

OpenFOAM

A little User-Manual

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Abstract

This document is a collection of my own experience on learning and using OpenFOAM. Herein, knowledge and background information is assembled which may be useful to others when learning to use OpenFOAM.

WARNING:

During the assembly of this manual OpenFOAM and other tools, e.g. *pyFoam*, have been continuously updated. This manual was started with OpenFOAM-2.0.x installed and over the time the author has worked with all major point releases of OpenFOAM and the development versions. Consequently it is possible that some parts may be hopelessly outdated by the time you read this. Furthermore, functionalities may have been extended, modified or superseded. Nevertheless, this manual is intended to cast some light on the inner workings of OpenFOAM and explain the usage in a rather practical way.

Furthermore, this document is, and will always be, *work in progress*. As it is extended whenever something interesting is encountered or learned, parts of the document will always be fragmentary. This fragmentary nature and the piecewise work on updating or extending this document may also lead to duplication of information. In the best case, these duplicates do not contradict each other.

All errors and omissions are the sole product of the author.

All information contained in this manual can be found in the internet (<http://www.openfoam.org>, <http://www.cfd-online.com/Forums/openfoam/>); in the source code of OpenFOAM, or it was gathered by trial and error (*What happens if ...?* *Why did that happen?!*). All errors in this manual are the solely the product of the author. The interested reader is invited to contact the author to point out any discovered errors.

Since originally posting this document first on the OpenFOAM Forum of CFD-Online, back in September 2014, several people have reached out to highlight errors in this document and suggest corrections. Thank you for that.

Another note of caution, since this document has been in the works for over a decade now, some parts might be wildly outdated. Please keep that in mind. However, the study of older versions of OpenFOAM and the comparison with the current one, might still provide some benefit to the interested reader.

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1 Getting help

Apart from this manual, there are lots of resources on the internet to find help on OpenFOAM.

- The OpenFOAM User Guide
<http://www.openfoam.org/docs/user/>

- The CFD Online Forum
<http://www.cfd-online.com/Forums/openfoam/>

- The OpenFOAM Wiki
http://openfoamwiki.net/index.php/Main_Page

The OpenFOAM Wiki is maintained by a community of developers behind the OpenFOAM-extend project. This wiki covers not only the OpenFOAM but also tools that developed for OpenFOAM, e.g. *pyFoam* or *swak4foam*.

- The OpenFOAM tutorial collection
<https://wiki.openfoam.com>

This is a community driven effort to collect all the various sources of information, which are all over the internets. This tutorial collection is more of a register of tutorials from various sources. There are two curated lists of tutorials, the first glimpse series and the more in-depth three-weeks series which span a range of topics from the general introduction to quite specific topics. Furthermore, there are also lists of tutorials sorted by topic or by contributor.

- The CoCoons Project

<http://www.cocoons-project.org/>

This is a community driven effort to create a documentation on solvers, utilities and modelling.

- The materials of the course CFD with open source software of Chalmers University

http://www.tfd.chalmers.se/~hani/kurser/OS_CFD/

- The CAELinux Wiki

<http://caelinux.org/wiki/index.php/Doc:OpenFOAM>

CAELinux is a collection of open source CAE software including several CFD codes (OpenFOAM, Code_Saturne, Gerris, Elmer).

- Q&A on the internets

You can find questions – and hopefully answers – on the various Q&A sites on the internets, such as StackExchange (<http://stackexchange.com/>), which is a collection of Q&A site specific to a topic or region of interest.

Currently, OpenFOAM questions tend to get posted on the Computational Science Q&A site.

<http://scicomp.stackexchange.com/>

- Word of mouth

https://github.com/ParticulateFlow/OSCCAR-doc/blob/master/openFoamUserManual_PFM.pdf

This is where this manual is hosted.

2 Lessons learned

- For production-use we strongly recommend to use the point-releases of OpenFOAM. As the development versions of OpenFOAM continuously get updated, OpenFOAM's behaviour might change. Thus, users are advised to base their work entirely on point-releases of OpenFOAM. That way, once your simulation cases run, they will run indefinitely, or as long as you are able to install the respective version of OpenFOAM on a computer.
- Keep an eye on developments in OpenFOAM. A more recent version might provide some functionality or feature you desperately need. Even if you added this feature yourself to e.g. your custom solver or model, the developers of OpenFOAM might provide a cleaner or more powerful implementation of that feature. As it is easily possible to install several versions of OpenFOAM side by side on a computer, play around with the latest version.
- Build the source-code documentation of your local installation. It is located e.g. in `$HOME/OpenFOAM/OpenFOAM-2.3.x/doc/Doxygen` if you installed OpenFOAM in your home directory. This makes you independent of being online and the doxygen gives you e.g. a very well-structured overview of a classes methods and members.
- Study the code. Even as “*the documentation is in the code*” does not sound helpful at all, the code in fact tells you what is going on provided you are able to make sense of the C++ syntax. Become familiar with basic concepts of *object-oriented* (OO) software design.
- The more I used and tinkered with OpenFOAM, the more I am convinced that its design is really ingenious. However, it takes time and effort to come to this conclusion. It is also probably a matter of taste.
- Document your own work and stuff you tried. There is no need to create hundreds of pages, but paper or dead electrons have a longer memory as mere mortal humans. Furthermore, the fact “*I have already tried X at some point in the past, and I wrote it down at Y*” is more likely to be remembered than “*I tried X, and that's how it went in all detail*”.

2.1 Philosophy

OpenFOAM is largely following the general rules of the UNIX philosophy – see e.g. Eric S. Raymond [22] or <http://www.catb.org/esr/writings/taoup/html/ch01s06.html> – by accident, by design or by law.

1. Rule of Modularity: *Write simple parts connected by clean interfaces.*
We see this rule in action, when we take a look at all the small pre- and post-processing
2. Rule of Clarity: Clarity is better than cleverness.
3. Rule of Composition: *Design programs to be connected to other programs.*
OpenFOAM's extensive use of text files can be interpreted as a consequence of the Rule of Composition.
The structured, textual formal makes it easy to define and interpret OpenFOAM's in- and output.
4. Rule of Separation: Separate policy from mechanism; separate interfaces from engines.
5. Rule of Simplicity: Design for simplicity; add complexity only where you must.
6. Rule of Parsimony: *Write a big program only when it is clear by demonstration that nothing else will do.*
Again, OpenFOAM is a large collection of specialized tools, rather than a big monolithic – one size fits nobody – monster.
7. Rule of Transparency: *Design for visibility to make inspection and debugging easier.*
Here, we quote Eric S. Raymond¹: “A software system is transparent when you can look at it and immediately understand what it is doing and how.” CFD is admittedly very complex, however, the close-to-mathematical notation of OpenFOAM's high-level code, can be seen as an example of OpenFOAM's obedience to the Rule of Transparency.
8. Rule of Robustness: Robustness is the child of transparency and simplicity.

¹<http://www.catb.org/esr/writings/taoup/html/ch01s06.html>

9. Rule of Representation: *Fold knowledge into data so program logic can be stupid and robust.*
Although this rule was stated without object-orientation in mind, we can observe, that OpenFOAM's data structures and classes absorb much of the complexity. Thus, the top level solver source code looks quite unspectacular.
10. Rule of Least Surprise: *In interface design, always do the least surprising thing.*
We see this rule in action, when we look at all the shared command line options. All tools that support time selection offer common options, such as `latestTime` or `noZero`.
11. Rule of Silence: *When a program has nothing surprising to say, it should say nothing.*
This rule is obeyed by most function objects, which provide the user with the choice of deactivating writing to the Terminal. This output may be useful during testing. As soon as the case is properly set up, however, it is sufficient for the function object to write its output to the corresponding file in the folder `postProcessing`.
12. Rule of Repair: *When you must fail, fail noisily and as soon as possible.*
Ever noticed the FOAM FATAL ERROR messages?
13. Rule of Economy: *Programmer time is expensive; conserve it in preference to machine time.*
If we allow ourselves a very broad view of this rule, we might postulate, that OpenFOAM's mechanism to specify default values for keywords² is one example for following this rule from a user's perspective, i.e. it is the user's time which is conserved.
14. Rule of Generation: *Avoid hand-hacking; write programs to write programs when you can.*
We can see the heavy use of templates as an example of OpenFOAM following the Rule of Generation. The `TurbulenceModels` framework³ is an example of a modelling framework, which is coded once and applied in several different incarnations.
However, this applies only in a wider sense, since this rule was stated not with C++'s templates in mind.
15. Rule of Optimization: Prototype before polishing. Get it working before you optimize it.
16. Rule of Diversity: *Distrust all claims for “one true way”.*
OpenFOAM offers the user plenty of choice such as the solvers to use, the solution algorithms, and discretisation and interpolation schemes.
17. Rule of Extensibility: *Design for the future, because it will be here sooner than you think.*
OpenFOAM sometimes exhibits a different behaviour based on its version, or the format of the input files. See Section 43.4.1 for an example on differences in the input syntax of `fixedValue` boundary conditions. The important lesson in this case is to allow for evolution of the code without breaking compatibility.

2.2 Learning by using OpenFOAM

- Numerical errors can ruin your day in CFD. Not every simulation crash is the fault of some bug in OpenFOAM. The numerics of CFD is also keen to crash simulations.
- Never deactivate the unit checking of OpenFOAM.
- Many classes provide optional debug information. Debug flags can be controlled via a global `controlDict` as well as the case's `controlDict`.
- Play around! A great part of learning is trial and error. Although many of us regard themselves as scientists or aspire to become scientists, never disregard the value of plain trial and error.

²See Section 68.3.2

³See Section 39.

2.3 Learning by tinkering with OpenFOAM

2.3.1 *I learned something today.*

- Have a look at the `test` directory in the `applications` folder of your installation, e.g. in `$HOME/OpenFOAM/OpenFOAM-2.3.x/applications/test`. There, you find examples of how to use certain data structures, which may be exactly what you need when implementing something.
- Create your own test application, if you are about to implement something new. With a test application, you can keep the problem nearly primitive, thus, allowing yourself more mental freedom to explore and to learn. Later, you might be more likely to implement your solver / library with less bugs and errors.
- OpenFOAM makes heavy use of C++'s language features and other smart moves in OO software design. Thus, make sure you understand the basics of the following concepts / language features before you try to study / modify the code of OpenFOAM. Your life gets easier if you do.

inheritance virtually everything of OpenFOAM is described and implemented using the concept of classes.

Classes can be derived from other classes to implement an *is a* relationship, i.e. every cat is an animal but not vice versa.

Note: C++ support multiple inheritance, i.e. a class can be derived from a number of classes, not just one. Other programming languages are (slightly) different in this aspect, e.g. Java allows you to derive only from one class, however, you can implement interfaces.

poly-morphism is a wider concept, however it applies also to inheritance and classes.

templates allow the user to write code for as-of-yet unspecified data types. Container classes are the prime example for the use of templates (or generics as this concept is called in Java).

Examples of the excellent use of the aforementioned concepts is the turbulence modelling framework discussed in Section 39.1.2, or the Lagrangian modelling framework discussed in Section 47.2.

2.3.2 Trouble with the code?

it does not compile

- Due to the heavy use of templates the syntax and the compiler error messages are quite lengthy and often hard to read. However, the compiler error message might contain exactly the information you need to track down the error, e.g. a data-type mismatch. Familiarize yourself with C++'s syntax if you haven't already.

If you are baffled by the very lengthy error messages, take special care to the top and the bottom of the error message, as it is there where you might find the most useful clues.

it does not run

- Spurious crashes (e.g. caused by floating point errors) may be an indication of class members being un-initialized.
- No offence, but it's most probably your fault.

Part I

Installation

3 Install OpenFOAM

Most of this Section was written a long time ago, e.g., Listing 2 was created when OpenFOAM-2.1.x was the most current release of OpenFOAM. These lines here, in this paragraph, were added when OpenFOAM-12 was the current release, some 12 years later. Please make sure, you follow the current, proper guidelines for installing the version of OpenFOAM you want to install.

While parts of this Section may be outdated, e.g., in terms of the specific packages to install, the general description of the process may still be somewhat valid.

3.1 Prerequisites

OpenFOAM is easily installed by following the instructions from this website: <http://www.openfoam.org/download/git.php>.

First of all, you need to make sure all required packages are installed on your system. This is easily done via the package management software. OpenFOAM is a software made primarily for Linux systems. It can also be installed on Mac or Windows platforms. However, the authors uses a Ubuntu-Linux system, therefore this manual will be based on the assumption that a Linux system is used.

```
sudo apt-get install git-core
sudo apt-get install build-essential flex bison cmake zlib1g-dev qt4-dev-tools libqt4-dev
    gnuplot libreadline-dev libxt-dev
sudo apt-get install libscotch-dev libopenmpi-dev
```

Listing 1: Installation of required packages

If OpenFOAM is to be used by a single user, then the User Manual suggests to install OpenFOAM in the `$HOME/OpenFOAM` directory.

3.2 Download the sources

First of all the source files need to be downloaded. This is done with the version control software *Git*. Afterwards we change into the new directory and check for updates. All steps to perform the described operations are listed in Listing 2.

```
cd $HOME
mkdir OpenFOAM
cd OpenFOAM
git clone git://github.com/OpenFOAM/OpenFOAM-2.1.x.git
cd OpenFOAM-2.1.x
git pull
```

Listing 2: Installation von *openFOAM*

Prior to compiling the sources some environment variables have to be defined. In order to do that a line (see Listing 3) has to be added to the file `$HOME/.bashrc`.

```
source $HOME/OpenFOAM/OpenFOAM-2.1.x/etc/bashrc
```

Listing 3: Addition to `.bashrc`

When the command `source $HOME/.bashrc` is issued or when a new Terminal is opened this change is effective. Now with the defined environment variables OpenFOAM can be installed on the system. Before compiling a system check can be made by running *foamSystemCheck*.

```

user@host:~/OpenFOAM/OpenFOAM-2.1.x$ foamSystemCheck
Checking basic system... -----
Shell:          /bin/bash
Host:          host
OS:           Linux version 2.6.32-39-generic
User:          user

System check: PASS
=====
Continue OpenFOAM installation.

```

Listing 4: *foamSystemCheck*

3.3 Compile the sources

If the system check produced no error messages then OpenFOAM can be compiled. This is done by executing `./Allwmake`. This is an installation script that takes care of all required operations. Compiling OpenFOAM can be done by using more than one processor to save time. In order to do this, an environment variable needs to be set before invoking `./Allwmake`. Listing 5 shows how to compile OpenFOAM using 4 processors.

```

export WM_NCOMPPROCS=4
./Allwmake

```

Listing 5: Parallel compilation using 4 processes.

For working with OpenFOAM a user directory needs to be created. The name of this directory consists of the username and the version number of OpenFOAM. With version 2.1.x this folder needs to be named like this: `user-2.1.x`

3.4 Install paraView

paraView is a post processing tool, see <http://www.paraview.org/>. The OpenFOAM Foundation distributes *paraView* from its homepage and recommends to use this version. The source code can be downloaded from <http://www.openfoam.org/> in an archive, e.g. `ThirdParty-2.1.0.tgz`. This archive has to be unpacked into a folder named correspondingly to the OpenFOAM directory, e.g. `ThirdParty-2.1.x` when `OpenFOAM-2.1.x` is used. This naming scheme is mandatory because there is an environment variable that points to the location of *paraView*. As there is no development of *paraView* by the OpenFOAM developers, there is no repository release of third-party tools.

Subsequently *paraView* can be compiled by the use of an installation script. Afterwards some *plug-ins* for *paraView* need to be compiled.

```

cd $WM_THIRD_PARTY_DIR
./makeParaView

cd $FOAM_UTILITIES/postProcessing/graphics/PV3Readers
wmSET
./Allwclean
./Allwmake

```

Listing 6: Installation of *paraView*

3.5 Remove OpenFOAM

If OpenFOAM is to be removed from the system, then a few simple operations do the job⁴, provided the installation was done following the installation guidelines of OpenFOAM⁵.

Listing 7 shows how OpenFOAM can be removed from the system. We assume, we want to remove an installation of OpenFOAM-2.0.1. The first line changes the working directory to the installation directory of

⁴<http://www.cfd-online.com/Forums/openfoam-installation/57512-completely-remove-openfoam-start-fresh.html>

⁵<http://www.openfoam.org/download/git.php>

OpenFOAM. This folder contains all files of the OpenFOAM installation. Listing 8 shows the content of the `~/OpenFOAM`. In this example, two versions of OpenFOAM are installed.

The second line removes all files of OpenFOAM and the third line removes the files of the user related to OpenFOAM. The last line of Listing 7 removes a hidden folder. If there are several versions of OpenFOAM installed, then this folder should not be removed.

```
cd ~/OpenFOAM
rm -rf OpenFOAM-2.0.1
rm -rf user-2.0.1
cd
rm -rf ~/.OpenFOAM
```

Listing 7: Removing *OpenFOAM*

```
cd ~/OpenFOAM
ls -1
user-2.0.x
user-2.1.x
OpenFOAM-2.0.x
OpenFOAM-2.1.x
ThirdParty-2.0.x
ThirdParty-2.1.x
```

Listing 8: Content of `~/OpenFOAM`

Another thing to remove is the entry in the `.bashrc` file in the home directory. Delete the line shown in Listing 3.

3.6 Install several versions of OpenFOAM

It is possible to install several versions of OpenFOAM on the same machine. However due to the fact that OpenFOAM relies on some environment variables some precaution is needed. See <http://www.cfd-online.com/Forums/blogs/wyldckat/931-advanced-tips-working-openfoam-shell-environment.html> for detailed information about OpenFOAM and the Linux shell.

The most important fact about installing several versions of OpenFOAM is to keep them separated.

3.7 Installing newer versions of OpenFOAM on older systems

New software is generally released at a faster cadence than computing systems are renewed, e.g., see the releases of OpenFOAM over time here: <https://openfoam.org/download/history/>. This list suggests that every year, there is a new major release of OpenFOAM. While certain aspects of OpenFOAM might not change all that much from one major release to the next, this can not be held true generally.

Computers, on the other hand, have longer life cycles. Laptops and desktops are generally renewed every 3 to 5 years, while servers may be in service somewhat longer. Thus, you might end up in a situation in which the most current release of OpenFOAM has requirements that an older system can not readily fulfill.

3.7.1 Compiling a newer GCC in the ThirdParty directory

One example, of OpenFOAM being too new for a computing system, is when the minimum version of GCC is higher than the system's version of GCC. This is the case with a computing server⁶ running CentOS-7.9 Linux⁷, which was released in 2020. The first version of CentOS-7 was released in 2014.

CentOS-7.9 has GCC version 4.8.5 installed, which was released in 2015. The initial version of CentOS-7 came with GCC version 4.8.2, which was released in 2013.

With OpenFOAM-11, released in 2023, the minimum version of GCC was increased to 5.4. Thus, if we want to install OpenFOAM-11 or above on a computing server running CentOS-7.9, then we need to first compile a more recent version of GCC.

⁶Server operating systems are generally ones with longer support durations, e.g., SUSE Enterprise Linux, Red Hat Enterprise Linux and CentOS provide security updates for 10 years or longer.

⁷One reason for not upgrading the server's operating system is the fact, that the related hardware is only supported up to a certain version of the operating system. Hence, the hardware might still be too old to be certified for a newer version. This does not necessarily mean, that an upgrade does not work. However, admins are generally quite risk-averse when it comes to servers.

The developers of OpenFOAM have taken care of this need, and provide us with the relevant instructions, see <https://github.com/OpenFOAM/ThirdParty-11>. There, the minimum required version of GCC is listed along with links to its dependencies.

Listing 9, shows the help text of OpenFOAM's build script for its minimum version of GCC. Thus, if your system has version of GCC that it too old, you can compile OpenFOAM's mimimum required version of GCC in the ThirdParty directory. Thus, in order to compile the required version of GCC, we simply need to download the required sources (of GCC and its dependencies) and run `makeGcc`. When this has concluded successfully, OpenFOAM has its own built-in version of GCC, which meets its minimum requirements.

```
user@host:~/OpenFOAM/ThirdParty-12$ ./makeGcc -help

usage: makeGcc [option] [gmp-VERSION] [mpfr-VERSION] [mpc-VERSION] <gcc-VERSION>
options:
  -no-multilib      for 64-bit systems that don't have 32-bit support
  -help

* build combinations of gmp, mpfr, mpc and gcc
  gmp-5.1.2
  mpfr-3.1.2
  mpc-1.0.1
```

Listing 9: The help-text of the build script for OpenFOAM's `gcc`.

Alternatively, you could also install a newer version of GCC as a system-wide upgrade. However, this might not be possible in certain situations, e.g., when you do not have admin privileges on the system in question.

3.8 Installing older versions of OpenFOAM on newer systems

You might also encounter difficulties (of lesser severity) when trying to install old versions of OpenFOAM on quite new computers. While in the previous section, we dealt with current OpenFOAM on old servers; now the issue is generally encountered on laptops or desktops, which are generally updated (getting a new version of the operating system) or upgraded (getting new hardware) more often.

This issue was encountered when installing OpenFOAM-6, which was released in 2018, on a workstation running Ubuntu-22.04. While OpenFOAM itself installed without a hitch, ParaView could not be compiled successfully.

So, if you have the need for fully functioning old installations of OpenFOAM, consider keeping an older workstation around. Note that with outdated systems, there are some additional security concerns to keep in consideration.

4 Updating the repository release of OpenFOAM

4.1 Version management

OpenFOAM is distributed in two different ways. There is the *repository release* that can be downloaded using the *Git repository*. The version number of the repository release is marked by the appended x, e.g. OpenFOAM 2.1.x. This release is updated regularly and is in some ways a development release. Changes and updates are released quickly, however, there is a larger possibility of bugs in this release. Because this release is updated frequently an OpenFOAM installation of version 2.1.x on one system may or will be different to another installation of version 2.1.x on an other system. Therefore, each installation has an additional information to mark different builds of OpenFOAM. The version number is accompanied by a hash code to uniquely identify the various builds of the repository release, see Listing 10. Whenever OpenFOAM is updated and compiled anew, this hash code gets changed. Two OpenFOAM installations are on an equal level, if the build is equal.

```
Build : 2.1.x-9d344f6ac6af
```

Listing 10: Complete version identification of *repository releases*

Apart from the repository release there are also *pack releases*. These are upadated periodically in longer intervals than the repository release. The version number of a pack release contains no x, e.g. OpenFOAM 2.1.1. In contrast to the repository release all installations of the same version number are equal. Due to the longer release cycle the pack release is regarded to be less prone to software bugs.

There are several types of those releases. The are precompiled packages for widely used Linux distributions (Ubuntu, SuSE and Fedora) and also a source pack. The source pack can be installed on any system on which the source codes compile (usually all kinds of Linux running computers, e.g. high performance computing clusters, or even computers running other operation systems, e.g. Mac OSX⁸ or even Windows⁹).

4.2 Check for updates

If OpenFOAM was installed from the repository release, updating is rather simple. To update OpenFOAM simply use *Git* to check if there are newer source files available. Change in the Terminal to the root directory of the OpenFOAM installation and execute `git pull`.

If there are newer files in the repository *Git* will download them and display a summary of the changed files.

```
user@host:~$ cd $FOAM_INST_DIR
user@host:~/OpenFOAM$ cd OpenFOAM-2.1.x
user@host:~/OpenFOAM/OpenFOAM-2.1.x$ git pull
remote: Counting objects: 67, done.
remote: Compressing objects: 100% (13/13), done.
remote: Total 44 (delta 32), reused 43 (delta 31)
Unpacking objects: 100% (44/44), done.
From git://github.com/OpenFOAM/OpenFOAM-2.1.x
  72f00f7..21ed37f  master      -> origin/master
Updating 72f00f7..21ed37f
Fast-forward
.../extrude/extrudeToRegionMesh/createShellMesh.C |    10 +- 
.../extrude/extrudeToRegionMesh/createShellMesh.H |     7 +- 
.../extrudeToRegionMesh/extrudeToRegionMesh.C |   157 ++++++-----+
.../Templates/KinematicCloud/KinematicCloud.H |     6 +- 
.../Templates/KinematicCloud/KinematicCloudI.H |     7 + 
.../baseClasses/kinematicCloud/kinematicCloud.H |    47 ++++++- 
6 files changed, 193 insertions(+), 41 deletions(-)
```

Listing 11: There are updates available

If OpenFOAM is up to date, then *Git* will output a corresponding message.

```
user@host:~/OpenFOAM/OpenFOAM-2.1.x$ git pull
Already up-to-date.
```

⁸See http://openfoamwiki.net/index.php/Howto_install_OpenFOAM_v21_Mac

⁹See http://openfoamwiki.net/index.php/Tip_Cross_Compiling_OpenFOAM_in_Linux_For_Windows_with_MinGW

Listing 12: OpenFOAM is up to date

4.3 Check for updates only

If you want to check for updates only, without actually making an update, *Git* can be invoked using a special option (see Listings 13 and 14). In this case *Git* only checks the repository and displays its findings without actually making any changes. The option responsible for this is `--dry-run`. Notice, that `git fetch` is called instead of `git pull`¹⁰.

```
user@host:~$ cd OpenFOAM/OpenFOAM-2.0.x/
user@host:~/OpenFOAM/OpenFOAM-2.0.x$ git fetch --dry-run -v
remote: Counting objects: 189, done.
remote: Compressing objects: 100% (57/57), done.
remote: Total 120 (delta 89), reused 93 (delta 62)
Receiving objects: 100% (120/120), 17.05 KiB, done.
Resolving deltas: 100% (89/89), completed with 56 local objects.
From git://github.com/OpenFOAM/OpenFOAM-2.0.x
  5ae2802..97cf67d  master      -> origin/master
user@host:~/OpenFOAM/OpenFOAM-2.0.x$
```

Listing 13: Check for updates only – updates available

```
user@host:~$ cd OpenFOAM/OpenFOAM-2.1.x/
user@host:~/OpenFOAM/OpenFOAM-2.1.x$ git fetch --dry-run -v
From git://github.com/OpenFOAM/OpenFOAM-2.1.x
 = [up to date]      master      -> origin/master
user@host:~/OpenFOAM/OpenFOAM-2.1.x$
```

Listing 14: Check for updates only – up to date

4.4 Install updates

After updates have been downloaded by `git pull` the changed source files need to be compiled in order to update the executables. This is done the same way as is it done when installing OpenFOAM. Simply call `./Allwmake` to compile. This script recognises changes, so unchanged files will not be compiled again. So, compiling after an update takes less time than compiling when installing OpenFOAM.

4.4.1 Workflow

Listing 15 shows the necessary commands to update an existing OpenFOAM installation. However this applies only for repository releases (e.g. OpenFOAM-2.1.x). The point releases (every version of OpenFOAM without an x in the version number) are not updated in the same sense as the repository releases. For simplicity an update of a point release (OpenFOAM-2.1.0 → OpenFOAM-2.1.1) can be treated like a complete new installation, see Section 3.6.

The first two commands in Listing 15 change to the directory of the OpenFOAM installation. Then the latest source files are downloaded by invoking `git pull`.

The statement in red can be omitted. However if the compilation ends with some errors, this command usually does the trick, see Section 4.5.2. The last statement causes the source files to be compiled. If `wclean all` was not called before, then only the files that did change are compiled. If `wclean all` was invoked then everything is compiled. This may or will take much longer.

If there is enough time for the update (e.g. overnight), then `wclean all` should be called before compiling. This will in most cases make sure that compilation of the updated sources succeeds.

```
cd $FOAM_INST_DIR
cd OpenFOAM-2.1.x
git pull
```

¹⁰`git pull` calls `git fetch` to download the remote files and then calls `git merge` to merge the retrieved files with the local files. So checking for updates is actually done by `git fetch`.

```
wclean all  
./Allwmake
```

Listing 15: Update an existing OpenFOAM installation. The complete workflow

4.4.2 Trouble-shooting

If compilation reports some errors it is helpful to call `./Allwmake` again. This reduces the output of the successful operations considerably and the actual error messages of the compiler are easier to find.

4.5 Problems with updates

4.5.1 Missing packages

If there has been an upgrade of the operating system¹¹ it can happen, that some relevant packages have been removed in the course of the update (e.g. if these packages are only needed to compile OpenFOAM and the OS 'thinks' that these packages aren't in use). Consequently, if recompiling OpenFOAM fails after an OS upgrade, missing packages can be the cause.

4.5.2 Updated Libraries

When libraries have been updated, they have to be recompiled. Otherwise solvers would call functions that are not (yet) implemented. In order to avoid this problem the corresponding library has to be recompiled.

```
wclean all
```

Listing 16: Prepare recompilation with `wclean`

The brute force variant would be, to recompile OpenFOAM as a whole, instead of recompiling a updated library.

4.5.3 Updated sources fail to compile

In some cases, e.g. when there were changes in the organisation of the source files, the sources fail to compile right away. Or, if there is any other reason the sources won't compile and the cause is not found, then a complete recompilation of OpenFOAM may be the solution of choice. Although compiling OpenFOAM takes its time, this may take less time than tracking down all errors.

To recompile OpenFOAM the sources need to be reset. Instead of deleting OpenFOAM and installing it again, there is a simple command that takes care of this.

```
git clean -dfx
```

Listing 17: Reset the sources using `git`

The command listed in Listing 17 causes `git` to erase all files `git` does not track. That means all files that are not part of the `git`-repository are deleted. In this case, this is the official `git`-repository of OpenFOAM. `git clean` removes all files that are not under version control recursively starting from the current directory. The option `-d` means that also untracked folders are removed.

After the command from Listing 17 is executed, the sources have to be compiled as described in Section 3.3.

4.5.4 Own code fails to run

Updating your repository release of OpenFOAM leads to interesting effects. When libraries of OpenFOAM are updated, their implementation might change. Even if the updated code is fully compatible with the previous one, the compiled libaries might look different after the update. Thus, even if the update maintains code-compatibility¹², the update might break binary compatibility. Thus, a recompilation of your own code following the update of the underlying OpenFOAM installation is required.

¹¹An *upgrade* of an OS is indicated by a higher version number of the same (Ubuntu 11.04 → Ubuntu 11.10). An *update* leaves the version number unchanged.

¹²This is the general behaviour of an update. In an ideal world only newer versions are allowed to introduce incompatibility.

Lost binary compatibility after an update of OpenFOAM leads to segmentation faults when loading a library with lost binary compatibility. This happens because our own solvers dynamically load the required libraries of OpenFOAM at start-up and the memory layout of certain objects of the library has changed since the update.

See the following resources for further information on this topic:

- https://community.kde.org/Policies/Binary_Compatibility_Issues_With_C%2B%2B
- https://en.wikipedia.org/wiki/Binary_code_compatibility
- https://en.wikipedia.org/wiki/Source_code_compatibility

Losing binary compatibility happens not after every update, and it also does not happen to every library. Thus, you may encounter such problems long after the update, and after you successfully used other solvers and libraries of your creation. Thus, the source of the issues described in this Section may not be immediately clear to the user. Thus, if your code suddenly fails to run properly for no good reason, recompile and see what happens.

```

gerhard@gerhardWork:~/software/OpenFOAM-6$ git init
Initialisierte leerer Git-Repository in /home/gerhard/software/OpenFOAM-6/.git/
gerhard@gerhardWork:~/software/OpenFOAM-6$ ls -al
insgesamt 92
drwxrwxr-x 11 gerhard gerhard 4096 Apr 19 14:45 .
drwxrwxr-x 18 gerhard gerhard 4096 Apr 19 14:45 ..
-rw-rw-r-x 1 gerhard gerhard 1109 Jän 8 17:54 Allwmake
drwxrwxr-x 5 gerhard gerhard 4096 Jän 8 17:54 applications
drwxrwxr-x 3 gerhard gerhard 4096 Jän 8 17:54 bin
-rw-rw-r- 1 gerhard gerhard 35646 Jän 8 17:54 COPYING
drwxrwxr-x 5 gerhard gerhard 4096 Jän 8 17:54 doc
drwxrwxr-x 8 gerhard gerhard 4096 Jän 8 17:54 etc
drwxrwxr-x 7 gerhard gerhard 4096 Apr 19 14:45 .git
-rw-rw-r-- 1 gerhard gerhard 1349 Jän 8 17:54 .gitignore
-rw-rw-r-- 1 gerhard gerhard 1626 Jän 8 17:54 README.org
drwxrwxr-x 41 gerhard gerhard 4096 Jän 8 17:54 src
drwxrwxr-x 3 gerhard gerhard 4096 Jän 8 17:54 test
drwxrwxr-x 17 gerhard gerhard 4096 Jän 8 17:54 tutorials
drwxrwxr-x 6 gerhard gerhard 4096 Jän 8 17:54 wmake
gerhard@gerhardWork:~/software/OpenFOAM-6$ 

```

Figure 1: Initializing a new git repository.

5 Updating OpenFOAM-6 source installation

5.1 Motivation

OpenFOAM-6 is kind-of rolling point-release, i.e. the version number remains unchanged, yet there are occasional patch-releases. According to the OpenFOAM Foundation¹³:

Version 6 is a snapshot of the OpenFOAM development version which, through sustainable development, is always-releasable. It provides new functionality and major improvements to existing code, with strict demands on usability, robustness and extensibility.

The initial installation of OpenFOAM-6 follows the steps of any other installation from-source. However, when a subsequent patch-release is released, we're left with an OpenFOAM-6 installation that is not equal in capabilities, features and bugs, than the current OpenFOAM-6 sources.

In ye olden days, we would have been gifted with an OpenFOAM-X.Y++. However, as OpenFOAM-6 is OpenFOAM-6, which sort of isn't OpenFOAM-6¹⁴, we need a way to properly update our source-pack installation of OpenFOAM-6.

5.2 Make the OpenFOAM-6 source pack able to being updated

Since the OpenFOAM-6 source pack is a snapshot of the OpenFOAM-6 git repository¹⁵, updating the source pack is pretty easy. The basic steps are:

1. Initialize a new git repository within the source pack, using `git init`
2. Point the remote-URL of the newly created git repository to the remote repository of OpenFOAM-6, using `git remote`
3. Download the updates, using `git pull`
4. And finally update the local state of your source pack, using `git checkout`

Alternatively, we could simply remove the current installation of OpenFOAM-6, download the latest source pack and re-install afresh. Yet, this would be the less elegant brute-force method of updating our OpenFOAM-6 installation. Connoisseurs, read on.

5.2.1 Initialization

With `git init`, we tell git to create a new git repository. If we run this command in a directory with files being already present, this does not change anyone of them.

After running `git init`, we will find that a new folder has been created: `.git`. The file `.gitignore` has been part of the source pack.

¹³<https://openfoam.org/release/6/>

¹⁴The reader may apologize the rambling babble.

¹⁵<https://github.com/OpenFOAM/OpenFOAM-6>

```
gerhard@gerhardWork:~/software/OpenFOAM-6$ git remote add origin git@github.com:OpenFOAM/OpenFOAM-6.git
gerhard@gerhardWork:~/software/OpenFOAM-6$
```

Figure 2: Pointing the new git repository to the proper remote repository.

```
gerhard@gerhardWork:~/software/OpenFOAM-6$ git pull
remote: Enumerating objects: 104, done.
remote: Counting objects: 100% (104/104), done.
remote: Compressing objects: 100% (84/84), done.
remote: Total 144740 (delta 35), reused 50 (delta 19), pack-reused 144636
Empfange Objekte: 100% (144740/144740), 80.58 MiB | 16.01 MiB/s, Fertig.
Löse Unterschiede auf: 100% (103494/103494), Fertig.
Von github.com:OpenFOAM/OpenFOAM-6
 * [neuer Branch]    master      -> origin/master
 * [neues Tag]      20180710   -> 20180710
 * [neues Tag]      20180805   -> 20180805
 * [neues Tag]      20181130   -> 20181130
 * [neues Tag]      20181221   -> 20181221
 * [neues Tag]      20190108   -> 20190108
 * [neues Tag]      20190304   -> 20190304
 * [neues Tag]      Version-3.0.0 -> version-3.0.0
 * [neues Tag]      version-4.0 -> version-4.0
 * [neues Tag]      version-5.0 -> version-5.0
 * [neues Tag]      version-6 -> version-6
Es gibt keine Tracking-Informationen für den aktuellen Branch.
Bitte geben Sie den Branch an, welchen Sie zusammenführen möchten.
Siehe git-pull(1) für weitere Details.

        git pull <remote> <branch>

Wenn Sie Tracking-Informationen für diesen Branch setzen möchten, können Sie dies tun mit:

        git branch --set-upstream-to=origin/<Branch> master
gerhard@gerhardWork:~/software/OpenFOAM-6$
```

Figure 3: Updating the new git repository by pulling from the remote repository.

5.2.2 Pointing to the remote repository

Next, we need to tell git where to find the updates. We do this, by calling `git remote add origin git@github:OpenFOAM/Op`

5.2.3 Pulling the updates

After, our repository has been made aware, where to get updates, it is time to download them. This is done with `git pull`.

5.2.4 Updating the local repository

After, we have downloaded the updates to our repository, we need to update the local, working files of our repository. Right now, the updates are present locally, yet the working files – the files we can open and read with our text editor have not been updated yet. The local, working files are updated by applying the changes we just downloaded by running `git checkout -t -f -b master origin/master`.

The checkout command now applies all the changes that have been made to the remote master branch to our local master branch. Now, all the local files have been updated, and we can recompile the source files.

Note, that we need to update the third-party source-code directory in the same way as we updated the OpenFOAM source-code directory.

```
gerhard@gerhardWork:~/software/OpenFOAM-6$ git checkout -t -f -b master origin/master
Branch master konfiguriert zum Folgen von Remote-Branch master von origin.
Bereits auf 'master'
gerhard@gerhardWork:~/software/OpenFOAM-6$ git pull
Already up-to-date.
gerhard@gerhardWork:~/software/OpenFOAM-6$
```

Figure 4: Updating the local files of our OpenFOAM-6 installation.

5.3 Recompile the source pack

The last step to update any installation from source, is to recompile the sources. This can be conveniently done by running

```
./Allwmake -update
```

Listing 18: Recompile an updated source pack

6 Maintaining your OpenFOAM installation

Due to the ease of having multiple versions of OpenFOAM installed side-by-side on your system, there is the issue of long-term maintaining of your OpenFOAM installations. Over the years OpenFOAM installations may accumulate on your system. Furthermore, the operating system as well receives attention from its developers in the form of updates and upgrades.

6.1 Dealing with OS updates

Over time, the operating system you are running will receive lots of updates, unless you only work on machines that are not connected to the internet. Usually, updates to the operating system do not affect your OpenFOAM installation. If your OpenFOAM installation ceases to work properly following an OS update, a version conflict is the most likely culprit. In such a case, a total rebuild from source, as outlined in Listing 19 should solve the problem.

Trouble-shooting tip: reboot your machine and try again, this may actually help

OS updates can cause weird errors. Your trusted author encountered a situation in which `mpirun` ceased to work, and the error message, contained a stack trace which featured words such as memory mapping and such. This problem was most likely caused by OS updates which updated the MPI library and/or kernel updates. However, the problems disappeared when the machine was rebooted.

Having a long uptime, i.e. it has been a very long time since the computer last rebooted, is only recommended for computing server, which do not receive updates frequently, and are best not connected to the general internet. A normal workstation, which is frequently updated, should be rebooted regularly. The author has experienced multiple occasions, when the workstation after several kernel updates (these are ones that require a reboot to take effect) with no reboot started to behave weirdly.

6.2 Dealing with OS upgrades

Upgrading the operating system nearly always required a total rebuild from source of your OpenFOAM installation. An upgrade to your OS is very likely to update many or even all libraries and packages OpenFOAM depends on. Thus, trying to run OpenFOAM applications after an upgrade to the OS might result in odd errors, e.g. OpenFOAM failing to launch due to its inability to load shared libraries such as `libmpi.so.XX`, with `XX` being a version number.

In the case of the updated OS, `libmpi.so.YY` was present at the system, with `YY` being a different version number than `XX`. This slight oddity of the error: OpenFOAM reporting a missing `libmpi` library, with a `libmpi` library being present at the system; indicates a version conflict due to the OS upgrade. OpenFOAM tries to load the version of the library when it was installed, yet due to the intervening OS update a newer version of the library replaced the older one.

Hence, after an OS upgrade total rebuild from source is nearly in all cases warranted. Especially when the underlying OS is some sort of long-term release, such as the LTS versions of Ubuntu, which are released every two years. With a long OS release cycle, we are almost guaranteed to run into version problems after the OS upgrade.

Thus, after upgrading the OS, we run a total rebuild from source as shown in Listing 19. First, we enter the installation directory, clear the installation with `wclean all` and finally run `Allwmake`. Note, that this needs to be done with all your OpenFOAM installations, that were installed prior to the upgrade.

```
cd $WM_PROJECT_DIR
wclean all
./Allwmake
```

Listing 19: Performing a total rebuild from source

Running old versions of OpenFOAM is generally not recommended, as they might or will contain bugs which have long been fixed since. However, for checking on old simulations or re-running them to compare them with current runs, it is quite handy to have a functional installation at hand.

7 Install third-party software

The software presented in this section is optional. Without this software OpenFOAM is complete and perfectly useable. However, the software mentioned in this section can be very useful for specific tasks.

7.1 Install *pyFoam*

See http://openfoamwiki.net/index.php/Contrib_PyFoam#Installation for the instructions on the installation of *pyFoam*.

7.2 Install *swak4foam*

See <http://openfoamwiki.net/index.php/Contrib/swak4Foam> for instructions on installing *swak4foam*.

7.3 Compile external libraries

There is the possibility to extend the functionality of OpenFOAM with additional external libraries, i.e. libraries for OpenFOAM from other sources than the developers of OpenFOAM. One example of such an external library is a large eddy turbulence model from <https://github.com/AlbertoPa/dynamicSmagorinsky>. The source code is stored in `OpenFOAM/AlbertoPa/`.

Such a library is compiled with `wmake libso`. This is also the case when libraries of OpenFOAM have been modified. The reason why typing `wmake libso` is sufficient is because all information `wmake` requires is stored in the files `Make/files` and `Make/options`. These files tell `wmake` – and therefore also the compiler – where to find necessary libraries and where to put the executable. A more detailed description of this two files can be found in Section 69.2.2.

To use an external library the solver needs to be told so. See Section 11.3.3.

```
cd OpenFOAM/AlbertoPa/dynamicSmagorinsky
wmake libso
```

Listing 20: Compilation of a library

8 Setting up the environment

8.1 Sourcing OpenFOAM

OpenFOAM makes use of plenty of environment variables, see Section 11.1.1 for a brief discussion. In order to use OpenFOAM, we need to assign values to the variables. Another task enabling the convenient use of OpenFOAM is to add the directories in which OpenFOAM executables are located to the system's `$PATH` variable.

The name of this section stems from the Linux command `source`, which is used in setting up the proper environment for using OpenFOAM. Setting up the environment for using OpenFOAM can be done in two ways, which are discussed below. Each of these variants involves editing a `.bashrc` file¹⁶. This `.bashrc` file can be either a systemwide one for systemwide installations, or belonging to the user who installed OpenFOAM in his/her home directory.

Once the OpenFOAM environment has been sourced in a Terminal, OpenFOAM is ready to use as long as the Terminal is open.

8.1.1 Permanently sourcing OpenFOAM

If we only use one OpenFOAM installation, we could permanently source OpenFOAM. In this case, once this is set up, OpenFOAM is ready for use without any further user action. To achieve this, we add the following line to the appropriate `.bashrc` file. In the case of a single user's installation, this would be the file `$HOME/.bashrc`. The `$HOME/.bashrc` file is loaded every time a Terminal is opened. Thus, if we add the command of Listing 21 to the `$HOME/.bashrc` file, then OpenFOAM is ready to use, whenever the user opens a Terminal. This also applies to login shells, thus remote connections via SSH or systems without any graphical desktop are covered as well.

```
source $HOME/OpenFOAM/OpenFOAM-4.0/etc/bashrc
```

Listing 21: Permanently sourcing OpenFOAM

8.1.2 Sourcing OpenFOAM on demand

Permanently sourcing OpenFOAM is impossible if we want to use several OpenFOAM versions alongside each other. If we have OpenFOAM-3.0 and OpenFOAM-4.1 installed on our system, where should/does `$FOAM_SRC` point to?

In this case, we need a solution to set up the OpenFOAM environment on demand for a specific version of OpenFOAM. Again, we need to add instructions to the `.bashrc` file. However, now we add definitions for *aliases*. An *alias* is a placeholder for a set of instructions, which are to be executed only on demand. Since, we add the *alias* definitions to the `.bashrc` file, the *aliases* we defined are available in every Terminal. However, in contrast to sourcing OpenFOAM permanently, the OpenFOAM environment is set up only when we invoke the *alias*. An *alias* is a convenient way to save on typing effort, since we can assign one or several commands of arbitrary length¹⁷ to a rather short *alias*. We are free to choose the *alias*' name, as long as this name does not collide with an existing command¹⁸.

In Listing 22 two *aliases* are shown for enabling OpenFOAM-3.0 and OpenFOAM-4.1. If we want to use OpenFOAM-3.0, we simply type `of30` into the Terminal, this will source the environment for OpenFOAM-3.0. The use of these four letter *aliases*, which include the major and minor version number of OpenFOAM, saved us from typing a 46 character command to enable the OpenFOAM environment.

```
alias of30='source $HOME/OpenFOAM/OpenFOAM-3.0/etc/bashrc'
alias of41='source $HOME/OpenFOAM/OpenFOAM-4.1/etc/bashrc'
```

Listing 22: Sourcing OpenFOAM on demand by using an *alias*

¹⁶If you for some reason unthinkable to the author do not want to edit any `.bashrc` file, you can simply enter the instruction shown in Listing 21 into the Terminal whenever you want to use OpenFOAM.

¹⁷There is a limit on how long a single command can be. On the author's Linux system, this is north of 2 million bytes.

¹⁸We can, in fact, define an *alias* which has the same name as an existing command. In this case, the *alias* "shadows" the corresponding command. This is used in Ubuntu Linux to add some eye candy, e.g. for `ls`, which is shadowed by `alias ls='ls -color=auto'`. In this case, the Terminal expands the *alias*, whenever a user types `ls`.

8.2 Working with Environment Modules

On a personal machine/workstation we can source our OpenFOAM environment as described in Section 8.1.2, however, on computational clusters thinks may work differently. Especially on managed clusters, i.e. computational clusters not managed by ourselves, there are more sophisticated methods of dealing with the environment, namely Environment Modules¹⁹.

With Environment Modules we define a modulefile containing all relevant information regarding the software in question. A modulefile is written using Tcl (Tool Command Language)²⁰.

8.2.1 Variables: set vs. setenv

In a modulefile, we can define variables and environment variables. In the context of this discussion, variables are only visible within the modulefile, whereas environment variables are visible to the outside world. However, we can not make use of environment variables within the modulefile. If we want to define a variable (within the context of the modulefile) from an environment variable, we need to take special precaution. Line 1 of Listing 23 shows how an environment variable, e.g. \$HOME, can be used within a modulefile.

This leads to a sort-of two-step workflow within the modulefile. First, we define all the relevant variables; and then, we define the relevant environment variables. This two-step workflow is shown in Lines 4 and 7 of Listing 23: first, a variable is created to be used within the modulefile; and then an environment variable is created which will be available to the system once the corresponding module has been loaded.

```
set HOME "$env(HOME)"
set USER "$env(USER)"

set WM_PROJECT "OpenFOAM"
set WM_PROJECT_VERSION "9"

setenv WM_PROJECT "$WM_PROJECT"
setenv WM_PROJECT_VERSION "$WM_PROJECT_VERSION"
```

Listing 23: Snippets of a modulefile for OpenFOAM

8.2.2 Using a custom gcc installation

If we are using a custom installation of gcc, e.g. because of a gcc system installation which is too old, there are some modifications required for the corresponding OpenFOAM modulefile. In the case discussed here, OpenFOAM-9 failed to compile on a CentOS-7.8.2003 system with its gcc-4.8.5 due to the adoption of the C++-14 standard²¹. Thus, a newer version of gcc was necessary. This, however, is quite easily accommodated by OpenFOAM.

Listing 24 shows the necessary changes respectively additions to the modulefile for our OpenFOAM version which needs a custom gcc installation. First, in Line 2 of Listing 24, we change the compiler setting from `system` to `ThirdParty`. Next, we need to provide the specific versions of the packages required for compiling gcc, these entries are dependent on your exact version of OpenFOAM and gcc. These packages are listed in the description of the `ThirdParty` repository²², where the download links are provided. Subsequently, paths are defined and the proper environment variables are created and the proper paths are made available.

Note, we need to make sure that `$WM_THIRD_PARTY_DIR`, `$WM_ARCH` and `$WM_COMPILER_LIB_ARCH` are available as variables within the modulefile. If this is not the case, the instruction of Line 14 would cause an error.

```
# wmake
setenv WM_COMPILER_TYPE "ThirdParty"

# custom gcc environment variables
set gmp_version "gmp-5.1.2"
set mpfr_version "mpfr-3.1.2"
set mpc_version "mpc-1.0.1"
set gcc_version "gcc-7.5.0"
```

¹⁹<http://modules.sourceforge.net>

²⁰<https://www.tcl-lang.org>

²¹<https://github.com/OpenFOAM/OpenFOAM-9/commit/0257ab14596f658708b4164963bcd5b5d654efc2>

²²<https://github.com/OpenFOAM/ThirdParty-9>

```

setenv gmp_version "$gmp_version"
setenv mpfr_version "$mpfr_version"
setenv mpc_version "$mpc_version"
setenv gcc_version "$gcc_version"

set gccDir "$WM_THIRD_PARTY_DIR/platforms/$WM_ARCH/$gcc_version"
set gmpDir "$WM_THIRD_PARTY_DIR/platforms/$WM_ARCH/$gmp_version"
set mpfrDir "$WM_THIRD_PARTY_DIR/platforms/$WM_ARCH/$mpfr_version"
set mpcDir "$WM_THIRD_PARTY_DIR/platforms/$WM_ARCH/$mpc_version"
setenv gccDir "$gccDir"
setenv gmpDir "$gmpDir"
setenv mpfrDir "$mpfrDir"
setenv mpcDir "$mpcDir"
setenv MPFR_ARCH_PATH "$mpfrDir"
setenv GMP_ARCH_PATH "$gmpDir"

# custom gcc paths
prepend-path PATH "$gccDir/bin"
prepend-path LD_LIBRARY_PATH "$gccDir/lib$WM_COMPILER_LIB_ARCH"
prepend-path LD_LIBRARY_PATH $gmpDir/lib$WM_COMPILER_LIB_ARCH"
prepend-path LD_LIBRARY_PATH $mpfrDir/lib$WM_COMPILER_LIB_ARCH"
prepend-path LD_LIBRARY_PATH $mpcDir/lib$WM_COMPILER_LIB_ARCH"

```

Listing 24: Snippets of a modulefile for OpenFOAM using a custom gcc installation.

Part II

General Remarks about OpenFOAM

9 Units and dimensions

This section discusses the treatment of physical units (e.g. meter, second, etc.) and dimensions (scalar, vector, etc.) in OpenFOAM. In OpenFOAM physical units are referred to as *dimensions* and they are covered by the class `dimensionSet`. The dimensionality (a quantity being a scalar or a vector) is treated implicitly by the data types. The data types `scalar` or `vector` do not need any further specification of their dimensionality.

9.1 Unit inspection

Basically, OpenFOAM uses the International System of Units, short: SI units. Nevertheless, also other units can be used. In that case it is important to remember, that some physical constant, e.g. the universal gas constant, are stored in SI units. Consequently the values need to be adapted if other units than SI should be used.

OpenFOAM performs in addition to its calculations also a inspection of the physical units of all involved variables and constants. For fields, like the velocity, or constants, like viscosity, the unit has to be specified. The unit is defined in the *dimension set*. Units in the International System of Units are defined as products of powers of the SI base units.

$$[Q] = \text{kg}^\alpha \text{m}^\beta \text{s}^\gamma \text{K}^\delta \text{mol}^\epsilon \text{A}^\zeta \text{cd}^\eta \quad (1)$$

A dimension set contains the exponents of (1) that define the desired unit. With the dimension set OpenFOAM is able to perform unit checks.

```
dimensions      [0 1 -2 0 0 0 0];
```

Listing 25: False *dimensions* for U

```
--> FOAM FATAL ERROR:
incompatible dimensions for operation
[U[0 1 -3 0 0 0 0] ] + [U[0 1 -4 0 0 0 0] ]

From function checkMethod(const fvMatrix<Type>&, const fvMatrix<Type>&)
in file /home/user/OpenFOAM/OpenFOAM-2.1.x/src/finiteVolume/lnInclude/fvMatrix.C at line
1316.

FOAM aborting
```

Listing 26: Incompatible *dimensions* for summation

Listing 25 shows an incorrect definition of the dimension of the velocity, e.g. in the file `0/U`. m/s^2 has been defined instead of m/s . OpenFOAM recognises this false definition, because mathematical operations do not work out anymore. Listing 26 shows a corresponding error message produced by two summands having different units. Therefore, OpenFOAM aborts and displays an error message.

9.1.1 An important note on the base units

The order in which the base units are specified differs between OpenFOAM and many publications dealing with SI units, compare (2) and (3). The order of the base units as it is used by OpenFOAM swaps the first two base units. As the list of base units in [4, 3] starts with the metre followed by the kilogram, OpenFOAM reverses this order and begins with the kilogram followed by the metre. Also the fourth, fifth and sixth base units appear in a different position.

$$[Q]_{\text{OpenFOAM}} = \text{kg}^\alpha \text{m}^\beta \text{s}^\gamma \text{K}^\delta \text{mol}^\epsilon \text{A}^\zeta \text{cd}^\eta \quad (2)$$

$$[Q]_{\text{SI}} = \text{m}^\alpha \text{kg}^\beta \text{s}^\gamma \text{A}^\delta \text{K}^\epsilon \text{mol}^\zeta \text{cd}^\eta \quad (3)$$

Eq. (2) is based on the source code of OpenFOAM, see Listing 27. Eq. (3) is based on [4, 3].

```

1 // - Define an enumeration for the names of the dimension exponents
2 enum dimensionType
3 {
4     MASS,           // kilogram    kg
5     LENGTH,         // metre        m
6     TIME,           // second       s
7     TEMPERATURE,   // Kelvin       K
8     MOLES,          // mole         mol
9     CURRENT,        // Ampere      A
10    LUMINOUS_INTENSITY // Candela    Cd
11};

```

Listing 27: The definition of the order of the base units in the file `dimensionSet.H`

The reason for changing the order of the base units may be motivated from a CFD based point of view. For fluid dynamics involving compressible flows as well as reactive flows and combustion the first five units of OpenFOAM's set of base units suffice.

9.1.2 Input syntax of units

Listing 28 shows the definition of a phase in a two-phase problem. Notice the difference between the first two definitions and the third one. The unit of `d` is defined by the full set of seven exponents, whereas the other two units (`rho` and `nu`) are defined only by five exponents. Apparently it is allowed to omit the last two exponents (defining candela and ampere).

Defining units with five entries (for kilogram, metre, second, kelvin and mol) seems to be perfectly appropriate. Neither the OpenFOAM User Guide [52] or the OpenFOAM Programmer's Guide [51] mention this behaviour. Defining a unit with an other number of values than five or seven leads to an error (see Listing 29).

```

phaseb
{
    rho          rho [ 1 -3 0 0 0 ] 1000;
    nu           nu [ 0 2 -1 0 0 ] 1e-06;
    d            d [ 0 1 0 0 0 0 0 ] 0.00048;
}

```

Listing 28: Definition of the unit

```

--> FOAM FATAL IO ERROR:
wrong token type - expected Scalar, found on line 22 the punctuation token ']'

file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bed/constant/transportProperties::
phaseb::nu at line 22.

From function operator>>(Istream&, Scalar&)
in file lnInclude/Scalar.C at line 91.

FOAM exiting

```

Listing 29: Erroneous definition of units

9.1.3 Programming syntax of units

Single numbers or entire fields in OpenFOAM are not only read from file, they are also calculated from existing ones or they created completely new, independent of existing quantities. Let's take a look on how to create dimensioned quantities from the programming point of view. In OpenFOAM there are dimensioned and undimensioned data types, e.g. there are the data types `scalar` and `dimensionedScalar`. The type `dimensionedScalar` is basically a `scalar` with an additional `dimensionSet`.

Calculating dimensioned quantities

Calculated fields inherit their dimension set from the involved operations and operands. Listing 30 shows the creation of the kinetic energy field K from the square of the velocity fields²³. The newly created field, bears the name K, as this is passed as an argument to the constructor. The dimension set of the field K is derived from the constructor's second argument. Since all mathematical operations on numeric types are mirrored for dimensions, any mathematical operation on a dimensioned type not only yields a numerical result, it also yields a resulting dimension. In this case the resulting dimension is square metre per square second.

```
1 Info<< "Creating field kinetic energy K\n" << endl;
2 volScalarField K("K", 0.5*magSqr(U));
```

Listing 30: Computing the kinetic energy fields

Creating dimensioned quantities

When creating a dimensioned quantity from scratch, the dimension set needs to be stated explicitly. In Listing 31 the dimension set is explicitly passed to the constructor of `dimensionedScalar` as the second argument. Note the use of the five argument constructor of `dimensionSet`. As the last two SI units (for current and luminous intensity) are scarcely needed in fluid dynamics, the five argument constructor is a convenience feature of this data type.

```
1 dimensionedScalar foo("foo", dimensionSet(0, 3, 0, 0, 0), scalar(1.0))
```

Listing 31: Create a new variable of the `dimensionedScalar` datatype

Always explicitly stating the dimension set with its 5 or 7 exponents would seriously bloat the code for no benefit. Thus, there are a number of global constants of the data type `dimensionSet`. These constants define the most common dimension sets and offer a very convenient short-hand notation²⁴ as seen in Listing 32.

```
1 dimensionedScalar bar("bar", dimless, scalar(0.0))
```

Listing 32: Create a new variable of the `dimensionedScalar` datatype

Since all mathematical operations performed on the numeric part of a dimensioned quantity are also performed on the dimension set, the class `dimensionSet` implements mathematical operations. We can use these and the global short-hands to define the dimension set of our new dimensioned quantity. In Listing 33, we needlessly compute the dimension set for a velocity, however, this Listing demonstrates the use of mathematical operations on dimension sets.

```
1 dimensionedScalar baz("baz", dimLength/dimTime, 42.0)
```

Listing 33: Create a new variable of the `dimensionedScalar` datatype

9.2 Dimensions

Fields in fluid mechanics can be scalars, vectors or tensors. There are in OpenFOAM different data types to distinguish between quantities of different dimensions.

volScalarField A scalar field throughout the whole computational domain, e.g. pressure.

volScalarField p

volVectorField A vector field throughout the whole domain, e.g. velocity.

volVectorField U

²³The kinetic energy is defined in textbooks as $k = \frac{1}{2}\rho u^2$, which involves the fluid density ρ , which the definition in Listing 30 is lacking. However, the fluid density field `rho` enters the scene as second argument in the terms of the energy transport equation, as can be seen in the temporal derivative and convective terms of `rhoPimpleFoam`'s energy equation: `fvc::ddt(rho, K) + fvc::div(phi, K)`. Thus, OpenFOAM's kinetic energy K is in fact a specific kinetic energy.

²⁴You can find these definitions in `$FOAM_SRC/OpenFOAM/dimensionSet/dimensionSets.C`

volTensorField A tensor field throughout the whole domain, e.g. Reynolds stresses.

volTensorField Rca

surfaceScalarField A scalar field, defined on surfaces (surfaces of the finite volumes), e.g. flux.

surfaceScalarField phi

dimensionedScalar A scalar constant throughout the whole domain (i.e. no field quantity).

dimensionedScalar nu

9.2.1 Dimension check

The data type defines also, as described before, the dimension of a quantity. The dimension of a quantity defines the syntax how quantities have to be entered.

Listing 35 shows the error message OpenFOAM displays when the value of a scalar quantity is entered as a vector (Listing 34).

```
dimensions          [ 0 0 0 0 0 0 ];
internalField      uniform ( 0 0 0 );
boundaryField
{
    inlet
    {
        type          fixedValue;
        value         uniform 0;
    }
}
```

Listing 34: Erroneous definition of α

```
--> FOAM FATAL IO ERROR:
wrong token type - expected Scalar, found on line 19 the punctuation token ')'

file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bed/0/alpha::internalField at line
19.

From function operator>>(Istream&, Scalar&)
in file lnInclude/Scalar.C at line 91.

FOAM exiting
```

Listing 35: Error message caused by invalid dimension

9.3 Kinematic viscosity vs. dynamic viscosity

To determine if OpenFOAM uses the kinematic viscosity [$\text{Ns/m}^2 = \text{Pas}$] or the dynamic viscosity [m^2/s] one has simply to take a look on the dimension.

```
nu          nu [ 0 2 -1 0 0 0 ] 0.01;
```

Listing 36: *dimensions* of the viscosity

The type of viscosity is primarily determined by the used solver, e.g. compressible or incompressible.

9.4 Pitfall: pressure vs. pressure

The definition of pressure in OpenFOAM differs between the compressible and incompressible solvers. Compressible solvers work with the pressure itself. Incompressible solvers use a modified pressure. The reason for this is, because of $\rho = \text{const}$ the incompressible equations are divided by the density and to eliminate density entirely the modified pressure is introduced into the pressure term.

$$\hat{p} = \frac{p}{\rho} \quad (4)$$

For this reason the entries in the 0/p files differ depending on the solver in use. This is visible by the unit of pressure.

9.4.1 Incompressible

The unit of the pressure in an incompressible solver is defined by (4)

$$[\hat{p}] = \frac{\text{N}}{\text{m}^2} \cdot \frac{\text{m}^3}{\text{kg}} = \text{N} \frac{\text{m}}{\text{kg}} = \frac{\text{kNm}}{\text{s}^2} \cdot \frac{\text{m}}{\text{kg}} = \frac{\text{m}^2}{\text{s}^2} \quad (5)$$

```
dimensions [0 2 -2 0 0 0 0];
```

Listing 37: Unit of pressure - incompressible

9.4.2 Compressible

The unit of the pressure in a compressible solver is the physical unit of pressure.

$$[p] = \frac{\text{N}}{\text{m}^2} = \frac{\frac{\text{kNm}}{\text{s}^2}}{\text{m}^2} = \frac{\text{kg}}{\text{ms}^2} \quad (6)$$

```
dimensions [1 -1 -2 0 0 0 0];
```

Listing 38: Unit of pressure - compressible

9.4.3 Pitfall: Pressure in incompressible multi-phase problems

When solving a multi-phase problem in an Eulerian-Eulerian fashion, for each phase a momentum equation is solved. In most cases it is assumed that the pressure is equal in all phases. For this reason the incompressible equations can not be divided by the density, because each phase has a different density and therefore, the modified pressure would be different for each phase. To avoid this issue, incompressible Euler-Euler solvers, like *bubbleFoam*, *twoPhaseEulerFoam* or *multiPhaseEulerFoam*, use the physical pressure like compressible solvers do.

10 Files and directories

OpenFOAM saves its data not in a single file, like Fluent does, it uses several different files. Depending on its purpose a specific file is located in one of several folders.

10.1 Files in general

10.1.1 C++ syntax

OpenFOAM's case files are generally in a human-readable ASCII format. They follow a C++-style syntax. Most importantly, we can use the C/C++ comments in OpenFOAM's case files.

Comments

Listing 39 a case file of OpenFOAM, which demonstrates this point. There are several comments in this file providing some optical niceties. At the top, the multi-line comment is the OpenFOAM banner. This is a non-functional part of each case or data file that is written by OpenFOAM by default. OpenFOAM will work normally, and it will not complain, if we remove this banner.

Using semi-colons

Keyword-value pairs are terminated by a semi-colon (;) character in a similar fashion as C/C++ statements are terminated by a semi-colon. Section 11.2.3 discusses the consequences of omitting the semi-colon, which triggers a syntax error when OpenFOAM reads the affected file.

Listing 39 shows an exception to the rule on semi-colons terminating statements. While the keyword-value pairs and also lists are terminated by a semi-colon, the dictionary `RAS` is not terminated in such a manner. This is not needed since dictionaries are delimited with curly braces ({ }). This is analogous to the way code blocks are delimited in C/C++.

Lists terminated by semi-colons are shown in Listing 42. Essentially, a list is a keyword-value pair with the list's name as keyword and the list proper as value. Conceptually, we think of lists separately from keyword-value pairs, so that we can consider the value of a keyword-value pair as a single entity, while a list is a collection of entities.

10.1.2 Data file header

The next entry in the file in Listing 39 is the data file header. This is a functional part of OpenFOAM, and all files that are read or written need to have such a header. The data file header is a dictionary in OpenFOAM's parlance, and it contains a couple of keyword-value pairs.

Next, there is a single-line comment dividing the banner and the data file header from the rest of the file's content. Then, there is a single keyword-value pair with an associated additional dictionary. The file is closed with another single-line comment.

```
1 /*-----* C++ -----*/
2 ====== |
3   \\\    / Field      | OpenFOAM: The Open Source CFD Toolbox
4   \\\    / Operation  | Website: https://openfoam.org
5   \\\    / And        | Version: 12
6   \\\    / Manipulation | 
7 /*
8 FoamFile
9 {
10     format      ascii;
11     class       dictionary;
12     location    "constant";
13     object      momentumTransport;
14 }
15 // * * * * *
16
17 simulationType RAS;
18
19 RAS
20 {
```

```

21     model      kOmegaSST;
22
23     turbulence    on;
24     printCoeffs   on;
25 }
26
27 // ****

```

Listing 39: A case file from OpenFOAM, shown with C++ syntax highlighting.

10.1.3 The data file header

With the release of OpenFOAM-9²⁵, the `version` entry into the data file header was made optional. Listing 40 shows basically the same file from a much older release of OpenFOAM. Functionally, these files are identical, i.e., both files select the same turbulence model. See Section 68.3.2 for an in-depth discussion how OpenFOAM enables the use of optional keywords.

In between the releases of OpenFOAM, these files changed a little. Apart from the `version` entry, the file was renamed: in the older version of OpenFOAM, turbulence model selection was done in a file named `turbulenceProperties`, in later versions of OpenFOAM, this is done in a file named `momentumTransport`. We can tell this name change from Listings 39 and 40 by comparing the value of the `object` keyword-value pair. This entry is a mandatory one, i.e., it needs to be present, but it is not used apparently. Renaming files over time occasionally happens in the continuous development of OpenFOAM.

```

1  /*----- C++ -----*/
2  | =====
3  | \ \ / F i e l d           | OpenFOAM: The Open Source CFD Toolbox
4  | \ \ / O peration          | Version: 2.3.0
5  | \ \ / A nd                | Web: www.OpenFOAM.org
6  | \ \ \ M anipulation       |
7  \*-----*/
8 FoamFile
9 {
10    version    2.0;
11    format     ascii;
12    class      dictionary;
13    location   "constant";
14    object     turbulenceProperties;
15 }
16 // * * * * *
17
18 simulationType RAS;
19
20 RAS
21 {
22    RASModel      kOmegaSST;
23
24    turbulence    on;
25
26    printCoeffs   on;
27 }
28
29 // ****

```

Listing 40: An older case file from OpenFOAM, shown with C++ syntax highlighting.

10.1.4 Reinstating the `version` entry

To make case files from newer versions of OpenFOAM (in which `version` was omitted since it is optional) compatible with older versions which require the presence of the `version` entry, we need to reinstate it in all case and data files, which do not have it present. For a few case files, we could do this using a simple text editor: simply open the files and insert the `version` entry by copy&paste. However, if we deal with a large number of files, this becomes a tedious exercise at best. At worst, we also have to deal with binary data files,

²⁵See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/01494463d068d66ab94efc4984a1148f2b4652cb>

which can not be edited to easily. Thus, we need a programmatic way to perform the task at hand: reinstating the version entry in all of our files.

Listing 41 shows how this is done via a combination of a Linux command and one of OpenFOAM's case management tools. While the command in Listing 41 is a one-liner, there is still a bit to unpack.

```
user@host:~$ find 0 -type f | xargs -L 1 foamDictionary -entry FoamFile.version -add 2.0
--> FOAM Warning :
  From function bool Foam::dictionary::add(Foam::entry*, bool)
  in file db/dictionary/dictionary.C at line 884
  Reading ".FoamFile" from line 10 to line 14
  attempt to add entry version which already exists in dictionary ".FoamFile"
user@host:~$
```

Listing 41: Displaying the help message

First, we shall discuss the `find` command, i.e., everything preceding the pipe (the `|` character). We call `find` and specify 0 and its working directory. We furthermore tell `find` to report any files it finds within its working directory. The argument `-t` is used to tell `find` that we are interested only in matches of the type: file. Note, that this also works for sub-directories. This command assumes that the working directory of our Linux Terminal is the case directory itself. If we wanted to do this operation to all case files, we could pass the current directory to `find`.

Then, we have a pipe, or pipeline²⁶, which passes the results of one command to the next one. Thus, pipes allow us to chain together several commands. With pipes we read from left to right, thus the results of `find` are piped to the command which follows the pipe operator.

Following the pipe operator is the command `xargs -L 1`, which is used to convert the input from standard input into arguments for the following command²⁷. The `-L 1` argument is important in this case, since `foamDictionary` only allows a single argument. Other tools, especially standard tools of Linux have no issues processing a list of arguments instead of being passed only a single one.

`foamDictionary` is already discussed in Section 34.2, thus we shall not discuss this tool in great detail here. However, what we do is we select the entry `version` of the dictionary `FoamFile`, which is the data file header, and we add the value 2.0. Note, that `add` issues a warning if the entry is already present, which was the case once in Listing 41. Alternatively, we could also use `-set` instead of `-add`, then we get no warnings.

This programmatic reinstatement of the version entry works for all files: small ASCII files or large binary files. By using the command `find` to provide the argument for `foamDictionary`, we can reduce the treatment of a whole case to a one-liner in the Linux command line.

10.1.5 Whitespace for formatting

Listing 42 shows a case file of an OpenFOAM case, which contains a dictionary which in turn contains various types of input data: keyword-value pairs and two lists. Note, how the contents are indented²⁸ by spaces to visually group elements belonging together.

Apart from indentation, we also see the use of spaces to align the values of the keyword-value pairs to start at the same column. This is to give this part of the file a table-like look. In a keyword-value pair, at least a single whitespace character is required to separate the keyword from its value. We can, however, use an arbitrary number of whitespace characters. Of the commonly used characters, space, tab and newline are all whitespace characters. However, we strongly advise against separating a keyword from its value by a newline.

We see, however, the use of a newline in separating the list-name from the opening parenthesis. The short list `libs` uses only spaces for separation, while the longer list `fields` uses also newline.

```
1 /*----- C++ -----*/
2 =====
3   \\\ / F ield      | OpenFOAM: The Open Source CFD Toolbox
4   \\\ / O peration  | Website: https://openfoam.org
5   \\\ / A nd        | Version: 12
6   \\\ M anipulation |
7 */
8 FoamFile
```

²⁶See [https://en.wikipedia.org/wiki/Pipeline_\(Unix\)](https://en.wikipedia.org/wiki/Pipeline_(Unix))

²⁷See <https://en.wikipedia.org/wiki/Xargs>

²⁸Indentation in general is discussed at Wikipedia: see https://en.wikipedia.org/wiki/Indentation_style

Listing 42: Another case file from OpenFOAM, demonstrating the use of whitespace for pretty formatting.

10.2 Required directories

An OpenFOAM case has a minimal set of files and directories. The directory that contains those folders is called the root directory of the case or case directory. Listing 43 shows the output of the commands `pwd` and `ls` when they are invoked from a case directory. The first command returns the absolute path of the current working directory. The second command prints the contents of the current folder. When `ls` is invoked without any options it returns the names of all non-hidden files and folders. In this case there are three subdirectories (*0*, *constant* and *system*). The fact that these three items are directories and not files is indicated by a different color. If `ls` is called with the option `-l` a more detailed list is printed. This detailed list indicates if an entry is a file or a directory.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ pwd  
/home/user/OpenFOAM/user-2.1.x/run/icoFoam/cavity  
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls  
0 constant system  
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls -l  
insgesamt 12  
drwxrwxr-x 2 user group 4096 Okt 2 14:53 0  
drwxrwxr-x 3 user group 4096 Okt 2 14:53 constant  
drwxrwxr-x 2 user group 4096 Okt 2 14:53 system
```

Listing 43: Case directory

- 0 This is the first of the time-directories. It contains the initial and boundary conditions of all variable quantities. A case does not have to start at time $t = 0$. However, if there is no specific reason for a case to start at another time than $t = 0$, a case will always begin at time $t = 0$. The name of a time-directory is simply the number of elapsed seconds.

constant This folder contains all files dealing with constant quantities as well as the mesh.

polymesh This is a subdirectory of *constant*. In this folder all files defining the mesh reside.

system In this folder all files that control the solver or other tools are located

In the course of computing the case two kinds of folders are created. First of all, at defined times all information is written to the harddisk. A new time-directory is created with the number of elapsed seconds in its name. In

this folder all kinds of files are saved. The number of files is equal or larger than in the *0*-directory containing the initial conditions.

The second category of directory subsumes all kinds of folders created for all kind of reasons or by all kind of tools, see Section 10.3 for a brief introduction to some of the more common of them.

10.3 Supplemental directories

Directories described in this Section may be created in the course of a computation.

10.3.1 *processor**

If a case is solved in parallel, i.e. the case is computed using more than one processor at the time. In this case the computational domain has to be decomposed into several parts, to divide the problem between the involved parallel processes. The tool that is used to decompose the case created the *processor**-directories. The * stands for a consecutive number starting with 0. So, if a case is to be solved using 4 parallel processes, then the domain has to be split into 4 parts. Therefore, the folders *processor0* to *processor3* are created.

Every one of the *parallel**-directories contains a *0*- and also a *constant*-directory containing only the mesh. The *system*-directory remains in the case folder. See Section 12.5 for more information about conducting parallel calculations.

10.3.2 functions

functions or functionObjects perform all kind of operations during the computation. Each function creates a folder of the same name to save its data in. See Section 59 for more information about functions.

10.3.3 sets

If the tool *sample* has been used, then all data generated by *sample* is stored in a folder named *sets*. See Section 60 for more information about *sample*.

10.4 Files in *system*

In the directory named *system* there are three files for controlling the solver. This files are necessary to run a simulation. Besides them there may also be additional files controlling other tools.

10.4.1 The main files

This files have to be present in the system folder to be able to run a calculation

controlDict This file contains the controls related to time steps, output interval, etc.

fvSchemes In this file the finite volume discretisation schemes are defined

fvSolution This files contains controls related to the mathematical solver, solver algorithms and tolerances.

10.4.2 Additional files

This list contains a selection of the most common files to be found in the system-directory.

probesDict Alternative to the use of the file *probesDict*, *probes* can also be defined in the file *controlDict*.

decomposeParDict Used by *decomposePar*. In this file the number of subdomains and the method of decomposition are defined.

setFieldsDict Necessary for the tool *setFields* to initialise field quantities.

sampleDict Definitions for the post-processing tool *sample*.

11 Controlling OpenFOAM

11.1 The means of exerting control

Classical UNIX applications know several means of controlling their configuration [22]:

- *System-wide run-control files*

An example for these are files in `/etc` on Linux or UNIX systems. For OpenFOAM, such system-wide run-control files are located in `$FOAM_ETC`, which might be `home/user/OpenFOAM/OpenFOAM-3.0.0/etc`. There, we can find the global `controlDict`, controlling OpenFOAM's behaviour installation-wide.

- *System-wide environment variables*

Such a system-wide variable on a Linux system is `$HOSTNAME`, which is the name associated to identify the computer within a network. This name is the same for all users logged in at a certain machine, and it can and should not be changed by a user. For OpenFOAM such system-wide environment variables are `$FOAM_ETC`, `$FOAM_INST_DIR` or `$WM_THIRD_PARTY_DIR`. These variables are equal for all users of a certain installation.

The distinction between system-wide and user-defined settings blurs, when we install OpenFOAM in our home directory, then we are the administrator and the single user of our installation. This distinction was made for clusters, which provide one installation to many users.

- *User-defined run-control files*

A perfect example of a user-defined run-controlled file is the file `.bashrc` in the user's home directory. This file contains user-specific settings. During the installation process of OpenFOAM, this file needs to be edited to make the OpenFOAM installation available to the user.

- *User-set environment variables*

These aren't quite common. On a Linux or UNIX system, a user might set the `$EDITOR` variable, then applications, which might call an editor can simply query this variable to call the preferred editor of the user.

- *Switches and arguments passed on the command line*

These are very common. A widely known example are the command line arguments `-h`, `-help` or `--help` for displaying a summary of the application usage.

The order of the above listed means of control is descending from the system-level down to the per-execution level. With the freedom to choose between five mechanisms to control the behaviour of an application comes great responsibility to the software developer to choose wisely. Nobody wants to pass the same, never-changing command line arguments every time an application is run. Otherwise, user often do not have the possibility to edit system-wide run-control files, so these might be a bad location for settings which change on a daily basis.

11.1.1 Variables

Variables are the best place to store information, which is repeatedly needed. E.g. it would make no sense to specify the installation directory of OpenFOAM in every run-control file which needs to know where OpenFOAM is installed on the system, instead a variable `$FOAM_INST_DIR` is defined in one of OpenFOAM's global run-control files. In all other run-control files, which need to know the installation path, this variable is used. Thus, information redundancy is avoided. Imagine the poor cluster administrators, if some information were stored in multiple places, and this information were to change. Good luck finding and updating ALL occurrences of this data.

Variables offer the freedom to use the same name (i.e. the variable) regardless of what the actual information is. OpenFOAM is always installed at `$FOAM_INST_DIR`, whether that is `/home/user/OpenFOAM`, `/opt/OpenFOAM` or `/home/user/Desktop/important_softWare`.

11.1.2 Dictionaries

Dictionaries are the run-control files of OpenFOAM. Most of the controls of OpenFOAM are set in so called *dictionaries*. An important *dictionary* is the file `controlDict`. Dictionaries offer a convenient way to store structured information of arbitrary size, which would be rather impossible using variables or command line arguments. Imagine typing all contents of `controlDict` every time you run a solver.

The distinction between global and local dictionaries saves ourselves from messing up the OpenFOAM installation when fiddling with a case's set-up.

11.1.3 Command line arguments

Besides the dictionaries, there are also command-line arguments to control certain aspects of OpenFOAM's solvers and utilities. Command line arguments are the best way to pass information to an application that might change from one run to the other, even when the case is the same.

An example is the `-parallel` command line switch. Regardless of whether we run a case with a single process or in parallel, the case's settings are unchanged. Thus, it would be inconsistent to tell the solver to run in parallel via a case file.

Command line switches are command line arguments, which do not need any additional information. Adding `-help` to a solver name is sufficient to make the solver display its usage summary. A command line argument, on the other hand, needs additional information. An example is the `-time` argument used to tell post-processing tools on which time steps to act upon. Passing `-time` alone without any further information leaves the tool clueless and it will issue an error message.

11.2 Syntax of the dictionaries

The dictionaries need to comply a certain format. The OpenFOAM User Guide states, that the dictionaries follow a syntax similar to the C++ syntax.

The file format follows some general principles of C++ source code.

The most basic format to enter data in a dictionary is the key-value pair. The value of a key-value pair can be any sort of data, e.g. a number, a list or a dictionary.

11.2.1 Keywords - the banana test

As OpenFOAM offers no graphical menus, in some cases allowed entries are not visible at a glance. If a key expects a value of a finite set of data, then the user can enter a value that is definitely not applicable, e.g. `banana`. Then, OpenFOAM produces an error message with a list of allowed entries.

```
--> FOAM FATAL IO ERROR:  
expected startTime, firstTime or latestTime found 'banana'
```

Listing 44: Wrong keyword, or the banana test

Listing 44 shows the error message that is displayed when the value `banana` is assigned to the key `startFrom` that controls at which time a simulation should start. The error message contains a note that is formated in this way: *expected X, Y or Z found ABC*.

If in a dictionary several key-value pairs are erroneous, only the first one produces an error, as OpenFOAM aborts all further operations.

Pitfall: assumptions & default values

In some cases the banana test behaves differently than expected. Listing 45 shows the warning message OpenFOAM returns, when the banana test is used with the control `compression` of `controlDict`. See Section 11.3.2 for a description of this control. In this case, OpenFOAM does not abort but continues to run the case. Instead of returning an error message and exiting, OpenFOAM simply assumes a value in place of the invalid entry.

```
--> FOAM Warning :  
From function IOstream::compressionEnum(const word&)  
in file db/IOstreams/IOstreams/IOstream.C at line 80  
bad compression specifier 'banana', using 'uncompressed'
```

Listing 45: Failed banana test

11.2.2 Mandatory and optional settings

Some settings are expected by the solver to be made. If they are not present, OpenFOAM will return an error message. Other settings have a default value, which is used if the user does not specify a value. In this sense, settings can be divided into mandatory and optional ones.

As mandatory settings causes an error if they are not set, a simulation can be run only if all mandatory settings were made.

About errors

- There will be an error when mandatory settings were not made.
- There is no error message if an optional setting (that is necessary) was omitted. All optional controls have a default value and will be in place.
- There is no error message if a setting was made and that setting is not needed. The solver simply ignores it. Consequently the definition of a variable time step in *controlDict* does not necessarily mean, that the simulation is performed with variable time steps, e.g. if *icoFoam* (a fixed time step solver) is used.
- Sometimes an error message points to the setting of a keyword that is actually not faulty. See Section [11.2.3](#).

See Section [68.3](#) for a detailed discussion – including a thorough look at some source code – about reading keywords from dictionaries.

11.2.3 Pitfall: semicolon (;)

Similar to C++, lines are terminated by a semicolon. Listing [46](#) shows the content of the file *U1* in the *0*-directory. The line defining the boundary condition (BC) for the outlet was not terminated properly. Listing [47](#) shows the provoked error message. This error message does not mention *outlet*, but rather *walls* – keyword *walls is undefined*. The definiton of the boundary condition for the walls comes after the outlet definition. One reason for this may be, that OpenFOAM terminates reading the file after the missing semicolon causes a syntax error, and therefore the boundary condition for the walls remain undefined.

This example demonstrates that the error messages are sometimes not very meaningful if they are taken literally. The error was made at the definiton of the BC for the outlet. If only the definition. of the BC of the walls is examined, the cause for the error message will remain unclear, because the BC definition of the walls is perfectly correct.

```
dimensions      [0 1 -1 0 0 0 0];  
  
internalField    uniform (0 0 0);  
  
boundaryField  
{  
    inlet  
    {  
        type          fixedValue;  
        value         uniform (0 0 0.03704);  
    }  
  
    outlet  
    {  
        type          zeroGradient  
    }  
  
    walls  
    {  
        type          fixedValue;  
        value         uniform (0 0 0);  
    }  
}
```

Listing 46: Missing semicolon in the definition of the BC

```
--> FOAM FATAL IO ERROR:
keyword walls is undefined in dictionary "/home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam
/case/0/U1::boundaryField"

file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/case/0/U1::boundaryField from line
25 to line 47.

From function dictionary::subDict(const word& keyword) const
in file db/dictionary/dictionary.C at line 461.

FOAM exiting
```

Listing 47: Error message caused by missing semicolon

11.2.4 Switches

Besides key-value pairs there are switches. These enable or disable a function or a feature. Consequently, they only can have a logical value.

Allowed values are: *on/off*, *true/false* or *yes/no*. See Section 68.4.1 for a detailed discussion about valid entries.

11.3 The controlDict

In this *dictionary* controls regarding time step, simulation time or writing data to hard disk are located.

The settings in the **controlDict** are not only read by the solvers but also by all kinds of utilities. E.g. some mesh modification utilities obey the settings of the keywords **startFrom** and **startTime**. This has to be kept in mind when using a number of utilities for pre-processing.

11.3.1 Time control

In this Section the most important controls with respect to time step and simulation time are listed. This list makes no claim of completeness.

startFrom controls the start time of the simulation. There are three possible options for this keyword.

firstTime the simulation starts from the earliest time step from the set of time directories.

startTime the simulation starts from the time specified by the **startTime** keyword entry.

latestTime the simulation starts from the latest time step from the set of time directories.

startTime start time from which the simulation starts. Only relevant if **startFrom** **startTime** has been specified. Otherwise this entry is completely ignored²⁹.

stopAt controls the end of the simulation. Possible values are *{endTime, nextWrite, noWriteNow, writeNow}*.

endTime the simulation stops when a specified time is reached.

writeNow the simulation stops after the current time step is completed and the current solution is written to disk.

endTime end time for the simulation

deltaT time step of the simulation if the simulation uses fixed time steps. In a variable time step simulation this value defines the initial time step.

adjustTimeStep controls whether time steps are of fixed or variable length.³⁰ If this keyword is omitted, a fixed time step is assumed by default. When an adjustable time step is used, then the time step length Δt is controlled via a Courant number criterion. See Section 68.6.4 for more on the Courant number and its influence on the time step.

²⁹If the simulation is set to start from *firstTime* or *latestTime*, this keyword can be omitted or the value of this keyword can be anything – **startTime banana** does not lead to an error, what would be the case if the simulation started from a specific start time.

³⁰This keyword is important only for solvers featuring variable time stepping. A fixed time step solver simply ignores this control without displaying any warning or error message.

runTimeModifiable controls whether or not OpenFOAM should read certain dictionaries (e.g. *controlDict*) at the beginning of each time step. If this option is enabled, a simulation can be stopped by using setting **stopAt** to one of these values *{nextWrite, noWriteNow, writeNow}*, see Section 12.2.

maxCo when the simulation is run with an adjustable time step, then we can specify the maximum Courant number, which is used to impose an upper boundary on the time step size.

maxDeltaT when we run a simulation with an adjustable time step, we can provide a manual, hard upper boundary for the maximum time step. This setting limits the time step size, regardless of other conditions allowing for a larger time step, e.g. the Courant number criterion.

In Section 68.6 a couple of aspects regarding time step control are discussed.

11.3.2 Data writing

In *controlDict* the controls regarding data writing can be found. Often, it is not necessary to save every time step of a simulation. OpenFOAM offers several ways to define how and when the data is to be written to the hard disk.

writeControl controls the timing of writing data to file. Allowed values are *{adjustableRunTime, clockTime, cpuTime, runTime, timeStep}*.

runTime when this option is chosen, then every **writeInterval** seconds the data is written. This option has no influence on the time step. Hence, the interval at which data is written may/does not exactly match the entry in **writeInterval**, i.e. for a 1 s interval the data may be written at $t = 1.0012, 2.0005, \dots$ s.

adjustableRunTime this option allows the solver to adjust the time step, so that every **writeInterval** seconds the data can be written. This option imposes an upper boundary upon the time step. There must be at least 5 time steps between two instances at which data is written, i.e. $\Delta t \leq 0.2 * \text{writeInterval}$.

timeStep the data is written every **writeInterval** time steps. In this case, **writeInterval** is an integer, not a time.

writeInterval a value that controls the interval of data writing. This value gets its meaning from the value assigned to *writeControl*.

writeFormat controls how the data is written to hard disk. It is possible to write text files or binary files. Consequently, the options are *{ascii, binary}*.

writePrecision controls the precision of the values written to the hard disk.

writeCompression controls whether to compress the written files or not. By default compression is disabled. When it is activated, all written files are compressed using *gzip*.

timeFormat controls the format that is used to write the time step folders.

timePrecision specifies the number of digits after the decimal point. The default value is 6. If a simulation necessitates very small time step, then the default value for the time precision might interfere with the automatic Courant number based time step determination.

purgeWrite this setting control whether to clear out old time steps. The default value is 0, which means that no clearing out will be conducted. For enabling clearing out old time steps, valid values are positive integer numbers. If enabled with a non-zero value N , only the last N time steps will be retained. Once the simulation has written N time steps to disk, for every new time step saved, the oldest one will be deleted. The initial time step is not affected and will always remain in the case³¹.

³¹In the file *TimeIO.C* we see, that each time we reach write-time, the current time step is added to a FIFO stack. Subsequently, the stack's size is checked against the **purgeWrite** value. If the stack is larger, then one item will be removed.

Pitfall: timePrecision

OpenFOAM is able to automatically increase the value of `timePrecision` parameter if need arises, e.g. due to a reduction in (dynamic) time step size³². This is typically the case when a simulation diverges and the (dynamic) time step gets decreased by orders of magnitudes. However, simulations that do not diverge may also create the need for an increase in time precision.

```
Increased the timePrecision from 6 to 7 to distinguish between timeNames at time 4.70884
```

Listing 48: Exemplary solver output in the case of an automatic increase of the `timePrecision` value.

If a simulation that increased its time precision is to be restarted or continued from the latest time step, then the chosen time precision may not be sufficient to represent the present time step values, i.e. a `timePrecision` of 3 is not sufficient to represent the latest time step at $t = 0.1023$ s. OpenFOAM will apply rounding to the reach the selected number of digits behind the comma. Consequently, OpenFOAM will fail to find files at time $t = 0.102$ s.

This behaviour is hard to detect for an unaware user. The only clue for detection lies in this case in the fourth digit behind the comma, which is present in only in the name of the time step directory but not in the `timeName` that is looked up by OpenFOAM. Listing 49 shows the according error message and a directory listing of the case directory. It is up to the reader to decide whether this is an easy to spot error. The author took some time, which motivated him to elaborate on this issue in this little collection of errors and misbehaviour.

```
--> FOAM FATAL IO ERROR: cannot find file
file: /home/user/OpenFOAM/user-2.3.x/run/icoFoam/cavity/0.102/p at line 0.

From function regIOobject::readStream()
in file db/regIOobject/regIOobjectRead.C at line 73.

FOAM exiting

user@host:~/OpenFOAM/user-2.3.x/run/icoFoam/cavity$ ls
0 0.1023  constant  system
user@host:~/OpenFOAM/user-2.3.x/run/icoFoam/cavity$
```

Listing 49: Exemple of an error caused by an automatic increase of the `timePrecision` value in the previous simulation run. We fail to restart the simulation as OpenFOAM is not able to find the correct time step.

Non-pitfall: time step control & writeInterval control of functionObjects

Note, that the general settings in the file `controlDict` are not the only settings controlling the time step size. When we use `functionObjects` to extract data from a running simulation, we can control the interval at which the data from the `functionObjects` is written independently from the general write interval of the simulation. The `functionObjects` allow to use the setting `adjustableRunTime` in the same manner as we can use it for the simulation in general.

Thus in such a case, the time step of the simulation is controlled by the `functionObject` in addition to the general simulation settings. This can lead to a situation, when the write interval of the `functionObject` is sufficiently small, that the maximum allowed Courant number is not reached when running the simulation. This is normal behaviour, since there are multiple criteria at work to determine the time step size, and figuratively spoken: the lowest bidder wins.

Somewhat-non-pitfall: time step control & writeInterval

The OpenFOAM manual says, that when we select `runTime` as write-control, then the data is written every `writeInterval` seconds to disk. This does however, allow for the somewhat strange case of a write-interval which is actually (much) larger than the `writeInterval`.

³²A dynamic increase of the `timePrecision` value in simulations with fixed time steps indicates a setting in which the time precision is not sufficient to adequately represent the time step. This leads to a automatic increase of time precision after the first time step is written to disk. I.e. if Δt can't be represented with `timePrecision` number of digits after the comma, then $t_1 + \Delta t$ also can't be represented. Thus, t_1 and $t_1 + \Delta t$ would get the same time name and would consequently be indistinguishable. See Section 68.6.3 on more implementation details on this matter.

Since, we selected `runTime` as write-control, the `writeInterval` has no effect on the time step size. If the time step controls allow for a time step larger than `writeInterval`, e.g. via the Courant criterion, then OpenFOAM will oblige. In this case, after every time step OpenFOAM notices, that the time elapsed since the last write-to-disk is larger than the `writeInterval`. Thus, it is time to write to disk again.

If we do not want this kind of behaviour, then we need to select `adjustableRunTime` as our write-control, because then the time step will be checked against the `writeInterval`.

More an observation than a pitfall: time step control & `writeInterval`

If we select `adjustableRunTime` as our write-control, then the time step is adjusted to conform the interval set by `writeInterval`. It has been observed, that in this case the time step adjustment adheres to the following boundary:

$$\Delta t \leq \frac{\text{writeInterval}}{5}$$

Thus, OpenFOAM performs at least 5 time steps between writing data to disk. This behaviour might be confusing, and it is not explained in the documentation. Also, your trusted author has not been able to infer this behaviour from OpenFOAM's source code.

11.3.3 Loading additional Libraries

Additional libraries can be loaded with an instruction in `controlDict`. Listing 50 shows how an external library (in this case a turbulence model that is not included in OpenFOAM) is included. This model can be found at <https://github.com/AlbertoPa/dynamicSmagorinsky/>.

```
libs ( "libdynamicSmagorinskyModel.so" ) ;
```

Listing 50: Load additional libraries; *controlDict* entry

Note that the line in Listing 50 is a keyword (`libs`) followed by a list-type entry. Thus, the space between the keyword and the opening parenthesis is vital, since whitespace is used to separate a keyword from its value.

11.3.4 *functions*

functions, or *functionObjects* as they are called in OpenFOAM, offer a wide variety of extra functionality, e.g. probing values or run-time post-processing. See Section 59.

functions can be enabled or disabled at run-time.

11.3.5 Outsourcing a *dictionary*

Some definitions can be outsourced in a separate *dictionary*, e.g. the definition of a *probe-functionObject*.

All inclusive

In this case the *probe* is defined completely in *controlDict*.

```
functions
{
    probes1
    {
        type probes;
        functionObjectLibs ("libsampling.so");

        fields
        (
            p
            U
        );
        outputControl    outputTime;
        outputInterval   0.01;

        probeLocations
    };
}
```

```

        (
            (0.5 0.5 0.05)
        );
    }
}

```

Listing 51: Definition of a *probe* in *controlDict*

Separate *probesDict*

In this case the definition of the *probe* is done in a separate file – the *probesDict*. In *controlDict* the name of this dictionary is assigned to the keyword *dictionary*. This dictionary has to be located in the *system-directory* of the case. It is not possible to assign the path of this dictionary to this keyword.

```

functions
{
    probes1
    {
        type probes;
        functionObjectLibs ("libsampling.so");

        dictionary probesDict;
    }
}

```

Listing 52: External definition of *probes*; Entry in *controlDict*

```

fields
(
    P
    U
);

outputControl    outputTime;
outputInterval   0.01;

probeLocations
(
    (20.5 0.5 0.05)
);

```

Listing 53: Definition of *probes* in the file *probesDict*

Everything external

There is also the possibility to move the whole definition of a *functionObject* into a separate file. In this case the macro `#include` is used. This macro is similar to the pre-processor macro if C++.

```

functions
{
    #include "cuttingPlane"
}

```

Listing 54: Completely external definition of a *functionObject*; Entry in *controlDict*

```

cuttingPlane
{
    type           surfaces;
    functionObjectLibs ("libsampling.so");
    outputControl  outputTime;

    surfaceFormat  raw;
    fields         ( alpha1 );

    interpolationScheme cellPoint;
}

```

```

surfaces
(
    yNormal
    {
        type              cuttingPlane;
        planeType        pointAndNormal;
        pointAndNormalDict
        {
            basePoint      (0 0.1 0);
            normalVector   (0 1 0);
        }

        interpolate     true;
    );
}

```

Listing 55: Definition of a *cuttingPlane functionObject* in a seperate file named `cuttingPlane`

11.3.6 Pitfalls

timePrecision

If the time precision is not sufficient, then OpenFOAM issues a warning message and increases the time precision without aborting a running simulation.

Listing 56 shows such a warning message. The simulation time exceeded 100s and OpenFOAM figured that the time precision was not sufficient anymore.

```
--> FOAM Warning :
From function Time::operator++()
in file db/Time/Time.C at line 1024
Increased the timePrecision from 6 to 13 to distinguish between timeNames at time 100.001
```

Listing 56: Warning message: automatic increase of time precision

A side effect of this increase in time precision was a slight offset in simulation time. The time step of this simulation was 0.001s and the time steps were written every 0.5s. As it is clearly visible in Listing 57, the names of the time step folders indicate this offset. This effect on the time step folder names was the reason, the automatic increase of time precision was noticed by the author.

However, automatic increase of time precision has no negative effect on a simulation. This purpose of this section is to explain the cause for this effect.

```
101.5000000002
101.0000000002
100.5000000002
100
99.5
99
98.5
```

Listing 57: Time step folders after increase of time precision

11.4 Run-time modifications of dictionaries

If the switch *runTimeModifiable* is set *true*, *on* or *yes*; certain files (e.g. *controlDict* or *fvSolution*) are read anew, if a file has changed. In this way, e.g. the write interval can be changed during the simulation. If OpenFOAM detects a run-time modification it issues a message on the Terminal.

```
regIOobject::readIfModified() :
Re-reading object controlDict from file "/home/user/OpenFOAM/user-2.1.x/run/
multiphaseEulerFoam/bubbleColumn/system/controlDict"
```

Listing 58: Detected modifaction of *controlDict* at run-time of the solver

11.5 The fvSolution dictionary

The file `fvSolution` contains all settings controlling the solvers and the solution algorithm. This file must contain two dictionaries. The first controls the solvers and the second controls the solution algorithm.

11.5.1 Solver control

The `solvers` dictionary contains settings that determine the work of the solvers (e.g. solution methods, tolerances, etc.).

11.5.2 Solution algorithm control

The dictionary controlling the solution algorithm is named after the solution algorithm itself. I.e. the name of the dictionary controlling the PIMPLE algorithm is `PIMPLE`. Note, that the name of this dictionary is in upper case letters unlike most other dictionaries.

Listing 59 shows an example of a `PIMPLE` dictionary. See Section 52.2 for a detailed discussion on the PIMPLE algorithm.

```
PIMPLE
{
    nOuterCorrectors 1;
    nCorrectors      2;
    nNonOrthogonalCorrectors 0;
    pRefCell         0;
    pRefValue        0;
}
```

Listing 59: The `PIMPLE` dictionary

11.6 Command line arguments

OpenFOAM's solvers and utilities can be controlled by a set of command line arguments. Some of them are common to all or many executables, some might be special to a certain tool.

11.6.1 Getting help: `-help`

The most important command line argument is `-help`. This is common to all solvers and tools of OpenFOAM and it displays a summary of the respective tool.

11.6.2 Getting in control: `-dict`

Certain tools expect to find a specific dictionary containing necessary information. With the `-dict` option, the user can tell the executable, where to look for the dictionary. To the authors knowledge, all tools expecting a dictionary assume a default location and filename. E.g. in older versions of OpenFOAM `blockMesh` expected to find a dictionary named `blockMeshDict` in the `constant/polyMesh` sub-directory of the case's root, in newer versions it checks also the `system` directory. If the user chooses to put the dictionary containing into a different folder, he or she can do so, however, the path to the dictionary now needs to be passed using the `-dict` command line argument.

no control dict

The help summary displayed by `-help`, in some cases, describes the `-dict` options as follows: *read control dictionary from specified location*. However, the dictionary specified with the `-dict` option is not the `controlDict`. Thus, all entries that go into `controlDict` need to go into `controlDict`. For some tools the description of the `-dict` option seems a little ambiguous. What is meant by control dictionary in this case is the dictionary controlling this specific tool, such as `blockMeshDict` controls `blockMesh` or `snappyHexMeshDict` controls `snappyHexMesh`.

12 Usage of OpenFOAM

12.1 Use OpenFOAM

In the most simple case, Listing 60 represents a complete simulation-run.

