

## Learning Objectives

- To understand
  - Bernoulli Equation
  - Derivation of Bernoulli equation
  - Explanation of each Term in Bernoulli equation
  - Venturi Effect
  - How to apply Bernoulli equation to explain many problems in everyday life





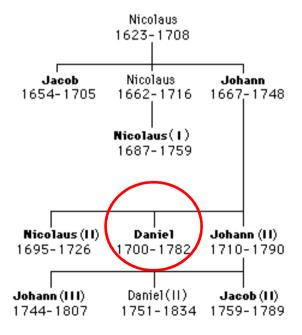
## Bernoulli Equations

#### Bernoulli's Family

- Daniel Bernoulli (1700-1782) was born in the Netherlands – he wrote the book Hydrodynamica. He hold a Chair at St Petersburg together with his brother Nicolaus II
- His father Johann wrote the first book on calculus (after Newton & Leibniz)
- His uncle Jacob was the first to use the term "integral" ("Bernoulli differential equation")
- His cousin Nicolaus I has contributed to Riccati equations
- His brother Nicolaus II worked on differential equations and probability
- His brother Johann II worked in heat & ligh he occupied the same chair as his father at Basel University
- His nephews Johann III, Daniel II and Jacob II are also mathematicians of note in their days



The Bernoulli family



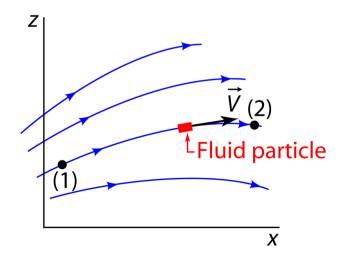
## Bernoulli Equations

• Bernoulli's Equation for Incompressible Flow

$$\frac{p}{\rho} + \frac{1}{2}V^2 + gz = \text{constant}$$

where  $\rho$  is density, g is gravity, p is pressure, V is velocity, and z is the elevation of the point above a reference plane, with the positive z-direction pointing upward — so in the direction opposite to the gravitational acceleration

- The above Bernoulli equation is valid for steady, incompressible flow along a streamline in an "inviscid regions of flow"
- Constant of integration in general varies from one streamline to another, but remains constant along a particular streamline



- Integral from NS Equation
  - Steady, incompressible, inviscid flow (Euler equation)

$$\frac{\partial w}{\partial t} + (\vec{V} \cdot \nabla) u = X - \frac{1}{\rho} \frac{\partial p}{\partial X}$$

$$\frac{\partial v}{\partial t} + (\vec{V} \cdot \nabla) v = Y - \frac{1}{\rho} \frac{\partial p}{\partial Y}$$

$$\frac{\partial w}{\partial t} + (\vec{V} \cdot \nabla) w = Z - \frac{1}{\rho} \frac{\partial p}{\partial Z}$$

- Only consider gravity; rewrite in vector form

$$\left(\vec{V} \bullet \nabla\right) \vec{V} = \vec{g} - \frac{1}{\rho} \nabla p$$

• Integral from NS Equation

$$abla imes \vec{V}$$
 旋度 curl or rotation

$$(\vec{V} \cdot \nabla) \vec{V} = \nabla \frac{\vec{V}^2}{2} - \vec{V} \times \nabla \times \vec{V}$$
 Feynman subscript notation

$$\nabla \frac{\vec{V}^2}{2} - \vec{V} \times \nabla \times \vec{V} = \vec{g} - \frac{1}{\rho} \nabla p$$

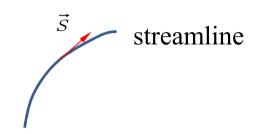
- Multiple by the unit vector  $\vec{s} = \frac{\vec{V}}{|\vec{V}|}$  along a streamline

amline
$$\vec{s} \cdot \nabla \frac{\vec{V}^2}{2} - \frac{\vec{V}}{|\vec{V}|} \cdot \vec{V} \times \nabla \times \vec{V} = \vec{s} \cdot \vec{g} - \frac{1}{\rho} \vec{s} \cdot \nabla p$$

$$\vec{s} \cdot \nabla \frac{\vec{V}^2}{2} = \vec{s} \cdot \vec{g} - \frac{1}{\rho} \vec{s} \cdot \nabla p$$
streamline

Integral from NS Equation

$$\frac{\partial}{\partial s} \left( \frac{\vec{V}^2}{2} + \frac{p}{\rho} \right) + \vec{s} \cdot \vec{g} = 0$$



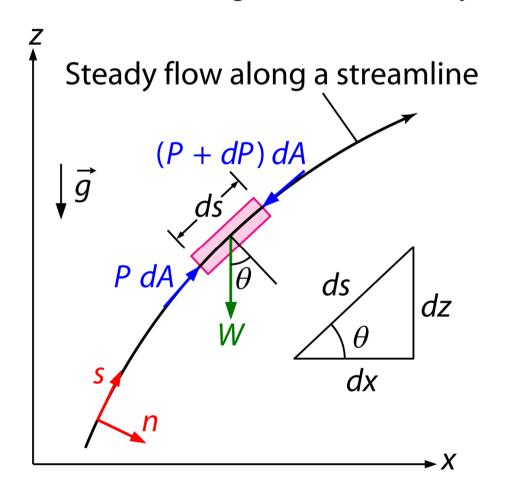
Integrate along streamline

$$\frac{\vec{V}^2}{2} + \frac{p}{\rho} + \int \vec{s} \cdot \vec{g} ds = C$$

$$C \text{ is constant}$$

$$\frac{\vec{V}^2}{2} + \frac{p}{\rho} + gz = C$$

- Newton's second law
  - Consider motion of fluid particle in a steady flow



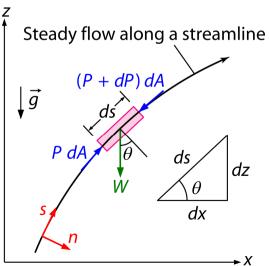
- Newton's second law
  - Applying Newton's second law in the s-direction on a particle moving along a streamline

