

**Lab 6: Batch Growth and Chemostat**

The model for the growth of an organism has been developed as below

$$r_g = \mu X = \mu_{max} \left(1 - \frac{P}{P^*}\right)^{0.52} \frac{XS}{K_S + S}$$

$$r_d = k_d X$$

$$r_m = mX$$

If the growth of the organism in a batch reactor can be represented using the following equations

$$V \frac{dX}{dt} = (r_g - r_d) V$$

$$V \frac{dS}{dt} = Y_{SX} (-r_g) V - (r_m) V$$

$$V \frac{dP}{dt} = Y_{PX} (r_g V)$$

with the parameters given below

$$Y_{XS} = 0.08 \text{ g/g}$$

$$Y_{PS} = 0.45 \text{ g/g}$$

$$\mu_{max} = 0.33 \text{ h}^{-1}$$

$$K_s = 1.7 \text{ g/l}$$

$$k_d = 0.01 \text{ h}^{-1}$$

$$P^* = 90 \text{ g/l}$$

$$m = 0.03 \text{ g substrate / (g cells.h)}$$

$$V = 10 \text{ l}$$

If  $X_0 = 1 \text{ g/l}$ ;  $S_0 = 250 \text{ g/l}$ , obtain

- A plot of substrate, cell concentration, and product concentration with time till substrate concentration reduces to 10 g/l when grown in batch reactor mode.
- Obtain plots of  $\mu$ ,  $r_d$  and  $r_m$  for the course of the batch fermentation.
- After the substrate concentration of 10 g/l is reached, the reactor is run as a chemostat with the following feed parameters ( $X_0 = 0 \text{ g/l}$ ;  $S_0 = 100 \text{ g/l}$ ;  $D = 0.5 \text{ h}^{-1}$ ). Obtain a plot for cell, product and substrate concentration in the exit stream of the chemostat as a function of time to their steady state concentrations.