



PID auto-tuning

UNICOS

MOC3002, Feedback systems & Tuning

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on behalf of the UNICOS team



Outline

1. Introduction
2. CERN installations (UNICOS)
3. PID auto-tuning: Solution and methods
4. Experimental results
5. Conclusions



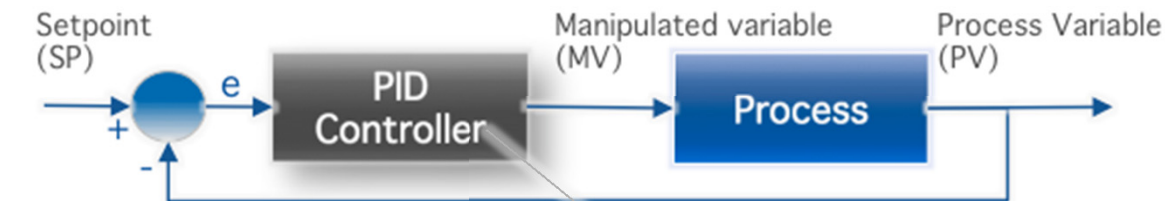
Introduction

- The **PID** feedback control algorithm dates back to early nineteens'
- The **right tuning** of those controllers is essential to increase plant availability and maximize profits in many processes
- Operators and control engineers spend a considerable **time** in tuning those controllers
- **GOAL:** (1) Provide automatic methods to tune the PID controllers and (2) make them usable by plant operators



PID control basics

- Basics



SISO control loop schema

$$K_c \cdot \left(e(t) + \frac{1}{T_i} \cdot \int e(t) dt + T_d \cdot \frac{d}{dt} e(t) \right)$$

Parameters: K_c , T_i , T_d

- PID are usually tuned by **operators** (or control engineers).
- The majority of the controllers in industry are **PIs**



CERN installations

- **Industrial facilities** for the accelerator complex and the associated experiments
- Continuous process control: temperature, pressure, levels...
- Large and/or **complex** dynamics



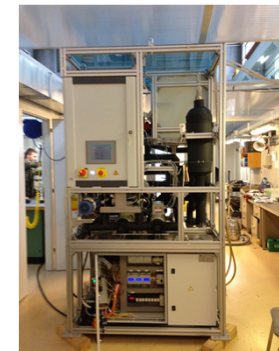
LHC 4.5 K Cryogenics refrigerators



TPC gas system



LHC cooling towers



CO2 Cooling (MARCO)



CERN installations



Enormous **number** of PID based controllers: > **8000**

- LHC cryogenic control system: ~ **5000** PID controllers
- Cooling and Ventilation: ~ **870** PID controllers

PIDs tuned extremely **conservative** or initial parameters untouched

- Fine tuning systematically avoided

Implementation:

- **PLCs** (Programmable Logic Controller): > 400
- **UNICOS** (Unified Industrial Control System) framework.

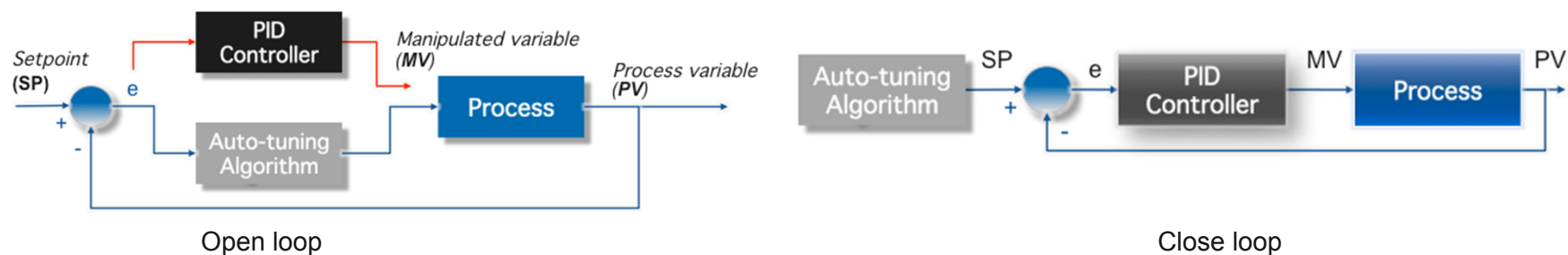


PID auto-tuning

Create a tool to **automatically find the PID parameters** and tune the control loops always **initiated deliberately** by operators and/or control engineers.

