일반적 열 전달 방정식 Heat Transfer In General Formula

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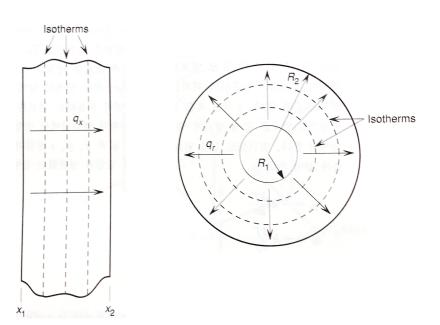
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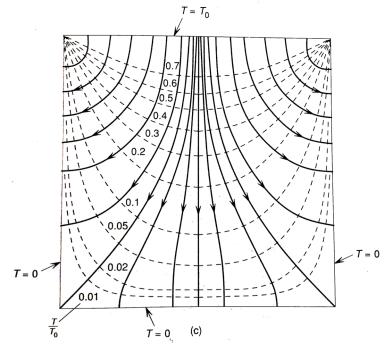


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일반(다차원적) 열전도 방정식

□앞서 우리는 평면벽이나 원통형벽을 통해 1차원적인 열 전도 (즉, 단한방향으로의 열전도)만을 고려하였다.





□더욱 복잡한 형상이나, 다차원적 열 경계 조건에서는 일반적 열전도 방정식을 사용하여 열전도 현상을 설명해야 한다.



등방성 재료의 열전도도

- \square 따라서, 열 흐름 (heat flux) q는 벡터로 표현되며 \vec{q} 3차원 공간에서 세 성분이 필요하다: \vec{q}_x , \vec{q}_y , \vec{q}_z
- □따라서 3차원 공간의 일반적 열흐름 문제를 설명하기 위해서는 Fourier 법칙을 다음과 같이 표현하여야 한다.

$$\vec{q}_{x} = -kA_{x} \frac{dT}{dx}$$

$$\vec{q} = -\bar{k} \cdot \vec{\nabla} T$$

$$\vec{q}_{i} = -\bar{k}_{ij} \vec{\nabla}_{j} T$$

 $\overrightarrow{\nabla}T$: Temperature Gradient

 \overline{k} : 열전도도 tensor

$$\vec{q}_x = -\bar{\bar{k}}_{xx}\vec{\nabla}_x T - \bar{\bar{k}}_{xy}\vec{\nabla}_y T - \bar{\bar{k}}_{xz}\vec{\nabla}_z T$$

$$\vec{q}_{y} = -\bar{\bar{k}}_{yx}\vec{\nabla}_{x}T - \bar{\bar{k}}_{yy}\vec{\nabla}_{y}T - \bar{\bar{k}}_{yz}\vec{\nabla}_{z}T$$

$$\vec{q}_z = -\bar{\bar{k}}_{zx} \vec{\nabla}_x T - \bar{\bar{k}}_{zy} \vec{\nabla}_y T - \bar{\bar{k}}_{zz} \vec{\nabla}_z T$$

$$\vec{q}_x = -\bar{\bar{k}}_{xx}\vec{\nabla}_x T$$

$$\vec{q}_y = -\bar{\bar{k}}_{yy}\vec{\nabla}_y T$$

$$\vec{q}_z = -\bar{\vec{k}}_{zz} \vec{\nabla}_z T$$

$$\vec{q}_x = -k \vec{\nabla}_x T$$

$$\vec{q}_y = -k \vec{\nabla}_y T$$

$$\vec{q}_z = -k \vec{\nabla}_z T$$

Let's assume $\bar{\bar{k}}_{ij} = 0$ if $i \neq j$

열전도도가 등방성을 가질 때.



