

Law of Thermodynamics

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1 First Law

Suppose we have the function $f(x)$, where x are parameters of the state. If the integral:

$$\Delta f = \int_{x_i}^{x_f} df = f(x_f) - f(x_i) \quad (1)$$

i.e., if Δf is independent of the path chosen, then we call f a **function of state**, which only depend on the system parameter at a certain instance.

Equation of states are equation that contain only function of states: i.e., for ideal gas, we have $pV = RT$ which depend on p, V, T , all of them are function of states.

First law: energy is conserved in the form of heat and work.

Writting U as the internal energy, The equation of states can be written as

$$\Delta U = \Delta Q + \Delta W \quad (2)$$

$$dU = dQ + dW = dQ - pdV \quad (3)$$

where Δ gives the total change and d represent differential change. d represent changes that are path dependent. It is clear that the heat absorbed and the work done to the system depend on the specific process, and thus they cannot be exact differentiated with respect to the system parameters, while volume V is a function of states.

Heat capacity of gas at constant volume or pressure

For ideal gas, we have:

$$dQ = dU + pdV \quad (4)$$

$$dQ = \left(\frac{\partial U}{\partial T} \right)_V dT + \left(\frac{\partial U}{\partial V} \right)_T dV + pdV \quad (5)$$

$$\frac{dQ}{dT} = \left(\frac{\partial U}{\partial T} \right)_V + \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] \frac{dV}{dT} \quad (6)$$

Therefore, at fixed volume, $dV = 0$ and we have:

$$C_V = \left(\frac{dQ}{dT} \right)_V = \left(\frac{\partial U}{\partial T} \right)_V \quad (7)$$

at fixed pressure:

$$C_p = \left(\frac{dQ}{dT} \right)_p \quad (8)$$

$$= C_V + \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] \left(\frac{dV}{dT} \right)_p \quad (9)$$

For ideal gas, we have $\left(\frac{\partial U}{\partial V} \right)_T = 0$. and $p \left(\frac{dV}{dT} \right)_p = R$, so that we have: $C_p = C_V + R$. For an equilibrium gas at constant pressure, the volume of the gas also expand when the temperature of the gas is increased (gas do work to the environment). So we in generally need to input more heat to the increase the temperature of the gas, compared to the case of constant volume.

In general gas, we define the ratio γ called **adiabatic index**:

$$\gamma = \frac{C_p}{C_V} \quad (10)$$

2 Second Law

Reversible process

we define a process to be reversible if **at every moment during the process, the system is in equilibrium**. As an example, for an ideal gas, if the equation of state $pV = RT$ is hold true at every moment during the process, then it implies that the gas is always in an equilibrium state and the process is reversible: If this process is reversed we could not notice. We consider two types of reversible process in terms of gas: First is called **Isothermal process** and the second is called **Adiabatic process**.

In the isothermal process, the temperature of the system is fixed:

$$\Delta T = 0 \quad (11)$$

For ideal gas, this implies that $\Delta U = 0$, for reversible process of ideal gas, The equation of states is always true. This gives:

$$\Delta U = dQ - \frac{RT}{V}dV = 0 \quad (12)$$

$$\Delta Q = \int_{V_1}^{V_2} dQ = \int_{V_1}^{V_2} \frac{RT}{V}dV = RT \ln \frac{V_2}{V_1} \quad (13)$$