Classification (one) on how the data is extracted from the plant

- **Open loop:** e.g. turn off PID and excite the process by changing the MV
- **Close loop:** e.g. tune online while the PID is working (SP is changed)



PID auto-tuning

Tuning methods

- Trial & Error
- Experimental based
- Model based analytical
- Automatic tuning: **Auto-tuning** methods
 - Relay Method
 - SIMC (*Skogestad* Internal Model Control)
 - IFC (Iterative Feedback Tuning)

The choice is not straight forward and depends mostly on the **process knowledge**



PID auto-tuning: [1] Relay

Astrom and Hagglund (1995)

The process is brought to oscillation by replacing the PID controller with a relay function. The ultimate Gain (K_{cu}) and the ultimate period (T_u) are determined

User parameters

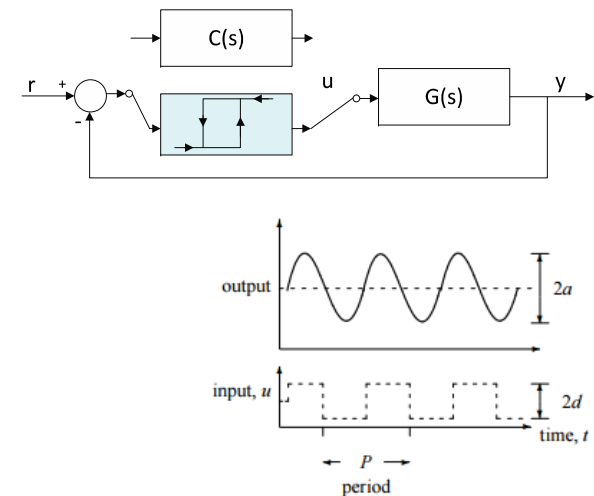
- Maximal deviation of the control effort: MV
- Number of cycles to detect the ultimate condition

Advantages

- Single action (vs. trial and error)
- Little a priori knowledge of the process

Disadvantages

- Preferably to execute it under stable conditions
- Process must be controllable with a P-controller.



	K_c	T_i	T_d
P	$0.5 K_u$		
PI	$0.4 K_u$	$0.8 T_u$	
PID	$0.6 K_u$	$0.5 T_u$	$0.125 T_u$



PID auto-tuning:[2] SIMC

Method based on an internal model (*Skogestad IMC*)

- Two phases: Process identification (first or second order) and application of tuning rules

Parameterization

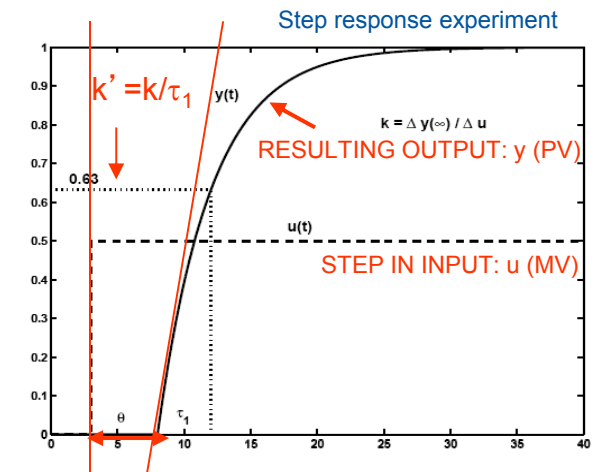
- **Desired performance:** *Tight* vs. *smooth* control

