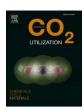
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# Review article



# Activated carbon from biomass: Preparation, factors improving basicity and surface properties for enhanced CO<sub>2</sub> capture capacity – A review

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#### ABSTRACT

There has been a concerted and continued effort to enhance the  $CO_2$  capture capacity of activated carbon (AC) by adopting various physical and chemical treatments on the AC materials. This review is aimed for the compilation of works performed by various researchers on the synthesis of AC from biomass and two major modification works performed on them to improve their basicity for the application towards  $CO_2$  adsorption. The different methods of preparation of ACs utilizing biomass as starting materials have been reviewed. The effects of carbonization and activation on the surface properties of the ACs were discussed. Basicity of AC plays a vital role in the adsorption of  $CO_2$  along with the activation of carbon obtained from the carbonization of biomass. The improvement of basicity of ACs by i) nitrogen incorporation and ii) metal oxide impregnation, the various methods adopted to incorporate the above components and their effect on  $CO_2$  capture have been discussed in detail.

# 1. Introduction

The life-threatening problems, such as climate changes and global warming faced by the human beings in this 21st century is the outcome of elevated release of  $\mathrm{CO}_2$  to the atmosphere. The major sources of  $\mathrm{CO}_2$  pollutions are anthropogenic activities such as fossil fuel combustion, deforestation, industrial emissions etc. The concentration of atmospheric  $\mathrm{CO}_2$  has reached 412 ppm in the year 2021 and it is responsible for an average raise in temperature by 1.2 °C [1]. The resultant effects are melting of glaciers, rise in sea level, heat waves etc. which will disrupt the usual balance of nature.

The continuous increase in the  $CO_2$  concentration in atmosphere has to be curbed in an effective manner.  $CO_2$  can be either directly absorbed from the atmosphere or collected from flue gas streams following efficient techniques. The captured  $CO_2$  is either stored using appropriate methods (Carbon Capture and Sequestration) or used to convert into useful chemicals (Carbon Capture and Utilization). A number of techniques such as absorption, membrane separation and adsorption are being used for the removal of  $CO_2$  [2]. Adsorption using liquid ammonia was the widely used technique, but due to its high cost of regenerations, high volatility and high alkalinity researchers were on the study to develop an alternative way. Later on, a cost-effective as well as efficient technique was developed, which is by using the process of adsorption

technique. Adsorption involves use of several adsorbents such as AC [3], zeolites [4], mesoporous silica [5], Metal Organic Frameworks (MOFs) [6] and Covalent Organic Frameworks (COFs) [7]. AC possesses significant advantage over the other adsorbents as it can be obtained from natural and cost-effective sources. It has high surface area, porosity, pore volume those form important factors for better adsorption, in addition to their very easy processability.

A great variety of carbon precursors are available such as petroleum coke, polymers, wood, coal and biomass. Among them, different kinds of biomass such as chitosan, shells, seeds, rice husk, saw dust etc. serve as better carbon precursors as they are inexpensive and can be easily processed to prepare ACs [8–10]. The adsorption capacity of the AC is enhanced when the number of basic sites, such as nitrogen as well as metal oxides on the carbon increases [11]. For instance, the N-doped AC prepared by the stepwise crosslinking of melamine and ZnCl<sub>2</sub>/NaCl with polyethylene terephthalate (PET) resulted in an enhanced CO2 adsorption capacity due to the enhanced nitrogen content in the carbon as well as the enhanced basicity [12]. The N-doped AC not only serves as better CO<sub>2</sub> adsorbents but also as supercapacitors as well as catalyst for oxygen reduction [13–15]. For example Kaare et al. prepared AC from wood biomass followed by nitrogen doping on the AC using dicyandiamide (DCDA). This N-doped AC was used as a catalyst for oxygen reduction [16,17]. Similarly, Li et al. prepared N-doped AC which showed

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excellent electrochemical performance, where corncob was used as carbon precursor and urea as nitrogen source [18]. In another study conducted by Ying Zhao, it can be seen that the CO2 is adsorbed due to the presence of Ba<sup>2+</sup> ions as well as uncoordinated nitrogen species trapped in a porous surface making a highly polar host and thereby electrostatic interaction is occurred between CO<sub>2</sub> and the porous surface [19]. These basic sites react with the Lewis acidic CO<sub>2</sub> molecules, thereby enhancing the chemisorption of CO<sub>2</sub> molecule. The basicity of AC can be improved either incorporating/doping nitrogen onto the carbon framework or by incorporating basic metal ions or basic metal oxides on the carbon. However, related review articles are lacking in literatures on this topic, where the role of basicity in the adsorption of CO2 is discussed. Existing reviews mainly focus on the preparation of carbon, its activation using different activating agents and the role of surface properties on the carbon capture. Therefore in this review we mainly focus various methods to improve basic sites on the AC for an enhanced CO2 capture capacity.

# 2. Carbon capture technologies

Many technologies are commercially used to capture carbon dioxide from gaseous stream. The production of synthesis gas, ammonia, hydrogen are the processes, which involves separation of  $CO_2$  from the gas streams on a large scale [20]. The major technologies involved are mainly, as follows:

# 2.1. Post-combustion

where CO2 is captured from flue gases after combustion. In this process the flue gas is passed through a gas separation unit in which CO<sub>2</sub> is removed. The obtained gas stream, which is rich in CO2 further undergo compression and hydration for transporting and storing, while the remaining flue gases such as N2 and O2 are evolved to the atmosphere. The gas separation involves processes such as absorption, adsorption and membrane separation. A major disadvantage of this method is the low partial pressure of CO2 in flue gases, which is of about 0.03-0.15 bar. This is due to the fact that the flue gas evolved from the combustion system will be usually at atmospheric pressure and the flue gas themselves contain a very low concentration of CO2. Post-combustion procedure requires a large amount of flue gas to process and it produces a large volume of impurities also. Regardless of these drawbacks, it is the most suitable process that can be used in gas-fired power plants. Also it can retrofitted without any change in its configuration in the coal-fired power plants [21]. Fig. 1 exhibits schematic representation of Post-Combustion CO2 capture.

