

# FLUID MECHANICS

10.

Momentum balance

$$M_{in}^2 - M_{out}^2 + \sum F = 0$$

$$\Rightarrow \Delta x \omega L \cdot w \cdot z_{x+\Delta n} - L w z_x + g \cdot \rho \Delta n L w \cos \beta = 0$$

$$\Rightarrow (z_{x+\Delta n} - z_x) = - \rho \Delta n g \cos \beta$$

$$\Rightarrow \frac{\partial z}{\partial n} \cos \beta = - \rho g \cos \beta$$

$$\Rightarrow z = - \rho g n \cos \beta + c$$

$$z = - \frac{(\partial v)}{(\partial n)} \Rightarrow - \frac{(\partial v)}{(\partial n)} = - \rho g n \cos \beta + c$$

$$\Rightarrow v = \left( - \frac{\rho g n^2}{2} \cos \beta + c n + d \right) \frac{1}{\mu}$$

Boundary equations

$$A \cap n = 0, \quad z = 0$$

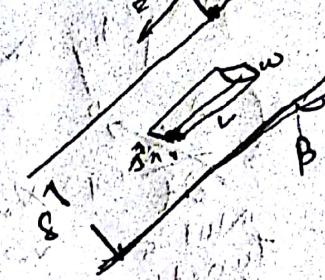
$$\Rightarrow c = 0$$

$$A \cap n = \delta, \quad v = 0$$

$$\Rightarrow \text{also } d = - \frac{\rho g \delta^2}{2} \cos \beta$$

$$\Rightarrow v = - \frac{\rho g (n^2 - \delta^2)}{2 \mu} \cos \beta$$

$$= \frac{\rho g (\delta^2 - \mu n^2)}{2 \mu} \cos \beta - \frac{\rho g \delta (1 - (n/\delta)^2) \cos \beta}{2 \mu}$$



Solving by Navier Stokes equation.

$$\rho \left( \frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = - \frac{dp}{dz} + \rho g z + \mu \left( \frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right)$$

not a function of time  
not a function of z  
no imposed pressure gradient

$$- \mu \frac{\partial^2 v_z}{\partial z^2} = \rho g \cos \beta$$

$$+ \frac{\partial v_z}{\partial z} = \rho g \cos \beta$$

same equations obtained hence verified.

$$Q = \text{flow rate} = \langle v_z \rangle \times \text{flow area}$$

$$\langle v_z \rangle = \iint_{0 \delta}^{w \delta} v_z dx dy = \frac{\rho g \delta^2 \cos \beta \pi \left( 1 - \left( \frac{w}{\delta} \right)^2 \right)}{2 \mu} \left( \frac{w}{\delta} \times \delta \right)$$

$$= \frac{\rho g \delta^2}{2 \mu} \cos \beta \times \left( w - \frac{w^3}{3 \delta^2} \right) \frac{2 \delta^2}{3}$$

$$= \frac{\rho g \delta^2 \cos \beta}{2 \mu}$$

$$Q_2 = \frac{\rho g \delta^2 \cos \beta}{2 \mu} \times \delta \times w$$

$$= \frac{\rho g \delta^3 \times w \cos \beta}{3 \mu}$$

② Diaminate flow in narrow slit

⇒ Momentum balance

$$\text{① } \Sigma u = (\times w) \Big|_{n=n} - L w > \Sigma u_{\text{mean}} \Big|_{n=n} \rightarrow 2\beta \leftarrow w$$

$$+ \rho g x (\Delta n) \times L \times w$$

$$+ (P_0 - P_L) w \Delta n$$

$$\Rightarrow \frac{\Sigma u_{\text{mean}} - \Sigma u}{\Delta n} = \left( \rho g + \frac{P_0 - P_L}{L} \right)$$

$$\Rightarrow \frac{\partial z}{\partial n} = \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right]$$

$$\Rightarrow z = \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right] n + C$$

$$\Rightarrow -\mu \frac{\partial v_x}{\partial n} = \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right] n + C$$

$$\Rightarrow \cancel{\frac{\partial v_x}{\partial n}} v_x = -\mu \left( \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right] \frac{n^2}{2} + Cn + D \right)$$

