



Chapter 2

Basic Aerothermodynamics

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- > First law of thermodynamics
- > Second law of thermodynamics
- > Aerodynamics fundamental equations
 - > Continuity equation
 - > Energy equation
 - > Bernoulli's equation
 - Sound speed and Mach number
 - > Stagnation parameters of flow and aerodynamic functions
 - ➤ Momentum equation
 - > Shockwaves and expansion waves

1. Basic Aerodynamics

The conservation equations for the continuity, momentum and energy of the flow can be expressed in the following form:

$$\frac{\partial U}{\partial t} + \frac{\partial F(U)}{\partial x} + \frac{\partial G(U)}{\partial y} = S(U)$$

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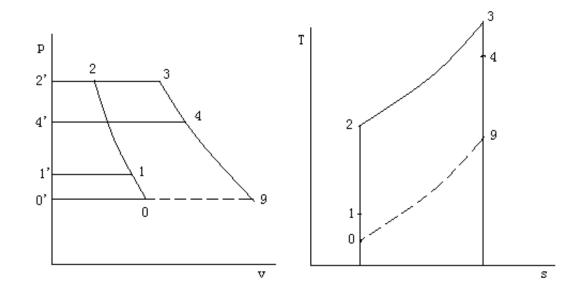
$$U = \begin{bmatrix} \rho \\ \rho u \\ \rho v \\ \rho E \\ \rho Y_1 \end{bmatrix}, F(U) = \begin{bmatrix} \rho u \\ \rho u v \\ \rho u v \\ u(\rho E + p) \\ \rho u Y_1 \end{bmatrix}, G(U) = \begin{bmatrix} \rho v \\ \rho u v \\ \rho v^2 + p \\ v(\rho E + p) \\ \rho v Y_1 \end{bmatrix}, S(U) = \begin{bmatrix} 0 \\ 0 \\ 0 \\ R_1 \end{bmatrix}$$
Scalar Equation \longrightarrow

1. Basic Aerodynamics

Solution Methods

- Semi-Implicit Method for Pressure-Linked Equations (SIMPLE)
- ➤ Semi-Implicit Method for Pressure-Linked Equations-Consistent (SIMPLEC)
- Pressure Implicit with Splitting of Operator (PISO)
- Approximate Riemann Solvers; e.g. Harten Lax and van Leer- Contact (HLLC), HLL, etc.
- Advection Upwind Splitting Method (AUSM)
- ➤ Advection Upwind Splitting Method- Plus (AUSM-plus)

Gas Turbine Cycle



First law of thermodynamics

- > Equation of state of ideal gas
 - ➤ Ideal gas
 - Gas molecule has only a mass but not volume
 - There is no attractive force between the molecules
 - >Ideal gas does NOT exist
 - ► Idealization for real gas

First law of thermodynamics

> Equation of state of ideal gas

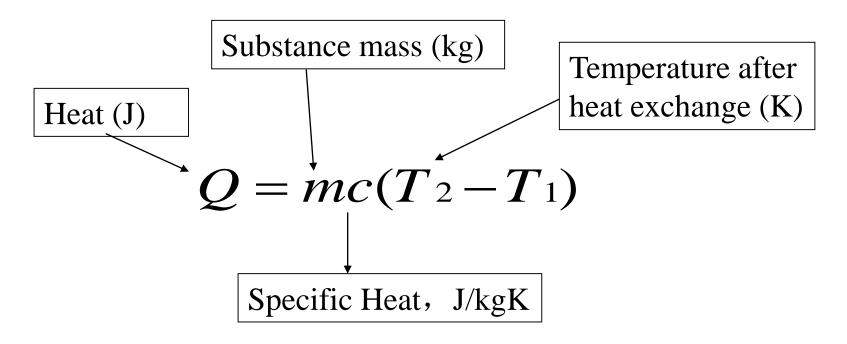
$$pv = RT$$
, or $p = \rho RT$

- $\triangleright p$ ——Pressure, N/m^2
- $\triangleright v$ ——Specific volume, m^3/kg
- $\succ T$ —Temperature, K
- \triangleright R Gas constant, J/kgK (287.1 for air and 288 for gas)

First law of thermodynamics

Heat

➤ Heat is a form of energy exchange



First law of thermodynamics

- > Specific heat
 - ➤ Heat needed to increase *T* of 1K for 1kg of substance
 - > Dependent on substance, temperature and process
- > Specific heat at constant volume

$$Q_{v} = mc_{v}(T_{2} - T_{1})$$

First law of thermodynamics

> Specific heat at constant pressure

$$Q_p = mc_p(T_2 - T_1)$$

- ➤ In reality in general, and in particular for certain substances, Cv and Cp are functions of temperature.
- These temperature defined properties are defined in terms of polynomial functions; e.g. **Janaf Table**.

$$\frac{C_p(T)}{R} = a[1] + a[2]T + a[3]T^2 + a[4]T^3 + a[5]T^4$$

$$\frac{H(T)}{R} = a[1]T + \frac{a[2]T^2}{2} + \frac{a[3]T^3}{3} + \frac{a[4]T^4}{4} + \frac{a[5]T^5}{5} + a[6]$$

$$\frac{S(T)}{R} = a[1]\ln T + a[2]T + \frac{a[3]T^2}{2} + \frac{a[4]T^3}{3} + \frac{a[5]T^4}{4} + a[7]$$

First law of thermodynamics

> Ratio of specific heats

$$\gamma = c_p / c_v$$

- > For air 1.4;
- \triangleright For a mixture of gases ~ 1.33 ;
- \triangleright The value of γ can vary based on composition.
- ➤ In addition, the ratio is also temperature dependent when the specific heats are calculated as temperature-dependent functions.
- ightharpoonup Hypersonic limit: $\gamma \rightarrow 1$.

