

ABSTRACT

Title of thesis: ANALYSIS OF PROPANE GAS FIRE EXPERIMENTS AND SIMULATIONS IN RESIDENTIAL SCALE STRUCTURES

Joseph M. Willi, Master of Science, 2017

Thesis directed by: Professor James A. Milke
Department of Fire Protection Engineering

Nine full-scale fire experiments were conducted in two residential-sized structures with a fire source provided by three propane gas burners. Five of the experiments were conducted in a single-story structure, and four were conducted in a two-story structure. The structures were instrumented to measure temperature; oxygen and carbon dioxide gas concentrations; gas velocity; and heat flux. Various doors and vents were opened and closed during the experiments to change the ventilation through the structures. Numerical simulations of the nine experiments were conducted using Fire Dynamics Simulator (FDS) (version 6.5.3). The model data output by the simulations were compared to the corresponding experimental data, and the temperature, gas species concentration, and heat flux data produced by the simulations were within the expected agreement range based on the values of experimental relative standard deviation, model relative standard deviation, and model bias factor provided by the FDS Validation Guide for each specific data type. The one significant discrepancy between expected agreement and actual agreement

of the simulation data and experimental data occurred with the gas velocity measurements, which produced a model relative standard deviation that was 0.18 larger than the value from the FDS Validation Guide. Overall, comparing the FDS simulation output to the experimental data shows sufficient agreement between the predicted and measured data, thus indicating that FDS is capable of accurately modeling different aspects of fire scenarios in residential-sized structures.

Analysis of Propane Gas Fire Experiments and Simulations in
Residential Scale Structures

by

Joseph Martin Willi

Thesis submitted to the Faculty of the Graduate School of the
University of Maryland, College Park in partial fulfillment
of the requirements for the degree of
Master of Science
2017

Advisory Committee:
Professor James A. Milke, Chair
Professor Arnaud Trouve
Dr. Craig Weinschenk

© Copyright by
Joseph Martin Willi
2017

Acknowledgments

The National Institute of Standards and Technology (NIST) provided the resources necessary to complete this project. Specifically, I'd like to thank Daniel Madrzykowski, Roy McLane, Kristopher Overholt, Keith Stakes, and Craig Weinschenk for their contributions in preparing and conducting the experiments. I'd also like to thank the team from the Delaware County Emergency Services Training Center, namely Deputy Director Kerby Kerber, for providing the location and logistical support needed to successfully conduct the tests for this study.

Thank you also to Dr. Kevin McGrattan of NIST for his guidance and assistance with preparing the FDS input files and for providing advice and expertise throughout the FDS-related components of this project. I'd like to thank my advisor from the University of Maryland, Dr. James Milke, for his help and direction during my time at Maryland. Additionally, thank you to Dr. Arnaud Trouv  for being a member of my defense committee and providing valuable feedback about this project.

Table of Contents

List of Tables	v
List of Figures	vi
List of Abbreviations	ix
1 Introduction	1
2 Experimental Setup	4
2.1 Test Structures	4
2.1.1 Construction	4
2.1.2 Layout	8
2.2 Instrumentation	10
2.2.1 East Structure	11
2.2.2 West Structure	14
2.2.3 Measurement Uncertainty	17
3 Experimental Procedure	20
3.1 East Structure Tests	22
3.1.1 Tests 2–4	22
3.1.2 Tests 5 & 6	24
3.2 West Structure Tests	25
3.2.1 Tests 22 & 23	26
3.2.2 Tests 24 & 25	28
4 Numerical Model Description	30
4.1 Computational Domain	31
4.1.1 Numerical Mesh	32
4.2 Source Fire Characterization	34
4.3 Additional Input Parameters	38

5	Results and Discussion	43
5.1	Mesh Sensitivity Studies	43
5.2	FDS Model Data Compared to Experimental Data	49
5.2.1	Temperature	52
5.2.2	Gas Species Concentration	62
5.2.3	Gas Velocity	66
5.2.4	Total Heat Flux	69
5.2.5	Summary	71
6	Conclusion	74
A	Channel Lists	76
A.1	East Structure	76
A.2	West Structure	80
B	Experimental and FDS Data Plots	86
B.1	Temperature	86
B.2	Gas Species Concentration	112
B.3	Gas Velocity	128
B.4	Total Heat Flux	129
	Bibliography	130

List of Tables

3.1	Summary of Propane Gas Burner Experiments.	21
3.2	Heat Release Rates for Tests 5 and 6.	22
3.3	Heat Release Rates for Tests 22–25.	26
4.1	Tests 2–4 Estimated Heat Release Rates Using MQH Correlation.	37
4.2	Various Materials Defined Within Each FDS Input File and the Corresponding MATL Namelist Group Parameter Values.	41
4.3	Instrumentation Specified within FDS Input File and Corresponding DEVC Namelist Group Properties.	42
5.1	Calculated δ , σ_E , and σ_M Values Compared to Values Stated in FDS Validation Guide.	71
A.1	East Structure Channel List	76
A.2	West Structure Channel List	80

List of Figures

2.1	North side of the East and West Structures	6
2.2	Ceiling support of the West Structure	7
2.3	Dimensioned floor plan of the East Structure	8
2.4	Dimensioned floor plans of the West Structure	9
2.5	Instrumentation legend	10
2.6	Three propane burners used as the fuel source.	11
2.7	Locations and labels of instrumentation in the East Structure	12
2.8	Bi-directional probe plus solid thermocouple arrays in East Structure	13
2.9	Locations and labels of instrumentation in the West Structure.	15
2.10	Locations and labels of instrumentation in the West Structure	16
3.1	Tests 2–4 layout and event times.	23
3.2	Test 5 layout and event times.	24
3.3	Test 6 layout and event times.	25
3.4	Tests 22–23 layout and event times.	27
3.5	Tests 24–25 layout and event times.	29
5.1	O_2 concentrations for East Structure simulation with different grid cell sizes.	44
5.2	Ceiling jet temperatures for East Structure simulation with different grid cell sizes.	45
5.3	O_2 concentrations for West Structure simulation with different grid cell sizes.	46
5.4	Ceiling jet temperatures for West Structure simulation with different grid cell sizes.	47
5.5	Plots of measured and predicted hot gas layer temperatures during Test 22.	54
5.6	Summary of measured and predicted hot gas layer temperatures.	55
5.7	Plots of measured and predicted ceiling jet temperatures during Test 4.	57
5.8	Summary of measured and predicted ceiling jet temperatures.	58
5.9	Plot of the measured and predicted upper temperatures from array A1 during Test 24.	60

5.10	Summary of measured and predicted temperatures at the individual thermocouple locations within the different thermocouple arrays.	61
5.11	Plots of measured and predicted O_2 concentration during Test 3.	62
5.12	Summary of measured and predicted O_2 concentrations.	63
5.13	Plots of measured and predicted CO_2 concentration during Test 3.	64
5.14	Summary of measured and predicted CO_2 concentrations.	65
5.15	Plots of measured and predicted gas velocity through the roof vent during Test 5.	67
5.16	Summary of measured and predicted gas velocity measurements.	68
5.17	Plots of measured and predicted heat flux during Test 23.	69
5.18	Summary of measured and predicted heat flux measurements.	70
B.1	Plots of measured and predicted hot gas layer temperatures during Test 2.	86
B.2	Plots of measured and predicted hot gas layer temperatures during Test 3.	87
B.3	Plots of measured and predicted hot gas layer temperatures during Test 4.	88
B.4	Plots of measured and predicted hot gas layer temperatures during Test 5.	89
B.5	Plots of measured and predicted hot gas layer temperatures during Test 6.	90
B.6	Plots of measured and predicted hot gas layer temperatures during Test 23.	91
B.7	Plots of measured and predicted hot gas layer temperatures during Test 24.	92
B.8	Plots of measured and predicted hot gas layer temperatures during Test 25.	93
B.9	Plots of measured and predicted ceiling jet temperatures during Test 2. .	94
B.10	Plots of measured and predicted ceiling jet temperatures during Test 2. .	95
B.11	Plots of measured and predicted ceiling jet temperatures during Test 3. .	96
B.12	Plots of measured and predicted ceiling jet temperatures during Test 3. .	97
B.13	Plots of measured and predicted ceiling jet temperatures during Test 4. .	98
B.14	Plots of measured and predicted ceiling jet temperatures during Test 5. .	99
B.15	Plots of measured and predicted ceiling jet temperatures during Test 5. .	100
B.16	Plots of measured and predicted ceiling jet temperatures during Test 6. .	101
B.17	Plots of measured and predicted ceiling jet temperatures during Test 6. .	102
B.18	Plots of measured and predicted ceiling jet temperatures on the first floor during Test 22.	103
B.19	Plots of measured and predicted ceiling jet temperatures on the second floor during Test 22.	104
B.20	Plots of measured and predicted ceiling jet temperatures on the first floor during Test 23.	105
B.21	Plots of measured and predicted ceiling jet temperatures on the second floor during Test 23.	106

B.22 Plots of measured and predicted ceiling jet temperatures on the first floor during Test 24.	107
B.23 Plots of measured and predicted ceiling jet temperatures on the second floor during Test 24.	108
B.24 Plots of measured and predicted ceiling jet temperatures on the first floor during Test 25.	109
B.25 Plots of measured and predicted ceiling jet temperatures on the second floor during Test 25.	110
B.26 Plots of measured and predicted thermocouple array temperatures during Test 24.	111
B.27 Plots of measured and predicted O_2 concentration during Test 2.	112
B.28 Plots of measured and predicted O_2 concentration during Test 4.	113
B.29 Plots of measured and predicted O_2 concentration during Test 5.	114
B.30 Plots of measured and predicted O_2 concentration during Test 6.	115
B.31 Plots of measured and predicted O_2 concentration during Test 22.	116
B.32 Plots of measured and predicted O_2 concentration during Test 23.	117
B.33 Plots of measured and predicted O_2 concentration during Test 24.	118
B.34 Plots of measured and predicted O_2 concentration during Test 25.	119
B.35 Plots of measured and predicted CO_2 concentration during Test 2.	120
B.36 Plots of measured and predicted CO_2 concentration during Test 4.	121
B.37 Plots of measured and predicted CO_2 concentration during Test 5.	122
B.38 Plots of measured and predicted CO_2 concentration during Test 6.	123
B.39 Plots of measured and predicted CO_2 concentration during Test 22.	124
B.40 Plots of measured and predicted CO_2 concentration during Test 23.	125
B.41 Plots of measured and predicted CO_2 concentration during Test 24.	126
B.42 Plots of measured and predicted CO_2 concentration during Test 25.	127
B.43 Plots of measured and predicted gas velocity through the roof vent during Test 5.	128
B.44 Plots of measured and predicted heat flux during Test 23.	129

List of Abbreviations

CFD	Computational Fluid Dynamics
FDS	Fire Dynamics Simulator
NIST	National Institute of Standards and Technology
OSB	Oriented Strand Board
TJI	Truss Joist I-beams

Chapter 1: Introduction

The development and behavior of compartment fires, such as those inside residential structures, depend greatly on the ventilation conditions within the compartment. Nine full-scale fire experiments were conducted in residential-sized structures to study how opening and closing different doors and vents affect ventilation and the fire environment. Two experimental structures designed to replicate a single-story and a two-story dwelling were used. The fire source for each experiment was provided by three gas propane burners. The flow of propane to the burners was controlled by a high-precision turn valve and the total displaced gas volume was measured using a rotary gas meter. Local measurements of temperature, gas species concentration, gas velocity, and total heat flux at various locations throughout the structure were collected while the ventilation within the structure was varied through the opening and closing of doors and vents.

Numerical simulations of the nine tests were performed using the program Fire Dynamics Simulator (FDS) (version 6.5.3) [1]. FDS is a computational fluid dynamics (CFD) model of thermally-driven fluid flow that is developed and maintained by the National Institute of Standards and Technology (NIST). FDS numerically solves a form of the Navier-Stokes equations for low-speed ($Ma < 0.3$), thermally-driven

flows with an emphasis on smoke and heat transport from fires. The FDS Technical Reference Guide [2] provides a complete description of the model, including the formulation of the equations and numerical algorithm utilized by the software. FDS is mathematically verified [3] and validated against a continually growing database of experimental data from a variety of fire scenarios [4].

Fire protection engineers commonly use CFD models to predict fire dynamics and smoke movement for potential fire scenarios as they are developing certain fire safety designs. FDS is the most commonly used program for this type of application. Therefore, it's crucial that the program is validated for a range of fire scenarios, including those within residential structures. Currently, there are a limited number of experiments for which FDS has been validated that involve fires within residential-sized structures. Furthermore, there are no cases described within the FDS Validation Guide that involve fire scenarios inside multi-story residential scale structures. Thus, generating FDS simulations of the nine gas burner experiments and comparing the results to the experimental data from the nine gas burner tests will provide an important addition to the FDS validation database.

This report contains a thorough description of the experimental structures and instrumentation used to collect data during the nine propane gas fire experiments. The procedures followed during each test are also outlined. Following the description of the experimental setup and procedures, the FDS input files that define experiment simulations are discussed in detail. Next, the data output by the models are compared to the corresponding sensor data of temperature; oxygen and carbon dioxide concentration; gas velocity; and heat flux. Figures of simulation data

and experimental data plotted over the duration of the tests are presented alongside log/log scatter plots that summarize the overall results for each data type. The relative standard deviation values for the model and experimental data and the resulting model bias factor are reported with each summary plot. Then, the relative standard deviation values and model bias factor for each data type are compared to the corresponding values listed within the FDS Validation Guide.

Chapter 2: Experimental Setup

The series of field experiments described in this report were conducted in two structures of similar design located at the Delaware County Emergency Services Training Center in Sharon Hill, Pennsylvania. Three propane burners were used as the fire source for all experiments, and the structures were instrumented with various sensors to collect gas temperature, gas velocity, total heat flux, and gas species concentration measurements.

2.1 Test Structures

2.1.1 Construction

Each test structure was built on a concrete slab as shown in Figure 2.1. The East Structure and West Structure were designed to simulate a single-story and two-story residential structure, respectively.

First Floor of Both Structures

The first floor of each structure had outer walls composed of interlocking concrete blocks measuring 0.6 m (2.0 ft) wide, 0.6 m (2.0 ft) high, and 1.2 m (4.0 ft)

long. The joints and gaps between the blocks were filled with high temperature insulation. All doors along the outer walls were composed of steel.

The interior walls on the first floor of each structure were framed with steel studs set to 400 mm (16 in) centers and track. Two layers of 16 mm (0.63 in) Type X gypsum board lined the steel studs, and a layer of 13 mm (0.5 in) thick Durock cement board covered the gypsum board. The interior ceiling of each structure was covered by two layers of 13 mm (0.5 in) thick Durock cement board.

The first floor ceiling support of each structure was composed of wood truss joist I-beams (TJIs). Each TJI had a depth of 298 mm (11.75 in) and contained laminated veneer lumber flanges with a cross section of 29 mm (1.13 in) by 44 mm (1.75 in) and an 11 mm (0.43 in) thick oriented strand board (OSB) web as shown in Figure 2.2. A layer of 18.3 mm (0.72 in) thick tongue and groove OSB was attached to the top of the TJIs.

Second Floor of West Structure

The second floor of the West Structure was built on the structure's first floor wood ceiling support. The two floors were connected by an interior stairwell. A door made of lauan plywood was located at the top of the stairwell. The walls on the second floor were of wood frame with 51 mm (2 in) by 102 mm (4 in) studs set to 400 mm (16 in) centers. Two layers of 16 mm (0.63 in) Type X gypsum board lined the interior side of the wood studs, and a layer of 13 mm (0.5 in) thick Durock cement board covered the gypsum board. The interior ceiling of the second story was



Figure 2.1: North side of the East Structure (top) and West Structure (bottom).



Figure 2.2: First floor ceiling support of the West Structure composed of wood truss joist I-beams. View is of the southeast corner of the structure.

covered by two layers of 13 mm (0.5 in) thick Durock cement board. The exterior sides of the outer walls on the second floor were protected by 11 mm (0.44 in) thick OSB and 8 mm (0.31 in) fiber cement lap siding.

Leakage

An air leakage measurement system [5] from Infiltec, Inc. (model E3-A-DM4), was used to measure the amount of leakage associated with each structure. The amount of leakage in the East Structure was measured as 0.024 m^2 . For the West Structure, the leakage was measured as 0.027 m^2 when the stairway door was fully closed, 0.054 m^2 when the stairway door was fully opened, and 0.048 m^2 when the stairway door was in the “closed” position (having a 152 mm (6 in) gap between the door and the frame) used during Tests 24 and 25.

2.1.2 Layout

Dimensioned floor plans of the East and West Structures are presented in Figures 2.3 and 2.4, respectively.

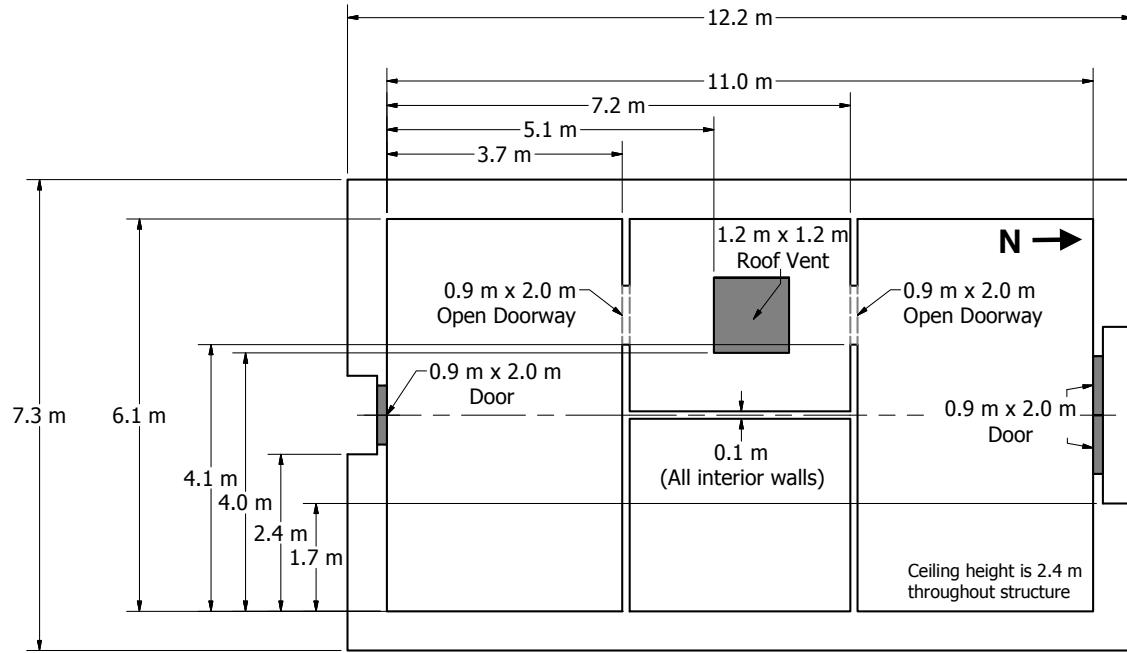


Figure 2.3: Dimensioned floor plan of the East Structure. Structure dimensions are symmetric across horizontal centerline.

The exterior doors of both structures, the stairwell door in the West Structure, and the square roof vent with a depth of 320 mm (12.75 in) in the East Structure were opened and closed at certain instances during the experiments to change the ventilation patterns within the structures.

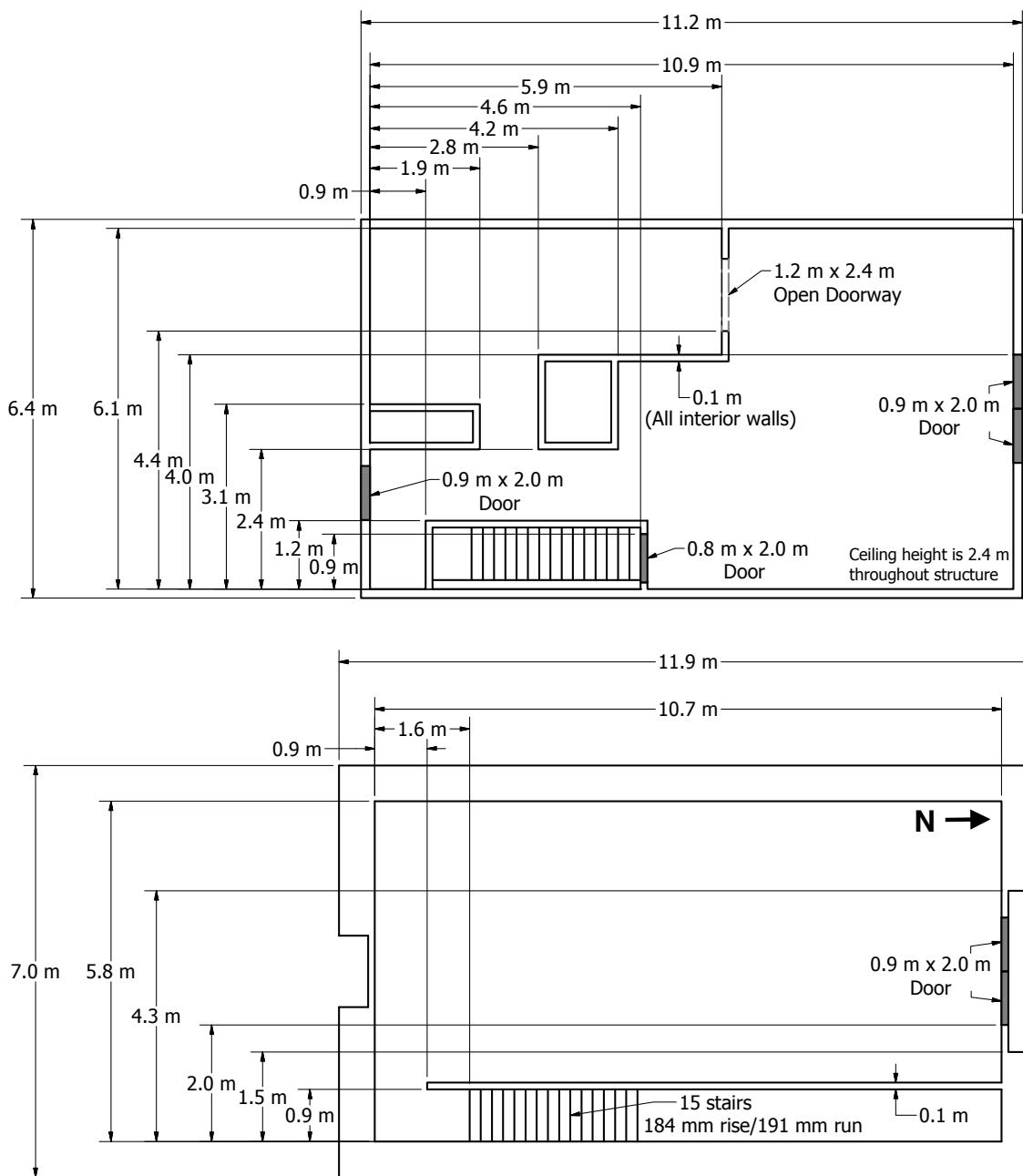


Figure 2.4: Dimensioned floor plan of the second floor (top) and first floor (bottom) of the West Structure.

2.2 Instrumentation

The structures were instrumented for temperature, gas velocity, heat flux, and gas concentration measurements. Gas temperatures in the burn rooms were measured with bare-bead, Chromel-Alumel (type K) thermocouples. Additional single thermocouples were installed in conjunction with bi-directional probes for gas velocity measurements. The single thermocouples were bare-bead, Chromel-Alumel (type K) thermocouples with a 1.0 mm (0.04 in) nominal diameter. The thermocouple wire was protected with a 3.2 mm (0.13 in) diameter inconel sheath. Water-cooled Schmidt-Boelter gauges were used to measure the total heat flux at different locations throughout the structures. Calibrated pumps pulled gas samples through a sample conditioning system to eliminate moisture in the sample. Then, the dry gas samples were piped to a series of gas analyzers and the gas concentrations of oxygen and carbon dioxide were measured. A legend is presented in Figure 2.5 to clarify the instrumentation schematic diagrams presented in the follow sections.

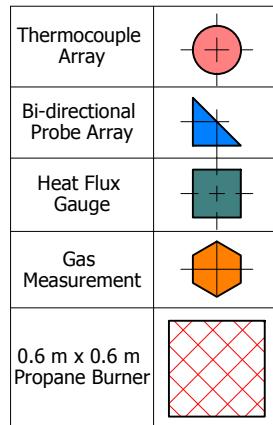


Figure 2.5: Legend used for schematic diagrams of instrumentation locations.

Three diffusion flame burners, pictured in Figure 2.6, were used as the fuel source for each experiment. Each burner had a square opening of side length 0.6 m (2 ft) located 0.14 m (5.5 in) above the floor and were positioned 0.6 m (2 ft) from the interior side of the south and west walls on the ground floor of each structure. Propane was flowed from a supply truck to the gas burners for all experiments. The flow of propane to each burner was controlled by a high-precision turn valve, and the total displaced gas volume was measured using a rotary gas meter.



Figure 2.6: Three propane burners used as the fire source for the experiments located 0.6 m (2 ft) off the interior side of the south and west walls in the East Structure.

2.2.1 East Structure

The East Structure was instrumented with five bare-bead thermocouple arrays, four bi-directional probe plus solid thermocouple arrays, four total heat flux gauges,

and two gas sample inlet pipes at the locations shown in Figure 2.7.

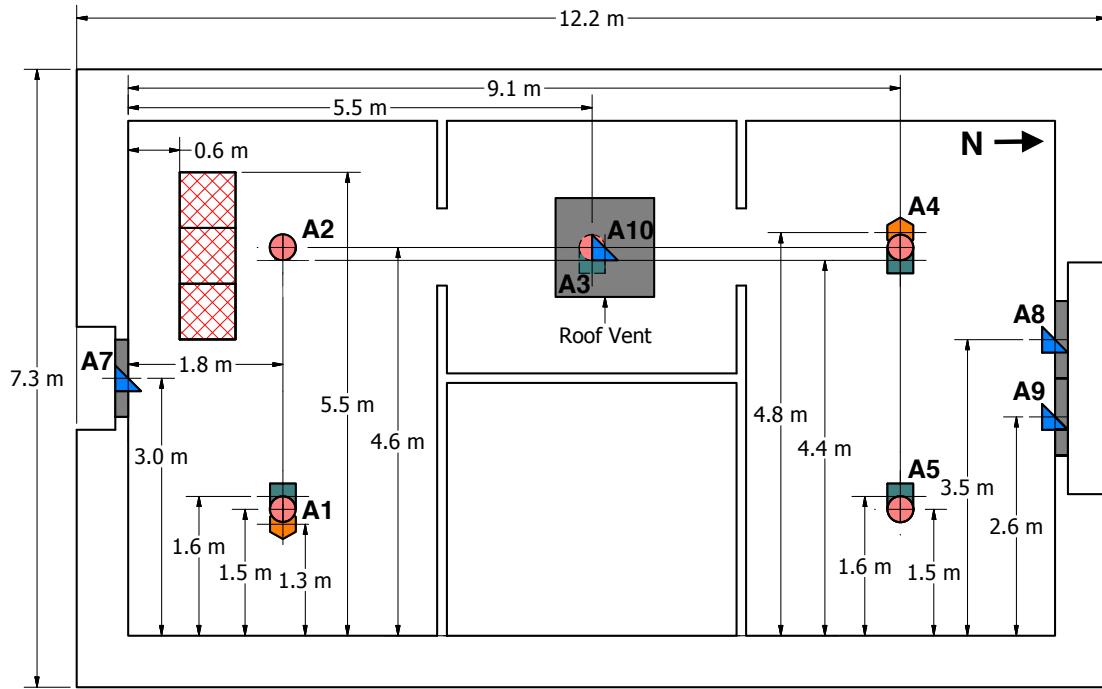


Figure 2.7: Locations and labels of instrumentation in the East Structure.

Each bare-bead thermocouple array (A1, A2, A3, A4, and A5) was composed of eight vertically-aligned thermocouples spaced between the floor and ceiling. Three bi-directional probe and solid thermocouple arrays (A7, A8, and A9) were centered in the exterior doorways of the structure and contained eight probes as shown in Figure 2.8. The fourth bi-directional probe and solid thermocouple array (A10), also presented in Figure 2.8, was located at the opening of the roof vent, 320 mm (12.75 in) above the compartment ceiling. The array contained three probes centered between the east and west sides of the vent. The position of each probe and thermocouple pair relative to the south wall of the vent is listed in Table A.1 of

Appendix A. The total heat flux gauges (A1, A3, A4, and A5) were located near the floor and aimed to view the ceiling. Lastly, gas samples were pulled from the environment through 9.5 mm (0.38 in) diameter stainless steel tubing (A1 and A4). The height of each individual sensor in the sensor arrays is listed in Table A.1 of Appendix A.



Figure 2.8: Bi-directional probe plus solid thermocouple array at the south exterior doorway (top) and roof vent (bottom) of the East Structure.

2.2.2 West Structure

The first floor of the West Structure was instrumented with three bare-bead thermocouple arrays (A1, A2, and A3), two bi-directional probe plus solid thermocouple arrays (A5 and A6), and one gas sample inlet pipe (A1). The second floor was equipped with three bare-bead thermocouple arrays (A7, A8, and A9), four bi-directional probe plus solid thermocouple arrays (A10, A11, A13, and A14), two total heat flux sensor pairs (A16 and A17), and one gas sample inlet pipe (A10).

The location of the instrumentation in the West Structure is shown in Figure [2.10](#).

The thermocouple arrays and bi-directional probe plus solid thermocouple arrays contained eight sensors per array. Gas samples were pulled through 9.5 mm (0.38 in) diameter stainless steel tubing located 1.2 m (4 ft) above the floor. Each pair of total heat flux sensors was located 1.0 m (3.3 ft) above the floor. The pair at A16 contained one sensor facing the ceiling and another facing the north side of the room, and the pair at A17 contained one sensor facing the ceiling and another facing the stairway door. The height of each individual sensor in the sensor arrays is listed in the channel list found in Table [A.2](#).

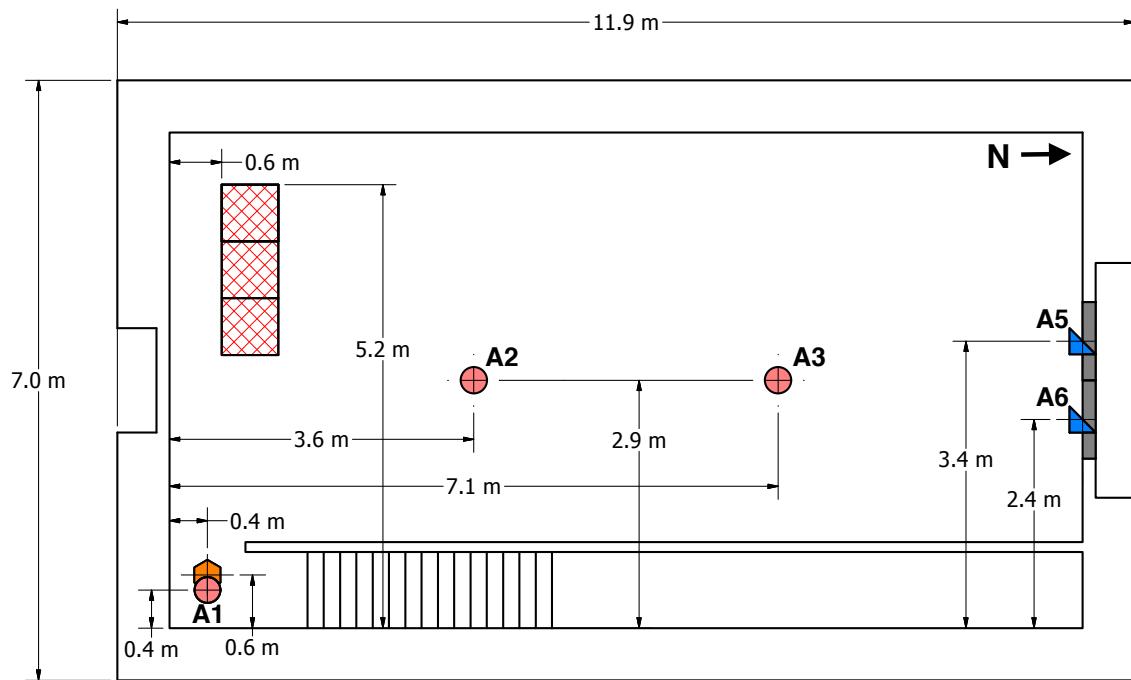
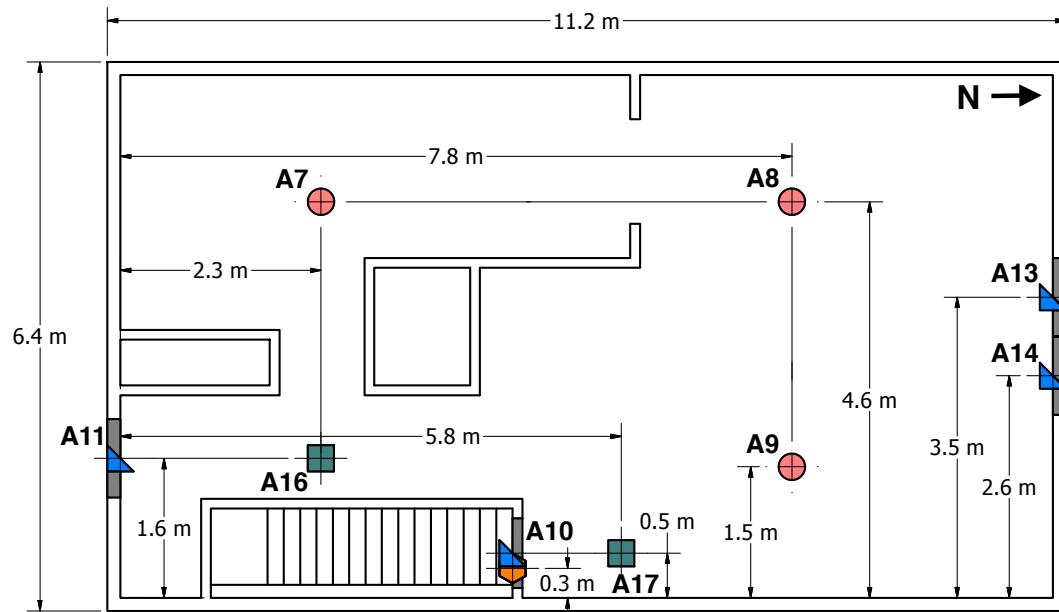


Figure 2.9: Locations and labels of instrumentation in the second floor (top) and first floor (bottom) of the West Structure.

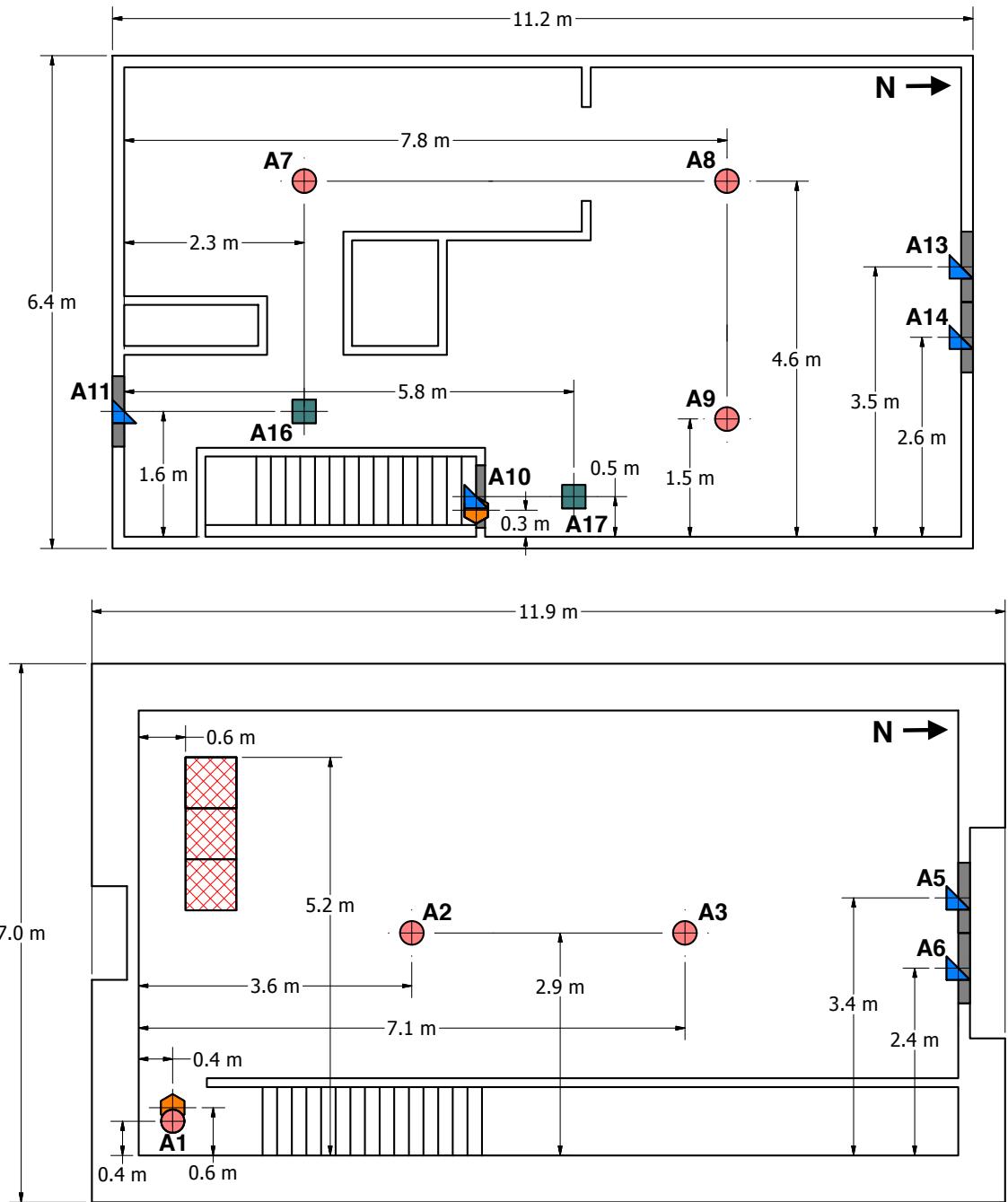


Figure 2.10: Locations and labels of instrumentation in the second floor (top) and first floor (bottom) of the West Structure.

2.2.3 Measurement Uncertainty

This section lists the uncertainties in the reported length, mass, temperature, heat flux, gas species concentration, gas velocity, and heat release rate measurements. Uncertainty estimates are based either on manufacturer literature or analyses performed by others for similar measurement devices and techniques. In accordance with NIST guidelines [6], measurement accuracy is reported as an *expanded uncertainty*, or 95 % (2σ) confidence interval. Most manufacturer specifications express accuracy in terms of a *standard uncertainty*, or 68 % (1σ) confidence interval.

Compartment Dimensions

Room dimensions and instrumentation location measurements were made with a hand held laser measurement device with a standard uncertainty of ± 6.0 mm (0.25 in) over a range of 0.6 m (2.0 ft) to 15 m (50.0 ft) according to the manufacturer [7]. Steel measuring tapes with a resolution of ± 0.5 mm (0.02 in) were used to locate measurement devices. The steel measuring tapes were manufactured in compliance with NIST Manual 44 [8], which specifies a tolerance of ± 1.6 mm (0.06 in) for 9.1 m (30 ft) tapes and ± 6.4 mm (0.25 in) for 30.5 m (100 ft) tapes. These uncertainties are all well within the precision of the reported dimensions, which are typically rounded to the nearest 0.1 m.

Thermocouples

The standard uncertainty in the temperature of the thermocouple wire itself as stated by the wire manufacturer, OMEGA Engineering, Inc., is ± 2.2 °C at 277 °C and increases to ± 9.5 °C at 871 °C [9]. The variation of the temperature in the environment surrounding the thermocouple is known to be much greater than that of the wire uncertainty. Expanded uncertainties as high as 20 % for upper layer temperatures measured by a 1 mm bare-bead type K thermocouple have been reported by NIST researchers [10,11]. Small diameter thermocouples were used during these experiments to limit the impact of radiative heating and cooling. The estimated expanded uncertainty associated with the temperature measurements is ± 15 %.

