

Training Session 3: TRANSFORM Advanced I

M. Scott Greenwood, PhD

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U.S. DEPARTMENT OF
ENERGY

TRANSFORM Advanced I (60 Minutes)

- Create a model of a force-flow reactor model using TRANSFORM (60 min)

Grab Bag:

- Some random, important information



Parameter GUI: “Inputs” group

- Time dependent inputs use generally use GUI rather than connector
 - To maintain flexibility in application
 - While reducing number of “connections” (lines all over the screen)
 - Allows a wide variety of applications to be supported

plane in TRANSFORM.HeatAndMassTransfer.Examples.ResistanceCheck

General Visualization Add modifiers Attributes

Component

Name

Comment

Model

Path TRANSFORM.HeatAndMassTransfer.Resistances.Heat.Plane

Comment Plane Wall

Icon

Plane

Inputs

L	<input type="text"/>	m	Wall thickness parallel to heat flow
crossArea	<input type="text"/>	m ²	Cross-sectional area perpendicular to heat flow
lambda	<input type="text"/>	W/(m·K)	Thermal conductivity

OK Cancel Info

Hands-On Examples:

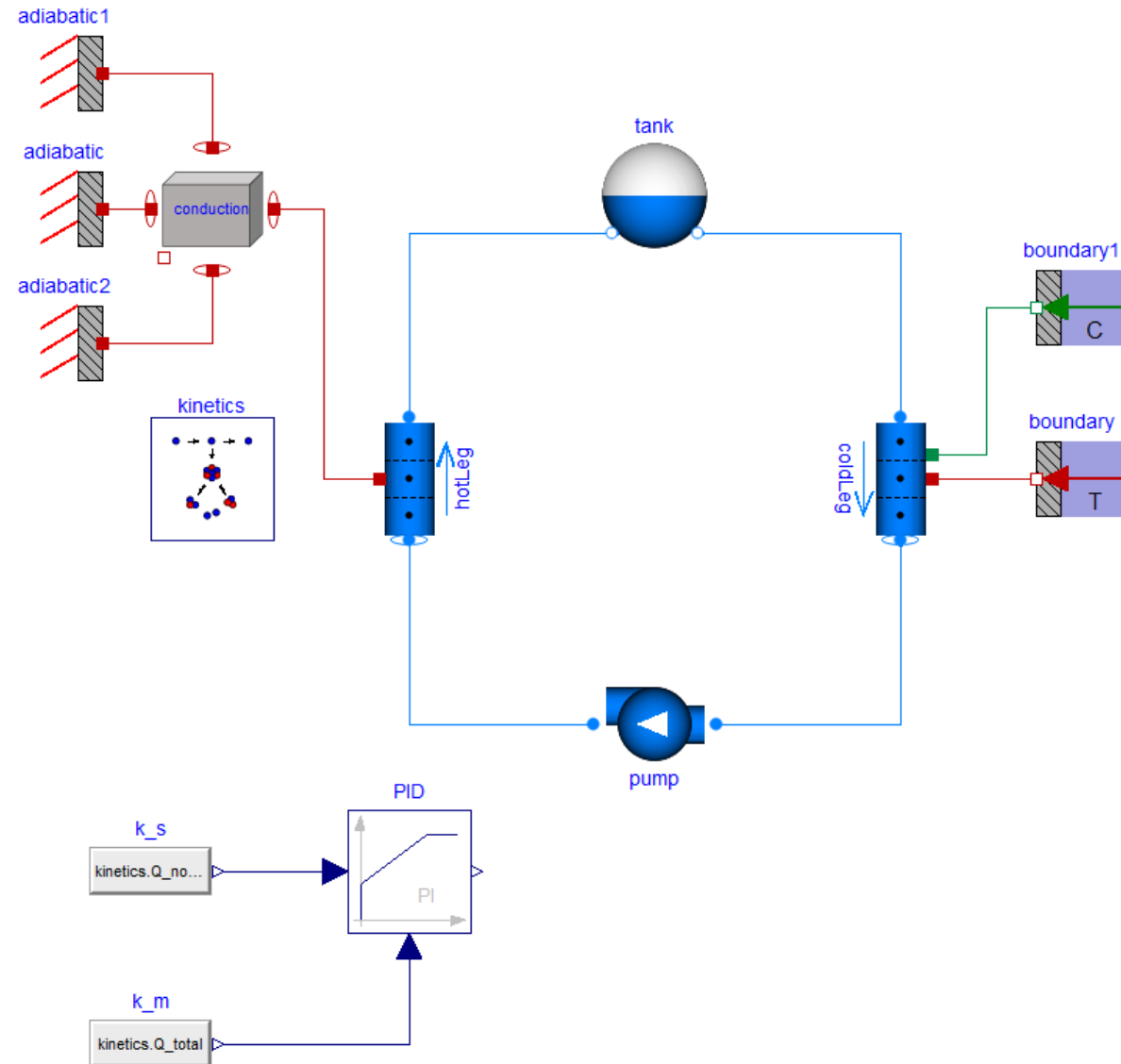
Create a Reactor Model

- Steps to create a simple model and gradually make it more complex



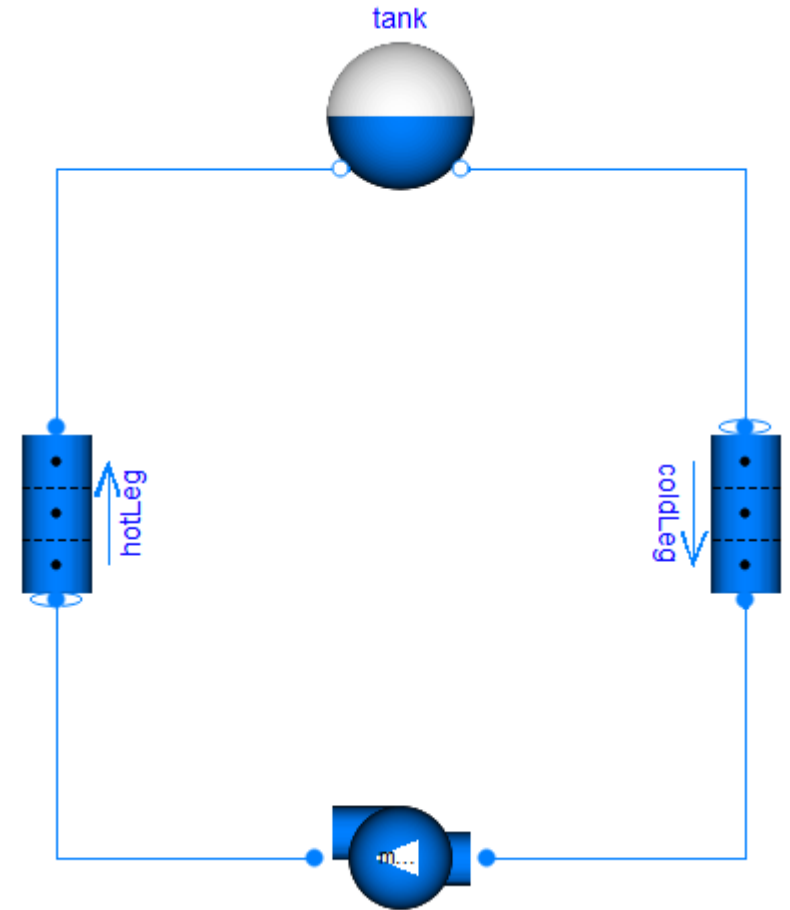
Example: Loopty Loop

- Goal:
 - Using TRANSFORM components, create a forced flow reactor model with:
 - Nuclear heating
 - Level indicators
 - Pump curves
 - PID control
 - Heat transfer



Step 1: Add base components

1. Add a new model to your packager
2. Add 2 pipes to the model
 - `TRANSFORM.Fluid.Pipes.GenericPipe_MultiTransferSurface`
3. Add a tank. Why do we need this?
 - `TRANSFORM.Fluid.Volumes.ExpansionTank`
4. Add a pump
 - `TRANSFORM.Fluid.Machines.Pump_SimpleMassFlow`
5. Connect components like in the picture



Tips:

- While selecting a component, click “H”, “V”, or “ctrl+R” to flip horizontally, vertically, or rotate.
- In the editor, click “ctrl+A” to select all and then “ctrl+shift+L” to autoformat code. May have to do twice.