# 2.2. Oxyfuel

where the combustion of carbonaceous fuel takes place in pure oxygen atmosphere instead of air, which in turn will increase the

concentration of  $CO_2$  in the flue gas. This process eliminates nitrogen from the flue gas and combustion of hydrocarbon or the carbonaceous fuel occurs in a completely pure oxygen atmosphere [23] at a combustion temperature of 3500 °C, which is comparatively high for typical power plant materials. The products obtained by the combustion of flue gas in oxyfuel technology are highly concentrated  $CO_2$  and water vapour, from which  $CO_2$  is removed by dehydration and purification under low temperature. Due to the different fuels used, such as  $SO_x$ , HCl,  $NO_x$  etc., and the diluents used in the oxygen streams there are chances for creating impurities. Similarly, the air leakage in the system is also prone to increase the impurities in the system.  $CO_2$  captured using the oxy-combustion system is compressed and transported using aluminium, iron or steel pipelines. Fig. 2 represents the schematic diagram for oxyfuel process.

#### 2.3. Pre-combustion

where CO2 is captured from the reformed synthesis gas of an upstream gasification unit. In the pre-combustion process, a primary fuel is reacted with oxygen, or air and/or steam to produce CO and H2 which is called synthesis gas or syngas. A catalytic reactor also called a shift converter is included in the combustion unit where CO is made to react with steam to produce CO2 and more H2. This CO2 formed can be separated, compressed and made available for transport and storage, whereas the remaining H<sub>2</sub> can be used as in applications such as boilers, fuel cells, furnaces, gas turbines and engines [23]. The commonly used  ${\rm CO_2}$  capture method is absorption using a physical or chemical solvent. Chemical solvents like tertiary amine methyldiethanolamine (MDEA) degases CO<sub>2</sub> from the syngas at a partial pressure of about 1.5 MPa, while physical solvent processes extracts CO<sub>2</sub> at higher partial pressures. Adsorption is another method, which is used to separate the gases at both high and low temperature. For example, water gas shift reaction uses solid adsorbents for the conversion of CO combined with CO2

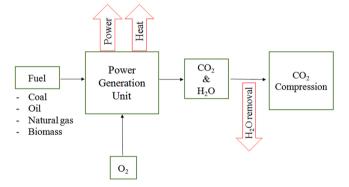


Fig. 2. Schematic representation of Oxyfuel process [22].

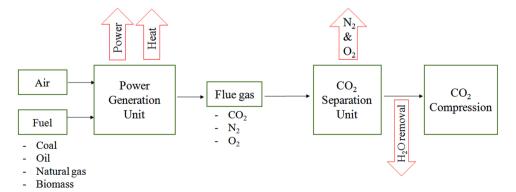


Fig. 1. Post-Combustion CO<sub>2</sub> capture process [22].

removal. Other possible methods are membrane technology and low temperature separation processes (e.g. cryogenic distillation) [24]. Fig. 3 represents the schematic diagram for pre-combustion process.

Among the  $\mathrm{CO}_2$  separation processes used in the pre-combustion as well as post combustion technologies, adsorption carries a lot of advantages such as i) reduction in the cost of  $\mathrm{CO}_2$  capture ii) higher efficiency of carrying  $\mathrm{CO}_2$  iii) lesser conditions for regeneration iv) faster rate of reaction v) minimum pressure drop [25]. For adsorption, AC acts as the suitable material which adsorbs  $\mathrm{CO}_2$  from a mixture of gases. Industrial applications such as urea production, extractant synthesis, beverages, fire extinguishers etc., use AC as the adsorbent. The characteristics of AC including cost effectiveness, higher surface properties, ease of availability etc., makes it a better adsorbent for pre-combustion as well as post-combustion  $\mathrm{CO}_2$  capture [26].

# 3. Preparation of AC from biomass

Different kinds of precursors are used to produce porous carbon materials such as hybrid organic-inorganic composites, synthetic polymers and biomass. However, the use of synthetic hybrid composites and synthetic polymers often suffer from extreme use of raw chemicals as well as highly complicated synthesis process [27]. Biomass is a renewable biogenic organic-inorganic energy source, which is produced by natural and anthropogenic processes, where it is naturally formed as the vegetation in land or water by photosynthesis reaction and the anthropogenic activity, which involves the processing of these natural constituents [28]. The major advantage of using biomass as the carbon precursor is its ease of processability, economical benefit as well as recyclability [29]. The benefits of biomass over other carbon precursors are, they are naturally abundant, renewable, environmental friendly, sustainable and has a greater surface area and complex pore structure [27]. However, preparation of activated carbon from certain sulfur containing biomasses such as oak and corn stover releases sulfur to the surroundings resulting in environmental hazards [30,31]. The commonly used biomass involves cellulosic based precursors, such as coconut shell, palm kernel shell, lotus stalk, date seeds, leaves, barks, sugarcane bagasse, rice husk, algae, etc. Biopolymers such as, glucose, chitin, chitosan, gelatin, starch have also been used as renewable carbon sources. The structural, surface properties as well as the chemical composition of AC vary according to the source of biomass used for their preparation [32]. Preparation of AC from the biomass involves two main

steps, i.e., i) carbonization of the biomass in the absence of oxygen at a temperature below 800  $^{\circ}\text{C}$  followed by ii) activation of the carbon for improving the microstructural properties such as, surface area, porosity, pore volume and pore diameter.