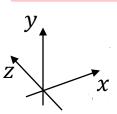
열 에너지 수지

$$\vec{q}_x = -k \vec{\nabla}_x T$$

$$q_x = -k \frac{\partial T}{\partial x}$$

$$q_x = -k \frac{\partial T}{\partial x}$$
 $q_y = -k \frac{\partial T}{\partial y}$ $q_z = -k \frac{\partial T}{\partial z}$

$$q_z = -k \frac{\partial T}{\partial z}$$



$$\vec{q}_z = -k \vec{\nabla}_z T$$

 $\vec{q}_{\mathcal{V}} = -k \vec{\nabla}_{\mathcal{V}} T$

$$\left(\frac{\text{들어온열}}{t}\right) - \left(\frac{\text{나간 9}}{t}\right) + \left(\frac{\text{발생한 9}}{t}\right) = \text{시간당 열에너지 변화}$$

(발생한 g/t) = $\dot{q}\Delta V = \dot{q} \cdot \Delta x \Delta y \Delta z$

열에너지 변화/
$$t=$$
 부피내 재료의 엔탈피 변화/ $t=rac{\partial H}{\partial t}\Delta x\Delta y\Delta z=
ho C_{p(m)}rac{\partial T}{\partial t}\Delta x\Delta y\Delta z$

$$\left(q_x' \Big|_{x} - q_x' \Big|_{x + \Delta x} \right) \Delta y \Delta z + \left(q_y' \Big|_{y} - q_y' \Big|_{y + \Delta y} \right) \Delta x \Delta z$$

$$+ \left(q_z' \Big|_{z} - q_z' \Big|_{z + \Delta z} \right) \Delta x \Delta y + \dot{q} \cdot \Delta x \Delta y \Delta z = \rho C_{p(m)} \frac{\partial T}{\partial t} \Delta x \Delta y \Delta z$$

$$\frac{(q_x'|_x - q_x'|_{x+\Delta x})}{\Delta x} + \frac{\left(q_y'|_y - q_y'|_{y+\Delta y}\right)}{\Delta y} + \frac{\left(q_z'|_z - q_z'|_{z+\Delta z}\right)}{\Delta z} + \dot{q} = \rho C_{p(m)} \frac{\partial T}{\partial t}$$

$$\begin{vmatrix} q'_{z}|_{z+\Delta z} \Delta x \Delta y \\ \Delta y \\ \Delta z \end{vmatrix}$$

$$\begin{vmatrix} q'_{z}|_{z+\Delta z} \Delta x \Delta y \\ A y \Delta z \end{vmatrix}$$

$$\begin{vmatrix} q'_{z}|_{z+\Delta x} \Delta y \Delta z \\ A y \Delta z \end{vmatrix}$$

$$\begin{vmatrix} q'_{z}|_{z} \Delta x \Delta y \\ A y \Delta z \end{vmatrix}$$

$$-\left(\frac{\partial q_{x}}{\partial x} + \frac{\partial q_{y}}{\partial y} + \frac{\partial q_{z}}{\partial z}\right) + \dot{q} = \rho C_{p(m)} \frac{\partial T}{\partial t}$$

$$-k\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) + \dot{q} = \rho C_{p(m)} \frac{\partial T}{\partial t}$$



열전도 방정식

$$-k\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) + \dot{q} = \rho C_{p(m)} \frac{\partial T}{\partial t}$$

Steady-state

No heat-generation

$$-k\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) + \dot{q} = 0 \qquad -k\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial z^2}\right) = 0 \rightarrow \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) = 0$$

$$\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) = 0$$

 $\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) = 0$ Laplacian: Divergence of Gradient: $\sum_{i} \left(\frac{\partial^2 f}{\partial x_i^2}\right)$

정상상태의 수학적 표현방법에 널리 쓰임



2차원 정상상태의 열전도

$$\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2}\right) = 0 \longrightarrow \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2}\right) = 0$$
온도 분포 $T(x, y)$ 및 온도 구배 $\left(\frac{\partial T}{\partial x}, \frac{\partial T}{\partial y}\right)$?

적절한 열경계 조건 (boundary condition)과 적분을 통해 구할 수 있겠다.

$$T(x,y) = \frac{4T_0}{\pi} \sum_{n=0}^{\infty} \frac{1}{n} \frac{\sinh(n\pi y/L)}{\sinh(n\pi)} \sin\frac{n\pi x}{L}$$

왼편에 보시다 시피, 이러한 방법은 매우 까다롭거나, 어렵다...