$$\sum F_{s} = ma_{s}$$

Assuming viscous forces are negligible, only forces acting on fluid particle in s-direction are pressure forces and component of particle's weight

$$PdA - (P + dP)dA - W\sin\theta = ma_s$$
$$-dPdA - W\sin\theta = ma_s$$

 $\theta$  is the angle between normal to streamline and vertical z-axis



- Newton's second law
  - Velocity along fluid particle

$$V = \frac{ds}{dt}$$

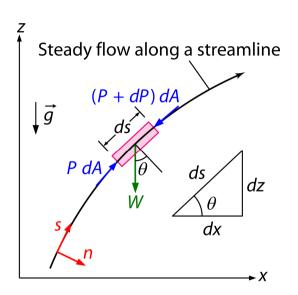
Velocity is a function of s and t

$$dV = \frac{\partial V}{\partial s} ds + \frac{\partial V}{\partial t} dt$$
$$dV \quad \partial V \ ds \quad \partial V$$

$$\frac{dV}{dt} = \frac{\partial V}{\partial s} \frac{ds}{dt} + \frac{\partial V}{\partial t}$$

- Steady flow  $\partial V/\partial t = 0$ 

$$a_{s} = \frac{dV}{dt} = \frac{\partial V}{\partial s} \frac{ds}{dt} = \frac{\partial V}{\partial s} V$$



Newton's second law

$$-dPdA - W\sin\theta = m\frac{\partial V}{\partial s}V$$

– Volume of the fluid particle  $\Omega$ 

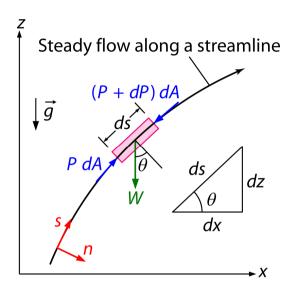
$$m = \rho \Omega = \rho dAds$$

$$W = mg = \rho g dA ds$$

$$\sin\theta = \frac{dz}{ds}$$

$$-\frac{dPdA}{ds} - \rho g dA ds \frac{dz}{ds} = \rho dA ds \frac{\partial V}{\partial s} V$$

$$-dP - \rho g dz = \rho V dV$$

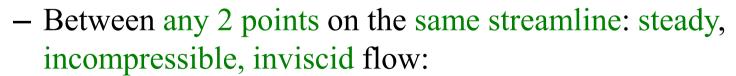


Newton's second law

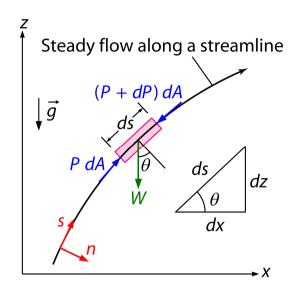
$$VdV = \frac{1}{2}d(V^2)$$
$$-\frac{dP}{\rho} - gdz = \frac{dV^2}{2}$$

Integrate the above equation

$$\frac{V^2}{2} + gz + \frac{P}{\rho} = C$$



$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$



- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy

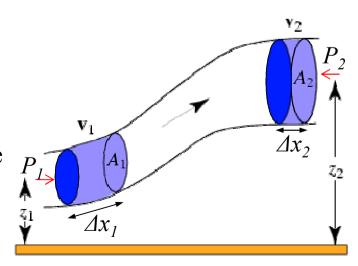
$$\Delta W = \Delta K + \Delta U$$
Work Kinetic Energy Potential Energy

✓ Work

$$\begin{split} \Delta W &= F_1 \Delta x_1 - F_2 \Delta x_2 \\ &= P_1 A_1 \Delta x_1 - P_2 A_2 \Delta x_2 \\ &= P_1 \Omega_1 - P_2 \Omega_2 \end{split}$$

Recall continuity equation of incompressible flow,  $\Omega_1 = \Omega_2 = \Omega$ 

$$\Delta W = P_1 \Omega - P_2 \Omega$$

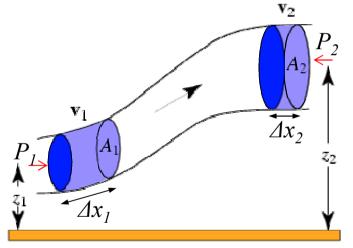


- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy
    - ✓ Change in kinetic energy

$$\Delta E = \frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2$$

✓ Change in potential energy

$$\Delta U = m_2 g z_2 - m_1 g z_1$$



Recall continuity equation of incompressible flow,  $m_1 = m_2 = m$ 

$$\Delta U = mgz_2 - mgz_1$$

- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy

Kinetic energy and potential energy
$$\Delta W = \Delta K + \Delta U$$

$$P_1\Omega - P_2\Omega = \frac{1}{2}mv_2^2 - \frac{1}{2}mv_1^2 + mgz_2 - mgz_1$$

$$\rho = \frac{m}{\Omega} \implies P_1 - P_2 = \frac{1}{2}\rho v_2^2 - \frac{1}{2}\rho v_1^2 + \rho gz_2 - \rho gz_1$$

