



Ethylene/Ethane Separation in Metal-Organic Frameworks by Computational Modeling

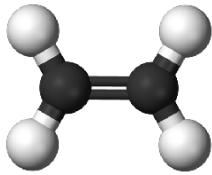
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10/31/2019

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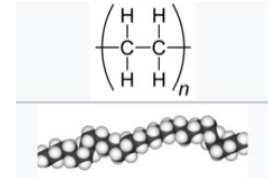
Chapter 1: Motivation for C₂H₄/C₂H₆ Separation



C₂H₄
>150 million tonnes in 2016
 (Raw material)



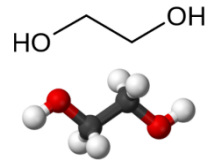
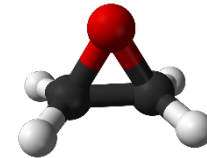
Polyethylene:
plastic



Plant hormone:
ripen fruits



Ethylene oxide:
Ethylene glycol



Stream Cracking

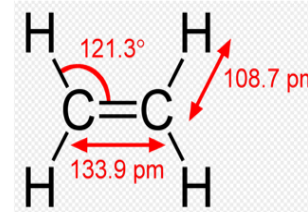


OCM

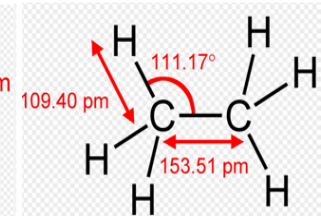
C₂ products



Ethylene: C₂H₄



Ethane: C₂H₆



Kinetic diameter

4.163 Å

4.443 Å

Boiling point

-103 °C

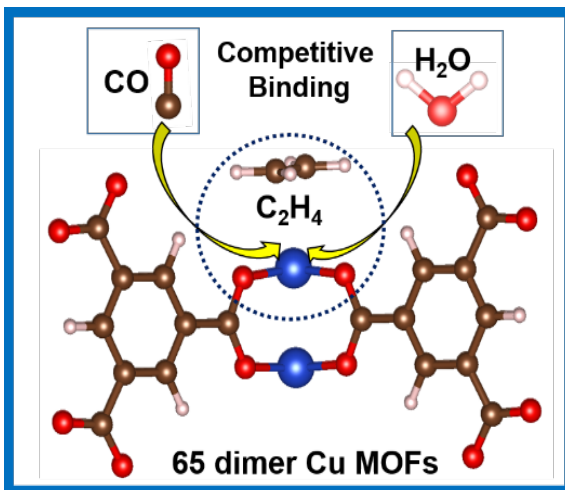
-89 °C

A key step in producing ethylene is the separation of ethylene from ethane

MOFs with OMS: Adsorption-based C₂H₄/ C₂H₆ Separation

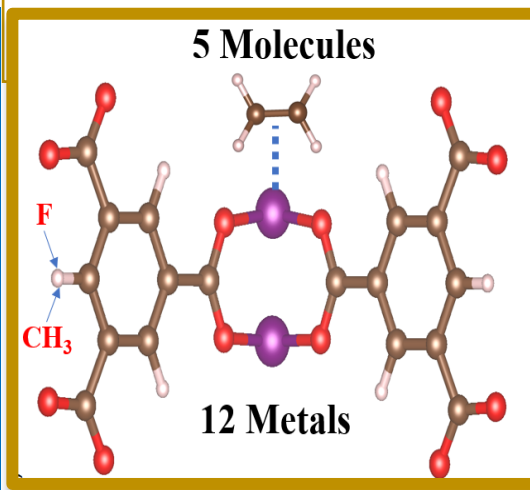
Chapter 2 (Published)

Competitive binding of H₂O, CO, and C₂H₄ in 65 dimer Cu MOFs^[1]



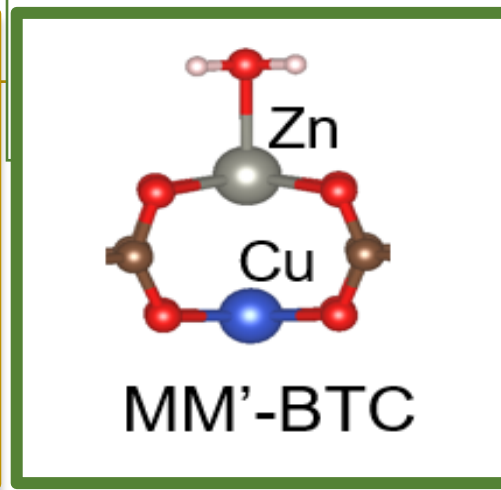
Chapter 3 (Published)

