

Feuerzangenbowle

Physics of Imbibition and Porous Media Flow

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Physik (Master of Science)



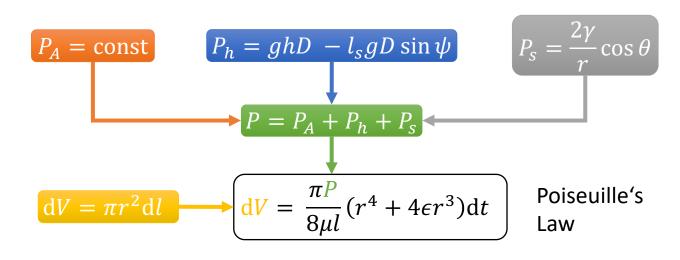
WHAT IS IMBIBITION?





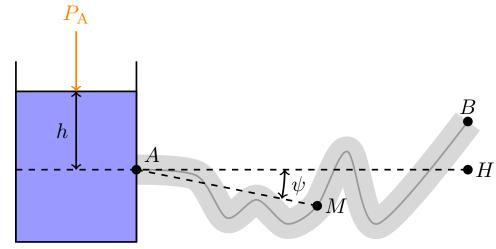


IMBIBITION AND DYNAMICS OF CAPILLARY FLOW



$$\Rightarrow \frac{\mathrm{d}l}{\mathrm{d}t} = \frac{\left(P_A + gD(h - l_S\sin\psi) + \frac{2\gamma}{r}\cos\theta\right)}{8\mu l}(r^2 + 4\epsilon r)$$

$$\Rightarrow \frac{\mathrm{d}l}{\mathrm{d}t} = \frac{(r^2 + 4\epsilon r)}{8\mu} \frac{\left(P_A + gDh + \frac{2\gamma}{r}\cos\theta - gDl\sin\psi\right)}{l}$$



- $\theta = const$
- = const
- $\psi = 0, \pi/2$
- $l_s = l$

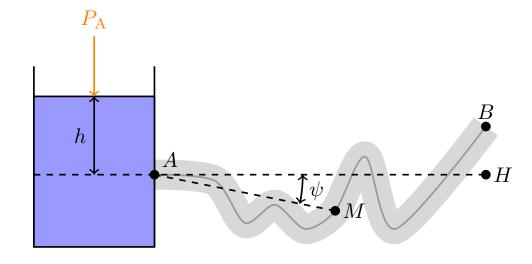
IMBIBITION AND DYNAMICS OF CAPILLARY FLOW

$$\frac{\mathrm{d}l}{\mathrm{d}t} = \frac{(r^2 + 4\epsilon r)}{8\mu} \frac{\left(P_A + gDh + \frac{2\gamma}{r}\cos\theta - gDl\sin\psi\right)}{l}$$

$$= \frac{(r^2 + 4\epsilon r)}{8\mu} \frac{\left(P_A + gDh + \frac{2\gamma}{r}\cos\theta - gD\sin\psi\right)}{l}$$

$$= R\frac{\left(P_R - C_h l\right)}{l} = \frac{RC_h(1 - (C_h/P_R)l)}{(C_h/P_R)l}$$

$$\int_0^l \mathrm{d}l' \, \frac{\mathrm{d}t}{\mathrm{d}l'} \ \Rightarrow RC_h t = -l \ -\frac{1}{(C_h/P_R)} \ln(1 - (C_h/P_R)l)$$



- $\theta = const$
- $\epsilon = \text{const}$
- $\psi = 0, \pi/2$
- $l_s = l$
- $R = \frac{(r^2 + 4\epsilon r)}{8\mu}$
- $P_R = P_A + gDh + \frac{2\gamma}{r}\cos\theta$
- $C_h = gD \sin \psi$

IMBIBITION AND DYNAMICS OF CAPILLARY FLOW

$$RC_h t = -l - \frac{1}{(C_h/P_R)} \ln(1 - (C_h/P_R)l)$$

$$\ln(1 - ax) \approx -ax - \frac{a^2}{2}x^2 + \text{h.o.t}$$

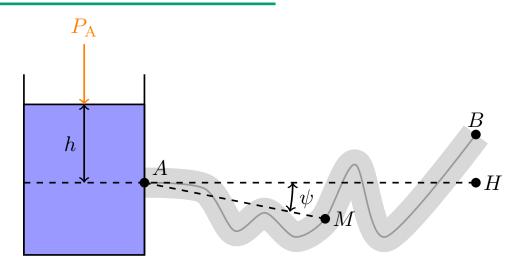
$$\Rightarrow RC_h t = -l + \frac{1}{(C_h/P_R)} \left((C_h/P_R)l + \frac{(C_h/P_R)^2}{2} l^2 \right)$$

$$=\frac{(C_h/P_R)}{2}l^2$$

$$\left(\Rightarrow l^2 = \left(\frac{\gamma \cos \theta}{\mu} \right) rt \right)$$