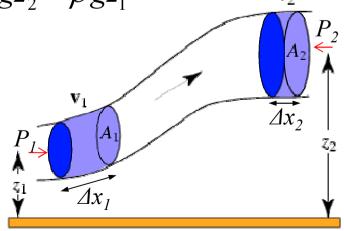
$$P_1 = \frac{1}{2}\rho v_2^2 + \rho gz_2 - \rho gz_1$$

$$P_{1} + \frac{1}{2}\rho v_{1}^{2} + \rho g z_{1}$$

$$= P_{2} + \frac{1}{2}\rho v_{2}^{2} + \rho g z_{2}$$

$$= constant$$

constant



More explanation

$$\frac{P}{\rho} + \frac{1}{2}v^2 + gz = \text{constant (along a streamline)}$$

 Each term in the above equation has same units of energy per unit mass

✓  $P/\rho$ : Flow energy

 $\sqrt{v^2/2}$ : Kinetic energy

✓ gz: Potential energy

- Bernoulli equation can be viewed as a restatement of conservation of mechanical energy
- The sum of the specific (per unit mass) kinetic, potential, and flow energies of a fluid particle is constant along a streamline in a steady, incompressible and inviscid flow.

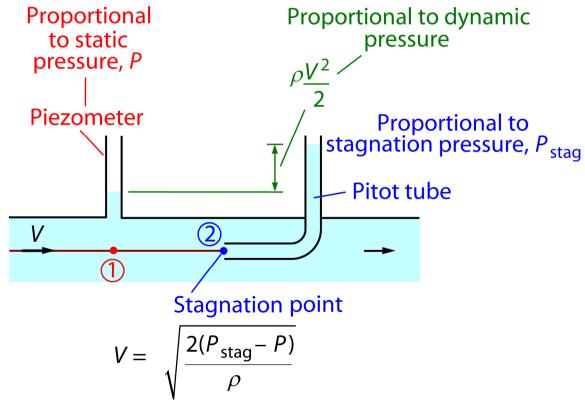
More explanation

$$P + \frac{1}{2}\rho v^2 + \rho gz = \text{constant (along a streamline)}$$

- Each term in the above equation has same units as pressure
  - ✓ P: static pressure → represents the actual thermodynamic pressure of fluid
  - ✓  $\rho v^2/2$ : dynamic pressure → represents pressure rise when fluid in motion is brought to reset
  - $\checkmark \rho gz$ : hydrostatic pressure  $\rightarrow$  account for the elevation effects
- Total pressure  $(P_T)$ : sum of static, dynamic and hydrostatic pressure
- Bernoulli equation:  $P_T$  along streamline is constant

$$P + \frac{1}{2}\rho v^2 + \rho gz = P_T = \text{constant (along a streamline)}$$

- Stagnation Pressure
  - Sum of static and dynamic pressure
  - Represents pressure at stagnation point where fluid is brought to rest



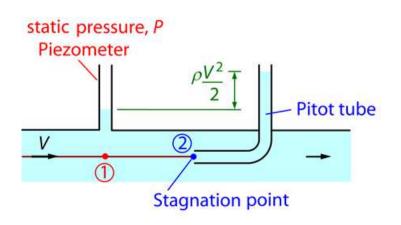
- Velocity Measurement
  - Point 1:  $V_1 = V$ ,  $P_1 = P$  (static pressure)
  - Point 1:  $V_2 = 0$ ,  $P_2 = P_{stag}$  (static pressure)  $z_1 = z_2$
  - Apply Bernoulli equation along streamline between 1 and 2:

$$P_{1} + \rho \frac{V_{1}^{2}}{2} + \rho g z_{1} = P_{2} + \rho \frac{V_{2}^{2}}{2} + \rho g z_{2}$$

$$P_{stag} = P + \rho \frac{V^{2}}{2}$$

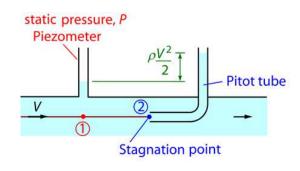
 Fluid velocity can be deduced from measurement of static and stagnation pressures:

$$V = \sqrt{\frac{2(P_{stag} - P)}{\rho}}$$

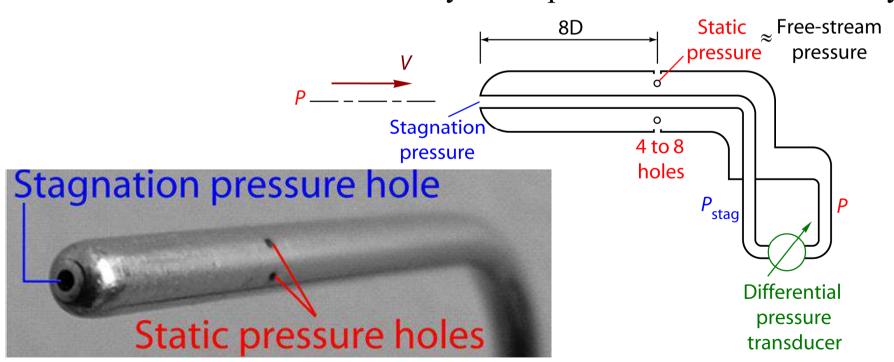


- Devices for pressure measurement
  - Static pressure tap: a small hole drilled into a wall such that plane of hole is parallel to flow direction → measures static pressure
  - Pitot tube: a small tube with its open end aligned into the flow so as to sense full impact pressure of the flowing fluid → measures stagnation pressure
  - Piezometer: vertical transparent tube attached to static pressure tap or Pitot tube: liquid rises in piezometer tube to a column height (head) proportional to pressure being measured





- Devices for pressure measurement
  - Pitot-static probe: integrates static pressure holes on a Pitot probe
  - Pitot-static probe connected to pressure transducer or manometer → measures dynamic pressure and hence velocity



- Devices for pressure measurement
  - Static pressure holes (point a) of the outer tube are located such that they measure correct upstream static pressure
  - Two tubes provide the necessary pressure difference measurement using the mercury in it
  - It is possible to use pressure transducers instead of mercury columns to obtain accurate digital readings.

