

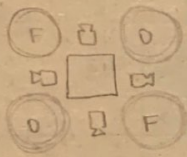
Name: Veronica Loomis

Problem 8.4

Given: N_2O_4/MMH propellant combo
 Equal volumes for both fuel & oxidizer tanks
 Payload mass = 10 kg
 $I_{sp} = 300$ sec
 Required $\Delta v = 1000$ m/s
 $\lambda = 0.5$

Find: a) propellant mixture ratio
 b) total propellant mass required
 c) radius of spherical tanks
 d) tank wall thickness if $P_{burst} = 5$ MPa and is titanium

Schematic:



Assumptions:

Each tank has same volume
 Keep grav in Δv eq so units work
 Thin wall tanks
 $\rho_{ox} = 1440 \text{ kg/m}^3$
 $\rho_f = 880 \text{ kg/m}^3$ } googled

Basic Equations:

$$r = \frac{m_{ox}}{m_f}, \quad \rho = \frac{m}{V}, \quad MR = \frac{m_o}{m_f}, \quad m_o = m_{pl} + m_p + m_i, \quad \lambda = \frac{m_p}{m_p + m_i}$$

$$V_{sph} = \frac{4}{3}\pi R^3, \quad \Delta v = I_{sp} \ln\left(\frac{m_o}{m_f}\right), \quad m_p = m_{pl} \left(\frac{MR-1}{MR-(MR-1)/\lambda} \right)$$

$$t_c = P_t R / \sigma_w, \quad \sigma_w = \min(F_t/1.1, F_{tu}/1.25) \quad \text{Go to 1.4}$$

Analysis:

a) Propellant mixture ratio

$$\Delta v = g I_{sp} \ln\left(\frac{m_o}{m_f}\right) \rightarrow \frac{m_o}{m_f} = e^{\Delta v / g I_{sp}}$$

$$\frac{m_o}{m_f} = e^{(1000 \text{ m/s}) / (9.81 \text{ m/s}^2)(300 \text{ s})}$$

$$\boxed{\frac{m_o}{m_f} = 1.4 = MR}$$

b) Total propellant mass required

$$m_p = m_{pl} \left(\frac{MR-1}{MR-(MR-1)/\lambda} \right) = 10 \left(\frac{0.4}{1.4 - \frac{0.4}{0.5}} \right) \text{ kg}$$

$$\boxed{m_p = 6.67 \text{ kg}}$$

c) Radius of spherical tanks

know $m_p = 6.67 \text{ kg}$

need $r = \frac{m_{ox}}{m_f}$

have $\rho_{ox} = \frac{m_{ox}}{V_{ox}}$ & $\rho_f = \frac{m_f}{V_f}$

told $V_f = V_{ox}$

\therefore we can say $\frac{\rho_{ox}}{\rho_f} = \frac{m_{ox}}{m_f}$

$\rho_{ox}/\rho_f = 1440/880 = 1.636 = r$

$m_f = \frac{m_p}{1+r} = 2.53 \text{ kg}$

$m_{ox} = r m_f = 4.14 \text{ kg}$

$V_f = \frac{m_f}{\rho_f} = 0.002875 \text{ m}^3$ } yes they are the same

$V_{ox} = \frac{m_{ox}}{\rho_{ox}} = 0.002875 \text{ m}^3$

$R = \sqrt[3]{\frac{3V}{4\pi}} = \sqrt[3]{\frac{3(0.002875 \text{ m}^3)}{4\pi}}$

$R = 0.0882 \text{ m}$

d) Tank wall thickness

$t_c = \frac{P_t(\max) R}{\sigma_w}$ $P_t = 5 \text{ MPa}$

$\sigma_w = \min\left(\frac{\text{yield}}{1.1}, \frac{\text{ult tens. strength}}{1.4}\right)$ look up for titanium

$\sigma_w = \min\left(\frac{241 \text{ MPa}}{1.1}, \frac{1400 \text{ MPa}}{1.4}\right) = 219.1 \text{ MPa}$

$t_c = \frac{5 (0.0882)}{219.1} \frac{\text{MPa} \cdot \text{m}}{\text{MPa}}$

$t_c = 0.00201 \text{ m} = 2.01 \text{ mm}$

Comments:

The wall thickness is allowed to be SUPER thin because of the material.