#### 3.1. Carbonization

Carbonization is the process in which the carbon content of the sample is enriched by thermally treating the precursor in an oxygen free environment, which results in the removal of the non-carbonaceous species from the carbon network structure. The exclusion of oxygen is important so as to prevent the oxidation of the carbon as well as to limit the formation of water and other gases. Carbonization generally involves the formation of carbon, which has lower surface area, pore volume and pore diameter but still has an influence in the final product. The final product depends mainly on the carbonization temperature, flow rate of inert gas, heating rate and the dwell time. As the carbonization temperature increases the amount of carbon content simultaneously increases but the yield is decreased due to higher ash content. Similarly lower the heating rate, higher will be the carbon content due to a higher degree of dehydration. In addition, the increase in the dwell time helps to develop greater number of pores in the carbon. Furthermore, if the flow rate of inert gas is too low, it takes more time to create an inert atmosphere in the furnace which in turn results in the ashing of sample due to the presence of oxygen. Table 1 represents the yield of carbon content as well as ash content and moisture content at different carbonization temperatures for various biomass.

#### 3.2. Activation

Next important factor, which affects the physico-chemical properties and yield of the final product is the method of activation of carbon. As the surface area and pore volume of AC increases, the number of adsorbing sites increases and as a result  $\mathrm{CO}_2$  adsorption also increases. Thus the enhancement in the surface properties such as surface area, porosity, pore volume, and pore diameter as well as the incorporation of surface functional groups can be achieved by the process of activation. Activation can be performed in two ways, viz., physical activation and chemical activation methods. Physical activation uses steam or  $\mathrm{CO}_2$  as the activating agents while in chemical activation the activating agents used are certain chemicals such as  $\mathrm{ZnCl}_2$ ,  $\mathrm{KOH}$ ,  $\mathrm{K}_2\mathrm{CO}_3$ ,  $\mathrm{H}_3\mathrm{PO}_4$ , etc.

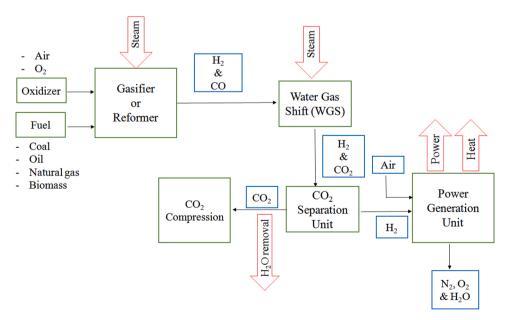


Fig. 3. Schematic representation of Pre-combustion process [22].

**Table 1**Yield of carbon content as well as ash content and moisture content at different carbonization temperatures for various biomass.

Carbon Precursor	Carbonization temperature (°C)	Carbon yield (%)	Ash content (%)	Moisture content (%)	Ref
Palm shell	300	_	0.85	7.40	[33]
Coconut					
Shell	300	_	4.20	6.80	[33]
Palm Kernel					
Shell	350	-	2.6	6	[34]
Paw paw					
trunk	400	69	10.20	3.50	[35]
Rubber					
wood	500	80	8.00	4.00	[36]
Sugarcane					
Bagasse	680	19.5	3.3	8.4	[37]
Coconut					
leaves	700	35	0.16	0.59	[38]
Spruce bark	700	41	2.70	-	[39]

Physical activation of biomass with  $CO_2$  will proceed through certain reactions (Eq. 1), which results in higher surface area and pore volume [40].

$$C(s) + CO_2(g) \rightarrow 2CO(g) \tag{1}$$

 $CO_2$  activation results in the formation of microporous carbons, while steam activation results in meso and macroporous carbons [41]. The activation depends on factors such as, activation temperature and activation time. Ogungbenro et al. prepared AC from date seeds using  $CO_2$  as the activating agent [42]. The different activation time and temperature used in the study led to a significant alteration in the textural characteristics as well as  $CO_2$  capture capacity of as formed ACs. Prolonged activation time resulted in the pore damage reducing the surface area and pore volume. Activation temperature at 900 °C gave a surface area of 723.72 m²/g for the resulting AC.  $CO_2$  activation along with NH<sub>3</sub> modification demonstrated by Zhang et al. produced AC with enhanced surface area and improved nitrogen content [43]. The surface are of the sample increased from 224 m²/g (for the untreated biochar) to  $627 \text{ m}^2/\text{g}$  (AC).

Another method of physical activation is using steam. The activation proceeds through the following reaction (Eq. 2)

$$C(s) + H_2O(g) \rightarrow CO(g) + H_2(g)$$
 (2)

Steam activation is an effective activation technique, which results in the decrease of acidic and increase of phenolic functional groups. Also, steam activation has an effect on pore size distribution and elemental composition. Heo et al. prepared steam AC using cellulose fiber [44]. The carbonized material was activated at 800 °C using steam showed an adsorption capacity of 3.77 mmol/g and a good CO2/N2 selectivity due to the enhanced interaction energy between CO2 and carbon. However, the activation of carbon using a combination of steam and CO2 is always preferred over activation using either steam or CO2 alone. Roman et al. reported the preparation of AC using olive stones as the carbon precursor and steam, CO2 and combination of both for the activation of carbon. The surface area of steam activated sample was 1074 m<sup>2</sup>/g and the CO<sub>2</sub> activated sample was 572 m<sup>2</sup>/g while a CO<sub>2</sub>/steam combined activation resulted in a surface area of 1187  $\text{m}^2/\text{g}$  [45]. This is due to the fact that the combination of CO2 and steam results in the increase in their partial pressures. As a result the interaction between them and carbon gets improved, enhancing the porosity of the carbon.