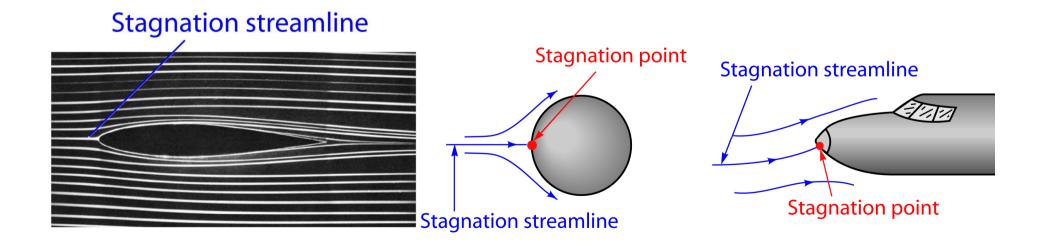
$$P_{o} = P_{x} + \rho \frac{V_{x}^{2}}{2}$$

$$P_{o} - P_{x} = (\rho_{m} - \rho)gh_{m}$$

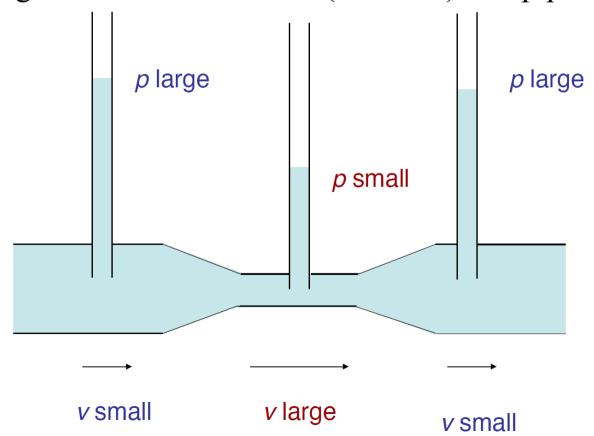
$$V_{x} = \sqrt{2(P_{stag} - P_{x})/\rho} = \sqrt{2gh_{m}(\frac{\rho_{m}}{\rho} - 1)}$$

$$\rho_{m}$$

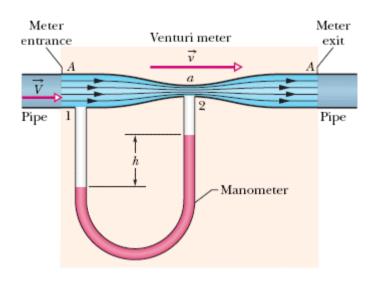
- Stagnation point
  - When a stationary body is immersed in a flow, the fluid is brought to rest at nose of body (stagnation point)
  - Stagnation streamline → streamline that extends from far upstream to stagnation point



- Venturi Effect
  - The reduction in fluid pressure that results when a fluid flows through a constricted section (or choke) of a pipe



- Venturi Effect
  - Devices to measure the flow rate of liquids



$$P_{1} + \frac{1}{2}\rho_{v}v_{1}^{2} + \rho_{v}gz_{1} = P_{2} + \frac{1}{2}\rho_{v}v_{2}^{2} + \rho_{v}gz_{2}$$

$$P_{1} - P_{2} = \frac{1}{2}\rho_{v}\left(v_{2}^{2} - v_{1}^{2}\right)$$

 $Q = v_1 A_1 = v_2 A_2$ 

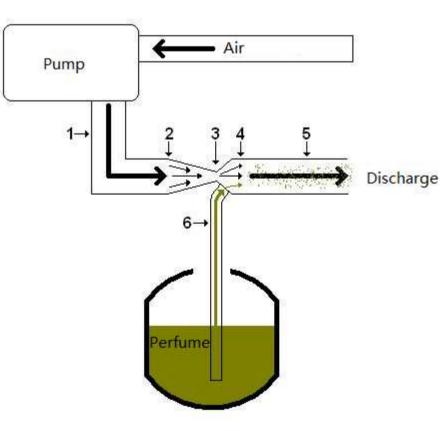
- $\triangleright$  The densities of fluids in Venturi and Manometer are  $\rho_v$  and  $\rho_m$
- The areas of cross sections at point 1 and point 2 are known as  $A_1$  and  $A_2$

$$P_1 - P_2 = \rho_m g h$$

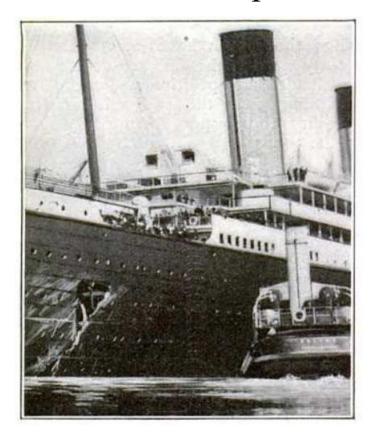
- Venturi Effect
  - Disperse perfume or spray paint (Atomizers)