Heat Flux Gauges

Total heat flux measurements were made using water-cooled Schmidt-Boelter gauges. The manufacturer, MEDTHERM Corporation, reports a ± 3 % calibration expanded uncertainty for these devices [12]. Results from an international study on total heat flux gauge calibration and response demonstrated that the expanded uncertainty of a Schmidt-Boelter gauge is typically ± 8 % [13].

Gas Sampling

A gas sampling system from California Analytical Instruments, Inc. (model 602P) with a relative expanded uncertainty of ± 1 % when compared to span gas volume fractions [14] was used to make gas concentration measurements. However,

according to a study by Lock et al. [15], the non-uniformity and movement of exhaust gases contribute to an estimated expanded uncertainty of $\pm 12\%$.

Bi-Directional Probes

Bi-directional probes with Setra 264 pressure transducers from Setra Systems, Inc. were used to measure gas velocity through doorways. An expanded uncertainty ranging from $\pm 14\%$ to $\pm 22\%$ for bi-directional probes of similar design was calculated by Bryant of NIST [16].

Heat Release Rate

A positive displacement rotary gas meter was used to measure the volume flow rate of propane into the gas burners. The manufacturer, Romet Limited, reports a relative standard uncertainty of $\pm 2\%$ for this type of meter (model RM-3000) [17]. A volumetric flow rate was calculated from the gas meter volume readings and used in conjunction with the heat of combustion of propane to calculate the heat release rate of the fire for each experiment. The total expanded uncertainty for the heat release rate obtained from this method is estimated to be $\pm 8\%$.

Chapter 3: Experimental Procedure

A similar procedure was followed for all nine propane gas burner experiments described in this report. First, the three propane burners were ignited in sequential order. Next, various doors and vents were opened and closed to change the ventilation pattern in the structure. Then, the burners were turned off, extinguishing the fire. After the burners were extinguished, data continued to be collected while different doors and vents were opened to cool the interior of the structure. A positive pressure ventilation (PPV) fan was used during some tests to expedite the cooling of the structure.

The nine propane gas burner tests were conducted in series with a variety of other experiments. In order to be consistent with the original test numbering, the gas burner experiments described in this report are referred to as Tests 2–6 and Tests 22–25. The experiments and their different parameters are summarized in Table 3 below.

Table 3.1: Summary of Propane Gas Burner Experiments.

Name	Structure	Duration of Fire (min:sec)	Heat Release Rate Rate (kW)	Ventilation
Test 2	East	16:01	N.R.*	Both double doors, south door, PPV after fire
Test 3	East	16:58	N.R.*	Both double doors, south door, PPV after fire
Test 4	East	16:59	N.R.*	Both double doors, south door, PPV after fire
Test 5	East	9:36	1190	Roof vent, both double doors
		10:15	1190	Roof vent, both double doors
		9:32	1190	Roof vent, both double doors
Test 6	East	5:27	1190	Roof vent, west double door
		5:03	1190	Roof vent, west double door
		5:12	1180	Roof vent, west double door
Test 22	West	16:58	1240	Both sets of double doors, 2nd floor south door, PPV fan
Test 23	West	16:58	1290	Both sets of double doors, PPV fan
Test 24	West	16:58	1270	West double door on both floors, 2nd floor south door, PPV fan
Test 25	West	16:58	1270	West double door on both floors, 2nd floor south door, PPV fan

*Not reported because propane flow rate was not accurately measured during tests

3.1 East Structure Tests

Five different tests, Tests 2–6, were conducted in the East Structure. Table 3.2 lists the heat release rates for Tests 5 and 6. The time between the ignition of each gas burner for Tests 5 and 6 was on the order of seconds. As a result, a single heat release rate, one for all three burners ignited, is reported.

Table 3.2: Heat Release Rates for Tests 5 and 6.

Test	Heat Release Rate (kW) All Burners On
Test 5 - Seq. 1	1190
Test 5 - Seq. 2	1190
Test 5 - Seq. 3	1190
Test 6 - Seq. 1	1190
Test 6 - Seq. 2	1190
Test 6 - Seq. 3	1180

3.1.1 Tests 2–4

Tests 2–4 followed a nearly identical order of events. Figure 3.1 includes a schematic floor plan and table of event times corresponding to the data files for each test. A 0.61 cm (2.0 ft) diameter PPV fan located 1.6 m (5.2 ft) away from the south exterior door was aimed at the center of the doorway and used after all burners were extinguished. During Tests 2–4, the south exterior door was not able to completely close due to an obstruction caused by the hoses used to transport the propane to the burners. So, when the south door was in the “closed” position, a 133 mm (5.25 in) opening was present between the door and its frame. For all other experiments, however, the south exterior door was not used and the doorway

remained closed for the entirety of the test. To fully close the doorway during these tests, the hinged door was removed and replaced by a piece of gypsum board that completely covered the doorway.

Event Times (sec) for Tests 2–4 Data Files

Event	Test 2	Test 3	Test 4
(1) Corner burner on	0	0	0
(2) Middle burner on	181	181	179
(3) Center burner on	361	361	360
(4) West double door opened	418	416	415
(5) East double door opened	538	536	535
(6) South exterior door opened	604	597	597
(7) Center burner off	720	778	778
(8) Middle burner off	840	898	897
(9) Corner burner off	961	1018	1019
(10) PPV fan on	1256	1316	1319
(11) PPV fan off	1892	N/A	1380
(12) PPV fan on	N/A	N/A	1487

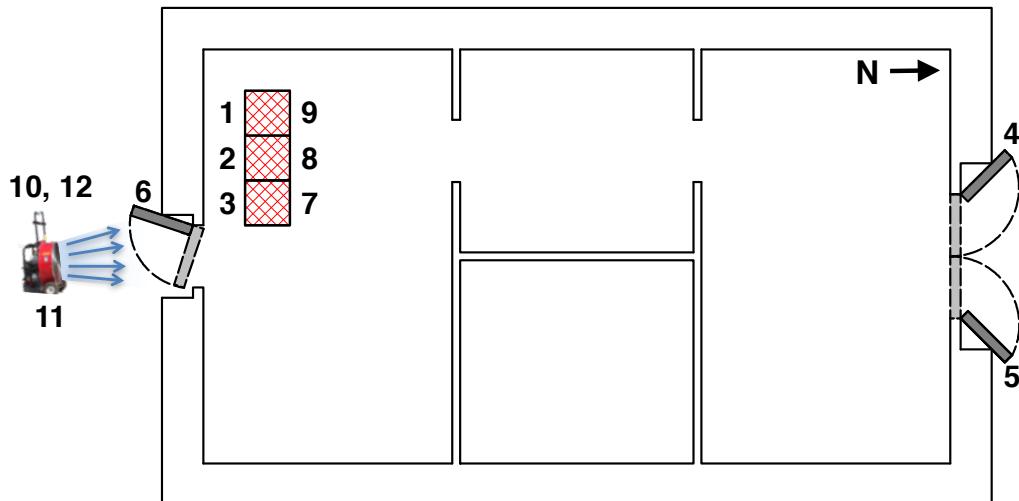


Figure 3.1: Tests 2–4 layout and event times.

3.1.2 Tests 5 & 6

The procedures for Tests 5 and 6 are outlined in Figures 3.2 and 3.3, respectively. Both tests involved repeating a specific set of events three times in a row. To avoid listing the identical actions three separate times in the “event” column of the tables, each repetition of events is denoted as a “sequence” (abbreviated as “seq.”), and each table contains three columns of times — one for each sequence.

Event Times (sec) for Test 5 Data File			
Event	Seq. 1	Seq. 2	Seq. 3
(1) All burners on	0	1225	2425
(2) Roof vent opened	154	1345	2545
(3) West double door opened	175	1432	2632
(4) East double door opened	361	1524	2730
(5) Roof vent closed	445	1723	2852
(6) All burners off	576	1840	2997
(7) Roof vent opened	720	1890	3086
(8) East double door closed	1148	2311	N/A
(9) West double door closed	1164	2330	N/A
(10) Roof vent closed	1179	2387	N/A

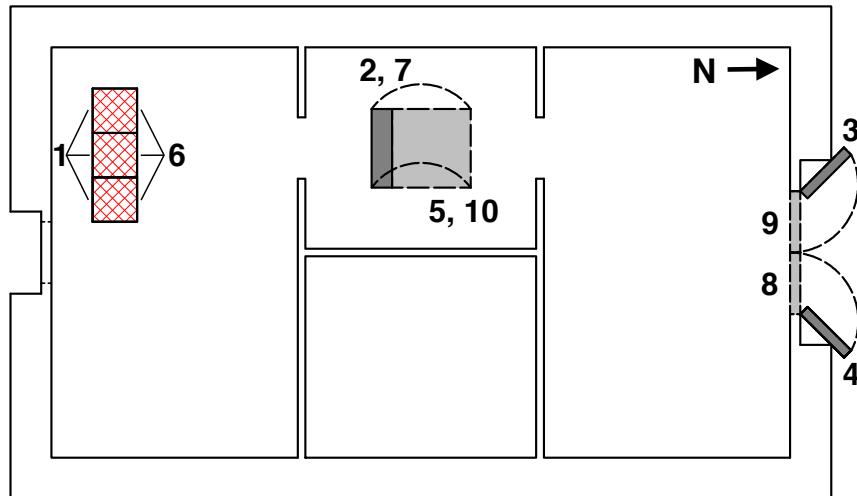


Figure 3.2: Test 5 layout and event times.

Event Times (sec) for Test 6 Data File

Event	Seq. 1	Seq. 2	Seq. 3
(1) All burners on	0	565	1075
(2) West double door opened	116	685	1195
(3) Roof vent opened	207	747	1287
(4) All burners off	327	868	1387
(5) East double door opened	369	911	1446
(6) Roof vent closed	494	1040	N/A
(7) East double door closed	522	1012	N/A
(8) West double door closed	538	1025	N/A

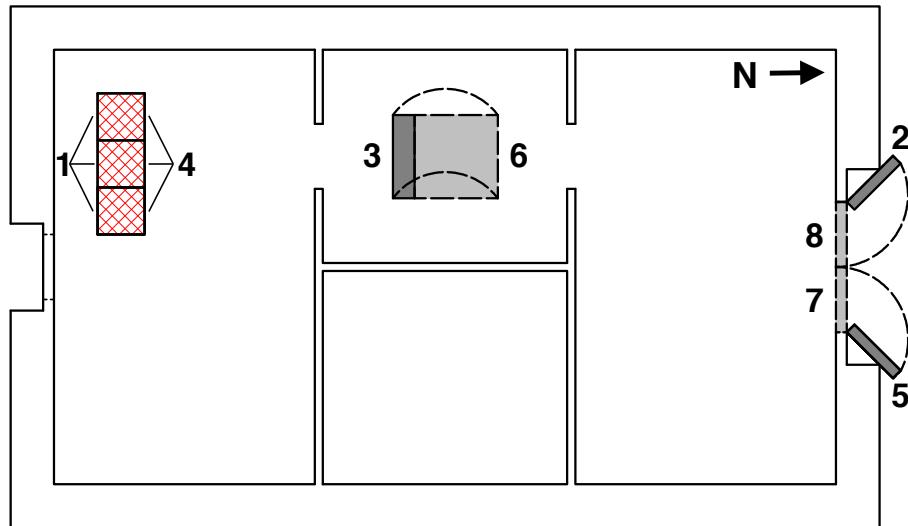


Figure 3.3: Test 6 layout and event times.

3.2 West Structure Tests

Four of the gas burner experiments, Tests 22–25, were conducted in the West Structure. Table 3.3 lists the calculated heat release rate for each test. Similar to Tests 5 and 6, Tests 22–25 had a duration on the order of seconds between the ignition of each burner, so only the heat release rate for all three burners is reported.

Table 3.3: Heat Release Rates for Tests 22–25.

Test	Heat Release Rate (kW) All Burners On
Test 22	1240
Test 23	1290
Test 24	1270
Test 25	1270

3.2.1 Tests 22 & 23

Tests 22 and 23 followed nearly identical procedures. The starting configuration for Test 22 had the second-story, south exterior door in the opened position, while the starting configuration for Test 23 had the same door in the closed position. Figure 3.4 includes a floor plan schematic and table of event times corresponding to the data files for Tests 22 and 23. A 0.61 m (2.0 ft) diameter PPV fan located 2.3 m (7.5 ft) away from the first level double doors and aimed at the center of the two doors was used towards the end of both tests.

Event Times (sec) for Tests 22–23 Data Files

Event	Test 22	Test 23
(1) All burners on	0	0
(2) 2nd floor west double door opened	194	130
(3) 1st floor west double door opened	314	252
(4) 1st floor east double door opened	450	371
(5) 2nd floor south exterior door closed	511	N/A
(6) 2nd floor east double door opened	585	498
(7) PPV fan on	652	612
(8) PPV fan off	798	761
(9) All burners off	829	794
(10) 2nd floor south exterior door opened	899	849
(11) PPV fan on	1065	940
(12) 2nd floor south exterior door closed	1176	N/A

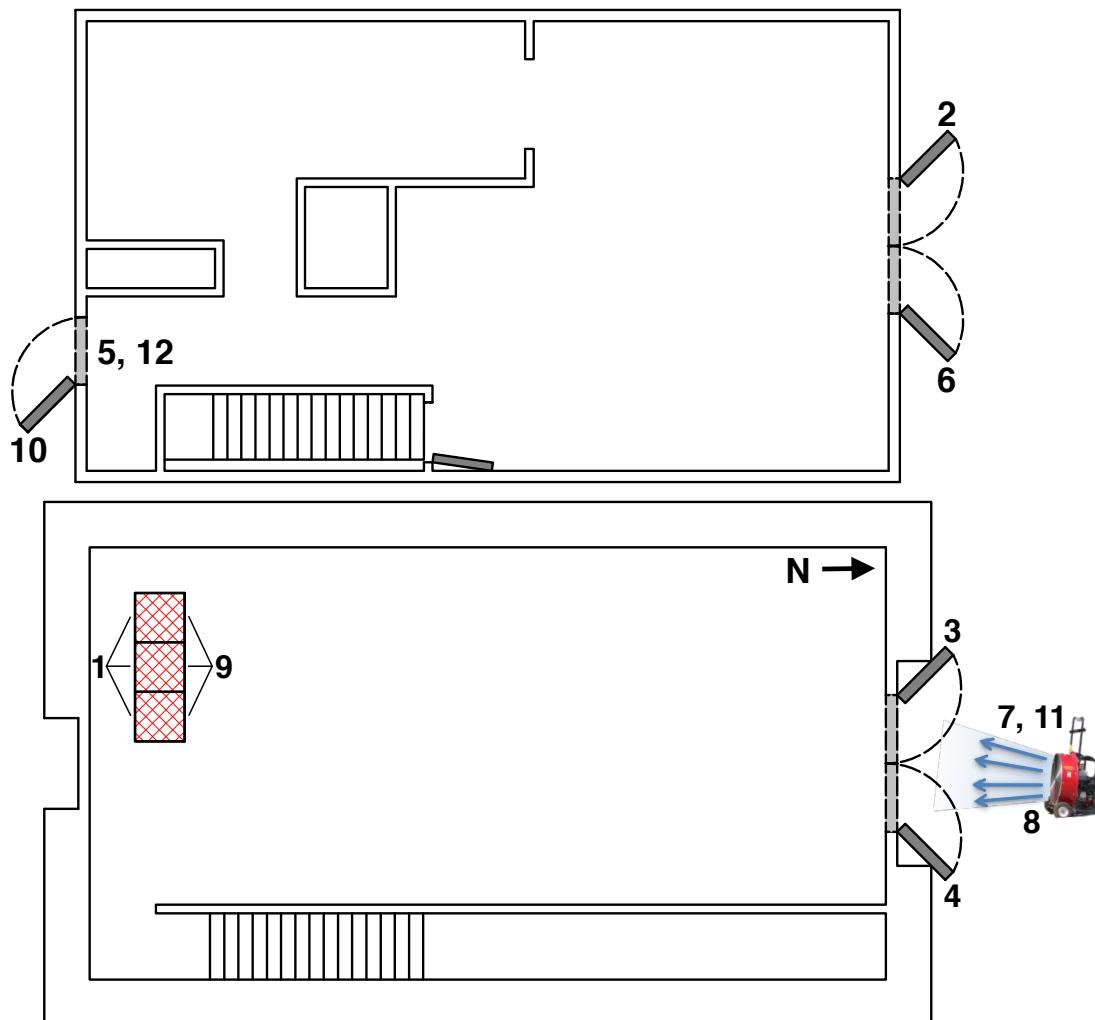


Figure 3.4: Tests 22–23 layout and event times.

3.2.2 Tests 24 & 25

As with Tests 22 and 23, Tests 24 and 25 followed a nearly identical procedure. The starting configuration for Test 24 had the south exterior door on the second level in the opened position, while the starting configuration for Test 25 had the same door in the closed position. During both tests, the stairwell door was unable to completely close. When it was in the “closed” position at the beginning of each test, there was a 152 mm (6.0 in) gap between the door and its frame. Figure 3.5 includes a floor plan schematic and table of event times corresponding to the data files for Tests 24 and 25. A 0.61 m (2.0 ft) diameter PPV fan located 2.3 m (7.5 ft) away from the first level double doors and aimed at the center of the west double door was used towards the end of both tests.

Event Times (sec) for Tests 24–25 Data Files

Event	Test 24	Test 25
(1) All burners on	0	0
(2) Interior stairwell door opened	144	112
(3) 1st floor west double door opened	265	244
(4) 2nd floor west double door opened	383	353
(5) 2nd floor south exterior door closed	452	N/A
(6) 2nd floor south exterior door opened	502	474
(7) PPV fan on	624	594
(8) All burners off	746	721
(9) 2nd floor east double door opened	877	N/A
(10) 1st floor east double door opened	N/A	836

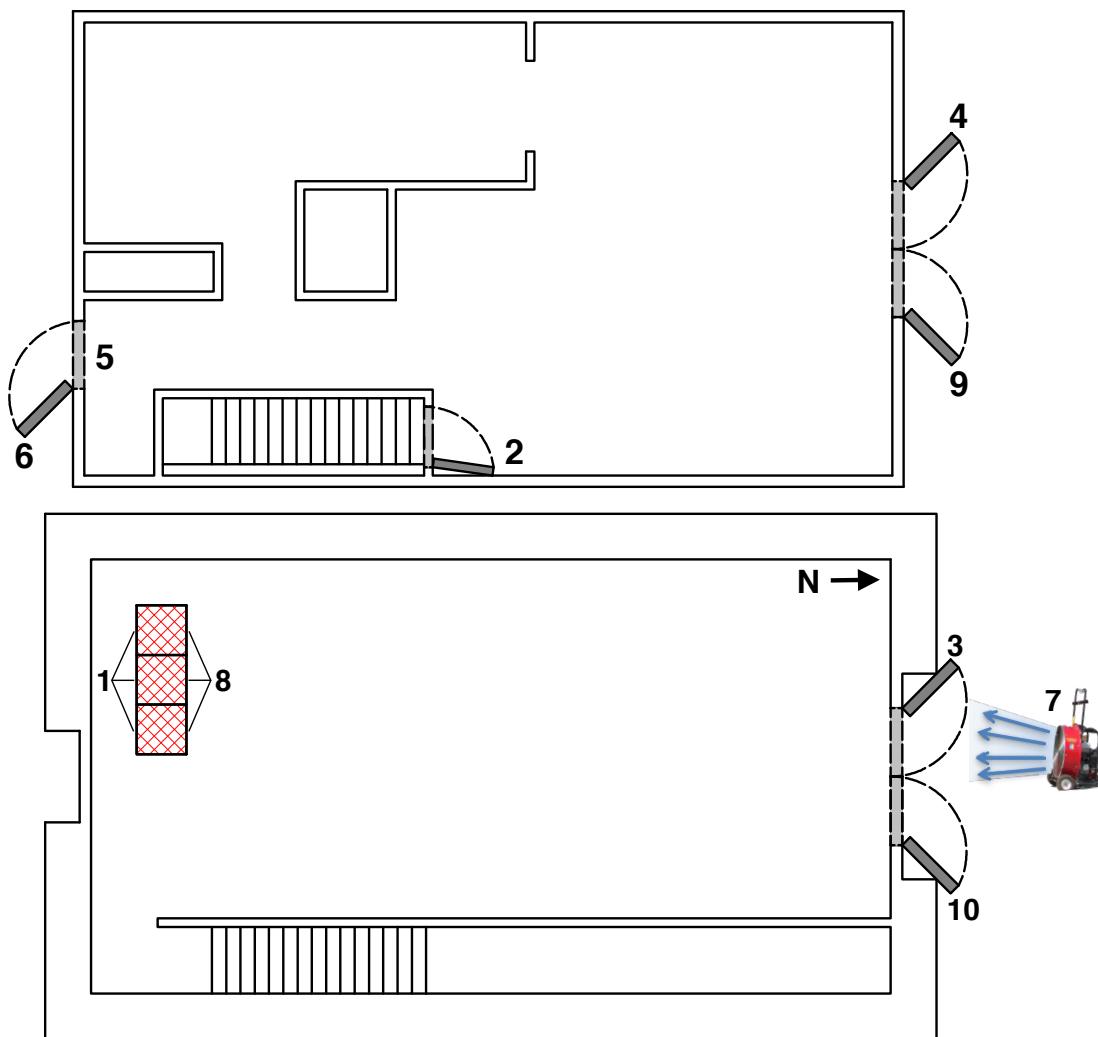


Figure 3.5: Tests 24–25 layout and event times.

Chapter 4: Numerical Model Description

Fire Dynamics Simulator (version 6.5.3) [1], a CFD model of thermally-driven fluid flow that is developed and maintained by NIST, was used to model the burner experiments described in Chapter 3. FDS numerically solves a form of the Navier-Stokes equations for low-speed ($Ma < 0.3$), fire-driven flows with an emphasis on smoke and heat transport from fires. The FDS Technical Reference Guide [2] provides a complete description of the model, including the formulation of the equations and numerical algorithm utilized by the software. FDS is mathematically verified [3] and validated against a continually growing database of experimental data from different fire scenarios [4].

FDS performs calculations within a computational domain that is composed of rectilinear volumes called meshes. Each mesh is divided into three-dimensional rectangular computational cells. Using the laws of mass, momentum, and energy conservation, FDS calculates the gas density, velocity, temperature, pressure, and species concentration within each grid cell and determines the generation and movement of fire gases within the domain. In general, the number of cells within each mesh (i.e., the grid cell size) determines the resolution of the mesh: the smaller the size of the cells, the higher the resolution of the simulation. However, increasing the

resolution of a simulation increases the need for more computational resources and produces a longer simulation run time. Thus, it's critical to determine a proper grid cell size for the meshes within an FDS computational domain based on available resources and desired level of model fidelity. In order to select an appropriate cell size for the simulations of the gas burner experiments, a mesh sensitivity analysis, described in Section 4.1.1, was performed.

In addition to defining the meshes and cells within the computational domain, other types of input data must be known and considered to properly formulate a fire model. Key input parameters that were specified within the FDS input files and additional characteristics of the model setup are described throughout the sections of this chapter.

4.1 Computational Domain

The computational domain for the East Structure simulations was set to span 14 m in the x direction, 8 m in the y direction, and 3 m in the z direction, and the computational domain for the West Structure simulations spanned 14 m in the x direction, 8 m in the y direction, and 5.4 m in the z direction. Each structure was centered between the x and y boundaries of its respective domain, and the ground of the first floor was set at $z = 0$ m. The structures were modeled based on the dimensions shown in the floor plan drawings presented in Figures 2.3 and 2.4 of Chapter 2.

The entire computational domain for each simulation was divided into eight

different meshes to utilize the Message-Passing Interface (MPI) feature of FDS that allows multiple computers, or multiple cores on one computer, to run a multi-mesh FDS job with each mesh as its own process. All simulations were executed by utilizing MPI parallel processing on a multi-processor Linux machine.

4.1.1 Numerical Mesh

According to the FDS User Guide, a measure of how well the flow field is resolved for a simulation involving buoyant plumes is provided by the result of the expression $D^*/\delta x$, known as the resolution index (RI), in which D^* is the characteristic fire diameter defined as

$$D^* = \left(\frac{\dot{Q}}{\rho_\infty c_p T_\infty \sqrt{g}} \right)^{2/5} \quad (4.1)$$

where \dot{Q} is the total heat release rate of the fire (kW), δx is the nominal size of each grid cell (m), ρ_∞ is the density (kg/m^3) of the surrounding gas (air), c_p is the specific heat ($\text{kJ}/(\text{kg}\cdot\text{K})$) surrounding air, T_∞ is the temperature (K) surrounding air, and g is gravity (m/s^2).

To determine the grid cell size to prescribe the meshes within the model simulations, a mesh sensitivity study was performed for the Test 4 simulation in the East Structure and the Test 25 simulation in the West Structure. Tests 4 and 25 were selected for the analysis because they have shorter durations compared to other East Structure and West Structure experiments. Three different grid cell sizes corresponding to the coarse, medium, and fine meshes were used in the mesh sensitivity

study: 14 cm, 10 cm, and 5 cm for the East Structure and 7 cm for the West Structure, respectively. These corresponded to RI values ranging from 5–7 for the coarse grid, 8–11 for the medium grid, and 15–20 for the fine grid. Previous FDS validation work from the U.S. Nuclear Regulatory Commission suggests that RI values from 4 to 16 generated adequate results in terms of engineering calculations [18].

The characteristic fire diameter (and thus, the RI values) were similar for all nine FDS simulations, so the results from the mesh sensitivity analysis of one simulation was used to determine and justify the grid cell size for all burner experiment simulations conducted within the same structure. From the analysis, it was determined that a cell size of 10 cm (medium mesh) was appropriate for all nine simulations. This cell size results in a domain with 336,000 computational grid cells for the East Structure and a domain with 604,800 computational grid cells for the West Structure. The results of the sensitivity study are presented and discussed in Section 5.1 of Chapter 5.

As previously mentioned, the computational domain was divided into eight equally sized meshes. The first mesh was defined by the **MESH** namelist group and was assigned a **MULT_ID** quantity corresponding to a multiplier utility defined by the **MULT** namelist group. For example, the mesh in the Test 2 input file was defined by the following

```
&MESH IJK=35,40,30, XB=-1.5,2.0,-0.8,3.2,0.0,3.0,  
      MULT_ID='mesh' /
```

with the assigned **MULT_ID** defined as

```
&MULT ID='mesh', DX=3.5, DY=4.0, I_UPPER=3, J_UPPER=1 /
```

This creates an array of eight meshes with identical z_1 and z_2 bounds from 0.0 to 3.0 and x_1 , x_2 , y_1 , y_2 bounds that vary according to the following:

$$x_1' = -1.5 + 3.5i \quad \text{for } 0 \leq i \leq 3$$

$$x_2' = 2.0 + 3.5i \quad \text{for } 0 \leq i \leq 3$$

$$y_1' = -0.8 + 4j \quad \text{for } 0 \leq j \leq 1$$

$$y_2' = 3.2 + 4j \quad \text{for } 0 \leq j \leq 1$$

where i and j are integers.

4.2 Source Fire Characterization

Each propane burner in the simulations was modeled as having steel sides and a 0.6 m x 0.6 m surface located 0.1 m above the ground with a specified mass flux ($\text{kg}/(\text{m}^2\text{s})$) of propane in the positive z direction corresponding to the burner's heat release rate. In order to provide an example of the exact lines that were included in the input files to define the burners and propane fires in this manner, the following lines defined the surfaces with specified propane mass fluxes corresponding to the heat release rate of each burner in the Test 2 FDS input file:

```
&SURF ID='BURNER 1', MASS_FLUX(1)=0.0264, SPEC_ID(1)='PROPANE',
COLOR='RED', RAMP_MF(1)='burner1', TMP_FRONT=500. /
&SURF ID='BURNER 2', MASS_FLUX(1)=0.0246, SPEC_ID(1)='PROPANE',
COLOR='RED', RAMP_MF(1)='burner2', TMP_FRONT=500. /
```

```

&SURF ID='BURNER 3', MASS_FLUX(1)=0.0060, SPEC_ID(1)='PROPANE',
      COLOR='RED', RAMP_MF(1)='burner3', TMP_FRONT=500. /

```

Additionally, the following lines were used in the Test 2 input file to define each gas burner as having steel sides and a top surface with the specified propane mass flux from above:

```

&OBST XB= 0.60, 1.20, 4.90, 5.50, 0.00, 0.10,
      SURF_IDS='BURNER 1','STEEL PLATE','STEEL PLATE' /

&OBST XB= 0.60, 1.20, 4.30, 4.90, 0.00, 0.10,
      SURF_IDS='BURNER 2','STEEL PLATE','STEEL PLATE' /

&OBST XB= 0.60, 1.20, 3.70, 4.30, 0.00, 0.10,
      SURF_IDS='BURNER 3','STEEL PLATE','STEEL PLATE' /

&OBST XB= 0.60, 0.60, 3.70, 5.50, 0.10, 0.20,
      SURF_ID='STEEL PLATE' /

&OBST XB= 1.20, 1.20, 3.70, 5.50, 0.10, 0.20,
      SURF_ID='STEEL PLATE' /

&OBST XB= 0.60, 1.20, 3.70, 3.70, 0.10, 0.20,
      SURF_ID='STEEL PLATE' /

&OBST XB= 0.60, 1.20, 5.50, 5.50, 0.10, 0.20,
      SURF_ID='STEEL PLATE' /

```

The heat release rates listed in Table 3 from Chapter 3 were used to determine the values of propane mass flux to prescribe to the burners defined in the FDS input files for Tests 5–6 and Tests 22–25. The propane mass flux, $\dot{m}_{C_3H_8}''$, was calculated

using the equation

$$\dot{m}_{C_3H_8}'' = \frac{\dot{Q}}{A\Delta h_c} \quad (4.2)$$

in which \dot{Q} is the burner heat release rate; A is the area of the top surface of the burner, 0.36 m^2 for all burners; and Δh_c is the effective heat of combustion of the fuel (propane), which was taken to be 46334.6 kJ/kg [REF?].

As mentioned in Chapter 3, the rate of propane flow to the burners was not able to be accurately measured during Tests 2–4. Instead, the heat release rates prescribed to the simulations of Tests 2–4 during the periods in which one, two, and three burners were ignited were estimated using the hot gas layer (HGL) temperature of the fire room during each period in conjunction with the following correlation derived by McCaffrey, Quintiere, and Harkleroad (MQH) for compartment fires [19]:

$$T_g = 6.85 \left(\frac{\dot{Q}^2}{A_0 \sqrt{H_0} h_k A_T} \right)^{1/3} + T_\infty \quad (4.3)$$

$$\Rightarrow \dot{Q} = \left[A_0 \sqrt{H_0} h_k A_T \left(\frac{T_g - T_\infty}{6.85} \right)^3 \right]^{1/2}$$

where \dot{Q} is the heat release rate of the fire (kW), A_0 is the area of the compartment opening (m^2), H_0 is the height of the compartment opening (m), h_k is the effective heat transfer coefficient ($\text{kW}/(\text{m}^2\text{K})$), A_T is the total area of the compartment enclosing surfaces (m^2), T_g is the temperature of the upper gas layer (K), and T_∞ is the ambient temperature (K). The HGL temperatures of the fire room were calculated using the experimental data from the thermocouple arrays in the fire room (A1 and A2). The exact methodology of obtaining the hot gas layer temperature from the

thermocouple data is outlined in Chapter 5.

Using Equation 4.3, the heat release rates for the periods with one, two, and three burners ignited were estimated and used to determine the propane mass flux value of each burner surface in the FDS input files for Tests 2–4. Table 4.1 lists the heat release rates obtained from this method, rounded to the nearest 10 kW.

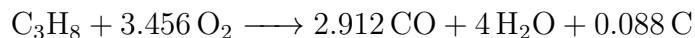
Table 4.1: Tests 2–4 Heat Release Rates (kW) Estimated using the Average Hot Gas Layer Temperature and MQH Correlation.

Test #	1 Burner Ignited	2 Burners Ignited	3 Burners Ignited
2	440	850	950
3	520	940	1110
4	550	970	1130

The reaction mechanisms for combustion in all simulations were modeled using the default mixing-controlled, simple chemistry model (reaction rate is infinite and limited only by species concentrations) and were specified via the following code:

```
&REAC ID = 'R1'
FUEL = 'PROPANE'
SPEC_ID_NU='PROPANE','OXYGEN','CARBON MONOXIDE',
'WATER VAPOR','SOOT'
NU= -1,-3.456,2.912,4.0,0.088
```

which corresponds to the following single-step reaction mechanism for propane:



Additionally, the production of carbon dioxide was tracked via

```

&REAC ID = 'R2'

FUEL = 'CARBON MONOXIDE'

SPEC_ID_NU='CARBON MONOXIDE', 'OXYGEN', 'CARBON DIOXIDE'

NU= -1,-0.5,1

RADIATIVE_FRACTION=0.30

```

and nitrogen was set as the background species. Note, FDS has built-in properties for a number of different fuels, including PROPANE and CARBON MONOXIDE. Therefore, it was not necessary to explicitly list thermophysical properties for the prescribed fuels. Finally, because of the presence of multiple chemical reactions, gas phase combustion was eliminated by setting SUPPRESSION=.FALSE. on the MISC line.

4.3 Additional Input Parameters

In addition to those already presented in the previous sections, a variety of other parameters were specified within the simulation input files. These include the ambient temperature, timing information, thermophysical properties of materials that weren't already predefined by FDS, leakage associated with the structure, and the different devices to model the various types of instrumentation used during the physical experiments.

The ambient temperature was explicitly set in each input file based on the average temperature throughout the test structure before ignition, which was obtained by averaging the temperatures measured by the thermocouple arrays throughout the structure at the start of the test. The average ambient temperatures ranged from

35 °C to 62 °C. The variation in ambient temperatures is a result of the fact that some of the burner tests were conducted shortly after another fire experiment in the same structure, so significant residual heat from the first test was present within the structure at the start of the next test.

The timing information specified within the FDS input files consisted of the simulation run time and event times listed in the tables presented with Figures 3.1–3.5 in Chapter 3. The vents were modeled by first defining a hole via the HOLE namelist group at the location of the vent, setting an obstruction via the OBST namelist group to cover the hole at the start of the simulation, and assigning a control to the obstruction using the CTRL namelist group. The control was set to a timer defined by the DEVC namelist group and used a ramp function defined by the RAMP namelist group to change the PERMIT_HOLE value for the obstruction from .FALSE. to .TRUE. at the time of the vent opening. For example, the following lines were included within the Test 2 FDS input file to initially define the north side, east double door as closed and then opened at 538 s:

```
&HOLE XB=10.99,11.11, 2.10, 3.00, 0.00, 2.00  
  / Cut-out for North-East Door  
  
&OBST XB=11.00,11.10, 2.10, 3.00, 0.00, 2.00, SURF_ID='DOOR',  
  PERMIT_HOLE=.FALSE., CTRL_ID='east controller'  
  / North-East Door  
  
&CTRL ID='east controller', FUNCTION_TYPE='CUSTOM',  
  INPUT_ID='east timer', RAMP_ID='east cycle' /
```

```

&DEVC ID='east timer', QUANTITY='TIME', XYZ=0,0,0 /
&RAMP ID='east cycle', T= 0., F= 1 /
&RAMP ID='east cycle', T= 537., F= 1 /
&RAMP ID='east cycle', T= 538., F=-1 /

```

Four materials were explicitly defined via the **MATL** namelist group to assign to different surfaces within the simulation input files. The specific heat, thermal conductivity, and density of each material was defined by assigning appropriate values to the **SPECIFIC_HEAT** (kJ/(kg·K)), **CONDUCTIVITY** (W/(m·K)), and **DENSITY** (kg/m³) parameters within the corresponding **MATL** namelist group. For example, concrete was defined by the lines

```

&MATL ID          = 'CONCRETE'
CONDUCTIVITY    = 1.75
SPECIFIC_HEAT   = 1.04
DENSITY         = 2200. /

```

A complete list of the explicitly defined materials and their properties are listed in Table 4.2.

Table 4.2: Various Materials Defined Within Each FDS Input File and the Corresponding MATL Namelist Group Parameter Values.

Material ID	Reference	SPECIFIC_HEAT (kJ/(kg·K))	CONDUCTIVITY (W/(m·K))	DENSITY (kg/m ³)
Steel	[20]	0.48	62.0	7850
Gypsum	[20]	0.90	0.16	770
Concrete	[20]	1.04	1.75	2200
Fiber Cement	[21]	1.0	0.15	1300

The materials in Table 4.2 were explicitly specified within the FDS input files to ensure that the solid boundary surfaces throughout the model were properly defined as described in Chapter 2. For example, based on the description of the exterior walls from Chapter 2:

“The first floor of each structure had outer walls composed of interlocking concrete blocks measuring 0.6 m (2.0 ft) wide... Two layers of 16 mm (0.63 in) Type X gypsum board lined the steel studs, and a layer of 13 mm (0.5 in) thick Durock cement board covered the gypsum board.”

the surface of the exterior walls were defined in the FDS input file by the following lines:

```

&SURF_ID          = 'EXTERIOR WALL'
DEFAULT           = .TRUE.
RGB               = 150,150,150
MATL_ID           = 'FIBER CEMENT', 'GYPSUM', 'CONCRETE'
THICKNESS         = 0.013,0.03,0.610 /

```

To account for the structure leakage described in Chapter 2, the pressure

zone leakage approach outlined by the FDS User Guide [1] in which a leakage flow is computed via the program’s HVAC model to capture bulk leakage through structure walls was used. This approach involves defining a pressure zone using the ZONE namelist group and assigning a leakage area via the LEAK_AREA quantity of the zone.

Various instrumentation devices can be modeled within FDS through the DEVC namelist group. Different devices were specified in the FDS input files at the sensor locations described in Chapter 2. The QUANTITY parameter within the DEVC namelist group was set based on the type of sensor being modeled. Table 4.3 lists each type of sensor that was modeled, its corresponding QUANTITY parameter, and the combined uncertainty associated with the QUANTITY parameter as given by the FDS Validation Guide.

Table 4.3: Instrumentation Specified within FDS Input File and Corresponding DEVC Namelist Group Properties.

Instrumentation Type	Assigned QUANTITY	Combined Uncertainty
Thermocouple	'THERMOCOUPLE'	7 %
Gas Concentration	'VOLUME FRACTION'	8 %
BDP	'VELOCITY'	8 %
Heat Flux Gauge	'GAUGE HEAT FLUX'	11 %

Chapter 5: Results and Discussion

Three different types of figures are presented in this chapter to assist with the discussion of the results. One type is presented with the discussion of the mesh sensitivity study results that were used to select an appropriate grid cell size for the simulations. The other two types are presented throughout the comparison of the predicted data output by the FDS simulations to the corresponding experimental data.

5.1 Mesh Sensitivity Studies

Figures 5.1–5.4 show the oxygen volume fractions and ceiling jet temperatures output by FDS simulations of Test 4 and Test 25 using the coarse, medium, and fine grid sizes across the computational domain.