In the adiabatic process, the system is not allowed to exchange heat with the environment, thus we have $dQ = 0$. We find:

$$dU = dW \quad (14)$$

$$C_V dT = -pdV = -\frac{RT}{V}dV \quad (15)$$

$$\ln \frac{T_2}{T_1} = -\frac{R}{C_V} \ln \frac{V_2}{V_1} \quad (16)$$

For ideal gas, $C_p = C_V + R$, $\gamma = 1 + R/C_V$ and we find:

$$\ln \frac{T_2}{T_1} = (1 - \gamma) \ln \frac{V_2}{V_1} \quad (17)$$

$$\frac{T_2}{T_1} = \left(\frac{V_2}{V_1} \right)^{1-\gamma} = \left(\frac{V_1}{V_2} \right)^{\gamma-1} \quad (18)$$

$$TV^{\gamma-1} = \text{const} \quad (19)$$

$$pV^\gamma = \text{const} \quad (20)$$

where we used relationship $pV = RT$ to obtain the last relationship. Equation pV^γ enable us to find the pressure of the system if we know the volume of the system during a adiabatic expansion or compression. Temperature can be derived using the ideal gas law then, if we know the pressure and volume.

second law

The second law can be stated in the following two equivalent form:

Clausius statement No process whose sole effect is to transfer heat from cold to hot body

Kelvin statement No process is possible whose sole effect is to convert heat into work

It is important to note the work "sole effect". For example, in an isothermal process of ideal gas, $dQ + dW = 0$ so all the heat is converted into work done by the system. However, the accompanying effect is that the volume of the gas expanded. Therefore, To study the ability to convert heat into work, we should consider process which has no other effect other than the conversion, such as Carnot engine which work in cycles

Carnot engine

We define a carnot engine which consist of two reversible adiabatic and two reversible isothermal process, working between temperature T_h and T_l . The carnot engine do work in the following process:

| | | |
|-------------------|------------------------|---|
| $A \rightarrow B$ | isothermal expansion | $Q_h = RT_h \ln \frac{V_B}{V_A}$ |
| $B \rightarrow C$ | adiabatic | $\frac{T_h}{T_l} = \left(\frac{V_C}{V_B}\right)^{\gamma-1}$ |
| $C \rightarrow D$ | isothermal compression | $Q_l = -RT_h \ln \frac{V_D}{V_C}$ |
| $D \rightarrow A$ | adiabatic | $\frac{T_h}{T_l} = \left(\frac{V_D}{V_A}\right)^{\gamma-1}$ |

The adiabatic process lead to $\frac{V_C}{V_B} = \frac{V_D}{V_A}$, with $V_B > V_A$. Finally, we find the important result for a carnot energy:

$$\frac{Q_h}{T_h} = \frac{Q_l}{T_l} \quad (21)$$

$$Q_h - Q_l = W \quad (22)$$

where W is the work done in one carnot cycle. We can find the efficiency of the engine ¹:

$$\eta = \frac{W}{Q_h} = 1 - \frac{T_l}{T_h} \quad (23)$$

We have the following statement related to the (reversible) carnot engines:

- Carnot engine is the most efficient engine
- all reversible engine operating at the same temperature environment have the same efficiency
- Clausius statement of the second law is the same as Kelvin's statement ²

Refrigerator

We consider the above carnot energy run backwards: it absorb heat Q_l from the low temperature side with an isothermal expansion. Input work W is provided during the adiabatic process, and dump heat Q_h into the the hot side with an isothermal compression process. The result for such a refrigerator is:

$$Q_l + W = Q_h \quad (24)$$

$$\frac{Q_h}{T_h} = \frac{Q_l}{T_l} \quad (25)$$

$$\eta = \frac{Q_l}{W} = \frac{T_l}{T_h - T_l} \quad (26)$$

Clausius theorem

Suppose we have a series of heat exchange in a working cycle of an engine. At each step, the engine exchange heat dQ_i from a **contact** with temperature T_i . The maximum work this engine can produce is then:

$$\Delta W = \sum_i dQ_i \quad (27)$$

Furthermore, each of these contact are connect to a **single environment** with temperature T through a carnot cycle. Each of these carnot cycle can be considered as heat pumps or refrigerators, which operates to provide (absorb) heat dQ_i at each contact. We have the relationship for these carnot cycles:

$$\frac{dQ}{T} = \frac{dQ_i}{T_i} \quad (28)$$

$$dQ = dQ_i + dW_i \quad (29)$$

¹This carnot engine seems to convert all the heat absorbed into work, $Q_h - Q_l \rightarrow W$. But it has the additional effect to transport heat from one source to another. Therefore, this does not conflict with Kelvin's statement