"Lucas-Washburn Law"

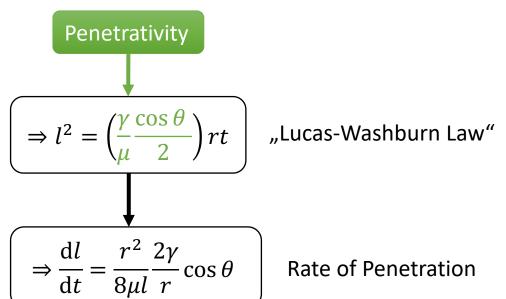
Same result for $\psi = 0$

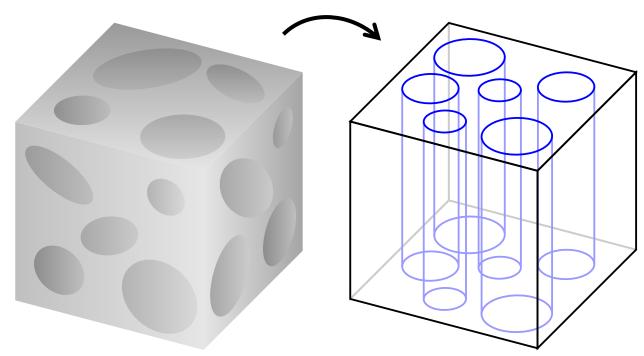


- $\theta = const$
- $\psi = \pi/2$
- $l_s = l$
- $R = \frac{(r^2 + 4\epsilon r)}{8\mu} = \frac{r^2}{8\mu}$
- $P_R = P_A + gDh + \frac{2\gamma}{r}\cos\theta \approx \frac{2\gamma}{r}\cos\theta$
- $C_h = gD \sin \psi = gD$
- $C_h l \ll P_R$

Theory

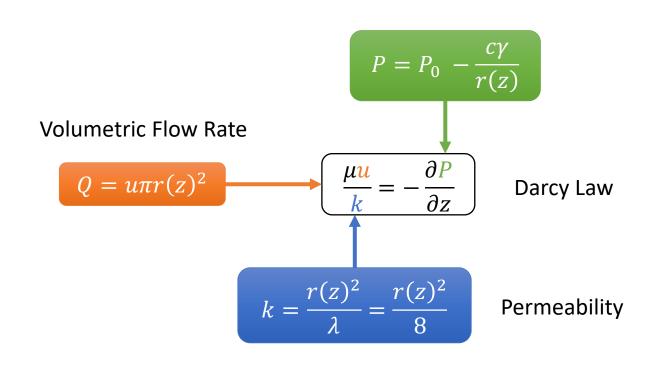
IMBIBITION AND DYNAMICS OF CAPILLARY FLOW



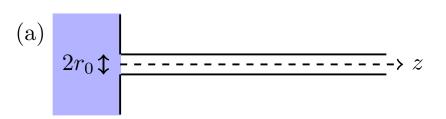


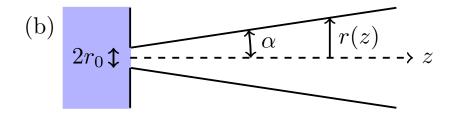
$$\Rightarrow V = \sum_{i=1}^{N} \pi r_i^2 l = \frac{\pi}{2} \left(\frac{t}{\mu}\right)^{1/2} \sum_{i=1}^{N} \left(\frac{2\gamma}{r_i} \cos \theta\right)^{1/2} r_i^3 = S\left(\frac{\gamma}{\mu}\right)^{1/2} t^{1/2}$$