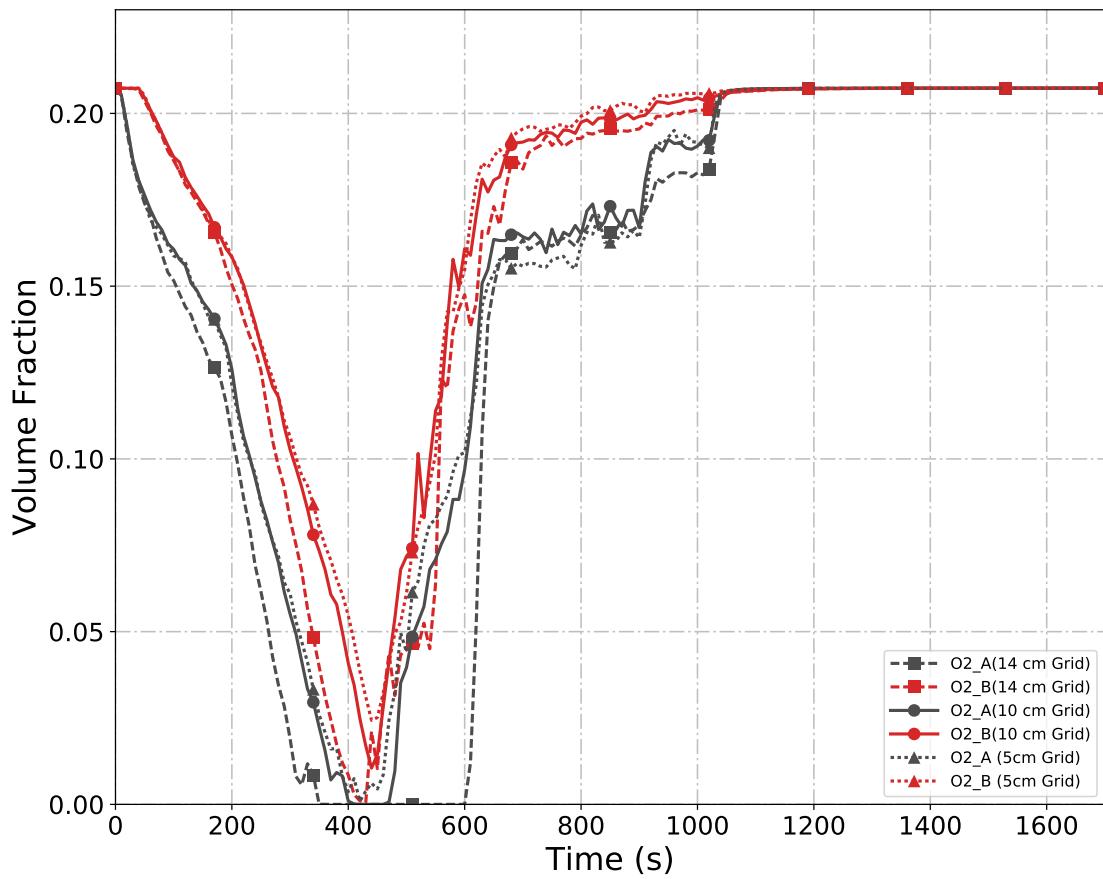


Figure 5.1: O_2 concentrations output by the FDS simulation of Test 4 in the East Structure using three different grid cell sizes.

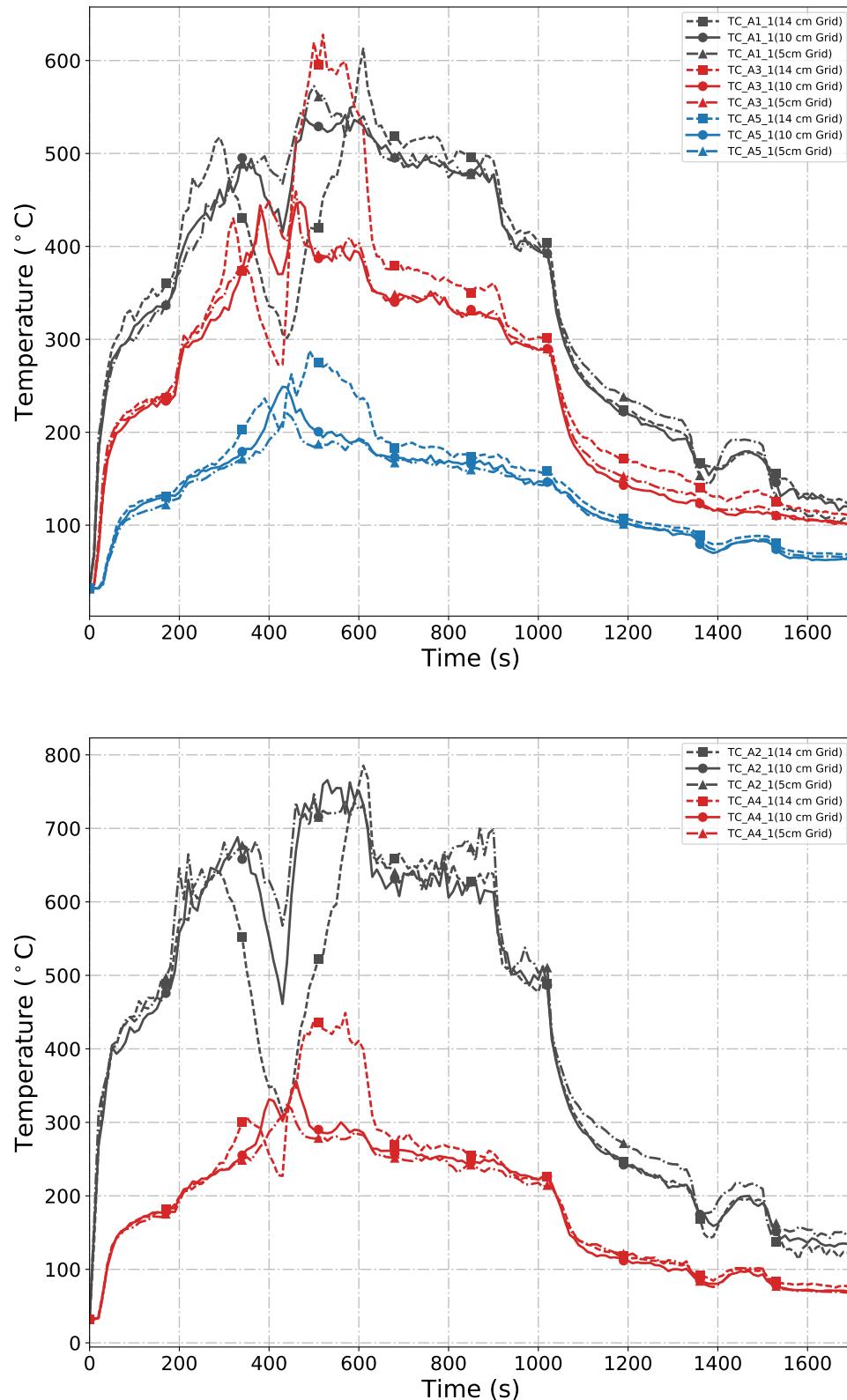


Figure 5.2: Ceiling jet temperatures output by the FDS simulation of Test 4 in the East Structure using three different grid cell sizes.

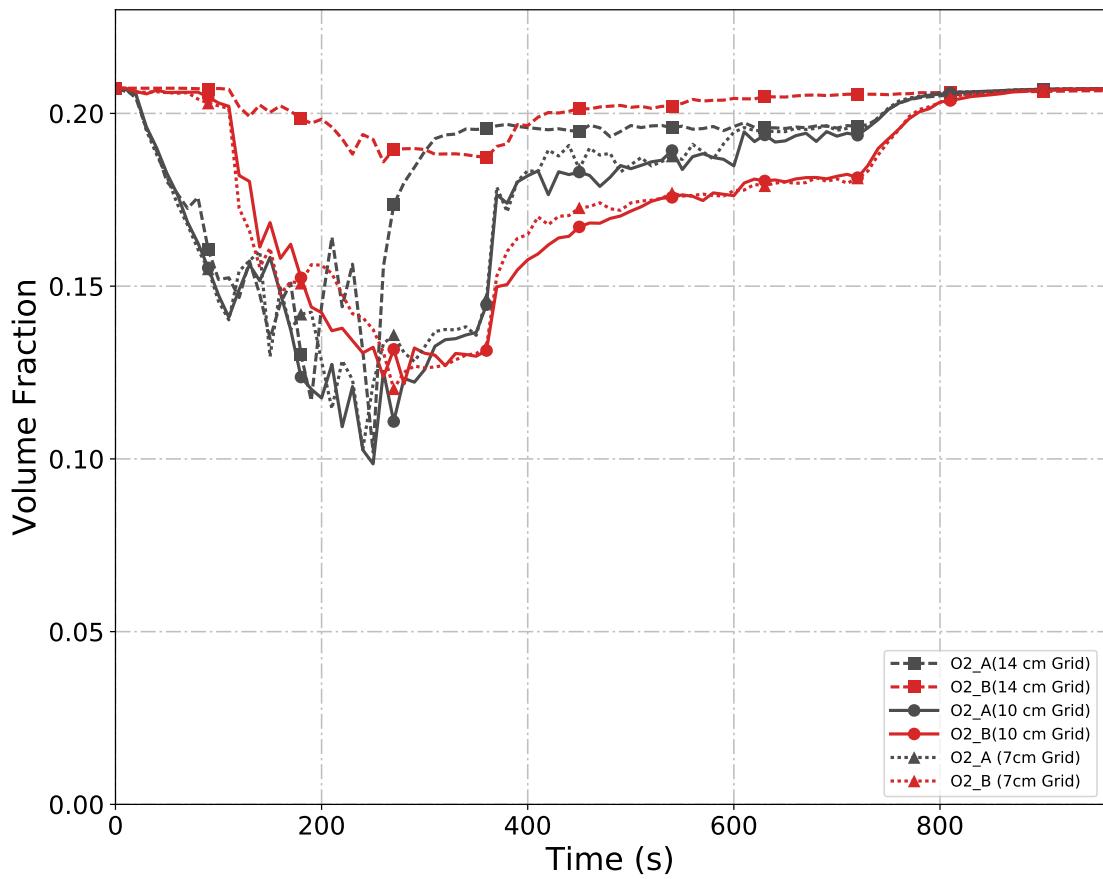


Figure 5.3: O_2 concentrations output by the FDS simulation of Test 25 in the West Structure using three different grid cell sizes.

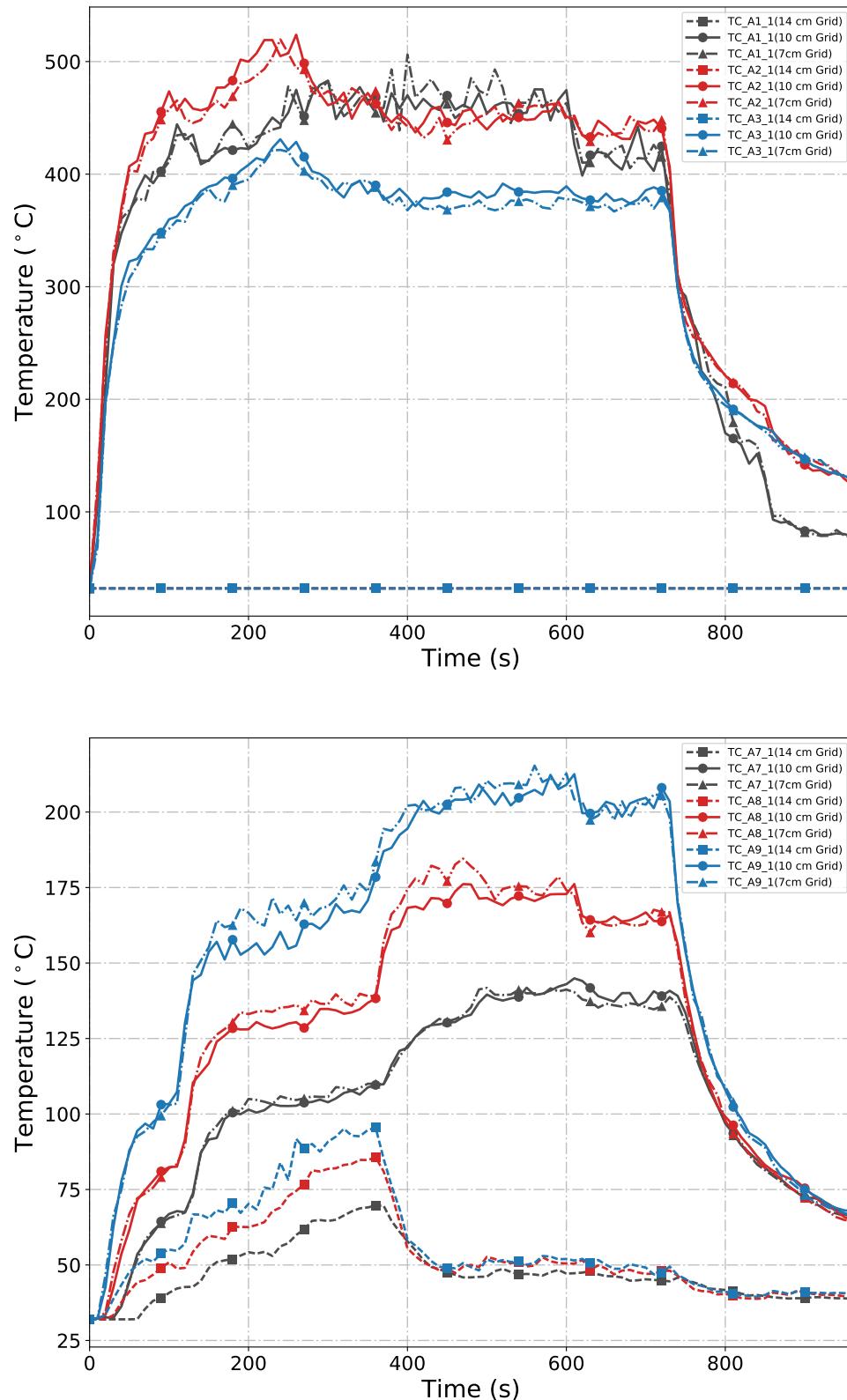


Figure 5.4: Ceiling jet temperatures output by the FDS simulation of Test 25 in the West Structure using three different grid cell sizes.

The plots presented above show that significant differences occur at various times between the model data produced using the coarse grid and the same model data produced using the medium and fine grid resolutions. For example, looking at Figure 5.3, the oxygen volume fraction data on the first floor of the West Structure output by the coarse grid deviates significantly from the data produced by medium and fine grid sizes around 300 seconds. Furthermore, the oxygen volume fraction data on the second floor output using the coarse grid drops to a minimum of approximately 0.18 during the portion of the simulation in which the burners are ignited, while the volume fraction data output using the medium and fine grids drop to a similar minimum that is around 0.13.

Looking at the oxygen volume fraction and ceiling jet temperature data output by the East Structure simulation, Figures 5.1 and 5.2, respectively, for different mesh resolutions, the data from the coarse grid exhibits more agreement with the medium and fine grid data than the West Structure simulation data plots. However, significant differences still arise between the coarse grid data and the simulation data produced by the medium and fine resolutions, such as the larger decline in ceiling jet temperature seen around 400 seconds.

Due to the large discrepancies between the coarse grid data and the data produced by the other two mesh resolutions, the coarse grid was considered too coarse for all simulations of the burner experiments. However, there doesn't appear to be any significant differences between the simulation data produced by the medium mesh resolution and the simulation data produced by the fine mesh resolution. As a result, the medium grid cell size of 10 cm was selected for all nine FDS simulations.

5.2 FDS Model Data Compared to Experimental Data

In the following subsections, the temperature, gas species concentration, gas velocity, and heat flux measurements predicted by the FDS simulations are compared to the corresponding sensor data measured during the propane burner experiments. Two different types of graphs are included to aid in the comparison of the model data and experimental data. The first type is similar to the mesh sensitivity study figures in that it shows the simulation data and experimental data (time-averaged over 10 seconds) plotted over the duration of an experiment for a specific data type at a specific location(s). Only one plot is presented for each discussed data quantity; the remaining figures of the discussed data types plotted over the duration each experiment for the different measurement locations are included in Appendix B.

The second type of figure presented with each data quantity discussion summarizes the model uncertainty in predicting the specific data quantity. The summary graphs are similar to those presented in the FDS Validation Guide [4] — each is a log/log scatter plot in which the x value of each point is based on a set of measured, experimental data and the y value of each point is based on the equivalent set of predicted data from the FDS simulation. No data from Tests 2–4 were used to generate the summary scatter plots because the heat release rates prescribed to the FDS simulations of the tests were determined through the use of a correlation (MQH) based on the experimental temperature data instead of through a direct physical measurement, such as the flow rate of propane to the burners used to determine the prescribed heat release rates for the other six simulations. The procedure used to

generate the scatter plots and statistical data is briefly outlined below. Full details of the analysis are described in detail in by McGrattan and Toman in Ref. [22].

Taking M_i and E_i to represent the change in the value of a quantity from its ambient at a specific time based on the data output by the FDS simulation and measured by instrumentation during the experiment, respectively, the mean and standard deviation of the distribution can be estimated by first calculating

$$\overline{\ln(M/E)} = \frac{1}{n} \sum_{i=1}^n \ln\left(\frac{M_i}{E_i}\right) \quad (5.1)$$

Note, the natural logarithm function is used so that the variance of the random variable can be expressed in terms of the relative uncertainty. The assumption that $\ln(M/E)$ is normally distributed has been tested for each data type of interest by the developers of FDS, and the results are shown in the FDS Validation Guide. The standard deviation of the logarithm of a normally distributed random variable is approximately equal to the standard deviation divided by its mean, the relative standard deviation. The least squares estimate of the standard deviation of the combined distribution is defined as:

$$\tilde{\sigma}_m^2 + \tilde{\sigma}_E^2 \approx \frac{1}{n-1} \sum_{i=1}^n \left[\ln(M_i/E_i) - \overline{\ln(M/E)} \right]^2 \quad (5.2)$$

Using the pair of measured and predicted values with the known $\tilde{\sigma}_E$, the expression on the right can be evaluated. Eq. 5.2 imposes a constraint on the experimental uncertainty value, $\tilde{\sigma}_E$, and in combination with a second constraint that $\tilde{\sigma}_M$ cannot

be less than $\tilde{\sigma}_E$ because it's impossible to show that the model is more accurate than the measurements against which it's compared, the following is produced:

$$\tilde{\sigma}_E^2 \leq \frac{1}{2} \text{Var}(\ln(M/E)) \quad (5.3)$$

Using the mean of the distribution, an estimate of a bias factor, δ , which expresses the tendency of the model to over or under-predict the measured quantity, can be found:

$$\delta \approx \exp \left(\overline{\ln(M/E)} + \frac{\tilde{\sigma}_M^2}{2} - \frac{\tilde{\sigma}_E^2}{2} \right) \quad (5.4)$$

The values of δ , σ_M , and σ_E are reported with each log/log plot in the following sections. For each plot, the solid red line and solid black line represent the expected values for M and E , respectively, and the dashed lines represent $\pm\sigma$, or standard deviations, of the data corresponding to the line color. Each plotted gray point represents an average value of the specific data quantity across a 30 second test period in which one or more gas burners were ignited and only natural ventilation was present throughout the structure (i.e., no PPV fan was turned on). All the points are based on computed values over the applicable time periods of Tests 5–6 and Tests 22–25. Table 5.1 in the final section of this chapter summarizes the statistical values calculated for each data type and is presented alongside a brief discussion of how the values compare to the same statistical values listed in the FDS Validation Guide.

5.2.1 Temperature

Hot Gas Layer

A quantity that is commonly estimated for compartment fire scenarios is the location of the interface between the hot, smoke-laden upper layer and cooler, lower layer. Some fire models, such as two-zone models, calculate this value directly, along with the average temperature of the upper (hot gas) layer and lower layer. Being that it's a CFD model, FDS computes a continuous profile of temperature and thus, does not directly calculate the interface location or the average temperature of each layer. However, numerous techniques exist to estimate the layer height and average temperatures from a continuous vertical profile of temperature. The temperatures measured by the thermocouples in the vertical arrays throughout the experimental structures were used to define a vertical profile of temperature, $T(z)$, in which z is the height above the floor ($z = 0$ at the floor and $z = H$ at the room's ceiling). Then, the vertical temperature profile was used to estimate the hot gas layer temperature by a method developed by Janssens and Tran [23]. Taking T_u as the upper layer temperature, T_l as the lower layer temperature, and z_{int} as the hot gas layer interface height, the method is outlined below, starting with the calculation of the quantities I_1 and I_2

$$I_1 = \int_0^H T(z)dz = (H - z_{int})T_u + z_{int}T_l$$

$$I_2 = \int_0^H \frac{1}{T(z)}dz = (H - z_{int})\frac{1}{T_u} + z_{int}\frac{1}{T_l}$$

I_1 and I_2 are then used to solve for z_{int} as follows

$$z_{int} = \frac{T_l(I_1 I_2 - H^2)}{I_1 + I_2 T_l^2 - 2T_l H} \quad (5.5)$$

T_l is the temperature in the lowest mesh cell (or thermocouple) and T_u is the average upper layer temperature defined by

$$(H - z_{int})T_u = \int_{z_{int}}^H T(z)dz \quad (5.6)$$

Figure 5.5 shows the hot gas layer temperature derived from experimental data plotted with the same quantity derived from the FDS simulation data for Test 22, and Figure 5.6 shows the log/log scatter plot of the hot gas layer temperatures obtained from the predicted data from the FDS simulations compared to the values obtained by the measured data for the six applicable gas burner experiments.

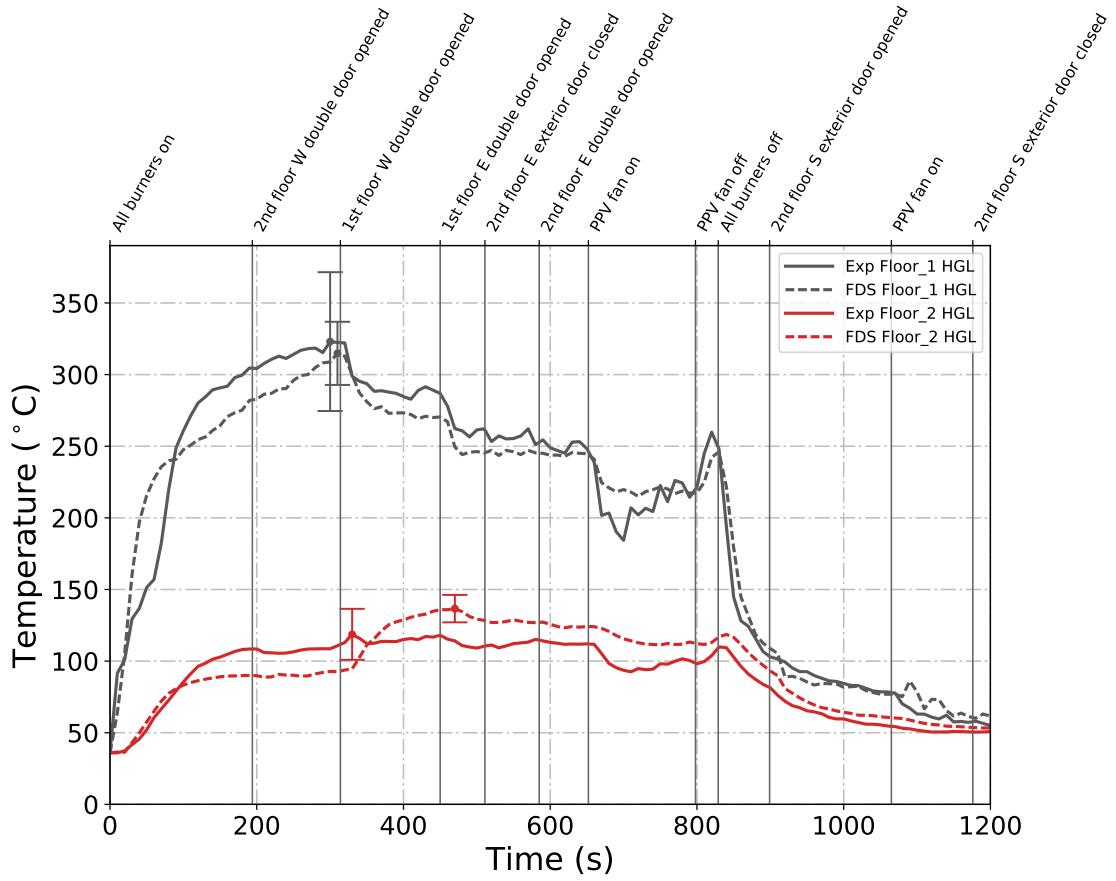


Figure 5.5: Plots of measured and predicted hot gas layer temperatures on the first and second floors of the West Structure during Test 22.

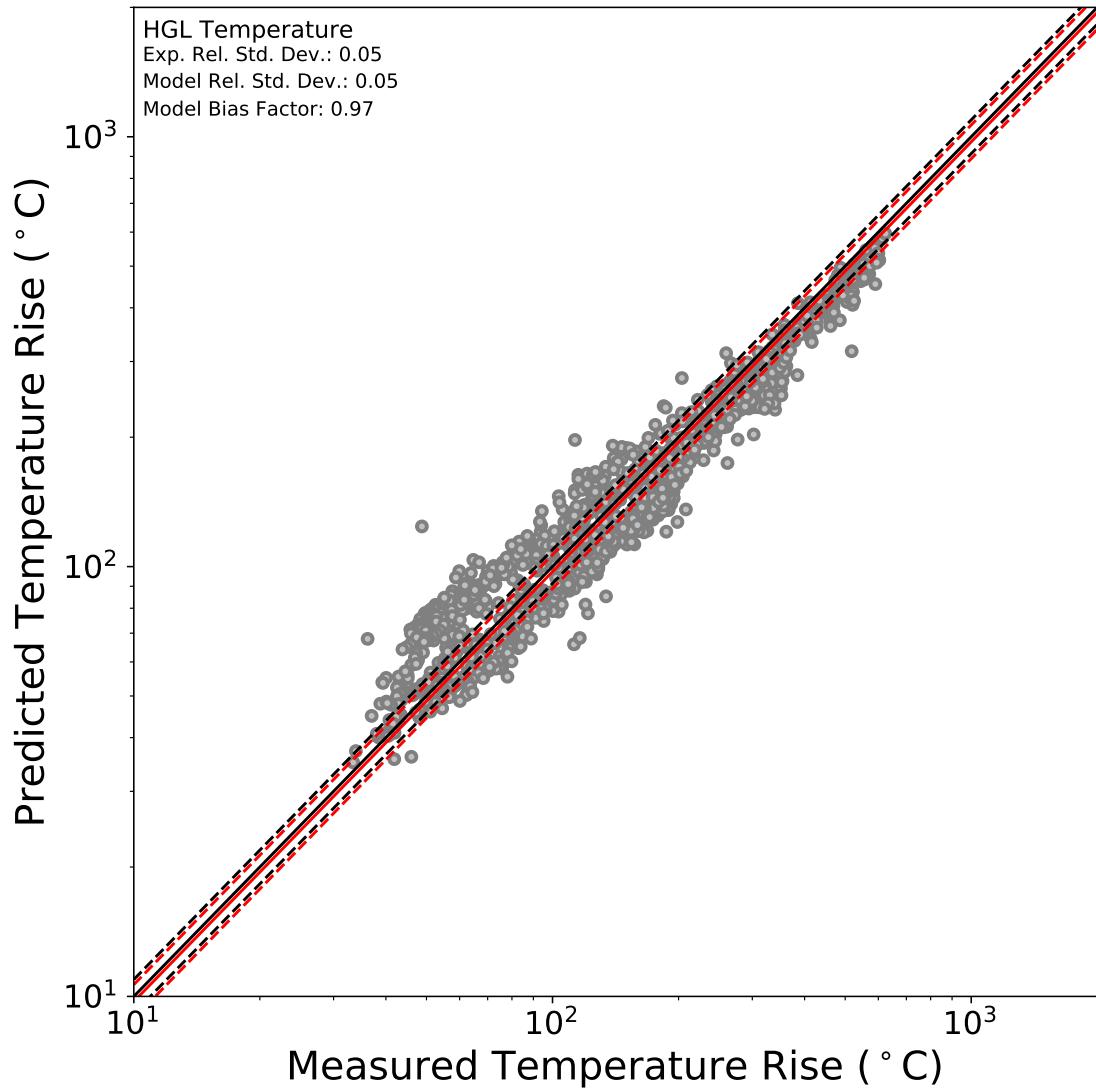


Figure 5.6: Summary of measured and predicted hot gas layer temperatures.

Ceiling Jet

The temperature near the ceiling can be used to evaluate a model's ability to predict the activation times of sprinklers, smoke detectors, and other fire protection devices at ceiling height. The “ceiling jet” temperature used throughout this report refers to the temperature measured by the top thermocouple (closest to the ceiling) of the various thermocouple arrays located throughout the experimental structures. Figure 5.7 shows the ceiling jet temperatures measured during Test 4 plotted with the ceiling jet temperatures predicted by the FDS model for the same duration. Figure 5.8 shows the log/log scatter plot of the ceiling jet temperatures predicted by the FDS simulations compared to the corresponding measured ceiling jet temperatures for the six applicable gas burner experiments.

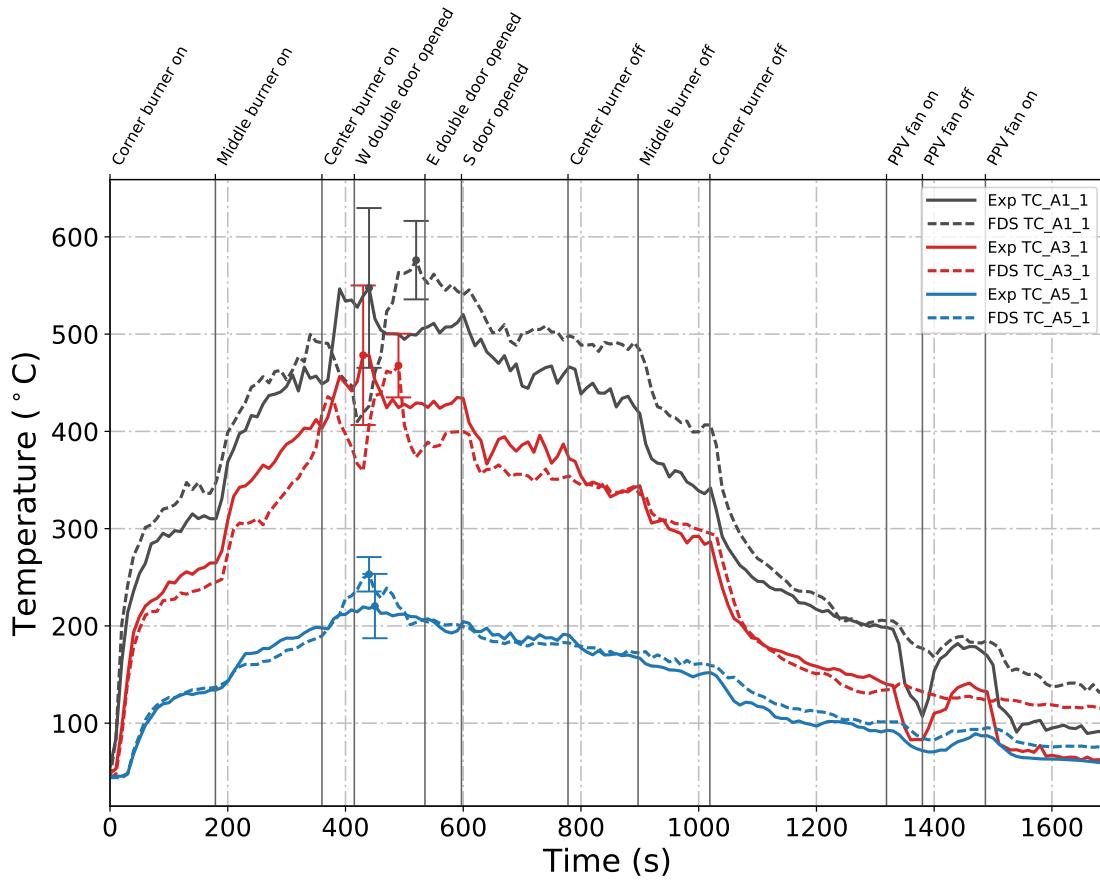


Figure 5.7: Plots of measured and predicted ceiling jet temperatures during Test 4 obtained from thermocouple arrays A1, A3, and A5 located in the fire room, middle room, and north room, respectively.

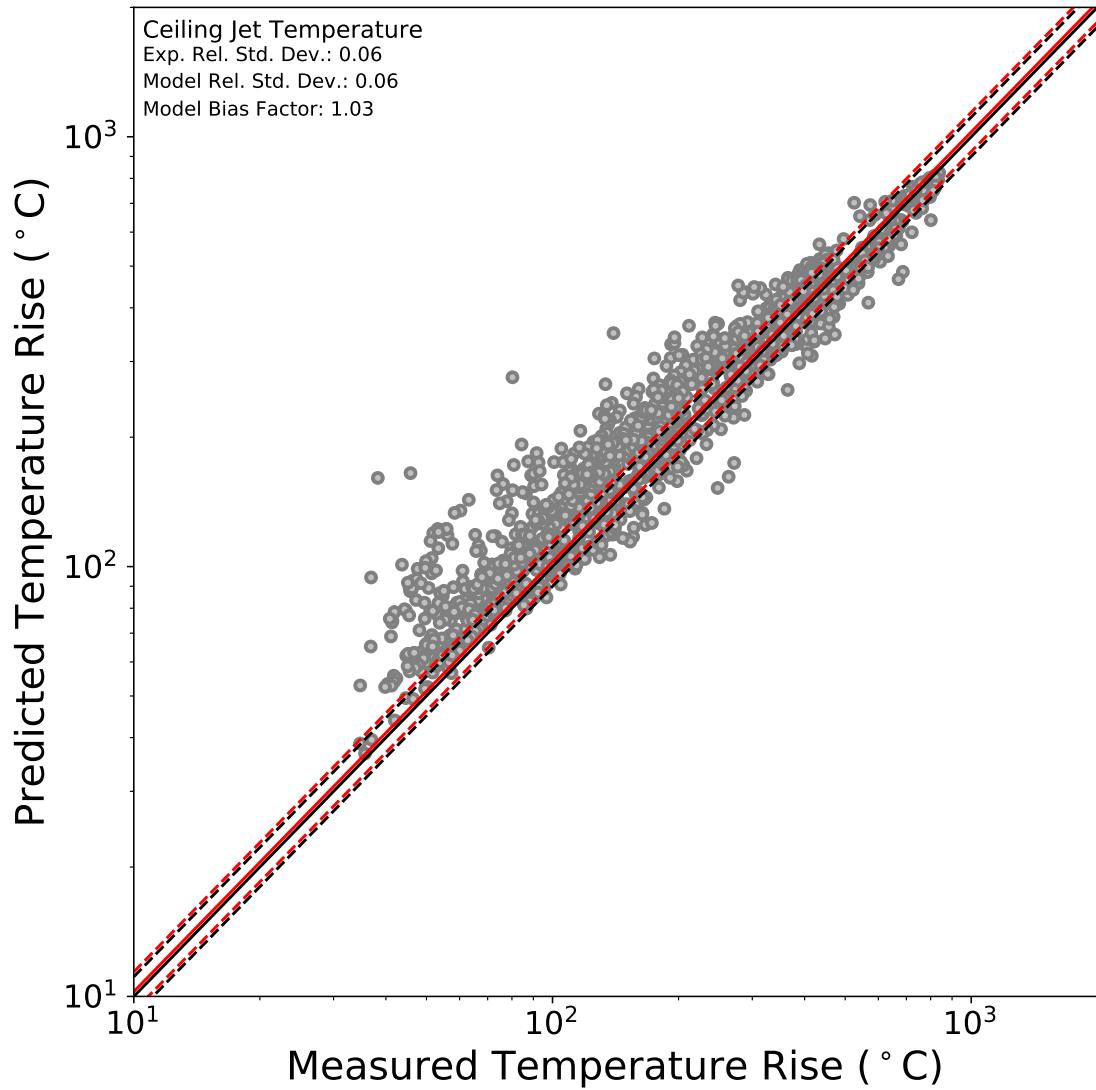


Figure 5.8: Summary of measured and predicted ceiling jet temperatures.

Thermocouple Arrays

In addition to the hot gas layer and ceiling jet temperatures, the measured and predicted temperatures at each thermocouple location for each thermocouple array were compared. Two figures of the temperatures over the duration of each test were generated for each thermocouple array: one of the “upper” temperatures corresponding to the four thermocouple locations nearest to the ceiling and one of the “lower” temperatures corresponding to the four thermocouple locations nearest to the floor. Figure B.26 contains the measured and predicted upper temperatures from array A1 over the duration of Test 24 and Figure 5.10 shows the log/log scatter plot of the temperatures measured at the different thermocouple locations within the thermocouple arrays compared to the temperatures at the same locations predicted by the FDS simulations for Tests 5–6 and Tests 22–25.

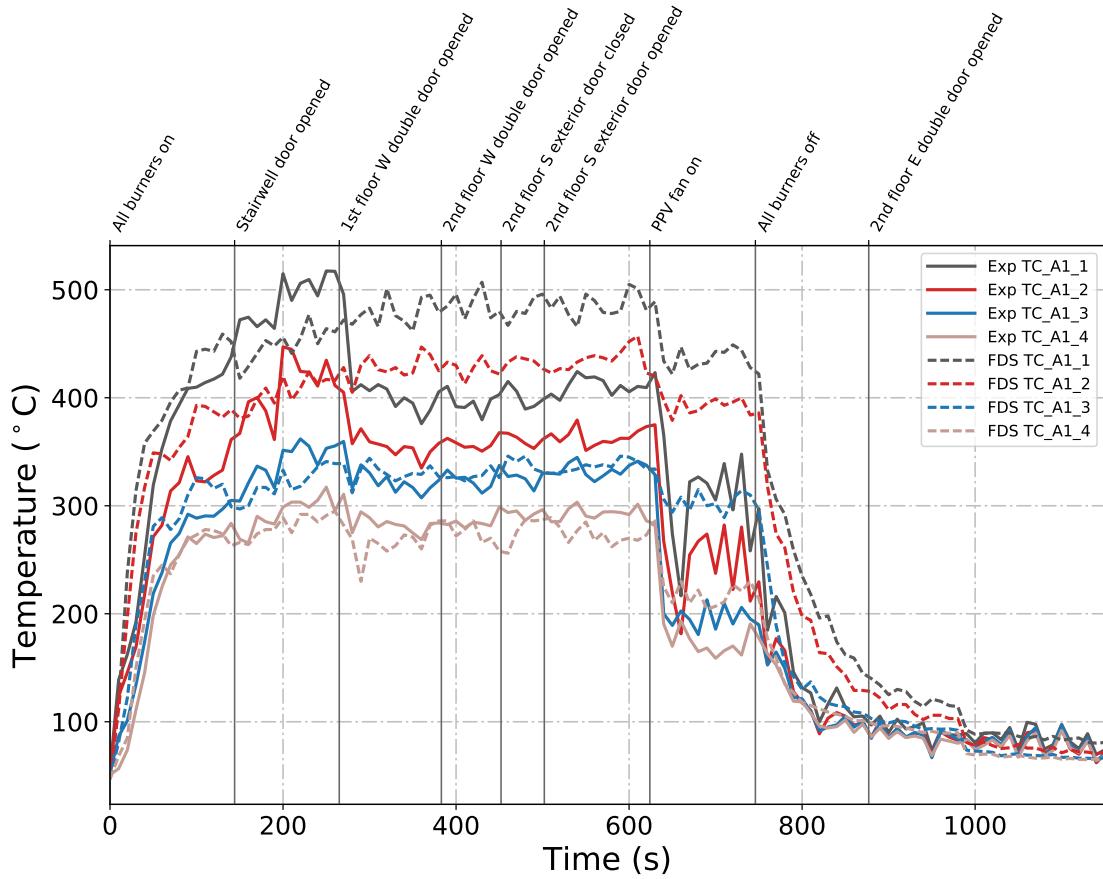


Figure 5.9: Plots of measured and predicted “upper” temperatures from array A1 during Test 24.