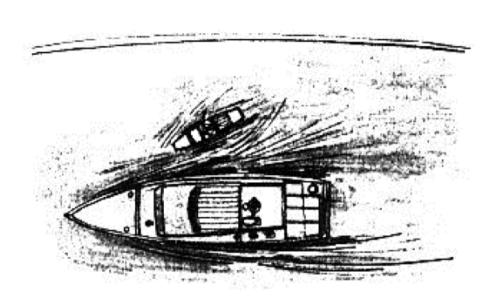


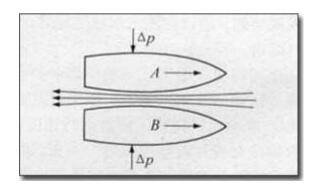


• Bernoulli's Equation



Olympic collided with Hawke, 1911





• Bernoulli's Equation





A high speed train passing a platform causes a suction effect

Long vehicle and bicycle

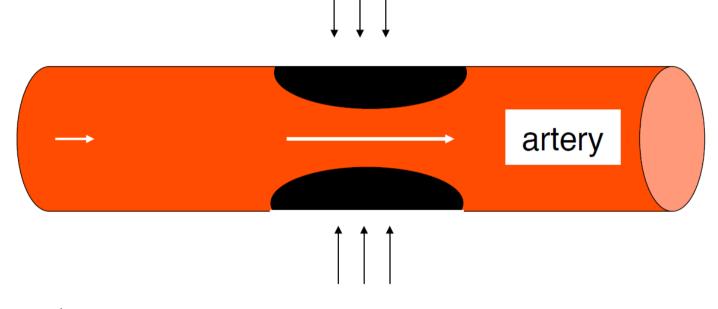
• Pour Out Beer





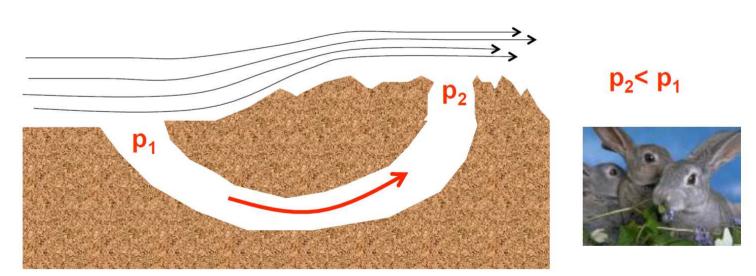
歪门斜倒(邪道) 杯壁(卑鄙)下流 改斜(邪)归正

• Arteriosclerosis and Vascular Flutter



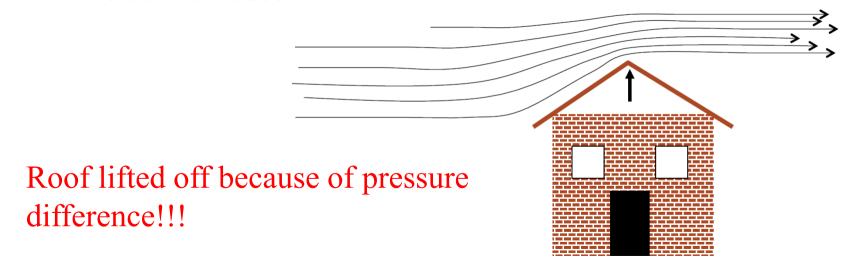
- ✓ Flow speeds up at constriction
- ✓ Pressure is lower
- ✓ Internal force acting on artery wall is reduced
- ✓ External forces are unchanged
- ✓ Artery can collapse

- Why do rabbits not suffocate in the burrows
  - Air must circulate. The burrows must have two entrances.
  - Air flows across the two holes is usually slightly different
  - One hole is usually higher than the other and the a small mound is built around the holes to increase the pressure difference.
    - ✓ Slight pressure difference
    - ✓ Forces flow of air through burrow



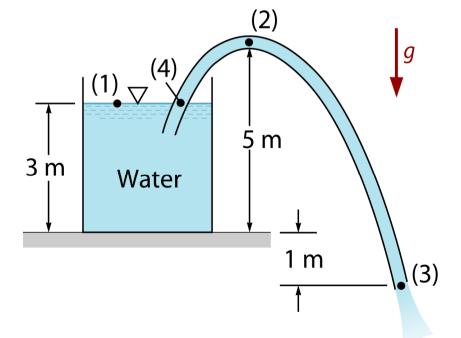
- Why does a house lose its roof in strong wind
  - Air flow is disturbed by the house.
     The "streamlines" crowd around the top of the roof
  - Faster flow above house
  - Reduced pressure above roof to that inside the house





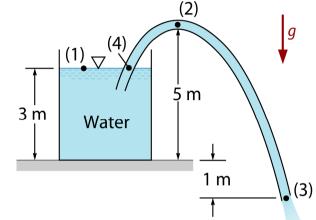
- Siphon Phenomenon
  - Water is siphoned from a large tank through a constant diameter hose
  - Determine:
    - a) velocity of water leaving (3) as a free jet
    - b) water pressure in tube at (2)
    - c) water pressure in tube at (4)