- > Specific internal energy
 - Summation of molecule average kinetic and potential energy
 - ➤ Potential energy for ideal gas = 0 (no attractive forces between the molecules).
 - > Specific internal energy of ideal gas is function of temperature

$$u = u(T)$$
 J/kg

➤ Since 'T' represents molecular average kinetic energy of the gas.

First law of thermodynamics

> Heating gas in container of constant volume

$$q_{v} = \int_{T_{1}}^{T_{2}} c_{v}(T) dT = c_{v}(T_{2} - T_{1})$$

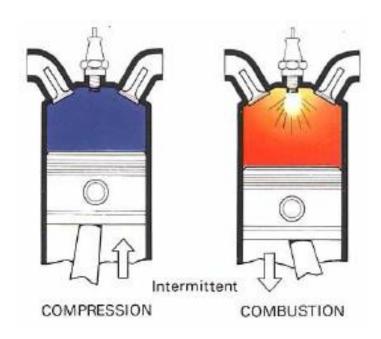
- $\triangleright Cv$ average specific heat (volume)
- ➤Internal energy increase

$$\Delta u = q_v = c_v (T_2 - T_1)$$

➤ No sense for absolute value of internal energy

First law of thermodynamics

- > Work
 - Mechanical work
 - In thermal process, gas expansion does work on objects
 - Or work can compress gas



First law of thermodynamics

 \triangleright Volume change for a unit mass gas dv, then work:

$$\rightarrow$$
 $dW = pdv$

➤ By integration

P constant:
$$W = \int_{v_1}^{v_2} p dv$$

$$W = p(v_2 - v_1)$$

 \triangleright If V=constant, W=0.

Enthalpy

- $\triangleright h = u + pv = u + p/\rho (J/kg)$
- \triangleright u is internal energy
- > pv considered as pressure potential energy
- $h(T) = u(T) + p/\rho = u(T) + RT$
- \triangleright Enthalpy, a state parameter, is a single value function of T.

$$q_p = \int_{T_1}^{T_2} c_p(T) dT = c_p(T_2 - T_1) = c_v(T_2 - T_1) + p(v_2 - v_1)$$

Since, Heat = U + W,
=
$$(c_v + R)(T_2 - T_1) = \Delta h$$

$$\therefore \Delta h = c_p(T_2 - T_1)$$

Enthalpy

 \rightarrow dq = du + pdv = Relation of heat, internal energy and work (transformations and conservation)

$$\triangleright u = h - pv$$

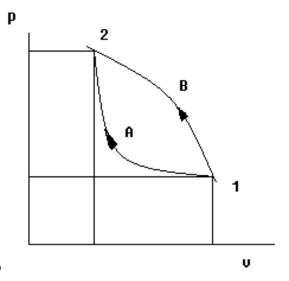
$$\triangleright du = dh - d(pv) = dh - pdv - vdp$$

$$> dq = dh - vdp$$
 (pressure work)

$$\triangleright$$
 or, $dh = dq + vdp$

 \triangleright For no heat addition, dh = vdp)

$$q = h_2 - h_1 - \int_{p_1}^{p_2} v dp = c_p(T_2 - T_1) - \int_{p_1}^{p_2} v dp$$



For constant pressure combustion, dq = dh

Adiabatic Process

$$c^{h} dT + b dh = 0$$

$$c_{h} dT = \frac{c_{h}}{R} (\nu dp + p d\nu) \qquad bh = KL$$

$$\frac{c_v}{c_p - c_v} (vdp + pdv) + pdv = 0$$

$$\frac{dp}{p} + \gamma \frac{dv}{v} = 0$$

$$\frac{dp}{d\rho} = \gamma \frac{p}{\rho} \qquad \left(\frac{dp}{d\rho}\right)_{s} = a^{2}$$

 $\triangleright pv^{\gamma} = constant$

$$\frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^{\gamma} = \left(\frac{T_2}{T_1}\right)^{\frac{\gamma}{\gamma-1}}$$
 Adiabatic Process

$$W = -\Delta u = Cv(T_1 - T_2) = \frac{R}{\gamma - 1}(T_1 - T_2) = \frac{RT_1}{\gamma - 1} \left[1 - \left(\frac{p_2}{p_1} \right)^{\frac{\gamma - 1}{\gamma}} \right]$$

 \triangleright I.E. =>Work

- > Reversible process
 - \triangleright Path 1=>2 is the same as 2=>1
 - ➤ Uniform, no friction—gas, machine, gas/machine
- > Irreversible process
 - > Friction exists
- Polytropic process
 - > pvⁿ=constant

Polytropic Process

$$\frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^n = \left(\frac{T_2}{T_1}\right)^{\frac{n}{n-1}}$$

Irreversible & Polytropic Process

$$\frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^n = \left(\frac{T_2}{T_1}\right)^{\frac{n}{n-1}}$$

n polytropic index

Const P	n=0	p= const
Const V	$n=\infty$	v= const
Const T	n= 1	T= const
Adiabatic	$n=\gamma$	$pv^{\gamma} = \text{const}$
Irreversible	Compression n> g Expansion 1 <n<g< td=""><td></td></n<g<>	