Boundary conditions

$$\text{at } n = \beta, v = 0$$

$$n = 0, z = 0$$

$$\Rightarrow C = 0$$

$$\therefore d \approx \frac{1}{\mu} \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right] \frac{B^2}{2}$$

$$v_x \approx \frac{1}{\mu} \left[ \rho g + \left( \frac{P_0 - P_L}{L} \right) \right] \frac{B^2}{2} \times \left( 1 - \frac{n^2}{\beta^2} \right)$$

② Using Navier-Stokes equation

$$P \left( \frac{\partial v_x}{\partial t} + v_n \frac{\partial v_x}{\partial n} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = - \frac{dp}{dx} + \rho g + \mu \left( \frac{\partial^2 v_x}{\partial n^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right)$$

$$\Rightarrow -\mu \left( \frac{\partial^2 v_z}{\partial n^2} \right) = -\left( \frac{\partial p}{\partial n} \right) + \rho g$$

$$\Rightarrow -\frac{\partial z}{\partial n} = \rho g + \left( \frac{p_0 - p_L}{L} \right)$$

Average  $v_z$

$$\langle v_z \rangle = \left[ \iint_D v_z \partial n dy \right]$$

$$= \frac{w}{B} \left[ \iint_D \left( \frac{p_0 - p_L}{L} \right) \partial n dy \right]$$

$$= \frac{w}{B} \left[ \frac{-p}{2\mu} \left[ \rho g + \frac{p_0 - p_L}{L} \right] \left( 1 - \frac{w^2}{B^2} \right) \partial n \times w \right]$$

$$= \frac{B^2}{3\mu} \times \left( \rho g + \frac{p_0 - p_L}{L} \right)$$

$$Q = \frac{B^2}{3\mu} \times \left( \rho g + \frac{p_0 - p_L}{L} \right) \times (2B) \times w$$

$$= \frac{2B^3 w}{3\mu} \left( \rho g + \frac{p_0 - p_L}{L} \right)$$

### (3) LIQUID FLOWING THROUGH A PIPE

using Navier-Stokes equation

$$\frac{d}{dz} \left( v_z \right) = v_n \frac{\partial v_z}{\partial n} + \frac{v_n}{\pi} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial^2 v_z}{\partial z^2}$$



$$= \rho g - \frac{\partial P}{\partial z} + \mu \left[ \frac{1}{\pi} \frac{\partial}{\partial n} \left( \pi \frac{\partial v_z}{\partial n} \right) \right]$$

$$+ \frac{1}{\pi^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right)$$

$$\Rightarrow -\mu \left( \frac{1}{\pi} \frac{\partial}{\partial n} \left( \pi \frac{\partial v_z}{\partial n} \right) \right) = \rho g - \left( \frac{P_0 - P_L}{L} \right)$$

$$= \rho g \cdot \left( \frac{P_0 - P_L}{L} \right)$$

$$\Rightarrow -\mu \frac{\partial}{\partial n} \left( \pi \left( \frac{\partial v_z}{\partial n} \right) \right) = \left( \rho g + \frac{P_0 - P_L}{L} \right) \pi$$

$$\Rightarrow \frac{\partial}{\partial n} \left( \pi \left( \frac{\partial v_z}{\partial n} \right) \right) = \rho g \left( \frac{P_0 - P_L}{L} \right) \frac{\pi^2}{2} + C$$

$$\Rightarrow \frac{\partial v_z}{\partial n} = \frac{-1}{\mu} \left[ \left( \frac{P_0 - P_L}{L} \right) \frac{\pi^2}{2} + \frac{C}{\pi} \right]$$