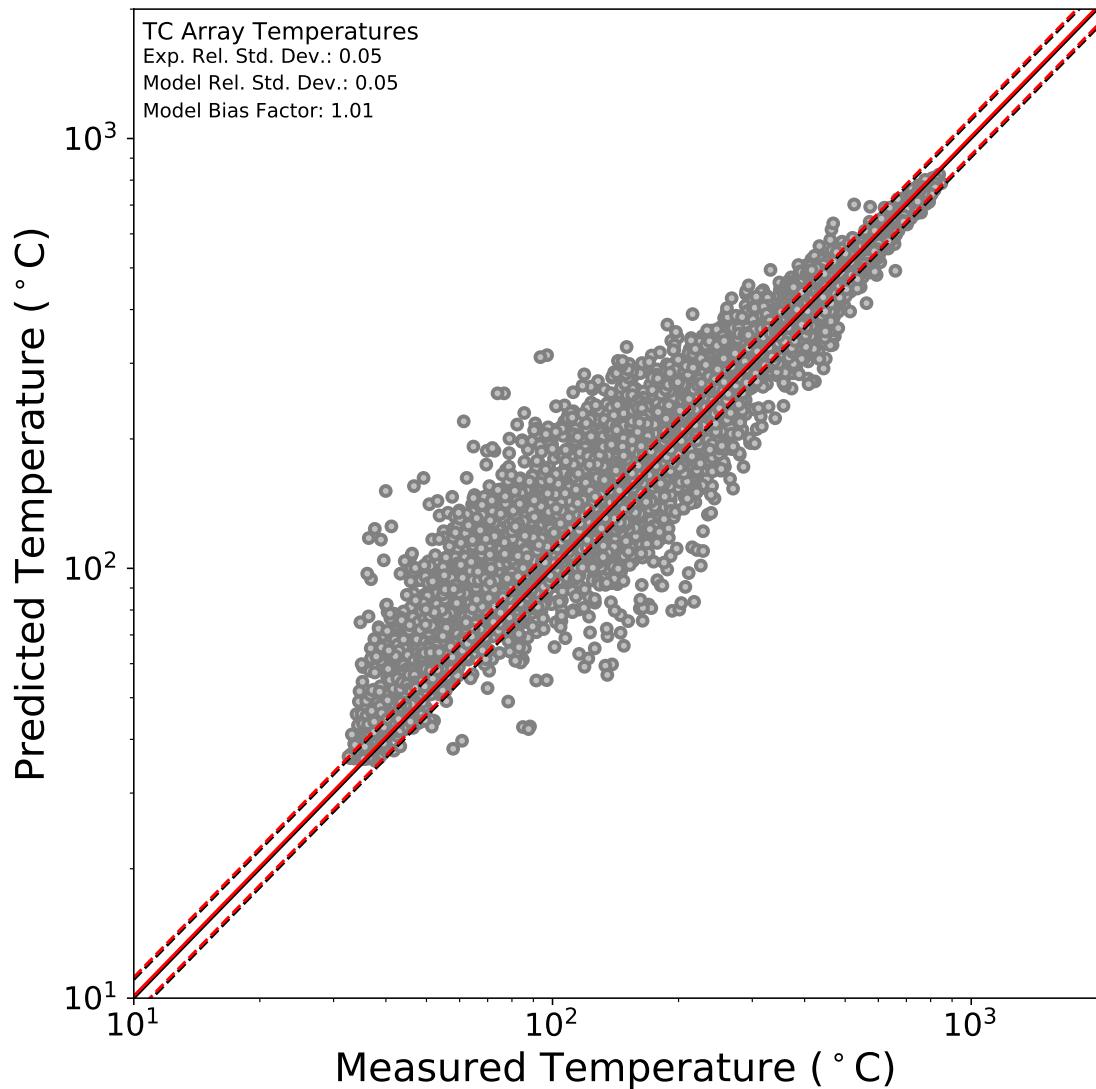


Figure 5.10: Summary of measured and predicted temperatures at the individual thermocouple locations within the different thermocouple arrays.

5.2.2 Gas Species Concentration

O_2 Concentration

The measured and predicted oxygen concentrations of Room 1 (fire room) and Room 3 in the East Structure for the duration of Test 3 are shown in Figure 5.11 as the black and red plots, respectively. Additionally, the summary log/log scatter plot of the predicted oxygen concentrations compared to the corresponding measured oxygen concentrations for Tests 5–6 and Tests 22–25 is shown in Figure 5.12.

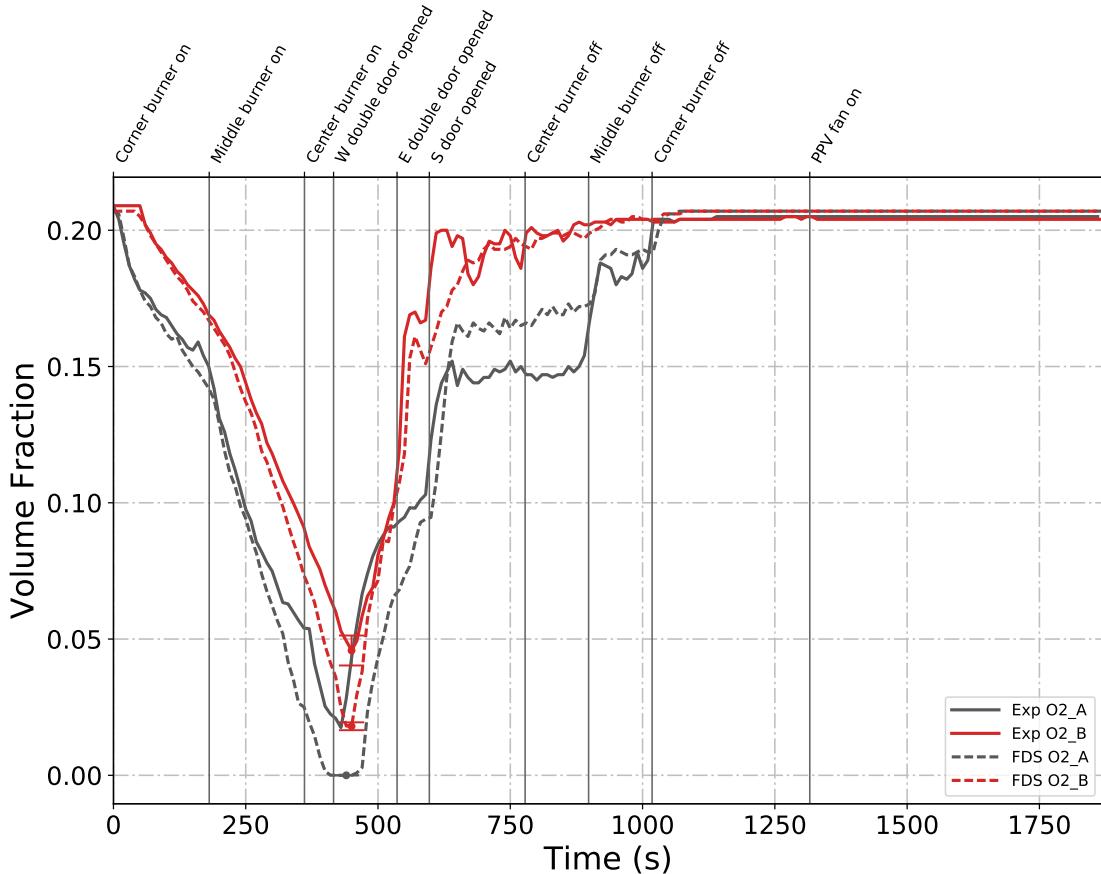


Figure 5.11: Plots of measured and predicted O_2 concentration in the fire room (black plots) and north room (red plots) during Test 3.

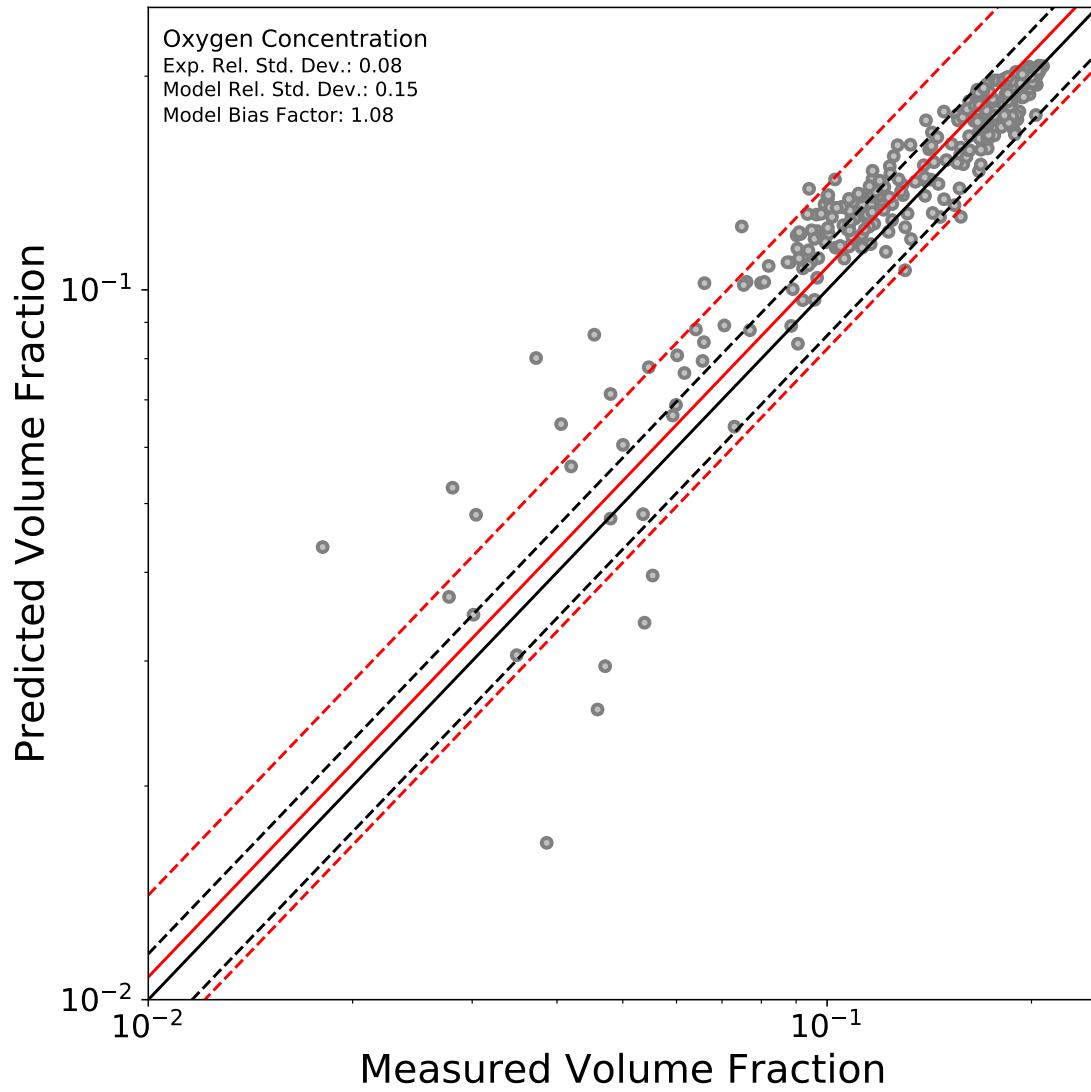


Figure 5.12: Summary of measured and predicted O_2 concentrations.

CO_2 Concentration

The measured and predicted carbon dioxide concentrations of Room 1 (fire room) and Room 3 in the East Structure for the duration of Test 3 are shown in Figure 5.13 as the black and red plots, respectively. Note, the gas sampling system used to measure gas species concentrations could measure CO_2 concentrations below

0.10. Thus, data pairs from the applicable time ranges of Tests 5–6 and Tests 22–25 for which the measured CO_2 volume fraction was 0.10 were not used to create the summary log/log scatter plot of the predicted carbon dioxide concentrations compared to the corresponding measured carbon dioxide concentrations shown in Figure 5.14 below.

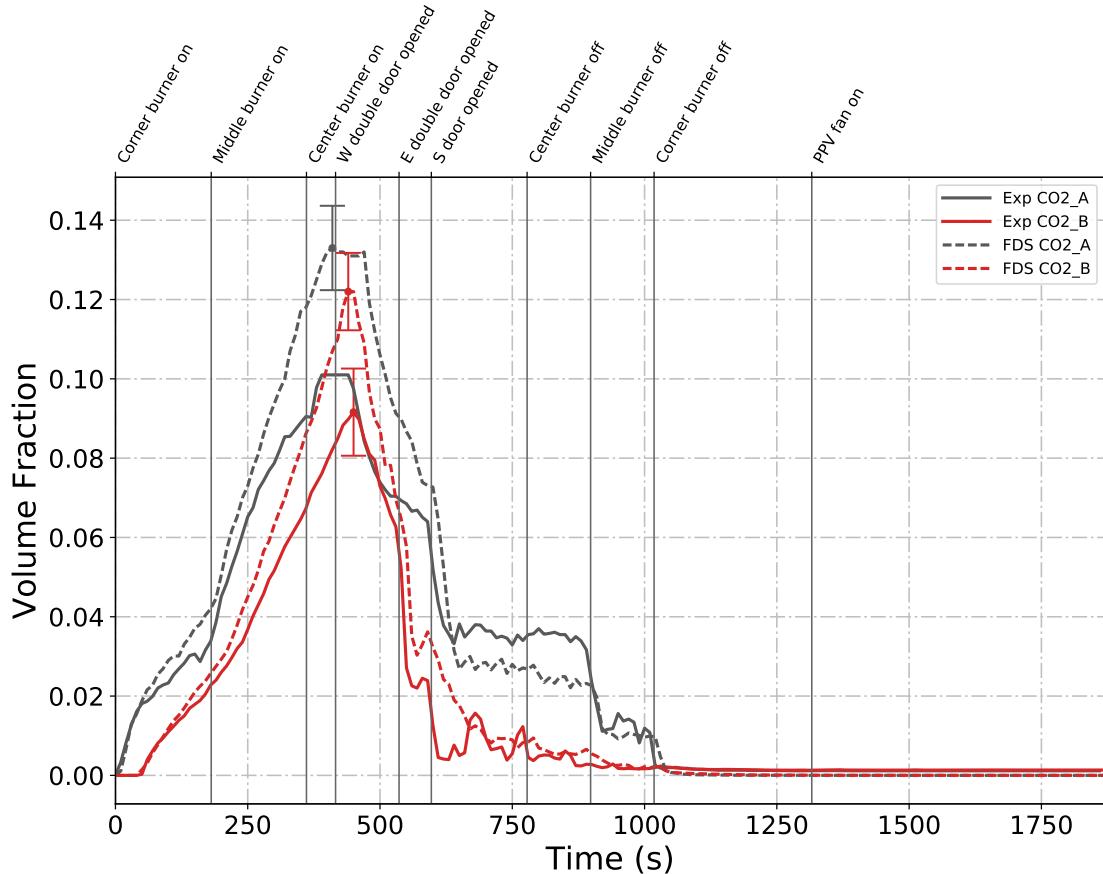


Figure 5.13: Plots of measured and predicted CO_2 concentration in the fire room (black plots) and north room (red plots) during Test 3.

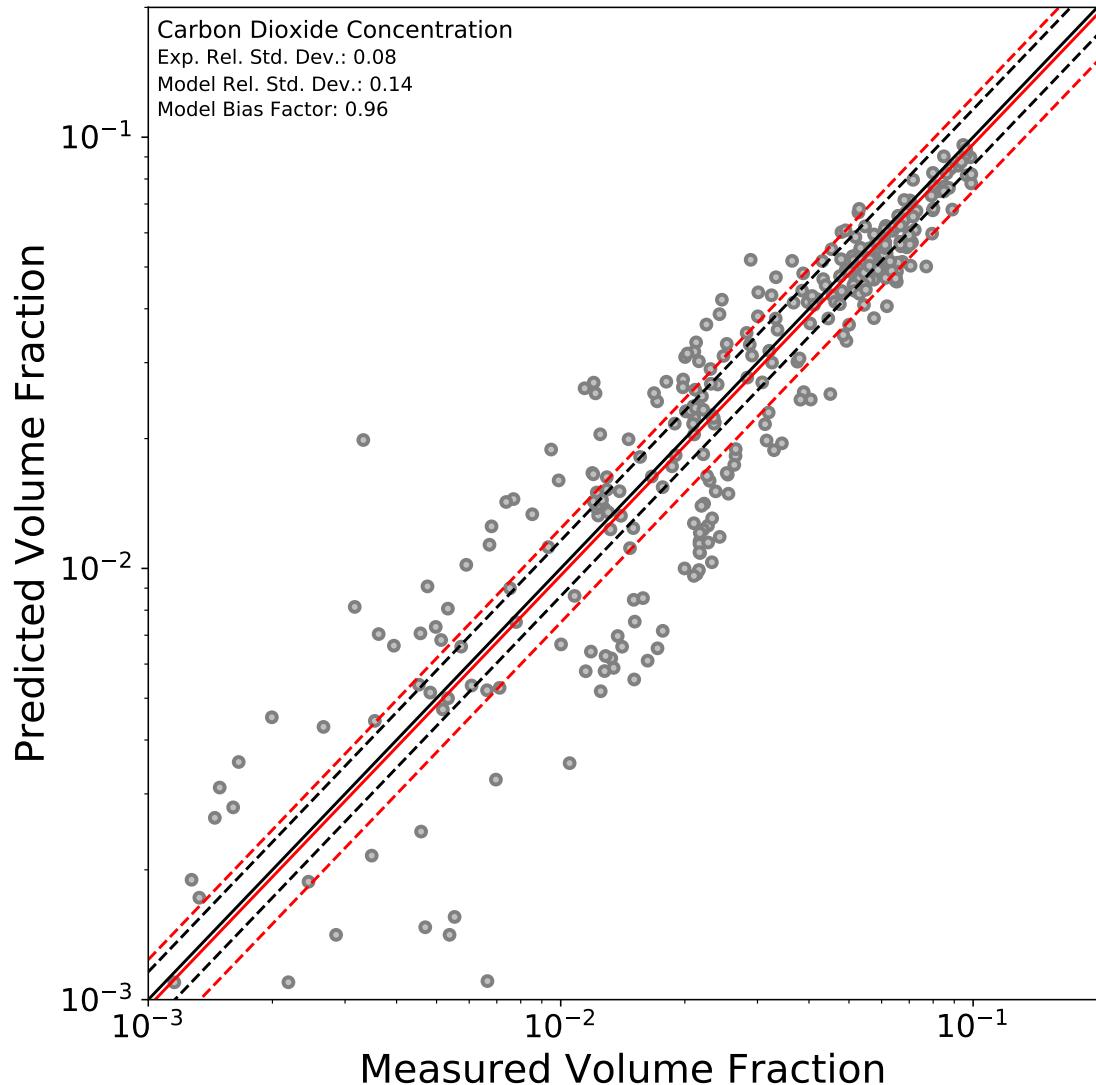


Figure 5.14: Summary of measured and predicted CO_2 concentrations.

5.2.3 Gas Velocity

Because the gas burner experiments were conducted outdoors, they were subject to environmental conditions, such as wind. To minimize the effect such environmental conditions could have on the analysis of the results, the only gas velocity measurements that are considered in this section are those that were indoors, or well-protected from the exterior. The one gas velocity measurement location in the East Structure that was well-protected from the effects of environmental conditions is the location at the roof vent, the set of three BDPs at the location A10. Tests 5 and 6 were the only East Structure tests that incorporated the roof vent as a ventilation opening. Similarly, there was only one set of BDPs in the West Structure that was well protected from the exterior environment: the set of eight BDPs at the top of the stairs at measurement location A10. All four tests conducted in the West Structure used the stairwell door as a ventilation opening. For Tests 22 and 23, the door was in the open position the entire duration of the experiments, and for Tests 24 and 25, the door was opened at a point during the test. Only the measured and predicted data corresponding to when the door was in the open position is considered in the analysis below.

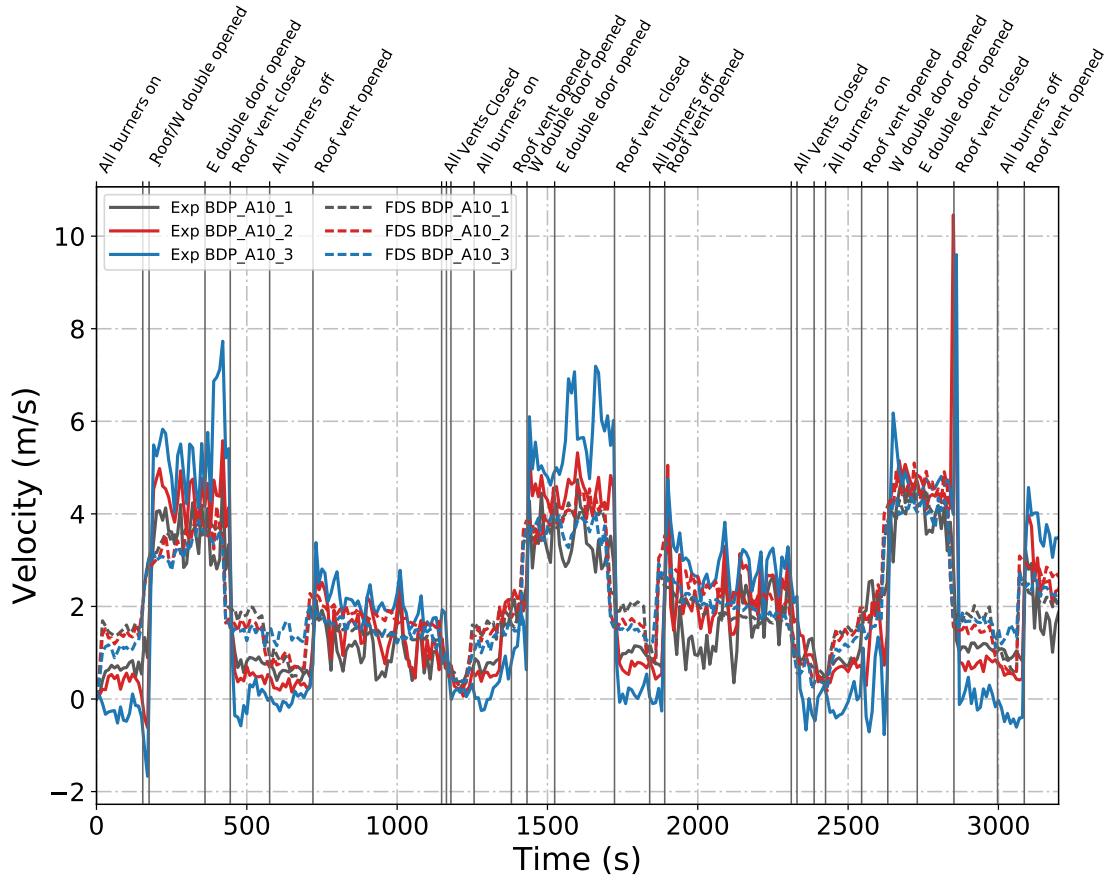


Figure 5.15: Plots of measured and predicted gas velocity through the roof vent during Test 5.

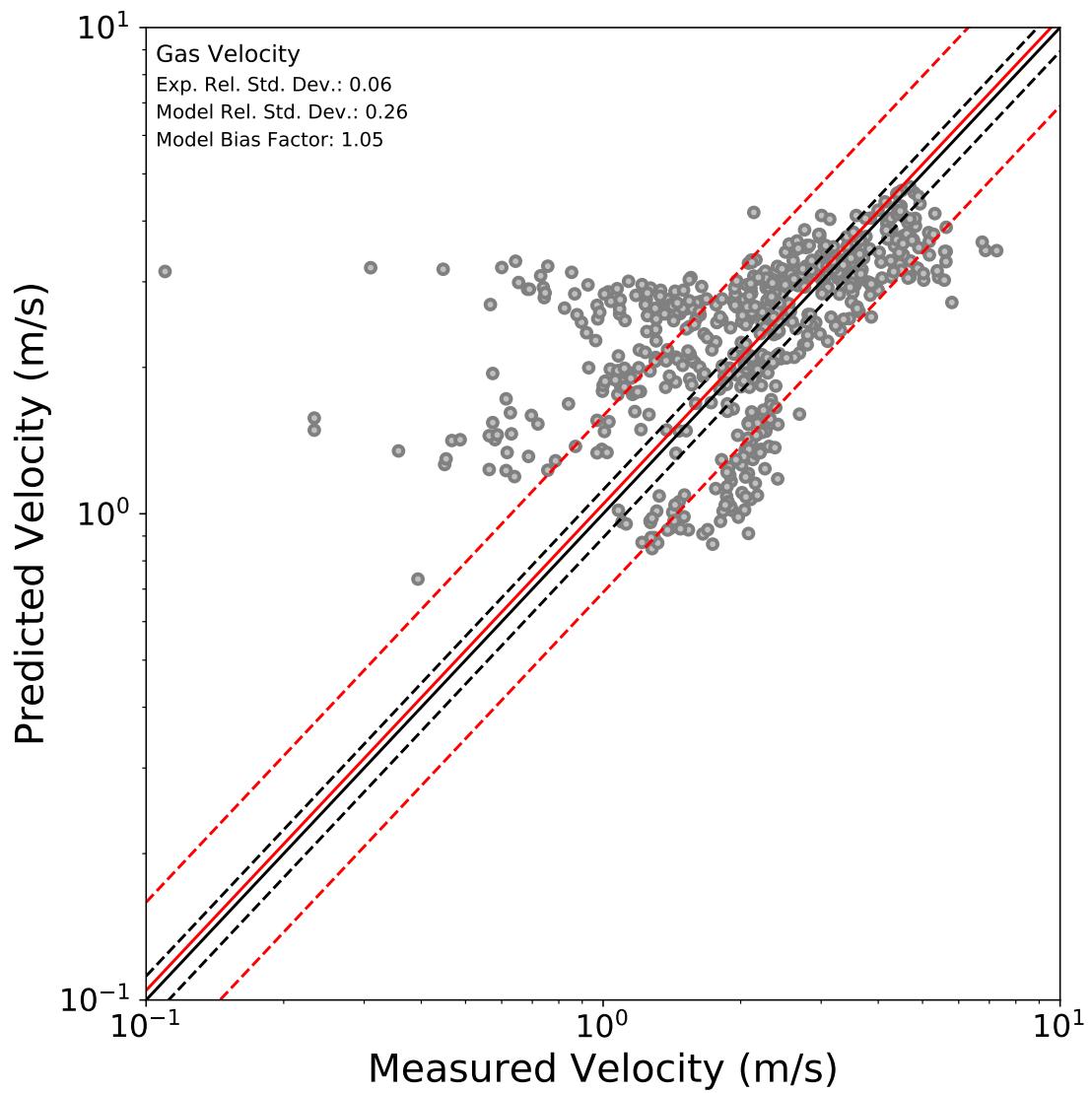


Figure 5.16: Summary of measured and predicted gas velocity measurements.

5.2.4 Total Heat Flux

The heat flux measured by the total heat flux gauges near the stairway door and near the south door on the second floor of the West Structure during Test 23 are plotted with the heat flux data generated by the Test 23 FDS simulation at the same locations in Figure 5.17 below. The log/log scatter plot comparing the heat flux data measured by the various heat flux gauges to the heat flux output by FDS at the same locations for the applicable time periods throughout Tests 5–6 and Tests 22–25 is shown in Figure 5.18.

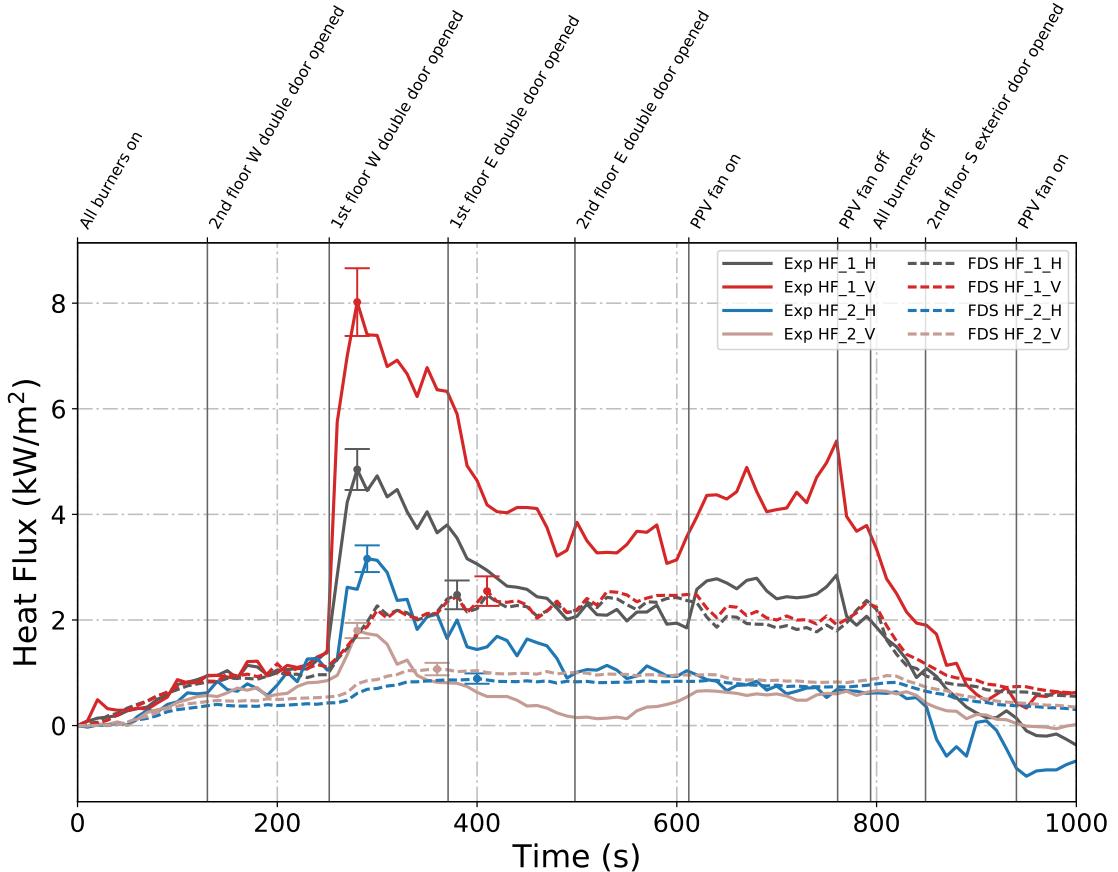


Figure 5.17: Plots of measured and predicted heat flux measured by total heat flux gauges at the top of the stairs facing the stair doorway ('H') and facing the ceiling ('V').

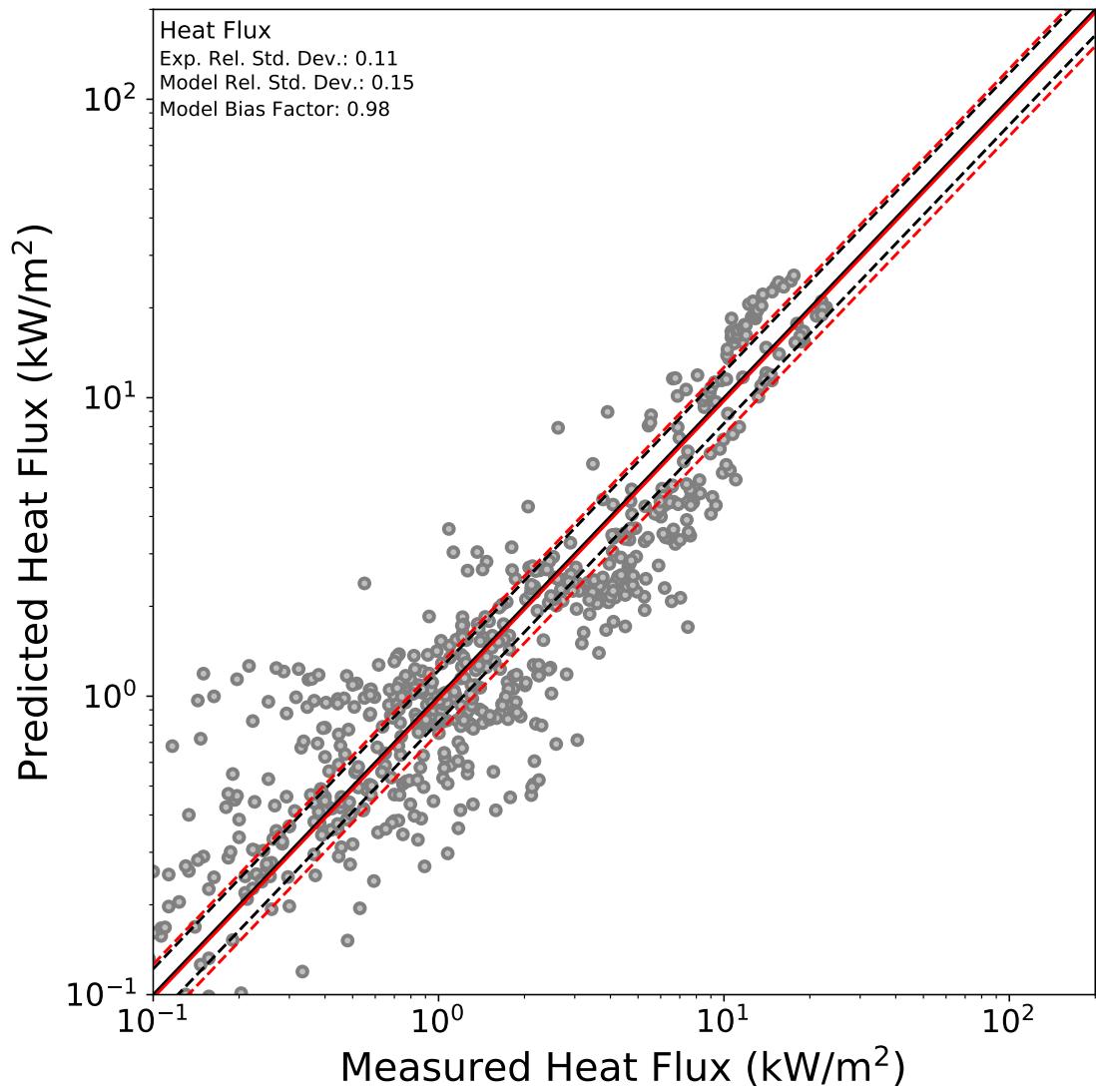


Figure 5.18: Summary of measured and predicted heat flux measurements.

5.2.5 Summary

Table 5.1 compares the model bias factor (δ), the experimental relative standard deviation (σ_E), and model relative standard deviation (σ_M) for each data quantity discussed above calculated across all appropriate time durations of the burner experiments to the same values that are listed in FDS Validation Guide for the corresponding data type based on all data within the FDS validation database.

Table 5.1: Comparison of Model Bias Factor (δ) and Relative Standard Deviation of Experimental Data (σ_E) and Model Data (σ_M) from all Tests and Same Values Listed in FDS Validation Guide for Each Data Type.

Quantity	<u>Calculated Values</u>			<u>FDS Validation Guide</u>		
	δ	σ_E	σ_M	δ	σ_E	σ_M
Hot Gas Layer Temperature	0.97	0.05	0.05	1.04	0.07	0.07
Ceiling Jet Temperature	1.03	0.06	0.06	1.04	0.07	0.13
Oxygen Concentration	1.08	0.08	0.15	0.99	0.08	0.14
Carbon Dioxide Concentration	0.96	0.08	0.14	1.00	0.08	0.12
Gas Velocity	1.05	0.06	0.26	0.99	0.08	0.09
Heat Flux	0.98	0.11	0.15	0.98	0.11	0.24

Overall, the agreement between the FDS simulation data and experimental data for the gas burner experiments is consistent with the statistical values given

by the FDS Validation Guide. For the hot gas layer temperature, ceiling jet temperature, and heat flux, the model bias calculated for the gas burner simulations is equal to or better than (closer to the ideal value of 1) the overall model bias values given by the FDS Validation Guide. Additionally, the relative standard deviations of the experimental data and model data for these three quantities are equal to or less than (better than) the corresponding values for the same data types listed in the validation guide.

The δ , σ_E , and σ_M values produced by the gas burner model and experimental data for both the O_2 and CO_2 gas concentrations were very close to the values documented in the FDS Validation Guide. The σ_E values are equal in both comparisons and the σ_M values are greater in magnitude by only 0.01 and 0.02 compared to the validation guide values for oxygen and carbon dioxide concentration, respectively. Finally, based on the data from gas burner simulations, the oxygen concentration model bias is worse (further from the ideal value of 1) by 7 % and carbon dioxide concentration model bias is worse by 4 % compared to the documented values in the FDS Validation Guide.

The most significant discrepancy between the documented values and values from the gas burner models is seen in the gas velocity comparison, in which σ_M was calculated as being greater than the σ_M from the validation guide by a value 0.18. This discrepancy may exist for a few of reasons. First, gas velocity was one of the quantities with the highest uncertainty associated with the experimental measurements. Also, as previously mentioned, the experiments were conducted outdoors, so environmental conditions may have affected the measurements, even

though only data from BDPs that were fully inside the structures were considered. All the tests used to calculate the δ , σ_E , and σ_M within the validation guide were conducted in an indoors laboratory setting, which could explain the significantly smaller model relative standard deviation. Finally, due to the nature of the fire environment at the time of the measurements, it's possible that turbulent flow was occurring through the vents (especially the roof vent in Tests 5 and 6) at the time of the measurements. LES CFD models, like FDS, tend to be limited more in terms of accurately measuring turbulent flow than compared to measurements during other conditions.

Chapter 6: Conclusion

Nine full-scale fire tests were conducted in two residential-sized structures. Five of the experiments occurred in a single-story structure with three different rooms, and the other four experiments were performed in a two-story structure with the ground level having an open floor plan and the second level having two rooms and a hallway. The fire source for each experiment was provided by a set of three diffusion flame burners with propane as the fuel. Various doors and vents were opened and closed during each test to change ventilation within the structure. Local measurements of temperature, gas velocity, heat flux, and gas concentrations were collected at various locations throughout the structure during the experiments.

The dimensions of each structure were carefully measured, and their construction materials were well-defined. The locations of the experimental instrumentation were also measured and the times of different experimental events were recorded. Additionally, the total volume of propane delivered to the burners was measured by a rotary gas meter and was used to calculate the heat release rate of the fire during each test. Using this information as input data, simulations of the experiments were created and executed using NIST's Fire Dynamics Simulator — the most common CFD modeling software used by fire protection engineers to predict fire dynam-

ics and smoke movement for potential fire scenarios. The simulation results were compared to the experimental data from the experiments.

The agreement between the FDS simulation data and experimental data for the gas burner experiments is consistent with the statistical values given by the FDS Validation Guide. For the quantities of hot gas layer temperature, ceiling jet temperature, and heat flux, the model bias value was equal to or better than (closer to the ideal value of 1) the overall model bias values given by the FDS Validation Guide. Similarly, the relative standard deviations of the experimental data and model data were equal to or less than (more accurate) the corresponding values for the same data types listed in the validation guide. The model bias and experimental and model relative standard deviations produced for both the O_2 and CO_2 gas concentrations were very close to or better than the values documented in the FDS Validation Guide. The most significant discrepancy between the documented values and values from the gas burner models was seen in the gas velocity comparison. The difference could be a result of the fact that the tests were conducted outdoors, that the instrumentation used to measure gas velocity had a relatively large uncertainty range, and/or the limitations of LES models like FDS to model turbulent gas flow at a fine resolution.

Overall, the comparison of the simulation data to the experimental data suggests that the accuracy of the FDS models of the gas burner experiments in residential-scale structures is sufficient and comparable to the accuracy of other FDS models of different fire scenarios described in the FDS Validation Guide.