Irreversible & Polytropic Process

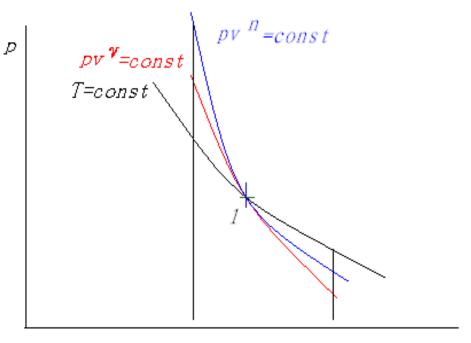
- $\triangleright pv^n = \text{const}, \text{ intersect at '1'}$
- Compression

$$\triangleright W = W_n + q_{in}$$

- Add more work for compression
- > Expansion

$$\gg W = W_n - q_{in}$$

➤ Get less work done at expansion



V

Irreversible & Polytropic Process

$$W_{n} = \frac{R}{n-1}(T_{1} - T_{2}) = \frac{RT_{1}}{n-1}(1 - \frac{1}{\left(\frac{v_{2}}{v_{1}}\right)^{n-1}}) = \frac{RT_{1}}{n-1}(1 - \left(\frac{p_{2}}{p_{1}}\right)^{\frac{N-1}{n}})$$

Irreversible & Polytropic Process

> Entropy

$$ds = rac{dq}{T}$$
 J/kg.K
$$\Delta s = Cv \ln rac{T_2}{T_1} + R \ln rac{v_2}{v_1}$$

$$= Cp \ln rac{T_2}{T_1} - R \ln rac{p_2}{p_1}$$

$$= Cp \ln rac{v_2}{v_1} + Cv \ln rac{p_2}{p_1}$$

$$q = \int_{S_1}^{S_2} T ds$$

Irreversible & Polytropic Process

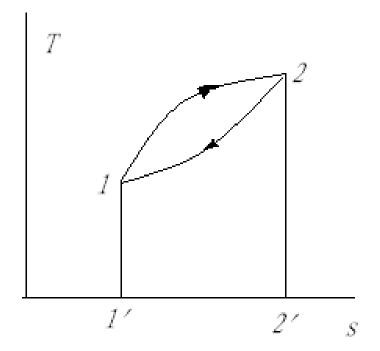
- Entropy is an abstract parameter for a useful thermodynamic concept ('entity')
- > State parameter, that is a function of any two out of p, v and T
- Can be used to get heat

$$\triangleright dq = Tds$$

J/kg

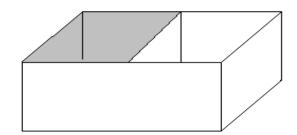
- \triangleright dq and ds retain same sign
- When irreversible, q contains q_{in} (friction heat)

$$q = \int_{S_1}^{S_2} T ds$$



Second law of thermodynamics

- > Any natural thermal process is irreversible.
- > Example:



$$\Delta s = Cp \ln \frac{v_2}{v_1} + Cv \ln \frac{p_2}{p_1} = (Cp - Cv) \ln 2$$

$$\Delta s > 0$$

Second law of thermodynamics

- > Or,
- ➤ Without work, heat can NOT automatically go from LT to HT or it goes always naturally from HT to LT.

$$\Delta S_1 = \int \frac{dq}{T_1} \qquad \frac{dq}{T_2}$$

$$\Delta s = \int \left(\frac{1}{T_2} - \frac{1}{T_1}\right) dq \qquad T_1 > T_2$$

Second law of thermodynamics

- ➤ Unique heat source engine can not be made.
- > Natural thermal process follows path of entropy increase.
- ➤ Naturally go **from ordered to unordered**.
- > Notes
 - ➤ Naturally
 - ➤ Isolated system
 - > Can be used in other domain, such as in social sciences

The Stagnation Process

- From above equations, flow kinetic energy (speed), enthalpy and pressure potential energy can be converted from one to others.
- \triangleright If flow stagnates (U= 0) as isentropic process, the kinetic energy is converted totally to enthalpy. It is called stagnation enthalpy, or total enthalpy:

$$h^* = c_p T + \frac{U^2}{2} \qquad U \uparrow \Rightarrow h \downarrow \quad \text{and} \quad p \downarrow$$

- > *U*: ordered movement
- > T: disordered movement

The Stagnation Process

> Corresponding stagnation temperature or total temperature:

$$T^* = T + \frac{U^2}{2c_p}$$

> Since,

$$c_p = \frac{\gamma}{\gamma - 1} R \qquad c = \sqrt{\gamma R T}$$

$$\frac{T^*}{T} = 1 + \frac{\gamma - 1}{2}M^2$$

The Stagnation Process

➤ With the stagnation process under isentropic assumption:

$$\frac{P^*}{p} = \left(\frac{v}{v^*}\right)^{\gamma} = \left(\frac{T^*}{T}\right)^{\frac{\gamma}{\gamma-1}}$$

$$\frac{p^*}{p} = \left(1 + \frac{\gamma - 1}{2}M^2\right)^{\frac{\gamma}{\gamma-1}}$$

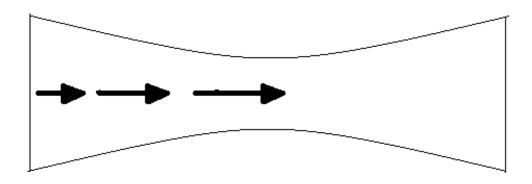
$$\frac{\rho^*}{\rho} = \left(1 + \frac{\gamma - 1}{2}M^2\right)^{\frac{1}{\gamma-1}}$$

The Stagnation Process

- According to the 3 equations above, for a given gas flow, the ratios of the total parameters and steady parameters are function of Mach number.
- When air flows isentropically in a tube without energy added, the total parameters (Enthalpy, temperature, pressure and density) remain unchanged.