$$\Rightarrow \tau = \left( \frac{P_0 - P_L}{L} \right) \frac{\pi}{2} + C/\pi$$

$$v_z = \frac{-1}{\mu} \left[ \left( \frac{P_0 - P_L}{L} \right) \frac{\pi^2}{4} + C \ln \pi + d \right]$$

$$\text{At } n=0, \tau=0 \Rightarrow C=0$$

$$\text{At } r_L=R, v=0$$

$$-\left( \frac{P_0 - P_L}{L} \right) \frac{R^2}{4} = d$$

$$V_z = \frac{\eta}{\mu} \left[ \frac{(P_0 - P_L)}{L} \cdot R^2 - R^2 \right]$$

$$= \frac{(P_0 - P_L) \times R^2}{\eta \mu L} \left( 1 - \frac{\eta^2}{R^2} \right)$$

$$Q = \langle V_z \rangle \times \pi R^2$$

$$\int_0^{2\pi} \int_0^R V_z \eta d\theta d\phi$$

$$\frac{(P_0 - P_L) \times R^2}{\eta \mu L} \cdot \frac{2\pi R^2 (1 - \frac{\eta^2}{R^2})}{6}$$

$$\left( \frac{2\pi}{3} \right) \cdot \pi \cdot \frac{\eta R^2}{6} \left( \left( \frac{1}{2} \right)^2 - \left( \frac{1}{3} \right)^2 \right)$$

$$\left( \frac{2\pi}{3} \right) \cdot \pi \cdot \frac{\eta R^2}{6} = \frac{P_0 - P_L}{\eta \mu L} \times R^2 \times \frac{R^2}{2\pi} \times \frac{\pi}{\pi R^2}$$

$$\left( \frac{2\pi}{3} \right) \cdot \pi \cdot \frac{\eta R^2}{6} = \langle V_z \rangle \cdot \frac{(P_0 - P_L) R^2}{8\mu L}$$

$$Q = \frac{(P_0 - P_L) \pi R^4}{8\mu L}$$

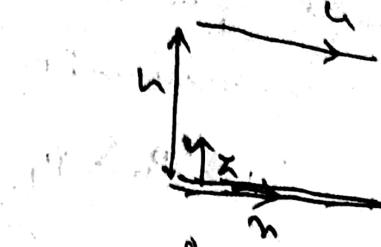
$$\left( \frac{2\pi}{3} \right) \cdot \pi \cdot \frac{\eta R^2}{6} = Q$$

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## ① Couette flow

$$\frac{\partial u}{\partial t} \rightarrow \rho f(\partial)$$



$$\rho \left( \frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{dp}{dz} + \mu \left[ \frac{\partial^2 v_x}{\partial z^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial x^2} \right] + f_{x_2}$$

If there is no imposed pressure gradient,

$$\mu \frac{\partial^2 v_x}{\partial z^2} = 0$$

$$\Rightarrow \mu \frac{\partial v_x}{\partial z} = C$$

$$\Rightarrow v_x = Cz + d$$

Boundary conditions

$$\text{At } z=0, \quad v_x = 0$$

$$\text{At } z=h, \quad v_x = u$$

$$\Rightarrow v_x = Cz$$

$$\text{At } z=h, \quad u = Ch$$

$$\Rightarrow C = \frac{u}{h}$$

$$\Rightarrow v_x = \frac{uz}{h}$$

$$v_z = -\frac{u\mu}{h}$$

Pressure gradient =  $\frac{P_L - P_0}{L}$   
 Favourable when  $P_0 > P_L$

In Couette flow, there exists a pressure gradient

$$\Rightarrow \frac{dp}{dz} = \mu \frac{\partial^2 v_n}{\partial z^2} \quad \text{det } \frac{dp}{dz} = C$$

