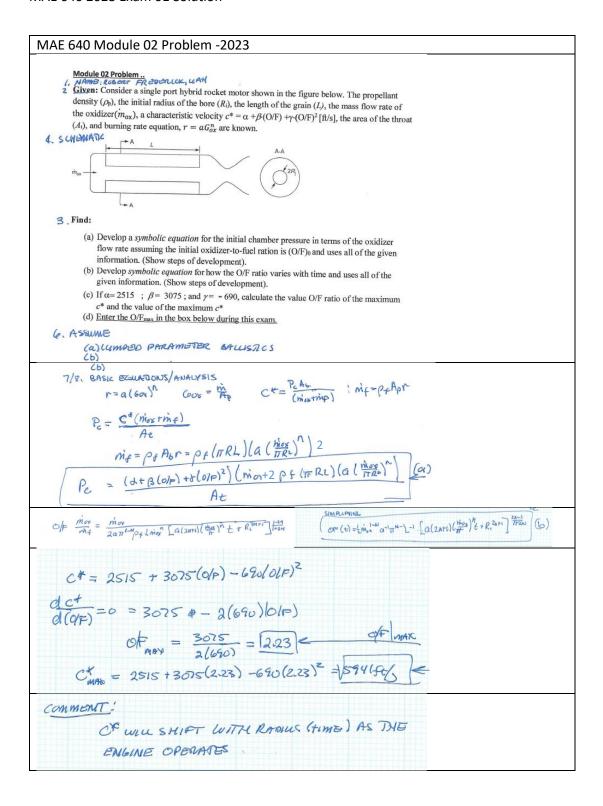
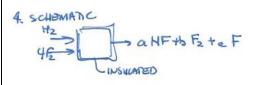
MAE 640 Module 01 Problem - 2023 Module 01 Problem I. NAWE: DR. ROBBET FREDERIKK Z. Given: The TRW Ultra Low Cost Engine (ULCE) shown in 4. Schematic figure (dimensions are in inches) operates nominally at a chamber pressure of 700 psi and uses LOX/LH2 propellant with a c*=7800 ft/s and a mixture ratio (O/F = 6.0), and a $\gamma = 1.2$. (a) Total engine propellant flow rate in lbm/s (b) Sea level thrust in lbf (c) Vacuum thrust lbf (d) Sea level and vacuum I_{sp} (e) If the engine is tested at sea level, determine the area ratio in the exit cone where the flow is likely to separate assuming $p_{sep}/p_a = 0.33333$ (f) Enter the area ratio that you calculated for part (e) in the online box S. ASSUME (4) STENDY STATE (6) ATM = 14.7 psc (c) ISEMMONIC, 1-0 FLOW 6. BASIC EQUATIONS F = Co Atle Is = Cost CR = PEAL At = TID== TI (28.8 IN) = 651.44 In2 m = 7000bt/in2 (651,41m2) (322.0bmft) = 1882,5 cmm 7800FEK FROM GRAPH E=(128.8/288) = 20, 8= 62 (Figure 4.6), Pc/Parm= 700 = 48 READING FROM FIGURES 46 PULLE -> CEVAC= 1.8205, CFSL = 1.8205 - (4.7/200)(20) = 1.400 (10) Frac = 1.8000(051.41n2)(200006+/1, 2) = [830,165 lbf (0) = [638,411. 854 FSL = FVAC (:1,400) = Is = CACX | IsVM= 1.8208(1800495) = 1441 sec (d) Issz = (1.400) (440s) = (33980 CPUNC $P_{\rm c}/P_{\rm a} = \infty$ mac 640 - Boam of (2 1000 Line of maximum 500 thrust coefficient. PROBLEM -01 (e) Psep = 0,3333 (147 psc)= 4,9 psc $P_o = P_o$ Private 10 PSOD = 4.9 PSE = 0.007 => PE = 0.007 FOR LEARNING C NORMARCHION OF SEPARATION 150 (A) Ü PURPOS CP TABLES 8=1.2. 1.2 So Esep = 15.6 (8) Po / Pc Line of separat CHECKS ON SPREAMSHEET ,007 100677 10 6 TSIB L E=20 Area ratio (A_/A_) FELSON = 1.467 (651.44) (100) = 66% 9030 bg CFSL=1.467 ABOUT 54-HIGHER 9. COMMENT · THE OPENATION CAM BE VISUALITIED OF A CA PLET AND CROSS -CHECKED · THE SEA-LEVEL THRUST WOULD BE OFF IF THE FLOW SOPARADED AS PREDICTED AND WOLLD ACTUALLY BE HIGHER