Tune the binding tendencies by metal substitution and linker functionalization^[2]



Chapter 4 (Done)

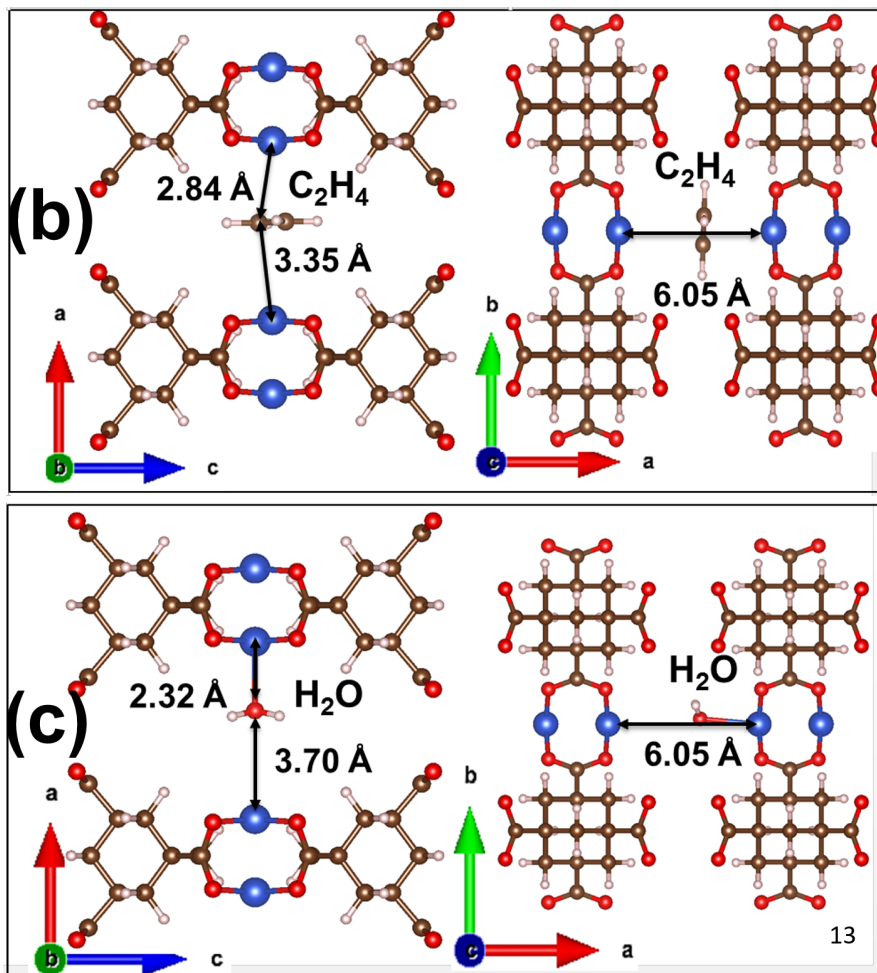
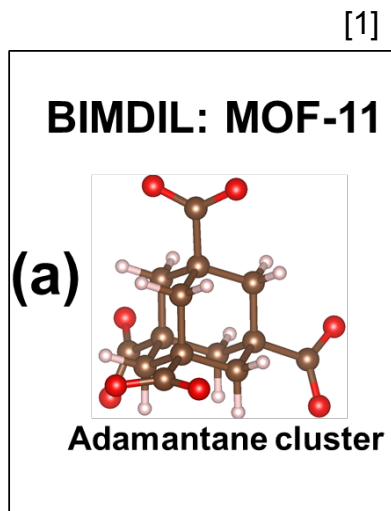
Performance of the mixed-metal MOFs



[1] You, W.; Liu, Y.; Howe, J. D.; Sholl, D. S., *J. Phys. Chem. C* **2018**, 122 (16), 8960-8966.