Activation using chemical activating agents is the widely used activation technique for the preparation of AC due to their simple and convenient methodology, among which KOH is commonly used one. The process of KOH activation proceeds through the following reactions (Eqs. 3 to 7). The evaluation of volatile species enhances the microstructural properties of the ACs.

$$Biomass(s) + KOH(s) \rightarrow Biomass.K_2O(s) + H_2O(1)$$
 (3)

$$Biomass(s) + H2O(l) \rightarrow C(s) + H2O(g) + tar(l)$$
(4)

$$C(s) + H2O(g) \rightarrow H2(g) + CO(g)$$
(5)

$$CO(g) + H2O(g) \rightarrow H2(g) + CO(g)$$
(6)

$$2K_2O(s) + H_2(g) + CO_2(g) + C(s) \rightarrow C(s) + K_2CO_3(s) + H_2O(g)$$
 (7)

The surface area and porosity of the KOH AC depends on the ratio of KOH to the carbon as well as on the residence time. For example, Sun et al. prepared AC from raw hemp stem using different ratios of KOH such as 1, 3 and 5 at an activation temperature of 800 °C. Among the three ratios, carbon: KOH of ratio 1:3 was the optimal ratio to produce AC with enhanced surface area (2879  $\text{m}^2/\text{g}$ ). The impregnation ratio 1:1 produced higher microporous material while the ratio 1:5 produced a material with diminished microporosity due to the intense chemical reaction [46]. Zinc chloride is another chemical activating agent, which is mainly mixed in situ with the biomass for the preparation of AC. At lower activation temperature (400 °C to 500 °C), ZnCl2 acts as a strong dehydrating agent, while higher activation temperature (above 500 °C) results in the decomposition ZnCl<sub>2</sub> to zinc and chlorine resulting in the improved porosity and surface area of the AC [47,48]. The use of ZnCl<sub>2</sub> as the activating agent also improves the carbon content through the formation of aromatic graphitic structures. However, as the amount of ZnCl<sub>2</sub> used increases the yield is reduced [49]. Spagnoli et al. reported the synthesis of AC from cashew nut shell using ZnCl<sub>2</sub> as the activating agent with an impregnation ratio 1.5:1 (ZnCl<sub>2</sub>: cashew nut shell) at activating temperatures 400 °C and 500 °C. The results showed that as the activation temperature increased from 400 °C to 500 °C, there occurred an enhancement the surface characteristics as well as the adsorption capacity [50]. Phosphoric acid is another activating used to improve the surface properties of AC. Olivares et al. reported that during the activation process, H<sub>3</sub>PO<sub>4</sub> polymerizes to form polyphosphoric acid [51]. The monomer H<sub>3</sub>PO<sub>4</sub> dehydrates to form P<sub>2</sub>O<sub>5</sub> and further reacts with carbon to form P and CO2, while the polyphosphoric acids decompose into steam, P and O in the gaseous state.

$$5C(s) + 2P_2O_5(1) \rightarrow P_4(g) + 5CO_2(g)$$
 (8)

$$2H_2P_2O_7^{2-}(1) \rightarrow P_4(g) + 6O_2(g) + 2H_2O(g)$$
 (9)

The gases formed in the above reactions create porosity on the carbon framework. Table 2 represents surface characteristics as well as  $CO_2$  adsorption of the ACs prepared from biomass using various activating agents. Once the chemical activation process is completed, the AC are washed thoroughly with hot deionized water, in order to remove excess  $ZnCl_2$ , KOH or  $H_3PO_4$  on the carbon which otherwise tend block the pores of the carbon and thus prevent the  $CO_2$  adsorption process [52].

In certain cases the carbonization and activation are combined in a single step. The carbon precursor is mixed with the activating agent and is carbonized at a high temperature in an inert atmosphere to obtain the AC [66]. For example, Lee et al. prepared N-doped AC by mixing chitosan with urea (nitrogen source), KOH (activating agent) and carbonized at 700–1000 °C. Here the activating agent was mixed with the carbon precursor before carbonization. In another study, Thote et al. prepared AC from soybean where the precursor was mixed with ZnCl2 which served as the activating agent and was carbonized at 600 °C [67].

# 4. Modification of AC to improve basicity

The basicity of AC is one of the important factors, which affect the adsorption as well as selectivity of  $CO_2$  over  $N_2$ . Since  $CO_2$  is acidic in nature, strong basic functional groups such as nitrogen or basic metal oxides can donate the lone pair of electrons resulting in the enhancement of chemisorption of  $CO_2$ . The major advantages and disadvantages

Table 2
Surface characteristics as well as CO<sub>2</sub> adsorption of the ACs prepared from biomass using various activating agents.