²See book

Since this system work in cycles, it cannot absorb heat from a single heat resevior (environment at T) and output work (second law). So the total work output by this system is necessary zero (do nothing) or negative (external work need to be provided to get this system going). So we have the following requirement:

$$\sum_i dW_i + \Delta W \leq 0 \quad (30)$$

We have:

$$dW_i = dQ - dQ_i = dQ_i \left(\frac{T}{T_i} - 1 \right) \quad (31)$$

$$\Delta W = \sum_i dQ_i \quad (32)$$

So we can find:

$$\sum_i dQ_i \frac{T}{T_i} \leq 0 \quad (33)$$

$$\sum_i \frac{dQ_i}{T_i} \leq 0 \quad \text{or} \quad \oint \frac{dQ}{T} \leq 0 \quad (34)$$

The second equation is the result of the Clausius theorem. The equal sign is only achieved for a reversible energy, which we write:

$$\oint \frac{dQ_{rev}}{T} = 0 \quad (35)$$

entropy

For an reversible process, we have the relationship:

$$\oint \frac{dQ_{rev}}{T} = 0 \quad (36)$$

suggesting that the integral:

$$\int_A^B \frac{dQ_{rev}}{T} \text{ is path independent} \quad (37)$$

We therefore define a value $dS = dQ_{rev}/T$ and the value of S is an function of state. S is called the entropy. For adiabatic process, $dQ = 0$ and $dS = 0$

In general, we consider a general cycle consists of both reversible and irreversible process. According to Clausius theorem, we have:

$$\oint \frac{dQ}{T} = \int_A^B \frac{dQ}{T} + \int_B^A \frac{dQ_{rev}}{T} \leq 0 \quad (38)$$

so that we have:

$$\int_A^B \frac{dQ}{T} \leq \int_A^B \frac{dQ_{rev}}{T} = \int_A^B dS \quad (39)$$

taking the process from A to B infinitesimal, we thus find:

$$\frac{dQ}{T} \leq dS \quad (40)$$

and the equality only happens for reversible process.

In thermally isolated system, $dQ = 0$, and we reach an important conclusion that for such isolated system, the entropy of the system can only increase: $dS \geq 0$.

For a reversible process, $dQ = TdS$ and the first law gives:

$$dU = TdS + dW \quad (41)$$

$$= TdS - pdV \quad (42)$$

Since value U, T, S, p, V are all function of state. This result is independent of the process and also holds for irreversible process. For an irreversible process, $dU = dQ + dW$ but:

$$dQ \neq TdS \quad (43)$$

$$dW \neq -pdV \quad (44)$$

but

$$dQ + dW = dQ_{rev} - pdV = TdS - pdV \quad (45)$$

Equation.42 also give the result:

$$p = - \left(\frac{dU}{dV} \right)_S \quad (46)$$

$$T = \left(\frac{dU}{dS} \right)_V \quad (47)$$

Joule Expansion

We consider a process of Joule expansion as an example of irreversible process: suppose a container is separate into half, each with volume V_0 . The gas is initially confined one side of the container with pressure p_i . The other side of the container is vacuum. Now we remove the separation and let the gas take up the volume of the whole container.

We have the equation of states:

$$p_i V_0 = RT_i \quad (48)$$

$$p_f 2V_0 = RT_f \quad (49)$$

since the internal energy of the gas does not change, $\Delta U = 0$ and therefore for ideal gas, its temperature remain the same: $T_i = T_f$. We thus have: $p_f = \frac{1}{2}p_i$. and

$$dU = TdS - pdV = 0 \quad (50)$$

$$dS = \frac{p}{T} dV \quad (51)$$

$$\Delta S = \int_i^f dS = \int_i^f \frac{p}{T} dV = \int_i^f \frac{R}{V} dV = R \ln 2 \quad (52)$$

where we consider the process as a reversible isothermal expansion, but is since S is function of state, the result is true for any process ³.