Assume water to be inviscid, incompressible and flow to be steady



#### • Siphon Phenomenon

- Solution:
  - ✓ Part (a): velocity of water leaving (3)  $z_1 z_3 = 4 \text{ m}$



$$P_1 = P_3 = 0$$
 (atmospheric pressure, 0 gage pressure)

$$V_1 \approx 0$$
 (large tank)

Applying Bernoulli equation between (1) and (3)

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

$$\frac{V_3^2}{2} = g(z_1 - z_3)$$

$$V_3 = \sqrt{2g(z_1 - z_3)} = \sqrt{(2)(9.81)(4)}$$

$$V_3 = 8.86 \text{ m/s}$$

- Siphon Phenomenon
  - Solution:
    - ✓ Part (b): water pressure in tube at (2)

Applying continuity equation between (2) and (3):

$$A_2V_2 = A_3V_3$$

Since 
$$A_2 = A_3$$
,  $V_2 = V_3 = 8.86 \text{ m/s}$ 

Applying Bernoulli equation between (2) and (3)

$$\frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

$$\frac{P_2}{\rho} = g(z_3 - z_2) \qquad z_2 - z_3 = 6 \text{ m}$$

$$P_2 = \rho g(z_3 - z_2) = (1000)(9.81)(-6) \qquad P_2 = -58.9 \text{ kPa}$$

- Siphon Phenomenon
  - Solution:
    - ✓ Part (c): water pressure in tube at (4)

Applying continuity equation between (4) and (3):

$$A_4V_4 = A_3V_3$$

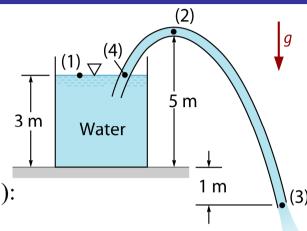
Since 
$$A_4 = A_3$$
,  $V_4 = V_3 = 8.86 \text{ m/s}$ 

Applying Bernoulli equation between (4) and (3)

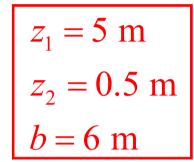
$$\frac{P_4}{\rho} + \frac{V_4^2}{2} + gz_4 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

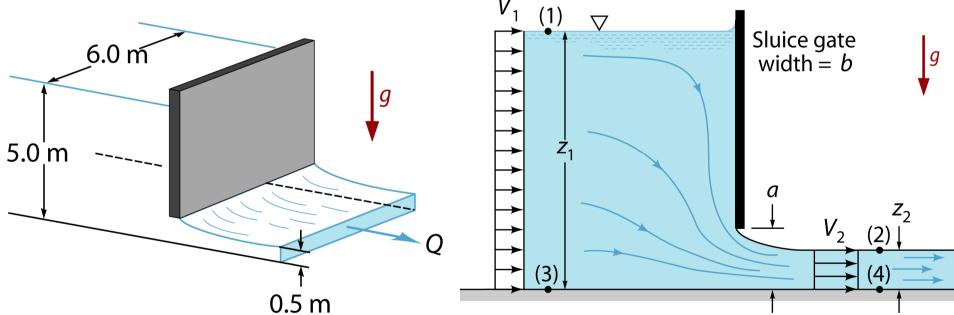
$$\frac{P_4}{\rho} = g(z_3 - z_4) \qquad z_4 - z_3 = 4 \text{ m}$$

$$P_4 = \rho g(z_3 - z_4) = (1000)(9.81)(-4) \qquad P_2 = -39.24 \text{ kPa}$$



- Water flows under sluice gate
  - Determine flow rate Q





Assume water to be inviscid, incompressible and flow to be steady

- Water flows under sluice gate
  - Solution:

Applying continuity equation between (1) and (2):

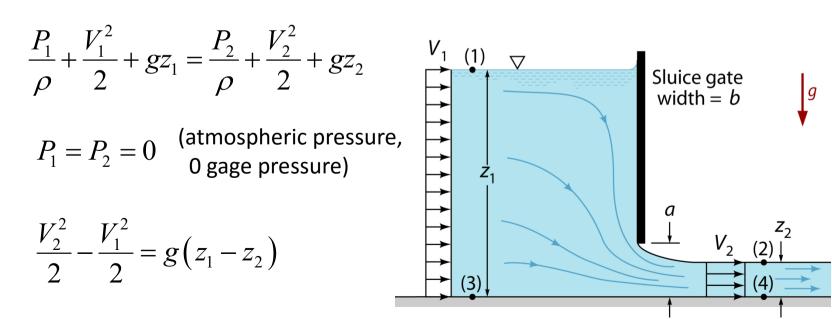
$$Q = A_1 V_1 = b z_1 V_1 = A_2 V_2 = b z_2 V_2$$
  $V_1 = V_2 \left(\frac{z_2}{z_1}\right)$ 

Applying Bernoulli equation between (1) and (2):

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$

$$P_1 = P_2 = 0$$
 (atmospheric pressure)

$$\frac{V_2^2}{2} - \frac{V_1^2}{2} = g(z_1 - z_2)$$



- Water flows under sluice gate
  - Solution:

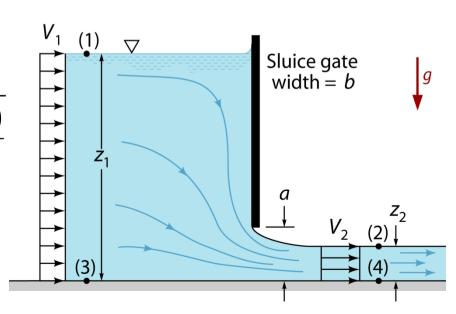
$$\frac{V_2^2}{2} - \frac{V_2^2}{2} \left(\frac{z_2}{z_1}\right)^2 = g(z_1 - z_2) \qquad V_2 = \sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$V_2 = \sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$Q = bz_2V_2 = bz_2\sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$Q = (6)(0.5)\sqrt{\frac{(2)(9.81)(5.0 - 0.5)}{1 - (0.5/5.0)^2}}$$

$$Q = 28.33 \text{ m}^3/\text{s}$$



- Water flows under sluice gate
  - Solution:

