

Property	Unit	Model equations	Input parameters	ARD (%) ^{cj}		Referen ces
				Reported	This study	
Cetane number (CN)	-					
Model 1		<p>Global FAMEs mixture correlation :^{a)}</p> $CN = 61.1 + 0.088 \cdot w_{14:0} + 0.133 \cdot w_{16:0} + 0.152 \cdot w_{18:0} - 0.101 \cdot w_{16:1} - 0.039 \cdot w_{18:1} - 0.243 \cdot w_{18:2} - 0.395 \cdot w_{18:3} \quad (1.1)$ $R^2 = 0.88$ <p>Performs better at: ^{b)}</p> <p>$w_{18:1} > 17.82$; $w_{16:0} \leq 25$ and $w_{18:0} \leq 16$</p>	w_i , weight prop. of the C14:0, C16:0, C16:1, C18:0, C18:1, C18:2, and C18:3 FAMEs.	3.18 (1.98-4.02); N=19	11.75, N=274/9.91, N=6	(Bamgbaye and Hansen, 2008; Tong et al., 2011)
Model 2		<p>CNs of individual FAMEs (cetane number of the i^{th} FAME in the mixture) :^{e)}</p> $\varphi_i = -52.974 + (13.767 - 1.202 \cdot ndb_i + 0.152 \cdot ndb_i^2) \cdot nc_i - 0.351 \cdot nc_i^2 \quad (1.2)$ $R^2 = 0.946$ <p>To obtain the global CN for FAMEs mixture, Linear mixing rule (Modified Grunberg–Nissan model) is applied as follows :</p> $CN = \sum_i^n w_i \cdot \varphi_i \quad (1.3)$	<p>ndb_i, numb. of double bonds of the i^{th} FAME;</p> <p>nc_i, numb. of carbon atoms of the i^{th} FAME;</p> <p>w_i, weight prop. of the i^{th} FAME.</p>	6.5 (1.5-25.1); N=11	11.78, N=274/5.34, N=6	(Lapuerta et al., 2009; Tong et al., 2011)
Model 3		<p>CNs of individual FAMEs (cetane number of the i^{th} FAME in the mixture) :</p> $\varphi_i = 58.1 + 2.8 \cdot \left(\frac{nc_i - 9}{2} \right) - 15.9 \cdot ndb_i \quad (1.4)$ <p>Linear mixing rule : cf. (1.3)</p> <p>Performs better at:</p> <p>$14 < w_{18:2} \leq 29$ and $w_{20:0} > 1$</p>	<p>ndb_i, numb. of double bonds of the i^{th} FAME;</p> <p>nc_i, numb. of carbon atoms of the i^{th} FAME;</p> <p>w_i, weight prop. of the i^{th} FAME.</p>	5.55; N=35	11, N=274/11.39, N=6	(Klopferstein, 1985; Su et al., 2011)
Model 4		<p>CNs of individual FAMEs (cetane number of the i^{th} FAME in the mixture) :</p>	<p>nc_i, numb. of carbon atoms of the i^{th} FAME;</p> <p>w_i, weight prop. of the i^{th} FAME.</p>	0.96 (0.02-2.98); N=19	11.26, N=274/5.14, N=6	(Tong et al., 2011)