[2] You, W.; Liu, Y.; Dai T.; Howe, J. D.; Sholl, D. S., *J. Phys. Chem. C* **2018**, 122(48), 27486-27494

Chapter 2: Two Top Ethylene-Selective MOFs



Notable dual site binding

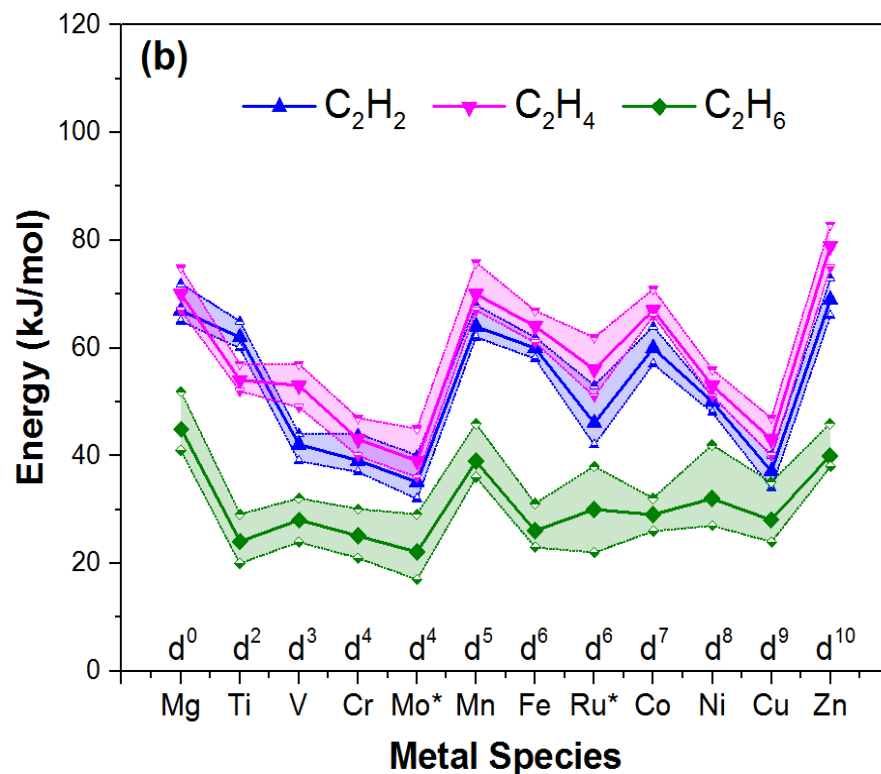
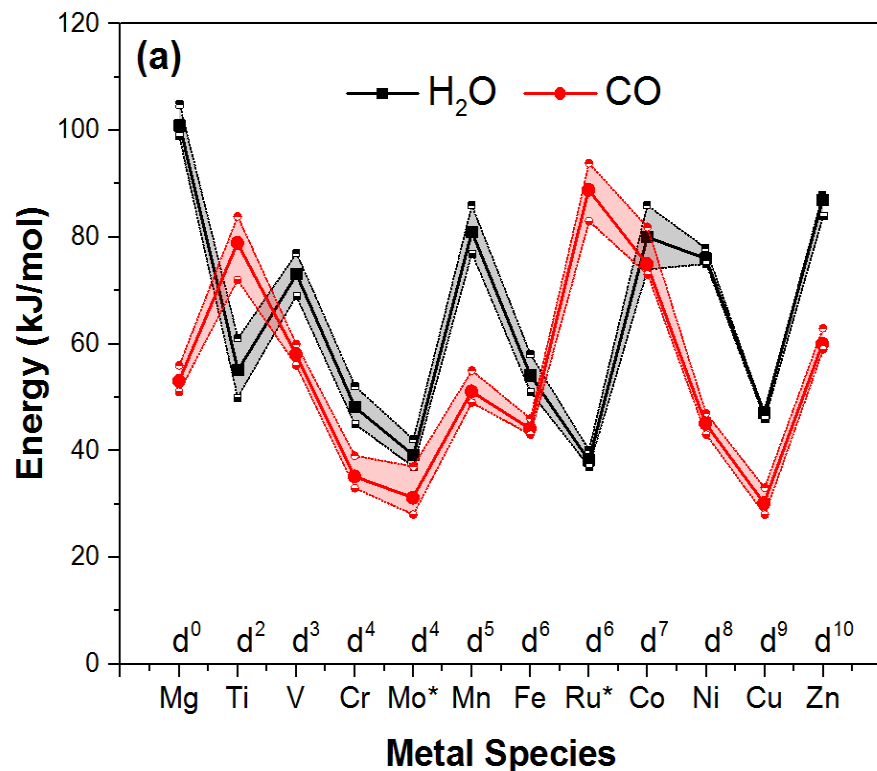
Negligible dual site binding

Finding 4: Suggests a possible avenue for developing other MOFs in which the $BE_{C_2H_4}$ is higher than the BE_{H_2O}

[1] Chen, Banglin, et al. *Journal of the American Chemical Society* 122.46 (2000): 11559-11560.

