='cube';
m=mesh data(caseName);
Nc=m.numberOfElements;
Ni=m.numberOfInteriorFaces:
Nb=m.numberOfBElements;
A=zeros(Nc,Nc);
b=zeros(Nc,1);
    = ones(Nc,1);
T0
    = zeros(Nc,1);
   = -alpha*A:
   = -alpha*b:
for i=1:Nc
       = m.elements(i).volC;
   A(i,i) = A(i,i) + Vc/dt;
end
```

$$\frac{V_P}{\Delta t} T_C^{(n+1)} - a_C T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = -b_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

A matrix implemention, as well as B.C. for laplacian term discretization, is extactly the same of the steady state case.

However, it is mandatory to switch **A** and **b** entries sign deriving from spatial terms discretization.

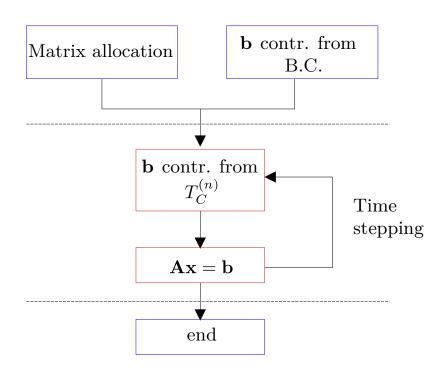
$$\frac{V_P}{\Delta t}$$

**A** matrix diagonal terms contributions deriving from unsteady term discretization.

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#### **Ex3\_FVM** - Unsteady state heat conduction

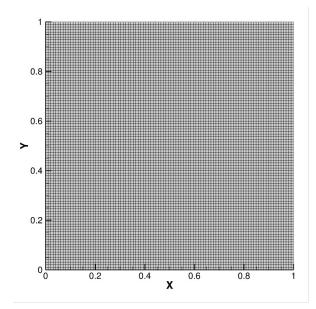
```
bn = zeros(Nc,1);
flow time = 0;
for i= 1: (Time/dt)
   for j=1:Nc
       Vc = m.elements(j).volC;
        bn(j) = b(j) + (Vc/dt)*T0(j);
    end
%
   Tc = bicq(A,b,1e-12,1000);
   Tc = pcg(A,b,1e-12,1000,L,U);
   T0 = Tc;
   bn = zeros(Nc,1);
   flow time = flow time + dt;
   if (mod(i,500) == 0)
          wrtfld(flow time, m , Tc, 'Tc', caseName)
    end
end
```



$$\frac{V_P}{\Delta t} T_C^{(n+1)} - a_C T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = -b_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

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### **Ex3\_FVM** - Unsteady state heat conduction in 1-D configuration



$$\frac{\partial T}{\partial t} - \alpha \nabla^2 T = 0$$

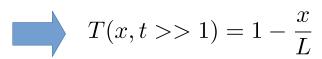
$$T(x = 0, t) = 1$$

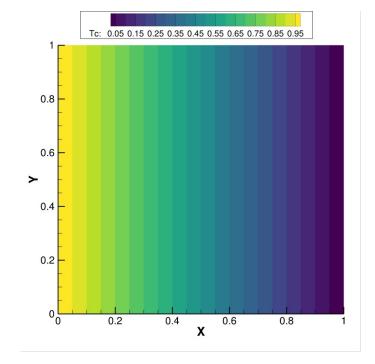
$$T(x = 1, t) = 0$$

$$\partial_n T (y = 0, t) = 0$$

$$\partial_n T (y = 1, t) = 0$$

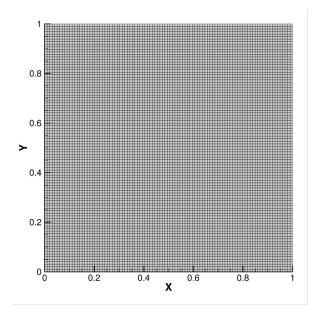
$$T(x, t = 0) = 1$$





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### **Ex3\_FVM** - Unsteady state heat conduction in 1-D configuration



$$\frac{\partial T}{\partial t} - \alpha \nabla^2 T = 0$$

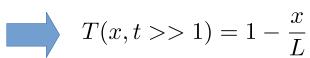
$$T(x = 0, t) = 1$$

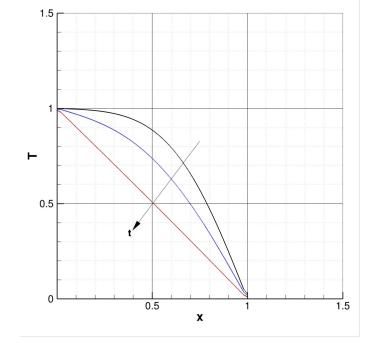
$$T(x = 1, t) = 0$$

$$\partial_n T (y = 0, t) = 0$$

$$\partial_n T (y = 1, t) = 0$$

$$T(x, t = 0) = 1$$

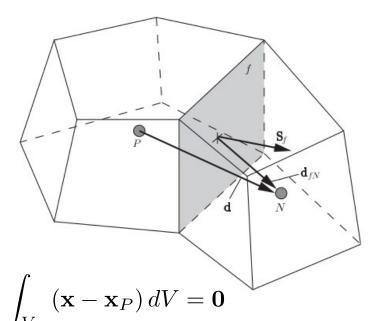




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### Finite volume discretization of general heat conduction equation

General heat conduction equation is discretized its integral form over each control volume:



$$\rho c \frac{\partial T}{\partial t} - \lambda \nabla^2 T = \rho_b c_{p,b} \omega_b \left( T_{a,0} - T \right) + G_L$$

$$G_L = \alpha I(x)$$
  $I(x) = I_0 e^{-\alpha x}$   $g_p = \frac{\rho_b c_{p,b} \omega_b}{\rho c}$ 

$$\frac{\partial T}{\partial t} - \alpha \nabla^2 T + g_p T = g_p T_{a,0} + \frac{1}{\rho c} G_L$$



$$\int_{V_P} \left( \frac{\partial T}{\partial t} - \alpha \nabla^2 T + g_p T \right) dV = \int_{V_P} \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right) dV$$

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### Finite volume discretization of general heat conduction equation

The FVM discretization of general heat conduction equation differes from the previous case only for the source terms.