		$\varphi_i(\text{Cn:0}) = -107.71 + 31.126 \cdot nc_i - 2.042 \cdot nc_i^2 + 0.0499 \cdot nc_i^3$ $R^2 = 0.9835$ $\varphi_i(\text{Cn:1,2,3}) = 109 - 9.292 \cdot nc_i + 0.354 \cdot nc_i^2$ $R^2 = 0.9058$ <p>Linear mixing rule :</p> $CN = 1.068 \cdot \sum_i^n (w_i \cdot \varphi_i) - 6.747 \quad (1.6)$ <p>Performs better at: $w_{18:1} > 18$ and $w_{18:0} \leq 6$</p>				
Model 5		<p>CNs of individual FAMES (cetane number of the i^{th} FAME in the mixture) :</p> $\varphi_i = -7.8 + 0.302 \cdot M_i - 20 \cdot ndb_i \quad (1.7)$ <p>Linear mixing rule :</p> $CN = \sum_i^n x_i \cdot \varphi_i, \text{ where: } x_i = \frac{\frac{w_i}{M_i}}{\sum_i^n \left(\frac{w_i}{M_i} \right)} \quad (1.8)$ <p>Performs better at: $x_{18:1} > 0.3$ and $x_{20:0} \leq 0.03$</p>	<p>ndb_i, numb. of double bonds of the i^{th} FAME; w_i, weight prop. of the i^{th} FAME; x_i, mol. mass fraction of the i^{th} FAME; M_i, mol. weight of the i^{th} FAME.</p>	3.24 (2.4-5.85); N=5	11.43, N=274/ 5.2, N=6	(Ramírez-Verduzco, 2012)
Cold Filter Plugging Point (CFPP)	°C					
Model 1		<p>Global FAMES mixture correlation :</p> $CFPP = 0.511 \cdot w_{16:0} - 7.823, \text{ with } 0 < w_{16:0} < 45 \quad (2.1)$	$w_{16:0}$, weight prop. of the C16:0.	0.88	3.9, N=20/ 2.99, N=6	(Sarin et al., 2009)
Model 2		<p>Global FAMES mixture correlation :</p> $CFPP = 18.019 \cdot \overline{nc} - 0.804 \cdot w_{n:1,2,3} \quad (2.2)$ <p>Where $\overline{nc} = \frac{\sum_i^n x_i \cdot nc_i}{\sum_i^n x_i} \quad (2.3)$, with x_i as defined in equation (1.8)</p>	<p>$w_{n:1,2,3}$, weight prop. of the unsaturated FAMES; \overline{nc}, weighted avg. no. of carbon atoms.</p>	0.83	4.6, N=20/ 5.26, N=6	(Su et al., 2011)
Model 3		<p>Global FAMES mixture correlation :</p> $CFPP = (3.1417 \cdot LCSF) - 16.477 \quad (2.4)$	w_i , weight prop. of the saturated	n.d.	8.41, N=20/	(Ramos et al.,

		Where the long-chain saturated factor (LCSF) of the mixture is defined as: $LCSF = 0.1 \cdot w_{16:0} + 0.5 \cdot w_{18:0} + 1 \cdot w_{20:0} + 1.5 \cdot w_{22:0} + 2 \cdot w_{24:0}$ (2.5)	FAMEs.		5.91, N=6	2009)
Cloud point (CP)	°C					
Model 1		Global FAMEs mixture correlation : $CP = 0.526 \cdot w_{16:0} - 4.992$, with $0 < w_{16:0} < 45$ (3.1) $R^2 = 0.963$	$w_{16:0}$, weight prop. of the C16:0.	n.d.		(Sarin et al., 2009)
Model 2		Global FAMEs mixture correlation : $CP = 18.134 \cdot \overline{nc} - 0.79 \cdot w_{n:1,2,3}$ (3.2), with \overline{nc} as defined in equation (2.3)	$w_{n:1,2,3}$, weight prop. of the unsaturated FAMEs; \overline{nc} , weighted avg. no. of carbon atoms.	n.d.		(Su et al., 2011)
Density (ρ), 20°C	g/cm ³					
Model 1		ρ s of individual FAMEs (density of the i^{th} FAME in the mixture) : $\rho_i = 851.4714 + \frac{250.718 \cdot ndb_i + 280.899}{1.214 + nc_i}$ (4.1) $R^2 = 0.969$ Linear mixing rule : $\rho = \sum_i^n w_i \cdot \rho_i$ (4.2)	ndb_i , numb. of double bonds of the i^{th} FAME; nc_i , numb. of carbon atoms of the i^{th} FAME; w_i , weight prop. of the i^{th} FAME.	0.66 (0.02-5.31); N=32	1.16, N=79/ 0.65, N=6	(García et al., 2013; Lapuerta et al., 2009)
Model 2		ρ s of individual FAMEs (density of the i^{th} FAME in the mixture) : $\rho_i = 0.8463 + \frac{4.9}{M_i} + 0.0118 \cdot ndb_i$ (4.3) Linear mixing rule : $\rho = \sum_i^n x_i \cdot \rho_i$ (4.4)	ndb_i , numb. of double bonds of the i^{th} FAME; x_i , mol. mass fraction of the i^{th} FAME; M_i , mol. weight of the i^{th} FAME;	0.47 (0.24-0.67); N=5	1.4, N=79/ 1, N=6	(Ramírez-Verduzco, 2012)
Flash point (FP)	°C					
Model 1		Global FAMEs mixture correlation : $FP = 23.362 \cdot \overline{nc} + 4.854 \cdot \overline{ndb}$ (5.1)	\overline{nc} , weighted avg. no. of carbon atoms; \overline{ndb} , weighted avg. no. of double bonds;	1.81	14.47, N=45/ 22.49, N=6	(Su et al., 2011)

