

1<sup>st</sup> Order, Linear  $\rightarrow C_A = k_p DC_{A0}(1 - e^{-t/\tau})$

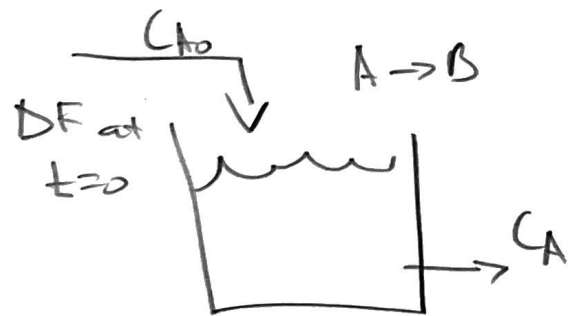
● 2<sup>nd</sup> Order Linear  $\rightarrow C_A = k_p DC_{A0}(1 - e^{-t/\tau}) - k_p DC_{A0} \frac{t}{\tau} e^{-t/\tau}$

3<sup>rd</sup>, 4<sup>th</sup>, 5<sup>th</sup> order  $+ t^2 e^{-t/\tau}, t^3 e^{-t/\tau} \dots$

Non linear  $\rightarrow$  in many cases, can linearize to a 1<sup>st</sup> order linear. (e.g. non linear rate).

- What if we have multiple disturbances?
- What if we cannot easily solve using integrating factor method?
- Is there a better way to solve and analyze dynamic systems? (yes!)

Reactor with disturbance in  $F$



Balance:

$$V \frac{dC_A}{dt} = FC_{A0} - \underbrace{FC_A}_{\text{non-linear}} - VK_1 C_A$$

Deviation Variables  $\rightarrow$  need to linearize

$$V \frac{dC_A'}{dt} = C_A0' - C_A' - VK_1 C_A'$$

FCA is non-linear. Need to linearize.

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$$f(F, C_A) \approx f(F_S, C_{A_S}) + \left. \frac{\partial f}{\partial F} \right|_{F_S, C_S} (F - F_S) + \left. \frac{\partial f}{\partial C_A} \right|_{F_S, C_S} (C_A - C_{A_S})$$

$$F C_A \approx F_S C_{A_S} + C_{A_S} (F - F_S) + F_S (C_A - C_{A_S})$$

Plug into balance:

$$V \frac{dC_A}{dt} = F C_{A_0} - F_S C_{A_S} - C_{A_S} (F - F_S) - F_S (C_A - C_{A_S}) - V k_1 C_A$$

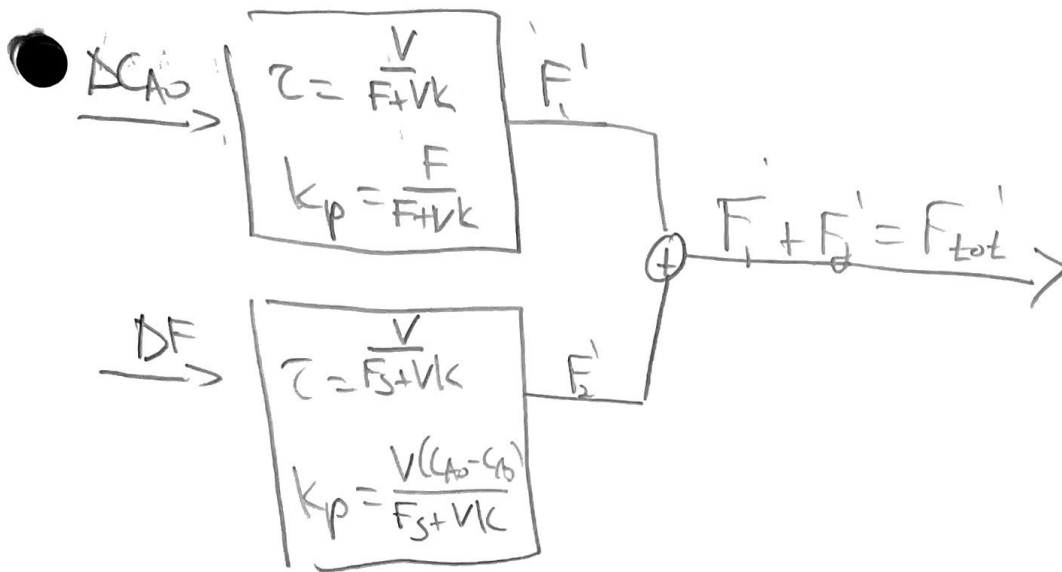
Write in terms of deviation variables  $\Delta F, C_A'$

$$V \frac{dC_A'}{dt} = \Delta F C_{A_0} - C_{A_S} \Delta F - F_S C_A' - V k_1 C_A'$$

$$\frac{dC_A'}{dt} + \underbrace{\frac{F_S + V k_1}{V}}_{1/\tau} C_A' = \underbrace{\frac{1}{V} (C_{A_0} - C_{A_S})}_{K_P / \tau} \Delta F$$

$$C_A' = K_P \Delta F (1 - e^{-t/\tau}), \quad \tau = \frac{V}{F_S + V k_1}, \quad K_P = \frac{C_{A_0} - C_{A_S}}{F_S + V k_1}$$