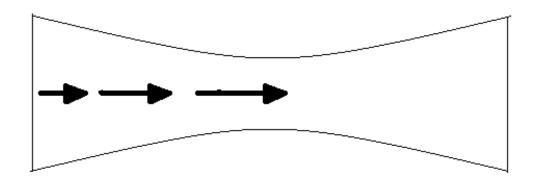
The Stagnation Process

 \triangleright Critical sound speed c_{cr} (in tunnel)



- U increases along the tunnel (ex. Laval nozzle)
- ➤ When *U* increases, *T* decreases. Sound speed *c* is function of *T*, it goes down.

The Stagnation Process



- When U = c, ie M= 1, this c has special meaning, called **critical sound speed** c_{cr} . This section is called critical section and it is the smallest section in the tunnel, also called **throat**.
- $\succ c_{cr}$ does not change, even when c does.

The Stagnation Process

➤ Definition of **speed coefficient** in a section

$$\lambda = \frac{U}{c_{cr}}$$

Writing the stagnation state relation $\frac{c_{cr}}{T} = 1 + \frac{\gamma - 1}{2}M^2$ in

terms of the critical condition, we obtain

$$T_{cr} = \frac{2}{\gamma + 1} T^*$$

The Stagnation Process

> Thus

$$T_{cr} = \frac{2}{\gamma + 1} T^*$$

$$c_{cr}^2 = \frac{2}{\gamma + 1} \gamma R T^*$$

$$\lambda^{2} = \frac{\frac{\gamma + 1}{2}M^{2}}{1 + \frac{\gamma - 1}{2}M^{2}}$$

$$c_{cr} = \sqrt{\frac{2}{\gamma + 1}} \gamma R T^*$$

$$M^2 = \frac{\frac{2}{\gamma + 1} \lambda^2}{1 - \frac{\gamma - 1}{\gamma + 1} \lambda^2}$$

The Stagnation Process

Therefore, the stagnation state equations are written in terms of the speed coefficient as,

$$\tau(\lambda) = \frac{T}{T^*} = \left(1 - \frac{\gamma - 1}{\gamma + 1}\lambda^2\right)$$

$$\pi(\lambda) = \frac{p}{p^*} = \left(1 - \frac{\gamma - 1}{\gamma + 1}\lambda^2\right)^{\frac{\gamma}{\gamma - 1}}$$

$$\varepsilon(\lambda) = \frac{\rho}{\rho^*} = \left(1 - \frac{\gamma - 1}{\gamma + 1}\lambda^2\right)^{\frac{1}{\gamma - 1}}$$

The Stagnation Process

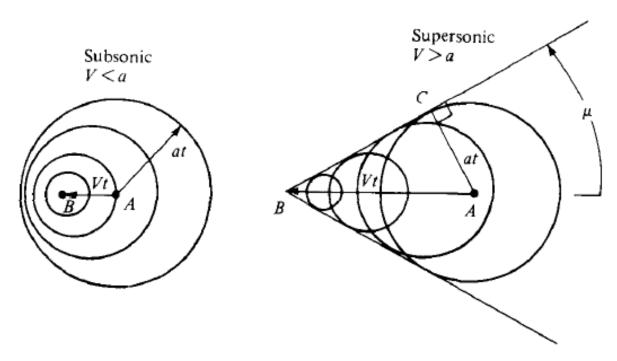
> Flow density function

$$q_m = \rho v A$$

$$q(\lambda) = \frac{\rho v}{(\rho v)_{cr}} = \frac{A_{cr}}{A} = \left(\frac{\gamma + 1}{2}\right)^{\frac{1}{\gamma - 1}} \lambda \left(1 - \frac{\gamma - 1}{\gamma + 1}\lambda^2\right)^{\frac{1}{\gamma - 1}}$$

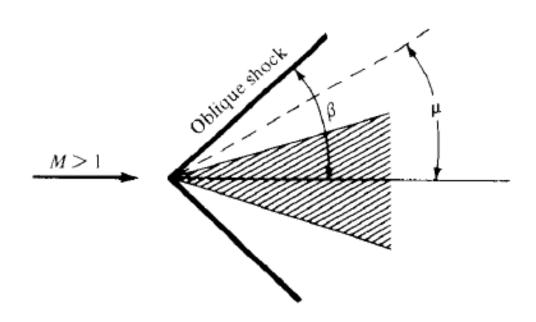
- $ightharpoonup q(\lambda)$ presents relative flow density in section A to the critical section even though the critical section does not exist.
- > Ratio of the cross-sections.

Shock Waves



▶ If the disturbances are stronger than a simple sound wave, then the wave front becomes stronger than a Mach wave, creating an oblique shock wave at an angle β to the freestream, where β > μ .