Carbon precursor	Activating agent	Activating temperature (°C)	BET surface area (m²/g)	Pore volume (cc/g)	CO <sub>2</sub> adsorption (mmol/g) capacity	Adsorption temperature (°C) & pressure (bar)	Ref
Date seeds	CO <sub>2</sub>	900	723.72	0.26	3.20	20, 1.013	[42]
Cherry stones	$CO_2$	885	1045.00	0.48	2.60	25, 1.013	[53]
Rice husk	$CO_2$	900	1097.00	0.83	3.1	25, 1.013	[54]
Walnut shell	$CO_2$	500	810.85	0.34	1.58	20, 1.013	[55]
Cellulose fiber	Steam	800	863.00	0.34	3.77	25, 1.013	[44]
Willow	Steam	800	840.60	0.57	_	_	[56]
Walnut shell	Steam	850	1361.00	0.94	_	_	[57]
Cherry stones	Steam	850	998.00	0.53	2.4	25, 1.013	[53]
Olive stones	Steam & CO <sub>2</sub>	850	1187.00	0.70	_	_	[45]
Coconut shells	Steam & CO <sub>2</sub>	900	2194.0	1.29	_	_	[58]
Commercial AC FPV	KOH	850	2406.00	0.46	3.67	25, 1	[59]
Tea seed shell	KOH	700	1503.20	0.64	3.15	25, 1	[60]
Argan hard shells	KOH	850	1889.63	0.87	5.63	25, 1	[61]
Argan hard shells	NaOH	850	1826.96	0.96	3.73	25, 1	[61]
	LiCl-ZnCl <sub>2</sub>						
Chitosan	molten salt	1000	2025.00	1.15	5.6	25, 1	[62]
Citrus aurantium							
Waste Leaves	$ZnCl_2$	800	937.00	0.57	6.5	25, 1	[63]
Raw bamboo	$H_3PO_4$	500	1492.00	0.93	1.45	25, 1	[64]
Subabul wood	$H_3PO_4$	800	823.00	0.26	4.52	25, 1.013	[65]

in the modification of AC to improve the basicity are tabulated in Table 3.

# 4.1. Nitrogen doped AC

The acidic nature of CO<sub>2</sub> derives it to get adsorbed on basic groups such as nitrogen containing groups. Moreover, when the graphene layer of AC is doped with nitrogen atoms, it is doped flat on to the surface of the AC, which is more stable as compared to oxygen containing functional groups (e.g., OH, COOH, and CO). When nitrogen is doped on to the carbon framework, the carbon atoms are replaced with nitrogen atoms to form a pentagonal or hexagonal shape with adjacent carbon atoms on the graphene layer. Thus, nitrogen when incorporated on to the AC commonly available in three different forms such as pyridinic, pyrrolic, and graphitic which contributes towards the higher microporosity and surface area resulting in an enhanced CO2 capture capacity [68]. A pyridinic-N atom is included in a hexagonal structure, which is bonded to two carbon atom and has a sp<sup>2</sup> hybridization, which can donate one p electron to the  $\Pi$  system. Pyrrolic-N atom is consisted in a pentagonal structure and is bonded to two carbon atoms with a sp<sup>3</sup> hybridization, which will donate two p electrons to the  $\Pi$  system. Graphitic-N is the species for which nitrogen is sp<sup>2</sup> hybridized and bonded with three carbon atoms [69]. Both pyridinic and pyrrolic N exist at the edges of graphitic carbon layers, while graphitic N exist inside the graphitic carbon layer. Oxidized-N and aminic-N are other nitrogen species observed in AC besides these three N species [70]. The formation of these nitrogen species can be controlled by changing the carbonization temperature. Aminic-N is formed at a carbonization

**Table 3**Advantages and disadvantages in the modification of AC to improve basicity.

Advantages	Disadvantages
Improvement in the lone pair of electrons which functions as Lewis bases	Byproducts formed during the modification reaction bring chemical waste to the environment Higher energy consumption as it requires high temperature for the surface
Improvement in the CO <sub>2</sub> adsorption capacity	modification to incorporate functional groups
Enhancement in textural properties such as surface area and pore volume Improvement in the carbon, nitrogen	
and oxygen contents	

temperature below 300 °C while around 600 °C pyridinic and pyrrolic nitrogens existed. As the carbonization temperature increases above 700 °C, the presence of graphitic nitrogen increases while the existence of all other nitrogen species diminishes [70,71]. Among these nitrogen species the pyridinic and pyrrolic nitrogen shows the maximum CO2 adsorption capacity since the lone pair of electrons on pyridinic as well as pyrrolic nitrogen species are available for donation to the Lewis acidic CO2 molecule enhancing the chemisorption of CO2. Among these two, the pyridinic nitrogen shows improved basicity than pyrrolic nitrogen and thus the maximum CO2 adsorption capacity since the lone pair of electrons in the pyrrolic nitrogen engages in delocalization while that of pyridinic nitrogen can share its lone pair of electrons [72]. Thus the increase in the number of pyrrolic as well as pyridinic nitrogen on the AC results in the enhancement of CO<sub>2</sub> capture capacity of the same. The amount of nitrogen doped in to the AC can be found out by using CHN analysis which gives quantitative information about the amount of C, H and N available on the sample. The qualitative as well as quantitative identification of nitrogen species present on the N-doped AC can also be performed using XPS analysis. The ratio of the peak intensities of N 1 s and C1 s from the XPS spectra gives the amount of nitrogen content on the AC. The deconvoluted N 1 s spectrum gives the qualitative information about the species of nitrogen present on the sample. Each nitrogen species possess characteristic binding energies in the XPS spectra. Pyridine, pyrrole, graphitic nitrogen and oxidized nitrogen has binding energies  $398.5 \pm 0.4 \text{ eV}, \ 400.5 \pm 0.4 \text{ eV}, \ 401.2 \pm 0.4 \text{ eV} \ \text{and} \ 402.9$  $\pm$  0.4 eV respectively [73]. For instance, Khan et al. prepared N-doped AC from chitosan for electrocatalytic and photocatalytic application. The XPS studies for the samples exhibited the presence of pyridinic-N, pyrrolic-N, graphitic-N, and N - O at the binding energies 398.4 eV, 399.9 eV, 400.8 eV, and 401.8 eV, respectively [70]. Fig. 4 represents the interaction between CO2 and N-doped AC. The incorporation of nitrogen into the carbon framework can be performed through three processes, viz., (i) by amine functionalization (ii) by in-situ nitrogen doping and (iii) single-step nitrogen doping. The doping of nitrogen on AC helps in the improvement of surface properties of the AC. This is due to the fact that the incorporation of a heteroatom into the carbon framework, besides an increased basicity, causes defects in the carbon structure creating pores in the carbon network structure during pyrolysis [74].