		<p>Where $\overline{ndb} = \frac{\sum_i^n x_i \cdot ndb_i}{\sum_i^n x_i}$ (5.2), and \overline{nc} as defined in equation (2.3)</p> <p>Performs better at: $\overline{nc} > 17.6$ and $FP \leq 170$ °C</p>	x_i , mol. mass fraction of the i^{th} FAME;			
Model 2		<p>FPs of individual FAMES (flash point of the i^{th} FAME in the mixture) :</p> $\theta_i = (0.3544 \cdot T_{bi}^{1.14711} \cdot nc_i^{-0.07677}) - 273.15 \quad (5.2)$ <p>Linear mixing rule :</p> $FP = \sum_i^n w_i \cdot \theta_i \quad (5.3)$	nc_i , numb. of carbon atoms of the i^{th} FAME; T_{bi} , normal ebullition point of the i^{th} FAME. w_i , weight prop. of the i^{th} FAME.	<i>n.d.</i>	18, N=49/ 12.4, N=6	(Catoire, 2006)
Higher heating value (HHV)	MJ/kg					
Model 1		<p>HHVs of individual FAMES (higher heating value of the i^{th} FAME in the mixture) :</p> $\delta_i = 46.19 - \frac{1794}{M_i} - 0.21 nc_i \quad (6.1)$ <p>Linear mixing rule :</p> $HHV = \sum_i^n x_i \delta_i \quad (6.2)$	x_i , mol. mass fraction of the i^{th} FAME; M_i , mol. weight of the i^{th} FAME.	1.92	0.87, N=38/ 0.49, N=6	(Ramírez-Verduzco, 2012)
Iodine value (IV)	g I ₂ /100 g					
Model 1		<p>Global FAMES mixture correlation (slightly tuned in this study) :</p> $IV = 89.79 - 1.11 \cdot w_{10:0} - 0.85 \cdot w_{12:0} - 0.97 \cdot w_{14:0} - 0.43 \cdot w_{16:0} - 0.59 \cdot w_{16:1} - 0.81 \cdot w_{18:0} - 0.11 \cdot w_{18:1} + 0.77 \cdot w_{18:2} + 1.49 \cdot w_{18:3} - 0.8 \cdot w_{20:0} \quad (7.1)$ $R^2 = 0.898$ <p>Performs better at: $w_{14:0} \leq 17$; $w_{12:0} \leq 44$; $w_{18:0} \leq 18$; $w_{16:0} \leq 26$; and $w_{18:0} > 10$</p>	w_i , weight prop. of the C10-20:0, C16:1 and C18:1-3 FAMES.	1.79 (-0.26, 3.37); N=10	11.08, N=158/ 3.75, N=5*	(Gopinath et al., 2009)
Model 2		<p>Global FAMES mixture correlation :</p> $IV = \sum_i^n 100 \left(\frac{253.81 \cdot w_i \cdot ndb_i}{M_i} \right) \quad (7.2)$	ndb_i , numb. of double bonds of the i^{th} FAME; w_i , weight prop. of the i^{th} FAME;	<i>n.d.</i>	8.29, N=158/ 2.96, N=5*	(Knothe, 2002)