[2] You, W.; Liu, Y.; Howe, J. D.; Sholl, D. S., *J. Phys. Chem. C* **2018**, 122 (16), 8960-8966.

Chapter 3: Metal-Substitution on Isostructural MOFs



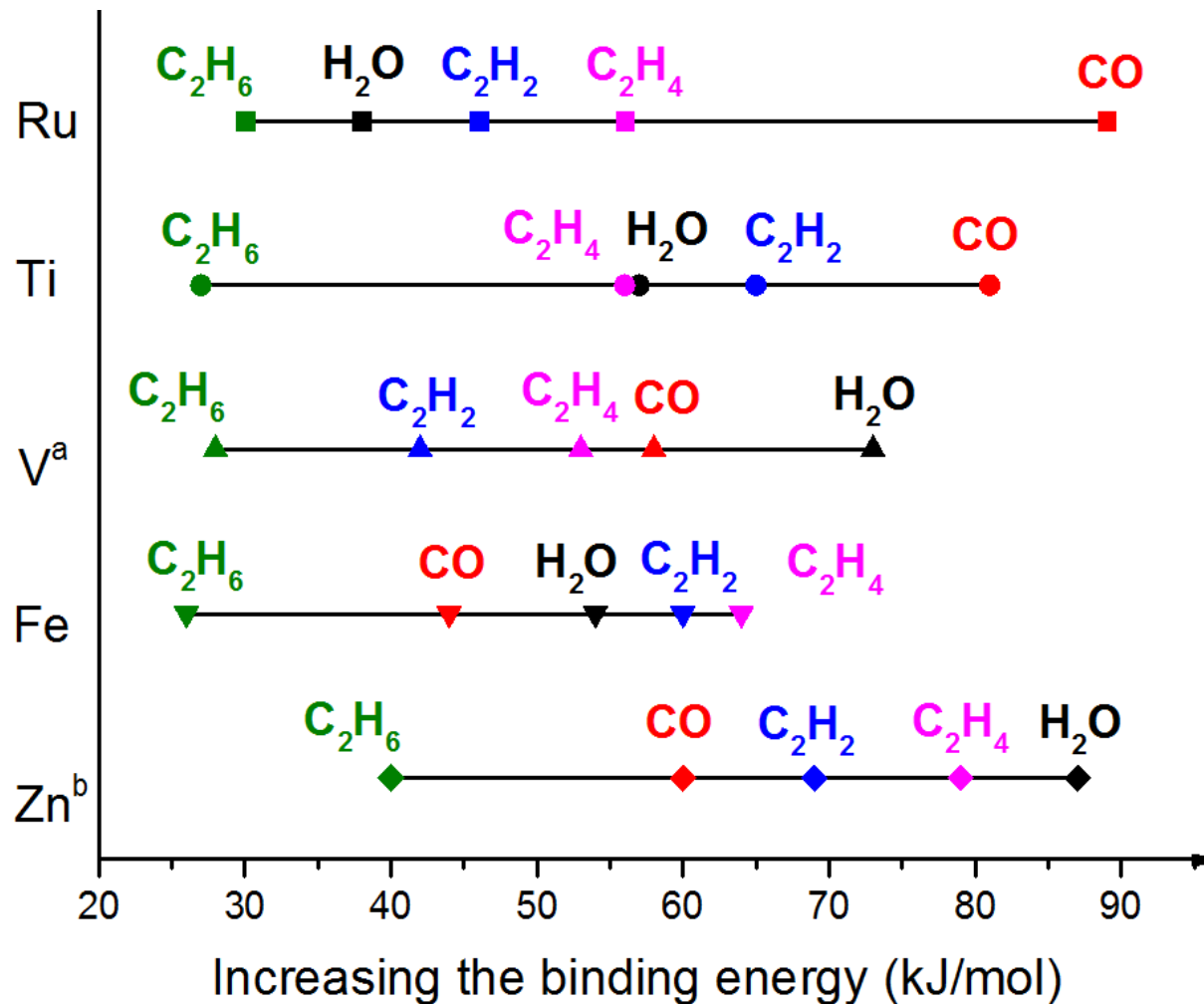
- Each data point shows average of 5 MOFs.
- The energy variation due to metals is stronger than the identity of linker
- C₂H₆ has the lowest binding affinity in all cases.

