

**CHE 524 Process Control Laboratory**  
**Group 1 – Prelab for Multivariate Process Control**  
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This lab we performed close loop system identification using Matlab and transfer function. Assuming that the system fit a first order a first order response.

$$G_p = \frac{K_p}{\tau_p s + 1}$$

And we use a PI controller,

$$G_c = K_c + \frac{K_c}{\tau_I s}$$

We develop a transfer function and used lsqcurvefit to find the process parameter  $\tau_p$  and  $K_p$ .

### **Close loop System Identification**

Since this experiment is conducted in close loop condition,  
We need a new model to describe system behavior.

$$\frac{T'(s)}{T_{sp}(s)} = \frac{G_c G_p}{1 + G_c G_p} = \frac{\left(K_c + \frac{K_c}{\tau_I s}\right) \left(\frac{K_p}{\tau_p s + 1}\right)}{1 + \left(K_c + \frac{K_c}{\tau_I s}\right) \left(\frac{K_p}{\tau_p s + 1}\right)} \times \frac{\tau_p s + 1}{\tau_p s + 1}$$

$$= \frac{\left(K_c + \frac{K_c}{\tau_I s}\right) K_p}{\tau_p s + 1 + \left(K_c + \frac{K_c}{\tau_I s}\right) K_p} = \frac{K_c K_p + \frac{K_c K_p}{\tau_p s}}{\tau_p s + 1 + K_c K_p + \frac{K_c K_p}{\tau_I s}} \times \frac{s}{s}$$

$$\frac{T'(s)}{T_{sp}(s)} = \frac{K_c K_p s + \frac{K_c K_p}{\tau_I}}{\tau_p s^2 + \left(K_c K_p + 1\right) s + \frac{K_c K_p}{\tau_I}}$$

$$T'(s) = \frac{K_c K_p s + \frac{K_c K_p}{\tau_I}}{\tau_p s^2 + \left(K_c K_p + 1\right) s + \frac{K_c K_p}{\tau_I}} \times T_{sp}(s) = \frac{K_c K_p s + \frac{K_c K_p}{\tau_I}}{\tau_p s^2 + \left(K_c K_p + 1\right) s + \frac{K_c K_p}{\tau_I}} \times \frac{M}{s}$$

$T'(s)$  has the form of

$$F(s) = \frac{M(as + b)}{s(cs^2 + ds + e)}$$

Using Matlab symbolic math tool box,

```
EDU>> syms a b c d e M s t
EDU>> F=(M*(a*s+b))/(c*s^3+d*s^2+e*s)

F =

(M*(b + a*s))/(c*s^3 + d*s^2 + e*s)

EDU>> ilaplace(F,t)

ans =

(M*b)/e - (M*b*exp(-(d*t)/(2*c)))*(cosh((t*(d^2/4 - c*e)^(1/2))/c) - (c*sinh((t*(d^2/4 - c*e)^(1/2))/c)*(d/(2*c) +
(M*a*e - M*b*d)/(M*b*c)))/(d^2/4 - c*e)^(1/2)))/e
```

Adding appropriate symbol for element and element multiplication, we obtained formula X, a time domain model that describes PI and first order (PIAFO) behaviour.

$$X = (M.*b)/e - (M.*b.*exp(-(d.*t)./(2.*c)).*(cosh((t.(d.^2/4 - c.*e).^(1/2))/c) - (c.*sinh((t.(d.^2/4 - c.*e).^(1/2))./c).* (d./ (2.*c) + (M.*a.*e - M.*b.*d)/(M.*b.*c)))/(d.^2/4 - c.*e)^(1/2)))./e$$

Comparing  $F(s)$  and PIAFO model we obtained,

$$\begin{aligned} a &= K_c K_p \\ b &= \frac{K_c K_p}{\tau_I} \\ c &= \tau_p \\ d &= K_c K_p + 1 \\ e &= \frac{K_c K_p}{\tau_I} \end{aligned}$$

### Developing a Matlab function for PIAFO model

A PIAFO Model requires the knowledge of time (s), step change (M), control gain ( $K_c$ ), control integrative action ( $\tau_I$ ), process gain ( $K_p$ ), process time constant ( $\tau_p$ )

```

1   function X=PIAFO(x,M,kc,tauI,t)
2
3 -    kp=x(1)
4 -    taup=x(2)
5
6 -    a =kc.*kp
7 -    b =kc.*kp./tauI
8 -    c=taup
9 -    d=kc*kp+1
10 -   e=b
11 -   X=(M.*b)/e - (M.*b.*exp(-(d.*t)./(2.*c)).*(cosh((t.*d.^2/4 - c.*e).^(1/2))/c) - (c.*sinh((t.*
12 -   end

```

We have the knowledge of all except process gain and process time delay. In order to use optimization algorithm to solve for them, we put Kp and taup in a column vector x where x is

$$x = \frac{K_p}{\tau_p}$$

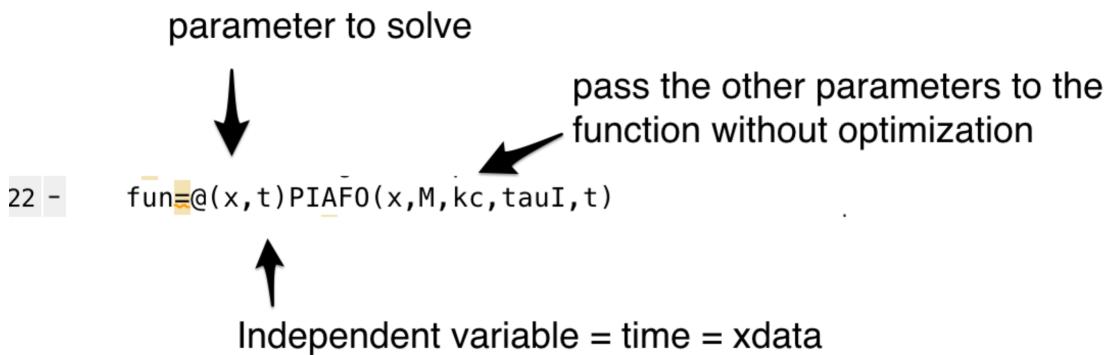
We want to use lsqcurvefit to solve for Kp and taup. See appendix for the full Matlab script. The script is explained below.

The function takes the following form:

### Syntax

```
x = lsqcurvefit(fun,x0,xdata,ydata)
```

where fun is the model we want to fit using function handle. X0 is the initial guess for vector x, xdata is the independent variables and ydata is the dependent variable. Since our PIAFO model have many parameters but we are only solving for 2 of them, we use function handle to tell Matlab which parameters we want to solve.

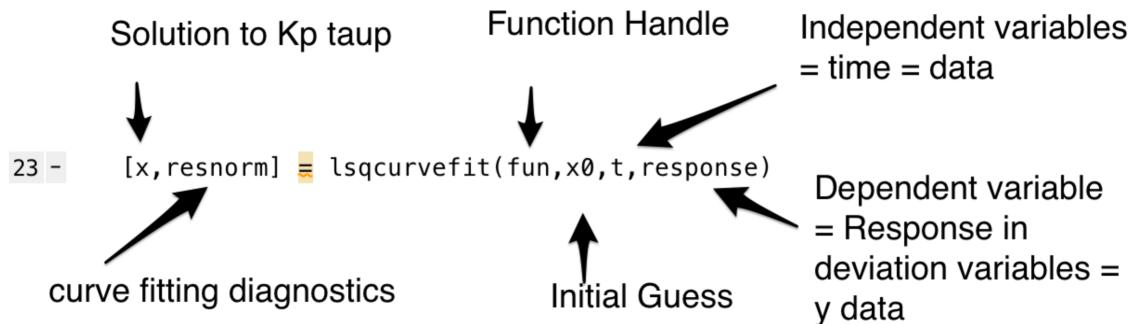


Then we called the lsqcurvefit function using our function handle (fun), initial guess where

$$x_0 = \frac{0.3}{5}$$

Which is determined by trial and error.

```
23 - [x, resnorm] = lsqcurvefit(fun, x0, t, response)
```



We determined that the software take sample every 6 seconds. Instead of importing time vector every time, we create a column time vector that starts from 0 with increment of 6 until it match the length of the response data.

```
21 - t=(0:6:6*(length(response)-1))'
```

The response vector, step change, and  $K_c$  and  $\tau_p$ , title of the plot are defined in the beginning of the code

```
9 %input file
10 - response=PS40T50
11 %title of the plot
12 - name='fitted plot for pressure setpoint change 40 to 50'
13 %what is the step change and control parameters
14 - M=10
15 - kc=1
16 - tauI=0.5
17 %initial guess
18 - x0=[0.3;5]
```