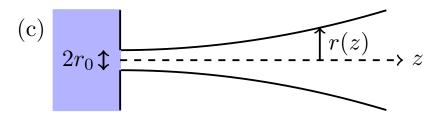
IMBIBITION IN GEOMETRIES WITH AXIAL VARIATIONS IN 3D



$$\Rightarrow \frac{8\mu Q}{\pi r(z)^4} = -\frac{\partial P}{\partial z}$$







Theory

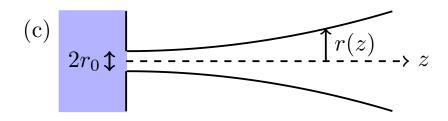
IMBIBITION IN GEOMETRIES WITH AXIAL VARIATIONS IN 3D

$$\frac{8\mu Q}{\pi r(z)^4} = -\frac{\partial P}{\partial z} \qquad \Rightarrow -\int_0^l \mathrm{d}z \, \frac{\partial P}{\partial z} = P_0 - \left(P_0 - \frac{c\gamma}{r(l)}\right) = \frac{c\gamma}{r(l)}$$

(a)
$$2r_0 \updownarrow \xrightarrow{-----} > z$$

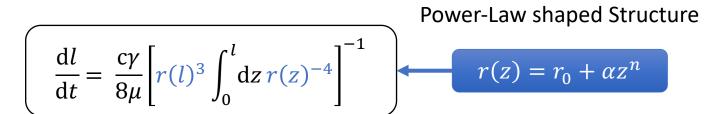
$$\frac{\mathrm{d}l}{\mathrm{d}t} = \frac{Q}{\pi r(l)^2} \longrightarrow \Rightarrow Q = \frac{\mathrm{c}\pi\gamma}{8\mu} \left[r(l) \int_0^l \mathrm{d}z \, r(z)^{-4} \right]^{-1}$$

(b)
$$2r_0 \updownarrow \qquad \qquad \uparrow \alpha \qquad \uparrow r(z) \longrightarrow z$$



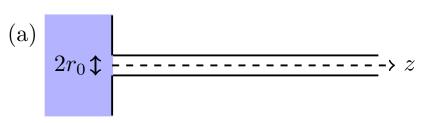
General Imbibition Equation for Invasion into structured Solid in 3D

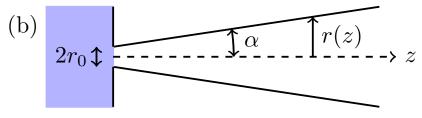
IMBIBITION IN GEOMETRIES WITH AXIAL VARIATIONS IN 3D

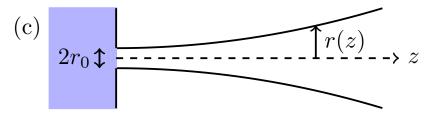


$$\Rightarrow \frac{\mathrm{d}l}{\mathrm{d}t} = \frac{\mathrm{c}\gamma r_0}{8\mu} \left[\left(1 + \frac{\alpha}{r_0} l^n \right)^3 \int_0^l \mathrm{d}z \left(1 + \frac{\alpha}{r_0} z^n \right)^{-4} \right]^{-1}$$

$$\int \frac{\mathrm{d}L}{\mathrm{d}T} = \left[(1 + L^n)^3 \int_0^L \mathrm{d}Z \, (1 + Z^n)^{-4} \right]^{-1}$$







•
$$c(l) = 2\cos\left(\theta + \arctan\left(\frac{dr}{dz}(l)\right)\right) \approx \text{const}$$

•
$$L = (\alpha/r_0)^{1/n}l$$
 and $T = \frac{c\gamma r_0}{8\mu} (\alpha/r_0)^{2/n}t$

Theory

IN GEOMETRIES WITH AXIAL VARIATIONS IN 3D

$$\frac{dL}{dT} = \left[(1 + L^n)^3 \int_0^L dZ (1 + Z^n)^{-4} \right]^{-1}$$

(I)
$$n = 0$$
 $(r(z) = r_0)$: $\Rightarrow L \frac{dL}{dT} \simeq \text{const} \quad \Rightarrow L \sim T^{1/2}$

(II) $n \geq 1$:

"Lucas-Washburn Law"

(i) Short Times:

$$L \ll 1$$
 and $\int_0^L dZ (1 + Z^n)^{-4} \simeq L \implies L \frac{dL}{dT} \simeq \text{const}$ $\implies L \sim T^{1/2}$