```
blockMesh
checkMesh
icoFoam
paraFoam
```

Listing 60: Compute a simple simulation case

The first command, *blockMesh*, creates the mesh. The geometry has to be defined in *blockMeshDict*. *checkMesh* performs, as the name suggests, checks on the mesh. The third command is also the name of the solver. All solvers of OpenFOAM are invoked simply by their name. The last command opens the post-processing tool ParaView.

There are additional tasks that extend the sequence of commands shown in Listing 60. These can be

- Convert a mesh created by an other meshing tool, e.g. import a Fluent mesh
- Initialise fields
- Set up an parallel simulation; see Section 12.5

12.1.1 Redirect output and save time

The solver output can be printed to the Terminal or redirected to a file. Listing 61 shows how the solver output is redirected to a file named *foamRun.log*.

```
mpirun -np N icoFoam -parallel > foamRun.log
```

Listing 61: Redirect output to a file

Redirecting the solver output does not only create a log file, it also save the time that is needed to print the output to the Terminal. In some cases this can reduce simulation time drastically. However, writing to hard disk also takes its time.

Time steps	Cells	Print to Terminal		Redirect to file	
		executionTime	clockTime	executionTime	clockTime
5000	400	6,36	9	4,6	6
10000	400	12,71	18	9,22	10
12500	400	15,8	23	11,54	12
25000	400	32,33	47	22,99	23
5000	1600	9,74	11	9,3	10
5000	6400	282,19	283	282,83	283

Table 1: Run-time *cavity* test case

executionTime is the time the processor takes to calculate the solution of the case. *clockTime* is the time that elapses between start and end of the simulation, this is the time the wall clock indicates. The value of the *clockTime* is always larger than the value of the *executionTime*, because computing the solution is not the only task the processor of the system performs. Consequently, the value of the *ClockTime* depends on external factors, e.g. the system load.

Redirect output to nowhere

If the output of a program is of no interest it can be redirected to virtually nowhere to prevent it from being displayed on the Terminal. Listing 62 shows how this is done. `/dev/null` is a special file on unix-like systems that discards all data written to it.

```
mpirun -np N icoFoam -parallel > /dev/null
```

Listing 62: Redirect output to nowhere

12.1.2 Run OpenFOAM in the background, redirect output and read log

In Section 12.1.1 the redirection of the solver output was explained. To monitor the progress of running calculation the end of the log can be read with the `tail` command.

Listing 63 shows how a simulation with `icoFoam` is started and the solver output is redirected. The `&` at the end of the line causes the invoked command to be executed in the background. The Terminal remains therefore available. Otherwise the Terminal would be waiting for `icoFoam` to finish before executing any further commands.

The second command invoked in Listing 63 prints the last 5 lines of the log file to the Terminal. `tail` returns the last lines of a text file. Without the parameter `-n` `tail` returns by default the last 10 lines.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ icoFoam > foamRun.log &
[1] 10416
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ tail foamRun.log -n 5
ExecutionTime = 0.74 s  ClockTime = 1 s

Time = 1.12

Courant Number mean: 0.444329 max: 1.70427
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$
```

Listing 63: Read redirected output from log file while the solver is running

12.1.3 Save hard disk space

OpenFOAM saves the data of the solution in intervals in time directories. The name of a time directory represents the time of the simulation. Listing 64 shows the content of a case directory after the simulation has finished. Besides the three folders that define the case (`0`, `constant` and `system`) there are more time directories and a `probes1`-folder present.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls
0 0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8 0.9 1 constant probes1 system
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$
```

Listing 64: List folder contents

The `probes1`-directory contains the data generated by the functionObject named `probes1`. The time-directories contain the solution data of the whole computational domain. Listing 65 shows the contents of the `0`- and the `0.1`-directory. Typically, time-directories generated in the course of the computation contain more data than the `0`-directory defining the initial conditions.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavityBinary$ ls 0
p_U
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavityBinary$ ls 0.1
p_phi_U_uniform
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavityBinary$
```

Listing 65: List folder contents

Using binary files or compressing files

In general the time-directories use the majority of the hard disk space a completed case takes. If the time-directories are saved in binary instead of ascii format, these use generally a little less space. Another advantage of storing time step data in binary format, the time step data has full precision.

OpenFOAM also offers the possibility to compress all files in the time step directories. For compression OpenFOAM uses *gzip*, this is indicated by the files names in the time step directories, i.e. `alpha1.gz` instead `alpha1`.

Table 2 shows a comparison of hard disk use. The most reduction is achieved by compressing ascii data files. However, storing the time step data in ascii has the disadvantage that the numerical precision is limited to the number of digits stated with the `writePrecision` keyword in the `controlDict`. In this case `writePrecision` was set to 6, i.e. numbers have up to 6 significant digits. Compressing the binary files shows less effect than compressing the ascii files, which indicates that the binary files contain less redundant bytes.

Write settings	Used space	reduction	
ascii	45.5 MB		
ascii, compressed	16.7 MB	28.8 MB	-63.3 %
binary	33.8 MB	11.7 MB	-25.7 %
binary, compressed	28.8 MB	16.7 MB	-36.7 %

Table 2: Comparison of hard disk space consumption

Make sure to avoid unnecessary output

Disk space can easily be wasted by writing everything to disk. Not only writing too many time steps to disk can waste space, *functionObjects* can be the culprit too. See [59.6.3](#).

12.2 Abort an OpenFOAM simulation

An OpenFOAM simulation ends when the simulation time reaches the value specified with the `endTime` keyword in `controlDict`. However, we also need to be able to stop a simulation prematurely. This section explains how to end a simulation in a controlled manner, i.e. the current state of the solution is written to the harddisk in order to be able to continue the simulation at a later time.

As a prerequisite, the `runTimeModifiable` flag has to be enabled in `controlDict`. This keyword controls whether `controlDict` is monitored for changes during the run-time of the simulation. This is necessary for this method to work. Otherwise, the simulation will stop at `endTime`.

To abort a simulation we simply need to change the value of the `stopAt` entry in `controlDict` from `endTime` to `writeNow`. When OpenFOAM detects the change and re-reads `controlDict`, this causes OpenFOAM to finish its current time step and write the state of the solution to disk before ending the run.

12.3 Terminate an OpenFOAM simulation

This section describes how to terminate a running OpenFOAM simulation. See Section [12.2](#) on how to abort a simulation in a controlled manner, i.e. saving the current solution and stop the simulation.

This section explains how terminate a running simulation immediately and without saving the current solution. Use this approach when you wouldn't use the solution anyway, e.g. because you chose incorrect settings.

12.3.1 Terminate a process in the foreground

If a command is executed in the Terminal without any additional parameters the process runs in the foreground. The Terminal is therefore busy and can not be used until the process is finished. When a process is running in the foreground it can easily terminated by pressing **[CTRL]+[C]**. Listing [66](#) features the GNU command `sleep`. The only function of this command is to pause for a specified amount of time. With this command the premature termination of a process can be tried.

```
user@host:~$ sleep 3
user@host:~$
```

Listing 66: Keep the Terminal busy

12.3.2 Terminate a background process

If a process runs in the background, the Terminal is free to be used for further tasks while the process is running. In this case, the background process can not be terminated by pressing **[CTRL]+[C]** because the Operating System can not tell which background process the user wants to terminate.

Identify the process

On UNIX based systems every process is identified by a unique number. This is the PID, the **process identifier**. The PID is equivalent to a licence plate for a car. During run-time this number is unique. However, after a process has finished the PID of this process is available for other, later processes.

To find out which processes are currently running, invoke the command *ps*. This lists all running processes. Without any further parameters only the processes that were executed from the current Terminal are listed. Listing 67 shows the result if a new Terminal is opened and *ps* is called. The first entry – *bash* – is the Terminal itself. The second entry – *ps* – is the only other process active at the time *ps* looks for all running processes. The PID is listed in the first column of Listing 67. Depending on the parameters passed to *ps* the output can be formatted differently.

```
user@host:~$ ps
  PID TTY      TIME CMD
13490 pts/1    00:00:00 bash
13714 pts/1    00:00:00 ps
user@host:~$
```

Listing 67: List processes in a fresh Terminal

The output of 67 is rather dull. However, there are lots of parameters telling *ps* what to do. The option **-e** makes *ps* list all systemwide running processes. The output of such a call can be quite long, because *ps* lists all processes started by the users as well as all system processes³³.

The option **-F** controls the output format of *ps*. In this case **-F** stands for *extra full*. This means the output contains a lot of information. Another option to display much information is **-1**. This option truncates the names of the processes to 15 characters, whereas **-F** displays not only the full name of the process, it also displays the parameters with which the processes were called.

```
ps -ef
```

Listing 68: List all running processes of the system

ps displays much information about a process. For terminating a process only the PID is necessary.

Search in the list of processes

The output of *ps* is a list which can be quite long. To terminate a certain process its PID has to be known. Searching a number in a list of numbers can be quite painful and errorprone. Therefore it would be handy to search in the list *ps* has returned for the desired process.

Before all else, *grep* does the trick. And now for something more detailed. *grep* is a program that searches the lines of its input for a certain pattern. *grep* can use a file or the standard input as its input. As it is unpractical to redirect the output of *ps* into a file only for *grep* to read it, we directly redirect the output of *ps* to the input of *grep*. This is achieved by the use of a pipe.

Listing 69 shows how this is done. The first part of the command invoked – **ps -ef** – calls *ps* to list all processes currently running in great detail. The option **-F** is used to make sure long process names can be distinguished, e.g. to tell *buoyantBoussinesqPimpleFoam* apart from *buoyantBoussinesqSimpleFoam*.

³³System processes are processes run by the Operating System itself.

Both are standard solvers of OpenFOAM. The bold part are the first 15 characters of the solver's name. If the option `-F` was omitted and both solvers were running, the results of `ps` would be ambiguous.

The second part of the command invoked in Listing 69 shows the call of `grep`. `grep` can be called with one or two arguments. If only one argument is passed to `grep`, `grep` uses the standard input as input. If `grep` is called with two parameters, the second argument has to specify the file from which `grep` has to read. As `grep` is called with only one argument, it reads from the standard input.

Because it would be even more boring to type the list returned by `ps` we redirect the output of `ps` to the standard input of `grep`. This is done by the pipe. The character `|` marks the connection of two processes in the Terminal. The command left of the `|` passes its output directly to the command specified right of the `|`.

Now we can read and interpret Listing 69. It shows the output of the search for all running processes containing the pattern `Foam`. In this case a parallel computation is going on. The first line of the result is `mpirun`. This process controls the parallel running solvers. The next four lines are the four instances of the solver. How parallel simulation works is explained in Section 12.5. The second last entry of the result is `grep` waiting for input³⁴. The last line of the result is the pdf viewer which displays this document at that time. This example shows that is important to choose the pattern wisely, the search may return unexpected results.

```
user@host:~$ ps -ef | grep Foam
user 11005 5117 0 17:11 pts/2    00:00:05 mpirun -np 4 twoPhaseEulerFoam -parallel
user 11006 11005 99 17:11 pts/2   00:40:27 twoPhaseEulerFoam -parallel
user 11007 11005 99 17:11 pts/2   00:40:28 twoPhaseEulerFoam -parallel
user 11008 11005 99 17:11 pts/2   00:40:27 twoPhaseEulerFoam -parallel
user 11009 11005 99 17:11 pts/2   00:40:26 twoPhaseEulerFoam -parallel
user 11673 11116 0 17:52 pts/12  00:00:00 grep --color=auto Foam
user 32041     1 0 Aug01 ?      00:00:31 evince /tmp/lyx_tmpdir.J18462/lyx_tmpbuf0/open
    FoamUserManual_CD Lv2.pdf
user@host:~$
```

Listing 69: Search for processes

List only specified processes

You can tell `ps` directly in which processes you are interested. The option `-C` of `ps` makes `ps` list only those processes that stem from a certain command. Listing 70 shows the output when `ps -C twoPhaseEulerFoam` is typed into the Terminal. In this case also there are four parallel processes running. Notice, that only the processes directly related to the solvers are shown. No other results are displayed unlike in Listing 69.

One has to bear in mind, that `ps -C` does not search for patterns. If the command name passed to `ps` as an argument is misspelled, `ps` will not display the desired result. Listing 71 shows the effect of typos in this case. The truncation of the process name in the list does not affect the search if the passed command name is equal or longer than the truncated process name. The first two commands issued in Listing 71 result in a list of all running instances of the solver. If the passed argument is shorter than the truncated process name – the third command – `ps` does not output any results. Also if there is a typo in the passed argument, `ps` does not find anything.

```
user@host:~$ ps -C twoPhaseEulerFoam
  PID TTY      TIME CMD
11006 pts/2    00:47:44 twoPhaseEulerFoam
11007 pts/2    00:47:44 twoPhaseEulerFoam
11008 pts/2    00:47:44 twoPhaseEulerFoam
11009 pts/2    00:47:43 twoPhaseEulerFoam
user@host:~$
```

Listing 70: List all instances of `twoPhaseEulerFoam`

```
user@host:~$ ps -C twoPhaseEulerFoa
  PID TTY      TIME CMD
12741 pts/0    00:00:34 twoPhaseEulerFo
12742 pts/0    00:00:34 twoPhaseEulerFo
12743 pts/0    00:00:34 twoPhaseEulerFo
12744 pts/0    00:00:34 twoPhaseEulerFo
```

³⁴On most Unix-like systems processes connected by a pipe are started at the same time. For this reason `grep` is already running while `ps` is listing all running processes.

```

user@host:~$ ps -C twoPhaseEulerFo
    PID TTY          TIME CMD
12741 pts/0    00:00:36 twoPhaseEulerFo
12742 pts/0    00:00:36 twoPhaseEulerFo
12743 pts/0    00:00:36 twoPhaseEulerFo
12744 pts/0    00:00:36 twoPhaseEulerFo
user@host:~$ ps -C twoPhaseEulerF
    PID TTY          TIME CMD
user@host:~$ ps -C twPhaseEulerFoa
    PID TTY          TIME CMD

```

Listing 71: List all instances of *twoPhaseEulerFoam* – the effect of typos

Terminate

The operating system interacts with running processes using signals. The user can also send signals to processes using the command *kill*. *kill* sends by default the termination signal. To identify the process to which the signal is to be sent, the PID of this process has to be passed as an argument.

Listing 72 shows how the programm sleep is executed, all running processes are listed, the running instance of sleep is terminated and the running processes are listed again. When *ps* was executed the second time, a message is displayed stating the process has been terminated³⁵. If the process would not have been terminated the message at the “natural” end of the process would be like in Listing 73³⁶.

```

user@host:~$ sleep 20 &
[1] 13063
user@host:~$ ps
    PID TTY          TIME CMD
12372 pts/0    00:00:00 bash
13063 pts/0    00:00:00 sleep
13064 pts/0    00:00:00 ps
user@host:~$ kill 13063
user@host:~$ ps
    PID TTY          TIME CMD
12372 pts/0    00:00:00 bash
13065 pts/0    00:00:00 ps
[1]+  Beendet                  sleep 20
user@host:~$

```

Listing 72: Terminate a process using *kill*

```

user@host:~$ sleep 1 &
[1] 13126
user@host:~$ ps
    PID TTY          TIME CMD
12372 pts/0    00:00:00 bash
13127 pts/0    00:00:00 ps
[1]+  Fertig                  sleep 1
user@host:~$

```

Listing 73: The natural end of a process

```

user@cluster user> sleep 10 &
[1] 31406
user@cluster user> kill 31406
user@cluster user>
[1]  Terminated                sleep 10
user@cluster user>

```

Listing 74: Terminate a process using *kill* on a different machine

³⁵On other systems this message is displayed immediately – see Listing 74. In this case the procedure was tried on the local computing cluster.

³⁶A system with English language setting the message would read **Terminated** if the process would have been terminated and **Done** if the process would have been allowed to finish.

12.4 Continue a simulation

If a simulation has ended at the end time or if it has been aborted there may be the need to continue the simulation. The most important setting to enable a simulation to be continued has to be made in the file `controlDict`. There, the keyword `startFrom` controls from which time the simulation will be started.

The easiest way to continue a simulation is to set the `startFrom` parameter to `latestTime`. Then, if necessary, the value of `endTime` needs to be adjusted. After this changes, the simulation can be continued by simply invoking the solver in the Terminal.

12.5 Do parallel simulations with OpenFOAM

OpenFOAM is able to do parallel simulations. There is no great difference between calculating a case with one single process or using many parallel processes. The only obvious additional task is to split the computation domain into several pieces. This step is called *domain decomposition*. After the domain is decomposed several instances of the solver are running the case on a subdomain each. Additionally, the invocation of the solver differs from the single process case.

In fact, not only solvers are capable to be run in parallel, also many pre- and post-processing tools can be similarly applied in parallel.

12.5.1 Starting a parallel simulation

To enable a simulation using several parallel instances of a solver, OpenFOAM uses the MPI standard in the implementation of OpenMPI. OpenMPI ensures that all parallel instances of the solver run synchronously. Otherwise the simulation would generate no meaningful results. In order to be able to manage all parallel processes the simulation has to be started using the command `mpirun`.

Listing 75 shows how a parallel simulation using 4 parallel processes is started. The solver outputs are redirected into a file called `> foamRun.log` and the simulation runs in the background of the Terminal. So the same Terminal can be used to monitor the progress of the calculation. See Section 12.1.2 for a discussion about running a process in the background.

The output message in the Listing shows the PID of the running instance of `mpirun`. This PID can be used to terminate the parallel calculation, like it is explained in Section 12.3.2.

```
user@host:~$ mpirun -np 4 icoFoam -parallel > foamRun.log &
[1] 11099
user@host:~$
```

Listing 75: Run OpenFOAM with 4 processes

The number of processes, in this case 4, has to be equal the number of *processor** folders. These folders are created by `decomposePar` and their number is defined in `decomposeParDict`. See Section 12.5.2 for information about domain decomposition.

If this numbers – the number of *processor** folders and the number of parallel processes with which `mpirun` is invoked – are not equal OpenFOAM issues an error message similar to Listing 76. In this case the domain was decomposed into 4 subdomains and it was tried to start the parallel simulation with 2 processes. If the parallel simulation is called with too many processes, OpenFOAM issues an error message like in Listing 77. The first example shows, that OpenFOAM reacts differently whether the parallel job was started with too little or too many processes.

```
[0] --> FOAM FATAL ERROR:
[0] "/home/user/OpenFOAM/user-2.1.x/run/icoFoam/cavity/system/decomposeParDict" specifies 4
processors but job was started with 2 processors.
```

Listing 76: Run OpenFOAM with too little parallel processes

```
[0] --> FOAM FATAL ERROR:
[0] number of processor directories = 4 is not equal to the number of processors = 8
```

Listing 77: Run OpenFOAM with too many parallel processes

Pitfall: -parallel

The parameter `-parallel` is important. If this parameter is omitted, the solver will be executed n times. Listing 78 shows the output of the command `ls` when it is run with `mpirun` with two processes. In this case `ls` is simply run twice.

If the parameter `-parallel` is missing, the same happens as in the case of `ls`. The simulation is run by n processes at roughly the same time. Listing 79 shows the first lines of output of a situation where the `-parallel` parameter was omitted. All solvers start the calculation of the whole case and write their output to the Terminal. The output appears on the Terminal in the order as it is generated by the solvers – in other words, the output on the Terminal is completely disarranged. If the `processor*` folders are present.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ mpirun -np 2 ls
0 constant system
0 constant system
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$
```

Listing 78: Run `ls` using 2 processes

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ mpirun -np 4 icoFoam
/*-----*/
| ====== | F ield | OpenFOAM: The Open Source CFD Toolbox
| \ \ / O peration | Version: 2.1.x
| \ \ / A nd | Web: www.OpenFOAM.org
| \ \ \ M anipulation |
\*-----*/
Build : 2.1.x-6e89ba0bcd15
Exec  : icoFoam
Date  : Jan 29 2013
Time  : 10:51:12
Host  : "host"
PID   : 25622
/*-----*/
| ====== | F ield | OpenFOAM: The Open Source CFD Toolbox
| \ \ / O peration | Version: 2.1.x
| \ \ / A nd | Web: www.OpenFOAM.org
| \ \ \ M anipulation |
\*-----*/
Build : 2.1.x-6e89ba0bcd15
Exec  : icoFoam
```

Listing 79: Run `icoFoam` without the `-parallel` parameter

Pitfall: domain decomposition

If there was no domain decompositin prior to starting a parallel simulation, OpenFOAM will issue an corresponding error message.

```
[0] --> FOAM FATAL ERROR:
[0] twoPhaseEulerFoam: cannot open case directory "/home/user/OpenFOAM/user-2.1.x/run/
twoPhaseEulerFoam/testColumn/processor0"
[0]
[0] FOAM parallel run exiting
```

Listing 80: Missing `domain decomposition`

Pitfall: domain resonstruction

After a parallel simulation has ended, all data is residing in the `processor*` folders. If `paraView` is started – without prior domain reconstruction – `paraView` will only find the data of the 0 directory.

12.5.2 Domain decomposition

Before a parallel simulation can be started the domain has to be decomposed into the correct number of subdomains – one for each parallel process. The parallel processes calculate on their own subdomain and exchange data of the border regions at the end of each time step. This is also the reason why the parallel processes have to be synchronous. Otherwise, processes with a lower computational load would overtake other processes and they would exchange data from different times.

Just before starting the simulation the domain has to be decomposed. The tool *decomposePar* is used for this purpose. Other operations, e.g. initialising fields using *setFields* have to take place before the domain decomposition. *decomposePar* reads from *decomposeParDict* in the *system* directory. This file has to contain at least the number of subdomains and the decomposition method.

decomposePar creates the *processor** directories in the case directory. Inside the *processor** folders a *0* and a *constant* folder are created. The *0* folder contains the initial and boundary conditions of the subdomain and the *constant* folder contains a *polyMesh* folder containing the mesh of the subdomain.

All parallel processes read from the same *system* directory, as the information stored there is not affected by the domain decomposition. Also the files in the *constant* directory are not altered.

Pitfall: Existing decomposition

If the domain has already been decomposed and *decomposePar* is called again, e.g. because the number of subdomains has been changed or some fields have been reinitialised, OpenFOAM issues an error message. Listing 81 shows an example. In this case the domain has already been decomposed into 2 subdomains and the attempt is made to decompose it again. OpenFOAM always issues an error message, whether the number of subdomains has changes or not.

The resulting error message proposes two possible solutions. The first is to invoke *decomposePar* with the *-force* option to make *decomposePar* remove the *processor** folders before doing its job. The second proposed solution is to manually remove the *processor** folders. In this case the error message contains the proper command to do so. The user can retype the command or copy and paste it into the Terminal.

```
--> FOAM FATAL ERROR: Case is already decomposed with 2 domains, use the -force option or
    manually
remove processor directories before decomposing. e.g.,
  rm -rf /home/user/OpenFOAM/user-2.1.x/run/icoFoam/cavity/processor*
```

Listing 81: Already decomposed domain

Time management with *decomposePar*

In the course of an update of OpenFOAM decompose gained the option *-time*. This enhancement took place between the release of OpenFOAM 2.1.0 and OpenFOAM 2.1.1. Such enhancements typically first appear in the repository release OpenFOAM 2.1.x. So, it may be, that some installations of OpenFOAM 2.1.x contain this feature and some not depending on the time of installation or the time of the last update.

The option *time* lets the user specify a time from which or a time range in which the domain is to be decomposed. Listing 82 shows some examples of how this option works.

The option *-latestTime* makes *decomposePar* use the latest time step as starting time step for the subdomains.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls
0 0.1 0.2 constant probes1 processor0 processor1 processor2 system
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ decomposePar -time 0.1:0.2 -force > /dev/null
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls processor0
0.1 0.2 constant
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ decomposePar -time 0.2 -force > /dev/null
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls processor0
0.2 constant
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$
```

Listing 82: Time management with *decomposePar*

12.5.3 Domain reconstruction

To be able to look at the results the data has to be reassembled again. This job is done by *reconstructPar*. This tool collects all data of the *processor** folders and reconstructs the original domain using all the generated time step data. After *reconstructPar* has finished the data of the whole domain resides in the case directory and the data of the subdomains resides in the *processor** folders.

Listing 83 shows the content of the case directory after a parallel simulation has finished. The first command is a simple call of ls to display the contents of the case directory. This is not different from the situation before the parallel simulation was started with the exception of the log file. However, this log file could be from a previous run. So, listing the contents after a parallel simulation has finished carries no real information.

The second command lists the contents of the *processor0* directory. In this directory – as well as in all other *processor** folders – there is time step data. The third command reconstructs the domain. After this tool has finished, the case directory also contains time step data. The last command lists the contents of the *processor0* folder again. This data has not been removed. So, a finished parallel case stores its time step data twice and therefore uses a lot of space.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls
0 constant foamRun.log probes1 processor0 processor1 processor2 processor3 system
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls processor0
0 0.1 0.2 0.3 0.4 0.5 constant
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ reconstructPar > foamReconstruct.log &
[1] 26269
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls
0 0.1 0.2 0.3 0.4 0.5 constant foamReconstruct.log foamRun.log probes1 processor0
processor1 processor2 processor3 system
[1]+  Fertig                  reconstructPar > foamReconstruct.log
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$ ls processor0
0 0.1 0.2 0.3 0.4 0.5 constant
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/cavity$
```

Listing 83: A finished parallel simulation

Time management

If a simulation has been startet from $t = t_1$ the domain has to be reconstructed for times $t > t_1$. Calling *reconstructPar* without any options regarding time, the program starts reconstructing the domain at the earliest time. To prevent the tool from reconstructing already reconstructed time steps the *-time* option can be used. Listing 84 shows how simulation results are reconstructed for $t \leq 60$ s.

```
reconstructPar -time 60:
```

Listing 84: Zeitparameter für *reconstructPar*

Another option to reconstruct only the new time steps is the command line option *-newTimes*. By using this option the proper time span to reconstruct is automatically determined.

12.5.4 Run large studies on computing clusters

Simulating parallel on a machine brings some advantages and enables the user to run even large simulations on a workstation. However, if the cases is very large, or parametric studies are to be conducted, using the workstation can be counter productive. Therefore, simulating on a computing cluster is the method of choice for large scale calculations. The user can follow a two step method.

1. Set up the case and run some test simulations, e.g. for a small number of time steps, on the workstation to ensure the simulation runs
2. Do the actual simulation on the cluster

The fact, that OpenFOAM runs on a great number of platforms enables the user to do simulations on the workstation as well as on a big cluster with tens or hundreds of processors.

Run OpenFOAM using a script

Section 78.5 explaines how to set up a script that runs multiple cases.

12.5.5 Weird MPI behaviour

Parallel simulation silently fails when a network interface is disconnected

Some weird behaviour was observed by your trusted author with regards to running parallel simulations. Although, not the fault of OpenFOAM, it still is of interest, as this behaviour can be quite annoying and mysterious. Furthermore, when OpenFOAM simulations silently fail, then the first route of investigation for most users is most probably related to OpenFOAM, as can be seen here³⁷ in the OpenFOAM forums.

It was observed that parallel simulations on a laptop simply stopped without error message, when its fragile wifi connection dropped. Apparently, MPI uses all interfaces it can find for communication between its child processes. If at the start of a simulation, wifi is available, MPI will use the wifi network interface. If the wifi connection fails, then `mpirun` silently stops.

This behaviour was reported in OpenFOAM's bug reporting platform³⁸, yet the reason is caused by MPI itself. Thus, OpenFOAM is not at fault here. This behaviour was also reported with respect to general MPI use³⁹.

Thus, if a network connection causes problems, `mpirun` can be explicitly told not to use a specific interface. Listing 85 shows how to keep `mpirun` from using the wifi interface. What is important to note in the listing, is the twofold exclusion of the wifi interface. Both, OOB (out of band messaging) and BTL (MPI point-to-point Byte Transfer Layer, used for MPI point-to-point messages on some types of networks) need to be told not to use wifi.

```
mpirun --mca oob_tcp_if_exclude wlp3s0 --mca btl_tcp_if_exclude wlp3s0 -np 2
someFoamApplication -parallel > logFile.log &
```

Listing 85: Excluding the wifi interface (named `wlp3s0` in this case) form use by `mpirun`

Alternatively, this setting can also be made permanent via an environment variables⁴⁰.

12.6 Using tools

OpenFOAM consists besides of solvers of a great collection of tools. These tools are used for all kind of operations.

All solvers and tools of OpenFOAM⁴¹ assume that they are called from the case directory. If an executable is to be called from another directory the path to the case direotry has to be specified. Then the option `-case` has to be used to specify this path.

Listing 86 shows the error message displayed by the tool `fluentMeshToFoam` as it was executed from the `polyMesh` directory. The tool added the relative path `system/controlDict` to the current working directory. This resulted in an invalid path to `controlDict` as the error message tells the user. Actually, the error message states that the file could not be found. This does not solely imply an invalid path. The file could simply be missing.

```
--> FOAM FATAL IO ERROR:
cannot find file

file: /home/user/OpenFOAM/user-2.1.x/run/icoFoam/testCase/constant/polyMesh/system/controlDict
at line 0.

From function regIOobject::readStream()
in file db/regIOobject/regIOobjectRead.C at line 73.

FOAM exiting
```

Listing 86: Wrong path

³⁷<https://www.cfd-online.com/Forums/openfoam-bugs/191087-openfoam-stops-when-there-no-internet.html>

³⁸<https://bugs.openfoam.org/view.php?id=2821>

³⁹<https://stackoverflow.com/questions/32162317/mpirun-hangs-when-connected-to-wifi/49662866>

⁴⁰<https://www.open-mpi.org/faq/?category=tuning#setting-mca-params>

⁴¹No exception known to the author.

The correct usage of the `-case` option is shown in Listing 87. There the correct path to the case directory – two levels upwards – is specified using `../..`⁴²

```
user@host:~/OpenFOAM/user-2.1.x/run/icoFoam/testCase/constant/polyMesh$ fluent3DMeshToFoam -  
case ../../caseMesh.msh
```

Listing 87: Specify the correct path to the case

12.7 Using OpenFOAM on a local machine and a cluster

If you are using OpenFOAM, or learning to use OpenFOAM, there is a big chance that you will use OpenFOAM not only on your local machine, the computer you sit in front of, but also on a remote computing cluster.

12.7.1 General tips

Use the same versions locally and remotely

In order to avoid obscure problems stemming from version conflicts, make sure to use the same version on the local machine as on the cluster. Usually, a computing cluster is managed by an IT department, which is responsible to maintain the cluster. Ideally, the cluster has the point-release(es) of OpenFOAM installed. This ensures, that the behaviour of OpenFOAM will be clearly defined.

Thus, we can only influence which versions of OpenFOAM are installed on our local machine. Installing several versions of OpenFOAM side-by-side is no problem. Thus, there should be no reason not to install the same version(s) of OpenFOAM, which are installed on the cluster, on the local machine. This way you can make sure that a case will run on the cluster by testing it on the local machine first.

12.7.2 Pitfalls

Delete dynamicCode folder

A very common workflow, when using OpenFOAM on a remote computing cluster, involves setting-up the case on your local machine, and then pass the case to the number crunching cluster. Set-up the case, and subsequent trouble-shooting is best done locally, since generally time on clusters is a limited resource, which is best not wasted with trouble-shooting.

However, when tinkering with a case with dynamic code, e.g. coded boundary conditions or coded function objects, we need to delete the `dynamicCode` directory from the case, before passing the case on to the cluster. The local machine and the cluster, are most probably not completely binary compatible, causing the parts relying on dynamic code to cause OpenFOAM to abort. By deleting the `dynamicCode` folder, we ensure that the OpenFOAM installation compiles all dynamic code related parts of the case by itself.

A common nuisance related to this topic occurs when dealing with cases featuring coded boundary conditions, such as `codedFixedValue`. Operations on the local machine, e.g. parallel decomposition, cause the local OpenFOAM installation to compile the coded boundary condition. Later, when starting the parallel run of the case on the remote machine, the coded boundary condition is not recognized by the remote OpenFOAM installation, and thus (remote) OpenFOAM aborts with an error message saying that the specified boundary condition does not exist.

12.8 Using scripts to run OpenFOAM

Running a typical OpenFOAM simulation case involves the use of several tools and solvers. At the minimum, we need to create a mesh and run a solver. Typically, there might be more operations related to pre- and/or post-processing.

In the tutorials of OpenFOAM we can see that heavy use is made of shell scripts to combine all the individual tasks regarding the running of a case into a single script for convenience.

While technically using shell scripts is a topic related to the general use of Linux, the author deems the use of shell scripts quite integral to the way OpenFOAM was and is designed. Thus, discussing the use of

⁴²On most Linux or Unix systems `.` refers to the current directory and `..` refers to the directory above the current one. To change in the Terminal one directory upwards on Linux `cd ..` does the job and on MS-DOS or Windows `cd..` is the proper command.

Also, on Linux systems the tilda `~` refers to the home directory of the current user.

shell scripts with respect to using OpenFOAM deserves a prominent place in this section on the general use of OpenFOAM. Section 78.5.1 of this document also discusses the use of shell script when running simulations using OpenFOAM.

12.8.1 Allrun & Allclean

In the tutorials, we see a lot of cases featuring `Allrun` and `Allclean` scripts, which contain all operations necessary to run a case and to clean-up afterwards. The use of such scripts is strongly encouraged by the author of these lines, since this is a very concise way of documenting what the case needs to have done.

Pitfall: an unintended endless loop

Listing 88 shows an `Allrun` script from the author. There, the mesh creation is handled in a sub-directory of the case. That sub-directory has its own `Allrun` script. Can you spot the potential error?

```

1 #!/bin/sh
2 cd ${0%/*} || exit 1      # Run from this directory
3
4 # Source tutorial run functions
5 . $WM_PROJECT_DIR/bin/tools/RunFunctions
6
7 application=$(getApplication)
8
9 cp -r 0.org 0
10
11 rm -rf constant/polyMesh
12 cd meshing
13 ./Allrun
14 cd ..
15 cp -r meshing/constant/polyMesh constant/
16
17 runApplication $application

```

Listing 88: An `Allrun` script, which can result in an endless loop.

The script shown in Listing 88 results in an endless loop, when the case is copied and the meshing sub-directory has been omitted. This, results in the `cd` command in Line 12 failing. This, however, does not end the execution of the `Allrun` script itself, thus it continues. In Line 13, the `Allrun` script of the meshing sub-directory is called. However, due to the identical names, the `Allrun` script of the case is called instead. Hence, we are left with an endless loop.

12.8.2 Supporting multiple Versions of OpenFOAM

While a shell script is simply a collection of commands that are executed successively, one can run into trouble if one wants to support multiple versions of OpenFOAM. Over the development of OpenFOAM, the way some tools are being called from the command line may change.

Listing 89 shows how to accomodate such a change of the way a tool is being called. With the release of OpenFOAM-9⁴³, the way the tool `transformPoints` is being called was changed. Thus, if our run-script which uses `transformPoints` should work across all versions of OpenFOAM, we need to introduce a version-dependent call of the tool. This can easily be done by using an `if` statement and use the version of OpenFOAM for comparison. Note that the test shown in Listing 89 is quite simplistic.

```

#!/bin/bash

# scale the mesh
if [ $WM_PROJECT_VERSION -eq '9' ]
then
    transformPoints "scale=(3 3 3)"
else
    transformPoints -scale='(3 3 3)'
fi

```

⁴³<https://github.com/OpenFOAM/OpenFOAM-dev/commit/845d5b16e30d568af3eb71c69ff7f8079347522e>

Listing 89: Using version-dependent commands in a run-script.

13 Features of OpenFOAM

13.1 General mathematical functions

OpenFOAM has, at the time of writing, three different general functions to offer: functions of one variable (Function1), functions of two variables (Function2) and polynomial functions (Polynomial).

13.1.1 Function1

Functions of one variable are most prominently used in OpenFOAM for boundary conditions. Function1 is a class hierarchy with Function1 being the abstract base class for a variety of derived functions.

The Function1 family of functions features a number of specialized ramps and continuous functions such as sine, cosine and polynomial. There are various trivial functions, such as zero, one and constant. Furthermore, there is the option of providing tabulated data for interpolation. There is also a dynamically coded function, which allows a user full freedom to implement an arbitrary function. Some of the available functions, are discussed in this section along with examples of their practical use.

The Function1 framework allows the developers of OpenFOAM and developers working with OpenFOAM a convenient way to implement time-variant values without the need to actually implement this oneself. Boundary conditions are a prime example for the use of the Function1 framework, however, many models within OpenFOAM use this framework.

Constant

The constant function takes a single value, which is held constant. Since the Function1 framework is a versatile one, it also needs to include the trivial options, such as constant. There is even a templated zero function.

```
inlet
{
    type          uniformFixedValue;
    uniformValue  constant (0 0 0.1);
}
```

Listing 90: Definition of a fixed velocity boundary condition using the `constant` function.

Table

The table function allows the user to provide a set of data points which will be used to interpolate. Listing 91 shows the use of the table function in the context of a boundary condition.

```
inlet
{
    type          uniformFixedValue;
    uniformValue  table
    2
    (
        (0 (0 0 0))
        (1 (0 0 1))
    );
}
```

Listing 91: Definition of a piecewise linear velocity boundary condition using the `table` function.

As per the class's header description, the tabulated data can also be provided via a CSV file. However, your author has no experience in doing so.

Square

Square implements a square-wave function with an offset. In Listing 92, such a square-wave definition is shown in the context of a velocity boundary condition. The resulting velocity over time is shown in Figure 5.

```

inlet
{
    type          uniformFixedValue;
    uniformValue
    {
        type      square;
        amplitude   (0 0 1);
        frequency   3;
        start       0;
        level       (0 0 1);
        markSpace   0.25;
    }
}

```

Listing 92: Definition of a pulsating velocity boundary condition using the `square` function.

Figure 5 shows the square-wave defined in Listing 92. The duration of the pulses is a quarter of the period of the square-wave. This is due to `markSpace` being 0.25 of value⁴⁴. Since the offset `level` is equal to the `amplitude`, both having the value 1, the curve in Figure 5 oscillates between the values of 0 and 2. `frequency` is self-explanatory. With the `start` parameter, we can shift the curve in time, e.g., if we wanted to start from a low state, we would need to shift the curve by at least the product of `markSpace` and the wave-period.

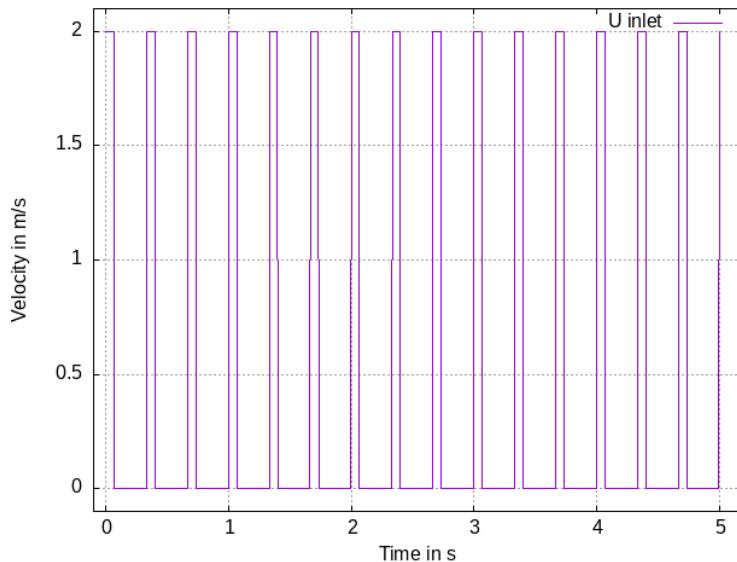


Figure 5: The velocity resulting from the settings shown in Listing 92.

coded

We can also easily create our own functions, by using OpenFOAM's run-time compilation framework, which also allows us to create custom functions. In this case, we provide the entry, that expects input of the type `Function1` with the keyword `coded`. Then, the necessary input for the coded function follows.

In Figure 5, we see velocity profile created by the `square` function. This function toggles between a high- and a low-value, which can be adjusted by the parameters `amplitude` and (offset) `level`. However, if we imaging a velocity boundary condition to change suddenly from 0 to a high value, this might pose numerical problems. Thus, we can create a coded function, which has more gradual transitions.

Listing 93 shows a coded function in use in the context of a velocity boundary condition. The value provided to the keyword `uniformValue` is `coded`. With the code borrowing heavily from the source code of the `square` function, we achieved a smoother transitioning pulse-like function..

⁴⁴*Mark and Space* are terms used in telecommunication describing signal states, essentially denoting the high- and low-states of a binary signal. In early electric telegraphs, the signal states would either create a mark on paper or a blank space; see https://en.wikipedia.org/wiki/Mark_and_space.

```

1 inlet
2 {
3     type          uniformFixedValue;
4     uniformValue  coded;
5     name         pulse;
6
7     codeInclude
8     #{
9         #include "mathematicalConstants.H"
10    #};
11
12    code
13    #{
14        // parameters of the Square function
15        const scalar markSpace(0.25);
16        const vector level(0, 0, 1);
17        const scalar start(0);
18        const scalar frequency(3);
19        const vector amplitude(0,0,1);
20
21        // flank space, percentage of the mark-space to use for the flanks
22        const scalar flankSpace(0.2);
23
24        // constant for convenience
25        const scalar ThreePiByTwo(1.5*constant::mathematical::pi);
26
27        // compute fractions
28        const scalar markFraction = markSpace/(1 + markSpace);
29        const scalar flankFraction(flankSpace*markFraction);
30
31        // compute phases, values from 0 to 1
32        const scalar phi = frequency*(x - start);
33        const scalar fraction = phi - floor(phi);
34
35        // phase-limits of the transitions
36        const scalar phi1(0.5*flankFraction);
37        const scalar phi2(markFraction - 0.5*flankFraction);
38        const scalar phi3(markFraction + 0.5*flankFraction);
39        const scalar phi4(1.0 - 0.5*flankFraction);
40
41        vector value(0, 0, 0);
42
43        if (fraction < phi1) {
44            // rising flank
45            value += sin(constant::mathematical::piByTwo*fraction/phi1)*amplitude;
46        } else if (fraction < phi2) {
47            // high, constant
48            value += amplitude;
49        } else if (fraction < phi3) {
50            // falling flank
51            value += sin(constant::mathematical::piByTwo
52                + constant::mathematical::pi*(fraction-phi2)/(phi3-phi2))*amplitude;
53        } else if (fraction < phi4) {
54            // low, constant
55            value += -amplitude;
56        } else {
57            // rising flank
58            value += sin(ThreePiByTwo
59                + constant::mathematical::piByTwo*(fraction-phi4)/(1.0 - phi4))*amplitude;
60        }
61
62        // finally, add the offset-level before returning the value
63        return value + level;
64    #};
65 }

```

Listing 93: A coded pulsating velocity boundary condition similar to the `square` function, with sinoid transitions. The style of the if-else statement blocks was adopted purely for formatting reasons, the listing would otherwise not fit a page.

Figure 6 shows the velocity over time resulting from the code shown in Listing 93. The plot is focused on just two pulses to highlight the smoother transition between the high-value (2 m/s) and the low-value (0 m/s). The other parameters (frequency, mark-space, etc.) are equal to the values shown for the `square` function depicted in Figure 5.

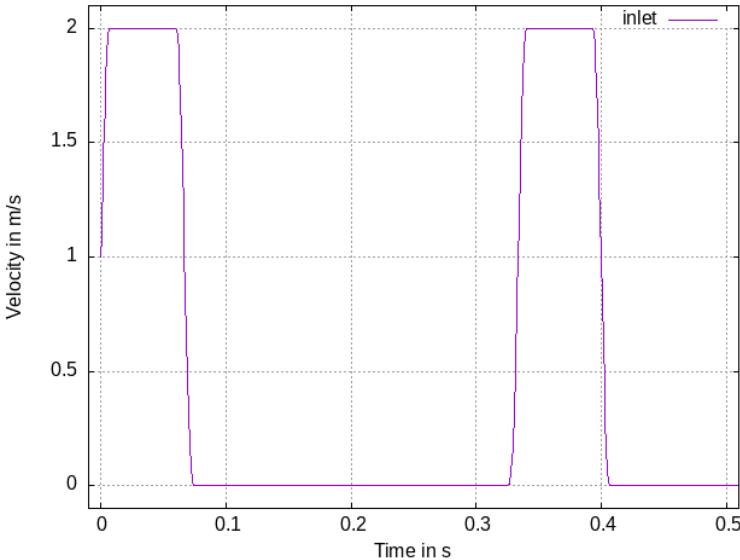


Figure 6: The velocity resulting from the settings shown in Listing 93.

13.1.2 Polynomial

The name of this class of general mathematical function is pretty self-explanatory. The `Polynomial` class provides a templated class for polynomials.

```

1 Class
2     Foam::Polynomial
3
4 Description
5     Polynomial templated on size (order):
6
7 \verbatim
8     poly = sum(coeffs[i]*x^i) + logCoeff*log(x)
9 \endverbatim
10
11 where <tt> 0 <= i <= N </tt>

```

Listing 94: Part of the description in the header file of the `Polynomial` class.

The class's template parameter of this class is the polynomial size, which is of the integer type. Thus, a single templated class suffices to be able to construct polynomials of all sizes. Listing 95 shows the class's template parameter along with a static assertion, which enforces a positive polynomial size at compile time⁴⁵.

```

1 template<int PolySize>
2 class Polynomial
3 {
4     public VectorSpace<Polynomial<PolySize>, scalar, PolySize>
5     {
6         static_assert(PolySize > 0, "Size must be positive (non-zero)");

```

Listing 95: Part of the class declaration in the header file of the `Polynomial` class.

⁴⁵See https://en.cppreference.com/w/cpp/language/static_assert.

Polynomial functions are used in OpenFOAM among others by the polynomial thermodynamical models, which compute the heat capacity of a fluid from a polynomial function of temperature. While the polynomial thermodynamic models are not yet discussed in this document, the JANAF thermodynamic model follows a similar idea, see Section 40.5.1. However, the JANAF model directly implements its polynomial, due to the special definition of the JANAF coefficients.

13.2 Run-time compilation

13.2.1 Overview

OpenFOAM supported run-time compiled code from quite early on. Run-time code compilation is noted in the release notes of OpenFOAM-2.0.0⁴⁶ in the form of the `#codeStream` directive as well as the coded function object.

Coded functions, i.e., coded Function1, were introduced with OpenFOAM-8 (see <https://openfoam.org/release/8/>). Use of coded input was improved with further releases of OpenFOAM, among others of OpenFOAM-11 and OpenFOAM-12⁴⁷.

The array of available coded models includes boundary conditions, function objects, fvModels and mathematical functions (Function1 and Function2).

Search the tutorials for the keyword `coded`, there are several examples of run-time compiled code, e.g., as shown in Listing 96. Note, that here it pays off to have several installations of OpenFOAM on your system. The Foundation release and the ESI release of OpenFOAM differ a lot in their results to the search shown in Listing 96.

```
user@host:~/OpenFOAM/OpenFOAM-12/tutorials$ find . -type f | xargs grep coded
```

Listing 96: Using the Linux Terminal to search the OpenFOAM tutorials for the `coded` keyword.

Coded function objects Coded function objects are discussed by example in Sections 59.10 and 46.3.2.

Coded (mathematical) functions

The use of coded functions, i.e., a mathematical function of one variable, is discussed in Section 13.1.1. There, a coded function is used to customize a boundary condition.

13.2.2 Use

Whenever a coded model is being used, OpenFOAM compiles it on demand. This results in the presence of a folder named `dynamicCode` in the case directory. Note, when transferring a case between machines, e.g., between a work-station and a computing cluster, do not copy the `dynamicCode` folder.

13.2.3 codedFixedValue boundary condition

With boundary conditions, its quite common to use dictionary keywords as one would use variables, see Listing 97. There, we define a keyword `inletVelocityMagnitude`, which we later use in the definition of a velocity boundary condition. This example is quite primitive, but we could do some inline calculations in between.

```
1 inletVelocityMagnitude 1.0;
2
3 inlet
4 {
5     type          uniformFixedValue;
6     uniformValue   constant ($inletVelocityMagnitude 0 0);
7 }
```

Listing 97: Defining a dictionary keyword and using it for a boundary condition.

⁴⁶See <https://openfoam.org/release/2-0-0/run-time-control-code-compilation/>

⁴⁷See <https://openfoam.org/release/11/> and <https://openfoam.org/release/12/>.

With coded boundary conditions, we might want to do something similar. This is, however, only partially possible. Listing 98 shows a sinusoidal velocity boundary condition that is implemented as a `codedFixedValue` boundary condition. There, we define the keywords *amplitude* and *frequency*, which are later used in the code. However this only works for the ESI release of OpenFOAM, this code was tested with OpenFOAM-24.06.

```

1  amplitude 1.0;
2  frequency 3.0;
3
4  boundaryField
5  {
6      inlet
7  {
8      type          codedFixedValue;
9      value         uniform (0 0 0);
10     name          myCodedSinusoidalVelocityBC;
11
12     codeInclude
13     #{
14         #include "mathematicalConstants.H"
15     #};
16
17     codeContext
18     {
19         amplitude $amplitude;
20         frequency $frequency;
21     }
22
23     code
24     #{
25         static bool init{false};
26         static scalar amplitude{0};
27         static scalar frequency{1};
28
29         if (!init)
30     {
31             init = true;
32             amplitude = this->codeContext().get<scalar>("amplitude");
33             frequency = this->codeContext().get<scalar>("frequency");
34         }
35
36         const vector amplitudeVec(0,0,amplitude);
37
38         operator==(amplitudeVec*sin(2.0*constant::mathematical::pi*frequency*this->db() .
39             time().value()));
40     };
41 }
```

Listing 98: Defining dictionary keywords and using them for a boundary condition. Note, that this works only for the ESI release of OpenFOAM.

Note that the implementation shown in Listing 98, only works when done in the context of a `codedFixedValue` boundary condition. Using a `codedFunction` in a `uniformFixedValue` boundary condition fails.

With the Foundation release, we can only use external tools such as `sed` to replace placeholders in the source code with actual values.

13.3 Inline calculations

Inline calculations are a simple variant of run-time compiled code. Inline calculations allow the user of OpenFOAM to perform mathematical operations within normal dictionary files. Inline calculations are enabled by the `#code` directive follow by code delimited by quotation marks “...” or `#{ ... }#`. The former delimiter allows only one-liners for the code, while the latter delimiter also allows code to span multiple lines.

Note that when using divisions, spaces need to be put around the / operator, otherwise this will be confused by the dictionary’s interpreter with the operator for the scoping of variables. Listing 99 shows an example of this. Strictly speaking, only the space preceding the / operator is required. However, using two spaces, one before and one after the / operator, leads to a visually more appealing code.

```
1 interpolationCoordOutside #calc "$radius / sqrt(2.0)";
```

Listing 99: Taking care of the / operator when performing divisions in inline calculations.

Searching for `#calc` in OpenFOAM's tutorials yields many more examples of inline calculations in use:

```
user@host:~/OpenFOAM/OpenFOAM-12/tutorials$ find . -type f | xargs grep '#calc'
```

Listing 100: Searching OpenFOAM's tutorials for cases using inline calculations.

13.3.1 Performing calculations in `blockMeshDict`

Listing 101 shows a practical example of using inline calculations in `blockMeshDict`. Here, we create an axi-symmetric mesh of a pipe. Standard pipe sizes⁴⁸ are generally tabulated stating outer diameter and wall thickness. Thus, when we select a nominal pipe size, we need to calculate the inner pipe diameter. The numbers in Listing 101 are for a 2.5 inch diameter pipe, Schedule 40⁴⁹. In order to be explicit about this, we enter the outer diameter and the wall thickness, and then compute the inner diameter. In Listing 101, this is done in a single line. We could be more obvious by defining separate variables for the outer diameter and the wall thickness. The pipe's length is stated in relation to the diameter, i.e., the pipe is 12 (inner) diameters long.

Furthermore, the domain's half-angle is given by the user in degrees and later converted into radians via an inline calculation. Subsequently, we can compute coordinates using the diameters and the half-angle..

```
1 /*----- C++ -----*/
2 | ====== |
3 | \   /   F ield      | OpenFOAM: The Open Source CFD Toolbox |
4 | \   /   O peration  | Version: 2.1.x |
5 | \   /   A nd        | Web:     www.OpenFOAM.org |
6 | \   /   M anipulation |
7 \*-----*/
8 FoamFile
9 {
10     version      2.0;
11     format       ascii;
12     class        dictionary;
13     object       blockMeshDict;
14 }
// * * * * *
16
17 // half-angle in degrees
18 halfAngleDeg 0.5;
19
20 // pipe diameter
21 pipeDiameter01 #calc "0.07303 - 2.0*0.00516";
22
23 // pipe length
24 pipeLength01 #calc "12.0*$pipeDiameter01";
25
26 /* no more user input beyond this point */
27 halfAngle #calc "degToRad($halfAngleDeg)";
28
29 x0 0.0;
30 x1 #calc "$pipeLength01";
31
32 y1 #calc "0.5*$pipeDiameter01*cos($halfAngle)";
33 z1b #calc "-0.5*$pipeDiameter01*sin($halfAngle)";
34 z1f #calc "0.5*$pipeDiameter01*sin($halfAngle)";
35
36 // .. code omitted for brevity
37
38 convertToMeters 1.0;
```

⁴⁸See https://en.wikipedia.org/wiki/Nominal_Pipe_Size

⁴⁹For historical reasons, one can not find the nominal pipe size on an actual pipe. Nominal sizes were initially the inner diameter. As materials and manufacture improved over time, it became possible to produce pipes with thinner walls. For compatibility with existing stock, newer pipes with thinner walls kept the same outer diameter. Thus, a nominal 2.5 inch pipe grew its inner diameter to something slightly larger than 2.5 inches.

```

39
40 vertices
41 (
42     ( $x0 0 0 )      // 0
43     ( $x0 $y1 $z1b ) // 1
44     ( $x0 $y1 $z1f ) // 2
45
46 // ... code omitted for brevity

```

Listing 101: Performing inline calculations in `blockMeshDict`.

13.3.2 Performing complex calculations in `blockMeshDict`

The examples shown in Listing 101 are all rather simple, as they are all one-liners. However, OpenFOAM's inline calculations allow for much more complex computations.

In this example, we show how to do complex numerical computations using OpenFOAM's inline calculation framework. Here, we want to compute the required number of cells from a block's length, an expansion ratio for mesh grading and the final cell width. The background of this calculation is discussed in Section 17.4.1. The motivation for this seemingly odd task is that we want to achieve a matching cell width with the subsequent block. Thus, the final cell width is a given along with the block's length and the expansion ratio. Note, if we didn't use mesh grading, this calculation would be also a one-liner.

As discussed in Section 17.4.1, such a calculation boils down to a numerical computation of the root of a function. If we repeat Eq. (16) in a slightly reformulated manner, we get:

$$f(N) = L E^{\frac{1}{N-1}} - \delta_1 E^{\frac{N}{N-1}} - L + \delta_1 \quad (7)$$

This function of the unknown N , the number of cells, depends on three given geometric quantities: the length L , the expansion ratio E and the initial cell width δ_1 . Note, that using the initial cell width is no different from using the final cell width, since they are linked via the expansion ratio $E = \frac{\delta_N}{\delta_1}$.

Listing 102 shows how we solve for $f(N) = 0$ using a multi-line inline calculation featuring find the root of the function via the bisection method.

```

1  /*----- C++ -----*/
2  | =====
3  |   / F ield           | OpenFOAM: The Open Source CFD Toolbox
4  |   / O peration        | Version: 2.1.x
5  |   / A nd              | Web:      www.OpenFOAM.org
6  |   \ M anipulation    |
7  \*-----*/
8 FoamFile
9 {
10     version      2.0;
11     format       ascii;
12     class        dictionary;
13     object       blockMeshDict;
14 }
15 // * * * * *
16
17 // input pipe geometry
18 pipeLength01 2.0;
19 pipe01expansionRatio 0.25;
20
21 // ... code omitted for brevity
22
23 pipe01AxialCellNumber #calc
24 #{
25     const float E = $pipe01expansionRatio;
26     const float dN = $pipe01finalAxialCellSize;
27     const float d1 = dN/E;
28
29     const float L = $pipeLength01;
30
31     const float n1 = L/d1;
32     const float nN = L/dN;

```

```

33 // find f(x) = 0 by bisection of the interval [n1 nN], respectively [nN n1]
34 #define FUN(var) (L*pow(E,1.0/(var-1.0)) - d1*pow(E,var/(var-1.0)) - L + d1)
35
36 float x0 = n1 > nN ? nN : n1;
37 float x1 = n1 > nN ? n1 : nN;
38 float x = 0.0;
39 float funVal0, funVal1, funVal;
40 do
41 {
42     // evaluate function at the interval boundary
43     funVal0 = FUN(x0);
44     funVal1 = FUN(x1);
45
46     // bisect the current search interval
47     x = 0.5*(x0+x1);
48     funVal = FUN(x);
49
50     // set new interval
51     x0 = (funVal0*funVal > 0.0) ? x : x0;
52     x1 = (funVal1*funVal > 0.0) ? x : x1;
53
54     // Test for convergence
55 } while (mag(funVal) > 1e-9);
56
57 // round to the nearest integer number
58 os << round(x);
59 #};
60
61 // .. code omitted for brevity

```

Listing 102: Performing complex inline calculations in `blockMeshDict`.

Notes on the code

In Line 35 of Listing 102, we use a pre-processor macro to define a sort-of local function. Since, we need to evaluate our function several times, avoiding code-duplication was the motivation behind this move.

In Lines 37, 38, 52 and 53, we use the ternary operator to create our search interval. Since, the expansion ratio can be either smaller or larger than 1, the cell widths might increase or decrease. Thus, for an arbitrary expansion ratio, we have no way of knowing whether the initial cell width is smaller or larger than the final cell width. By using the ternary operator, we manage to keep the code valid for any case. At compile-time, the interval is constructed in the proper order, such that `x0` is smaller than `x1`.

In Line 56, we see the criterion to end the loop. In this case, we chose to test the magnitude of the function value as the test criterion. If the function value is below a certain threshold, we stop the iterations. However, since we are converting our solution, the required number of cells, we can stop when the solution is found within integer resolution. It makes no difference if we find that the required cell number is 273 or 273.1365, the result will be rounded anyway. In tests, though depending on the specific numbers, we could reduce the number of iterations in half. Thus, we could also change Line 56 to a condition like this one: `while ((x1-x0) > 1.0) ;`.

In Line 59, the computed value is returned via an OStream to the file interpreter of OpenFOAM. Thus, a value is assigned to the variable `x`. Regardless of the length of the code, the assignment beginning at Line 23 follows the pattern: `variable value;`. In case of an inline calculation has the form `variable #calc #{ /* some C++ code */ #};`.

Another note on the code - avoiding code duplication

If we do such computations multiple times, we can avoid code-duplication. Listing 103 shows an example, which does the complex calculation twice. For reasons of avoiding clutter, we include a file for use by the `#calc` directive, see Line 24. Then, two `#calc` directives make use of the `FIND_NUM_OF_CELLS_BY_BISECTION` macro.

```

1 /*----- C++ -----*/
2 | =====
3 | \ / F ield | OpenFOAM: The Open Source CFD Toolbox |
4 | \ / O peration | Version: 2.1.x |

```

```

5 | \ /   A nd           | Web:      www.OpenFOAM.org |
6 | \/   M anipulation  | |
7 /*-----*/
8 FoamFile
9 {
10     version      2.0;
11     format       ascii;
12     class        dictionary;
13     object       blockMeshDict;
14 }
15 // * * * * *
16
17 // input pipe geometry
18 pipeLength01 2.0;
19 pipe01expansionRatio 0.25;
20
21 pipeLength02 1.0;
22 pipe02expansionRatio 3.0;
23
24 #calcInclude "${FOAM_CASE}/system/myFun.H"
25
26 // .. code omitted for brevity
27
28 pipe01AxialCellNumber #calc
29 #{
30     const float E = $pipe01expansionRatio;
31     const float dN = $pipe01finalAxialCellSize;
32     const float d1 = dN/E;
33
34     const float L = $pipeLength01;
35
36     // solving for x has been moved to myFun.H
37     float x = 0.0;
38     FIND_NUM_OF_CELLS_BY_BISECTION(L,E,d1,dN,x)
39
40     // round to the nearest integer number
41     os << round(x);
42 #};
43
44 pipe02AxialCellNumber #calc
45 #{
46     const float E = $pipe02expansionRatio;
47     const float d1 = $pipe01finalAxialCellSize;
48     const float dN = d1*E;
49
50     const float L = $pipeLength02;
51
52     // solving for x has been moved to myFun.H
53     float x = 0.0;
54     FIND_NUM_OF_CELLS_BY_BISECTION(L,E,d1,dN,x)
55
56     // round to the nearest integer number
57     os << round(x);
58 #};
59
60 // .. code omitted for brevity

```

Listing 103: Performing complex inline calculations in `blockMeshDict` repeatedly.

Listing 104 shows the file, which is included in Line 24 in Listing 103. This file contains the function, we need to evaluate multiple times, as well as the bisection method itself.

```

1 #define FUNCTION(var) (L*pow(E,1.0/(var-1.0)) - d1*pow(E,var/(var-1.0)) - L + d1)
2
3 #define FIND_NUM_OF_CELLS_BY_BISECTION(L,E,d1,dN,x) { \
4     const float n1 = L/d1; \
5     const float nN = L/dN; \
6 \
7     float x0 = n1 > nN ? nN : n1; \
8     float x1 = n1 > nN ? n1 : nN; \
9     float funVal0, funVal1, funVal; \

```

```

10
11 do
12 {
13     funVal0 = FUNCTION(x0);
14     funVal1 = FUNCTION(x1);
15
16     x = 0.5*(x0+x1);
17     funVal = FUNCTION(x);
18
19     x0 = (funVal0*funVal > 0.0) ? x : x0;
20     x1 = (funVal1*funVal > 0.0) ? x : x1;
21 } while ((x1-x0) > 1.0 );
22 }

```

Listing 104: Putting code away for re-use into a separate file `myFun.H`, when doing complex inline calculations repeatedly.

14 OpenFOAM is subject to change over time

Over the years, since your trusted author started work on this ever growing document, OpenFOAM has evolved. A lot. Thus, as the disclaimer at the title page states: this document may be in parts wildly outdated. Apart from reminding the reader that this document may be outdated, this section should also serve to highlight the fact that other information on OpenFOAM may be outdated. There is plenty of material made available by the community, which is indispensable for beginners. This material is also subject to being outdated, however, once we understand this, and account for that, it should not pose a problem. We can learn certain concepts using an old version of OpenFOAM, and once we have understood it, transform our knowledge to the current version of OpenFOAM. Hence, it is advisable to keep multiple OpenFOAM installations on your machine. Your trusted author has half a dozen releases installed.

Here, we shall discuss typical changes encountered over the years using specific examples. However, these should only serve to highlight the general ways in which OpenFOAM changes. This is by no means an exhaustive list of changes.

14.1 A note on backward compatibility

Sometimes we see that the developers add specific code to maintain backward compatibility. However, this is not guaranteed in any way and the developers of OpenFOAM make no promises about backward compatibility. Thus, one should not be surprised when older cases do not run immediately with a newer version. They might, but they also might not.

Maintaining backward compatibility can range from trivial to impossible, thus it is up to the developers of OpenFOAM to weigh the inconvenience to the users when breaking backward compatibility against the benefits of keeping the code clean and not having to maintain obsolete features.

Whether OpenFOAM is good at maintaining backward compatibility or not, is impossible for this author to tell. However, if we search for *backward compatibility* in OpenFOAM's GitHub repository, we find plenty of commit messages discussing backward compatibility. Thus, we can at least surmise, that the developers of OpenFOAM are not happy to introduce breaking changes without having a good reason to do so.

14.1.1 Ways to maintain backward compatibility

Have old model names refer to the new ones

When models are renamed, the old names can be retained in the run time selection table. It appears that this feature was added with OpenFOAM-11⁵⁰, though the commit message merely states that backward compatibility is maintained with respect to a code reorganisation. The fact that models can be referred to using their old as well as their new names, which was a new addition along with this commit, is not mentioned. The commit message states:

Rationalised thermal boundary condition class names and simplified user input Renamed classes:

```
turbulentTemperatureCoupledBaffleMixedFvPatchScalarField -> coupledTemperatureFvPatchScalarField  
externalWallHeatFluxTemperatureFvPatchScalarField -> externalTemperatureFvPatchScalarField
```

Radiation heat-flux support in turbulentTemperatureRadCoupledMixed transferred to coupledTemperatureFvPatchScalarField and turbulentTemperatureRadCoupledMixed removed.

Renamed boundary condition type names in T field files:

```
compressible::turbulentTemperatureCoupledBaffleMixed -> coupledTemperature  
compressible::turbulentTemperatureRadCoupledMixed -> coupledTemperature  
compressible::externalWallHeatFluxTemperature -> externalTemperature
```

Backward-compatibility is provided for all three of the above BC specifications so existing cases will run as before but we recommend migrating to the new simpler names.

From what your trusted author can gather, this seems to be a relatively recent feature. Note, that having old and new names for the same model can be a source of confusion.

Backward compatibility by retaining old model names in the run time selection table is maintained via a new macro, which is aptly named: `addBackwardCompatibleToRunTimeSelectionTable`. Listing 105 shows the

⁵⁰See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/5c01fef1559749ddfcfffb7c7038079f174176e5>

macro in use, registering the old name for the new model.

```
1 addBackwardCompatibleToRunTimeSelectionTable
2 (
3     fvPatchScalarField,
4     coupledTemperatureFvPatchScalarField,
5     patchMapper,
6     turbulentTemperatureCoupledBaffleMixed,
7     "compressible::turbulentTemperatureCoupledBaffleMixed"
8 );
```

Listing 105: Registering an old model name with the run time selection table to maintain backward compatibility.

Maintain the old interface

With the release of OpenFOAM-4.0⁵¹, a naming convention was changed in OpenFOAM's source code: the Boolean variable `outputTime_` was renamed to `writeTime_`. Along with this, the access method was also renamed. However, the old access method was retained, which returned the value of the new variable. Thus, any code using the old access method still compiled correctly, since the old interface was maintained. This is a perfect example of the benefits of data encapsulation, a concept in software engineering.

With the release of OpenFOAM-11⁵², the old interface, i.e., the old access method `outputTime()` was removed. Thus, any code still using the old access method won't compile with OpenFOAM-11 or later.

Thus, for the intervening years between OpenFOAM-4.0 and OpenFOAM-11, roughly seven years, backward compatibility was maintained.

14.2 Renaming of files or keywords

One of the least severe changes encountered to OpenFOAM, which requires user attention is the renaming of things. Figure 7 shows how the specification of the case's turbulence modelling changed between OpenFOAM-6 and OpenFOAM-8. The change in behaviour was introduced with the release of OpenFOAM-8⁵³.

The file name itself was changed from `turbulenceProperties` to `momentumTransport`, which is quite apparent. However, there is also a smaller change in the way the specific model is selected.

⁵¹See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/758dfc2c1fc84bc7b73df5805530aa678829ab4c>

⁵²See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/f9de03d97978d3305392eac81bb035e2520579c5>

⁵³See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/7f5144312ece8c6706ecc5d9a3309ea2df4bcbed>.

```

turbulenceProperties --- momentumTransport
Meld Datei Bearbeiten Änderungen Ansicht
Neuer Vergleich... Speichern Rückgängig Wiederholen Vorherige Änderung Nächste Änderung Stopp
turbulenceProperties - tumTransport | momentumTransport
FoamFile
{
    version 2.0;
    format ascii;
    class dictionary;
    location "constant";
    object turbulenceProperties;
}
// ****
simulationType RAS;
RAS
{
    RASModel kEpsilon;
    turbulence on;
    printCoeffs on;
}
// ****
FoamFile
{
    version 2.0;
    format ascii;
    class dictionary;
    location "constant";
    object momentumTransport;
}
// ****
simulationType RAS;
RAS
{
    model kEpsilon;
    turbulence on;
    printCoeffs on;
}
// ****

```

Figure 7: Comparing the dictionary file for specifying the turbulence modelling options in OpenFOAM-6 and OpenFOAM-8 using `meld`.

14.3 Change in input format

Occasionally, the expected input format of a certain tool or model changes between releases. This is most likely due to some re-write of underlying code.

14.3.1 Case study: `setFieldsDict` in versions 12 and 13

Figure 8 shows the `setFieldsDict` of OpenFOAM version 12 and 13 from the `etc/caseDicts/annotated` folder. Hence, these are the representative examples of the respective releases. While superficially, these two files look quite similar, they differ in almost everything.

The only unchanged part of the file is the header at the top, with only the Version information having been changed. Apart from the header at the top, the definition of the box is the only remaining unchanged part of the file.

The specification of the default field values changed in its implementation from a list to a dictionary. Furthermore, the specification of the field type is apparently not necessary anymore. Also the specification of the regions/zones changed from a list-based approach to also a dictionary-based one.

```

[OpenFOAM-12] setFieldsDict — [OpenFOAM-13] setFieldsDict
Meld Datei Bearbeiten Änderungen Ansicht
Neuer Vergleich... Speichern Rückgängig Wiederholen Vorherige Änderung Nächste Änderung Stopp
[OpenFOAM-12] setFieldsDict | [OpenFOAM-13] setFieldsDict
/*----* C++ -*----*/
=====
| Field | OpenFOAM: The Open Source CFD Toolbox
| Operation | Website: https://openfoam.org
| And | Version: 12
| Manipulation |
FoamFile
{
    format      ascii;
    class       dictionary;
    object      setFieldsDict;
}
// ****
defaultFieldValues
{
    volScalarFieldValue alpha1 0
    volVectorFieldValue U (0 0 0)
};

regions
{
    // Set cell values
    // (does zero gradient on boundaries)
    boxBoxCell
    {
        box (0 0 -1) (0.1461 0.292 1);
        fieldValues
        {
            volScalarFieldValue alpha1 1
        };
    }
    // Set patch values (using ==)
    boxBoxFace
    {
        box (0 0 -1) (0.1461 0.292 1);
        fieldValues
        {
            volScalarFieldValue alpha1 1
        };
    }
}

// ****
=====
| Field | OpenFOAM: The Open Source CFD Toolbox
| Operation | Website: https://openfoam.org
| And | Version: dev
| Manipulation |
FoamFile
{
    format      ascii;
    class       dictionary;
    object      setFieldsDict;
}
// ****
defaultFieldValues
{
    alpha.water 0;
    U           (0 0 0);
};

zones
{
    // Set cell values
    cells
    {
        type   box;
        box (0 0 -1) (0.1461 0.292 1);
    }
    values
    {
        alpha.water 1;
    }
};

extrapolatePatches
{
    "inletOutlet" (alpha.water);
}

// ****

```

Figure 8: Comparing the `setFieldsDict` of OpenFOAM-12 and OpenFOAM-13 using `meld`.

The changes to the required input format of `setFieldsDict` discussed in this example are nothing scary, both list-based and dictionary-based input ought to be well known to users of OpenFOAM. However, running `setFields` of OpenFOAM-13 with a `setFieldsDict` from OpenFOAM-12 will end in error, since the expected input is not correct. Thus, while `setFields` did not change from the perspective of the user, it requires a different input format.

The take-away message of this section is, that seemingly unchanged tools, the purpose of `setFields` was not changed in any way, might be subject to change in the background. This might lead to problems when copying case files from older versions to newer ones. If we always base our case on current files, i.e., we copy dictionary-files from the release's `caseDicts` folder to our case and edit their contents, we completely avoid this issue.

14.4 Outright replacement

Sometimes, certain features are completely re-implemented or certain tools are replaced by other tools.

14.4.1 changeDictionary

The pre-processing/case-manipulation tool `changeDictionary` was replaced by the `foamDictionary` tool. `changeDictionary` has been part of OpenFOAM since basically forever⁵⁴. The `foamDictionary` tool was first added to OpenFOAM with the release of OpenFOAM-4.0.

With the release of OpenFOAM-7, a warning message was added to `changeDictionary` informing the user that this is deprecated and being replaced by `foamDictionary`. However, as of time of writing (OpenFOAM-13 is the current version), `changeDictionary` has not been removed so far and continues to function.

Thus, while being deprecated and being in the process of being replaced, this tool is (up to now, at the time of writing) still in place.

14.4.2 Solver modules

The introduction of solver modules is a big change, which is discussed more in Section 51. This represents a deeper reaching change, which may break backward compatibility.

⁵⁴On the OpenFOAM GitHub repository, it was added with the third commit. The two preceding commits added the licence and ReadMe to the repository as well as the `.gitignore` file. Thus, it was present in OpenFOAM ever since OpenFOAM was hosted on GitHub.

The change to solver modules encompassed so many aspects, it is too much to describe in simple terms. However, the change to solver module is perfect to demonstrate another aspect of OpenFOAM's development over time: *stages of replacement*.

14.4.3 Stages of replacement

With OpenFOAM, we can see various stages in the replacement of tools or features. In the following examples, we shall see a number of those. They range from a warning message informing the user of the impending replacement of the old tool and the suggestion to use the new tool instead, to an error message with a note which tool to use instead.

Legacy solvers which are retained

There are a number of legacy solvers present in OpenFOAM-13, which are not actively developed. These are solvers, that are still present and run, but they are not actively developed anymore.

This is described in the commit message⁵⁵ as follows:

applications/legacy containing legacy solver applications which are not currently being actively developed but the functionality of which will be merged into the solver modules or form the basis of new solver modules as the need arises

Mild supersedence

We refer this form of replacement as *mild supersedence*, since it does not interfere with the user in a drastic manner. We see an example of this, and how it is achieved, in Listing 106. If we try to run pimpleFoam, we will be shown an error message, and then, the appropriate replacement solver module is executed. Depending on whether the case itself is compatible⁵⁶, the case may or may not successfully run.

```
cat <<EOF

pimpleFoam has been superseded and replaced by the more general
incompressibleFluid solver module executed by the foamRun application:

foamRun -solver incompressibleFluid

EOF

exec env foamRun -solver incompressibleFluid "$@"

```

Listing 106: What is actually run, when we call pimpleFoam in OpenFOAM-13.

Hard supersedence

The alternative to mild supersedence, where OpenFOAM informs one about the replacement but runs anyway, is *hard supersedence*. Here, we are met with an informational (error) message and nothing more.

Listing 107 shows an example of hard supersedence: particleFoam. This solver has been fully replaced, and when we try to run it, we only see an informational message of what to use instead.

```
cat <<EOF

particleFoam has been superseded and replaced by the more general functions
solver module executed by the foamRun application:

foamRun -solver functions

The incompressibleFluid solver specified by either the subSolver or if not
present the solver entry in the controlDict is instantiated to provide the
physical fields needed by fvModel functionObject in which the clouds fvModel is
selected to evolve the Lagrangian particles. See:


```

⁵⁵See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/e744fdb5f1b6f3813114141274c30319955e9ebf>

⁵⁶See Section 51.3.3 for an example, where we compare the *pitzDaily* case for the old solver and new solver module.

```
tutorials/incompressibleFluid/hopperParticles  
tutorials/incompressibleFluid/mixerVesselHorizontal2DParticles  
  
EOF
```

Listing 107: What is actually run, when we call `pimpleFoam` in OpenFOAM-13.

Note, how Listings 106 and 107 are mere bash scripts. Both show a message using the shell command `cat`. The former, furthermore, contains a call to the appropriate tool to run instead. These bash scripts are located in the `bin` directory of your OpenFOAM installation, in `$WM_PROJECT_DIR/bin`, which evaluates to `/home/user/OpenFOAM/OpenFOAM-13/bin` for OpenFOAM-13 and a single-user installation.

Part III

Pre-processing, mainly everything Mesh

This part of the document deals with all issues related to pre-processing, i.e. all the tasks necessary to set-up a valid simulation case. The majority of the following sections deal with the mesh, mesh creation and the related tools. The final sections of this part deal with general case manipulation and initialisation.

One can grasp the importance of the topic “*the mesh, and everything related*” by the page count in this document. Of the 503 pages of content, 137 pages are devoted to this part.

Meshing tools

OpenFOAM brings along two important mesh creation tools: *blockMesh* and *snappyHexMesh*. However, there are even more tools that can be used in mesh creation, e.g., *extrudeMesh* or *mirrorMesh*. Furthermore, we will also discuss external mesh creation tools, i.e., third-party tools which can directly or indirectly (via mesh conversion) create meshes for OpenFOAM.

Apart from mesh-creation tools, there are plenty of mesh-manipulation tools. These tools may perform vital precursor steps during mesh-creation. Hence, they are discussed here along with the mesh-creation tools.

Many of the tools discussed here follow the paradigm of the UNIX philosophy “*make each program do one thing well*”, and thus are created for one or a small number of specific tasks. This results in a well stocked toolbox. However, this also results in the need to know about many tools, their capabilities and how to utilize them best.

Meshing strategies

Since there is no one tool to do everthing, one can achieve the intended goal possibly by more than one route. Here, again, it is vital to have a good understanding about the tools and their capabilities. With this in mind, one can develop a meshing strategy and select the proper tools for the various tasks.

For the beginner this might sound off-putting, but meshing is a task for which the user’s experience and practical knowledge are very beneficial. This manual showcases many tools and their purposes, sometimes using standalone examples and sometimes as part of a toolchain implementing a certain meshing strategy.

Mesh import and export

Figure 9 shows possible routes of importing and exporting mesh data to and from OpenFOAM. The image shows the involved tools (as boxes) and denotes the involved file formats (as labels of the arrows).

Note, that the certain file formats have their specific limitations. E.g., STL files can only describe triangular surface meshes, hence they can not be used to export a volume mesh or accurately export a surface mesh containing quadrangles.

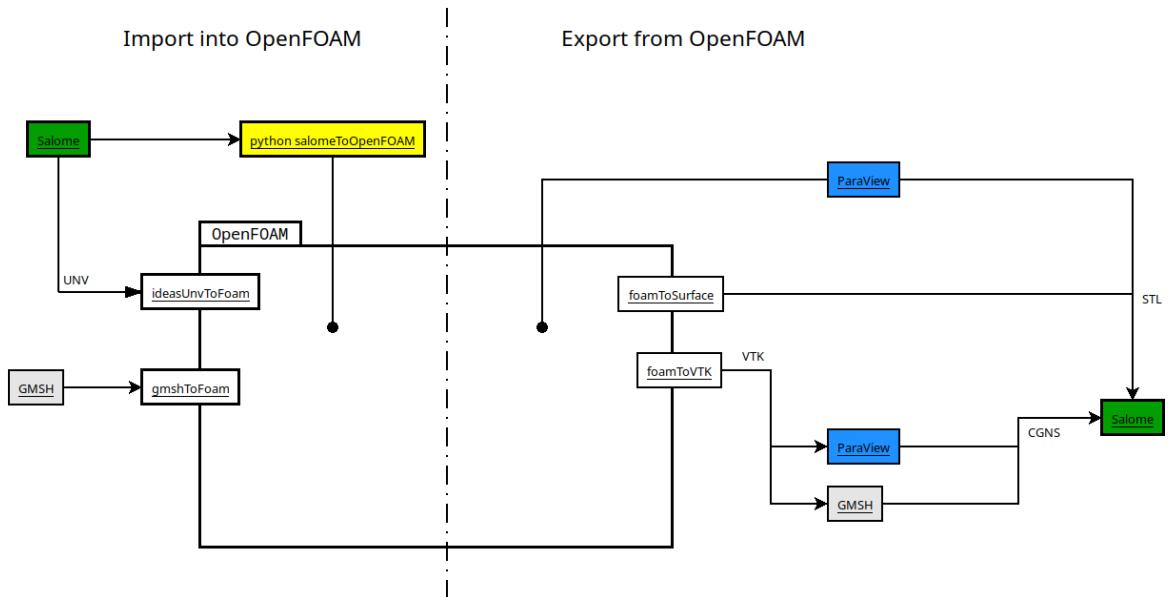


Figure 9: Possible routes of import and export. The boxes denote tools, whereas the labels of the arrows denote file formats. External tools are shown with coloured boxes. The import and export converters of OpenFOAM are shown in the style of “adapters” of the big box labelled OpenFOAM. The lines with the big solid dots denote native mesh access, e.g., ParaView is able to (more or less) natively read an OpenFOAM mesh.

15 Mesh basics

15.1 Basics of the mesh

15.1.1 Files

A mesh is defined by OpenFOAM using several files. All of these files reside in `constant/polyMesh/`. The names of these files are rather self explanatory, the rest is explained in the OpenFOAM User Guide [52].

boundary contains a list of all faces forming the boundary patches. This file is always written in ASCII format.

faces contains the definition of all faces. A face is defined by the points that form the face.

neighbour contains a list of the neighbouring cells of the faces

owner contains a list of the owning cells of the faces

points contains a list of the coordinates of all points

The description of a mesh is based on the faces. The geometry is discretised into finite volumes – the cells. Each cell is delimited by a number of faces, e.g. a hexahedron has 6 faces. The faces can be divided into two groups. Boundary faces border only one cell. These faces make up the boundary patches. All other faces can be seen as the connection between two cells and are called internal faces. A face bordering more than two cells is not possible. An internal face is, by definition, owned by one cell and neighboured by the other one. So, the two cells connected by a face can be distinguished.

This five files are absolutely necessary to describe a mesh regardless of how the mesh was created in the first place. However, some ways of creating a mesh produce additional files. Listing 108 shows a list of all files created with Gambit and converted by `fluentMeshToFoam`.

```
user@host:~/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/columnCase$ ls constant/polyMesh/
boundary  cellZones  faces  faceZones  neighbour  owner  points  pointZones
```

Listing 108: Content of `constant/polyMesh`

15.1.2 Definitions

Face

A face is defined by the vertices or points that are part of the face. The points need to be stated in an order which is defined by the face normal vector pointing to the outside of the cell or the block. The way faces are defined is the same for cells of the mesh or for blocks of the geometry.

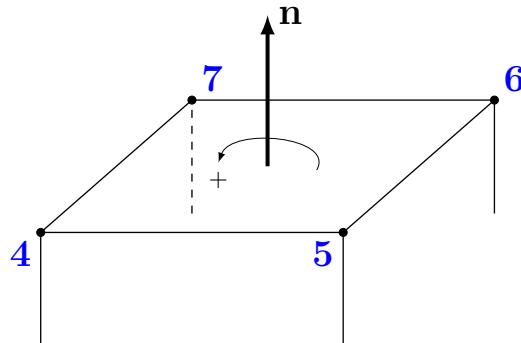


Figure 10: The top face of the generic block of Figure 13

To elaborate this further we look at the top face of the generic block of Figure 13 in Figure 10. The vertices with the numbers 4, 5, 6 and 7 are part of the face. The face normal vector – denoted by **n** in Figure 10 – that points outwards of the block is parallel to the local *z* axis. Therefore we need to specify the vertices defining

the face in counter-clockwise circular order, when we look at the block from the top. The direction of rotation is marked in Figure 10 with the + sign. The starting vertex is arbitrary but it must not appear twice in the list.

Correct definitions			
(4 5 6 7)	(7 4 5 6)	(6 7 4 5)	(5 6 7 4)
Wrong direction of rotation			
(7 6 5 4)	(4 7 6 5)	(5 4 7 6)	(6 5 4 7)
Non-circular			
(7 5 6 4)	Starting point repeated (4 5 6 7 4)		

Table 3: Valid and invalid face definitions

While the definition of the face normal of boundary faces is straight forwards, as discussed above, the face normal of internal faces is not as obvious. Internal faces connect two adjacent cells. While internal faces are created by OpenFOAM’s meshing utilities, and no valid use-case for manually specifying internal faces comes to mind, the face-normal orientation of internal faces may be important when specifying sets of internal faces for run-time post-processing. The user-guide⁵⁷ states, that the orientation of the face-normal of internal faces is such, that the face normal points from the cell with the lower cell label to the cell with the higher cell label. As all cells are consecutively numbered from 0 to N , with N being the number of cells, the stated rule provides a clear rule for the face-normal direction of internal faces.

15.1.3 Some notes on practical use

Use the binary writing format or sufficient writePrecision

Whenever, there is no specific reason to use ascii format, one should always use the binary write format. As the `points` file contains a list of coordinates, we avoid losing information, i.e. geometric precision, by using the binary format. If you need to write in ascii, use a large setting for the `writePrecision`, at least for mesh generation and manipulation.

The binary format might not be compatible across various OpenFOAM variants

If we run `checkMesh` of `foam-extend` on a mesh which was written in binary format by OpenFOAM-6, then an error as in Listing 109 occurs. Thus, make sure to pass the mesh between OpenFOAM variants in ASCII format. See Section 30.6.4 for a discussion on how to convert mesh files from the binary to the ASCII format.

```
--> FOAM FATAL IO ERROR:
unexpected class name faceCompactList expected faceList
    while reading object faces

file: /home/user/foam/run-4.0/meshTesting/constant/polyMesh/faces at line 15.

From function regIOobject::readStream(const word&)
in file db/regIOobject/regIOobjectRead.C at line 108.

FOAM exiting
```

Listing 109: A possible error when reading a binary mesh with a different OpenFOAM variant.

15.2 General advice on meshing and mesh/case manipulation

15.2.1 Division of labour: keep mesh creation/manipulation separate from field definition

Since, OpenFOAM’s toolbox contains lots of tool, which are specifically created for one job, OpenFOAM lends itself well for creating meshing cases, which are cases that run a sequence of meshing and mesh-manipulation

⁵⁷ <https://cfd.direct/openfoam/user-guide/v6-mesh-description/>

tools to create the intended mesh. The most basic of such a mesh-creation & mesh-manipulation sequence would be to first run *blockMesh* and subsequently run *renumberMesh*.

Thus, we should aspire to organize our cases in a way to achieve a separation of separated tasks, i.e. creating the mesh, running the case and post-processing the case. Such a separation can be translated into an actual division of labour by creating sub-scripts for each task. Listing 110 shows a pattern for an *Allrun* script, which embodies this separation of tasks. Instead of calling tools and solvers directly, we call sub-scripts which we created for those specific tasks.

```
#!/bin/sh

# this script contains all steps for mesh-creation and mesh-manipulation
./createMesh

# now, that the mesh is in its final form, we instate the initial time step 0
cp -r 0.org 0

# beyond this point, calls to initialization tools, such as setFields,
# or case-decomposition for parallel running, are the only remaining pre-processing steps
./runCase

# run post-processing
./runPostProcessing
```

Listing 110: Division of labour in an exemplary *Allrun* script.

If we introduced our fields too early, then missing – yet to be created – patches may cause some pre-processing tools to fail. By eliminating the fields from the mesh-creation stage, we eliminate one source of error. Furthermore, dragging the fields through the mesh-generation process, with creation of patches, adding or removing cells, any many other non-trivial mesh-modifications, is a useless waste of computational effort, and a needless source of error. Thus, it is advised to follow this rough guideline:

1. Create the mesh, without involving the fields
2. Set up the fields for the final form of the mesh

15.3 General mesh-related topics

15.3.1 Two-dimensional meshes, and meshes of even lesser dimensions

In OpenFOAM, a two-dimensional mesh is a mesh which is one cell in thickness direction. This is a rather elegant way of avoiding the 2D-3D distinction, at least of the user-facing surface and in parts of the underlying framework.

Thus, a two-dimensional mesh features one spatial direction which is resolved only by one cell. Similarly, a one-dimensional mesh features two spatial dimensions which are resolved by only one cell. Brought to an extreme, a zero-dimensional mesh is resolved by one cell in all spatial directions, i.e. the entire mesh is a single cell.

The fact that all meshes in OpenFOAM are technically three-dimensional meshes allows us to create all types of meshes using the same tools. Hence, there is no *blockMesh2D* for two-dimensional meshes. We can create all kinds of meshes using the same *blockMesh*, from fully three-dimensional down to zero-dimensional.

Tools for three dimensions and tools for three dimensions or less

Not all tools in OpenFOAM's arsenal allow for lesser-dimensional meshes. The two main mesh creation tools serve as a perfect example. While *blockMesh* is perfectly capable to create meshes for three dimensions or less; *snappyHexMesh* is a purely three-dimensional mesher⁵⁸.

⁵⁸Since there are always exceptions to any rule, there is also an exception for this rule. We can create a two-dimensional snappy-like mesh by meshing a quasi two-dimensional block using *snappyHexMesh*, and then extrude a single-cell layer from this mesh and discard the base mesh.

15.3.2 Pitfall: combined front-and-back patch in a 2D wedge geometry

While it is perfectly normal and valid to define a combined front-and-back patch of the `empty` type in “normal” two-dimensional simulations, axisymmetric 2D simulations do not allow for a combined front-and-back patch of the type `wedge`.

If we defined such a combined front-and-back patch, OpenFOAM will complain about encountering a non-planar `wedge`-type patch. While, the front and the back surface might be perfectly planar, a combined front-and-back patch will inevitably cause problems. OpenFOAM’s definition for the planarity of a patch is that the surface normal of the individual faces of a patch is parallel to the patch-average normal vector. A combined front-and-back patch will violate this condition.

Thus, with axi-symmetric mesh must have separate front and back patches of the type `wedge`.

15.3.3 Pitfall: visual inspection

When creating a mesh, visual inspection of the intermediate and/or final mesh is often beneficial. However, one may, under certain circumstances, be led astray.

Figure 11 shows an example when the author needlessly trouble-shooted a mesh, which had in fact no errors. The cause was purely one the part of the visualisation done in ParaView. A certain ParaView installation showed the mesh in a way that suggested trouble. However, if we compare the two other visualisations, the mesh looks just fine.

Thus, if the visual inspection suggests flaws in the mesh, you might want to take a closer look at the results of `checkMesh`, and if in doubt test a different installation of ParaView.

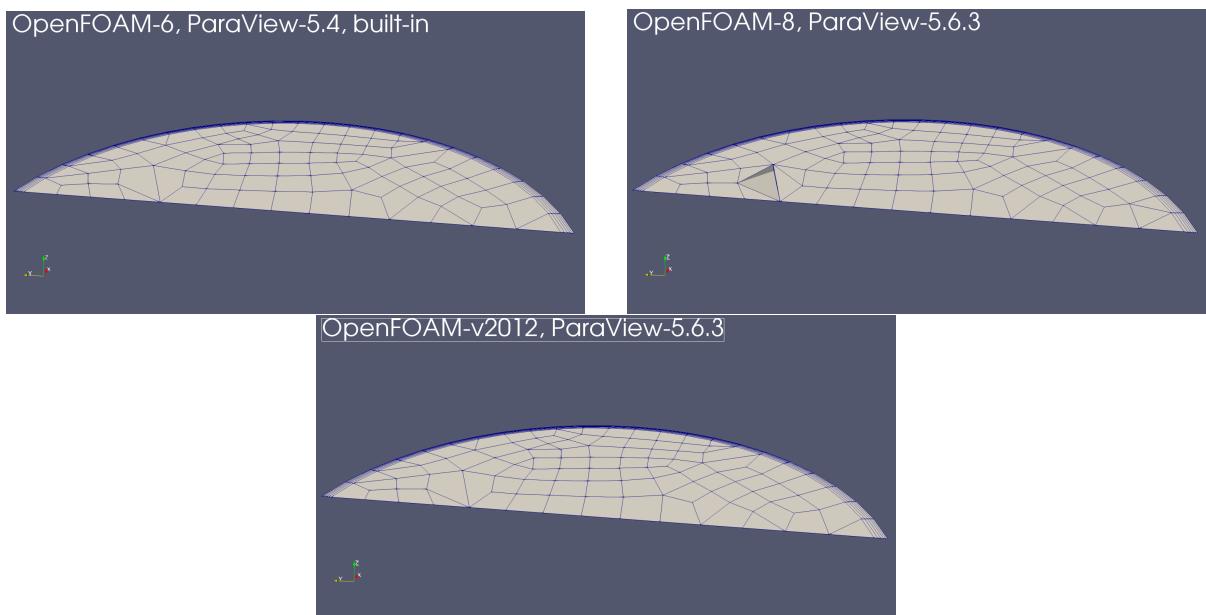


Figure 11: The same axi-symmetric two-dimensional viewed with three different installations of ParaView.

16 Geometry creation & other pre-processing software

There are many ways to create a geometry. There is a great number of CAD software, there is a number of CFD pre-processors capable of creating geometries and there is the good old *blockMeshDict*.

This section is about the different ways to generate the geometry for creating a finite volume mesh.

16.1 *blockMesh*

blockMesh is one of OpenFOAM's own pre-processing tools. It is able to create the domain geometry and the corresponding mesh. See Section 17 for a discussion on *blockMesh*. For the reason of simplicity all aspects of *blockMesh* – geometry creation as well as meshing – are covered in Section 17.

16.2 CAD software

There is a great number of CAD software around. Each CAD program usually uses its own file format. However most CAD programs support exporting the geometry in different formats, e.g. STL, IGES, SAT. If CAD software is used to create the geometry the data has to be exported to be used by a meshing program. A common file format for this purpose is the STL format. *snappyHexMesh* can be used with STL⁵⁹ geometry definitions.

16.2.1 OpenSCAD

OpenSCAD [<http://www.openscad.org/>] is an open source CAD tool for creating solid 3D CAD models. A CAD model is created by using primitive shapes (cubes, cylinders, etc.) or by extruding 2D paths. Models are not created interactively like in other CAD software. The user writes an input script which is interpreted by OpenSCAD. This makes it easy to create parametric models.

For further information on usage see the documentation http://en.wikibooks.org/wiki/OpenSCAD_User_Manual.

Pitfall: STL mesh quality

OpenSCAD is a tool to create CAD models. Therefore the requirements on the produced STL mesh are completely different than on a mesh for CFD simulations. OpenSCAD produces STL meshes that define the geometry correctly but the mesh is of a bad quality from a CFD point of view.

Figure 12 shows the STL mesh of a circular area. All triangles defining the circular area share one vertex. This vertex is probably the base point for the mesh creation of OpenSCAD. From a CFD point of view the triangular face elements are highly distorted and have a bad aspect ratio. However from a CAD point of view these triangles are perfectly sufficient to represent the circular area.

If a finite volume mesh is to be derived from the STL surface mesh (e.g. with GMSH) problems may arise. If the only purpose of the STL mesh is to represent some geometry – like it is the case with *snappyHexMesh* – then this quality issues can be ignored.

⁵⁹STL is in fact a surface mesh enclosing the geometry. Therefore the term STL mesh or STL surface mesh is also valid.

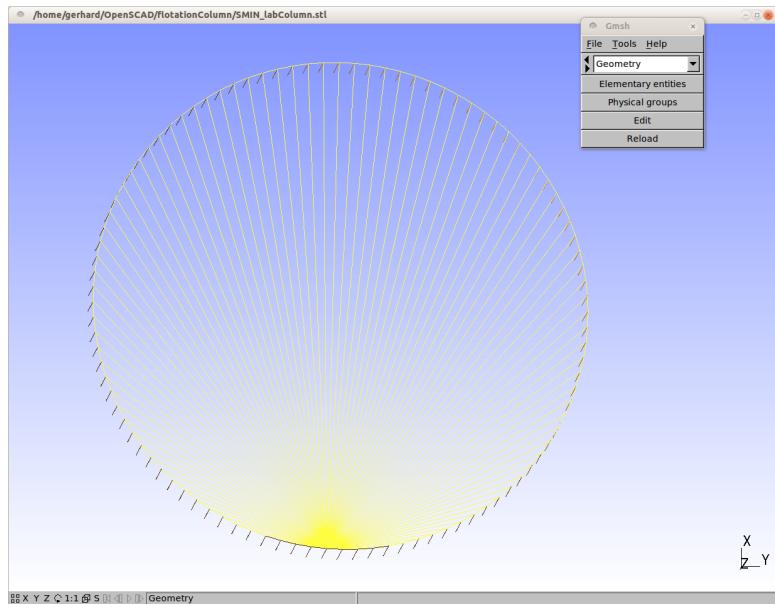


Figure 12: The STL mesh of a circular area generated by OpenSCAD

16.3 Salome

Salome [<http://www.salome-platform.org/>] is a powerful open source pre-processing software developed by EDF. Salome can be used to create a geometry interactively or by interpreting a python script⁶⁰. Salome comes with a number of internal and external meshing utilities. Salome has also a post-processing module.

Salome is a part of a collection of open source software developed by EDF. Salome serves as the pre- and post-processor for Code_Aster (structural analysis) and Code_Saturne (CFD).

16.3.1 Geometry

Salome can be used for geometry generation only. A common way of doing so, is to use Salome's meshing module to create a surface mesh of the CAD geometry, which can be exporting using the STL format. The resulting STL file can then be used by other meshing tools, e.g. *snappyHexMesh*.

16.3.2 Mesh

Salome can also used to create the geometry and subsequently the mesh. This mesh needs to be exported by Salome in the UNV format, which can be converted by the *ideasUnvToFoam* utility of OpenFOAM.

See <http://caelinux.org/wiki/index.php/Doc:Salome> for documentation and usage examples of Salome, and Section 26 for some further points on creating the mesh with Salome.

16.4 GMSH

GMSH is a meshing tool with some pre- and post-processing capabilities [<http://www.geuz.org/gmsh/>]. The meshes generated by GMSH can be converted to OpenFOAM's format using the *gmshToFoam* utility.

⁶⁰Salome can be controlled completely by Python. Thus parametric geometry or mesh creation is possible.

17 *blockMesh*

blockMesh is used to create a mesh. The geometry is defined in *blockMeshDict*. This file also contains all necessary parameters needed to create the mesh, e.g. the number of cells. Therefore, *blockMesh* is a combined tool to define and mesh a geometry in contrast to other meshers that use CAD files to import a geometry created by some other software.

17.1 The block

The geometry created by *blockMesh* is based on the generic block. Figure 13 shows a generic block.

The blue numbers are the local vertex numbers of the block. The vertices are numbered counter-clockwise⁶¹ in the local $x - y$ plane starting at the origin of the local coordinates⁶². Then the vertices above the local $x - y$ plane are counter-clockwise numbered starting with the vertex on the local z axis.

The local vertex numbers are important when defining the block. The first part of the *blockMeshDict* is generally a list of vertices. From this vertices the blocks are constructed. A block is defined by a list of 8 vertices which have to be ordered in a way to match the local vertices. Therefore the first entry in the list of vertices is the local 0 vertex, then the local 1 vertex follows. The local vertex numbers define the order in which the vertices have to be passed when constructing a block.

The coordinate system originating from vertex 0 are the local coordinates. The local coordinates are important when specifying the number of cells or mesh grading (see *simpleGrading* in Section 17.4). The local coordinate axes do not need to be parallel or to coincide with the global coordinate axes.

The edges are also numbered and have a direction. Starting with the edge parallel to the local x axis the edges are numbered counter-clockwise starting with the edge emanating from the origin of the local coordinates. Next the edges parallel to the local y axis are numbered and finally the edges parallel to the local z axis. The edge number is important when specifying a grading for each edge individually (see *edgeGrading* in Section 17.4).

As it is indicated on Figure 13, the edges do not need to be parallel or straight. See Section 17.2.4 on how to define curved edges.