Appendix A: Channel Lists

A.1 East Structure

Table A.1: East Structure Channel List

Device Location	Channel Name	Channel Location	Measurement Type
A1	TC_A1_1	0.03 m below ceiling	Temperature
	TC_A1_2	0.30 m below ceiling	Temperature
	TC_A1_3	0.61 m below ceiling	Temperature
	TC_A1_4	0.91 m below ceiling	Temperature
	TC_A1_5	1.22 m below ceiling	Temperature
	TC_A1_6	1.52 m below ceiling	Temperature
	TC_A1_7	1.83 m below ceiling	Temperature
	TC_A1_8	2.13 m below ceiling	Temperature
	HF_A1	0.15 m above floor	Total heat flux
	CO_A	1.22 m above floor	CO concentration
A2	CO2_A	1.22 m above floor	CO ₂ concentration
	O2_A	1.22 m above floor	O ₂ concentration
	TC_A2_1	0.03 m below ceiling	Temperature
	TC_A2_2	0.30 m below ceiling	Temperature
	TC_A2_3	0.61 m below ceiling	Temperature
	TC_A2_4	0.91 m below ceiling	Temperature
	TC_A2_5	1.22 m below ceiling	Temperature
	TC_A2_6	1.52 m below ceiling	Temperature
	TC_A2_7	1.83 m below ceiling	Temperature
	TC_A2_8	2.13 m below ceiling	Temperature

Table A.1: East Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A3	TC_A3_1	0.03 m below ceiling	Temperature
	TC_A3_2	0.30 m below ceiling	Temperature
	TC_A3_3	0.61 m below ceiling	Temperature
	TC_A3_4	0.91 m below ceiling	Temperature
	TC_A3_5	1.22 m below ceiling	Temperature
	TC_A3_6	1.52 m below ceiling	Temperature
	TC_A3_7	1.83 m below ceiling	Temperature
	TC_A3_8	2.13 m below ceiling	Temperature
	HF_A3	0.15 m above floor	Total heat flux
A4	TC_A4_1	0.03 m below ceiling	Temperature
	TC_A4_2	0.30 m below ceiling	Temperature
	TC_A4_3	0.61 m below ceiling	Temperature
	TC_A4_4	0.91 m below ceiling	Temperature
	TC_A4_5	1.22 m below ceiling	Temperature
	TC_A4_6	1.52 m below ceiling	Temperature
	TC_A4_7	1.83 m below ceiling	Temperature
	TC_A4_8	2.13 m below ceiling	Temperature
	HF_A4	0.15 m above floor	Total heat flux
	CO_B	1.22 m above floor	CO concentration
A5	CO2_B	1.22 m above floor	CO ₂ concentration
	O2_B	1.22 m above floor	O ₂ concentration
	TC_A5_1	0.03 m below ceiling	Temperature
	TC_A5_2	0.30 m below ceiling	Temperature
	TC_A5_3	0.61 m below ceiling	Temperature
	TC_A5_4	0.91 m below ceiling	Temperature
	TC_A5_5	1.22 m below ceiling	Temperature
	TC_A5_6	1.52 m below ceiling	Temperature
	TC_A5_7	1.83 m below ceiling	Temperature
	TC_A5_8	2.13 m below ceiling	Temperature
	HF_A5	0.15 m above floor	Total heat flux

Table A.1: East Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A7	TC_A7_1	0.08 m below soffit	Temperature
	TC_A7_2	0.34 m below soffit	Temperature
	TC_A7_3	0.61 m below soffit	Temperature
	TC_A7_4	0.88 m below soffit	Temperature
	TC_A7_5	1.15 m below soffit	Temperature
	TC_A7_6	1.42 m below soffit	Temperature
	TC_A7_7	1.68 m below soffit	Temperature
	TC_A7_8	1.95 m below soffit	Temperature
	BDP_A7_1	0.08 m below soffit	Velocity
	BDP_A7_2	0.34 m below soffit	Velocity
	BDP_A7_3	0.61 m below soffit	Velocity
	BDP_A7_4	0.88 m below soffit	Velocity
	BDP_A7_5	1.15 m below soffit	Velocity
	BDP_A7_6	1.42 m below soffit	Velocity
	BDP_A7_7	1.68 m below soffit	Velocity
	BDP_A7_8	1.95 m below soffit	Velocity
A8	TC_A8_1	0.08 m below soffit	Temperature
	TC_A8_2	0.34 m below soffit	Temperature
	TC_A8_3	0.61 m below soffit	Temperature
	TC_A8_4	0.88 m below soffit	Temperature
	TC_A8_5	1.15 m below soffit	Temperature
	TC_A8_6	1.42 m below soffit	Temperature
	TC_A8_7	1.68 m below soffit	Temperature
	TC_A8_8	1.95 m below soffit	Temperature
	BDP_A8_1	0.08 m below soffit	Velocity
	BDP_A8_2	0.34 m below soffit	Velocity
	BDP_A8_3	0.61 m below soffit	Velocity
	BDP_A8_4	0.88 m below soffit	Velocity
	BDP_A8_5	1.15 m below soffit	Velocity
	BDP_A8_6	1.42 m below soffit	Velocity
	BDP_A8_7	1.68 m below soffit	Velocity
	BDP_A8_8	1.95 m below soffit	Velocity

Table A.1: East Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A9	TC_A9_1	0.08 m below soffit	Temperature
	TC_A9_2	0.34 m below soffit	Temperature
	TC_A9_3	0.61 m below soffit	Temperature
	TC_A9_4	0.88 m below soffit	Temperature
	TC_A9_5	1.15 m below soffit	Temperature
	TC_A9_6	1.42 m below soffit	Temperature
	TC_A9_7	1.68 m below soffit	Temperature
	TC_A9_8	1.95 m below soffit	Temperature
	BDP_A9_1	0.08 m below soffit	Velocity
	BDP_A9_2	0.34 m below soffit	Velocity
	BDP_A9_3	0.61 m below soffit	Velocity
	BDP_A9_4	0.88 m below soffit	Velocity
	BDP_A9_5	1.15 m below soffit	Velocity
	BDP_A9_6	1.42 m below soffit	Velocity
	BDP_A9_7	1.68 m below soffit	Velocity
	BDP_A9_8	1.95 m below soffit	Velocity
A10	TC_A10_1	0.91 m from S side of vent	Temperature
	TC_A10_2	0.61 m from S side of vent	Temperature
	TC_A10_3	0.30 m from S side of vent	Temperature
	BDP_A10_1	0.91 m from S side of vent	Velocity
	BDP_A10_2	0.61 m from S side of vent	Velocity
	BDP_A10_3	0.30 m from S side of vent	Velocity

A.2 West Structure

Table A.2: West Structure Channel List

Device Location	Channel Name	Channel Location	Measurement Type
A1	TC_A1_1	0.03 m below ceiling	Temperature
	TC_A1_2	0.30 m below ceiling	Temperature
	TC_A1_3	0.61 m below ceiling	Temperature
	TC_A1_4	0.91 m below ceiling	Temperature
	TC_A1_5	1.22 m below ceiling	Temperature
	TC_A1_6	1.52 m below ceiling	Temperature
	TC_A1_7	1.83 m below ceiling	Temperature
	TC_A1_8	2.13 m below ceiling	Temperature
	CO_A	1.22 m above floor	CO concentration
	CO2_A	1.22 m above floor	CO ₂ concentration
	O2_A	1.22 m above floor	O ₂ concentration
A2	TC_A2_1	0.03 m below ceiling	Temperature
	TC_A2_2	0.30 m below ceiling	Temperature
	TC_A2_3	0.61 m below ceiling	Temperature
	TC_A2_4	0.91 m below ceiling	Temperature
	TC_A2_5	1.22 m below ceiling	Temperature
	TC_A2_6	1.52 m below ceiling	Temperature
	TC_A2_7	1.83 m below ceiling	Temperature
	TC_A2_8	2.13 m below ceiling	Temperature
A3	TC_A3_1	0.03 m below ceiling	Temperature
	TC_A3_2	0.30 m below ceiling	Temperature
	TC_A3_3	0.61 m below ceiling	Temperature
	TC_A3_4	0.91 m below ceiling	Temperature
	TC_A3_5	1.22 m below ceiling	Temperature
	TC_A3_6	1.52 m below ceiling	Temperature
	TC_A3_7	1.83 m below ceiling	Temperature
	TC_A3_8	2.13 m below ceiling	Temperature

Table A.2: West Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A5	TC_A5_1	0.08 m below soffit	Temperature
	TC_A5_2	0.34 m below soffit	Temperature
	TC_A5_3	0.61 m below soffit	Temperature
	TC_A5_4	0.88 m below soffit	Temperature
	TC_A5_5	1.15 m below soffit	Temperature
	TC_A5_6	1.42 m below soffit	Temperature
	TC_A5_7	1.68 m below soffit	Temperature
	TC_A5_8	1.95 m below soffit	Temperature
	BDP_A5_1	0.08 m below soffit	Velocity
	BDP_A5_2	0.34 m below soffit	Velocity
	BDP_A5_3	0.61 m below soffit	Velocity
	BDP_A5_4	0.88 m below soffit	Velocity
	BDP_A5_5	1.15 m below soffit	Velocity
	BDP_A5_6	1.42 m below soffit	Velocity
	BDP_A5_7	1.68 m below soffit	Velocity
	BDP_A5_8	1.95 m below soffit	Velocity
A6	TC_A6_1	0.08 m below soffit	Temperature
	TC_A6_2	0.34 m below soffit	Temperature
	TC_A6_3	0.61 m below soffit	Temperature
	TC_A6_4	0.88 m below soffit	Temperature
	TC_A6_5	1.15 m below soffit	Temperature
	TC_A6_6	1.42 m below soffit	Temperature
	TC_A6_7	1.68 m below soffit	Temperature
	TC_A6_8	1.95 m below soffit	Temperature
	BDP_A6_1	0.08 m below soffit	Velocity
	BDP_A6_2	0.34 m below soffit	Velocity
	BDP_A6_3	0.61 m below soffit	Velocity
	BDP_A6_4	0.88 m below soffit	Velocity
	BDP_A6_5	1.15 m below soffit	Velocity
	BDP_A6_6	1.42 m below soffit	Velocity
	BDP_A6_7	1.68 m below soffit	Velocity
	BDP_A6_8	1.95 m below soffit	Velocity

Table A.2: West Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A7	TC_A7_1	0.03 m below ceiling	Temperature
	TC_A7_2	0.30 m below ceiling	Temperature
	TC_A7_3	0.61 m below ceiling	Temperature
	TC_A7_4	0.91 m below ceiling	Temperature
	TC_A7_5	1.22 m below ceiling	Temperature
	TC_A7_6	1.52 m below ceiling	Temperature
	TC_A7_7	1.83 m below ceiling	Temperature
	TC_A7_8	2.13 m below ceiling	Temperature
A8	TC_A8_1	0.03 m below ceiling	Temperature
	TC_A8_2	0.30 m below ceiling	Temperature
	TC_A8_3	0.61 m below ceiling	Temperature
	TC_A8_4	0.91 m below ceiling	Temperature
	TC_A8_5	1.22 m below ceiling	Temperature
	TC_A8_6	1.52 m below ceiling	Temperature
	TC_A8_7	1.83 m below ceiling	Temperature
	TC_A8_8	2.13 m below ceiling	Temperature
A9	TC_A9_1	0.03 m below ceiling	Temperature
	TC_A9_2	0.30 m below ceiling	Temperature
	TC_A9_3	0.61 m below ceiling	Temperature
	TC_A9_4	0.91 m below ceiling	Temperature
	TC_A9_5	1.22 m below ceiling	Temperature
	TC_A9_6	1.52 m below ceiling	Temperature
	TC_A9_7	1.83 m below ceiling	Temperature
	TC_A9_8	2.13 m below ceiling	Temperature

Table A.2: West Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A10	TC_A10_1	0.08 m below soffit	Temperature
	TC_A10_2	0.34 m below soffit	Temperature
	TC_A10_3	0.61 m below soffit	Temperature
	TC_A10_4	0.88 m below soffit	Temperature
	TC_A10_5	1.15 m below soffit	Temperature
	TC_A10_6	1.42 m below soffit	Temperature
	TC_A10_7	1.68 m below soffit	Temperature
	TC_A10_8	1.95 m below soffit	Temperature
	BDP_A10_1	0.08 m below soffit	Velocity
	BDP_A10_2	0.34 m below soffit	Velocity
	BDP_A10_3	0.61 m below soffit	Velocity
	BDP_A10_4	0.88 m below soffit	Velocity
	BDP_A10_5	1.15 m below soffit	Velocity
	BDP_A10_6	1.42 m below soffit	Velocity
	BDP_A10_7	1.68 m below soffit	Velocity
	BDP_A10_8	1.95 m below soffit	Velocity
A11	CO_B	1.22 m above floor	CO concentration
	CO2_B	1.22 m above floor	CO ₂ concentration
	O2_B	1.22 m above floor	O ₂ concentration
A11	TC_A11_1	0.08 m below soffit	Temperature
	TC_A11_2	0.34 m below soffit	Temperature
	TC_A11_3	0.61 m below soffit	Temperature
	TC_A11_4	0.88 m below soffit	Temperature
	TC_A11_5	1.15 m below soffit	Temperature
	TC_A11_6	1.42 m below soffit	Temperature
	TC_A11_7	1.68 m below soffit	Temperature
	TC_A11_8	1.95 m below soffit	Temperature
	BDP_A11_1	0.08 m below soffit	Velocity
	BDP_A11_2	0.34 m below soffit	Velocity
	BDP_A11_3	0.61 m below soffit	Velocity
	BDP_A11_4	0.88 m below soffit	Velocity
	BDP_A11_5	1.15 m below soffit	Velocity
	BDP_A11_6	1.42 m below soffit	Velocity
	BDP_A11_7	1.68 m below soffit	Velocity
	BDP_A11_8	1.95 m below soffit	Velocity

Table A.2: West Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A13	TC_A13_1	0.08 m below soffit	Temperature
	TC_A13_2	0.34 m below soffit	Temperature
	TC_A13_3	0.61 m below soffit	Temperature
	TC_A13_4	0.88 m below soffit	Temperature
	TC_A13_5	1.15 m below soffit	Temperature
	TC_A13_6	1.42 m below soffit	Temperature
	TC_A13_7	1.68 m below soffit	Temperature
	TC_A13_8	1.95 m below soffit	Temperature
	BDP_A13_1	0.08 m below soffit	Velocity
	BDP_A13_2	0.34 m below soffit	Velocity
	BDP_A13_3	0.61 m below soffit	Velocity
	BDP_A13_4	0.88 m below soffit	Velocity
	BDP_A13_5	1.15 m below soffit	Velocity
	BDP_A13_6	1.42 m below soffit	Velocity
	BDP_A13_7	1.68 m below soffit	Velocity
	BDP_A13_8	1.95 m below soffit	Velocity
A14	TC_A14_1	0.08 m below soffit	Temperature
	TC_A14_2	0.34 m below soffit	Temperature
	TC_A14_3	0.61 m below soffit	Temperature
	TC_A14_4	0.88 m below soffit	Temperature
	TC_A14_5	1.15 m below soffit	Temperature
	TC_A14_6	1.42 m below soffit	Temperature
	TC_A14_7	1.68 m below soffit	Temperature
	TC_A14_8	1.95 m below soffit	Temperature
	BDP_A14_1	0.08 m below soffit	Velocity
	BDP_A14_2	0.34 m below soffit	Velocity
	BDP_A14_3	0.61 m below soffit	Velocity
	BDP_A14_4	0.88 m below soffit	Velocity
	BDP_A14_5	1.15 m below soffit	Velocity
	BDP_A14_6	1.42 m below soffit	Velocity
	BDP_A14_7	1.68 m below soffit	Velocity
	BDP_A14_8	1.95 m below soffit	Velocity

Table A.2: West Structure Channel List (continued)

Device Location	Channel Name	Channel Location	Measurement Type
A16	HF_2_H	1 m above floor, facing N wall (horizontal)	Total heat flux
	HF_2_V	1 m above floor, facing ceiling (vertical)	Total heat flux
A17	HF_1_H	1 m above floor, facing doorway (horizontal)	Total heat flux
	HF_1_V	1 m above floor, facing ceiling (vertical)	Total heat flux

Appendix B: Experimental and FDS Data Plots

B.1 Temperature

Hot Gas Layer Temperatures

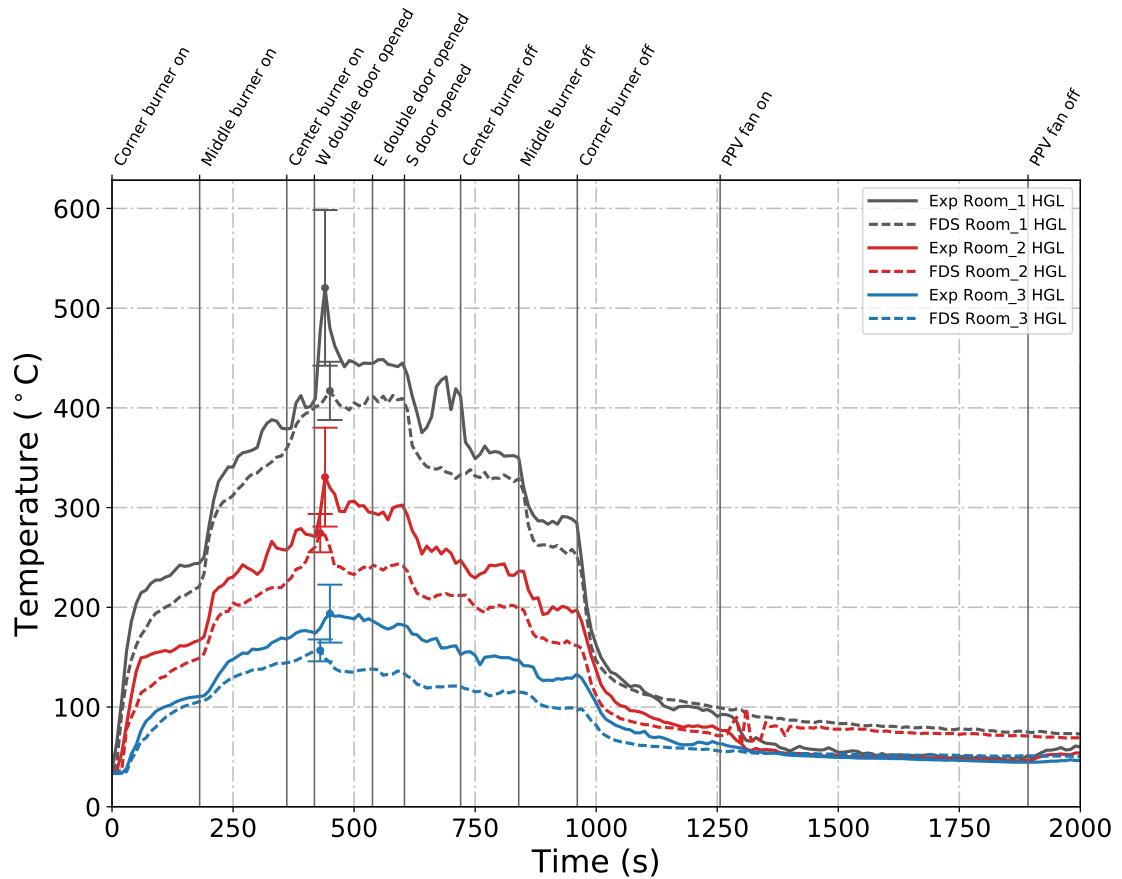


Figure B.1: Plots of measured and predicted hot gas layer temperatures in the three rooms of the East Structure during Test 2.

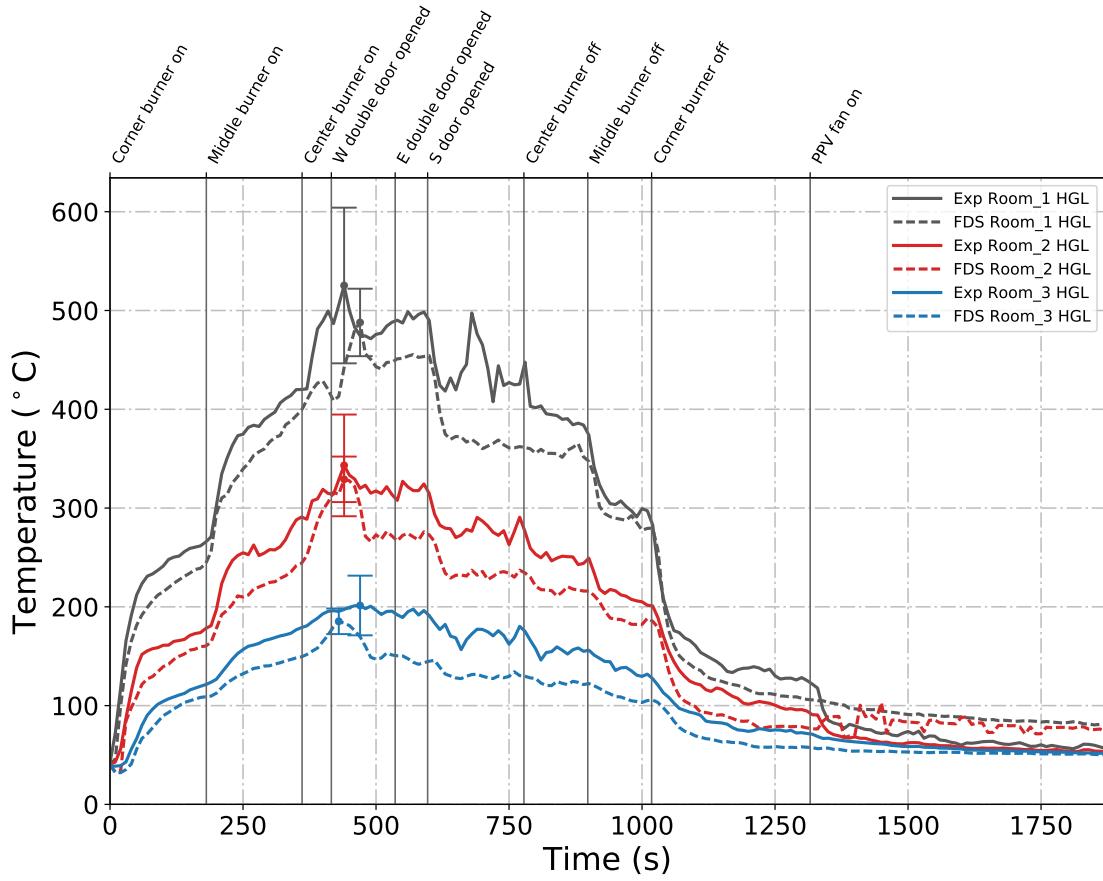


Figure B.2: Plots of measured and predicted hot gas layer temperatures in the three rooms of the East Structure during Test 3.

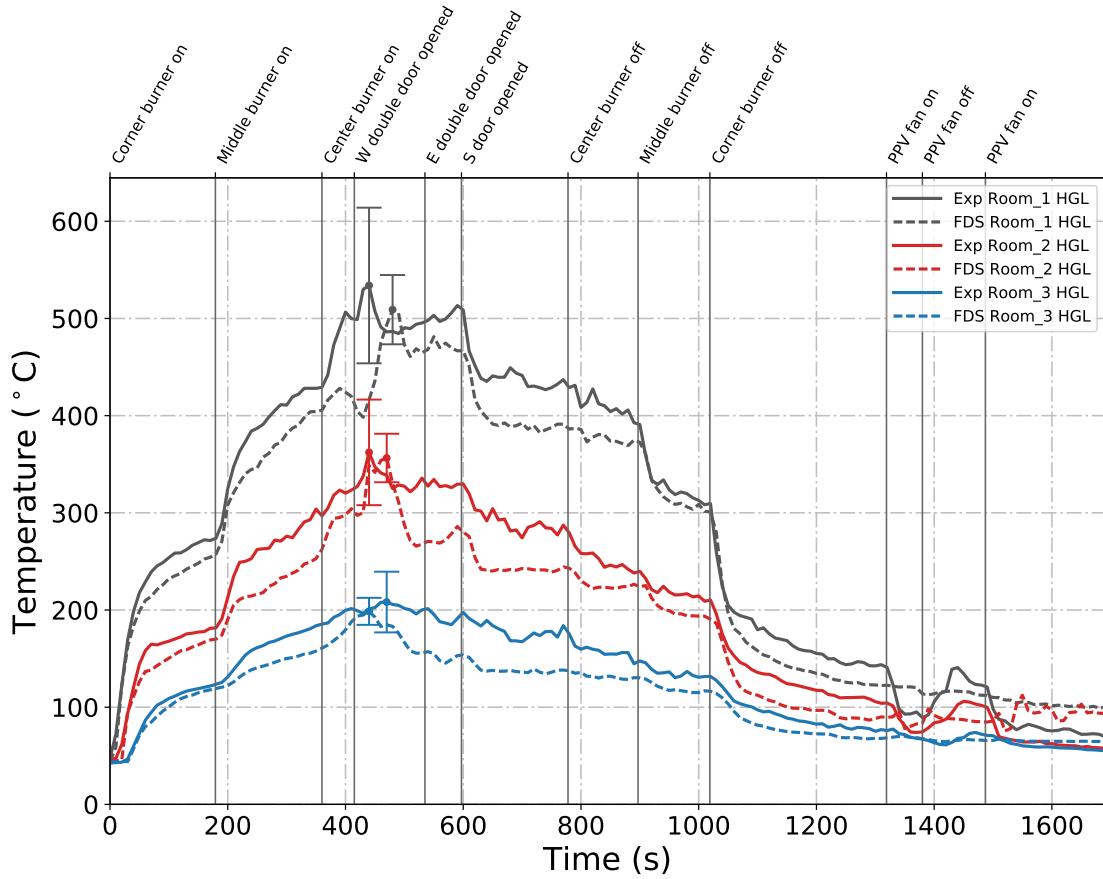


Figure B.3: Plots of measured and predicted hot gas layer temperatures in the three rooms of the East Structure during Test 4.

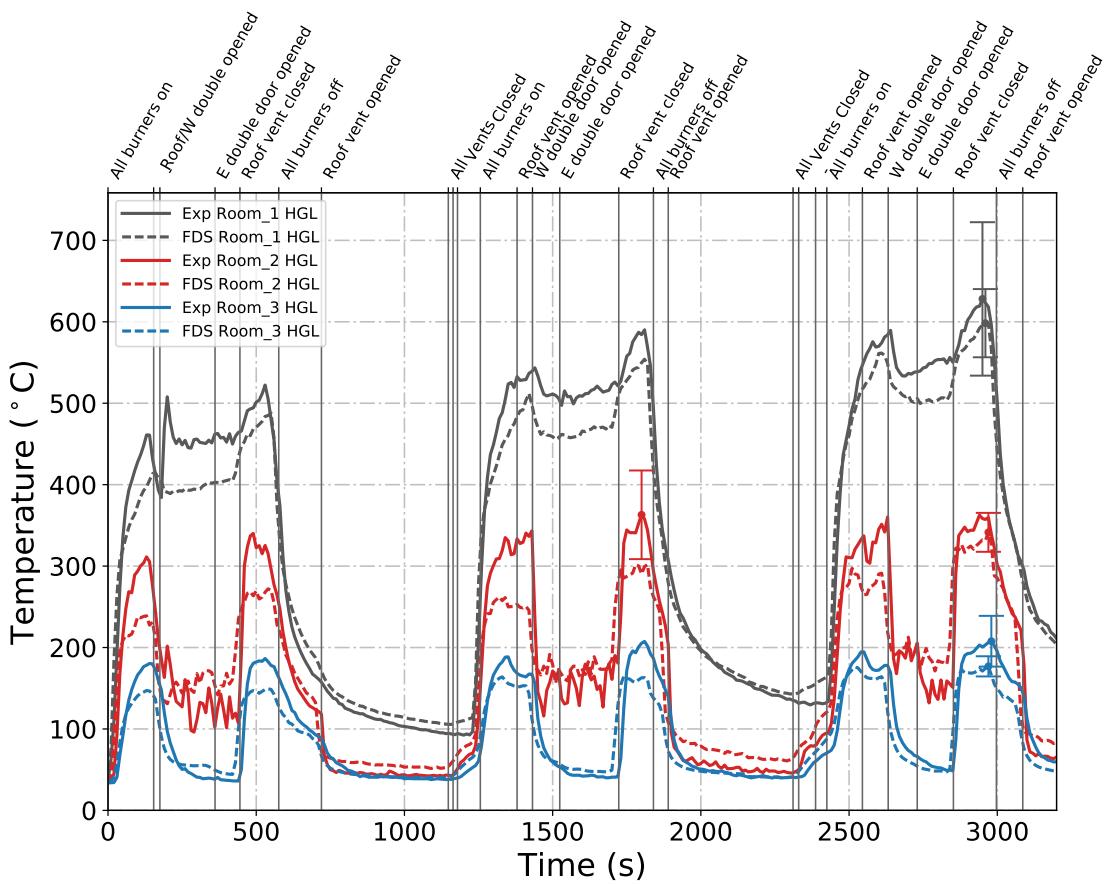


Figure B.4: Plots of measured and predicted hot gas layer temperatures in the three rooms of the East Structure during Test 5.

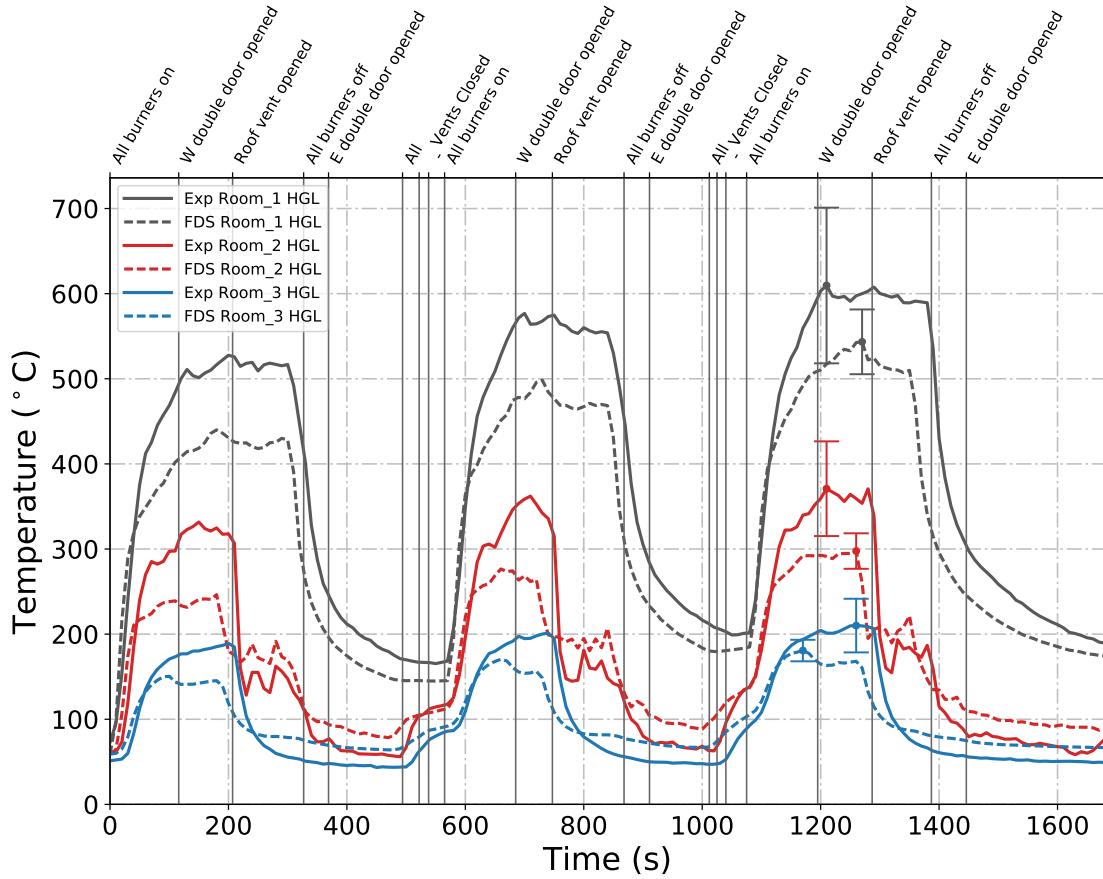


Figure B.5: Plots of measured and predicted hot gas layer temperatures in the three rooms of the East Structure during Test 6.

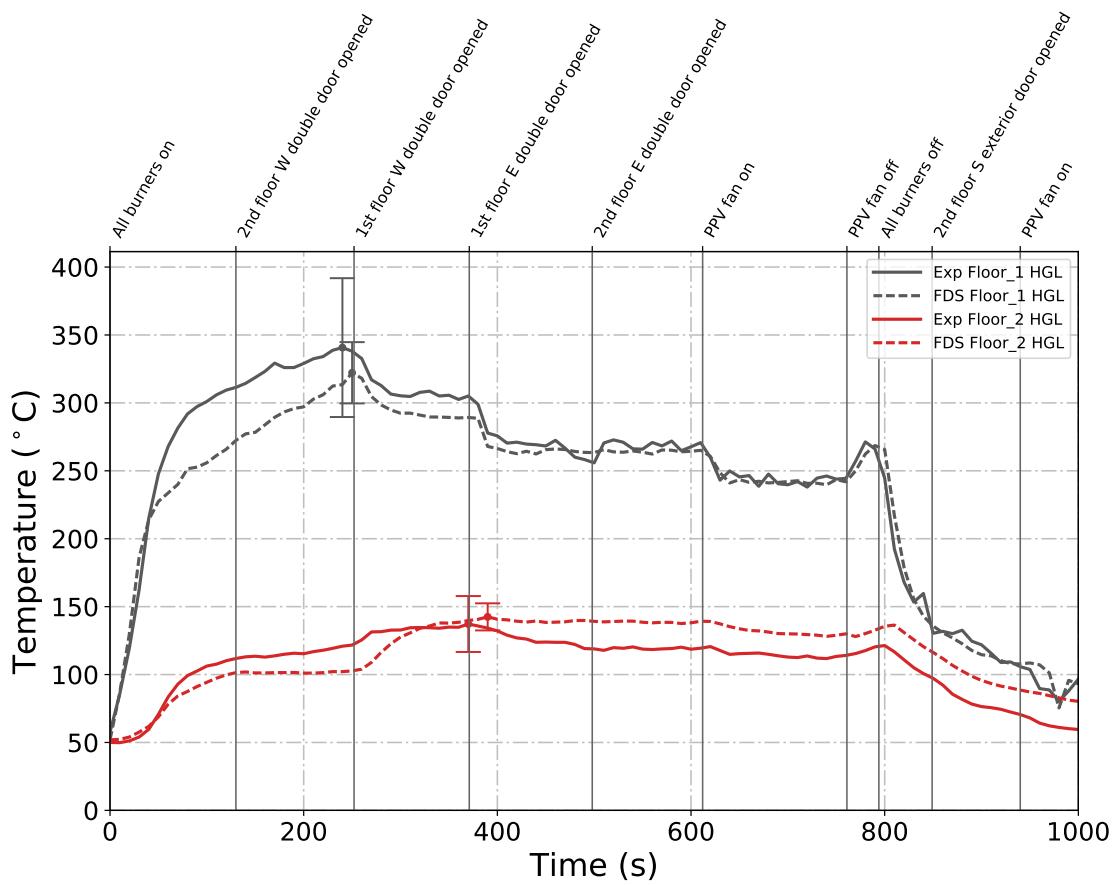


Figure B.6: Plots of measured and predicted hot gas layer temperatures on the first and second floors of the West Structure during Test 23.

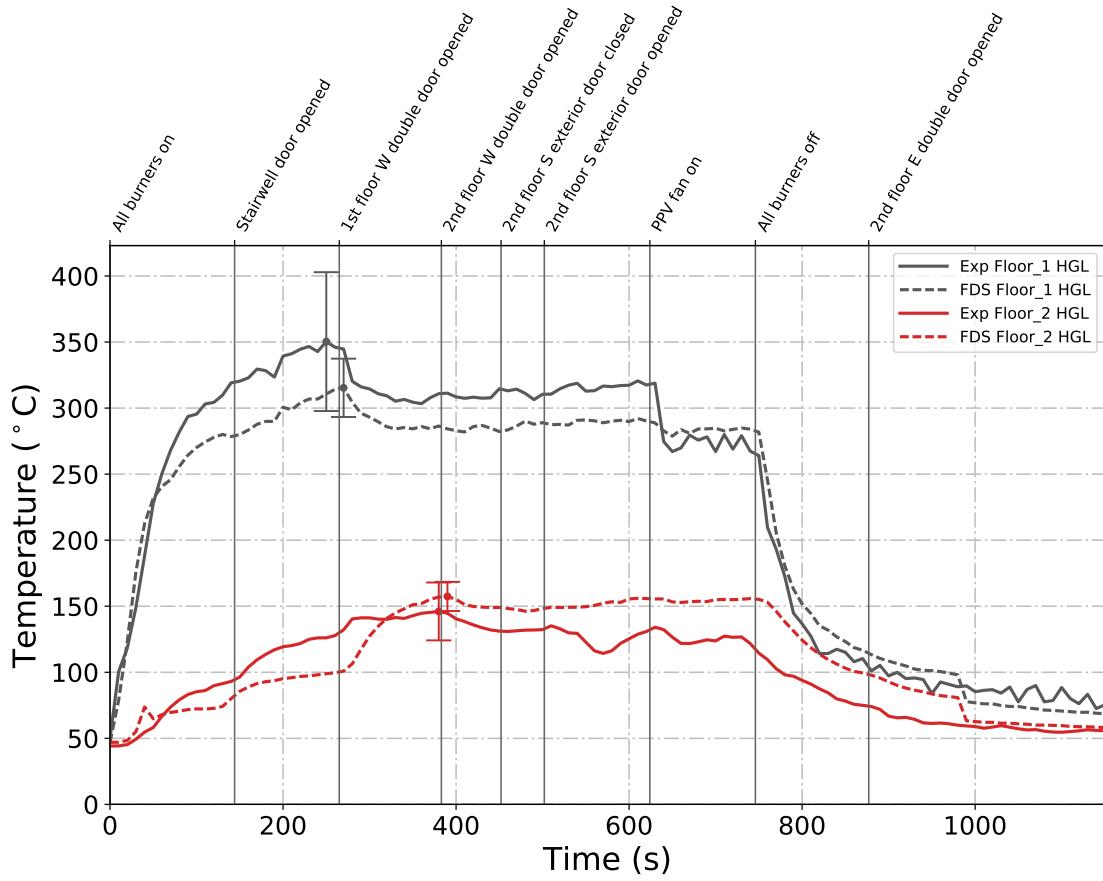


Figure B.7: Plots of measured and predicted hot gas layer temperatures on the first and second floors of the West Structure during Test 24.

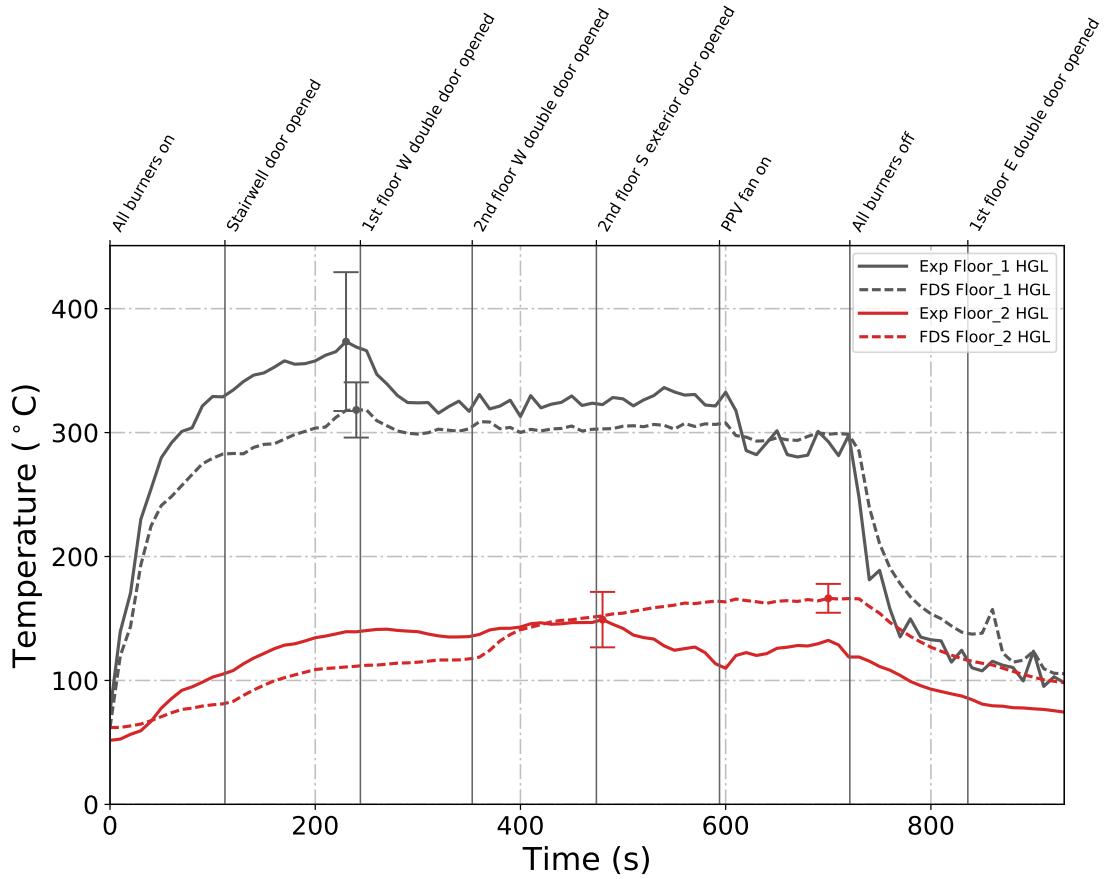


Figure B.8: Plots of measured and predicted hot gas layer temperatures on the first and second floors of the West Structure during Test 25.

