## Supplementary Document

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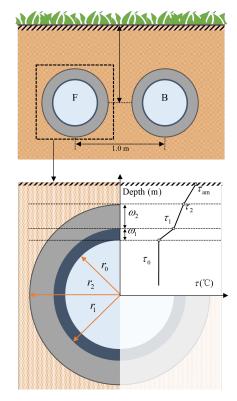


Fig. 1. Structure of underground cooling pipelines.

## I. PIPELINE NETWORK THERMAL LOSS

The structure of the underground cooling pipeline is illustrated in Fig.1. The energy equation for the chilled water flowing in a cooling pipeline can be formulated [1] as:

$$\rho A C_p \frac{\partial \boldsymbol{\tau}}{\partial t} + \rho A C_p \boldsymbol{u} \cdot \nabla \boldsymbol{\tau} = \nabla \cdot A k \nabla \boldsymbol{\tau}$$
$$+ f^{D} \frac{\rho A}{2d_h} |\boldsymbol{u}|^3 + Q^{\text{wall}} + Q^p, \qquad (1)$$

where  $\rho$ , A, and  $C_p$  are the density, pipe cross section area, and heat capacity of chilled water, respectively;  $\tau$  and u denote the water temperature and velocity field; k is the thermal conductivity;  $Q^{\rm p}$  is the heat brought by pressure drop. Since it's attributed to pumps' power,  $Q^{\rm p}=0$ ;  $Q^{\rm wall}$  represents radial heat transfer from the surroundings into the pipe, which is given by:

$$Q^{\text{wall}} = \frac{(h \cdot A_Q)^{\text{eff}}}{\Delta L} (\tau^{\text{ext}} - \tau),$$
(2)  
$$(hA_Q)^{\text{eff}} = \frac{1}{\frac{1}{r_0 h^{\text{int}}\Theta} + \frac{\ln(r_1/r_0)}{k_1 \Theta} + \frac{\ln(r_2/r_1)}{k_2 \Theta} + \frac{1}{r_2 h^{\text{ext}}\Theta}},$$
(3)

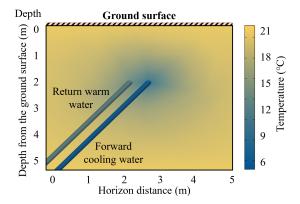


Fig. 2. Underground temperature field.

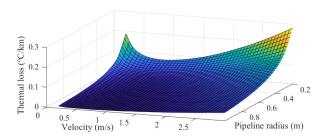


Fig. 3. Underground temperature field.

where  $A_Q$  denotes the area available for heat flux into the wall;  $\Delta L$  is a short length section of pipe;  $\tau^{\rm ext}$  represents the external temperature;  $h^{\rm int}$  and  $h^{\rm ext}$  are internal film resistance and external film resistance, respectively;  $\Theta = 2\pi \cdot \Delta L$ .To get the more detailed derivation, please check the Reference Manual in [2].

Then with the recorded soil temperature, chilled water temperature and mass flow rate  $\dot{m}$ , the temperature field and thermal loss can be calculated by COMSOL 6.1 [2]. The underground temperature field is illustrated in Fig. 2. Furthermore, the simulation result, thermal loss of different pipelines with different mass flow rates is demonstrated in Fig. 3.

## REFERENCES

- [1] M. V. Lurie, "Modeling of oil product and gas pipeline transportation," in *Modeling of oil product and gas pipeline transportation*, pp. 1–214, WILEY, 2009.
- [2] "COMSOL: Multiphysics Software for Optimizing Designs." https://www.comsol.com/. [Accessed 20-02-2025].

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