$$\Rightarrow \zeta = \mu \left( \frac{\partial^2 v_n}{\partial z^2} \right)$$

$$\Rightarrow (cz + d) = \mu \frac{\partial v_n}{\partial z}$$

$$\Rightarrow \left( \frac{cz^2}{2} + dz + e \right) = \mu (v_n)$$

Same boundary conditions

$$\text{At } z=0, v_n=0$$

$$z=h, v_n=u \Rightarrow \frac{ch^2}{2} + dh = u$$

$$\mu \left( \frac{ch^2}{2} + dh \right) = \mu u$$

$$(ch + dh) = u$$

$$\left( \frac{ch^2}{2} + dh \right) \Rightarrow (dh \approx ah)$$

$$\Rightarrow d = \frac{1}{h} \left( \mu u - \frac{ch^2}{2} \right)$$

$$\Rightarrow v_n = \frac{1}{\mu} \left[ \frac{cz^2}{2} + \frac{1}{h} \left( \mu u - \frac{ch^2}{2} \right) \right]$$

Now, let an unfavourable pressure gradient is applied so that net flow rate = 0

$$\langle v_x \rangle = 0$$

$$\Rightarrow \int_0^h \left[ \frac{Cz^2}{2} + \frac{1}{4} (\mu u - \frac{ch^2}{2}) z \right] dz = 0$$

$$= 0$$

$$\Rightarrow \left( \frac{Cz^3}{6} + \frac{\mu z^4}{2h} - \frac{ch^2 z^2}{4} \right) = 0$$

$$= 0$$

$$\frac{Ch^3}{6} + \frac{\mu h^4 u}{2} - \frac{ch^3}{4} = 0$$

$$\Rightarrow \frac{\mu u}{2} = ch^2 \left( \frac{1}{4} - \frac{1}{6} \right)$$

$$\frac{ch^2}{12}$$

$$\Rightarrow \frac{ch^2}{12} = \frac{\mu u}{2}$$

we can find fav. pressure.

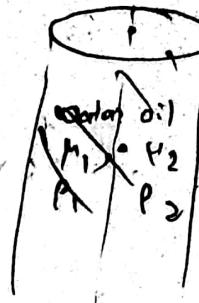
gradient from  $v_x$  to be max.

similarly, by equating

$$\frac{\partial v_x}{\partial z} = 0$$

## # Remember

If there is an interface of two liquids flowing, then at that section, the velocities of both the fluids are the same.



→ Also, the stress at interface are same.

6. Magnet wire being coated with varnish in a tube wine assembly. Find the force required to pull.

$$d = 0.8 \text{ mm}$$

$$L = 20 \text{ mm}$$

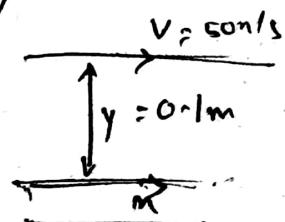
$$D = 0.9 \text{ mm}$$

$$\mu = 20 \text{ cP}$$

$$V = 50 \text{ m/s}$$

When the separation between two layers is very small, we can convert the cylindrical coordinate system to cartesian coordinate system.

$$f \left( \frac{\partial \phi}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right)$$



$$= - \frac{dp}{dn} + f \left[ \frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right] + pg$$

$$\Rightarrow \frac{dP}{dy} = \mu \frac{\partial^2 v_n}{\partial y^2}$$

It is similar to a Couette flow.

$$\Rightarrow \mu \frac{\partial^2 v_n}{\partial y^2} = 0$$

$$\Rightarrow \frac{\partial v_n}{\partial y} = C$$

$$\Rightarrow v_n = Cy + d$$

$$At \quad y=0, \quad v_n=0$$

$$\Rightarrow At \quad y = \cancel{0.05} \text{ mm}$$

$$v_n = 50 \text{ m/s}$$

$$\Rightarrow C = \frac{50}{0.05 \times 10^{-3}} = \frac{(5 \times 10^5)}{10^{-3}} = 1 \times 10^8$$

$$v_n = Cy$$

$$-\mu \frac{\partial v_n}{\partial y} = -\mu C = \frac{2 \times 10^{-5}}{10^{-3}} \times 1 \times 10^8 = (2 \times 10^5) \\ = 2 \times 10^5$$