Chapter 3: Relative Binding Energies in 12-metal MOFs

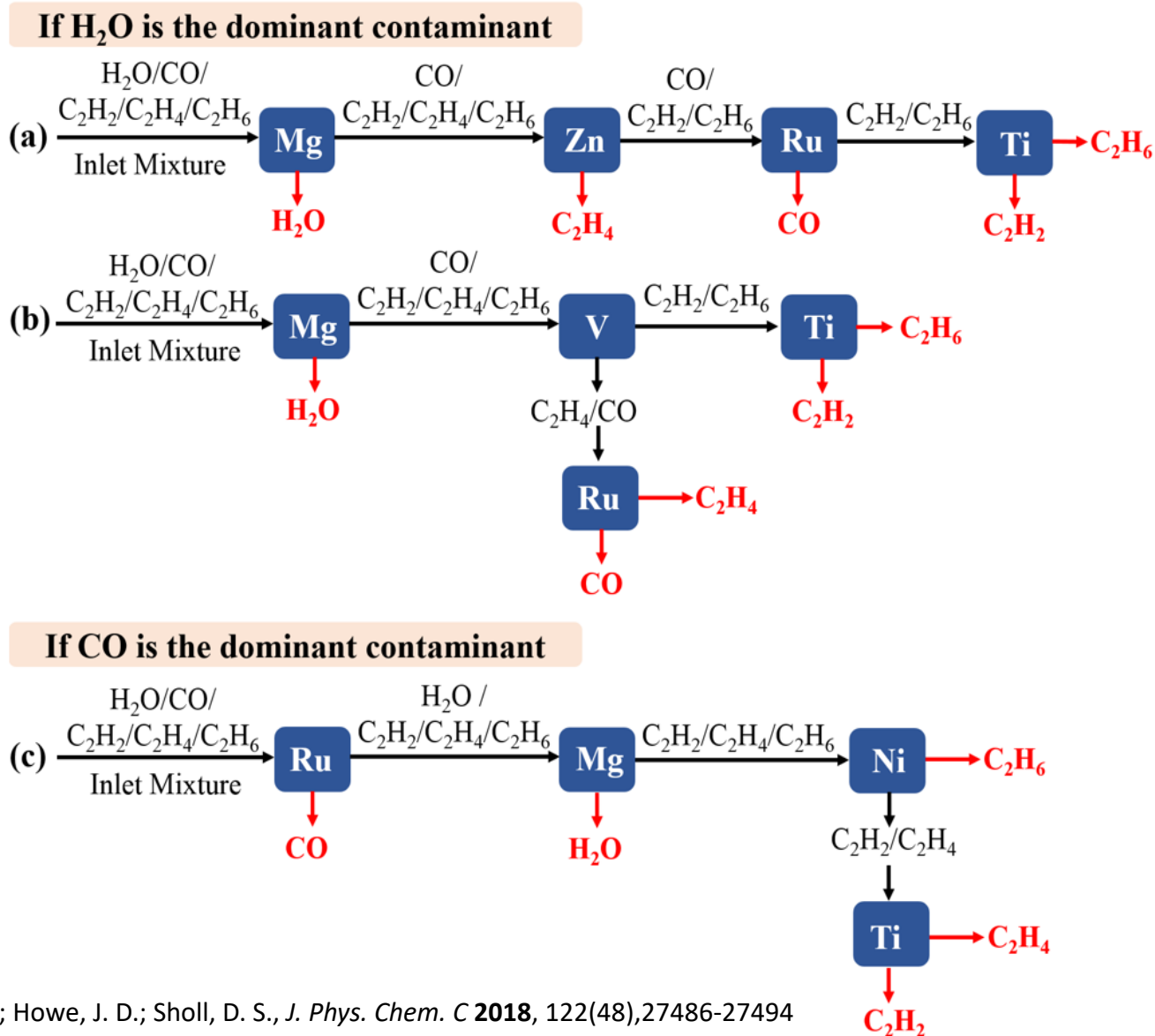
		60	20				5	-5	-20	-60				
		Strong				Weak	No	Weak	Strong Separation					
Separation Pairs	H ₂ O-C ₂ H ₆	34	56	31	45	23	17	42	28	8	51	44	19	47
	C ₂ H ₄ -C ₂ H ₆	27	25	30	24	18	17	31	37	26	38	21	15	39
	CO-C ₂ H ₆	24	8	55	30	10	9	12	18	59	46	13	2	20
	C ₂ H ₂ -C ₂ H ₆	22	22	38	14	14	13	25	34	16	31	18	9	29
	H ₂ O-C ₂ H ₂	12	34	-7	31	9	4	17	-6	-8	20	26	10	18
	H ₂ O-CO	11	48	-24	15	13	8	30	10	-51	5	31	17	27
	H ₂ O-C ₂ H ₄	7	31	1	20	5	0	11	-10	-18	13	23	4	8
	C ₂ H ₄ -C ₂ H ₂	5	3	-8	11	4	4	6	4	10	7	3	6	10
	C ₂ H ₄ -CO	3	17	-25	-5	8	8	19	20	-33	-8	8	13	19
C ₂ H ₂ -CO	-2	14	-17	-16	4	4	13	16	-43	-15	5	7	9	
Avg.			Mg	Ti	V	Cr	Mo	Mn	Fe	Ru	Co	Ni	Cu	Zn
Metal Species														