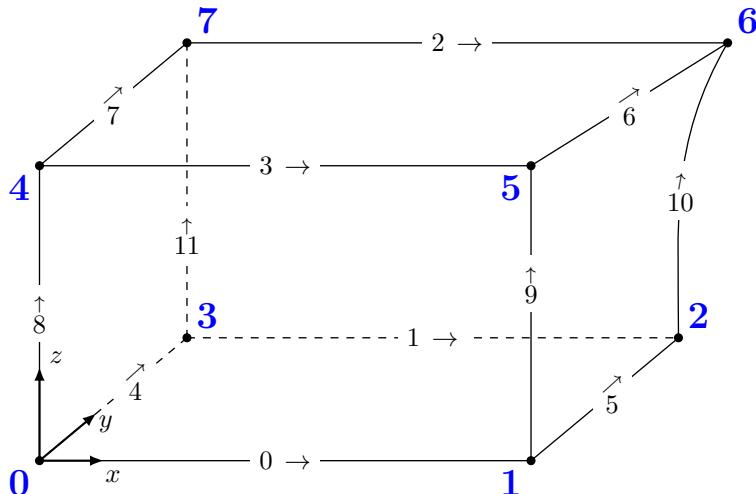


Figure 13: The generic block

⁶¹In mathematics the positive direction of rotation is generally determined with the right-hand or cork-screw rule. Let the thumb of your right hand point in the positive direction of the rotation axis, then the fingers of the right hand point in the positive direction of revolution.

⁶²If we number all vertices in the $x - y$ plane then the local z axis is the axis of revolution. Thus the counter-clockwise direction is the mathematically positive direction of revolution.

17.2 The blockMeshDict

The file `blockMeshDict` defines the geometry and controls the meshing process of `blockMesh`. Listing 111 shows a reduced example of the `blockMeshDict`. This file was taken from the *cavity* tutorial case.

```

/*----- C++ -----*/
| ====== |
| \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox
| \ \ / O p e r a t i o n | Version: 2.1.x
| \ \ / A n d | Web: www.OpenFOAM.org
| \ \ / M a n i p u l a t i o n | 
| *----- */

FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    object       blockMeshDict;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //


convertToMeters 0.1;

vertices
(
    (0 0 0) // 0
    (0 0 0.1) // 1
    ...
);

blocks
(
    hex (0 1 2 3 4 5 6 7) (20 20 1) simpleGrading (1 1 1)
);

edges
(
);

boundary
(
    movingWall
    {
        type wall;
        faces
        (
            (3 7 6 2)
        );
    }
    ...
);

mergePatchPairs
(
);

// ****

```

Listing 111: A minimal `blockMeshDict`

17.2.1 convertToMeters

`convertToMeters` is a scaling factor to convert the vertex coordinates of `blockMeshDict` into meters. If the vertex coordinates are entered in an other unit than meters, this value has to be chosen accordingly. Listing 112 shows how to set this factor if the vertex coordinates are entered in millimeters.

```
convertToMeters 0.001:
```

Listing 112: *convertToMeters*

If the keyword `convertToMeters` is missing in the `blockMeshDict`, then no scaling is used, i.e. the default value of 1 is assumed.

To make sure if a scaling factor has been used, the output of `blockMesh` can be checked. Listing 113 shows the message issued by `blockMesh` regarding the scaling factor defined with `convertToMeters`.

```
Creating points with scale 0.1
```

Listing 113: Output of *blockMesh* when `convertToMeters` is set to 0.1

`convertToMeters` is a uniform scaling factor. Non-uniform scaling or other operations can be performed with another tool. See Section 30.1 and 33.3.4.

17.2.2 vertices

The `vertices` sub-dictionary contains a list of vertices. Each vertex is defined by its coordinates in the global coordinate system. By default OpenFOAM treats these coordinates as in metres. However, with the help of the keyword `convertToMeters`, the vertices can be specified in other units.

The index of a vertex in this list is also the global number of this vertex, which is needed when constructing blocks from the vertices. Remember, counting starts from zero. Thus the first vertex is the list of vertices can be addressed by its index 0. A way to keep oneself aware of this fact is to add comments⁶³ to the vertex list as in Listing 111.

17.2.3 blocks

The only valid entry in the `blocks` sub-dictionary is the `hex` keyword. The `blocks` section of the `blockMeshDict` contains a list of `hex` commands. Listing 114 shows an example of a block definition with the `hex` keyword.

After the word `hex` a list of eight numbers defining the eight vertices of the block follows. The order of the entries in this list is the same order as the local vertex numbers of the block in Figure 13.

Then a list of three positive integer numbers follows. These numbers tell `blockMesh` how many cells need to be created in the direction of the local coordinate axes. Thus, the first number is the number of cells in the local *x* direction.

The next entry is a word stating the grading of the edges. This entry is in fact redundant. In OpenFOAM-2.1.x only the last entry, the list of expansion ratio, controls the grading. The third entry could even be omitted. However, maybe future versions of OpenFOAM make use of this entry. So the author does not advocate to omit this parameter.

The last entry of the block definition is a list of either three or twelve positive numbers. These numbers define the expansion ratio of the grading. In the case of three numbers, *simpleGrading* is applied. If twelve numbers are stated, then *edgeGrading* is performed.

If the list contains only one entry, then all edges share the same expansion ratio. Any other number of entries in this list leads to an error.

```
hex (0 1 2 3 4 5 6 7) (20 20 1) simpleGrading (2 4 1)
```

Listing 114: The `hex` command in `blockMeshDict`.

Setting up cell zones

The cells belonging to a block can be assigned to a cell set at mesh creation by inserting the name of the to-be-created cell set between the vertex list and the list with the number of cells. This feature is not really documented in the official OpenFOAM User Guide, however, it seems to be present in OpenFOAM ever since.

```
hex (0 1 2 3 4 5 6 7) CELL_SET_NAME (20 20 1) simpleGrading (2 4 1)
```

Listing 115: The `hex` command in `blockMeshDict` with a cell set definition.

⁶³As OpenFOAM treats its dictionaries much in the same way as C/C++ source files are treated by the C/C++ compiler. Therefore comments work the same way as they do in C or C++.

Creating a block with 6 faces

The `hex` instruction can also be used to create a prism with a triangular cross-section. Such blocks are needed for simulations that make use of axi-symmetry. In such a case, an “axis-patch” is created using only two vertices, as shown in Figure 14. This patch is constructed from the vertex list (4 5 5 4), instead of (4 5 6 7) as it would be the case for an ordinary block.

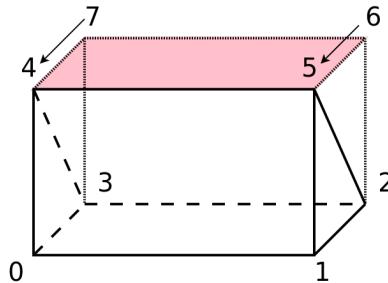


Figure 14: Creating a wedge geometry for 2D, axisymmetric domains. Reproduced after [52].

This collapsed patch results in an empty patch, i.e. one that contains no faces. In Listing 116, we see the summary on the patches, which is printed to the Terminal by `blockMesh`. Here, we can see the empty patch `axis`.

Patches

```
-----
patch 0 (start: 10159 size: 5) name: inletCH4
patch 1 (start: 10164 size: 70) name: wallOutside
patch 2 (start: 10234 size: 61) name: wallTube
patch 3 (start: 10295 size: 5) name: inletPilot
patch 4 (start: 10300 size: 60) name: inletAir
patch 5 (start: 10360 size: 71) name: outlet
patch 6 (start: 10431 size: 0) name: axis
patch 7 (start: 10431 size: 5170) name: frontAndBack_pos
patch 8 (start: 15601 size: 5170) name: frontAndBack_neg
```

Listing 116: The patch list of an axisymmetric case from the OpenFOAM tutorials.

When setting up a two-dimensional case, pay attention to velocity boundary conditions, especially those with a user-provided flow-rate. OpenFOAM is not aware, that the inlet patch is only a fraction of the real inlet. Thus, a flow rate at the inlet needs to be corrected by the area ratio, i.e. the ratio of the inlet patch of the two-dimensional simulation domain and the real inlet area.

Pitfall: `writePrecision` and wedge geometry

When we create and manipulate an axisymmetric geometry, we have two patches of the type `wedge`. If we use an insufficient number of digits to define the geometry, then OpenFOAM may issue warning messages similar to the one below, informing the us, the user, of non-planar faces.

```
--> FOAM Warning :
    From function virtual void Foam::wedgePolyPatch::calcGeometry(Foam::PstreamBuffers&
in file meshes/polyMesh/polyPatches/constraint/wedge/wedgePolyPatch.C at line 70
Wedge patch 'front' is not planar. At local face at (4.07936 -0.000130603 0.0149657) the
    normal (0 -0.999962 -0.00872414) differs from the average normal (8.95761e-21 -0.999962
    -0.00872653) by 5.70802e-12
Either correct the patch or split it into planar parts
```

Listing 117: Insufficient `writePrecision` in `controlDict` when creating/using a 2D axisymmetric geometry.

If we create a single, wedge block, we specify only six points in space. All the intermediate points are computed and written by `blockMesh`. If in such a case, the `writePrecision` setting in the `controlDict` is insufficient, i.e. a too small number of digits is used to write the points file. `blockMesh`, by default⁶⁴, writes

⁶⁴At least in OpenFOAM-5.0. This might vary among the various version of OpenFOAM. Other versions have not been checked. This behaviour might have been introduced sometime in the past, or it have been there from the beginning.

with at least 10 digits.

```
1 // Set the precision of the points data to 10
2 IOstream::defaultPrecision(max(10u, IOstream::defaultPrecision()));
```

Listing 118: Using at least 10 digits for writing the `points` file; excerpt from the file `blockMesh.C` of OpenFOAM-5.0

However, some mesh manipulation tools, simply use the setting from the `writePrecision` setting in the `controlDict`. If a too small number of digits is specified in combination with writing in ascii format, information (geometric precision) may be lost. This lost precision may be sufficient to trigger the warning messages, which were discussed above.

OpenFOAM is, at times, quite generous when it comes to the information provided in its error messages. Below, the example warning message is shown again. This time, the relevant bit of information is highlighted in red. This very small difference between the local face-normal vector and the patch-average normal-vector is indicative of an issue regarding writing precision.

```
--> FOAM Warning :
    From function virtual void Foam::wedgePolyPatch::calcGeometry(Foam::PstreamBuffers&
in file meshes/polyMesh/polyPatches/constraint/wedge/wedgePolyPatch.C at line 70
Wedge patch 'front' is not planar. At local face at (4.07936 -0.000130603 0.0149657) the
normal (0 -0.999962 -0.00872414) differs from the average normal (8.95761e-21 -0.999962
-0.00872653) by 5.70802e-12
Either correct the patch or split it into planar parts
```

Listing 119: Insufficient `writePrecision` in `controlDict` when creating/using a 2D axisymmetric geometry.

This indication could also be gleaned from a comparison of the two listed vectors, the affected local face-normal and the patch-average normal-vector. However, the highlighted number, which is the magnitude of the difference, is much easier to read and comprehend.

Pitfall: `writePrecision` and wedge geometry II - inline code

A very similar problem was observed, when creating an axi-symmetric domain by using some inline code to compute vertex coordinates. Apparently, the `writePrecision` setting in the `controlDict` affects the precision of the calculated vertex coordinates. Thus, if the write precision is too low, `blockMesh` will warn about non-planar wedge patches. However, this can easily be remedied by using a write precision of 10 digits or above. Note, that writing in binary format does not alleviate this problem.

17.2.4 edges

The `edges` sub-dictionary contains pairs of vertices that define an edge. By default edges are straight, by explicitly specifying the shape of the edge, curved edges can be created. This sub-dictionary can be omitted. Listing 120 shows the message issued by `blockMesh` when `edges` is omitted.

```
No non-linear edges defined
```

Listing 120: Output of `blockMesh` when `edges` is omitted

Otherwise, `blockMesh` issues a message as in Listing 121 regardless whether curved edges are actually created or only an empty `edges` sub-dictionary is present.

```
Creating curved edges
```

Listing 121: Output of `blockMesh` when `edges` is present

Creating arcs

With the keyword `arc` a circular arc between two vertices can be created. Listing 122 shows the definition of a circular arc between the vertices 0 and 3. In order to define a circular arc three points are necessary. Therefore the third point follows the indizes of the two vertices defining the edge.

```
edges
(
    arc 0 3 (0 0.5 0.05)
);
```

Listing 122: Definition of a circular edges in the `edges` sub-dictionary

The keyword `arc` can not be used to define a straight edge. If the two vertices and the additional interpolation point are co-linear, `blockMesh` will abort issuing an error message as in Listing 123.

```
--> FOAM FATAL ERROR:
Invalid arc definition - are the points co-linear? Denom =0

From function cylindricalCS arcEdge::calcAngle()
in file curvedEdges/arcEdge.C at line 55.
```

FOAM aborting

Listing 123: Output of `blockMesh` when the three points defining an arc are co-linear

Creating splines

The keyword `spline` defines a spline. After the two vertices defining the edge a list of interpolation points has to follow.

```
edges
(
    spline 0 3 ((0 0.25 0.05) (0 0.75 0.05))
);
```

Listing 124: Definition of a spline in the `edges` sub-dictionary

Creating a poly-line

Other than a spline, a poly-line connects several points with straight lines.

```
edges
(
    polyLine 0 3 ((0 0.25 0.05) (0 0.75 0.05))
);
```

Listing 125: Definition of a poly-line in the `edges` sub-dictionary

Creating a straight line

For the sake of completeness there is the keyword `line`. This keyword takes the two vertices defining the edge as arguments. Straight lines are created by `blockMesh` by default. So there is no need for the user to specify straight lines.

```
edges
(
    line 0 3
);
```

Listing 126: Definition of a line in the `edges` sub-dictionary

Summary

Edges defined within the `blockMeshDict` are used to compute the locations of a block's internal nodes. The edge however, is approximated linearly as shown in Figure 15, i.e. the number of cells along the edge determine the resolution of the edges.

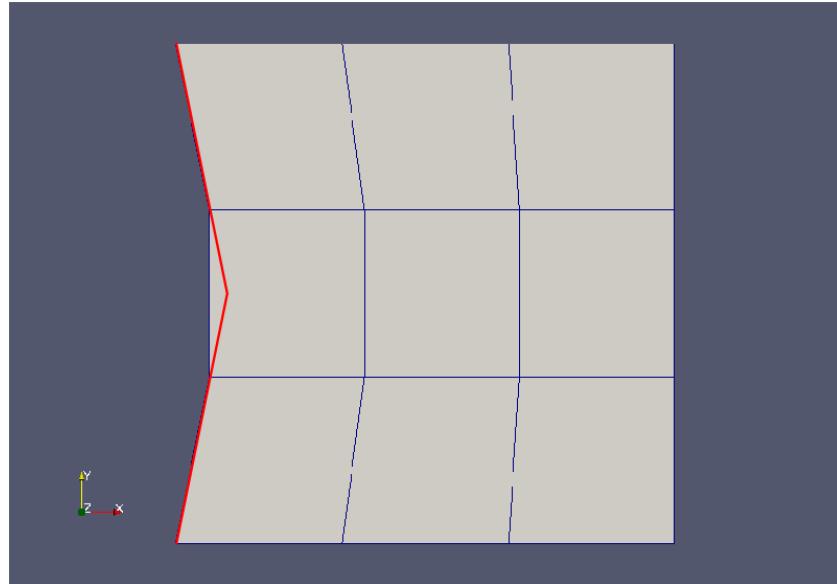


Figure 15: A block with a poly-line at the left side. The red line indicates the poly-line. This figure makes it obvious that edges defined in the `blockMeshDict` serve to compute the locations of the block's internal nodes. The block itself however, does not obey the poly-line.

Another feature of the edge definition is, that the two vertices defining the edge can be supplied in any order.

Pitfalls

Edge creation of `blockMesh` sometimes fails silently⁶⁵. If we define an arc between two vertices not directly connected by an edge, e.g. the vertices 0 and 2 in Figure 13, then `blockMesh` proceeds without any warning or error. The faulty edge definition seems to be simply ignored. This, silence in the face of error might make it hard for the user building his or her `blockMeshDict` to spot the reason why the definition of curved edges does not result in curved edges.

17.2.5 boundary

The `boundary` list contains a dictionary per patch. This dictionary contains the type of the patch and the list of faces composing the patch. Listing 127 shows an example of how a patch consisting of one face is defined.

```
boundary
(
    inlet
    {
        type patch;
        faces
        (
            (0 3 2 1)
        );
    }
    ...
);
```

⁶⁵An example non `blockMesh` failing noisily is the definition of a co-linear interpolation point for an arc.

Listing 127: The boundary list of `blockMeshDict`

Pitfall: `defaultFaces`

If faces are forgotten in the boundary definition, then `blockMesh` creates an additional patch named `defaultFaces`. This patch has an `empty` boundary condition automatically assigned. Listing 128 shows a warning message issued by `blockMesh`. In this case some faces were missing in the boundary definition. This, however, does not cause `blockMesh` to abort mesh generation. If a 2D mesh is to be created, the creation of the default patch with an `empty` boundary condition can be expected behaviour. However, it is not advisable to rely this kind of default behaviour when building a case.

```
Creating block mesh topology --> FOAM Warning :  
From function polyMesh::polyMesh(... construct from shapes...)  
in file meshes/polyMesh/polyMeshFromShapeMesh.C at line 903  
Found 6 undefined faces in mesh; adding to default patch.
```

Listing 128: A warning message of `blockMesh` caused by an incomplete boundary definition.

If faces are forgotten in the creation of a 3D mesh, this behaviour might hide the source of error. `blockMesh` quietly creates the mesh with the default patch – save the warning message as in Listing 128. Running the case with the erroneous mesh definition will not immediately crash the solver. Even the fact that none of the fields have a boundary condition specified for the default patch does not cause the solver to abort. A patch with an `empty` boundary condition does not require any further entries in the field-files (e.g. `U` or `p`). OpenFOAM knows already all it needs to know about this specific patch and there is no reason to throw an error message. When the case is run with a 3D mesh and one or more `empty` patches, the solver starts running without complaints. At some point the solution might run into numerical trouble.

Only running `checkMesh` is able to give an indication to detect such kind of error. Listing 129 shows the warning message issued by `checkMesh` when a 3D mesh contains one `empty` default patch. Although, the warning states that there is something wrong with the mesh, in the end `checkMesh` reports no failed mesh checks.

```
Checking topology...  
Boundary definition OK.  
***Total number of faces on empty patches is not divisible by the number of cells in the mesh  
. Hence this mesh is not 1D or 2D.
```

Listing 129: A warning message of `checkMesh` caused by an incomplete boundary definition of a 3D mesh.

Patch groups

Patches can be grouped to save ourselves the hassle to prescribe large numbers of identical boundary conditions. Patch groups were introduced with OpenFOAM-2.2.0 see <http://openfoam.org/release/2-2-0/pre-processing-macros-patch-groups/>. All boundaries of the constraint type, e.g. `empty` or `processor`, are automatically added to patch groups of the same name. Furthermore, since OpenFOAM-2.3.0⁶⁶, the patches of the type `wall` are added to a group named `wall`. Also, with OpenFOAM-2.3.0 the order of precedence for defining boundary conditions for fields was defined:

1. An exact match of the patch name, e.g. `inlet`
2. A match by a `patchGroup`
3. A match by regular expression, e.g. `"wallPatch.*"` for `wallPatch0815`

```
2  
(  
wall 4(0 1 2 3)  
empty 1(4)  
)
```

⁶⁶<http://openfoam.org/release/2-3-0/pre-processing/>

Listing 130: The automatically defined patch groups of the *cavity* tutorial of `icoFoam`. The list was created with the method `groupPatchIDs()` of the `Foam::polyBoundaryMesh` and printed to Terminal with the `Info` statement.

Keep in mind, that we can not apply regular expressions to group names.

Pitfall: multiple patch group membership

If patches are members of more than two groups, and the boundary conditions are specified via group membership, then the actual boundary condition that get applied is kind of undetermined. Some tests done by the author suggest that the last patch group entry in the field file prevails.

To demonstrate the issue, the *cavity* tutorial was slightly modified. The three patches representing the fixed walls, are members of the patch group `wall` by default and are members of the patch group `banana`, see Listing 131 below.

```
3
(
wall 4(0 1 2 3)
banana 3(1 2 3)
empty 1(4)
)
```

Listing 131: The patch groups of the modified *cavity* tutorial of `icoFoam`.

The velocity field BC definition was changed to employ patch groups.

```
boundaryField
{
    movingWall
    {
        type          fixedValue;
        value         uniform (1 0 0);
    }
    wall
    {
        type          noSlip;
    }
    banana
    {
        type          fixedValue;
        value         uniform (-1 0 0);
    }
}
```

Listing 132: The velocity field boundary conditions of the modified *cavity* tutorial. The entry for `frontAndBack` is omitted for brevity. Only `movingWall` is specified by exact patch name. The fixed walls are specified via patch groups.

The resulting initial velocity field depends on the order of the entries for `wall` and `banana`.

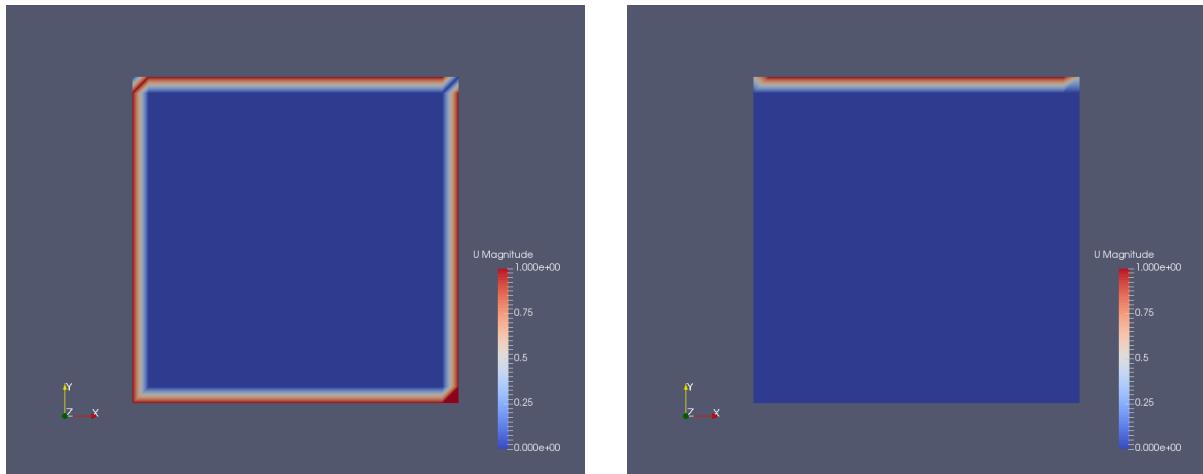


Figure 16: The initial velocity field depending on the order of the `wall` and `banana`. **Left:** Setting as in Listing 132. **Right:** `wall` and `banana` have changed places.

Thus, users are suggested to avoid situations involving multiple group membership when specifying boundary conditions via patch groups.

Pitfall: identical names of patches and patchGroups

When patches have the same name as a patchGroup, OpenFOAM may issue a warning or exit with an error. Up to, and including, OpenFOAM-4.0 a warning message was issued, as in Listing 133. In later versions, OpenFOAM aborts with an error, as in Listing 134.

```
--> FOAM Warning :
From function const Foam::HashTable<Foam::List<int>, Foam::word>& Foam::polyBoundaryMesh::
groupPatchIDs() const
in file meshes/polyMesh/polyBoundaryMesh/polyBoundaryMesh.C at line 448
Patch fixedWall01 specifies a group banana which is also a patch name. This might give
problems later on.
```

Listing 133: OpenFOAM is warning about identical names of a patch and a patchGroup.

```
--> FOAM FATAL ERROR:
Patch 'fixedWall01' specifies the group 'banana' which clashes with a patch name.
Please choose patch names which are not patch type/group names.

From function const Foam::HashTable<Foam::List<int>, Foam::word>& Foam::polyBoundaryMesh::
groupPatchIDs() const
in file meshes/polyMesh/polyBoundaryMesh/polyBoundaryMesh.C at line 448.
```

FOAM exiting

Listing 134: Identical names for patches and patchGroups are not allowed anymore.

Pitfall: patches

In older versions of OpenFOAM, there was a `patches` sub-dictionary instead of the boundary sub-dictionary, see <http://www.openfoam.org/version2.0.0/meshing.php>. In some tutorial cases the old `patches` sub-dictionary can be found. However, it is recommended to use the boundary sub-dictionary because in some cases the use of the `patches` sub-dictionary results in errors.

To find out if there are still tutorial cases present that use the `patches` sub-dictionary the command of Listing 135 searches all files with the name `blockMeshDict` in the tutorials for the word `patches`.

```
find $FOAM_TUTORIALS -name blockMeshDict | xargs grep patches
```

Listing 135: Find cases that still use the `patches` sub-dictionary in the `blockMeshDict` to define the boundaries

17.2.6 mergePatchPairs

The `mergePatchPairs` list contains pairs of patches that need to be connected by the mesher.

Nothing to merge

This entry can be omitted. Listing 136 shows the message issued by `blockMesh` when `mergePatchPairs` is omitted.

```
There are no merge patch pairs edges
```

Listing 136: Output of `blockMesh` when `mergePatchPairs` is omitted

Patches to merge

When two patches need to be merged, then the patch pair needs to be stated in the `mergePatchPairs` list. The first patch of the pair is considered the master patch the second is the slave patch. The reason and consequences of this are described in the official User Manual [52].

```
mergePatchPairs
(
    (master slave)
);
```

Listing 137: The `mergePatchPairs` list in the `blockMeshDict`

If the patches that are part of the merging operation contain faces which are unaffected by the merging, the merge operation will fail. When the blocks of Figure 20 are to be connected, then the patch pair consists only of the face (1 2 6 5) and (12 15 11 8). If one of the two patches contains an additional face, `blockMesh` will crash with an error. Thus the patches need to be defined as in Listing 138.

```
boundary
(
    master
    {
        type patch;
        faces
        (
            (1 2 6 5)
        );
    }
    slave
    {
        type patch;
        faces
        (
            (12 15 11 8)
        );
    }
    ...
);
```

Listing 138: The patch definitions needed to connect the blocks of Figure 20 with `mergePatchPairs` in the `boundary` sub-dictionary

`blockMesh` creates hanging nodes in order to connect the mesh of the blocks. Figure 17 shows the mesh of two merged blocks. Figure 18 shows the larger of the two blocks. The diagonal lines – one of them is marked with a red square in Figure 18 – are artefacts of the depiction of ParaView. The diagonal line that divides the L-shaped area is not present in the mesh. The right image in Figure 18 was edited with an image manipulation program to reflect the actual situation of the mesh. During the merging operation the face touching the second block is divided to match the second block. Thus, a quadrangular cell face is divided to two faces. The face denoted with the red 1 consists of 6 nodes and the face with the red 2 consists of four nodes.

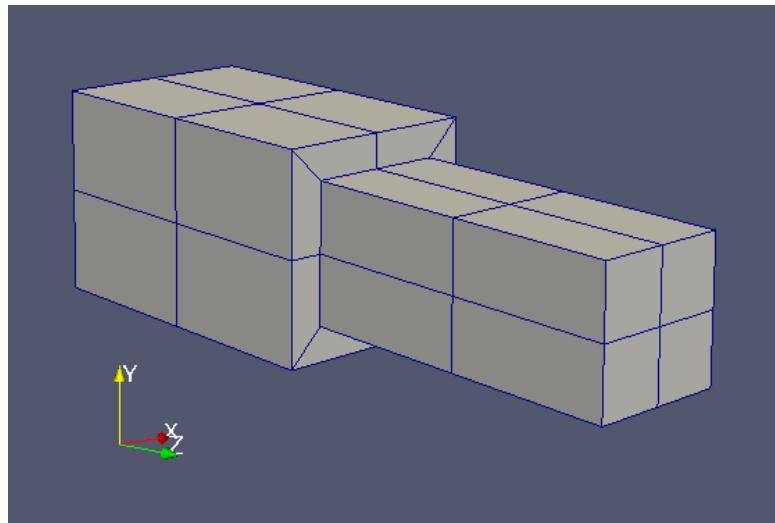


Figure 17: The mesh of two merged blocks

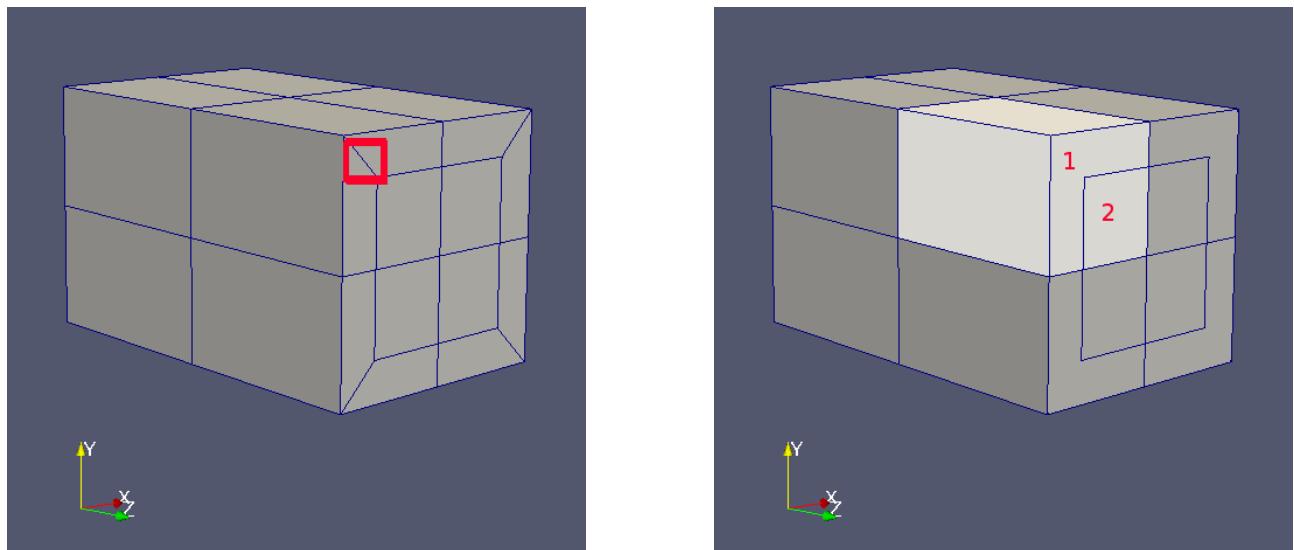


Figure 18: The mesh of two merged blocks. Left: screenshot of ParaView. Right: edited image to depict the actual faces.

17.3 Create multiple blocks

A single block is almost never sufficient to model the geometry of a CFD problem. *blockMesh* offers the possibility to create an arbitrary number of blocks which can be connected. If blocks are constructed in a fashion that they share vertices, then they are connected by *blockMesh* by default.

17.3.1 Connected blocks

Figure 19 shows two connected blocks. These blocks share vertices. Therefore, the blocks are connected automatically.

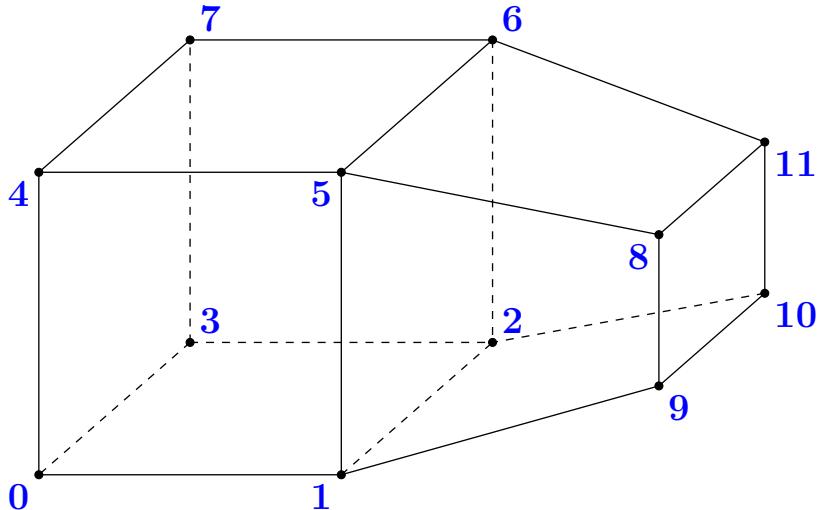


Figure 19: Two connected blocks

Listing 139 shows the `blocks` sub-dictionary to create two connected blocks as they are depicted in Figure 19. The global vertex numbering is arbitrary. However, the order in which the vertex numbers are listed after the `hex` keyword corresponds with the local vertex numbering of the generic block in Figure 13.

```
blocks
(
    hex (0 1 2 3 4 5 6 7) (10 10 10) simpleGrading (1 1 1)
    hex (1 9 10 2 5 8 11 6) (10 10 10) simpleGrading (1 1 1)
);
```

Listing 139: The `blocks` entries in `blockMeshDict` to create the connected blocks of Figure 19

17.3.2 Unconnected blocks

Figure 20 shows a situation in which two blocks were created that share no vertices. Creating multiple blocks is done simply by adding a further entry in the `blocks` list. The blocks are connected by the statements in the `mergePatchPairs` section of the `blockMeshDict`.

Listing 140 shows the `blocks` sub-dictionary to create two unconnected blocks as they are depicted in Figure 20.

```
blocks
(
    hex (0 1 2 3 4 5 6 7) (10 10 10) simpleGrading (1 1 1)
    hex (8 9 10 11 12 13 14 15) (10 10 10) simpleGrading (1 1 1)
);
```

Listing 140: The `blocks` entries in `blockMeshDict` to create the unconnected blocks of Figure 20

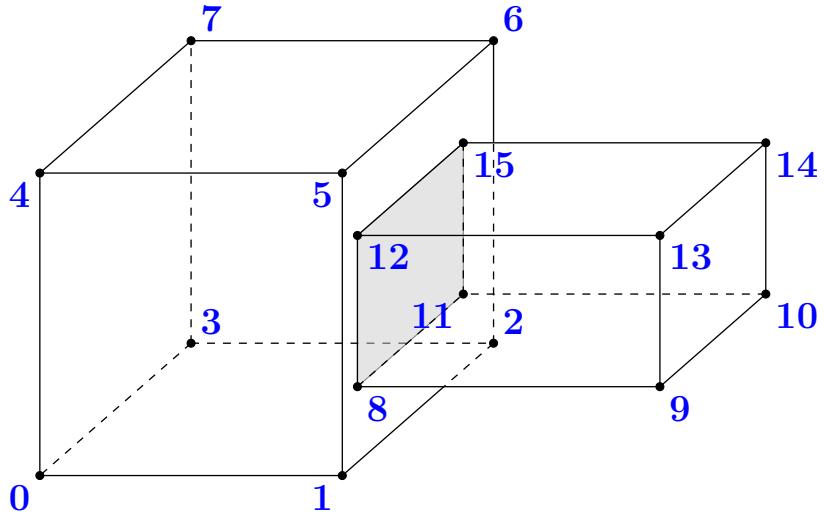


Figure 20: Two unconnected blocks

In order to generate a connected mesh of the two blocks, the `mergePatchPairs` section of the `blockMeshDict` has to be provided with the two touching patches.

17.4 *Grading*

In the file `blockMeshDict` the grading can be defined globally for the edges of the block or for all edges individually. The grading is specified by the expansion ratio. This is the ratio of the widths of the first and the last cell along an edge. The direction of an edge is defined in the general definition of a block (see OpenFOAM Users Manual [52]).

simpleGrading

The global grading is defined for all edges parallel to the local x , y and z direction of the block. In Listing 141 the grading of all edges parallel to the local x axis of the block is one, the grading of all edges parallel to the local y axis is two and the grading of all edges parallel to the local z axis is three.

```
simpleGrading (1 2 3)
```

Listing 141: *simpleGrading*

edgeGrading

With the keyword `edgeGrading` the grading of each edge of the block is specified individually. Therefore, the value of this keyword is a list with 12 numbers. The numbering of the edges – the list index corresponds to the edge number – is defined in the general definition of a block (see OpenFOAM Users Manual [52]). Listing 142 has the same effect as Listing 141.

```
edgeGrading (1 1 1 1 2 2 2 2 3 3 3 3)
```

Listing 142: *edgeGrading*

multiGrading

With the release of OpenFOAM-2.4.0⁶⁷, a new option for defining complex grading was introduced. Now, we can use a list of triples to specify the fraction of the block in terms of length, the fraction of the cells and

⁶⁷See <https://openfoam.org/release/2-4-0/>.

the grading factor. Listing 143 shows a block definition, which uses simple grading in x and z direction, and multiGrading is used.

Note, that the fractions do not need to add up to 1 or 100. OpenFOAM normalizes the provided fractions. However, for the sake of your own sanity, the use of percentages is advised. When looking at Listing 143, most people would assume percentages.

In this example, the block is divided into tree parts. These parts are 20%, 60% and 20% of the block's length. The parts use 30%, 40% and 30% of the specified number of cells. Lastly, the grading factors for these three parts are 4, 1 and 0.25.

```
blocks
(
    hex (0 1 2 3 4 5 6 7) (20 60 20)
        simpleGrading
        (
            1
            ((0.2 0.3 4) (0.6 0.4 1) (0.2 0.3 0.25))
            1
        )
);

```

Listing 143: *multiGrading*

Pitfall: inconsistent grading

When a mesh consists of more than one block, then the grading of coincident edges must be consistent, i.e. these edges must have the same grading. In Listing 144 the grading of the last block is erroneous – the grading is set to 2 instead of 3. The error message caused by this fault is shown in Listing 145. The message mentions the blocks 5 and 8. This is correct, because OpenFOAM counts – like C, C++ and many more programming languages – from 0. Therefore, block 8 is the ninth block.

```
blocks
(
    hex (0 16 20 4 1 17 21 5) (30 5 10) simpleGrading (1 0.5 0.33) // 1
    hex (1 17 21 5 2 18 22 6) (30 5 2) simpleGrading (1 0.5 1) // 2
    hex (2 18 22 6 3 19 23 7) (30 5 15) simpleGrading (1 0.5 3) // 3

    hex (4 20 24 8 5 21 25 9) (30 2 10) simpleGrading (1 1 0.33) // 4
    hex (5 21 25 9 6 22 26 10) (30 2 2) simpleGrading (1 1 1) // 5
    hex (6 22 26 10 7 23 27 11) (30 2 15) simpleGrading (1 1 3) // 6

    hex (8 24 28 12 9 25 29 13) (30 5 10) simpleGrading (1 2 0.33) // 7
    hex (9 25 29 13 10 26 30 14) (30 5 2) simpleGrading (1 2 1) // 8
    hex (10 26 30 14 11 27 31 15) (30 5 15) simpleGrading (1 2 2) // 9
);

```

Listing 144: Inconsistent grading

```
--> FOAM FATAL ERROR:
Inconsistent point locations between block pair 5 and 8
probably due to inconsistent grading.

From function blockMesh::calcMergeInfo()
in file blockMesh/blockMeshMerge.C at line 294.
```

FOAM exiting

Listing 145: Error message caused by inconsistent grading

Pitfall: inconsistent discretisation

When a mesh consists of more than one block, then the number of cells of neighbouring blocks must be consistent, i.e. the blocks must have the same number of cells along coincident axes. In Listing 146 the number of cells of the first block is erroneous – the number is set to 44 instead of 45 along the local *z* direction. The

error message caused by this faulty definition is shown in Listing 147. The message mentions the blocks 0 and 1. This error message indicates more clearly – other than Listing 145 – that OpenFOAM counts from 0.

```
blocks
(
    hex (0 1 5 4 8 9 13 12 ) (9 1 44) simpleGrading (1 1 1) // 1
    hex (1 2 6 5 9 10 14 13 ) (2 1 45) simpleGrading (1 1 1) // 2
    hex (2 3 7 6 10 11 15 14 ) (9 1 45) simpleGrading (1 1 1) // 3
);
```

Listing 146: Inconsistent discretisation

```
--> FOAM FATAL ERROR:
Inconsistent number of faces between block pair 0 and 1

From function blockMesh::calcMergeInfo()
in file blockMesh/blockMeshMerge.C at line 221.

FOAM exiting
```

Listing 147: Error message caused by inconsistent discretisation

Interesting observation

The source code also allows to state a list with only one entry. This is not documented in the official User Manual [52].

Listing 148 proves this observation in the form of the responsible source code. The first command reads a scalar list from the input stream `is`. Then the three valid cases – one, three or twelve entries – are handled. If none of the three branches of the `if-else` branching is entered an error is reported.

This code listing is a beautiful example of deducting the behaviour of a program from its source code. Unfortunately not all parts of OpenFOAMs source code are that easy to read and understand.

```
1 scalarList expRatios(is)
2
3 if (expRatios.size() == 1)
4 {
5     // identical in x/y/z-directions
6     expand_ = expRatios[0];
7 }
8 else if (expRatios.size() == 3)
9 {
10    // x-direction
11    expand_[0] = expRatios[0];
12    expand_[1] = expRatios[0];
13    expand_[2] = expRatios[0];
14    expand_[3] = expRatios[0];
15
16    // y-direction
17    expand_[4] = expRatios[1];
18    expand_[5] = expRatios[1];
19    expand_[6] = expRatios[1];
20    expand_[7] = expRatios[1];
21
22    // z-direction
23    expand_[8] = expRatios[2];
24    expand_[9] = expRatios[2];
25    expand_[10] = expRatios[2];
26    expand_[11] = expRatios[2];
27 }
28 else if (expRatios.size() == 12)
29 {
30     expand_ = expRatios;
31 }
32 else
33 {
34     FatalErrorIn
```

```

35   (
36     "blockDescriptor::blockDescriptor"
37     "(const pointField&, const curvedEdgeList&, Istream&)"
38   ) << "Unknown definition of expansion ratios: " << expRatios
39   << exit(FatalError);
40 }

```

Listing 148: Some content of `blockDescriptor.C`

Pitfall: grading on a wedge geometry

Axisymmetric simulation domains are created in the form of a wedge geometry. In this case, the axis patch is constructed from two vertices, which causes the axis patch to collapse into a straight line. Internally, OpenFOAM knows what to do in such a case.

However, it was observed when applying some grading along the axis of the domain, that not all faces of the axis patch are collapsed, resulting in a non-empty axis patch.

In Listing 149 the relevant part of the output of `blockMesh` is shown. In this case, some grading, in the direction of the symmetry axis, was used. In that specific case, there were nearly 1500 cells in axis-direction and only 6 faces in the axis patch. This discrepancy is highly suspicious, and it was assumed that during grading the collapsing of faces on the axis patch somehow failed for some points, resulting in 6 triangular faces.

```

Patches
-----
patch 0 (start: 118329 size: 14) name: inlet
patch 1 (start: 118343 size: 7) name: outlet
patch 2 (start: 118350 size: 1577) name: walls
patch 3 (start: 119927 size: 6) name: axis
patch 4 (start: 119933 size: 59938) name: front
patch 5 (start: 179871 size: 59938) name: back

```

Listing 149: The patch list of an axisymmetric case with a non-empty axis patch.

Having a non-empty axis patch poses no problem for `blockMesh` during mesh-creation, however, all other tools and solvers fail to construct a proper mesh. Listing 150 shows an example of the error message issued by OpenFOAM. Unfortunately, this error message is relatively inexpressive.

```

Create polyMesh for time = constant

#0 Foam::error::printStack(Foam::Ostream&) at ??:?
#1 Foam::sigFpe::sigHandler(int) at ??:?
#2 ? in "/lib/x86_64-linux-gnu/libc.so.6"
#3 Foam::polyMesh::calcDirections() const at ??:?
#4 Foam::polyMesh::polyMesh(Foam::IObject const&) at ??:?
#5 ? at ??:?
#6 __libc_start_main in "/lib/x86_64-linux-gnu/libc.so.6"
#7 ? at ??:?

Floating point exception (core dumped)

```

Listing 150: The result of having an axisymmetric case with a non-empty axis patch.

This problem was overcome by manually changing the patch type in `constant/polyMesh/boundary` of the axis patch from `empty` to `patch`, running `collapseEdges`, and finally manually changing the patch type back to `empty`. The manual changing of the patch type is necessary for `collapseEdges` to be able to read and construct the mesh. In Listing 151 we see the output of `checkMesh` after the solution procedure was applied to that example case. Now, the axis patch is empty, i.e. it contains no faces. Whether the patch is of the type `empty` or of the type `patch`, is not printed by `checkMesh`.

```

Checking patch topology for multiply connected surfaces...
Patch          Faces      Points    Surface topology
inlet           14         29        ok (non-closed singly connected)
outlet          7          15        ok (non-closed singly connected)
walls           1577       3156      ok (non-closed singly connected)
axis            0          0         ok (empty)
front           59938      61486     ok (non-closed singly connected)

```

back 59938 61486 ok (non-closed singly connected)

Listing 151: The patch list of an axisymmetric case after fixing the problem with the non-empty axis patch.

Simply, increasing the `writePrecision` or switching to writing in binary format did not resolve the problem.

Pitfall: local vs. global axes

Note, that grading is enacted on the local axes of the block. The author of these lines has encountered an amusing error of his own. Falsely setting grading along an axis, which happened to be, in a two-dimensional simulation, the non-solution axis. Thus, the discretisation in this direction was a single cell, and grading did nothing. Even when trying to force an inconsistent grading error, nothing happened. Finally, the author realised, that he had global and local axes mixed up.

In some cases, we can construct our blocks that local and global axes are nicely aligned, e.g., in axisymmetric or two-dimensional simulations. However, in other cases, especially in three dimensional geometries, this might not be able.

Hence, keep good awareness about the local and global axes.

17.4.1 Some math around grading

Grading refers to the gradual elongation of cells along a block edge. Figure 21 shows a generic edge of length L . There, we can define two quantities: the global expansion ratio E , and the local expansion ratio e .

The global expansion ratio E is defined as the ratio of the cell widths of the last and the first cell. The local expansion ratio e is the ratio of the widths of adjacent cells.

$$E = \frac{\delta_N}{\delta_1} \quad (8)$$

$$e = \frac{\delta_{i+1}}{\delta_i} \quad (9)$$

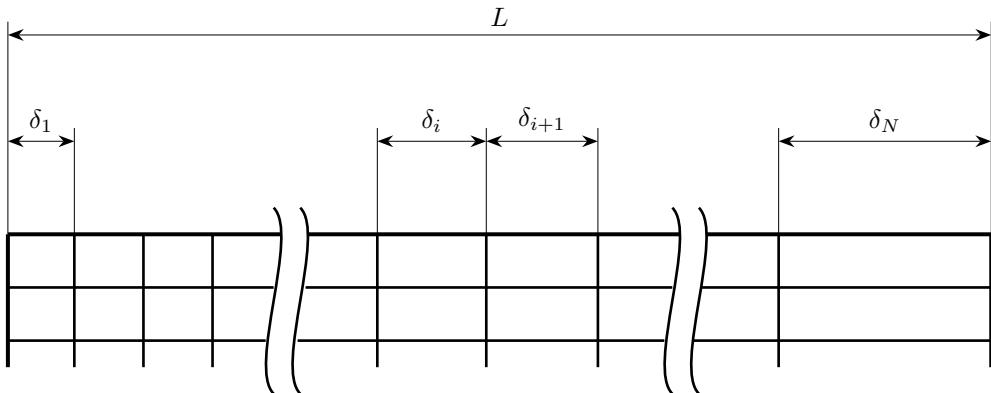


Figure 21: Mesh grading along a block edge.

Before we dive deeper into this topic, let us first state some more or less obvious relations:

$$L = \sum_1^N \delta_i \quad (10)$$

$$L = \sum_1^N (\delta_1 e^{i-1}) \quad (11)$$

$$E = e^{N-1} \quad (12)$$

Normally, we specify a mesh in `blockMeshDict` by providing the number of cells N and the global expansion ratio E , and by indirectly providing the edge's length L . The edge's length is computed automatically from the

vertices defining the edge. Note that this is a vast simplification for the user, since we can easily define edges being arcs or splines. However, in that case, computing the edge's length would be quite tricky for the user.

How to compute the number of cells from the cell width

Imagine a situation, in which our cell width δ_N needs to match the cell width of a neighboring block. If we used no grading at all, this would be easy, since the cell width can easily be computed via the edge length and the number of cells. Thus, computing the number of cells from the edge length and the cell width is equally easy. We simply need to rearrange Eq. (13).

$$\delta = \frac{L}{N} \quad (13)$$

In the case of mesh grading, the task becomes difficult. While Eq. (8) links the global expansion ratio with the cell widths at the start and the end of an edge. There is no obvious way to compute the required number of cells N for a given L , E and δ_N .

First, we multiply Eq. (11) by the local expansion ratio e :

$$e L = \sum_1^N (\delta_1 e^i) \quad (14)$$

Next, we subtract Eq. (14) from (11)

$$L - e L = \delta_1 - \delta_1 e^N \quad (15)$$

We then rearrange a bit and insert Eq. (12)

$$L E^{\frac{1}{N-1}} - \delta_1 E^{\frac{N}{N-1}} - L + \delta_1 = 0 = f(N) \quad (16)$$

Eq. (16) constitutes a function of N , for which we need to find the solution. This can not be done analytically.

Since pure math may not be sufficient for all readers, we now enlist the helpful service of a diagram. In Figure 22 we see an example. We have a given length L , a final cell width δ_N and an expansion ratio E . First, we can specify our boundaries within which we will find our solution. If we assume a uniform discretisation using the final cell width δ_N and the initial cell width $\delta_1 = \frac{\delta_N}{E}$, then we get two limiting cell numbers, with the solution being somewhere inbetween. Since the expansion ratio can be smaller or larger than 1, we shall make no assumptions whether the initial cell width is smaller or larger than the final cell width.

The two limiting cases are depicted in Figure 22 by the two blue square boxes. The function $f(N)$, given by Eq. (16) is shown by the blue line. The number of cells, actually fulfilling Eq. (16), is marked by the red circle. This solution can be found using a bisection method, since the function $f(N)$ is a monotonic function and its values at the boundary of the search interval have a different sign.

Thus, we calculate the center of the search interval, evaluate the function at this center value. Then, we take the lower or the upper half of the initial search interval as our new search interval, such that the function values of the new interval boundaries are again of opposite sign. With the new search interval, we begin anew by bisecting it. We stop our method, once we get sufficiently close⁶⁸ to the root of the function. Finally, we need to convert the solution into an integer number, since `blockMesh` will not generate 257.3131 cells.

⁶⁸At first, we judged whether we are sufficiently close to the root of the function based on the function's value. However, we can also base the criterion on the solution itself. Since we are looking for a number of cells, we can stop the search, when we have reached integer resolution. A solution of 257.3 is no less accurate than 257.3131, since both are rounded to the nearest integer.

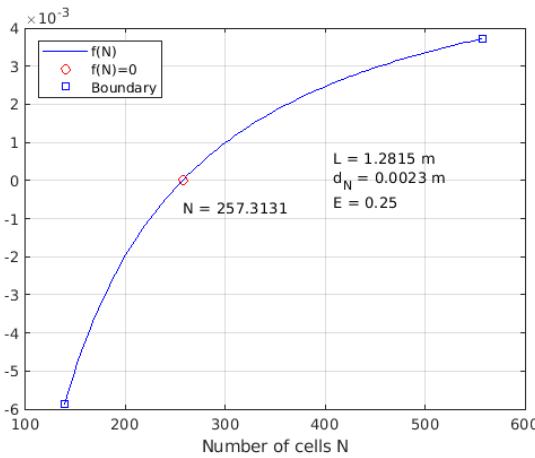


Figure 22: Computing the number of cells for a given cell width and grading expansion factor: the plot shows the function given by Eq. (16) for a specific set of given values (listed in the plot).

17.5 Parametric meshes by the help of *m4* and *blockMesh*

In *blockMeshDict* only plain text is allowed, i.e. no symbols can be used. Also, no calculations can be made by *blockMesh* with the exception of the keyword `convertToMeters`.

17.5.1 The *blockMeshDict* prototype

If the user wants to create parametrised meshes, i.e. properties of the mesh are calculated from certain parameters, an additional working step is necessary. In order to create a parametric mesh a prototype of the file *blockMeshDict* is needed. This prototype contains symbols. Listing 152 shows the block definition of such a prototype. This block definition is not fully parametric, only the number of cells is calculated. Note, that in local *y* direction only one cell is used for discretisation. This indicates a 2D problem.

```
blocks
(
    hex (0 1 5 4 8 9 13 12) (N1x 1 N1z) simpleGrading (1 1 1) // 1
    hex (1 2 6 5 9 10 14 13) (N2x 1 N1z) simpleGrading (1 1 1) // 2
    hex (2 3 7 6 10 11 15 14) (N1x 1 N1z) simpleGrading (1 1 1) // 3
);
```

Listing 152: Block definition of the prototype

17.5.2 The macro programming language *m4*

In order to replace the symbols of the prototype with meaningful numbers, the prototype has to be processed by a macro programming language interpreter. In this case the programming language *m4*⁶⁹ is used. The interpreter of this language scans the prototype for valid expressions (macros) and replaces them with their result.

To replace a symbol of the prototype with a meaningful number, a macro has to be defined. Listing 153 shows the definition of the symbols used in Listing 152. In the first line a general variable *h* is defined. The second and the third instruction calculate the number of cells in the local *x* direction based on the variable *h*. The last instruction calculates the number of cells in the local *z* direction.

```
define(h,2)

define(N1x, `eval(9*h)')
define(N2x, `eval(2*h)')

define(N1z, `eval(45*h)')
```

⁶⁹*m4* is part of the GNU project. See <http://www.gnu.org/software/m4/manual/index.html>

Listing 153: Block definition of the prototype

This kind of parametrisation allows to specify a multiplier for the number of cells. The discretisation length can not be refined gradually this way. Specifying the discretisation length requires more complex math than integer operations.

Complex math - first shot

The builtin mathematic macros of *m4* are restricted to integer operations only. As *m4* supports system calls, floating point calculations can be done by an external program. Consequently, the symbol is replaced by the result of the system call.

In Listing 154 some variables are defined. In line 13 a macro is defined that passes its arguments to the operating system via a system call. The argument of the command `esyscmd` gets executed in the command line. This is the reason for the rather complicated argument of `esyscmd`. The output of the command echo is the input of the command `bc`⁷⁰. Note the use of the pipe.

The input of the command `echo` is composed of three successive operations that need to be performed by the calculator. The first instruction says that two digits after the decimal point should be used. The second instruction calculates the difference between the first two arguments and the last instruction divides this difference by the third argument. These operations compute first the length of the block that needs to be discretised. Then by dividing this length by the discretisation length the number of cells is calculated.

The output is then formatted by the macro `format`. Note the formatting string `%.0f`. This causes the result to loose its digits after the decimal point. This step is absolutely necessary, because only integers are allowed to define the number of cells.

```
1 // # enter discretization length
2 define(dx,0.005)
3 define(dz,0.005)
4
5 // # enter x coordinates
6 define(x1,0.0555)
7 define(x2,0.0945)
8
9 // # enter heights (z coordinates)
10 define(H1, 0.20)
11
12 // # relDiff: ($1 - $2) / $3    # decimal places truncated (done by format %.0f)
13 define(relDiff,'format('%.0f', esyscmd(echo "scale=2; a=$1-$2; a/$3" | bc))')
14
15 define(N1x,'relDiff(x1,0,dx)')
16 define(N2x,'relDiff(x2,x1,dx)')
17
18 define(N1z,'relDiff(H1,0,dz)')
```

Listing 154: Block definition of the prototype

Listing 154 allows to calculate the number of cells from a specified discretisation length. Due to rounding operations the specified discretisation length is not exactly met. Listing 155 shows the result after the macros from Listings 152 and 154 have been processed.

```
blocks
(
    hex (0 1 5 4   8   9 13 12 ) (11 1 40) simpleGrading (1 1 1) // 1
    hex (1 2 6 5   9 10 14 13 ) (7   1 40) simpleGrading (1 1 1) // 2
    hex (2 3 7 6   10 11 15 14 ) (11 1 40) simpleGrading (1 1 1) // 3
);
```

Listing 155: Resulting parametric block definition

⁷⁰*bc* is a calculator program. It is part of the GNU project.

Complex math - the better solution

The above described way to do mathematical operations is not very elegant. At this place a more elaborate solution is presented.

Listing 156 shows some examples taken from a *m4* script found in the tutorials. The first statement changes the delimiter for comments. By changing the delimiter to //, comments have the same delimiter as C or C++. Remember, OpenFOAM dictionaries follow the C++ syntax, therefore, anything following a // is treated as a comment. Now, commented lines are always treated as comments by *m4* as well as OpenFOAM. See the first line of Listing 154. There, the // starts a comment for OpenFOAM and the # starts a comment for *m4*. Setting the delimiter for comments to be the same as in C++ removes an ambiguity and a possible source for errors.

The second line of Listing 156 redefines the quote delimiter. Changing this delimiters from the standard to the brackets is probably done to improve readability.

In line 4 of Listing 156 a macro named **calc** is defined. This macro also uses a system call to outsource the actual math. In this case the interpreter of the script programming language Perl⁷¹ is called. This interpreter receives a command line argument and an instruction. The command line argument -e tells the interpreter that only one line of code will follow. The interpreter will interpret this single line and exit. The instruction **print (\$1)** is a function that prints its argument on the standard output. The argument of the **print** function is the argument of the **calc** macro. Therefore, the mathematical operation can be written directly in the code. See line 9 for an example. There, the symbols **rb** and **Rb** are replaced my *m4* by their definition. The argument of the **calc** macro is passed via the system call to the Perl interpreter. As Perl is able to do mathematical operations, the interpreter computes the result of the expression and executes the function **print**. The macro **esyscmd** returns the standard output of the command it executed.

Line 12 of Listing 156 shows that even more complex math – e.g. using trigonometric functions – is possible.

```
1 changeom(//)
2 changequote([,])
3
4 define(calc, [esyscmd/perl -e 'print ($1)'])
5
6 define(rb, 0.5)
7 define(Rb, 0.7)
8
9 define(ri, calc(0.5*(rb + Rb)))
10
11 define(pi, 3.14159265)
12 define(ca0, calc(cos((pi/180)*a0)))
```

Listing 156: Doing complex math with *m4*

We can also convert Listing 154 to use **perl** instead of **bc**. Here, we do the same calculation, only we are converting the result into an integer type before printing it. In Listing 154, we used the **format** instruction to ensure that the result is not a floating point number.

Comparing Line 13 of Listing 154 with Line 1 of Listing 157 reveals some simplification. In both cases, we defined a macro named **relDiff**. The usage of this macro is the same.

```
1 define(relDiff, 'esyscmd/perl -e "print(int(($1-($2))/$3))" ')
2
3 define(N1x,'relDiff(x1,0,dx)')
```

Listing 157: Doing complex math with *m4*; an alternative for Listing 154: using **perl** instead of **bc** for calculations.

17.5.3 Conclusion

Parametric meshes can be created by using the macro language *m4*, this is demonstrated in real live by the OpenFOAM tutorials. Also the author of this work has done so; up to a level which prompted his colleagues to make fun of him. This highlights the major shortcoming of using *m4* for parametric meshes. At some point, the parametric geometry creation poses the need for complex math or even high-level data structures. Thus, we soon are in need of a general purpose programming (or scripting) language.

⁷¹See <http://www.perl.org/>

The mesh in Figure 23 was created with a parametric geometry. It features a variable, user-selectable number of rotor-paddles n_b and stator-baffles n_p , with the constraint of that numbers being an integer divisor of 12. The two numbers n_b and n_p are independent of each other, as demonstrated in Figure 23. The infinitely thin baffles and paddles are created by preventing selected blocks from getting connected by the use of collocated points.

$$n_b, n_p \in \{1, 2, 3, 4, 6, 12\} \quad (17)$$

In total the mesh shown in Figure 23 consists of 459 blocks. This mesh (most probably⁷²) would have been impossible to create using *m4*. The scripting language of choice for this mesh was *python*⁷³, which is an interpreted high-level, general-purpose programming language.

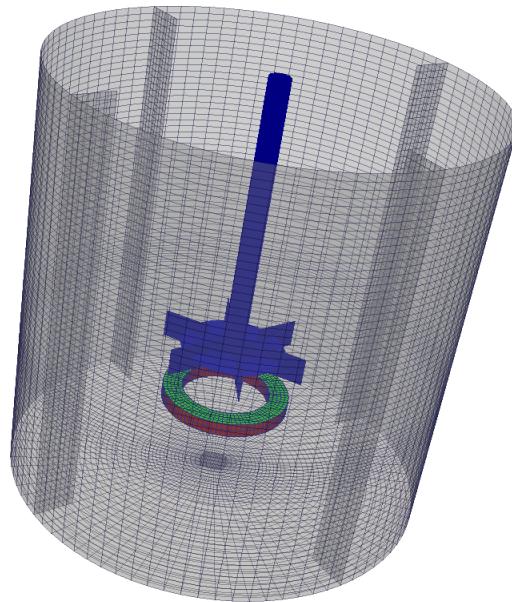


Figure 23: The mesh of a stirred tank with a Rushton impeller, stator baffles and an aeration device.

Thus, we conclude this section on using *m4* for geometry creation with Eric S. Raymond's view on *m4*:

The *m4* macro language supports conditionals and recursion. The combination can be used to implement loops, and this was intended; *m4* is deliberately Turing-complete. But actually trying to use *m4* as a general-purpose language would be deeply perverse.

This quote from Eric S. Raymond [22] should not be seen as trying to discourage the use of *m4* for simple task. It is intended to point out the limitations of macro languages. The limitation met and experienced by the author are the following:

Math In the sections above, we discussed two ways to perform complex mathematical operations within an *m4* script, by utilizing *bc* or *perl* via a system call. In *python*, we can do complex math directly, without having to perform system calls to programs which, might or might not be installed on the user's system.

Data structures The mesh generation script for the stirred tank makes use of *python*'s high-level data structure reflecting the organisation of the points on the geometry. Thus, the resulting script is far better to understand than an even less complex *m4* script.

File I/O With *m4*, all we can do is macro substitution. Thus, everything comes from one file and goes to one file. With a high-level language such as *python*, we can write several files. Thus, all files containing geometric information can be written by the same script, e.g. the *blockMeshDict* and the *topoSetDict(s)*. This improves maintainability and reduces code duplication and manual labour.

⁷²After some initial attempts, the author gave up.

⁷³<https://www.python.org/>

17.5.4 Parametric meshes by the help of Python

As mentioned in the previous sub-section on the creation of parametric meshes with the scripting language *m4*, Python offers a great deal more versatility. This can partly be attributed to the passage of time, since *m4* first appeared in 1977 and Python was released in 1990. However, the main factor is language-design, since Python has been designed around high-level data structures among other things.

Furthermore, repeated tasks can be more easily encapsulated into functions, e.g. write a block-definition from a list of nodes and a list of cell numbers.

17.5.5 Parametric meshes with OpenFOAM's on-board tools

Using the `#calc` directive

We can do complex math by using OpenFOAM's `#calc` directive, as shown in Listing 158. Here we assign the result of an inline calculation to a variable, which we can use just as any other variable with OpenFOAM's macro expansion.

As Listing 158 shows, we can use all functions that are part of the C standard library.

```
1 // compute the x-discretisation of the first block
2 NX1 #calc "std::ceil( ($X1 - $X0) / $dx )";
3
4 // manually assign a value
5 NZ1 10;
6
7 // the block-definition of the first block; here NX1 and NZ1 are being used
8 hex (0 1 5 4 12 13 17 16) ($NX1 $NY1 $NZ1) simpleGrading (1 1 1) // 1
```

Listing 158: Using the `#calc` directive for inline calculations in `blockMeshDict`.

```
1 #include "dictionary.H"
2 #include "Ostream.H"
3 #include "Pstream.H"
4 #include "unitConversion.H"
5
6 namespace Foam
7 {
8
9 extern "C"
10 {
11     void codeStream_faaac6ab5d5819d340ee97b4ed5bc6ec9820e7fb
12     (
13         Ostream& os,
14             const dictionary& dict
15     )
16     //{{ begin code
17     #line 1 "" os << (std::ceil( (7.500000e-02 - 0.000000e+00) / 3.000000e-02 ));
18     //}} end code
19     }
20 }
21
22 } // End namespace Foam
```

Listing 159: OpenFOAM creates and runs this code from the `#calc` directive in Line 2 of Listing 158.

Use the following command to find examples on the use of the `#calc` directive in the OpenFOAM tutorials:

```
find $FOAM_TUTORIALS -type f | xargs grep '#calc'
```

Listing 160: Find usage examples of the `#calc` directive in the tutorials.

Drawback

Using OpenFOAM to do the math, or any other tasks, has the drawback that we don't get to see the final `blockMeshDict` file. If we have an error in our math or our logic, then `blockMesh` will interpret its input in the `blockMeshDict` file, and the error will lead to an error in mesh-creation. The result will be an error message

on the part of OpenFOAM. However, since the process is as follows, and everything happens within *blockMesh*, debugging will be more difficult.

- Read and interpret the **blockMeshDict**
- Run all blocks of code
- Create the mesh

In the case of a scripting language, such as *mg* or Python, the interpreter runs the script and writes the **blockMeshDict** to disk. Any math or logic error can be found in the resulting **blockMeshDict** file, e.g. in terms of non-matching discretisation between adjacent blocks.

17.6 Trouble-shooting

17.6.1 Don't be misled by error messages

During manually building a small mesh with *blockMesh* by hand, i.e. writing the **blockMeshDict** using nothing but an ordinary text editor, I made a rather interesting observation. To save myself the effort of scrolling back and forth between the vertex list and the patch definition, I copied a part of the vertex list and pasted it right where I specified the boundary faces. Thus, vertex definitions ended up, where patch definitions are expected. After I ran *blockMesh* without removing the vertex definitions from the list of patches, *blockMesh* unsurprisingly failed. However, this example shows that OpenFOAM's error messages can be misleading.

Listing 161 shows the output of *blockMesh* resulting from the above outlined scenario. The warning message correctly reports an unexpected input, the error message however, reports a hanging pointer. The hanging pointer is certainly caused by the faulty entry, however, the error message does not indicate an error within the **blockMeshDict**. In this case, the warning message bears the relevant information, hence users are advised to carefully read OpenFOAM's output (warning and error messages) in case something goes wrong.

```
Creating topology blocks
Creating topology patches
--> FOAM Warning :
    From function entry::getKeyword(keyType&, Istream&
    in file db/dictionary/entry/entryIO.C at line 80
    Reading /home/user/OpenFOAM/user-4.0/run/meshing/testCase/system/blockMeshDict.boundary
    found on line 135 the punctuation token '('
    expected either } or EOF

...
--> FOAM FATAL ERROR:
    hanging pointer at index 8 (size 12), cannot dereference

    From function const T& Foam::UPtrList<T>::operator[](Foam::label) const [with T = Foam::
    entry; Foam::label = int]
    in file /home/user/OpenFOAM/OpenFOAM-4.0/src/OpenFOAM/lnInclude/UPtrListI.H at line 107.

FOAM aborting
#0  Foam::error::printStack(Foam::Ostream&) at ???:?
```

Listing 161: The output of *blockMesh* with a faulty **blockMeshDict**. The red dots indicate removed warning messages were removed for brevity.

This observation the warning message carries more useful information than the error message might apply also to other parts of the OpenFOAM framework.

17.6.2 Viewing the blocks with *ParaView*

A mesh created by *blockMesh* consists of blocks. Listing 162 shows how *ParaView* can be used to visualise the blocks.

```
paraFoam -block
```

Listing 162: Visualising the blocks

This way, only the blocks are displayed. ParaView only reads the file `blockMeshDict`. Figure 24 shows the blocks of a parametric mesh. It consists of nine blocks. The image shows also the numbers of the vertices.

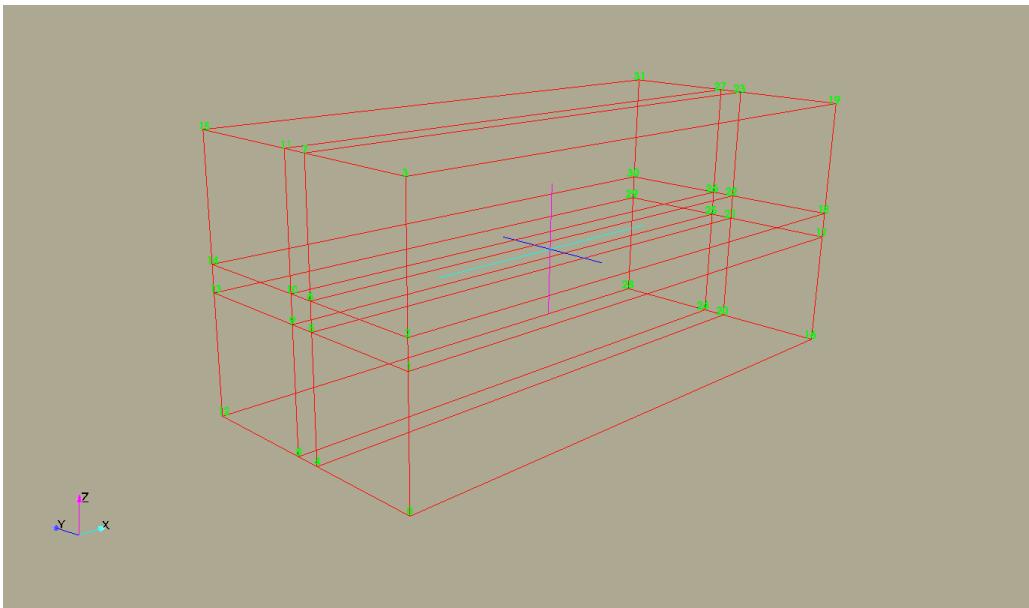


Figure 24: The blocks of a parametric mesh consisting of nine blocks.

17.6.3 Viewing the blocks with *pyFoam*

Troubleshooting can be difficult when `blockMesh` doesn't create a mesh and displays some error messages instead.

See Section 17.6.2 for the discussion of a tool which is able to display the blocks as they are defined in `blockMeshDict`. This tool even works, when `blockMesh` fails due to an erroneous definition in `blockMeshDict`.

18 *snappyHexMesh*

snappyHexMesh, also referred to as *snappy*, is a meshing tool that is able to mesh the space around an arbitrary triangulated surface, e.g. an STL surface-mesh. This is generally the case in external aerodynamics. *snappyHexMesh* can only be used in conjunction with *blockMesh*, since it requires a background mesh.

18.1 Documentation

Unfortunately, the complexity of *snappyHexMesh* outweighs the available on-board documentation. The on-board documentation (User Guide) can be found in `doc/Guides-a4` or `doc/Guides-usletter` of your local OpenFOAM installation or online at <http://www.openfoam.org/docs/user/>. You find a commented `snappyHexMeshDict` at `$FOAM_UTILITIES/mesh/generation/snappyHexMesh`. This is the case for all utilities which are controlled by an utility-specific dictionary file, such as `decomposePar`, `topoSet` and many more.

Individual features of *snappy* are in some cases discussed in the release notes of the release with which these features were rolled out. Another source of good documentation of *snappy* are presentations held at the OpenFOAM Workshops. An internet search with appropriate keywords will point the reader to them, since some of them are publicly available on the internets.

As with any other tool, the reader is encouraged to run the tutorials provided by OpenFOAM and play around with them. The tutorial cases also provide a good starting base for building your own cases.

18.2 Work flow

The creation of a mesh by *snappyHexMesh* is typically following a two step approach:

1. The background mesh is created by *blockMesh*⁷⁴. This is absolutely necessary to the later work of *snappy*. It is advised for the background mesh to consist of all-hex cells with an aspect ratio of 1, i.e. cube-shaped cells. It is furthermore beneficial to have many intersections of the background mesh's cell-edges with the tri-surface.
2. *snappyHexMesh* then performs three basic steps:
 - (a) *Castellating*
The tri-surface is approximated by splitting and removing cells outside the tri-surface.
Cell splitting The cells of the background mesh near the object's surface are refined.
Cell removal Cells of the background mesh inside the object are removed.
 - (b) *Snapping*
Cell snapping The remaining background mesh is modified in order to reconstruct the surface of the object.
 - (c) *Layer addition*
Layer addition Additional hexahedral cells are introduced on the boundary surface of the object to ensure a good mesh quality.

The three basic steps of *snappyHexMesh* can be performed independently of each other, and one can perform any combination of them. One approach making use of this fact, is to use *snappyHexMesh* solely as a layer addition tool.

18.3 Example: Bath Tub

With the help of an actual example, we will now discuss some of *snappyHexMesh*'s features, as problems and insights most often come with practical use. Our bath tub has a non-trivial shape, thus we are not inclined to painfully create the `blockMeshDict` by hand or by script. For complicated geometries a sophisticated meshing tool such as *snappy* is the way to go.

⁷⁴Strictly speaking, any valid OpenFOAM mesh can be used as input for *snappyHexMesh*.

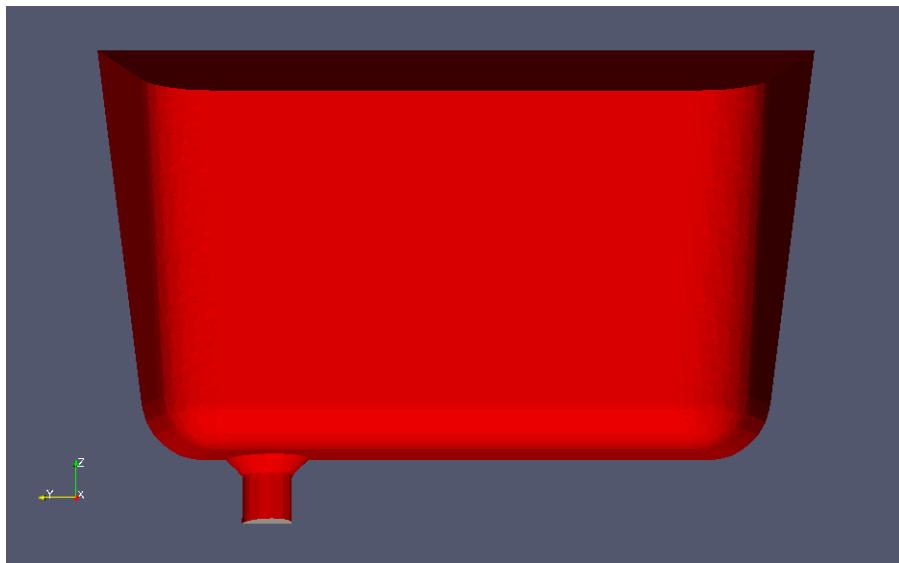


Figure 25: A bath tub. The outlet patch is marked grey at the very bottom of the drain tube.

18.3.1 Boundary layers

Boundary layers are added in the last stage of *snappy*'s operation. These are added on a per-patch basis. Thus, it is not possible to add layers only to parts of a patch. On the patch itself, we can control the regions in which to add a layer by the keyword `featureAngle`. The operation of the layer addition stage is controlled by the `addLayersControls` dictionary of `snappyHexMeshDict`.

Some of the entries of the `addLayersControls` dictionary are self-explanatory, such as the `layers` dictionary specifying the patches on which to add layers of cells. However, other parameters are not that obvious in their meaning.

`featureAngle`

The `featureAngle` is the angle between two consecutive faces. This parameter controls the behaviour of the layer addition stage at corners and bends.

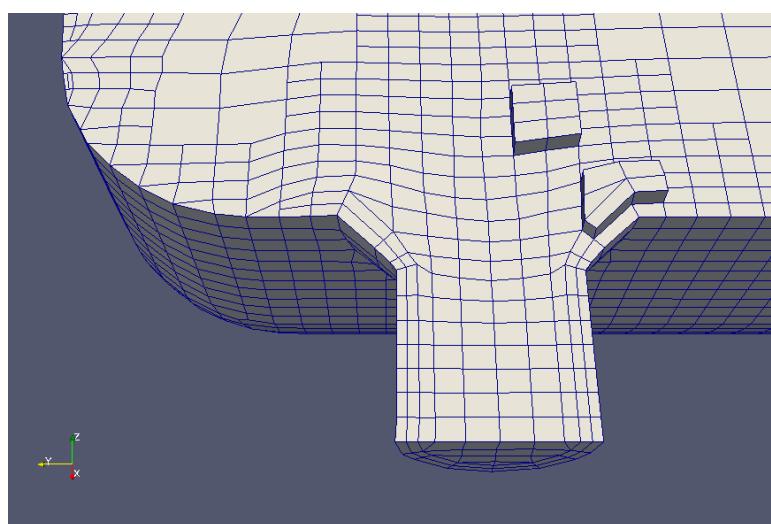


Figure 26: A badly chosen `featureAngle` causes *snappy* to add incomplete boundary layers.

slipFeatureAngle

At the outlet patch of our domain, the layer added to the wall patch meets the outlet patch, i.e. vertices need to be added to the outlet patch in order to properly grow a layer of cells onto the wall patch. See the left side of Figure 27. In order to achieve this, we must be able to alter the outlet patch during layer addition even though, we do not add a layer to the outlet patch itself.

This feature is discussed in the release notes⁷⁵ of OpenFOAM-2.2.0.

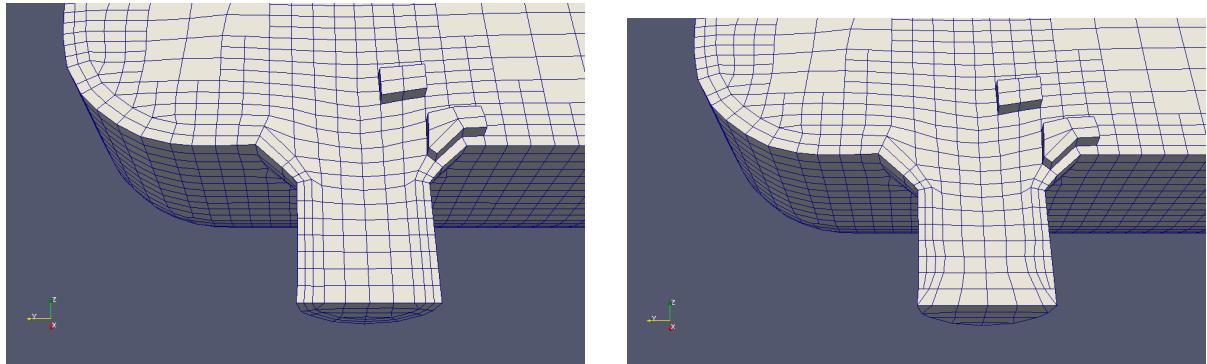


Figure 27: The boundary layers added by snappy. On the left, layer addition went as we intended it to do; on the right, we see the effect of the (missing) keyword `slipFeatureAngle` of the `addLayersControls` dictionary of `snappyHexMeshDict`.

Exclude patches

We have to freedom to tell *snappyHexMesh* to leave patches alone. Thus, during layer addition these patches remain untouched. This allows us to reverse the effect we achieved with the `slipFeatureAngle` parameter. By specifically excluding the outlet from any layer addition activity (see Listing 163), we end up with a collapsing cell layer at the boundary of the outlet patch, see Figure 28.

```
layers
{
    bathTub
    {
        nSurfaceLayers 2;
    }
    outlet
    {
        nSurfaceLayers 0;
    }
}
```

Listing 163: The `layers` sub-dictionary of the `addLayersControl` dictionary: specifically excluding a patch from layer addition.

This example of use may most probably not meet practical requirements, however, it demonstrates how *snappy* works. The take-away message might be that `nSurfaceLayers` beats `slipFeatureAngle`.

A non-academic (read less-useless) theoretical use-case for excluding patches from layer addition might be, when we later merge different meshes. In that case, we might want to preserve some patches for the merging operation.

⁷⁵<http://www.openfoam.org/version2.2.0/snappyHexMesh.php>

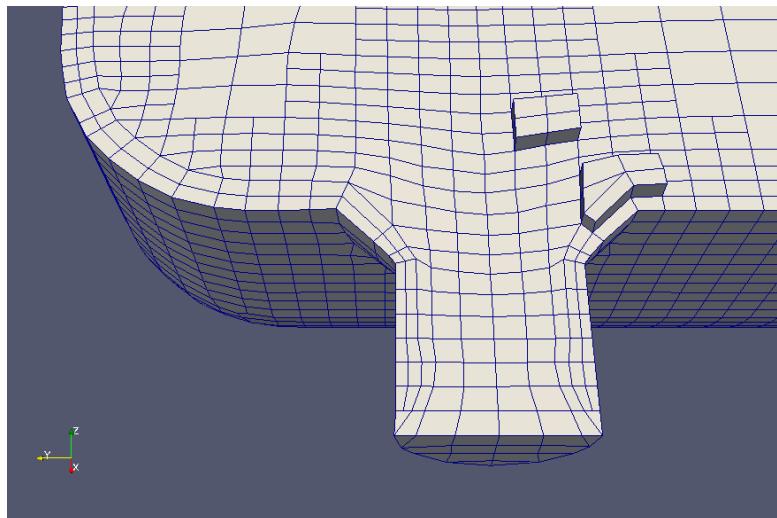


Figure 28: A collapsing boundary layer. Maybe we did not want the mesh that way, however, we told *snappy* to create it exactly that way.

18.3.2 Pitfalls, sources of error and hints on malfunction

Run time

If *snappyHexMesh* is finished in less than a second, then something is wrong. As *snappyHexMesh* performs up to three work intensive steps (castellation, snapping and layer addition), a run of *snappyHexMesh* takes a couple of seconds or even longer (tens of seconds).

Units

When creating a mesh with *snappyHexMesh* different scales (meter vs. millimeter) of the background mesh and the STL-mesh are a frequent source of error. Check the following things:

1. The unit of the vertex coordinates in `blockMeshDict`
2. The value of the `convertToMeters` keyword in `blockMeshDict`
3. The unit in which the STL was created

18.4 Example: Layer-Addition only

Figure 29 shows a mesh featuring a boundary layer which was created by *snappyHexMesh*. Thus, *snappyHexMesh* was used only for its layer addition stage. In normal operation, the background mesh is often created by *blockMesh*, however, any valid OpenFOAM mesh can serve as the input mesh for *snappyHexMesh*.

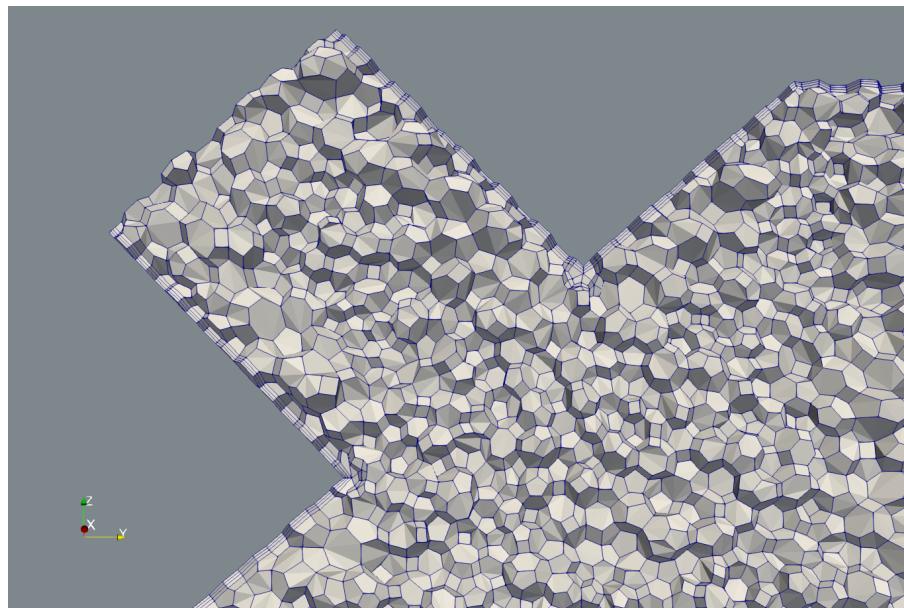


Figure 29: A boundary layer was created by *snappyHexMesh* on a polyhedral mesh which was created by other mesh creation tools.

19 *foamyHexMesh*

With OpenFOAM-2.3.0⁷⁶ the new meshing tool *foamyHexMesh* was released. This tool is to some degree similar to *snappyHexMesh*. The main distinction between *foamyHexMesh* and *snappyHexMesh* is that meshes by *foamyHexMesh* are better aligned with the boundary surfaces. This is achieved by a different mode of operation. *foamyHexMesh* generates an internal tetrahedral mesh fitting the boundaries, and then generates and massages the dual mesh of this internal tetrahedral mesh.

19.1 Crude comparison between a snappy and a foamy bath tub

In this section we compare the way foamy- and snappyHexMesh work on the example of meshing a bath tub. For this demonstration an STL-surface of a bath tub was created using OpenSCAD.

Figure 30 shows the outline and a part of the background mesh as well as our bath tub.

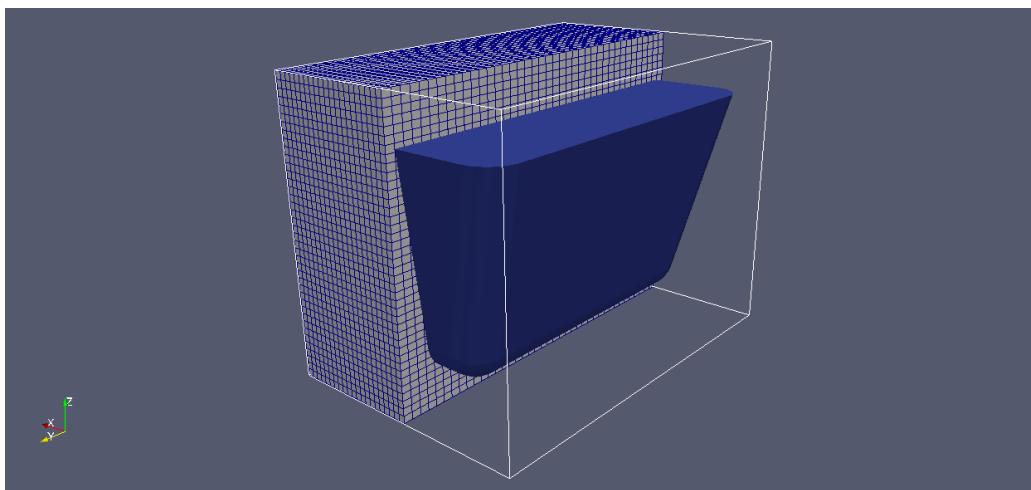


Figure 30: A bath tub with a background mesh enclosing the STL-surface of the bath tub.

19.1.1 SnappyBathTub

A first, the bath tub is meshed using *snappyHexMesh*. Figure 31 shows the resulting mesh. We clearly see, that the interior cells are aligned with the global coordinate axes. At the side walls, this leads to some minor flaws.

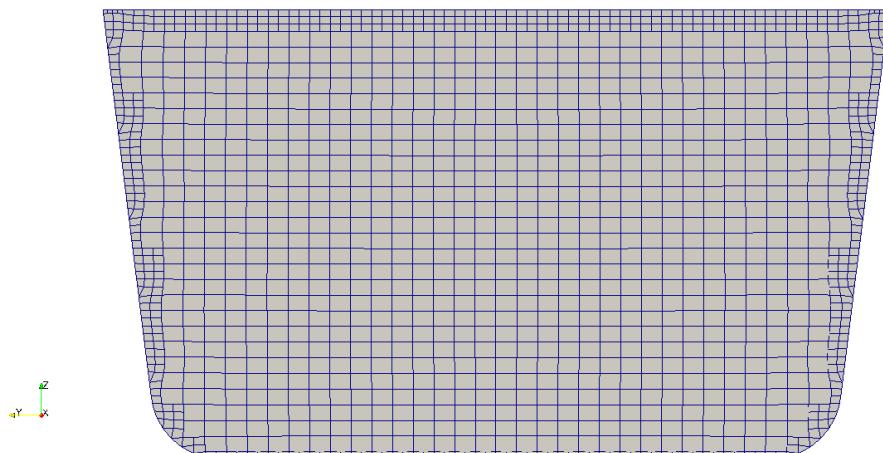


Figure 31: SnappyBathTub

⁷⁶<http://www.openfoam.org/version2.3.0/foamyHexMesh.php>

19.1.2 FoamyBathTub

Next, the bath tub was meshed using *foamyHexMesh*. In Figure 32 we see a good alignment of the cells with the boundaries. The interior cells are not aligned with the global coordinate axes.

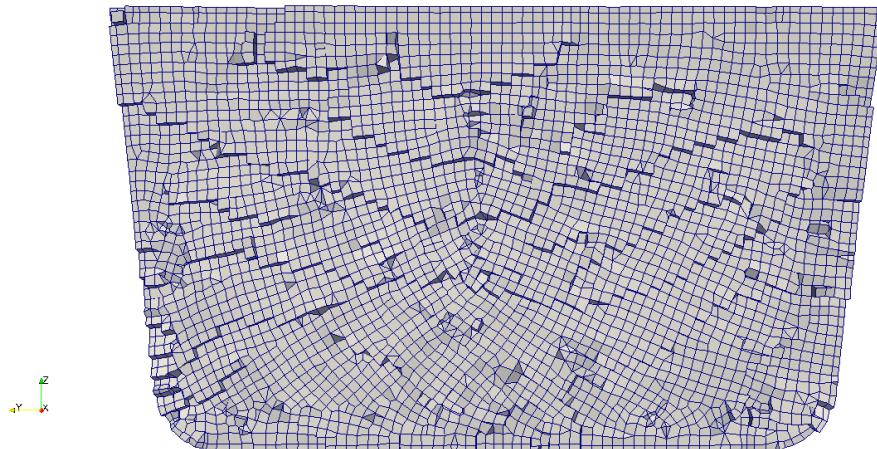


Figure 32: FoamyBathTub

20 *cfMesh*

cfMesh is a collection of meshing tools⁷⁷ provided by the company Creative Fields. This company offers the basic *cfMesh* suite under the GPL for free. At the time of writing *cfMesh* consists of four meshing tools which offer a workflow comparable to the workflow offered by *snappy-* and *foamyHexMesh*.

The meshing tools of *cfMesh* generate their mesh based on a user-provided surface-triangulation of the geometry. There is no need for a background mesh similar as it is the case with *foamyHexMesh*. All of the tools are capable of generating boundary layers on all or on selected surfaces. All the tools are controlled by a dictionary named `meshDict`, which resides in the `system` directory. In general the control of the user over the meshing tools is not as tight as with *snappy-* or *foamyHexMesh*. However, this less tight control manifests itself in a lightweight control dictionary compared to *snappy-* and *foamyHexMesh*.

The meshers of *cfMesh* are:

cartesian2DMesh is the tool to generate 2D meshes

tetMesh generates tetrahedral meshes

cartesianMesh generates meshes consisting mainly of hexahedrals, similar to *snappyHexMesh*

pMesh generates polyhedral meshes

cfMesh also provides a range of utilities (21 at the time of writing) for various tasks.

Integration into OpenFOAM-17.12

With the release of OpenFOAM-17.12⁷⁸, cfMesh was integrated into the ESI release of OpenFOAM.

20.1 Usage

20.1.1 To treat feature edges, or not to ...

Feature edges must be specified explicitly by the user for cfMesh to obey these edges.

In the case of the bath tub, which has a single patch a boundary, we see the effect of not providing feature edges explicitly in Figure 33. In this case the provided STL surface was not obeyed perfectly in favour of nicer cells. If we wanted to resolve the feature edge, we need to split the boundary of the geometry into more than one patch. As the edges between neighbouring patches are resolved by default by the mesher, diving the bath tub's boundary into several patches would solve the problem shown in Figure 33.

⁷⁷<http://cfmesh.com/>

⁷⁸<https://www.openfoam.com/news/main-news/openfoam-v1712/pre-processing#pre-processing-cfmesh>

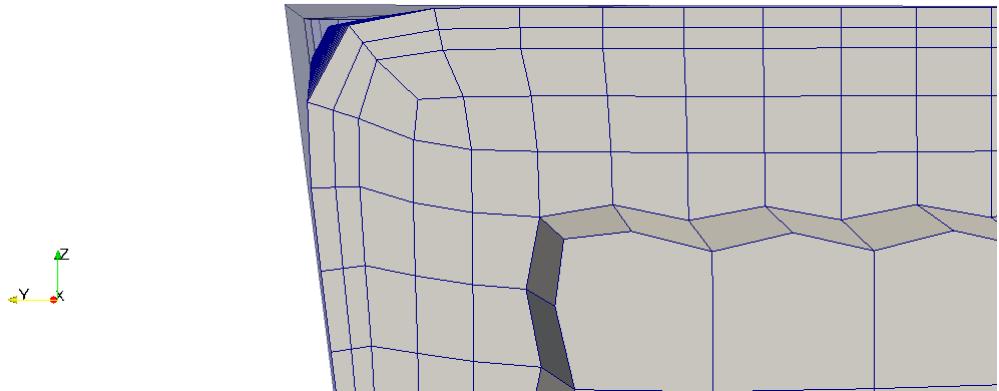


Figure 33: Poor feature edge resolution caused by not providing information on feature edges. Note, the whole geometry is bounded by a single patch.

If we want to resolve a feature edge which is not the boundary of two patches, we can use the utility tool `surfaceFeatureEdges` to extract the feature edges from the geometry. This tool checks the angles of neighbouring triangles of the surface triangulation and creates additional patches. E.g. the patch `wall` is divided into the patches `wall_0` to `wall_N`, if the specified feature angle results in `wall` being divided into N individual zones. `cfMesh` resolves the edges between neighbouring patches by default. Thus, the mesher is agnostic of our feature edge treatment. After finishing meshing, the mesher can rename patches. This feature of the mesher allows us to combine all the intermediate patches back into our initial `wall` patch.

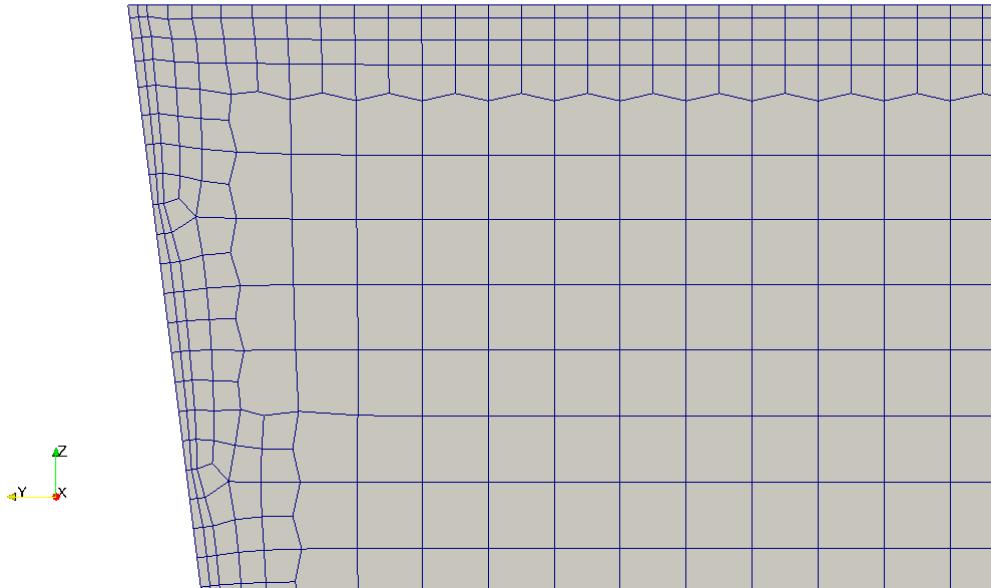


Figure 34: Resolved feature edge of the bath tub. In this case, the boundary consists of two patches: the top surface and the rest.

We note in Figure 34 the hanging nodes inserted by the mesher to join the different refinement levels. These hanging nodes protrude from the face they are inserted into. This prevents the faces connecting the cells of different refinement level from being coplanar, as it is the case with *snappyHexMesh*.

20.2 Generate boundary layers

The meshing tools of cfMesh are capable of generating boundary layer cells. The workflow follows a two-step approach: first, the base mesh is created, and then in a second step, the boundary layers are created by extrusion. Boundary layer generation is enabled when boundary layers are specified in the `boundaryLayers` dictionary in the `meshDict` file.

20.2.1 Standalone boundary layer generation

Similarly to snappyHexMesh, see Section 18.4, we can also use *cfMesh* to only create boundary layers. For this purpose, *cfMesh* provides the tool `generateBoundaryLayers`. This tool implements only the second step of the work-flow discussed above.

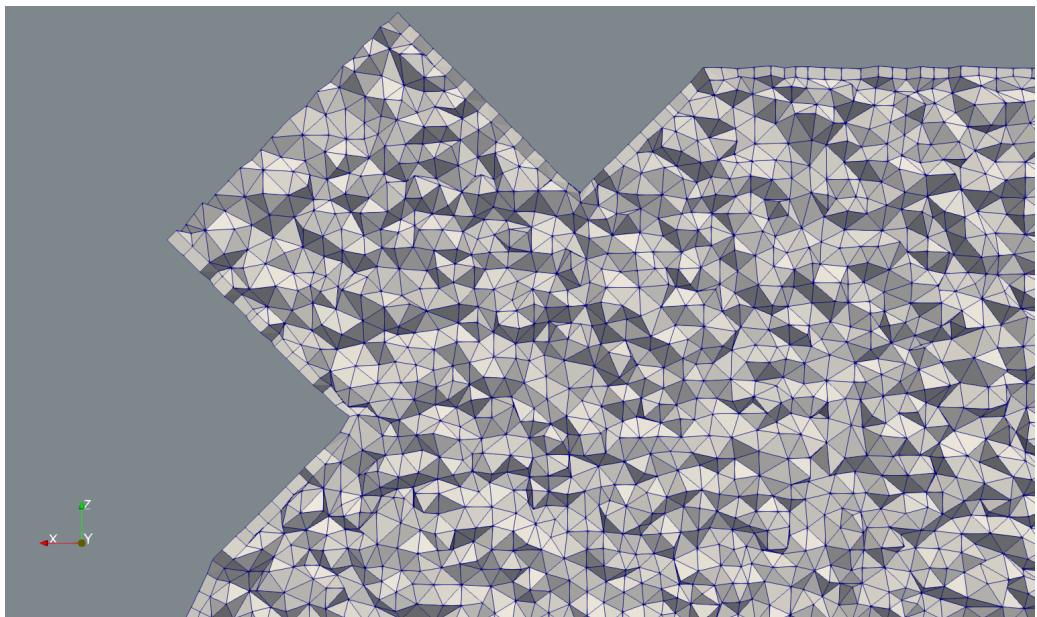


Figure 35: A single-cell thickness boundary layer on a tet-mesh created by the `generateBoundaryLayers` utility of *cfMesh*.

21 *checkMesh*

checkMesh is a tool to perform tests on an existing mesh. *checkMesh* is simply invoked by its name. Like other tools, *checkMesh* assumes to be called from the case directory. When *checkMesh* is to be called from an other location than the case directory, the path to the case directory has to be specified with the option **-case**.