~~$(F \times \pi D L)$~~  = F

$$\Rightarrow F = \frac{10^5}{2 \times (0.8 \times 10^{-3}) \times 2 \times 10^5}$$

~~$(2 \times \pi D L)$~~  = F

$$\Rightarrow F = 2 \times 10^5 \times \pi \times D \times L$$

$$= 2 \times 10^5 \times \pi \times 0.8 \times 10^{-3} \times 2 \times 10^5$$

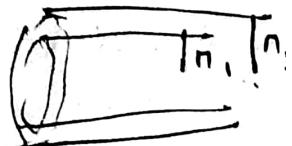
$$= 10.05 \text{ N}$$

TRYING TO SOLVE IN CYLINDRICAL  
SYSTEM OF CO-ORDINATE

$\hat{x}$  is the direction of flow here.

$$\rho \left( \frac{\partial v_x}{\partial t} + v_r \frac{\partial v_z}{\partial r} + v_\theta \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_r}{\partial r} + \frac{v_\theta v_z}{r} \frac{\partial v_r}{\partial \theta} \right) = \rho g z \frac{\partial p}{\partial z} + \mu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right]$$

$$\Rightarrow \frac{\mu}{\rho} \frac{\partial}{\partial r} \left( r \frac{\partial v_z}{\partial r} \right) = 0$$



$$\Rightarrow r \frac{\partial v_z}{\partial r} = C$$

$$\Rightarrow -\mu \frac{\partial v_z}{\partial r} = \frac{\mu C}{r}$$

$$\Rightarrow v_z = (C \ln r) + d$$

$$\text{At } r = r_1, v_z = u \quad \text{At } r = r_2, v_z = 0$$

$$\Rightarrow C \ln r_2 + d = u$$

$$C \ln r_1 + d = 0$$

$$\Rightarrow C \ln \left( \frac{r_2}{r_1} \right) = u$$

$$\Rightarrow C = \frac{u}{\ln \left( \frac{r_2}{r_1} \right)}$$

$$\gg v_2 = \frac{u(1/n)}{\ln(\pi_2/\pi_1)} \approx u$$

$$d = -ct\ln n_1$$

$$\Rightarrow v_2 = \frac{u}{\ln(\pi_2/\pi_1)} \left[ \ln \frac{\pi_1}{\pi_2} \right]$$

$$= \frac{u (\ln n_1 - \ln n_2)}{\ln(\pi_2/\pi_1)}$$

$$\boxed{z = \frac{1}{n} \partial(n v_2)}$$

$$At \quad n = \pi_1 \quad z = \frac{-\mu + \mu \left( \ln \pi_1 + 1 - \ln \pi_1 \right)}{\ln(\pi_2/\pi_1) \quad \frac{n}{n}}$$

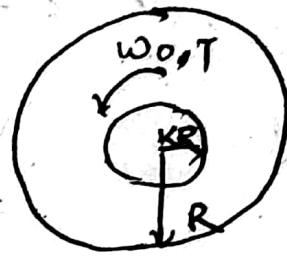
$$= \frac{-\mu + \mu}{\pi_1 (\ln(\pi_2/\pi_1))}$$

$$F = \frac{\mu}{\pi_1 \ln(\pi_2/\pi_1)} \times 2\pi \pi_1 \times L \times u$$

$$= \frac{2\pi \mu u L}{\ln(\pi_2/\pi_1)} = 10.66 \text{ N}$$

7. Two cylinders with inner one rotating by application of a known torque  $T$ .

Find expression of velocity in terms of  $T$ .