## Result of Close Loop System Identification

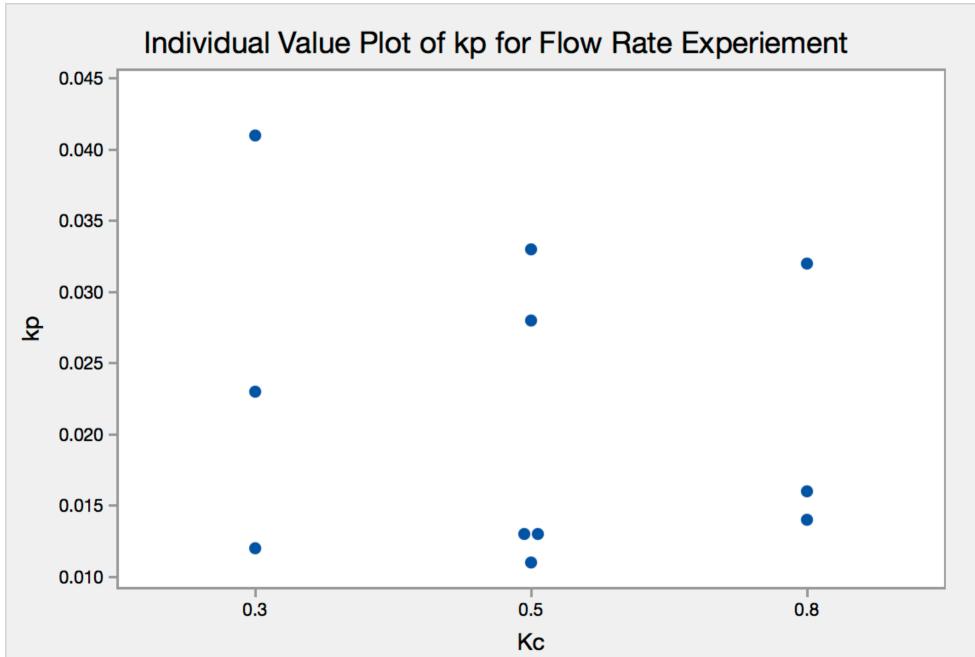
### Flow rate Experiment

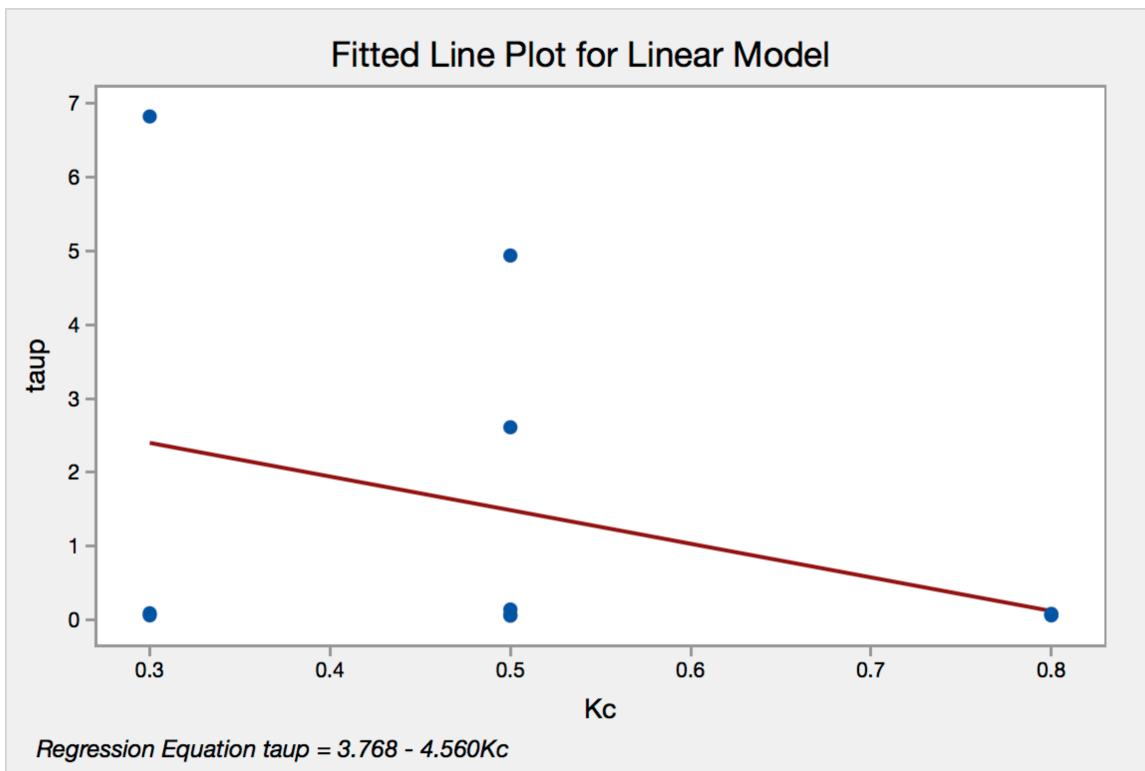
	Vector Name	$K_p$	$\tau_p$
$K_c = 0.5$	FL20T30	0.011	2.611
	FL30T40	0.028	0.064
	FL40T50	0.013	4.94
	FL50T60		
	FL60T40	0.033	0.056
	FL40T20	0.013	0.14

<b>Kc=0.3</b>	FL20T30	0.012	6.826
	FL30T40	0.023	0.089
	FL40T50	0.041	0.06
<b>kc=0.8</b>	FL20T30	0.014	0.081
	FL30T40	0.032	0.06
	FL40T50	0.016	0.068
<b>Average</b>		0.021	1.363
<b>Standard Deviation</b>		0.010	2.396
<b>Upper bound</b>		0.0276	2.7793
<b>Lower bound</b>		0.015	0.000

#### Statistics

Variable	Kc	Total											
		Count	N	N*	Mean	SE Mean	StDev	Minimum	Q1	Median	Q3	Maximum	
kp	0.3	3	3	0	0.025333	0.008452	0.014640	0.012000	0.012000	0.023000	0.041000	0.041000	
	0.5	5	5	0	0.019600	0.004534	0.010139	0.011000	0.012000	0.013000	0.030500	0.033000	
	0.8	3	3	0	0.020667	0.005696	0.009866	0.014000	0.014000	0.016000	0.032000	0.032000	





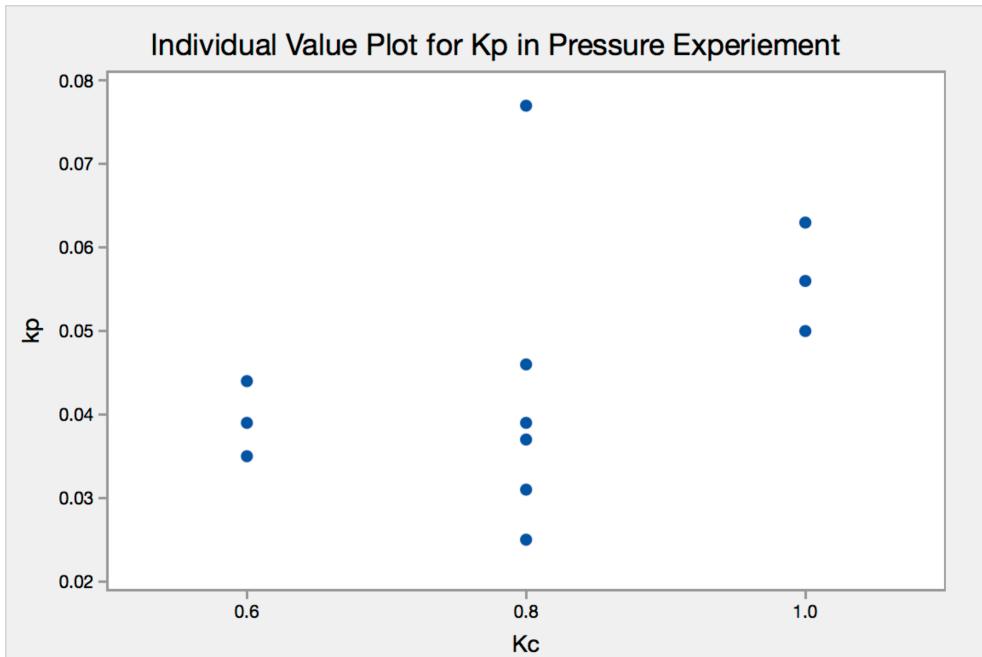
We determined that process gain ( $K_p$ ) is between 0.015 - 0.0276 and process time constants is between 0~2.77. The average is 0.021 and 1.363, respectively. Experiment conducted in low  $K_c$  has higher variance than when  $K_c$  is high. However, the variation at the 3 conditions is negligible.

## Pressure Experiment

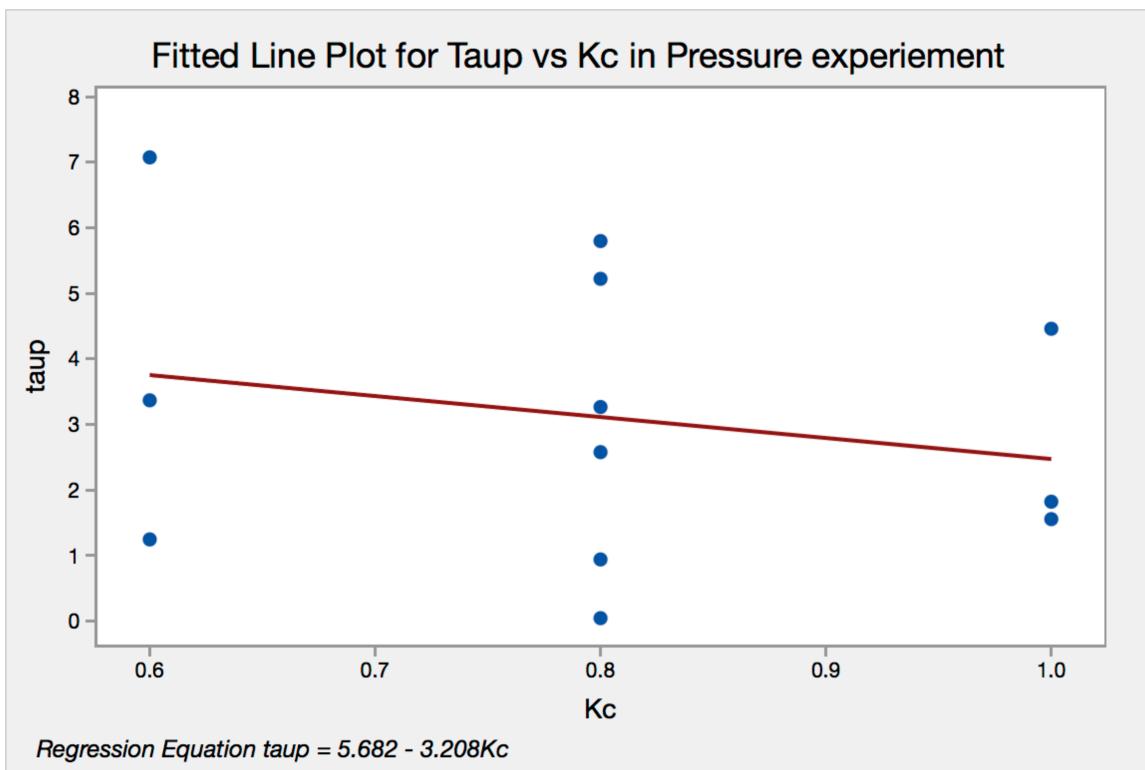
<b>tauc=0.5</b>	<b>Vector Name</b>	<b>kp</b>	<b>taup</b>
<b>kc=0.8</b>	PS20T30	0.025	0.047
	PS30T40	0.037	5.797
	PS40T50	0.039	0.943
	PS50T60	0.046	3.267
	PS60T40	0.077	2.579
	PS40T20	0.031	5.222
<b>kc=0.6</b>	PS20T30	0.044	1.248
	PS30T40	0.039	7.073
	PS40T50	0.035	3.369
<b>kc=1.0</b>	PS20T30	0.063	4.46
	PS30T40	0.05	1.823
	PS40T50	0.056	1.557
<b>Avg</b>		0.045	3.115
<b>STDEV</b>		0.015	2.157
<b>Upper bound</b>		0.053	4.336
<b>Lower bound</b>		0.037	1.895

### Statistics

Variable	Kc	Total											
		Count	N	N*	Mean	SE Mean	StDev	Minimum	Q1	Median	Q3	Maximum	
kp	0.6	3	3	0	0.039333	0.002603	0.004509	0.035000	0.035000	0.039000	0.044000	0.044000	
	0.8	6	6	0	0.042500	0.007491	0.018349	0.025000	0.029500	0.038000	0.053750	0.077000	
	1.0	3	3	0	0.056333	0.003756	0.006506	0.050000	0.050000	0.056000	0.063000	0.063000	



We determined that the process gain for the pressure experiment is between  $0.037 \sim 0.053$ , the process time constant is  $1.895 \sim 4.336$ . We found that experiment runs at  $K_c=0.8$  have the highest variance and the experiment runs at  $K_c=1$  have the highest average process gain. Estimation of process time constant decreased as  $K_c$  increase.