Advantages

- Simplicity of parameterization

Disadvantages

- Applicable to processes without complex dynamics
- Stable processes: open loop test



$$K_c = \frac{1}{k'} \cdot \frac{1}{(\theta + \tau_c)}$$
$$\tau_I = \min(\tau_1, 4(\tau_c + \theta))$$

$k' = k/\tau_1$ = initial slope step response

$\tau_c \geq 0$: desired closed-loop response time (**tuning parameter**)

For robustness select : τ_c, θ (gives $K_c \leq K_{c,max}$)

For disturbance rejection select : $K_c \geq K_{c,min} = u_{d0}/y_{max}$



PID auto-tuning: [3] IFT

Iterative Feedback Tuning (IFT): inspired in the iterative parametric optimization approach. Makes random perturbations on the SP. Minimize the current value of the measured value and a desired first order response.

Parameterization

- Just safeguards (thresholds)
- Desired 1st order response shape

Advantages

- close loop method with minimal disturbances
- model free

Disadvantages

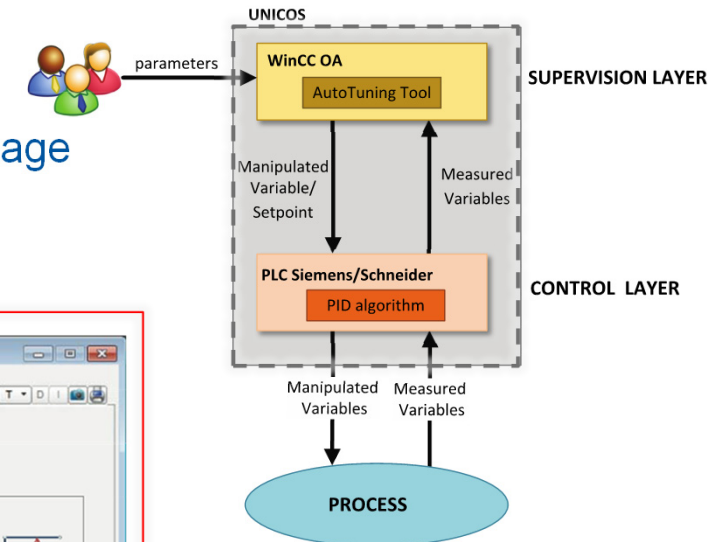
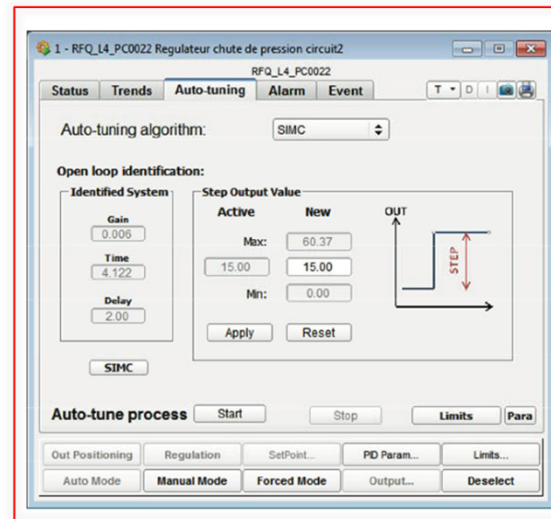
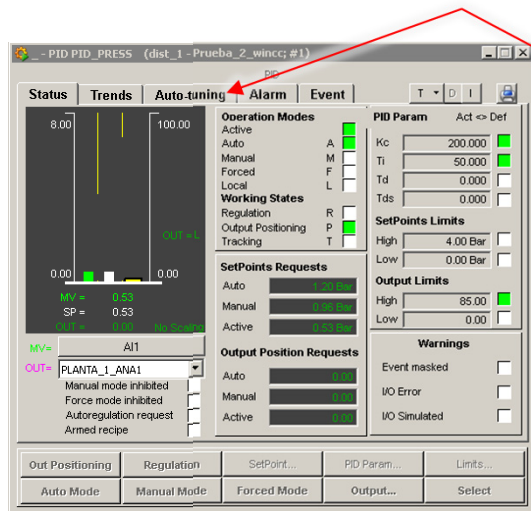
- A local minima could be found

$$J(\rho) = \frac{1}{2N} \left[a \sum_{t=1}^N (L_y \cdot \tilde{y}_t(\rho))^2 + l \sum_{t=1}^N (L_u \cdot u_t(\rho))^2 \right]$$
$$\rho^* = \underset{\rho}{\operatorname{argmin}} J(\rho)$$
$$\tilde{y}_t = y_t - y_d$$