Step 2: Specify parameters

1. Select both pipes.

- Specify `diameter = 2"` with `nV = 4`
- Under "Initialization" tab set `p_start = 1 bar`, `T_a_start = 50°C`, and `m_flow_a_start = 1 kg/s`

2. For "coldLeg" pipe only, under "Advanced" tab specify

- `exposeState_a = false`
- `exposeState_b = true`

3. Select the tank.

- Set tank `area` based on a 1' pipe ($A=\pi r^2$)
- Set `level_start = 1 m`, `p_start = 1 bar`, and `h_start` based on $p = 1 \text{ bar}$ and $T = 50^\circ\text{C}$
 - `h_start = tank.Medium.specificEnthalpy_pT(tank.p_start, 50 + 273.15)`

4. Select the pump

- Set `m_flow_nominal = 1 kg/s`

5. Select all components.

- Set `Medium = Modelica.Media.Water.StandardWater`

Statistics
Original Model
Number of components: 189
Variables: 1641
Constants: 62 (62 scalars)
Parameters: 298 (357 scalars)
Unknowns: 1281 (1761 scalars)
Differentiated variables: 44 scalars
Equations: 823
Nontrivial: 628
Translated Model
Constants: 881 scalars
Free parameters: 58 scalars
Parameter depending: 102 scalars
Continuous time states: 26 scalars
Time-varying variables: 334 scalars
Alias variables: 805 scalars
Assumed default initial conditions: 18
Number of mixed real/discrete systems of equations: 0
Sizes of linear systems of equations: {2, 2, 2, 2, 2, 2, 2, 2}
Sizes after manipulation of the linear systems: {0, 0, 0, 0, 0, 0, 0, 0}
Sizes of nonlinear systems of equations: {}
Sizes after manipulation of the nonlinear systems: {}
Number of numerical Jacobians: 0

```
Integration started at T = 0 using integration method DASSL
(DAE multi-step solver (dassl/dasslrt of Petzold modified by Das
Integration terminated successfully at T = 100
CPU-time for integration           : 0.168 seconds
CPU-time for one grid interval    : 0.336 milliseconds
CPU-time for initialization       : 0.002 seconds
Number of result points          : 502
Number of grid points            : 501
Number of accepted steps         : 76
Number of f-evaluations (dynamics) : 158
Number of crossing function evaluations : 576
Number of Jacobian-evaluations   : 54
Number of model time events      : 0
Number of input time events      : 0
Number of state events           : 0
Number of step events            : 0
Minimum integration stepsize     : 1.69e-010
Maximum integration stepsize     : 37.6
Maximum integration order        : 1
```

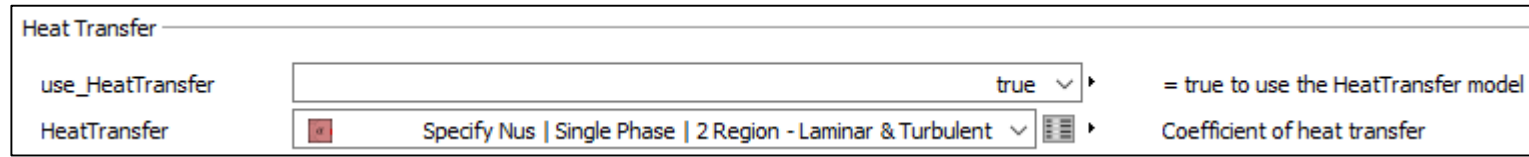
Tips:

- While in code editor or in a parameter GUI, click "ctrl+SPACE" to get autocomplete