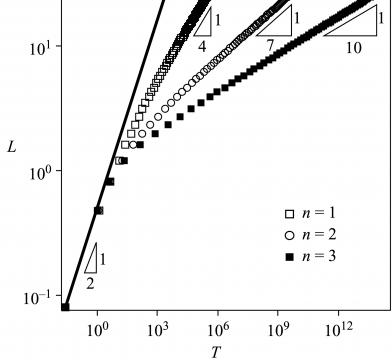


(ii) Long Times:

$$L \gg 1$$
, $(1 + L^n) \simeq L^n$ and

$$\int_0^L dZ (1 + Z^n)^{-4} \approx \int_0^\infty dZ (1 + Z^n)^{-4} = \text{const for } n > 1/4$$

$$\Rightarrow L^{3n} \frac{dL}{dT} \simeq \text{const} \quad \Rightarrow L \sim T^{1/(3n+1)}$$

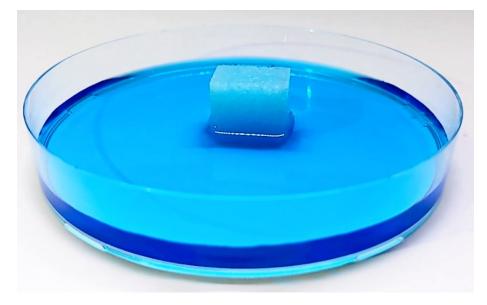


•
$$c(l) = \text{const}$$

•
$$L = (\alpha/r_0)^{1/n}l$$
 and $T = \frac{c\gamma r_0}{8\mu} (\alpha/r_0)^{2/n}t$

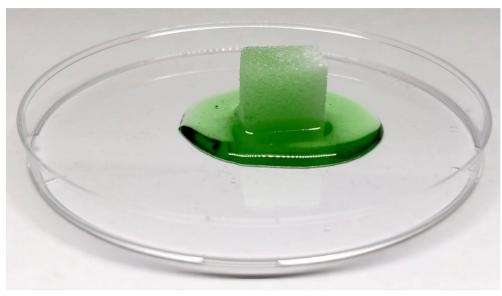
IMBIBITION WITH SUGAR IN WATER AND GLYCERIN