Ceiling Jet Temperatures

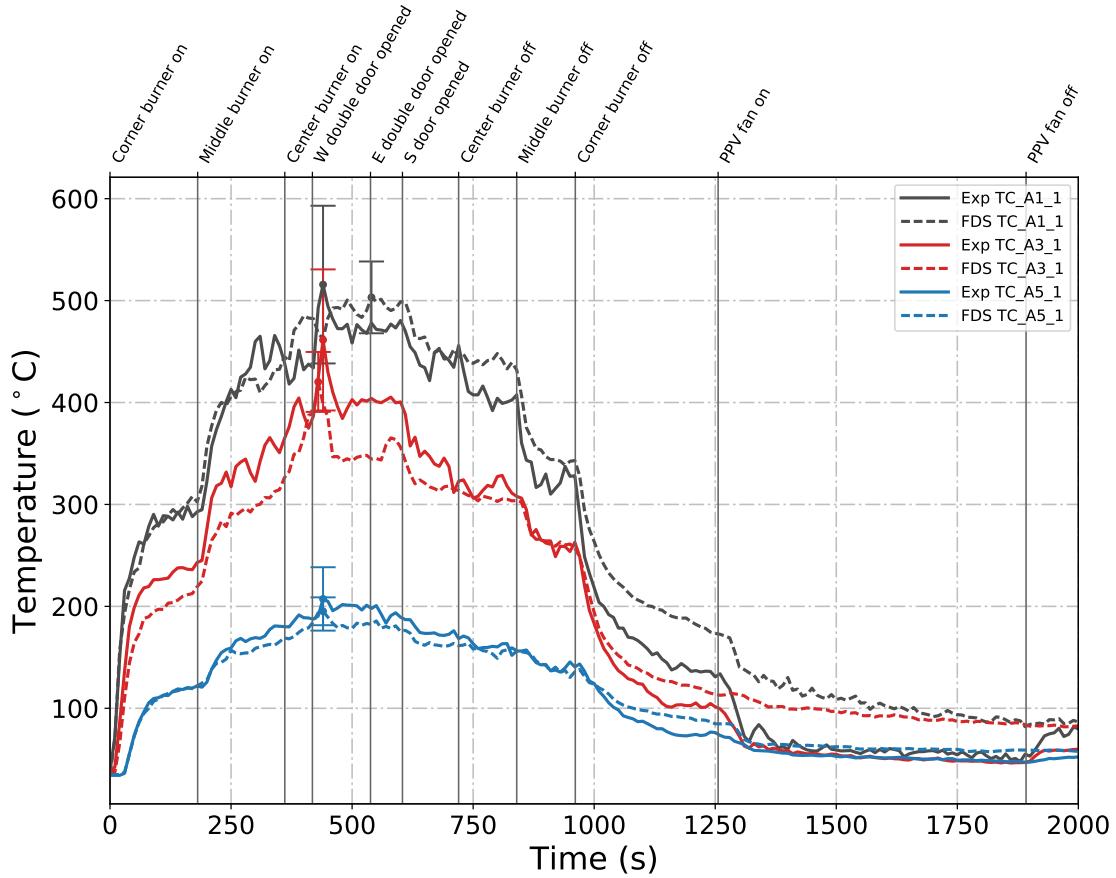


Figure B.9: Plots of measured and predicted ceiling jet temperatures during Test 2 obtained from thermocouple arrays A1, A3, and A5 located in the fire room, middle room, and north room of the East Structure, respectively.

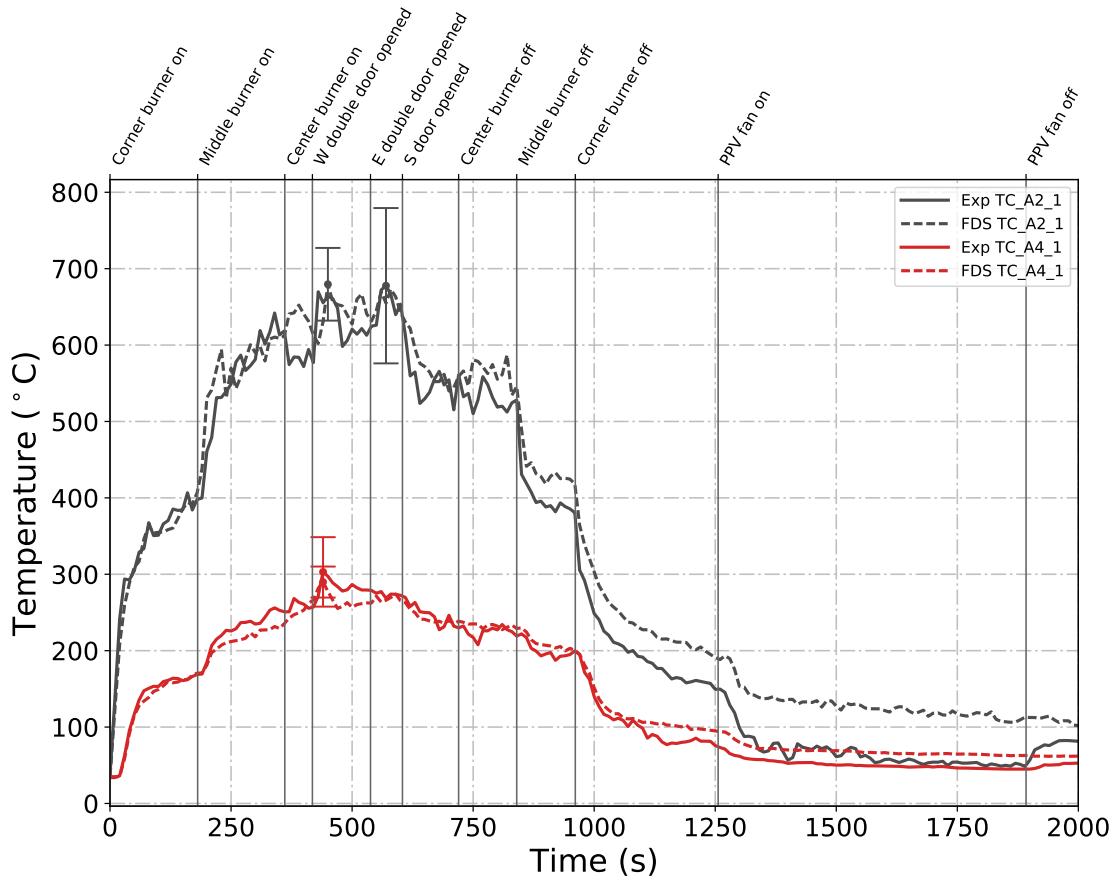


Figure B.10: Plots of measured and predicted ceiling jet temperatures during Test 2 obtained from thermocouple arrays A2 and A4 located in the fire room and north room of the East Structure, respectively.

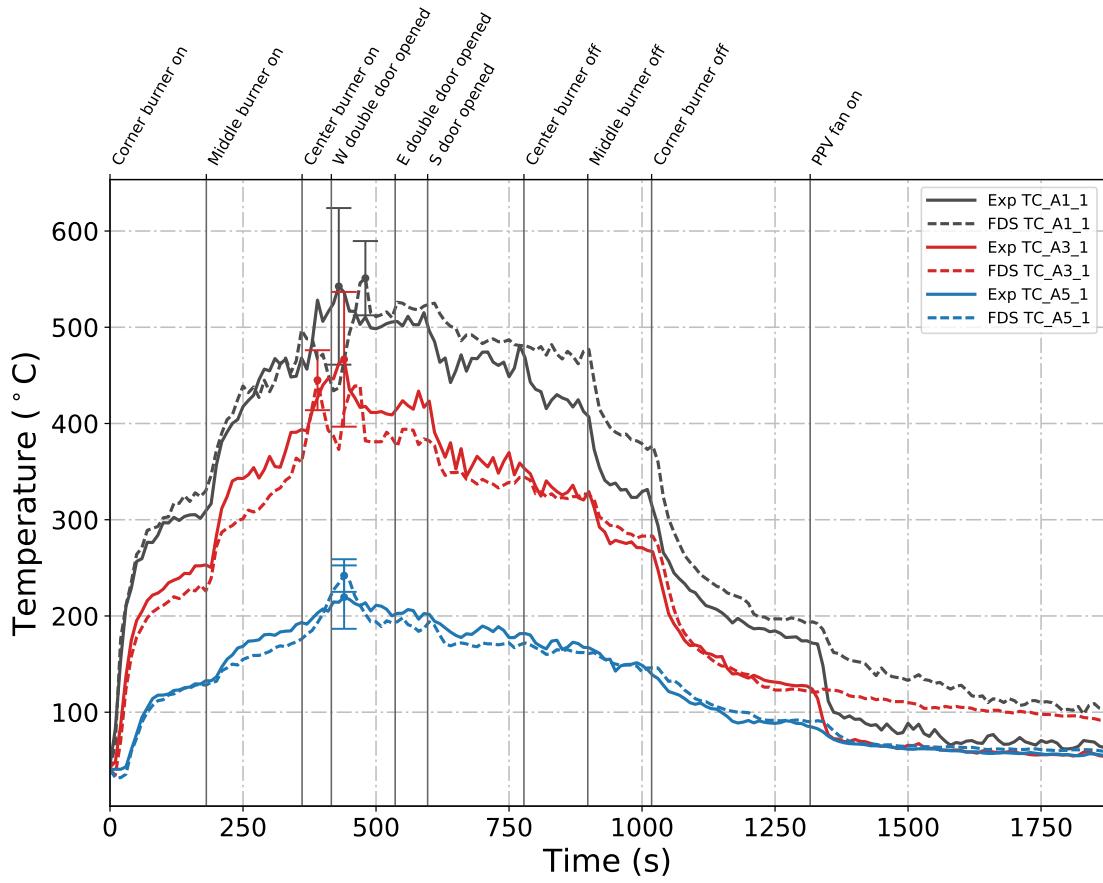


Figure B.11: Plots of measured and predicted ceiling jet temperatures during Test 3 obtained from thermocouple arrays A1, A3, and A5 located in the fire room, middle room, and north room of the East Structure, respectively.

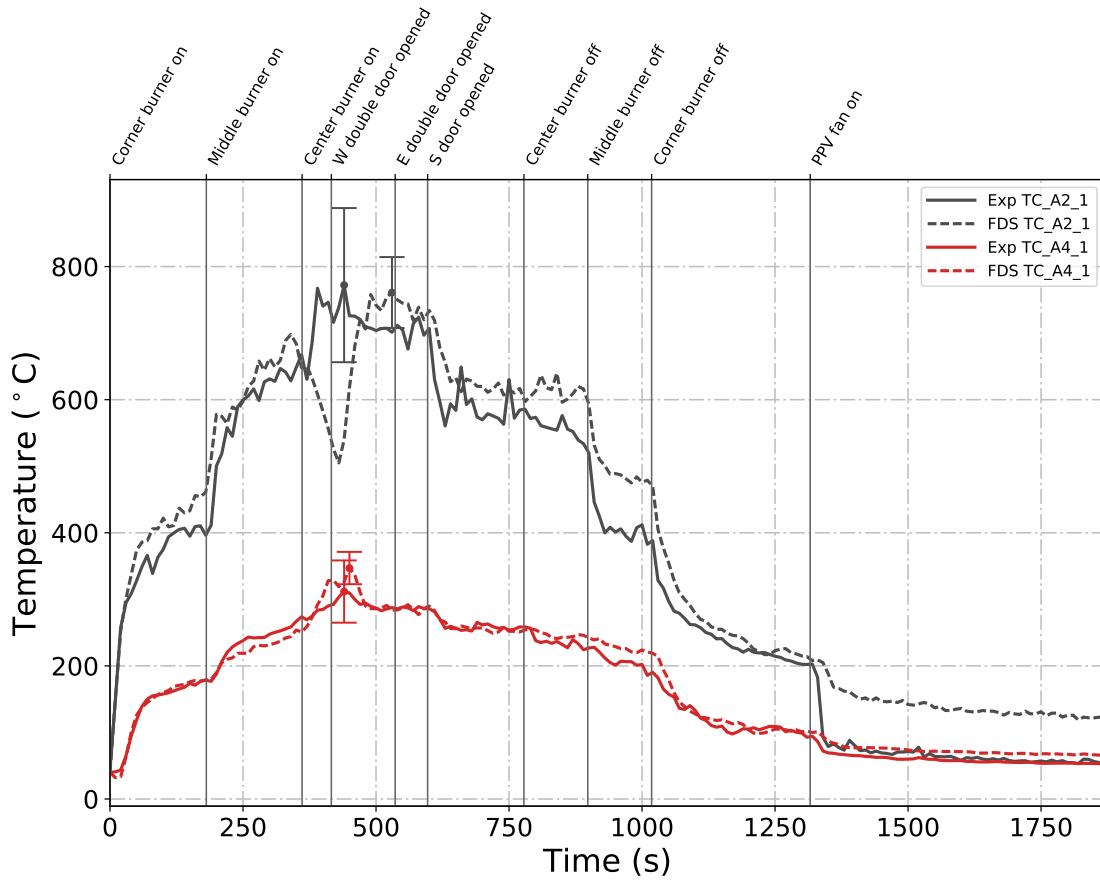


Figure B.12: Plots of measured and predicted ceiling jet temperatures during Test 3 obtained from thermocouple arrays A2 and A4 located in the fire room and north room of the East Structure, respectively.

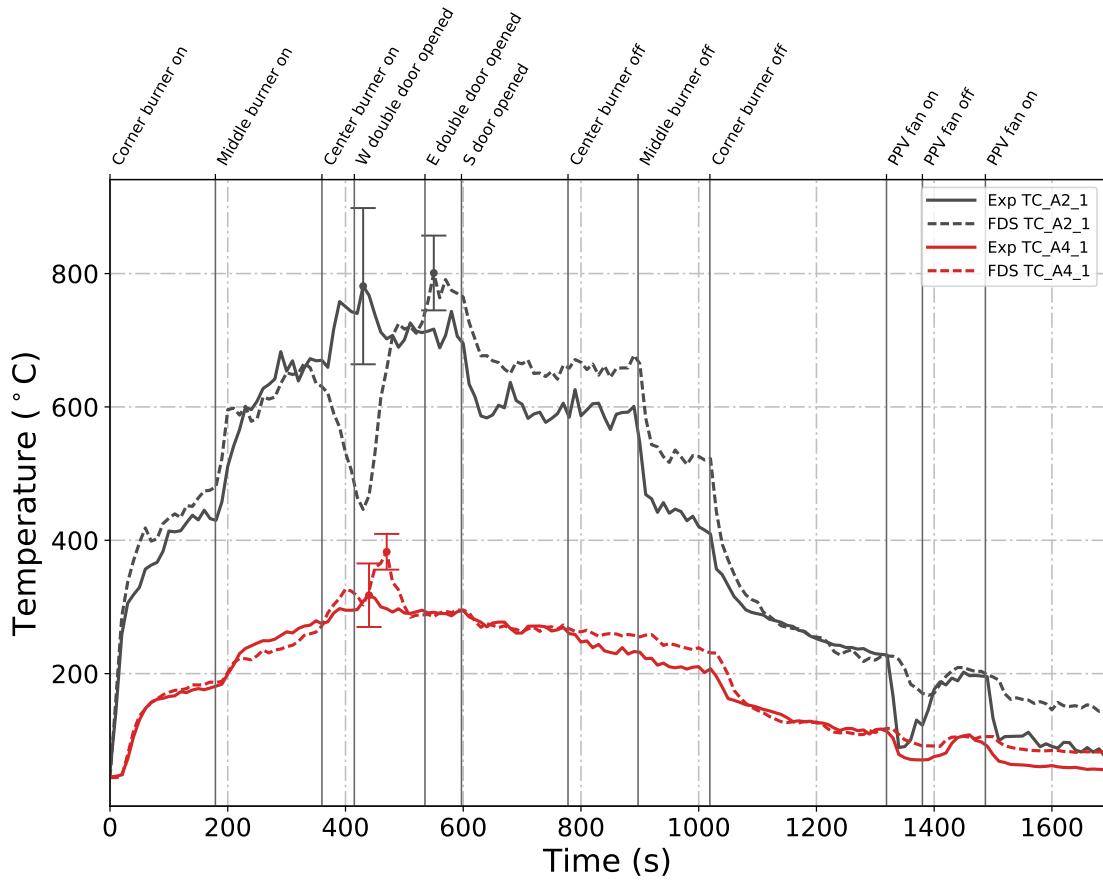


Figure B.13: Plots of measured and predicted ceiling jet temperatures during Test 4 obtained from thermocouple arrays A2 and A4 located in the fire room and north room of the East Structure, respectively.

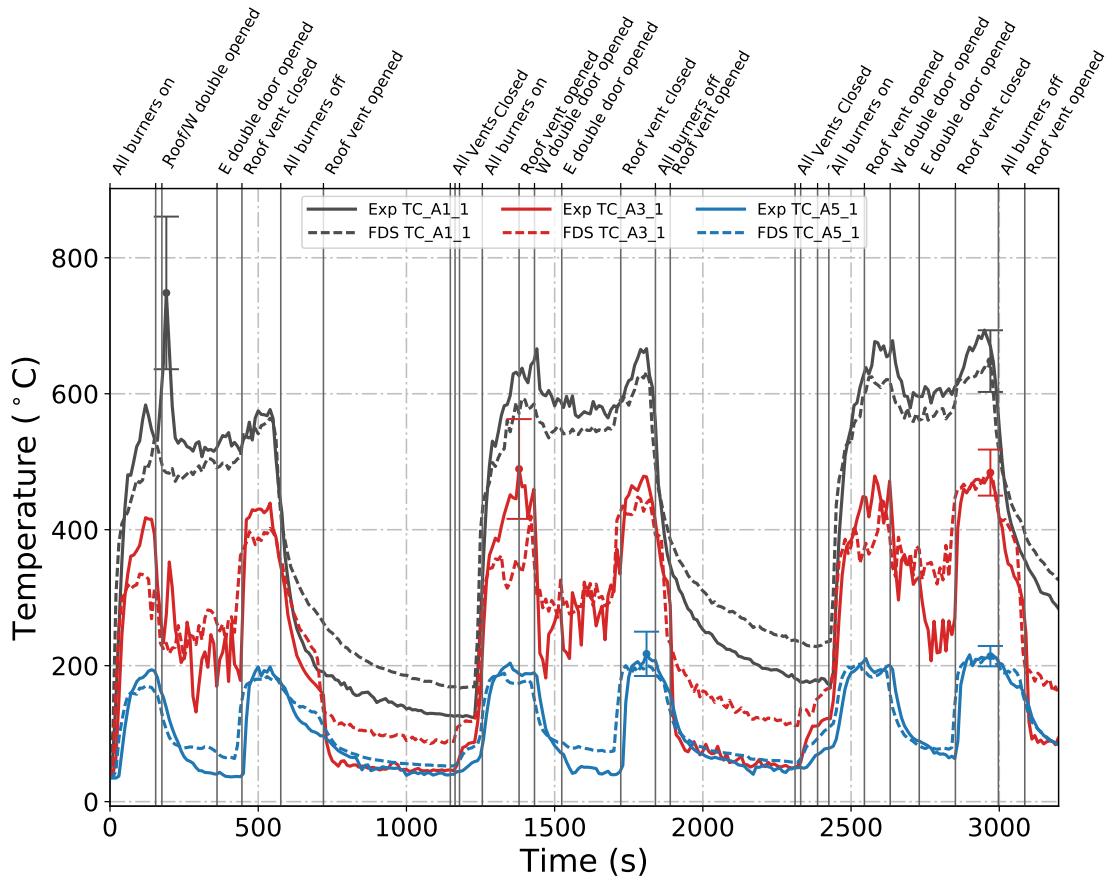


Figure B.14: Plots of measured and predicted ceiling jet temperatures during Test 5 obtained from thermocouple arrays A1, A3, and A5 located in the fire room, middle room, and north room of the East Structure, respectively.

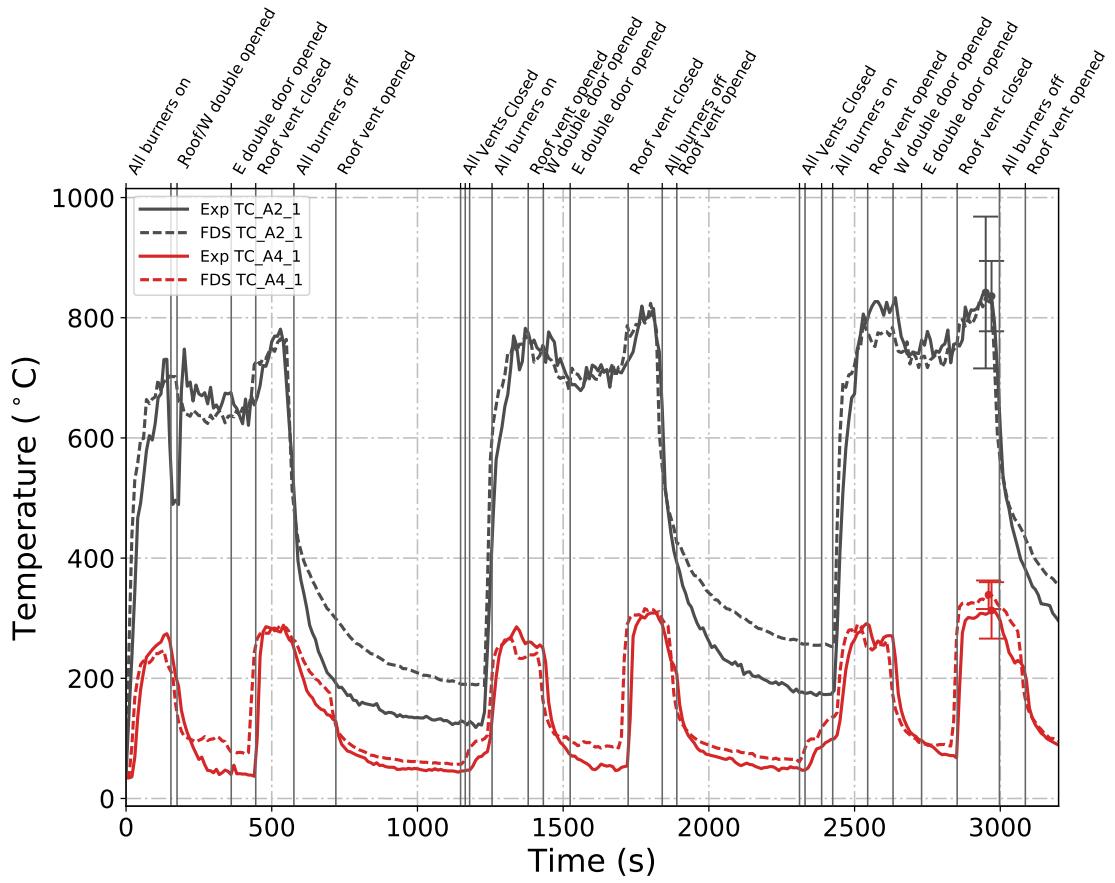


Figure B.15: Plots of measured and predicted ceiling jet temperatures during Test 5 obtained from thermocouple arrays A2 and A4 located in the fire room and north room of the East Structure, respectively.

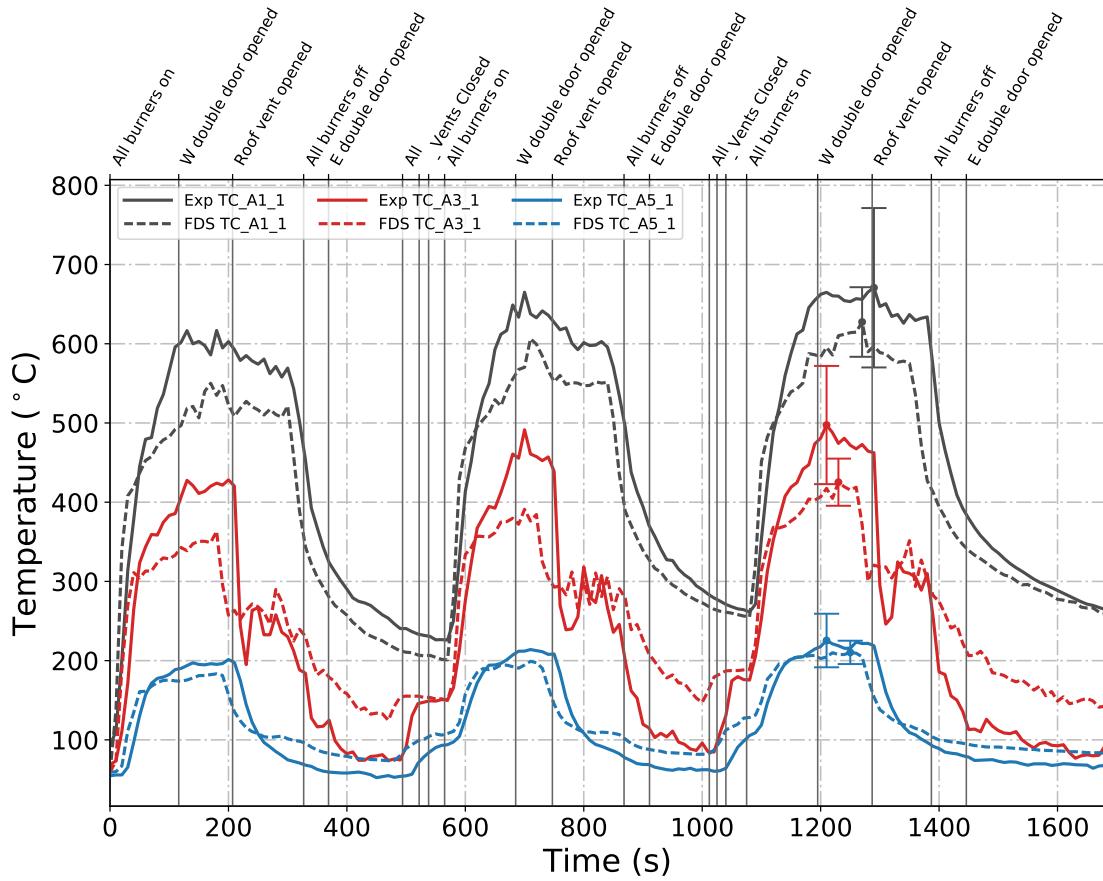


Figure B.16: Plots of measured and predicted ceiling jet temperatures during Test 6 obtained from thermocouple arrays A1, A3, and A5 located in the fire room, middle room, and north room of the East Structure, respectively.

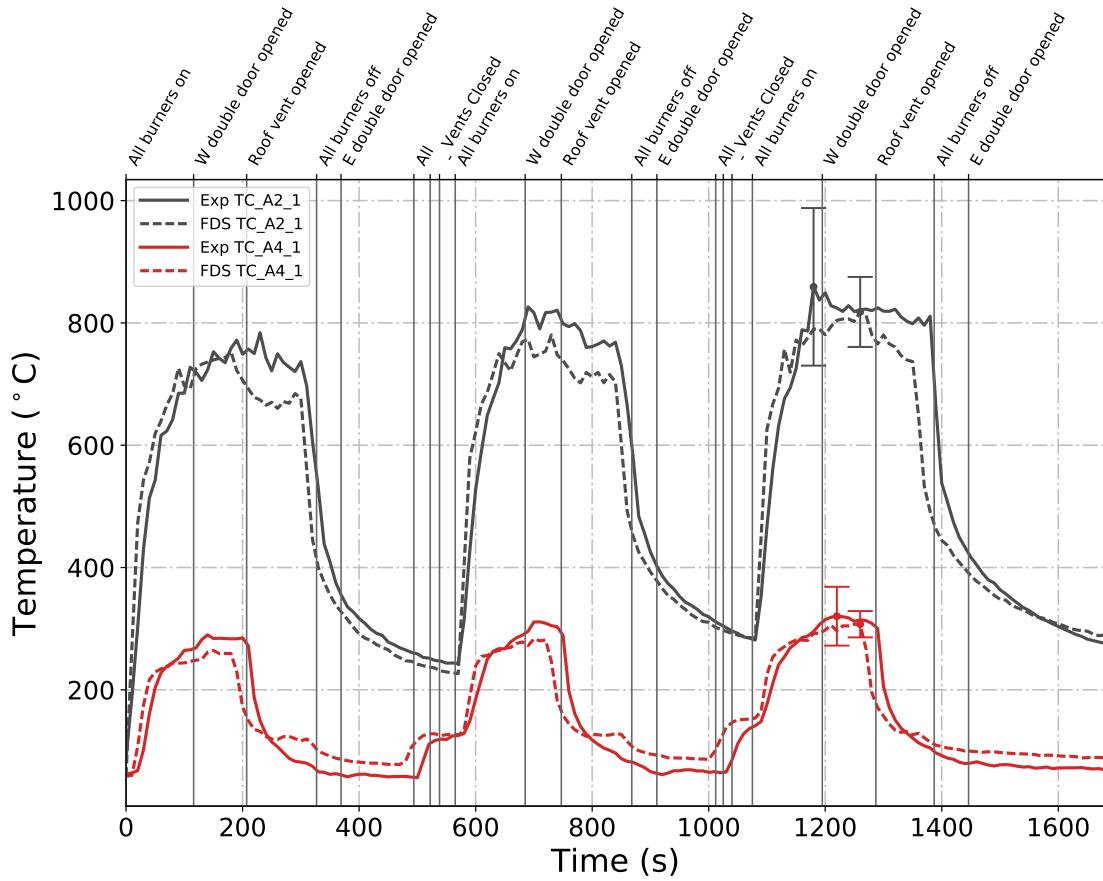


Figure B.17: Plots of measured and predicted ceiling jet temperatures during Test 6 obtained from thermocouple arrays A2 and A4 located in the fire room and north room of the East Structure, respectively.

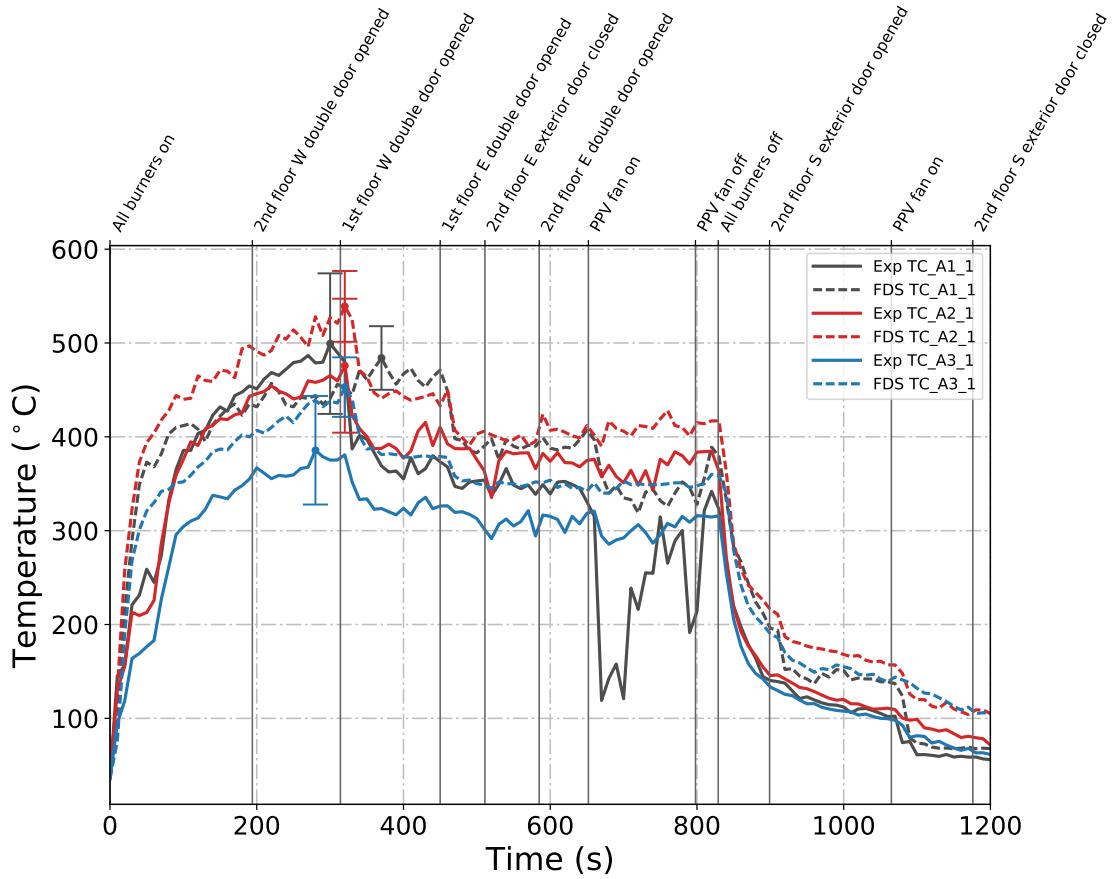


Figure B.18: Plots of measured and predicted ceiling jet temperatures on the first floor of the West Structure during Test 22.

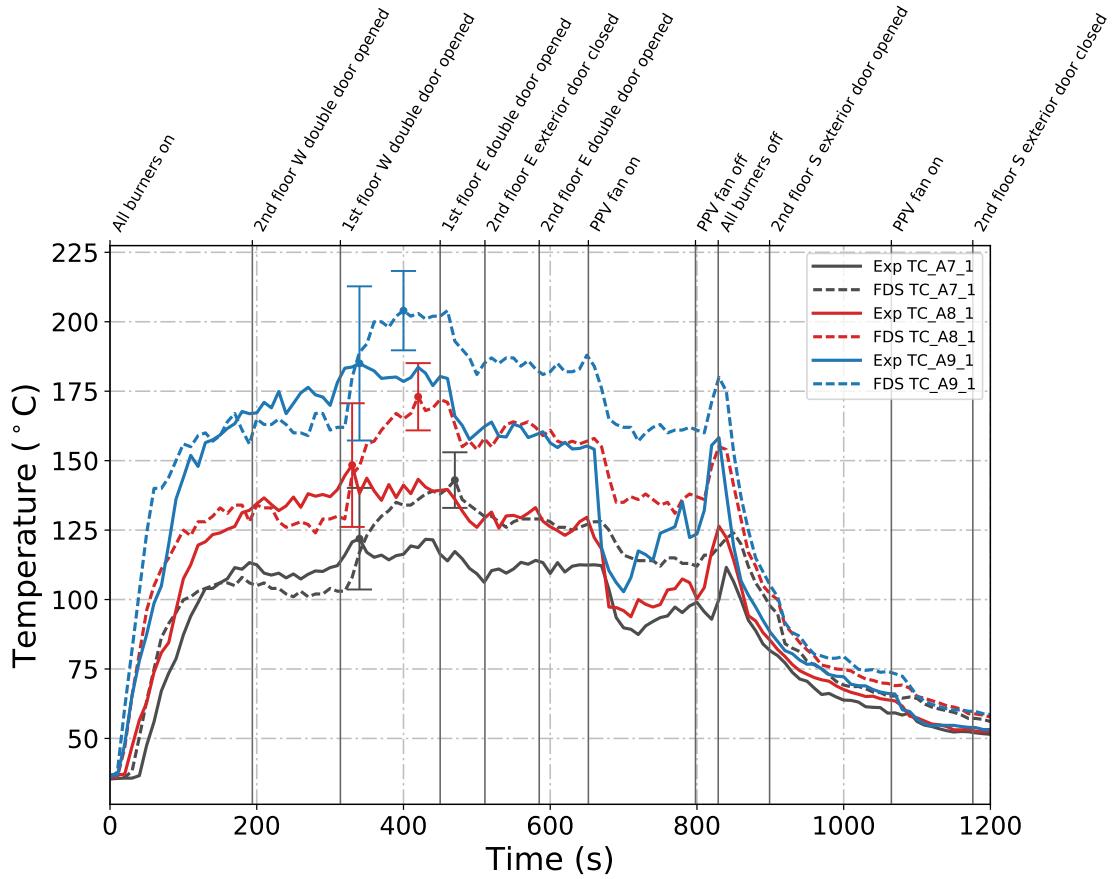


Figure B.19: Plots of measured and predicted ceiling jet temperatures on the second floor of the West Structure during Test 22.

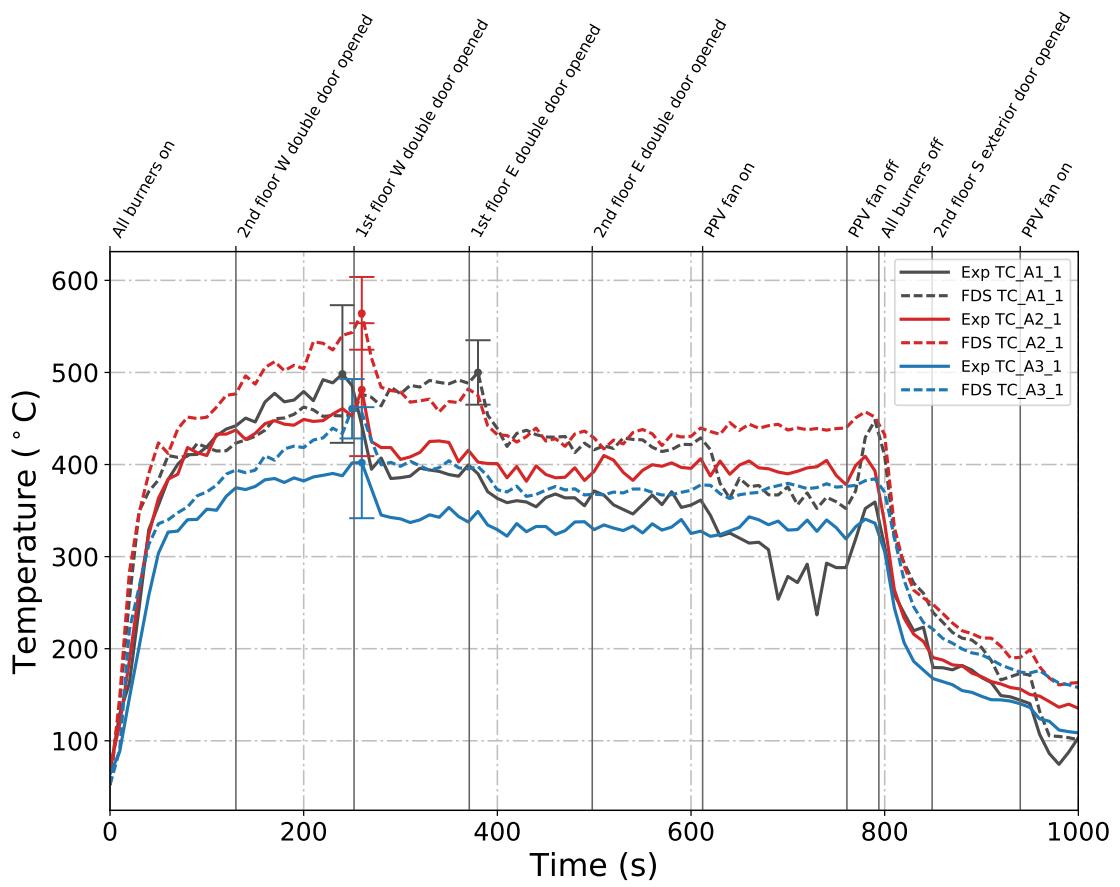


Figure B.20: Plots of measured and predicted ceiling jet temperatures on the first floor of the West Structure during Test 23.