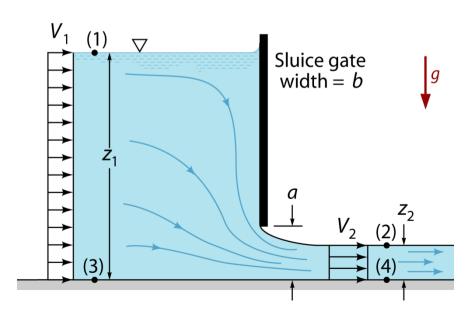
In the limit of  $z_1 >> z_2$ 

$$Q = bz_{2}V_{2} = bz_{2}\sqrt{\frac{2g(z_{1} - z_{2})}{1 - (z_{2}/z_{1})^{2}}}$$

$$Q = bz_2 \sqrt{2gz_1}$$

$$Q = (6)(0.5)\sqrt{(2)(9.81)(5.0)}$$

$$Q = 29.71 \text{ m}^3/\text{s}$$



- Water flows under sluice gate
  - Solution:

Applying continuity equation between (1) and (2):

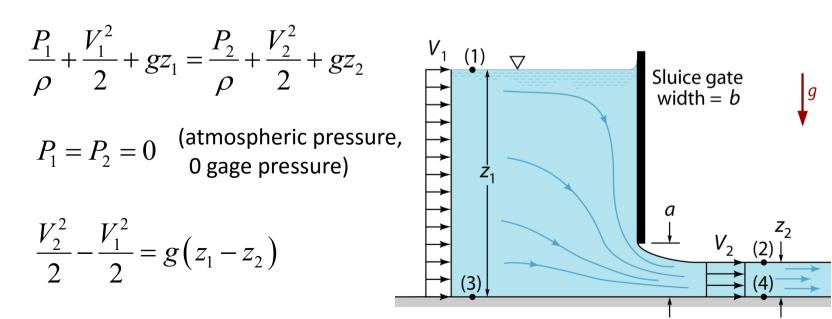
$$Q = A_1 V_1 = b z_1 V_1 = A_2 V_2 = b z_2 V_2 \qquad V_1 = V_2 \left(\frac{z_2}{z_1}\right)$$

Applying Bernoulli equation between (1) and (2):

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$

$$P_1 = P_2 = 0$$
 (atmospheric pressure)

$$\frac{V_2^2}{2} - \frac{V_1^2}{2} = g(z_1 - z_2)$$



- Water flow through a hole of a tank
  - Determine: the flow velocity  $V_2$  at section 2-2?
  - Solution:

Applying Bernoulli equation between (1-1) and (2-2):

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$

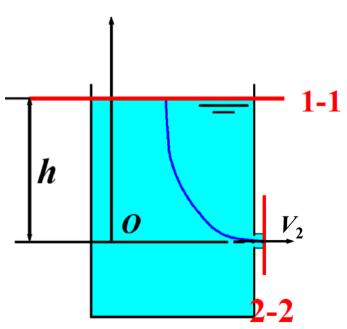
$$P_1 = P_2 = P_{atm}$$

$$z_1 - z_2 = h$$

$$V_1 \approx 0$$

$$V_2 = \sqrt{2gh}$$



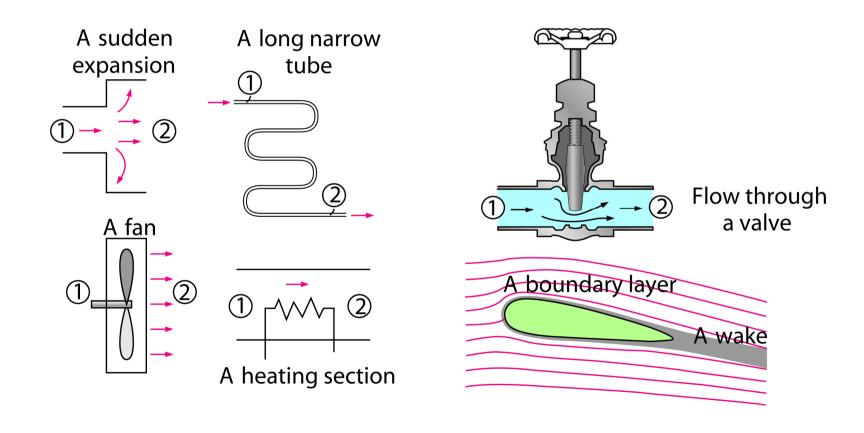


#### Limitations on Use of Bernoulli Equation

- Assumptions for Bernoulli Equation
  - Steady flow
  - Incompressible flow ⇒ acceptable if flow Mach number is less than 0.3
  - Frictionless (inviscid) flow ⇒ solid walls, wakes downstream of an object, diverging flow sections (diffusers) and flow through long and narrow passages introduce frictional effects
  - Flow along a streamline
  - No shaft work ⇒ pumps, turbines, fans and other fluid machinery carry out energy interactions with fluid particles ⇒ mechanical energy no longer conserved along streamline
  - No heat transfer