# 4.1.1. Amine functionalization

In this process, the porous AC was modified with amine functionalization resulting in a more basic amine grafted AC, which improves the

Fig. 4. Interaction between CO2 and N-doped AC.

CO<sub>2</sub> adsorption extensively. When the carbon comes in contact with ammonia, the oxides on the carbon reacts with ammonia to form ammonium salt, and the amine groups undergoes dehydration or dehydrogenation producing nitriles, amides and pyridinic and pyrrolidic functionalities [75]. Heidari et al., synthesized AC from eucalyptus wood using H<sub>3</sub>PO<sub>4</sub> as activating agent, modified by ammonia. Nitrogen doping was dependent on the temperature and the maximum nitrogen incorporation happened for samples aminated at 800 °C. The nitrogen content of the modified AC reached 7.76% from a value of 0.52%. The basicity of the sample was determined by finding the pH at point zero charge (pH<sub>pzc</sub>) and was found that the value increased after amine modification resulting in the improvement of basicity of AC. The surface area and total pore volume of the ammonia modified carbon was found to be 2079 m<sup>2</sup>/g, 1.292 cm<sup>3</sup>/g respectively whereas for the unmodified carbon it was  $1889 \text{ m}^2/\text{g}$ ,  $1.178 \text{ cm}^3/\text{g}$  respectively which showed that the surface area and the porous nature of the AC were improved due to the ammonia modification. It had a significant effect on the CO2 adsorption capacity also [76]. The unmodified carbon showed an adsorption capacity of 2.98 mmol/g while the ammonia modified carbon exhibited an enhanced adsorption capacity of 3.32 mmol/g. Ammonia decomposes at high temperature to produce NH2, NH radicals and atomic H which reacts with carbon to form CH<sub>4</sub>, (CN)<sub>2</sub>, HCN, and H<sub>2</sub> [77]. Since these gases evolved through the surface of the AC, the BET surface area as well as porosity of the samples increases resulting in the increment of CO2 adsorption capacity. But the use of ammonia is being reduced as it is lost at higher activation temperature and also due to the unpleasant odor during activation process [76,78]. The most common amine used for nitrogen doping on AC was urea. Dilokekunakul et al., prepared AC from bamboo waste and nitrogen doping was performed using urea. The sample prepared showed an enhanced nitrogen content of 3.87% and an adsorption capacity of 2.63 mmol/g while the reference sample had a nitrogen content of 0.57% and an adsorption capacity of 2.52 mmol/g [79]. Similarly Rajasekaran et al. in 2021, developed an AC from coconut shell, modified using tetraethylene pentamine (TEPA) as the dopant. The unmodified carbon showed a nitrogen content of 0.72% and a surface area of 1246 m<sup>2</sup>/g while the N-doped carbon exhibited a nitrogen content of 4.34% and a surface area of 1078 m<sup>2</sup>/g. The N-doped carbon also showed an excellent CO2 adsorption capacity of 9.9 mmol/g. Here also the surface basicity and the microporosity of the N-doped carbon synergistically tailors the adsorption of CO2 on to the AC [80].

# 4.1.2. In-situ nitrogen doping

In-situ nitrogen doping can be performed by carbonization of nitrogen containing compounds such as melamine, gelatin, etc. These compounds, already possess nitrogen in their chemical structure, which when carbonized will be grafted on to the carbon framework. Chitosan is another biomass which serves as both carbon and nitrogen source. The synthesis of N-doped AC was carried out using chitosan as the carbon/nitrogen precursor by Fujiki et al. Chitosan was mixed with different alkali carbonates for activation, and carbonized. The AC using Rb<sub>2</sub>CO<sub>3</sub> as the activating agent at an activation temperature of 600 °C showed a surface area of 1496 m<sup>2</sup>/g, pore volume of 0.63 cc/g, nitrogen content 3.15% and CO<sub>2</sub> capture capacity of 4.88 mmol/g [81]. Similarly, Alabadi et al. synthesized AC by the co-carbonization of gelatin and starch. Here gelatin served as the carbon & nitrogen source. Therefore, its carbonization along with starch resulted in the formation of AC with improved surface properties, nitrogen content and thus CO<sub>2</sub> enhanced capture capacity [82].