I also realized afterwards that (c) could just have been $V = \frac{m_p}{\rho_f + \rho_{ox}}$... but I guess it was good to make sure $V_f = V_{ox}$ like we assumed.

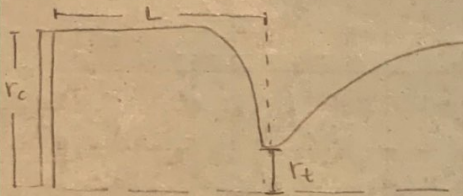
Name: Veronica Loomis

Problem 8.6

Given: LOX & Ethanol
 $c^* = 5900 \text{ ft/s}$
 $\gamma = 1.2$
 $F_v = 30000 \text{ lbf}$
 $\epsilon = 50$
 $P_c = 1200 \text{ psi}$
 $M \leq 0.1$
 $L^* = 40 \text{ inches}$ - char. chamber dim.

Find: a) I_{sp}
 b) r_t
 c) r_c
 d) L (chamber)

Schematic:



Assumptions:

Purdue tables

~~Analysis~~ Basic Equations:

$$I_{sp} = \frac{c_{fv} \cdot c^*}{g}, \quad F_v = c_{fv} P_c A_t, \quad A_c = (N_{ox} + N_{fuel}) / N_D$$

$$\epsilon_c = A_c / A_t, \quad \frac{A_c}{A_t} = \frac{1}{M} \left[\frac{2 + (\gamma - 1) M^2}{\gamma + 1} \right]^{(\gamma + 1) / 2(\gamma - 1)}$$

$$L^* = \frac{\sqrt{V_c}}{A_t}$$

Analysis:

a) I_{sp}

$$I_{sp} = \frac{c_{fv} \cdot c^*}{g} \quad \text{Using } \gamma = 1.2, \epsilon = 50$$

$$c_{fv} = 1.90236$$

$$I_{sp} = \frac{(1.90236)(5900 \text{ ft/s})}{32.2 \text{ ft/s}^2}$$

$$I_{sp} = 348.57 \text{ sec}$$

b) r_t

$$F_v = C_{Fv} P_c A_t$$

$$A_t = \frac{F_v}{C_{Fv} P_c} = \frac{30000 \text{ lbf}}{(1.90236)(1200 \text{ lbf/in}^2)}$$

$$A_t = 13.14 \text{ in}^2$$

$$r_t = \sqrt{A_t / \pi}$$

$$r_t = 2.045 \text{ in}$$

c) r_c ($M=0.1$)

$$A_c = A_t \left(\frac{1}{0.1} \left[\frac{2 + (0.2)(0.1)^2}{2.2} \right]^{2.2/0.4} \right)$$

$$A_c = 78.22 \text{ in}^2$$

$$r_c = \sqrt{A_c / \pi}$$

$$r_c = 5.0 \text{ in}$$

d) L (chamber)

$$L^* = r_c^2 / A_t$$

$$L^* = \frac{\pi r_c^2 L_c}{A_t}$$

$$L_c = \frac{L^* A_t}{\pi r_c^2} = \frac{40 \text{ in} (13.14 \text{ in}^2)}{\pi (5.0 \text{ in})^2}$$

$$L_c = 6.69 \text{ in}$$

Comment

$r_c > r_t \rightarrow$ expected

L_c is close to r_c

SP05A**Name** Veronica Loomis

Given: Mixture Ratio 5.5
Area Ratio 16
Oxidizer LOX
Fuel LH

Find Tc
C*
M
Isp, v

Analysis

Pc (Bar)	OF	T (K)	MW	CSTAR (m/s)	ISPV (m/s)	ISP(sec)
40		16 1563.140259	22.72205925	1710	3120.118408	318.0548836
50		16 1559.670044	22.72236633	1712	3121.952393	318.2418341
60		16 1556.937988	22.72259521	1714	3123.390137	318.3883931
80		16 1552.812744	22.72292328	1717	3125.551025	318.6086672
100		16 1549.766479	22.72314835	1719	3127.138916	318.7705317