Listing 164 shows an error message produced by *checkMesh*, if *checkMesh* has been called with no mesh present. In this case the tool can't find the files specified in Section 15.1.

```
--> FOAM FATAL ERROR:  
Cannot find file "points" in directory "polyMesh" in times 0 down to constant  
  
From function Time::findInstance(const fileName&, const word&, const IOobject::readOption,  
        const word&)  
in file db/Time/findInstance.C at line 188.  
  
FOAM exiting
```

Listing 164: No mesh present

A more thorough testing is performed when *checkMesh* is called with two additional options. Then *checkMesh* performs some further tests.

```
checkMesh -allGeometry -allTopology
```

Listing 165: Do more checks

checkMesh has also the **-latestTime** option like many other OpenFOAM tools. This option is particularly useful when examining meshes created by *snappyHexMesh*. *snappyHexMesh* stores intermediate meshes if it is not told otherwise. By default, after a completed run of *snappyHexMesh* there are the background mesh and the results of the three basic stages of a *snappyHexMesh* run (castellation, snapping and layer addition). Depending on which of these steps are active up to four meshes may be present. Restricting *checkMesh* to the final mesh reduces runtime and avoids the unnecessary examination of an intermediate mesh.

21.1 Definitions

In order to understand the output of *checkMesh* it is necessary to define some quantities calculated by *checkMesh*.

21.1.1 Face non-orthogonality

Non-orthogonality is a property of the faces of the mesh. We need to discriminate between internal faces and boundary faces.

Internal faces

Each internal face connects two cells. The non-orthogonality is the angle between the vector connecting the cell centres and the face normal vector. In Figure 36 the vector connecting the cell centres is denoted **d** and the face normal vector⁷⁹ **S**.

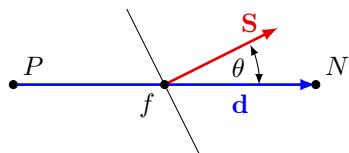


Figure 36: Definition of non-orthogonality for internal faces

⁷⁹The face normal vector or face area vector is a vector normal to a face. The length of this vector is equal to the area of the face.

In a perfectly orthogonal mesh the vectors \mathbf{d} and \mathbf{S} are parallel. If a mesh is non-orthogonal these vectors draw an angle as in Figure 36. This angle can be calculated from \mathbf{d} and \mathbf{S} by Eq. 20.

$$\mathbf{d} \cdot \mathbf{S} = \|\mathbf{d}\| \|\mathbf{S}\| \cos(\theta) \quad (18)$$

$$\frac{\mathbf{d} \cdot \mathbf{S}}{\|\mathbf{d}\| \|\mathbf{S}\|} = \frac{\|\mathbf{d}\| \|\mathbf{S}\| \cos(\theta)}{\|\mathbf{d}\| \|\mathbf{S}\|} = \cos(\theta) \quad (19)$$

$$\theta = \arccos\left(\frac{\mathbf{d} \cdot \mathbf{S}}{\|\mathbf{d}\| \|\mathbf{S}\|}\right) \quad (20)$$

Eq. 20 can also be found in the sources of OpenFOAM in the function `faceNonOrthogonality` in the file `cellQuality.C`⁸⁰. Listing 166 shows a loop over all faces. For each face the non-orthogonality is computed. The vectors \mathbf{d} and \mathbf{s} are the connecting vector between the cell centres, and the face area vector, respectively. The scalar `cosDDotS` is the angle θ of Figure 36.

Note the two precautions that were taken to avoid numerical issues. First, the denominator is the sum of the product of the magnitudes and `VSMALL`. `VSMALL` is a number with a very small value to prevent division by zero. Second, the argument of the `acos` function is `min(1.0, (d & s)/(mag(d)*magS + VSMALL))`. Keeping the argument of the arc-cosine equal or below 1 makes perfect sense, because the arc-cosine is defined only for values between -1 and 1. The limit of -1 is inherently ensured. The inner product of two vectors is always positive. `VSMALL` is also positive.

```

1  forAll(nei, faceI)
2  {
3      vector d = centres[nei[faceI]] - centres[own[faceI]];
4      vector s = areas[faceI];
5      scalar magS = mag(s);
6
7      scalar cosDDotS =
8          radToDeg(Foam::acos(min(1.0, (d & s)/(mag(d)*magS + VSMALL))));
9      result[faceI] = cosDDotS;
10 }

```

Listing 166: A detail of the function `faceNonOrthogonality` in the file `cellQuality.C`

The non-orthogonality reported by `checkMesh` is the angle θ of Figure 36. Therefore the reported non-orthogonality lies in the range between 0 and 90. A non-orthogonality of 0 means the mesh is orthogonal and consists of hexahedra (cuboids) or regular tetrahedra. Listing 170 shows the output of `checkMesh`. In this case the mesh is orthogonal, the maximum and average non-orthogonality is 0.

Listing 172 shows the output of `checkMesh` in case of a non-orthogonal mesh. Listing 173 indicates that a non-orthogonality of above 70 triggers `checkMesh` to issue a warning message.

Boundary faces

Non-orthogonality is also defined for boundary faces. Figure 37 shows a schematic boundary face with its face center f . Non-orthogonality of boundary faces is defined as the angle in degrees between the face area vector \mathbf{S} and the vector \mathbf{d} , which connects the cell center P and the face center f .

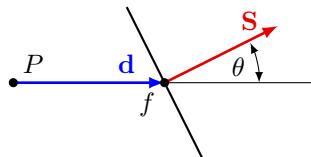


Figure 37: Definition of non-orthogonality for boundary faces

⁸⁰In the file `cellQuality.C` there are two methods defined: `nonOrthogonality()` and `faceNonOrthogonality()`. Comparing the code of this two methods reveals, that they compute the same thing. However, the method `nonOrthogonality()` returns the affected cells, whereas `faceNonOrthogonality()` returns the affected faces.

```

1 const labelUList& faceCells = mesh_.boundaryMesh()[patchI].faceCells();
2 const vectorField::subField faceCentres = mesh_.boundaryMesh()[patchI].faceCentres();
3 const vectorField::subField faceAreas = mesh_.boundaryMesh()[patchI].faceAreas();
4
5 forAll(nei, faceI)
6 {
7     vector d = faceCentres[faceI] - centres[faceCells[faceI]];
8     vector s = areas[faceI];
9     scalar magS = mag(s);
10
11    scalar cosDDotS =
12        radToDeg(Foam::acos(min(1.0, (d & s)/(mag(d)*magS + VSMALL)))); 
13    result[globalFaceI++] = cosDDotS;
14 }

```

Listing 167: A detail of the function `faceNonOrthogonality` in the file `cellQuality.C`

21.1.2 Face skewness

OpenFOAM defines skewness in a mesh different than other tools, e.g. Gambit. The reason for this OpenFOAM-specific definition is that this definition is associated with the definition of a skewness error in [38] as part of mesh induced discretisation errors.

Skewness is a property of the faces of the mesh. We need to discriminate between internal faces and boundary faces.

Internal faces

Each internal face connects two cells. Figure 38 shows the cell centres P and N of two adjacent cells. The face face_{PN} is the face connecting these two cells. The point F is the face centre of the face face_{PN} . The line $c = \overline{PN}$ connects the cell centres. This connecting line intersects with the face face_{PN} . This intersection point I divides the line c into the two parts c_1 and c_2 .

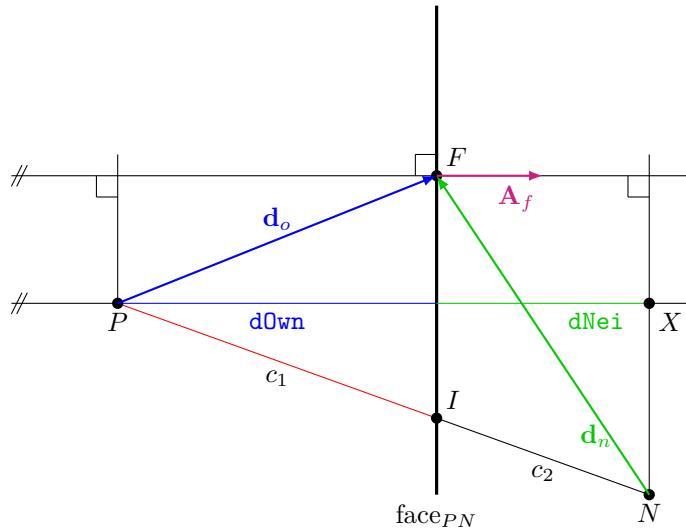


Figure 38: Definition of skewness of internal faces

To calculate the location of I the length of c_1 is of key interest because the skewness is defined in Eq. 21. The location (the vector to) the points P , N and F are easily obtained. From this three vectors \mathbf{d}_o , \mathbf{d}_n and \mathbf{c} is computed. With \mathbf{d}_o and \mathbf{d}_n the inner product with the face area vector \mathbf{A}_f is computed to obtain \mathbf{d}_{Down} and \mathbf{d}_{Nei} ⁸¹.

⁸¹ \mathbf{d}_{Down} and \mathbf{d}_{Nei} are actual variable names. Therefore these symbols are written in typewriter font.

$$\text{skewness} = \frac{|\vec{IF}|}{|\vec{PN}|} \quad (21)$$

$$\mathbf{d}_o = \vec{F} - \vec{P} \quad (22)$$

$$\mathbf{d}_n = \vec{F} - \vec{N} \quad (23)$$

$$\mathbf{c} = \vec{N} - \vec{P} \quad (24)$$

$$d_{\text{Own}} = \frac{\mathbf{d}_o \cdot \mathbf{A}_f}{\|\mathbf{A}_f\|} \quad (25)$$

$$d_{\text{Nei}} = \frac{\mathbf{d}_n \cdot \mathbf{A}_f}{\|\mathbf{A}_f\|} \quad (26)$$

$$\angle(XPN) = \alpha \quad (27)$$

$$\cos(\alpha) = \frac{d_{\text{Own}}}{c_1} = \frac{d_{\text{Own}} + d_{\text{Nei}}}{c_1 + c_2} = \frac{d_{\text{Own}} + d_{\text{Nei}}}{\|\mathbf{c}\|} \quad (28)$$

$$c_1 = \frac{d_{\text{Own}}}{d_{\text{Own}} + d_{\text{Nei}}} \|\mathbf{c}\| \quad (29)$$

$$\vec{I} = \vec{P} + c_1 \mathbf{c} \quad (30)$$

$$\text{skewness} = \frac{\|\vec{F} - \vec{I}\|}{\|\mathbf{c}\|} \quad (31)$$

Note that both \vec{P} and \mathbf{c} are vectors. The reader hopefully excuses this lack of consistency in mathematical notation. \vec{P} denotes the position vector of the point P . In this case the symbol \vec{P} is preferred to \mathbf{P} in order to use symbols that can be found in Figure 38.

Listing 168 shows a detail of the function `faceSkewness` from the file `cellQuality.C`⁸². There a loop over all internal faces is traversed. The loop body contains the calculation of the skewness. First `dOwn` and `dNei` are computed. Then the location of the point I is determined. The variable `faceIntersection` of the type `point` contains the position vector to the point I – the point at which the connection line between the cell centres intersects the face. Finally, the skewness is calculated (compare Eq. 31). Notice the precaution against a possible division by zero (adding `VSMALL` to the denominator).

```

1  forAll(nei, faceI)
2  {
3      scalar dOwn = mag
4      (
5          (faceCtrs[faceI] - cellCtrs[own[faceI]]) & areas[faceI]
6      )/mag(areas[faceI]);
7
8      scalar dNei = mag
9      (
10         (cellCtrs[nei[faceI]] - faceCtrs[faceI]) & areas[faceI]
11     )/mag(areas[faceI]);
12
13     point faceIntersection =
14         cellCtrs[own[faceI]]
15     + (dOwn/(dOwn+dNei))*(cellCtrs[nei[faceI]] - cellCtrs[own[faceI]]);
16
17     result[faceI] =
18         mag(faceCtrs[faceI] - faceIntersection)
19         /(mag(cellCtrs[nei[faceI]] - cellCtrs[own[faceI]]) + VSMALL);
20 }
```

Listing 168: A detail of the function `faceSkewness` in the file `cellQuality.C`

⁸²In the file `cellQuality.C` there are two methods defined: `skewness()` and `faceSkewness()`. Comparing the code of this two methods reveals, that they compute the same thing. However, the method `skewness()` returns the affected cells, whereas `faceSkewness()` returns the affected faces.

Boundary faces

Skewness is also defined and checked for boundary faces. Figure 39 shows the sketch of a boundary face with its face center F_C . The vector \mathbf{d} from the cell center P to the face center F_C is depicted in red. At the point F_C we see the face normal vector \mathbf{n} . If we project the vector \mathbf{d} on the vector \mathbf{n} we gain the face-intersection point F_I . This is the point, where the face normal departing from the cell center intersects with the face. The face-intersection does not necessarily need to be part of the face, as it is the case in Figure 39.

We then compute the vector \mathbf{f} , which is the connection between the points F_I and F_C . The ratio of the magnitudes of the vectors \mathbf{f} and \mathbf{d} defines the skewness of a boundary face.

Listing 169 shows the code that computes the skewness of the boundary faces. The points P and F_C are

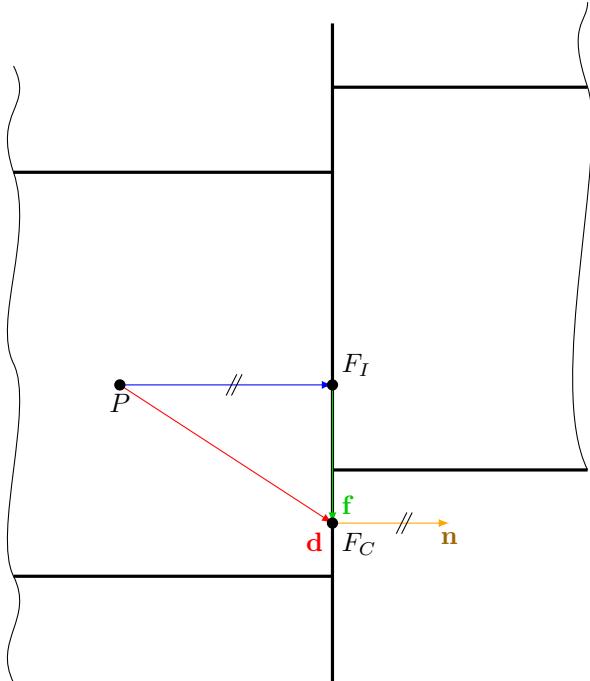


Figure 39: Definition of skewness of boundary faces

returned by the methods `faceCells()` and `faceCentres()`. The normal vector \mathbf{n} is easily computed from the face-area vector given by the method `faceAreas()`.

$$\mathbf{n} = \text{faceAreas}[\text{faceI}] / \text{mag}(\text{faceAreas}[\text{faceI}]) \quad (32)$$

$$\mathbf{d} = \text{faceCentres}[\text{faceI}] - \text{cellCtrs}[\text{faceCells}[\text{faceI}]] \quad (33)$$

$$\vec{F}_I = \text{cellCtrs}[\text{faceCells}[\text{faceI}]] + ((\text{faceCentres}[\text{faceI}] - \text{cellCtrs}[\text{faceCells}[\text{faceI}]]) \& \mathbf{n}) * \mathbf{n} \quad (34)$$

$$\vec{F}_I = \vec{P} + (\mathbf{d} \cdot \mathbf{n}) \mathbf{n} \quad (35)$$

$$\mathbf{f} = \text{faceCentres}[\text{faceI}] - \text{faceIntersection} \quad (36)$$

$$\mathbf{f} = \vec{F}_C - \vec{F}_I \quad (37)$$

```

1  label globalFaceI = mesh_.nInternalFaces();
2
3  forAll(mesh_.boundaryMesh(), patchI)
4  {
5      const labelULList& faceCells =
6          mesh_.boundaryMesh()[patchI].faceCells();
7
8      const vectorField::subField faceCentres =
9          mesh_.boundaryMesh()[patchI].faceCentres();
10     const vectorField::subField faceAreas =
11         mesh_.boundaryMesh()[patchI].faceAreas();

```

```

12
13     forAll(faceCentres, faceI)
14     {
15         vector n = faceAreas[faceI]/mag(faceAreas[faceI]);
16
17         point faceIntersection = cellCtrs[faceCells[faceI]]
18             + ((faceCentres[faceI] - cellCtrs[faceCells[faceI]])&n)*n;
19
20         result[globalFaceI++] = mag(faceCentres[faceI] - faceIntersection)
21         /(
22             mag(faceCentres[faceI] - cellCtrs[faceCells[faceI]])
23             + VSMALL
24         );
25     }
26 }
```

Listing 169: A detail of the function `faceSkewness` in the file `cellQuality.C`

21.1.3 Face concavity

pending

21.1.4 Face warpage

A face is warped, when its vertices do not lie within a plane. Figure 40 shows a simplified situation of a warped face. Any three points, which do not fall onto a single line, span a plane. In Figure 40 the area vector \mathbf{S}_1 of the triangle $\Delta 457$ is parallel to the face area vector \mathbf{S}_f . Thus, we identify point 6 as being out-of-plane.

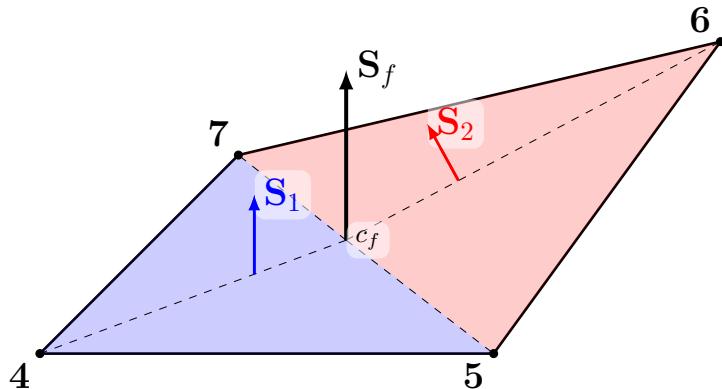


Figure 40: Face warpage

If we decompose the face into individual triangles, we can compare the individual triangle area vectors to the face normal vector. In Figure 40 a crude decomposition is chosen for simplicity. In OpenFOAM's internals, the individual triangles are defined by the face center and two consecutive vertices of the face. As, face vertices need to be stored consecutive, a simple loop over the vertices of a face is sufficient to generate all individual triangles. Thus, in OpenFOAM's implementation of the test for warpage, the face of Figure 40 would be decomposed into four triangles, as indicated by the thin dashed lines.

We bear in mind, that in OpenFOAM a face area vector has two important properties. It is normal to the face's plane and its magnitude is proportional to the face's area⁸³. By diving the face area vector by its magnitude we gain the face normal vector, see (39).

OpenFOAM checks for warpage by computing the inner product of the triangle area vectors with the face normal vector, and summing up the results, see (40). This sum is equal to the magnitude of the face area vector, when all vertices are in-plane. If the two vectors of an inner product are not parallel, then the magnitude of the inner product is smaller by the cosine of the enclosed angle.

⁸³Since a length can not be an area in terms of physical units, we avoid the statement, that the face normal vectors length is the face's area. However, the factor of proportionality is 1.

$$\|\mathbf{a} \cdot \mathbf{b}\| = \|\mathbf{a}\| \|\mathbf{b}\| \cos(\alpha) \quad (38)$$

$$\mathbf{n}_f = \frac{\mathbf{S}_f}{\|\mathbf{S}_f\|} \quad (39)$$

$$S_f \stackrel{?}{=} \sum_i \mathbf{n}_f \cdot \mathbf{S}_i \quad (40)$$

21.1.5 Cell concavity

When a cell is concave

21.2 Pitfalls

The results of *checkMesh* need to be taken with a grain of salt. Therefore, it is helpful to know how *checkMesh* defines the quality measures it tests for (Section 21.1) and also to know about the shortcomings of the tests performed by *checkMesh* (Section 21.2).

The tests performed by *checkMesh* do not necessarily guarantee the mesh to be suitable for simulation. Furthermore, if a mesh fails a test, that does not necessarily mean that it is unsuitable for calculation.

21.2.1 Mesh quality - aspect ratio

checkMesh performs a number of quality checks. However, the user has to be careful. *checkMesh* does only check if a mesh makes a simulation impossible. There are some situations in which *checkMesh* does not issue an error or a warning, however, a mesh can nevertheless be unsuitable for a successful calculation.

The aspect ratio is the ratio of the largest and the smallest dimension of the cells. For the aspect ratio there are no limits. Listing 170 shows the output of *checkMesh* when a mesh with high aspect ratio cells is tested. Although *checkMesh* does not complain, the mesh is not suitable for simulation. Even with extremely small time steps numerical problems appear.

```

Checking geometry...
Overall domain bounding box (0 0 0) (0.1 0.1 0.01)
Mesh (non-empty, non-wedge) directions (1 1 1)
Mesh (non-empty) directions (1 1 1)
Boundary openness (-9.51633e-17 1.17791e-18 -4.51751e-17) OK.
Max cell openness = 1.35525e-16 OK.
Max aspect ratio = 100 OK.
Minimum face area = 2.5e-07. Maximum face area = 2.5e-05. Face area magnitudes OK.
Min volume = 1.25e-09. Max volume = 1.25e-09. Total volume = 0.0001. Cell volumes OK.
Mesh non-orthogonality Max: 0 average: 0
Non-orthogonality check OK.
Face pyramids OK.
Max skewness = 2e-06 OK.
Coupled point location match (average 0) OK.

Mesh OK.

End

```

Listing 170: *checkMesh* output for a mesh with high aspect ratio

21.2.2 Mesh quality - skewness

There are different ways to calculate the skewness of a finite volume cell. To test whether *checkMesh* complains about high skewness, a mesh is distorted by the use of edge grading. Figure 41 shows this mesh. Parallel edges are graded alternately – alternating between the expand ratio and its reciprocal value. Listing 171 shows the grading settings. The test case for this examination is the *cavity* case of *icoFoam*. This case can be found in the tutorials.

```
hex (0 1 2 3 4 5 6 7) (20 20 2) edgeGrading (3 0.33 3 0.33 1 1 1 1 1 1 1)
```

Listing 171: Block definition in *blockMeshDict* to achieve high skewness

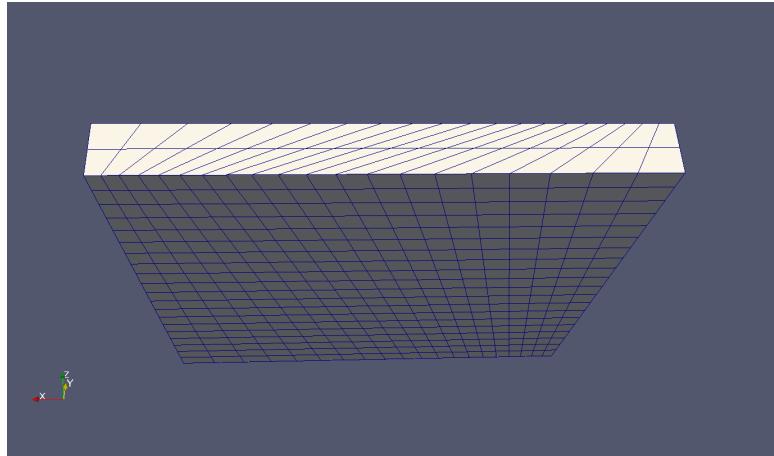


Figure 41: A distorted mesh

checkMesh issues no warnings for the value pair 3 and 0.33. The values 4 and 0.25 cause a warning about *severely non-orthogonal faces*.

However, a simulation is impossible for much lower values. The simulation runs for the value pair 1.33 and 0.75. The values 1.4 and 0.714 cause the simulation to crash. The limits of stability of a simulation are therefore reached earlier than the limits of *checkMesh*.

To conclude this section, the user should bear the following statement in mind. Numerical problems of a simulation may be caused by bad mesh quality. In some cases – like the one presented above – bad mesh quality is the root of the problem, but *checkMesh* issues no warnings. However, the values of the quality characteristics may give a hint. Some manuals of CFD software propose numerical ranges for characteristics like aspect ratio to ensure good quality.

```
Checking geometry...
Overall domain bounding box (0 0 0) (0.1 0.1 0.01)
Mesh (non-empty, non-wedge) directions (1 1 1)
Mesh (non-empty) directions (1 1 1)
Boundary openness (4.23516e-18 9.03502e-18 1.60936e-16) OK.
Max cell openness = 1.67251e-16 OK.
Max aspect ratio = 3.63059 OK.
Minimum face area = 1.42648e-05. Maximum face area = 7.1694e-05. Face area magnitudes OK.
Min volume = 1.03854e-07. Max volume = 1.69673e-07. Total volume = 0.0001. Cell volumes OK

.
Mesh non-orthogonality Max: 69.4798 average: 32.8092      Non-orthogonality check OK.
Face pyramids OK.
Max skewness = 2.35485 OK.
Coupled point location match (average 0) OK.

Mesh OK.
```

End

Listing 172: *checkMesh* output for the distorted mesh; grading ratios 3 and 0.33

```
Checking geometry...
Overall domain bounding box (0 0 0) (0.1 0.1 0.01)
Mesh (non-empty, non-wedge) directions (1 1 1)
Mesh (non-empty) directions (1 1 1)
Boundary openness (4.23516e-18 -6.21157e-18 1.18585e-16) OK.
Max cell openness = 2.37664e-16 OK.
Max aspect ratio = 4.23706 OK.
Minimum face area = 1.23181e-05. Maximum face area = 8.67874e-05. Face area magnitudes OK.
```

```

Min volume = 1.00882e-07. Max volume = 1.84055e-07. Total volume = 0.0001. Cell volumes OK
.
Mesh non-orthogonality Max: 73.1635 average: 36.2131
*Number of severely non-orthogonal faces: 80.
Non-orthogonality check OK.
<<Writing 80 non-orthogonal faces to set nonOrthoFaces
Face pyramids OK.
Max skewness = 2.93978 OK.
Coupled point location match (average 0) OK.

Mesh OK.

End

```

Listing 173: *checkMesh* output for the distorted mesh; grading ratios 4 and 0.25

21.2.3 Possible non-pitfall: `twoInternalFacesCells`

If a mesh for a two-dimensional simulation is created and checked using *checkMesh* with the `-allTopology` option enabled⁸⁴, then *checkMesh* will issue a message like in Listing 174. This message indicates, that there are cells present with only two internal faces. This message can be ignored when 2D meshes are concerned. The corner cells of a rectangular mesh have – by definition – only two internal faces.

```

Checking topology...
Boundary definition OK.
Cell to face addressing OK.
Point usage OK.
Upper triangular ordering OK.
Face vertices OK.
Topological cell zip-up check OK.
Face-face connectivity OK.
<<Writing 4 cells with two non-boundary faces to set twoInternalFacesCells
Number of regions: 1 (OK).

```

Listing 174: *checkMesh* output for a 2D mesh with `-allTopology` option set.

If this message appears when a 3D mesh is examined, then there is probably some error in the definition of the mesh. A cell in a 3D mesh should have at least three internal faces. A message stating the presence of cells with two internal faces in a 3D mesh indicates non-connected regions.

If there are, in a 3D mesh, cells present with only two internal faces – this is sometimes the case with tetrahedral meshes and the tet-cells in corners – then these cells will be written into a `twoInternalFacesCells` cell set, furthermore, these cells will also be written into a cell set named `underdeterminedCells`.

Listing 175 and Figure 42 show such an example. An all-tet, 3D-mesh has been checked by *checkMesh*, and it complained about cells with two internal faces, and underdetermined cells. In both cases the number of affected cells was the same. Comparing the actual cellSets, as shown in Listing 175, revealed that in-fact, all cells with two internal faces are considered under-determined, as the contents of the two files exactly match with the name of the cell set being the only exception.

```

gerhard@gerhardWork:/home/user/OpenFOAM/user-6/case-directory/constant/polyMesh/sets$ diff
    twoInternalFacesCells  underdeterminedCells
14c14
<     object      twoInternalFacesCells;
---
>     object      underdeterminedCells;

```

Listing 175: Comparing the cell sets `twoInternalFacesCells` and `underdeterminedCells` in a case with an all-tet, 3D-mesh.

⁸⁴When the `-allTopology` option is enabled, *checkMesh* performs two additional topological checks. Checking the face connectivity is one of these checks.

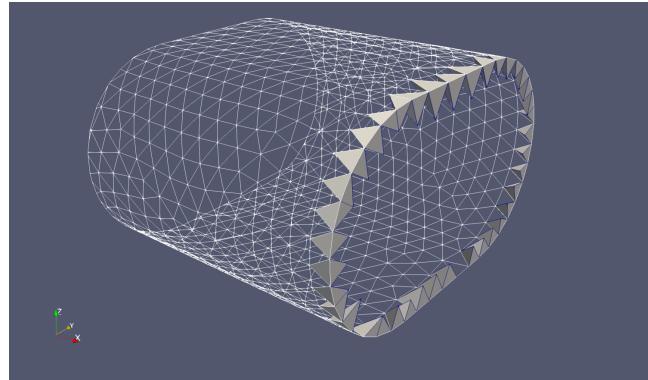


Figure 42: The cells with two internal faces in an all-tet, 3D-mesh.

21.2.4 Non-pitfall: underdetermined cells & aspect ratio

In certain cases, checkMesh reports under-determined cells, which are apparently the result of them having a relatively large aspect ratio, yet these cells pass the test of checkMesh for aspect ratio itself. Here, we discuss an example the author encountered when creating an axi-symmetric mesh. Listing 176 shows the output of checkMesh, which reports one failed test, the test for under-determined cells.

```

Checking geometry...
Overall domain bounding box (-1.87738e-14 -0.3105 -0.00628287) (0.359945 0.28176
0.00628287)
Mesh has 2 geometric (non-empty/wedge) directions (1 1 0)
Mesh has 3 solution (non-empty) directions (1 1 1)
Wedge back with angle 1 degrees
Wedge front with angle 1 degrees
All edges aligned with or perpendicular to non-empty directions.
Boundary openness (2.65459e-17 -2.56868e-15 -3.5724e-14) OK.
Max cell openness = 6.00189e-16 OK.
Max aspect ratio = 273.429 OK.
Minimum face area = 1.70066e-08. Maximum face area = 0.000559933. Face area magnitudes OK
.
Min volume = 9.31147e-12. Max volume = 6.7098e-06. Total volume = 0.000535521. Cell
volumes OK.
Mesh non-orthogonality Max: 35.0627 average: 10.6127
Non-orthogonality check OK.
Face pyramids OK.
Max skewness = 0.997295 OK.
Coupled point location match (average 0) OK.
Face tets OK.
Min/max edge length = 3.44218e-05 0.0349612 OK.
All angles in faces OK.
Face flatness (1 = flat, 0 = butterfly) : min = 1 average = 1
All face flatness OK.
Cell determinant (wellposedness) : minimum: 0.00012646 average: 2.46777
***Cells with small determinant (< 0.001) found, number of cells: 16
<<Writing 16 under-determined cells to set underdeterminedCells
Concave cell check OK.
Face interpolation weight : minimum: 0.289549 average: 0.486008
Face interpolation weight check OK.
Face volume ratio : minimum: 0.328662 average: 0.931884
Face volume ratio check OK.

Failed 1 mesh checks.

End

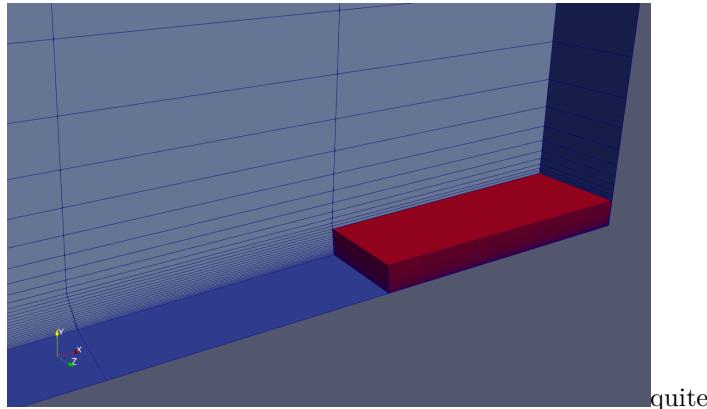
```

Listing 176: *checkMesh* output for a 2D, axi-symmetric mesh with *-allGeometry* and *-allTopology* option set.

In Figure 43, we see the under-determined cells, which were found by checkMesh. From Listing 176, we see that the cells have a high aspect ratio, with the maximum aspect ratio well above 250. However, checkMesh

determined the test for the aspect ratio to be OK, yet *checkMesh* found under-determined cells. However, these cells, depicted in Figure 43 are regular hex cells, although quite thin ones.

As the simulation, this mesh was created for, runs perfectly fine, the reported under-determined cells pose no problem for the numerics of OpenFOAM. Most likely some threshold value was exceeded by these high-aspect ratio cells, which triggered *checkMesh* to report under-determined cells.



quite

Figure 43: The under-determined cells, which were found by *checkMesh* in the mesh of an axi-symmetric simulation. These cells are on a far corner of the 2-D domain, and grading towards the more interesting regions led them to have a high aspect ratio. In fact, these cells have the highest aspect ratio of the whole mesh. The proximity to the lower wall results in these cells to be quite fine in the *y*-direction. Since, these cells are furthest from the axis of symmetry, they are relatively large in radial and tangential direction.

21.3 Useful output

The output of *checkMesh* in Listing 174 also shows another interesting thing to know about *checkMesh*. The line `<Writing 4 cells with two non-boundary faces to set twoInternalFacesCells` tells the user that *checkMesh* created a set of cells that are found to have some problems.

Figure 44 shows the content of the case which resulted in Figure 41. There we see a directory named `sets` inside the `polyMesh` folder. The `sets` folder was created by *checkMesh* and inside this folder *checkMesh* stores any sets it creates. The file names are rather self-explanatory, e.g. the file `skewFaces` contains all faces which failed the test for skewness. All these cell or face sets can be viewed with *paraView*.

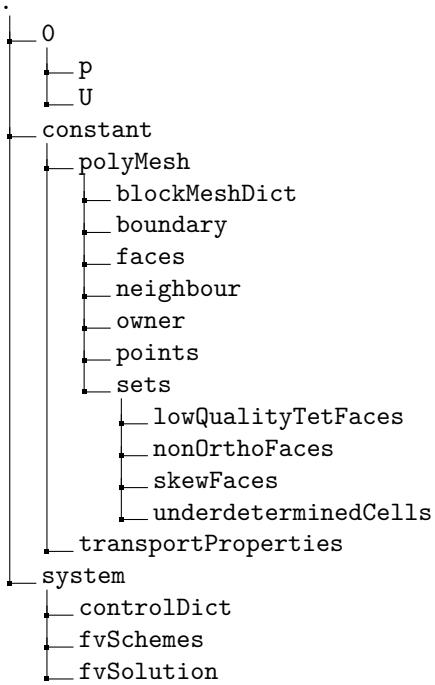


Figure 44: Sets created by *checkMesh* in the **sets** directory.

22 *extrudeMesh*

extrudeMesh is a rather special tool. OpenFOAM lists *extrudeMesh* under the mesh generation tools, however, *extrudeMesh* has a role between mesh generation and mesh manipulation. We can do mesh generation, e.g. extruding one cell layer from a 2D STL surface in order to prepare the mesh for a 2D study in OpenFOAM. However, we can also do mesh manipulation, which is essentially mesh extension, as we “grow” cell layers on surfaces.

22.1 Control

extrudeMesh is controlled by the file `extrudeMeshDict`. This file contains all necessary settings for using this tool, which can roughly be divided into the categories: “where to grow”, “what to grow”, and “how to grow”.

22.1.1 `constructFrom`

The `constructFrom` setting is used to determine the source of the extrusion. This basis for cell extrusion can be either a patch of an existing mesh or an STL surface. In the case of a patch of a mesh, the source may also be a patch from another case, e.g. extrude patch X from case Y to create the mesh of case Z.

For the case of an STL surface, the corresponding STL file needs to be provided using the `surface` keyword. If we use the patch of a mesh, we can choose between retaining the source mesh or discarding it. Figure 45 shows the difference between these two options, when extruding a patch from the current case.

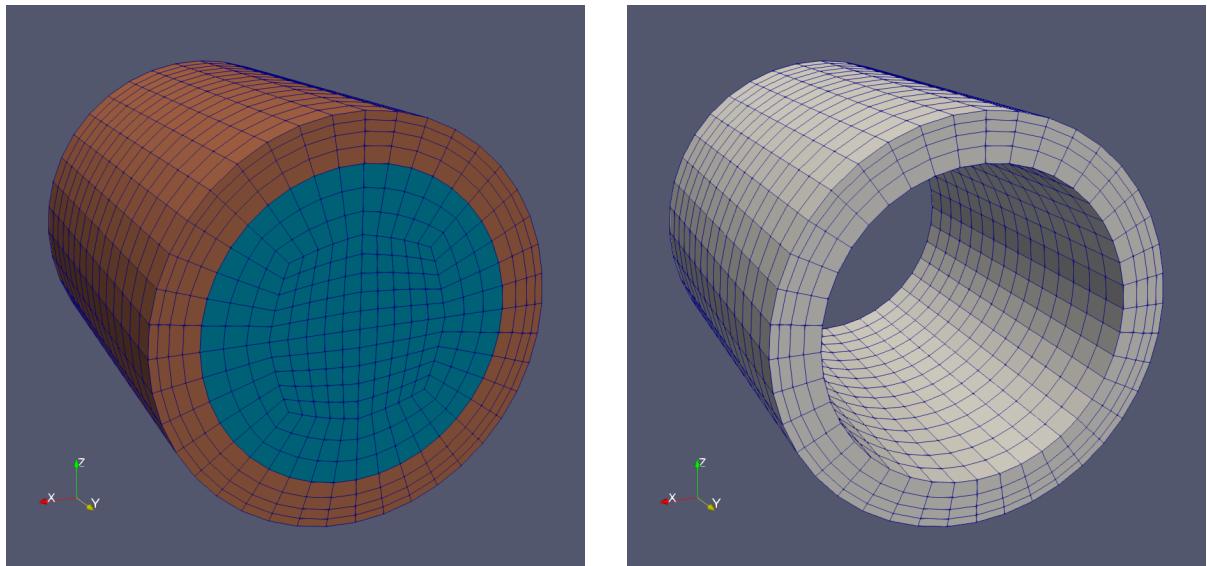


Figure 45: Extrude the wall patch from a cylinder mesh. left: `constructFrom mesh`. right: `constructFrom patch`.

22.1.2 Layer control

The “what to grow” part consists of the number of cells in thickness direction of the new cell layer, the thickness and an optional expansion ratio.

`expansionRatio`

Note, that the expansion ratio describes the expansion of thickness from one layer to the other. This is in contrast to the expansion ratio we use with the grading feature of `blockMesh`, there the expansion ratio describes the thickness ratio between the smallest and the largest cells at the boundaries of a block.

22.1.3 Extrusion models

The extrusion models control the “how to grow”. There is a number of models available, some of which will be discussed below.

Plane extrusion

The plane extrusion model is specifically for the creation of (quasi) 2D meshes. A single layer of cells is extruded in normal direction to the provided surface. By default the front and back patches are created to be of type `empty`.

In Figure 46 we see the mesh created from an STL, which was created by GMSH. In this case we could also have used GMSH to create a mesh with a single cell in thickness direction.

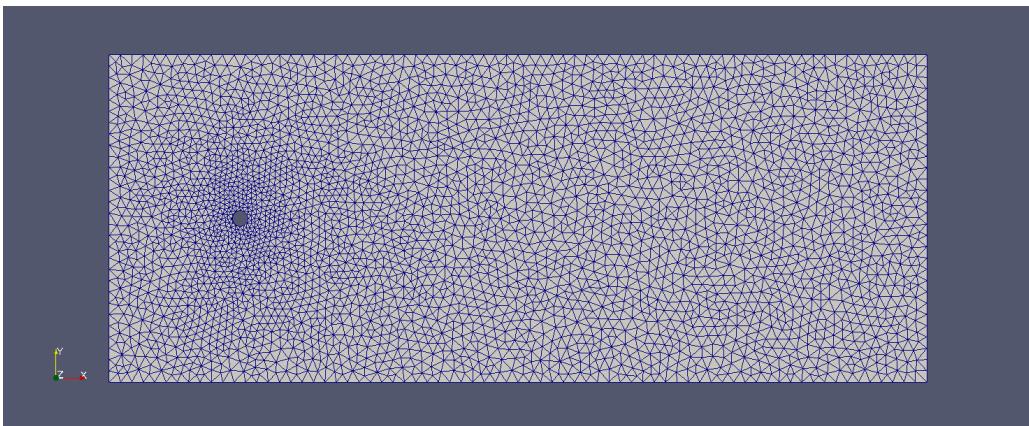


Figure 46: The mesh for a 2D study generated from an STL surface.

Sector extrusion

Figure 47 shows the result of the `sector` extrusion model. For this model, the user needs to specify a point in space (`axisPnt`), an axis of rotation (`axis`) and an `angle`. In this case the outlet patch of the original mesh (shown in grey) was extruded. The original mesh was created by `blockMesh` and consists of 5 blocks (easily scripted with e.g. Python). The `axisPnt` lies in the plane of the outlet patch, however, the point is well outside the patch. The distance between the `axisPnt` and the centerline of the original pipe mesh determines the radius of the pipe bend. The positive x-axis was selected as `axis`. The newly generated cells are by default added to a `cellSet` named `addedCells`.

This use of `extrudeMesh` opens a rather cheap way to create good meshes of pipe bends. The `blockMeshDict` for a straight pipe is easily scripted, and by extruding along the section of a circle, the mesh is continued along a bend. Directly scripting the `blockMeshDict` for a pipe bend would definitely be a little bit harder.

The `sector` extrusion model also has a 2D “cousin”, which is called `wedge`. The class underlying the `wedge` extrusion model is derived from the `sector` model. However, the `wedge` model is the axisymmetric analogue of the `plane` model. Thus, only one cell layer is created, which is centered about the source surface, i.e. the cell layer is extruded half the `angle` in both directions from the source surface.

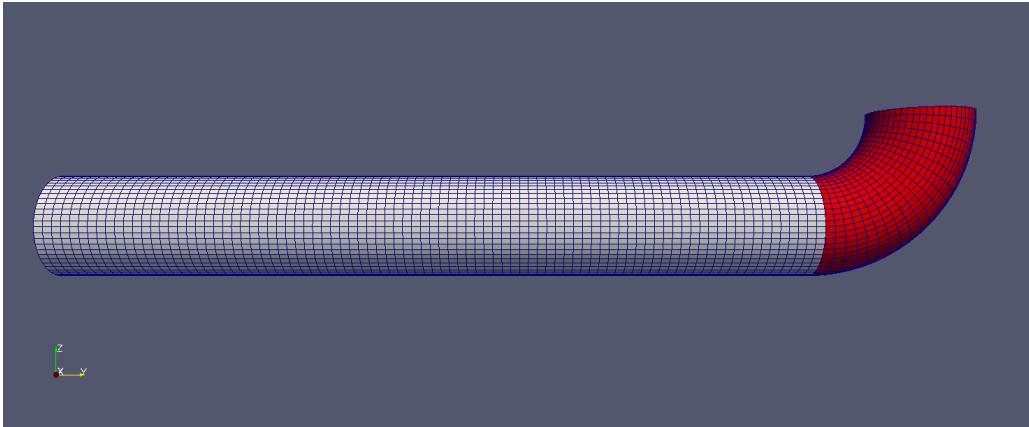


Figure 47: A cheap 90° pipe bend. The outlet patch of the original mesh was extruded along the sector of a circle.

Linear extrusion

There are two models for linear extrusion in `extrudeMesh`. There is `linearNormal`, which extrudes in normal direction of the underlying surface. This can be used to grow a cell layer on the pipe's wall, see Figure 49. Furthermore, there is `linearDirection`, which extrudes cells along a specified direction.

In Figure 48 we see the result of subsequent use of `extrudeMesh`. Unfortunately, at the time of writing (using OpenFOAM-4.0), `extrudeMesh` does not offer the `-dict` option. Thus, we need to repeatedly edit the `extrudeMeshDict` for subsequent applications of `extrudeMesh`. First, a bend was created by using the `sector` model. Afterwards a straight pipe section was created using `linearNormal`, which is followed by a slanted pipe section, which was created using `linearDirection`.

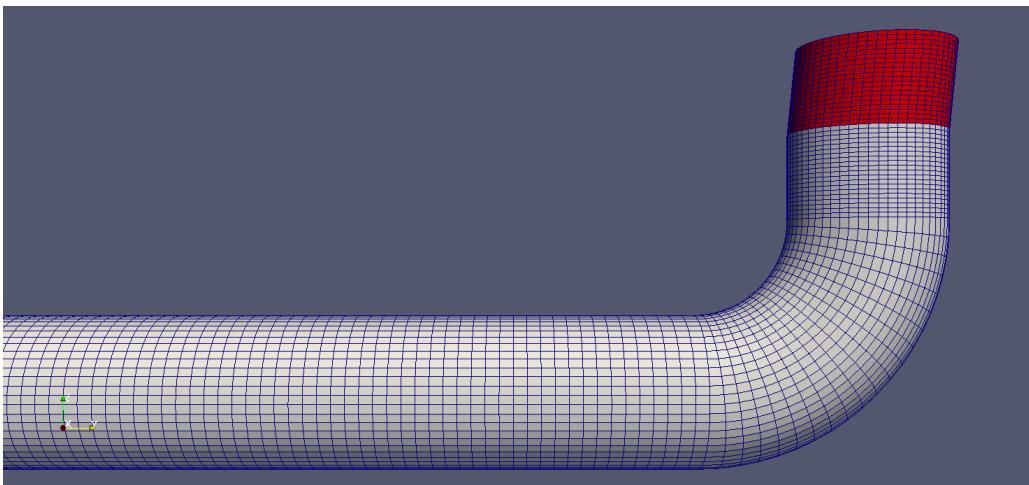


Figure 48: Subsequent mesh extrusions: `sector`, `linearNormal` and `linearDirection`.

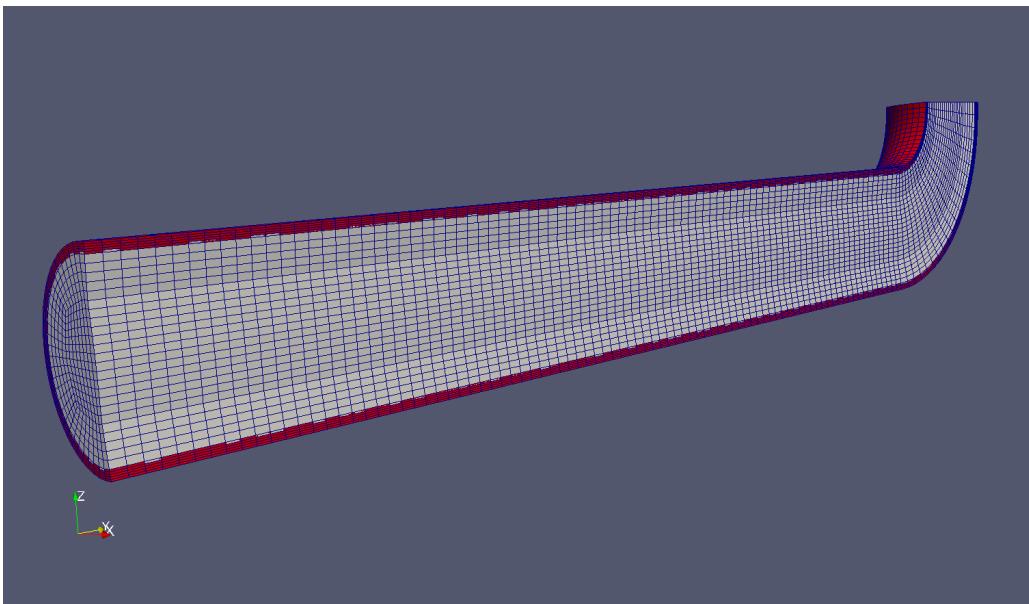


Figure 49: Grow a wall! The *walls* patch of the pipe mesh was extruded using the `linearNormal` model.

22.2 Extruding 2-D meshes

We can use `extrudeMesh` also to create two-dimensional meshes, either from a STL surface mesh or an existing OpenFOAM mesh.

22.2.1 `extrudeMesh` + `snappyHexMesh` = `snappy2D`

While `snappyHexMesh` is a fully three-dimensional meshing tool, we can create snappy-like meshes for two dimensions with the help of `extrudeMesh`. Figure 50 shows an example of such a mesh. The work flow for the mesh shown is pretty straight forward and is not discussed any further.

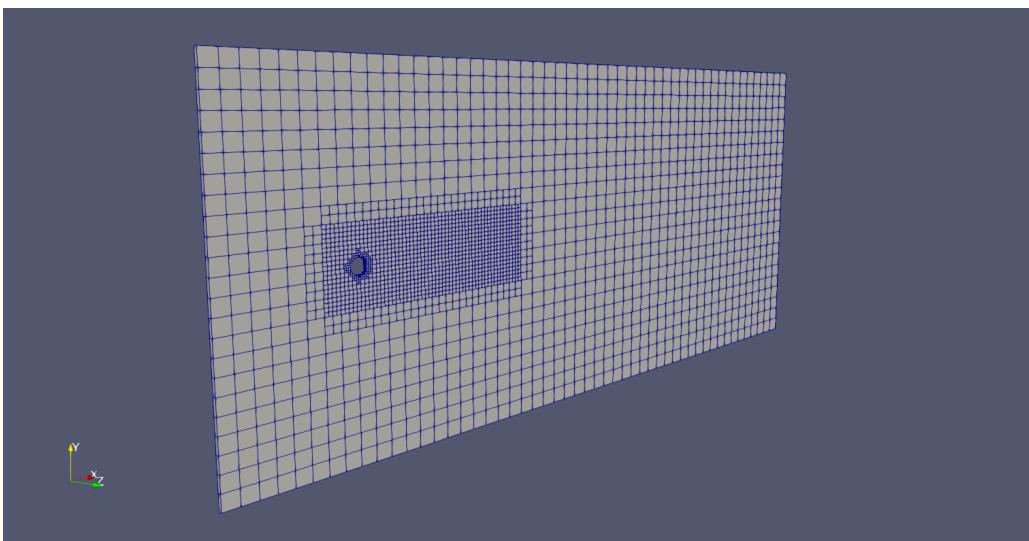


Figure 50: Snappy two-dimensional meshing. The side patch of a snappy mesh was extruded using the `linearNormal` model, with the base mesh being discarded. Thus, we remain with a snappy-like mesh for the two-dimensional flow around a cylinder.

22.2.2 Pitfall: extruding a too narrow 2D slice

The mesh for an axi-symmetric simulation is a slice of the full 3D domain, which is 1 cell in circumferential direction. Figure 51 shows two examples, which differ only in the angle of the slice. Both seem like valid meshes, when viewed in ParaView.

Yet, with the narrow angle, OpenFOAM complains of the wedge-type patches being non-planar. Listing 177 shows an example of such a warning message. Increasing the angle from 1 to 5 degrees solved this problem. This problem could not be solved by increasing the write precision to large values.

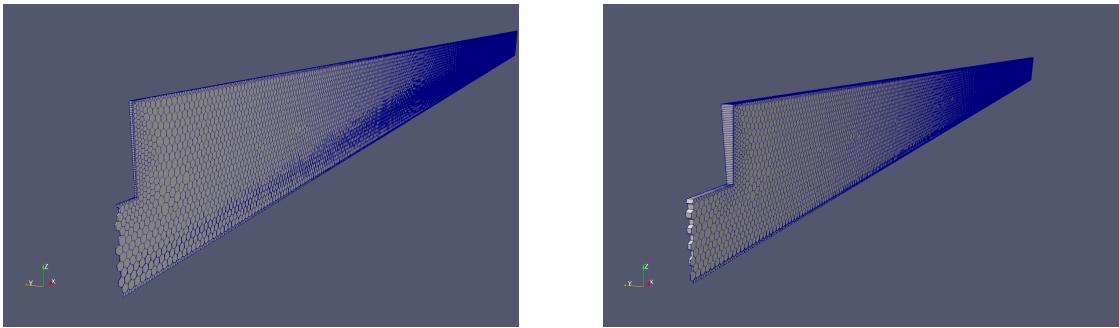


Figure 51: Extruding a slice. **Left:** a 1 degree sector extrusion, **Right:** a 5 degrees sector extrusion.

```
--> FOAM Warning :
  From function virtual void Foam::wedgePolyPatch::calcGeometry(Foam::PstreamBuffers&
  in file meshes/polyMesh/polyPatches/constraint/wedge/wedgePolyPatch.C at line 70
  Wedge patch 'front' is not planar.
At local face at (5.433932e-05 -4.157483e-07 4.764003e-05) the normal (5.662783e-19 -0.9999619
-0.008726535)
differs from the average normal (-1.335286e-10 -0.9999618 -0.008682201) by 1.965596e-09
Either correct the patch or split it into planar parts
```

Listing 177: Warning message about a non-planar wedge-type patch.

22.2.3 Pitfall: remnant faces

Figure 52 shows a case, which caused the author some trouble-shooting. A 2-D slice of a hollow sphere was the intended result. Thus, we extruded a patch from an imported mesh. The base patch, which is not visible in the image, was used for extrusion. The red and green patches in Figure 52 were also present in the base mesh, all other surfaces of the base mesh were subsumed automatically by OpenFOAM as a default patch.

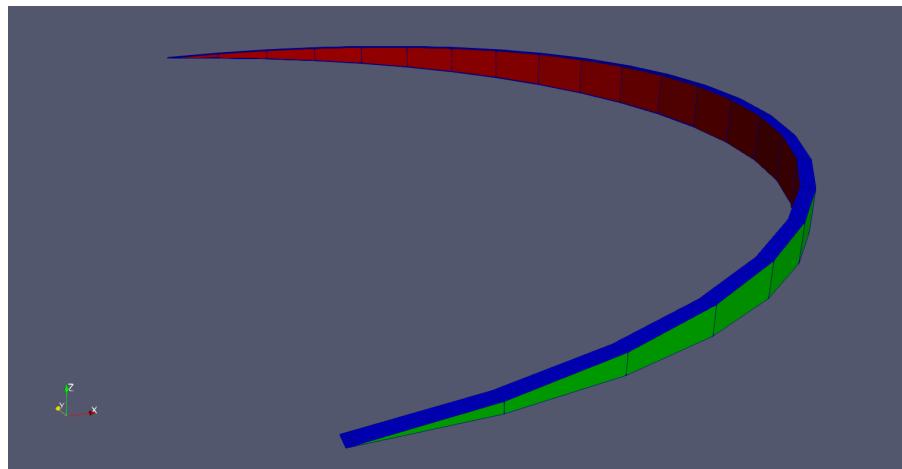


Figure 52: Extruding the mesh for a 2-D slice of a hollow sphere.

After extruding the mesh, OpenFOAM was reporting a non-planar patch: the default patch. As it happened, `extrudeMesh` also created zero-length faces at the axis of symmetry. A run of `collapseEdges` fixed the issue. If we compare the stats of `checkMesh` shown in Listing 178, we can clearly see that something was not right after mesh extrusion, i.e. at `Time = constant`. However, at `Time = 0.005`, i.e. after the execution of `collapseEdges`, the mesh's stats look much more reasonable.

```

Time = constant

Mesh stats
  points:          288
  faces:           488
  internal faces: 202
  cells:            115
  faces per cell:  6
  boundary patches: 4

Overall number of cells of each type:
  hexahedra:      115

Checking patch topology for multiply connected surfaces...
Patch          Faces    Points   Surface topology
  faceBubble     115      144      ok (non-closed singly connected)
  bubbleInnerSurf 23       48      ok (non-closed singly connected)
  bubbleOuterSurface 23       48      ok (non-closed singly connected)
  defaultPatches 125      156      ok (non-closed singly connected)

Checking geometry...
  <<Writing 288 points on non-aligned edges to set nonAlignedEdges
  ***Zero or negative face area detected. Minimum area: 0
  <<Writing 4 zero area faces to set zeroAreaFaces
  ***Max skewness = 661.5314, 4 highly skew faces detected which may impair the quality of the
      results
  <<Writing 4 skew faces to set skewFaces

Failed 3 mesh checks.
  Above: after calling extrudeMesh; Below: after calling collapseEdges
Time = 0.005

Mesh stats
  points:          276
  faces:           478
  internal faces: 202
  cells:            115
  faces per cell:  5.913
  boundary patches: 4

Overall number of cells of each type:
  hexahedra:      105
  prisms:          10

Checking patch topology for multiply connected surfaces...
Patch          Faces    Points   Surface topology
  faceBubble     115      144      ok (non-closed singly connected)
  bubbleInnerSurf 23       46      ok (non-closed singly connected)
  bubbleOuterSurface 23       46      ok (non-closed singly connected)
  defaultPatches 115      144      ok (non-closed singly connected)

Checking geometry...
  <<Writing 276 points on non-aligned edges to set nonAlignedEdges
  Minimum face area = 1.1657e-07. Maximum face area = 2.9696e-05. Face area magnitudes OK.
  Max skewness = 0.33015 OK.

Failed 1 mesh checks.

```

Listing 178: The most relevant lines of `checkMesh`'s output, before and after executing `collapseEdges`.

A clear indicator of the problem encountered is the number of cell types. This mesh of a 2-D slice should not contain only hexahedra, since at the axis the cells should be prisms. This is the case after fixing the problem. Further indication of the problem can be found in the numerous warnings about zero-area faces. Note the

reduced number of points and faces before and after calling `collapseEdges`, this is a further indication that faces due to zero-length edges have been removed.

The removed zero-area faces were perpendicular to the blue patch shown in Figure 52. Since these zero-area faces would have been part of the blue patch of Figure 52, OpenFOAM was rightly complaining of this patch not being planar.

22.2.4 Pitfall: remnant patches

When we create axi-symmetric meshes by extruding a patch from a source mesh, we may end up with an empty patch, i.e. a patch with zero faces. Figure 53 shows how we can create an axi-symmetric mesh from a regular mesh. In this case, the resulting mesh after extrusion may contain the patch *axis* with zero faces. While this is no problem in itself, having a patch present requires us to specify boundary conditions. Thus, it is good practice to remove all patches with zero faces. How this can be done is discussed in Section 30.8.1.

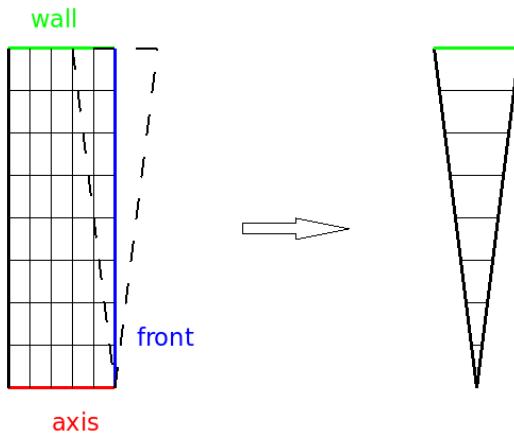


Figure 53: Creating an axi-symmetric mesh by extruding a patch (the patch *front* shown in blue).

22.3 Extruding 3-D meshes

22.3.1 Extruding boundary layers

In theory, we could use `extrudeMesh` to create a boundary layer at the wall. However, this only works well in special cases.

Segmented pipe bend

Here, we created a segmented pipe bend using `blockMesh`. The resulting mesh has no boundary layer, hence we tried to achieve this using `extrudeMesh`.

Figure 54 shows two examples of extruding a boundary layer mesh. On the left, we used the standard `linearNormal` extrusion model `linearNormal`, which has issues with the inner corners. On the right, we see the result of the extrusion model `offsetSurface`, which fares better in the inner corners.

However, both extrusion models extrude strictly in the normal direction, which leads to a slight mis-alignment of cells near the segment joints.

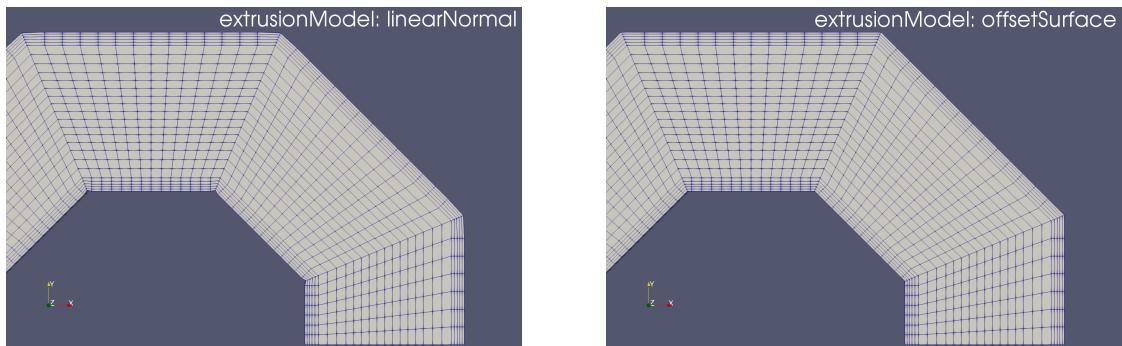


Figure 54: Extruding a boundary layer for a segmented pipe bend. **Left:** using the extrusion model *linearNormal*, **Right:** using the extrusion model *offsetSurface*, which is available in the ESI release since 2016.

Segmented pipe fork

Figure 55 shows another example of problems when trying to create a boundary layer by extrusion. In this case, a pipe fork or tee has been created, and the wall patch was extruded using the *linearNormal* extrusion model. In the 90 degree corner of the tee, the extruded cells even intersect each other.

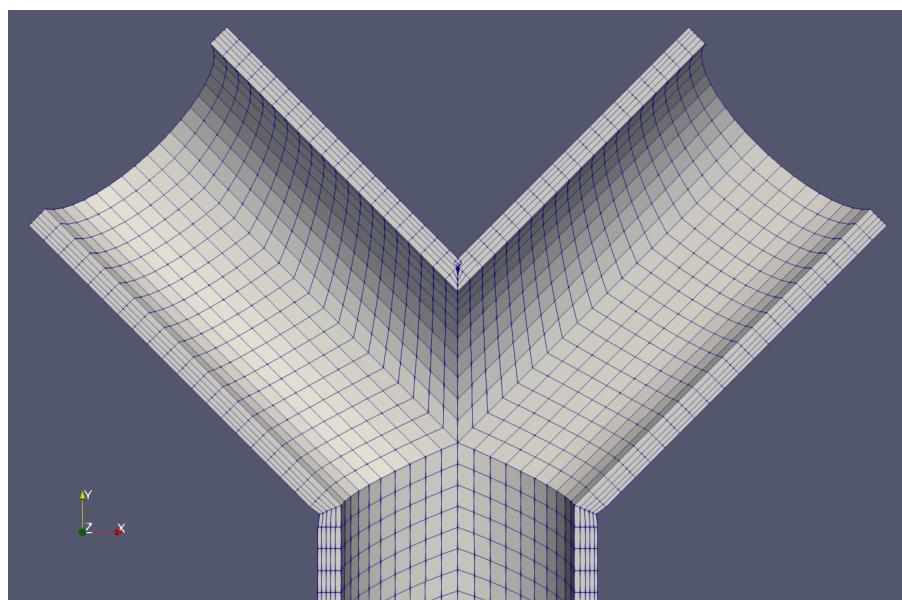


Figure 55: Problematic extrusion in the corners of a pipe fork or tee.

23 polyDualMesh

This tool falls into a similar category as `extrudeMesh`. While it operates on an existing mesh, the result is very different from the initial mesh, so that this tool can be considered a mesh generation tool.

`polyDualMesh` takes any valid mesh and computes the dual of the provided mesh. As the dual of a mesh is a rather abstract concept, this is best explained by a simple example. In Figure 56, the Voronoi diagram is shown. In this example the centers of the circumcircles of a triangular grid are used to create the Voronoi diagram. Thus, a polygonal grid can be created from a triangular grid.

`polyDualMesh` applies this approach to the provided mesh, which can be of any type.

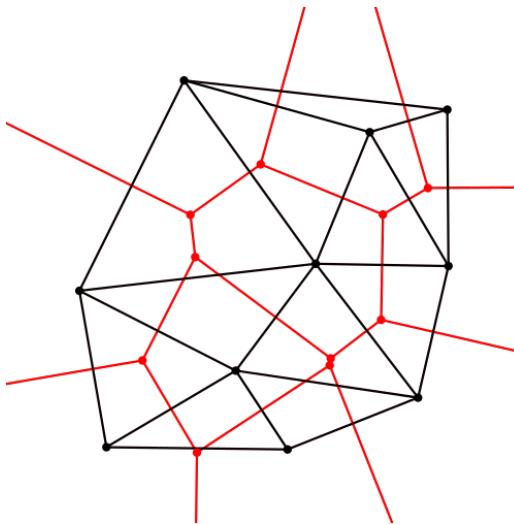


Figure 56: Connecting the centers of the circumcircles produces the Voronoi diagram (in red). Source https://commons.wikimedia.org/wiki/File:Delaunay_Voronoi.svg.

`polyDualMesh` is a vital tool to create polyhedral meshes. Since it takes tetrahedral (tet) meshes as its input, and tools to create tet meshes are plenty, `polyDualMesh` is our gateway to running simulations on polyhedral meshes. Generally we can state, that the more elaborate meshes are to be, the rarer (in case of open source solutions) or the costlier (in case of proprietary tools) the mesh generation software is.

23.1 Examples

23.1.1 Example: the elbow tutorial

Figure 57 shows the result of running `polyDualMesh` on the *elbow* tutorial case. The initial mesh is a triangular mesh, and the resulting mesh is a mesh of polygons. Note, that OpenFOAM implements a 2D mesh as a 3D with a thickness of a single cell. Since `polyDualMesh` acts in all spatial dimensions, the resulting mesh is not a valid 2D mesh anymore. However, if we extrude the top patch as a single cell layer, and delete all old cells, we end up with a valid 2D mesh again.

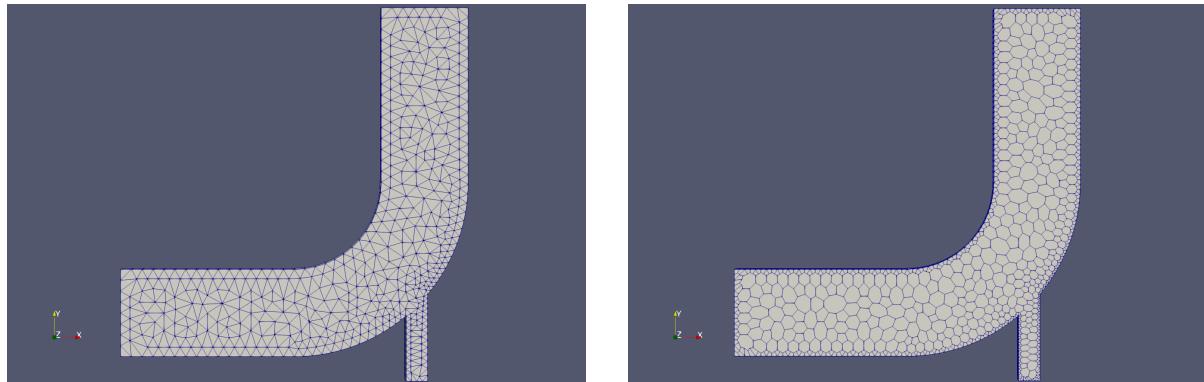


Figure 57: The mesh of the *elbow* tutorial case; before and after the application of `polyDualMesh`.

23.1.2 Example: 2D bubble column tutorial

`polyDualMesh` can take any valid mesh as its input. In Figure 58, on the right, we see the result of applying `polyDualMesh` on a 2D all-hex mesh. This example also shows how the resulting mesh is not a valid 2D mesh anymore, since the resulting mesh is 2 cells in thickness. The resulting mesh is hexahedral-dominant, since at the boundary polyhedrals are created, which resemble hexahedrals with intermediate hanging nodes.

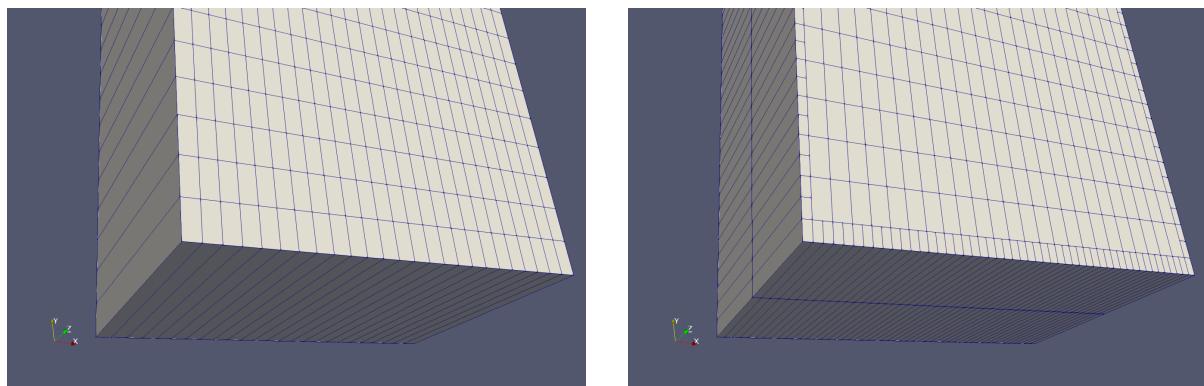


Figure 58: The mesh of the *bubble column* tutorial case; before and after the application of `polyDualMesh`.

23.1.3 Example: single cells

For curiosity's sake, we take the dual mesh of individual cells.

In Figure 59 we see the result of creating the dual mesh of an initial mesh consisting of a single tetrahedral cell. We see from the face decomposition, that the face-centroids are used as vertices for the new cells of the dual mesh. In addition with the volume-centroid, new cells can be constructed. As there are no cells to recombine the newly created cells, we end up with 4 hex-cells.

In Figure 60 we see the dual mesh of a mesh consisting of a single hexahedral cell. Here, we end up with 8 hex-cells.

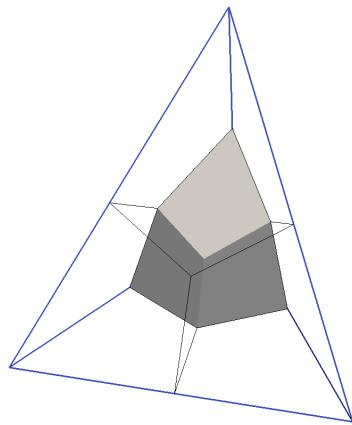


Figure 59: The dual mesh of a single tetrahedron: the original tet-cell is outlined in blue, the face-decomposition is outlined in black, and one of the resulting cells is shown in grey.

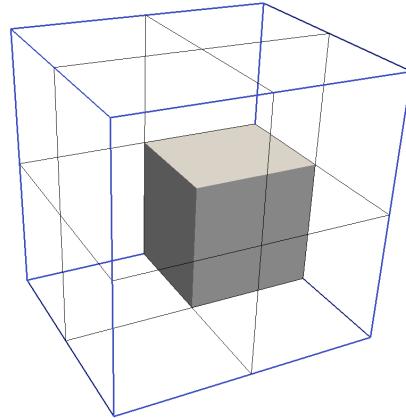


Figure 60: The dual mesh of a single hexahedron: the original hex-cell is outlined in blue, the face-decomposition is outlined in black, and one of the resulting cells is shown in grey.

23.2 Pitfalls

23.2.1 Pitfall: polyDualMesh vs. wall layers

Convex edges

`polyDualMesh` works reasonably well at convex edges. However, at sharp corners the cells directly at the edge are not perfect.

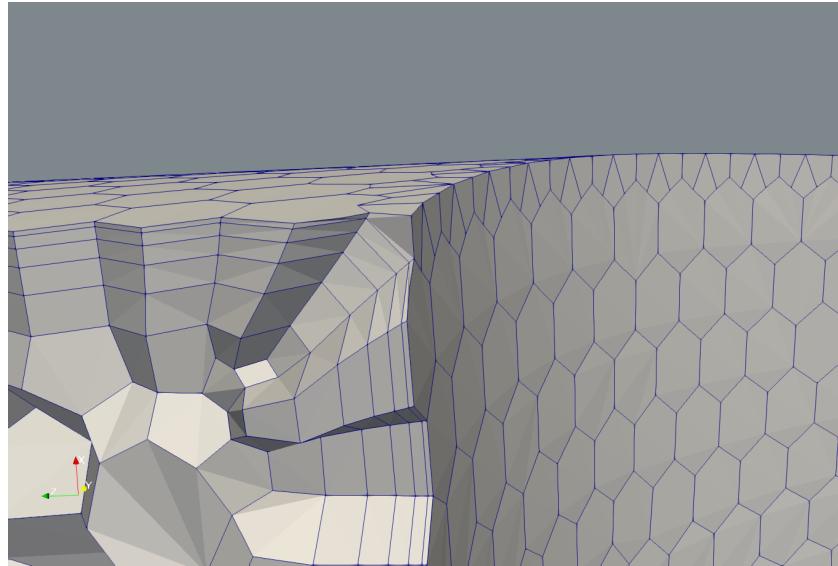


Figure 61: A detailed view of the dual mesh at a convex edge. The cells at the edge are not ideal, however, they are not as problematic as cells at a concave edge.

Concave edges

`polyDualMesh` yields problematic results when the initial mesh features wall layers and concave edges. Figure 62 shows a before-and-after comparison. Here, we created a tet-mesh with wall layers in Salome and then applied `polyDualMesh` on the imported mesh. While the overall result seems quite good, at the concave edge, the mesh has serious issues. Figure 63 shows this in more detail.

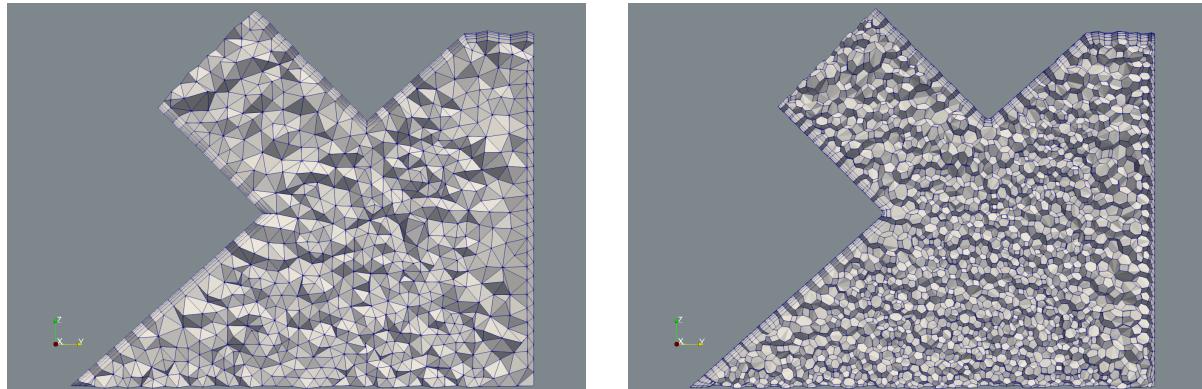


Figure 62: A tet-mesh with wall layers created with Salome. Left: the initial mesh. Right: the dual mesh.

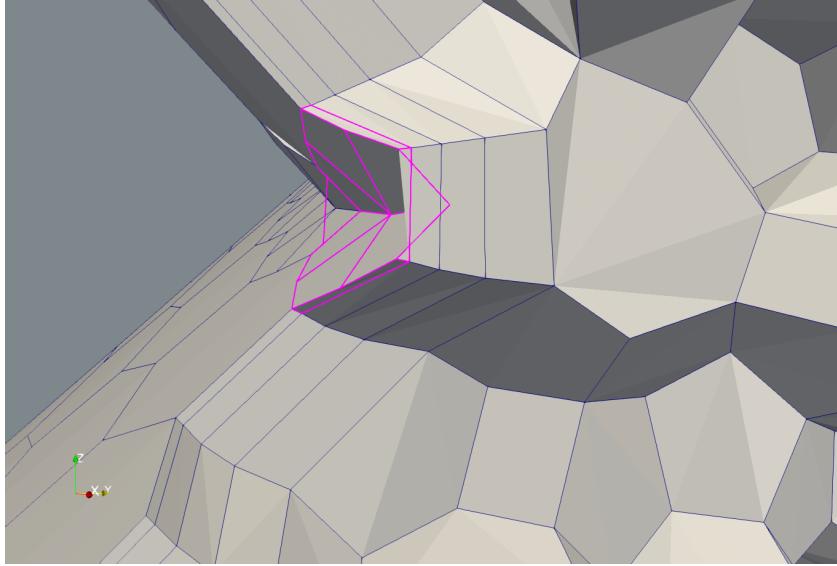


Figure 63: A detailed view of the dual mesh at a concave edge. The highlighted cell is seriously twisted.

Section 31.2 discusses a method which can generate polyhedral meshes with boundary layers even when concave edges are present. The trick is to alter the sequence of mesh generation steps. In this case discussed here, tet-mesh and boundary layer creation prior to the creation of the dual-mesh does not lead to success.

23.2.2 Pitfall: shrinkage

When we create the dual-mesh with polyDualMesh, we may experience some geometric shrinkage. Figure 64 illustrates this point using a triangular mesh in black which follows a grey curved boundary. The dual-mesh, shown in red, is computed from the original mesh in black. While the nodes, i.e., the corners of the triangles, of the original mesh perfectly match the grey boundary, the edges of the triangles do not by virtue of discretization of a curve with linear segments.

Hence, when we compute the dual-mesh of the triangular mesh, the only geometric information available to the dual-mesh mesh-generator is the triangular mesh. Thus, the new boundary nodes of the dual-mesh respect the boundary of the initial mesh. Thus, the discretization error inbetween the boundary nodes of the initial mesh determines the geometric error of the boundary nodes of the dual-mesh.

One way to mitigate this issue, would be to perform a mesh movement step to move the boundary nodes of the dual-mesh to coincide with the actual geometric boundary, i.e., the grey curve.

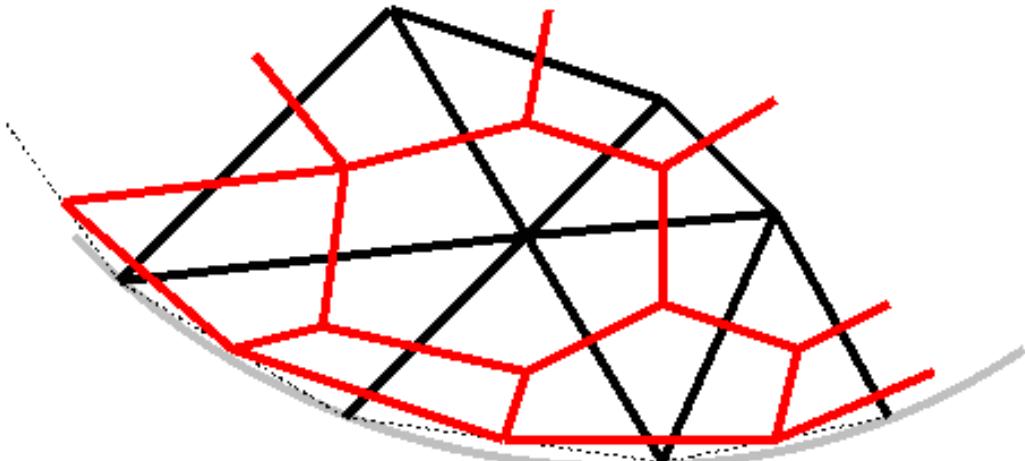


Figure 64: A detailed view of the dual mesh at a concave edge. The highlighted cell is seriously twisted.

Another way to mitigate this error is to ensure a sufficiently fine discretization of the triangular mesh at curved boundaries.

23.2.3 Pitfall: cell sets and cell zones

`polyDualMesh` does not operate on respectively conserve cell sets and/or cell zones. Thus, if you need sets or zones in place, create them after the conversion to polyhedral cells.

24 combinePatchFaces

This mesh manipulation tool checks for multiple patch faces on same cell and combines them. Having multiple patch faces on the same cell might be result of some mesh manipulation operations, e.g. polyDualMesh in the example of the elbow tutorial created such cells at the domain boundary.

Example: the elbow tutorial

In Figure 57, on the right, we see the dual mesh of the elbow tutorial case. It appears as if at the boundary the cells were a lot smaller than within the domain. However, at close inspection, we see that the cells at the boundary have multiple faces belonging to the same patch. Thus, if we run `combinePatchFaces`, all of these multiple patch faces are combined, as we see in Figure 65 on the right. Now the cells at the boundary do not appear to be much smaller than the cells in the interior.

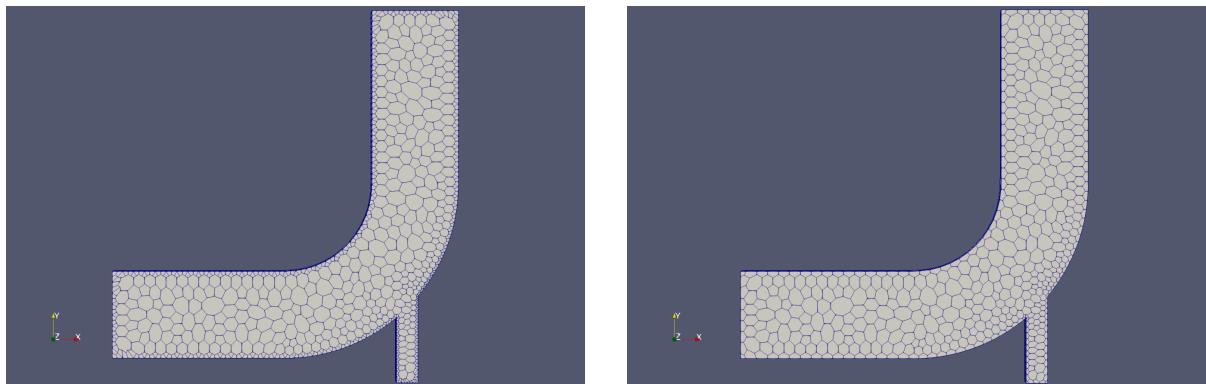


Figure 65: The dual mesh of the *elbow* tutorial case; before and after the application of `combinePatchFaces`.

25 mergeMeshes

`mergeMeshes` is a tool to combine two meshes into one mesh. While `mergeMeshes` combines two meshes, the resulting mesh is not connected. Thus, we need to use `stitchMesh` to connect the two mesh regions into a single, connected mesh. However, we may not need to do this, if we aim to create a mesh for a CHT case. Then, we are perfectly fine with multiple unconnected mesh regions.

25.1 sets vs. zones

`mergeMeshes` carries over the zones of the constituent meshes, but not the sets. While this is important to know, it does not represent any limitation since we can convert sets to zones and vice versa.

26 Salome

The Salome platform is a powerful multitool, which features a meshing module. This meshing module offers a number of meshing tools.

26.1 Export & Conversion

Meshes can be exported by Salome into several formats. The go-to procedure for OpenFOAM-use is to export the mesh in the UNV format and use the `ideasUnvToFoam` mesh converter.

26.1.1 Salome's native UNV export

However, there is an issue when using the UNV format. Apparently, see Figure 66, Salome's mesh export tool for the UNV format does not export pyramid cells.

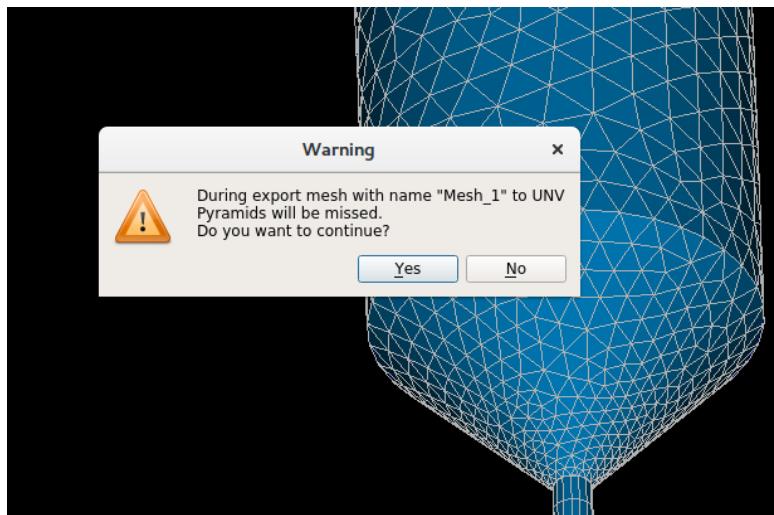


Figure 66: Mesh export issue in Salome with the UNV format.

Apart from pyramid cells, there is also an issue when the mesh contains edge-groups. While Salome is perfectly happy to export a mesh containing groups of edges, the converter for making this mesh usable for OpenFOAM is happy to import groups of edges. This is discussed in Section 29.2.2.

26.1.2 salomeToOpenFOAM

A third-party Python script⁸⁵ can be used to export a mesh containing pyramid cells to OpenFOAM. This script directly writes the essential files⁸⁶. In order to export a mesh, simply select it in the Object Browser of Salome and then execute the `salomeToOpenFOAM.py` Python script. This can be done by using `File > Load Script` menu.

26.1.3 Pitfall: Check your patches/patch types

In Salome we are able to define patches by creating face groups. These face groups are translated to patches, when exporting the mesh. However, Salome has no way to distinguish between general patches and wall patches. Thus, you may want to check `constant/polyMesh/boundary` for the patch types.

With Salome's native export to UNV function, all patches are equal. After importing with OpenFOAM's native `ideasUnvToFoam` converter all patches are of the type `patch`. You need to take care yourself, to assign the type `wall` to wall patches⁸⁷. This can be done manually or with the tool `changeDictionary`. See Section 34.1 for more information on `changeDictionary` and an example of how to change the patch type.

⁸⁵<https://github.com/nicolasedh/salomeToOpenFOAM>

⁸⁶The files `boundary`, `faces`, `neighbour`, `owner` and `points` in `constant/polyMesh`.

⁸⁷If this has not been done, the wall functions of turbulent simulations will complain about patch/data types.

The third party conversion script `salomeToOpenFOAM.py` makes all patches wall patches, when their names contain the word `wall`.

```
1 if "wall" in gname.lower():
2     fileBoundary.write("wall;\n")
3 else:
4     fileBoundary.write("patch;\n")
```

Listing 179: Determining the patch type in `salomeToOpenFOAM.py`.

26.1.4 Export all mesh groups from Salome Python-script

The standard export features of Salome might sometimes fail to fit our needs. However, since Salome is powered in the background by Python, this allows us full access to a very powerful tool: Python scripting.

In Listing 180, we see an example of these opportunities, a script to export all mesh groups of a mesh into their own UNV files. This can be quite handy when we create the geometry for a multi-region case with Salome.

```
1 # Export all mesh groups of a mesh into individual files
2 #   Exporting a mesh including all mesh groups is nice, however,
3 #   exporting them individually into their own files is quite labourious.
4 #
5 # It is supposed that a mesh exists, along with mesh groups containing
6 # mesh elements is selected in the activated Mesh module
7 #
8 # Usage:
9 #   Create a mesh in SMESH module
10 #   Create mesh groups
11 #   Select the mesh and run this script, e.g. File -> Load Script
12 #   Copy and rename the exported files from /tmp/ to where you need it
13 #
14 # Written by Gerhard Holzinger
15 #   March 31. 2020
16 #
17 # Known to work:
18 #   Salome 9.4 & OpenFOAM-7
19
20
21 import salome, SMESH
22 from salome.gui import helper
23
24 segMeshSO = helper.getSoObjectSelected()[0]
25 if not segMeshSO:
26     raise RuntimeError("Select a mesh!")
27
28 segMesh = segMeshSO.GetObject()
29 if not segMesh:
30     meshComp = salome.myStudy.FindObjectByPath("/Mesh").GetObject()
31     if not meshComp:
32         raise RuntimeError("Activate Mesh module!")
33     else:
34         raise RuntimeError("Select a mesh!")
35
36 if not hasattr( segMesh, "GetGroups" ):
37     raise RuntimeError("Select a mesh!")
38
39 mesh = segMesh.GetMesh()
40 meshName = segMeshSO.GetName()
41
42 # loop over all mesh groups
43 for group in segMesh.GetGroups():
44     curGroupName = group.GetName()
45
46     outGroupName = meshName+'_'+curGroupName
47
48     fileName = '/tmp/'+outGroupName+'.unv'
49
50     mesh.ExportPartToUNV(group, fileName)
51 # end for
```

Listing 180: `exportMeshGroupsUNV.py`: a powerful Python script to export all mesh groups into their separate UNV files.

26.2 Combined operations: `blockMesh` & `salome`

26.2.1 Motivation

Figure 67 shows a simulation domain with a comparatively small geometric feature. If we were to create a `blockMesh`-mesh for this geometry we end up with plenty of rather useless fine cells next to that fine feature, as can be seen in Figure 68. Note that in Figure 68 we even can not make out individual cells, or even the cut-out slot in the center.

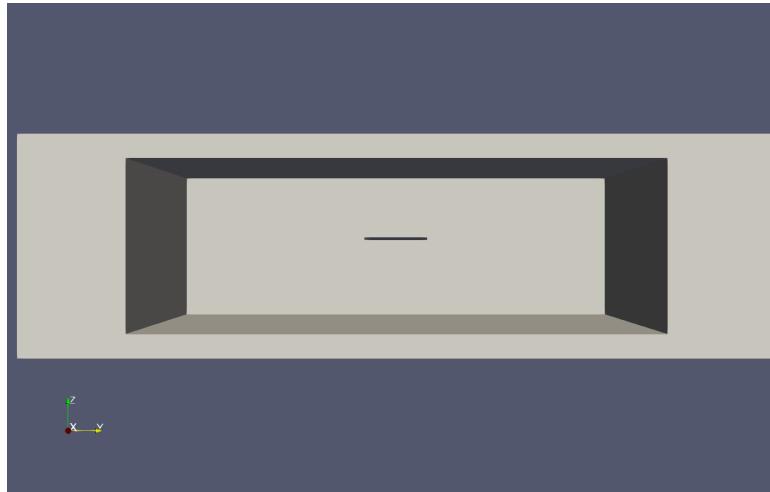


Figure 67: A big simulation domain with a quite small geometric feature: the geometry.

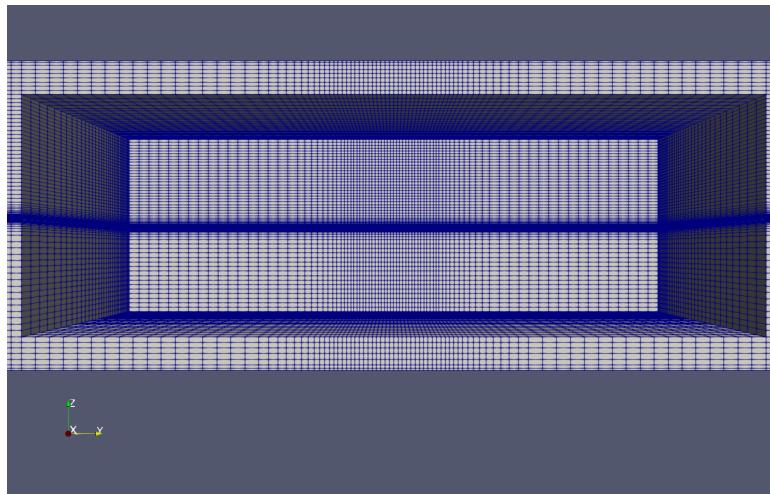


Figure 68: A big simulation domain with a quite small geometric feature: the *blockMesh*-only mesh.

26.2.2 Workflow

An alternative to an outcome as shown in Figure 68, we could choose to create a bigger central block which encompasses the cut-out slot, instead of representing the cut-out. This cut-out block will remain a part of the mesh, and then we will split the mesh into the cut-out block and the remaining mesh.

Then, we create a geometry representation of the cut-out block with the cut-out slot in Salome. When, we mesh the cut-out block, we follow this workflow.

1. Create groups on the geometry: the sides, the front face and the inner edges
2. Import the surface mesh from the meshed cut-out block, as shown in Figure 69
3. Mesh the geometry with the following sub-meshes, preferably in this order
 - (a) The sides with the “Import 1D-2D Elements from Another Mesh” algorithm
 - (b) The inner edges with a suitable 1D algorithm
 - (c) The front face with a suitable 2D algorithm
 - (d) The geometry with the “Extrusion 3D” algorithm

Figure 70 shows the mesh, which we created in Salome.

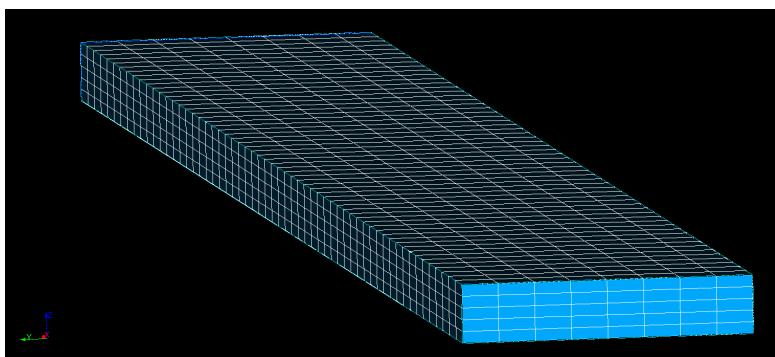


Figure 69: The mesh of the cut-out block in salome.

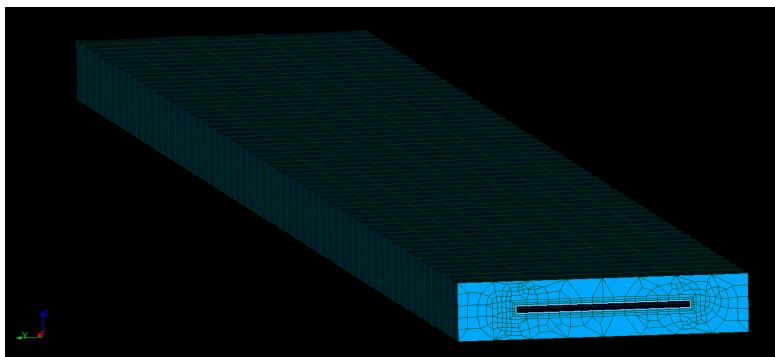


Figure 70: Meshing of a block in salome.

Finally, we need to export our mesh from Salome into OpenFOAM, and combine it with the mesh of the remaining domain. Figure 71 shows the result of our procedure. Thus, we are able to create a relatively fine mesh around the fine geometric feature, without the mesh fine-ness spreading out along the principal directions as in the example shown in Figure 68.

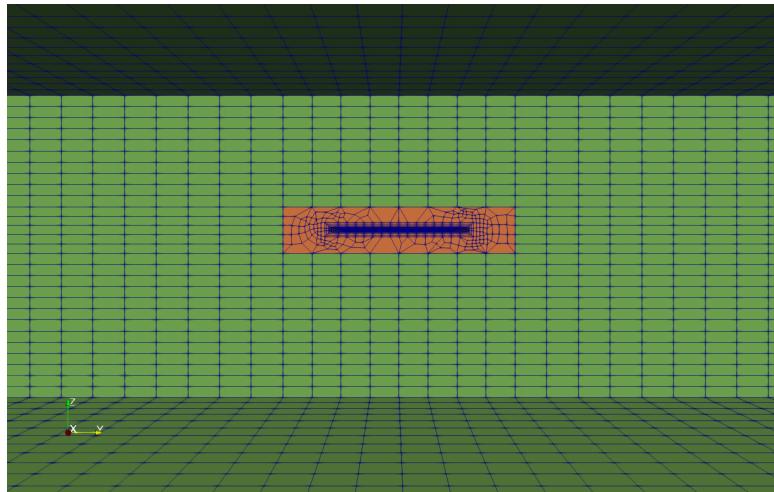


Figure 71: Combining blockMesh and salome: the meshed block was re-combined with the initial mesh.

26.3 Meshing tips for Salome

26.3.1 Bottom-up mesh creation

Salome is quite well suited for creating meshes in a bottom-up procedure. However, proper care needs to be taken with respect to the order in which sub-meshes are created. Proper mesh creation in a bottom-up approach entails a two-stage work-flow: first, define all necessary and useful groups and sub-shapes in the Geometry module, and subsequently create the appropriate sub-meshes and meshes in the Mesh module.

On complex geometries, this two-stage work-flow might be followed several times in a sort of loop, especially if a particular geometry is quite complex or if one is rather new to the process. If you find your geometry lacking certain groups or shapes to enable a more convenient mesh creation, going back to the geometry module and creating the missing features is time well spent in most of the cases.

Pitfall: order of mesh creation

Even though Salome tries to create sub-meshes in the appropriate order, sometimes it might be necessary to manually create all the sub-meshes in the intended order. Especially in situation when we import a surface mesh from another mesh and subsequently create a volume mesh. This is especially the case, when we use a wide variety of meshing algorithms, e.g., importing surface meshes, meshing using Netgen in complex regions and meshing using extrusion in more simple regions.

Figure 72 shows an example of a rather complex geometry for which we use a mixed meshing work-flow. The two coils are meshed by using an extrusion technique, which is quite simple. The fluid domain, on the other hand, is meshed using a mix of free tet-generation and extrusion combined with the importing of the surface mesh from the two coils. This is an example for which Salome's automatic sequence of sub-mesh generation does not work for the author⁸⁸.

⁸⁸As a rule of thumb, this may as well be simply a case of user error. The author is in no way sufficiently expert enough to claim that this is the fault of Salome.

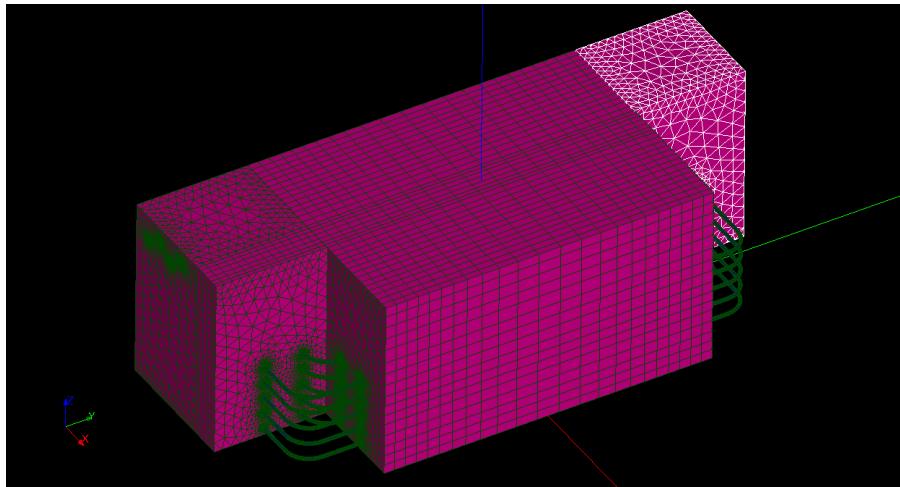


Figure 72: A complex geometry warranting a complex meshing work-flow. Two pipe coils represent a heat-exchanger in a box-shaped vessel.

26.3.2 Extrusion3D with guidance

Mesh extrusion is a powerful tool for mesh generation, which is not only beneficial for pipes or other prismatic bodies, it also allows us to create all-hex or hex-dominant meshes using Salome. Figure 73 shows the geometry of a pipe which has been created by extruding a face.

We want to create a mesh for this geometry as well as the interior of the pipe, which is not shown in the picture. Our method of choice for mesh-creation is extrusion as well. We begin with the body for the pipe's interior. First, we create a mesh for the cross-sectional face and a discretisation of the pipe's axis. Extrusion3D yields a perfectly serviceable mesh.

Next, we want to create a mesh for the pipe's walls, i.e., the geometry shown in Figure 73. In order to achieve matching meshes, we first import the surface-mesh of the pipe's interior and use it as the sub-mesh for the interior-surface of our geometry. Then, we create a mesh for the cross-sectional area. Finally, we create a volume-mesh by running Extrusion3D with no further parameters or settings other than the two sub-meshes, i.e.; interior surface and cross-section. The resulting mesh is shown in Figure 74 on the left. This resulting mesh poses some problems.