Water



Slowed down with 1s = 0.125s

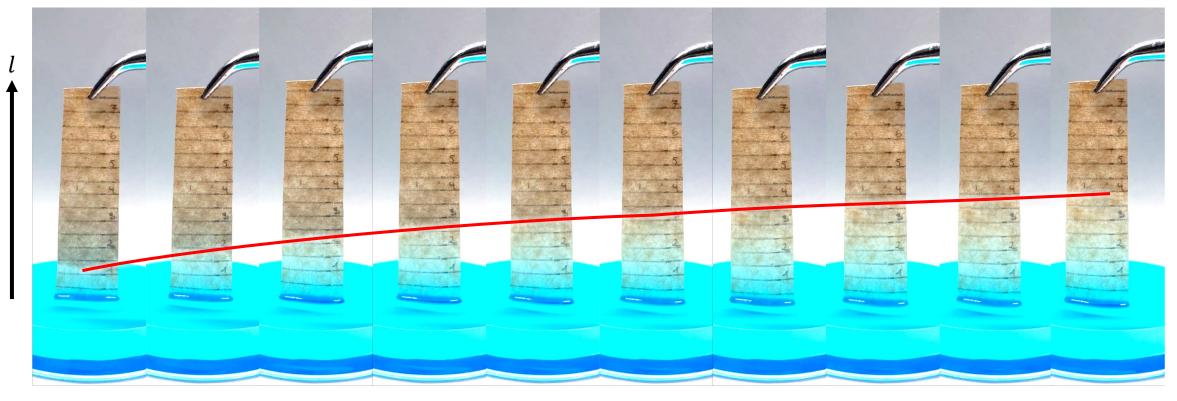
Glycerin



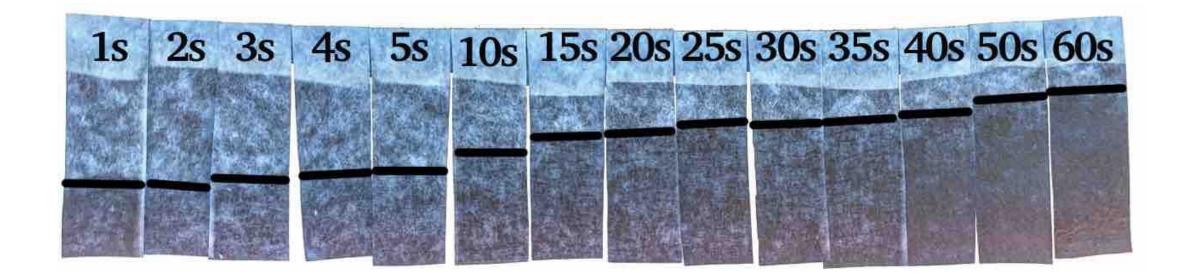
Sped up with 1s = 30s

IMBIBITION WITH FILTER PAPER IN WATER

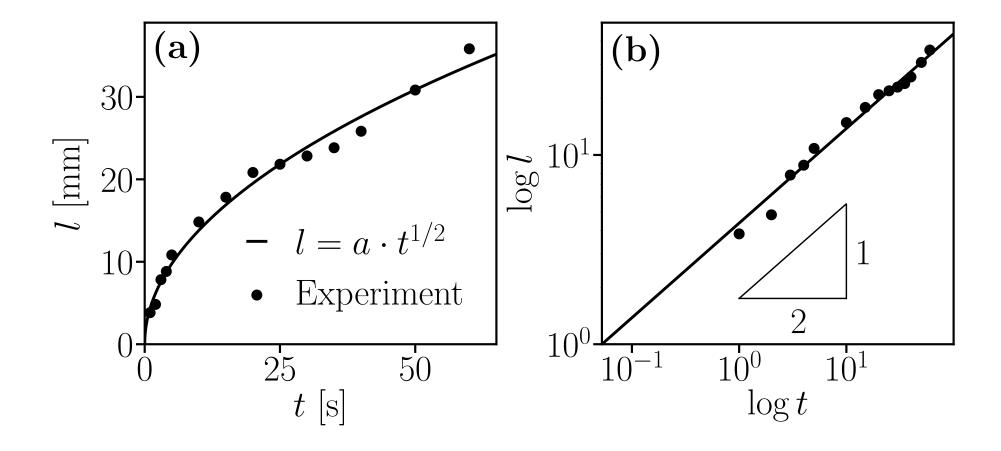
Sped up with 1s = 10s



IMBIBITION WITH FILTER PAPER IN WATER



IMBIBITION WITH FILTER PAPER IN WATER



IMBIBITION: TAKE HOME MESSAGES

- Imbibition is an important process in nature and industry
- Capillarity-driven imbibition can be described by "Lucas-Washburn Law"

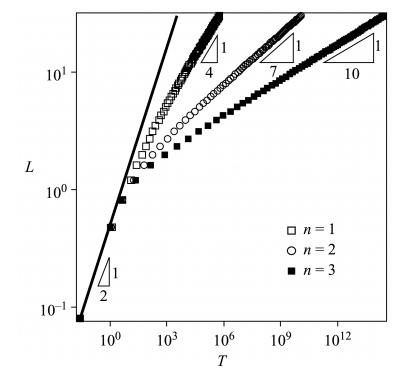
$$l^2 = \left(\frac{\gamma}{\mu} \frac{\cos \theta}{2}\right) rt$$

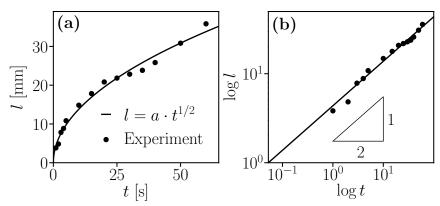
 Varying the geometry of the capillary (3D) results in two time regimes:

$$L \sim T^{1/2}$$
Short times

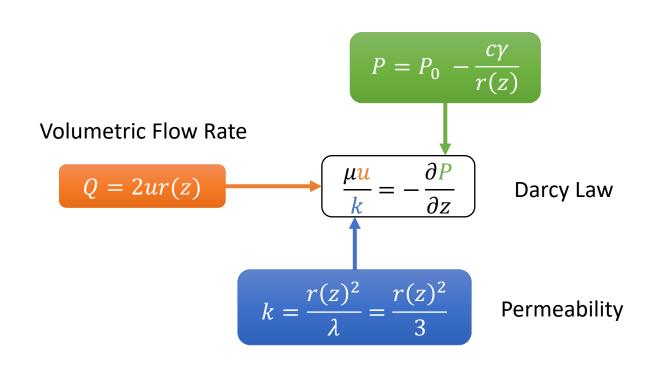
$$L \sim T^{1/(3n+1)}$$
Long times

- The more diverging the geometry, the slower the dynamics become at long time
- Simple experiment with coffee filter paper proofs the "Lucas-Washburn Law"