			x_i , mol. mass fraction of the i^{th} FAME; M_i , mol. weight of the i^{th} FAME.			
Model 3		Global FAMEs mixture correlation (slightly tuned in this study) : $IV = w_{n:1} + 1.5 \cdot w_{n:2} + 2.51 \cdot w_{n:3}$ (7.3)	$w_{n:1}$, weight prop. of the monounsaturated FAMEs; $w_{n:2}$, $w_{n:3}$, weight prop. of the ployunsaturated FAMEs.	10.6 (5.5, 12.24); N=10	10, N=158/ 7.44, N=5*	(Kyriakidis and Katsiloulis, 2000)
Induction period (IP)	h					
Model 1		$IP = 6.1924 + 0.85242 \cdot w_{8:0} - 1.31462 \cdot w_{10:0} + 0.24307 \cdot w_{12:0} + 0.23174 \cdot w_{14:0} + 0.15171 \cdot w_{16:0} - 0.13884 \cdot w_{18:0} + 0.01139 \cdot w_{18:1} - 0.07447 \cdot w_{18:2} - 0.06931 \cdot w_{18:3} - 0.67224 \cdot w_{20:0} - 0.05735 \cdot w_{20:1} - 0.07329 \cdot w_{22:1}$	w_i , weight prop. of the C8-20:0, C18:1-3, C20:1 and C22:1 FAMEs.	n.d.	22, N=55/ 13.9, N=6	(Barradas Filho et al., 2015)
Model 2		Global FAMEs mixture correlation : $IP = \frac{117.9295}{(w_{18:2} + w_{18:3})} + 2.5905$ (8.1) Conditions: $0 < (w_{18:2} + w_{18:3}) < 100$	w_i , weight prop. of the C18:2, and C18:3 FAMEs.	n.d.	28, N=50/-	(Park et al., 2008)
Model 3		Global FAMEs mixture correlation : $OS = 0.27 \cdot w_{n:0} + 0.31 \cdot w_{n:1} - 0.09 \cdot w_{n:2,3}$ (8.2) $R^2 = 0.88$ Conditions: $7.2 \leq w_{n:0} \leq 92.9$; $5.9 \leq w_{n:1} \leq 83.1$; and $1.2 \leq w_{n:2,3} \leq 61.3$ Global FAMEs mixture correlation : $OS = 49.0 \cdot w_{n:2,3}^{-0.50}$ (8.3) $R^2 = 0.91$ Conditions: $1.2 \leq w_{n:2,3} \leq 61.3$	$w_{n:0}$, weight prop. of the saturated FAMEs; $w_{n:1}$, weight prop. of the monounsaturated FAMEs; $w_{n:2,3}$, weight prop. of the ployunsaturated FAMEs.	5.29-24; N=10	42.6, N=24/ 60, N=6	(Serrano et al., 2014)

Model 4		Global FAMEs mixture correlation : $OS = -0.0384 \cdot DU + 7.770 \quad (8.4)$ $R^2 = 0.6421$ Where the degree of unsaturation (DU) is defined as: $DU = 1 \cdot w_{n:1} + 2 \cdot w_{n:2} + 3 \cdot w_{n:3} \quad (8.5)$	$w_{n:1}$, weight prop. of the monounsaturated FAMEs; $w_{n:2}$, $w_{n:3}$, weight prop. of the polyunsaturated FAMEs.	n.d.	20.5, N=50/-	(Wang et al., 2012)
Pour point (PP)	°C					
Model 1		Global FAMEs mixture correlation : $PP = 0.571 \cdot w_{16:0} - 12.24 \quad (9.1), \text{ with } 0 < w_{16:0} < 45$ $R^2 = 0.863$	$w_{16:0}$, weight prop. of the C16:0.			(Sarin et al., 2009)
Model 2		Global FAMEs mixture correlation : $PP = 18.880 \cdot \overline{nc} - w_{n:1,2,3} \quad (9.2)$	\overline{nc} , weighted avg. no. of carbon atoms; $w_{n:1,2,3}$, weight prop. of the unsaturated FAMEs.			(Su et al., 2011)
Saponification value (SV)	g KOH/100g					
Model 1		Global FAMEs mixture correlation (slightly tuned in this study) : $241.85 + 0.08 \cdot w_{10:0} + 0.38 \cdot w_{12:0} + 0.02 \cdot w_{14:0} - 0.17 \cdot w_{16:0} - 1.67 \cdot w_{16:1} - 0.47 \cdot w_{18:0} - 0.45 \cdot w_{18:1} - 0.42 \cdot w_{18:2} - 0.41 \cdot w_{18:3} - 0.46 \cdot w_{20:0} \quad (10.1)$ $R^2 = 0.715$	w_i , weight prop. of the C10-20:0, C16:1 and C18:1-3 FAMEs.	1.13 (0.19-2.29); N=10	2.25, N=125/4.68, N=6	(Gopinath et al., 2009)
Model 2		Global FAMEs mixture correlation : $SV = \sum_i^n \left(\frac{561.06 \cdot w_i}{M_i} \right) \quad (10.2)$	w_i , weight prop. of the i^{th} FAME; M_i , mol. weight of the i^{th} FAME.	n.d.	5.2, N=125/ 0.52, N=5	(Knothe, 2002)
Kinematic viscosity (η), 40°C	mm ² /s					
Model 1		η s of individual FAMEs (kinematic viscosity of the i^{th} FAME in the mixture) : $\ln(\eta_i)_{C_{n:0}} = a \cdot nc_i^b + \frac{c \cdot nc_i^d}{e \cdot \ln(nc_i) + f + T} \quad (11.1)$	ndb_i , numb. of double bonds of the i^{th} FAME;	1.33; N=247	5.33, N=183/ 6.73, N=5	(Chavarría-Hernand