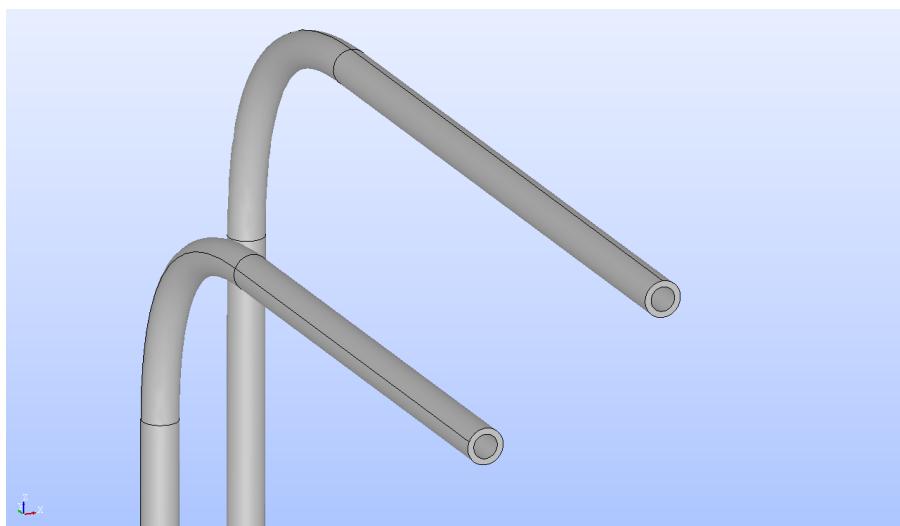


Figure 73: The geometry of a pipe, both ends of a single coil are visible. The geometry was created by extruding a face along a path.

While we may think that everything has been settled for Extrusion3D by providing a mesh for the cross-

section and a mesh for the pipe's interior surface, the meshing algorithm disagrees. While we may have fixed the axial discretisation on the interior surface, the exterior surface is without constraints. Hence, the meshing algorithm chose a different discretisation.

While this only leads to slight visual displeasure in the example shown on the left of Figure 74, this may as well lead to serious errors .

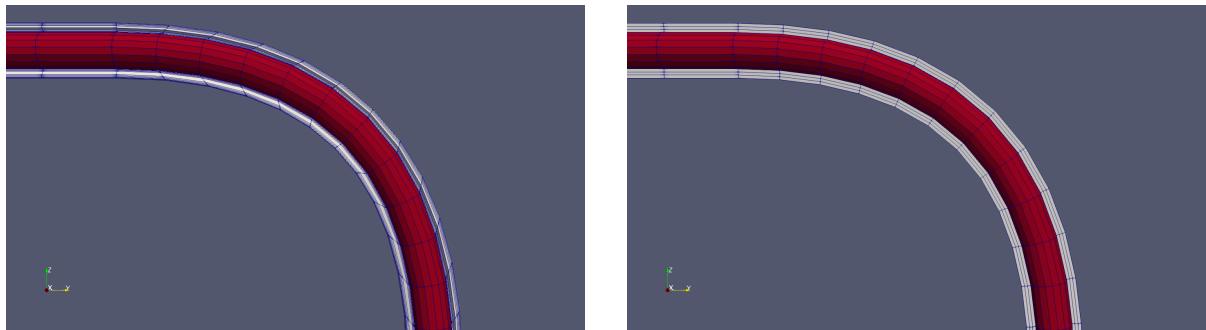


Figure 74: Left: insufficiently guided extrusion. Right: extrusion with proper guidance.

Figure 75 shows an example of a serious meshing error due to insufficient guidance. The strongly misaligned axial discretisation leads to some cells having a negative volume, i.e., the cells are distorted to such a degree that they are turned at least partially inside-out.

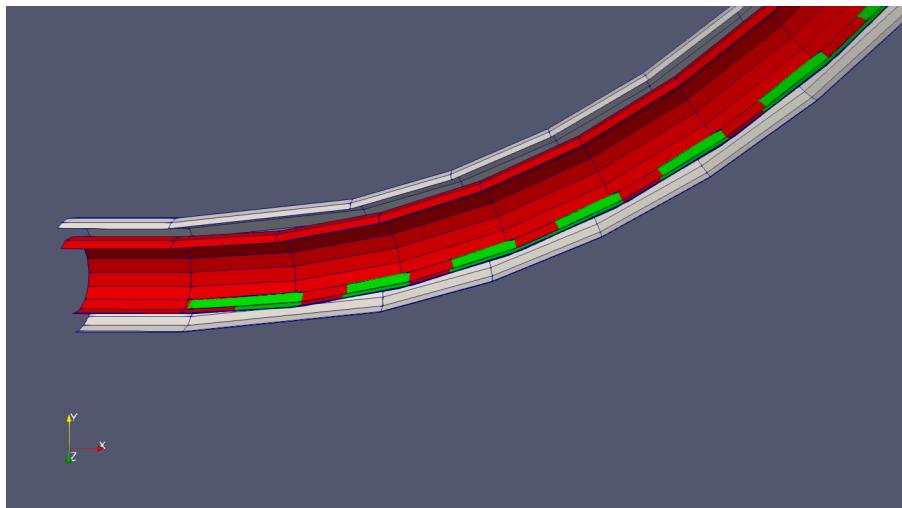


Figure 75: Extrusion gone bad: the inner and outer surface of the pipe, shown in grey and red. Cells with negative volume are shown in green. Note the vertices on the inner and the outer surfaces.

We can avoid these meshing problems when using Extrusion3D, if we specify the axial discretisation also on the outside of the pipe. Hence, by enforcing the use of the same discretisation on the outside as well as on the inside of the pipe, we create an error-free and visually pleasing mesh as shown in Figure 74 on the right.

Note, that in order to use the same axial discretisation on the outside of the pipe, the axial discretisation should be specified in terms of *Number of Segments* rather than *Local Length*. Since the length of an axial edge along the pipe's outside is larger than the length of an axial edge on the inside, using *Local Length* for discretisation might lead to different numbers of element in axial direction for the inside and the outside, which causes Extrusion3D to fail.

26.3.3 Scripted mesh creation

Bottom-up meshing approaches can involve many steps and may even necessitate a specific order in which these steps need to be processed. While such an approach may be cumbersome to set up, playing around with mesh

parameters might be even more cumbersome.

However, since Salome can be controlled using Python scripts, once a work-flow has been worked out, it is advantageous to translate this workflow into a Python script. With such a script, we can then adjust individual parameters, execute the script to create the entire mesh and then check the results.

In Listing 181 contains a snippet of the mesh creation script for the geometry shown in Figure 72. The mesh of the fluid domain depends on several other meshes. First, the surface meshes of the coils are imported, hence *innerCoilSurface* and *outerCoilSurface* being the first sub-meshes to be created.

One of the next sub-meshes (*bottomInOutCorner*) imports a surface mesh from another mesh (*MeshBottomInOutCorner*). Thus, the mesh *MeshBottomInOutCorner* is created before everything else.

Another sub-mesh (*bottomFrontCorner*) depends in a similar manner from another mesh (*MeshBottomFrontCorner*), which in turn depends on the mesh of the main fluid domain. Hence, the processing chain of events is split, and the mesh *Mesh_bottomFrontCorner* is created at the appropriate place in the succession of the sub-meshes of the main fluid domain, i.e., right between the sub-meshes *frontMiddle* and *bottomFrontCorner*.

While the discussion of the script in Listing 181 seems quite academic without the proper reference to the underlying geometry and mesh definitions, we can nevertheless observe how a bottom-up meshing approach with specific inter-dependencies can be translated into a script.

Since scripting saves us from the effort of clicking (a lot), time invested in setting up such scripts is generally well spent.

```

1 import salome
2 import SMESH
3 from salome.smesh import smeshBuilder
4
5 mySubShapeSequence1 = list()
6 mySubShapeSequence1.append('innerCoilSurface')
7 mySubShapeSequence1.append('outerCoilSurface')
8 mySubShapeSequence1.append('bottomInOutCorner')
9 mySubShapeSequence1.append('inOutCorner')
10 mySubShapeSequence1.append('frontMiddle')
11
12 mySubShapeSequence2 = list()
13 mySubShapeSequence2.append('bottomFrontCorner')
14 mySubShapeSequence2.append('frontCorner')
15
16 myMesh_ref = salome.myStudy.FindObjectByPath("/Mesh/FluidDomain").GetObject()
17 smesh = smeshBuilder.New()
18 myMesh = smesh.Mesh(myMesh_ref) myMesh.Clear()
19 subMeshes = myMesh_ref.GetSubMeshes()
20
21 corner01Mesh_ref = salome.myStudy.FindObjectByPath("/Mesh/MeshBottomInOutCorner").GetObject()
22 corner01Mesh = smesh.Mesh(corner01Mesh_ref)
23 corner01Mesh.Clear() corner01Mesh.Compute()
24
25 for shapeName in mySubShapeSequence1:
26     for curSubMesh in subMeshes:
27         if curSubMesh.GetSubShape().GetName() == shapeName:
28             print('Processing ' + curSubMesh.GetSubShape().GetName())
29             curSubShape = curSubMesh.GetSubShape()
30             mySubMesh = myMesh_ref.GetSubMesh(curSubShape, curSubShape.GetName())
31             mySubMesh.Compute()
32
33         break
34
35 corner02Mesh_ref = salome.myStudy.FindObjectByPath("/Mesh/MeshBottomFrontCorner").GetObject()
36 corner02Mesh = smesh.Mesh(corner02Mesh_ref)
37 corner02Mesh.Clear()
38 corner02Mesh.Compute()
39
40 for shapeName in mySubShapeSequence2:
41     for curSubMesh in subMeshes:
42         if curSubMesh.GetSubShape().GetName() == shapeName:
43             print('Processing ' + curSubMesh.GetSubShape().GetName())
44             curSubShape = curSubMesh.GetSubShape()
45             mySubMesh = myMesh_ref.GetSubMesh(curSubShape, curSubShape.GetName())
46             mySubMesh.Compute()
47
48         break

```

Listing 181: Creating a bottom-up approach mesh using a Python script.

26.4 Tips & Tricks

26.4.1 Dealing with unconnected regions after meshing a compound solid

The problem

Salome is a very flexible and useful mesh generation tool, however, sometimes we run into issues when we want to use meshes created by Salome with OpenFOAM. Note, that the problem we are solving in this section can probably be avoided by taking certain measures within Salome, however, that would mean doing most if not all of the mesh generation in Salome all over again. So, at times, dealing with the problem on the side of OpenFOAM might be more time-efficient.

When we create a mesh using compound solids, we might end up on the Salome-side with a mesh that is perfectly fine, however, after the export/import operations, OpenFOAM might report. Listing 182 shows the output of `checkMesh` which reports unconnected regions and the presence of a patch named `defaultFaces`.

Unconnected regions can be avoided by ensuring on the Salome-side, that we only have a single solid, which might be partitioned. However, by using a compound solid, we end up with unconnected regions on the OpenFOAM-side. The complexity of the geometry might dictate the use of a compound solid, so we need to deal with this using OpenFOAM's onboard tools.

The presence of a patch named `defaultFaces` indicates, that there are boundaries of the geometry which have not been part of the face-groups in Salome. This does not indicate a problem per se, we simply might have forgotten to define face-groups for all the boundaries. However, in our case, there is a surface between the constituting solids of our compound solid. And this surface results in the patch named `defaultFaces`.

```
Checking topology...
Boundary definition OK.
Cell to face addressing OK.
Point usage OK.
Upper triangular ordering OK.
Face vertices OK.
*Number of regions: 2
The mesh has multiple regions which are not connected by any face.
<<Writing region information to "constant/cellToRegion"
<<Writing region 0 with 229500 cells to cellSet region0
<<Writing region 1 with 41760 cells to cellSet region1

Checking patch topology for multiply connected surfaces...
Patch          Faces    Points   Surface topology
pipeWall        5760     5796    ok (non-closed singly connected)
ringWall        3132     3132    ok (closed singly connected)
inlet           1809     1864    ok (non-closed singly connected)
outlet          1809     1864    ok (non-closed singly connected)
defaultFaces    11520    11592   ok (non-closed singly connected)
```

Listing 182: The most relevant lines of `checkMesh`'s output showing the problem of unconnected regions.

Figure 76 shows a schematic representation of our problem. The two solids constituting the compound solid in Salome resulted in two regions, which are separated by the patch `defaultFaces` (shown in green in Figure 76). The patches `inlet` and `outlet` span both regions. The walls are of no further interest here.

The meshing strategy we used in Salome ensured that all the faces of the patch `defaultFaces` pointing in one direction have a co-inciding face pointing in the other direction. The face normals, which by definition point to the outside, are also shown schematically in Figure 76.

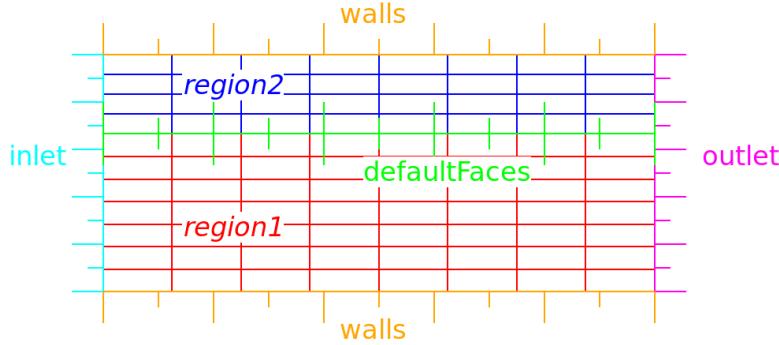


Figure 76: A schematic representation of a mesh with two unconnected regions resulting from meshing a compound solid in Salome.

The work-around

We can fix this issue by first splitting the mesh into proper mesh regions using `splitMeshRegions`. Figure 77 shows the resulting sub-folders containing the meshes of the mesh-regions.

```
user@host:~/OpenFOAM/user-9/run/meshing/unconnectedRegions$ tree constant
constant
├── region1
│   └── polyMesh
│       ├── boundary
│       ├── faces
│       ├── neighbour
│       ├── owner
│       └── points
└── region2
    └── polyMesh
        ├── boundary
        ├── faces
        ├── neighbour
        ├── owner
        └── points
```

Figure 77: The directory structure of the meshes of the mesh-regions after splitting. Note that the original mesh has already been deleted, hence there is no `polyMesh` folder directly in the `constant` folder.

Now that we have separate meshes, we can then rearrange these meshes in preparation for using `mergeMeshes`. `mergeMeshes` expects a master-case to work on, and an add-case to take the to-be-added mesh from.

Thus, we replace the original mesh with the mesh of one mesh-region, and create the add-case from the other mesh-region. Figure 78 shows the directory structure prior to the merging of the meshes. The `polyMesh` directories have been marked by colours in Figures 77 and 78 to highlight the necessary case manipulation.

```

user@host:~/OpenFOAM/user-9/run/meshing/unconnectedRegions$ tree constant addCase
constant
└── polyMesh
    ├── boundary
    ├── faces
    ├── neighbour
    └── owner
        └── points
addCase
├── constant
│   └── polyMesh
│       ├── boundary
│       ├── faces
│       ├── neighbour
│       └── owner
└── system

```

Figure 78: The directory structure prior to the merging of the meshes.

Another necessary step prior to merging the meshes is to rename the patch named `defaultFaces` in one of the meshes. After renaming the patch in one of the meshes, we execute `mergeMeshes`. This, again, produces a single mesh with two unconnected regions. However, now there are two patches delimiting the two regions. Hence, we can now use `stitchMesh` to stitch the two mesh-regions using the two newly created patches.

```

Checking topology...
Boundary definition OK.
Cell to face addressing OK.
Point usage OK.
Upper triangular ordering OK.
Face vertices OK.
*Number of regions: 2
The mesh has multiple regions which are not connected by any face.
<<Writing region information to "constant/cellToRegion"
<<Writing region 0 with 229500 cells to cellSet region0
<<Writing region 1 with 41760 cells to cellSet region1

Checking patch topology for multiply connected surfaces...
Patch          Faces      Points     Surface topology
pipeWall        5760       5796      ok (non-closed singly connected)
ringWall        3132       3132      ok (closed singly connected)
inlet           1809       1864      ok (non-closed singly connected)
outlet           1809       1864      ok (non-closed singly connected)
defaultFaces    5760       5796      ok (non-closed singly connected)
otherFaces      5760       5796      ok (non-closed singly connected)

```

Listing 183: The most relevant lines of `checkMesh`'s output showing the intermediate state of our mesh.

We have renamed the patch `defaultFaces` in one of the constituent meshes to `otherFaces`. Hence, after merging the two meshes, we have both patches present: `defaultFaces` and `otherFaces`. Note, that each of these patches has the same number of faces and each patch is half the size of the patch `defaultFaces` in Listing 182. Thus, we have split the original patch `defaultFaces` in two.

Figure 79 shows the result of our splitting and merging operations with the intermediate renaming of one of the patches.

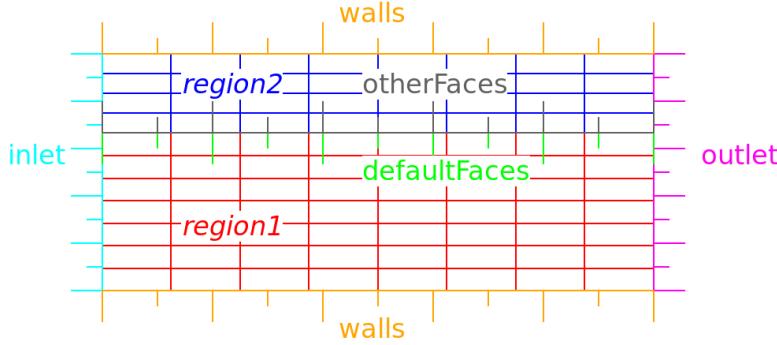


Figure 79: A schematic representation of a mesh with two unconnected regions resulting from meshing a compound solid in Salome.

After calling `stitchMesh defaultFaces otherFaces`, we have eliminated these two patches, since they match perfectly. Listing 184 shows the final report of `checkMesh`. The two constituent patches of the stitching operation are still present, though with a zero number of faces. They can be eliminated by executing `createPatch`, see Section 30.8.1.

```

Checking topology...
Boundary definition OK.
Cell to face addressing OK.
Point usage OK.
Upper triangular ordering OK.
Face vertices OK.
Number of regions: 1 (OK).

Checking patch topology for multiply connected surfaces...
Patch          Faces      Points   Surface topology
pipeWall        5760       5796    ok (non-closed singly connected)
ringWall        3132       3132    ok (closed singly connected)
inlet           1809       1864    ok (non-closed singly connected)
outlet           1809       1864    ok (non-closed singly connected)
defaultFaces     0          0        ok (empty)
otherFaces       0          0        ok (empty)

```

Listing 184: The most relevant lines of `checkMesh`'s output showing the final state of our mesh.

26.5 Two-dimensional mesh creation using Salome

This section discusses the workflow necessary to create two-dimensional meshes for OpenFOAM using Salome. The implied complication is that OpenFOAM's two-dimensional meshes are in fact three-dimensional with only one cell in the third direction. To ensure this, we create a truly two-dimensional mesh in Salome, which is then extruded creating a single layer.

In this example, we want to create an axi-symmetric mesh, which is the slightly more complex variant of the two possible two-dimensional meshes. The other variant being a straight-forward two-dimensional mesh, which amounts to a mesh with a single cell in thickness direction. The axi-symmetric mesh is a wedge, which is by definition of non uniform thickness.

Figure 80 shows our already completed two-dimensional mesh in Salome. There, we meshed a partition consisting of several faces. This allows us to directly create wall-layers consisting of quadrilateral elements, since they are separate geometry entities. The remaining interior is meshed using triangular elements using Netgen.

The collection of geometric groups as well as sub-meshes in the Object Browser visible in Figure 80 is indicative of a bottom-up approach to mesh generation.

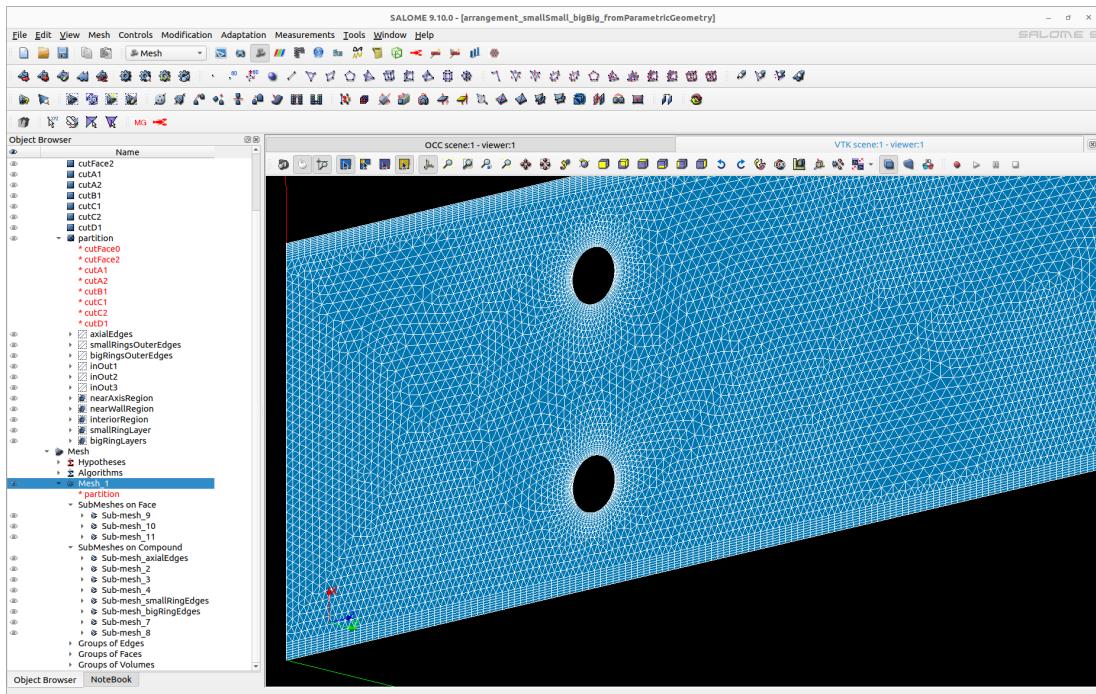


Figure 80: A true 2D mesh of quads and triangles created with Salome.

Figure 81 shows the creation of the axi-symmetric mesh for OpenFOAM. We extrude the two-dimensional mesh along an axis using the *Revolution* operation of Salome. Note, that we only create a single layer of cells – this is achieved by the setting *Number of steps*, and we only create a 5 degree wedge – this is controlled by the setting *Angle by Step* or *Total Angle*, which are interchangeable in our special case. The preview, shown in Figure 81 in yellow, clearly shows the non-uniform thickness of the wedge.

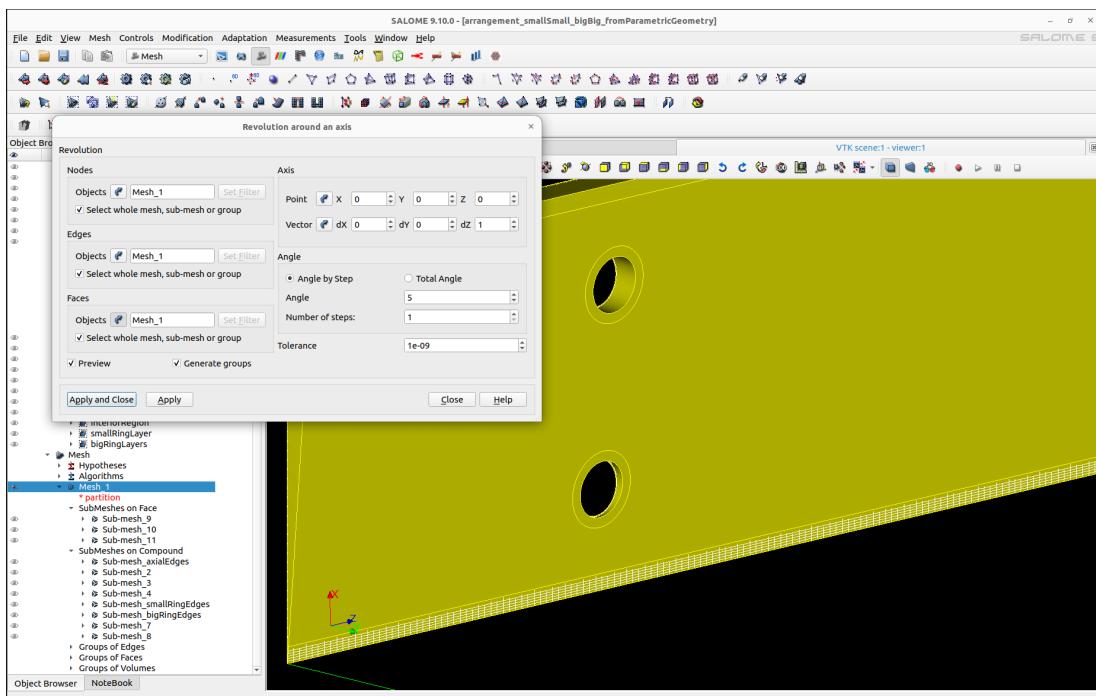


Figure 81: A revolution of the 2D mesh creates our axi-symmetric wedge-like mesh for OpenFOAM.

Figure 82 shows the last step of our work-flow. We rotate the mesh back half the wedge-angle. We do this in order to ensure the mesh straddles a principal plane. Since the revolution-extrusion operates in only one

direction, we need to rotate the resulting mesh back half the extruded angle to get a mesh that is symmetric with respect to x - z plane.

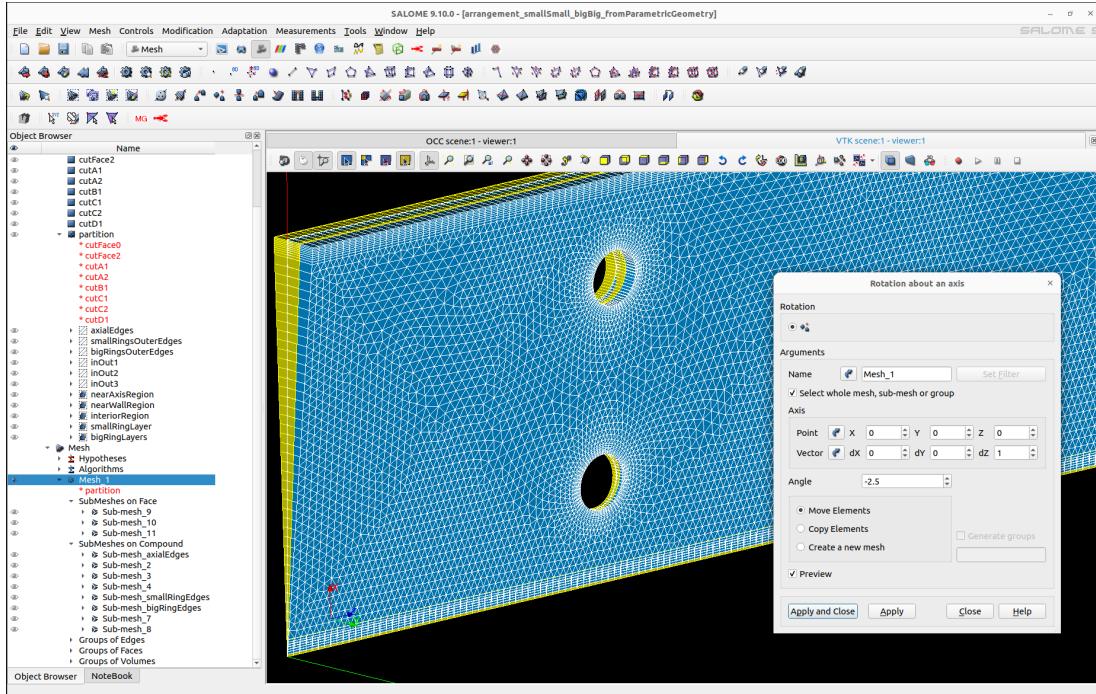


Figure 82: Rotating the mesh back half the wedge angle.

After these operations, Salome automatically created groups of faces from pre-existing groups of edges. Also some new groups of edges were created. Depending on the way we want to export the mesh, we might need to clean-up or even delete some of those groups.

Alternative approaches

This workflow, i.e., creating a true 2D mesh and then extruding it, is not the only way to create a two-dimensional mesh for OpenFOAM. We could also create a thin wedge or slab, create a 2D sub-mesh on one of the principal faces, and then create a 3D mesh with only one cell in thickness-direction. However, while this full-3D approach may work perfectly well for a slab-type two-dimensional mesh, an axi-symmetric wedge-type mesh may prove difficult or even impossible (the author has not tried).

Alternatively, one might create slab-type meshes and perform the revolution-extrusion and back-rotation operations on the OpenFOAM side as shown in Section 22.2.

27 Gmsh

Gmsh⁸⁹ is a 3D finite element meshing software. Gmsh is operated via its GUI or via ASCII input files in Gmsh's own scripting language. Gmsh is able to create all cell shapes from tets to hexes. The meshes generated by GMSH can be converted to OpenFOAM's format using the *gmshToFoam* utility.

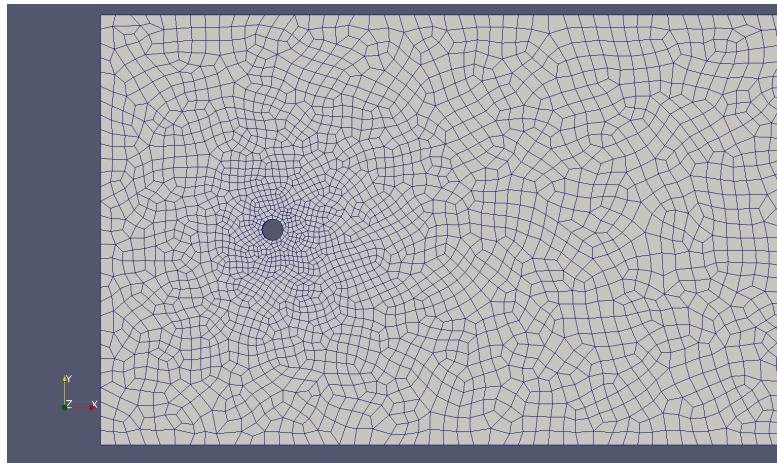


Figure 83: An extruded 2D mesh of quad elements created with Gmsh.

⁸⁹<http://gmsh.info/>

28 enGrid

enGrid⁹⁰ is an open source mesh generation software with CFD applications in mind. It uses the netgen⁹¹ meshing library. enGrid primarily creates tet meshes, however, it also allows for the creation of prismatic boundary layers and the conversion of tets to polyhedras. enGrid natively exports its meshes to OpenFOAM. enGrid is operated via its GUI.

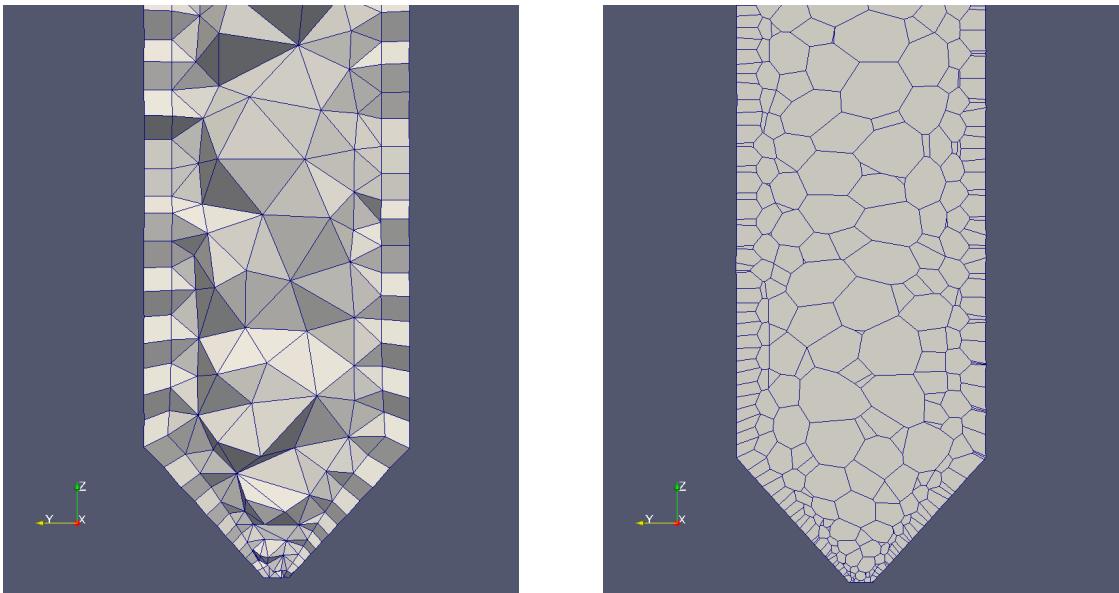


Figure 84: Meshes by enGrid: **left:** tet-mesh with prismatic boundary layer, **right:** polyhedral mesh with boundary layer.

⁹⁰<https://github.com/enGits/engrid/wiki>

⁹¹<https://sourceforge.net/projects/netgen-mesher/>

29 Mesh converters

To use meshes created by programs other than *blockMesh* there is a number of converters. The User Guide [52] lists the following converters:

- *fluentMeshToFoam*
- *starToFoam*
- *gambitToFoam*
- *ideasToFoam*
- *cfx4ToFoam*

The names of the converters are pretty self explanatory.

General recommendations

Always write in ASCII format

Any data exchange between your current installation of OpenFOAM and any other software is best handled in ASCII format.

29.1 *fluentMeshToFoam* and *fluent3DMeshToFoam*

fluentMeshToFoam converts meshes stored in the `*.msh` file format into the format of OpenFOAM. To be more specific, *fluentMeshToFoam* converts only 2D meshes, whereas 3D meshes can be converted using *fluent3DMeshToFoam*.

The converter expects the path to the `*.msh` file as an argument. The converter saves the mesh in the format of OpenFOAM in the `constant/polymesh` directory.

If converter is invoked from a directory other than the case directory, then the path to the case directory has to be specified via an additional argument. See Section 12.6.

If the mesh was created using an other dimension than in metres, the command line parameter `-scale` can be used to correct the scaling. OpenFOAM expects the mesh data to be expressed in metres.

All other possible option can be displayed with this command line parameter `fluentMeshToFoam -help`.

29.2 *ideasUnvToFoam*

ideasUnvToFoam is a converter which is commonly used to convert meshes in the UNV format to OpenFOAM's format, Salome is a well-known meshing software, which exports meshes in the UNV format, see Section 26.

29.2.1 Mesh regions

At some time between the releases of OpenFOAM-6 and OpenFOAM-9⁹², the *ideasUnvToFoam* converter got extended with the `-region` command line option. This is especially useful when creating a multi-region case from external geometries/meshes, e.g., when we use Salome for geometry and mesh creation.

29.2.2 Pitfall: Groups of Edges

If we export a mesh from Salome in the UNV format containing groups of edges, then we might not be able to convert the mesh into OpenFOAM's format using *ideasUnvToFoam*.

Listing 185 shows the relevant lines of error message, which are somewhat enigmatic. Only with the knowledge that *LineThick* and *LineCircumference* are edges of the geometry do we have a chance to figure out what is going wrong. The output shown in the Lines 3 and 4 indicates that the groups of edges written out by Salome are treated as patches by the converter. As an edge is no face, trouble looms.

⁹²The author couldn't be bothered to narrow this down more specifically.

```

1 Processing tag:2467
2 Starting reading patches at line 1382.
3 For group 1 named LineThick trying to read 4 patch face indices.
4 For group 2 named LineCircumference trying to read 21 patch face indices.
5 For group 3 named faceThick trying to read 84 patch face indices.
6
7 Sorting boundary faces according to group (patch)
8 0: LineThick is faceZone
9
10 --> FOAM FATAL ERROR: 1 not found in table.  Valid entries:
11 218
12 (
13 105
14 106
15 ... further output omitted

```

Listing 185: A not so telling error message encountered with `ideasUnvToFoam`.

Hence, check-for and delete all groups of edges prior to exporting the mesh. Figure 85 shows the relevant entry in the object browser of Salome.

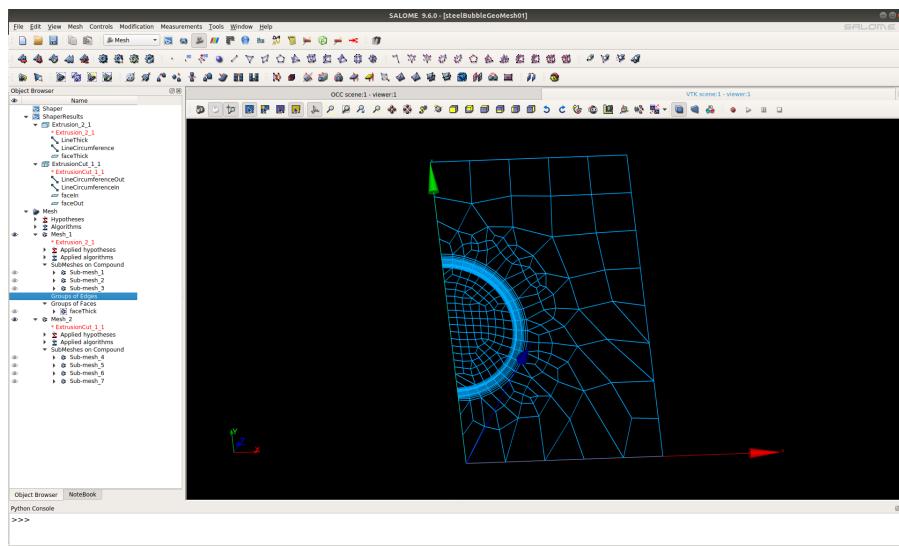


Figure 85: The entry for groups of edges in the object browser of Salome.

29.2.3 Pitfall: Groups of Volumes

In a similar fashion as Groups of Edges, also Groups of Volumes present in the mesh at time of exporting into UNV-format may cause the `ideasUnvToFoam` converter to crash.

29.2.4 Pitfall: faulty patch definition

A faulty patch definition within Salome can lead to an error when converting the exported mesh from the UNV-format into OpenFOAM's native mesh format using the `ideasUnvToFoam` mesh converter.

Listing 186 shows the relevant lines of output. In this case, an annular face was extruded along a curved path. Figure 86 shows a detail of the resulting mesh. Note, that the mesh in question is created by extruding the mesh of the base surface, in this case the annular cross-section, along a path. With this bit of relevant information, we now turn our attention to Lines 5 and 6 of Listing 186. Here we see that the number of reported faces of the inner and the outer surface of the pipe is not equal. If both inner and outer surface were properly defined, then this numbers should be equal.

This faulty patch definition causes `ideasUnvToFoam` to treat the inner-surface as a face-zone, as indicated in Line 12 of Listing 186.

The output at Line 24 indicated that mesh conversion fails at the stage when processing face- and cell-zones. Since there are no cell-zones in our mesh, it is the face-zone that causes the error. In the experience of the author, cell-zones pose no problem in conversion.

In this example, the outer-surface contained also some faces which should have belonged to the inner-surface. Since, the outer-surface was processed first, these faces were added to the outerSurface patch. Since the inner-surface also contained these wrongly-assigned faces, the converter could not make the inner-surface a patch, since this would have resulted in faces belonging to two patches⁹³. Hence, the converter treated the inner-surface as a face-zone. Consequently, the converter created a new patch for the remaining unassigned faces, as indicated by Line 22 in Listing 186.

```

Processing tag:2467
Starting reading patches at line 568030.
For group 1 named inface trying to read 39 patch face indices.
For group 2 named outface trying to read 39 patch face indices.
For group 3 named outerSurface trying to read 31200 patch face indices.
For group 4 named innerSurface trying to read 30550 patch face indices.

Sorting boundary faces according to group (patch)
0: inface is patch
1: outface is patch
2: outerSurface is patch
3: innerSurface is faceZone

Constructing mesh with non-default patches of size:
    inface    39
    outface   39
    outerSurface  31200

--> FOAM Warning :
From function Foam::polyMesh::polyMesh(const Foam::IOobject&, Foam::pointField&&, const
cellShapeList&, const faceListList&, const wordList&, const wordList&, const Foam::word&,
const Foam::word&, const wordList&, bool)
in file meshes/polyMesh/polyMeshFromShapeMesh.C at line 595
    Found 29900 undefined faces in mesh; adding to default patch.

Adding cell and face zones
Face Zone innerSurface 30550
ideasUnvToFoam: ideasUnvToFoam.C:1287: int main(int, char**): Assertion `nouveau > -1' failed.
Abgebrochen (Speicherabzug geschrieben)

```

Listing 186: The relevant output of the mesh conversion error.

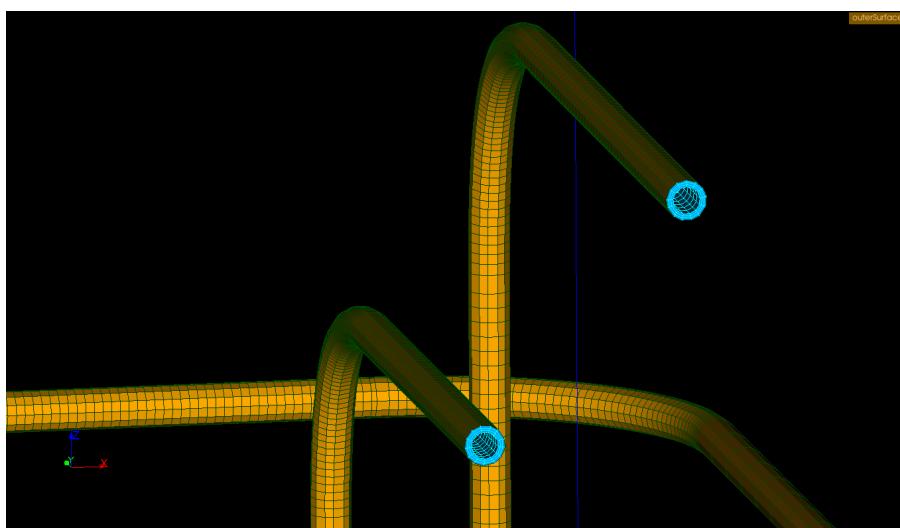


Figure 86: The extruded mesh of a heat-exchanger coil

⁹³Salome does not have a problem with a face belonging to multiple face-groups. However, when trying to convert the exported mesh into an OpenFOAM mesh, the converter falls over. An individual face can not be part of more than one patch.

After the error was fixed in Salome, conversion finished without error, as can be seen from Listing 187. Now the number of faces for the inner- as well as the outer-surface is equal, and both surfaces are treated as patches by the converter.

```

Processing tag:2467
Starting reading patches at line 568030.
For group 1 named inface trying to read 39 patch face indices.
For group 2 named outface trying to read 39 patch face indices.
For group 3 named outerSurface trying to read 30550 patch face indices.
For group 6 named innerSurface trying to read 30550 patch face indices.

Sorting boundary faces according to group (patch)
0: inface is patch
1: outface is patch
2: outerSurface is patch
3: innerSurface is patch

Constructing mesh with non-default patches of size:
    inface    39
    outface   39
    outerSurface  30550
    innerSurface  30550
End

```

Listing 187: The relevant output of the mesh conversion after the error has been fixed.

29.3 Pitfall: length units

Third party meshes may be based on millimetres instead of metres as expected by OpenFOAM. Point coordinates will be interpreted by OpenFOAM as being expressed in metres, i.e. $P_{in\ file} = (120, 240, left(120\ 0))$ mm will be read by OpenFOAM as $P_{in\ mesh} = (120, 240, 0)$ m. Thus, the imported mesh will be scaled by a factor of 1000.

Some mesh converters (e.g. `fluent3DMeshToFoam`) offer a `-scale` option to fix the length scales along with mesh conversion. Other mesh converters (e.g. `ideasUnvToFoam`) do not offer such a scaling function. However, there is a utility (`transformPoints`) which, among other tasks, can be used to correct the length scales of the mesh.



Always run `checkMesh`, ideally with its options `-allGeometry` and `-allTopology`, to, first, check the mesh quality, and secondly, to check the mesh bounding box. The bounding box will be expressed in metres, as any other length in OpenFOAM. This will give you a chance to spot a millimetre vs. metre situation.

Listing 188 shows the relevant lines of `checkMesh`'s output. Unless, we calculate meteorological flows, a simulation domain in kilometre scale seems a bit off.

```

Checking geometry...
Overall domain bounding box (-752.264 -325 -684.294) (752.264 1400 3754.35)

```

Listing 188: The bounding box of our mesh

30 Other mesh manipulation tools

30.1 *transformPoints*

The tool *transformPoints* can be used to scale, translate or rotate the points a mesh. Section 33.3.4 contains a case in which this tool can be useful.

30.1.1 Rotation

Rotating the geometry can be specified in two ways.

Using two vectors

Here, the rotation is defined by providing a vector before and after the rotation. From these two vectors, the transformation matrix can be computed

Yaw, Pitch and Roll

There are actually two options: *rollPitchYaw* and *yawPitchRoll*. Here, the rotation is defined by specifying three angles in degrees, which are subsequently applied to the **x**-axis, the **y**-axis and the **z**-axis.

30.2 *topoSet*

The tool *topoSet* creates point, face or cell sets from a geometric definition. There are a number of ways to define the geometric region containing the intended points, faces or cells.

30.2.1 Usage

The dictionary *topoSetDict* is used to define the geometric region. Find some examples in the tutorials using the following command.

```
find $FOAM_TUTORIALS -name topoSetDict
```

Listing 189: Find examples for the use of *topoSet*

A face or cell set will contain only faces or cells whose centres lie within the specified geometric region.

30.2.2 Life hack: apply *topoSet* on decomposed cases

The tool *topoSet* can be applied to decomposed cases, by running the tool in parallel in the same fashion as we would run a solver in parallel.

```
mpirun -np 4 topoSet -parallel
```

Listing 190: Run *topoSet* in parallel, i.e. apply *topoSet* on a decomposed case.

This will apply all definitions for the creation of sets and zones to the sub-domains of the decomposed case.

This can also be done with cases that are currently running, e.g. as a long-duration simulation is running, we are preparing sets and zones for the subsequent post-processing. However, if we apply *topoSet* on a case, which is at that time being simulated, we need to take extra care not to alter, remove or mess in any other way with already existing sets or zones.

The sets and zones we created for the sub-domains of the decomposed case need to be reconstructed, so that they are present when the case is finished, and the subsequent post-processing is done on the reconstructed case. We can reconstruct sets and zones, which were created with the decomposed case, by calling *reconstructPar* with the **-constant** command line argument.

30.2.3 Pitfall: The definition of the geometric region

To demonstrate the function of `topoSet` a cell set was defined for the cavity tutorial-case. The mesh of the cavity case is $1 \times 1 \times 0.1$ m and the box defining the cell set was chosen to be $0.5 \times 0.5 \times 0.05$ m. The dimensions of this box are simply half the dimensions of the mesh. However, only cells whose cell centre is located in the box are contained in the cell set. As the mesh is one cell in depth and 0.1 m in depth, all the cell centres are exactly at $z = 0.05$ m. Due to inevitable numerical errors in calculating the cell centre⁹⁴, the numerical errors decided whether a cell was included into the cell set or not.

To avoid this error, always make sure the geometric region contains all the intended cells.

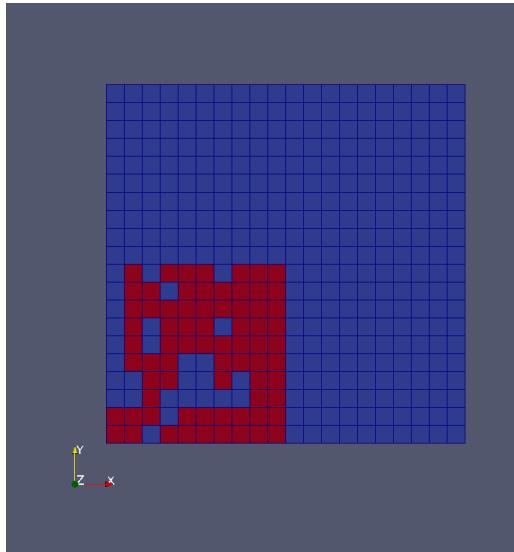


Figure 87: A faulty cell set definition. The red cells are part of the cell set. All other cells are blue.

30.2.4 Pitfall: the face-normal of internal faces

For simulations with run-time post-processing, we might need sets of internal faces, e.g. for extracting the pressure at certain cross-sectional planes. With `topoSet` we can create sets of internal faces by using the `boxToFace` source to select all faces in a slice of geometry, and the `normalToFace` source to select all faces with a face-normal parallel to the normal of the cross-sectional plane in question, and finally perform a boolean operation to eliminate all faces not oriented parallel to the cross-sectional plane.

While this procedure requires a bit of trial-and-error to determine the proper size of the box to include only a single layer of faces parallel to the cross-sectional plane, the procedure is generally appropriate for the task in question. However, there is one flaw in the discussed procedure: the orientation of the face-normal vectors of internal faces.

If we imagine a pipe with its principal axis parallel to the x axis, then the internal faces we need for our cross-sectional plane have their face-normals oriented parallel to the x axis. However, the face-normals of the internal faces may point into the positive x direction or into the negative x direction. Thus, our procedure from above needs to be extended by a second use of the `normalToFace` source, this time with the opposite normal vector.

30.2.5 Legacy pitfall: renumbered mesh

At the point of writing, using OpenFOAM-2.something, the utility `renumberMesh` does not consider cell sets⁹⁵. If `renumberMesh` is called after cell sets were created by `topoSet`, the cell set is invalid. The reason for this is, that the cell labels of the cell set remain unchanged as `renumberMesh` completely relabels the mesh. Thus, the cell set still exists and the number of cells is unchanged, however, as other cells bear the labels of the original members of the cell set, the cell set is invalid.

⁹⁴The location of the cell centre is not stored in any file, thus this quantity has to be computed.

⁹⁵This behaviour was reported in bug report 1377 (<http://openfoam.org/mantisbt/view.php?id=1377>), and has been fixed for OpenFOAM-3.0 and later versions.

To resolve this problem, `topoSet` needs to be run after `renumberMesh`. This even works in parallel, when the case has been decomposed.

30.3 `setsToZones`

The utility `setsToZones` serves the purpose to:

Add `pointZones/faceZones/cellZones` to the mesh from similar named `pointSets/faceSets/cellSets` [52].

This utility is needed when we create some `cellSets` which we later want to use e.g. with a `functionObject` (the `cellSource functionObject` acts on all cells or on a `cellZone`). `cellSets` can be created with `topoSet`. After we ran `topoSet` we simply run `setsToZones` without any further parameters or providing a dictionary. `setsToZones` creates `cellZones` which contain the same cells as the corresponding `cellSets`.

30.3.1 Pitfall: sets vs. zones

One major difference between sets and zones, which is not (yet) mentioned elsewhere (at the time of writing) in this manual, is that cells can be part of an arbitrary number of sets, however, a cell can only be an exclusive member of a zone. Hence, a cell can not be part to two or more zones.

30.4 `refineMesh`

The tool `refineMesh` is used – just as the name suggests – to refine a mesh.

30.4.1 Usage

First a cell set has to be defined, this can be done using the tool `topoSet`.

With the dictionary `refineMeshDict` the rules for refining a particular cell set can be stated. When rules have been defined in `refineMeshDict`, then the command line option `-dict` has to be used.

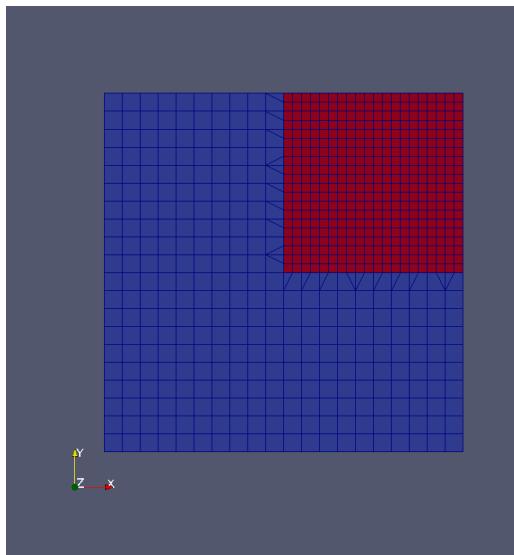


Figure 88: An example of a refined mesh. The refined region is marked in red.

30.4.2 Pitfall: no command line parameters

If the tool `refineMesh` is called without any command line parameters then the whole mesh is refined. For `refineMesh` to obey the rules set in the `refineMeshDict` the command line option `-dict` has to be used when calling `refineMesh`. See this useful post in the CFD-Online Forum <http://www.cfd-online.com/Forums/openfoam-meshing-utilities/61518-blockmesh-cellset-refinemesh.html#post195725>

Notice the different meaning of the `-dict` command line option of the tools `topoSet` and `refineMesh`. If you are in doubt about this difference, check the summary of the command line usage printed by the `-help` option.

30.5 *refineWallLayer*

`refineWallLayer` is a tool to refine cells that are adjacent to a set of user-specified patches.

30.5.1 Control

The list of patches is provided by the user via a command line argument. The next argument is the edge fraction, which is to be applied in the refinement. Listing 191 shows an example of how this tool is called. The list of patches and the edge fraction are mandatory arguments.

```
refineWallLayer -overwrite (top bottom sideLeft) 0.4
```

Listing 191: Invoking `refineWallLayer` for the cells adjacent to three patches.

30.5.2 Refining at edges

Figures 89, 90 and 91 show the results of a successive application of this tool along with the base mesh. In this case, the patch of the inner void is refined. Figures 90 and 91 show the treatment of sharp, concave edges.

Figure 92 shows the result of `refineWallLayer` when the cells belonging only one patch are refined.

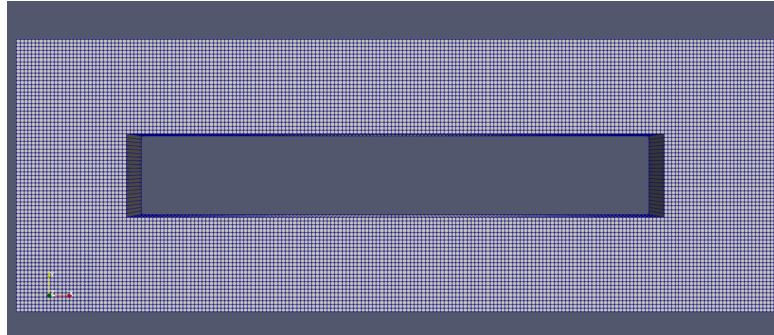


Figure 89: The base mesh for the wall layer refinement.

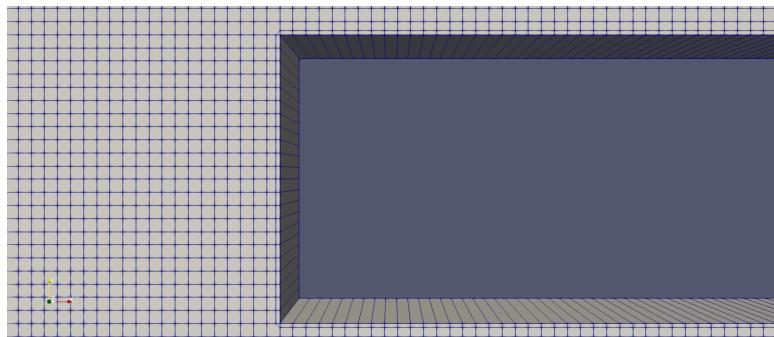


Figure 90: Applying the wall layer refinement once.

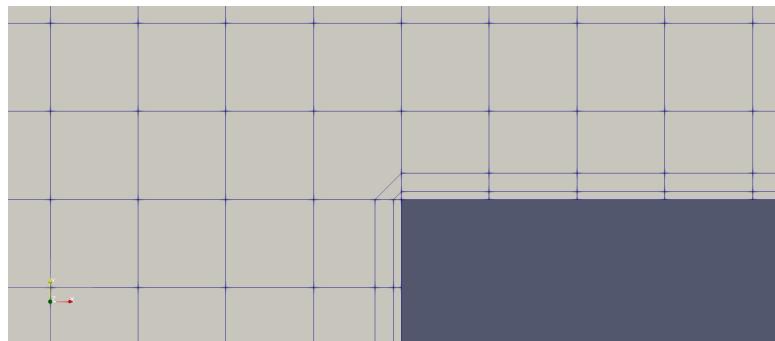


Figure 91: Applying the wall layer refinement a second time.

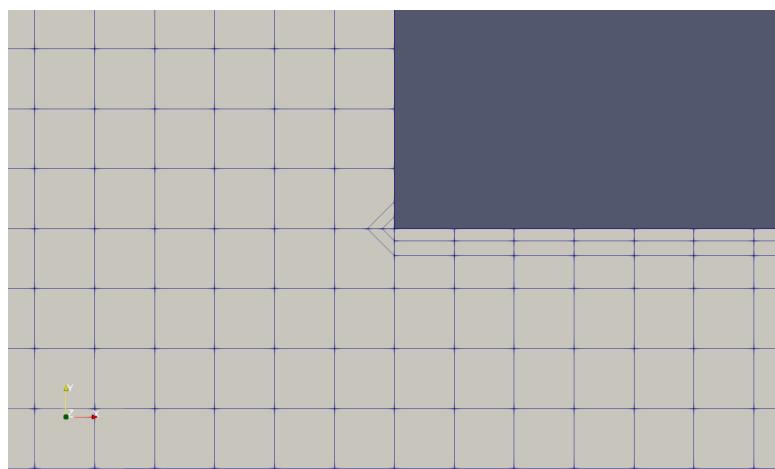


Figure 92: Applying the wall layer refinement twice on the horizontal patch at a concave edge.

Figures 93 and 94 show how `refineWallLayer` treats convex edges. If the edge is formed by two distinct patches, `refineWallLayer` can be applied to each patch individually, which leads to a different outcome, compare Figures 93 and 95.

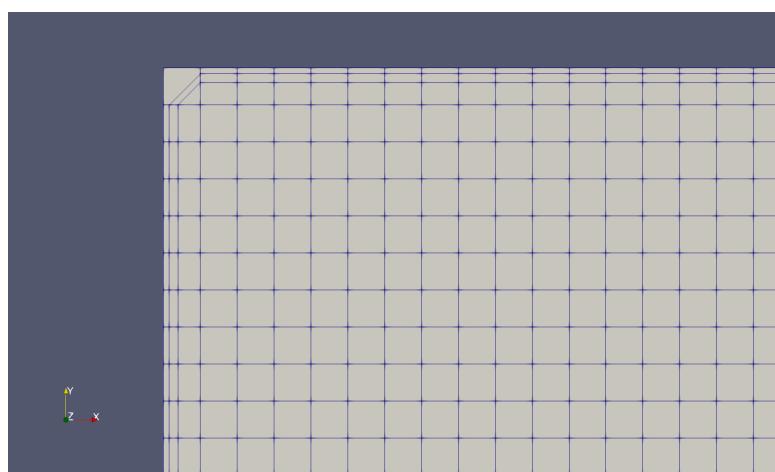


Figure 93: Applying the wall layer refinement twice on both patches of a convex edge.

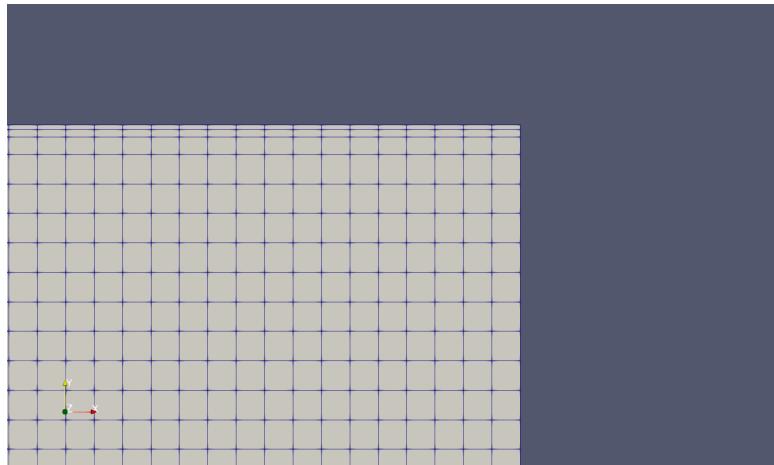


Figure 94: Applying the wall layer refinement twice on one patch of a convex edge.

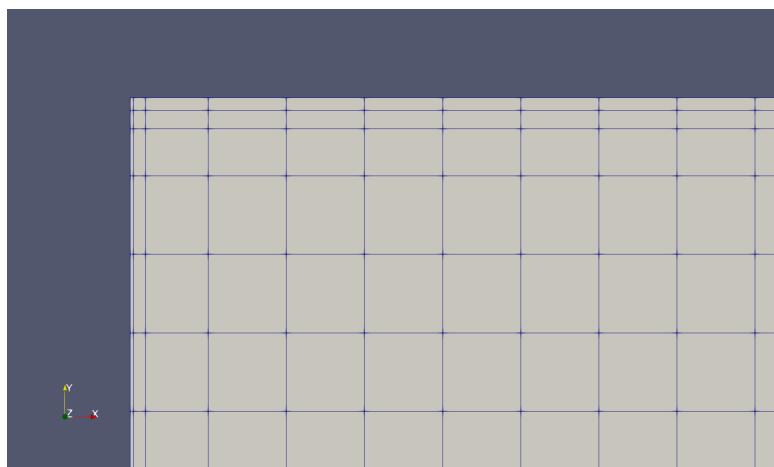


Figure 95: Applying the wall layer refinement successively on two patches of a convex edge. This approach leads to a different outcome than the one shown in Figure 93.

30.5.3 Refining-creating boundary layers

Here, we created a segmented pipe bend using `blockMesh`. The resulting mesh has no boundary layer, hence we tried to achieve this using `refineWallLayer`.

Figure 96 shows the result of multiple calls of `refineWallLayer`. The cells in the boundary layer share the orientation of the interior cells. Note, that the whole segmented bend has a single wall patch. Hence, there were no edges between different wall patches to cause trouble.

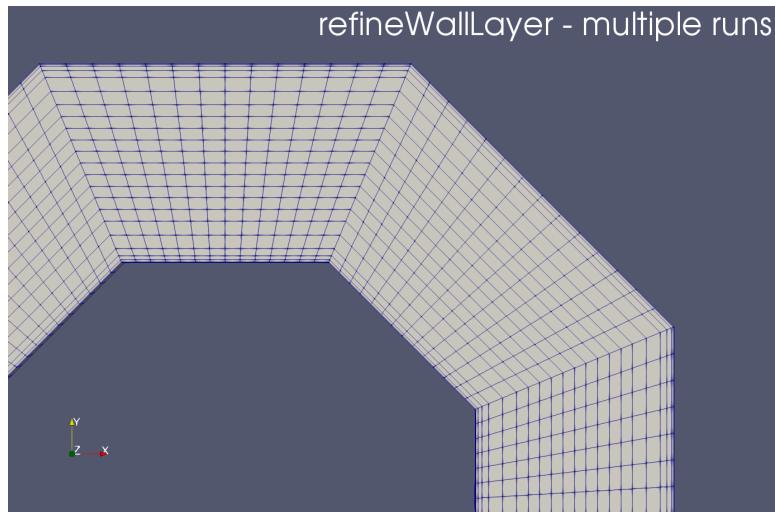


Figure 96: Creating a boundary layer mesh by splitting the wall-adjacent cells.

Figure 97 shows the creation of a wall boundary layer on the example of a pipe fork. The refined wall patch was one single patch.

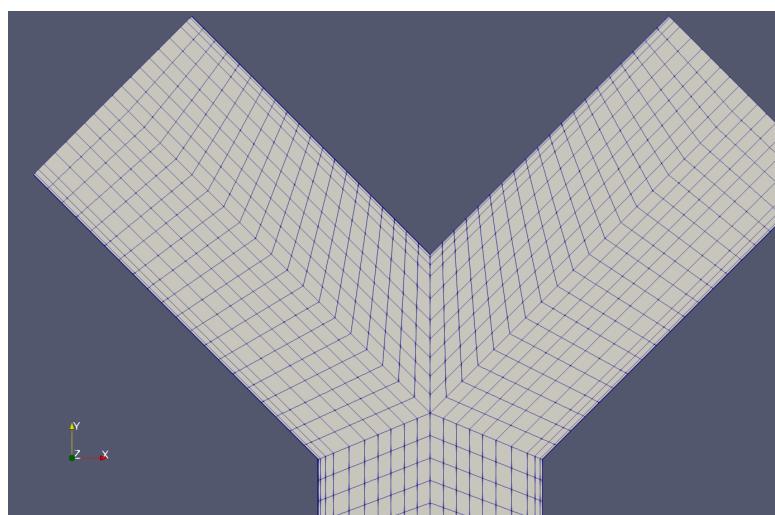


Figure 97: Creating a boundary layer mesh by splitting the wall-adjacent cells.

Figure 98 shows the same geometry as Figure 97, however, the wall patch was split into two distinct patches. The `refineWallLayer` operation was applied to both wall patches together though.

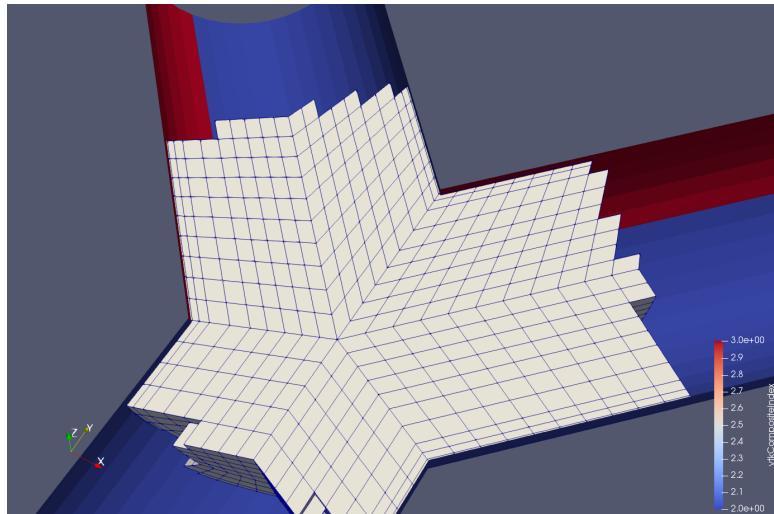


Figure 98: Creating a boundary layer mesh by splitting the wall-adjacent cells.

30.6 *renumberMesh*

30.6.1 General information

The tool *renumberMesh* modifies the arrangement of the cells of the mesh in order to create lower bandwidth for the numerical solution. For further information about the role and the influence of the bandwidth in numerical simulation see books on the numerical solution of large equation systems, e.g. [37].

Renumbering the mesh can reduce computation times as it re-arranges the data to benefit the numerical solution of the resulting equation system. The benefit of renumbering the mesh strongly depends on several factors. However, testing is recommended.

Renumbering the mesh even has an effect at the simplest possible simulation case – the cavity case of the tutorials. This mesh consists of a single block and it is quasi 2D (i.e. it is only 1 block in depth). The mesh resolution was chosen to $40 \times 40 \times 1$, resulting in 1600 cells. *icoFoam* was run for 10 s. Execution time was reduced by *renumberMesh* from 6.18 s to 6.08 s.

A simulation with a mesh consisting of 120000 cells defined by 9 blocks was run for 5 s of simulated time with *twoPhaseEulerFoam*. Execution time was reduced by *renumberMesh* from 9383.81 s to 9273.13 s.

Even though the reduction of execution time is small in this examples, this reduction comes at no cost. Running *renumberMesh* takes little time and at run-time of the simulation no additional work has to be done.



Run *renumberMesh* before any other tools which generate sets or zones. Why the order of execution of certain tools is significant is explained in Section 30.6.3 on a case which went slightly wrong.

30.6.2 Background

The discretized finite volume problem results in a linear equation system, which is usually expressed in matrix-form.

$$\mathbf{Ax} = \mathbf{b} \quad (41)$$

The vector \mathbf{x} contains the field values at the cell centers. The matrix \mathbf{A} contains non-zero elements for each pair of neighbouring cells. This is a consequence of our assumption that only adjacent cells interact. If we used some sort of higher order discretisation or interpolation, we might get into a situation where also second neighbours interact. However, for sake of ease, we limit ourselves in this discussion to direct neighbours.

Regardless of our computational mesh being one-, two- or three dimensional, we label all cells with positive ascending integers. Thus, we can store the values of a scalar field into a vector. The number of elements of this vector (N) is equal to the number of cells in our domain. Consequently, the matrix \mathbf{A} is of the size $N \times N$. However, as only adjacent cells interact, most of the elements of \mathbf{A} will be zero-entries.

If the cells with the labels i and j are adjacent, then the elements a_{ij} and a_{ji} of \mathbf{A} will be non-zero. Since we focus on the general structure of \mathbf{A} we do not care whether a_{ij} equals a_{ji} , or if both of them are actually non-zero⁹⁶.

The arrangement of the cells – or, to be more precise, the labelling – has a strong impact on the structure of the matrix \mathbf{A} , i.e. the distribution of the non-zero elements.

A simple example

Here we examine the effect of cell labelling with a very simple example. Figure 99 shows a simple mesh with 8 cells. Two different cell labelling schemes are indicated by the numbers inside the cells.

In Figure 100 we see the connections between the cells depicted as a graph. A $N \times N$ matrix can be from the interaction perspective seen as a graph with N nodes. An edge between the nodes i and j represents the non-zero elements a_{ij} and a_{ji} .

<table border="1"><tr><td>0</td><td>1</td><td>2</td><td>3</td></tr><tr><td>4</td><td>5</td><td>6</td><td>7</td></tr></table>	0	1	2	3	4	5	6	7	<table border="1"><tr><td>0</td><td>2</td><td>4</td><td>6</td></tr><tr><td>1</td><td>3</td><td>5</td><td>7</td></tr></table>	0	2	4	6	1	3	5	7
0	1	2	3														
4	5	6	7														
0	2	4	6														
1	3	5	7														

Figure 99: A simple mesh with 8 cells and different cell labelling schemes.

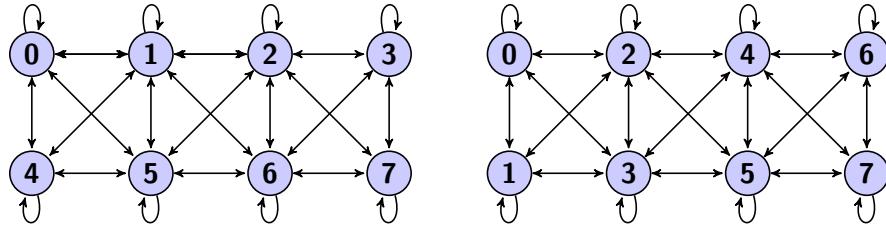


Figure 100: The connectivity graph of our mesh.

Figure 101 shows the corresponding matrix structure. The labelling scheme on the right hand side of Figures 99 and 100 results in a matrix with a lower bandwidth.

	0	1	2	3	4	5	6	7		0	1	2	3	4	5	6	7
0	*	*	0	0	*	*	0	0		*	*	*	*	0	0	0	0
1	*	*	*	0	*	*	*	0		*	*	*	*	0	0	0	0
2	0	*	*	*	0	*	*	*		*	*	*	*	0	0	0	0
3	0	0	*	*	0	0	0	*		*	*	*	*	0	0	0	0
4	*	*	0	0	*	*	0	0		0	0	*	*	*	*	*	*
5	*	*	*	0	*	*	*	0		0	0	*	*	*	*	*	*
6	0	*	*	*	0	*	*	*		0	0	0	0	*	*	*	*
7	0	0	*	*	0	0	*	*		0	0	0	0	*	*	*	*

Figure 101: The matrix structure. A * denotes a non-zero element. Notice the lower bandwidth of the matrix on the right hand side. The number of zero-entries is equal, however, the different distribution leads to a different numerical behaviour.

⁹⁶The upwind differencing scheme causes the downstream cell to depend on the upstream cell. However, the upstream cell is not directly influenced by the downstream cell.

30.6.3 Pitfall: sets and zones will break my bones

The use of `renumberMesh` carries a certain risk. In simulation cases which make use of tools like `topoSet` and `renumberMesh`, the order in which those tools are invoked is of importance. **Update:** This has been resolved at some point. In OpenFOAM-4.0 this is no issue any more.

The reason behind this, is the way OpenFOAM stores its mesh information. The only actual geometric information is stored in the list of points in the file `constant/polyMesh/points`. The faces are defined via the point labels of the points defining the mesh. Thus, if the points P_k, P_m, P_u and P_w define a face, then the entry in `constant/polyMesh/faces` for this very face reads `(k m u w)`. The same principle applies for the definition of cells. There, the labels of the faces defining the cell are stored. This way, no redundant information is stored. If we define a `cellSet` with `topoSet` e.g. all cells within a certain geometrical region we simply store the cell labels of all cells for which the condition is fulfilled. Thus, if we now run `renumberMesh`, we shuffle the cells within the mesh. No actual change is applied in the mesh, however, the cell with the label A which was at the location (x_A, y_A, z_A) before renumbering, may or most certainly will be at location (x_B, y_B, z_B) with $B \neq A$ after renumbering.

Figure 102 shows the simulation domain of an aerated stirred tank. The red cells are part of a `cellZone` on which source terms using the `fvOptions` mechanism act⁹⁷. A run of `renumberMesh` after the `cellZone` was created caused the `cellZone` to get scrambled. However, the simulation worked nonetheless and yielded some unexpected results.

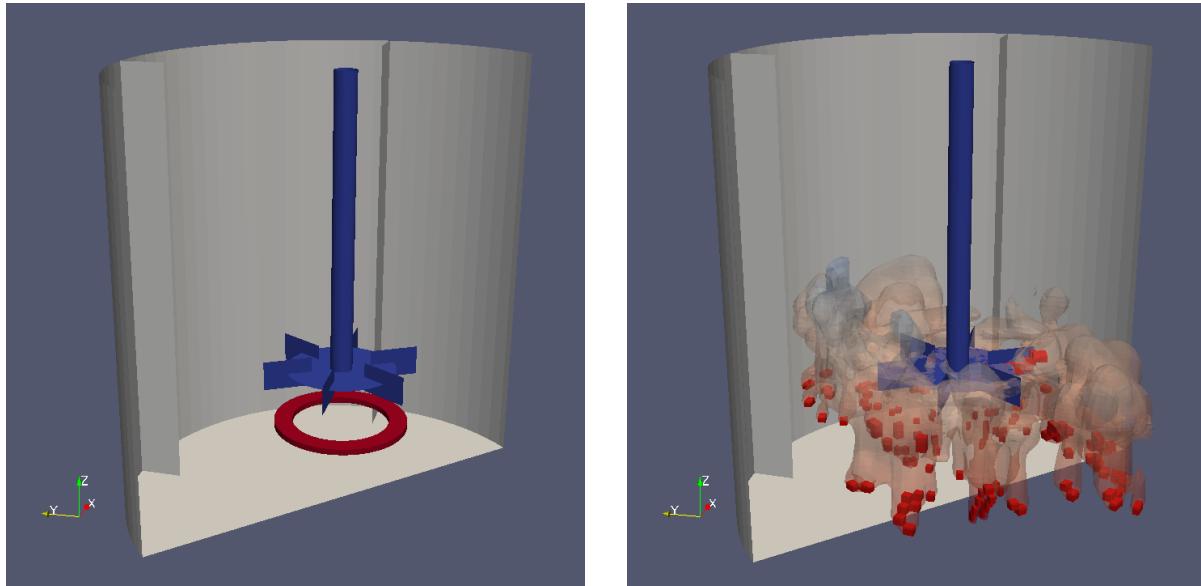


Figure 102: **Left:** The cut-away of the walls of a stirred tank with the rotor (blue) and the aeration device (red). The aeration device is a `cellZone` on which source terms are applied via the `fvOptions` mechanism in OpenFOAM-2.3.x.

Right: The stirred tank was simulated using parallel processes. After decomposing the domain, a parallel renumbering of the mesh was conducted. Renumbering the subdomains scrambled the `cellZone` within their respective subdomains. The transparent iso-volume shows the gas-phase volume fraction 0.25 s into the simulation. The cells of the `cellZone` act as source for the gas-phase, although not on their original location.

30.6.4 Life-hack: converting mesh (and fields) from binary to ASCII

You may run into a situation, my dear reader, when you might need to convert the mesh data of your OpenFOAM case from the binary format into the ASCII format, or vice-versa. What we need in this situation is a tool, which reads and writes the mesh, and `renumberMesh` is just the tool we need⁹⁸. In this case, we simple use to tool for its I/O, and not for its actual use, i.e. re-ordering the mesh to improve numerical solutions.

⁹⁷Have a look on the injection tutorial of `twoPhaseEulerFoam-2.3.x`.

⁹⁸We could think of using the tool `transformPoints` with a scaling factor of 1.0, yet this only affects the file `points`, but not `faces`, `neighbour` and `owner`.

One such occasion of the former need, i.e. convert a mesh from binary to ascii, is when you want to use tools of several OpenFOAM-variants, e.g. the `checkMesh` utility tool of foam-extend-4.0 can not read a mesh in binary format, which was created by a mesh conversion tool (such as `fluentMeshToFoam`) of OpenFOAM-6. For some reason, the binary formats of foam-extend and OpenFOAM (foundation release) are not compatible⁹⁹. However, foam-extend is perfectly happy with meshes written by OpenFOAM in ASCII format. This, rather lengthy prelude, leads us a use-case of the tool `renumberMesh`, which might be considered harmless abuse: use the tool to change the format the mesh is stored on disk.

The procedure is rather simple:

1. Create a new case directory, in which the conversion should take place
2. Copy the relevant folders, i.e. `constant` and `system`, into this new case directory. Also copy time step folders, if necessary.
3. Change the `writeFormat` setting in `system/controlDict` from `binary` to `ascii`.
4. Run `renumberMesh -overwrite`

Now, all the mesh-files, such as `points` or `faces`, are stored on disk in ASCII format.

A note on converting fields

As `renumberMesh` is not a classical pre- or post-processing tool for the case's solution data, there is no option to renumber all fields present in a case. Hence, only one time step is subject to renumbering. This is generally the lowest time step.

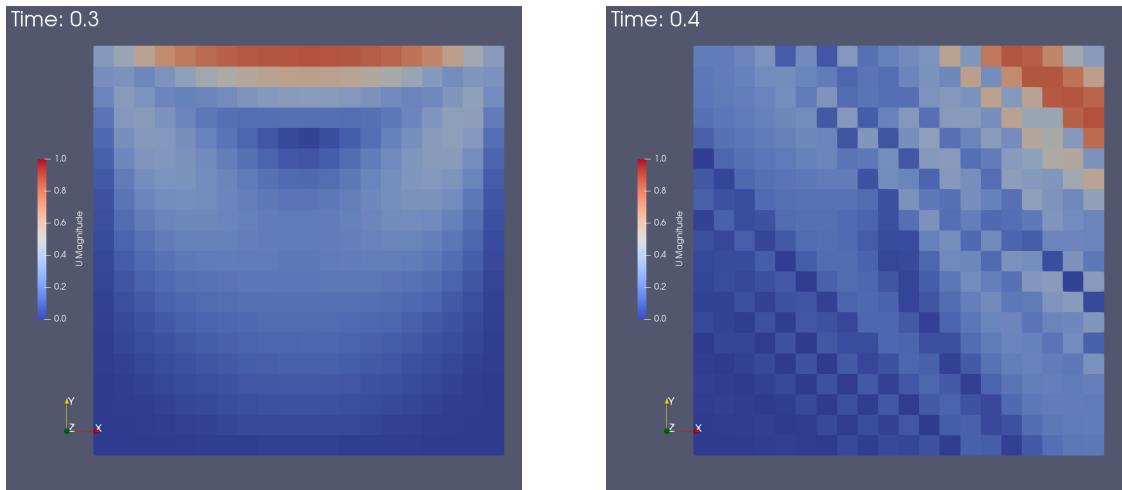


Figure 103: Renumbering the solution of the cavity case: the case was run, and all time steps prior to 0.3 were deleted. Then `renumberMesh -overwrite` was run. As 0.3 was the first time step, the fields in the time step 0.3 were renumbered along with the mesh. The later time steps, however, were left untouched.

Thus, if you want to convert a case with mesh and fields from binary to ASCII format, simply create a copy of the case with one time step only, and perform the renumbering. The tool `renumberMesh` only allows the user to specify one specific time, yet not a range of times. Thus, we consider it not possible to convert a case with multiple time steps from binary to ASCII, or the other around.

30.6.5 Case study: a big mesh on many processors

When running big CFD cases, running them in parallel on multiple/many processors is standard procedure. While distributing the load among many processors helps to accelerate a simulation, parallelisation brings its own additional workload, i.e., the communication between all parallel processes. The tool `decomposePar` prints

⁹⁹This incompatibility, however, is a uni-directional one. A binary mesh written by foam-extend-4, can be read and used by OpenFOAM-6.

a summary of faces and boundaries between processors, which is a proxy for assessing the workload due to this additional communication: the less faces/boundaries between processors, the less communication needs to be done.

Table 4 shows the statistics printed by `decomposePar` when a big CFD case was prepared for a parallel simulation run. The mesh was created by refinement using `refineMesh`. Thus, a 5138560 cell mesh was created from a 642320 cell mesh. Regardless of whether the initial mesh was renumbered, the refined mesh is bound to have a large bandwidth in its mesh structure.

While, the tool `refineMesh` prints its own statistics, i.e., *band* and *profile*, we use the statistics of `decomposePar` as a proxy for the parallel-communication workload. Here, the numbers are more intuitive, since the number of patches between processors is something that is immediately and easily understood. The numbers listed in Table 4 clearly show that renumbering a big mesh prior to decomposition is beneficial, even if we can not directly quantify this benefit¹⁰⁰.

	Num. of processor faces	Number of proc. patches	Number of faces between proc.
Without renumbering	226647	7 (max), 5.278 (avg)	17679 (max), 12591.5 (avg)
After renumbering	186748	5 (max), 4 (avg)	12866 (max), 10374.9 (avg)

Table 4: Some statistics of `decomposePar` from the preparation of a case with 5138560 cells for parallel execution with 36 parallel processes.

30.7 `subsetMesh`

`subsetMesh` is a tool to remove certain cells from a mesh. The tool expects the name of a *cellSet* as a command line argument. The cells of this *cellSet* will remain in the resulting mesh, all other cells are removed.

Pitfall: sets and zones will break my bones

At the time of writing (OpenFOAM-4.0), `subsetMesh` does not treat *cellSets* or *cellZones*. Thus, when we use `subsetMesh` to remove large parts of the mesh, then the *cellSet* may contain cells that are no longer part of the mesh. This error will be felt when the cell indices associated with the *cellSet* or *cellZone* are larger than the total number of cells in the mesh. Otherwise, if the cell indices are smaller than the total number of cells, the *cellSet* might still be valid from OpenFOAM's point of view, but it may contain different cells.

30.8 `createPatch`

30.8.1 Remove empty patches, i.e., patches without any faces

Apart from creating new patches from existing ones or changing the type of a patch, we can use `createPatch` to clean up our mesh. Listing 192 shows an empty `createPatchDict` file, which is the bare minimum to be able to run `createPatch` without error.

Hence, if we run `createPatch` with such an empty `createPatchDict` file, `createPatch` does nothing except remove patches with zero faces.

```
/*-----* C++ -----*/
| ====== |
| \ \ / F ield | OpenFOAM: The Open Source CFD Toolbox |
| \ \ / O peration | Version: 8 |
| \ \ / A nd | Web: www.OpenFOAM.org |
| \ \ / M anipulation |
\*-----*/
FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    object       createPatchDict;
}
// * * * * *
```

¹⁰⁰We could do, if we actually ran the case twice, once for each decomposition.

```

pointSync false;

// Patches to create.
patches
(
);

// ****

```

Listing 192: An empty `createPatchDict`

Listing 193 shows the patch list reported by `checkMesh` after an axi-symmetric mesh has been extruded from a patch. Note the presence of an empty patch, i.e., a patch with zero faces.

```

Checking patch topology for multiply connected surfaces...
Patch      Faces      Points      Surface topology
inlet       30         61          ok (non-closed singly connected)
outlet      30         61          ok (non-closed singly connected)
walls        270        542         ok (non-closed singly connected)
axis         0          0           ok (empty)
front        8100       8401        ok (non-closed singly connected)
back         8100       8401        ok (non-closed singly connected)

```

Listing 193: The patches listed by `checkMesh` of an axi-symmetric mesh after extrusion from a patch.

3

Running `createPatch -overwrite` with an empty `createPatchDict`, as shown in Listing 192, removes the patch with zero faces from the mesh. If we do not remove this patch, OpenFOAM would require us to specify boundary conditions for it.

```

Checking patch topology for multiply connected surfaces...
Patch      Faces      Points      Surface topology
inlet       30         61          ok (non-closed singly connected)
outlet      30         61          ok (non-closed singly connected)
walls        270        542         ok (non-closed singly connected)
front        8100       8401        ok (non-closed singly connected)
back         8100       8401        ok (non-closed singly connected)

```

Listing 194: The patches listed by `checkMesh` of an axi-symmetric mesh after running `createPatch -overwrite` with an empty `createPatchDict`.

Since the release of OpenFOAM version 10¹⁰¹, this removal of zero sized patches works only for non-constraint type patches. Thus, one might need to first change the patch's type to `patch` to make this clean-up work.

30.9 *stitchMesh*

`stitchMesh` is a tool to combine unconnected mesh regions by “stitching” two patches together. These patches need to at least partially overlap. There are several options for `stitchMesh` to operate.

Integral this option is used by default. The description of `stitchMesh` says on this mode of operation: “*integral* match: where the surfaces on both patches exactly match but the individual faces not”

Perfect this option is enabled by using the command line argument `-perfect`, and it is used when the two involved patches are a perfect fit. Note, that this option comes with tight tolerances.

Partial this option is enabled by using the command line argument `-partial`, and it is used when the two involved patches are not the same size and one only partially covers the other.

30.10 *tetDecomposition*

The mesh manipulation tool `tetDecomposition` is part of the OpenFOAM variant `foam-extend`¹⁰², and there is no comparable tool within the foundation release of OpenFOAM at the time of writing.

¹⁰¹See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/989cf27554bc9c80693c91b564eeb1688e9dea2e>.

¹⁰²<http://www.foam-extend.org/>

This tool takes an OpenFOAM mesh, computes the tet-decomposition and writes the resulting mesh to disk. Figures 104 and 105 illustrate how this tool works. The faces of the initial cell is decomposed into triangles. With such a triangle and the centroid of the cell, a sub-tetrahedron can be created.

Depending on the original mesh, the number of cells of the resulting mesh can rise dramatically. The single tetrahedron of Figure 104 is decomposed into 12 sub-tetrahedra. The initial hexahedron of Figure 105 is decomposed into 24 tetrahedra.

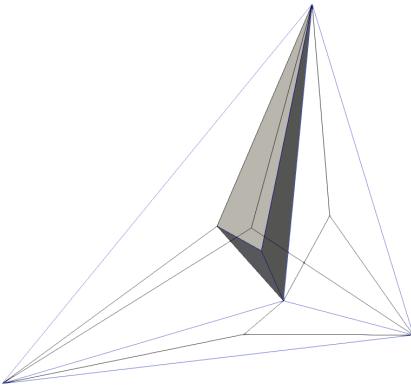


Figure 104: A tet-decomposed tetrahedron: the original tet-cell is outlined in blue, the face-decomposition is outlined in black, and one of the resulting sub-tets is shown in grey.

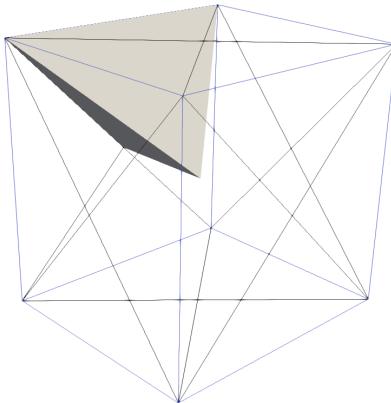


Figure 105: A tet-decomposed hexahedron: the original hex-cell is outlined in blue, the face-decomposition is outlined in black, and one of the resulting sub-tets is shown in grey.

All roads lead to FOAM

With the big number of tools included with OpenFOAM and also the surrounding bits and pieces of software, you should not be surprised to learn that there is also an alternative way to achieve a tetrahedralisation of an OpenFOAM mesh using completely different tools. See Section 61.4.1 for an alternative approach.

30.10.1 A note on compatibility

The tool `tetDecomposition` is from the foam-extend release of OpenFOAM, which has diverged a bit from the other releases of OpenFOAM. Listing 195 shows the error message of `tetDecomposition` when it is applied to a mesh created by OpenFOAM-12. The problem is caused by the missing `version` field in the file headers

of the mesh files. The foundation release of OpenFOAM has changed to treating this entry as optional since OpenFOAM-9¹⁰³.

```
--> FOAM FATAL IO ERROR:  
keyword version is undefined in dictionary "/home/user/OpenFOAM/user-12/run/meshing/myCase/  
constant/polyMesh/points"  
  
file: /home/user/OpenFOAM/user-12/run/meshing/myCase/constant/polyMesh/points from line 10 to  
line 13.  
  
From function const Foam::entry& Foam::dictionary::lookupEntry(const Foam::word&, bool,  
bool) const  
in file db/dictionary/dictionary.C at line 440.
```

FOAM exiting

Listing 195: The error message printed by `tetDecomposition` when being applied to a mesh created by OpenFOAM-12.

The ESI-release of OpenFOAM still writes the version field in the file headers. Thus, using OpenFOAM-v2406 to create the underlying mesh allowed us to use `tetDecomposition` on the resulting mesh.

30.10.2 A cautionary note on mesh quality

Your author has recently experienced something odd tangentially related to `tetDecomposition`. First, a mesh was created by extruding an STL surface mesh. The resulting mesh was to be decomposed into tets. However, decomposition stopped with a segmentation fault, which is shown in Listing 196.

Listing 196, unfortunately, is not very helpful. At first, the correct functioning of our foam-extend installation was questioned. However, testing showed it worked perfectly fine.

The underlying cause of the problem was a duplicate triangle in the STL mesh, which was used in creating the mesh in the first place. `extrudeMesh` did not complain in any way, and dutifully wrote the mesh to disk.

`surfaceCheck` revealed an illegal triangle in the STL surface mesh. Treating the STL surface mesh using `surfaceClean` fixed the STL surface mesh, which later allowed `extrudeMesh` a valid mesh, which could be decomposed.

```
/*-----*  
| ======  
| \\\ / F ield | foam-extend: Open Source CFD  
| \\\ / O peration | Version: 5.0  
| \\\ / A nd | Web: http://www.foam-extend.org  
| \\\ / M anipulation | For copyright notice see file Copyright  
\\*-----*/  
  
Build : 5.0-77674d7709ed  
Exec : tetDecomposition  
Date : Jan 02 2025  
Time : 18:30:17  
Host : "host"  
PID : 32006  
CtrlDict : "/home/user/OpenFOAM/user-12/run/meshing/myCase/system/controlDict"  
Case : /home/user/OpenFOAM/user-12/run/meshing/myCase  
nProcs : 1  
sigFpe : Enabling floating point exception trapping (FOAM_SIGFPE).  
allowSystemOperations : Disallowing user-supplied system call operations  
  
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //  
Create time  
  
Create mesh for time = 0  
  
Speicherzugriffsfehler (Speicherabzug geschrieben)
```

Listing 196: The error ending `tetDecomposition` when being applied to an invalid mesh.

¹⁰³See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/01494463d068d66ab94efc4984a1148f2b4652cb>

Thus, when faced with errors like these, investigate all parts of the process chain. In the example discussed here, the culprit was the STL mesh, which is two steps removed in our sequence of event from the failing tet decomposition. This episode also shows the utility of having multiple installations and releases of OpenFOAM on your computer.

30.11 decomposePar

The tool `decomposePar` is used to divide the domain for a parallel simulation run into smaller sub-domains.

30.11.1 Visualize the decomposition

The tool `decomposePar` has the command-line option `-cellDist`, which causes `decomposePar` to write the cell distribution as a field to disk. This cell distribution can then later be re-used with the `manual` decomposition method, or be visualized using ParaView. For this purpose, `decomposePar` writes a `volScalarField` and a `labelList` with the indices of the sub-domains.

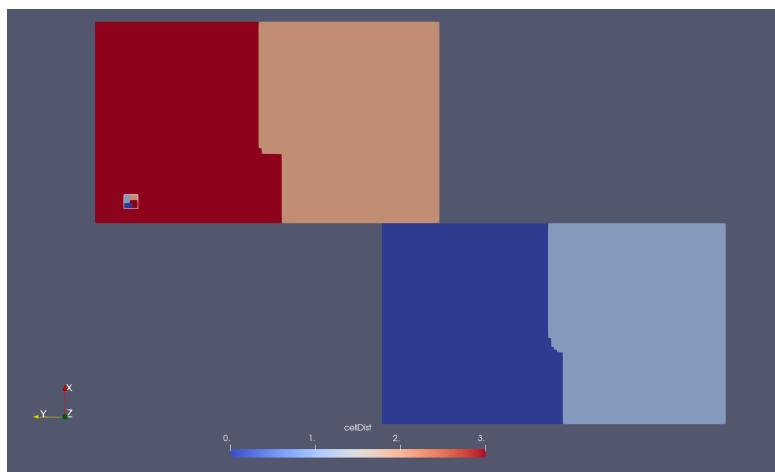


Figure 106: The cell distribution of a multi-region case, with 2 regions and 4 sub-domains for parallel processing. The small region outlined in white is the solid region, the surrounding larger region is the fluid region of this case. Each sub-domain (colour-coded from 0 to 3) is assigned a chunk of each region.

30.12 mirrorMesh

`mirrorMesh` is, similar to `extrudeMesh`, a mesh manipulation tool that is somewhere between mesh manipulation and mesh creation. This tool is controlled by entries in the file `system/mirrorMeshDict`. The set of parameters is quite limited, since we only need to provide a definition for the plane which is to act as the mirror, and a tolerance.

Listing 197 shows an example of a `mirrorMeshDict`, which consists of a plane definition (here we have three possible methods to choose from), and the tolerance.

```

planeType          pointAndNormal;

// Overall domain boundingBox: (0 0 0) (0.1 0.1 0.01)

pointAndNormalDict
{
    basePoint      (0.0 0.0 0.01);
    normalVector   (0 0 1);
}

// plane equation: ax + by + cz + d = 0
planeEquationDict
{
    a    0;
    b    0;
}

```

```

    c    1;
    d   -0.01;
}

embeddedPointsDict
{
    point1  (0 0 0.01);
    point2  (1 0 0.01);
    point3  (0 1 0.01);
}

planeTolerance      1e-5;

```

Listing 197: All the possible entries in the file `mirrorMeshDict` to mirror the initial mesh around an $x - y$ plane with a z -component of $z = 0.01$.

Potential pitfall: set and zones may break my bones

`mirrorMesh` does not apply the mirroring operation on the existing sets and zones of the mesh. This can be an issue depending on whether an existing `cellSet` or `cellZone` needs to be mirrored as well. If this is not necessary, users should remove all sets and/or zones prior to mirroring to avoid confusion.

In Figure 107, we see the result of the following sequence of operations: create the mesh using `blockMesh`, extrude a patch to grow a number of cell-layers, and finally mirror the mesh. The extrusion operation created the `cellSet addedCells`, which was not mirrored by `mirrorMesh`.

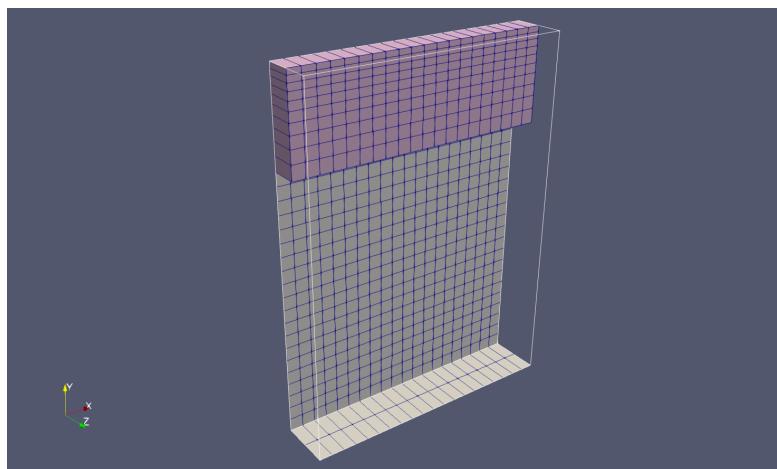


Figure 107: A cellSet after running `mirrorMesh` to mirror the mesh using the $x - y$ plane.

31 Combined mesh generation operations

Sometimes it is necessary to relegate certain tasks to certain tools, and split the work among several tools in some sort of *one tool for one task* UNIX philosophy fashion. Here, we showcase some examples of mesh-creation tool-chains that result in acceptable meshes that would otherwise, using a single tool, not be possible.

31.1 Example: complex pipe

Figure 108 shows a two-part mesh that was created using a mix of methods. In the centre, there is a section of pipe into which a smaller pipe enters from the side and which features a 90 degree bend such that it runs coaxial to the larger pipe. This center section was created as an all-tet mesh in Salome with additional wall layers at the wall patches. In a second step, the dual-mesh was created by *polyDualMesh*.

The upstream section is a simple section of pipe, which was created by extruding the upwind-facing patch using *extrudeMesh*. These two sections form the first part of the mesh. The second part was entirely created using Salome by means of unstructured 2D Netgen meshes and extrusion. These two mesh parts were then connected using *stitchMesh*.

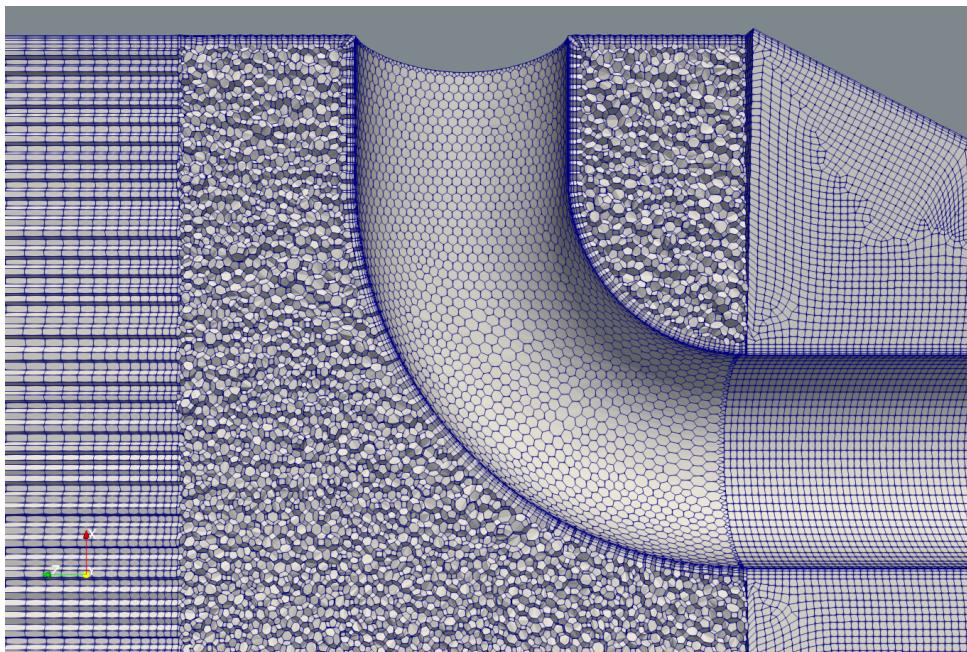


Figure 108: A mesh created by a mix of methods.