#### 4.1.3. Single step nitrogen doping

Another method of nitrogen incorporation is the single step Ndoping, where the carbon precursor is mixed with a nitrogen source such as urea or melamine before carbonization. Here carbonization will result in the doping of nitrogen from the nitrogen source on to the carbon framework. Nitrogen doped AC was prepared using sugarcane bagasse, where it is mixed with urea that serves as the nitrogen source in a study by Han et al. In this study, the N-doped AC possessed a nitrogen content of 1.98% with an enhanced surface area and pore volume and possessed a CO<sub>2</sub> capture capacity of 4.8 mmol/g [83]. This suggested that the incorporation of nitrogen had a significant effect on the texture properties as well as the CO<sub>2</sub> adsorption capacity of the AC. In a recent study, Zgrzebnicki et al. mixed polyfurfuryl alcohol with urea which served as the nitrogen dopant for the preparation of N-doped AC. The surface area as well as the pore volume of the N-doped AC was found to be  $616 \text{ m}^2/\text{g}$ and 0.26 cm<sup>3</sup>/g respectively. Here also the doping of nitrogen had a strong influence on the pore structure and basicity of the AC which in turn enhanced the CO2 adsorption capacity from 0.8 mg/g to 1.8 mg/g [84]. However, in some cases addition of nitrogen source to the carbon precursor can reduce the surface area as well as the CO2 adsorption capacity. Malini et al., prepared AC from chitosan using hexamethylene tetramine (HMT) as an additional nitrogen source. The adsorption capacity of chitosan derived AC was greater than that of chitosan/HMT derived AC. The deterioration in the surface area, pore volume as well as CO<sub>2</sub> capture capacity can be ascribed to the hydrogen bonding interaction between chitosan and HMT which results in the reduction of free volume of the polymer network. Also, the increase in the pH due to the addition of HMT to chitosan causes the physical crosslinking of chitosan polymer which in turn decreases the surface are of the AC [85].

Table 4 represents the various N-dopants on AC and their effect on surface properties as well as the  $CO_2$  adsorption capacity.

Here in the study by Quan et al., the adsorption capacity of N-doped AC is seen to be lower than the undoped counterpart [60]. In this case, the specific surface area of the AC was considered as the dominant factor than the basicity for  $\rm CO_2$  capture and the undoped carbon possessed the maximum specific surface area. The decrease in the surface properties for the N-doped ACs was due to the collapsing of pores during the thermal process for nitrogen doping.

# 4.2. Metal oxide doped AC

Another important criteria to enhance the basicity, surface chemistry as well as the  $\rm CO_2$  capture capacity other than nitrogen doping is the incorporation of basic metal oxide on to the AC surface. The adsorption as well as selectivity of  $\rm CO_2$  over  $\rm N_2$  is enhanced by the electrostatic interaction between the  $\rm CO_2$  molecule and the impregnated metal ion. The commonly used metal oxides are alkaline earth metal oxides such as MgO, CaO, etc., and transition metal oxides such as CuO, NiO, CoO etc. The mechanism of adsorption of  $\rm CO_2$  on to the metal impregnated AC was illustrated in Fig. 5. The metal oxides are commonly impregnated on to the AC surface through wet impregnation method. The carbon precursor is mixed with metal oxide solutions and prior to a high

Table 4
Surface properties and CO<sub>2</sub> adsorption capacity for various N –doped ACs.

Carbon precursor	N source used	Amine functionalization/ Insitu nitrogen doping	N content (%)	BET surface area (m <sup>2</sup> /g)	Pore volume (cc/g)	CO <sub>2</sub> adsorption capacity (mmol/g)	Adsorption temperature (°C) & pressure (bar)	Ref
Eucalyptus								
wood	Ammonia	Amine functionalization	7.76	2079	1.29	3.22	30,1	[76]
Cotton stalk	Ammonia	Amine functionalization	0.71	434.92	0.19	1.81	20, 1.013	[78]
Black locus	Ammonia	Amine functionalization	7.21	2511	1.35	5.05	25, 1	[86]
Microalgea	Ammonia	Amine functionalization	2.57	1509	0.82	4.03	25, 1.013	[87]
Bamboo waste	Urea	Amine functionalization	3.87	532	_	2.63	25, 1	[79]
Coconut shell	Urea	Amine functionalization	1.23	1535	0.96	4.80	25, 1	[88]
Rice husk	Chitosan	Amine functionalization	_	1496	0.78	3.68	25, 1	[89]
Tea seed	Melamine	Amine functionalization	3.41	1187.93	0.52	2.75	25, 1	[60]
Chitosan	_	In-situ N doping	3.15	1496	0.63	4.88	25, 1	[81]
Gelatin and								
starch	_	In-situ N doping	3.00	1636	0.51	3.84	25, 1	[82]
Chitosan	_	In-situ N doping	4.59	1381	0.57	3.86	25, 1.013	[90]
Microalgae and								
glucose	_	In-situ N doping	1.47	1940	0.82	4.50	25, 1	[91]
Prawn shell	_	In-situ N doping	6.00	554.7	0.17	_		[92]
Sugarcane								
Bagasse	Urea	Single step N doping	1.98	1113	0.51	4.80	25, 1	[83]
Coconut shell	Glucosamine	Single step N doping	4.61	984.91	0.65	4.23	30, 1	[93]
Glucose	Melamine	Single step N doping	2.07	3247	3.09	4.95	25, 1	[94]

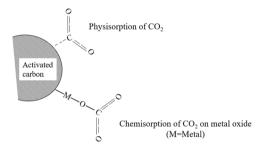


Fig. 5. Mechanism of metal oxide impregnated AC.