Step 3: Add heat transfer

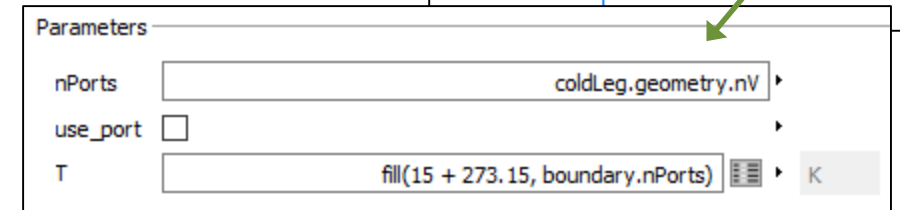
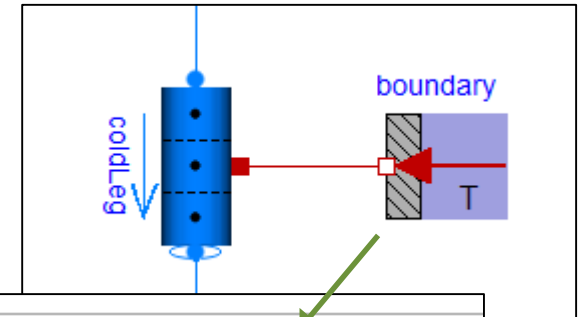
1. Select the coldLeg pipe

- Turn on heat transfer and select a heat transfer correlation
- Add multi-node temperature boundary
 - `TRANSFORM.HeatAndMassTransfer.BoundaryConditions.Heat.Temperature_multi`



2. Select the hotLeg pipe

- Add 10 kW of internal heating to each volume



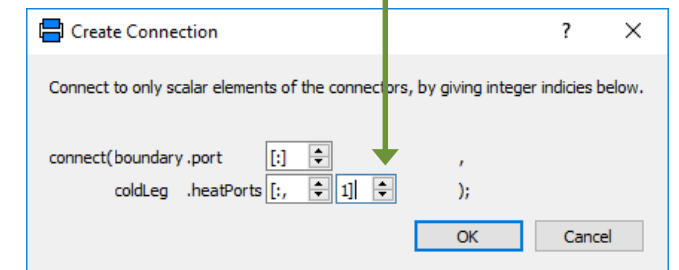
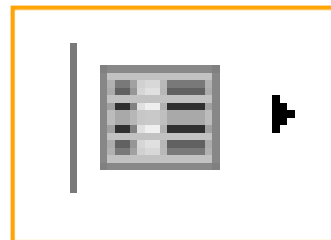
3. Simulate for 10,000 seconds

4. Run plot_FlowLoop_Step_3.mos

5. Change `boundary.T` back to default.

- Can you explain the behavior observed?

Specify the first heat transfer surface



Tips:

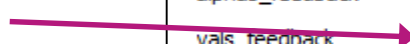
- Check model early and often!!!

Step 4: Add nuclear kinetics

1. Add a nuclear kinetics component to the model
 - `TRANSFORM.Nuclear.ReactorKinetics.PointKinetics_L1_powerBased`
 - Set `Q_nominal = 40 kW`
 - Set a temperature feedback ("kinetics" tab) based on hotLeg effective temperature
2. Change the internal heat generation in the hotLeg
 1. Set `Q_gen = kinetics.Q_total/4`
3. Simulate. What just happened!?
4. Try easing the reactor with some simple logic
 - Modify `vals_feedback` to have a time delay
5. Simulate. Is the issue fixed?