Chapter 3: Five Types of Binding Tendencies

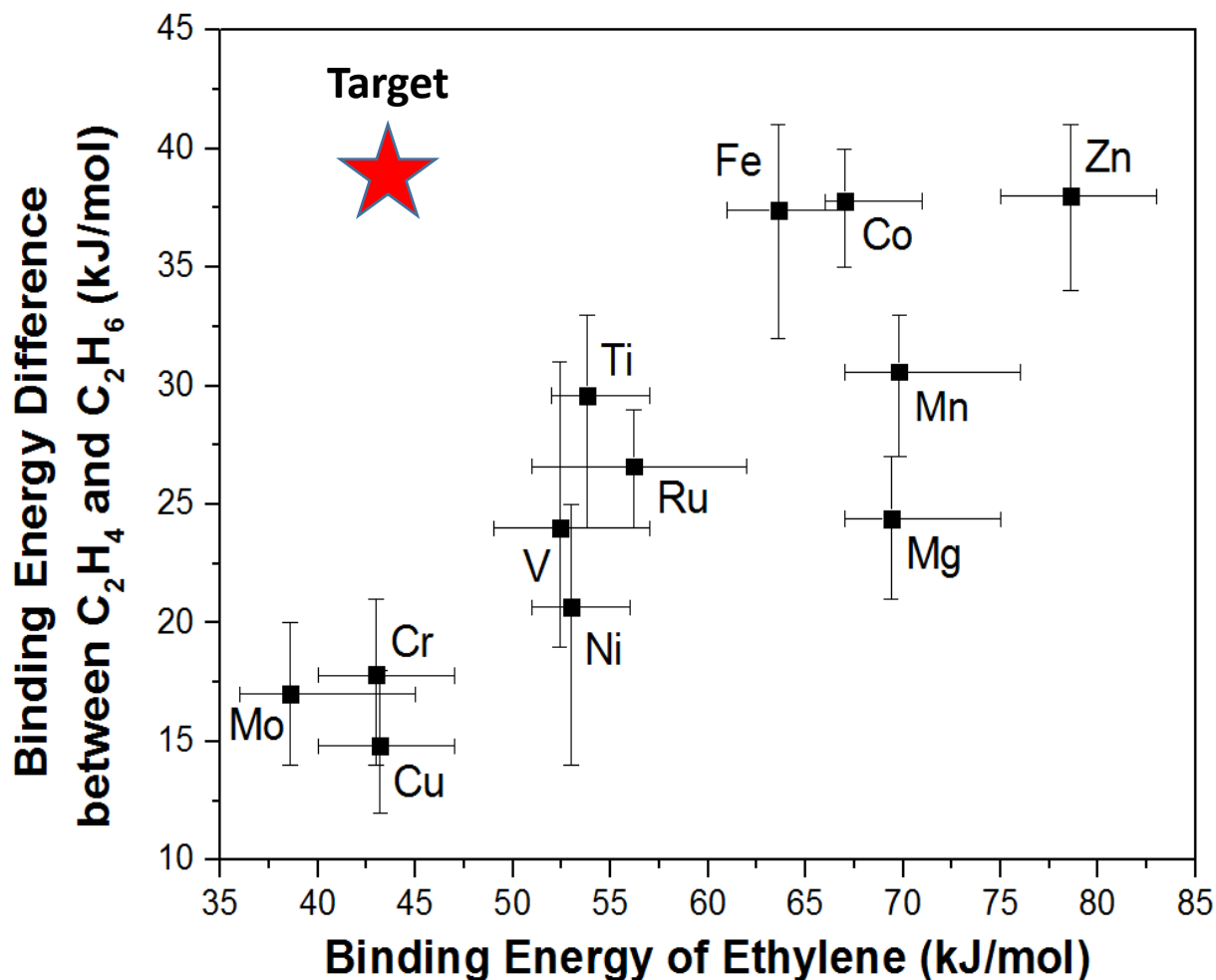
		60		20		5		-5		-20		-60			
		Strong				Weak		No		Weak		Strong Separation			
Separation Pairs		H ₂ O-C ₂ H ₆	34	56	31	45	23	17	42	28	8	51	44	19	47
		C ₂ H ₄ -C ₂ H ₆	27	25	30	24	18	17	31	37	26	38	21	15	39
		CO-C ₂ H ₆	24	8	55	30	10	9	12	18	69	46	13	2	20
		C ₂ H ₂ -C ₂ H ₄	22	22	38	14	14	13	25	34	16	31	18	9	29
		H ₂ O-C ₂ H ₄	12	34	-7	31	9	4	17	-6	-8	20	26	10	18
		H ₂ O-CO	11	48	-24	15	13	8	30	10	-51	5	31	17	27
		C ₂ H ₂ -CO	7	31	1	20	5	0	11	-10	-18	13	23	4	8
		C ₂ H ₄ -CO	5	3	-8	11	4	4	6	4	10	7	3	6	10
		C ₂ H ₂ -C ₂ H ₄	3	17	-25	-5	8	8	19	20	-33	-8	8	13	19
		C ₂ H ₂ -CO	-2	14	-17	-16	4	4	13	16	-43	-15	5	7	9
Avg			Mg	Ti	V	Cr	Mo	Mn	Fe	Ru	Co	Ni	Cu	Zn	
			Metal Species												