temperature carbonization process or the AC is mixed with metal oxide solution and then is calcined at a higher temperature. For example, Botome et al. prepared AC using CCA (chromated copper arsenate) treated wood pyrolyzed at 700 °C for CO2 capture and the sample showed an adsorption capacity of 1.88 mmol/g [95]. The impregnation of metal oxide on the AC makes a significant effect on the structural as well as CO2 adsorption property depending on the amount of metal loading. If the metal loading is considerably low, there won't be any improvement in the adsorption capacity. While significantly high amount of metal loading will lead to the clogging of pores resulting in the lowering of surface area and pore volume. Hosseini et al. suggested that the catalytic surfaces produced on the Cu or Zn modified AC provides active sites to capture CO2. Lesser adsorption energy is needed for the chemisorption oxygen atoms of CO<sub>2</sub> on cationic Cu<sup>2+</sup> and Zn<sup>2+</sup> since there is a shorter distances between these cations and CO2 molecule [96]. Investigations on the effect of metal impregnation on carbon before and after activation showed that, when transition metal oxides such as CrO<sub>3</sub>, CoO, Co<sub>3</sub>O<sub>4</sub>, etc., were added to the carbon before activation process these metals acted as catalysts for the degasification reaction resulting in the formation of meso and micropores on the carbon. The development of wider mesopores results in the dispersion of metal species while the micropore formation results in the deposition of metal oxides on the surface improving the efficiency of the AC [97,98]. On the other hand doping of these metal oxides after activation of the carbon results in the reduction of surface properties due to the blocking of pores on the surface by the metal ions. Moradi et al. developed Fe-impregnated AC for hydrogen storage where the AC before metal impregnation had a surface area of 1640 m<sup>2</sup>/g and a pore volume of 0.93 cc/g which reduced to 1511 m<sup>2</sup>/g and 0.81 cc/g respectively after impregnation [99].

On comparison of the CO2 adsorption capacity of metal oxide impregnated AC derived from palm-kernel shell studied by Hidayu et al., it was found out that CeO2 impregnated AC showed the maximum adsorption capacity than that of  ${\rm TiO_2}$  and BaO impregnated AC. Here metal Ce donate the oxygen atoms to oxidize with CO2 enhancing the CO<sub>2</sub> adsorption [100]. The metal oxide impregnation on AC was confirmed from the XRD studies. The XRD patterns for AC showed two broad peaks at  $2\theta = 20-30^{\circ}$  and  $40-50^{\circ}$ , while in the case of metal oxide impregnated AC these two broad peaks disappeared and substituted with additional diffraction peaks of metal oxide. In a similar study by Hidayu et al., where the AC was impregnated with different metal oxides, the BaO impregnated AC showed the higher and MgO showed the lowest CO<sub>2</sub> adsorption capacity [101]. Here the loading of MgO resulted in the blockage of pores and thus the decrease in the adsorption capacity. On the other hand impregnation of BaO improved the basicity of AC, which in turn increases the electrostatic interaction between CO2 and BaO resulting in the chemisorption of CO2. In a recent report, Malini et al. impregnated barium oxide in various ratios onto AC derived from chitosan using wet impregnation method followed by thermal treatment at under nitrogen atmosphere. The studies showed that 10 wt% barium oxide loaded AC exhibited improved surface properties as well as CO<sub>2</sub> adsorption capacity while an increase in the concentration of barium oxide resulted in the decline CO<sub>2</sub> adsorption properties [102]. The amounts of BaO loaded in to the carbon was quantitatively confirmed using the UV-Visible spectroscopic method, which was found to be 5.2% for 10 wt% barium oxide loaded AC as consistent with the EDS mapping and spot analysis results. The structural and CO<sub>2</sub> adsorption property of ACs mixed with various metal salts are tabulated in Table 5.

# 5. Conclusion and way forward

Global warming is the major concerns faced by the human being in this century and the main cause for that is the increased  $\mathrm{CO}_2$  concentration in the atmosphere. The most important way to control the increasing level of  $\mathrm{CO}_2$  is Carbon Capture and Sequestration, which uses adsorption as the significant method. Use of AC helps to adsorb the  $\mathrm{CO}_2$  in an effective way. In this review the recent works on the synthesis of AC from biomass using different carbonization and activation processes have been summarized. The surface characteristics as well as  $\mathrm{CO}_2$  capture can be improved by increasing the basicity of the AC either by nitrogen doping or by metal impregnations. The various nitrogen dopants as well as metal oxides used in the recent studies, as well as their effect on the surface characteristics and  $\mathrm{CO}_2$  capture capacity were compared,

Table 5
Structural and CO<sub>2</sub> adsorption property of ACs mixed with various metal salts.

Carbon precursor	Metal impregnated	BET surface area (m²/g)	Pore volume (cc/g)	$CO_2$ adsorption capacity (mmol/g)	Adsorption temperature (°C) & pressure (bar)	Ref
	Chromium copper					
Wood	arsenate	1215	0.750	1.88	25, 1	[95]
Coconut shell	CuO	1339	0.540	0.37	25, 1	[103]
Saw dust	MgO	306	_	2.70	50, 1	[104]
Persian						
ironwood	CuO	1918	1.570	6.78	30, 1	[105]
Whitewood	MgO	760	0.399	1.11	25, 1	[106]
Palm kernel						
shell	BaO	1260	0.670	_		[101]
Nypha fruticans	CuO & MgO	727.7	0.260	_		[107]
Chitosan	BaO	259.01	0.027	1.95	25, 1	[102]

#### tabulated and discussed.

There are still many challenges faced in the field of  $\mathrm{CO}_2$  adsorption by biomass derived AC. The large scale production of porous AC from biomass is yet to be investigated. The production cost of the precursors, other chemicals as well as the experimental setup has to be thoroughly examined. The bulk production of the AC material should meet the conditions such as efficiency of  $\mathrm{CO}_2$  capturing capacity and environmental sustainability. Another study should be conducted on the conversion of side products produced during the fabrication of the AC material on account of pollution control. Lastly, there is a dearth of scientific information regarding the conversion of adsorbed  $\mathrm{CO}_2$  into useful products. Therefore more studies on the practical application of  $\mathrm{CO}_2$  conversion need to be conducted.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

# **Data Availability**

No data was used for the research described in the article.

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