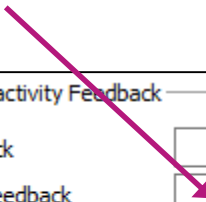
Inputs: Reactivity Feedback

nFeedback	<input type="text" value="1"/>	▶
alphas_feedback	<input type="text" value="{ -2.5e-5 }"/>	▶
vals_feedback	<input type="text" value="{hotLeg.summary.T_effective}"/>	▶
vals_feedback_reference	<input type="text" value="{92.67 + 273.15}"/>	▶



Inputs: Reactivity Feedback

nFeedback	<input type="text" value="1"/>	▶
alphas_feedback	<input type="text" value="{ -2.5e-5 }"/>	▶
vals_feedback	<input type="text" value="{if time < 5000 then kinetics.vals_feedback_reference[1] else hotLeg.summary.T_effective}"/>	▶
vals_feedback_reference	<input type="text" value="{92.67 + 273.15}"/>	▶



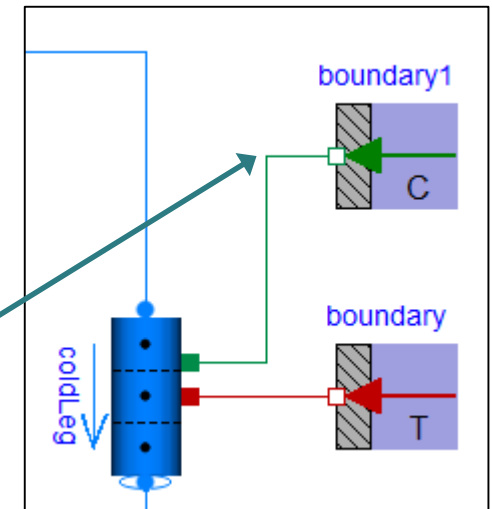
Tips:

- Autocomplete in the GUI only works if no other text exists beyond the cursor

Step 5: Add and remove a trace component

```
model FlowLoop_Step_5 "Add nuclear heating"  
  
package Medium = Modelica.Media.Water.StandardWater(extraPropertiesNames={"Tritium"});
```

1. Need to modify the media to indicate an extra substance
 - Add to the code side the following line
 - `package Medium = Modelica.Media.Water.StandardWater(extraPropertiesNames={"Tritium"});`
 - Select all fluid components and change media to "Medium"
2. In the hotLeg InternalTraceGen model
 - Set `mC_gen = {1e-4*kinetics.Q_total} -/s`
 - Trace components are unitless. "-" can mean whatever the user desires (e.g., atoms)
3. In the coldLeg, turn on mass transfer
 - Set mass transfer to specify `alphaM`
 - Set `D_ab0 = 1` and `alphaM0 = {1000}`
4. Add a multi-node concentration boundary
 - `TRANSFORM.HeatAndMassTransfer.BoundaryConditions.Mass.Concentration_multi`
 - Default values are fine
5. Simulate. Can you see your substance in the system?
 - Search in variable browser for `mC`

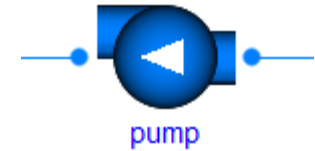


Tips:

- The Dymola simulation search permits the use of wild cards "*". Use it!

Step 6: Change pump component

1. Right click the pump and select “Change Class”
2. Select “Pump_Controlled”
3. In the pump component
 - Set $p_{a_start} = 1$ bar, $p_{b_start} = 1.1$ bar
 - Set $T_{a_start} = 50^{\circ}\text{C}$ and $m_{flow_start} = 1$ kg/s
4. Simulate. What changed and why?
5. In the pump change “controlType” from “RPM” to “m_flow”
6. Simulate. What changed and why?

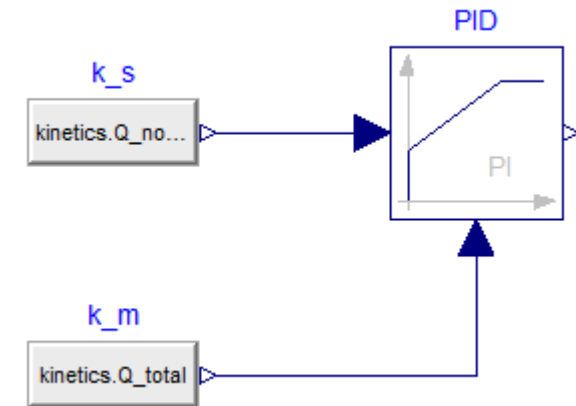


Tips:

- Using GUI to change component names will update all references to it.
- Update variable using the Edit>Variables for all uses to be updated as well.