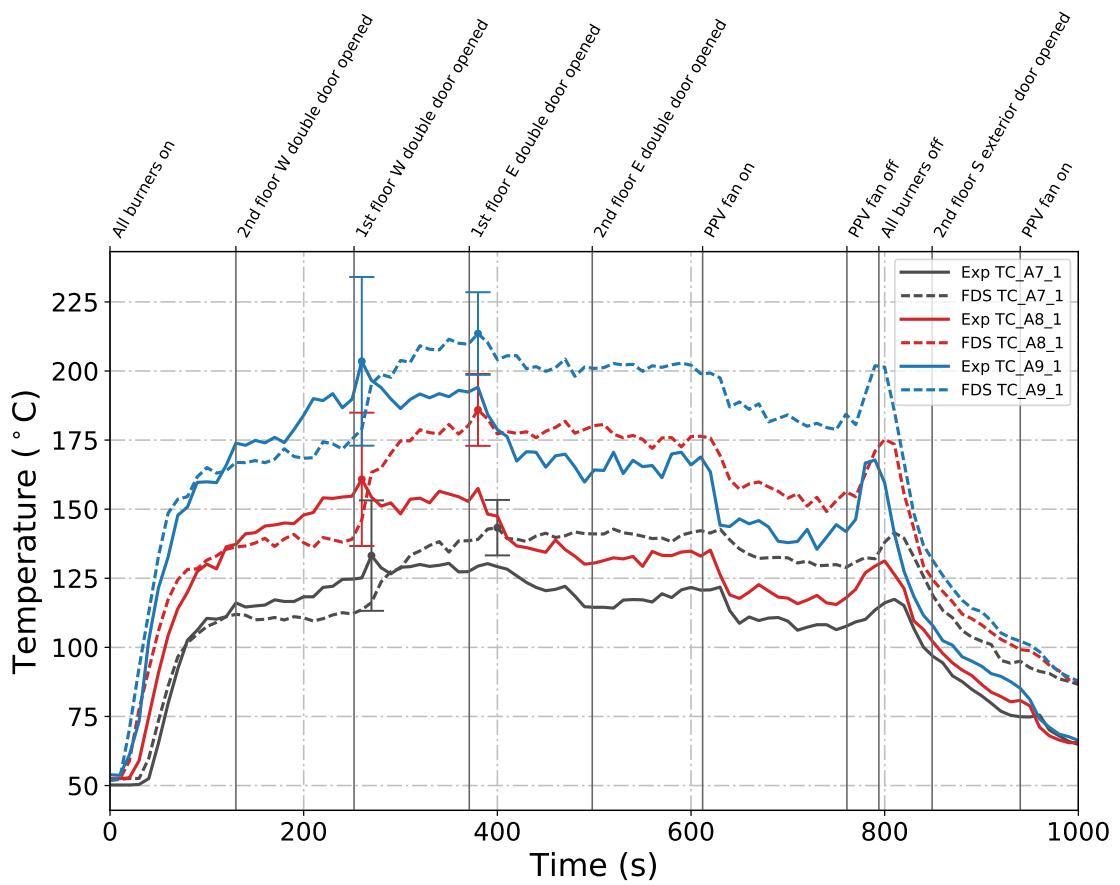


Figure B.21: Plots of measured and predicted ceiling jet temperatures on the second floor of the West Structure during Test 23.

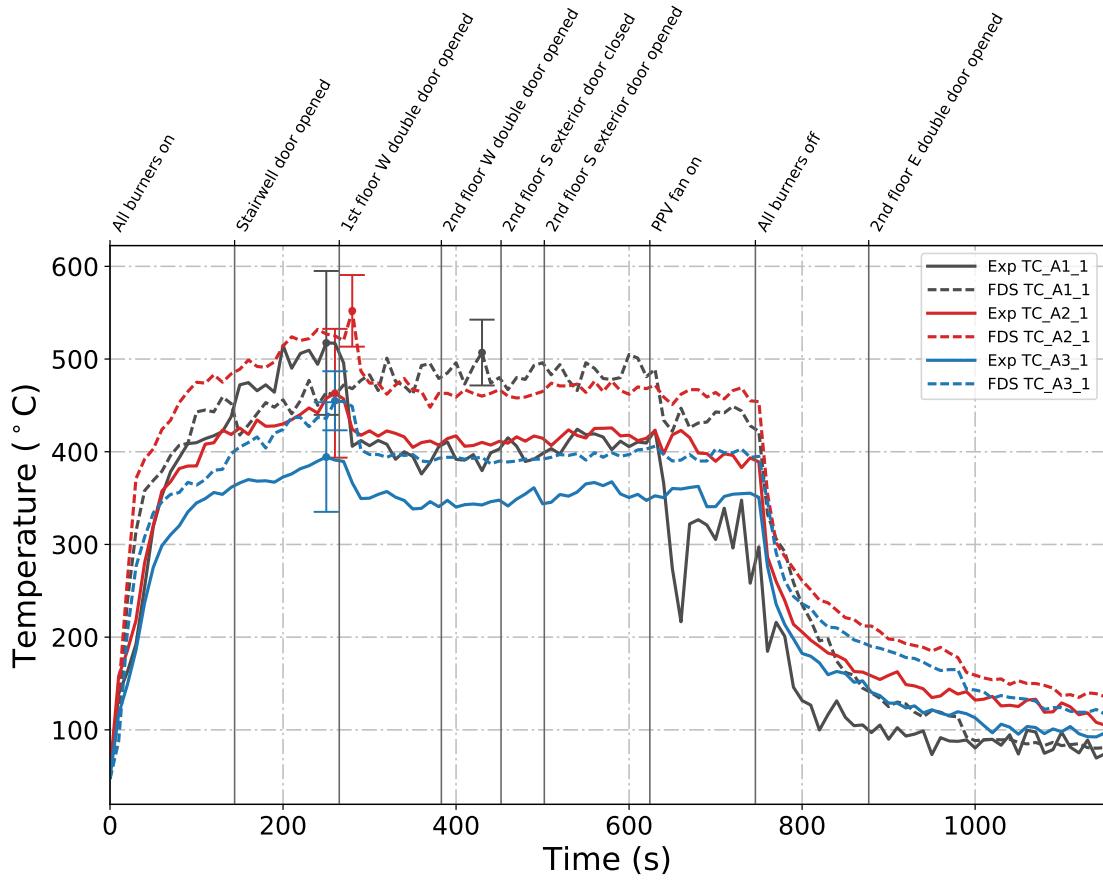


Figure B.22: Plots of measured and predicted ceiling jet temperatures on the first floor of the West Structure during Test 24.

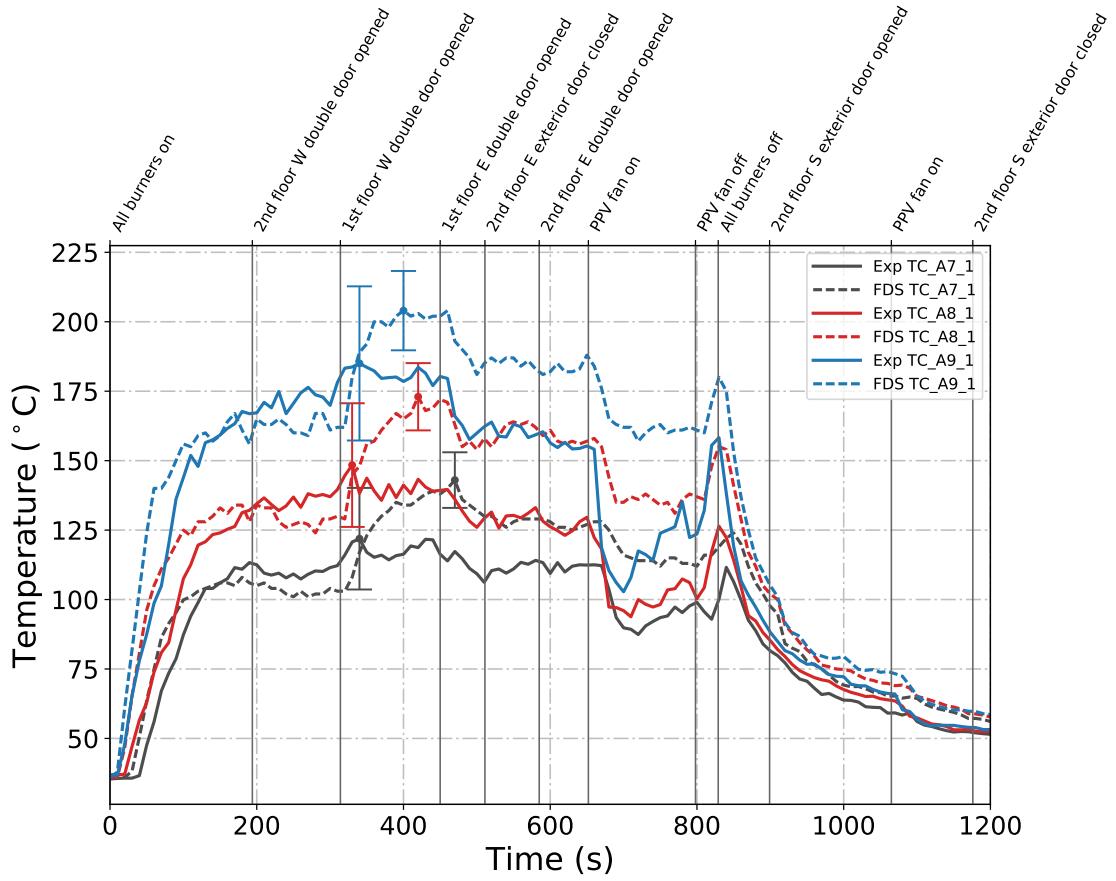


Figure B.23: Plots of measured and predicted ceiling jet temperatures on the second floor of the West Structure during Test 24.

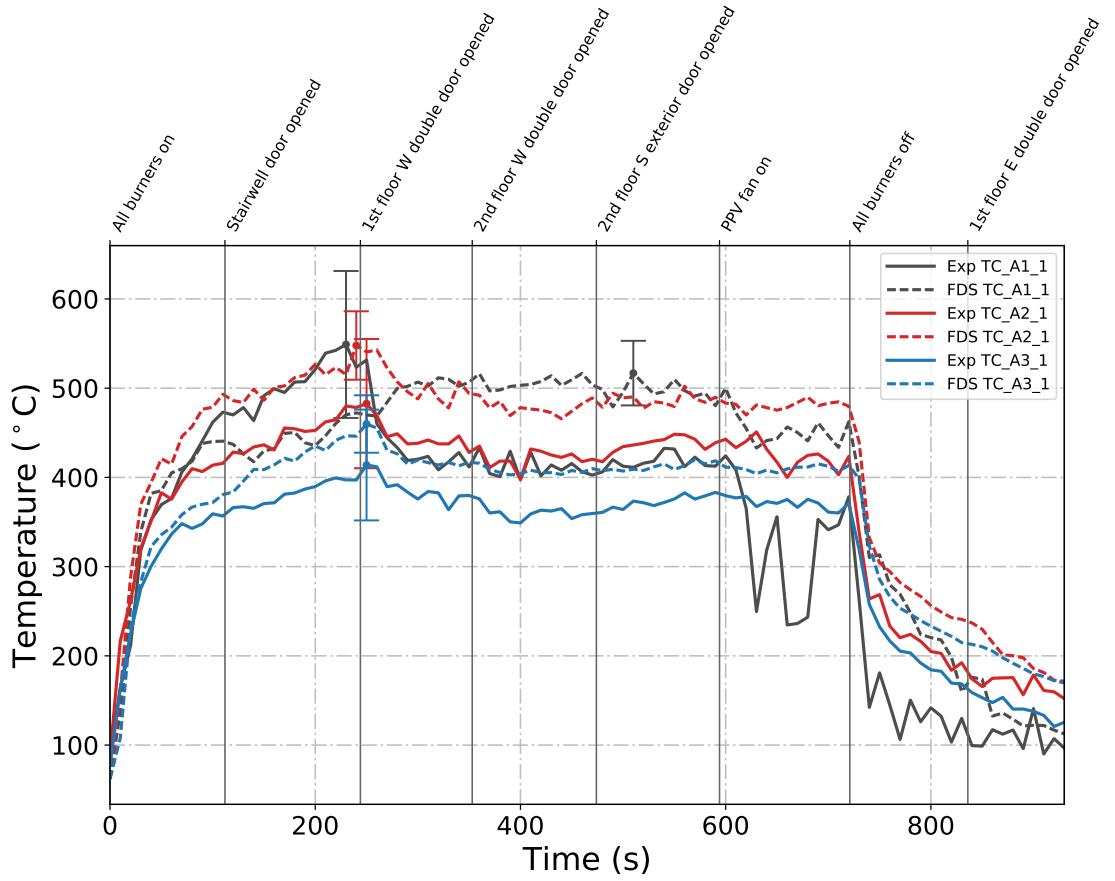


Figure B.24: Plots of measured and predicted ceiling jet temperatures on the first floor of the West Structure during Test 25.

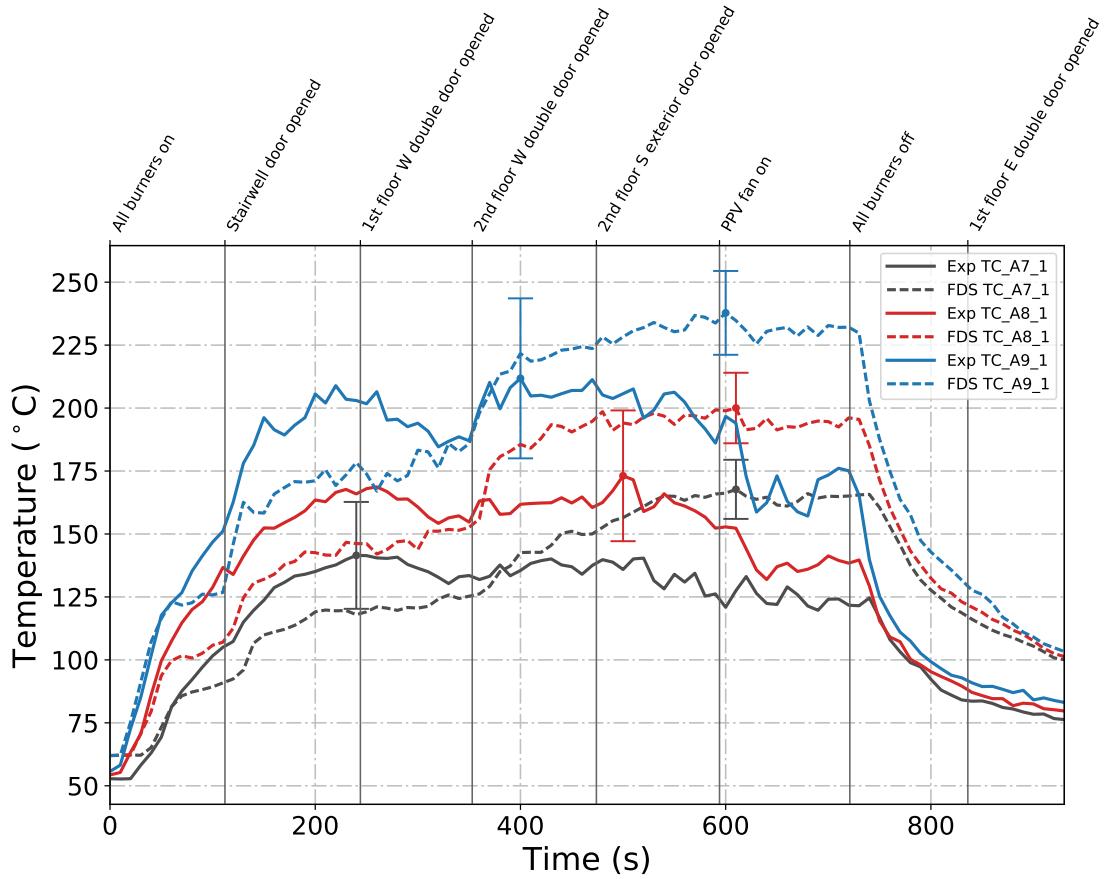


Figure B.25: Plots of measured and predicted ceiling jet temperatures on the second floor of the West Structure during Test 25.

Thermocouple Array Temperatures

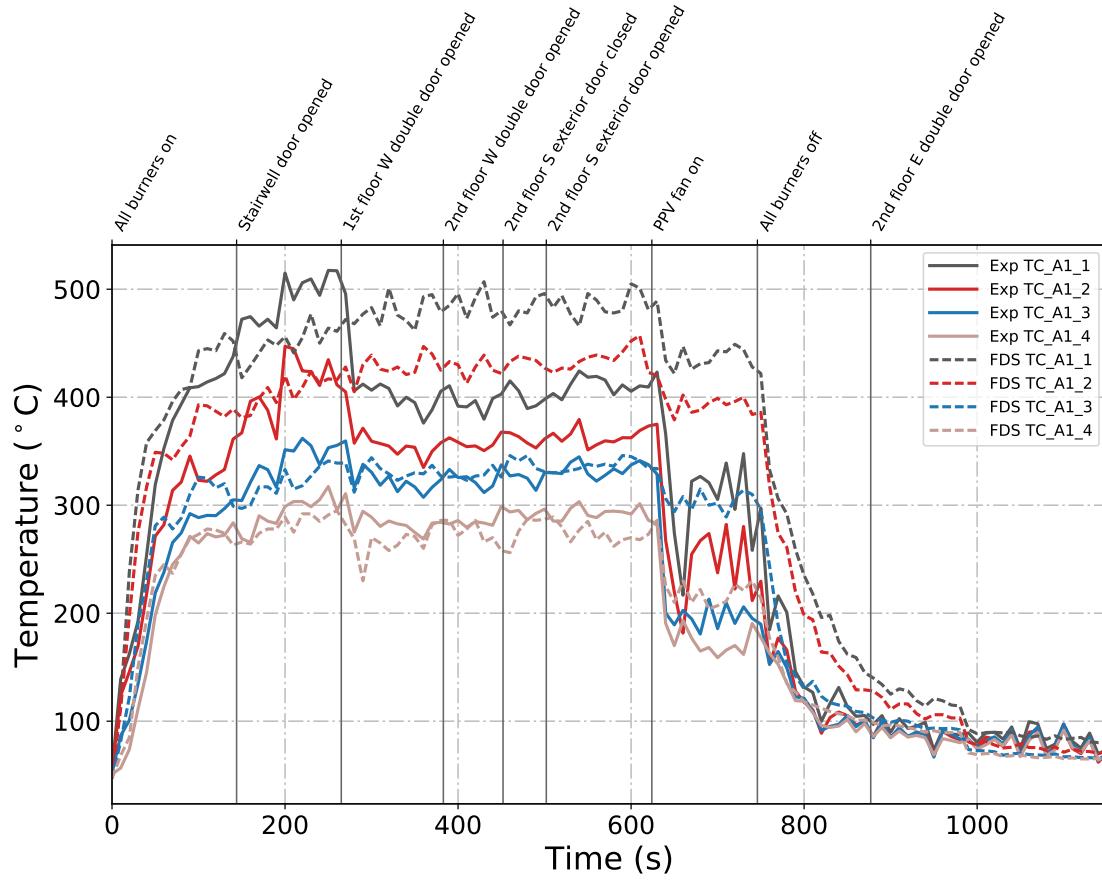


Figure B.26: Plots of measured and predicted temperatures during Test 24 obtained from thermocouple array A1.

B.2 Gas Species Concentration

O_2 Concentration

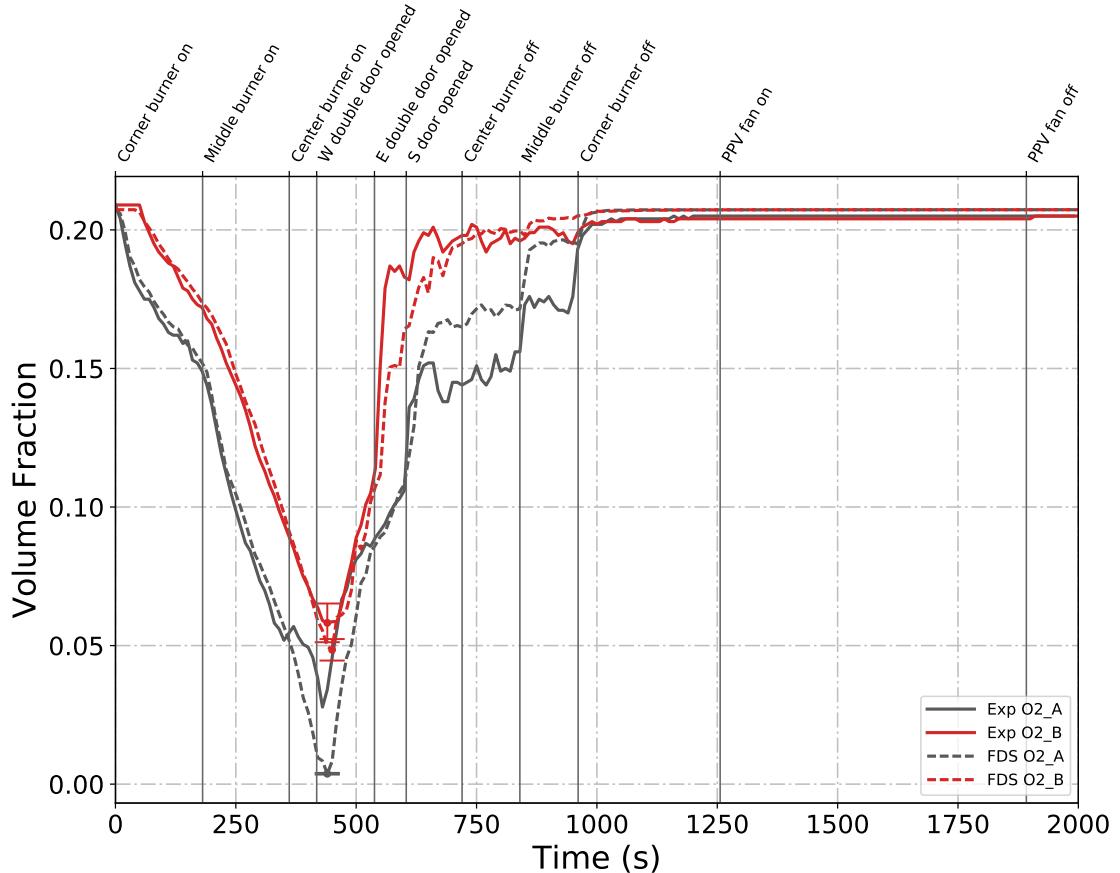


Figure B.27: Plots of measured and predicted O_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 2.

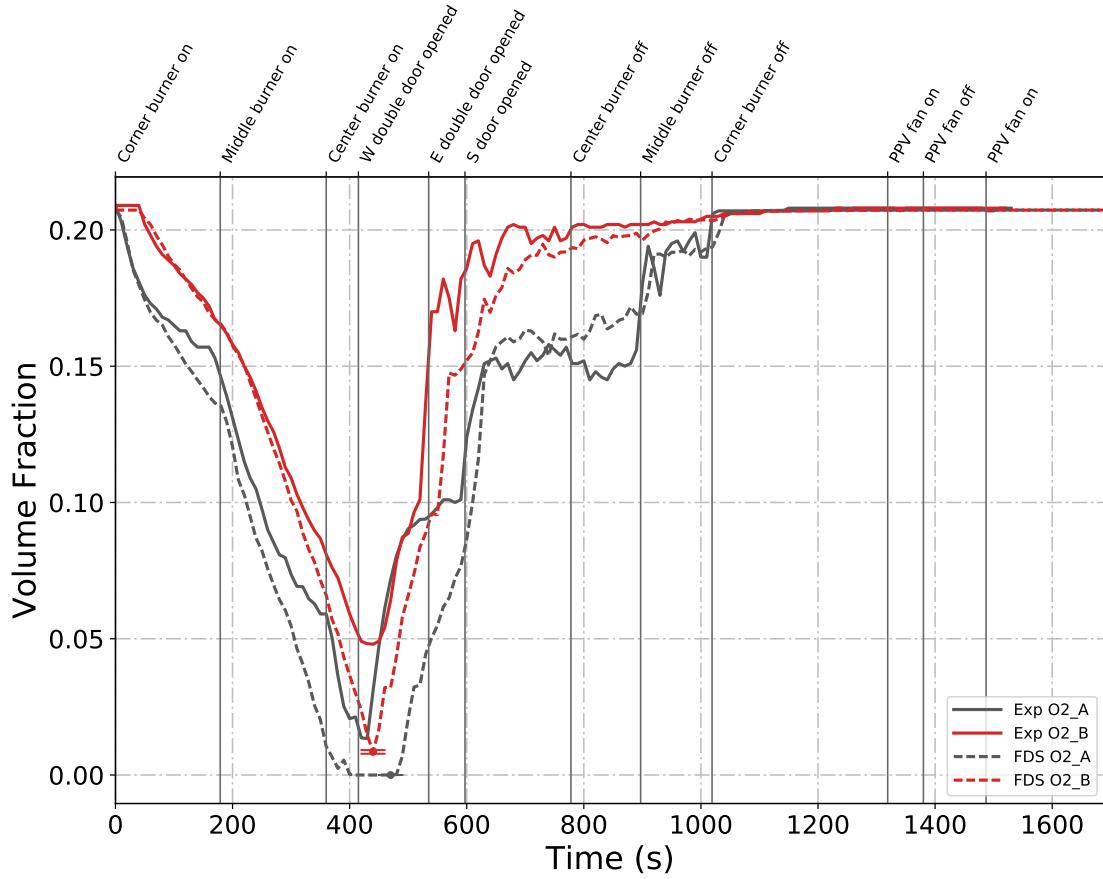


Figure B.28: Plots of measured and predicted O_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 4.

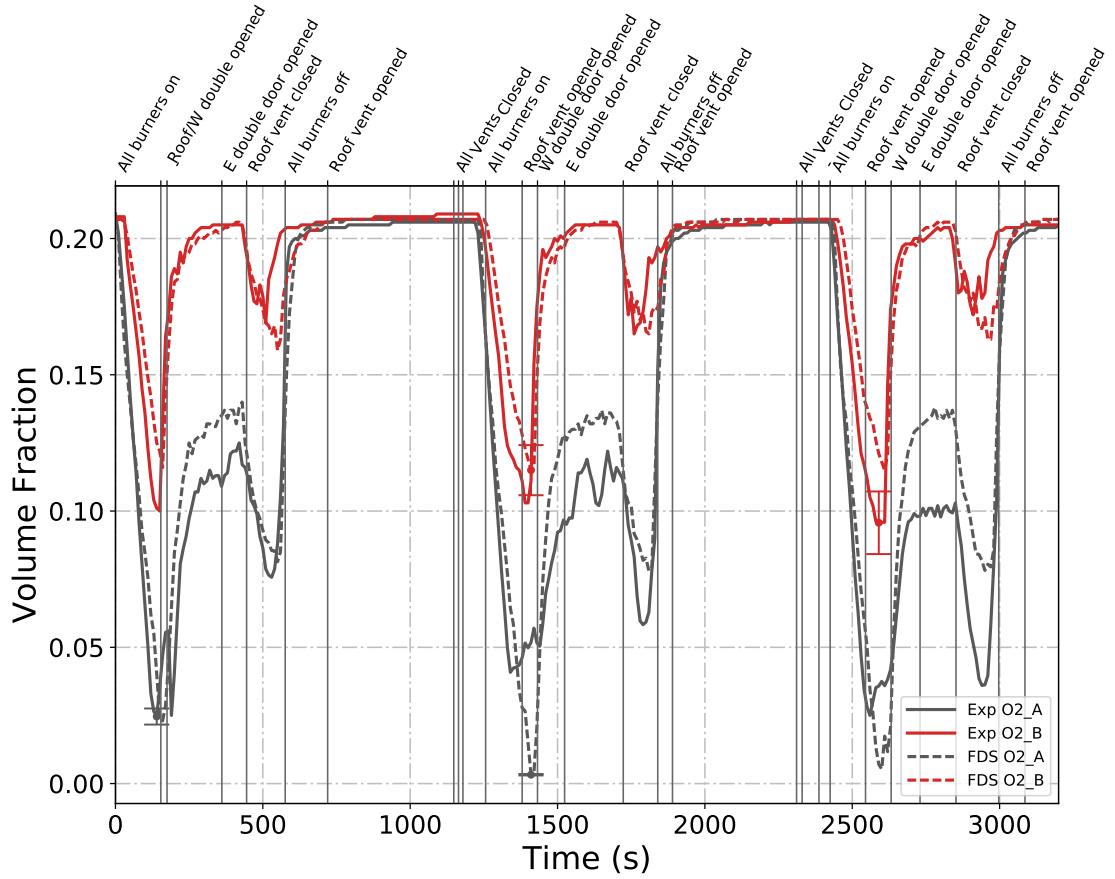
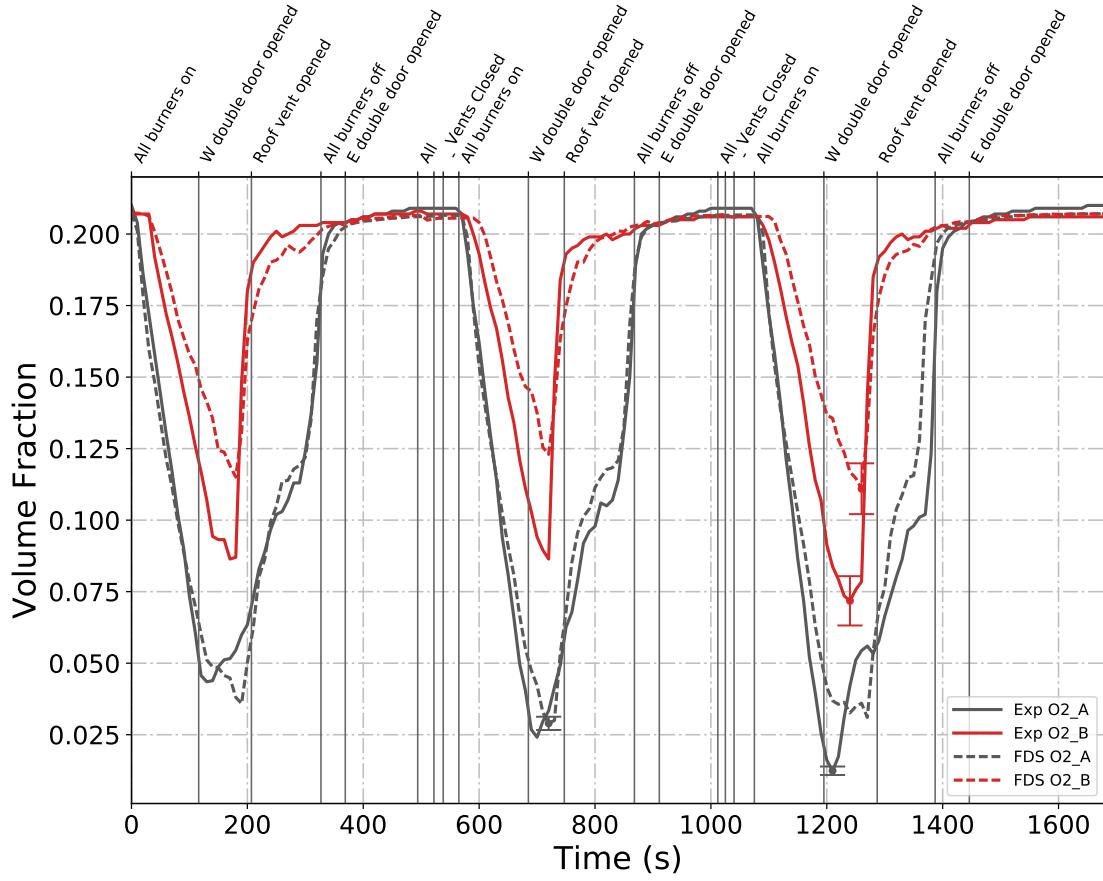


Figure B.29: Plots of measured and predicted O_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 5.



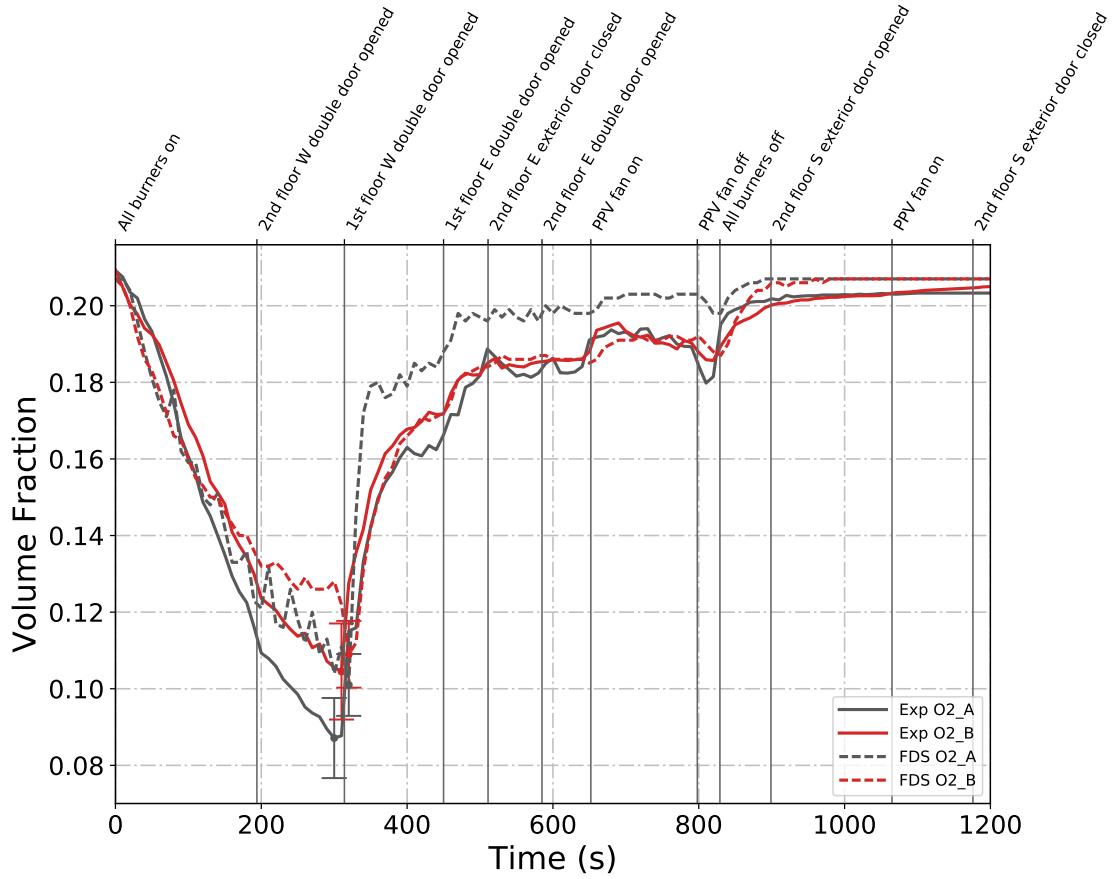


Figure B.31: Plots of measured and predicted O_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 22.

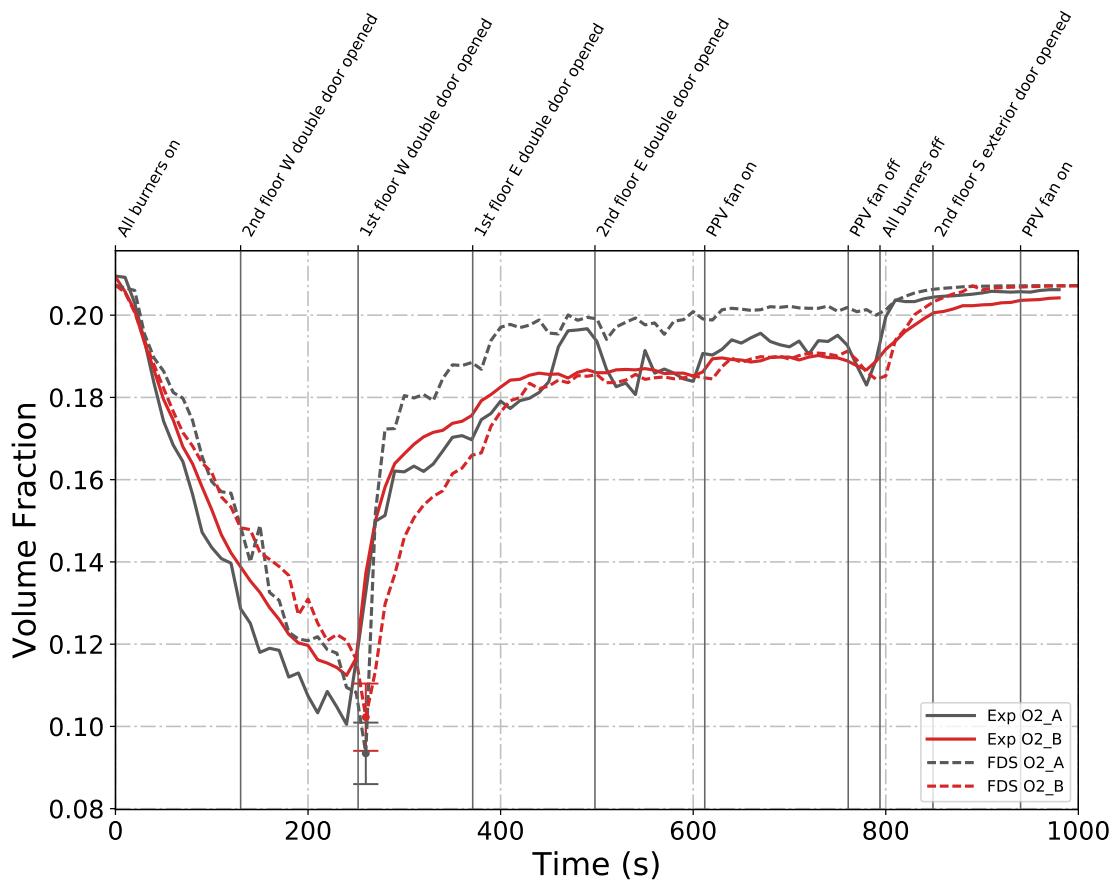


Figure B.32: Plots of measured and predicted O_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 23.

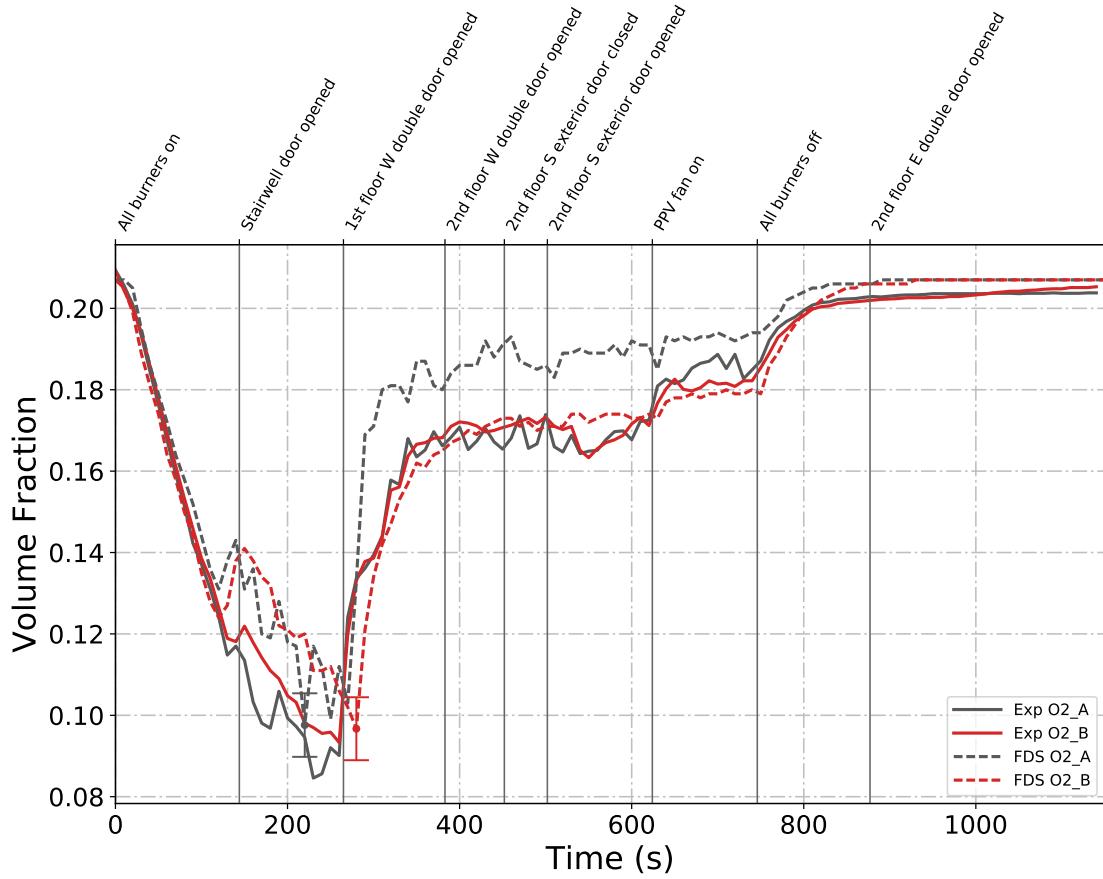


Figure B.33: Plots of measured and predicted O_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 24.