Shock Waves



The Mach wave is a limiting case for an oblique shock wave, i.e. it is an infinitely weak shock wave.

Shock Waves

$$M_{n,1} = M_1 \sin \beta$$

$$M_2 = \frac{M_{n,2}}{\sin\left(\beta - \theta\right)}$$

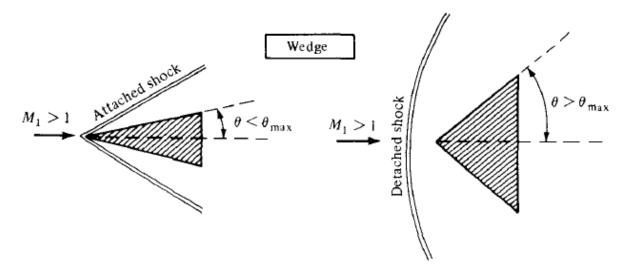
$$M_{n,2}^2 = \frac{1 + [(\gamma - 1)/2] M_{n,1}^2}{\gamma M_{n,1}^2 - (\gamma - 1)/2}$$

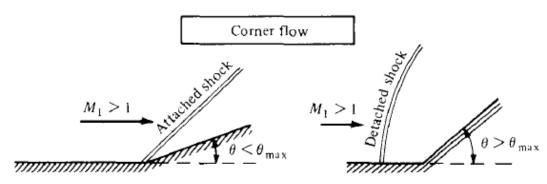
$$\frac{\rho_2}{\rho_1} = \frac{(\gamma + 1)M_{n,1}^2}{2 + (\gamma - 1)M_{n,1}^2}$$

$$\frac{p_2}{p_1} = 1 + \frac{2\gamma}{\gamma + 1} \left(M_{n,1}^2 - 1 \right)$$

$$\tan \theta = 2 \cot \beta \frac{M_1^2 \sin^2 \beta - 1}{M_1^2 (\gamma + \cos 2\beta) + 2}$$

Shock Waves

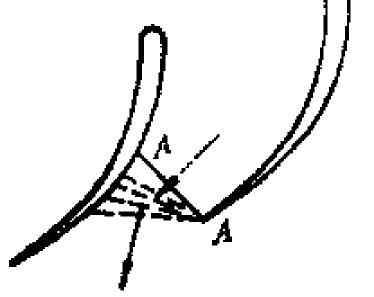




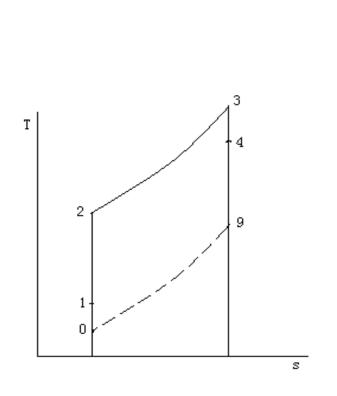
- Supersonic flow passing through the shock wave is not isentropic process. Partial mechanical energy Irreversibly changes to heat, and total pressure decreases.
- This is shock wave loss, and usually total pressure recovery (σ) is used to present the loss. It is function of the wave strength; the stronger the wave, the greater the loss.

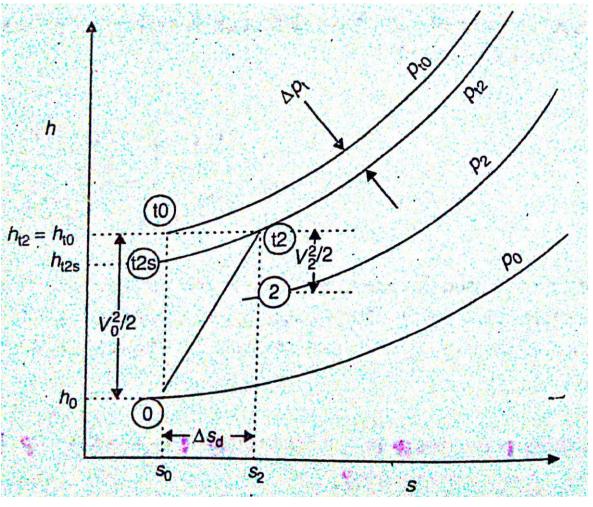
- When a supersonic air flows to a lower pressure zone, there are expansion waves due to air continuous expansion.
- ➤ In Fig, turbine cascade passage. In the throat A—A, critical section, flow becomes supersonic.
- In downstream, it is low pressure zone. The flow accelerates, it passes through a series of expansion waves, and speed increases, temperature and pressure decrease.

- The flow changes also the direction. The bigger the turned angle, the more expansion and flow parameters change more.
- The turned angle depends on exit pressure. The lower the pressure, the bigger the angle.
- ➤ If pressure increases, expansion waves may disappear and the flow may be subsonic.