Step 7: Use controller to alter power behavior

1. Drag a PID component in the model
 - `TRANSFORM.Controls.LimPID`
 - Set `controllerType = PI`
 - Set `k_s` and `k_m = 1/kinetics.Q_nominal`
 - Set `k = 1e-5`
2. Add 2 real expression inputs into the model
 - `Modelica.Blocks.Sources.RealExpression`
 - Connect them to the PID
 - Set the one connected to `k_s` equal to `kinetics.Q_nominal`
 - Set the one connected to `k_m` equal to `kinetics.Q_total`
3. Set `kinetics.rho = PID.y`
4. Simulate. What happened?
5. Remove the “if then” logic from `vals_feedback`
6. Simulate. Much better now, yes?



Inputs: Reactivity Feedback	
nFeedback	1
alphas_feedback	{-2.5e-5}
vals_feedback	{hotLeg.summary.T_effective}
vals_feedback_reference	{92.67 + 273.15}

Tips:

- Hover over connections to get connector information

Step 8: Include a solid heating element (e.g., fuel)

1. Turn on heat transfer in the hotLeg
2. Turn off internal heat generation
3. Drag a 2D Conduction component into the model
 - `TRANSFORM.HeatAndMassTransfer.DiscretizedModels.Conduction_2D`
 - Under “Advanced” tab set all `exposeStates* = true`
 - Under “Initialization” tab and set temperatures 50°C
 - Set geometry as shown
 - Under “InternalHeatModel”
 - Set $Q_{gen} = \text{kinetics.Q_total} / (\text{conduction.geometry.nX} * \text{conduction.geometry.nY})$
 - Set Material to SS316
4. Drag 3 adiabatic multi-node boundary conditions into the model
 - `TRANSFORM.HeatAndMassTransfer.BoundaryConditions.Heat.Adiabatic_multi`
 - Set “adiabatic” `nPorts = conduction.geometry.nY` and the other two to `nX`
5. Connect models as shown

Heat Transfer

use_HeatTransfer ☐ true ▾ = true to use the HeatTransfer model

HeatTransfer ☐ Specify Nus | Single Phase | 2 Region - Laminar & Turbulent ▾ Coefficient of heat transfer

