

AFD L2

~~Continued~~

Continuity & Momentum equations

Re:

- fluid: continuous medium that flows
- collisional vs collisionless fluid
- Eulerian & Lagrangian frameworks

$$\frac{DQ}{Dt} = \frac{\partial Q}{\partial t} + \underline{u} \cdot \nabla Q$$

Lagrangian Eulerian convective
 time derivative derivative

- concept of streamlines, particle paths & streaklines
- goal: set up PDEs describing properties as function of time
 non-relativistic fluids

conservation of mass
 continuity equation

conservation of momentum
 pressure & stress tensor
 momentum eq for fluid
 concept of non-pressure

conservation of mass
Eulerian volume, fluid flowing throughout

$$\frac{\partial S}{\partial t} \int_V S dV = - \int_S \underline{u} \cdot d\underline{s}$$

$$\Rightarrow \int_V \frac{\partial S}{\partial t} dV = - \int_V \nabla \cdot (S \underline{u}) dV$$

$$\Rightarrow \int_V \left(\frac{\partial S}{\partial t} + \nabla \cdot (S \underline{u}) \right) dV = 0$$

arrive to:
Eulerian continuity equation

$$\frac{\partial S}{\partial t} + \nabla \cdot (S \underline{u}) = 0$$

Lagrangian view using Eulerian view

$$\frac{D S}{D t} = \frac{\partial S}{\partial t} + \underline{u} \cdot \nabla S = - \nabla \cdot (S \underline{u}) + \underline{u} \cdot \nabla S$$

$$\cancel{\frac{D S}{D t}} = - S \nabla \cdot \underline{u} - \underline{u} \cdot \nabla S + \underline{u} \cdot \nabla S$$

$$= - S \nabla \cdot \underline{u}$$

arrive to:
Lagrangian continuity equation

$$\frac{D S}{D t} + S \nabla \cdot \underline{u} = 0$$

suppose incompressible fluid: $\frac{D S}{D t} = 0$

$$\Rightarrow \nabla \cdot \underline{u} = 0$$

i.e. flow is not converging or diverging
(so it is incompressible)

Conservation of Momentum

$$d\mathbf{F} = \rho d\mathbf{S}$$

$d\mathbf{F}$ & $d\mathbf{S}$ align.

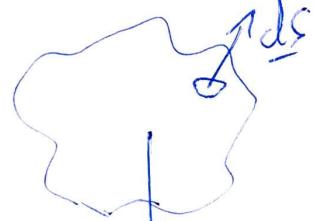
can think pressure as flux of momentum

more generally:

$$d\mathbf{F}_i = \sigma_{ij} d\mathbf{S}_j$$

if $\sigma_{ij} \propto I$, $d\mathbf{S}$ & $d\mathbf{F}$ do not align.

consider fluid element subject to forces & external force field



total pressure force

$$\underline{\mathbf{F}} = - \int_S \rho \mathbf{n} \cdot d\mathbf{S} = - \int_V \nabla \cdot (\rho \hat{\mathbf{n}}) dV$$

$\hat{\mathbf{n}}$: arbitrary dir.

$$= - \int_V \mathbf{n} \cdot \nabla p dV$$

eq. of motion for fluid element:

$$\left(\frac{D}{Dt} \int_V S \underline{\mathbf{u}} dV \right) \cdot \hat{\mathbf{n}} = \int_V \hat{\mathbf{n}} \cdot \nabla p dV + \int_V S g \cdot \hat{\mathbf{n}} dV$$

$$\Rightarrow \frac{D}{Dt} (S \underline{\mathbf{u}}) \cdot \hat{\mathbf{n}} = - \int_V \mathbf{n} \cdot \nabla p + \int_V S g \cdot \hat{\mathbf{n}}$$

product rule is obeyed by Lagrangian derivative:

$$\Rightarrow \hat{\mathbf{n}} \cdot \underbrace{\frac{D}{Dt} (S \underline{\mathbf{u}})}_{0, \text{By mass conservation}} + S \underline{\mathbf{u}} \cdot \frac{D \hat{\mathbf{n}}}{Dt} = 0$$

$$\Rightarrow \int_V \underline{\mathbf{u}} \cdot \left(S \frac{D \underline{\mathbf{u}}}{Dt} + \nabla p - S g \right) = 0$$

$$\forall \int_V \underline{\mathbf{u}}$$

$$\Rightarrow S \frac{Du}{Dt} = -\nabla p + Sq \quad \begin{array}{l} \text{Lagrangian momentum} \\ \text{equation} \end{array}$$

write Lagrangian deriv. explicitly:

$$S \frac{\partial u}{\partial t} + S(\underline{u} \cdot \nabla) \underline{u} = -\nabla p + Sq$$

Newtonian
momentum
equation.

Notational convenience:

$$\frac{\partial}{\partial t} \equiv \partial_t \quad \frac{\partial}{\partial x_i} \equiv \partial_i$$

$$\frac{\partial}{\partial t} (Su_i) = \partial_t (Su_i)$$

$$= S \partial_t u_i + u_i \partial_t S$$

$$= \underbrace{-Su_j \partial_j u_i}_{\cancel{S} \cancel{u} \cancel{\partial} u} - \underbrace{\partial_j p \delta_{ij}}_{\partial_i p \equiv \nabla p} + \underbrace{Sq_i - u_i \partial_j Sq_j}_{\cancel{S} \cancel{u} \cancel{\partial} Sq}$$

$$- Su \cdot \nabla u$$

write $\partial_j \cdot$:

$$\partial_j (Su_i) = -\partial_j (Su_i u_j + p \delta_{ij}) + Sq_i$$

stress tensor
due to
bulk flow | random thermal
"Ran Poissone" | motions

$$= -\partial_j \sigma_{ij} + Sq_i$$

conservation
form

$$\partial_t (Su) = \nabla \cdot (Su \otimes u + p I) + Sq$$

flow of momentum
consistency

coordinate
free language

Eulerian form: $\partial_t S = \nabla \cdot (S u)$

Example: flow in a pipe

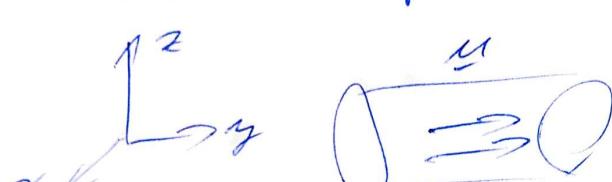


Diagram showing a pipe of diameter D with velocity u and pressure p . A coordinate system (x, y, z) is shown at the top left.

$$\sigma_{ij} = \begin{pmatrix} \mu & 0 & 0 \\ 0 & \mu + \rho u^2 & 0 \\ 0 & 0 & \mu \end{pmatrix}$$

Non pressure