이런경우, 해를 <mark>근사적</mark>으로 구할 수 있는 <u>유한</u> <u>차분법</u> (Finite difference method)이 유용하다.



5/28/18

유하 차분법

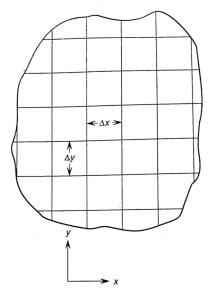
미분

$$\frac{\partial T}{\partial x} = \lim_{\Delta x \to 0} \frac{\Delta T}{\Delta x}$$

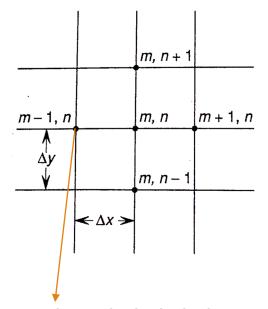
차분

$$\frac{\partial T}{\partial x} \approx \frac{T(x + \Delta x) - T(x)}{\Delta x}$$

$$\frac{\partial^2 T}{\partial x^2} \approx \frac{T(x + \Delta x) - 2T(x) + T(x - \Delta x)}{(\Delta x)^2}$$



열 구조물을 유한한 크기(Δx , Δy)의 grid로 세분한다.



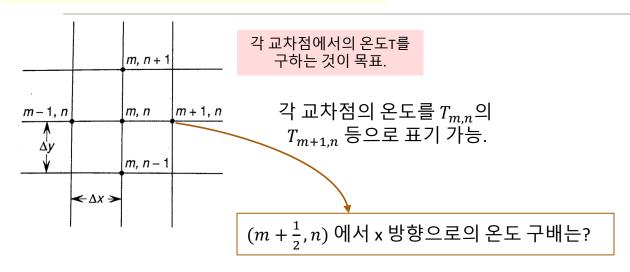
각 교차점에서의 온도T를 구하는 것이 목표.

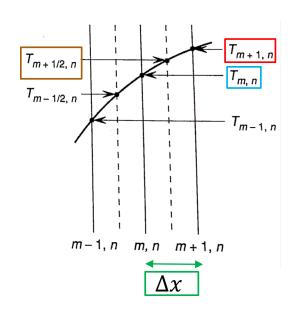
x축은 m Y축은 n을 사용하여 T(x,y)를 불연속적인 유한한 크기의 요소 (예를 들어 $T_{m-1,n}, T_{m,n}, T_{m+1,n}$ 로 표기된 온도 분포) 에서 찾아보는 방법.



$$\frac{\partial^2 T}{\partial x^2} \approx \frac{T(x + \Delta x) - 2T(x) + T(x - \Delta x)}{(\Delta x)^2}$$

도출해보자





$$\frac{\partial T}{\partial x}\Big|_{(m+\frac{1}{2},n)} \approx \frac{T_{m+1,n} - T_{m,n}}{\Delta x}$$

$$\frac{\partial T}{\partial x}\Big|_{(m-\frac{1}{2},n)} \approx \frac{T_{m,n} - T_{m-1,n}}{\Delta x}$$

$$\left. \frac{\partial^2 T}{\partial x^2} \right|_{(m,n)} \approx \frac{\frac{\partial T}{\partial x} \Big|_{(m+\frac{1}{2},n)} - \frac{\partial T}{\partial x} \Big|_{(m-\frac{1}{2},n)}}{\Delta x}$$

$$\frac{\partial^2 T}{\partial x^2}\Big|_{(m,n)} \approx \frac{\frac{T_{m+1,n} - T_{m,n}}{\Delta x} - \frac{T_{m,n} - T_{m-1,n}}{\Delta x}}{\Delta x}$$