Parameters

nX ▾

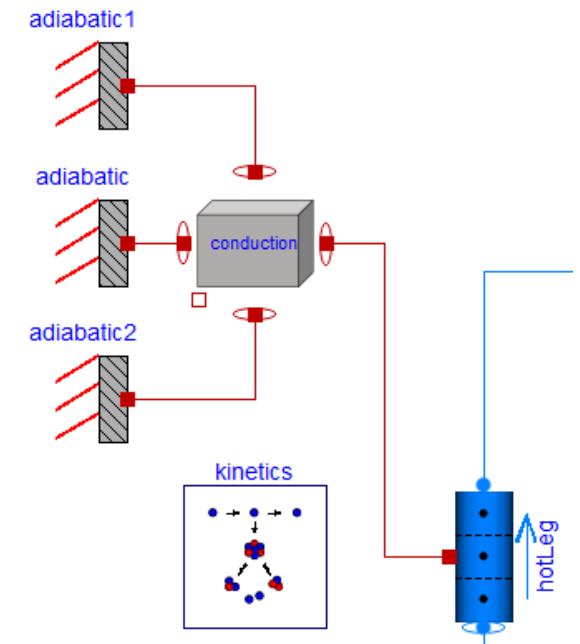
nY ▾

Inputs

length_x m Specify

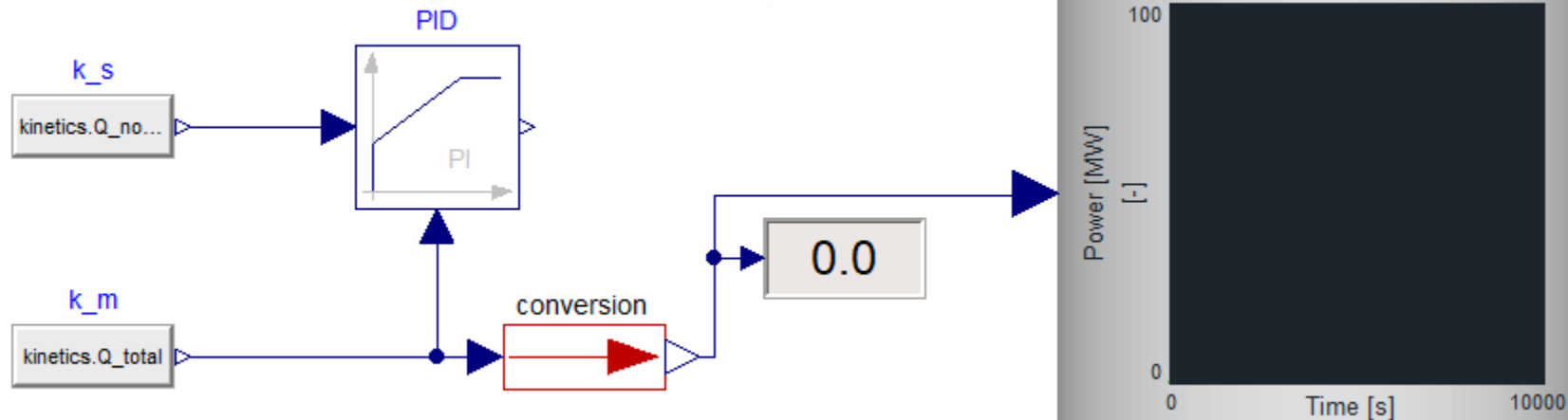
length_y m Specify

length_z m Specify




Step 9: Add Visual Components

1. Add the following to the model and connect
 - `TRANSFORM.Utilities.Visualizers.DynamicGraph`
 - `TRANSFORM.Utilities.Visualizers.displayReal`
 - `TRANSFORM.Units.Conversions.Models.Conversion`
2. For conversion, set `to_kilo`
3. In plot, set `y_max = 100` and `t_end = 10,000`
4. Under the coldLeg and hotLeg components
 - Under “Visualization” tab turn on `show_colors`
 - Set `val_min = 40°C` and `val_max = 100°C`
 - Careful with the units!

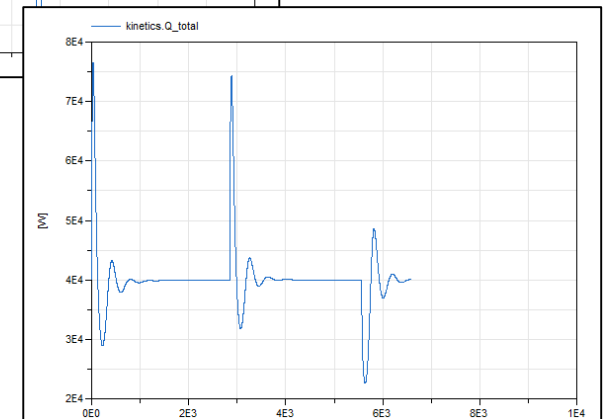
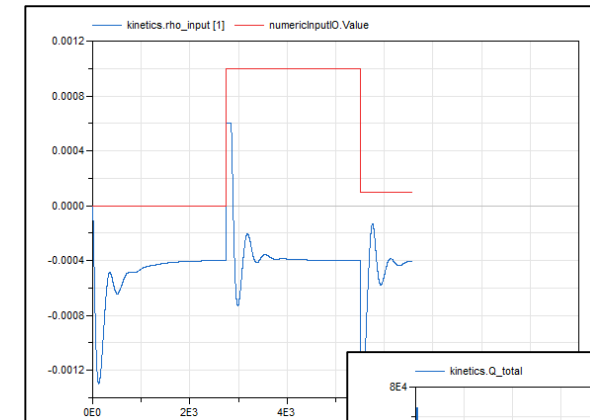