Name: Veronica Loomis**Two-Page Annotated Bibliography Template****A. Summarize**

Reference Document Examined:	Schulte, G., "Fuel Regression and Flame Stabilization Studies of Solid-Fuel Ramjets," <i>AIAA Journal of Propulsion and Power</i> , VOL. 2, NO. 4, July-August, 1986.
Reviewer:	Veronica Loomis
Source of Document:	Canvas
Date of Review:	March 8, 2023
Electronic File Name:	1986_Schulte_JPP_2_4.pdf

Summary:

This paper analyzes fuel regression and flame stabilization in solid fuel ramjets. This was tested by varying flight speed, altitude, chamber pressure, air mass flux, and inlet temperature over wide ranges. The aim was to minimize the ratios of the fuel port to nozzle throat area and the fuel port to injector area.

B. Assess:**Important Facts from Document:**

1. To be considered as a realistic alternative system for propulsion, a SFRJ must operate over the expected operating envelope of Mach numbers and altitudes.
2. The point of transition from recirculation zone to boundary layer redevelopment is not always obvious on fuel surface.
3. Flame holding limits are not sensitive to fuel changes.
4. As port diameter of solid fuel grain increases, average regression rate decreases because of diminished heat transfer to wall.
5. Flame holding limits play an important role in ramjet motor design.

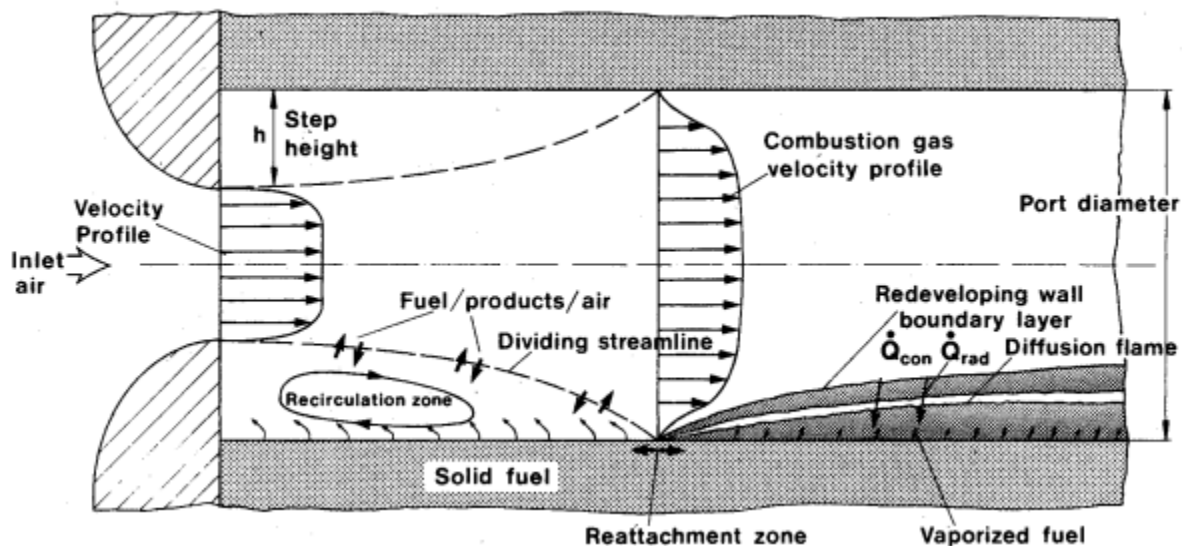
Key Figure from Document:

Figure 1: Schematic illustration of SFRJ dump combustor flow field.

Important Relationships among Parameters Described in the Paper:

1. The rate of solid fuel decomposition depends mainly on the air inlet temp, combustion pressure, and air mass flux.

2. As port diameter increases, regression rate decreases if all other parameters stay constant.

Important Conclusion(s):

1. You can improve motor performance by increasing fuel loading and decreasing pressure losses.
2. Flame holding limits play an important role in ramjet motor design.