$$\rightarrow \frac{T_{m+1,n} - T_{m,n} - (T_{m,n} - T_{m-1,n})}{(\Delta x)^2}$$

$$\left. \frac{\partial^2 T}{\partial x^2} \right|_{(m,n)} \approx \frac{T_{m+1,n} - 2T_{m,n} + T_{m-1,n}}{(\Delta x)^2}$$

$$\left. \frac{\partial^2 T}{\partial y^2} \right|_{(m,n)} \approx \frac{T_{m,n+1} - 2T_{m,n} + T_{m,n-1}}{(\Delta y)^2}$$



$$\frac{\partial^2 T}{\partial x^2} \approx \frac{T(x + \Delta x) - 2T(x) + T(x - \Delta x)}{(\Delta x)^2}$$

검증

$$\left. \frac{\partial^2 T}{\partial x^2} \right|_{(m,n)} \approx \frac{T_{m+1,n} - 2T_{m,n} + T_{m-1,n}}{(\Delta x)^2}$$

(x, y) 2차원 공간에서의 정상상태 열전도 방정식에 대입

$$\left. \frac{\partial^2 T}{\partial y^2} \right|_{(m,n)} \approx \frac{T_{m,n+1} - 2T_{m,n} + T_{m,n-1}}{(\Delta y)^2}$$

$$\left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2}\right) = 0$$

$$\left(\frac{T_{m+1,n} - 2T_{m,n} + T_{m-1,n}}{(\Delta x)^2} + \frac{T_{m,n+1} - 2T_{m,n} + T_{m,n-1}}{(\Delta y)^2}\right) = 0$$

$$\Delta x = \Delta y$$
 의 정사각형
요소를 사용한다면

$$T_{m+1,n} - 2T_{m,n} + T_{m-1,n} + T_{m,n+1} - 2T_{m,n} + T_{m,n-1} = 0$$

$$T_{m+1,n} - 4T_{m,n} + T_{m-1,n} + T_{m,n+1} + T_{m,n-1} = 0$$

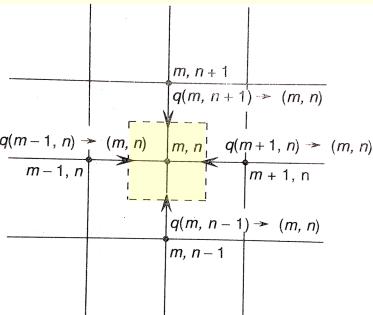
$$T_{m+1,n} + T_{m-1,n} + T_{m,n+1} + T_{m,n-1} = 4T_{m,n}$$

$$T_{m,n} = \frac{T_{m+1,n} + T_{m-1,n} + T_{m,n+1} + T_{m,n-1}}{T_{m,n} + T_{m,n} + T_{m,n} + T_{m,n} + T_{m,n}}$$



유한 차분법

$$T_{m,n} = \frac{T_{m+1,n} + T_{m-1,n} + T_{m,n+1} + T_{m,n-1}}{4}$$



(m.n)을 중심으로 하는 노란 요소 안으로 주위에서 유입되는 열량과 요소 내 발생하는 열량의 합이 zero :: Steady-state!

$$q_{(m-1,n)\to(m,n)} = -k \cdot A \cdot \frac{\partial T}{\partial x} \approx -k \cdot \Delta y \Delta z \cdot \frac{T_{(m,n)} - T_{(m-1,n)}}{\Delta x}$$

$$q_{(m,n)\to(m+1,n)} \approx -k \cdot \Delta y \Delta z \cdot \frac{T_{(m+1,n)} - T_{(m,n)}}{\Delta x}$$

$$q_{(m,n-1)\to(m,n)} \approx -k \cdot \Delta x \Delta z \cdot \frac{T_{(m,n)} - T_{(m,n-1)}}{\Delta y}$$

$$q_{(m,n)\to(m,n+1)} \approx -k \cdot \Delta x \Delta z \cdot \frac{T_{(m,n+1)} - T_{(m,n)}}{\Delta y}$$

