MAE 620-01 -jan 23 - wonday -- jan 25- wednesday - panoptu vo cuided lectures -- Pdf of Puwer Point Presentations-

# 2. Integral Forms of the Conservation Equations for Inviscid Flows

2.1. Philosophy
In aerodynamics, lift, drag, and moments on a vehicle are caused by collisions of atoms and molecules in tegral with that vehicle. We don't count all those collisions, we instead relate those at the macroscopic level 37 ective to things we can measure, pressure, temperature, density, and velocity. We want to know these properties in the flowfield so that we know what they are at the surface. From that knowledge, we can Lagrangian perspective-differential perspective calculated forces and heating rates.

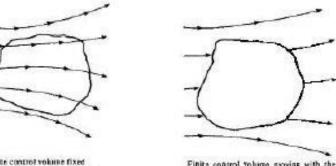
## 2.2. Approach

Everything in fluid mechanics is rooted in surroundings. The laws of mechanics govern thermodynamics, which is rooted in fundamental what happens when there is an interaction with conservation laws. If you understand these very the system at its surroundings. In Anderson's well, you can understand quite a few other book, we use a fixed control volume as shown disciplines. Think of thermodynamics as front below. row tickets to 100's of sporting events.

The control volume approach will not yield detailed results, but are based on one dimensional approximations applied at boundaries. It is great for 'ballparking' performance of a system or subsystem.

## Systems versus Control Volumes

A system is whatever we are going to study, usually defined by a fixed mass with well-defined boundaries, outside of which is called the



inite control volume fixed n apace with the fixed moving nough it

FIGURE 2.1 Finne control volume approach

Pinite control volume moving with the fluid such that the same fluid particles

So virtually everything dealing with fluid flow is modeled using conservation laws (mass or continuity, momentum, and energy). We are going to derive these here in integral form.

# Reynold's transport theorem (not in your 420 book, but from 310)

So we are going to take a fixed control volume approach. Let O (B is your 310 book) be any extensive property of the fluid and  $\beta = dQ/dm$  be the intensive value (Q per unit mass). The total Q in the control volume is

$$Q_{cv} = \int_{cv} \beta \, dm = \int_{cv} \beta \rho \, d \, \mathcal{V} \tag{1}$$

There are 3 sources of change for Q.

A change within the control volume  $\left(\frac{d}{dt}\left(\int_{cv}^{\beta}\beta\rho dv\right)\right)$ 

Inflow of  $\beta$  to the control volume  $\int_{CS} \beta \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta \int_{CS} \rho V \cos \theta dA_m \qquad \sigma V = 4 \cot \theta$ 

d(mass) = which is (vossing system or control system boundary

$$\frac{d}{dt}(Q_{syst}) = \frac{d}{dt} \left( \int_{CV} \beta \rho dV \right) + \int_{CS} \beta \rho V \cos\theta dA_{out} - \int_{CS} \beta \rho V \cos\theta dA_{in}$$

$$= \nabla \int_{CV} \int_{CV} \partial \rho dV + \int_{CS} \beta \rho V \cos\theta dA_{out} - \int_{CS} \beta \rho V \cos\theta dA_{in}$$

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$$= \nabla \int_{CV} \int_{CV} \partial \rho dV + \int_{CS} \partial \rho V \cos\theta dA_{out} - \int_{CS} \partial \rho V \cos\theta dA_{o$$

aka Reynold's transport theorem. This can also be written in more compact form  $\frac{1}{\sqrt{2}} = \frac{1}{\sqrt{2}} + \frac{1$ 

$$\frac{d}{dt}(Q_{syst}) = \frac{d}{dt} \left( \int_{CV} \beta \rho dV \right) + \int_{CS} \beta \rho (\mathbf{V} \cdot \mathbf{n}) dA$$

If we fix the control volume d V does not change with time so the time derivative term on the RHS can be written as

$$\frac{d}{dt} \left( \int_{cv} \beta \rho dv \right) = \int_{cv} \frac{\partial}{\partial t} |\beta \rho| dv \quad \text{Balance (amounts)}$$

$$\text{Boundary}$$

We are going to follow this approach for the conservation of mass, momentum, and energy. Here's the process:

Make a statement about the fundamental principle behind the conservation law.

2. use the fixed control volume to determine the rate of change of some property due to both - time derivative -- un steady part-- related change of B within volumetric and surface effects.

summarize the final formula.