UNICOS Implementation

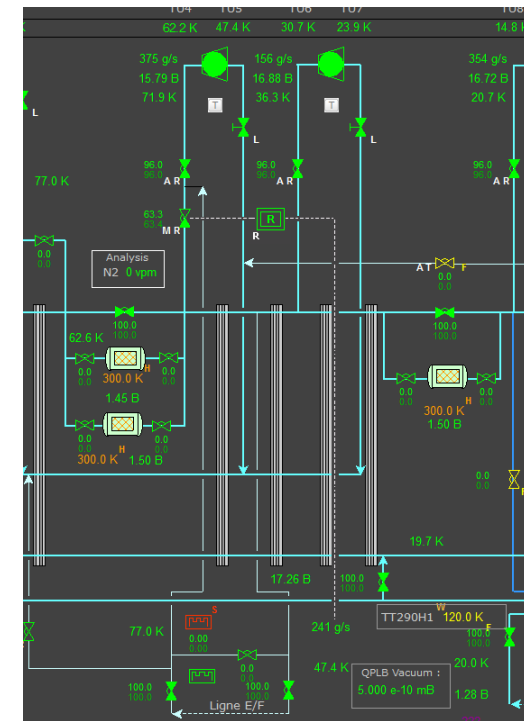
- Algorithms in the **WinCC OA** SCADA: Scripting language
- The **PLC** maintains the PID algorithm untouched
- HMI inside the PID controller faceplate



Experimental results (Ghe Flow control)

Use case: **Cryogenics flow control**: PI control
[Simulation]

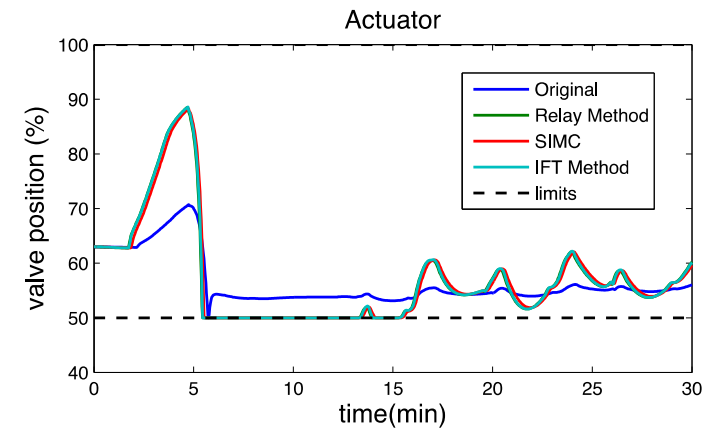
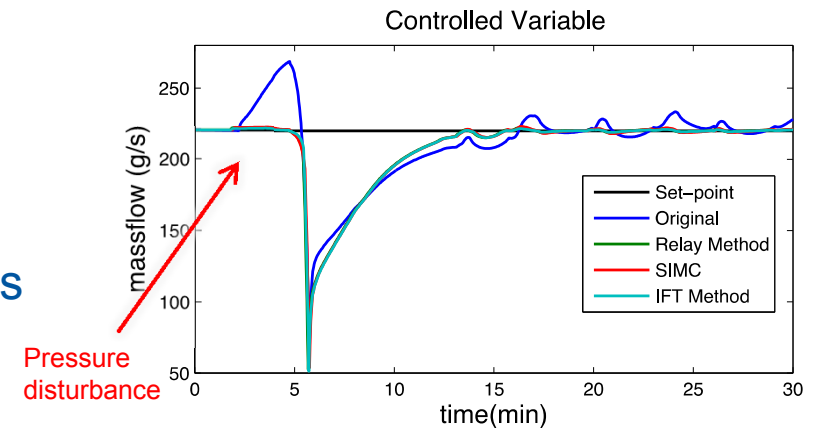
Gas helium circulating to maintain the thermal shielding of the LHC superconducting magnets at 80 K.