## Conclusion for Close loop System Identification

For flow rate experiment, we determined that process gain ( $K_p$ ) is between 0.015 - 0.0276 and process time constants is between 0~2.77. The average is 0.021 and 1.363, respectively.

For pressure MIMO experiment, we determined that the process gain for the pressure experiment is between 0.037~0.053, the process time constant is 1.895~4.336. The average is 0.045 and 3.115, respectively.

We found that for both experiments,  $K_p$  are not affected by  $K_c$ , but  $\tau_p$  decreases with increasing  $K_c$  for both experiment.

### Effect of Chaining $K_c$ Flowrate Experiment

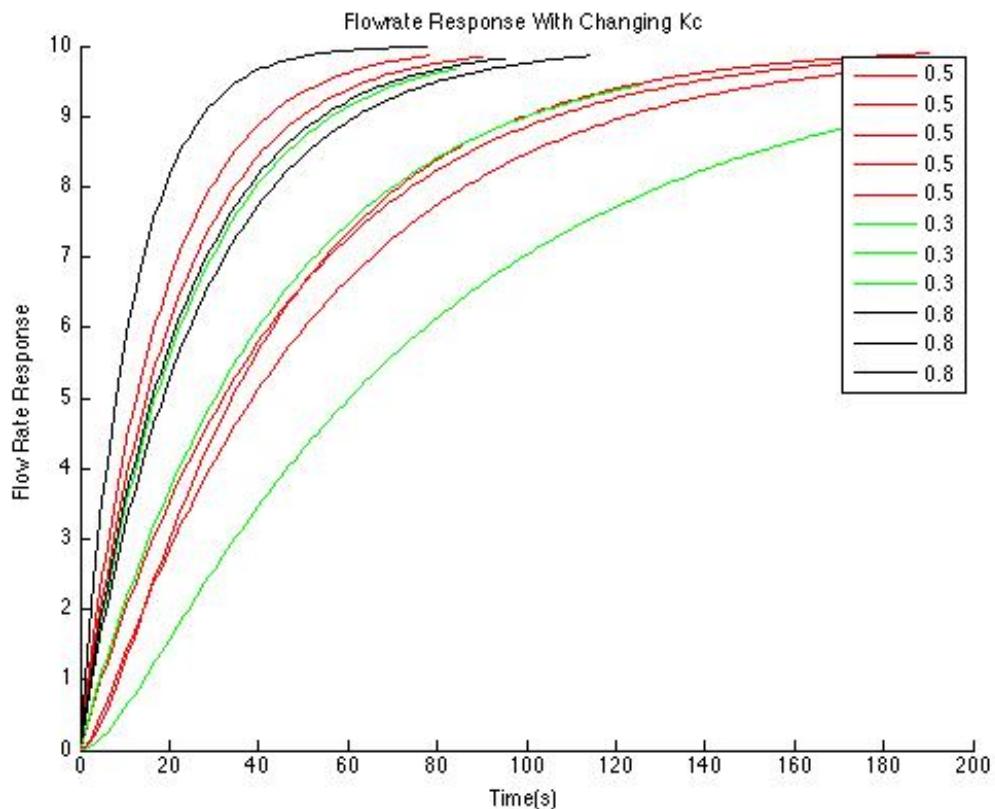
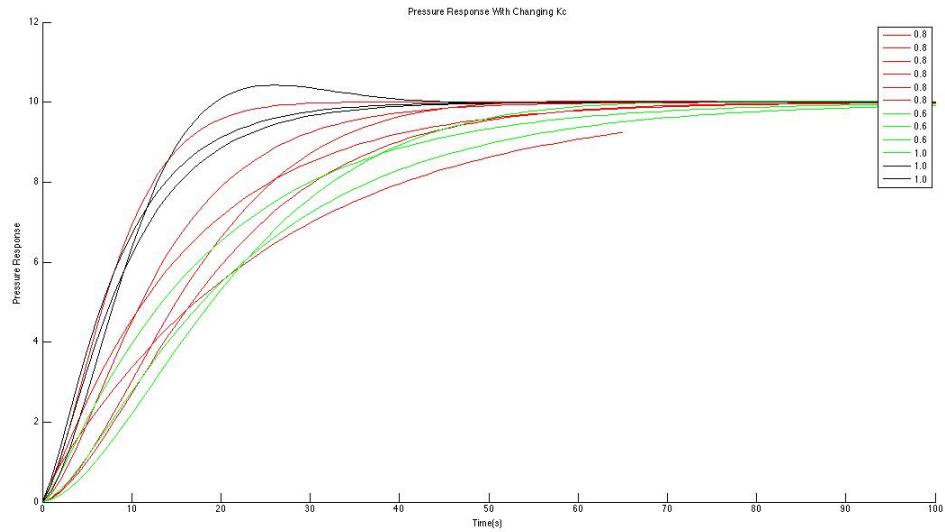


Figure compares all flow rate response with varying  $K_c$ . Though the data overlap with each other, it is clear that with increasing  $K_c$ , flow rate response are faster, and with lower variance between each runs.