Step 10: Add Realtime User Input

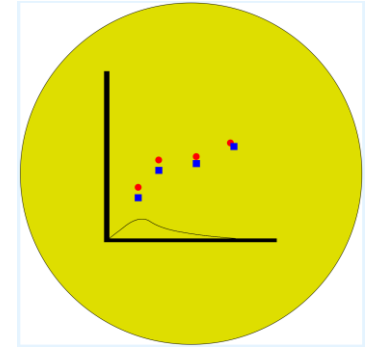
1. Add a user input to the model
 - `UserInteraction.Inputs.NumericInputIO`
2. Add the input value to the kinetic model
3. Switch to the simulation view
4. Open the model viewer 
5. Under simulation settings
 - “Realtime” tab – set settings
 - “Compiler” tab – select DDE server
6. Simulate and plot `kinetics.Q_total` and `kinetics.rho`
7. Change the input value and press enter. What happened?

Inputs

Q_fission_input	Q_nominal	W
Q_external	0	W
rho_input	PID.y + numericInputIO.Value	1



Step 11: Add Unit Test



1. Add unit test checker to model
 - `TRANSFORM.Utilities.ErrorAnalysis.UnitTests`
2. In unitTest parameter GUI assign one or more variables to **x**
3. Simulate to ensure everything is working
4. Open python/Spyder and
 - Run `createUnitScripts.py`
 - Run `regTestsWin_customBuildPy.py`
 - May require custom buildingspy regression script from ModelicaPy (see Session 4)
 - Select “y” if prompted
5. Check the **Resources** folder. What happened?

Step 12: Extend/Modify TRANSFORM – Heat Transfer

1. Create a new package in TRANSFORM_Training_2019 called **HeatTransfer**
2. Duplicate the used correlation into the new **HeatTransfer** package with a modified name and description
 - `TRANSFORM.Fluid.ClosureRelations.HeatTransfer.Models.DistributedPipe_1D_MultiTransferSurface.Nus_SinglePhase_2Region`
3. Replace Nu_DittusBoelter with Nu_SiederTate
 - Check the heat transfer model. What is missing?
4. Change the **hotLeg** correlation to the new correlation
5. Simulate. What changed?
 - Use the compare feature to view the difference in effective solid temperature
 - `conduction.summary.T_effective`

Step 13: Read results in Python/Matlab

Python

- Example in TRANSFORM Resources folder
- Install buildingspy: `pip install buildingspy`
- Change directory to location of '.mat'
- Create notebook or python file and add:

```
from buildingspy.io.outputfile import Reader

r = Reader("MATFILE.mat",'dymola')

time, variable = r.values('VARNAME')
```

Matlab

- Dymola provides useful functions
 - C:\Program Files\Dymola 2020\Mfiles\dymtools
- Example found in Resources folder
- Grab dymget.m and dymload.m from
 - C:\Program Files\Dymola 2020\Mfiles\dymtools

```
% Load the .mat file. If not found see 'err'
for error
[dymstr,err] = dymload(fullPath_mat);
```

```
% Get time variable. Only need to load
once as it is the same for all variables
t = dymget(dymstr,'Time');
```

Step 14: Create an FMU

1. Generate the FMU from the Dymola GUI
2. Open the FMU in FMU Simulator
 - FMPy Github (<https://github.com/CATIA-Systems/FMPy>)
 - Windows Executable: <https://www.3ds.com/products-services/catia/products/dymola/free-downloads/fmu-simulator/>
3. Simulate to ensure everything is working



Free Time

1. Explore capabilities. Try things such as:
 - Adding time dependent signals
 - Make variables dependent on other variables
 - Create summary of variables in the code side...
 - ... or create a “summary” model that you can drag in to populate
 - Add more trace components
 - Add a source/sink for another fluid stream
 - Try to remove the trace component using an ideal sink
 - Try a difference geometry for the conduction model

Tips:

- Try to avoid numerical Jacobians and non-linearities

Thank you.

Scott Greenwood
greenwoodms@ornl.gov