GHe Flow control

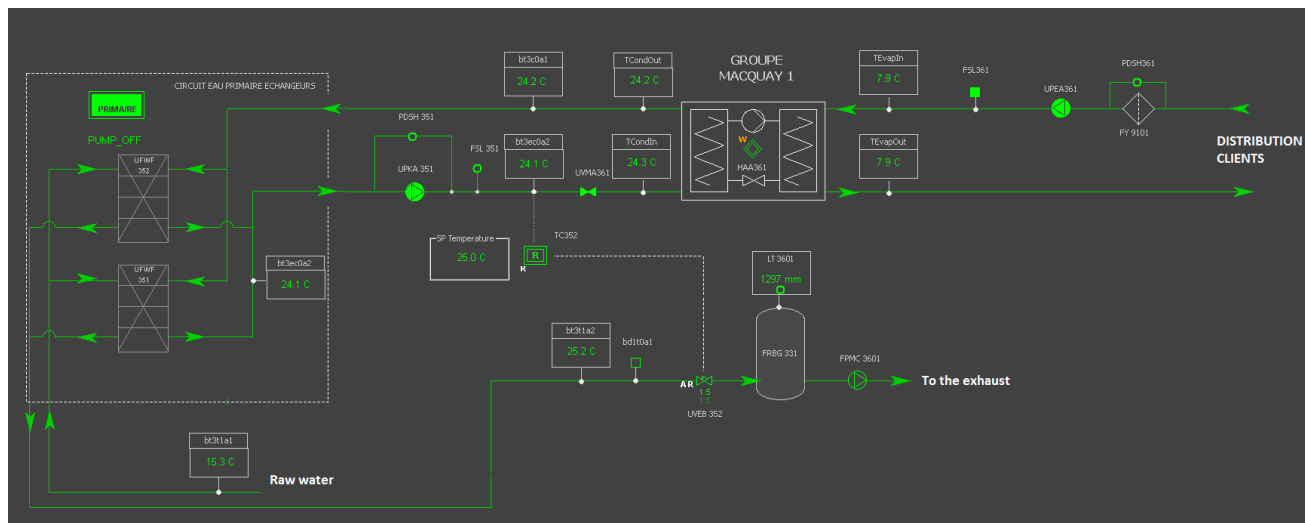
- Found too sluggish with oscillations and overshoots when disturb by pressure changes
- Three auto-tuning methods tested:
Relay, SIMC, IFT

Tuning	K_c	T_i	Overshoot	Oscillation
Original	1	200	22 %	6 %
Relay	9	12	0.5 %	1 %
SIMC	4.5	7	1 %	1.3 %
IFT	13	11	0.5 %	0.5 %



Experimental results (HVAC process)

- Use case: chilled water production unit providing water at 5° C for LHC
- Maintain at 25° C the condenser output temperature of a chiller
- PI controller: desired temperature deviation within 1° C