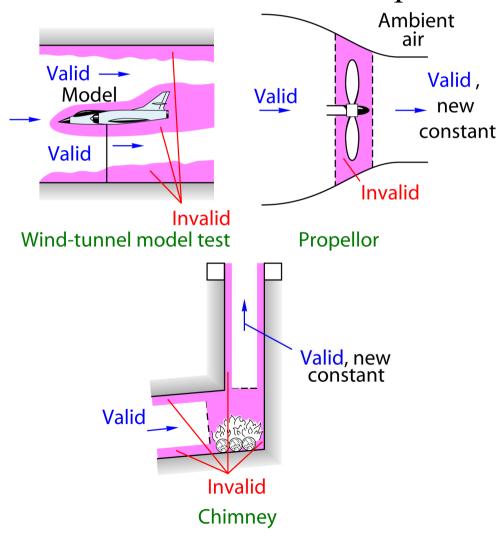
#### Limitations on Use of Bernoulli Equation

• Examples where use of Bernoulli equation is invalid:

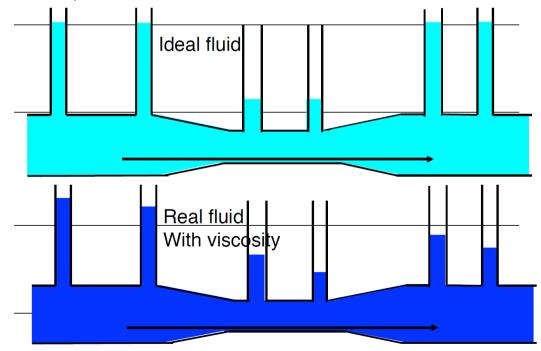


#### Limitations on Use of Bernoulli Equation

• Examples where use of Bernoulli equation is invalid:



- Viscous Effect
  - Frictional/viscous force converts mechanical energy into thermal energy
  - It corresponds to a rise in the internal energy of the fluid (heat up the fluid) or to the heat that is lost to the surroundings



#### Viscous Effect

- Introduce head loss  $h_f$  due to viscous force into the original Bernoulli equation
- $-h_f$  is an empirical parameter.

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 + h_f$$

#### • Pump Work

- Pump converts mechanical energy into hydraulic energy
- Pump head  $h_s$  can be introduced to Bernoulli equation

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 - h_s$$

- Pump head  $h_s$  is related to the power delivered to the fluid by the pump  $(P_f)$  as follows

$$P_f = \rho gQh_s$$

where *Q* is the volumetric flow rate that passes through the pump.

- Compressible fluid
  - Ideal gas at adiabatic condition

$$P_1V_1^{\gamma} = P_2V_2^{\gamma}$$

$$\frac{P_1}{\rho_1^{\gamma}} = \frac{P_2}{\rho_2^{\gamma}}$$

$$\frac{\gamma}{\gamma - 1} \frac{P_1}{\rho_1} + \frac{1}{2}v_1^2 + gz_1 = \frac{\gamma}{\gamma - 1} \frac{P_2}{\rho_2} + \frac{1}{2}v_2^2 + gz_2$$

v is velocity V is volume

- Bernoulli Equation

$$\frac{p}{\rho}$$
 +  $\frac{1}{2}V^2$  +  $gz = \text{constant}$ 

Flow energy Kinetic energy Potential energy

$$P + \frac{1}{2}\rho v^2 + \rho gz = \text{constant}$$

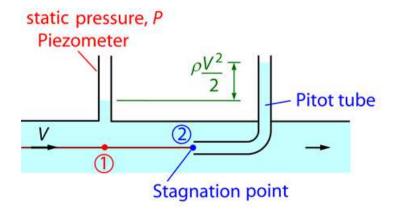
• Bernoulli equation is valid for steady, incompressible flow along a streamline in an "inviscid regions of flow"

- Stagnation Pressure : sum of static and dynamic pressure

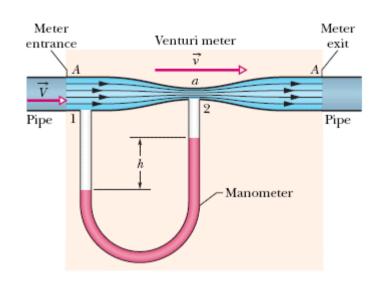
$$P_{stag} = P + \rho \frac{V^2}{2}$$

Velocity Measurement

$$V = \sqrt{\frac{2(P_{stag} - P)}{\rho}}$$



 Venturi Effect: the reduction in fluid pressure that results when a fluid flows through a constricted section (or choke) of a pipe



- Flow rate measurement:

$$Q = A_{1} \sqrt{\frac{2}{\rho_{v}} \cdot \frac{(P_{1} - P_{2})}{(\frac{A_{1}}{A_{2}})^{2} - 1}} = A_{2} \sqrt{\frac{2}{\rho_{v}} \cdot \frac{(P_{1} - P_{2})}{1 - (\frac{A_{2}}{A_{1}})^{2}}}$$

- Extended Bernoulli Equation
  - Viscous Effect

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 + h_f$$

• Pump Work

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 - h_s$$

• Compressible fluid

$$\frac{\gamma}{\gamma - 1} \frac{P_1}{\rho_1} + \frac{1}{2} v_1^2 + g z_1 = \frac{\gamma}{\gamma - 1} \frac{P_2}{\rho_2} + \frac{1}{2} v_2^2 + g z_2$$