Chapter 3: Separation Strategies



Chapter 3: Ethylene/Ethane Selectivity

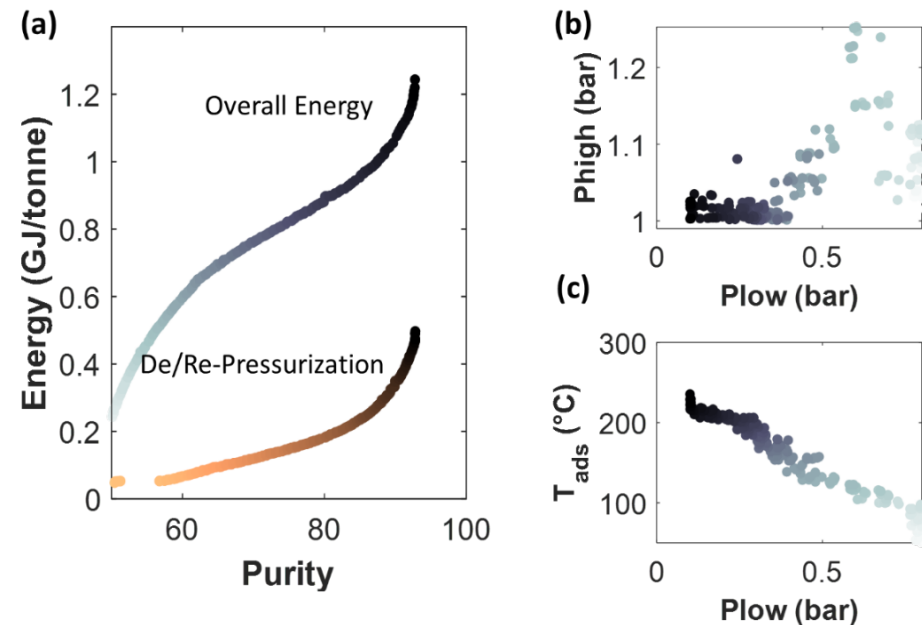


Trade off between larger $\Delta E(C_2H_4 - C_2H_6)$ and smaller $E_-(C_2H_4)$

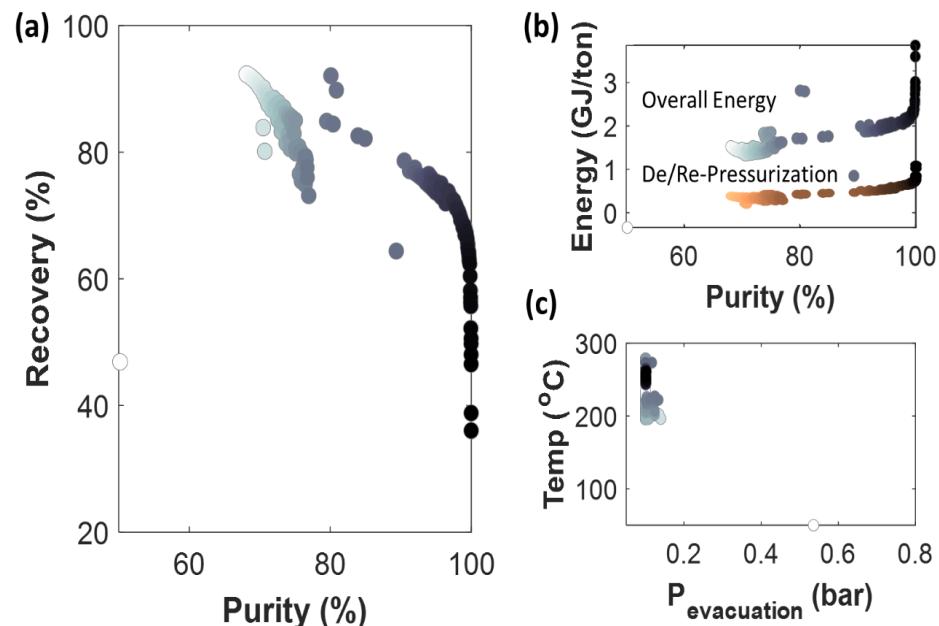
Chapter 4: Optimization of the Adsorption Process

Case Study for the Zn-BTC

Simplified Model