What if there are changes in both  $DC_{AO}$  and  $DF$ ? 24



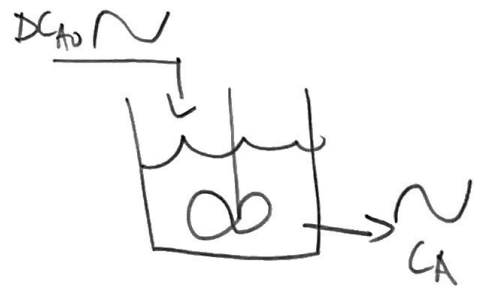
Add together deviations due to different disturbances

### Problem 3.5:

What if  $DC_{AO}$  is not a step function.  $DC_{AO} = A \sin(\omega t)$ .

Mitigating tank:

$$V \frac{dC_A}{dt} = F(C_{AO} - C_A)$$



$$\frac{dC_A'}{dt} + \frac{1}{\tau} C_A' = \frac{1}{\tau} DC_{AO} = \frac{1}{\tau} A \sin(\omega t)$$

Solve as before.

$$\frac{d}{dt} (e^{\pm t/\tau} C_A') = \frac{1}{\tau} A \sin(\omega t) e^{\pm t/\tau}$$

$$e^{\pm t/\tau} (C_A' - \frac{A}{\tau}) e^{\pm t/\tau} \sin(\omega t) dt + I$$

$$e^{t/\tau} C_A' = \frac{A}{\tau} \left[ \frac{\frac{1}{\tau} \sin \omega t - \omega \cos \omega t}{1/\tau^2 + \omega^2} \right] e^{t/\tau} + I$$

$$C_A' = \frac{A}{\tau} \left[ \frac{\tau \sin \omega t - \omega \tau^2 \cos \omega t}{1 + \omega^2 \tau^2} \right] + I e^{-t/\tau}$$

Set  $C_A' = 0$  at  $t=0$  gives  $I = \frac{A \omega \tau}{1 + \omega^2 \tau^2}$

$$C_A' = \frac{A}{1 + \omega^2 \tau^2} (\sin \omega t - \omega \tau \cos \omega t) + \frac{A \omega \tau}{1 + \omega^2 \tau^2} e^{-t/\tau}$$

Another example.

$$AR = \frac{1}{\sqrt{1 + \omega^2 \tau^2}}$$

$$\frac{dC_A}{dt} + \left( \frac{1}{\tau} + k \right) C_A = \frac{1}{\tau} C_{A0}$$

$\uparrow$   
 Not a constant

use integrating factor  $\exp\left(\int \left(\frac{1}{\tau} + k\right) dt\right) = e^{t/\tau + kt}$

$$= t e^{t/\tau + kt}$$

$$\frac{d}{dt} (C_A t e^{t/\tau + kt}) = \frac{t e^{t/\tau + kt}}{t} C_{A0}$$

## Numerical Solutions

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In some cases, it is not easy to linearize an equation, or perhaps you want a plot of the non-linear result. It is easy to calculate a numerical solution.

- 1) Derive the conservation equation

$$V \frac{dC_A}{dt} = F(C_{A0} - C_A) - VKC_A$$

- 2) Find the initial steady state value

$$\text{Set } \frac{dC_A}{dt} = 0, \quad C_{A0} = C_{A0, \text{init}}$$

$$0 = F(C_{A0, \text{init}} - C_A) - VKC_A$$

$$C_A = \underbrace{\frac{F}{F+VK}}_{K_p} C_{A0, \text{init}}$$

- 3) Define a time step,  $t = 0.001 \text{ s}$

- 4) Calculate  $\frac{dC_A}{dt}$  at  $t=0$

$$\frac{dC_A}{dt} = \frac{F}{V} (C_{A0} - C_A(t=0)) - VKC_A(t=0)$$

- 5) Find  $\Delta C_A$

$$\Delta C_A = \left. \frac{dC_A}{dt} \right|_{t=0} \cdot \Delta t$$

- 6) This gives  $C_A(t=0.001)$  Repeat Process