Gas Turbine Cycle

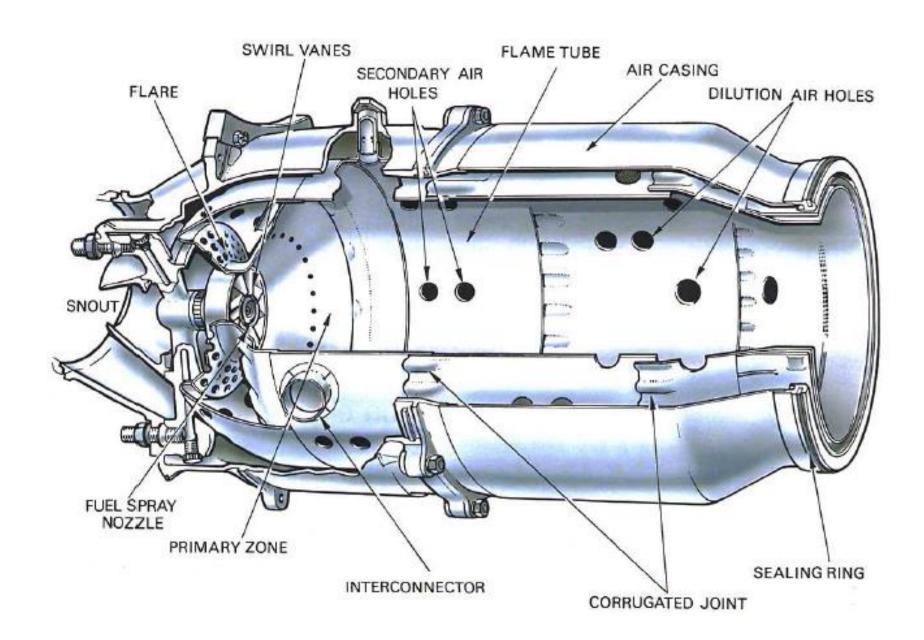




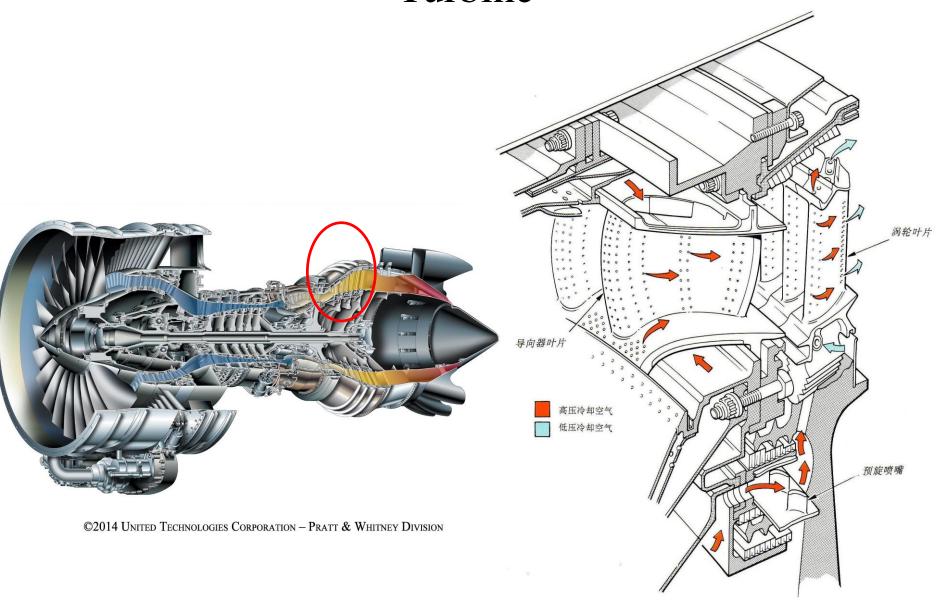
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- ➤ When supersonic flow passes through the shock wave, sharply speed decreases, pressure and temperature increase.
- After normal wave, the flow is certainly subsonic. But after oblique shock wave, it is still supersonic.
- ➤ Strength of the shock wave is described by pressure ratio of after and before. It is only function of M for normal shock wave, the greater M, the stronger the wave.
- For oblique shock wave, the greater M and q, the stronger the wave.

Combustion chamber

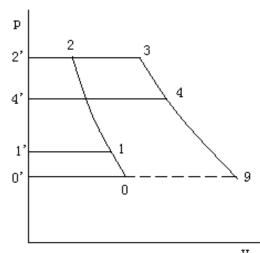


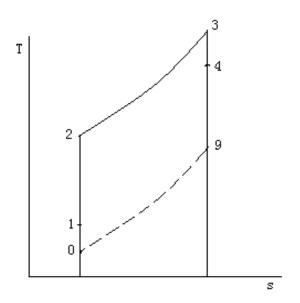
Turbine



Thermodynamic Cycle

➤ 1. Ideal cycle (Brayton cycle)

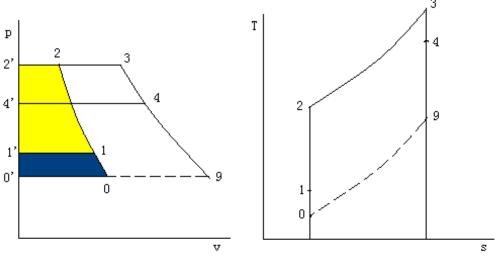




- ➤ 0-2 Isentropic compression
- ➤ 2-3 Isobar heating
- ➤ 3-9 Isentropic expansion
- ➤ 9-0 Isobar cooling

Thermodynamic Cycle

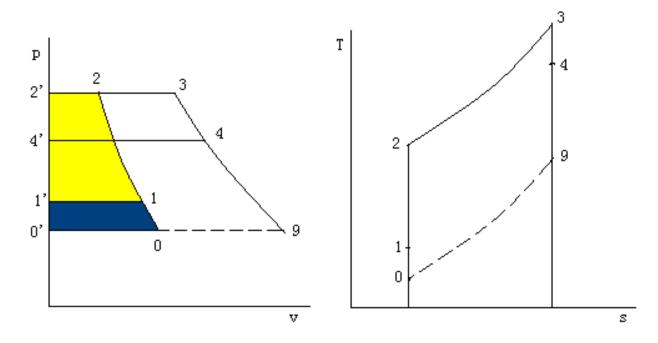
➤ 0-2 Isentropic compression



- ➤ Diffuser and compressor
- ➤ 0-1 speed pressure rise. 0 atmosphere condition. Add dynamic energy to substance and to increase pressure to 1. Area 011'0'0 presents dynamic energy difference.