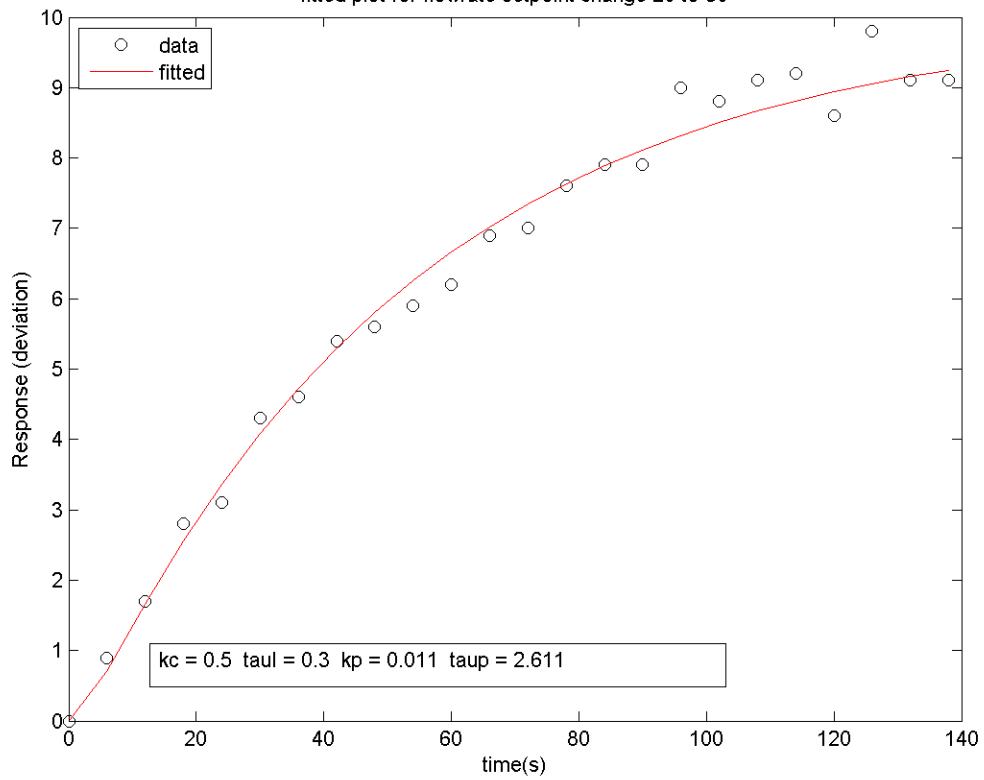
## Pressure Experiment

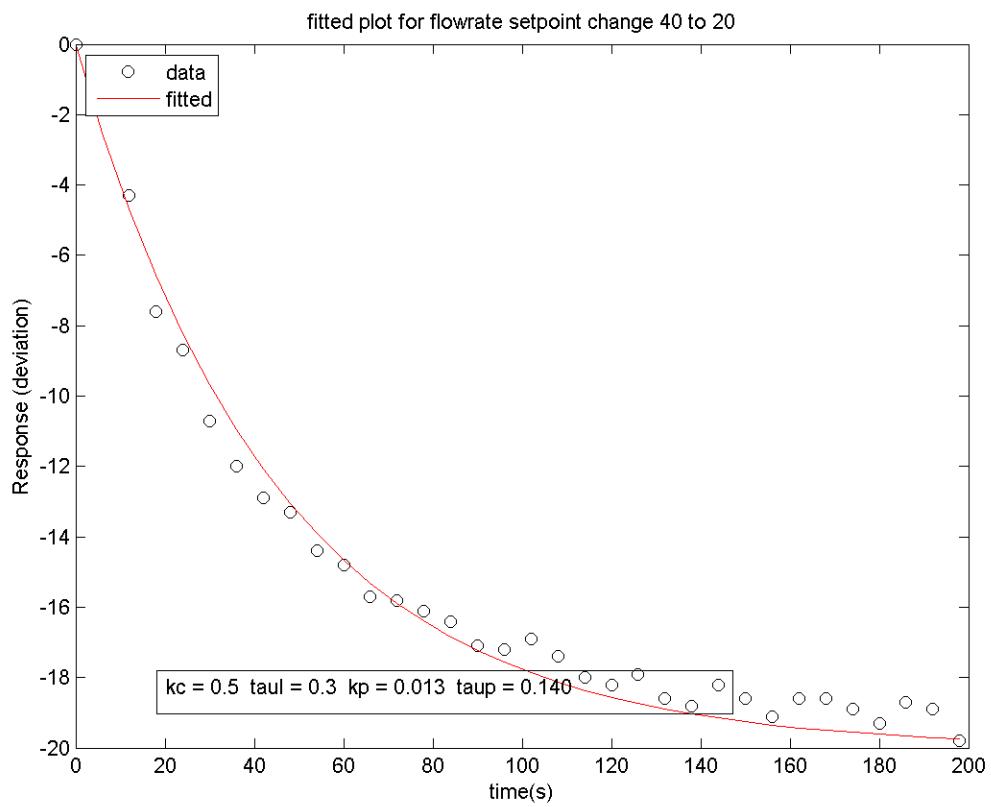


## Appendix A

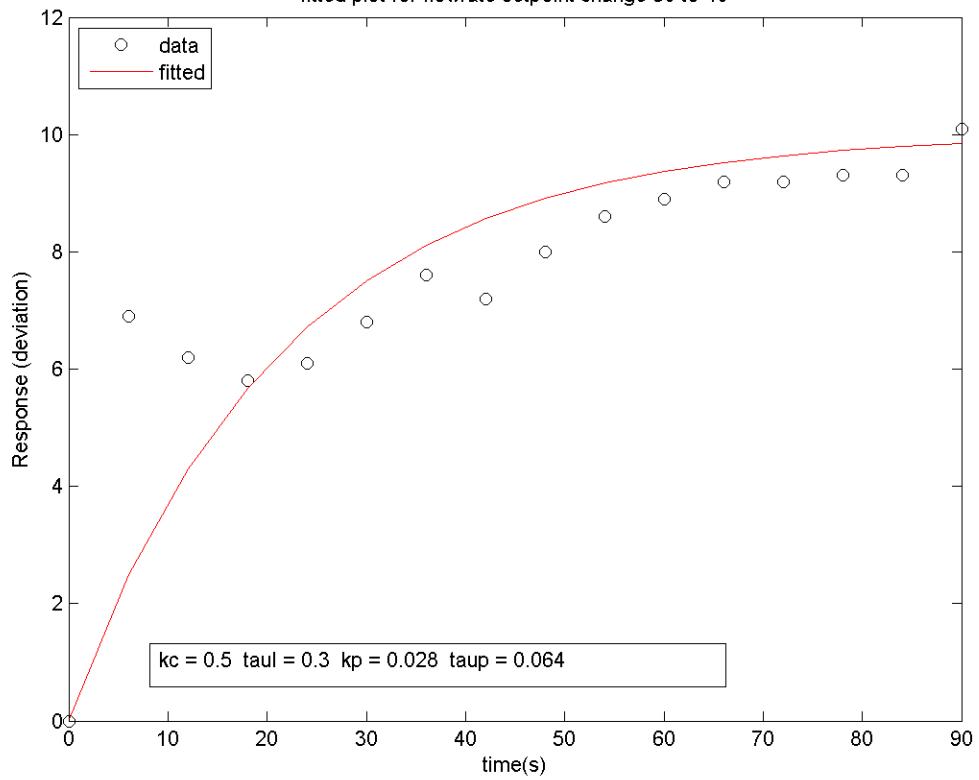
## Flow rate experiment

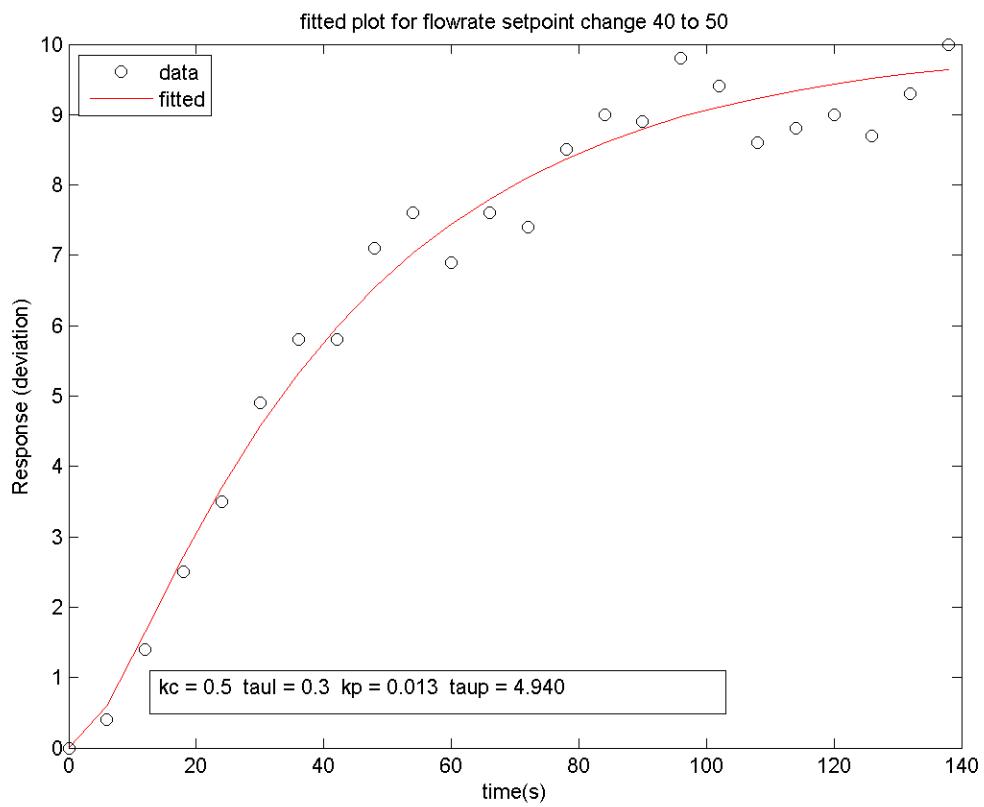
fitted plot for flowrate setpoint change 20 to 30



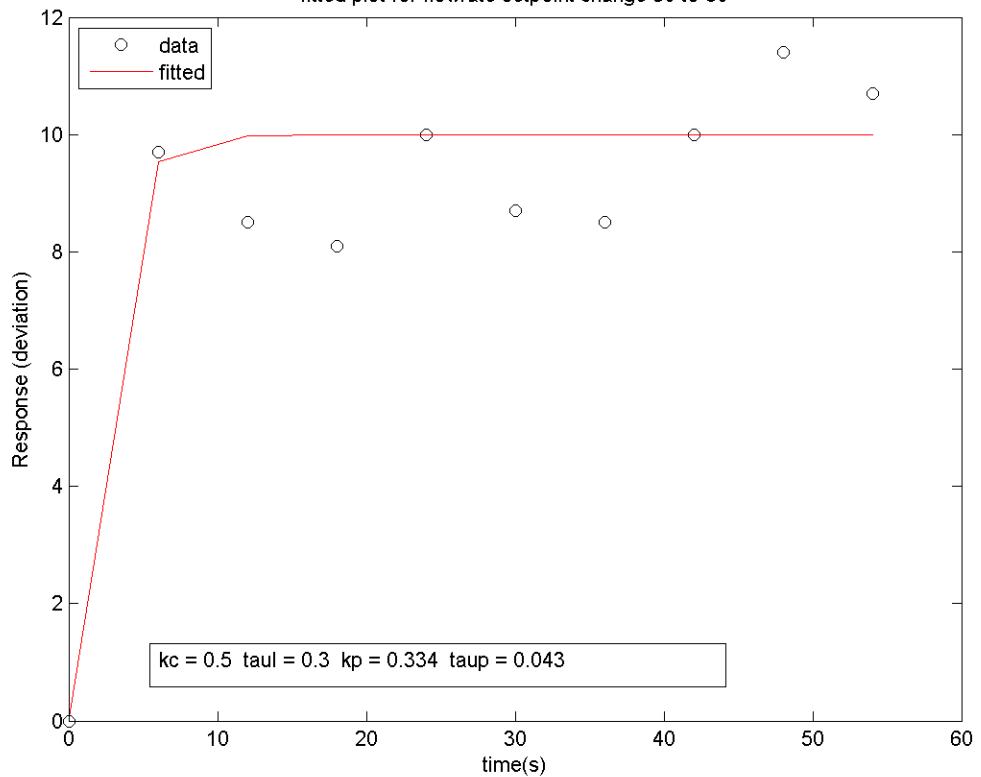


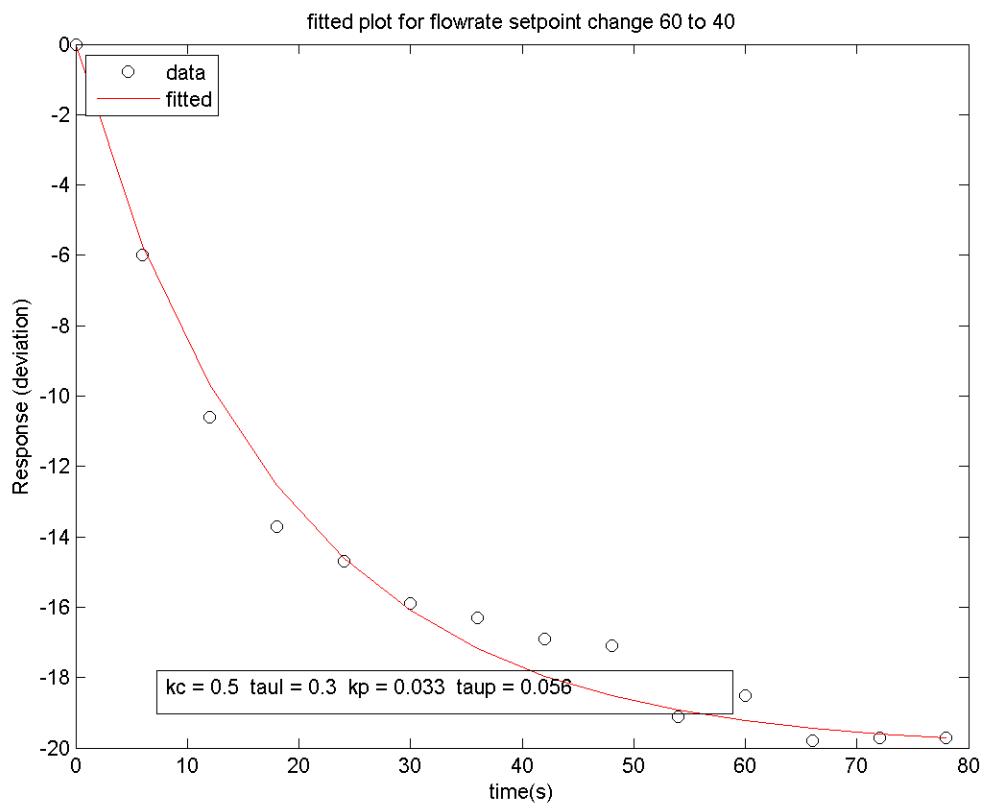
fitted plot for flowrate setpoint change 30 to 40