Entropy of macrostates and total entropy

Since we have the statistical definition of temperature

$$\frac{1}{k_B T} = \frac{d \ln \Omega}{dE} \quad (53)$$

where Ω is the number of microstates with energy E . Assume a microcanonical ensemble (each microstates have the same energy and are equally probably), then the internal energy coincide with energy E . Using the relation:

$$T = \left(\frac{\partial U}{\partial S} \right)_V \quad (54)$$

We find the result:

$$S = k_B \ln \Omega \quad (55)$$

which we call the Boltzmann's definition of entropy ⁴.

³Joule expansion is associated with Maxwell's Demon, which is an interesting read at page 149 of the book

⁴<https://physics.stackexchange.com/questions/141321/what-is-the-conceptual-difference-between-gibbs-and-boltzmann-entropies>

Now, we consider ensembles other than microcanonical ensemble. Suppose the system have in total N possible microstates of equal probability, which can be divided into i macrostates that we can distinguish by experimental measurement. Each of those macrostates contain n_i microstates. We define the Gibb's entropy:

$$S_{tot} = S + S_{micro} \quad (56)$$

where $S_{tot} = k_B \ln N$. The microscopic entropy is given by:

$$S_{micro} = \langle S \rangle = \sum_i P_i S_i = \sum_i P_i k_B \ln n_i \quad (57)$$

where the probability $p_i = n_i/N$ and $\sum_i p_i = 1$. We have:

$$S = k_B \left(\sum_i p_i \right) \ln N - \sum_i P_i k_B \ln n_i \quad (58)$$

$$= -k_B \sum_i p_i \ln p_i \quad (59)$$

Gibbs entropy formula is useful because we can generally measure the probability distribution is macroscopic distinguishable states and calculate the entropy from the probability distribution, while for Boltzmann's definition of entropy, it's only applicable for microcanonical ensemble and we cannot access the actual number of the microstates.

3 Third Law

We can measure the change of entropy of a system by measuring its heat capacity:

$$C_p = T \left(\frac{\partial S}{\partial T} \right)_p \quad (60)$$

$$S = \int \frac{C_p}{T} dT \quad (61)$$

so that we have:

$$S(T) = S(T_0) + \int_{T_0}^T \frac{C_p}{T} dT \quad (62)$$

The third law states that the entropy of a system at absolute zero will be zero:

Planck's statement of the third law The entropy of all systems in internal equilibrium is the same at absolute zero and may be taken to be zero.

It is noted that the system should be in a relaxed internal equilibrium, it is possible, for example, to freeze a metastable glass phase instead of a crystalline phase and go down o $T \rightarrow 0$ with non zero entropy.

As a consequence of the third law, Heat capacity, given by Eq.60 will necessarily go to zero as $T \rightarrow 0$.

As another implication, Using the statistical definition of the entropy $S = k_B \ln \Omega$ implies that the ground states of a system at absolute zero, is necessary non-degenerate with $\Omega = 1$ so that the entropy will be zero. Such non-degeneracy would be enforced by the third law for real systems, as well as the requirement for $C_p \rightarrow 0$. As an example, the curie's law gives a susceptibility $\chi \rightarrow \infty$ as $T \rightarrow 0$. But with the third law, we require $\partial \chi / \partial T \rightarrow 0$. This problem is caused because for Curie law, we assumed a mean field interaction where the interaction of magnetic moment is ignored⁵.