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2.3. Continuity Equation / conservation of mass

- Mass can never be created or destroyed Discuss.
- V is the volume of the fixed control volume

S is the surface area

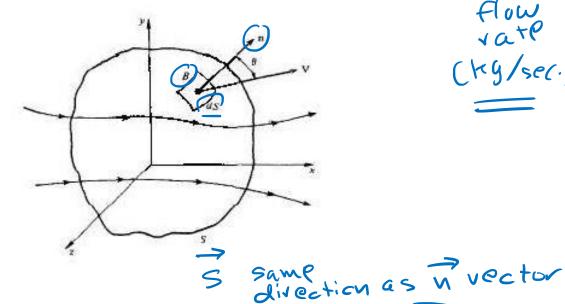
B is a point on the control surface

dS is the elemental area around B
n is the unit vector normal to the surface B

 $\sqrt{dS} = n dS$ .

V, ρ are the local velocity, density at B

 $\rho V_n$  is the mass flux



The mass flow rate is

$$d\dot{m} = \rho (V\cos\theta) dS = \rho V_n dS = \rho V \cdot dS$$
(6)

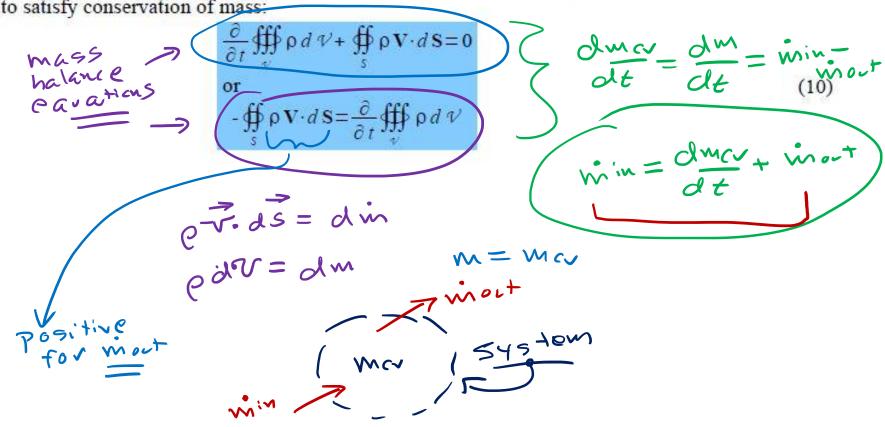
Net mass across the control volume surface is

The total mass is

The time rate of change of this mass is

$$\frac{\partial}{\partial t} \iiint_{\mathcal{V}} \rho \, d \, \mathcal{V} \tag{9}$$

 Therefore, the sum of the net rate increase in mass plus the net mass flux across the surface must be zero to satisfy conservation of mass:



# 2.4. Momentum Equation

- 1. The time rate of change of momentum on a body is equal to the net force exerted on it
- in vector form,

$$\frac{d}{dt}(m\mathbf{V}) = \mathbf{F} \tag{11}$$

side point: for constant mass this is F=ma

There are two types of forces, body and surface. Body forces are due to fields, like gravity, electromagnetic, and the force. surface forces act at the surface of a control volume, and are due to pressure and shear stress.

Total body force 
$$= \iiint_{\mathcal{V}} \rho \, \mathbf{f} \, d \, \mathcal{V}$$

$$\beta = V \tag{12}$$

(14)

Total surface force due to pressure 
$$= - \iint_{S} p \, d \, S$$
 (13)

The minus sign is because the pressure force acts inward, opposite in direction from direction of S.

Now we need to account for the change in momentum. There are two sources. First, momentum can move across the surface. Second, momentum can change inside the volume. So the time rate of change of momentum is the sum of these, the net flow of momentum across the surface plus the rate of change of momentum inside the volume. The time rate of change of momentum is thus

$$\frac{d}{dt}(m\mathbf{V}) = \oiint (\rho \mathbf{V} \cdot d\mathbf{S}) \mathbf{V} + \oiint \frac{\partial (\rho \mathbf{V})}{\partial t} d\mathbf{V}$$
3. Putting it all together,
$$\oiint (\rho \mathbf{V} \cdot d\mathbf{S}) \mathbf{V} + \oiint \frac{\partial (\rho \mathbf{V})}{\partial t} d\mathbf{V} = \oiint \rho \mathbf{f} d\mathbf{V} - \oiint \rho d\mathbf{S} + \mathbf{F}_{viscous}$$

$$\longleftrightarrow (\rho \mathbf{V} \cdot d\mathbf{S}) \mathbf{V} + \oiint \frac{\partial (\rho \mathbf{V})}{\partial t} d\mathbf{V} = \oiint \rho \mathbf{f} d\mathbf{V} - \oiint \rho d\mathbf{S} + \mathbf{F}_{viscous}$$

We are going to neglect the viscous term, but put it in here for completeness.