요소 내 발생하는 열량의 합: $\dot{q}\Delta x \Delta y \Delta z$

$$-k \cdot \Delta y \Delta z \cdot \frac{T_{(m,n)} - T_{(m-1,n)}}{\Delta x} - k \cdot \Delta x \Delta z \cdot \frac{T_{(m,n)} - T_{(m,n-1)}}{\Delta y}$$

$$-\left[-k \cdot \Delta y \Delta z \cdot \frac{T_{(m+1,n)} - T_{(m,n)}}{\Delta x} - k \cdot \Delta x \Delta z \cdot \frac{T_{(m,n+1)} - T_{(m,n)}}{\Delta y}\right]$$

$$+\dot{q}\Delta x \Delta y \Delta z = 0$$

$$T_{(m-1,n)} + T_{(m,n-1)} + T_{(m,n-1)}$$

$$+ \frac{\dot{q}\Delta x \Delta y}{k} - 4T_{(m,n)} = 0$$

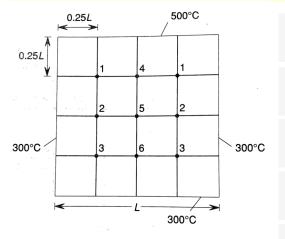
With
$$\Delta x = \Delta y$$

$$T_{(m-1,n)} + T_{(m,n-1)} + T_{(m+1,n)} + T_{(m,n+1)} + \frac{\dot{q}\Delta x \Delta y}{k} - 4T_{(m,n)} = 0$$



예제 6.10

□변의 길이가 L인 정사각형 판에서 장상상태하의 온도 분포를 계산하여라.



at Pt.1
$300 + 500 + T_2 + T_4 = 4T_1$

$$at Pt. 2$$

$$300 + T_1 + T_3 + T_5 = 4T_2$$

$$at Pt. 3$$

$$300 + 500 + T_2 + T_6 = 4T_3$$

$$at Pt. 4$$

$$500 + T_1 + T_1 + T_5 = 4T_4$$

$$at Pt.5 T_2 + T_2 + T_4 + T_6 = 4T_5$$

$$at Pt. 6$$

$$300 + T_3 + T_3 + T_5 = 4T_6$$

$$at Pt. 1 -4T_1 + T_2 + T_4 = -800$$

$$at Pt. 2 T_1 - 4T_2 + T_3 + T_5 = -300$$

$$at Pt. 3 T_2 - 4T_3 + T_6 = -800$$

$$at Pt. 4 2T_1 - 4T_4 - T_5 = -500$$

$$at Pt.5 2T_2 + T_4 - 4T_5 + T_6 = 0$$

$$at Pt. 6 2T_3 + T_5 - 4T_6 = -300$$

$$aT_1 + bT_2 + cT_3 + dT_4 + eT_5 + fT_6 = g$$

형태로 통합하면...

$$\begin{bmatrix} -4 & 1 & 0 & 1 & 0 & 0 \\ 1 & -4 & 1 & 0 & 1 & 0 \\ 0 & 1 & -4 & 0 & 0 & 1 \\ 2 & 0 & 0 & -4 & -1 & 0 \\ 0 & 2 & 0 & 1 & -4 & 1 \\ 0 & 0 & 2 & 0 & 1 & -4 \end{bmatrix} = \begin{bmatrix} -800 \\ -300 \\ -800 \\ -500 \\ 0 \\ -300 \end{bmatrix}$$

$$\begin{bmatrix} -4 & 1 & 0 & 1 & 0 & 0 \\ 1 & -4 & 1 & 0 & 1 & 0 \\ 0 & 1 & -4 & 0 & 0 & 1 \\ 2 & 0 & 0 & -4 & -1 & 0 \\ 0 & 2 & 0 & 1 & -4 & 1 \\ 0 & 0 & 2 & 0 & 1 & -4 \end{bmatrix} \begin{bmatrix} T_1 \\ T_2 \\ T_3 \\ T_4 \\ T_5 \\ T_6 \end{bmatrix} = \begin{bmatrix} -800 \\ -300 \\ -800 \\ -500 \\ 0 \\ -300 \end{bmatrix}$$