Hence,  $v_\theta$  is to be

considered as

velocity change occurs along  $\theta$ :

$$\rho \left( \frac{\partial v_\theta}{\partial t} + n \frac{\partial v_\theta}{\partial n} + \frac{v_\theta}{n} \frac{\partial v_\theta}{\partial \theta} - \frac{\partial v_\theta}{\partial n} \right)$$

$$\left( \rho \rho \omega - 1 + n \omega + v_\theta \frac{\partial v_\theta}{\partial \theta} \right) \rightarrow v_\theta \text{ changes with } \theta$$

$$= \rho g \omega - \frac{1}{n} \frac{\partial \rho}{\partial \theta} + \mu \left[ \frac{1}{n} \frac{\partial}{\partial n} \left( n \frac{\partial v_\theta}{\partial n} \right) \right]$$

~~$\frac{\partial \rho}{\partial \theta}$~~  || Doubt

$$\left( \frac{1}{n^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{1}{n^2} \frac{\partial^2 v_\theta}{\partial \theta \partial n} + \frac{2 v_\theta}{n^2} \frac{\partial^2 v_\theta}{\partial n^2} \right)$$

~~$\frac{\partial^2 v_\theta}{\partial n^2}$~~

$$+ \left( \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{\partial^2 v_\theta}{\partial \theta \partial n} \right)$$

$\omega = \sqrt{\frac{T}{I}}$

$$\Rightarrow \mu \frac{\partial v_\theta}{\partial n} = \frac{1}{n} \frac{\partial^2 v_\theta}{\partial \theta^2}$$

$$\mu \frac{\partial}{\partial n} \left( \frac{1}{n} \left( \frac{\partial}{\partial n} n V_0 \right) \right) = 0$$

$$\Rightarrow \frac{\partial}{\partial n} (n V_0) = C_n$$

$$\Rightarrow n V_0 = \frac{C_n^2}{2} + d$$

$$\Rightarrow V_0 = \frac{C_n}{2} + \frac{d}{n}$$

B.C

$$\text{At } H = KR, \quad N_0 = (\omega_0 \times KR)$$

$$\Rightarrow (\omega_0 \times KR = \frac{C \times KR}{2} + \frac{d}{KR})$$

$$\Rightarrow \omega_0 \times KR = \left( \frac{C \times KR}{2} - \frac{C R}{2K} \right)$$

$$n = R; \quad V_0 = 0$$

$$\Rightarrow \frac{C \times R}{2} + \frac{d}{R} = 0$$

$$\Rightarrow d = -\frac{C R^2}{2}$$

$$\begin{aligned} C &= \frac{\omega_0 \times KR}{\left( \frac{K}{2} - \frac{1}{2K} \right)} \\ &= \frac{2 \omega_0 R}{\left( 1 - \frac{1}{K^2} \right)} \end{aligned}$$

$$N_0 = \frac{\omega_0 R}{\left( 1 - \frac{1}{K^2} \right)} \cdot n - \frac{\omega_0 R^3}{\left( 1 - \frac{1}{K^2} \right) \cdot n}$$

$$= \frac{\omega_0 R^2}{\left( 1 - \frac{1}{K^2} \right)} \left[ n \frac{1}{R} - \frac{R}{n} \right]$$

$$\tau_{n0} = -\mu \left[ n \frac{\partial}{\partial n} \left( \frac{V_0}{n} \right) \right]$$

$$= \left( \frac{\omega_0 R}{1 - \frac{1}{K^2}} \right) - \mu \left[ n \times \frac{\partial}{\partial n} \left( \frac{1}{n} - \frac{R}{n^2} \right) \right]$$

$$= -\frac{\mu \times \omega_0 R}{1 - \frac{1}{K^2}} \times \frac{-2R}{n^2} = \frac{2\mu \omega_0 R^2}{\left( 1 - \frac{1}{K^2} \right) n^2}$$