4 Thermodynamic potentials

We call **Thermodynamic potentials** functions that are constructed from the functions of state. We define the following Thermodynamic potentials, The first being the internal energy, the following are the Enthalpy, Helmholtz function and the Gibbs function:

One convenience of these Thermodynamic potentials compared to the internal energy U is that they are presented in more convenient variables. For example, for a system that at a fixed volume and pressure during a process, we can know that its Gibbs function must remain the same during that process.

⁵See discussion in page 204-205

$$\begin{array}{lll}
U & dU = TdS - pdV & T = \left(\frac{\partial U}{\partial S}\right)_V, p = -\left(\frac{\partial U}{\partial V}\right)_S \\
H = U + PV & dH = TdS + pdV & T = \left(\frac{\partial H}{\partial S}\right)_V, V = \left(\frac{\partial H}{\partial p}\right)_S \\
F = U - TS & dF = -SdT - pdV & S = -\left(\frac{\partial F}{\partial T}\right)_V, p = -\left(\frac{\partial F}{\partial V}\right)_T \\
G = H - TS & dG = -SdT + Vdp & S = -\left(\frac{\partial G}{\partial T}\right)_p, V = \left(\frac{\partial G}{\partial p}\right)_T
\end{array}$$

Maxwell's relationship

Maxwell's relationship can be derived from the above definition of the thermodynamic potential function, and they are stated as below:

$$\left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial p}{\partial S}\right)_V \quad (63)$$

$$\left(\frac{\partial T}{\partial p}\right)_S = \left(\frac{\partial V}{\partial S}\right)_p \quad (64)$$

$$\left(\frac{\partial S}{\partial V}\right)_T = -\left(\frac{\partial p}{\partial T}\right)_V \quad (65)$$

$$\left(\frac{\partial S}{\partial p}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_p \quad (66)$$

Isothermal magnetization and adiabatic demagnetization

To generalize the above treatment in general system, we can write:

$$dW = Xdx \quad (67)$$

where X is some intensive generalized force and x is some extensive generalized displacement.

Consider a system of magnetic moments arranged in a lattice. We assume paramagnetic system with no interaction between the magnetic moments. The first law of Thermodynamic for such system is

$$dU = TdS - mdB \quad (68)$$

We define the magnetic susceptibility as:

$$\chi = \lim_{H \rightarrow 0} \frac{M}{H} \approx \frac{\mu_0 M}{B} \quad (69)$$

since $B = \mu_0(H + M)$ and $M \ll H$. Curie's law states $\chi \propto 1/T$ and therefore

$$\left(\frac{\partial \chi}{\partial T}\right)_B < 0 \quad (70)$$

Consider the Helmholtz function:

$$dF = -SdT - mdB \quad (71)$$

which gives the Maxwell relation:

$$\left(\frac{\partial S}{\partial B}\right)_T = \left(\frac{\partial m}{\partial T}\right)_B \approx \frac{VB}{\mu_0} \left(\frac{\partial \chi}{\partial T}\right)_B \quad (72)$$

The heat absorbed in an isothermal change of B is:

$$\Delta Q = T \left(\frac{\partial S}{\partial B}\right)_T \Delta B = \frac{TVB}{\mu_0} \left(\frac{\partial \chi}{\partial T}\right)_B \Delta B < 0 \quad (73)$$

So that an isothermal increase of B will release heat to the environment.

The change in temperature in an adiabatic change of B is

$$\left(\frac{\partial T}{\partial B}\right)_S = -\left(\frac{\partial T}{\partial S}\right)_B \left(\frac{\partial S}{\partial B}\right)_T \quad (74)$$

using

$$C_B = T \left(\frac{\partial S}{\partial T} \right)_B \quad (75)$$

we have:

$$\left(\frac{\partial T}{\partial B} \right)_S = - \frac{TVB}{\mu_0 C_B} \left(\frac{\partial \chi}{\partial T} \right)_B > 0 \quad (76)$$

So that in an adiabatic process, the temperature will decrease with the decrease of magnetization, which is called **adiabatic demagnetization**