C. Reflect

This source does not seem helpful to my current situation. However, it is good to learn more about different types of propulsion systems and their benefits and disadvantages as well as how they are tested.

OF	75.389
Pc	50 atm
Pc	50.6625 Bar
2Pc	101.325 Bar
T	198 K
Pc	50.6625
OF	75.38899994 DIMENSIONLESS
FPCT	1.309089065 DIMENSIONLESS
ERATIO	0.250019759 DIMENSIONLESS
Phi	0.250019759 DIMENSIONLESS
AR	0 DIMENSIONLESS
P	50.66249847 BAR
T	1800.416626 DEG K
RHO	7.754610062 KG/M^3
H	5.64978E-06 KJ/KG
U	-653.3210449 KJ/KG
GFE	-15377.97461 KJ/KG
S	8.541342735 KJ/(KG K)
Z	1 DIMENSIONLESS
MW	22.91305733 MOL WT
CP	5.016849518 KJ/(KG K)
CPG	1.223860383 KJ/(KG K)
GammaG	1.421459913 DIMENSIONLESS
Gamma	1.22964263 DIMENSIONLESS
C	896.2987061 M/S
MW_MIX	22.91305733 MOL WT
Viscosity	0.773292243 milliPOISE
Specific_Heat_Eq	5.016848087 KJ/(KG K)
Conductivity_Eq	4.860545158 milliW/(CM K)
Prandtl_Eq	0.79815942 DIMENSIONLESS
Specific_Heat_Fr	1.223860383 KJ/(KG K)
Conductivity_Fr	1.323586464 milliWATTS/(CM K)
Prandtl_FR	0.715028286 DIMENSIONLESS
PINJ_P	-999.9990234 N/A
PC_P	1 DIMENSIONLESS
MACH	0 DIMENSIONLESS
AR	0 DIMENSIONLESS
CSTAR	0 M/S
CF	DIMENSIONLESS
ISPV	M/S
ISP	M/S
ISPVRHO	KG/(M^2 S)
F	0.51214689 MOLE
F2	0.190263689 MOLE
HF	0.297589451 MOLE

Pc	101.325
OF	75.38899994 DIMENSIONLESS
FPCT	1.309089065 DIMENSIONLESS
ERATIO	0.250019759 DIMENSIONLESS
Phi	0.250019759 DIMENSIONLESS
AR	0 DIMENSIONLESS
P	101.3249969 BAR
T	1887.346558 DEG K
RHO	15.01261616 KG/M^3
H	1.62737E-05 KJ/KG
U	-674.932312 KJ/KG
GFE	-15649.16406 KJ/KG
S	8.291622162 KJ/(KG K)
Z	1 DIMENSIONLESS
MW	23.25027466 MOL WT
CP	4.665799141 KJ/(KG K)
CPG	1.226409674 KJ/(KG K)
GammaG	1.411612272 DIMENSIONLESS
Gamma	1.237751126 DIMENSIONLESS
C	914.0012207 M/S
MW_MIX	23.25027466 MOL WT
Viscosity	0.801559567 milliPOISE
Specific_Heat_Eq	4.665798187 KJ/(KG K)
Conductivity_Eq	4.74695015 milliW/(CM K)
Prandtl_Eq	0.78785646 DIMENSIONLESS
Specific_Heat_Fr	1.226409793 KJ/(KG K)
Conductivity_Fr	1.375738144 milliWATTS/(CM K)
Prandtl_FR	0.714554906 DIMENSIONLESS
PINJ_P	-999.9990234 N/A
PC_P	1 DIMENSIONLESS
MACH	0 DIMENSIONLESS
AR	0 DIMENSIONLESS
CSTAR	0 M/S
CF	DIMENSIONLESS
ISPV	M/S
ISP	M/S
ISPVRHO	KG/(M^2 S)
F	0.490249723 MOLE
F2	0.207781121 MOLE
HF	0.301969141 MOLE