Gnielinski_TF_Tube()
HEDH 2.5.1 (41)
管内，湍流, 完全发展
Inside tube, Turbulent flow, Fully developed.

$$Nu_t = \frac{(f/8)\,(Re_t - 1000)\,Pr_t}{1 + 1.27} \tag{1}$$

恒壁温及恒热流对传热系数没有影响。此方程的使用独立于热边界条件。

"No remarkable differences were found measuring heat transfer coefficients with the two boundary conditions of uniform wall temperature or constant wall heat flux."