Thermodynamic Cycle

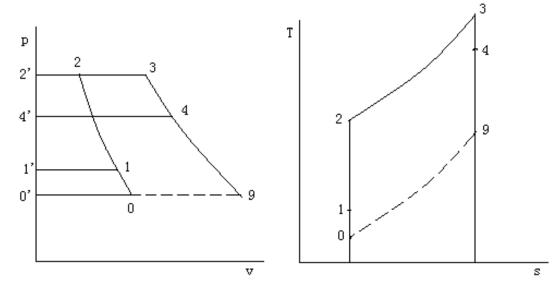
➤ 0-2 Isentropic compression



➤ 1-2: compressor. Pressure from 1 to 2, work added is the area 122'1'1.

Thermodynamic Cycle

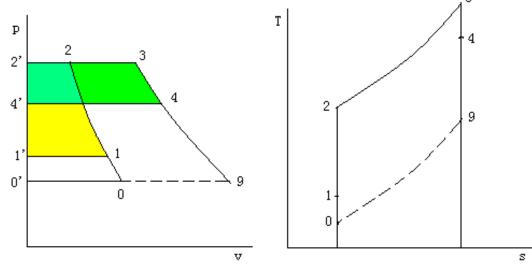
➤ 2-3 Isobar heating



- ➤ Combustion chamber
- ➤ Burn ideally kerosene at constant pressure in combustion chamber and substance properties unchanged.
- \triangleright Total temperature $T_2^* \Rightarrow T_3^*$ •

Thermodynamic Cycle

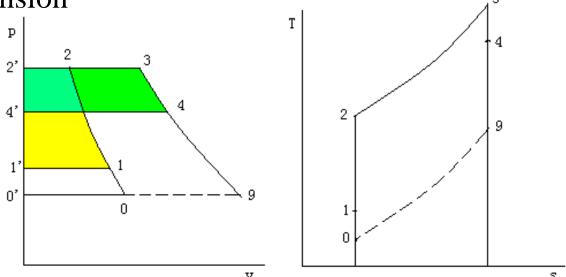
➤ 3-9 Isentropic expansion



- > Turbine and nozzle
- ⇒ 3-4 presents expansion in turbine, heat ⇒ mechanical energy giving to compressor. Area 344'2'3=Area 122'1'1, total pressure $p_3^* \Rightarrow p_4^*$.

Thermodynamic Cycle

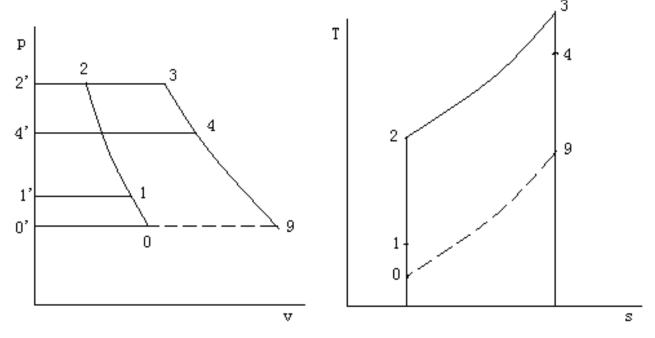
➤ 3-9 Isentropic expansion



- ➤ 4-9 complete expansion in exhaust system. Heat changes kinetic energy in substance, exits from the nozzle.
- As diffuser, kinetic energy change can be seen as output work.

Thermodynamic Cycle

> 9-0 Isobar heat release



➤ Dash line, accomplished in atmosphere. This process is unavoidable, The cycle is closed.

Thermodynamic Cycle

> Specific heat added in the cycle

$$q_1 = c_p (T_3^* - T_2^*)$$

> Specific heat lost to the surrounding

$$q_2 = c_p (T_9 - T_0)$$

> Specific work in the cycle

$$W = q_1 - q_2$$

Thermodynamic Cycle

> Thermal efficiency in the cycle

$$\eta_{t} = \frac{W}{q_{1}} = \frac{q_{1} - q_{2}}{q_{1}} = 1 - \frac{1}{\pi^{\frac{\gamma - 1}{\gamma}}}$$

➤ Where pressure ratio

$$\pi = \frac{p_2^*}{p_0}$$

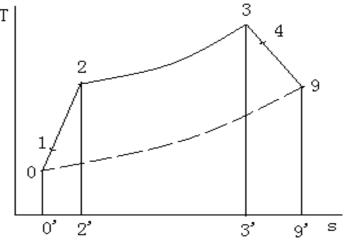
Thermodynamic Cycle

> Cycle work as mechanical energy

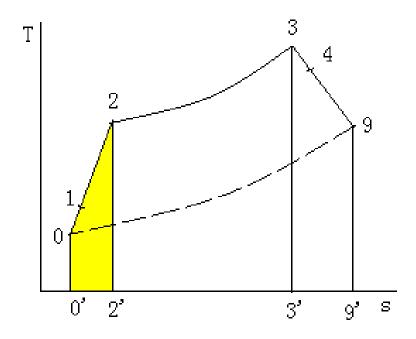
$$W = W_T + \frac{v_9^2}{2} - W_C - \frac{v_0^2}{2}$$