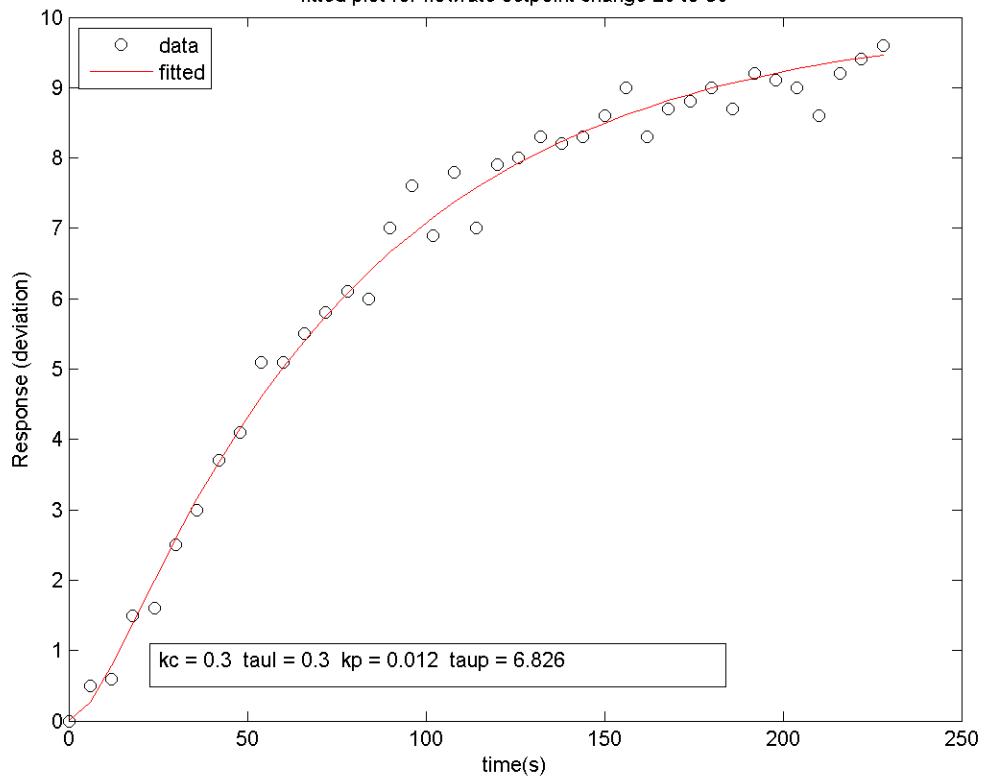


fitted plot for flowrate setpoint change 50 to 60

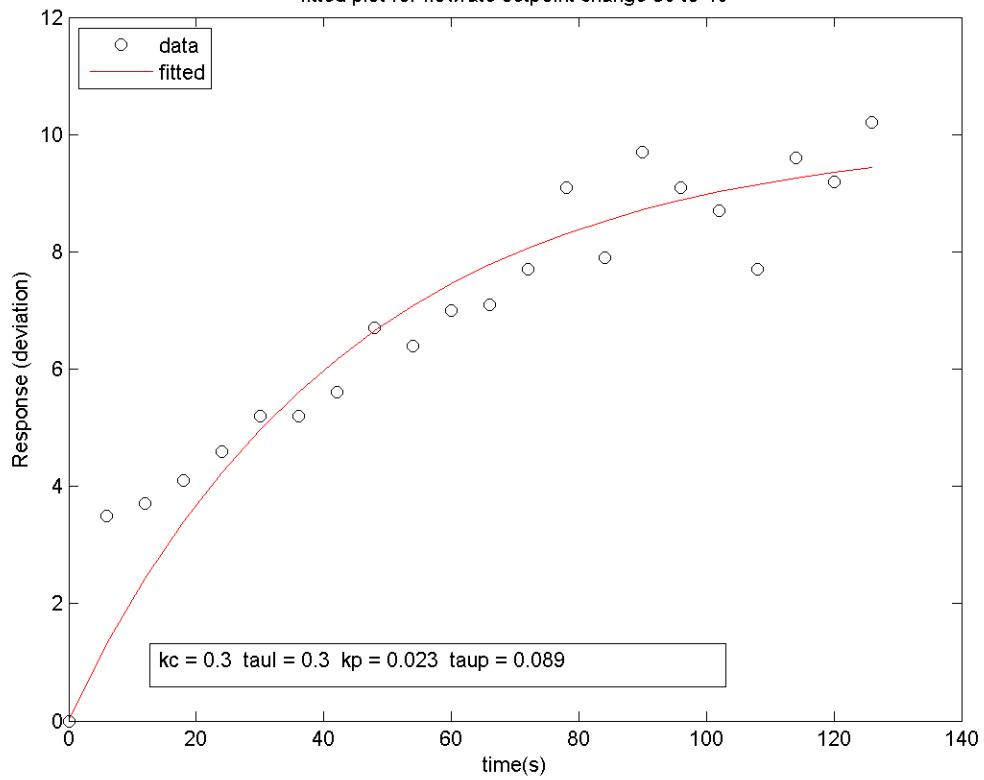




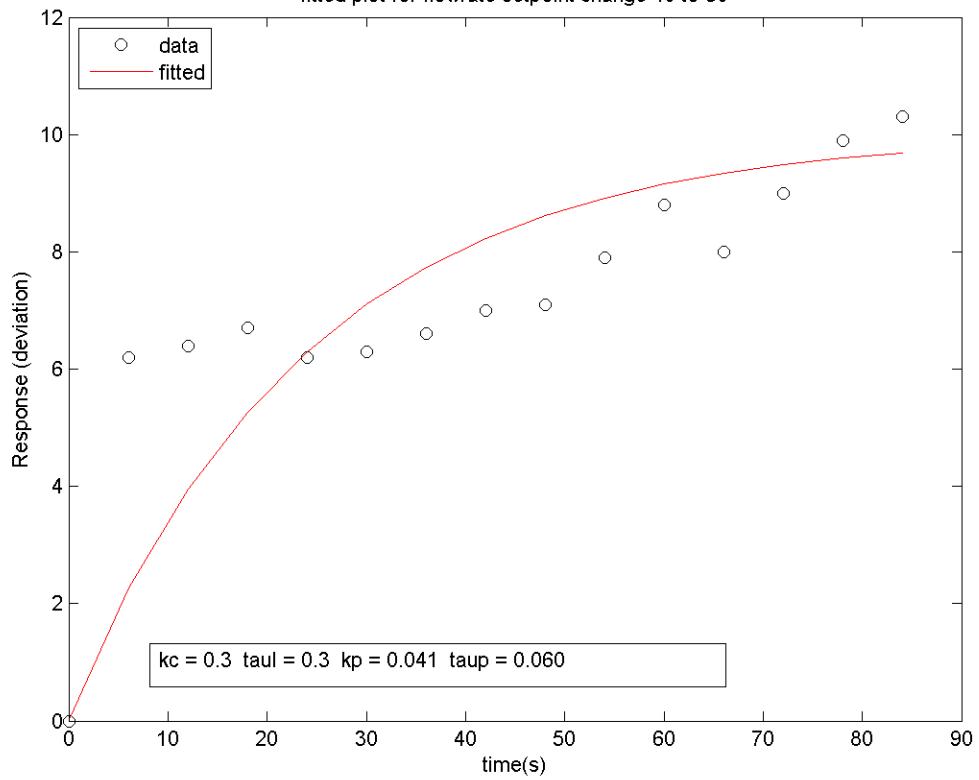
fitted plot for flowrate setpoint change 20 to 30



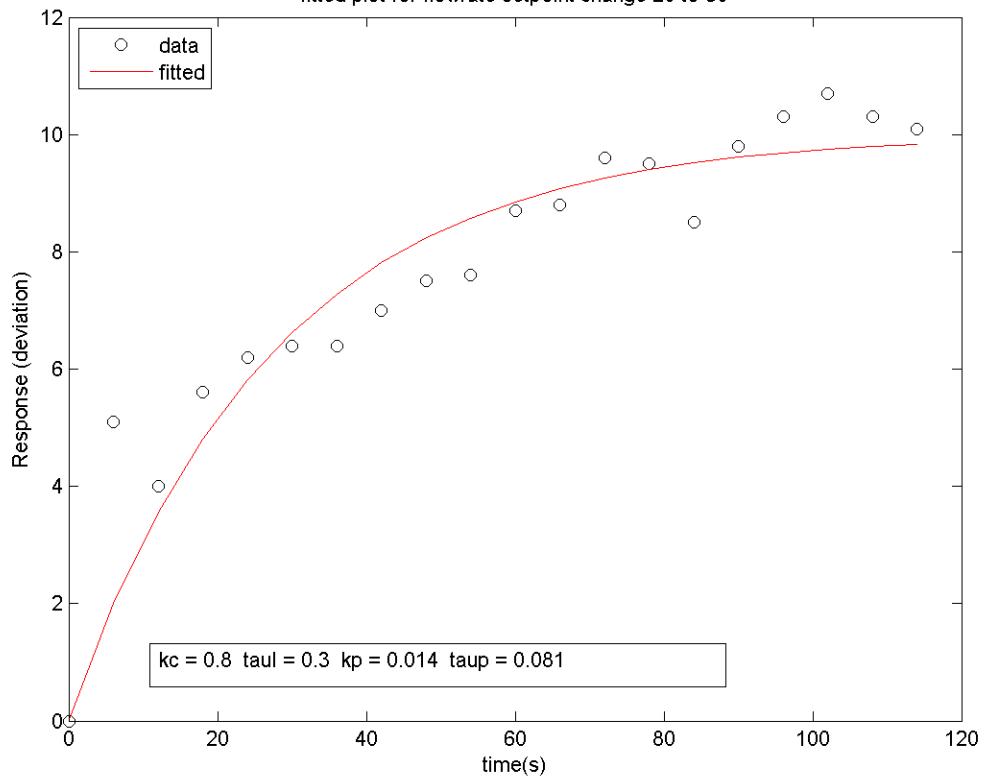
fitted plot for flowrate setpoint change 30 to 40