31.2 Polyhedral meshes and wall layers and concave edges

At the time of writing, when having to deal with concave edges one is pretty much forced to decide whether to have wall layers or to use *polyDualMesh*. However, if we use a base mesh without wall layers and manage to create the wall layer after applying *polyDualMesh*, then we might succeed.

Figure 109 shows a mesh which started out as an all-tet mesh created by Salome. Next, we created the dual-mesh using *polyDualMesh*. At this stage it was vital to use the `-concaveMultiCells` command line option of *polyDualMesh* to ensure that no single cell wraps around the concave edge. Furthermore, we also applied *combinePatchFaces* to clean-up the dual-mesh. Finally, the wall layer was created by *snappyHexMesh* using only its `layerAddition` stage.

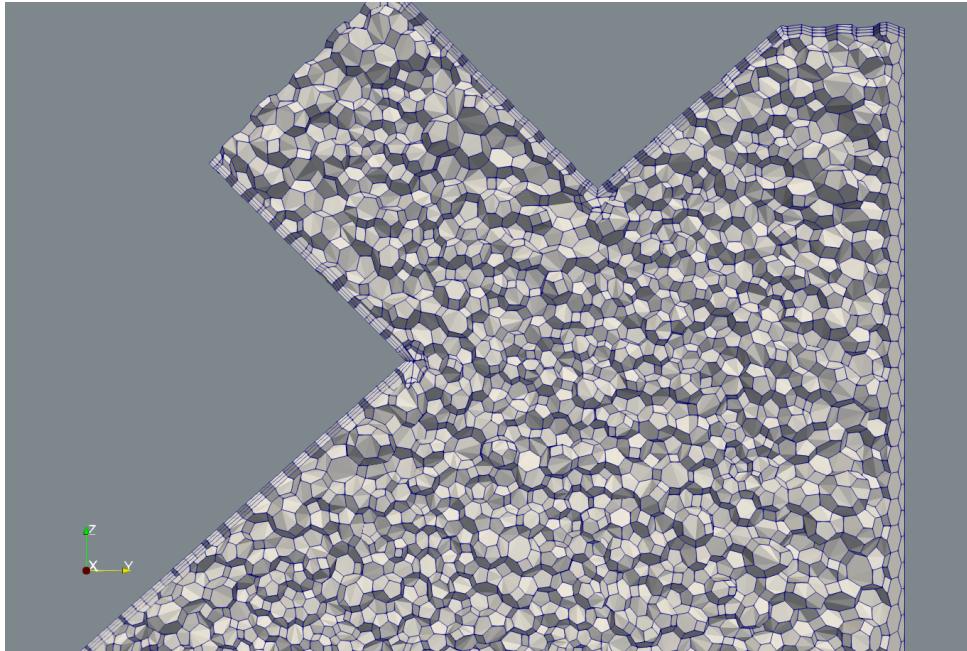


Figure 109: A wall layer at a concave edge.

In contrast to the approach discussed in Section 23.2.1, which aimed at the same result but failed, we altered the sequence of events. Thus, our successful workflow is as follows:

1. Create an all tet-mesh without boundary layers. Here, we used Salome's Netgen meshing algorithm.
2. Create the dual-mesh using polyDualMesh.
3. Create the boundary layers on the polyhedral mesh. Here, we used snappyHexMesh.

31.3 Combining mesh parts vs. boundary layers

It was observed, that stitching meshes with subsequent collapsing of remaining edges and faces is greatly helped, if we stitch mesh parts without boundary layers and then create the boundary layers for the whole mesh. This sequence of events leaves larger cells for the stitching procedure compared to the case if we create boundary layers for the mesh parts individually and then try to combine the parts by stitching.

31.3.1 Creating the boundary layer for each part prior to joining

Figure 110 shows two mesh parts, which already have boundary layers created. After stitching the meshes, some remnants of the former patches remain. These need to be eliminated by using collapseEdges. With the boundary layer already being created, collapseEdges has “less freedom” to do its work, since it can deform the wall-adjacent cells “only so much” before hitting some limits. Hence, the opening statement, that your trusted author has made the observation that joining meshes without boundary layers is easier.

With boundary layers in place, you may need to play longer around with tolerances and other settings to achieve full elimination of all remnant sliver faces. This, i.e., the fact that there always were some remaining faces which could not be collapsed, caused the author to try the other approach: joining first and creating the boundary layer later, which will be discussed right after this section.

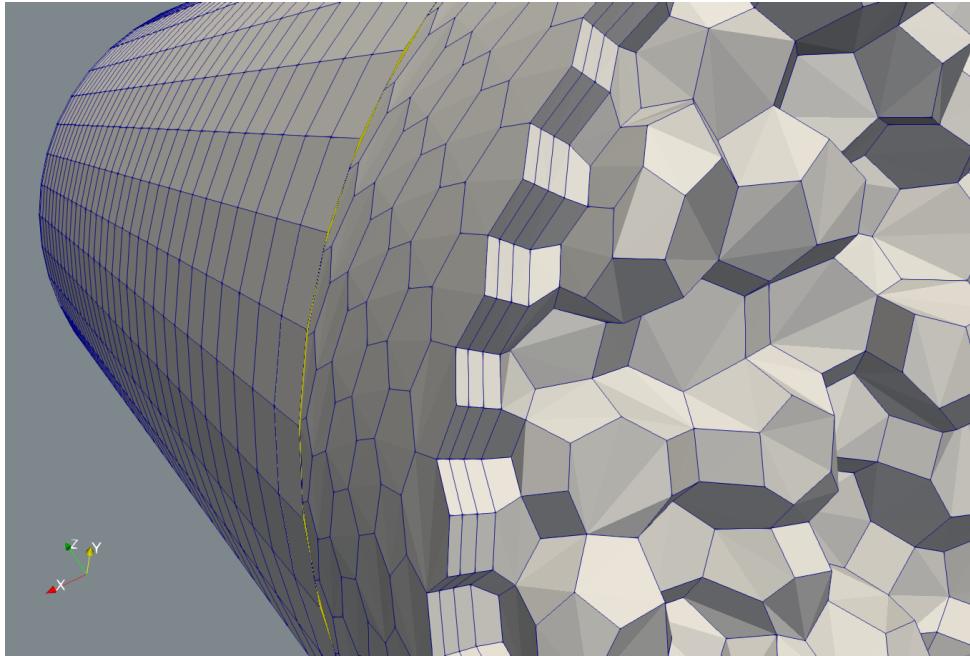


Figure 110: A wall layer for a mesh consisting of a polyhedral part and an all-hex part. This boundary layer was created for each part individually. The yellow slivers are the remnants of the former patches that were stitched. Note, that this image shows an intermediate state, prior to using *collapseEdges* to eliminate these slivers.

31.3.2 Creating the boundary layer last for the joined mesh

Leaving boundary layer creation as the last step also has the advantage, that we get a continuous boundary layer when the boundary layer stretches across both parts.

Figure 111 shows such a boundary layer, which was created for a pipe leading into a vessel with a complex shape. The pipe was meshed using `blockMesh`, since it was a simple enough geometry. The vessel, on the other hand, did not lend itself for meshing with `blockMesh`. Its mesh was created as an all-tet mesh by Salome, and was then converted into a polyhedral mesh using `polyDualMesh`.

By creating the boundary layer last, we avoided not only having to deal with remnants of the patches that were stitched. We also moved the discontinuity of the mesh slightly away from the wall. At least the cells of the boundary layer are perfectly matched to each other across the seam.

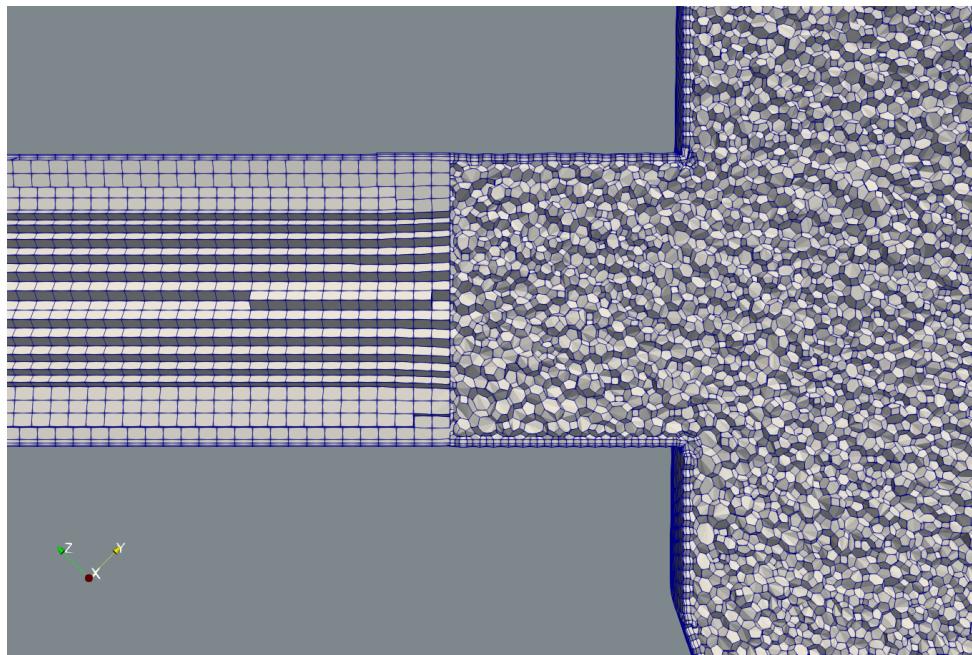


Figure 111: A wall layer for a mesh consisting of a polyhedral part and an all-hex part. This boundary layer was created after combining the two parts using *snappyHexMesh*.

32 Surface mesh manipulation tools

OpenFOAM ships with a number of surface mesh manipulation tools. A probable use-case for this kind of tools is doing some preprocessing on STLs prior to creating a mesh with *snappyHexMesh* or *cfMesh*.

32.1 surfaceAdd

This tool can be used to merge two STLs into one file. With the command line switch `-mergeRegions` regions with an equal name get joined into one region. Otherwise the two regions would remain separate, regardless of having the same name.

```
surfaceAdd -mergeRegions input1.stl input2.stl out.stl
```

Listing 198: Usage of `surfaceAdd` when joining two STL files.

32.2 surfaceSubset

With this tool a subset of an STL can be extracted. Via the `surfaceSubsetDict` various conditions can be specified to define the subset. The user provides the STL to operate on (`input.stl`) and a file name for the subset to be stored in (`outSubset.stl`). The faces of the subset get removed from the original STL.

```
surfaceSubset surfaceSubsetDict input.stl outSubset.stl
```

Listing 199: Usage of `surfaceSubset` when extracting a certain subset from an STL.

32.3 surfaceFeatureExtract

This is a tool to extract features from an STL. E.g. *snappyHexMesh* pays extra attention to geometric features which are explicitly provided, *surfaceFeatureExtract* is a tool to generate the necessary data. The tool is controlled by the `surfaceFeatureExtractDict`. Surface feature extraction is controlled by a user-provided feature angle, which is used to determine whether an edge between two surface elements constitutes a feature edge, or not.

This tool writes the feature edges into an `*.eMesh` file located in the `constant/triSurface` folder.

In the file `surfaceFeatureExtractDict` we can enable the switch `writeObj`, which causes the tool to write all sorts of extracted data into `*.obj` files located in the `constant/extendedFeatureEdgeMesh` folder. These files can be viewed in ParaView to assess whether all surface features have been correctly and completely been extracted.

32.4 surfaceFeatureConvert

This tool can be used to convert `*.eMesh` files to `*.vtk` files to view them in ParaView. This is important when trying to find the proper settings, e.g. the feature angle for the file `surfaceFeatureExtractDict`.

32.5 surfaceTransformPoints

This tool is the surface mesh equivalent to the tool `transformPoints`, see [30.1](#), which can be used to scale, translate and rotate surface meshes. Apart from the obvious transformation options, this tool expects two file names: first, the input file; and second, the output file.

32.6 surfaceClean

Some tools are happy create an STL surface mesh from any data. However, OpenFOAM or other tools, might have some minimum requirements on the STL quality. One example of a bad STL property is the existence of nearly collapsed triangles, i.e., a triangle that features two near-coincident vertices. Such bad triangles are easily missed by visual inspection of the STL mesh in e.g. ParaView.

Listing [200](#) shows an example of using `surfaceClean` to fix an STL mesh, which caused LIGGGHTS to abort due to bad mesh quality.

```

user@host:~$ surfaceClean input.stl 0.001 output.stl
... some output removed for clarity

Reading surface "input.stl"
Collapsing all triangles with edges or heights < 0.001
Writing result to "output.stl"

Reading surface from "input.stl" ...

Triangles      : 3502
Vertices       : 1799
Bounding Box : (-5.11463 -5.11682 -0.61377) (5.11755 5.11682 0.28866)
Collapsing triangles to edges ...

Collapsing triangle 2845 to edge mid (5.11755 -6.26719e-16 0.13013)
collapseEdge : collapsing 1 triangles
collapseEdge : collapsing 0 triangles
collapseEdge : collapsing 0 triangles
Detected 0 regions of faces to be collapsed

collapseBase : splitting 0 triangles

Resulting surface:
Triangles      : 3501
Vertices       : 1798
Bounding Box : (-5.11463 -5.11682 -0.61377) (5.11755 5.11682 0.28866)

Writing refined surface to "output.stl" ...

End

user@host:~$
```

Listing 200: Using `surfaceClean` to clean-up an STL surface mesh with one bad triangle.

32.7 Third party surface manipulation tools

32.7.1 `surfaceFeatureEdges`

With this tool, provided by `cfMesh` (see Section 20), feature edges can be extracted from a surface mesh file, e.g. an STL.

```
surfaceFeatureEdges -angle 30 input.stl out.fts
```

Listing 201: Usage of `surfaceFeatureEdges` when extracting feature edges from an STL.

32.7.2 `FMSToVTK`

The tool `FMSToVTK` can be used to convert the `*.fms` files created by the tool `surfaceFeatureEdges` to the VTK format. Thus, the user can review how well the feature edges have been identified by `surfaceFeatureEdges`. This is important when trying to find the proper setting for the feature angle, which is passed with the `-angle` parameter.

This tool, provided by `cfMesh` (see Section 20).

32.8 The Linux command line

When doing some pre-processing with ASCII STLs the linux command line offers some nice features. Listing 202 shows the basic syntax of an STL file in ASCII format. STLs can be stored on harddisk either in ASCII, i.e. in plain text, or in binary format (non-human-readable). An STL file consists of solids, which are defined by their bounding surface.

```

solid SOLIDNAME
  facet normal X Y Z
    outer loop
      vertex X Y Z
      vertex X Y Z
      vertex X Y Z
    endloop
  endfacet
...
endsolid

```

Listing 202: The basic syntax of an STL in ASCII format. See [https://en.wikipedia.org/wiki/STL_\(file_format\)](https://en.wikipedia.org/wiki/STL_(file_format)) for more on this.

32.8.1 Renaming solids

Certain CAD tools do not offer the feature to name a part. E.g. OpenSCAD names the exported STL solid `OpenSCAD_Model`. If our STL pre-processing based on an STL generated by OpenSCAD yields an STL file per patch, a likely result when using `surfaceSubset`, we end up with a number of STLS, containing each one solid named `OpenSCAD_Model`. Now, we need to assign proper names to the solids, i.e. the STL solid of the file `inlet.stl` should be named `inlet`.

When the STL is in ASCII format, we can use `sed`¹⁰⁴ to perform a simple text replacement. Since an STL is very unlikely to contain the string `OpenSCAD_Model`, we simply can tell `sed` to replace every occurrence of `OpenSCAD_Model` with `inlet`.

```
sed -i s/OpenSCAD_Model/inlet/g inlet.stl
```

Listing 203: Renaming STL an solid with `sed`.

32.8.2 Joining STL files

If our pre-processing left us with a large number of STL files, e.g. an STL file for each patch, which is a likely result when using `surfaceSubset`, we might need to join these STLS, e.g. because the meshing tool expects only one STL to contain all the information. Joining text files is a task easily done from the command line with the tool `cat`¹⁰⁵, however, this could also be done using `surfaceAdd`. Other than with `surfaceAdd`, joining STLS with this approach is limited to STLS containing different solids.

Listing 204 shows how to join three STLS, each containing one solid, i.e. the information of one patch. The first line is simply a copy operation. Alternatively, we might use `cp` or `mv` for the first operation. Note, that the resulting STL gets written to a different folder, `constant/triSurface` is a folder in which some meshing tools expect STLS. The second and third lines show how to append the output of `cat` to the specified file.

The difference between the first and the following lines is the redirection operator (`>` vs. `>>`), see e.g. [https://en.wikipedia.org/wiki/Redirection_\(computing\)](https://en.wikipedia.org/wiki/Redirection_(computing)). The `>` operator simply redirects the output to the specified file, if this was used in the second line, then the contents from the first line would get overwritten in `myDomainMesh.stl`. Using the `>>` operator redirects and appends the output to the specified file. Using the `>` operator in the first line ensures to overwrite an eventual existing file.

```
cat walls.stl > constant/triSurface/myDomainMesh.stl
cat inlet.stl >> constant/triSurface/myDomainMesh.stl
cat outlet.stl >> constant/triSurface/myDomainMesh.stl
```

Listing 204: Joining STL files with `cat`.

¹⁰⁴<https://www.gnu.org/software/sed/manual/sed.html>

¹⁰⁵[https://en.wikipedia.org/wiki/Cat_\(Unix\)](https://en.wikipedia.org/wiki/Cat_(Unix))

33 Initialize Fields

33.1 Basics

There are two ways to define the initial value of a field quantity. The first is to set the field to a uniform value. Listing 205 shows the O/U file of the *cavity* tutorial. There the internal field is set to a uniform value.

If a non-uniform initialisation is desired, then a list of values for all cells is needed instead. Listing 213 shows some lines of such a definition. Entering such a nonuniform list by hand would be very tiresome. To spare the user of such a painful and exhausting task, there are some tools to provide help.

```
/*-----* C++ -----*/
| ====== | OpenFOAM: The Open Source CFD Toolbox
| \ \ / F ield | Version: 2.1.x
| \ \ / O peration | Web: www.OpenFOAM.org
| \ \ / A nd |
| \ \ / M anipulation |
\*-----*/
FoamFile
{
    version      2.0;
    format       ascii;
    class        volVectorField;
    object       U;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * *
dimensions      [0 1 -1 0 0 0];

internalField    uniform (0 0 0);

boundaryField
{
    movingWall
    {
        type          fixedValue;
        value         uniform (1 0 0);
    }

    fixedWalls
    {
        type          fixedValue;
        value         uniform (0 0 0);
    }

    frontAndBack
    {
        type          empty;
    }
}
// **** -----
```

Listing 205: The file O/U of the *cavity* tutorial

33.2 *setFields*

setFields is a utility that allows to define geometrical regions within the domain and to assign field values to those regions. *setFields* reads this definitions from a file in the *system*-directory – the *setFieldsDict*. To initialize the field quantities *setFields* has to be executed after creating the mesh. *setFields* needs to read all files defining the mesh¹⁰⁶.

In Listing 206 a box is defined in which the field *alpha1* is set to a different value.

```
/*-----* C++ -----*/
| ====== | OpenFOAM: The Open Source CFD Toolbox
```

¹⁰⁶Only the file *neighbour* can be missing for *setFields* not to crash.

```

| \\ / O peration | Version: 2.1.x
| \\ / A nd | Web: www.OpenFOAM.org
| \\ / M anipulation |
\*-----*/
FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    object       setFieldsDict;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //*
defaultFieldValues
(
    volScalarFieldValue alpha1 1
);

regions
(
    boxToCell
    {
        box (-0.3 -0.3 0) (0.3 0.3 0.26);

        fieldValues
        (
            volScalarFieldValue alpha1 0
        );
    }
);
// ****

```

Listing 206: *setFieldsDict*

33.2.1 Defining regions

In Listing 206 we see the list named `regions` containing dictionaries defining regions in which to set field values. The `boxToCell` dictionary very much resembles something we also can see in the `topoSetDict` dictionary. In fact, `setFields` internally uses the machinery to create cell sets as `topoSet` does. A quick look into the main source files of `setFields` and `topoSet` reveals, that both make use of the class `topoSetSource`, which describes itself in the header file as: *Base class of a source for a topoSet*. All actual cell sources, such as `boxToCell` or `cylinderToCell`, directly inherit from `topoSetSource`. Thus, all cell sources available to `topoSet`, are also available to `setFields`. Such is the beauty of object-oriented programming.

33.2.2 Using sets, zones et al.

While, the annotated `setFieldsDict` only demonstrates the use of `boxToCell`, we can use all sources from `topoSet`, including already existing sets and zones. Note that the syntax is somewhat related to the syntax used in `topoSetDict`.

```

\*-----* C++ -----*/
| ====== |
| \\ / F ield | OpenFOAM: The Open Source CFD Toolbox
| \\ / O peration | Version: 2.1.x
| \\ / A nd | Web: www.OpenFOAM.org
| \\ / M anipulation |
\*-----*/
FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    object       setFieldsDict;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //*
defaultFieldValues
(
    volScalarFieldValue alpha.solid 0

```

```

);
regions
(
    zoneToCell
    {
        zone ore;
        fieldValues
        (
            volScalarFieldValue alpha.solid 0.5
        );
    }
);
// ****

```

Listing 207: An example of a *setFieldsDict* using an already existing cell zone.

33.2.3 Pitfalls

A nice, little collection of what may go wrong.

Geometric region is not part of the domain

If the geometric region, in which to initialise a field with a specified value, lies outside the domain, *setFields* does not issue any warning or error message.

Geometric region covers the whole domain

This may happen if the geometric region is defined with respect to the vertex coordinates found in *blockMeshDict*. When the vertex coordinates are entered in millimeters – and *convertToMeters* is set appropriately – then it may happen, that the geometric region, based on the vertex coordinates in millimeters, is too large by the factor of 1000.

Listing 208 and 209 show the root of such a situation. The plan is to create a box and initialise it in a way, that the domain is half filled with one phase. The definition of the box in the *setFieldsDict* relies solely on the vertex coordinates ignoring the scaling factor *convertToMeters* resulting in a way too large box. After executing *setFields* the domain is completely filled with one phase instead of half filled.

```

convertToMeters 1e-3;

vertices
(
    (0      0      0)
    (50     0      0)
    (50     0      250)
    (0      0      250)
    (0      50     0)
    (50     50     0)
    (50     50     250)
    (0      50     250)
);

```

Listing 208: *blockMeshDict* entry for a box of $50 \times 50 \times 250$ mm

```

regions
(
    boxToCell
    {
        box (0.0 0.0 0.0) (50.0 50.0 125.0);

        fieldValues
        (
            volScalarFieldValue alpha1 0
        );
    }
);

```

Listing 209: *setFieldsDict* entry for a box of $50 \times 50 \times 125$ m

Field not found

If the *setFieldsDict* specifies a field which is not present, then OpenFOAM issues an error message similar to Listing 210. In this case the file *setFieldsDict* was copied from a case which uses the old naming scheme of *twoPhaseEulerFoam*, i.e. *alpha* instead of *alpha1*. See Section 55.2 for further information about the naming scheme. Therefore, the dictionary contained a definition for the field *alpha* which was not present in the *0*-directory.

```
Setting field default values
--> FOAM Warning :
From function void setCellFieldType(const fvMesh& mesh, const labelList& selectedCells,
Istream& fieldValueStream)
in file setFields.C at line 103
Field alpha not found

--> FOAM FATAL IO ERROR:
wrong token type - expected word, found on line 19 the label 1
file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bubbleColumn/system/setFieldsDict::
defaultFieldValues at line 19.

From function operator>>(Istream&, word&)
in file primitives/strings/word/wordIO.C at line 74.

FOAM exiting
```

Listing 210: Missing field

33.3 *mapFields*

mapFields is a utility to transfer field data from a source mesh to target mesh. This may be useful after the mesh of case has been refined and existing solution data is to be used for initialising the case with the refined mesh. *mapFields* preserves the format of the data, if the source data was stored in binary format, the target data will also be binary.

To use *mapFields* the file *mapFieldsDict* has to be existent in the *system* folder of the case¹⁰⁷. *mapFields* expects as the only mandatory argument the path to the source case. The current directory is assumed to be the case directory of the target case. If there is no specification regarding time, the latest time steps of both cases are processes. That means the latest time step of the source case is mapped to the latest time step of the target case.

Listing 211 shows the last lines of output of *mapFields*. With lines like `interpolating alpha` *mapFields* indicates that it is processing some field data. Even when source and target meshes are equal and no interpolation is needed, *mapFields* displays lines like `interpolating alpha` anyway.

```
Source time: 0.325
Target time: 0
Create meshes

Source mesh size: 81000 Target mesh size: 273375

Mapping fields for time 0.325

    interpolating alpha
    interpolating p
    interpolating k
    interpolating epsilon
```

¹⁰⁷In the most basic case *mapFieldsDict* contains no other information than the header and empty definitions. Although this file may seem of no use, it has to exist in the *system* folder, and it has to contain the header and the empty definitions.

```

interpolating Theta
interpolating Ub
interpolating Ua

End

```

Listing 211: Output of *mapFields*

33.3.1 Pitfall: Missing files

mapFields issues no warning or error message when the source case contains no data. Listing 212 shows the output of *mapFields* as the target case contained no *0*-directory. Only the missing lines containing statements like `interpolating alpha` indicate that something is amiss and no field data is processed.

```

Source time: 0.325
Target time: 0
Create meshes

Source mesh size: 81000 Target mesh size: 273375

Mapping fields for time 0.325

End

```

Listing 212: Output of *mapFields*; Missing target *0*-directory

33.3.2 Pitfall: Unsuitable files

In the files containing the field data the values of the boundary fields as well as the values of the internal fields can be entered homogeneously (by the keyword `uniform`) or inhomogeneously (with the keyword `nonuniform`). Inhomogeneous field values have to be entered as a list of values. This list is preceded by the number of entries as well as the nature of the value. Listing 213 shows the beginning lines of the definition of a nonuniform vector field. The general syntax for such a list is the following:

```
nonuniform List<TYPE> COUNT ( VALUES )
```

the list. A wrong value of COUNT leads to reading errors.

If data is to be mapped from a source case, the source case's data will always be stored as a nonuniform list. Otherwise, mapping the data would make no sense, as uniform fields are most easily defined. If the data of the target case is uniform, then mapping makes no problems.

If the data of the target case is nonuniform – for whatever reason – then it is necessary that the nonuniform lists have the same length. Otherwise, *mapFields* will exit with an error message like in Listing 214. The target case should always be set up with uniform fields to avoid such errors. This is most easily done by removing the definition of the internal field. In the tutorials sometimes files with an `.org` file extension can be found. This is a way to preserve the uniform field data in the *0*-directory without causing any trouble.

```

dimensions      [0 1 -1 0 0 0 0];

internalField    nonuniform List<vector>
1600
(
(0.000174291 -0.000171512 0)
(0.000171022 -0.000143648 0)
(-0.000259297 0.000305772 0)
(-0.000380671 0.000374937 0)
(-0.00182755 0.000930701 0)

```

Listing 213: An inhomogeneous internal field definition in the file *0/U*

```

/*-----* C++ -----*/
| ====== | F ield | OpenFOAM: The Open Source CFD Toolbox |
| \ \ / O peration | Version: 2.1.x |
| \ \ / A nd | Web: www.OpenFOAM.org |
| \ \ \ M anipulation | |
\*-----*/
FoamFile
{
version      2.0;
format       ascii;
class        dictionary;
location     "system";
object       mapFieldsDict;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //

patchMap      ( );
cuttingPatches ( );

// ****

```

Listing 215: The file `mapFieldsDict`

```

Mapping fields for time 0.325

interpolating alpha

--> FOAM FATAL IO ERROR:
size 81000 is not equal to the given value of 10125

file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/Case/0/alpha from line 18 to line
      39.

From function Field<Type>::Field(const word& keyword, const dictionary&, const label)
in file /home/user/OpenFOAM-2.1.x/src/OpenFOAM/lnInclude/Field.C at line 236.

FOAM exiting

```

Listing 214: Error message of `mapFields`; unequal number of values

33.3.3 Pitfall: Mapping data from a 2D to a 3D mesh

In this section we deal with some difficulties of the `mapFields` utility. We have finished a simulation on a 2D mesh. The geometry of the 2D case is $20\text{ cm} \times 2\text{ cm} \times 45\text{ cm}$.

Now we want to transfer the 2D data to a 3D mesh to initialise the 3D simulation. The geometry of the 3D simulation is $20\text{ cm} \times 5\text{ cm} \times 45\text{ cm}$. Note the different dimension in y -direction.

Listing 215 shows the `mapFieldsDict` that was used. Because of the great similarity of the geometry, no entries are necessary.

The problem

Figure 112 shows the result of the `mapFields` run. Only the field values inside the 2D domain were altered. The part of the 3D domain that lies outside the 2D domain remains unchanged. This behaviour is not satisfactory.

The work-around

One way to solve this problem would be to choose the 2D domain of a similar size as the 3D domain. However, if the 2D is already finished, then it would take some time to re-simulate the case with a redefined geometry.

Another solution is:

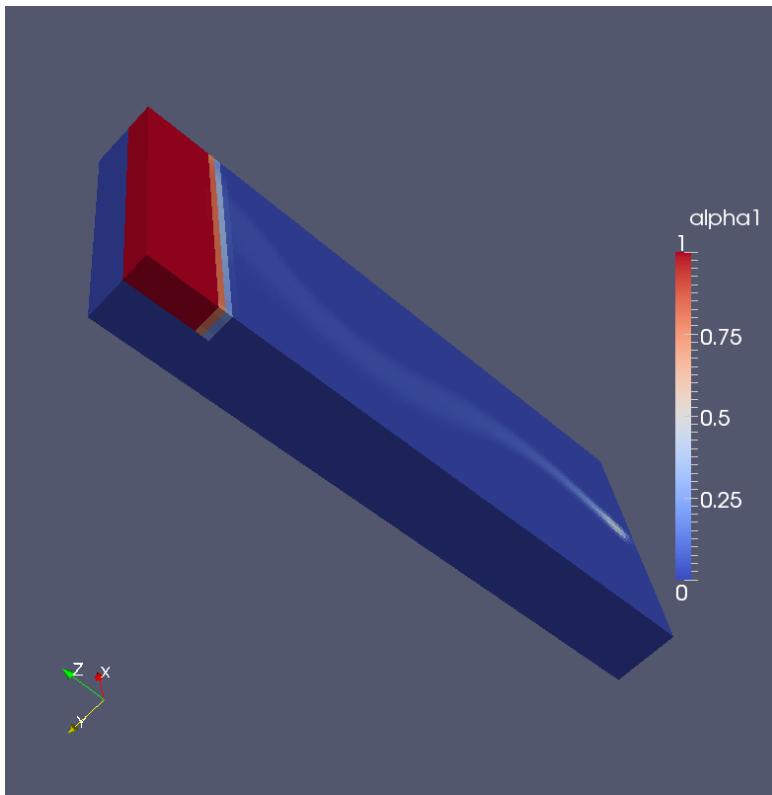


Figure 112: The mapped field

1. define the 3D domain to be of the same size as the 2D domain
2. map the fields
3. redefine the 3D domain to its intended size, without changing the total number of cells

33.3.4 The work-around: Mapping data from a 2D to a 3D mesh

The work-around to the problem of the previous section is rather unelegant. A 2D mesh that has the same depth as the 3D mesh but is discretised with only 1 cell in depth will have a very bad aspect ratio.

A more elegant solution is to transform the mesh after the 2D simulation has finished. In our example, the 2D mesh has the dimensions $20\text{ cm} \times 2\text{ cm} \times 45\text{ cm}$ and the 3D mesh is $20\text{ cm} \times 5\text{ cm} \times 45\text{ cm}$ big.

With the tool *transformPoints* the mesh can be scaled selectively in the three dimensions of space. Listing 216 shows how *transformPoints* can be used to scale the 2D mesh in *y*-direction by the factor of 2.5. After this scaling operation the 2D mesh has the desired dimensions of $20\text{ cm} \times 5\text{ cm} \times 45\text{ cm}$.

```
transformPoints -scale '(1.0 2.5 1.0)'
```

Listing 216: Scaling the 2D mesh in *y*-direction with *transformPoints*

After the mesh transformation the utility *mapFields* can be used to map the field from the scaled 2D mesh to the 3D mesh.

33.3.5 The importance of mapping

The purpose of this example is to highlight the need for the *mapFields* utility. A simulation of the bubble column has been made. Now, the user decides to change the size of the inlet patch. Thanks to the parametric mesh, this can be done easily only by changing some numbers in the file *blockMeshDict.m4*. See Section 17.5 for a discussion on creating a parametric mesh.

After the user changed the coordinates of some points, meshing yields a new mesh with the same number of cells as the old mesh had. Because the number of cells did not change, the data files from the finished simulation

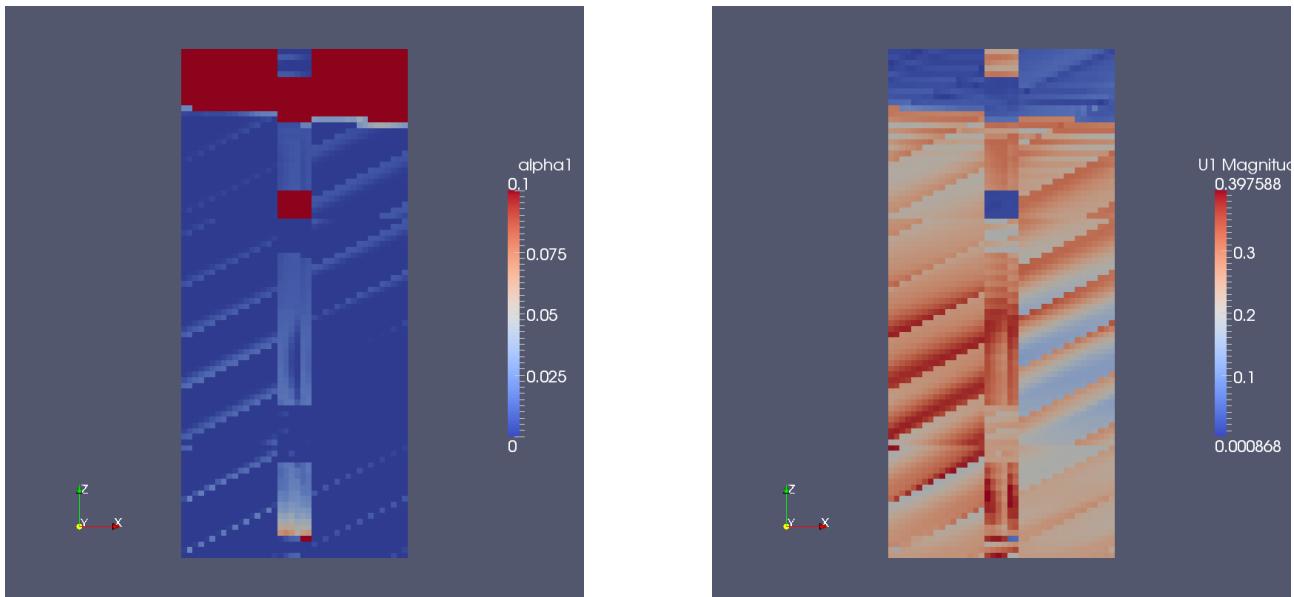


Figure 113: The unmapped fields

fit the new one. The user simply copies the necessary files from the latest time step of the finished simulation to the initial time step of the new simulation.

Starting the simulation resulted in a floating point exception. However, after reducing the time step, the simulation proceeded without any further errors. Figure 113 shows the initial α_1 and U_1 fields of the new simulation. Due to a change in the numbering of the cells, the formerly smooth fields are now completely distorted. The single blocks of the mesh can be distinguished from the figures. This indicates, that OpenFOAM numbers the cells block-wise.

33.3.6 Pitfall: binary files

If the source case has binary data files, then the boundary conditions need to be defined before mapping the fields. Therefore, the boundary conditions need to be defined in a suitable ascii file. Then, the fields can be mapped. Editing a binary file with a text editor may render this file defective.

34 Case manipulation

This section contains a discussion on tools for the manipulation of the simulation case which to not create or modify the mesh or are used for initialisation. While tools used solely for mesh-manipulation might also apply their operations on the data files of OpenFOAM, their primary purpose is the manipulation of the mesh. Thus, we think of them as distinctly different from initialisation tools, which “only” act on the data files, such as `setFields`. Utilities for these tasks have already been discussed in previous sections.

The category of “case manipulation” is a rather artificial one, since the tasks discussed in this section also work on mesh and data files. However, while these tasks might affect both mesh and data files, we deem them different due to their respective simplicity.

A perfect example for this distinction is renaming a boundary or changing the type of a boundary condition. This task applies to both the mesh and the data, the operation clearly does not fall into data initialisation. If we are generous, we might term such an operation as “mesh manipulation”.

The operations and tasks discussed in this section, may apply to only the mesh, to only the data, or both. Hence, we created a distinct category of “case manipulation”.

34.1 `changeDictionary`

The utility `changeDictionary` can be used to modify a dictionary, except those residing in `system`. We can of course manipulate any of our dictionaries using a simple text editor, even from the command line (*emacs*, *vim*, *nano*, etc.).

A possible scenario in which `changeDictionary` comes in handy is when we do spin-up simulations, i.e. run the simulation for a certain time with e.g. reduced inflow and continue afterwards with full inflow¹⁰⁸. This approach might improve the stability of the simulation.

Another case in which `changeDictionary` proves to be quite important is when we want to change boundary value of fields we have gained from a previous simulation. Editing ascii files which measure in the megabytes can be very tiresome with some text editors. If the files are stored in binary, using a text editor might not be an option anymore. In this `changeDictionary` provides a neat way to change boundary values.

Listing 217 shows a simple example of the `changeDictionaryDict`.

```
dictionaryReplacement
{
    U
    {
        boundaryField
        {
            inlet
            {
                type          fixedValue;
                value         uniform (20 0 0);
            }
        }
    }
}
```

Listing 217: A simple `changeDictionaryDict` used to change an inlet velocity

By default `changeDictionary` operates only on dictionaries living in the time step directories. By adding the command line option `-constant` the dictionaries of the `constant` folder can be edited.

34.1.1 A spin-up simulation

In this section we discuss what is termed a spin-up simulation in this manual. This simulation is intended to run without user intervention once the simulation is started. In this case we assume we have set up a simulation with a reduced inflow. Thus, the flow establishes within the domain in a much gentler regime. After the flow is established we increase the inflow to the desired value. Again, the build-up of the flow within the domain

¹⁰⁸In such a scenario we also would need to manipulate `controlDict` to increase the `endTime`. Well, we can't have everything.

happens in a gentler manner, as there is already a slower flow present through out the domain. Thus, we avoid punching the quiescent fluid in the domain with full force at the inlet¹⁰⁹.

Listing 218 shows the `Allrun` script for such a kind of simulation. In Line 11 the solver is run for the first time. Since none of the lines in the script is terminated by the ampersand (&), execution waits for the command of the current line to finish until the next command is invoked. Thus, we save to assume all commands are run in the stated order.

In Line 14 the log-file generated by `runApplication` is renamed (moving a file within a directory is essentially renaming). The reason for this operation is, that `runApplication` checks if there is already a log present. If there is, `runApplication` does not run the specified application.

In Line 15 `changeDictionary` is called. This is the step in which, in our example, we increase the inlet velocity. In Line 16 we use the GNU tool `sed` to edit `controlDict`¹¹⁰.

In Line 19 we call the solver for the second time. Here it is crucial that the keyword `startAt` is set to `latestTime` in `controlDict`.

In Line 20 we apply the same renaming to the solver-log of the second run. This is not necessary in principle, however, if we are to perform to automated processing of the logs, then a consistent naming scheme might be very helpful.

```

1 #!/bin/sh
2 cd ${0%/*} || exit 1      # run from this directory
3
4 # Source tutorial run functions
5 . $WM_PROJECT_DIR/bin/tools/RunFunctions
6
7 # Create the mesh using blockMesh
8 runApplication blockMesh
9
10 # Run the solver
11 runApplication pimpleFoam
12
13 # prepare second run
14 mv log.pimpleFoam log.pimpleFoamRun01
15 runApplication changeDictionary
16 sed -i 's/endTime          20/endTime          40/g' system/controlDict
17
18 # Run the solver again
19 runApplication pimpleFoam
20 mv log.pimpleFoam log.pimpleFoam02
21
22 # ----- end-of-file

```

Listing 218: The `Allrun` script of a spin-up simulation

The `Allrun` script was applied to a slightly modified *pitzDaily* tutorial case. A appropriate `changeDictionaryDict` file Listing 217 was added to the `system` directory, otherwise the tutorial is untouched. Figure 114 shows the flow field after `changeDictionary` was called. The increased inlet velocity is displayed as well as the established flow from the initial run with an inlet velocity of (10 0 0).

34.1.2 Change boundary types

Another, very handy use of `changeDictionary` is changing the type of certain boundaries. This may be necessary when using imported meshes. Some mesh formats or meshing tools do not support to assign patch-types to certain boundaries. Thus, when importing these meshes into OpenFOAM, all patches are of the general `patch` type. Hence, there is the necessity to change the patch type of the wall patches to the type `wall`. This could be done by manually editing the file `boundary`, yet this approach does not scale – what if we have hundreds of wall patches – and it is easy to forget this step.

¹⁰⁹Such a simple kind of thing could also be achieved with time-dependent boundary conditions. However, there are solvers which do not support time-variant boundary conditions, or we want to do something nastier, which can't be achieved with time-variant boundary conditions.

¹¹⁰We could also do the edit manually with any text editor, as `controlDict` will never reach megabytes or be stored in binary format. However, the whole idea of the spin-up simulation idea is to avoid manual intervention.

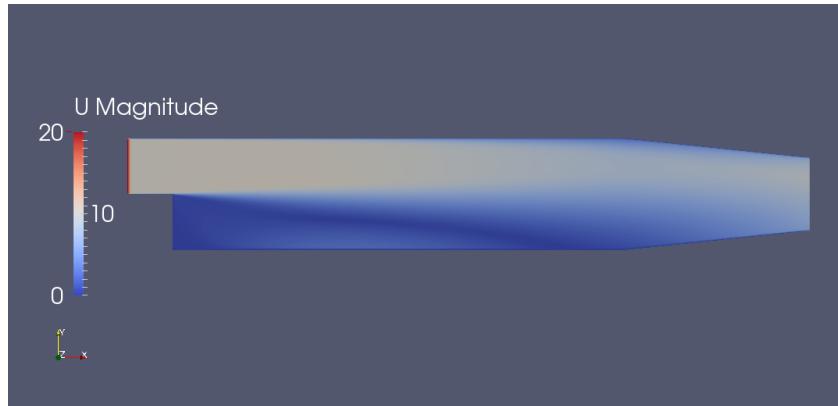


Figure 114: The established flow field and the increased inlet boundary condition of the *pitzDaily* tutorial case at $t = 1\text{ s}$

Using *changeDictionary* to change the patch type is a scalable solution, i.e. once the changes are specified in the file `changeDictionaryDict`, there is no additional work if we do the whole process of importing the mesh and changing the patch type all over again.

The second main advantage of using *changeDictionary* instead of manual editing, is that using a tool is scriptable, whereas manual file manipulation is not. Scripting ensures that no intermediate operation is omitted in any process.

```
boundary
{
    walls
    {
        type      wall;
    }
}
```

Listing 219: A simple `changeDictionaryDict` used to change the type of a patch *walls* to *wall*.

34.2 foamDictionary

The `foamDictionary` utility tool was introduced with the release of OpenFOAM-4.0 in 2016¹¹¹. We can use this tool to access dictionary entries for both reading and writing. With the release of OpenFOAM-7¹¹², `foamDictionary` is the replacement of `changeDictionary`.

```
foamDictionary -entry endTime -set $newEnd1 system/controlDict
```

Listing 220: Using `foamDictionary` to set a new end time for the simulation in `controlDict`.

34.2.1 Access entries within nested dictionaries

We can also access entries within nested dictionaries. See Listing 221, which shows the general syntax.

```
foamDictionary -entry dictionary.dictEntry -value dictionaryFile
```

Listing 221: Using `foamDictionary` to read a value from a dictionary within a dictionary file, using the dot-syntax.

Note, that the scoping operator used to separate the names of dictionary and sub-dictionary respectively the entry changed over time. Listing 221 shows the dot-syntax, which was standard in OpenFOAM until it was

¹¹¹See <https://openfoam.org/release/4-0/>

¹¹²See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/bd93bf10c82a264c70f7798ea0a0af7bfc65e4a4>.

replaced by the slash-syntax with the release of OpenFOAM-9¹¹³. Listing 222 is an update of Listing 221 which reflects the change in dictionary access. .

```
foamDictionary -entry dictionary/dictEntry -value dictionaryFile
```

Listing 222: Using `foamDictionary` to read a value from a dictionary within a dictionary file, using the later slash syntax.

The change in dictionary access syntax was motivated by the developers as follows¹¹⁴:

A new optional "slash" scoping syntax is now provided which is more intuitive than the current "dot" syntax as it corresponds to the common directory/file access syntax used in UNIX, and avoids limitations of the "dot" ...

34.2.2 Access entries within lists

Using `foamDictionary` to modify entries of dictionaries and sub-dictionaries is straight-forward. However, sometimes we encounter lists of dictionaries, such as the `boundaries` file of the mesh. Listing 223 shows such a list, which contains a patch definition we would like to modify.

```
5
(
    // ...

    wall
    {
        type           wall;
        inGroups       List<word> 1(wall);
        nFaces         474;
        startFace     94042;
    }
)
```

Listing 223: A typical patch definition in the `boundary` file with an `inGroups` entry.

Listing 224 shows the command which allows us to remove the `inGroups` entry from the patch definition shown in Listing 223. There, we address the list by the name `entry0`.

```
foamDictionary -entry entry0/wall/inGroups -remove constant/polyMesh/boundary
```

Listing 224: Using `foamDictionary` to remove the `inGroups` entry from the `wall` patch.

Using `entry0` is not immediately obvious, however, we find it hinted at in the header file of the class `dictionaryListEntry`¹¹⁵:

Read/write List of dictionaries.

The List entries get stored in a dictionary which itself is stored in the parent dictionary with keyword 'entryDDD' where DDD is the position in the parent dictionary. The printing is again in List format - the keyword is only printed as comment. Can be used to e.g. manipulate poly-Mesh/boundary files.

¹¹³See <https://openfoam.org/release/9/>

¹¹⁴See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/a7b842569064ede1574a77210b731904a206182a>

¹¹⁵This was added with the release of OpenFOAM-5, see <https://github.com/OpenFOAM/OpenFOAM-dev/commit/a7256d6fa9f8f54c5aa2f14d21236659d1fc44d3>.

35 The allmighty Linux Terminal

This section covers case manipulation we can do with the tools available in the Linux Terminal. The reason for this, is partly that for certain tasks there is to the authors knowledge no tool provided by OpenFOAM, or that the task can be done more conveniently with the tools of the Terminal rather than OpenFOAM's tools.

The primary reason we are able to manipulate cases with the might of the tools we find in a Linux Terminal is that everthing is a text file in OpenFOAM's case definition. If there is one thing Linux, or UNIX in general, has an over-abundance, it is text editors and text editing tools. This is due to a design decision of the UNIX creators which is best clarified by quoting Eric S. Raymond [22]:

Unix tradition strongly encourages writing programs that read and write simple, textual, stream-oriented, device-independent formats. Under classic Unix, as many programs as possible are written as simple filters, which take a simple text stream on input and process it into another simple text stream on output.

Despite popular mythology, this practice is favored not because Unix programmers hate graphical user interfaces. It's because if you don't write programs that accept and emit simple text streams, it's much more difficult to hook the programs together.

Text streams are to Unix tools as messages are to objects in an object-oriented setting. The simplicity of the text-stream interface enforces the encapsulation of the tools. More elaborate forms of inter-process communication, such as remote procedure calls, show a tendency to involve programs with each others' internals too much.

With a little help from a friend

If we combine the powers of the Linux Terminal and OpenFOAM's tools, anything is possible. In remainder of this section, some case manipulation scenarios of the combined use of the tools provided by Linux and OpenFOAM are presented

35.1 sed - stream editor

35.1.1 Rename a patch and edit the corresponding boundary condition

If we are in the lucky situation to have a symmetric mesh, we can remove half the domain and apply a symmetry constraint on the newly formed boundary. This is achived by the following sequence of steps:

1. Select all cells belonging to one half of the domain with *topoSet*
2. Remove the cells of the other half of the domain with *subsetMesh*
3. Change the definition of the newly formed boundary to a symmetry plane with *createPatch*.

After executing this steps, the mesh has a new symmetry boundary, however, all the fields retain their *oldInternalFaces* boundary introduced by *subsetMesh*. Thus, we need to rename the boundary condition in all fields and change the type of the boundary condition to symmetry.

Change BC type

We can change the type of a boundary condition with the tools *changeDictionary* or *foamDictionary*. The task of bulk-renaming is not possible with either of the tools. The tool *changeDictionary* is controlled by the *changeDictionaryDict* file. Within this file, we can use wildcards for the patch names, however, we can not use a wildcard for field names. Listings 225 and 226 show an allowed use-case of wildcards and one impossible use-case in *changeDictionaryDict*.

Our task, change the BC type for all fields, falls under the latter category. We could, however, work around this issue if we included all fields in the *changeDictionaryDict*.

```
T
{
    boundaryField
    {
        "./*"
        {

```

```

        type      zeroGradient;
    }
}

```

Listing 225: Possible use of wildcards with *changeDictionary*: Change all boundary conditions of the field T to **zeroGradient**.

```

".*"
{
    boundaryField
    {
        oldInternalFaces
        {
            type      symmetry;
        }
    }
}

```

Listing 226: Impossible use of wildcards with *changeDictionary*: Change the type of the boundary condition for the patch **oldInternalFaces** of all fields to **symmetry**.

The tool *foamDictionary* can also be used to change the type of a boundary condition. This tool is controlled by command line arguments, Listing 227 shows how the tool is called.

```
foamDictionary FILE -entry boundaryField.oldInternalFaces -set "{type symmetry;}"
```

Listing 227: Calling up *foamDictionary* to change the type of the BC of the patch **oldInternalFaces** for the field defined in **FILE**.

However, we can only pass one file at a time. This is where the Linux Terminal comes into play. With a simple **for** loop, we can loop over all files contained in the **0** directory and call *foamDictionary* for each individual file. Done!

```
for file in 0/*; do
    foamDictionary $file -entry boundaryField.oldInternalFaces -set "{type symmetry;}"
done
```

Listing 228: Changing the type of the BC of the patch **oldInternalFaces** for all fields.

Rename all BCs for all fields

Next, we would like to change the patch name in all field files. This operation is necessary, as *createPatch* operates only on the mesh. The fields are untouched by this tool. As we used *createPatch* to change the name and the type of the **oldInternalFaces** boundary for the mesh, we need to change the boundary name also for the fields.

This operation is a simple find&replace, which can be done with any text editor. For the sake of automation, we use the stream editor *sed*. Again, we loop over all files present in the **0** directory and we apply the find&replace operation on each file.

```
for file in 0/*; do
    sed -i 's/oldInternalFaces/symmetry/g' $file
done
```

Listing 229: Changing the name of the of the patch **oldInternalFaces** for all fields to **symmetry**.

35.1.2 Rename phases

The multi-phase solvers of OpenFOAM¹¹⁶ use the phase name as file extension in order to distinguish fields and files, e.g. **U.air** and **U.water**. In Listing 230 we see the content of the **0** directory of the bubble column

¹¹⁶From the release of OpenFOAM-2.3.0 onwards, see <http://openfoam.org/release/2-3-0/multiphase/>.

tutorial. This clearly demonstrates the use of file extensions to distinguish phases.

```
alpha.air      alphat.water  epsilon.water  k.water      p       Theta     U.water
alpha.air.orig  epsilon.air   k.air         nut.air    p_rgh   T.water
```

Listing 230: The content of the `0` directory of the bubble column tutorial.

If we wanted to simulate nitrogen gas in water, we would need to rename all files in order to follow this convention. Manually renaming files is tedious and can be automated by the use of the tools available in the Linux Terminal.

Rename files

First, we want to rename all files in order for them to have the proper file extension. This helps avoiding confusion. Thus, we use `find` to search for all files with the file extension `air` and pass them to `rename`, which renames the files according to the specified pattern.

```
find . -name '*.air' | xargs rename .air .nitrogen
```

Listing 231: Replacing the file extension `air` with the file extension `nitrogen` in all files in and below the current folder.

Replace text

Next, we need to replace the old phase name within the files itself. Again we use `find` to search for all files and pass them to `sed`, which replaces all text fitting the specified pattern. Note: applying `sed` to all files can lead to some trouble, as the text “pair” also gets treated and thus becomes “pnitrogen”. However, if the application of `sed` causes such a side effect, OpenFOAM will crash if vital entries were damaged in this way.

```
find . -type f | xargs sed -i s/air/nitrogen/g
```

Listing 232: Replacing the word `air` with the word `nitrogen` in all files in and below the current folder.

35.1.3 Insert data in a parametric case

Listing 233 shows a bare-bones shell script for running a parametric case. Here, we compute the initial conditions from the Reynolds number. The Reynolds number is also used by the post-processing script.

For any parametric case, we create a template case, which is then copied and the specific data is then inserted into the working case. In Listing 233, we use `sed` for inserting this data into Matlab/Octave scripts. The template case is created in such a way, that it itself reads data, e.g. the inlet velocity, from data files which in turn are written by the Matlab/Octave script.

This piecewise approach lends itself very well for setting up such cases. First, you create a base case with all the data it needs. Then you collect all the data that depends on your intended parameter, i.e., the Reynolds number in this example, into a separate data file. Such data files can be read by OpenFOAM using `#include` statements. Then, you work out e.g. a Matlab/Octave script that computes all relevant data from a given Reynolds number and writes a corresponding data file for the OpenFOAM case. Finally, you need to figure out a way how to feed a Reynolds number from the outside into the Matlab/Octave script, which is the Linux Terminal in the guise of `sed` in this case. Now, we could adapt the shell script to loop over a range of Reynolds numbers.

```
#!/bin/bash

# define Reynolds number
ReynoldsNumber=20000

# set up the case
curCase=runCase$ReynoldsNumber
rm -rf runCase* > /dev/null 2>&1
cp -r baseCase.org $curCase
```

```

# set up the post-processing template
cp Org_postProcessCase.m $curCase/postProcessCase.m

# copy the Reynolds number into the various Octave scripts
sed -i 's/XXX/'$ReynoldsNumber'/g' $curCase/computeInitialConditions.m
sed -i 's/XXX/'$ReynoldsNumber'/g' $curCase/postProcessCase.m

cd $curCase
./Allrun

```

Listing 233: A shell script for running a parametric case. Here, we use `sed` for replacing the word `XXX` with the Reynolds number in Matlab/Octave post-processing scripts.

35.1.4 Do math prior to data insertion

If we need to compute some values prior to using them in the replacement via `sed`, we can use `perl`¹¹⁷ for computations and pass the resulting value on. Listing 234 shows a simple example, how to achieve that. There, we compute a value from variables we assume to be given. Then, we replace the placeholder with the computed value, and finally we run the case.

```

#!/bin/bash

# compute quantities for inlet BC
amplitudeVal=$(perl -e "print($baseline*$curFactor)")

# replace placeholder in U file with actual values
sed -i "s/AMPLITUDE_VAL/$amplitudeVal/g" 0.org/U

# run the case
./Allrun

```

Listing 234: A shell script for running an OpenFOAM case. Here, we use `perl` for computing a quantity from given variables. Then, the word `AMPLITUDE_VAL` is replaced with the actual value, which was computed before.

We can use the snippet shown in Listing 234 to achieve very useful things.

35.2 Basic shell operations

This section is less a discussion on the use of individual commands and more a demonstration of the versatility of OpenFOAM and Linux's command line tools and shell scripting.

35.2.1 Running a parametric study

Expanding on the example above, we can use basic Linux shell tools to run a parametric study using OpenFOAM. Listing 235 shows the bare-bones shell script for running a parametric study.

Here, we have created a base case, which is copied to a working case directory. Into a working case, we then copy the relevant case files for the turbulence model and the mesh from the corresponding directory.

```

#!/bin/bash

# set up the cases directory for the parametrized cases
mkdir cases
studyRootDir=$(pwd)

# loop over all turbulence models
for tm in $turbModels
do
    # loop over all meshes
    for ms in $meshes
    do
        # build case directory

```

¹¹⁷We use `perl` because `bash` itself can only do integer math.

```

curCase=$ms\_$_tm
curCaseDir=cases/$curCase

# set-up current case
mkdir $curCaseDir
cp -r baseCase/* $curCaseDir

# copy turbulence model related files
cp turbulenceModels/$tm/turbulenceProperties $curCaseDir/constant

if [[ -d turbulenceModels/$tm/0.org ]] ; then
    cp turbulenceModels/$tm/0.org/* $curCaseDir/0.org/
fi

# copy mesh definition
cp meshes/$ms/blockMeshDict $curCaseDir/system/

# copy run script
# by default (see baseCase.org/runCase) all cases are run in serial
# the finer meshes contain an additional runScript which runs the case in parallel
if [[ -e meshes/$ms/runCase ]] ; then
    cp meshes/$ms/runCase $curCaseDir
fi

# run case
cd $curCaseDir
./Allrun
cd $studyRootDir
done
done

```

Listing 235: A shell script for running a parametric study. Here, we run the same base case for a number of turbulence models and meshes.

This parametric study is organised using directories. Looking at Figure 115, we see the base-study directory which contains the case template as well some shell scripts and two folders: *turbulenceModels* and *meshes*. Each of these of the two latter folders contains sub-folders which individually represent a parameter for our parametric study. We can see that we have several turbulence models and four meshes.

The turbulence model folders contain at least the *turbulenceProperties* file, if required there's also an *0.org* folder with specific data files. The meshes folders contain each a *blockMeshDict*, the latter two also contain an additional run-script for parallel execution.

```

user@host:~/OpenFOAM/run/parameterStudy2D$ ls
baseCase.org  clearStudy  meshes  Org_postProcessStudy.m  runStudy  turbulenceModels
user@host:~/OpenFOAM/run/parameterStudy2D$ tree turbulenceModels/
turbulenceModels
├── kEpsilon
│   └── turbulenceProperties
├── kOmega
│   └── turbulenceProperties
├── kOmegaSST
│   └── turbulenceProperties
└── LaunderSharmaKEpsilonLowRe
    ├── 0.org
    │   ├── k
    │   └── nut
    └── turbulenceProperties
├── realizableKEpsilon
│   └── turbulenceProperties
└── RNGkEpsilon
    └── turbulenceProperties
7 directories, 8 files

user@host:~/OpenFOAM/run/parameterStudy2D$ tree meshes
meshes
├── mesh00
│   └── blockMeshDict
├── mesh01
│   └── blockMeshDict
├── mesh02
│   ├── blockMeshDict
│   └── runCase
└── mesh03
    ├── blockMeshDict
    └── runCase
4 directories, 6 files

```

Figure 115: The directory structure of the input parameters of our parametric study. Each parameter, i.e., mesh or turbulence model, is defined by its own folder, which in turn contains all the relevant files.

This clearly demonstrates the versatility of OpenFOAM, since the only additional work that needs to be done to turn an ordinary OpenFOAM case into a parametric study over several parameters, is simply one of creative shell scripting.

The parametric study that was the basis for this discussion was a simple turbulent flow in a straight pipe, which was modelled in 2D. Thus, a rather simple example, however, we could also place complex meshes generated elsewhere into the meshes folder in order to study the influence of mesh fineness.

The simplicity of this example does not take away from the versatility of OpenFOAM and the creative use we can put the Linux Terminal to.

36 Meshing Gallery - a collection of meshes

This section is for showcasing meshes created by and/or with the various tools discussed here in this manual.

36.1 Gas riser

Figure 116 shows a gas riser, which consists of several branches and bends. This mesh was created mainly by using blockMesh along with extrudeMesh. The mesh creation procedure starts at the bottom with one of the four legs as a quarter geometry/mesh.

With the first leg completed, a Y-shaped branch is connected by using mergeMeshes and stitchMesh. Afterwards, by the use of topoSet and subsetMesh, we can ensure that we only create a quarter geometry/mesh. This quarter mesh is then mirrored to create one of the leg-forks. This is then built upon until the top Y-shaped branch is connected. Then, again, we use subsetMesh and mirrorMesh to create the full geometry/mesh.

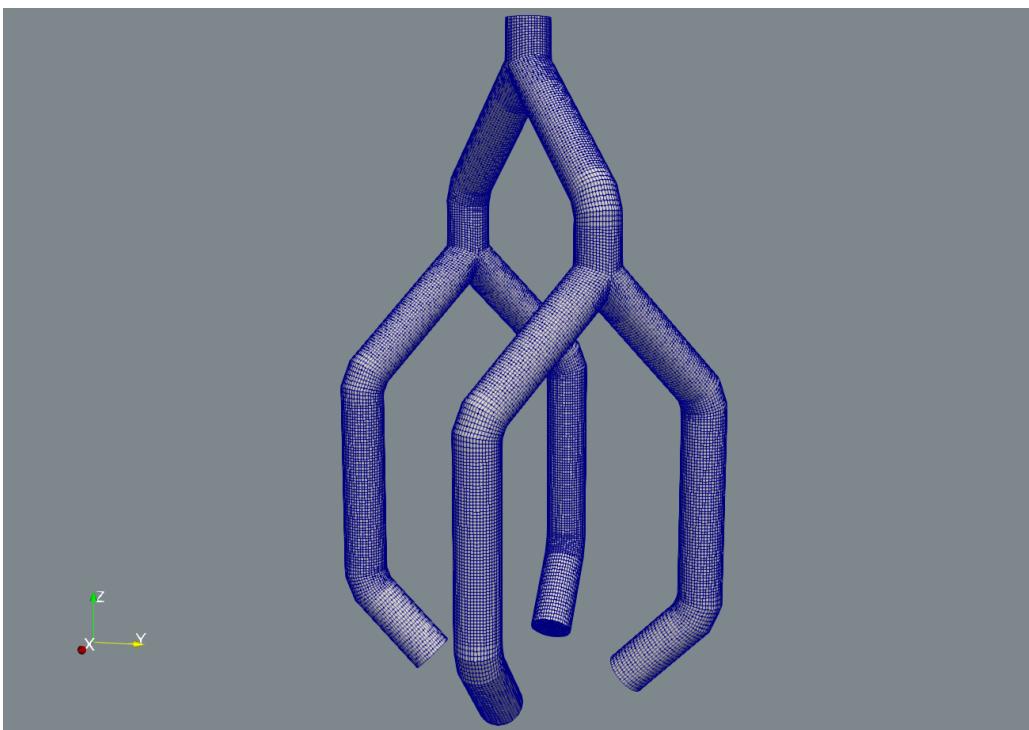


Figure 116: The mesh of a gas riser created using blockMesh and extrudeMesh along with stitchMesh and mirrorMesh as well as mergeMeshes and subsetMesh.

The mesh shown in Figure 116 consists of three basic building blocks, which are blockMesh-created meshes shown in Figure 117. These three building blocks are one type of Y-shaped branch and two types of a 45 degree, segmented bend. Two types of bend were used to achieve a perfect match, when stitching the meshes together. These two bends only differ in the orientation of their constitutive blocks. The straight sections of the gas riser were created using extrudeMesh. Thus, a hex-only mesh was achieved.

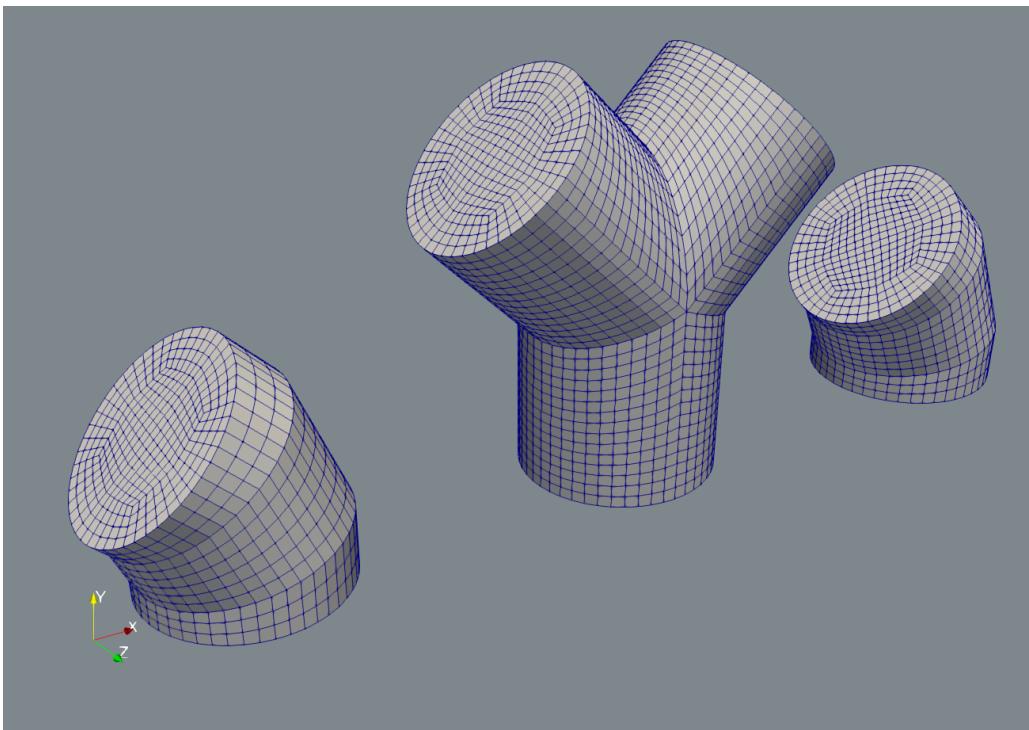


Figure 117: The mesh of a gas riser created using blockMesh and extrudeMesh along with stitchMesh and mirrorMesh as well as mergeMeshes and subsetMesh.

This mesh allows the use of refineWallLayer to create finer cells at the walls.

37 Pitfalls

This section discusses interesting errors encountered by the author of these lines during pre-processing.

37.1 Missing density field rho

If we use a mass flow rate boundary condition for velocity, then OpenFOAM computes the velocity based on the given mass flow rate and the fluid's density, which is provided by the solver's thermo-physical model, e.g., via the ideal gas law. The boundary condition itself needs to reference to the density field, since it assumes `rho` to be the density, which is the case most of the times.

Optionally, the user can provide the name of the density field, if this is not `rho`; and the user can also provide `rhoInlet`, which is a density value for situations when the density is not available at start-up.

If we run `decomposePar` or `renumberMesh`, then that tool fails since it needs access to a density to properly process the velocity field. The pre-processing tools have no access to the solver's thermo-physical model, hence they have no access to the density. Listing 236 shows the resulting error message.

```
--> FOAM FATAL ERROR:  
Did not find registered density field rho and no constant density 'rhoInlet' specified  
  
From function void Foam::flowRateInletVelocityFvPatchVectorField::updateValues(const  
AlphaType&) [with AlphaType = Foam::one]  
in file fields/fvPatchFields/derived/flowRateInletVelocity/  
flowRateInletVelocityFvPatchVectorField.C at line 115.  
  
FOAM exiting
```

Listing 236: Pre-processing fails due to a missing density field.

We can avoid the error shown in Listing 236 by two means. The first one, a rather trivial one, is to simply provide `rhoInlet`. However, this has the minor flaw, that this value is rather unnecessary, and it would be preferable if we could avoid having to deal with this value at all.

The more elegant way is to have OpenFOAM compute a density field from the case's data. We can do this by performing a post-processing step prior to pre-processing. Listing 237 shows the use of a post-processing tool to write the density field. Note, that Listing 237 applies to the modular solvers of OpenFOAM-11 and later. Earlier OpenFOAM versions most likely have a similar procedure.

```
foamPostProcess -solver fluid -func "writeObjects(rho)"
```

Listing 237: Perform post-processing prior to pre-processing: write the density field.

Part IV

Modelling

38 Solution dimensions

In OpenFOAM all meshes are three-dimensional, yet with a single-cell discretisation and a proper assignment of `empty-` or `wedge-type` boundary conditions, a simulation may have 0, 1, 2 or 3 solution dimensions, or solution directions as they are referred to by OpenFOAM's `checkMesh` tool.

```
Checking geometry...
Overall domain bounding box (0 -0.1 0) (0.07 0.11 0.001)
Mesh has 2 geometric (non-empty/wedge) directions (1 1 0)
Mesh has 2 solution (non-empty) directions (1 1 0)
All edges aligned with or perpendicular to non-empty directions.
```

Listing 238: A snippet of the output of `checkMesh`.

0-D simulations

In a 0-D simulation, the mesh consists of only a single cell, and all PDEs simplify into ODEs with time as the independent variable. This may seem too strong of a simplification, yet 0-D simulations may be useful to test the temporal development of certain models.

The OpenQBMM project¹¹⁸ uses a 0-D solver to test their population balance model¹¹⁹. In a 0-D domain, only sources and sinks can change the value of a field, as convection is ruled out.

1-D simulations

A 1-D simulation is resolved, respectively discretised, in only one spatial direction. This is a valid simplification for simulations when the axial flow dominates any lateral flow, e.g. very long pipelines. In the OpenFOAM tutorials, e.g. the `shockTube` tutorial case is a 1-D simulation.

2-D simulations

Many tutorials of OpenFOAM are 2-D cases, as they are detailed enough to represent realistic flow, yet they are simple enough to finish in a finite amount of time. 2-D simulations can be planar 2-D cases, e.g. a narrow channel, which is much greater in depth than it is in length and height; or axi-symmetric, e.g. a slice of a domain, which features rotational symmetry. The `cavity` tutorial case is an example of a planar 2-D simulation; and the `movingCone` case is an example of an axi-symmetric simulation case in the OpenFOAM tutorials.

3-D simulations

Full 3-D simulation feature no `empty-` or `wedge-type` patches.

38.1 Basic rules for simulations with reduced solution dimensions

An empty- or wedge-type boundary needs to be planar

One consequence of this rule is, that the two wedge-type patches need to be separate patches

There can't be a single wedge-type patch

Such a patch, consisting of both sides of the slice, would be non-planar, as the patch-mean normal-direction will be different from each face's normal-direction.

¹¹⁸<http://www.openqbmm.org/>

¹¹⁹<https://github.com/OpenQBMM/OpenQBMM/tree/master/applications/solvers/pbeFoam>

An empty-type boundary needs to be parallel to a coordinate plane

Listing 239 shows the output of checkMesh, after we rotated the mesh of the cavity tutorial case. Initially, the empty boundary is parallel to the x - y plane. However, after we rotated the mesh using `transformPoints`, the empty boundary normal direction is $(1, 1, 1)$. This, results in checkMesh reporting 0 solution directions. When we try to run the case, `icoFoam` fails with a rather obscure error message.

```
Checking geometry...
Overall domain bounding box (-0.0211325 -0.0211325 -0.11547) (0.084641 0.084641 0.0057735)
Mesh has 0 geometric (non-empty/wedge) directions (0 0 0)
Mesh has 0 solution (non-empty) directions (0 0 0)
***Number of edges not aligned with or perpendicular to non-empty directions: 2121
<<Writing 882 points on non-aligned edges to set nonAlignedEdges
```

Listing 239: The output of `checkMesh` after we applied a rotation from $(0, 0, 1)$ to $(1, 1, 1)$ to the simulation domain of the cavity tutorial.

```
--> FOAM FATAL ERROR:
Continuity error cannot be removed by adjusting the outflow.
Please check the velocity boundary conditions and/or run potentialFoam to initialise the
outflow.
Total flux : 2.22507e-308
Specified mass inflow : 0.000211325
Specified mass outflow : 0
Adjustable mass outflow : 0

From function bool Foam::adjustPhi(Foam::surfaceScalarField&, const volVectorField&, Foam
::volScalarField&)
in file cfdTools/general/adjustPhi/adjustPhi.C at line 107.

FOAM exiting
```

Listing 240: The output of `icoFoam` after we applied a rotation from $(0, 0, 1)$ to $(1, 1, 1)$ to the simulation domain of the cavity tutorial.

A wedge-type boundary mustn't be parallel to a coordinate plane

The mesh of an axi-symmetric simulation is a discretised slice of the geometry, with a single cell in circumferential direction. This slice is supposed to straddle a coordinate plane. If one of the `wedge`-type patches is parallel to a coordinate plane, then OpenFOAM issues an error message, similar to the one shown in Listing 241.

```
--> FOAM FATAL ERROR:
wedge back plane aligns with a coordinate plane.
The wedge plane should make a small angle (~2.5deg) with the coordinate plane
and the pair of wedge planes should be symmetric about the coordinate plane.
Normal of wedge plane is (6.451349e-20 1 5.042482e-20) , implied coordinate plane
direction is (0 1 0)

From function virtual void Foam::wedgePolyPatch::calcGeometry(Foam::PstreamBuffers&)
in file meshes/polyMesh/polyPatches/constraint/wedge/wedgePolyPatch.C at line 110.

FOAM exiting
```

Listing 241: The output of `checkMesh` when a wedge-type patch is parallel to a coordinate plane.

Do not base your residual-controls on the velocity

Listing 242 shows the residuals of an axi-symmetric, transient compressible case. The main flow direction is in x -direction. We can observe that the residual for U_x drops quite fast over the iterations of the PIMPLE-loop. The residual for U_y , the velocity component orthogonal to the main flow direction, shows only a minor decrease. The residual for U_z , the velocity component in the direction that is not solved for, remains quite constant at a higher order of magnitude compared to the other two velocity components.

Thus, basing the residual control on the velocity, i.e., determining when to stop the PIMPLE-loop for each time step, would not work since the residual in the non-solution direction does not decrease. Hence, the

PIMPLE-loop would always run for the specified maximum number of outer iterations.

```
PIMPLE: Iteration 1
DILUPBiCGStab: Solving for Ux, Initial residual = 0.00023981, Final residual = 1.63408e-08, No Iterations 1
DILUPBiCGStab: Solving for Uy, Initial residual = 0.00062661, Final residual = 2.42203e-07, No Iterations 2
DILUPBiCGStab: Solving for Uz, Initial residual = 0.00828632, Final residual = 8.78647e-07, No Iterations 1
DILUPBiCGStab: Solving for e, Initial residual = 1.57513e-05, Final residual = 6.51738e-10, No Iterations 1
...
PIMPLE: Iteration 2
DILUPBiCGStab: Solving for Ux, Initial residual = 3.86574e-05, Final residual = 9.41528e-09, No Iterations 1
DILUPBiCGStab: Solving for Uy, Initial residual = 0.00093254, Final residual = 1.306886e-07, No Iterations 2
DILUPBiCGStab: Solving for Uz, Initial residual = 0.0087383, Final residual = 6.101225e-07, No Iterations 1
DILUPBiCGStab: Solving for e, Initial residual = 1.10419e-05, Final residual = 6.146413e-10, No Iterations 1
...
PIMPLE: Iteration 3
DILUPBiCGStab: Solving for Ux, Initial residual = 9.83885e-06, Final residual = 6.74642e-09, No Iterations 1
DILUPBiCGStab: Solving for Uy, Initial residual = 0.00092617, Final residual = 2.26015e-07, No Iterations 2
DILUPBiCGStab: Solving for Uz, Initial residual = 0.0088544, Final residual = 6.081737e-07, No Iterations 1
DILUPBiCGStab: Solving for e, Initial residual = 6.18173e-06, Final residual = 3.794985e-10, No Iterations 1
...
PIMPLE: Converged
  Doing final iteration
PIMPLE: Iteration 4
DILUPBiCGStab: Solving for Ux, Initial residual = 3.90258e-06, Final residual = 5.04517e-09, No Iterations 1
DILUPBiCGStab: Solving for Uy, Initial residual = 0.00048341, Final residual = 1.15029e-07, No Iterations 2
DILUPBiCGStab: Solving for Uz, Initial residual = 0.0087934, Final residual = 6.317759e-07, No Iterations 1
DILUPBiCGStab: Solving for e, Initial residual = 3.35143e-06, Final residual = 5.094523e-10, No Iterations 1
...
DILUPBiCGStab: Solving for omega, Initial residual = 1.41300e-05, Final residual = 9.00674e-09, No Iterations 1
DILUPBiCGStab: Solving for k, Initial residual = 0.00014157, Final residual = 1.099701e-09, No Iterations 2
PIMPLE: Converged in 4 iterations
```

Listing 242: The solver output for one time step of a transient compressible axi-symmetric case.

The neglected geometric direction can be any principal axis

A planar two-dimensional simulation in OpenFOAM can be in any of the three principal planes, i.e., x - y , x - z or y - z . Similarly, the mesh of an axi-symmetric simulation may straddle any of the principal planes.

39 Turbulence-Models

39.1 Organisation

The way the source for the turbulence models is organized changed over the time¹²⁰ the author is dealing with OpenFOAM. With the release of OpenFOAM-2.3.0¹²¹ a new, (even) more general, way of code organisation was rolled out.

The old way relied essentially on namespaces and inheritance to achieve generality and abstraction. The new way to do stuff is based on templates, inheritance and inheritance from templates. This section discusses both ways of code organisation. Especially the new way – with all its template madness – may lead to difficulties to understand the code at first glances. Thus, the author hopes to be able to shed some light into the mysteries of the new way to do things.

With the release of OpenFOAM-3.0, the transition to the new turbulence modelling framework has been completed¹²². There is no `$FOAM_SRC/turbulenceModels` directory anymore in the sources. Thus, the discussion of the old ways is on its way to be of purely historical interest. However, the author hopes, that even the outdated sections of this ever-growing collection of stuff may provide some insights.

39.1.1 The old ways

Although, this section is not intended as a rant against everything new, the organisation was easier to understand. You can inspect it at `$FOAM_SRC/turbulenceModels`. The old turbulence modelling framework is based on namespaces to draw the distinction between compressible and incompressible models.

The multiphase solvers within this old framework either use a turbulence model on mixture quantities (`multiphaseEulerFoam` or `interFoam`), or the turbulence model was applied to the continuous phase only (`twoPhaseEulerFoam`). Within the old framework, only one turbulence model was applied in multiphase simulations.

Figure 118 shows the organisation of the old turbulence modelling framework. The class hierarchy is duplicated to some degree with largely identical or equivalent classes in each namespace, i.e. `Foam::compressible` and `Foam::incompressible`. A comparison of the files `RASModel.H` and `RASModel.C` in the namespaces `Foam::compressible` and `Foam::incompressible` reveals that these files share more common lines than they have differing lines.

This issue is also addressed in the release notes of the new turbulence framework in even more pressing terms:

The issue of compressibility has been managed for many years using two distinct turbulence modelling frameworks, one for constant density flows and another for variable density flows. However, neither framework is appropriate for multiphase systems, in conservative form, for which the phase-fraction must be included into all transport and source terms of the turbulence property equations. Code is largely duplicated between the two frameworks, which is inconsistent with the OpenFOAM code development policy to minimise code duplication to promote code maintainability and sustainability. Extension of the current code architecture to multiphase flows would increase the number of hierarchies from two to four, one for each combination of phase-fraction and density representation.

¹²⁰Since beginning of 2012 or OpenFOAM-2.0.x.

¹²¹<http://www.openfoam.org/version2.3.0/multiphase.php>

¹²²<http://openfoam.org/version3.0.0/>

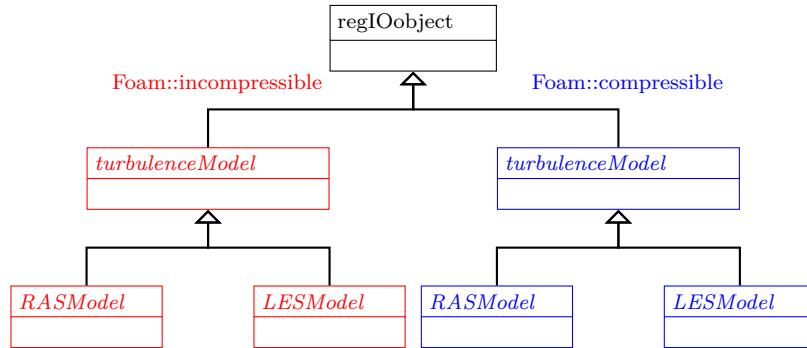


Figure 118: The class hierarchy of the basis of the old turbulence model framework. The namespaces `Foam::incompressible` and `Foam::compressible` are indicated by the colours red and blue.

39.1.2 The new order

The new framework for all turbulence models is located at `$FOAM_SRC/TurbulenceModels`, notice the capital T¹²³. The use of templates is necessary, since this framework is meant to be used by all solvers of OpenFOAM at some point of time. All solvers means compressible and incompressible, as well as single- and multiphase. This makes sense, since the concept of turbulence is general, and not related to the specific situation in question. The advantages of this approach is best said by the release note itself:

This new framework is very powerful and supports all of the turbulence modelling requirements needed so far. It will be enhanced and extended in future OpenFOAM releases to include a wide range of models and sub-models, with the expectation to replace the current dual hierarchies of turbulence models, to aid code maintainability and sustainability.

Initially the new turbulence modelling framework was introduced with an update of the multiphase solvers. In the OpenFOAM-2.3.0 release only `twoPhaseEulerFoam` and `DPMFoam`. As time progresses more and more solvers are updated to use the new framework instead of the old. By the time of writing this paragraph (October 2015) dozens of solvers in the OpenFOAM-dev repository were already ported.

One to rule them all

Whenever, a certain concept manifests itself in a variety of incarnations¹²⁴, the developers of OpenFOAM take this rough quote from Lord of the Rings by heart. A single turbulence model class was created to be applied to whatever physics OpenFOAM implements. For this to work, this most basic turbulence model contains only the things which can be abstracted enough to apply everything. The most trivial example of this (a feature independent of compressibility or the number of phases involved), is the sheer existence of a turbulence model¹²⁵.

Figure 119 shows the basic class hierarchy of the new turbulence framework. Besides this basic, non-templated class hierarchy, there is the templated hierarchy of the implementing classes. The basic classes represent the very abstraction. On top of the family tree is the class `IOdictionary`, which provides the IO facilities. From using OpenFOAM, we know, that there is a dictionary controlling the turbulence modelling. By deriving the turbulence model class from `IOdictionary`, the turbulence model is its dictionary.

From `IOdictionary` the class `turbulenceModel` is derived. Note the lower case letter at the beginning. This is not the only base class for turbulence models, we will also encounter a capital letter class. As already mentioned, OpenFOAM makes heavy use of the file system's case sensitivity. Thus, we need to pay attention to the letter (`turbulenceModel` ≠ `TurbulenceModel`).

The class `turbulenceModel` declares a large number of pure virtual functions which the derived classes down the family tree inevitably need to implement. This class is the source-code-wise incarnation of the fact that there is a turbulence model. No further information is as of this point known to the turbulence model, except

¹²³This is one of the reasons why OpenFOAM is not readily available on Windows, since it assumes that the file system is case-sensitive. In fact, OpenFOAM makes heavy use of case-sensitivity of the file system. Microsoft, however, reminds us not to expect, e.g. NTFS, to be case-sensitive. See: https://msdn.microsoft.com/en-us/library/aa365247%28VS.85%29.aspx#naming_conventions

¹²⁴Such as turbulence is present in single-phase, multi-phase, compressible, and incompressible flow.

¹²⁵This is not a non-statement, however trivial this might sound. We can relate the existence of turbulence modelling to a certain class, namely `turbulenceModel`, which is derived from `IOdictionary`, and serves as the absolute basis for everything further down the family tree.

that it is a turbulence model. The data of this class is consequently sparse. The most important data members of this class are references to the run-time object and the mesh. More information can be found in the file `$FOAM_SRC/TurbulenceModels/turbulenceModels/turbulenceModel.H`.

From the class `turbulenceModel` two classes are derived: `incompressibleTurbulenceModel` and `compressibleTurbulenceModel`. These two classes represent the fact, that flow can be considered incompressible or compressible. The consequence of this difference can be seen in the treatment of the density by these two classes. In Figure 119 we see, that the incompressible turbulence model has a `geometricOneField` as density data member, in contrast to the compressible model, which has a reference to the actual density field.

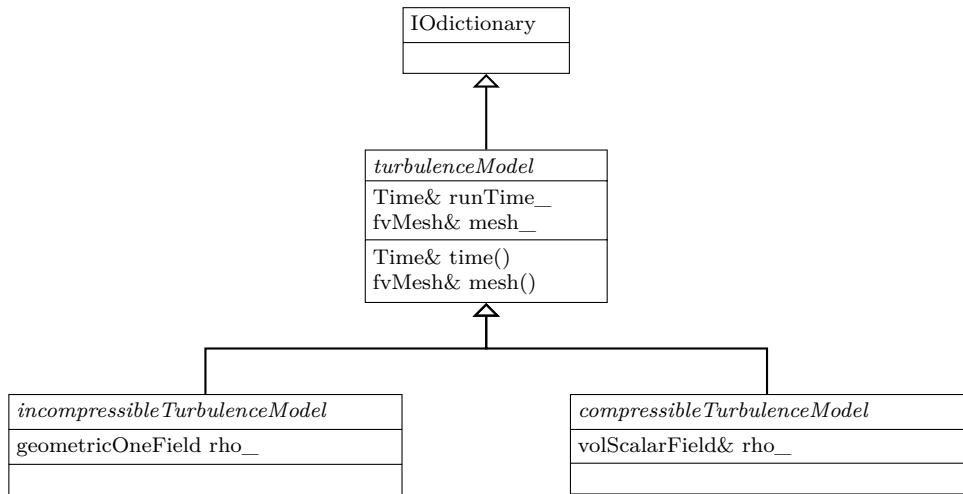


Figure 119: The class hierarchy of the basis of the new turbulence model framework.

A little note on ancestry: in the class hierarchy of the *ye olden ways*, see Figure 118, we saw that the base classes for the turbulence models, were derived from `regIOobject`. Thus, allowing access to the turbulence model via OpenFOAM's registry.

In the class hierarchy of the *fancy new order*, see Figure 119, we see that the base class for all turbulence models is derived from the class `IOdictionary`. In Figure 118, all the way down in Section 68.7, we see that the class `IOdictionary` is derived from `regIOobject`¹²⁶. Thus, the turbulence model base class is derived indirectly from `regIOobject`. Thus, allowing access to the turbulence model via OpenFOAM's registry.

A mere comparison of Figures 118 and 119 might have suggested otherwise, however, as the list of ancestors got longer for the new modelling framework, this fact (the derivation from `regIOobject`) has travelled up the family tree.

Many to rule the many

The distinction between incompressible and compressible, as well as, single-phase and multi-phase, turbulence modelling is made by passing appropriate template parameters to the base class `TurbulenceModel`. Note that `TurbulenceModel` is derived from the template parameter `BasicTurbulenceModel`. In Figure 120 we see the (templated) class hierarchy of the new turbulence modelling framework. This class hierarchy is related to the classes depicted in Figure 119 by the use of the template parameter `BasicTurbulenceModel`, which is either `incompressibleTurbulenceModel` or `compressibleTurbulenceModel`, note the lower case first letter.

The distinction between incompressible and compressible modelling is made by the template parameters `Rho` and `BasicTurbulenceModel`. In the case of incompressible models a `geometricOneField`¹²⁷ is passed for the parameter `Rho`. The distinction between single-phase and multi-phase modelling is made by the template parameter `Alpha`. In the case of single-phase modelling a `geometricOneField` is passed.

¹²⁶In OpenFOAM-5.0, the class `IOdictionary` is derived from a base class `baseIOdictionary`, which in turn is derived from `regIOobject` and `dictionary`. In earlier versions of OpenFOAM, `IOdictionary` is directly derived from `regIOobject` and `dictionary`.

¹²⁷The header file of the class `geometricOneField` describes its intention as follows:

A class representing the concept of a GeometricField of 1 used to avoid unnecessary manipulations for objects which are known to be one at compile-time.

Used for example as the density argument to a function written for compressible to be used for incompressible flow.

The approach, that `TurbulenceModel` is derived from its template parameter `BasicTurbulenceModel`, which is either an `incompressibleTurbulenceModel` or `compressibleTurbulenceModel`, which in turn are derived from a common base class, demonstrates the great flexibility a high-level programming language, such as C++. However, the presence of templates and their heavy, sophisticated use – as demonstrated in OpenFOAM – raises the bar when it comes to reading the source code and finding out what is happening.

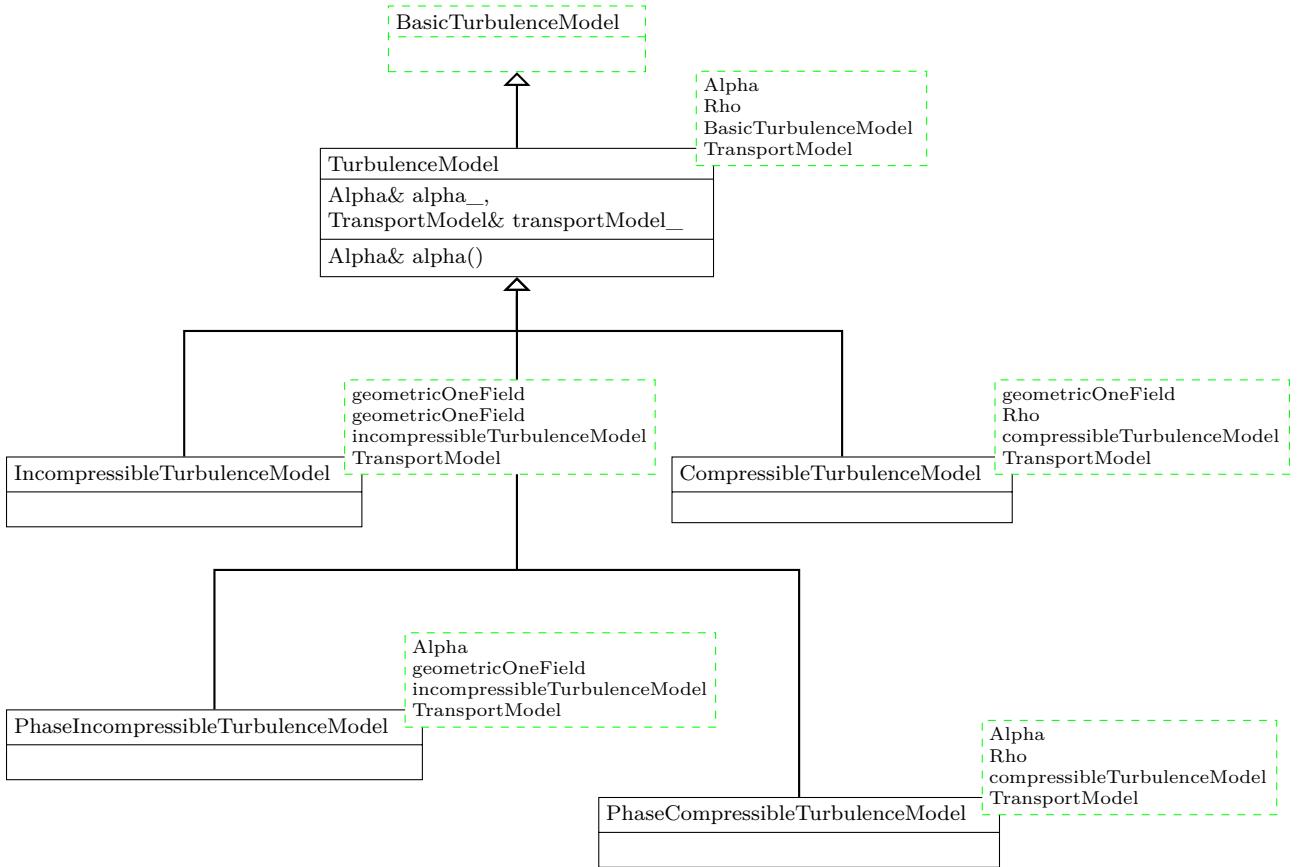


Figure 120: The base class `TurbulenceModel` has four template parameters and it is derived from one of its template parameters. Note, that the four derived classes – the four incarnations of the turbulence model – differ in the template parameters.

Branching the family tree

In turbulence modelling, we can identify three elementary choices: we can treat a fluid flow as laminar, or apply a RAS or LES turbulence model. This basic choice is reflected in the three classes derived from the template parameter in Figure 121. Since RAS and LES turbulence models are turbulence models¹²⁸, those two base classes are derived from the common template parameter `BasicTurbulenceModel`. The nature of `BasicTurbulenceModel` has been discussed above.

By treating the laminar case as a turbulence model, the OpenFOAM developers got rid of the special case laminar flow. In Figure 121, the behaviour of the `laminar` turbulence model is indicated by the methods `R()` and `nut()`. The `laminar` turbulence returns zero (with the appropriate dimension) for all turbulent quantities. Thus, the method `R()`, which computes the Reynolds stress tensor, returns a volumetric¹²⁹ field of symmetric tensors with all-zero components¹³⁰. This behaviour is indicated in Figure 121 with the `(= 0)` appended to the method's names.

¹²⁸Again, we encounter an *is a* relationship, which is a strong hint for relating two classes by inheritance.

¹²⁹I.e. all values are defined at the cell centers.

¹³⁰In the file `laminar.C`, we find this expression in the constructor of the returned tensor field: `dimensionedSymmTensor("R", sqr(this->U_.dimensions()), symmTensor::zero)`.

The class `eddyViscosity` is a class which implements the ideas behind the *Boussinesq hypothesis*, which is discussed below.

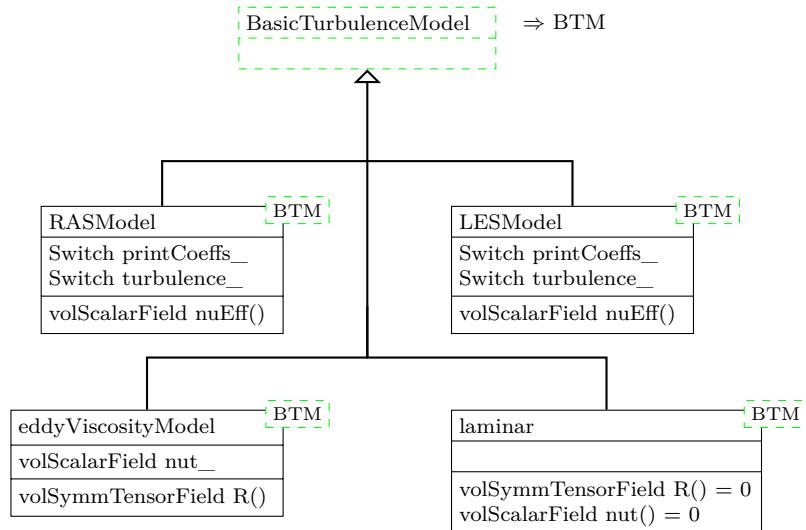


Figure 121: The class hierarchy of the elementary turbulence models of the new turbulence model framework. Note the shorthand notation BTM for the class `BasicTurbulenceModel`.

Further down the family tree

A great number of turbulence models are based on the so-called *Boussinesq hypothesis* which computes the Reynolds stresses from an *eddy viscosity* μ_t and the mean strain-rate tensor, and was proposed by Boussinesq [13] [66].

$$\mathbf{R} = \mu_t (\nabla \bar{\mathbf{u}} + \nabla \bar{\mathbf{u}}^T) - \frac{2}{3} \rho \mathbf{I} k \quad (42)$$

$$k = \frac{1}{2} \sum_i \overline{u'_i u'_i} = \frac{1}{2} \overline{\mathbf{u}' \cdot \mathbf{u}'} \quad (43)$$

The quantity k is the specific kinetic energy of the turbulent fluctuations. A great part of literature refers to k as *turbulent kinetic energy* [55, 37, 9, 10], most probably for reasons of keeping the vocabulary short. The unit tensor \mathbf{I} is often denoted with the Kronecker delta δ_{ij} in literature.

The Boussinesq hypothesis is common to both RAS and LES turbulence models. This can be translated into a class relationship. In Figure 122 we see how the `kEpsilon` and the `Smagorinsky` turbulence models are derived. Those two models are discussed since these are widely used. The class `eddyViscosityModel` implements the general idea of the Boussinesq hypothesis, thus, it is the common base for both turbulence models. In the case of LES models, an intermediate class (`lesEddyViscosityModel`) is in between the class `eddyViscosityModel` and the actual turbulence model. This class serves to hold data and define methods specific to LES models using the Boussinesq hypothesis.

The distinction between RAS models and LES models is made by the template parameter inserted in `eddyViscosityModel`. In the case of RAS models, the template parameter of `eddyViscosityModel` from which e.g. the `kEpsilon` model is derived is `RASModel<BasicTurbulenceModel>`. Since `RASModel` is derived from `BasicTurbulenceModel`, the class `RASModel` is a `BasicTurbulenceModel`. Thus, this operation is perfectly valid. In the case of LES models, `LESModel<BasicTurbulenceModel>` is inserted as the template parameter of `eddyViscosityModel`.

Sounds complicated, which it probably also is. Nevertheless, we admire the versatility of generality of the new turbulence modelling framework and stomach the mental pain caused by all the template and inheritance wizardry.

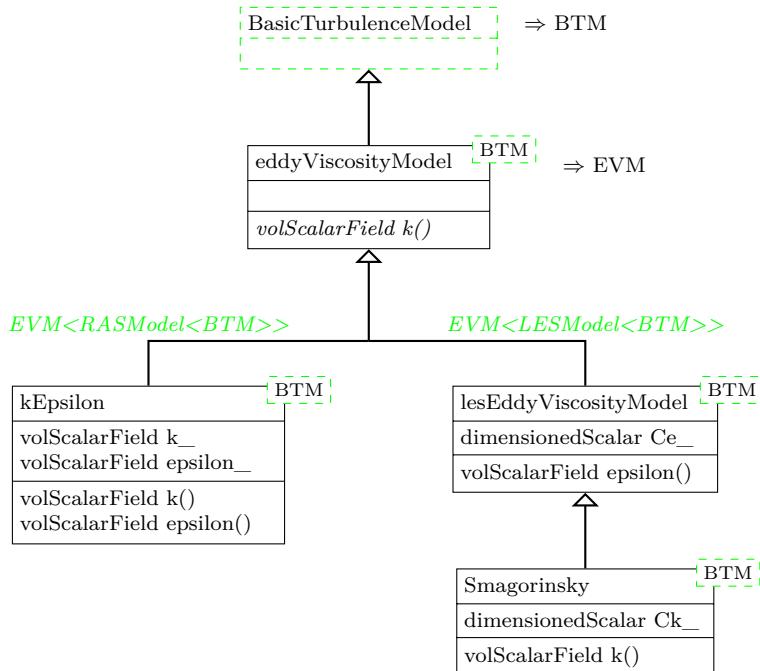


Figure 122: The class hierarchy of a selection of turbulence models of the new turbulence model framework. Note the shorthand notation BTM for the class `BasicTurbulenceModel`, and EVM for `eddyViscosityModel`.