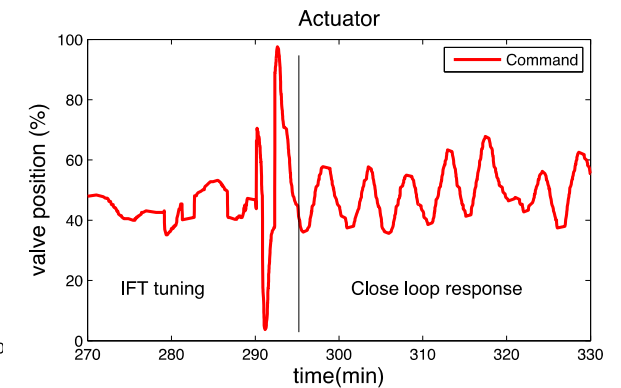
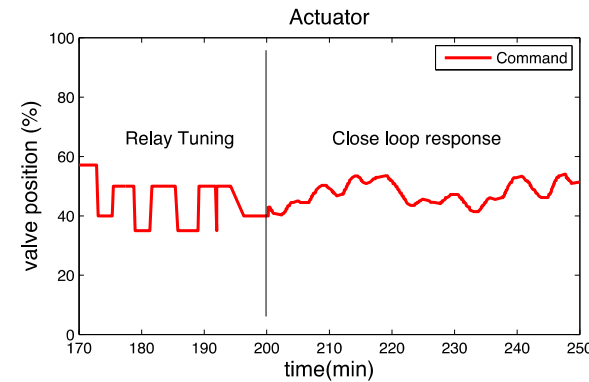
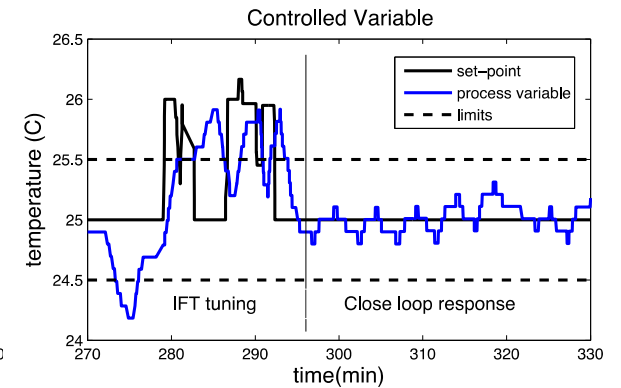
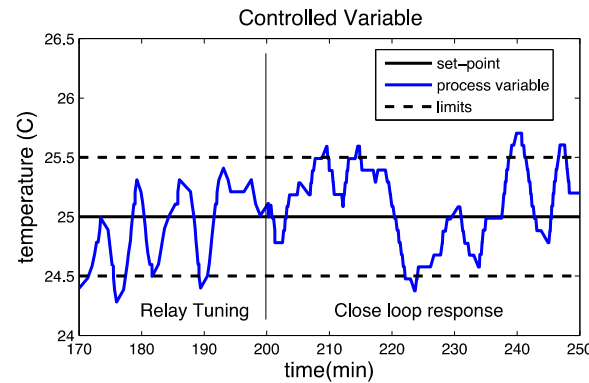


HVAC control

Operation team reported instabilities on a regulation loop action on a control valve

Results: Relay vs. IFT

Tuning	K_c	T_i	$ \Delta y $	$ \Delta u $
Original	8	0.5	2 °C	100 %
Relay	8.3	311	1.3 °C	10 %
IFT	50.9	5666	0.5 °C	20 %



Conclusions

- PID auto-tuning is not a dream. **Feasible** to implement
- Fully-**integrated** implementation: UNICOS
- **Flexible** solution: Open to new methods
- Improvement of plant availability and **engineering time**
- **Operator acceptance**



Acknowledgements

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UVA, Valladolid (Spain)





www.cern.ch

Unified
Industrial Control
System

UNICOS

UNICOS (UNified Industrial Control System) is a CERN-made framework to develop industrial control applications
<http://www.cern.ch/unicos>



Enrique Blanco: automation engineer, PhD in systems and process engineering. Head of the process control section (industrial controls group) in the engineering dpt. at CERN

Native integration advantages

Easy **integration**

- Avoid data extraction & third party tools (off line analysis)
- External connections
- Customized to our environment (event driven data, Customized scaling)

Ease **operation**

- Same philosophy & look and feel
- Ease parameterization
- Fully control and safe operation (boundaries)

Flexible and evolutive

- Easy integration of new algorithms