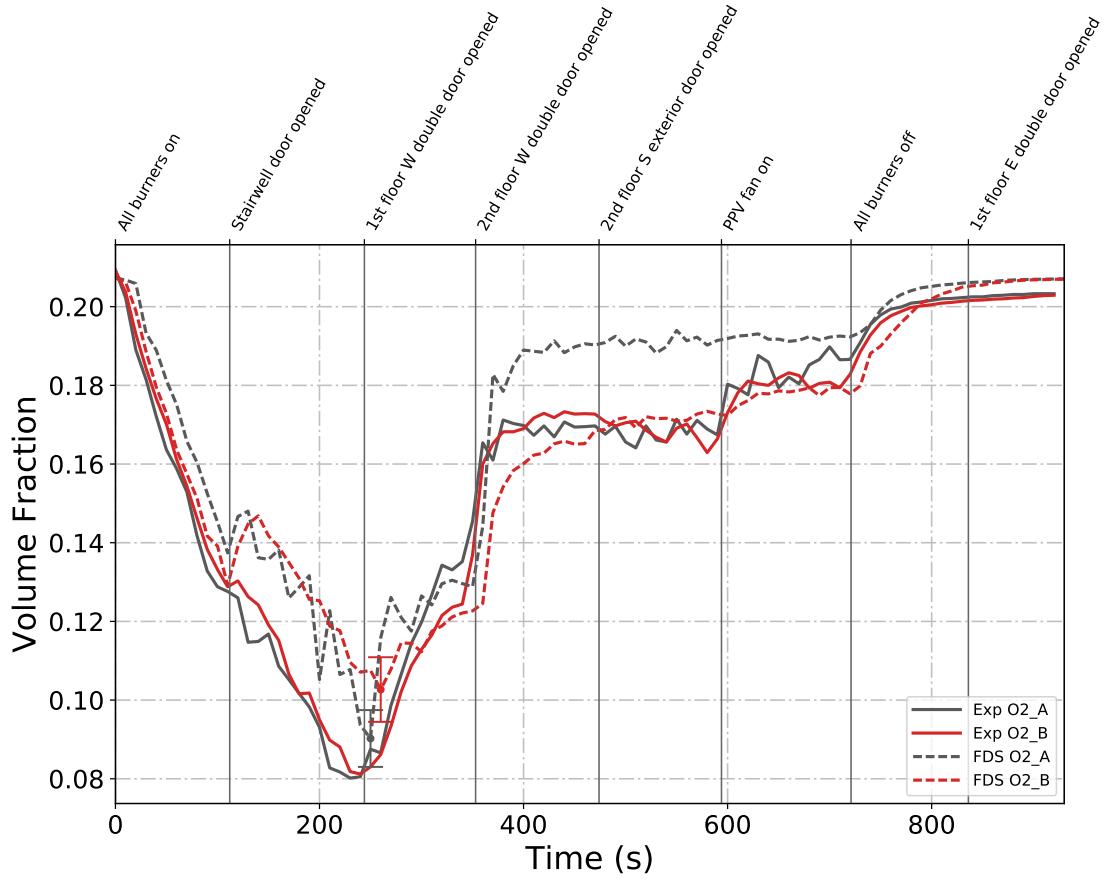


Figure B.34: Plots of measured and predicted O_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 25.

CO_2 Concentration

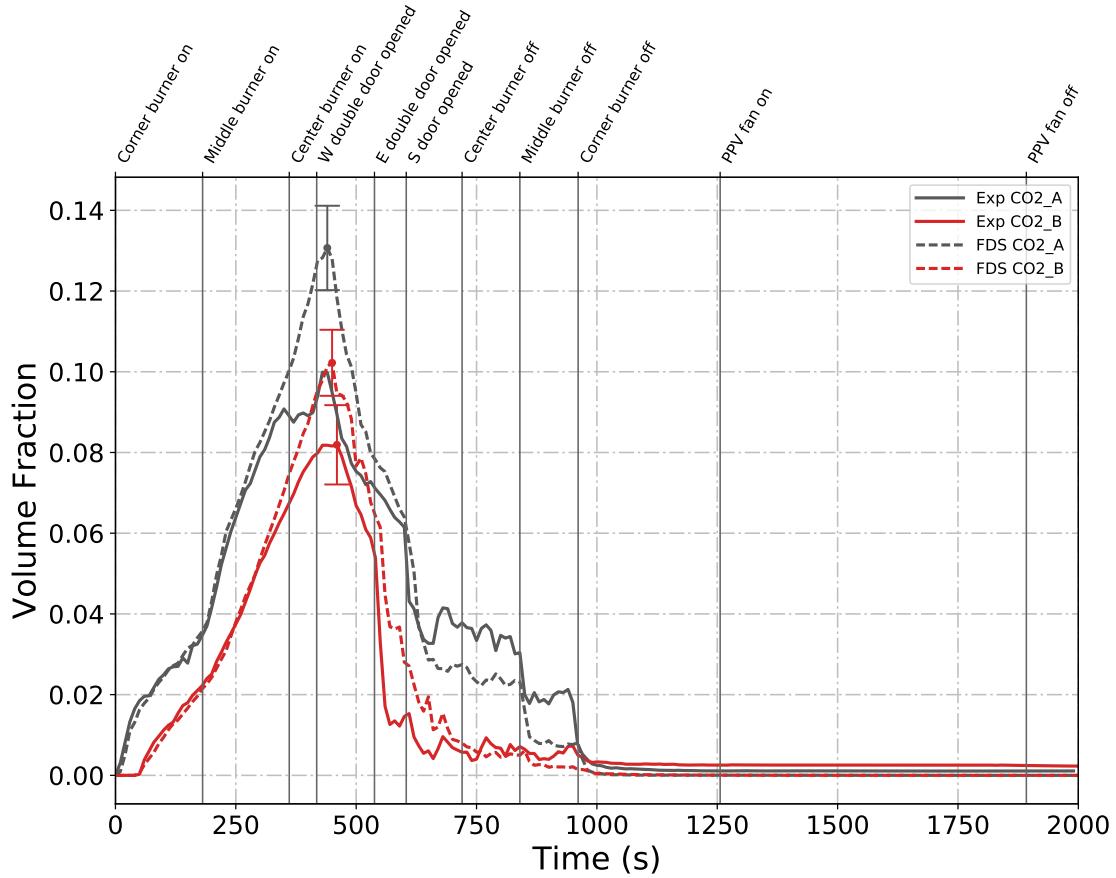


Figure B.35: Plots of measured and predicted CO_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 2.

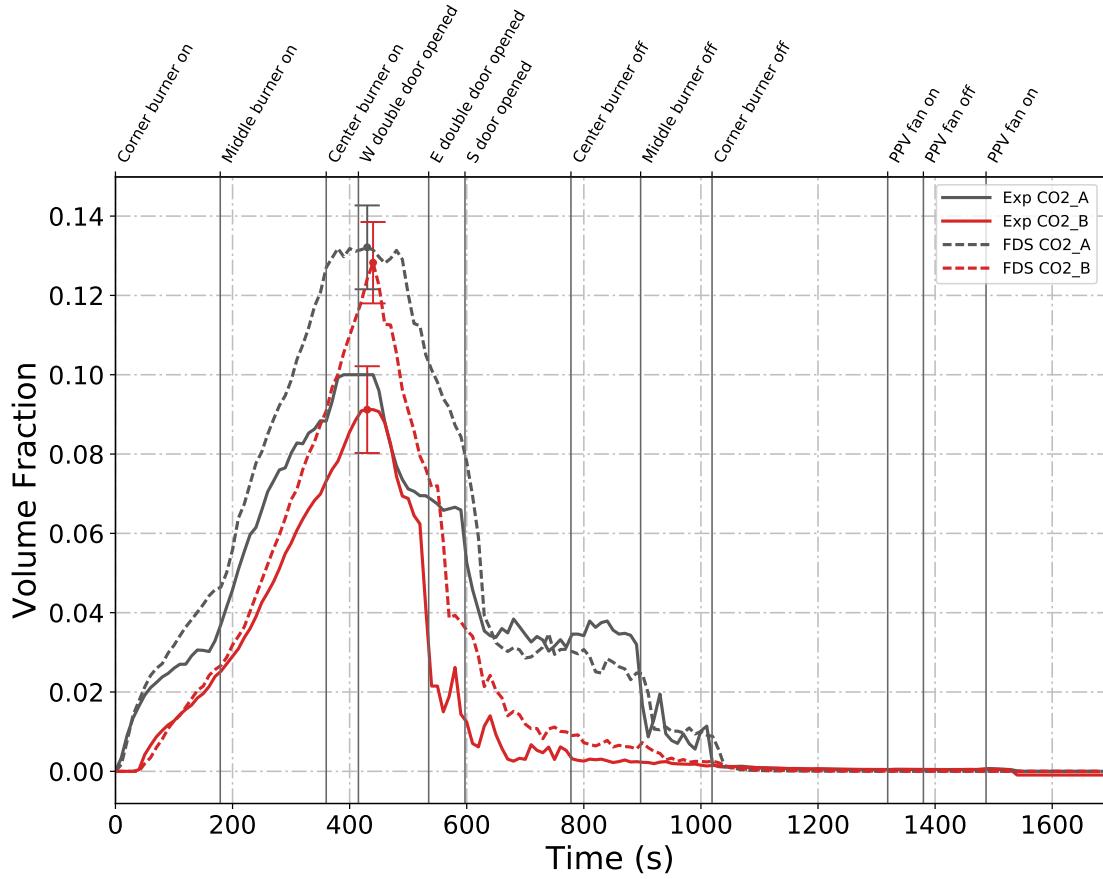


Figure B.36: Plots of measured and predicted CO_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 4.

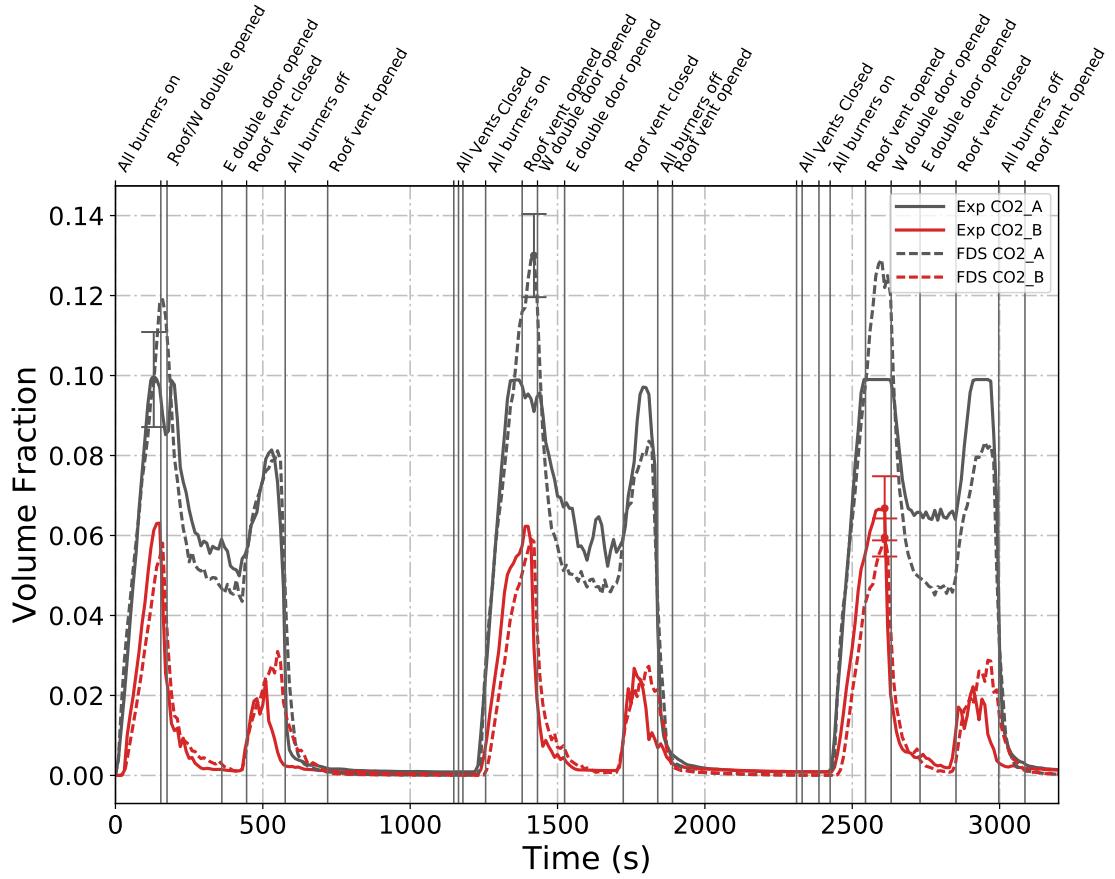


Figure B.37: Plots of measured and predicted CO_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 5.

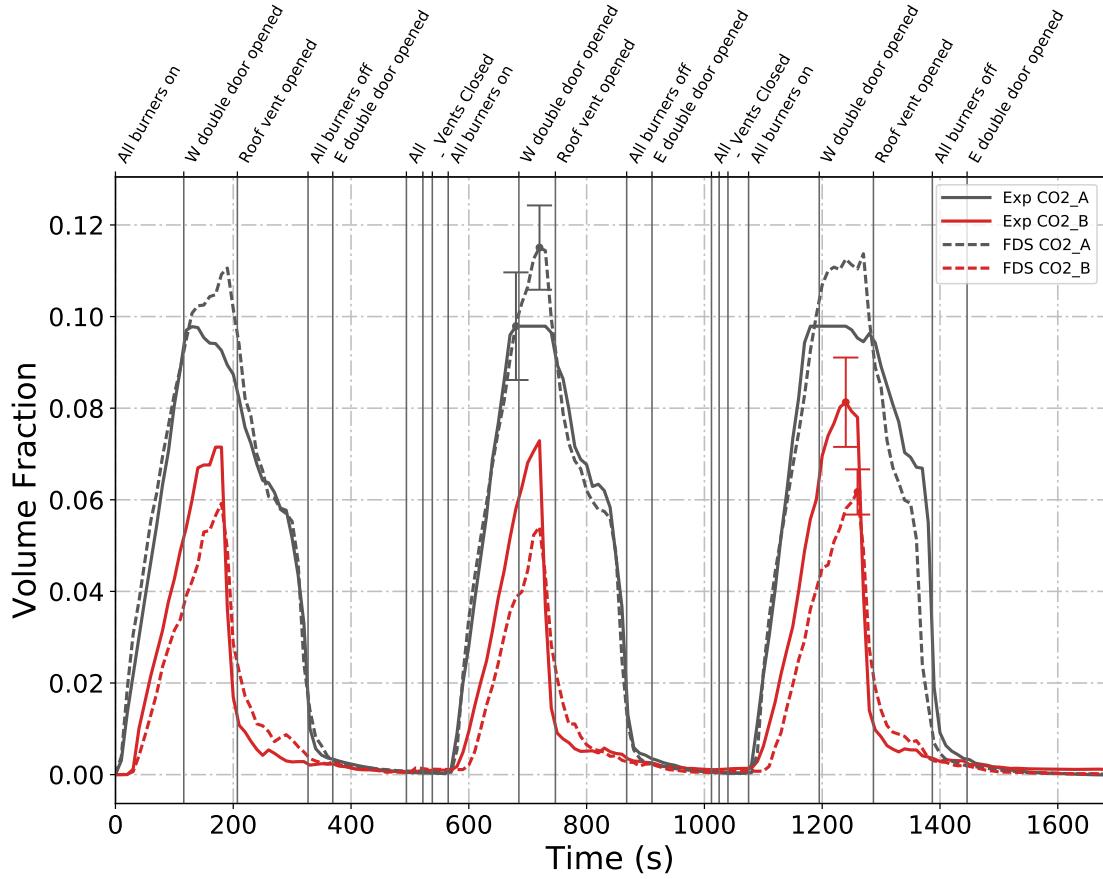


Figure B.38: Plots of measured and predicted CO_2 concentration in the fire room (black plots) and north room (red plots) of the East Structure during Test 6.

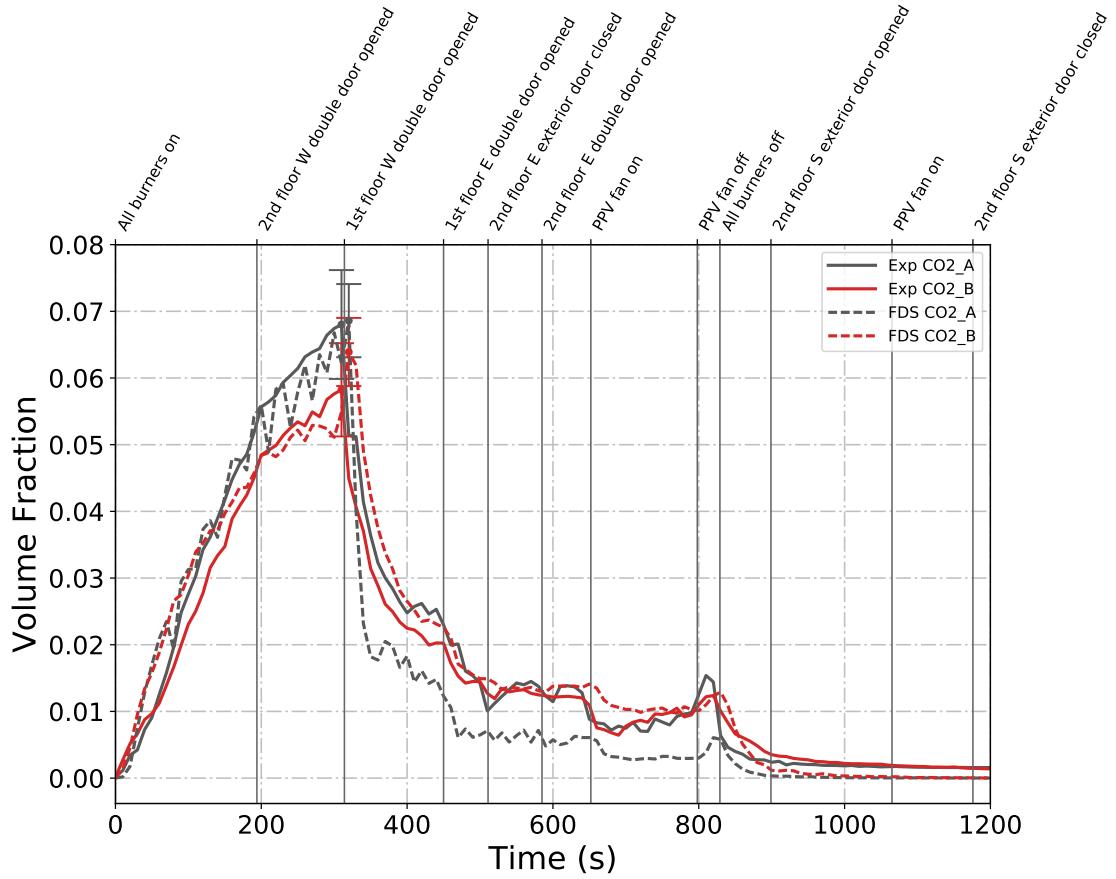


Figure B.39: Plots of measured and predicted CO_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 22.

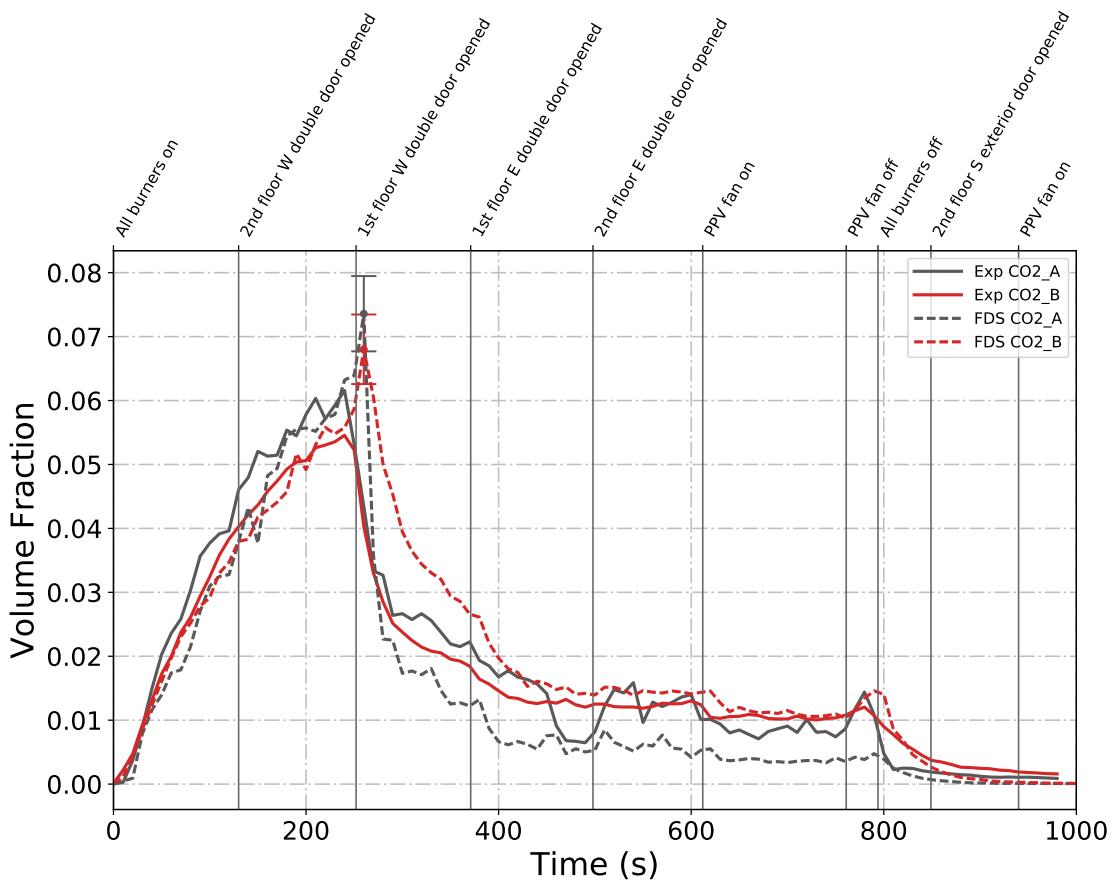


Figure B.40: Plots of measured and predicted CO_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 23.

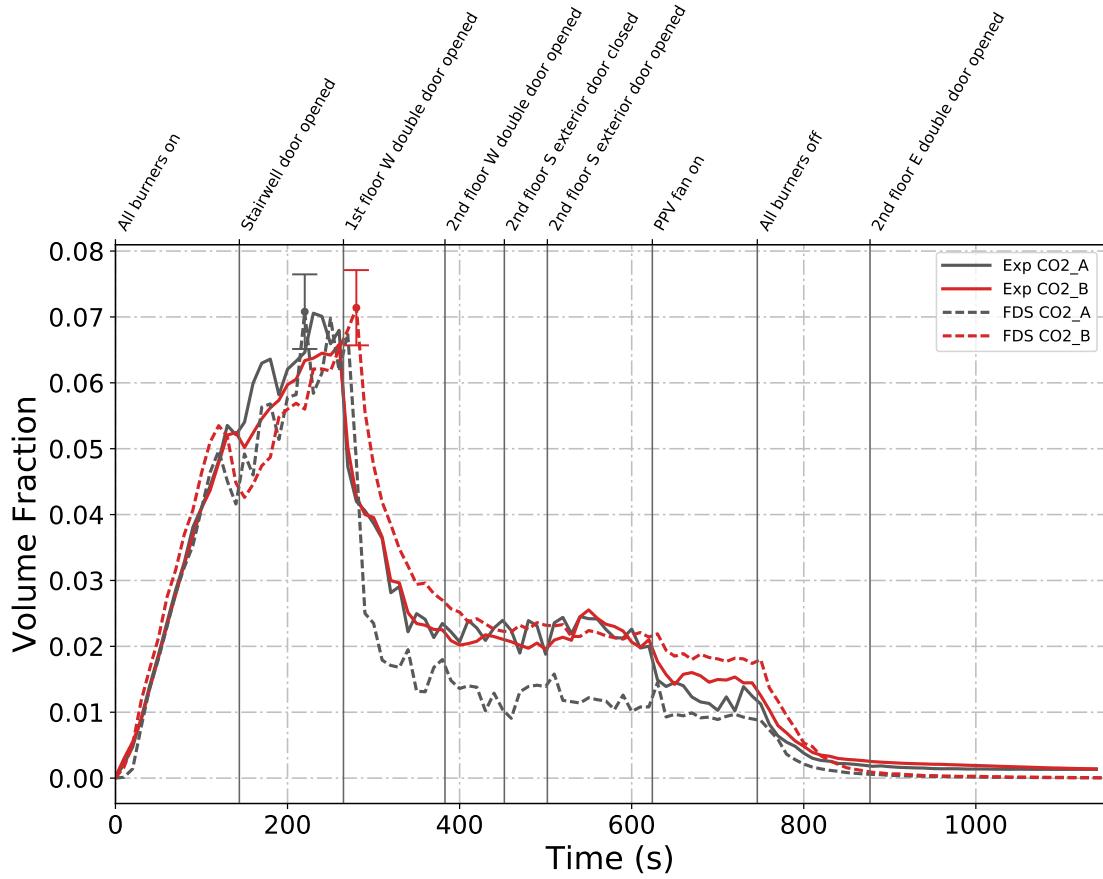


Figure B.41: Plots of measured and predicted CO_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 24.

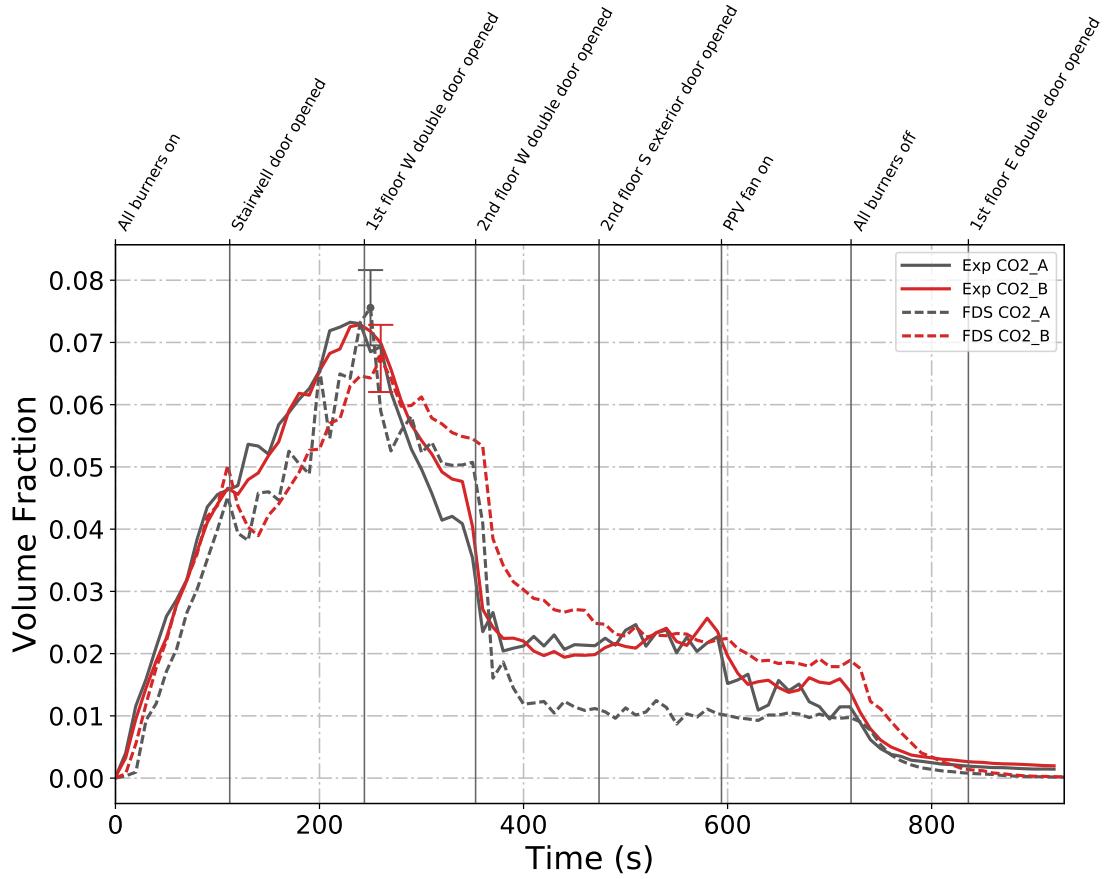


Figure B.42: Plots of measured and predicted CO_2 concentration on the first floor (black plots) and second floor (red plots) of the West Structure during Test 25.

B.3 Gas Velocity

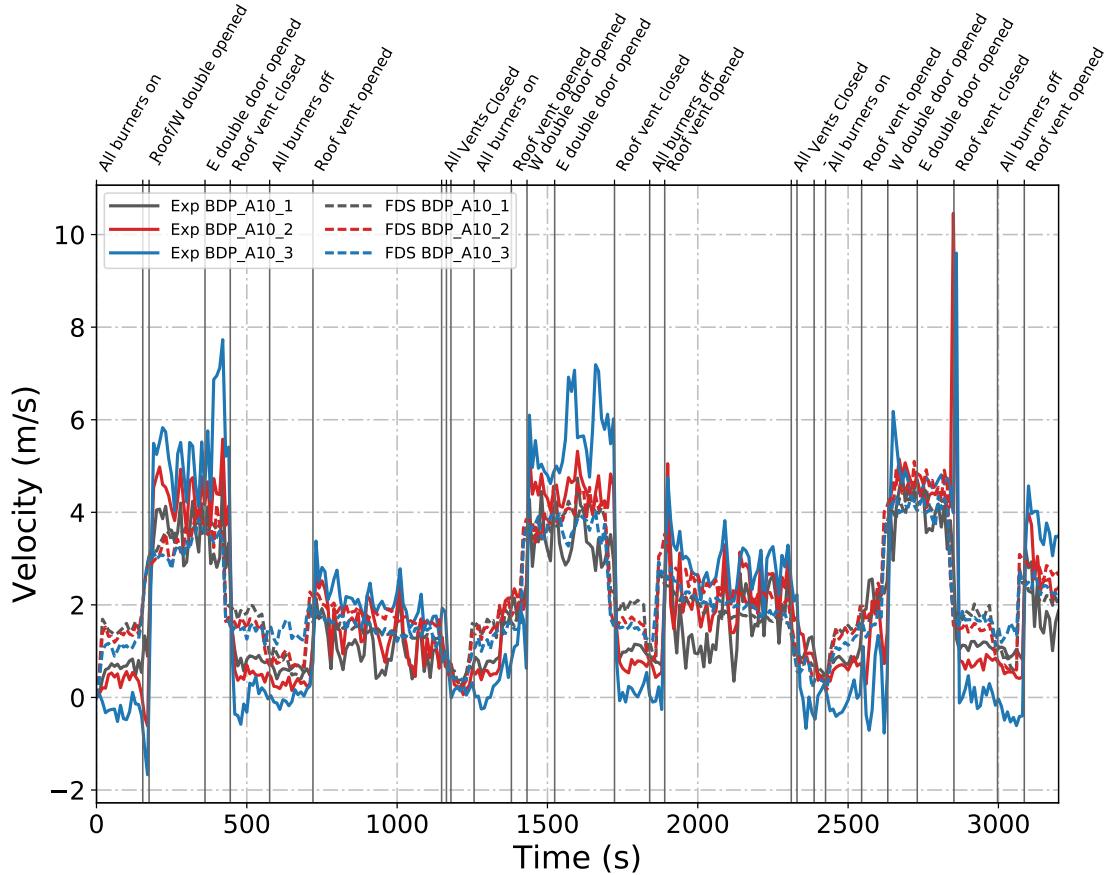


Figure B.43: Plots of measured and predicted gas velocity through the roof vent during Test 5.

B.4 Total Heat Flux

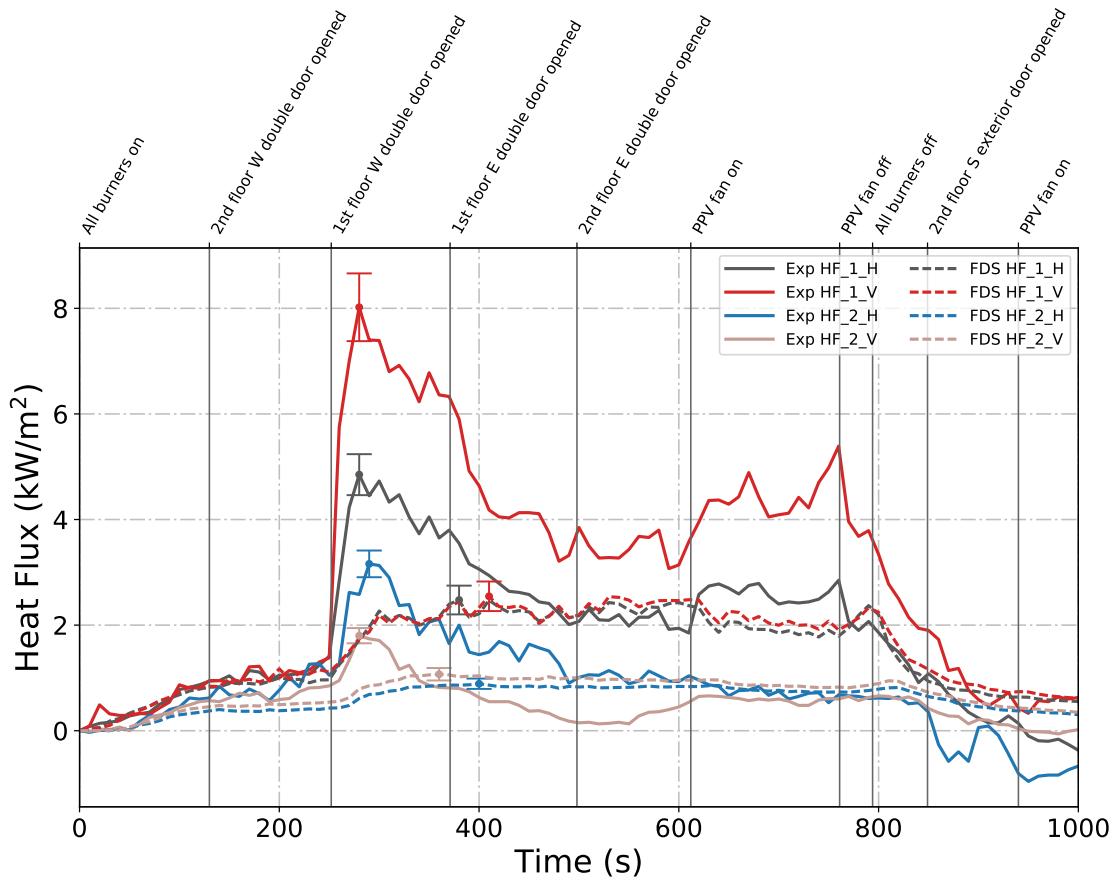


Figure B.44: Plots of measured and predicted heat flux measured by total heat flux gauges at the top of the stairs facing the stair doorway ('H') and facing the ceiling ('V').

Bibliography

- [1] K. McGrattan, S. Hostikka, R. McDermott, J. Floyd, C. Weinschenk, and K. Overholt. *Fire Dynamics Simulator, User's Guide*. National Institute of Standards and Technology, Gaithersburg, Maryland, USA, and VTT Technical Research Centre of Finland, Espoo, Finland, sixth edition, September 2013.
- [2] K. McGrattan, S. Hostikka, R. McDermott, J. Floyd, C. Weinschenk, and K. Overholt. *Fire Dynamics Simulator, Technical Reference Guide*. National Institute of Standards and Technology, Gaithersburg, Maryland, USA, and VTT Technical Research Centre of Finland, Espoo, Finland, sixth edition, September 2013. Vol. 1: Mathematical Model; Vol. 2: Verification Guide; Vol. 3: Validation Guide; Vol. 4: Configuration Management Plan.
- [3] K. McGrattan, S. Hostikka, R. McDermott, J. Floyd, C. Weinschenk, and K. Overholt. *Fire Dynamics Simulator, Technical Reference Guide, Volume 2: Verification*. National Institute of Standards and Technology, Gaithersburg, Maryland, USA, and VTT Technical Research Centre of Finland, Espoo, Finland, sixth edition, September 2013.
- [4] K. McGrattan, S. Hostikka, R. McDermott, J. Floyd, C. Weinschenk, and K. Overholt. *Fire Dynamics Simulator, Technical Reference Guide, Volume 3: Validation*. National Institute of Standards and Technology, Gaithersburg, Maryland, USA, and VTT Technical Research Centre of Finland, Espoo, Finland, sixth edition, September 2013.
- [5] Infiltec, Inc., Waynesboro, VA. *Infiltec E3 Blower Door Specifications*, January 2017.
- [6] B.N. Taylor and C.E. Kuyatt. Guidelines for Evaluating and Expressing the Uncertainty of NIST Measurement Results. NIST Technical Note 1297, National Institute of Standards and Technology, Gaithersburg, Maryland, 1994.
- [7] Stanley Hand Tools, New Britain, Connecticut. *User Manual TLM 100*, 2013.

- [8] T. Butcher, S. Cook, L. Crown, and R. Harshman. NIST Handbook 44: Specifications, Tolerances, and Other Technical Requirements for Weighing and Measuring Devices. *National Institute of Standards, Gaithersburg, MD*, 2012.
- [9] Omega Engineering Inc., Stamford, Connecticut. *The Temperature Handbook*, 2004.
- [10] L.G. Blevins. Behavior of bare and aspirated thermocouples in compartment fires. In *National Heat Transfer Conference, 33rd Proceedings*, pages 15–17, 1999.
- [11] W.M. Pitts, E. Braun, R. Peacock, H. Mitler, E. Johnson, P. Reneke, and L.G. Blevins. Temperature uncertainties for bare-bead and aspirated thermocouple measurements in fire environments. *ASTM Special Technical Publication*, 1427:3–15, 2003.
- [12] Medtherm Corporation, Huntsville, Alabama. *64 Series Heat Flux Transducers*, 2003.
- [13] W.M. Pitts, A.V. Murthy, J.L. de Ris, J. Filtz, K. Nygård, D. Smith, and I. Wetterlund. Round robin study of total heat flux gauge calibration at fire laboratories. *Fire Safety Journal*, 41(6):459–475, 2006.
- [14] M. Bundy, A. Hamins, E.L. Johnsson, S.C. Kim, G.H. Ko, and D.B. Lenhart. Measurements of Heat and Combustion Products in Reduced-Scale Ventilated-Limited Compartment Fires. NISTTN 1483, National Institute of Standards and Technology, Gaithersburg, MD, 2007.
- [15] A. Lock, M. Bundy, E.L. Johnsson, A. Hamins, G.H. Ko, C. Hwang, P. Fuss, and R. Harris. Experimental study of the effects of fuel type, fuel distribution, and vent size on full-scale underventilated compartment fires in an ISO 9705 room. NISTTN 1603, National Institute of Standards and Technology, Gaithersburg, MD, 2008.
- [16] R.A. Bryant. A comparison of gas velocity measurements in a full-scale enclosure fire. *Fire Safety Journal*, 44:793–800, 2009.
- [17] Romet Limited, East Mississauga, Ontario. *Rotary Gas Meter RM3000 Technical Specification*, 2014.
- [18] K. Hill, J. Dreisbach, F. Joglar, B. Najafi, K. McGrattan, R. Peacock, and A. Hamins. Verification and Validation of Selected Fire Models for Nuclear Power Plant Applications. NUREG-1824, United States Nuclear Regulatory Commission, Washington, DC, 2007.
- [19] B. McCaffery, J. Quintiere, and M. Harkleroad. Estimating Room Fire Temperatures and the Likelihood of Flashover Using Fire Test Data Correlations. *Fire Technology*, 17(2):98–119, 1981.

- [20] D. Gross. Data Sources for Parameters Used in Predictive Modeling of Fire Growth and Smoke Spread. NBSIR 85-3223, National Bureau of Standards (now NIST), Gaithersburg, Maryland, September 1988.
- [21] USG Corporation, Chicago, IL. *USG DUROCK Brand Cement Board Submittal Sheet CB399*, 2016.
- [22] K. McGrattan and B. Toman. Quantifying the predictive uncertainty of complex numerical models. *Metrologia*, 48:173–180, 2011.
- [23] M.L. Janssens and H.C. Tran. Data Reduction of Room Tests for Zone Model Validation. *Journal of Fire Science*, 10:528–555, 1992.