		<p>Individual monounsaturated FAMES :</p> $\ln(\eta_i)_{C_{n:1}} = g \cdot nc_i^h + \frac{i \cdot nc_i^j}{k + T} \quad (11.2)$ <p>Individual polyunsaturated FAMES :</p> $\ln(\eta_i)_{C_{n:2,3}} = g \cdot (nc_i - ndb_i^l)^h + \frac{i \cdot (nc_i - ndb_i^l)^j}{k + T} \quad (11.3)$ <p>with $T = 313.15 \text{ K}$ Linear mixing rule : $\ln(\eta) = \sum_i^n x_i \cdot \ln(\eta_i) \quad (11.4)$</p>	<p>nc_i, numb. of carbon atoms of the i^{th} FAME; w_i, weight prop. of the i^{th} FAME; Values of parameters $a - l$ given by the reference; x_i, mol. mass fraction of the i^{th} FAME.</p>			ez and Pacheco - Catalán, 2014)
Model 2		<p>ηs of individual FAMES (kinematic viscosity of the i^{th} FAME in the mixture) : $\ln(\eta_i) = -12.503 + 2.496 \cdot \ln(M_i) - 0.178 \cdot ndb_i \quad (11.5)$ Linear mixing rule : cf. (11.4)</p>	<p>ndb_i, numb. of double bonds of the i^{th} FAME; M_i, mol. weight of the i^{th} FAME.</p>	1.68	5.37, $N=183$ / 6.81, $N=6$	(Ramírez Verduzco, 2013)
Model 3		<p>Global FAMES mixture correlation : $\eta = A \cdot \overline{nc} + B \cdot \overline{ndb} + C \quad (11.6)$ Performs better at: $\eta \leq 4.77 \text{ mm}^2/\text{s}$</p>	<p>\overline{nc}, weighted avg. no. of carbon atoms; \overline{ndb}, weighted avg. no. of double bonds;</p>	5.45	11.37, $N=176$ / 10.82, $N=6$	(Su et al., 2011)

* Coconut oil value out of range

φ_i , cetane number of the i^{th} FAME; M_i , molecular weight of the i^{th} FAME; ndb_i , number of double bonds of the i^{th} FAME; nc_i , number of carbon atoms of the i^{th} FAME; w_i , weight proportion of the i^{th} FAME; x_i , molar mass fraction of the i^{th} FAME; $w_{14:0}$, weight proportion of C14:0 methyl-ester; $w_{16:0}$, weight proportion of C16:0 methyl-ester; $w_{18:0}$, weight proportion of C18:0 methyl-ester; $w_{16:1}$, weight proportion of C16:1 methyl-ester; $w_{18:1}$, weight proportion of C18:1 methyl-ester; $w_{18:2}$, weight proportion of C18:2 methyl-ester; $w_{18:3}$, weight proportion of C18:3 methyl-ester; n : total number of FAMES

ρ_i , density of the i^{th} FAME;

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