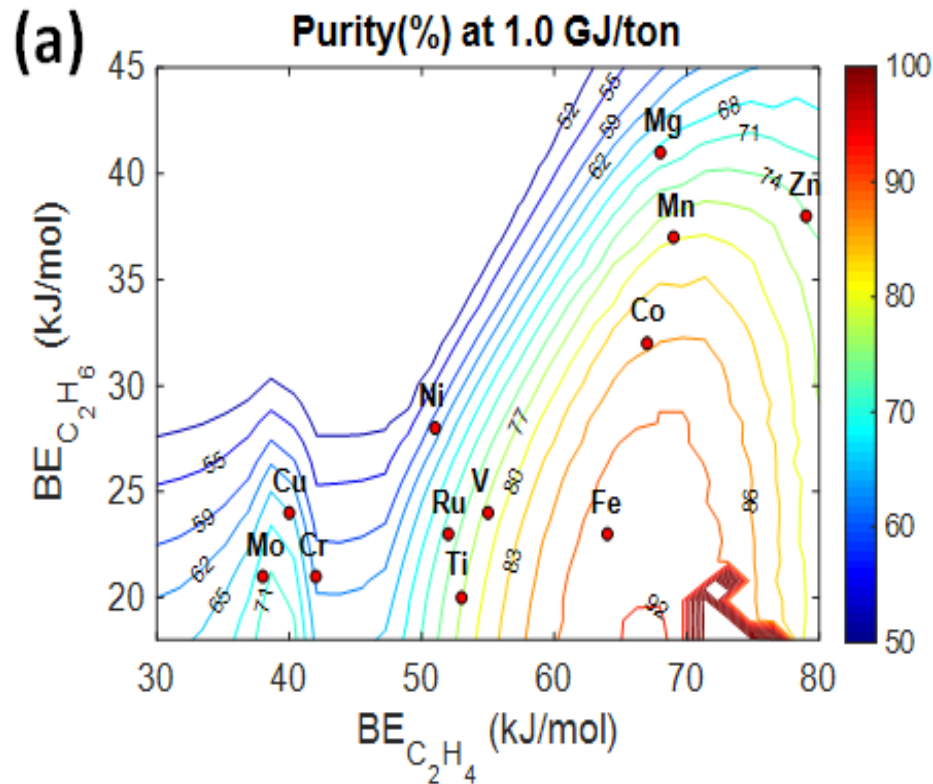
Full Process Model



Finding: Although the simple model underestimates the maximum possible purity and the energy consumed, it still provides a useful general estimate of optimal operating conditions and process performance.

Chapter 4: Performance of Pure Metal MOFs

Simplified Model



Full Process Model

