(a) Demonstrate that for an ideal gas:  $C_p - C_v = R$ .

[2 marks]

- (b) For an ideal gas undergoing a process, what does the area under a Cv vs. T graph represent? [2 marks]
- (c) For an ideal gas undergoing a process, what does the area under a Cp vs. T graph [2 marks]

ia, for ideal gas

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ou = stevdT = h = stepdT

sh = ou + s(pv) = ou+RoT = ou+ SROT  $= \int_{-\infty}^{T_2} (c_0 + R) dT = \int_{-\infty}^{T_2} C_p dT$ 

Cp = Co+R

cbs cv

Change in sperific internal energy

Cpd T = oh
Ti Change is specific
enthalpy.

## Problem 2 Solution

Ammonia, NH<sub>3</sub>, is contained in a sealed rigid tank at  $0^{\circ}$ C, x = 50% and is then heated to  $100^{\circ}$ C. Find the final state P<sub>2</sub>, u<sub>2</sub> and the specific work and heat transfer.

Solution:

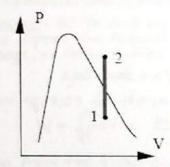
Continuity Eq.:  $m_2 = m_1$ ;

Energy Eq.5.11:  $E_2 - E_1 = {}_{1}Q_2$ ;  $({}_{1}W_2 = \emptyset)$ 

Process:  $V_2 = V_1 \implies v_2 = v_1 = 0.001566 + 0.5 \times 0.28763 = 0.14538 \text{ m}^3/\text{kg}$ 

Table B.2.2:  $v_2 \& T_2 \Rightarrow \text{between } 1000 \text{ kPa} \text{ and } 1200 \text{ kPa}$ 

$$P_2 = 1000 + 200 \frac{0.14538 - 0.17389}{0.14347 - 0.17389} = 1187 \text{ kPa}$$



$$u_2 = 1490.5 + (1485.8 - 1490.5) \times 0.935$$
  
= 1485.83 kJ/kg  
 $u_1 = 179.69 + 0.5 \times 1138.3 = 748.84$  kJ/kg

Process equation gives no displacement:  $_1w_2 = 0$ ;

The energy equation then gives the heat transfer as

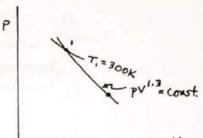
$$_{1}q_{2} = u_{2} - u_{1} = 1485.83 - 748.84 = 737 \text{ kJ/kg}$$

KNOWN: A gas mixture expands with a known pressure-volume relation. The initial state is fixed and the heat transfer for the process is known.

FIND: Determine (a) the final temperature, (b) the final pressure, (c) the final volume, and (d) the work.

SCHEMATIC & GIVEN DATA: M=33 kg/kmol P = 3 bar T, = 300K pV1.3 const. V, = 0.1 m3

For the mixture: Cy = 0.6 to 100 (F) (Times, Gr in kJ/kg·K)



ASSUMPTIONS: (1) The gas mixture is the closed system. (2) The gas mixture behaves as an ideal gas. (3) The process is polytropic with n=1.3. (4) Kinetic and potential energy effects are neglected.

ANALYSIS: (a) To find the final temperature, start with the energy balance and express the internal energy change and work in terms of temperature change, as follows. First

From Eq. 3.57 for the polytropic process
$$W = \int_{V}^{V} p dV = \frac{mR(T_2 - T_1)}{1 - n}$$
(\*)

Also, from the given co relation

$$\Delta U = m \int_{T_i}^{T_2} C_{\sigma}(T) dT = m \left[ (0.6)(T_2 - T_i) \right]$$
 (\*\*)

Incorporating (\*) and (\*\*) ruto the energy balance

The mass is found using the ideal gas equation at state 1

$$m = \frac{P_1 V_1}{RT_1} = \frac{(3 \text{ bar})(0.1 \text{ m}^3)}{\left(\frac{8.314}{33}\right) \frac{\text{kJ}}{\text{kg} \cdot \text{K}} (300 \text{K})} \left| \frac{10^3 \text{ N/m}^2}{1 \text{ bar}} \right| \frac{1 \text{kJ}}{10^3 \text{ N·m}} = 0.397 \text{ kg}$$

with m = 0.397 kg, T, = 300K, Q = 3.84 kJ, and R = 8.314/33 kJ/kg.K to solve for Tz:



- (b) To find p2, use Eq. 3.56 for the polytropic process Lyuse Eq. 3.56 for the polytropic process  $\frac{T_2}{T_1} = \left(\frac{P_3}{P_1}\right)^{n-1/n} \Rightarrow p_2 = \left(\frac{T_2}{T_1}\right)^{n-1} P_1 = \left(\frac{259.5}{300 \text{ K}}\right)^{\frac{1.3}{3}} \text{ (3 bar)}$
- (c) Again using Eq. 3.56 sing Eq. 3.56  $\left(\frac{P_{z}}{P_{l}}\right)^{(m-1)} = \left(\frac{V_{l}}{V_{z}}\right)^{n-1} \Rightarrow V_{z} = \left(\frac{P_{l}}{P_{z}}\right)^{\frac{1}{n}} V_{l} = \left(\frac{3bcn}{bar}\right)^{\frac{1}{1.3}} (0.1 \text{ m}^{3})$   $= \frac{3bcn}{bar} (0.1 \text{ m}^{3})$
- (d) Now, using (\*) to evaluate the work

$$W = \frac{mR(T_2 - T_1)}{(1 - n)}$$
=  $\frac{(0.397 \text{ kg})(\frac{8.314}{33}) \frac{\text{kJ}}{\text{kg} \cdot \text{K}}}{(1 - 1.3)}$ 
=  $\frac{13.5}{\text{kJ}}$