### 2.5. A Comment

1974 De wat transfer positive into rate = positive into arstem See comment in the TEXTBOOK!

# 2.6. Energy Equation

- 1. Energy can neither be created nor destroyed. It can only change form.
- 2. There are several ways to change energy of the system: heat transfer, work, energy flux into the system, source terms (like radiation). You can also convert one form of energy into another, like dissipation or acceleration. time derivative of energy within

Let's just jump right into it

First law is

$$\dot{Q} + \dot{W} = \dot{E} = \frac{\partial}{\partial t} \left( \iiint_{\mathcal{V}} \rho \, e_{tot} \, d \, \mathcal{V} \right) + \iint_{S} \rho \, e_{tot} \, \mathbf{V} \cdot d \, \mathbf{S}$$

etot transport
across
system boundary

(16)

where e<sub>tot</sub> is the total specific internal energy (see a few sections from pow). In words, the processes for changing energy are equal to the time rate of change of energy in the system. Positive Q/W denote heat added to/work done on the system. Now we are going to break this down into individual terms, energy transport with in tem across system boundary and put it all back together.

### 2.6.1. Heat transfer

The heat transfer per unit mass is  $\dot{q}$ . Thus the heat transfer rate to the control volume is

$$\frac{\dot{Q} = \iiint \dot{q} p \, d \, v}{e + t \, al} = e \, interval \\
+ e \, potential + e \, kinetic \\
+ e \, o + ho \, al$$

#### 2.6.2. Work

Work is the dot product of force with the distance. The rate of change of work, or power, is then the force acting on the body times the velocity,

$$\dot{W} = FV$$
  $\dot{W} = \omega o k$  =  $\gamma o \omega e \ell$  (18)

Work is split into

$$\dot{W} = \dot{W}_{shaft} + \dot{W}_{pressure} + \dot{W}_{body} + \dot{W}_{viscous\ stresses}$$

$$= \dot{W}_{s} + \dot{W}_{p} + \dot{W}_{b} + \dot{W}_{v}$$
(19)

Shaft work will be specified or computed, but no details are involved. Pressure work is

$$W_{p} = - \bigoplus_{S} (p \, dS) \cdot V \qquad \qquad P = P \times e + S \times V \cdot C \qquad (20)$$

and acts on the surface of the control volume. I call this the flow work term, as is done in Moran and

Shapiro. You add this to internal energy, and you get the enthalpy

For gravitation and other body forces, we have

$$\dot{W}_b = \iiint_{V} (\rho \mathbf{f} dV) \mathbf{V}$$

Shear work is similar, and given by

$$\dot{W}_{v} = -\int_{CS} \mathbf{\tau} \cdot \mathbf{V} \, d\mathbf{A} \tag{22}$$

This term is often small and neglected. At solid surfaces, V = 0 so this term vanishes at the wall.

## 2.6.3. **Energy**

On a per unit mass basis, the system energy.

$$e_{tot} = e_{internal} + e_{potential} + e_{kinetic} + e_{other}$$

or

$$e = \inf_{\text{energy}} e_{\text{tot}} = e + \frac{1}{2} V^2 + gz$$
 (24)

We will neglect potential energy and other sources of stored energy, and drop the subscript 'internal' so that 'e' implies internal energy. Just like conservation of mass and momentum, there are two ways the energy can change. The energy can change inside the volume, plus there can be energy flux across the

 $(\rho \mathbf{V} \cdot d\mathbf{S}) \left( e + \frac{V^2}{2} \right)$  Thus we have we have surface. The elemental flux of energy across dS is

Putting it all together

$$\iiint_{V} \dot{q} \rho d \mathcal{V} - \oiint_{S} (p d \mathbf{S}) \cdot \mathbf{V} + \oiint_{V} \rho \mathbf{f} \cdot \mathbf{V} d \mathcal{V} = \oiint_{S} \rho \left[ e + \frac{V^{2}}{2} \right] \mathbf{V} \cdot d \mathbf{S} + \oiint_{V} \frac{\partial}{\partial t} \left[ \rho \left[ e + \frac{V^{2}}{2} \right] \right] d \mathcal{V} \tag{26}$$

You can also add in shaft work or viscous stress terms, but we leave them out.