$$\frac{\mu w_0^2 R^2}{(1-\gamma_{k^2}) n^2}$$

$$T = \text{Torque} = F \times d$$

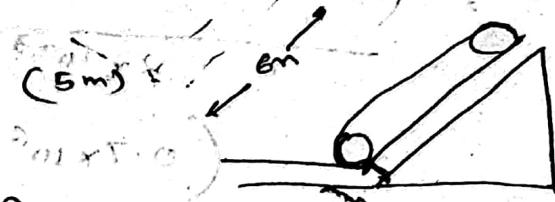
$$= [C_{\pi \theta} \times (2\pi K R) \times L] \times 2 \pi K R$$

$$(2 \pi K R) = \frac{\mu w_0}{(1-\gamma_{k^2})} \times \frac{4 \pi K^2 K^2 R^2 L}{n^2}$$

$$= \frac{\mu w_0}{(1-\gamma_{k^2})} \times \frac{4 \pi K^2 R^2 L}{(K R)^2}$$

$$= \frac{\mu w_0 \times 4 \pi R^2 L}{(1-\gamma_{k^2})}$$

$$P \left( \frac{\partial v_x}{\partial t} + v_n \frac{\partial v_z}{\partial t} + v_y \frac{\partial v_z}{\partial t} + v_z \frac{\partial v_z}{\partial t} \right)$$



$$= - \frac{dp}{dz} + \rho g_z + \mu \left( \frac{\partial^2 v_z}{\partial n^2} \right)$$

$$\Rightarrow \mu \left( \frac{\partial^2 v_z}{\partial n^2} \right) = \left( \frac{dp}{dz} - \rho g_z \right)$$

$$\Rightarrow \mu \frac{\partial^2 v_z}{\partial n^2} = (c - \rho g_z)$$

$$\Rightarrow \mu \left( \frac{\partial v_z}{\partial n} \right) = \left( c - \frac{\rho g}{2} \right) n + d$$

$$\Rightarrow \mu v_z = \left( c - \frac{\rho g}{2} \right) \frac{n^2}{2} + dn + c$$

$$\text{At } n = 0,$$

$$v_z = 0$$

$$\Rightarrow v_z = \frac{1}{\mu} \left[ \left( c - \frac{\rho g}{2} \right) \frac{n^2}{2} + dn \right]$$

$$\text{At } v = u, n = 2 \text{ mm}$$

$$\Rightarrow v_z = - \frac{\rho g}{4\mu} n^2 + cn$$

$$\text{At } n = 2 \text{ mm}, v_z = 3 \text{ m/s}$$

$$\Rightarrow 3 + \frac{19}{2\mu} n^2 = c_1 n$$

$$\Rightarrow c_1 = (\text{cancel})$$

$$V = \frac{\rho g n^2}{2\mu} - 436 \text{ m} - \frac{\rho n}{2\mu} = 2.1 \times 10^7$$

$$\therefore V_z = \frac{\rho g \cos \beta}{2\mu} + c n$$

$$\Rightarrow c = \frac{V_z - \frac{\rho g \cos \beta}{2\mu}}{n}$$

$$= \cancel{(1.21 \times 10^3)} / 1080$$

$$\begin{aligned} 1 \text{ poise} &= 1 N \\ 1 \text{ po} &= 10^{-1} \\ \mu &= 10^{-2} \\ &= 10^{-1} \\ (2.1 \times 10^7) & \end{aligned}$$

$$\left( \frac{2.1 \times 10^7 n^3}{3} + \cancel{\frac{c n^2}{2}} \right) \xrightarrow[2 \times 10^{-3}]{140} \left( \frac{2.1 \times 10^3 n}{3} + \frac{c}{2} \right) n$$

$$V_z = \frac{\rho g \cos \beta}{2\mu} + c n$$

$$\langle V_z \rangle = \left( \frac{2.1 \times 10^3 n}{2} + \frac{c}{2} \right) n$$

$$\Rightarrow c = \left( \frac{V_z - \rho g \cos \beta}{2\mu} \right) \frac{1}{n} = 1.36$$

$$Q = 1.36 \times 10 \times 10^3$$

$$\Rightarrow c = 1080$$

$$= 0.0136$$