iapws Documentation

Release 0.1.0

M. Skocic

CONTENTS:

GETTING STARTED

1.1 iapws library

ipaws is a Fortran library providing the formulas for computing light and heavy water properties. It also provides a API for the C language. The formulations are taken from http://iapws.org. A shared and a static library *libiapws* are compiled (f2008+) with the Fortran and C headers. The static and shared libraries can be installed in order to be included in Fortran or C programs.

The compilation was tested on Linux (Debian), MacOS and Windows.

Links:

- Sources: https://github.com/MilanSkocic/iapws.

- Online documentation: https://milanskocic.github.io/iapws/index.html.

- PDF documentation: `iapws`.

1.1.1 How to install

Create build directory

```
$ mkdir build
$ d build
```

Generate a makefile

- On Unix-like OS:

```
cmake -G "Unix Makefiles" -S .. -DCMAKE_BUILD_TYPE=release -DCMAKE_INSTALL_PREFIX=/
↪path/to/folder
```

- On windows with MSYS2:

```
cmake -G "Unix Makefiles" -S .. -DCMAKE_BUILD_TYPE=release -DCMAKE_INSTALL_PREFIX=/
↪path/to/folder
```

- On windows with ifort and msvc:

```
cmake -G "NMake Makefiles" -S .. -DCMAKE_BUILD_TYPE=release -DCMAKE_INSTALL_PREFIX=/
↪path/to/folder
```

Build

```
cmake --build .
```

Run tests

```
ctest
```

Install

```
cmake --install .
```

1.1.2 Dependencies

```
gcc>=4.6 or msvc>=14

gfortran>=4.6 or ifort>=18

cmake>=3.10
```

1.1.3 License

```
GNU General Public License v3 (GPLv3)
```

1.2 Python wrapper pyiapws

Python wrapper around the Fortran iapws library. Follow the installation instructions. for compiling and installing the library.

For now,the wrapper must be compiled on Linux, windows and MacOS platforms after installing the iapws library using the compiler that was used to compile your python interpreter.

1.2.1 How to install

```
pip install pyiapws
```

1.2.2 Dependencies

```
numpy>=1.20
```

1.2.3 License

```
GNU General Public License v3 (GPLv3)
```

1.3 Examples

1.3.1 Example in Fortran

```
program example_in_f
    use iso_fortran_env
    use iapws
    implicit none
```

(continues on next page)

```fortran
    real(real64) :: kh, kd
    character(len=5) :: gas = "O2"
    character(len=5) :: solvent = "H2O"
    real(real64) :: T = 25.0d0

    kh = iapws_kh(T, gas, solvent)
    print "(A10, 1X, A10, 1X, A2, F10.1, A, 4X, A3, SP, F10.4)", "Gas=", gas, "T=", T,
→ "C", "kh=", kh

    kd = iapws_kd(T, gas, solvent)
    print "(A10, 1X, A10, 1X, A2, F10.1, A, 4X, A3, SP, F15.4)", "Gas=", gas, "T=", T,
→ "C", "kh=", kd

end program
```

1.3.2 Example in C

```c
#include <string.h>
#include <stdio.h>
#include "iapws.h"

int main(int argc, char **argv){

    double T = 25.0; /* in C*/
    char *gas = "O2";
    char *solvent = "H2O";
    double kh, kd;

    if(argc > 1 ){
        printf("%s\n", argv[1]);
    }

    kh = iapws_capi_kh(T, gas, solvent, strlen(gas), strlen(solvent));
    printf("Gas=%s\tT=%fC\tkh=%+10.4f\n", gas, T, kh);

    kd = iapws_capi_kd(T, gas, solvent, strlen(gas), strlen(solvent));
    printf("Gas=%s\tT=%fC\tkd=%+15.4f\n", gas, T, kd);

    return 0;
}
```

IAPWS - THEORETICAL BACKGROUND

2.1 IAPWS G7-04

The computation is based on the parameters provided by the IAPWS 2004 [1].

2.1.1 Henry Contant: kh

The Henry constant kH is defined as shown in equation Eq.2.1.1.

$$k_H = \lim_{x_2 \to 0} f_2/x_2 \tag{2.1.1}$$

- f_2: liquid-phase fugacity

- x_2: mole fraction of the solute

The Henry's constant k_H is given as a function of temperature by:

$$\ln\left(\frac{k_H}{p_1^*}\right) = A/T_R + \frac{B \cdot \tau^{0.355}}{T_R} + C \cdot T_R^{-0.41} \cdot \exp\tau \tag{2.1.2}$$

- $\tau = 1 - T_R$

- $T_R = T/T_{c1}$

- T_{c1}: critical temperature of the solvent as recommended by IAPWS [2] (647.096 for H2O and 643.847 K for D2O)

- p_1^* is the vapor pressure of the solvent at the temperature of interest and is calculated from the correlation of Wagner and Pruss for H2O [3] and from the correlation of Harvey and Lemmon for D2O [4].

Both equations have the form:

$$\ln\left(p_1^*/p_{c1}\right) = T_R^{-1} \sum_{i=1}^{n} a_i \tau^{b_i} \tag{2.1.3}$$

- n is 6 for H2O and 5 for D2O

- p_{c1} is the critical pressure of the solvent recommended by IAPWS [2] (22.064 MPa for H2O and 21.671 MPa for D2O)

The Henry's constant k_H has a dimension of pressure expressed here in GPa^{-1}.