The method signature in italics of the class `eddyViscosityModel` indicates a pure virtual function. This method has to be implemented by the classes derived from `eddyViscosityModel`. In the case of the `kEpsilon` class it is the class derived directly from `eddyViscosityModel` which implements `k()`. In the case of the `Smagorinsky` class, the pure virtual function was inherited via `lesEddyViscosityModel`. A class containing a pure virtual function can not be instantiated, thus, there can be no usable turbulence model `lesEddyViscosityModel`. This class can only serve as an intermediary.

39.2 Reynolds averaged models (RAS)

39.2.1 kEpsilon and low-Reynolds flows

The standard wall functions require the `yPlus` value to fall into a certain range. If the `yPlus` value is outside of that range, the simulation's results can become quite wrong. Thus, the use of the `kEpsilon` model creates an effective upper limit on the mesh resolution at the walls [21]. This becomes a problem, when we want to finely resolve the flow at and near the wall, e.g. when solving heat-transfer problems.

For cases, when the `yPlus` value is too small, i.e. it is smaller than the lower bound of the standard wall-function's validity range, there are the so-called *low Reynolds* formulations.

Wall functions

From OpenFOAM-5.0 onwards, there are no special low-Reynolds wall-functions for `epsilon`, as the standard and low-Reynolds formulation have been merged into a single wall-function¹³¹.

However, other fields, such as `k` and `nut`, still require special wall-functions when a low-Reynolds model is used.

Disclaimer

Everthing of Section 39 after this point has been created a while ago. The some of the content of the sub-sections below might be outdated by the time you read this.

¹³¹See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/f260780b7310528505137bbfc8d5f85084379120>

39.2.2 kOmega and kOmega SST models

Here, we shall discuss issues specific to the kOmega family of turbulence models. General information on the theory behind this family of turbulence models is best found in the sources of more informed people.

Pitfall: specifying an omega equal to zero spells trouble

The inlet-outlet boundary condition shown in Listing 243 looks quite innocent, however, it is this boundary condition that spells doom for our simulation.

If we recall the basics of the k-omega turbulence model¹³², we find that the turbulent viscosity is defined as the ratio of the turbulent kinetic energy k and the dissipation of the turbulent kinetic energy ω , or in less words and slightly more math: $\nu = \frac{k}{\omega}$. And this is, why carelessly copying&pasting boundary conditions can lead to trouble.

```
outlet
{
    type          inletOutlet;
    inletValue    uniform 0;
    value         uniform 0;
}
```

Listing 243: A copy & pasted inletOutlet boundary condition,

Unfortunately, the error message, shown in Listing 244, is not very telling, at least it doesn't tell us explicitly. We can, if we have some experience, see that division is most probably the operation that triggers the floating point exception. We see hints of that in the lines marked with #3 (`Foam::divide`), #4 (`void Foam::divide`) and #5 (`Foam::operator/`).

```
#0  Foam::error::printStack(Foam::Ostream&) at ??:?
#1  Foam::sigFpe::sigHandler(int) at ??:?
#2  ? in "/lib/x86_64-linux-gnu/libc.so.6"
#3  Foam::divide(Foam::Field<double>&, Foam::UList<double> const&, Foam::UList<double> const&)
     at ??:?
#4  void Foam::divide<Foam::fvPatchField, Foam::volMesh>(Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh>&, Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh> const&, Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh> const&)
     at ??:?
#5  Foam::tmp<Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh> > Foam::operator /<Foam::fvPatchField, Foam::volMesh>(Foam::tmp<Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh> > const&, Foam::GeometricField<double, Foam::fvPatchField, Foam::volMesh> const&)
     at ??:?
#6  Foam::kOmegaSST<Foam::eddyViscosity<Foam::RASModel<Foam::compressibleMomentumTransportModel> >, Foam::compressibleMomentumTransportModel>::correct()
     at ??:?
#7  Foam::solvers::fluid::postCorrector() at ??:?
#8  ? in "/home/user/OpenFOAM/OpenFOAM-12/platforms/linux64GccDPInt32Opt/bin/foamRun"
#9  ? in "/lib/x86_64-linux-gnu/libc.so.6"
#10  __libc_start_main in "/lib/x86_64-linux-gnu/libc.so.6"
#11  ? in "/home/user/OpenFOAM/OpenFOAM-12/platforms/linux64GccDPInt32Opt/bin/foamRun"
Floating point exception (core dumped)
```

Listing 244: The error message caused by the inlet-outlet boundary condition for `omega` with a zero value.

Hence, always take care when copying & pasting boundary conditions. While an inlet value of zero might be perfectly reasonable for some quantities, it might turn out to be fatal for others.

39.3 Categories

The desired category of turbulence models can be specified in the file `turbulenceProperties`. There are three possible entries.

laminar The flow is modelled laminar

RASModel A Reynolds averaged turbulence model (RAS-model) is used.

¹³²See e.g. https://www.cfd-online.com/Wiki/Wilcox%27s_k-omega_model

LESModel Turbulence is modelled by a *large-eddy* model.

The file `turbulenceProperties` contains only one entry. In case of a large eddy simulation, this entry reads:

```
simulationType LESModel;
```

Listing 245: *turbulenceProperties*

39.4 RAS-Models

The entry in the file `turbulenceProperties` specifies only the class of turbulence models. The exact turbulence model is specified in the file `RASProperties`. This file must contain all necessary parameters.

Listing 344 shows the content of `RASProperties`. In this case a k- ϵ model is used and no further parameters are necessary.

```
RASModel      kEpsilon;
turbulence    on;
printCoeffs   on;
```

Listing 246: *RASProperties*

Depending on the exact model more parameters can be necessary.

39.4.1 Keywords

RASModel The name of the turbulence model. At this place laminar can also be chosen. The banana test (see Section 11.2.1) delivers a list of available models.

```
--> FOAM FATAL ERROR:
Unknown RASModel type banana

Valid RASModel types:

17
(
LRR
LamBremhorstKE
LauderGibsonRSTM
LauderSharmaKE
LienCubicKE
LienCubicKELowRe
LienLeschzinerLowRe
NonlinearKEShih
RNGkEpsilon
SpalartAllmaras
kEpsilon
kOmega
kOmegaSST
kkLOmega
laminar
qZeta
realizableKE
)
```

Listing 247: Possible RAS-model entries in *RASProperties*

turbulence This is a switch to activate or deactivate the turbulence modelling. Allowed values are: *on/off*, *true/false* or *yes/no*.

If this switch is deactivated, then a laminar simulation is conducted. This way of choosing a laminar model is not recommended, see Section 39.6.1.

printCoeffs If this switch is enabled, then the solver will display the coefficients of the selected turbulence model.

Even if the switch `turbulence` is disabled, the solver will display the coefficients at the beginning of the simulation, see Listing 254. The coefficients are not displayed only when `RASModel laminar` is chosen.

optional parameters Some models accept optional parameters to override the default values of the model. Listing 248 shows how the coefficients of the k- ϵ model can be overridden.

```
kEpsilonCoeffs
{
    Cmu      0.09;
    C1       1.44;
    C2       1.92;
    C3      -0.33;
    sigmak   1.0;
    sigmaEps 1.11; //Original value:1.44
}
```

Listing 248: Definition of model parameters in *RASProperties*

39.4.2 Pitfall: meaningless Parameters

In the above section it was shown how to override default values of the model constants. In this procedure, there is one source of error hidden. This is not an actual error, but it can lead to a fruitless search for an error.

If nonsensical parameters are added to the `kEpsilonCoeffs` dictionary, these will be read and also printed. Listing 249 shows the `kEpsilonCoeffs` dictionary of the file `RASProperties`. This dictionary is used to override default values of the model constants. A fake model constant has been added to this dictionary.

Listing 250 shows parts of the solver output, when this dictionary is used in a simulation. All constants of the dictionary are read and printed again. It seems as if the constant `banana` is part of the turbulence model. Varying this parameter yields no results, which is no error.

The reason for this behaviour is, there is no check whether the defined constants in the dictionary make sense or not.

```
kEpsilonCoeffs
{
    Cmu      0.09;
    C1       1.44;
    C2       1.92;
    C3      -0.33;
    sigmak   1.0;
    sigmaEps 1.11; //Original value:1.44
    banana   0.815; // nonsense parameter
}
```

Listing 249: Definition of model parameters in *RASProperties*

```
Selecting RAS turbulence model kEpsilon
kEpsilonCoeffs
{
    Cmu      0.09;
    C1       1.44;
    C2       1.92;
    C3      -0.33;
    sigmak   1.0;
    sigmaEps 1.11;
    banana   0.815;
}

Starting time loop
```

Listing 250: Solver output

39.5 LES-Models

39.5.1 Keywords

The keywords `turbulence` and `printCoeffs` have the same meaning with LES models. There is also the possibility – depending on the selected model – of defining optional parameters.

LESModel The name of the turbulence model. At this place laminar can also be chosen. The banana test (see Section 11.2.1) delivers a list of available models. Listing 251 shows the result of such a banana test. The model dynamicSmagorinsky was loaded from an external library. See Section 11.3.3 for how to include external libraries.

```
--> FOAM FATAL ERROR: Unknown LESModel type banana

Valid LESModel types:

16
(
    DeardorffDiffStress
    LRRDiffStress
    Smagorinsky
    SpalartAllmaras
    SpalartAllmarasDDES
    SpalartAllmarasIDDES
    dynLagrangian
    dynOneEqEddy
    dynamicSmagorinsky
    homogeneousDynOneEqEddy
    homogeneousDynSmagorinsky
    kOmegaSSTSAS
    laminar
    mixedSmagorinsky
    oneEqEddy
    spectEddyVisc
)
```

Listing 251: Possible LES-model entries in *LESProperties*

39.5.2 Algebraic sub-grid models

Algebraic sub-grid models introduce no further transport equation to the simulation. The turbulent viscosity is calculated from existing quantities.

39.5.3 Dynamic sub-grid models

The dynamic sub-grid models calculate the model constant C_S from known quantities instead of prescribing a fixed value. The way how C_S is calculated is determined by the sub-grid model.

39.5.4 One equation models

A further class of LES turbulence models are one equation models. These models add one further equation to the problem. Usually, an additional equation for the sub-grid scale turbulent kinetic energy is solved.

39.6 Pitfalls

39.6.1 Laminar Simulation

As already mentioned – see Section 39.4 – turbulence modelling can be deactivated in some ways.

In the following, different ways to conduct a laminar simulation are listed. This list applies only to solvers that utilize the generic turbulence modelling of OpenFOAM:

1. **turbulenceProperties: simulationType laminar**

This is the most general way to turn turbulence modelling off. **turbulenceProperties** controls the generic turbulence class. The generic turbulence class can take the form of the **laminar**, **RASModel** or **LESModel** class, see Figure 189. This is controlled by the parameter **simulationType**.

```
Selecting turbulence model type laminar
```

Listing 252: Solver output for **simulationType laminar**

2. **RASProperties:** RASModel laminar
LESProperties: LESModel laminar

In this case, a certain turbulence modelling strategy is chosen (`RASModel` or `LESModel`). However, there is a dummy turbulence model for laminar simulation. This dummy turbulence model is derived from the base class `RASModel` but it implements a laminar model. See Figure 190. Therefore, `RASModel laminar` selects the laminar RAS turbulence model. In this point `RASModel` and `LESModel` behave similar.

```
Selecting turbulence model type RASModel
Selecting RAS turbulence model laminar
```

Listing 253: Solver output for `RASModel laminar`

3. **RASProperties:** turbulence off

The switch `turbulence` can be used to enable or disable turbulence modelling. When the calculation is started, the turbulence model specified is used. However, in the source code of the solver, there is the test whether turbulence modelling is active or not. See Listing 336.

```
Selecting turbulence model type RASModel
Selecting RAS turbulence model kEpsilon
kEpsilonCoeffs
{
    Cmu           0.09;
    C1            1.44;
    C2            1.92;
    sigmaEps     1.3;
}
```

Listing 254: Solver output for `turbulence off`

Solver output

The last two possibilities to conduct a laminar simulation can lead to confusion because the solver output contains word like `RASmodel` or `RAS turbulence model`. See Listings 253 and 254. In both cases the simulation is laminar. In order to avoid this source of confusion, the user should use the parameter `simulationType` to perform a laminar calculation.

Independent from all other settings, `printCoeffs` prints the model constants of the selected turbulence model. This may also lead to confusion, when e.g. `turbulence off` is chosen to conduct a laminar simulation.

Exceptions

The above explanation only applies to solvers that utilize the generic turbulence models of OpenFOAM. However, there is no rule without its exceptions.

simpleFoam This solver uses only RAS turbulence models. Therefore, the entries of the file `turbulenceProperties` are redundant and the only ways to control turbulence modelling are items 2 and 3 of the list above.

twoPhaseEulerFoam This solver has the $k-\epsilon$ turbulence model hardcoded. Only item 3 of the list above applies to this solver. See Section 39.6.2 for a detailed discussion.

bubbleFoam The same as `twoPhaseEulerFoam`.

multiphaseEulerFoam This solver only uses LES turbulence models. Items 2 and 3 of the list above apply.

39.6.2 Turbulence models in `twoPhaseEulerFoam`

In the solver `twoPhaseEulerFoam`, the use of the $k-\epsilon$ turbulence model is hardcoded. This means that the solver does not use the generic turbulence modelling usually used by OpenFOAM solvers. The only choice the user of `twoPhaseEulerFoam` has is whether to enable or disable the $k-\epsilon$ turbulence model.

For this reason, the file `constant/turbulenceProperties` is not needed any more. This file can safely be deleted.

Another consequence of the $k-\epsilon$ turbulence model being hardcoded into *twoPhaseEulerFoam* is that the keyword **turbulenceProperties** in the file **RASproperties** is also not needed any more. This entry is only read if the generic turbulence modelling is used and if there is any choice of which RAS-model to use. The only mandatory keyword in **RASproperties** is the switch **turbulence**. This switch is the only way to decide whether to use turbulence modelling or not with *twoPhaseEulerFoam*. Solvers which use the generic turbulence modelling offer three possible ways to disable turbulence modelling, see Section [39.6.1](#).

39.6.3 Laminar simulation with *twoPhaseEulerFoam*

If *twoPhaseEulerFoam* is used and a laminar simulation is conducted, then the presence of the files like *0/k* or *0/epsilon* is mandatory. The solver read this files regardless of the fact, that a laminar simulation is conducted. This is due to the fact that the use of the $k-\epsilon$ model is hardcoded into *twoPhaseEulerFoam*.

Other solvers read this files based on the condition if and which turbulence model is used. Otherwise there would be the need for all possible files (*0/k*, *0/epsilon*, *0/omega*, etc.) to be present in any case, which would be utter madness.

39.6.4 Initial and boundary conditions

All turbulence models can be divided into classes depending on their mathematical properties.

Algebraic models These models add an algebraic equation to the problem. The turbulent viscosity is computed from known quantities using an algebraic equation (e.g. the Baldwin-Lomax model)

One equation models These models introduce an additional transport equation to the problem. The eddy viscosity is computed from this additional quantity (e.g. the Spalart-Allmaras model)

Two equation models These models introduce two additional transport equations to the problem. The eddy viscosity is computed from these additional quantities (z.B. $k-\epsilon$, $k-\omega$)

Every field quantity of a turbulence model needs its initial and boundary conditions. Consequently, there may be the need for additional files in the *0*-directory. One way to find out which files are needed is to look at the tutorials. There, a case may be found which utilises the needed turbulence model.

If a simulation is started and the solver is missing files – i.e. the solver tries to read files which are not present – then OpenFOAM will issue a corresponding error message. Listing 255 shows an error message of a case with a missing *0/k* file.

```
Selecting turbulence model type RASModel
Selecting RAS turbulence model kEpsilon
--> FOAM FATAL IO ERROR:  cannot find file
file: /home/user/OpenFOAM/user-2.1.x/run/pisoFoam/cavity/0/k at line 0.

From function regIOobject::readStream()
in file db/regIOobject/regIOobjectRead.C at line 73.

FOAM exiting
```

Listing 255: Solver error message: missing file

39.6.5 Additional files

RAS turbulence models produce additional files. Most RAS models calculate the turbulent viscosity from certain quantities. These quantities are usually field quantities and depend on the used turbulence model. However, the aim of all RAS turbulence models is to calculate the turbulent viscosity. The turbulent viscosity itself is a field quantity.

Listing 256 shows the folder contents before and after a simulation with *pisoFoam*. The *0*-directory contains only the mandatory files, in this case pressure and velocity as well as the turbulent quantities k and ϵ .

After the simulation has finished, the *0*-directory contains more files. The reason for creating the **.old* files is not known. However, the turbulence model created the file **nut** for storing the turbulent viscosity.

The file **phi** as well as the folder **uniform** is created by the solver.

```

user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ ls
0 constant system
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ ls 0/
epsilon k p U
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ pisoFoam > /dev/null
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ ls
0 0.5 1 constant system
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ ls 0/
epsilon epsilon.old k k.old nut p U
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$ ls 0.5/
epsilon k nut p phi U uniform
user@host:~/OpenFOAM/user-2.1.x/run/pisoFoam/ras/cavity$
```

Listing 256: Folder contents at the begin and the end of a simulation

The θ -directories of some tutorial cases may already contain such additional files, e.g. `nut`. In some cases the θ -directory may also contain several of such files due to a change in the naming scheme. Listing 257 shows the contents of the θ -directory of the *pitzDaily* tutorial case of *simpleFoam*. The case has not been run, so the files `nut` and `nuTilda` have not been generated by the solver. None of these two files is necessary to run the case with the $k-\epsilon$ turbulence model.

```
epsilon k nut nuTilda p U
```

Listing 257: The content of the θ -directory of the *pitzDaily* tutorial case of *simpleFoam*

39.6.6 Spalart-Allmaras

The Spalart-Allmaras is a one-equation turbulence model. Although it introduces only one additional equation to the problem it needs two additional files in the θ -directory. Listing 258 shows the content of the θ -folder of the *airFoil2D* tutorial case of *simpleFoam*. The files `nut` and `nuTilda` are both necessary to run the case. The former contains the turbulent viscosity and the latter contains the transported quantity of the turbulence model. Therefore, the rule *one additional transport equation entails one additional data file* is not violated.

Because the viscosity is not constant it has to be defined in a file in the θ -directory. And, because the viscosity is not the transported quantity of the Spalart-Allmaras model another file is added to the θ -directory.

```
nut nuTilda p U
```

Listing 258: The content of the θ -directory of the *airFoil2D* tutorial case of *simpleFoam*

40 Thermophysical modelling

OpenFOAM features a rich selection of models to account for a fluid's thermophysical properties, reaching from constant properties to elaborate models. While the official guide, see cfd.direct/openfoam/user-guide/thermophysical/, does a good job of summarizing the models, I feel the need to share some (non-)wisdom of mine on this topic.

40.1 The modelling framework

Much like the fully-templated turbulence modelling framework, the thermophysical modelling framework is also heavily templated. From inspecting the source code of OpenFOAM-1.1, which is the oldest version¹³³ that your trusted author has the source code for, this seems to have always been designed this way. However, the framework got extended over time to accommodate more models; and to be more granular, e.g. to also accommodate thermophysical modelling of solids.

40.1.1 The base classes

Similar to the turbulence modelling framework, there is a hierarchy of base classes, and a hierarchy of class templates. Figure 123 shows the class hierarchy of the base classes for the thermophysical modelling framework.

At the top is the class `basicThermo`, which is derived only from `I0dictionary`. `basicThermo` represents the smallest common denominator of all of OpenFOAM's thermophysical models. This class holds a reference to the pressure field and it contains the temperature field¹³⁴ as well as the laminar thermal diffusivity.

¹³³For the interested historians among the readers, visiting the following site is recommended: the repository at sourceforge <https://sourceforge.net/projects/foam/files/foam/>, and the archived versions section on the OpenFOAM homepage <https://openfoam.org/download/archive/>.

¹³⁴This is the reason that we can't find any code which reads the temperature field when we study the source code of solvers that involve temperature in some way, e.g. heat-transfer or compressible solvers. Another hint for the thermophysical model being the owner respectively the handler of the temperature field is that in `chtMultiRegionFoam` the temperature is accessed via `thermo.T()`.

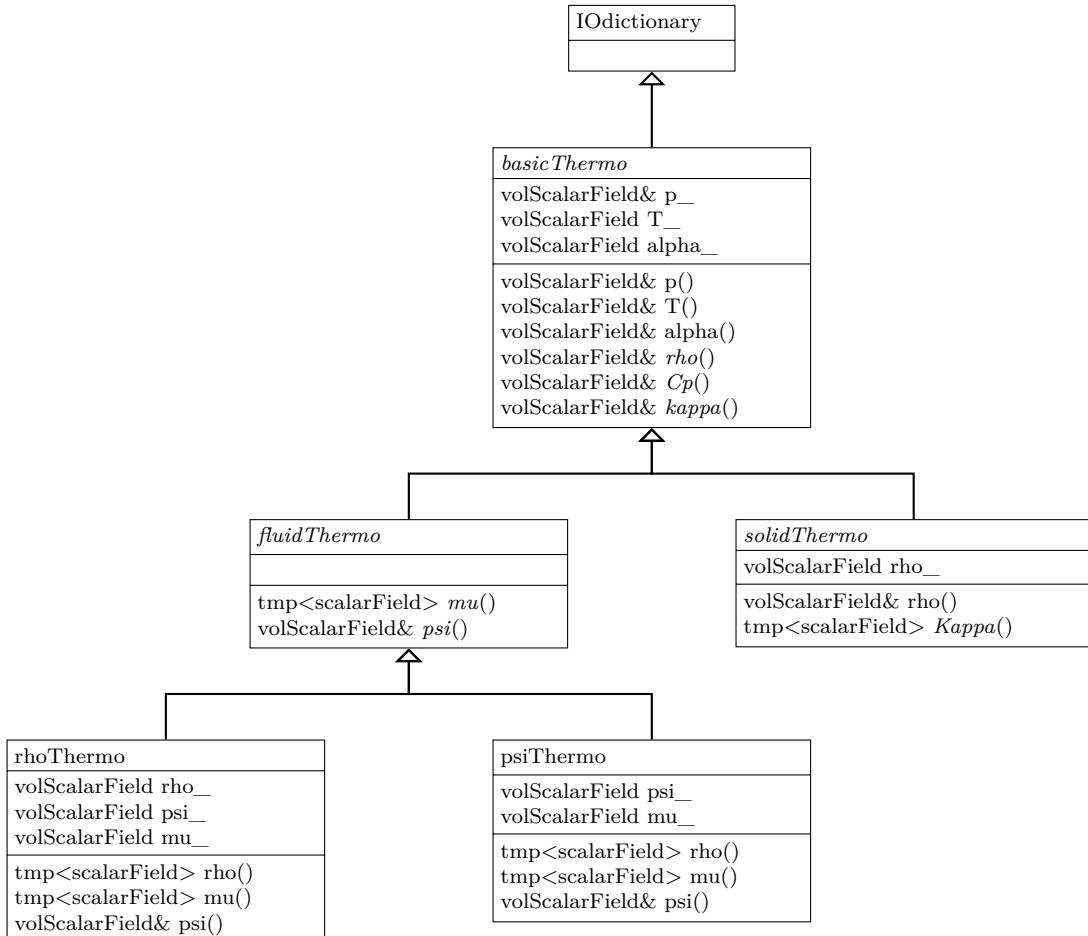


Figure 123: The class hierarchy of the basis of the thermophysical modelling framework in OpenFOAM-7.

The next classes down the family tree are `fluidThermo` and `solidThermo`. The class `solidThermo` is derived only from `basicThermo` and it holds a density field. The `solidThermo` class extends the thermal conductivity `kappa()`, which is provided by `basicThermo`, by an anisotropic thermal conductivity `Kappa()`. Anisotropic heat conduction is a property only solids can exhibit.

The class `fluidThermo` on the other hand is also derived from the class `compressibleTransportModel`, which is not shown in Figure 123. `fluidThermo` does not hold own data members, however it provides methods which are relevant for fluids, e.g. access to viscosity.

From `fluidThermo` the two classes `rhoThermo` and `psiThermo` are derived, which model thermodynamic properties based on density respectively compressibility.

The classes discussed in this section are base classes since these classes are used by the solvers of OpenFOAM. See the Listings 259 and 260, in which the thermophysical model is created, and used to access the temperature field.

```

1 Info<< "Reading thermophysical properties\n" << endl;
2
3 autoPtr<rhoThermo> pThermo(rhoThermo::New(mesh));
4 rhoThermo& thermo = pThermo();
5 thermo.validate(args.executable(), "h", "e");
6
7 volScalarField rho
8 (
9     IOobject
10    (
11        "rho",
12        runTime.timeName(),
13        mesh,
14        IOobject::NO_READ,
```

```

15     IOobject::NO_WRITE
16 ),
17 thermo.rho()
18 );
19
20 volScalarField& p = thermo.p();

```

Listing 259: An extract of *buoyantPimpleFoam*'s `createFields.H` file. Note the creation and the use of the thermophysical model.

```

1 // Initialise solid field pointer lists
2 PtrList<solidThermo> thermos(solidRegions.size());
3
4 // Populate solid field pointer lists
5 forAll(solidRegions, i)
6 {
7     Info<< "*** Reading solid mesh thermophysical properties for region "
8         << solidRegions[i].name() << nl << endl;
9
10    Info<< "      Adding to thermos\n" << endl;
11    thermos.set(i, solidThermo::New(solidRegions[i]));
12
13    Info<< "      Adding to radiations\n" << endl;
14    radiations.set(i, radiationModel::New(thermos[i].T()));

```

Listing 260: An extract of *chtMultiRegionFoam*'s `createSolidFields.H` file. Note the creation and the use of the thermophysical model.

An interesting observation on the pressure field

In Listing 259, we see that the solver's reference to the pressure field is provided by the thermophysical model, see Line 20 of that listing. As the `basicThermo` model holds only a reference to the pressure field, in contrast, the `basicThermo` model holds the temperature field as a field; i.e. the `basicThermo` “owns” the temperature field but only refers to the pressure field. Thus, we are left with the puzzle who created the pressure field, since the thermophysical model is able to provide the pressure field immediately after its construction, we turn our attention to the base classes of the thermophysical models.

Taking a look at the constructor of the class `basicThermo`, it appears as if the pressure field needs to be already existing, see Line 19 in Listing 261. The method `lookupOrConstruct()` strongly reminds us of the various `lookup*`() methods provided by OpenFOAM's object registry, see Section 68.7. However, this is not the case with this class: the method `lookupOrConstruct()` is provided by the class `basicThermo` itself, see Listing 262. This is actually a pretty elegant way to handle the pressure field.

This approach allows the designers of OpenFOAM not to care about the pressure field in regards to the thermophysical models. E.g. in multiphase solvers, there are two or more thermophysical models constructed, one for each phase, and the constructor of the first thermophysical model creates the pressure field, whereas all subsequent constructor-calls result in a look-up from the object registry.

```

1 Foam::basicThermo::basicThermo
2 (
3     const fvMesh& mesh,
4     const word& phaseName
5 )
6 :
7     IOdictionary
8     (
9         IOobject
10        (
11            phasePropertyName(dictName, phaseName),
12            mesh.time().constant(),
13            mesh,
14            IOobject::MUST_READ_IF_MODIFIED,
15            IOobject::NO_WRITE
16        )
17    ),
18    phaseName_(phaseName),
19    p_(lookupOrConstruct(mesh, "p")),

```

```

20   T_
21   (
22     IOobject
23     (
24       phasePropertyName("T"),
25       mesh.time().timeName(),
26       mesh,
27       IOobject::MUST_READ,
28       IOobject::AUTO_WRITE
29     ),
30     mesh
31   ),

```

Listing 261: An extract of a constructor of the class `basicThermo`.

```

1  Foam::volScalarField& Foam::basicThermo::lookupOrConstruct
2  (
3    const fvMesh& mesh,
4    const char* name
5  ) const
6  {
7    if (!mesh.objectRegistry::foundObject<volScalarField>(name))
8    {
9      volScalarField* fPtr
10     (
11       new volScalarField
12       (
13         IOobject
14         (
15           name,
16           mesh.time().timeName(),
17           mesh,
18           IOobject::MUST_READ,
19           IOobject::AUTO_WRITE
20         ),
21         mesh
22       )
23     );
24     // Transfer ownership of this object to the objectRegistry
25     fPtr->store(fPtr);
26   }
27   return mesh.objectRegistry::lookupObjectRef<volScalarField>(name);
28 }

```

Listing 262: The method `lookupOrConstruct()` of the class `basicThermo`.

40.1.2 The class templates

`heThermo`

Thermophysical modelling is all about the modelling of the temperature-dependent behaviour of a fluid or solid. Fully accommodating thermophysical modelling into a solver necessitates the inclusion of the energy conservation equation, which means we need to provide the solver with an energy field.

This energy field can be either the specific enthalpy `h` or the specific internal energy `e`. Using the specific enthalpy to solve the energy conservation equation was apparently done right from the start, code that uses `h` is around in OpenFOAM-1.1. The internal energy field `e` makes its debut¹³⁵ in OpenFOAM-1.6 with some of the compressible solvers.

From OpenFOAM-2.2.0 onwards¹³⁶, the class `heThermo` was used to provide the specific enthalpy respectively the specific internal energy. This is possible since both enthalpy and internal energy have the same physical unit, and are closely related.

¹³⁵Interestingly, the `ReleaseNotes` file of OpenFOAM-1.6 talks of a **New* (reinstated) =eThermo= thermodynamics package*. Prior to OpenFOAM-1.6, the specific internal energy `e` was only used by the `sonicFoam` solver in the form of a direct implementation without an underlying thermophysical model based on the internal energy.

¹³⁶<https://openfoam.org/release/2-2-0/thermophysical-multiphase-energy/>

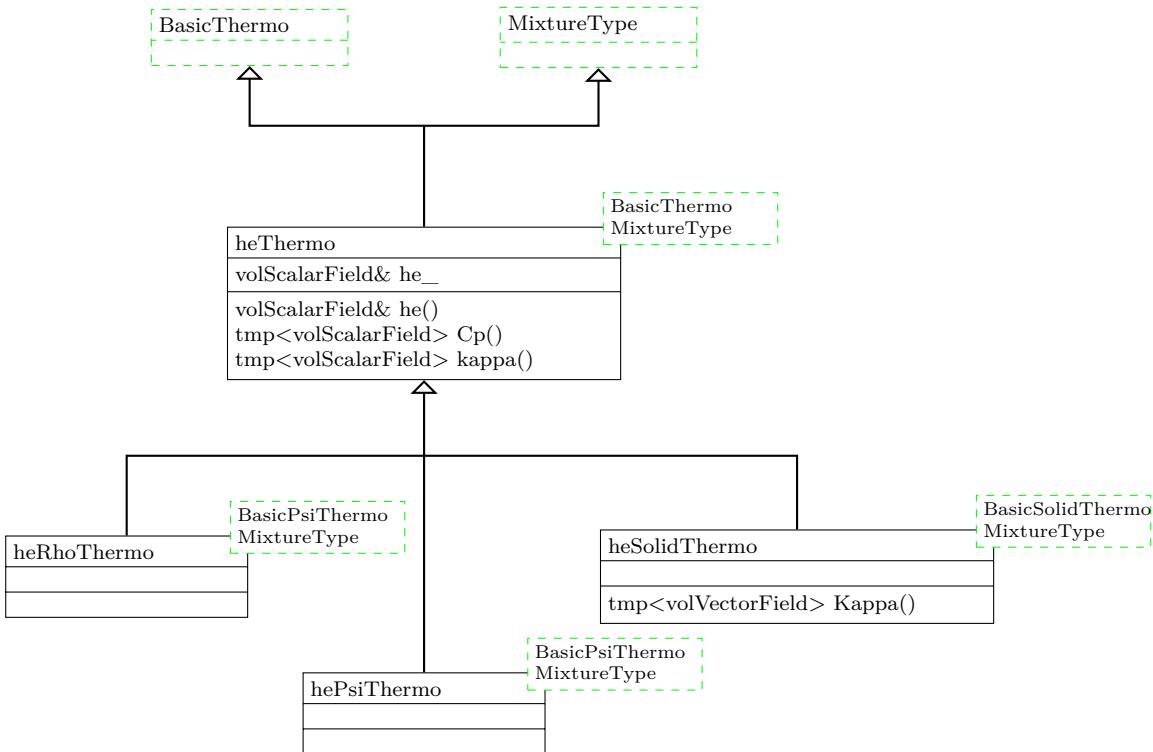


Figure 124: The class hierarchy of the templated classes of the thermophysical modelling framework in OpenFOAM-7.

Figure 124 shows the class hierarchy around the class `heThermo`, which serves the thermophysical modelling needs of both fluids and solids. As the need for a representation of thermal energy is independent of the simulated medium being a fluid or solid, the class providing this representation serves them both.

If we compare Figures 123 and 124, we see that the class `heThermo` provides the methods `Cp()` and `kappa()`, which were abstract methods in the class `basicThermo`. Furthermore, the class `heSolidThermo` now provides the method `Kappa()`, which was an abstract method in the class `solidThermo`.

40.2 Model selection

The framework for thermophysical modelling requires us to select a model for each of seven categories, see Listing 263 for an example. If you are unsure of the available options, just apply the *banana test*, i.e. enter a ridiculous value, and OpenFOAM will tell you the valid options.

```
thermoType
{
    type          hePsiThermo;
    mixture      pureMixture;
    transport    sutherland;
    thermo       janaf;
    equationOfState perfectGas;
    specie       specie;
    energy        sensibleInternalEnergy;
}
```

Listing 263: The selection of thermophysical models in the file `thermophysicalProperties` in the `constant` directory.

The only entry in the `thermoType` dictionary, which eludes the *banana test* is the entry for the keyword `specie`, since this is the only available option.

40.3 specie

The only entry in the specie dictionary in the thermophysical properties is the molar mass or molar weight, as seen in Listing 264. While the content of that listing is taken from a random tutorial case, it is representative of all tutorial cases¹³⁷.

```
mixture
{
    specie
    {
        molWeight    28.9647;
    }
    // ...
}
```

Listing 264: Specifying the molar weight in the `specie` sub-dictionary in the file `thermophysicalProperties` in the `constant` directory.

Note that the molar weight M in OpenFOAM is defined as being stated in the unit $\frac{\text{g}}{\text{mol}}$ or $\frac{\text{kg}}{\text{kmol}}$. If we wanted to compute a gas density, using the ideal gas law, from pressure, temperature and specific gas constant R_s , we need to take the units into account.

$$\rho = \frac{p}{R_s T} \quad (44)$$

with

$$R_s = \frac{R}{M} \quad (45)$$

The “proper” SI units are kilogram for mass and mole for the amount of a substance. Thus, $\frac{\text{g}}{\text{mol}}$ and $\frac{\text{kg}}{\text{kmol}}$ are both not quite properly stated in SI units, see Listing 273.

OpenFOAM accounts for this implicitly, since it specified the universal gas constant also in terms of kilomoles. Thus, when computing the specific gas constant by dividing the universal gas constant by the molar weight, we have kilomoles in both operands, thus they cancel out and yield the specific gas constant in proper SI units.

Prior to OpenFOAM-5, the number of moles was also stated, however, due to a rewrite of the code¹³⁸, this is no longer necessary. We find in some tutorial cases an additional entry `nMoles`, which is a hold-over from those earlier times.

40.4 transport models

The transport model deals among others with the computation of the fluid viscosity as well as thermal conductivity and diffusivity.

40.4.1 const

The constantTransport model provides constant properties. The model reads the dynamic viscosity μ and the Prandtl number Pr from its coefficient-dictionary.

$$\kappa = \frac{C_p \mu}{Pr} \quad (46)$$

Listing 265 shows how the dynamic viscosity and the Prandtl number are provided in an OpenFOAM case.

```
mixture
{
    transport
    {
        mu          18.205e-06;
```

¹³⁷You can try by executing the following command: `find $FOAM_TUTORIALS -type f | xargs grep molWeight -B 2 -A 2` and be prepared to scroll at lot. However, you will find that in almost all cases, `molWeight` is the only entry.

¹³⁸See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/abc50e214c45ae86d86ccded08da8e6dd1610182>

```

    Pr          0.7081;
}
// ...

```

Listing 265: The coefficients for the `const` transport model stated in the `transport` sub-dictionary in the file `thermophysicalProperties` in the `constant` directory.

40.4.2 Sutherland

The Sutherland transport model computes the viscosity from Sutherland's formula [60].

Viscosity

The Sutherland formula computes the dynamic viscosity μ from two model parameters A_s and T_s .

$$\mu = A_s \frac{\sqrt{T}}{1 + T_s/T} \quad (47)$$

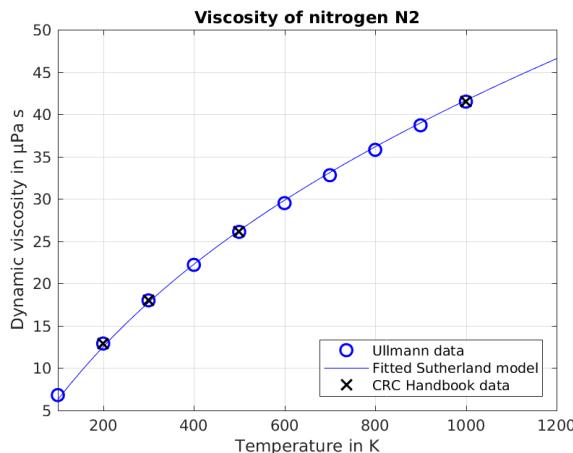


Figure 125: The dynamic viscosity of nitrogen: the model coefficients were fitted to data reported in [16], the model is compared to values reported in [2].

Thermal conductivity

For the thermal conductivity κ a modified Eucken correlation is used [54], which computes the thermal conductivity from the viscosity and other properties. This can be done, since the temperature dependence of the thermal conductivity is approximately the same as the temperature dependence of the viscosity [18, 23, 24].

$$\kappa = \mu c_v \left(1.32 + \frac{1.77 R_s}{c_v} \right) \quad (48)$$

Note that R_s in (48) is the specific gas constant. If we take a look at the actual source code in Listing 266, then we might be under the impression that we need the universal gas constant R . However, this is not the case. See Section 40.8.1 for further information.

In Line 8 of Listing 266 we see the modified Eucken relation from Eq. (48) translated into C++ and OpenFOAM.

```

1 template<class Thermo>
2 inline Foam::scalar Foam::sutherlandTransport<Thermo>::kappa
3 (
4     const scalar p, const scalar T
5 ) const

```

```

6  {
7      scalar Cv_ = this->Cv(p, T);
8      return mu(p, T)*Cv_*(1.32 + 1.77*this->R()/Cv_);
9 }

```

Listing 266: The method `kappa` of the class `sutherlandTransport`.

In Figure 126, we compare the thermal conductivity returned by the Sutherland model with data reported in literature [16, 2]. For the specific heat capacity, we used the JANAF model with OpenFOAM's model coefficients for nitrogen, which can be found in the file `$FOAM_ETC/thermoData/thermoData`. The good fit between the values of the Sutherland model and the reported data from literature shows the validity of the modified Eucken correlation.

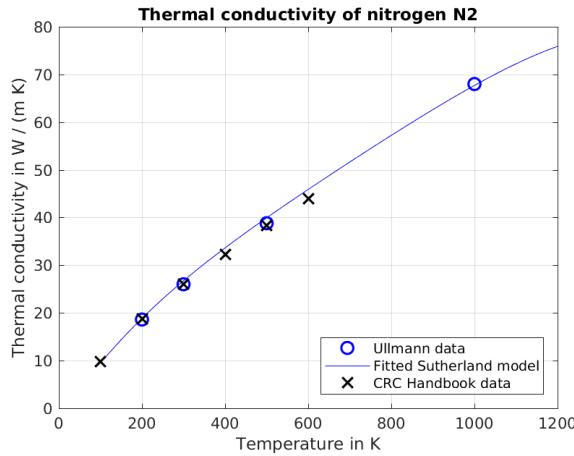


Figure 126: The thermal conductivity of nitrogen: the model is using a modified Eucken correlation with the viscosity model, which was fitted to viscosity data reported in [16], the model is compared to values of thermal conductivity reported in [2, 16].

Pitfall: standard units

When you are fitting model parameters for the Sutherland model to measured data from literature, make sure to use the correct values. OpenFOAM generally uses SI units¹³⁹ for all its computations. Thus, for dynamic viscosity the appropriate unit is the Pascal seconds Pa s. However, in literature, we often find the values for dynamic viscosity given in micro Pascal seconds $\mu\text{Pa s}$.

Fitting the model parameters to viscosity data given in $\mu\text{Pa s}$ will cause the parameter A_s to be too high by a factor of 10^6 . Make sure to use the correct values, when fitting model parameters.

40.4.3 WLF

This model is based on the work of Williams et al. [70].

$$\mu = \mu_0 \exp \left(\frac{-C_1(T - T_r)}{C_2 + T - T_r} \right) \quad (49)$$

The thermal conductivity is provided by this model by using the Prandtl number. Note that `rPr_` in Line 8 of Listing 267 is the reciprocal Prandtl number.

```

1 template<class Thermo>
2 inline Foam::scalar Foam::WLFTtransport<Thermo>::kappa
3 (
4     const scalar p,
5     const scalar T
6 ) const

```

¹³⁹Technically, OpenFOAM can also use USCS units, yet why would one choose to use non-SI units?

```

7  {
8     return this->Cp(p, T)*mu(p, T)*rPr_;
9 }
```

Listing 267: Definition of the thermal conductivity in the source code of the WLF model.

40.4.4 Andrade

The Andrade model [7, 8] allows to fit viscosity and thermal conductivity separately. This model was introduced into OpenFOAM sometime after the release of OpenFOAM-9.

$$\log \mu = C_{\mu,0} + C_{\mu,1}T + C_{\mu,2}T^2 + \frac{C_{\mu,3}}{C_{\mu,4} + T} \quad (50)$$

$$\log \kappa = C_{\kappa,0} + C_{\kappa,1}T + C_{\kappa,2}T^2 + \frac{C_{\kappa,3}}{C_{\kappa,4} + T} \quad (51)$$

Figure 127 shows the curves of the WLF and the Andrade model fitted to some data from literature. Not shown in the plot, is the divergence of the WLF curve. As one can see from Eq. (49), the denominator vanishes for a temperature of approximately 145 K. While this temperature is well out of the reasonable range for temperatures of a natural convection case involving an aqueous liquid, a viscosity model that returns bounded values seems nevertheless preferable. The Andrade model, seeing from Eq. (50), can also diverge when the denominator vanishes, this happens at a temperature of approximately 0.05 K.

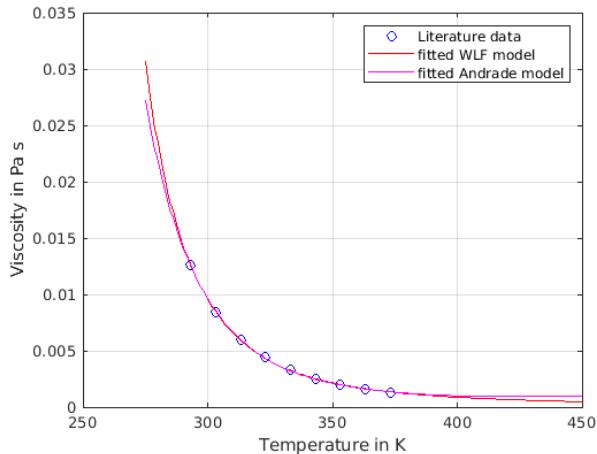


Figure 127: The viscosity of a fluid and the viscosity computed by the WLF and Andrade models fitted to the data.

40.5 thermo

The thermo model deals with the computation of the specific heat and other derived properties.

40.5.1 JANAF

The name JANAF stems from the Joint-Army-Navy-Air Force Thermochemical Working Group, which published thermodynamic properties of many compounds from the 1960s onwards. We also find references to JANNAF, which brings the NASA into the abbreviation. Furthermore, the polynomials underlying the JANAF tables are also referred to as the *NASA polynomials* or the *7 term NASA polynomials*¹⁴⁰.

In the time of limited computer resources, especially memory, polynomials were a very effective way of making the vast body of experimentally determined thermodynamic data usable for computing. Thus, huge amounts of data were reduced by virtue of polynomial-fitting to a small, finite number of polynomial coefficients [15].

¹⁴⁰http://combustion.berkeley.edu/gri_mech/data/nasa_plnm.html

Furthermore, the recursive formulation of (53) is considered most efficient in terms of the involved computational operations and memory [15].

The JANAF model is one of the thermo models provided by OpenFOAM. The JANAF model depends on two sets of model coefficients. The `lowCpCoeffs` are used when the temperature is below the threshold `Tcommon`, when temperatures are higher the coefficients in `highCpCoeffs` are used. Mathematically spoken, the JANAF model implements the following equation:

$$a = \begin{cases} \text{lowCpCoeffs} & T_{\text{low}} \leq T < T_{\text{common}} \\ \text{highCpCoeffs} & T_{\text{common}} \leq T \leq T_{\text{high}} \end{cases} \quad (52)$$

$$C_p = (((a_4 T + a_3)T + a_2)T + a_1)T + a_0 \quad (53)$$

The JANAF model coefficients are two sets of 7 coefficients. Using two polynomials allows to cover a wide temperature range. Thus, the first polynomial usually covers the low temperature region, 200-1000 K, whereas the second covers the high temperature region, 1000-6000 K. The two polynomials are constrained to yield the 1000 K value. Furthermore, the polynomial for the low temperature region is *pinned* to 298.15 K, which serves, in combination with a pressure of 1 bar, as the standard reference state. Pinning the polynomial to the standard state ensures, that the thermodynamic properties are exactly reproduced at the standard state [15].

The first 5 coefficients of a polynomial are used for computing the specific heat capacity C_p , as shown above. The remaining two coefficients are used to compute the enthalpy and the entropy. In Listing 268 an example, for the way JANAF model coefficients are defined, is shown.

```

mixture
{
    thermodynamics
    {
        Tlow           200;
        Thigh          6000;
        Tcommon        1000;
        highCpCoeffs   ( 3.08793 0.00124597 -4.23719e-07 6.74775e-11 -3.97077e-15 -995.263 5.95961 );
        lowCpCoeffs    ( 3.5684 -0.000678729 1.55371e-06 -3.29937e-12 -4.66395e-13 -1062.35 3.71583 );
    }
}

```

Listing

268:

The model coefficients of the JANAF thermophysical model in the file `thermophysicalProperties` in the `constant` directory.

In OpenFOAM's `etc/thermoData/thermoData` the JANAF coefficients for a large number of species can be found. However, if we want to use the JANAF model outside of OpenFOAM, e.g. in a MATLAB/Octave script, it turns out that these coefficients need to be multiplied by the specific gas constant of the respective species. As shown in Listing 269, this is done by the constructor automatically, see Lines 14 and 15 of Listing 269.

```

1 template<class EquationOfState>
2 Foam::janafThermo<EquationOfState>::janafThermo(const dictionary& dict)
3 :
4     EquationOfState(dict),
5     Tlow_(readScalar(dict.subDict("thermodynamics").lookup("Tlow"))),
6     Thigh_(readScalar(dict.subDict("thermodynamics").lookup("Thigh"))),
7     Tcommon_(readScalar(dict.subDict("thermodynamics").lookup("Tcommon"))),
8     highCpCoeffs_(dict.subDict("thermodynamics").lookup("highCpCoeffs")),
9     lowCpCoeffs_(dict.subDict("thermodynamics").lookup("lowCpCoeffs"))
10 {
11     // Convert coefficients to mass-basis
12     for (label coefLabel=0; coefLabel<nCoeffs_; coefLabel++)
13     {
14         highCpCoeffs_[coefLabel] *= this->R();
15         lowCpCoeffs_[coefLabel] *= this->R();
16     }
17
18     checkInputData();
19 }

```

Listing 269: The constructor of the class `janafThermo`.

In Figure 128 the specific heat capacity of air computed with the JANAF model is compared to data from [64].

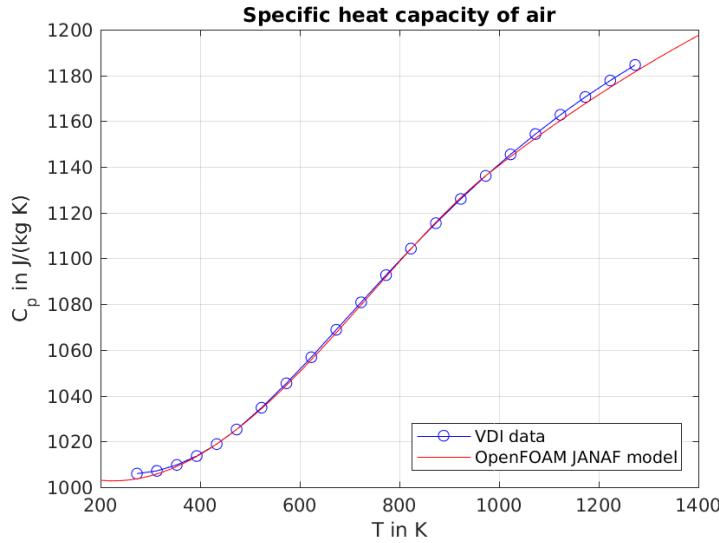


Figure 128: Specific heat capacity C_p of air computed with the JANAF model compared to data from [64].

40.6 equationOfState

The equation of state covers the computation of the fluid's density.

40.6.1 rhoConst

The `rhoConst` model provides a constant density. The model reads a density value from its coefficient dictionary.

40.6.2 perfectGas

This model uses the eponymous perfect gas model to compute the density from the other two state variables, i.e. pressure and temperature. This model does not require a coefficient dictionary, as it uses three states of the fluid (pressure, density and temperature), and the specific gas constant, which can readily be determined.

$$\rho = \frac{p}{R_s T} \quad (54)$$

Pitfall: zero pressure

Some rather odd behaviour was observed, when tinkering with cases. In this instance, files from an incompressible case ended up in an compressible case, which had the `perfectGas` selected as the `equationOfState`. Apart from a looming error due to the different dimensions of pressure in incompressible and compressible cases, another error was triggered.

As it is common with incompressible cases, the internal field value for the pressure was set to zero. When the compressible solver was launched, the following, quite cryptic error message was issued by OpenFOAM.

```
Selecting turbulence model type laminar
Selecting laminar stress model Stokes
Creating field dpdt

Creating field kinetic energy K

No MRF models present

No finite volume options present

#0  Foam::error::printStack(Foam::Ostream&) at ???:?
#1  Foam::sigFpe::sigHandler(int) at ???:?
#2  ? in "/lib/x86_64-linux-gnu/libc.so.6"
```

```

#3 Foam::divide(Foam::Field<double>&, Foam::UList<double> const&, Foam::UList<double> const&)
    at ???:?
#4 Foam::operator/(Foam::UList<double> const&, Foam::UList<double> const&) at ???:?
#5 ? at ???:?
#6 __libc_start_main in "/lib/x86_64-linux-gnu/libc.so.6"
#7 ? at ???:? Floating point exception (Core dumped)

```

Listing 270: A quite un-informative error message of *rhoPimpleFoam*.

The error message looks different, when a turbulence model other than laminar is selected. In this case, the error message is slightly more informative, as the error occurs within the turbulence model framework. If such an error occurs there, then the error message contains at least the method name, in which the error happened.

At some point, at the construction of all the necessary models, OpenFOAM inevitably divides by the density, which evaluates to zero in the case of zero pressure. In the case shown above, the laminar model was selected, which does not need to divide by the density.

The remarkable thing with the error message in Listing 270 is, that it contains no information other than that a floating point exception occurred during dividing numbers.

40.7 Energy

The thermophysical modelling framework of OpenFOAM allows for the use of internal energy or enthalpy as the primary variable describing the energy of the fluid¹⁴¹.

40.7.1 Solids

For solids, using internal energy seems to be the proper choice, as indicated by the following commit message¹⁴²:

chtMultiRegionFoam: Changed solid energy from enthalpy to internal energy

The solid is currently assumed incompressible (the solid pressure is not updated) and in general would be near incompressible so internal energy is a more appropriate energy choice than enthalpy which would require a pressure work term currently not implemented. Additionally due to the way in which the conduction is handled in terms of the gradient of energy the accuracy of the current enthalpy implementation is sensitive to the pressure distribution as this introduces an enthalpy gradient from the p/rho term which would need to be corrected; this issue is avoided by solving for internal energy instead.

This is consistent with the CHT tutorials of OpenFOAM-9.

40.7.2 Fluids

For incompressible or weakly compressible fluids, solving for internal energy seems favourable as indicated by the following commit message¹⁴³:

thermophysicalModels::equationOfState: Completed departure functions for all except adiabaticPerfectFluid

Changed liquid thermo from sensibleEnthalpy to sensibleInternalEnergy in tutorials. It is generally more convergent and stable to solve for internal energy if the fluid is incompressible or weakly compressible.

In the tutorials, the choice of internal energy versus enthalpy is not that clear as in the case of solids. With fluids we can find both uses.

Steady-state

However, another commit message states that enthalpy is preferable for steady-state cases¹⁴⁴:

tutorials/heatTransfer/buoyantSimpleFoam: Updated solver settings to improve convergence

Also changed from internal energy to enthalpy which is preferable for steady-state simulations.

¹⁴¹<https://cfd.direct/openfoam/energy-equation/>

¹⁴²<https://github.com/OpenFOAM/OpenFOAM-dev/commit/c109bec4cc3702ac6dba172efdd30ec6916e73a1>

¹⁴³<https://github.com/OpenFOAM/OpenFOAM-dev/commit/f9971f80d72a5318cdc81120a925ab9817b3ec62>

¹⁴⁴<https://github.com/OpenFOAM/OpenFOAM-dev/commit/5df9ec5b1e937817764adaf2932b964a1d188754>

40.8 Thermophysical properties

40.8.1 Pitfall: the gas constant(s)

The class `specie` provides the method `R()` to return the gas constant.

```
1 // - Gas constant [J/kg/K]
2 inline scalar R() const;
```

Listing 271: The declaration of the method `R()` in the header-file of the class `specie`.

```
1 inline scalar specie::R() const
2 {
3     return RR/molWeight_;
4 }
```

Listing 272: The implementation of the method `R()` in the header-file of the class `specie`.

The implementation in Listing 272 strongly suggests that the method `R()` returns a specific gas constant. This is confirmed by looking at Listing 273.

```
1 // - Universal gas constant (default in [J/kmol/K])
2 extern const scalar RR;
```

Listing 273: The declaration of the universal gas constant in the file `thermodynamicConstants.H`.

In this case, regarding the universal and specific gas constants, OpenFOAM's notation is not following the widely used convention to denote the universal gas constant as R , and the specific gas constant as R_s [50].

40.9 Mixture

OpenFOAM can not only deal with pure fluids, it can also deal with mixtures: e.g. a combustion solver solves for momentum and energy transport for a single gas phase, whereas the gas phase consists of the gaseous fuel (methane), the gaseous oxidizer (oxygen), the gaseous oxidation products (carbon-dioxide) and inert gases (nitrogen). The properties of the gas phase are evaluated on a cell-by-cell basis for the mixture of all gaseous species.

40.9.1 pureMixture

For a pure fluid, a dictionary named `mixture` contains the model definitions for all necessary sub-models.

```
mixture
{
    specie
    {
        //
    }

    thermodynamics
    {
        //
    }

    transport
    {
        //
    }
}
```

Listing 274: The definition of thermophysical modelling in the file `thermophysicalProperties` for a pure fluid.

40.9.2 multiComponentMixture

Thermophysical modelling

With the `multiComponentMixture` model, we need to provide a list of species, and a definition the thermophysical modelling for each individual species. The thermophysical modelling definition of the individual species follows the same pattern as the definition of the thermophysical modelling for pure fluids, see Section 40.9.1.

```
species
(
    Ar
    H2
);

Ar
{
    //
}

H2
{
    //
}
```

Listing 275: The definition of thermophysical modelling in the file `thermophysicalProperties` for a mixture of several fluids.

Composition

The composition of a `multiComponentMixture` is specified with the mass fractions of the individual components. The user can provide either a `Ydefault` field, if the mass fractions are to be initialized equally; or a mass fraction field for each component. In the example of Listing 275, a user can provide the components' mass fractions as fields with the name of the components, i.e. `Ar` and `H2`. We can also provide specific mass fraction fields for a subset of components, in this case the value of `Ydefault` is applied to the remaining components.

Upon construction of the mixture, the mass fractions are normalized, such that the sum of all mass fractions is equal to one. Thus, the values in the mass fraction fields do not necessarily sum-up to one.

The mixture's properties are computed using the mass fractions, e.g. below we see the relation for the mixture's density depending of the components' mass fractions and densities.

$$m_{\text{mix}} = m_1 + m_2 \quad (55)$$

$$m_{\text{mix}} = \rho_{\text{mix}} V_{\text{CV}} \quad (56)$$

$$m_{\text{mix}} = \rho_1 V_1 + \rho_2 V_2 \quad (57)$$

$$m_{\text{mix}} = \rho_{\text{mix}} (V_1 + V_2) \quad (58)$$

with the following relation for the individual species' mass m_i

$$m_i = Y_i m_{\text{mix}} = \rho_i V_i \quad (59)$$

we can derive a relation for the mixture density

$$m_{\text{mix}} = \rho_{\text{mix}} \left(\frac{Y_1 m_{\text{mix}}}{\rho_1} + \frac{Y_2 m_{\text{mix}}}{\rho_2} \right) \quad (60)$$

$$1 = \rho_{\text{mix}} \left(\frac{Y_1}{\rho_1} + \frac{Y_2}{\rho_2} \right) \quad (61)$$

$$\rho_{\text{mix}} = \frac{1}{\frac{Y_1}{\rho_1} + \frac{Y_2}{\rho_2}} \quad (62)$$

40.10 Model combination

Note, that models can not be freely combined.

40.10.1 Polynomial models

If you would like to use polynomial models, i.e. properties such as viscosity are computed from a polynomial depending on temperature, then you are basically restricted to use polynomial models for the categories `transport`, `thermo` and `equationOfState`. In Listing 276 all possible model combinations involving a polynomial model are shown. This list was generated by applying the *banana test* and filtering OpenFOAM's output for the occurrence of the expression `olynomial`, which is common to all polynomial models.

There are some combinations involving only one or two polynomial models.

hePsiThermo	pureMixture	polynomial	hPolynomial	PengRobinsonGas	specie	sensibleEnthalpy
hePsiThermo	pureMixture	polynomial	janaf	PengRobinsonGas	specie	sensibleEnthalpy
heRhoThermo	multiComponentMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleEnthalpy
heRhoThermo	multiComponentMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleInternalEnergy
heRhoThermo	pureMixture	polynomial	hPolynomial	PengRobinsonGas	specie	sensibleEnthalpy
heRhoThermo	pureMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleEnthalpy
heRhoThermo	pureMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleInternalEnergy
heRhoThermo	pureMixture	polynomial	janaf	PengRobinsonGas	specie	sensibleEnthalpy
heRhoThermo	reactingMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleEnthalpy
heRhoThermo	reactingMixture	polynomial	hPolynomial	icoPolynomial	specie	sensibleInternalEnergy

Listing 276: The selection of thermophysical models in the file `thermophysicalProperties` in the `constant` directory.

40.11 Solids : Thermophysical modelling

With the introduction of conjugate heat transfer (CHT) modelling, the need for thermophysical models for solids arises. In OpenFOAM, CHT was introduced with OpenFOAM-1.5 and OpenFOAM-1.6. With OpenFOAM-2.0.0, thermophysical modelling for solids was introduced. Prior to this version, all relevant fields, e.g. specific heat capacity or thermal conductivity, were simply read from disk.

The available models for solids are a subset of those for fluids. Some of the models can be used by both fluids and solids, whereas in other cases there are model specifically for solids.

40.11.1 transport

Similar to the thermophysical models for fluids, the `transport` model for solids is responsible to provide the thermal conductivity. However, other than with the fluids, no viscosity is provided.

constant

The `constant` model is the simplest available model. It takes only one model parameter, i.e. the thermal conductivity.

```
transport
{
    kappa          57.4781;
}
```

Listing 277: The model coefficients of the `constant` transport model in the file `thermophysicalProperties` in the `constant` directory.

polynomial

The `polynomial` model takes the polynomial coefficients as model parameters.

```
transport
{
    kappaCoeffs<8>  (127.821 -0.267 2.844e-04 -8.84e-08 -1.3e-08 9.3e-12 -3.6e-15 5.6e-19);
}
```

Listing 278: The model coefficients of the `polynomial` transport model in the file `thermophysicalProperties` in the `constant` directory.

exponential

The **exponential** model requires three model parameters, the constant coefficient κ_0 , the exponent n_0 and the reference temperature T_{ref} .

$$\kappa = \kappa_0 \left(\frac{T}{T_{\text{ref}}} \right)^{n_0} \quad (63)$$

```
transport
{
    kappa0          0.166;
    n0              1.6187e-12;
    Tref            0.17385;
}
```

Listing 279: The model coefficients of the **exponential** transport model in the file `thermophysicalProperties` in the `constant` directory.

constant-anisotropic

A special case of solid materials are anisotropic properties, e.g. fiber composites have a distinct two-dimensional internal structure as they are made from layers of fabric infused with resin. This may lead to a variation of properties depending on whether we consider a material property in the plane of the fibers or perpendicular to this plane. Wood is another prominent example of a solid material exhibiting anisotropic properties.

The `constAnIso` model allows the user to specify the heat conductivity `kappa` as a vector.

```
transport
{
    kappa          (42.0 48.0 42.0);
}
```

Listing 280: The model coefficients of the **constant** transport model in the file `thermophysicalProperties` in the `constant` directory.

In addition to the thermal conductivity in the form of a vector, the user must also provide a coordinate system. The necessity of reading the coordinate system is due to the solver `chtMultiRegionFoam`. This is useful, when the relevant local coordinates of the solid are not aligned with the global coordinate system of the simulation domain.

Pitfall: phase change

Some solid metals undergo a phase change, in which their crystalline structure changes, e.g. when iron changes from ferrite to austenite as it is heated up. Figure 129 shows the thermal conductivity of nickel, which decreases with increasing temperature, and at some point (its phase transition) increases with increasing temperature [29].

From the available models, only the **polynomial** model is capable to incorporate a transition of the kind shown in Figure 129. The **exponential** model only depicts a strictly monotonic increase or decrease, however, not a transition from one to the other.

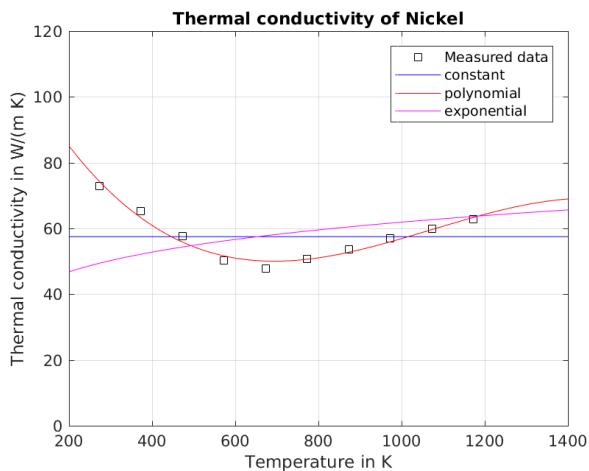


Figure 129: The thermal conductivity of nickel: data from literature [29], and the available, fitted models of OpenFOAM.

40.11.2 thermo

The `thermo` model is, similar to the case of fluids, responsible to provide the specific heat capacity, the entropy and various enthalpies.

In contrast to fluids, which offer models formulated in terms of enthalpy or internal energy, the thermophysical modelling of energy in solids is based solely on enthalpy.

`hConst`

The `hConst` model provides constant values. It reads in the specific heat capacity c_P and the standard enthalpy of formation H_f .

`hPower`

The `hPower` model computes the specific heat capacity according to Eq. (64). The model takes the model parameters of Eq. (64) and the standard enthalpy of formation H_f as inputs.

$$C_p(T) = c_0 \left(\frac{T}{T_{\text{ref}}} \right)^{n_0} \quad (64)$$

`hPolynomial`

The `hPolynomial` model computes its properties using user-provided polynomial coefficients. Additionally, it takes the standard enthalpy of formation H_f and the standard entropy S_f as model parameters.

40.11.3 equationOfState

`rhoConst`

The only valid equation of state for thermophysical modelling of solids is `rhoConst`.

40.11.4 energy

`sensibleEnthalpy`

The only valid model for energy transport for thermophysical modelling of solids is `sensibleEnthalpy`.

40.11.5 Model combination

Listing 281 shows the available models for solids in OpenFOAM-7. The model choice for solids is a small subset of the models available for fluids.

heSolidThermo	multiComponentMixture	constIso	hConst	rhoConst	specie	sensibleEnthalpy
heSolidThermo	pureMixture	constAnIso	hConst	rhoConst	specie	sensibleEnthalpy
heSolidThermo	pureMixture	constIso	hConst	rhoConst	specie	sensibleEnthalpy
heSolidThermo	pureMixture	exponential	hPower	rhoConst	specie	sensibleEnthalpy
heSolidThermo	pureMixture	polynomial	hPolynomial	rhoConst	specie	sensibleEnthalpy

Listing 281: The available thermophysical models for solids; determined with a *banana test* with the solver `chtMultiRegionFoam`.

40.12 Density: modelling degrees of (in-)compressibility

With a more realistic treatment of fluid properties, there is a range of models we can choose for our simulations.

40.12.1 Incompressible fluids

With incompressible fluids the density does not change at all, neither temperature nor pressure can change the fluid density. With incompressible solvers, this assumption is baked right into the solver, i.e., into the equation that are solved.

Incompressible fluids can be used in a compressible solver by using the `rhoConst` equation of state, which makes the fluid density a user-specified constant.

40.12.2 Incompressible, temperature-dependent fluids

This class of fluid models is generally used for natural convection cases, in which the change of density due to temperature is the main driving force and any changes of density caused by the pressure are negligible.

OpenFOAM offers tabulated and polynomial models which allow the user to depict quite complex relations between fluid density and temperature.

Boussinesq model

If our fluid features a change of density due to temperature however not due to pressure, then we can use the Boussinesq model for the equation of state. This equation of state model was introduced with OpenFOAM-4 to make the Boussinesq approximation available to compressible solvers, as the commit message clearly points out¹⁴⁵:

equationOfState/Boussinesq: New equation of state for the Boussinesq approximation for buoyant flows

Description Incompressible gas equation of state using the Boussinesq approximation for the density as a function of temperature only:

\verbatim rho = rho0*(1 - beta*(T - T0)) \endverbatim

To be used with the `buoyantPimpleFoam` and `buoyantSimpleFoam` solvers as an alternative to using `buoyantBoussinesqPimpleFoam` or `buoyantBoussinesqSimpleFoam`, providing consistency with all other solvers and utilities using the thermodynamics package in OpenFOAM.

The two incompressible solvers with the Boussinesq approximation, i.e., `buoyantBoussinesqPimpleFoam` and `buoyantBoussinesqSimpleFoam`, were retired with the release of OpenFOAM-7¹⁴⁶.

Since using the Boussinesq equation of state is akin to the use of an incompressible fluid model from the perspective of the dependence on pressure, the absolute pressure has little to no meaning as far as the flow is concerned. Thus, while the fluid density can change (due to temperature), the fluid is an incompressible one with respect to pressure.

¹⁴⁵<https://github.com/OpenFOAM/OpenFOAM-dev/commit/dfecb23b08c04c92401bc0bdf904ed0793c3be66>

¹⁴⁶[buoyantBoussinesqPimpleFoam](#) or [buoyantBoussinesqSimpleFoam](#)

40.12.3 Compressible fluids

For (fully) compressible fluids, the density does change due to both temperature and pressure. The perfect gas model is a typical example, however, OpenFOAM also supports tabulated and polynomial relationships of the fluid density with respect to temperature and pressure.

40.13 Under pressure: setting a reference

In a compressible solver, the absolute pressure has meaning as well any pressure differences. While a flow is generally driven by a pressure difference (between inlet and outlet), the absolute pressure determines the fluid density of compressible fluids. This in turn directly influences the relationship between volumetric and mass flow.

40.13.1 Provide a pressure reference

With incompressible fluids, the absolute pressure has no meaning. Thus, we need to provide a pressure reference for enclosed cases.

40.13.2 Setting the boundary

If we have an open domain, e.g., with inflow and outflow, a pressure is generally provided via the pressure boundary condition of the outlet.

40.13.3 Case study: natural convection in an enclosed domain

In this section, we take a closer look on the importance of the way we prescribe the pressure in a simulation of natural convection using the Boussinesq equation of state, which makes the case essentially an incompressible one.

In this comparison we apply the strategies for setting a pressure reference for both enclosed and open-domain cases on a case which has an enclosed domain. Thus, we hope to demonstrate the resulting error of choosing the wrong approach. Table 5 lists the relevant differences between the two cases.

Case	p_rgh BC top-patch	pRef in constant	Pressure reference in fvSolution
1	fixedFluxPressure	none	pRef 0
2	prghPressure	1.0e+5	none

Table 5: The different settings for pressure in the two compared cases. Case 1 follows the settings of the hotRoomBoussinesq tutorial, which is a natural convection case with an enclosed domain. Case 2 is based on the comfortHotRoom tutorial, which is an open domain case using the Boussinesq equation of state.

Figure 130 shows the mesh of our natural convection case. There are two vertical rows of warm pipes which will drive the natural convection. The mesh is a hybrid mesh, which is less ideal than the `blockMesh`-based meshes of the tutorials. Thus, we hope for a more realistic behaviour of this case in contrast to the small, near-perfect all-hex meshes of the tutorials.

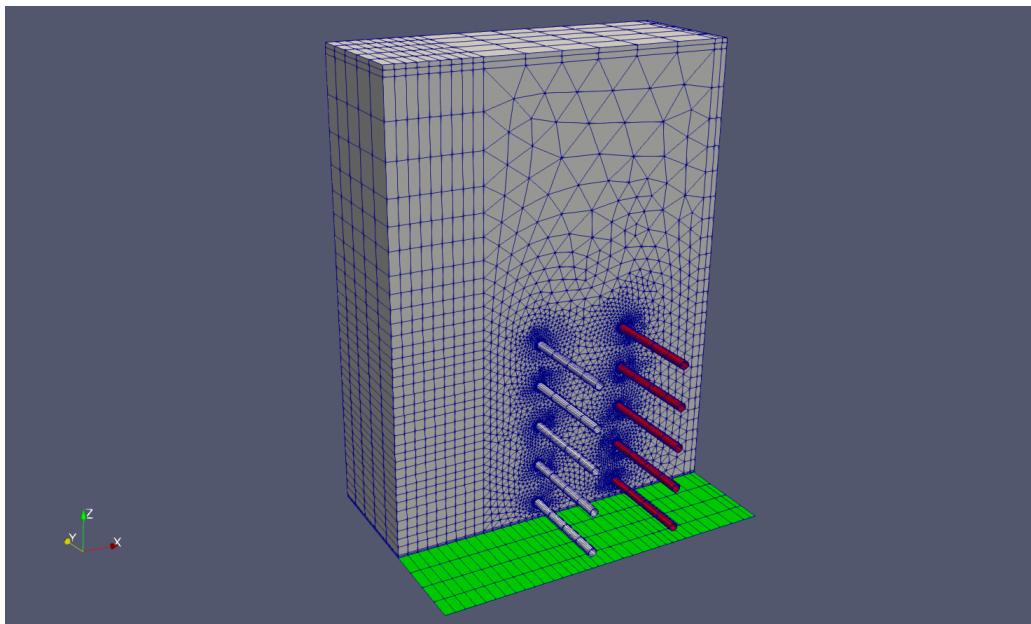


Figure 130: Two rows of warm pipes in a fluid domain. The mesh is a hybrid mesh consisting of hexahedral and prismatic cells, which was created by extruding a mixed tet-quad mesh.

Figures 131 to 133 show the development of the flow of our cases. While at first, both cases appear to develop among similar lines, the error near the top patch at some point dominates the flow within the domain.

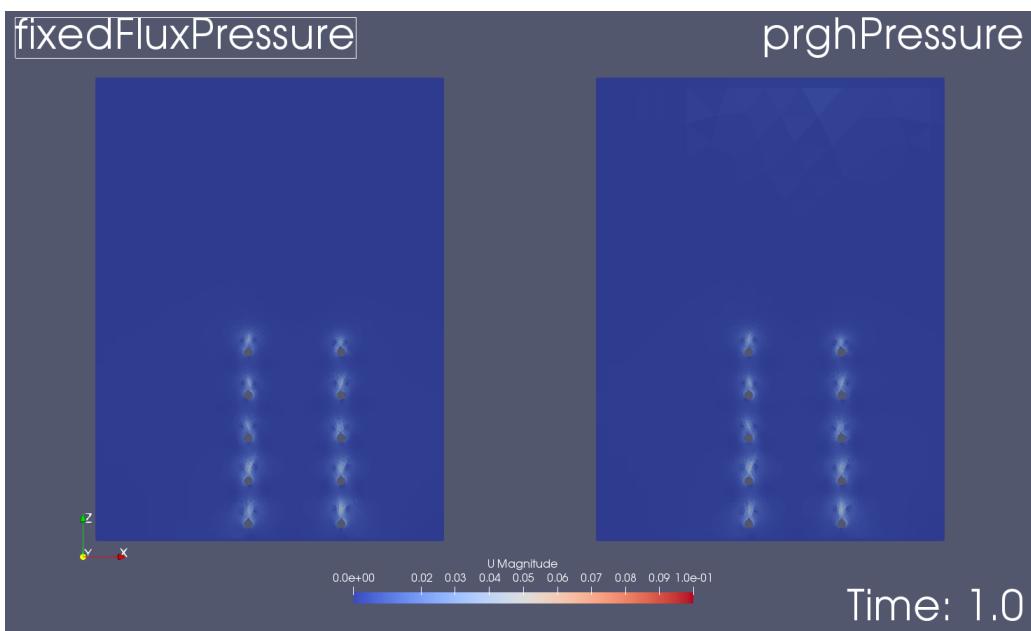


Figure 131: Onset of natural convection: both cases feature a quite similar velocity field.

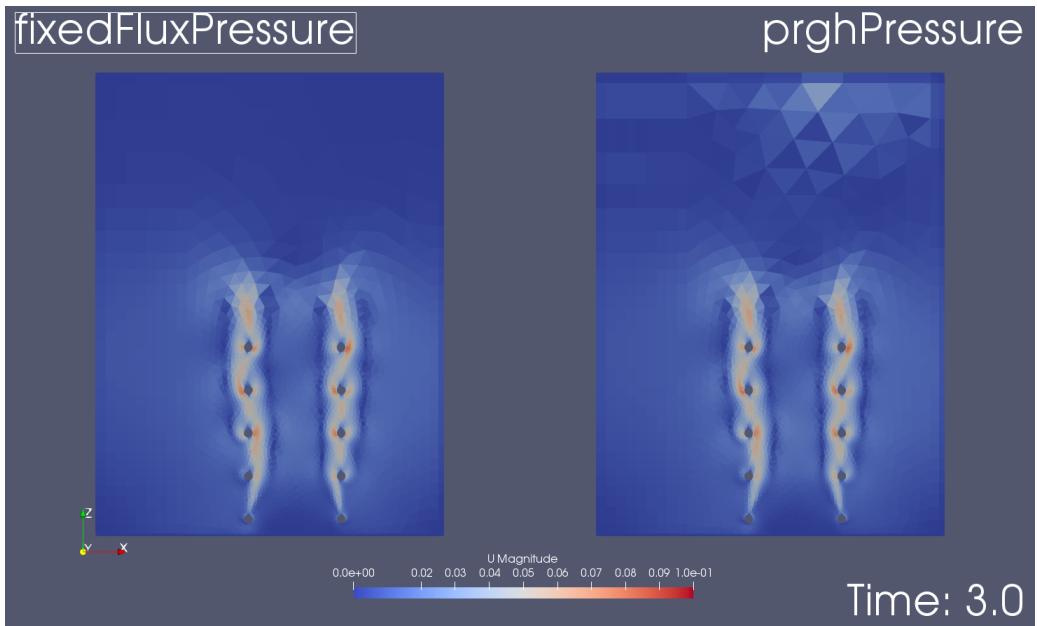


Figure 132: On-going development of natural convection: the flow field on the right shows developing errors in the flow caused by the pressure boundary condition.

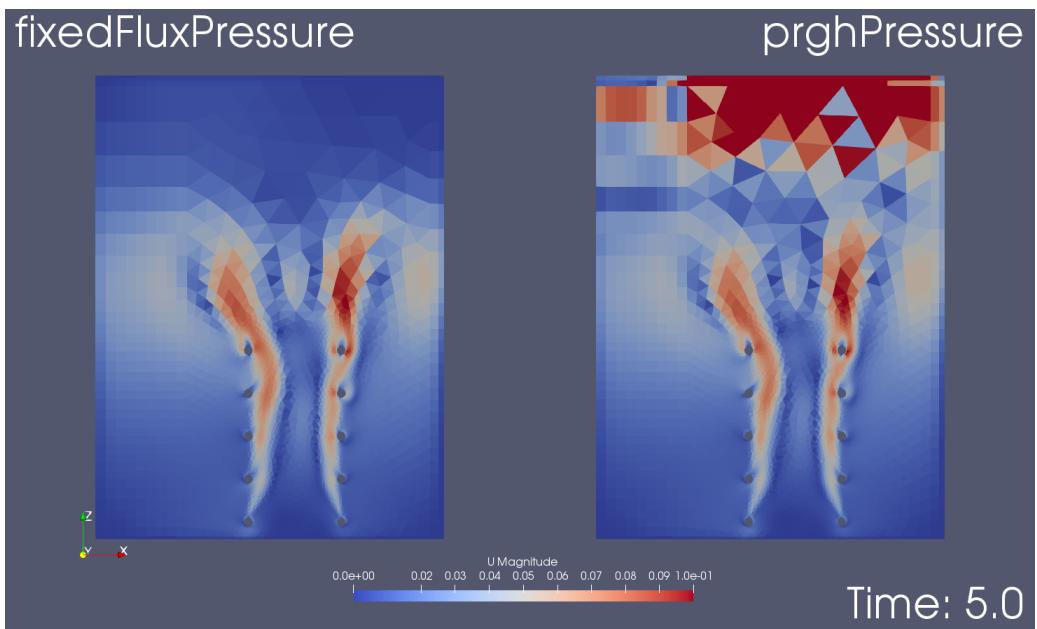


Figure 133: Further development of natural convection: in the flow field on the right, the errors in the flow field now outweigh the proper flow.

40.13.4 Natural convection in closed domains in OpenFOAM's tutorials

Here we collect the ways tutorial cases deal with setting a pressure reference.

Case + Solver		p_rgh		constant		fvSolution
		BCs	internalField	pRef	equationOfState	pRef
BenardCells	bPF	fixedFluxPressure	0	none	Boussinesq	pRef 0
hotRoomBoussinesq	bPF	fixedFluxPressure	0	none	Boussinesq	pRef 0
iglooWithFridges	bSF	fixedFluxPressure	0	none	Boussinesq	pRef 0
hotRoom	bPF	fixedFluxPressure	0	1.e+5	perfectGas	none
hotRoomRadiation	bSF	fixedFluxPressure	0	1.e+5	perfectGas	pRef 0

Table 6: The different settings for natural convection cases. bSF ... buoyantSimpleFoam, bPF ... buoyantPimpleFoam, cht ... chtMultiregionFoam.

41 Radiation modelling

Radiative heat transfer needs to be considered when temperatures are quite high. OpenFOAM offers several models to account for radiative heat transfer: the discrete ordinates model (fvDOM), the P1 model and the view factor model.

41.0.1 Solver control

The base class for all radiation models (`radiationModel`) provides controls on how often the radiation model needs to be solved. Since the radiation models can be computationally quite expensive, and temperature changes might be slower than the dynamics of the fluid flow, we may want to solve for radiation only every N-th time step.

This is achieved by the entry for the `solverFreq` keyword in the file `radiationProperties` dictionary. This keyword expects an integer value, which defaults to 1, and is also bounded to be at least 1 to prevent mischief caused by a user entering a negative value.

```
1 void Foam::radiationModel::initialise()
2 {
3     solverFreq_ = max(1, lookupOrDefault<label>("solverFreq", 1));
4
5     absorptionEmission_.reset
6     (
7         radiationModels::absorptionEmissionModel::New(*this, mesh_).ptr()
8     );
9
10    scatter_.reset(radiationModels::scatterModel::New(*this, mesh_).ptr());
11
12    soot_.reset(radiationModels::sootModel::New(*this, mesh_).ptr());
13 }
```

Listing 282: The `initialise()` method of the `radiationModel` class.

41.0.2 Radiative heat flux

Each of the radiation models writes, among other fields, the total radiative heat flux `qr` to disk. The sign-convention for the radiative heat flux is such¹⁴⁷, that it is positive, when the surface absorbs the heat flux. This is in line with the sign-convention for face normal vectors on a patch.

However, the convention for the wall heat flux, which is determined by a function object of that name is opposite. With the `wallHeatFlux` function object, a positive heat flux means that the heat flows from the wall into the domain.

41.1 Discrete ordinates - fvDOM

In OpenFOAM, the discrete ordinates (DO) model is named fvDOM. The eponymous discrete ordinates are a finite number of spatial directions, along which radiative heat transport is solved for. Listing 283 shows the diagnostic output of the model's constructor listing these directions.

```
fvDOM: Created 60 rays with average directions (dAve) and solid angles (omega)
Ray I0: dAve = (0.010235 0.0381976 0.0904495), omega = 0.0999985
Ray I1: dAve = (0.0279626 0.0279626 0.0904495), omega = 0.0999985
Ray I2: dAve = (0.0381976 0.010235 0.0904495), omega = 0.0999985
Ray I3: dAve = (0.0381976 -0.010235 0.0904495), omega = 0.0999985
Ray I4: dAve = (0.0279626 -0.0279626 0.0904495), omega = 0.0999985
```

Listing 283: The constructor of the `fvDOM` radiation model is reporting the discretized directions for radiative heat transport.

Each direction has its own radiative intensity field named `ILambda_XX_YY`, which has two suffixes: the first (XX) is a counter for the direction, and the second suffix (YY) is a counter for the wavelength band. Listing 284 shows an example of this naming scheme, which is taken from OpenFOAM's tutorials. In this specific case, we

¹⁴⁷See this note on OpenFOAM's bug tracker explaining the convention: <https://bugs.openfoam.org/view.php?id=2722#c9101>.

solve for 60 discrete ordinates, which is indicated in Listing 283, and for a single wavelength band. Thus, the first suffix runs from 0 to 59; and the second counter has only the value 0.

Since specifying identical BCs for each of the dozens of radiative intensity fields, the fvDOM model offers the possibility to specify BCs using a field named **IDefault**, which applies to all the fields.

```
Time = 910
DILUPBiCGStab: Solving for Ux, Initial residual = 0.000484957, Final residual = 8.59355e-07, No Iterations 1
DILUPBiCGStab: Solving for Uy, Initial residual = 0.000636378, Final residual = 1.3728e-06, No Iterations 1
DILUPBiCGStab: Solving for Uz, Initial residual = 0.00100732, Final residual = 1.64924e-06, No Iterations 1
DILUPBiCGStab: Solving for h, Initial residual = 0.000646664, Final residual = 9.12454e-07, No Iterations 1
Radiation solver iter: 0
GAMG: Solving for ILambda_0_0, Initial residual = 0.000289555, Final residual = 7.99208e-16, No Iterations 1
GAMG: Solving for ILambda_1_0, Initial residual = 0.000281662, Final residual = 7.86555e-16, No Iterations 1
GAMG: Solving for ILambda_2_0, Initial residual = 0.00028829, Final residual = 7.91439e-16, No Iterations 1
...
GAMG: Solving for ILambda_59_0, Initial residual = 0.00312848, Final residual = 2.98335e-06, No Iterations 1
DICPCG: Solving for p_rgh, Initial residual = 0.00253219, Final residual = 2.296e-05, No Iterations 35
time step continuity errors : sum local = 1.18082e-06, global = 1.41217e-19, cumulative = -7.81505e-19
rho max/min : 1.16452 0.69867
DILUPBiCGStab: Solving for epsilon, Initial residual = 0.000330527, Final residual = 6.62334e-06, No Iterations 1
DILUPBiCGStab: Solving for k, Initial residual = 0.000939773, Final residual = 1.06366e-05, No Iterations 1
ExecutionTime = 654.13 s ClockTime = 655 s
```

Listing 284: An extract of the solver output when using the fvDOM radiation model. The solver output for the radiation model follows the output of the solution for the momentum and energy equations. For each of the discrete ordinates a transport equation for the radiative intensity is solved.

When the solver writes a time step to disk, the radiative intensity field for each discrete ordinate is written into the time step folder. The fvDOM radiation model also writes some additional fields to disk, which are according to the description in the header file of the fvDOM model:

a Total absorption coefficient [1/m]

G Incident radiation [W/m²]

qin Incident radiative heat flux [W/m²]

qem Emitted radiative heat flux [W/m²]

qr Total radiative heat flux [W/m²]

41.2 P1

The P1 model is suited for optically thick problems, i.e. the medium through which the radiation is passing through does absorb or scatter some of the incident radiation.

41.3 View factor

The **viewFactor** model has been released with OpenFOAM-2.0.0¹⁴⁸. This model only considers radiative heat transfer between surfaces. Thus, this model is suitable for simulation cases with vacuum between hot surfaces, or for cases with non-participating gases. Non-participating gases do neither absorb nor scatter thermal radiation. Such gases are mono-atomic gases, such as argon or helium, or symmetric diatomic gases, such as oxygen, nitrogen or hydrogen [17, 31].

The announcement in the release notes of OpenFOAM-2.0.0 has the following to say about this model:

... view factor model for radiative heat transfer, specifically between surfaces. The method begins with the generation of rays between discrete faces of the surfaces, using the **viewFactorsGen** utility in OpenFOAM. Radiative heat transfer is then calculated by summing energy exchanges between ray end-points. A major benefit of this approach is that energy is only exchanged between parts of surface that are directly visible to one another, giving a representative solution to complex problems where some surfaces are shielded from radiative sources by others.

The view factor model is also referred to as *surface-to-surface (S2S)* model, e.g. in Fluent [9].

41.3.1 Pre-processing

The **viewFactor** model requires some pre-processing, which is a 2 step process that involves the following pre-processing tools:

¹⁴⁸<https://openfoam.org/release/2-0-0/thermophysical-modelling/>

faceAgglomerate

The announcement of the viewFactor model in the release notes of OpenFOAM-2.0.0 has the following to say about the computational requirements of the viewFactor model:

The computational time and memory requirement of the modelling is largely determined by the number of faces from which the rays emanate. In OpenFOAM, the cost can be reduced by grouping faces together using the faceAgglomerate pre-processing utility.

Hence, the faceAgglomerate tool is used in preparation to create a coarser representation of the surface to reduce computational effort. In Fluent, using face agglomeration to reduce the computational effort is referred to as *clustering* [9].

viewFactorsGen

This tool does the actual creation of rays between the involved surfaces, respectively it computes the view factors between the agglomerated faces.

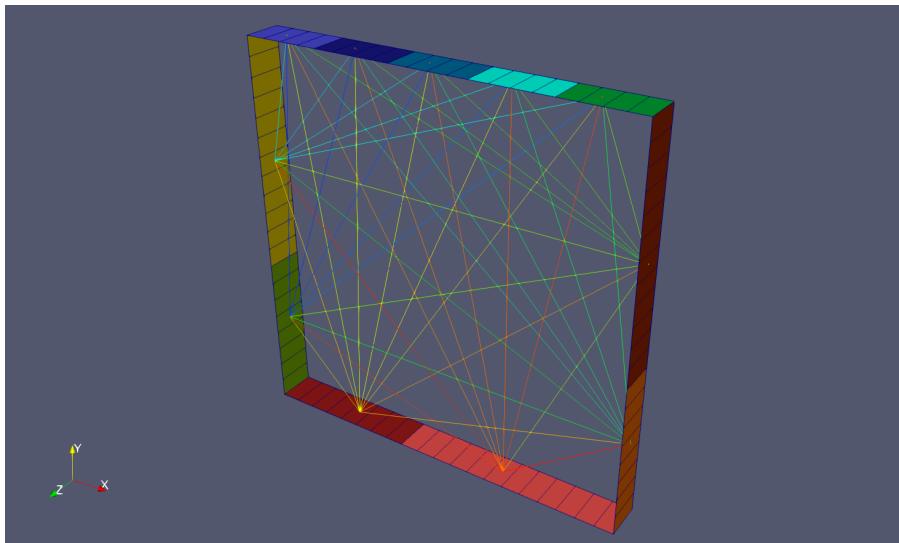


Figure 134: The result of `faceAgglomerate` and `viewFactorGen` applied to a slightly refined cavity case. The patches *movingWall* and *fixedWalls* have both been agglomerated, i.e. for the purposes of computing the view factor, several faces of a patch form a coarsened face. This is evident from the visualisation of the rays created by `viewFactorGen`, each bundle of rays starts from the center of such a coarsened face. The colour of the rays is a mere ID, not the actual view factor.

41.3.2 Visualising the pre-processing results

Inspecting the results of the pre-processing steps can be quite important, see Section 41.3.5. Also, you might wonder how Figure 134 was created.

Write the face-agglomeration

Enabling the `writeFacesAgglomeration` switch in the `viewFactorDict` dictionary causes `faceAgglomerate` to write a field named `facesAgglomeration`, which contains a trivial internal field, yet the boundary values correspond to a running index of the agglomerates. I.e. all faces with the value X belong to the agglomerate X.

Dump the rays

Enabling the `dumpRays` switch in the `viewFactorDict` dictionary causes `viewFactorsGen` to write a file named `allVisibleFaces.vtk`, which contains the rays from each agglomerate to all other agglomerates. These rays are shown in Figure 134 as lines connecting all agglomerates with each other.

41.3.3 Model use

The `viewFactor` model requires an additional field in the case setup, the new radiative heat flux `qr`. The unit of `qr` is given in the header description of the `viewFactor` model as W/m². In the field definition of `qr`, the dimension set corresponds to the unit kg/s³, which works out to be the same unit once the unit Watt is replaced by its SI representation.

The model furthermore reads the `finalAgglom` field, which is created by the `faceAgglomerate` tool.

41.3.4 Solution procedure

Once the view factors are determined by the pre-processing tools, the model can be used in a simulation. The `viewFactor` model essentially boils down to an algebraic equation linking the net radiative heat flux with the surface temperature via the view factors and other properties.

The model equation underlying the `viewFactor` model is the following:

$$C_{ij}q_i = b_i \quad (65)$$

$$\left[\delta_{ij} \frac{1}{E_j} - \left(\frac{1}{E_j} - 1 \right) F_{ij} \right] q_i = (delta_{ij} - F_{ij}) \sigma T_i^4 \quad (66)$$

With a static mesh, the view factors are constant, and the only major task for the `viewFactor` model is to compute the inverse of an $N \times N$ matrix \mathbf{C} , with N being the number of coarsened faces. As \mathbf{C} contains only constant entries, the inversion only needs to be done once, at the first iteration of the solver.

Thus, for big simulation cases, we can expect the `viewFactor` model to take long during pre-processing, especially when creating the rays using `viewFactorGen`; and it will take especially long, when it computes the inverse of \mathbf{C} during the first iteration. This is compounded by the fact, that the computation of the radiative flux happens on the master-process, i.e. parallelisation does not accelerate the `viewFactor` model, since the major computational work is done by a single process.

Afterwards, however, the `viewFactor` model doesn't incur significant computational effort anymore, since the inverse of \mathbf{C} is cached, and during each iteration, computing the radiative heat flux reduces to a simple matrix-vector multiplication. With a cached inverse matrix, we can solve Eq. (65) very efficiently over and over, since only the RHS changes from time step to time step.

The discussion above, about the computational effort, can be better understood if we take a look at the relevant code, shown in Listing 285. There, we see that the `viewFactor` model is only then efficient, when the emissivities are constant, otherwise we are not able to benefit from caching the inverse of the matrix \mathbf{C} , since it would change from time step to time step.

```

1  if (Pstream::master())
2  {
3      // Variable emissivity
4      if (!constEmissivity_)
5      {
6          scalarSquareMatrix C(totalNCoarseFaces_, 0.0);
7
8          // build equation system - code removed for brevity
9
10         Info << "\nSolving view factor equations..." << endl;
11         // Negative coming into the fluid
12         LUsolve(C, q);
13     }
14     else // Constant emissivity
15     {
16         // Initial iter calculates CLU and chaches it
17         if (iterCounter_ == 0)
18         {
19             // build equation system - code removed for brevity
20
21             if (debug)
22             {
23                 InfoInFunction
24                 << "\nDecomposing C matrix..." << endl;
25             }
26             LUDecompose(CLU_(), pivotIndices_);

```

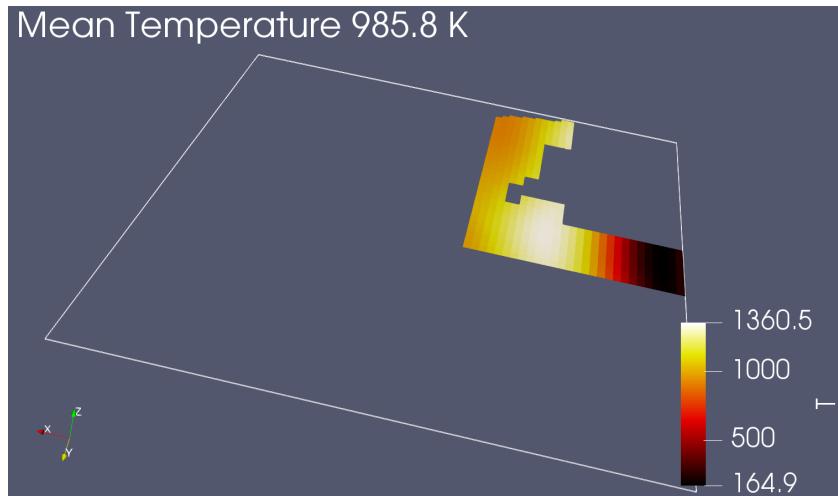


Figure 135: One of the aggressively agglomerated faces: On the right boundary the temperature is 300 K, yet the radiative heat-flux computed by the mean temperature cools the solid down to 165 K, which is very unphysical for a case that computes a heated solid interacting with a body of gas. No cooling should occur at all.

```

27
28
29     // build equation system - code removed for brevity
30
31     if (debug)
32     {
33         InfoInFunction
34             << "\nLU Back substitute C matrix.." << endl;
35     }
36     LUBacksubstitute(CLU_(), pivotIndices_, q);
37     iterCounter_++;
38 }
39 }
```

Listing 285: A snippet of the `calculate()` method of the `viewFactor` model.

41.3.5 Pitfall: too aggressive faceAgglomeration

The pre-processing operation of face-agglomeration is an important one, since it reduces the computational effort for computing the view-factors by orders of magnitude. However, don't be too aggressive with face-agglomeration, at least in regions in which you expect large temperature gradients.

In Figure 135 we see the result of an overly aggressive agglomeration, aggromeration if you like. The case in question is a solid which is volumetrically heated by Joule heating, i.e. an electrical current passing through the solid. The solid is embedded in a fluid region with a gas (nitrogen) as working fluid. The large agglomerate causes the radiative heat transfer locally to be under- or overestimated. In regions colder than the mean temperature of the agglomerate, the radiative heat transfer acts to cool the local cells. In regions hotter than the mean temperature of the agglomerate, the heat transfer is underestimated, thus, these regions get hotter than they ought to be.

Always check the face-agglomeration, i.e. view it in ParaView and judge whether it is fine enough in regions where you expect temperature gradients, as the radiative heat-transfer depends on the fourth power of the temperature, even a moderate within an agglomerate can lead to great error.

41.3.6 Pitfall: temperature boundary conditions in CHT cases

A pit the author has fallen into recently. When modifying an existing CHT case to incorporate radiation, take special care to get the temperature boundary conditions right. The motivation for tale of caution was a botched case setup, which turned out to be a very simple case of user error.

```

Class
  Foam::compressible::
    turbulentTemperatureCoupledBaffleMixedFvPatchScalarField

Description
  Mixed boundary condition for temperature, to be used for heat-transfer
  on back-to-back baffles.
}

```

Listing 286: A snippet from the header-file's description of the class `turbulentTemperatureCoupledBaffleMixedFvPatchScalarField`.

```

Class
  Foam::compressible::
    turbulentTemperatureRadCoupledMixedFvPatchScalarField

Description
  Mixed boundary condition for temperature and radiation heat transfer
  to be used for in multiregion cases.
}

```

Listing 287: A snippet from the header-file's description of the class `turbulentTemperatureRadCoupledMixedFvPatchScalarField`. The difference in the class name has been marked in red, since these three letters in the middle of a long name are easy to miss.

Listings 286 and 287 show the relevant header-file descriptions of the involved boundary conditions: a coupled temperature BC without and with radiation.

Listing 288 shows the relevant boundary condition of the temperature field. Note the similar names of the temperature BCs, i.e., the one without and the one with radiation.

So, what can go wrong if we do not adjust the temperature BC? Simply put, there will be no radiative heat transfer. Since the `viewFactor` model is entirely based on boundary surfaces, all the magic happens with the boundaries. If we get the temperature boundary wrong, we incur ourselves the cost of modelling radiative heat transfer without the benefit of actually accounting for radiative heat transfer in our simulation.

```

1  "SolidGasInterface.*"
2  {
3      /* this does not work!
4      type            compressible::turbulentTemperatureCoupledBaffleMixed;
5      Tnbr           T;
6      kappaMethod    solidThermo;
7      value          uniform 1800; */
8
9      // this will work
10     type            compressible::turbulentTemperatureRadCoupledMixed;
11     Tnbr           T;
12     kappaMethod    solidThermo;
13     qrNbr          qr;
14     qr              none;
15     value          uniform 1800;
16 }

```

Listing 288: Changing the relevant boundary conditions of the field `T` in a CHT simulation case to enable heat transfer due to radiation.

Your trusted author of this very collection of pitfalls has failed to make the according adjustment to his case and was left wondering why heat transfer was glacially slow. Beginner's errors happen all the time to all kinds of people, especially when we are beginning to create a new simulation case.

42 Eulerian multiphase modelling

In Eulerian two-phase modelling both phases are considered continua even though one phase might consist of dispersed phase elements (DPEs) such as bubbles, drops or particles. In these simulations the two phases can be distinguished into a continuous phase and a dispersed phase. This naming scheme refers to the physical situation. Within the (Eulerian) mathematical description, however, both phases are continua.

As two momentum equations are solved (one per phase), each phase has its own velocity field. However, there is only one pressure field. Thus, the pressure is the same for both phases; this also applies to the VOF method. Due to the fact that two continuity¹⁴⁹ and two momentum equations are solved, this approach is often referred to as *two fluid model*.

The Eulerian description of multi-phase flow is not limited to two phases, however, for reasons of simplicity, we limit ourselves to the case of two phases.