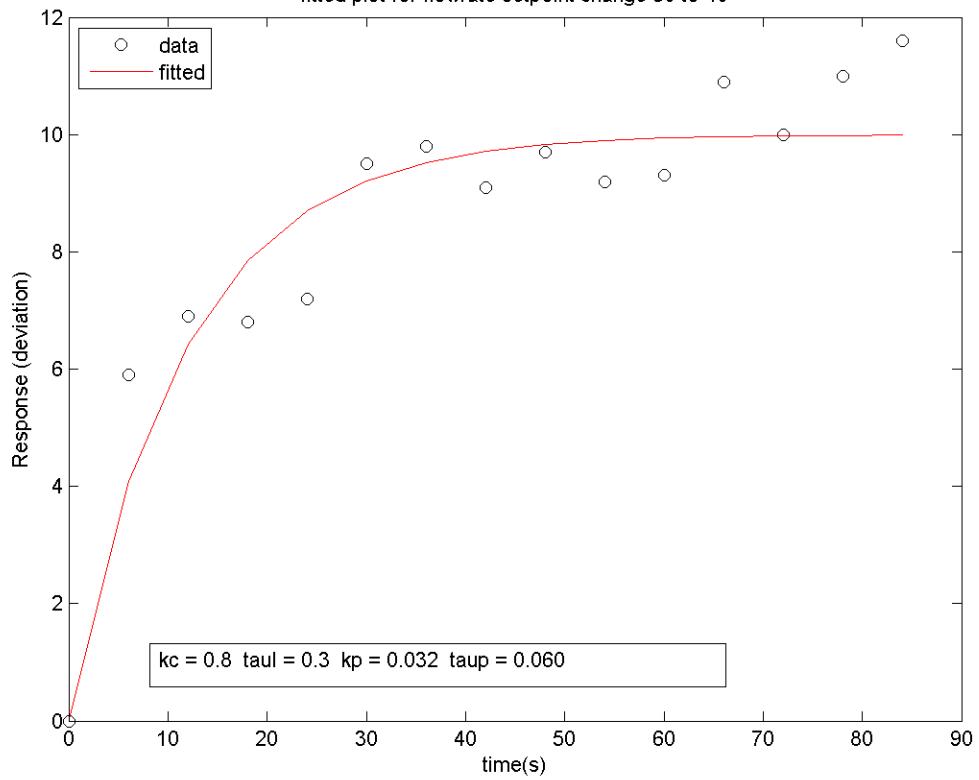
fitted plot for flowrate setpoint change 40 to 50



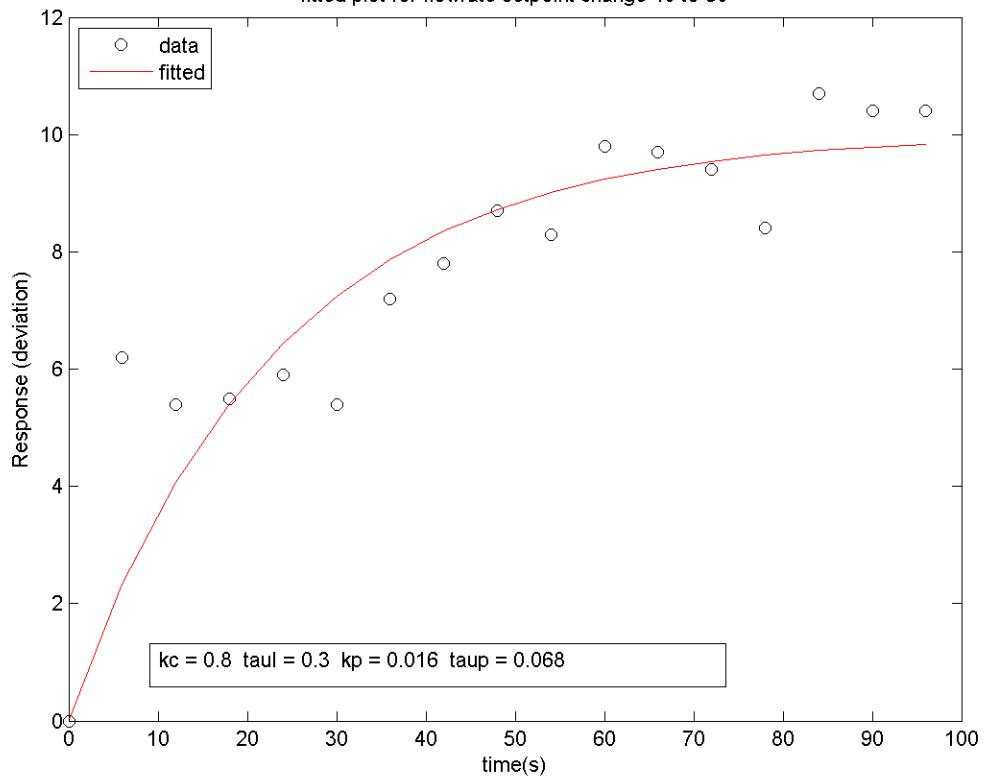
fitted plot for flowrate setpoint change 20 to 30



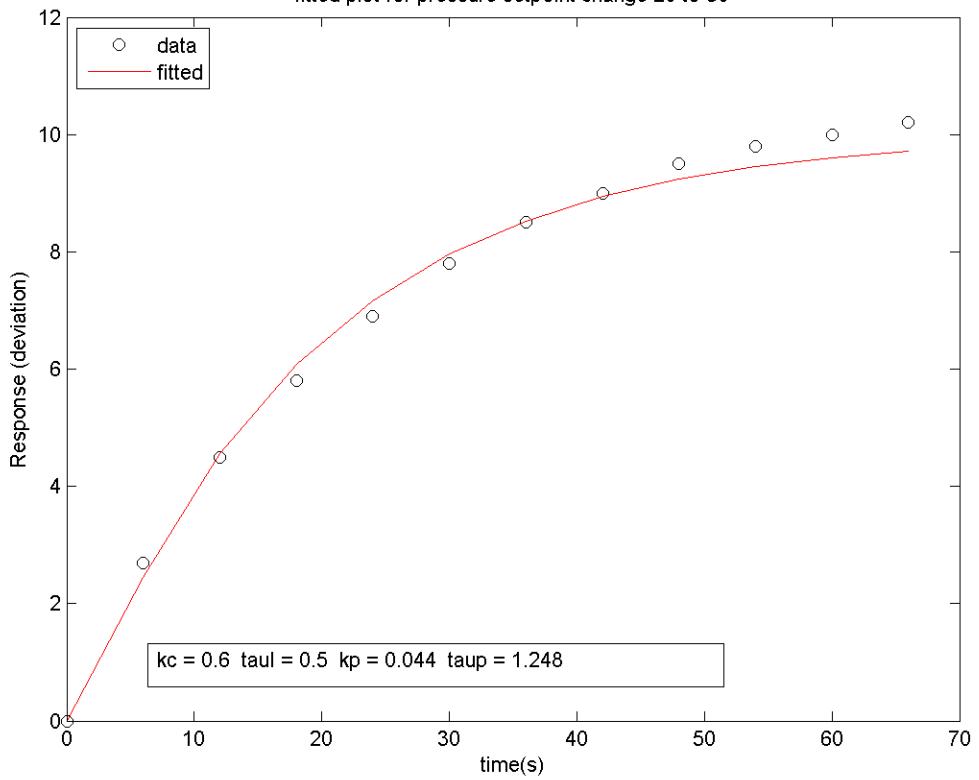
fitted plot for flowrate setpoint change 30 to 40



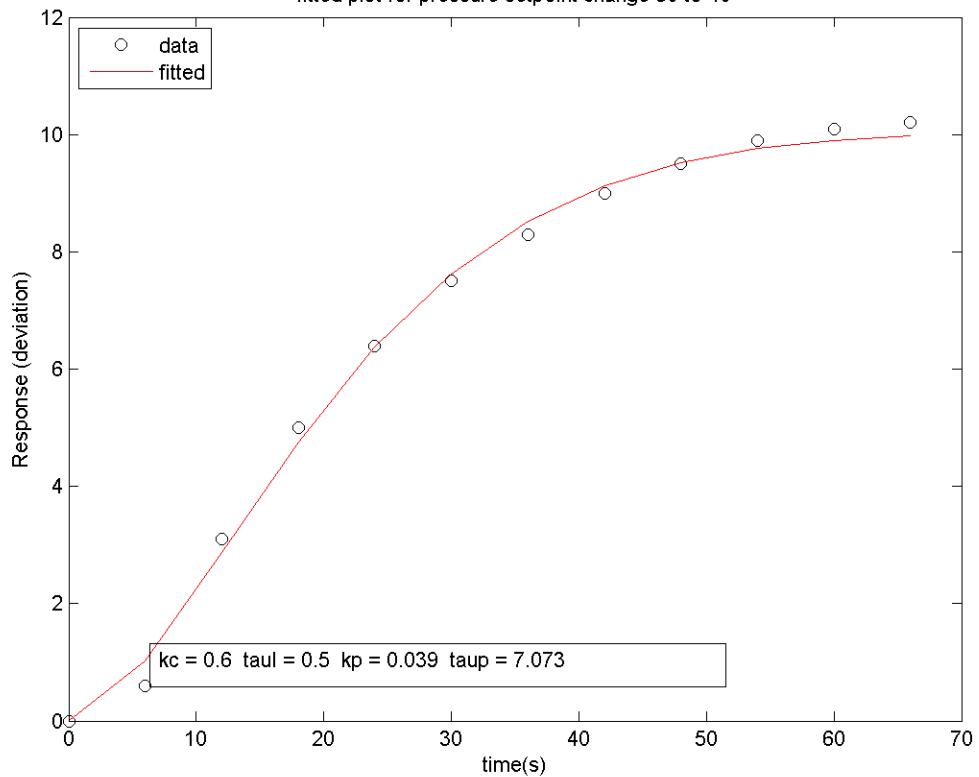
fitted plot for flowrate setpoint change 40 to 50

