

# AED L2

~~Continuum~~

## Continuity & Momentum equations

Re:

- fluid: continuous media that flows
- collisional vs collisionless fluid
- Eulerian & Lagrangian frameworks

$$\frac{DQ}{Dt} = \frac{\partial Q}{\partial t} + \underline{u} \cdot \nabla Q$$

Lagrangian Eulerian  
time derivative

convective  
derivative

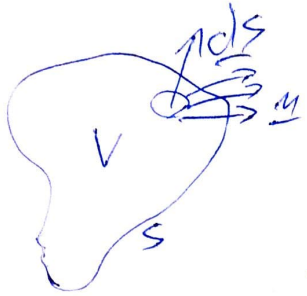
- concept of streamlines, particle paths & streaklines
- goal: set up PDEs describing properties as function of time
- non-relativistic fluids

conservation of mass  
continuity equation

conservation of momentum

pressure & stress tensor  
momentum eq for fluid  
concept of ram-pressure

conservation of mass  
Eulerian volume, fluid flowing through it



$$\frac{\partial}{\partial t} \int_V \rho dV = - \int_S \rho \underline{u} \cdot d\underline{S}$$

$$\Rightarrow \int_V \frac{\partial \rho}{\partial t} dV = - \int_V \nabla \cdot (\rho \underline{u}) dV$$

$$\Rightarrow \int_V \left( \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{u}) \right) dV = 0$$

arrive to:

Eulerian continuity equation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{u}) = 0$$

Lagrangian view using Eulerian view

$$\frac{D\rho}{Dt} = \frac{\partial \rho}{\partial t} + \underline{u} \cdot \nabla \rho = - \nabla \cdot (\rho \underline{u}) + \underline{u} \cdot \nabla \rho$$

$$\cancel{D\rho/Dt} = - \rho \nabla \cdot \underline{u} - \underline{u} \cdot \nabla \rho + \underline{u} \cdot \nabla \rho$$

$$= - \rho \nabla \cdot \underline{u}$$

arrive to:

Lagrangian continuity equation

$$\frac{D\rho}{Dt} + \rho \nabla \cdot \underline{u} = 0$$

suppose incompressible fluid:  $\frac{D\rho}{Dt} = 0$

$$\Rightarrow \nabla \cdot \underline{u} = 0$$

i.e. flow is not converging or diverging  
(so it is incompressible)

# Conservation of Momentum

$$d\mathbf{F} = p d\mathbf{S}$$

$d\mathbf{F}$  &  $d\mathbf{S}$  align.

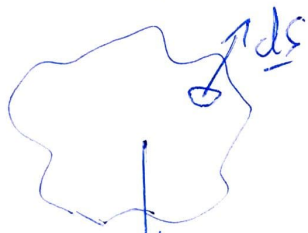
can think pressure as  
flux of momentum

more generally:

$$dF_i = \sigma_{ij} \cdot dS_j$$

if  $\sigma_{ij} \notin I$ ,  $d\mathbf{S}$  &  $d\mathbf{F}$   
do not align.

consider fluid element subject to forces & external force field  
& total pressure force



$\hat{n}$ : arbitrary dir.

$$\oint \hat{n} = - \int_S p \hat{n} \cdot d\mathbf{S} = - \int_V \nabla \cdot (p \hat{n}) dV$$

$$= - \int_V \hat{n} \cdot \nabla p dV$$

eq. of motion for fluid element:

$$\left( \frac{D}{Dt} \int_V \rho \mathbf{u} dV \right) \cdot \hat{n} = \int_V \hat{n} \cdot \nabla p dV + \int_V \rho \mathbf{g} \cdot \hat{n} dV$$

$$\Rightarrow \frac{D}{Dt} (\int_V \rho \mathbf{u} dV) = - \int_V \hat{n} \cdot \nabla p + \int_V \rho \mathbf{g} \cdot \hat{n}$$

Product rule is obeyed by Lagrangian derivative:

$$\Rightarrow \underbrace{\hat{n} \cdot \mathbf{u} \frac{D}{Dt} (\int_V \rho dV)}_{0, \text{ By mass conservation}} + \int_V \hat{n} \cdot \frac{D\mathbf{u}}{Dt} = 0$$

$$\Rightarrow \int_V \hat{n} \cdot \left( \rho \frac{D\mathbf{u}}{Dt} + \nabla p - \rho \mathbf{g} \right) = 0$$

$$\Rightarrow \rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \rho \mathbf{g} \quad \text{Lagrangian momentum equation}$$

write Lagrangian deriv. explicitly:

$$\rho \frac{\partial \mathbf{u}}{\partial t} + \rho (\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla p + \rho \mathbf{g}$$

Eulerian momentum equation.

Notational convenience:

$$\frac{\partial}{\partial t} \equiv \partial_t \quad \frac{\partial}{\partial x_i} \equiv \partial_i$$

$$\frac{\partial}{\partial t} (\rho u_i) = \partial_t (\rho u_i)$$

$$= \rho \partial_t u_i + u_i \partial_t \rho$$

$$= \underbrace{\rho u_j \partial_j u_i}_{-\rho \mathbf{u} \cdot \nabla \mathbf{u}} - \underbrace{\partial_j p \delta_{ij}}_{\partial_i p \equiv \nabla p} + \rho g_i - u_i \partial_j (\rho u_j)$$

write  $\partial_j \cdot$ :

$$\partial_t (\rho u_i) = -\partial_j (\underbrace{\rho u_i u_j}_{\text{stress tensor due to bulk flow "Ram Pressure"}} + \underbrace{p \delta_{ij}}_{\text{random thermal motions}}) + \rho g_i$$

$$= -\partial_j \sigma_{ij} + \rho g_i$$

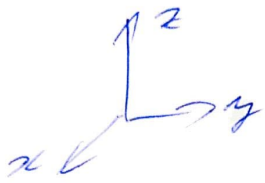
conservative form

$$\partial_t (\rho \mathbf{u}) = -\nabla \cdot (\underbrace{\rho \mathbf{u} \otimes \mathbf{u} + p \mathbf{I}}_{\text{flux of momentum density}}) + \rho \mathbf{g} \quad \text{coordinate free language}$$



Eulerian form:  $\partial_t S = -\nabla \cdot (S \underline{u})$

Example: flow in a pipe



$$\sigma_{ij} = \begin{pmatrix} p & 0 & 0 \\ 0 & p + S u^2 & 0 \\ 0 & 0 & p \end{pmatrix}$$

non pressure