

1. calendar life degradation = 2% / year
 cycle life degradation = 0.05% / cycle
 Annual driving distance = 20,000 km/year
 Energy consumption per year = 200 Wh/km

$$(a) E_{\text{year}} = 20,000 \text{ km} \times 200 \text{ Wh} = 4000 \text{ kWh/year}$$

$$N_{\text{cycles/year}} = \frac{E_{\text{year}}}{E_{\text{pack}}}$$

let's Assume $E_{\text{pack}} = 72 \text{ kWh}$ as per example 2.

$$N_{\text{cycles/year}} = \frac{4000 \text{ kWh}}{72 \text{ kWh}} \approx 55.55 = 56 \text{ cycles/year}$$

$$(b) \text{ Total degradation} = 5 \text{ years} \times 2\% = 10\% \text{ (Calendar loss)}$$

$$\text{Cycle loss} = 0.05\% \times 5 \text{ years} \times \frac{4000 \text{ kWh}}{72 \text{ kWh}} = 14\%$$

$$\text{Total Capacity loss} = 10\% + 14\% = 24\%$$

$$(c) \text{ Total allowable degradation} = 100\% - 80\% = 20\%$$

$$\text{loss per year} = 2\% + (0.05\% \times 56) = 2\% + 2.8\% = 4.8\%$$

$$\text{Time taken to reduce to } 20\% = \frac{20\%}{4.8\%} \approx 4.2 \text{ years}$$

2. 96S20p Cell mass = 48g $C_p = 3.8 \text{ kJ/kg}\cdot\text{K}$ $R_{\text{int}} = 0.01 \Omega$

Discharge current per string = 120A $t_{\text{max}} = 45^\circ\text{C}$ Cool plate temp: 25°C

Allowed coolant temp rise = 5°C

Coolant: $C_{p,\text{coolant}} = 3.6 \text{ kJ/kg}\cdot\text{K}$, $\rho = 1050 \text{ kg/m}^3$

1. Power loss per cell

$$20 \text{ cells in parallel} = \frac{120A}{20} = 6A$$

$$P_{\text{cell}} = I^2 \cdot R = 6^2 \cdot 0.01 \Omega = 0.36W$$

2. Heat generated per pack

$$N_{\text{cells}} = 96 \times 20 = 1920$$

$$\text{Total power loss, } Q_{\text{total}} = 1920 \text{ cells} \times 0.36W = 691.2W$$

3. Coolant mass flow rate required \rightarrow mass flow rate

$$\text{For steady state heat transfer, } Q = \dot{m} \times C_p \times \Delta T$$

$$\dot{m} = \frac{Q}{C_p \times \Delta T} = \frac{691.2W}{3.6 \text{ kJ/kg} \cdot \text{K} \times 5^\circ\text{C}} = 0.0384 \text{ kg/s}$$

4. Volumetric flow rate.

$$\dot{V} = \frac{\dot{m}}{\rho} = \frac{0.0384 \text{ kg/s}}{1050 \text{ kg/m}^3} = 3.66 \times 10^{-5} \text{ m}^3/\text{s} = 2.20 \text{ L/min}$$

5. Cell temp. rise for thermal resistance

$$\Delta T_{\text{cell}} = P_{\text{cell}} \cdot R_{\text{th}} = 0.36W \times 0.15 \text{ K/W} = 0.054^\circ\text{C}$$

Final design Summary:

Total power loss = 691.2W

Required coolant mass flow rate = 0.0384 kg/s

volumetric flow rate = 2.20 L/min

Cell - cold plate temp rise = 0.054°C

Coolant temp. rise = 5°C (Given).

\rightarrow Capable of delivering $\geq 2.20 \text{ L/min}$ in compatibility with ethylene glycol \rightarrow Thermally coupled to each cell.

Pump \rightarrow Manifold \rightarrow Cold plates (x96) \rightarrow Manifold return

Reservoir for coolant

Heat exchanger /
for cooled radiators
(sized for $\geq 700W$ dissipation at 5°C ΔT)

Manifold system

\rightarrow Can use parallel manifold system with 6-8 parallel branches with each branch feeding 12-16 cold plates