 \triangleright if $W_T = W_C$

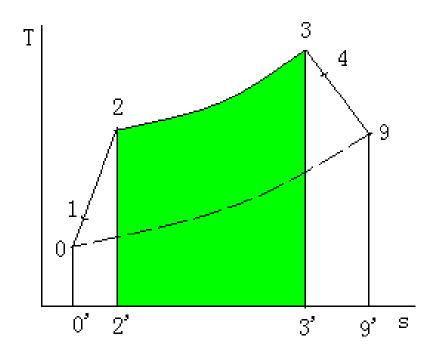
$$W = \frac{v_9^2 - v_0^2}{2}$$



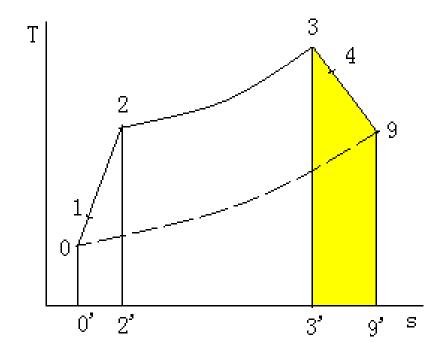
- ➤ 0-2 Compression (non isentropic)
- > 2-3 Heating (non isobar)
- ➤ 3-9 Expansion (non isentropic)
- > 9-0 Isobar heat release



- ➤ 0-2 Compression
 - ➤ Stagnation in diffuser and compression in compressor suffer from many types of losses.
 - ➤ Non isentropic



- > 2-3 Non isobar combustion
 - Existing flow losses and thermal resistance losses lowers the pressure in combustion chamber.
 - Composition of substance changes.



- ➤ 3-9 Expansion
 - There are always losses in turbine and nozzle.
 - ➤ Non isentropic

Actual Thermodynamic Cycle

➤ Heat added:

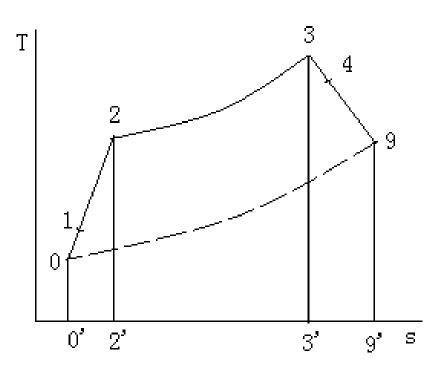
$$q_1 = c_p (T_3^* - T_2^*)$$

> Heat released

> Area 0'099'0'

$$q_2 = c_p (T_9 - T_0)$$

 \triangleright c_p ' gas specific heat



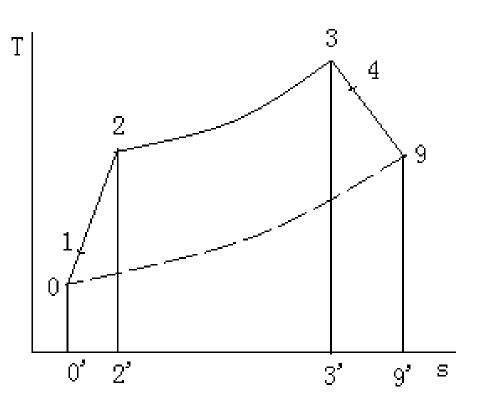
Actual Thermodynamic Cycle

> Efficiency

$$\eta_t = \frac{q_1 - q_2}{q_1}$$

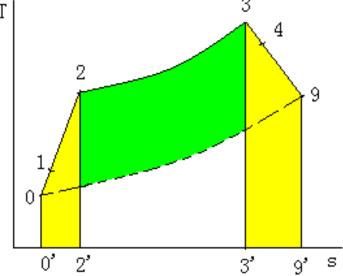
> Work

$$W = q_1 - q_2$$



- > If T_3 * lower, q_1 = q_2 , then η_t =0, no output work.
- Work can be presented by mechanical energy, same as ideal cycle:

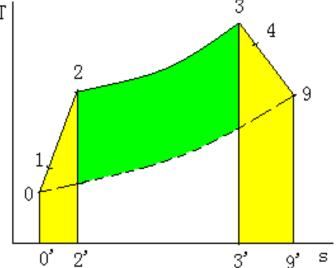
$$W = \frac{v_9^2 - v_0^2}{2}$$



Actual Thermodynamic Cycle

Under the same pressure ratio p and the same T_3 *, work is smaller in real cycle than ideal cycle.

➤ Note that area in diagram T-s is heat, not work.



- ➤ If not take into account the change in and increase in mass flow, differences between real cycle and ideal cycle are:
 - > Friction and flow losses
 - ➤ Total pressure loss
 - ➤ Heating resistance
- ➤ If nozzle gas kinetic energy is smaller, velocity of air jet is smaller.
- To improve the engine's efficiency, components with high efficiency and performance should be used.

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