2.1.2 Vapor-Liquid Distribution Constant: kd

The liquid-vapor distribution constant kD is defined as shown in equation Eq.2.1.4.

$$k_D = \lim_{x_2 \to 0} y_2/x_2 \tag{2.1.4}$$

- x_2: mole fraction of the solute

- y_2 is the vapor-phase solute mole fraction in equilibrium with the liquid

The vapor-liquid distribution constant k_D is given as a function of temperature by:

$$\ln K_D = qF + f(\tau) + (F + G\tau^{2/3} + H\tau)\exp\left(\frac{273.15 - T(K)}{100}\right) \tag{2.1.5}$$

- q : -0.023767 for H2O and -0.024552 for D2O.

- $f(\tau)$ [3] for H2O and [5] for D2O.

In both cases, $f(\tau)$ has the following form:

$$f(\tau) = \sum_{i=1}^{n} c_i \cdot \tau^{d_i} \tag{2.1.6}$$

- n is 6 for H2O and 4 for D2O

2.1.3 Molar fractions

$$x_2 = \frac{1}{k_H}$$
$$y_2 = \frac{k_D}{k_H} \tag{2.1.7}$$

RELEASE NOTES

3.1 iapws 0.1.0 Release Note

3.1.1 Changes

- Implementation of kH and kD from IAPWS G7-04 in fortran + C API
- Python wrapper for kH and kD.

3.1.2 Download

iapws

pyiapws

3.1.3 Contributors

Milan Skocic

3.1.4 Commits

Full Changelog: https://github.com/MilanSkocic/pyiapws/compare/. . .0.1.0

AUTOGENERATED DOCUMENTATION

4.1 iapws library

namespace `iapws`

Main module for IAPWS computations.

Functions

pure real(real64) function, public iapws_kh (t, gas, solvent)

Compute the henry constant for a given temperature and gas in solvent.

> **Parameters**
> - **T** – **[in]** Temperature in °C.
> - **gas** – **[in]** Gas.
> - **solvent** – **[in]** Solvents: H2O or D2O. Default is H2O.
>
> **Returns**
> kh Henry constant in mole fraction per GPa. NaN if gas not found.

pure real(real64) function, public iapws_kd (t, gas, solvent)

Compute the vapor-liquid constant for a given temperature and gas in solvent.

> **Parameters**
> - **T** – **[in]** Temperature in °C.
> - **gas** – **[in]** Gas.
> - **solvent** – **[in]** Solvents: H2O or D2O. Default is H2O.
>
> **Returns**
> kd Vapor-liquid constant. NaN if gas not found.

namespace `iapws_capi`

C API for the IAPWS module.

Functions

real(c_double) function, public iapws_capi_kh (t, gas, solvent, size_gas, size_solvent)

> Compute the henry constant for a given temperature and gas in solvent.
>
> > **Parameters**
> >
> > - **T** – **[in]** Temperature in °C.
> > - **gas** – **[in]** Gas.
> > - **solvent** – **[in]** Solvents: H2O or D2O. Default is H2O.
> > - **size_gas** – **[in]** Length of the string gas.
> > - **size_solvent** – **[in]** Length of the string gas.
> >
> > **Returns**
> >
> > kh Henry constant in mole fraction per GPa. NaN if gas not found.

real(c_double) function, public iapws_capi_kd (t, gas, solvent, size_gas, size_solvent)

> Compute the vapor-liquid constant for a given temperature and gas in solvent.
>
> > **Parameters**
> >
> > - **T** – **[in]** Temperature in °C.
> > - **gas** – **[in]** Gas.
> > - **solvent** – **[in]** Solvents: H2O or D2O. Default is H2O.
> > - **size_gas** – **[in]** Length of the string gas.
> > - **size_solvent** – **[in]** Length of the string gas.
> >
> > **Returns**
> >
> > kd Vapor-Liquid constant. NaN if gas not found.

4.2 Python wrapper

IAPWS computations.

pyiapws.iapws.**kd**(*temperature: int | float | ndarray[Any, dtype[ScalarType]]*, *gas: str*, *solvent: str*) → float | ndarray[Any, dtype[ScalarType]]

> Compute the vapor-liquid distribution constant for the gas and solvent at temperature.
>
> > **Parameters**
> >
> > **temperature: int, float or array-like.**
> > > Temperature in °C.
> >
> > **gas: str**
> > > Desired gas.
> >
> > **solvent: str**
> > > Desired solvent: H2O or D2O.
> >
> > **Returns**
> >
> > **kd: float or array-like**
> > > Henry constant in GPa-1.

---

pyiapws.iapws.**kh**(*temperature:* *int* | *float* | *ndarray[Any, dtype[ScalarType]]*, *gas:* *str*, *solvent:* *str*) → float | ndarray[Any, dtype[ScalarType]]

> Compute the Henry constant for the gas and solvent at temperature.

> > **Parameters**

> > > **temperature: int, float or array-like.**
> > > > Temperature in °C.

> > > **gas: str**
> > > > Desired gas.

> > > **solvent: str**
> > > > Desired solvent: H2O or D2O.

> > **Returns**

> > > **kh: float or array-like**
> > > > Henry constant in GPa-1.

BIBLIOGRAPHY

INDICES AND TABLES

- genindex
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[5] R. Fernandez-Prini, J.L. Alvarez, and A.H. Harvey. Henry's Constants and Vapor–Liquid Distribution Constants for Gaseous Solutes in H2O and D2O at High Temperatures. *Journal of Physical Chemistry Reference Data*, 32(2):903–916, 2003.

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