$$\int_{V_P} \left( \frac{\partial T}{\partial t} - \alpha \nabla^2 T + g_p T \right) dV = \int_{V_P} \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right) dV$$



$$V_P \frac{T_C^{(n+1)} - T_C^{(n)}}{\Delta t} - \sum_f \alpha \left( \nabla T \right)_f \cdot \mathbf{S}_f + V_P g_P T_C = V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

Backward Euler and an implcit time integration strategy is adopted:

$$V_{P} \frac{T_{C}^{(n+1)} - T_{C}^{(n)}}{\Delta t} - a_{C} T_{C}^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} + V_{P} g_{P} T_{C}^{(n+1)} = V_{P} \left( g_{p} T_{a,0} + \frac{1}{\rho c} G_{L} \right)$$

$$\frac{V_{P}}{\Delta t} T_{C}^{(n+1)} - a_{C} T_{C}^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = -b_{C} + \frac{V_{P}}{\Delta t} T_{C}^{(n)} \quad \text{Fourier equation}$$

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### Finite volume discretization of general heat conduction equation

$$V_P \frac{T_C^{(n+1)} - T_C^{(n)}}{\Delta t} - a_C T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} + V_P g_P T_C^{(n+1)} = V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

$$\frac{V_P}{\Delta t}T_C^{(n+1)} - a_C T_C^{(n+1)} - \sum_{t} a_{nb} T_{nb}^{(n+1)} = -b_C + \frac{V_P}{\Delta t} T_C^{(n)}$$
 Fourier equation



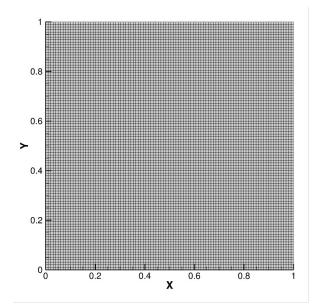
$$\frac{V_P}{\Delta t} T_C^{(n+1)} + \tilde{a}_c T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = \tilde{b}_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

$$\tilde{a}_c = -a_c + V_P g_P$$

$$\tilde{b}_C = -b_C + V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

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### Ex4\_FVM - Heat conduction in a biological tissue under laser heating



$$\rho c \frac{\partial T}{\partial t} - \lambda \nabla^2 T = c_{p,b} w_b (T_{a,0} - T) + G_L$$
$$T(x = 0, t) = 37$$

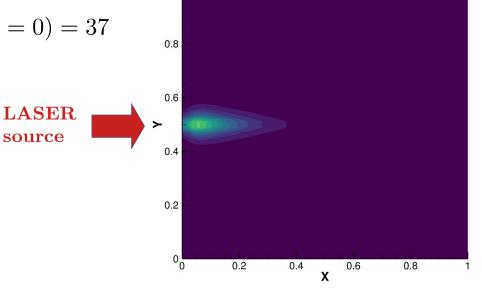
$$\partial_n T\left(x=1,t\right) = 0$$

$$\partial_n T\left(y=0,t\right)=0$$

$$\partial_n T\left(y=1,t\right)=0$$

$$T(\mathbf{x}, t = 0) = 37$$

- LASER source is active only for 10 s. It is applied at (x,y)=(0,0.5). the spot diameter is 1cm, while LASER intensity is  $15 \text{ MW/m}^2$ .
- Tissue properties are standard. (Take a look to the code on gitHub to obtain their values.)