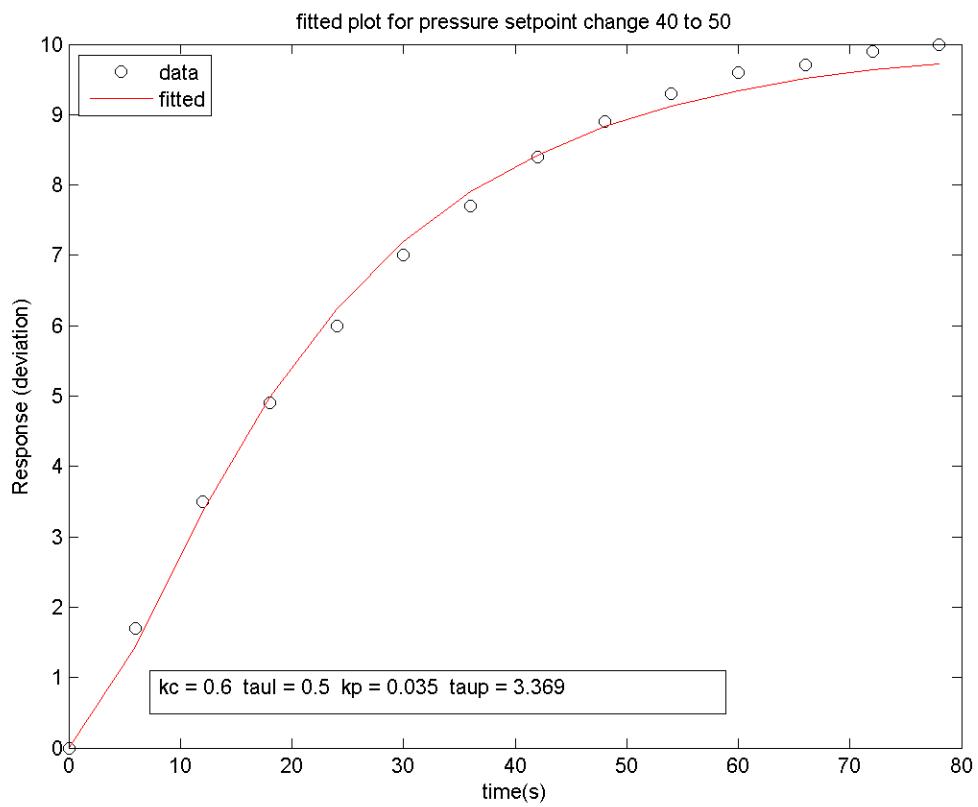


fitted plot for pressure setpoint change 20 to 30

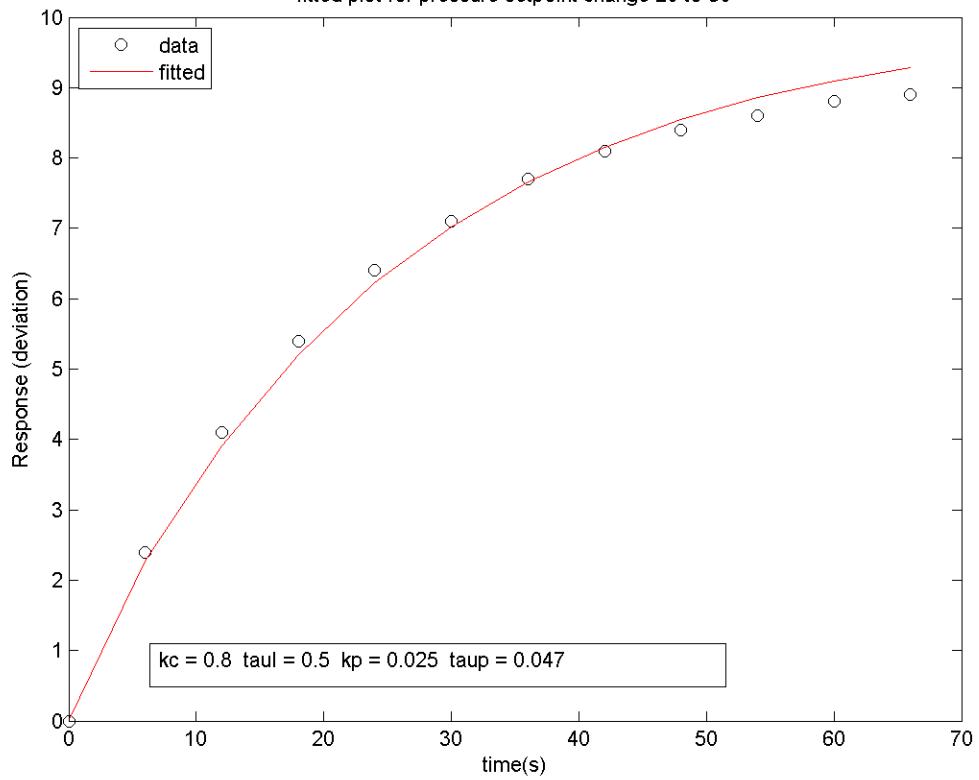


fitted plot for pressure setpoint change 30 to 40

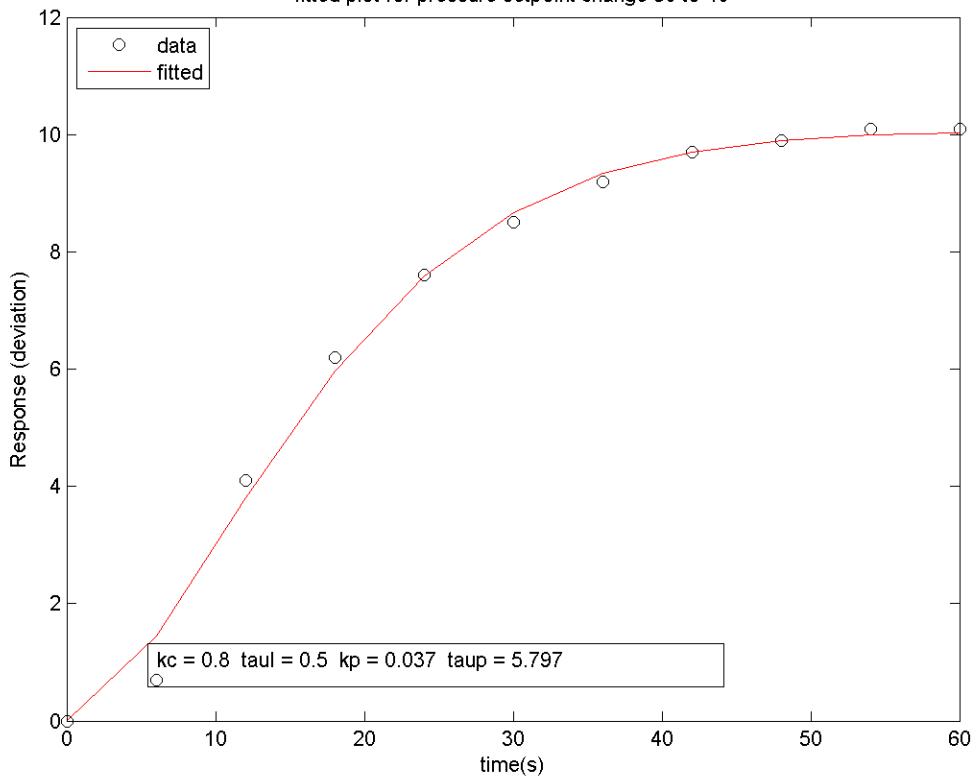


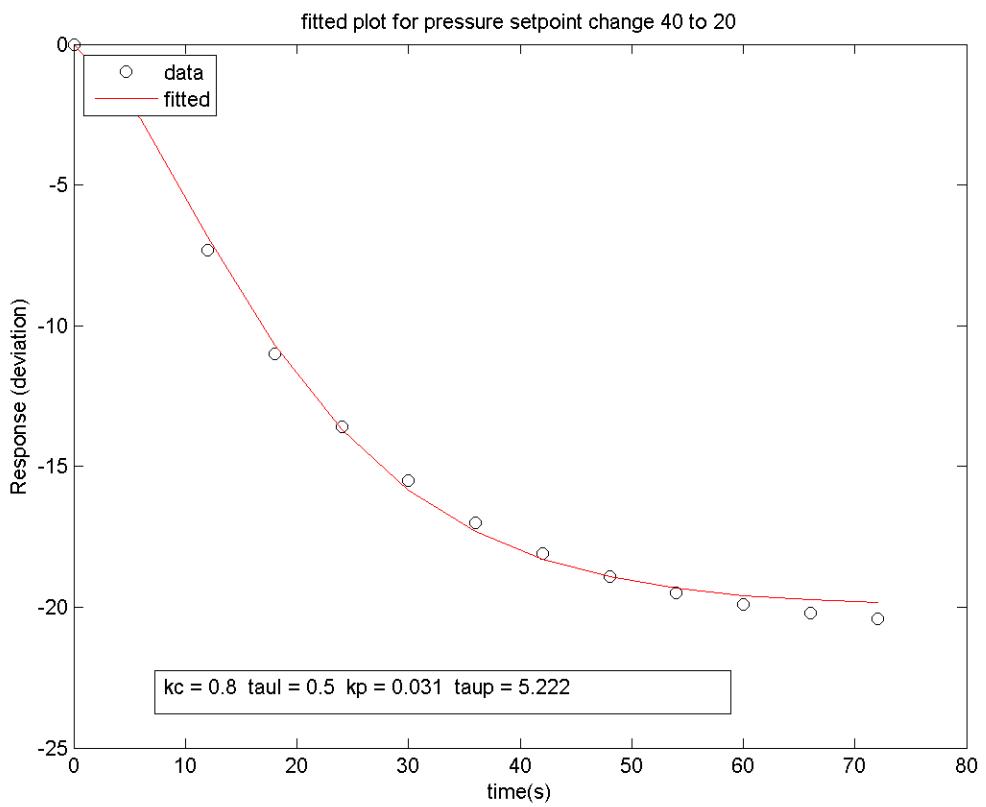


fitted plot for pressure setpoint change 20 to 30

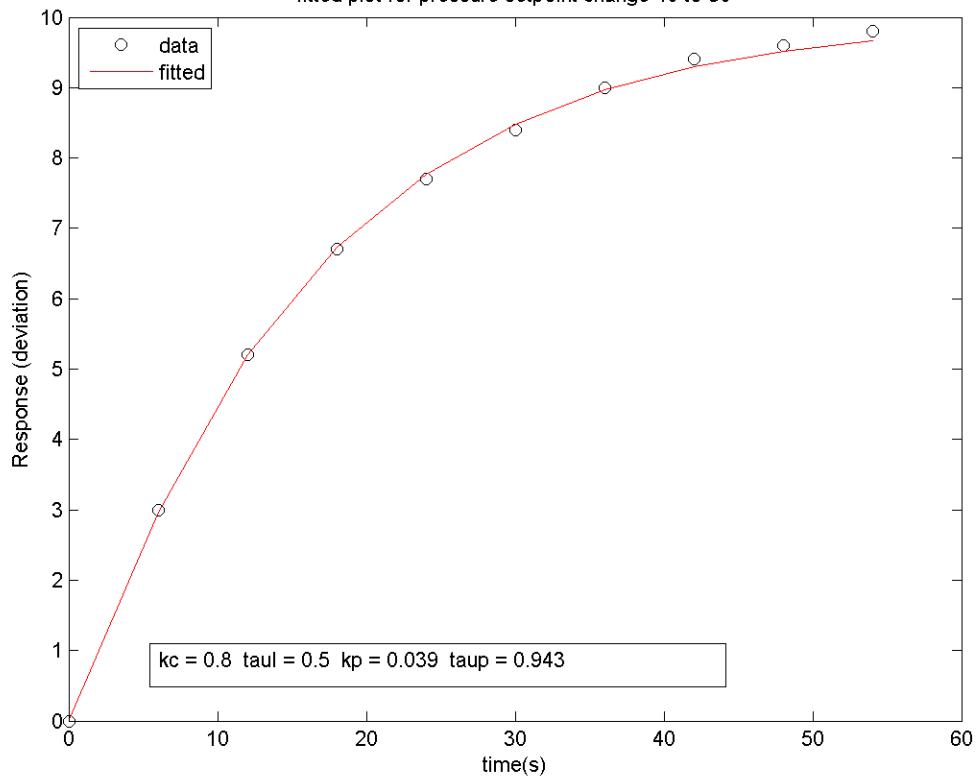


fitted plot for pressure setpoint change 30 to 40