MAE 640 Module 03 Problem - 2021

- (a) The O/F ratio of the reactants assuming difluorine F₂ is the oxidizer and H₂ is the fuel.
- (b) A mathematical *equation* for "c" as only a function of "b" by balancing the atoms in the reaction equation.
- (c) A *mathematical equation* for the equilibrium constant K_p for the dissociation reaction shown. Express K_p as a function of pressure (P) and "b".
- (d) A mathematical equation for the enthalpy balance of the products and the reactants for an adiabatic combustion, assuming that the specific heats all of the products do not change with temperature (i.e. $C_{\rm p,HF} = {\rm const.}$; $C_{\rm p,F2} = {\rm cont.}$; and $C_{\rm p,F} = {\rm const.}$). The equation should allow the calculation of enthalpy as a function of product temperature.
- (e) A *mathematical equation* for the enthalpy balance of the products and the reactants for an adiabatic combustion, assuming that the specific heats all of the products <u>do change</u> with temperature with a third-order polynomial curve fit as shown in the book. The equation should allow the calculation of enthalpy as a function of product temperature. Complete any mathematical integrations. Include <u>symbols for</u> any relevant heats of formation, and complete any integrals. (Do not solve)
- (f) If the pressure were doubled, would there be more or less dissociation of F₂? Would the calculated product temperature increase or decrease?
- (g) Enter the O/F ratio that you calculated in part (a) in the online box below



IL CONTINUT PRESSURE
COMBUSTION

2. DISSUCIATION REATION GIVEN

3. SPEARDY STATE

4- ADIABATK CUMBUSTION

S. CONSTRINT SPECIFIC MEAT VALUES FOR THE PRODUCTS AND REPORTANTS

6. BASIC GOLLATIONS /ANALYSIS

$$H_{2}+4F_{2} \longrightarrow a HF + bF_{2}+eF$$
 $H: a=a$
 $P = a+2b+e = c=6-2bF$
 $8=a+2n+e = c=6-2bF$

$$F_{2} = 2F$$

$$K_{P} = \frac{(X_{P})^{2}}{(X_{P})^{2}} P^{2-1} = \frac{(X_{P})^{2}}{X_{P2}} P$$

$$X_{F} = \frac{C}{n}$$

$$X_{F2} = \frac{b}{n}$$

$$N = a + b + C = 2 + b + (6 - 2b) = 8 - b$$

$$K_{P} = \frac{(6 - 2b)^{2}}{8 - b} P = \frac{(6 - 2b)^{2}}{b(8 - b)} P = K_{P}$$

$$CC)$$

$$CMARKET$$

$$H_{p}-H_{R} = a h_{HF} + b h_{F} + c h_{F} - 1 \cdot h_{HZ} - 4 h_{FZ} = 0$$

$$h = \int_{-\infty}^{T_{2}} c_{0} dT + h_{F} \Big[iF c_{pcontent} - (c_{p}(T_{2}-T_{0}) + h_{F}) \Big] dC_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] - 1 \cdot 0 \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] - 4 \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + b \Big[c_{p}(T_{2}-T_{0}) + h_{F} \Big] + c \Big[c_{p}(T_{2}-T_{0}) + c \Big[c_{p}(T_{2}-T_{0}) + c \Big[c_{p}(T_{2}-T_{0}) + c \Big[c_{p}(T_{2}-T_{0}) + c$$

olynomial
$$Cp = a' + b' \left(\frac{T}{1000}\right) + c' \left(\frac{T}{1000}\right)^2 + d' \left(\frac{T}{10000}\right)^3$$

$$\begin{split} H_2 &= 0 = 2 \left[a'T + \frac{b'T}{2} \left(\frac{T}{1000} \right) \right. \\ &+ \frac{c'T}{3} \left(\frac{T}{1000} \right)^2 \frac{d'T}{4} \left(\frac{T}{1000} \right)^3 \right]_{T^0}^{T_2} + \Delta h_f^0 \Big|_{HF} \\ &+ (b) \left[a'T + \frac{b'T}{2} \left(\frac{T}{1000} \right) \right. \\ &+ \frac{c'T}{3} \left(\frac{T}{1000} \right)^2 - \frac{d'T}{4} \left(\frac{T}{1000} \right)^3 + \Delta h_f^0 \Big|_{HF} \right]_{T^0}^{T_2} \Big|_{F_2} \\ &+ (6 - 2b) \left[a'T + \frac{bT'}{2} \left(\frac{T}{1000} \right) \right. \\ &+ \frac{c'T}{3} \left(\frac{T}{1000} \right)^2 + \frac{d'T}{4} \left(\frac{T}{1000} \right)^3 \right]_{T^0}^{T_2} \Big|_{F_2} \end{split}$$

IF PRESSURE DOUBLED LESS DISSOCIATION (LESS P)

COMMENT! IN REMOTY WOULD USE CO = FCT) AND CHINE PUTS POR

Pressure	100	200
riessule	100	200
OF	75.35	75.35
FPCT	1.309758	1.309758
ERATIO	0.250149	0.250149
Phi	0.250149	0.250149
Р	99.99996	199.9999
T	2847.332	2975.286
MW	22.10102	22.35648
AR	0	0
F	56%	55%
F2	15%	16%
HF	29%	29%