IMBIBITION IN GEOMETRIES WITH AXIAL VARIATIONS IN 2D



$$\Rightarrow \frac{3\mu Q}{\pi r(z)^3} = -\frac{\partial P}{\partial z}$$

$$\Rightarrow \frac{\mathrm{d}l}{\mathrm{d}t} = \frac{\mathrm{c}\gamma}{3\mu} \left[r(l)^2 \int_0^l \mathrm{d}z \, r(z)^{-3} \right]^{-1}$$

$$\Rightarrow \frac{\mathrm{d}L}{\mathrm{d}T} = \left[(1 + L^n)^2 \int_0^L \mathrm{d}Z \, (1 + Z^n)^{-3} \right]^{-1}$$

$$L\sim T^{1/2}$$

Short times

$$L \sim T^{1/(2n+1)}$$

Long times

•
$$c(l) = \text{const}$$

•
$$L = (\alpha/r_0)^{1/n}l$$
 and $T = \frac{c\gamma r_0}{8\mu} (\alpha/r_0)^{2/n}t$

WHY c(l) IS CONSTANT?

$$c(\ell) \propto \cos\left(\theta_e + \arctan\left(\frac{\mathrm{d}h}{\mathrm{d}z}(\ell)\right)\right),$$
 (A1)

Let us consider the profile $h(z) = h_0 + \alpha z^n$, with n > 1. The lubrication theory requirement $(dh/dz \ll 1)$ leads to the simplification $\arctan(dh/dz(\ell)) \simeq dh/dz(\ell) = n\alpha \ell^{n-1}$. If we now consider a completely wetting case with $\theta_e \ll 1$,

$$c \propto 1 - \frac{n^2}{2} \alpha^2 \ell^{2n-2} + \cdots \tag{A 2}$$

The approximation $c \simeq \text{constant}$ can then hold if $n^2 \alpha^2 \ell^{2n-2} \ll 1$, i.e.

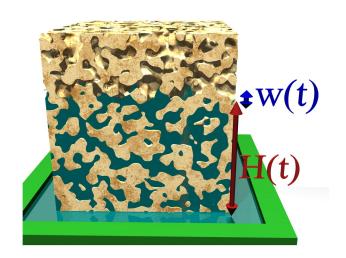
$$\ell \ll \left(\frac{1}{\alpha n}\right)^{1/(n-1)}.\tag{A3}$$

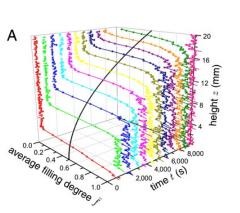
On the other hand, we know that the cross-over time between the two asymptotic limits occurs on a length scale $L \simeq 1$ or $\ell \simeq (h_0/\alpha)^{1/n}$. Thus, the approximation $c \simeq$ constant remains valid if

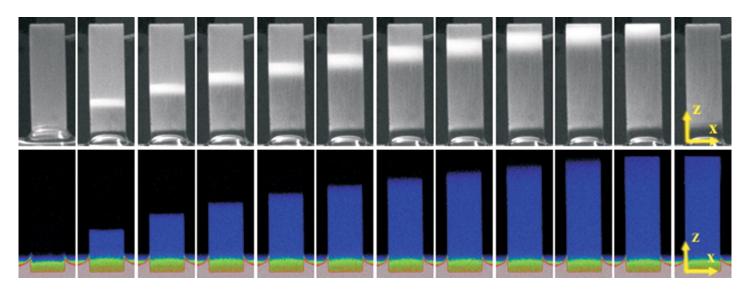
$$\left(\frac{h_0}{\alpha}\right)^{1/n} \ll \left(\frac{1}{\alpha n}\right)^{1/(n-1)} \quad \text{or} \quad h_0 \ll (\alpha n^n)^{1/(1-n)}. \tag{A4}$$

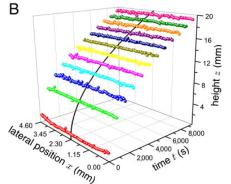
We assume the cases considered here to be under this condition.

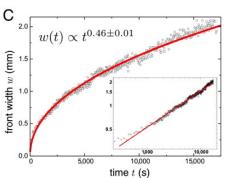
IMBIBITION EXPERIMENTS WITH VYCOR GLASS











OUTTAKES