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### **Ex4\_FVM** - Heat conduction in a biological tissue under laser heating

```
alpha = 1.26e-3;
rhot = 1050;
     = 3770;
cpb
      = 3340:
cpt
     = 0.5;
wb
      = 37;
Ta0
Tini = 37;
      = 0.05;
caseName='cube';
         = 0.01;
dt
Time
         = 1:
writeInt = 100;
m=mesh data(caseName);
Nc=m.numberOfElements:
Ni=m.numberOfInteriorFaces:
Nb=m.numberOfBElements:
A=zeros(Nc,Nc);
b=zeros(Nc,1);
```

$$\frac{V_P}{\Delta t} T_C^{(n+1)} + \tilde{a}_c T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = \tilde{b}_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

$$\tilde{a}_c = -a_c + V_P g_P \qquad \tilde{b}_C = -b_C + V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

- A matrix implementation, as well as **b** vector one, for laplacian and unsteady terms are exactly the same of the Fourier equation case.
- Pennes and Beer law terms can be implemented summing their contribution on **b** and **A** diagonal terms deriving from the Fourier equation discretization.

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#### Ex4\_FVM - Heat conduction in a biological tissue under laser heating

```
% Initial condition
    = zeros(Nc,1);
for i = 1:Nc
   TO(i) = TO(i) + Tini;
end
wrtfld(0, m , T0, 'Tc', caseName);
% A and b allocation
    = zeros(Nc,1);
   = -alpha*A;
   = -alpha*b;
for i=1:Nc
   Vc = m.elements(i).volC;
   A(i,i) = A(i,i) + Vc/dt;
end
```

$$\frac{V_P}{\Delta t} T_C^{(n+1)} + \tilde{a}_c T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = \tilde{b}_C + \frac{V_P}{\Delta t} T_C^{(n)}$$

$$\tilde{a}_c = -a_c + V_P g_P \qquad \tilde{b}_C = -b_C + V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

- A matrix implementation, as well as **b** vector one, for laplacian and unsteady terms are exactly the same of the Fourier equation case.
- **Pennes** and Beer law terms can be implemented summing their contribution on **b** and **A** diagonal terms deriving from the Fourier equation discretization.

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#### Ex4\_FVM - Heat conduction in a biological tissue under laser heating

```
% Initial condition
    = zeros(Nc,1);
for i = 1:Nc
   TO(i) = TO(i) + Tini;
end
wrtfld(0, m , T0, 'Tc', caseName);
. . .
% Beer law term
     = 0.5;
qamma = 8;
      = 1.5e7;
      = zeros(Nc,1);
for i=1:Nc
          = m.elements(i).volC;
   Vc
   if ( abs( m.elements(i).Cc(2) - yL ) < 0.01 )
        bl(i) = gamma*I0*exp(-
gamma*m.elements(i).Cc(1))/(rhot*cpt);
        bl(i) = bl(i)*Vc;
    end
end
```

$$\tilde{a}_c = -a_c + V_P g_P$$
 
$$\tilde{b}_C = -b_C + V_P \left( g_p T_{a,0} + \frac{1}{\rho c} G_L \right)$$

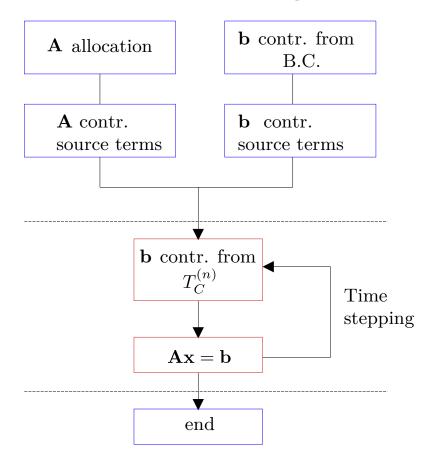
$$G_L = \alpha I(x)$$
  $I(x) = I_0 e^{-\alpha x}$ 

- A matrix implementation, as well as **b** vector one, for laplacian and unsteady terms are exactly the same of the Fourier equation case.
- Pennes and **Beer law** terms can be implemented summing their contribution on **b** and **A** diagonal terms deriving from the Fourier equation discretization.

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#### Ex4\_FVM - Heat conduction in a biological tissue under laser heating

```
bn = zeros(Nc,1);
flow time = 0;
for i= 1: (Time/dt)
    for j=1:Nc
              = m.elements(j).volC;
        bn(i) =
                  b(i) -
                   bl(j)*min( sign(flow time-10),0)
                 + (Vc/dt)*T0(j);
    end
   Tc = bicq(A,bn,1e-12,1000);
   Tc = pcq(A,bn,1e-12,1000,L, U);
    T0 = Tc:
    bn = zeros(Nc,1);
    flow time = flow time + dt;
    if ( mod(i,writeInt) == 0)
          wrtfld(flow time, m , Tc , 'Tc', caseName)
    end
end
```



$$\frac{V_P}{\Delta t} T_C^{(n+1)} + \tilde{a}_c T_C^{(n+1)} - \sum_{nb} a_{nb} T_{nb}^{(n+1)} = \tilde{b}_C + \frac{V_P}{\Delta t} T_C^{(n)}$$