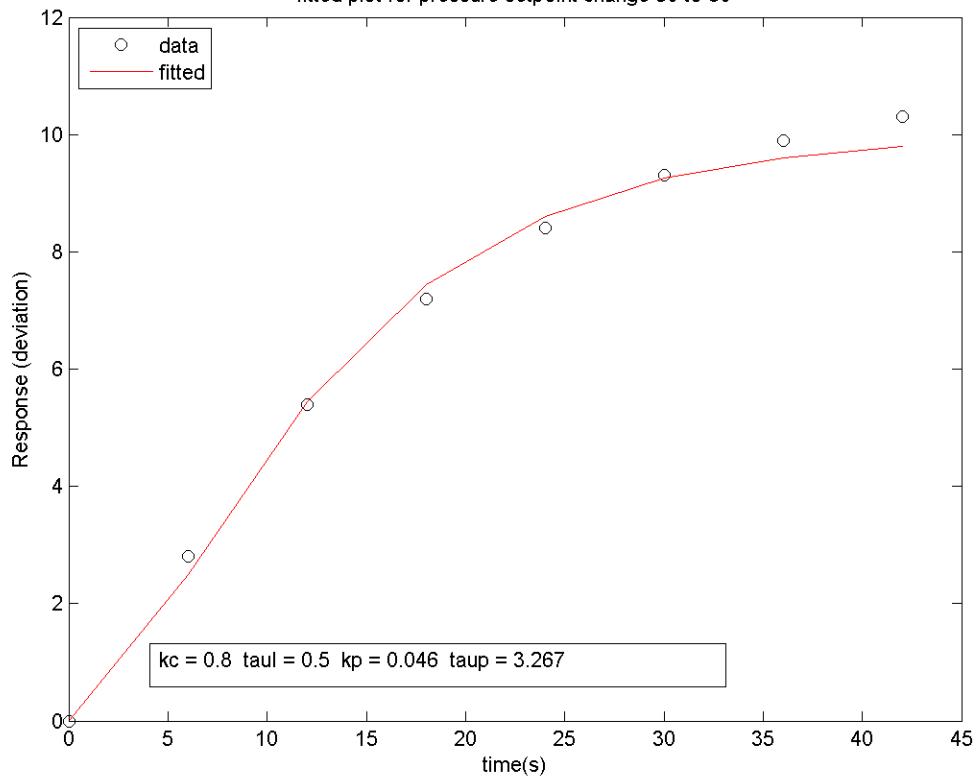


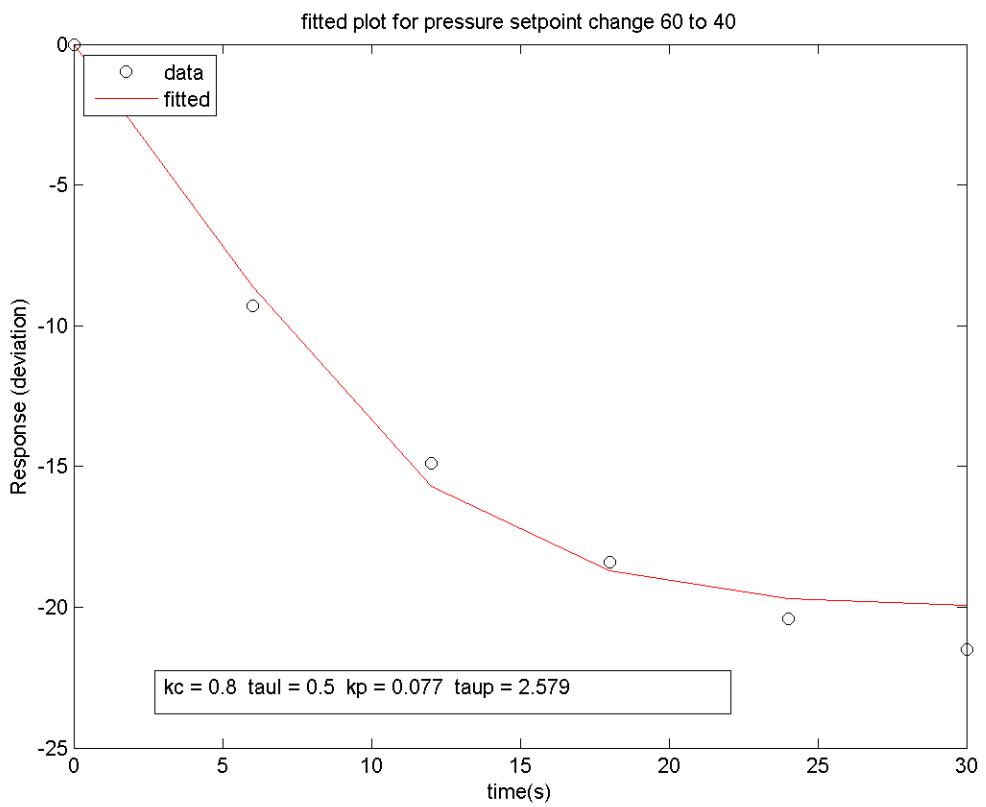


fitted plot for pressure setpoint change 40 to 50

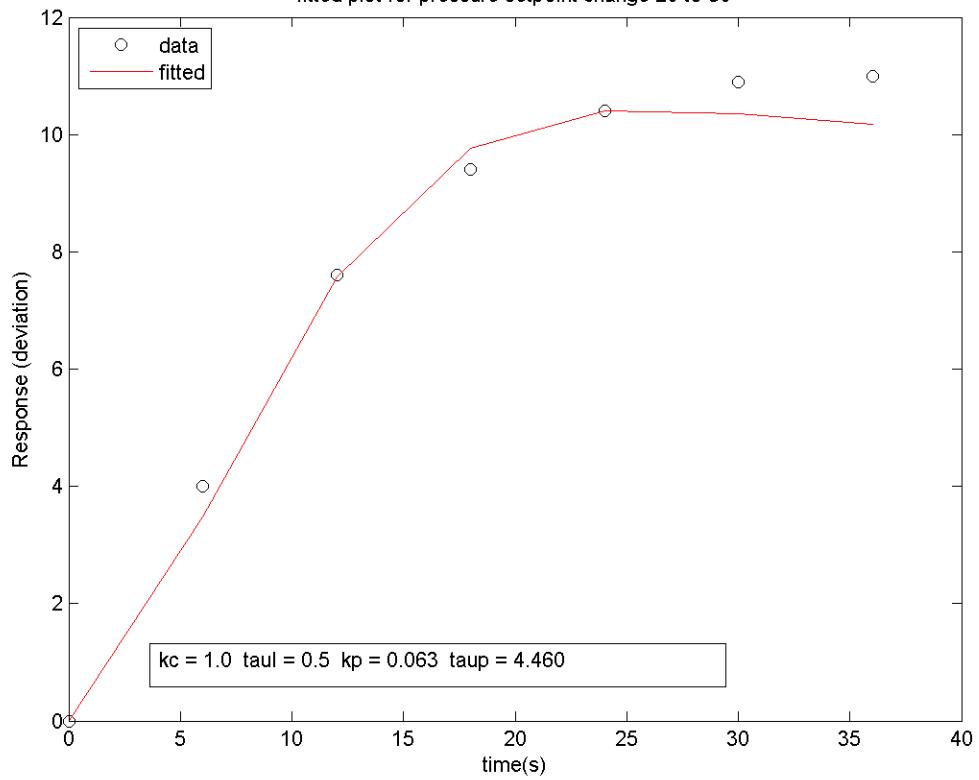


fitted plot for pressure setpoint change 50 to 60

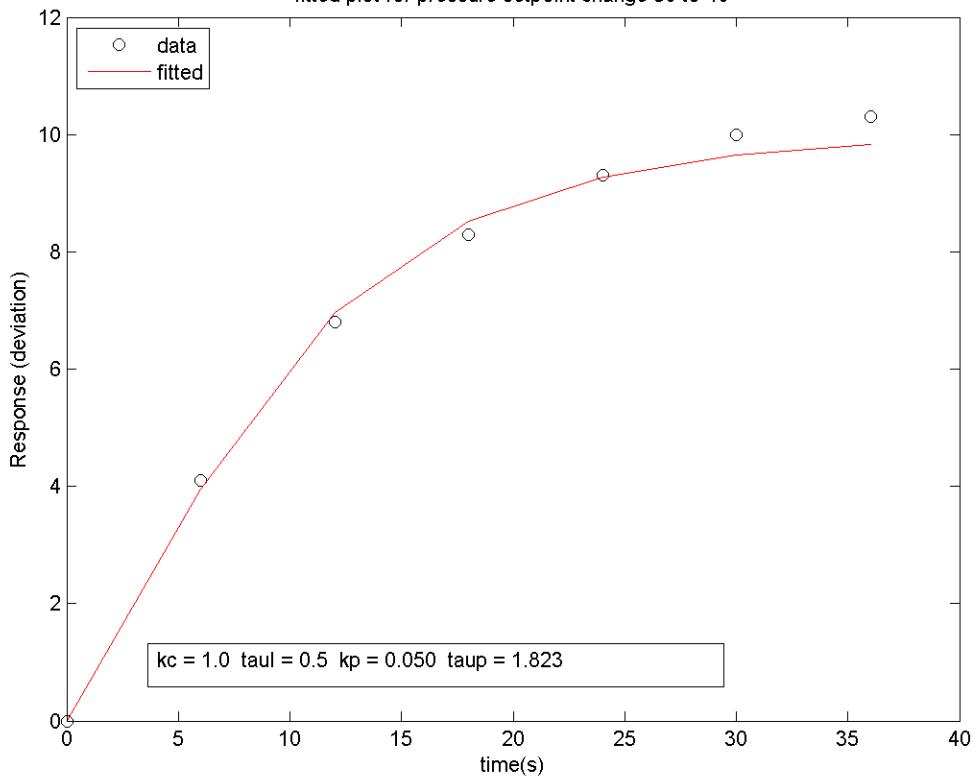




fitted plot for pressure setpoint change 20 to 30



fitted plot for pressure setpoint change 30 to 40



fitted plot for pressure setpoint change 40 to 50