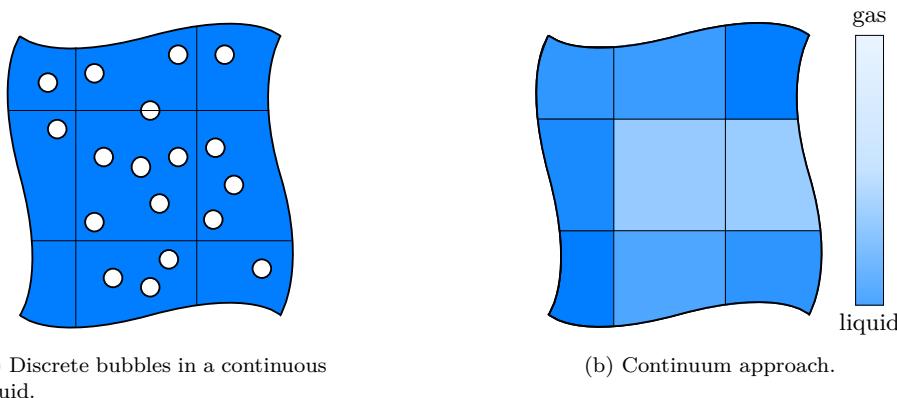


Figure 136: Modelling approach on the example of a gas-liquid two-phase system.

As the DPEs are considered to be a continuous phase, their properties are averaged over each cell of the computational domain. Thus, the properties of the dispersed phase are the mean properties of the dispersed matter. If all DPEs have equal properties (e.g. diameter, density, etc.), then the dispersed phase is referred to as being *mono-disperse*. Only in the case of mono-dispersity, the averaging over the cells introduces no additional errors. If the DPEs have variable properties (e.g. a diameter range), then the dispersed phase is referred to as being *poly-disperse*. The correct handling of poly-dispersity requires additional considerations on the models.

42.1 Phase model class

One of the strengths of object oriented programming is that the class structure in the source code can reflect the properties and relations of real-world things.

The phase model class in the various two- and multi-phase solvers of OpenFOAM is one example of how techniques of object oriented programming can be applied. In terms of a multi-phase problem in fluid dynamics we distinguish different phases.

We now violate the unwritten law of *to not cite Wikipedia* [Citation needed].

Phase (matter), a physically distinctive form of a substance, such as the solid, liquid, and gaseous states of ordinary matter—also referred to as a "macroscopic state"

<http://en.wikipedia.org/wiki/Phase>

In fluid dynamics phase is a commonly used term. When we intend our code to represent the reality we want to describe as closely as possible we need to introduce the concept of the phase into our source code. From a programming point of view properties of a phase – such as viscosity, velocity, etc. – are easy to implement. The viscosity of a phase is simply a field of values, velocity is another field of values.

¹⁴⁹The constraint that the sum of all volume fraction fields must yield unity, i.e. $\sum_i \alpha_i = 1$, allows for one continuity equation to be eliminated. In the case of two phases, only one continuity equation needs to be solved. However, both continuity equation can be combined.

Object orientation allows us to translate the idea of the phase into programming language. The basic idea is that a phase has a viscosity, it also has a velocity. We now create a class named `phaseModel` and this class needs to have a viscosity, a velocity and everthing else a phase needs to fit our needs.

The phase model classes follow the code of best practice in object oriented programming to hide internal data from the outer world and to provide access via the classes methods (data encapsulation, see http://www.tutorialspoint.com/cplusplus/cpp_data_encapsulation.htm).

No phases, please

In the single-phase solvers of OpenFOAM – such as `simpleFoam` – the concept of a phase is not used. As there is only one temperature and velocity to deal with, the concept of phases is not needed. In the single-phase solvers the phase-properties (viscosity, velocity, density, etc.) are linked according to the physical relations that are taken into account, but the concept of a phase is missing.

42.1.1 A comparison of the phase models in OpenFOAM-2.2

In this section we want to compare the implementation of the phase model class of the two solvers `twoPhaseEulerFoam` and `multiphaseEulerFoam`.

`twoPhaseEulerFoam`

The phase model class in `twoPhaseEulerFoam-2.2.x` collects the properties of a phase and offers an interface for accessing these properties. Listing 289 shows the essence of the header file of the phase model class. The listing is syntactically correct, however all pre-processor instruction (e.g. the `#include` statements) have been removed. Furthermore, most of the comments have been removed and the formatting has been adapted to reduce the line number. The purpose of Listing 289 is to present the data members and methods of the class by actual source code.

```

1  namespace Foam
2  {
3
4  class phaseModel
5  {
6      // Private data
7      dictionary dict_;
8      word name_;
9      dimensionedScalar d_;
10     dimensionedScalar nu_;
11     dimensionedScalar rho_;
12     volVectorField U_;
13     autoPtr<surfaceScalarField> phiPtr_;
14
15 public:
16     // Member Functions
17     const word& name() const { return name_; }
18
19     const dimensionedScalar& d() const { return d_; }
20
21     const dimensionedScalar& nu() const { return nu_; }
22
23     const dimensionedScalar& rho() const { return rho_; }
24
25     const volVectorField& U() const { return U_; }
26
27     volVectorField& U() { return U_; }
28
29     const surfaceScalarField& phi() const { return phiPtr_(); }
30
31     surfaceScalarField& phi() { return phiPtr_(); }
32 };
33
34 } // End namespace Foam

```

Listing 289: A boiled-down version of the file `phaseModel.H`

The phase model class of *twoPhaseEulerFoam*-2.2.x contains all phase properties needed for an incompressible two-phase solver that makes use of an important consequence of being limited to two phase problems. By taking a look on the members of the class we see that there is no volume fraction field. In two phase problems one volume fraction field (*alpha1*) suffices as the volume fraction field of the other phase is instantly known (*alpha2 = 1 - alpha1*). Thus, the volume fraction can be treated separately from other phase information.

Another missing item is the pressure. Most two- or multi-phase Eulerian solvers assume/use a common pressure for all phases. Thus, the pressure is independent of the phases and can be treated separately.

multiphaseEulerFoam

One difference between the phase model class used in *twoPhaseEulerFoam* and the one used in *multiphaseEulerFoam* follows directly from the simplification made in the two-phase case. When dealing with an arbitrary number of phases, each phase must keep track of its own volume fraction. Thus, the volume fraction must be included into the phase model.

The straight-forward way would be to add another reference to the data members. As the volume fraction field is a scalar field, this reference would be a reference to a *volScalarField*. In *multiphaseEulerFoam* a more subtle approach was chosen. This also presents the application of another object-oriented programming technique.

The phase model class of *multiphaseEulerFoam* is derived from the class *volScalarField*. Thus, the phase model class is among other things its own the volume fraction field.

Listing 290 shows a stripped version of the header file of *multiphaseEulerFoam*'s phase model class. Again, large parts of the file have been removed leaving only the data members and the methods of the class.

```

1  namespace Foam
2  {
3
4  class phaseModel
5  :
6  public volScalarField
7  {
8      // Private data
9      word name_;
10     dictionary phaseDict_;
11     dimensionedScalar nu_;
12     dimensionedScalar kappa_;
13     dimensionedScalar Cp_;
14     dimensionedScalar rho_;
15     volVectorField U_;
16     volVectorField DDTU_;
17     surfaceScalarField phiAlpha_;
18     autoPtr<surfaceScalarField> phiPtr_;
19     autoPtr<diameterModel> dPtr_;
20
21 public:
22
23     // Member Functions
24     const word& name() const { return name_; }
25
26     const word& keyword() const { return name(); }
27
28     tmp<volScalarField> d() const;
29
30     const dimensionedScalar& nu() const { return nu_; }
31
32     const dimensionedScalar& kappa() const { return kappa_; }
33
34     const dimensionedScalar& Cp() const { return Cp_; }
35
36     const dimensionedScalar& rho() const { return rho_; }
37
38     const volVectorField& U() const { return U_; }
39
40     volVectorField& U() { return U_; }
41
42     const volVectorField& DDTU() const { return DDTU_; }
43

```

```

44     volVectorField& DDtU() { return DDTU_; }
45
46     const surfaceScalarField& phi() const { return phiPtr_; }
47
48     surfaceScalarField& phi() { return phiPtr_; }
49
50     const surfaceScalarField& phiAlpha() const { return phiAlpha_; }
51
52     surfaceScalarField& phiAlpha() { return phiAlpha_; }
53
54     void correct();
55
56     bool read(const dictionary& phaseDict);
57
58 };
59 } // End namespace Foam

```

Listing 290: A boiled-down version of the file `phaseModel.H`

The statements following the class keyword and the class name indicates the derivation of a class. The class name (`phaseModel`) and the name of the class we are deriving from (`volScalarField`) are separated by a colon (:). The name of the base class (`volScalarField`) is preceded by a visibility specifier (`public`). Here, we see a prototype of a class definition. The class we define (`phaseModel`) is derived from a base class (`volScalarField`).

```

class phaseModel : public volScalarField
{
    /* some c++ code */
}

```

This example highlights, that the class `phaseModel` is derived from the class `volScalarField`. This information alone does no proof that the phase model is its own volume fraction field. However, a glance on the constructor in the implementation file brings clarity.

In Listing 291 we see, that the first instruction in the initialisation list of the constructor reads the volume fraction field of the respective phase. This proves that the phase model is in fact its own volume fraction field. For an explanation why we come to this conclusion we refer to any C++ textbook or online resource that covers the concept of inheritance, see e.g. <http://www.learnccpp.com/cpp-tutorial/114-constructors-and-initialization-of-derived-classes/> or [59].

```

// * * * * * Constructors * * * * * //
Foam::phaseModel::phaseModel
(
    const word& name,
    const dictionary& phaseDict,
    const fvMesh& mesh
)
:
    volScalarField
    (
        IOobject
        (
            "alpha" + name,
            mesh.time().timeName(),
            mesh,
            IOobject::MUST_READ,
            IOobject::AUTO_WRITE
        ),
        mesh
    ),
    name_(name),
    // code continues

```

Listing 291: The first few lines of the constructor of the phase model.

Besides being its own volume fraction field the phase model class of `multiphaseEulerFoam` was extended by several fields bearing information for the simulation of thermodynamics.

We can also observe the rudiment of giving the phase model a more active role. The phase model class of `twoPhaseEulerFoam` is simply an information carrier. The phase model of `multiphaseEulerFoam` features a

method named `correct()`. The `correct()` method is used in many models for actions performed at every time step. However, in *multiphaseEulerFoam*-2.2.x this method is empty.

With OpenFOAM-2.1.0 the class `diameterModel` was introduced into *multiphaseEulerFoam* and *compressibleTwoPhaseEulerFoam*. The phase model class of *multiphaseEulerFoam* uses a diameter model class for keeping track of the dispersed phase's diameter. The diameter model offers the choice of computing the diameter of the dispersed phase elements from thermodynamic quantities besides using a constant diameter. Thus, the data member `dimensionedScalar d_` is replaced by a reference to a diameter model (`autoPtr<diameterModel> dPtr_`).

42.1.2 A comparison of the phase models in OpenFOAM-2.3

In this section we want to compare the implementation of the phase model class of the two solvers *twoPhaseEulerFoam* and *multiphaseEulerFoam*.

A comment on *multiphaseEulerFoam*

The phase model class used for *multiphaseEulerFoam* in OpenFOAM-2.2.x and OpenFOAM-2.3.x differs very little with respect to the class's methods and members. Listing 292 shows that the header files of the `phaseModel` class of *multiphaseEulerFoam* differs only in the copyright notice. The implementation file shows slightly greater differences¹⁵⁰. However, the behaviour of this class can be considered nearly identical in OpenFOAM-2.2.x and OpenFOAM-2.3.x.

```
user@host:~/OpenFOAM$ diff
  OpenFOAM-2.2.x/applications/solvers/multiphase/multiphaseEulerFoam/phaseModel/phaseModel.H
  phaseModel.H
  OpenFOAM-2.3.x/applications/solvers/multiphase/multiphaseEulerFoam/multiphaseSystem/
  phaseModel/phaseModel.H
5c5
<    \\\ /   And           | Copyright (C) 2011 OpenFOAM Foundation
---
>    \\\ /   And           | Copyright (C) 2011-2013 OpenFOAM Foundation
```

Listing 292: The output of `diff` for the file `phaseModel.H` of the solver *multiphaseEulerFoam* of the versions OpenFOAM-2.2.x and OpenFOAM-2.3.x as of May 2014¹⁵¹.

twoPhaseEulerFoam

The two-phase model of *twoPhaseEulerFoam*-2.3.x makes heavy use of abstractions. The phase model class is used in conjunction with a class for the two-phase system.

```
1  namespace Foam
2  {
3
4      class phaseModel
5      :
6          public volScalarField ,
7          public transportModel
8      {
9          // Private data
10         const twoPhaseSystem& fluid_;
11         word name_;
12         dictionary phaseDict_;
13         scalar alphaMax_;
14         autoPtr<rhoThermo> thermo_;
15         volVectorField U_;
16         surfaceScalarField alphaPhi_;
17         surfaceScalarField alphaRhoPhi_;
18         autoPtr<surfaceScalarField> phiPtr_;
19         autoPtr<diameterModel> dPtr_;
20         autoPtr<PhaseCompressibleTurbulenceModel<phaseModel> > turbulence_;
21     }
```

¹⁵⁰The `diff` of the implementation file would be too long to be shown at this place. For general information on `diff` see Section 78.6.

¹⁵¹OpenFOAM Builds compared: 2.2.x-61b850bc107b and 2.3.x-0eb39ebe0f07.

```

22 public :
23
24     // Member Functions
25     const word& name() const { return name_; }
26
27     const twoPhaseSystem& fluid() const { return fluid_; }
28
29     const phaseModel& otherPhase() const;
30
31     scalar alphaMax() const { return alphaMax_; }
32
33     tmp<volScalarField> d() const;
34
35     const PhaseCompressibleTurbulenceModel<phaseModel>&
36     turbulence() const;
37
38     PhaseCompressibleTurbulenceModel<phaseModel>&
39     turbulence();
40
41     const rhoThermo& thermo() const { return thermo_(); }
42
43     rhoThermo& thermo() { return thermo_(); }
44
45     tmp<volScalarField> nu() const { return thermo_>nu(); }
46
47     tmp<scalarField> nu(const label patchi) const { return thermo_>nu(patchi); }
48
49     tmp<volScalarField> mu() const { return thermo_>mu(); }
50
51     tmp<scalarField> mu(const label patchi) const { return thermo_>mu(patchi); }
52
53     tmp<volScalarField> kappa() const { return thermo_>kappa(); }
54
55     tmp<volScalarField> Cp() const { return thermo_>Cp(); }
56
57     const volScalarField& rho() const { return thermo_>rho(); }
58
59     const volVectorField& U() const { return U_; }
60
61     volVectorField& U() { return U_; }
62
63     const surfaceScalarField& phi() const { return phiPtr_(); }
64
65     surfaceScalarField& phi() { return phiPtr_(); }
66
67     const surfaceScalarField& alphaPhi() const { return alphaPhi_; }
68
69     surfaceScalarField& alphaPhi() { return alphaPhi_; }
70
71     const surfaceScalarField& alphaRhoPhi() const { return alphaRhoPhi_; }
72
73     surfaceScalarField& alphaRhoPhi() { return alphaRhoPhi_; }
74
75     void correct();
76
77     virtual bool read(const dictionary& phaseProperties);
78
79     virtual bool read() { return true; }
80 };
81
82 } // End namespace Foam

```

Listing 293: A boiled-down version of the file `phaseModel.H`

The data members of the phase model class in *twoPhaseEulerFoam-2.3.x* contain a reference to the two-phase model class. This makes the phase model class aware of the other phase. The data members also contain a reference to a turbulence model and a thermophysical model. This is up to now the greatest generalisation we could observe in the multi-phase solvers of OpenFOAM.

42.2 Phase system classes

In a multiphase solver we can not only create an abstraction for the physical phase, e.g. water. We can also create an abstraction for the multi-phase system, i.e. the entirety of the involved phases. Again, *multiphaseEulerFoam* was the forerunner for this idea. Since the introduction of *multiphaseEulerFoam* there is a class named `multiphaseSystem`. In *twoPhaseEulerFoam-2.3* the class `twoPhaseSystem` was introduced. The most obvious purpose of this class is the implementation of the phase continuity equation. In both solvers the solution of the continuity equation(s) hides behind the function call `fluid.solve()`.

42.2.1 The class `twoPhaseSystem`

We now take a detailed look on the class `twoPhaseSystem`. This class was introduced with *twoPhaseEulerFoam-2.3* and this class seems to be a consequent continuation of ideas introduced in the class `multiphaseSystem`. We focus on the class `twoPhaseSystem`, since the class `multiphaseSystem` has not really evolved from the release of OpenFOAM-2.1 til the release of OpenFOAM-2.3. The header and the implementation file are largely identical.

Phase models

Two data members of the class are the two involved phase models `phase1_` and `phase2_`. The class provides methods to access this phase models. There is also a method to access the other phase. As there are only two phases involved, this operation is possible.

Phase pair models

In order to cover all possible flow situations the momentum exchange models are defined in the case pair-wise in a separated fashion, i.e. drag for air dispersed in water (bubbly flow) and drag for water dispersed in air (droplet flow).

The classes `phasePair` and `orderedPhasePair` provide an elegant way to deal with this situation. The phase pair models are used for blending the interfacial momentum exchange models.

Momentum exchange models

The class has member variables for the interfacial momentum exchange models. Listing 294 shows the members of the class related to momentum exchange models. The templated class `BlendedInterfacialModel<>` provides functionality that is needed for all momentum exchange models. As the class name suggests, the blending is covered by this class. The template parameter of this class stands for any one of the interfacial momentum exchange models.

```
1 // - Drag model
2 autoPtr<BlendedInterfacialModel<dragModel> > drag_;
3 // - Virtual mass model
4 autoPtr<BlendedInterfacialModel<virtualMassModel> > virtualMass_;
5 // - Heat transfer model
6 autoPtr<BlendedInterfacialModel<heatTransferModel> > heatTransfer_;
7 // - Lift model
8 autoPtr<BlendedInterfacialModel<liftModel> > lift_;
9 // - Wall lubrication model
10 autoPtr<BlendedInterfacialModel<wallLubricationModel> > wallLubrication_;
11 // - Wall lubrication model
12 autoPtr<BlendedInterfacialModel<turbulentDispersionModel> > turbulentDispersion_;
```

Listing 294: The declaration of the momentum exchange members of the class `twoPhaseSystem` in `twoPhaseSystem.H`

A momentum exchange model alone is nice, but what we really need are the contribution to the momentum equation. Thus, the class `twoPhaseSystem` provides methods to access the respective force terms or the respective coefficients. We have seen this force terms and coefficients in action in Section 55.6.

```
1 // - Return the drag coefficient
2 tmp<volScalarField> dragCoeff() const;
3 // - Return the virtual mass coefficient
4 tmp<volScalarField> virtualMassCoeff() const;
```

```

5   //-- Return the heat transfer coefficient
6   tmp<volScalarField> heatTransferCoeff() const;
7   //-- Return the lift force
8   tmp<volVectorField> liftForce() const;
9   //-- Return the wall lubrication force
10  tmp<volVectorField> wallLubricationForce() const;
11  //-- Return the wall lubrication force
12  tmp<volVectorField> turbulentDispersionForce() const;

```

Listing 295: The declaration of the accessing methods for the momentum exchange coefficients of the class `twoPhaseSystem` in `twoPhaseSystem.H`

42.2.2 The class `multiphaseSystem`

The solver `multiphaseEulerFoam` uses the class `multiphaseSystem`. This class seems to be the ancestor of the class `twoPhaseSystem`.

Phase pair

The class `multiphaseSystem` declares a nested class `interfacePair`. A nested class is a class definition within another class. Thus, the nested class is hidden from the outside world¹⁵².

The phase pair class is used to deal with surface tension, which by definition is a property of a pair of phases, and drag.

42.3 Turbulence modelling

42.3.1 Modelling strategies

The problem of turbulence modelling in multi-phase problems can be tackled in one of the following fashions. The methods are sorted by their perceived computational cost. Whereas the first two methods may be equivalent, the last is definitely more expensive in terms of memory and computational time. However, each of these methods has its strengths and weaknesses, and its use cases.

Continuous phase only This model solves computes the turbulent properties of the continuous phase and assumes an algebraic relationship between the turbulent properties of the continuous and the dispersed phase. The influence of turbulence on the dispersed phase can also be neglected altogether. In the Fluent Theory Guide [9] it is noted: [...] *is the appropriate model when the concentrations of the secondary phases are dilute. In this case, interparticle collisions are negligible and the dominant process in the random motion of the secondary phases is the influence of the primary-phase turbulence.* In Fluent this approach is referred to as *dispersed turbulence model*.

Mixture In this approach the turbulence model is evaluated for the mixture of all phases, i.e. the mixture velocity and mixture density are inserted into the turbulence model. The turbulent quantities of each individual phase are computed with the density ratio between the mixture and the corresponding phase. The applicability of this model is described in the Fluent Theory Guide [9] as follows: [...] *is applicable when phases separate, for stratified (or nearly stratified) multiphase flows, and when the density ratio between phases is close to 1.*

Per-phase In this case each phase has its own turbulent properties. Because there are additional transport equations to be solved per phase, this model is the most computational intensive. The Fluent Theory Guide [9] states: [...] *is the appropriate choice when the turbulence transfer among the phases plays a dominant role.*

42.3.2 Implementation in OpenFOAM

In Section 39.1 the frameworks for implementing turbulence modelling within OpenFOAM are discussed. Now we take a look on multi-phase turbulence and OpenFOAM's frameworks for modelling turbulence.

¹⁵²See http://pic.dhe.ibm.com/infocenter/compgbg/v121v141/topic/com.ibm.xlcpp121.bg.doc/language_ref/cplr061.html for details.

The old framework, see Section 39.1.1, allow only for the first two of the described strategies, since only one turbulence model is employed by the multiphase solvers. The turbulence model is generally a global object within the solver, as is also the mesh or the run-time object.

The new framework allows for greater flexibility. In the Eulerian multiphase solvers, the turbulence model has been moved to the phase model. Thus, each phase has its own turbulence model. This allows for all three modelling strategies discussed in Section 42.3.1. The turbulence modelling employed by *twoPhaseEulerFoam* within the new framework is discussed in Section 55.4.

42.4 Interfacial momentum exchange

On the RHS of the momentum equation there are two types of source terms. The first term $\mathbf{F}_{q,i}$ is a force density acting on the phase q . The second term is a force (density) coefficient $K_{qp,i}$ which is multiplied by the relative velocity $\mathbf{u}_R = \mathbf{u}_p - \mathbf{u}_q$ between the phases q and p .

The models for interfacial momentum transfer in OpenFOAM are implemented in a way, such that these models return either a force or a force coefficient¹⁵³. The distinction between forces and force coefficients is a matter of convenience. Contributions directly proportional to the velocity, e.g. drag, can be treated differently than contributions indirectly proportional to the velocity, e.g. the virtual mass force which is proportional to the time derivative of the relative velocity. Terms directly proportional to the velocity are numerically treated differently than other terms.

The interfacial momentum transfer due to drag, lift and virtual mass are based on the force acting on a single bubble. The turbulent dispersion force is observed when the turbulent eddies of the liquid phase interact with a swarm of bubbles. This interaction tends to disperse bubble swarms [46]. Figure 137 gives a schematic representation of the different momentum exchange mechanisms between the liquid and the gas phase.

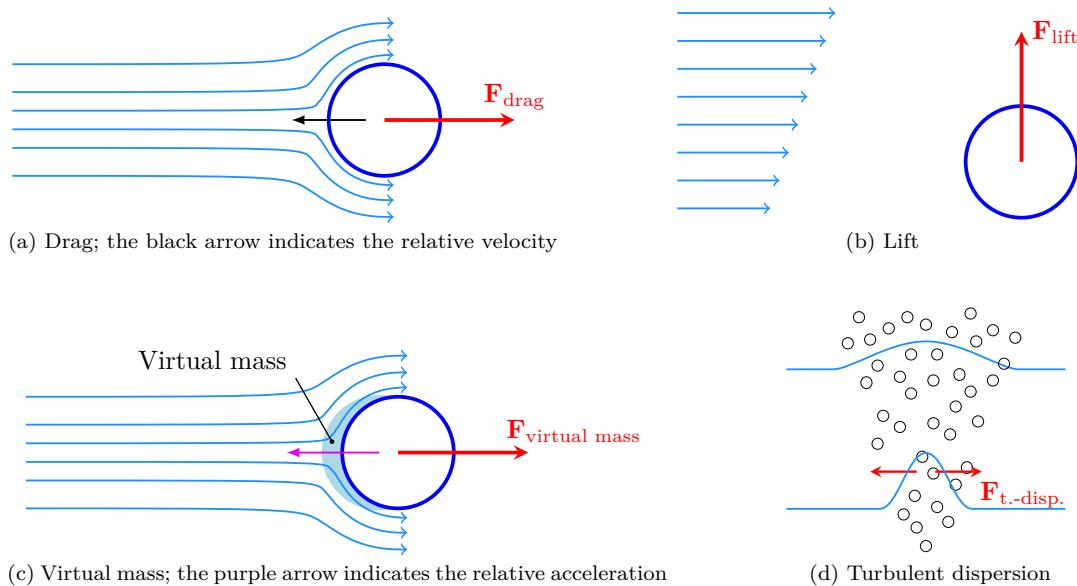


Figure 137: Modelling approach on the example of a gas-liquid two-phase system.

42.5 Diameter models

As mentioned in the previous Section, diameter models were introduced at some point in the multiphase models. The *multiphaseEulerFoam* offered since its introduction in version 2.1.0 two diameter models (constant and isothermal). With *twoPhaseEulerFoam*-2.3 a further diameter model was introduced, which is available only in *twoPhaseEulerFoam*.

¹⁵³The correct denomination would be force density and force density coefficient. In the source files of OpenFOAM related to these models, $\mathbf{F}_{q,i}$ and $K_{qp,i}$ are referred to as force and force coefficient, most probably for the sake of reducing typing effort. As OpenFOAM keeps track of the physical units of its variables, we can see from the actual source codes, that the force $\mathbf{F}_{q,i}$ is in fact a force density.

OpenFOAM	Constant, no model	Constant	Isothermal	IATE
<i>twoPhaseEulerFoam</i>				
2.0.x	x			
2.1.x	x			
2.2.x	x			
2.3.x		x	x	x
<i>multiphaseEulerFoam</i>				
2.1.x		x	x	
2.2.x		x	x	
2.3.x		x	x	

Table 7: Overview of diameter modelling in Eulerian multiphase solvers

42.5.1 No model

The older versions of *twoPhaseEulerFoam* ($\leq 2.2.x$) use no model for the diameter of the dispersed phase elements (DPE). In all of these versions the phase diameter is a scalar of type `dimensionedScalar` that is read from the `transportProperties` dictionary.

42.5.2 Constant

The `constantDiameter` diameter model is the implementation of a constant diameter in a framework that allows for a variable diameter.

Internally, the diameter is still a scalar which is read from `transportProperties` respectively from `phaseProperties`. However, the phase model returns the diameter as a field quantity. Listing 296 shows how a `volScalarField` is returned. The private variable `d_` is of the type `dimensionedScalar`.

```

1 Foam::tmp<Foam::volScalarField>
2 Foam::diameterModels::constant::d()
3 const
4 {
5     return tmp<Foam::volScalarField>
6     (
7         new volScalarField
8         (
9             IOobject
10            (
11                "d",
12                phase_.U().time().timeName(),
13                phase_.U().mesh()
14            ),
15            phase_.U().mesh(),
16            d_
17        )
18    );
19 }
```

Listing 296: Accessing the diameter in `constantDiameter`.

42.5.3 Isothermal

Gas bubbles change their diameter as the ambient pressure changes. The `isothermalDiameter` model implements this behaviour by assuming the change of state to be isothermal.

Generally, the ideal gas law (67) governs the state of a gas.

$$pV = nRT \quad (67)$$

under the assumption of an isothermal state

$$pV = \text{const} \quad (68)$$

Next we introduce the bubble volume

$$V = \frac{d^3\pi}{6} \quad (69)$$

Thus, we gain the relation

$$p_1 d_1^3 \frac{\pi}{6} = p_2 d_2^3 \frac{\pi}{6} \quad (70)$$

This leads to the isothermal diameter model

$$d_2 = d_1 \sqrt[3]{\frac{p_1}{p_2}} \quad (71)$$

For the `isothermalDiameter` model the user needs to specify a reference pressure and diameter. Listing 297 shows the `d()` method of the class `isothermalDiameter`. The reference pressure `p0_` and diameter `d0_` are private data members of the class¹⁵⁴. With Eqn. (71) the local diameter is computed (Line 10).

```

1  Foam::tmp<Foam::volScalarField>
2  Foam::diameterModels::isothermal::d()
3  const
4  {
5      const volScalarField& p = phase_.U().db().lookupObject<volScalarField>
6      (
7          "p"
8      );
9
10     return d0_*pow(p0_/p, 1.0/3.0);
11 }
```

Listing 297: The method `d()` of the class `isothermalDiameter`.

42.5.4 IATE

IATE stands for *interfacial area transport equation*. This model is based on [35]. The `IATE` diameter model solves a transport equation for the interfacial curvature `kappaI_`.

Solves for the interfacial curvature per unit volume of the phase rather than interfacial area per unit volume to avoid stability issues relating to the consistency requirements between the phase fraction and interfacial area per unit volume.

Class description in `IATE.H`

In Section 76 we cover the derivation of the governing equations implemented in OpenFOAM from the equations in [35].

42.6 Thermophysical models

Each phase in a multi-phase simulation is assigned its own set of models with regards to thermo-physical properties, such as density, dynamic viscosity and specific heat capacity. The set of available models is discussed in Section 40. In this section, we focus on the use of thermophysical modelling with respect to multiphase simulations.

42.6.1 A note on using thermophysical properties in BCs

If we want to specify a massflow boundary condition in a multiphase simulation, we need to specify which density is to be used for computing the velocity BC from the mass flow. Listing 298 shows an example, of how we can specify massflow BCs. Note, the entry `rho`, which tells OpenFOAM which density to use to compute the actual velocity BC.

¹⁵⁴An underscore (`_`) as suffix to the variable name apparently indicates private variables. Although the coding style guidelines of OpenFOAM (<http://openfoam.org/contrib/code-style.php>) do not explicitly say so. However, this is recommended style by other communities, e.g. <http://geosoft.no/development/cppstyle.html>.

```

boundaryField
{
    inlet
    {
        type          flowRateInletVelocity;
        massFlowRate  0.2;
        rho           thermo:rho.air;
        extrapolateProfile no;
        value         uniform (0 0 0);
    }
    // ...
}

```

Listing 298: Specifying a massflow BC in an `U.air` file, here we need to specify the phase-density.

In multiphase solvers, access to the density field is generally handled by the phase-model class. Thus, the multiphase solvers do not create registered density fields, in contrast to compressible single-phase solvers, such as `rhoPimpleFoam`. As access to the density is handled via the phase model's thermophysical model, this reflects in the way we refer to the phase's density when we e.g. specify a massflow BC.

Note, that in Line 7 of Listing 298 a single colon (:) is used as a separator. This can potentially be confused with the double colons (::), which are used in C++ to separate namespace qualifiers. However, in a certain way, we find that this is also a sort of namespace, since the `thermo` prefix indicates that this field is a field which is provided by the thermophysical model, as opposed to solver-managed fields, such as `p` or `U`.

42.6.2 A note on post-processing thermophysical quantities

Section 42.6.1 also applies, when we want to do some post-processing on thermophysical quantities, e.g. write out the gas-density field as shown in Listing 299. Here, we also use a single colon (:) to separate the `thermo` qualifier from the name of the field, i.e. `rho.air`. Using a double colon, or just the field's name alone would result in an error.

```

writeObjects1
{
    type      writeObjects;
    libs      ("libutilityFunctionObjects.so");

    objects   (
        thermo:rho.air
    );
    writeOption anyWrite;
}

```

Listing 299: Writing the gas-density field to disk, using the `writeObjects` function object.

43 Boundary conditions

When the geometry of a problem is meshed, then the boundary patches – i.e. the faces delimiting the geometry – need to be specified. Every boundary patch is of a certain type. In Section 43.1 the possible types are discussed.

43.1 Base types

43.1.1 Geometric boundaries

Some kinds of boundary patches can be described purely geometrically. The numerical treatment of this kind of patches is inherently clear to the solver and needs no more modelling.

symmetry plane If a problem is symmetric, then only half of the domain needs to be modelled. The boundary that lies in the symmetry plane is of type *symmetry plane*.

empty OpenFOAM creates always three-dimensional meshes. If a two-dimensional simulation needs to be conducted, then the mesh must be one cell in thickness. The boundaries that are parallel to the considered plane must be of the type *empty* to cause the simulation to be two-dimensional.

wedge If a geometry is axisymmetric, then the problem can be simplified. In this case, only a part of the geometry – a wedge – is modelled. The additional boundaries are of type *wedge*.

cyclic Cyclic boundary.

processor A boundary between sub-domains created during the domain decomposition is of type *processor*.

43.1.2 Complex boundaries

Some kinds of boundary patches are more than just a geometric boundary of the domain. E.g. on a wall, the no-slip condition usually applies, therefore there is need for further modelling.

patch This is the generic type for all boundaries. A boundary is of this type, if none of the following types applies.

wall This is a special type for walls. This type is mandatory for using wall models when modelling turbulence.

The boundaries of the types *patch* and *wall* need to be specified further. These boundaries can have boundary conditions of the *primitive* or *derived* types.

43.2 Primitive types

The most important *primitive type* boundary conditions are:

fixedValue The value of a quantity is prescribed directly.

fixedGradient The gradient of a quantity is prescribed directly.

zeroGradient The gradient of a quantity is prescribed to zero.

```
type          fixedValue;
value         uniform (0 0 0);
```

Listing 300: *fixedValue* boundary condition

43.3 Derived types

The boundary condition of the *derived types* are derived from the boundary conditions of the *primitive types*. The boundary conditions of this type can be used to model more complex situations.

43.3.1 inletOutlet

The behaviour of the *inletOutlet* boundary condition depends of the flow direction. If the flow is directed outwards, then a *zeroGradient* boundary condition is applied. If the flow is inwards, then a fixed value is prescribed. The value of the inflowing quantity is provided by the *inletvalue* keyword. The *value* keyword has to be present, but it is not relevant.

```
type           inletOutlet;
inletValue    uniform (0 0 0);
value         uniform (0 0 0);
```

Listing 301: inletOutlet boundary condition

43.3.2 surfaceNormalFixedValue

The `surfaceNormalFixedValue` boundary condition prescribes the norm of a vector field. The direction is taken from the surface normal vector of the patch. A positive value for `refValue` means, that this quantity is directed in the same direction as the surface normal vector. A negative value means the opposite direction.

```
type           surfaceNormalFixedValue;  
refValue      uniform -0.1;
```

Listing 302: `surfaceNormalFixedValue` boundary condition

43.3.3 pressureInletOutletVelocity

This boundary condition is a combination of *pressureInletVelocity* and *inletOutlet*.

43.4 Pitfalls

43.4.1 Syntax

When assigning a `fixedValue` boundary condition, OpenFOAM expects the keyword `uniform` or `nonuniform` after the `value` keyword.

Listing 303 shows the file `0/k`. There the inlet boundary definition differs from Listing 300. Note the missing `uniform` keyword. The reaction of OpenFOAM differs from the value after the keyword `version`.

Listing 304 shows the warning message OpenFOAM issues, when the value after the keyword `version` is 2.0 like in Listing 303. In this case, OpenFOAM assumes `uniform`.

If the value after the keyword `version` is 2.1, then OpenFOAM will issue an error message like in Listing 305.

In both cases OpenFOAM-2.1.x was used. The author assumes the reason for this distinction between version 2.0 and 2.1 lies in an extension of the possible boundary conditions. See the release notes of OpenFOAM-2.1.0 (<http://www.openfoam.org/version2.1.0/boundary-conditions.php>).

```
FoamFile
{
    version      2.0;
    format       ascii;
    class        volScalarField;
    object       k;
}

// * * * * * //

dimensions      [0 2 -2 0 0 0 0];

internalField   uniform 1e-8;

boundaryField
{
    inlet
}
```

```

{
    type      fixedValue;
    value     1e-8;
}

```

Listing 303: The file 0/k

```
--> FOAM Warning :
From function Field<Type>::Field(const word& keyword, const dictionary&, const label)
in file /home/user/OpenFOAM/OpenFOAM-2.1.x/src/OpenFOAM/lnInclude/Field.C at line 262
Reading "/home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bubblePlume/case/0/k::
boundaryField::inlet" from line 25 to line 26
expected keyword 'uniform' or 'nonuniform', assuming deprecated Field format from Foam
version 2.0.
```

Listing 304: Warning message: missing keywords

```
--> FOAM FATAL IO ERROR:
expected keyword 'uniform' or 'nonuniform', found on line 26 the doubleScalar 1e-08

file: /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bubblePlume/case/0/k::boundaryField
::inlet from line 25 to line 26.

From function Field<Type>::Field(const word& keyword, const dictionary&, const label)
in file /home/user/OpenFOAM/OpenFOAM-2.1.x/src/OpenFOAM/lnInclude/Field.C at line 278.
```

FOAM exiting

Listing 305: Warning message: missing keywords

43.5 Time-variant boundary conditions

Time-variant boundary conditions can help to avoid problems from an inept initialisation of the solution data. The most easy initialisation is to prescribe all values to be zero throughout the domain, see Listing 205 in Section 33.

At the start of a simulation when the non-zero values of some boundary meet the zero values of the neighbouring cells stability problems may arise due to the large relative velocities. One solution would be to choose a very small time step at the beginning. Another solution would be to prescribe a time-variant boundary condition. Thus, the field-values at the boundary are initially small and grow during a certain time span to their final value.

43.5.1 uniformFixedValue

This boundary condition is an generalisation of the `fixedValue` BC. See <http://www.openfoam.org/version2.1.0/boundary-conditions.php>.

Listing 306 shows the definition of a time-variant boundary condition with a fixed value. Between the time $t = 0.0\text{ s}$ and $t = 5.0\text{ s}$ the value of the boundary condition is linearly interpolated between the values for both ends of the interval. After this interval has ended, the value of the boundary condition remains constant.

```

inlet
{
    type      uniformFixedValue;
    uniformValue  table
    (
        ( 0.0    (0.0 0.0 0.0) )
        ( 5.0    (0.0 0.0 0.1) )
    );
}

```

Listing 306: Definition of a time-variant boundary condition

The boundary condition `uniformFixedValue` accepts any general function of one variable (`Function1`) as its `uniformValue`. See Section 13.1.1 for a more detailed discussion on functions of one variable. In this case, the independent variable of this functions is obviously the time.

Pitfall: old two-phase solvers

This boundary condition does not work with two-phase solvers of old OpenFOAM versions. With OpenFOAM-4 using time-variant boundary conditions poses no problem anymore.

43.6 plenumPressure - a deep dive into a somewhat complex BC

The plenumPressure boundary condition models an upstream reservoir with an optional entering mass flow. This boundary condition is described in its header file as follows:

This boundary condition provides a plenum pressure inlet condition. This condition creates a zero-dimensional model of an enclosed volume of gas upstream of the inlet. The pressure that the boundary condition exerts on the inlet boundary is dependent on the thermodynamic state of the upstream volume. The upstream plenum density and temperature are time-stepped along with the rest of the simulation, and momentum is neglected. The plenum is supplied with a user specified mass flow and temperature.

The result is a boundary condition which blends between a pressure inlet condition condition and a fixed mass flow. The smaller the plenum volume, the quicker the pressure responds to a deviation from the supply mass flow, and the closer the model approximates a fixed mass flow. As the plenum size increases, the model becomes more similar to a specified pressure.

Listing 307 shows an example of this boundary condition, taken from the description in the header file. There, we see the specification of the boundary condition's type followed by the isentropic exponent `gamma` and the specific gas constant `R`. Then, the properties of the supply are stated in the form of the mass flow rate and the temperature. Next, the plenum volume is stated followed by the initial condition of the reservoir in the form of the initial density and temperature.

```
<patchName>
{
    type          plenumPressure;
    gamma         1.4;
    R             287.04;
    supplyMassFlowRate 0.0001;
    supplyTotalTemperature 300;
    plenumVolume   0.000125;
    plenumDensity  1.1613;
    plenumTemperature 300;
    inletAreaRatio 1.0;
    inletDischargeCoefficient 0.8;
    timeScale      1e-4;
    value          uniform 1e5;
}
```

Listing 307: Definition of the `plenumPressure` boundary condition

Listing 308 shows the key working part of the boundary condition. Looking at Line ?? of Listing 308, we see the ideal gas relation, as the current plenum pressure is computed from density and temperature.

```
1 // Calcaulate the specific heats
2 const scalar cv = R_/(gamma_ - 1), cp = R_*gamma_/(gamma_ - 1);
3
4 // Calculate the new plenum properties
5 plenumDensity_ =
6     plenumDensityOld_
7     + (dt/plenumVolume_)*(supplyMassFlowRate_ - massFlowRate);
8 plenumTemperature_ =
9     plenumTemperatureOld_
10    + (dt/(plenumDensity_*cv*plenumVolume_))
11    *
12        supplyMassFlowRate_
13        *(cp*supplyTotalTemperature_ - cv*plenumTemperature_)
14        - massFlowRate*R_*plenumTemperature_
15    );
16 const scalar plenumPressure = plenumDensity_*R_*plenumTemperature_;
```

Listing 308: The core working part of the `plenumPressure` boundary condition: computing the current density, temperature and pressure.

In Lines 5 to 7 of Listing 308, we see the conservation of mass for the reservoir, i.e., the plenum. Note, that `supplyMassFlowRate` denotes the user-specified incoming mass flow rate, and `massFlowRate` denotes the mass flow rate which acts on the respective patch this boundary condition is applied to. From the plenum's perspective, this is the outgoing mass flow.

In order to proof this, we shall derive this equation from the mass conservation of a general reservoir.

$$m = \rho V \quad (72)$$

with m being the fluid mass in the reservoir, ρ the fluid density and V the (constant) volume of the reservoir. Next, we shall formulate the conservation of mass:

$$\frac{dm}{dt} = \dot{m}_{in} - \dot{m}_{out} \quad (73)$$

$$\frac{d(\rho V)}{dt} = \dot{m}_{in} - \dot{m}_{out} \quad (74)$$

$$V \frac{d\rho}{dt} = \dot{m}_{in} - \dot{m}_{out} \quad (75)$$

Next, we shall replace the temporal derivative of the density ρ with a finite difference in time, with ρ_n denoting the new value, and ρ_o denoting the old value:

$$V \frac{\rho_n - \rho_o}{\Delta t} = \dot{m}_{in} - \dot{m}_{out} \quad (76)$$

$$\rho_n - \rho_o = \frac{\Delta t}{V} (\dot{m}_{in} - \dot{m}_{out}) \quad (77)$$

after some rearrangement, we arrive at the formulation we see in Listing 308:

$$\rho_n = \rho_o + \frac{\Delta t}{V} (\dot{m}_{in} - \dot{m}_{out}) \quad (78)$$

In Equation (78), we see the plenum's volume in the denominator. Thus, if the volume is large, then the mass flows have only a small influence on the current density. If the volume is very small, then the contribution of the mass flows is significant. This confirms the header file's description, which states that:

The smaller the plenum volume, the quicker the pressure responds to a deviation from the supply mass flow, and the closer the model approximates a fixed mass flow. As the plenum size increases, the model becomes more similar to a specified pressure.

In Lines 8 to 15 of Listing 308, we see the conservation of energy. This is somewhat less immediately apparent than the conservation of mass, but we shall derive the conservation of energy for a general reservoir to demonstrate the point.

We shall start from the conservation of energy for an open system with no mechanical work done and no heat transferred. Thus, the only way the plenum can gain or loose energy is via mass flow across its boundaries.

$$\frac{dU}{dt} = \dot{Q}_{in} - \dot{Q}_{out} \quad (79)$$

with U being the internal energy of the fluid

$$\frac{d(c_v m T)}{dt} = c_p \dot{m}_{in} T_{in} - c_p \dot{m}_{out} T_{out} \quad (80)$$

Next, we apply the product rule of differentiation to the temporal derivative:

$$c_v \frac{dT}{dt} m + c_v T \frac{dm}{dt} = c_p \dot{m}_{in} T_{in} - c_p \dot{m}_{out} T_{out} \quad (81)$$

Next, we apply a finite difference to the temporal derivative of the temperature and we express the temporal derivative if the fluid mass in terms of the sum of the mass flows:

$$c_v \frac{T_n - T_o}{\Delta t} m + c_v T_o (\dot{m}_{in} - \dot{m}_{out}) = c_p \dot{m}_{in} T_{in} - c_p \dot{m}_{out} T_{out} \quad (82)$$

Next, we shall perform some rearrangement of terms:

$$c_v \frac{T_n - T_o}{\Delta t} m = c_p \dot{m}_{in} T_{in} - c_p \dot{m}_{out} T_{out} - c_v T_o (\dot{m}_{in} - \dot{m}_{out}) \quad (83)$$

$$T_n - T_o = \frac{\Delta t}{c_v m} \left[c_p \dot{m}_{in} T_{in} - c_p \dot{m}_{out} T_{out} - c_v T_o (\dot{m}_{in} - \dot{m}_{out}) \right] \quad (84)$$

$$T_n = T_o + \frac{\Delta t}{c_v \rho V} \left[c_p \dot{m}_{in} T_{in} - c_v T_o \dot{m}_{in} - c_p \dot{m}_{out} T_{out} + c_v T_o \dot{m}_{out} \right] \quad (85)$$

$$T_n = T_o + \frac{\Delta t}{c_v \rho V} \left[\dot{m}_{in} (c_p T_{in} - c_v T_o) - (c_p - c_v) \dot{m}_{out} T_{out} \right] \quad (86)$$

Now, we can use the thermodynamic relation $R = c_p - c_v$. Furthermore, we use the identity $T_o = T_{out}$:

$$T_n = T_o + \frac{\Delta t}{c_v \rho V} \left[\dot{m}_{in} (c_p T_{in} - c_v T_o) - R \dot{m}_{out} T_o \right] \quad (87)$$

Now, Equation (87) very much looks like the code in Lines 8 to 15 of Listing 308.

44 Mesh interfaces: AMI and ACMI

In a perfect world, the gods of CFD look favourably upon us mere earthly creatures. However, as the world is far from perfect, the gods of CFD, in their infinite wisdom, blessed us with some of their beloved nasties: non-conformal meshes, moving meshes and various other things.

However, not all hope is lost. OpenFOAM offers AMI and ACMI to address the issues of unconnected meshes and moving meshes.

44.1 AMI and ACMI in brevity

AMI

The arbitrary mesh interface (AMI) can be used for connecting two unconnected meshes, when the connecting patches fully overlap, e.g. a rotating, cylindrical mesh within a surrounding stationary mesh. AMI was introduced in OpenFOAM-2.1¹⁵⁵.

AMI can be used not only to solve rotating mixer within a stationary domain, as e.g. in the various *mixerVessel* tutorials of solvers capable of employing a dynamic mesh. We can also use AMI to couple two unconnected, stationary meshes. Thus, we may have an easier time at mesh creation since, we can mesh mesh sub-domains individually and couple them in the simulation using AMI.

ACMI

With OpenFOAM-2.3¹⁵⁶ the AMI method was extended and the arbitrary coupled mesh interface (ACMI) was introduced. The ACMI allows for having partially overlapping patches.

44.2 Arbitrary Mesh Interface - AMI

44.2.1 Use case - varying body orientation

If we wanted to study the drag on a triangular body at various orientations, we could either create a mesh for each individual orientation of the body in question, or we could harness the power of AMI.

In Figure 138 we see a simulation domain consisting of two unconnected regions. The outer domain, in grey, has a cylindrical void. The inner domain contains the body under investigation, and its outer boundary is such that the inner domain fills the void of the outer domain. The inner boundary of the outer domain as well as the outer boundary of the inner domain are both of the type `cyclicAMI`.

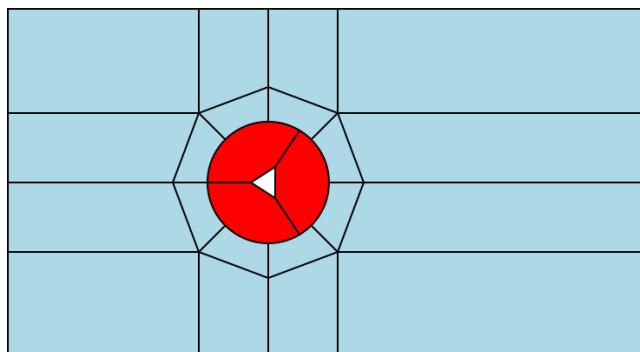


Figure 138: Our simulation domain. The block structure of outer domain, in blue, does not match the block structure of the inner domain, in red. However, by keeping the two regions separate, we can mesh each region individually, which is fairly easy, and use AMI to essentially connect the two regions. After meshing, we can rotate the inner domain with respect to the outer domain to change the orientation of the triangle in the center of the inner domain.

Thus, AMI will deal with the information exchange between the two unconnected mesh regions. When simulating the flow, the two regions will act as if they were a single one. Furthermore, AMI frees us from the

¹⁵⁵See <https://openfoam.org/release/2-1-0/ami/>

¹⁵⁶See <https://openfoam.org/release/2-3-0/non-conforming-ami/>

worry to create a matching mesh on the connecting boundary, i.e. the mesh of the inner patch of the outer domain, and the mesh of the outer patch of the inner domain do not need to match. The only thing we need to specify is which patch needs to talk with which other patch, i.e. we need to specify the neighbouring patch of each AMI patch.

When we study the flow for various orientations of the body in question, we simply rotate the inner domain with respect to the outer domain to get a proper mesh for current orientation. Thus, while we created a single mesh, we can study an arbitrary number of orientations without the need to create the same number of meshes. We simply use the utility `moveMesh` to rotate the inner domain to the new orientation, and we are good to go.

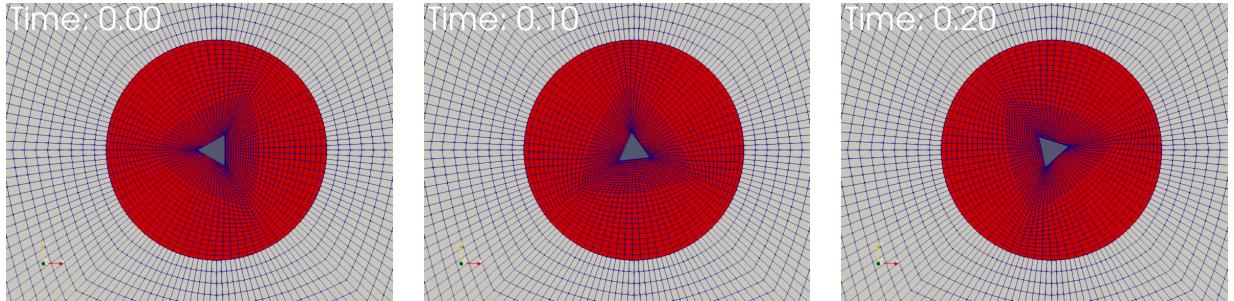


Figure 139: Varying the orientation of the investigated body. Since the body-fitting mesh of the inner domain is in an over-all cylindrical shape, we simply can rotate the inner domain with respect to the outer domain, to change the orientation of the investigated body with respect to the incident flow. After creating the mesh, we can use `moveMesh` to rotate the inner domain. With appropriate settings for the angular velocity and the write interval, we can get a mesh for any orientation of the triangular prism.

This case demonstrates the use of AMI for studies with a purely stationary mesh. If we apply all the steps described above, to each time step of a simulation, instead of an individual simulation of a parametric study, we end up with a sliding mesh simulation case. Thus, AMI enables simulations with a dynamic, sliding mesh.

However, AMI can also be used for simulations with purely stationary meshes. Sometimes it is easier to mesh individual regions of the simulation domain individually, and let AMI handle the connection of this regions. In the case of two stationary unconnected mesh regions¹⁵⁷, we could alternatively use `stitchMesh` to connect the two regions. Using `stitchMesh` will result in a mesh with one single region.

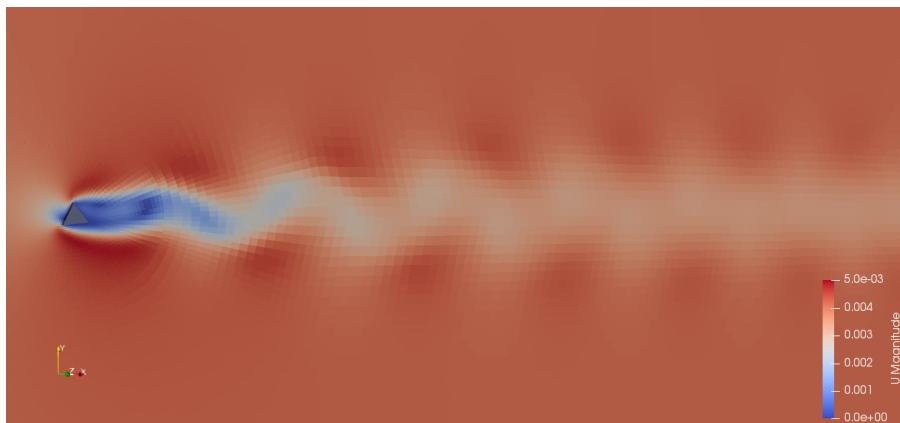


Figure 140: A 2D simulation of the triangular, prismatic body in laminar cross-flow using AMI to connect the body fitted mesh of the inner region with the mesh of the outer domain.

44.3 Arbitrary Coupled Mesh Interface - ACMI

The arbitrary coupled mesh interface works in a similar way as the AMI with the exception that the involved patches do not need to overlap completely.

¹⁵⁷Or any number of unconnected mesh regions.

44.3.1 Use case - varying body orientation

To demonstrate the ACMI, we use again the example from above. Only this time, our inner domain does not fill the outer domain completely, see Figure 141. In this example, the remaining void represents the body under investigation, i.e. a prismatic body with a semi-circular base. Again, by rotating the inner domain with respect to the outer domain, we change the orientation of the body under investigation.

The inner boundary of the outer domain is a patch with the form of a cylinder shell. The outer boundary of the inner domain, however, has the shape of the shell of a semi-cylinder. Thus, the two patches forming the interface of the outer and inner domain overlap only partially.

The ACMI needs to distinguish whether a face has a neighbour, i.e. the face is part of the overlapping section of the patch; or the face has no neighbour, i.e. the face acts as a wall. Thus, we need a pair of patch definitions for each domain: *couple* and *blockage*. In the case of *couple*, we need to specify the neighbouring patch, as we needed in the AMI case. In the case of *blockage*, we need to specify the behaviour, in most cases: being a wall.

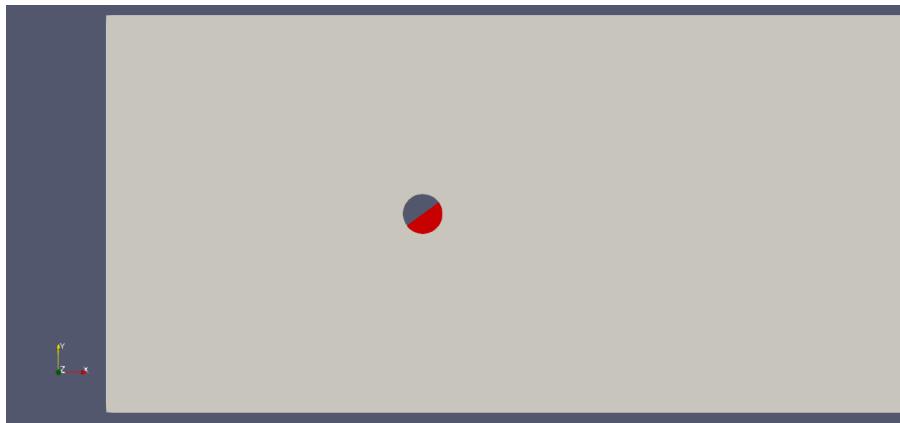


Figure 141: A simulation domain with two unconnected regions. Note that the inner region only partially fills the void of the outer region.

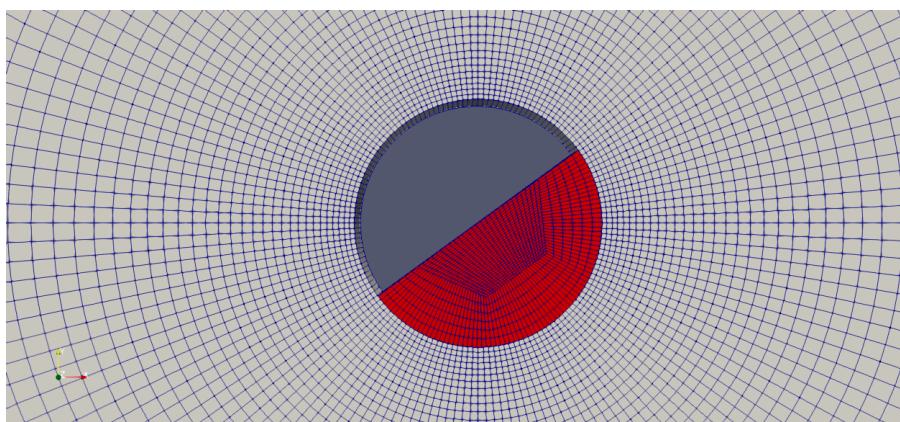


Figure 142: The inner domain in more detail. The block-structure of the inner domain is clearly recognizable. The remaining void is the body under investigation, in this case a semi-cylinder.

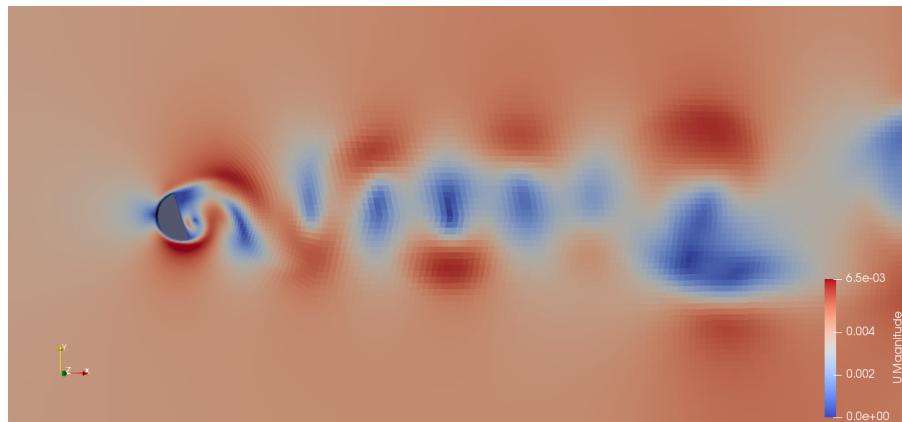


Figure 143: A 2D simulation of the semi-cylinder in laminar cross-flow using ACMI to connect the mesh of the inner region with the mesh of the outer domain.

44.4 Avoiding errors

44.4.1 AMI and MRF

When using AMI in conjunction with MRF, add the AMI patches to the list of non-rotating patches in the file `MRFProperties`.

45 The MRF method

The MRF method allows for the simulation of rotating machinery without an actually rotating mesh. By using multiple reference frames, we can simulate the problem with a static mesh. Although, this simplification introduces certain modelling errors, the reduced complexity and faster computation times compared to a simulation with a moving mesh, as well as the sufficient precision on a global scale, justifies this method under the right circumstances. See Section 77 for the theoretical background of the MRF method.

45.1 Usage

The MRF method is applied to cell zones. This is clearly indicated by the `cellZone` keyword in the `MRFProperties` dictionary, see Listing 309. Apart from where to apply the MRF method, we can enable/disable the application of the MRF method using the `active` keyword.

Another important input is the list of non-rotating patches, aptly named `nonRotatingPatches`, as the solid body rotation according to the rotation of the reference frame is applied to all wall patches. However, there might be the case of patches within the MRF cell zone, that are actually stationary, hence the option to exclude individual patches from the application of the MRF method.

Finally, in Listing 309, the nature of the rotation of the reference frame is specified. This is done by providing the axis of rotation (`axis`) and a point in space (`origin`). The point origin must be located somewhere on the axis of rotation. The keyword `omega` is used to specify the rotational velocity.

```
zone1
{
    cellZone      rotor;
    active        yes;

    // Fixed patches (by default they 'move' with the MRF zone)
    nonRotatingPatches ();

    origin        (0 0 0);
    axis          (0 0 1);

    omega         table
                  2(
                      (0      0.0)
                      (0.75  20.0)
                  );
}
```

Listing 309: Specifying the necessary inputs for the MRF method in the `MRFProperties` dictionary.

Figure 144 shows the cell zone for the mesh of a stirred tank. The cell zone, to which the MRF method is applied, is shown as white wireframe. Note, that this zone is of cylindrical shape and is aligned with the axis of rotation.

If we extended the cylinder from the very bottom to the very top, then the bottom and top patches of the stator would need to be entered into the list of non-rotating patches.

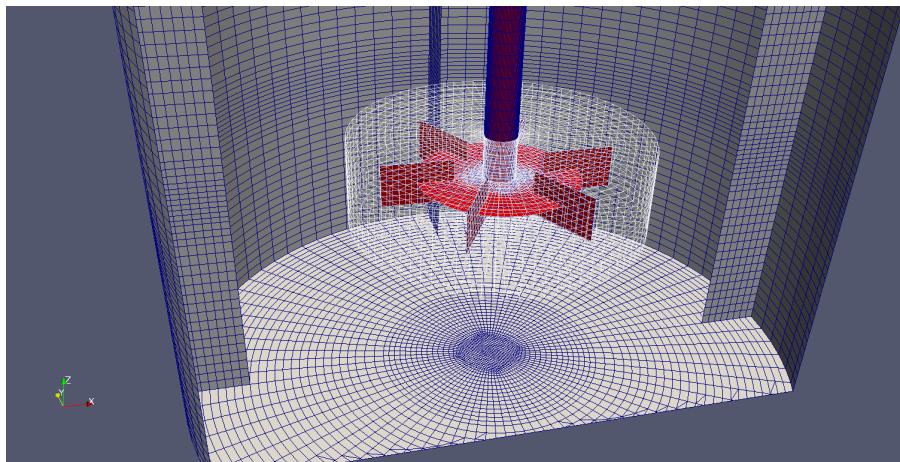


Figure 144: A baffled stirred tank with a Rushton impeller. The stator patch is shown in grey and the rotor patch is shown in red. The white wireframe shows the boundary of the rotor zone. For all cells of the rotor zone the MRF method is applied.

45.2 Avoiding errors

45.2.1 Non-rotating patches

AMI and MRF

It has been found, that AMI-type patches need to be added to the list of non-rotating patches, see Section [44.4.1](#).

Cyclic patches and MRF

It has been observed, that when using cyclic-type patches, e.g. when simulating half a stirred tank as in Figure [145](#), we need to add the cyclic-type patches to the list of non-rotating patches in the file `MRFProperties`.

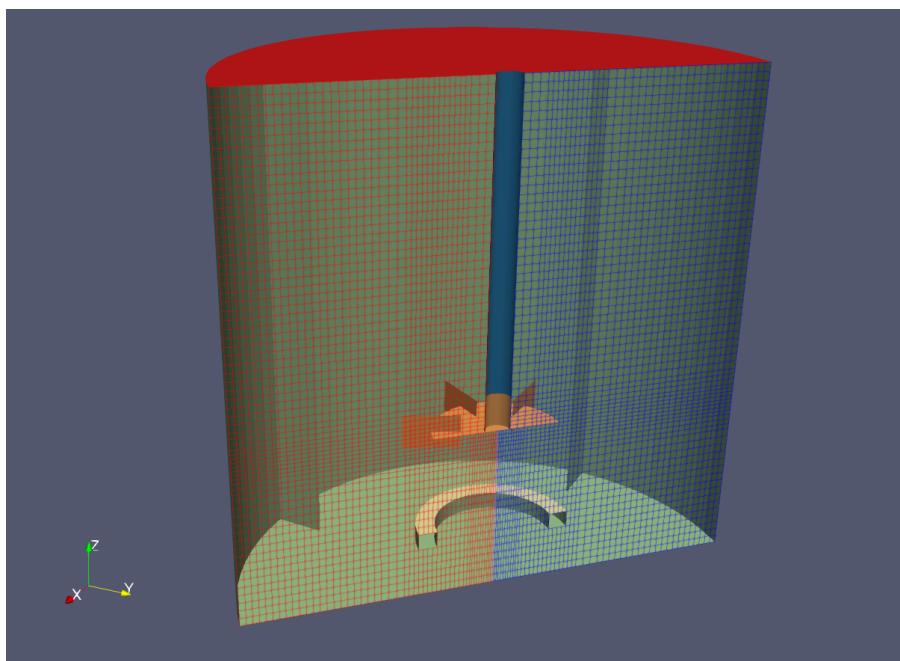


Figure 145: Half a baffled stirred tank with a Rushton impeller. The cyclic-type patches are shown as coloured wireframes, and all other patches are shown as coloured surfaces.

46 The fvOption framework

The `fvOption` framework handles sources and constraints of our numerical flow model. The `fvOption` framework allows us to plug various constraints or sources into an existing solver without any solver modification. Besides general sources and constraints, there is a number of specialised sources representing a specific physical models, e.g. the effect of a porous zone on the momentum equation.

The `fvOptions` framework was introduced with the release of OpenFOAM-2.2.0¹⁵⁸ in 2013 and has expanded since.

Motivation

The use of the `fvOption` framework is best explained on an example. Equation (88) shows a convective transport equation for a general scalar C , e.g. a passive tracer concentration. On the RHS, we see the general, linearized source term. If, in our example, the tracer enters the simulation domain through the inlet, then all is well and an inlet BC for the tracer concentration C suffices. If, however, the tracer is introduced via a probe, which we do not want to resolve with our mesh¹⁵⁹, then we need a mechanism to introduce the tracer C within our simulation domain. This is where `fvOptions` come to the rescue. These offer us to specify, at the location of the tip of the probe, an injection rate or a fixed value for the field C .

$$\frac{\partial C}{\partial t} + \nabla \cdot (C\mathbf{u}) = S_u + S_p C \quad (88)$$

The `fvOption` framework offers a fixed-value constraint and a semi-implicit source, with which we can model our tracer generating probe.

Application

Below, in Listing 310, we see the energy equation of a compressible flow solver of OpenFOAM. In this Listing, all calls to the `fvOptions` framework are marked in red, green and blue. There, we see that the `fvOptions` framework can act on the governing equation of a certain field itself, as well as act on the computed field after the governing equation has been solved.

```
1 {  
2     volScalarField& he = thermo.he();  
3     fvScalarMatrix EEqn  
4     (  
5         fvm::ddt(rho, he) + fvm::div(phi, he)  
6         + fvc::ddt(rho, K) + fvc::div(phi, K)  
7         + (  
8             he.name() == "e"  
9                 ? fvc::div  
10                (  
11                    fvc::absolute(phi/fvc::interpolate(rho), U),  
12                    p,  
13                    "div(phiv,p)"  
14                )  
15                : -dpdt  
16            )  
17            - fvm::laplacian(turbulence->alphaEff(), he)  
18            ==  
19            fvOptions(rho, he)  
20        );  
21  
22     EEqn.relax();  
23     fvOptions.constrain(EEqn);  
24     EEqn.solve();  
25     fvOptions.correct(he);  
26     thermo.correct();  
27 }
```

Listing 310: The energy equation in the file `EEqn.H` of the compressible, single-phase solver `rhoPimpleFoam`

¹⁵⁸<https://openfoam.org/release/2-2-0/fv-options/>

¹⁵⁹E.g. the smoke probe used in wind tunnels for the study of external aerodynamics.

A solver, that uses the fvOptions framework creates an object of the type `fvOptionList`, which is a list of `fvOptions`. This is also the reason why, for all calls to the fvOptions framework, parameters have to be passed. Otherwise, the framework would not be able to assign the options to their respective equations. In the case of a porous zone in the domain of a single-phase simulation, we might use the fvOptions framework to account for the additional flow resistance in the momentum equation and also to apply certain source terms for the turbulence model equations. Thus, the list of options has to be traversed to find and apply the proper `fvOption` to the respective model equation.

In the Listing 311 below, we see the method `fvOptionList::constrain()` as an example of how OpenFOAM applies the fvOptions. We traverse the list of all options, and for each options, we check whether this option applies to the provided model equation. If the option applies, it is determined whether the option is enabled, i.e. whether it is active, and if this is the case, the option is applied by calling the `constrain()` method of the `fvOption` class, i.e. calling the `constrain()` method of the source itself.

```

1 template<class Type> void Foam::fv::optionList::constrain(fvMatrix<Type>& eqn)
2 {
3     checkApplied();
4     forAll(*this, i)
5     {
6         option& source = this->operator[](i);
7         label fieldi = source.applyToField(eqn.psi().name());
8         if (fieldi != -1)
9         {
10             source.setApplied(fieldi);
11             if (source.isActive())
12             {
13                 if (debug)
14                 {
15                     Info<< "Applying constraint " << source.name()
16                         << " to field " << eqn.psi().name() << endl;
17                 }
18                 source.constrain(eqn, fieldi);
19             }
20         }
21     }
22 }
```

Listing 311: The method `constrain()` of the class `fvOptionList`

The mode of operation shown above is the same for all calls to the fvOptions framework, we see in Listing 310. Each call causes the list of options to be traversed, and all applicable options to be applied.

46.1 Controlling space & time

A number of `fvOptions` are derived from the base class `cellSetOption`, which implements control over when and where the `fvOption` is to be active. This is used for porous zones, which make up only part of the simulation domain, or for tracer injection, which might be of limited duration.

The active time of the `fvOptions` derived from `cellSetOption` is controlled by the keywords `timeStart` and `duration`. The region in which the option is to be acting can be selected by providing the name of a `cellSet` or a `cellZone`, by specifying points in space, or by providing cell labels.

This, however, does not apply to all `fvOptions`. For some of them, a restriction to a limited time span or a certain region would make no sense at all, e.g. for considering buoyant forces on the momentum equation.

46.2 Types of options

The fvOptions framework implements a number of different options, which fall into one of the following categories:

46.2.1 Constraint

A constraint acts on an already computed field. We can infer this from the point in the code when the method `fvOptions.constrain()` is called, the relevant line is high-lighted in green in Listing 310.

With a constraint, fixed values at certain locations can be enforced in an otherwise freely computed field, e.g. if we are solving the passive transport of a scalar acting as a tracer or marker, we can define certain cells,

in which the value of the scalar has a fixed value. These locations would be points in space, where the tracer is injected into our simulation domain.

Available constraints, at the time of writing, are:

- `fixedValueConstraint`
- `fixedTemperatureConstraint`

46.2.2 Correction

A correction is a type of option, that acts on a field after it has been computed. We can infer this from the point in the code when the method `fvOptions.correct()` is called, the relevant line is high-lighted in blue in Listing 310.

Available corrections, at the time of writing, are:

- `limitTemperature`
- `limitVelocity`

46.2.3 Source

A source adds source and sink terms to the governing equation of a certain field. Thus, a source influences a field via the solution process of its governing equation. We can infer this from the point in the code when `fvOptions()` is called, the relevant line is high-lighted in red in Listing 310. In contrast to the constraints and the corrections, the sources call the ()-operator class `fvOptionList`.

There is a large number of sources available in OpenFOAM, ranging from very general ones, such as `codedSource` or `semiImplicitSource` to specific sources for certain specific purposes, e.g. `actuationDiscForce`, `buoyancyForce` and many others.

46.3 Sources

This sub-section contains an incomplete list of sources from the `fvOptions` framework.

46.3.1 Porosity models

The `fvOptions` framework can be used to model the influence of porous zones on the flow, e.g. the catalytic converter in an exhaust system. The presence of a porous medium acts as a sink in the fluid's momentum equation. The `explicitPorositySource` fvOption can be used to model the effect of porous zones in a flow simulation.

Listing 312 shows the momentum equation of *pimpleFoam*. Here, the contributions from the `fvOptions` framework are on the RHS. A porosity model will introduce a negative term on the RHS, since porous zones require additional force to drive the fluid through them.

```

1   fvm::ddt(U) + fvm::div(phi, U)
2   + MRF.DDt(U)
3   + turbulence->divDevReff(U)
4   ==
5   fvOptions(U)

```

Listing 312: The momentum equation in the file *UEqn.H* of *pimpleFoam*

fixedCoeff

The `fixedCoeff` model calculates a momentum contribution \mathbf{S} which is proportional to the velocity and the squared velocity. The model features two model constants: α and β .

$$\mathbf{S} = -\rho_{\text{Ref}} (\alpha + \beta |\mathbf{u}|) \mathbf{u} \quad (89)$$

or a little rearranged

$$\mathbf{S} = -\rho_{\text{Ref}} (\alpha|\mathbf{u}| + \beta|\mathbf{u}|^2) \mathbf{u}$$

In OpenFOAM's implementation α and β are vectorial quantities. In addition with a reference coordinate system for the porous zone, anisotropic porosity can be considered. Isotropic porosity is then a special case covered by choosing all components of α and β to be equal.

powerLaw

The **powerLaw** model computes a momentum contribution \mathbf{S} , which is proportional to a model constant C_0 and the C_1 -th power of the velocity. The **powerLaw** model does not support anisotropy.

$$\mathbf{S} = -\rho C_0 |\mathbf{u}|^{(C_1-1)} \mathbf{u} \quad (90)$$

or a little rearranged

$$\mathbf{S} = -\rho C_0 |\mathbf{u}|^{C_1} \mathbf{e}_u$$

DarcyForchheimer

The **DarcyForchheimer** model is very similar to the **fixedCoeff** model. It also has two contributions proportional to the linear and the squared velocity. This model is a combination of the Darcy model $U = -\frac{\kappa}{\mu} \frac{dp}{dx}$, which is valid for laminar flow, and the its extension to higher Reynolds numbers, known as Forchheimer model $-\frac{dp}{dx} = \frac{\mu}{\kappa} U + \frac{\rho}{k_2} U^2$. The Darcy model is proportional to κ , the permeability of the porous medium, $[\kappa] = \text{m}^2$. The Forchheimer model introduces k_2 , the inertial permeability, $[k_2] = \text{m}$.

There are two model constants of OpenFOAM's implementation of the **DarcyForchheimer** model. The Darcy coefficient d is the inverser permeability $d = \frac{1}{\kappa}$, and the Forchheimer coefficient f is the inverse inertial permeability $f = \frac{1}{k_2}$.

$$\mathbf{S} = -(\mu d + 1/2 \rho |\mathbf{u}| f) \mathbf{u} \quad (91)$$

or a little rearranged

$$\mathbf{S} = -\rho (\nu d |\mathbf{u}| + 1/2 f |\mathbf{u}|^2) \mathbf{e}_u$$

In OpenFOAM's implementation d and f are vectorial quantities, as are the coefficients of the **fixedCoeff** model. In addition with a reference coordinate system for the porous zone, anisotropic porosity can be considered. Isotropic porosity is then a special case covered by choosing all components of d and f to be equal.

46.3.2 phaseLimitStabilization

With OpenFOAM-6¹⁶⁰ an fvOption source was introduced to specifically, numerically stabilize transport equations when the phase fraction falls below a certain threshold. This source adds an implicit source term to a transport equation for all cells in which the phase fraction falls below a certain limit.

Solving transport equations, which are formulated using a phase fraction field, becomes numerically more and more difficult when the phase fraction field tends to zero in some cells. Adding an implicit source term in those cells ensures the discretized equation system does not become ill-posed. When a transport equation becomes ill-posed due to a phase fraction tending towards zero, the solver of the linear equation system fails with a floating-point error.

Listing 313 shows the code of the relevant method of this source class. The `max()` statement ensures that the source is only applied to cells in which the phase fraction `alpha` is smaller than the limit `residualAlpha`.

```

1 template<class Type> void Foam::fv::PhaseLimitStabilization<Type>::addSup
2 (
3     const volScalarField& alpha,
4     const volScalarField& rho,
```

¹⁶⁰<https://openfoam.org/release/6/>

```

5     fvMatrix<Type>& eqn,
6     const label fieldi
7 }
8 {
9     const GeometricField<Type, fvPatchField, volMesh>& psi = eqn.psi();
10    uniformDimensionedScalarField& rate =
11        mesh_.lookupObjectRef<uniformDimensionedScalarField>(rateName_);
12
13    eqn -= fvm::Sp(max(residualAlpha_ - alpha, scalar(0))*rho*rate, psi);
14 }
```

Listing 313: The method `addSup()` of the class `PhaseLimitStabilization`

We see from the code in Listing 313, that a `uniformDimensionedScalarField` `rate` is used to compute the implicit source. This `uniformDimensionedScalarField` `rate` can be created by a `codedFunctionObject` and then be registered with the mesh. Only when the `uniformDimensionedScalarField` `rate` is registered with the mesh, can the `PhaseLimitStabilization` source access it via the `lookup()` method of the mesh. Listing 314 shows an example of how this can be done. The relevant line of code to register the computed rate field is highlighted in red. If this line is omitted, then the `fvOption` source will abort with an error caused by trying to lookup a non-existent field. See Section 68.7 for in-depth information on the object registry.

```

functions
{
    rate
    {
        libs          ("libutilityFunctionObjects.so");
        type coded;
        name rate;
        codeRead
        #{
            static autoPtr<uniformDimensionedScalarField> pField;
            if (!pField.valid())
            {
                pField.set
                (
                    new uniformDimensionedScalarField
                    (
                        IOobject
                        (
                            "rate.water",
                            mesh().time().timeName(),
                            mesh(),
                            IOobject::NO_READ,
                            IOobject::NO_WRITE
                        ),
                        dimensionedScalar("rateInit", dimensionSet(0, 0, -1, 0, 0, 0, 0), 1.0)
                    )
                );
            }
            uniformDimensionedScalarField& rate = pField();
            rate.checkIn();
        #};
    }
}
```

Listing 314: Computation of a rate field using a `codedFunctionObject` in the file `controlDict`.

47 The Lagrangian world

In OpenFOAM not only the *finite volume method* (FVM), which is part of the Eulerian world, is implemented. There are also Lagrangian methods available. The Lagrangian methods available in OpenFOAM cover fields such as:

- molecular dynamics
- discrete particle method
- sprays
- general Lagrangian particle tracking
- reacting and combusting particles

This section covers general Lagrangian particle tracking. The basics behind the Lagrangian methods apply to all models listed above, e.g. the molecule and the spray parcel are based on the `particle` class.

47.1 Background

47.1.1 Interaction between Lagrangian particles and Eulerian flow

The coupling between Lagrangian particles and the surrounding (Eulerian) flow can be characterised by their degree of interaction.

<i>one-way</i>	<i>two-way</i>	<i>four-way</i>
flow acts on particles	flow acts on particles particles act on the flow	flow acts on particles particles act on the flow particle-particle collisions
e.g. snow drift	e.g. dense particulate flows	e.g. fluidized beds

Table 8: Levels of coupling between Lagrangian particles and (Eulerian) flow

Controlling the level of interaction

OpenFOAM's Lagrangian model library is able to accommodate for one-way, two-way and four-way interaction.

47.1.2 Particle tracking

For particle tracking there are two general approaches, the *lose-find* method and the *face-to-face* method [49, 42]. Knowing the cell in which a particle is located is important when interaction with the flow fields is to be considered.

The *lose-find* method tracks the particle along its path according to its velocity. The information on the cell in which the particle is located, however, is lost in this process. Hence, this method is referred to as *lose-find*. Whenever, the current cell in which the particle is located is needed, the neighbouring cells need to be searched until the particle is found. This approach can pose some problems [49].

The *face-to-face* method, which is implemented by OpenFOAM, tracks the particles to the cell faces, updates the cell information and tracks the particle further on [42]. Thus, only once at the start of the simulation the cells at the particles' locations need to be searched. During the simulation the cell index to which a particle belongs is continuously updated whenever the particle crosses a cell face.

Barycentric tracking

With the release of OpenFOAM-5.0, the LPT algorithm was changed to barycentric tracking¹⁶¹, see also the relevant commit message¹⁶². Barycentric tracking has been implemented to increase the robustness of the tracking algorithm.

¹⁶¹<https://cfd.direct/openfoam/free-software/barycentric-tracking/>

¹⁶²<https://github.com/OpenFOAM/OpenFOAM-dev/commit/371762757dbe3cd38a3841a547a9bc8c1aff0b85>

47.2 Libraries

OpenFOAM offers two choices for implementing or using Lagrangian particle tracking (LPT). A discussion on these can be found in [44].

```
particle
```

The class `particle` is the root of all LPT in OpenFOAM, since it implements the tracking (i.e. the motion) of the particles itself.

47.2.1 basic solidParticle

The basic choice for LPT is the class `solidParticle`, which is derived from `particle`. The class `solidParticle` adds little to its ancestor class. The two additional data members are the particle's diameter and velocity. The two most important methods of `solidParticle` are `move()` and `hitWallPatch()`. With these two methods the particle's drag (via modifying the particle's velocity in `move()`) and the wall interaction (i.e. wall collision, via modifying the particle's velocity in `hitWallPatch()`) can be implemented. This is sufficient for one-way and two-way coupled simulations.

47.2.2 intermediate parcels

The advanced implementation of LPT in OpenFOAM is the `intermediate` library¹⁶³ in `$FOAM_SRC/lagrangian`. This library contains some heavily templated classes which provide a general framework to implement a range of additional models for LPT, e.g. collision modelling, heat transfer or reactions. The intermediate library was first published with OpenFOAM-1.5beta¹⁶⁴.

The basis for LPT itself is again the class `particle`, although hidden under layers of templates, Listings 315 and 316 show a prime example of OpenFOAM's template insanity.

```
1 namespace Foam
2 {
3     typedef ReactingMultiphaseParcel
4     <
5         ReactingParcel
6         <
7             ThermoParcel
8             <
9                 KinematicParcel
10                <
11                    particle
12                >
13            >
14        >
15     > basicReactingMultiphaseParcel;
16
17 /* the rest of the code ... */
```

Listing 315: The class definition of the `ReactingMultiphaseParcel` class, in `basicReactingMultiphaseParcel.H`

The class `KinematicParcel` is an example for the hardships one faces when trying to understand C++. `KinematicParcel` is a templated class, with `ParcelType` as template parameter. In addition `KinematicParcel` also is derived from its template parameter `ParcelType`.

Thus, `KinematicParcel` is a templated class built around `ParcelType`, however, it *is a* `ParcelType` too (by inheritance).

```
1 template<class ParcelType>
2 class KinematicParcel
3 :
4     public ParcelType
5 {
```

¹⁶³`$FOAM_SRC/lagrangian/intermediate` is actually a library, since it is a separate compilation unit and is compiled into `$(FOAM_LIBBIN)/liblagrangianIntermediate`.

¹⁶⁴<http://www.openfoam.org/download/version1.5beta.php>

```

6 public:
7
8 /* the rest of the code ... */

```

Listing 316: The class definition of the `KinematicParcel` class, in `KinematicParcel.H`

To underpin the claim made, that `particle` is the very root of LPT, we have a look at the most basic parcel-based class of the `intermediate` library of OpenFOAM. Listing 317 shows the definition of the class `basicKinematicParcel`, which is the class `particle` passed to the templated class `KinematicParcel` as a template parameter. From one of the above paragraphs, we know that this means also that `basicKinematicParcel` is derived from `particle`, hence it *is a particle*.

```

1 namespace Foam
2 {
3     typedef KinematicParcel<particle> basicKinematicParcel;
4
5     template<>
6     inline bool contiguous<basicKinematicParcel>()
7     {
8         return true;
9     }
10 }

```

Listing 317: The class definition of the `basicKinematicParcel` class, in `basicKinematicParcel.H`

47.3 Cloudy, with a chance of particles

In OpenFOAM and its class layout there is the distinction between the single particle and the entirety of all particles. The particle class defines the features and the behaviour of the single particle. The Lagrangian solver, however, needs to deal with all particles. Not all particles are equal, but the solver should not have to deal with this. In order to provide a common interface for the solver, OpenFOAM's creators thought of the `cloud` class.

The `cloud`¹⁶⁵ is class acts as a connection between the solver and the individual particles. It makes sure that commands are passed on to all particles within the cloud.

47.3.1 The code to rule them all

This section is one of the many examples of OpenFOAM's sources being case-sensitive. The class `Cloud` and the class `cloud` are completey different things. Admittedly, `Cloud` is derived from `cloud`, thus every `Cloud` *is a* `cloud`, however, not vice-versa. Always keep in mind: case matters.

The Cloud

A class is best described by taking a look on the code that actually defines it. Listing 318 shows from which classes `Cloud` is derived from. Looking at the inheritance actually tells us what the class `Cloud` is, since an inheritance relation is an “*is a*” relation. If A is derived from B, then A *is a* B.

The listing shows us, that `Cloud` is a `cloud` and a `IDLLList`. This poses two new questions, what is a `cloud` and a `IDLLList`?

```

1 template<class ParticleType>
2 class Cloud
3 :
4     public cloud,
5     public IDLLList<ParticleType>
6 {
7     // code
8 }

```

Listing 318: The class definition of `Cloud` in the file `Cloud.H`; the ancestry.

In anticipation of the following paragraphs we can state, that the inheritance from two base classes is an example of applied division of labour. As we will see, the `cloud` heritage is in charge of input and output (I/O) whereas the `IDLLList` legacy deals with the management of the single particles which form the cloud.

¹⁶⁵Not to be mixed up with the “cloud” in terms of information technology (IT) as in cloud storage, cloud computing, etc..

The cloud

The class `cloud` is an object registry similar to the mesh class¹⁶⁶. `cloud` is derived from the class `objectRegistry`, and so are `fvMesh` and `Time`. This enables us to register fields with the particle cloud. The class `objectRegistry` is in turn derived from `regIOobject` which is in turn derived from `IOobject`. Thus, the ancestry of `cloud` allows us to read and write the particle cloud to disk¹⁶⁷. See Sections 68.7 and 68.8 for a more detailed discussion on I/O and the concepts around the class `regIOobject`.

Disk I/O is most often seen in code that creates or reads fields. Via the `cloud` branch of a Lagrangian cloud's ancestry, disk I/O is controlled in a similar fashion. If we were able to sneak the line of code in Listing 319 e.g. into `DPMFoam`, right after the construction of the `kinematicCloud` object, then writing the Lagrangian solution data to disk would be permanently disabled.

```
1 kinematicCloud.writeOpt() = IOobject::NO_WRITE;
```

Listing 319: Disabling writing to disk for `kinematicCloud`

The IDLLList

The `IDLLList` is an *intrusive doubly-linked list*. The concept of a linked list is taught at programming classes when it comes to objects and data-structures. The traditional linked-list consists of a list class and a node class. The node class contains a pointer to, or the list-element itself. If the node class is implemented in a generic fashion, using templates, then one list implementation is sufficient for all datatypes. Otherwise, the node class would need to be implemented specifically for every datatype that is to be used by the list.

An intrusive linked-list is a very efficient implementation of a linked-list. However, the actual layout differs from the standard layout of a linked list¹⁶⁸. In an intrusive list, the list element serves also as the node. Figure 146 compares the schematic layouts of traditional and intrusive linked lists.

Intrusive linked-lists are generally considered as being much more efficient than traditional linked-lists¹⁶⁹. One of the downsides of using intrusive lists is that the implementation of the datatype which is to be used within the list is mangled with the implementation of the list itself. Generally, this (mangling the implementation of unrelated concepts) is considered a bad practice in *object-oriented design* (OOD). However, due to the performance gain, intrusive lists are widely used in fields where performance beats conformity with standards, such as computer games or number crunching.

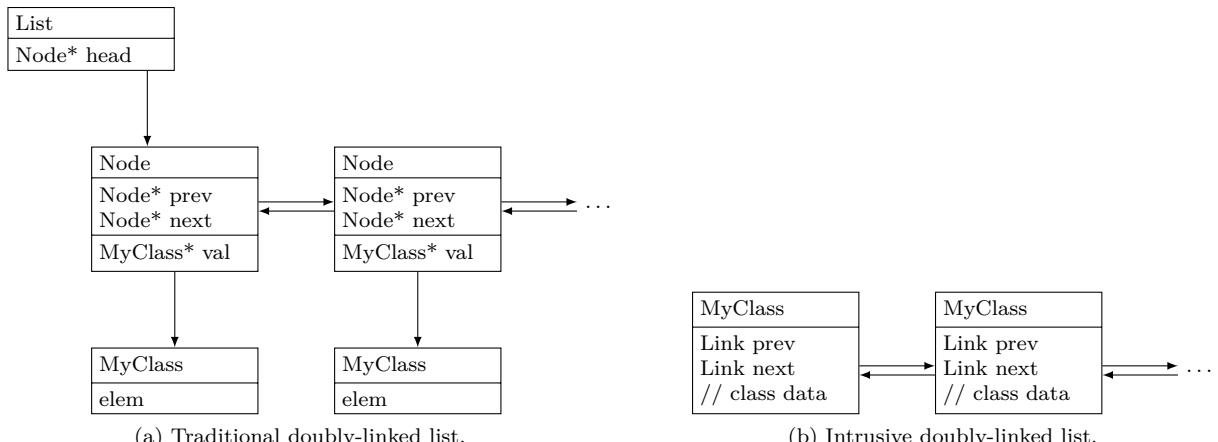


Figure 146: Schematic diagrams of doubly-linked lists.

¹⁶⁶In fact the class `polyMesh` is derived from `objectRegistry`. `fvMesh` is in turn derived from `polyMesh`. The mesh in a solver or an utility application is of the type `fvMesh`. Almost all solvers and utilities include the file `createMesh.H`, which resides in `OpenFOAM/include` of your installation.

¹⁶⁷Fields, such as `volScalarField` and others, are also derived from `regIOobject` via `GeometricField` and `DimensionedField`.

¹⁶⁸http://www.boost.org/doc/libs/1_43_0/doc/html/intrusive/intrusive_vs_nonintrusive.html

¹⁶⁹http://www.boost.org/doc/libs/1_58_0/doc/html/intrusive/performance.html

Again, we can take a look at the actual source code to find out what is really going on. Figure 147 shows the class diagram behind the singly- and doubly-linked intrusive lists. This diagram is in fact a great example of how far C++ developers can go with abstraction and encapsulation. The classes `SLLListBase` and `DLLListBase` define the behaviour as being single-linked or doubly-linked. The classes `UILList` and `ILList` are more or less helper or base classes. The class `UILList` provides STL-conforming iterators, whereas `ILList` adds some member functions. The reason for `UILList` and `ILList` being separate classes is unknown to the author.

In the case of classic linked lists (non-intrusive lists, either singly- or doubly-linked), the class `LList` derived from its template parameter `LListBase` provides the base class for concrete non-intrusive linked lists.

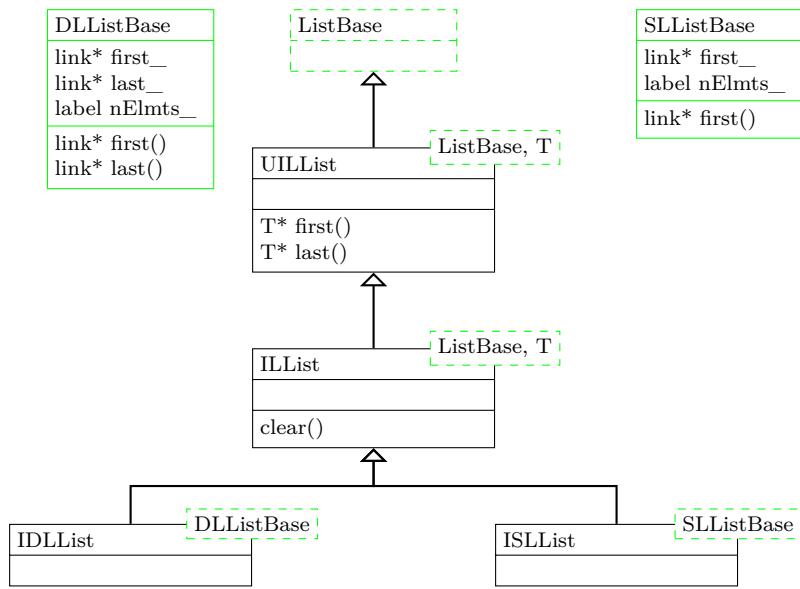


Figure 147: The class hierarchy needed for intrusive lists of objects of type `T`; this diagram can be regarded as a subset of the class diagram for singly- and doubly-linked lists, both classic and intrusive.

47.4 Cloudy Templates

The Lagrangian models are modularized by making heavy use of inheritance and templating. This compartmentalisation of functionality and data is done for the clouds as well as the particles themselves. This approach makes perfect sense as particles of the type `X` need a cloud of the type `X` to make `X`'s properties available to the outside world (i.e. the solver using model `X`). To be more specific, if we want to solve heat transport with Lagrangian particles, the particles themselves need to provide appropriate data (temperature) and methods (heat transfer), as well as the cloud needs to offer appropriate methods (heat transfer from the particles to the carrier phase and vice versa). Thus, most of the points discussed below hold also for the particles.

The templates for both the clouds and the particles create a framework which allows to create specific clouds and particles simply by combining the templates carrying the intended functionality.

47.4.1 Base classes

`kinematicCloud`

This virtual abstract class (note the lower case `k` in `kinematic`) specifies the behaviour of the templated class `KinematicCloud` (note the capital `K` in the class' name).

`thermoCloud`

Also the virtual abstract class `thermoCloud` declares some abstract methods, i.e. methods that a derived class must implement.

47.4.2 Templates

There are two kinds of cloud templates: the ones that are derived from a base class and their template parameter `CloudType`, and the ones that are solely derived from their template parameter. In the following we try to shed some light into the *tempest of templates*.

Base class + template parameter

One example for such a cloud template is the class `KinematicCloud` (note the capital K). This class is derived from the class `kinematicCloud` (minor k) and its template parameter `CloudType`. The base class defines the behaviour of the kinematic part, and the template parameter allows to add additional functionality.

A class passed as a template parameter can provide data and methods as well as a separate base class. However, pure abstract methods can realistically only be provided via the separate base class. The `kinematicCloud` (lower case k) base class provides, among others, the pure virtual method `nParcels()`, which returns the total number of parcels. If this method was provided by the `KinematicCloud` (capital K) template class, then we would not be able to instantiate the `basicKinematicCloud`, as in Listing 322, since we can not create objects of abstract classes.

Another reason for deriving a cloud template from a base class and their template parameter is to introduce the debugging mechanism of the run-time selection framework. Listing 320 shows the relevant lines for the example of the base class `thermoCloud`. This allows the use of the `debug` flag in the class `ThermoCloud`.

```

1  namespace Foam
2  {
3      defineTypeNameAndDebug(thermoCloud, 0);
4 }
```

Listing 320: Introduction of `thermoCloud` into the debugging mechanism in the file `thermoCloud.C`

Template parameter

The classes `CollidingCloud` and `MPPICCloud` are templated clouds, which are derived only from their template parameter. Both classes provide modelling for particle-particle interactions¹⁷⁰.

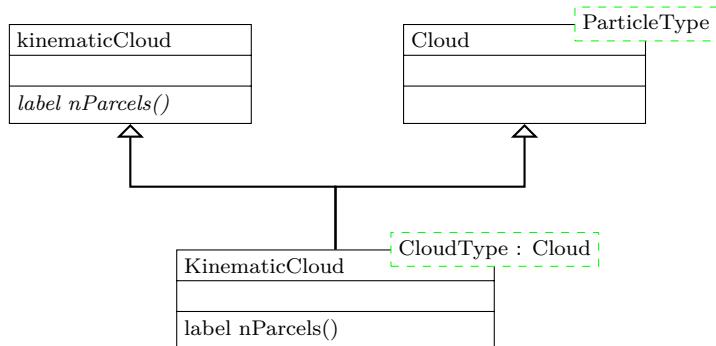


Figure 148: The class hierarchy of the class `basicKinematicCloud`.

47.4.3 Derived clouds

The derived cloud classes are the classes which we can actually use. The most basic derived cloud class is `basicKinematicCloud`, which offers the minimal set of functionality. As we see in Listing 321, the `basicKinematicCloud` is build from the `KinematicCloud` template with a `Cloud` of `basicKinematicParcel`¹⁷¹ as template parameter. Here the dual templated hell of Lagrangian modelling reveals itself nicely. The template parameter of `Cloud` is a particle type `basicKinematicParcel`. The definition of this particle type is shown in Listing 322. The type `basicKinematicParcel` is also the most basic particle type provided by the Lagrangian `intermediate` library of OpenFOAM.

¹⁷⁰See <https://openfoam.org/release/2-3-0/dpm/>

¹⁷¹As the reader might remember, the class `Cloud` takes a template parameter `ParticleType`.

We note, that the kinematic cloud is a cloud of kinematic particles. The kinematic particle class provides the means to move the particle around and the kinematic cloud type provides the means to move the particles collectively. This is useful since a solver using Lagrangian particles does not operate on the individual particles.

```
1 namespace Foam {
2     typedef KinematicCloud<Cloud<basicKinematicParcel>> basicKinematicCloud;
3 }
```

Listing 321: The class definition of `basicKinematicCloud` in the file `basicKinematicCloud.H`

```
1 namespace Foam {
2     typedef KinematicParcel<particle> basicKinematicParcel;
3 }
```

Listing 322: The class definition of `basicKinematicParcel` in the file `basicKinematicParcel.H`

To substantiate the claim from above, that the templates allow us to build custom Lagrangian models, we take a look at some more derived clouds. In Listing 323 we see the definition of a cloud class, which offers heat transfer modelling. This class throws the `ThermoCloud` template into the mix of the already known `KinematicCloud` class. In combination with Listing 324, we see that the `basicThermoCloud` is a `Cloud` of `basicThermoParcels`. Again, the type of the cloud is reflected in the type of the parcel.

```
1 namespace Foam {
2     typedef ThermoCloud
3     <
4         KinematicCloud
5         <
6             Cloud
7             <
8                 basicThermoParcel
9                 >
10            >
11        > basicThermoCloud;
12 }
```

Listing 323: The class definition of `basicThermoCloud` in the file `basicThermoCloud.H`

```
1 namespace Foam {
2     typedef ThermoParcel<KinematicParcel<particle>> basicThermoParcel;
3 }
```

Listing 324: The class definition of `basicThermoParcel` in the file `basicThermoParcel.H`

47.5 The evolution of clouds

The title of section is taken from the main method a solver calls during its run: `evolve()`. Listing 325 shows the heavily redacted run-time loop of DPMFoam, where we see a call of the cloud's `evolve()` method prior to the PIMPLE loop which computes the fluid flow. Hence, the title of this section.

```
1 while (pimple.run(runTime))
2 {
3     Info<< "Evolving " << kinematicCloud.name() << endl;
4     kinematicCloud.evolve();
5
6     // --- Pressure-velocity PIMPLE corrector loop
7     while (pimple.loop())
8     {
9         // ...
10    }
11
12    runTime.write();
13 }
```

Listing 325: The bare-bones run-time loop of the solver DPMFoam

47.5.1 Evolution calling

What happens exactly, when the `evolve()` method of the cloud is called? To answer this question, we have to travel the family tree. Figure 149 shows some of the involved methods and classes when a call to `evolve()` is made by a solver using a Lagrangian particle cloud.

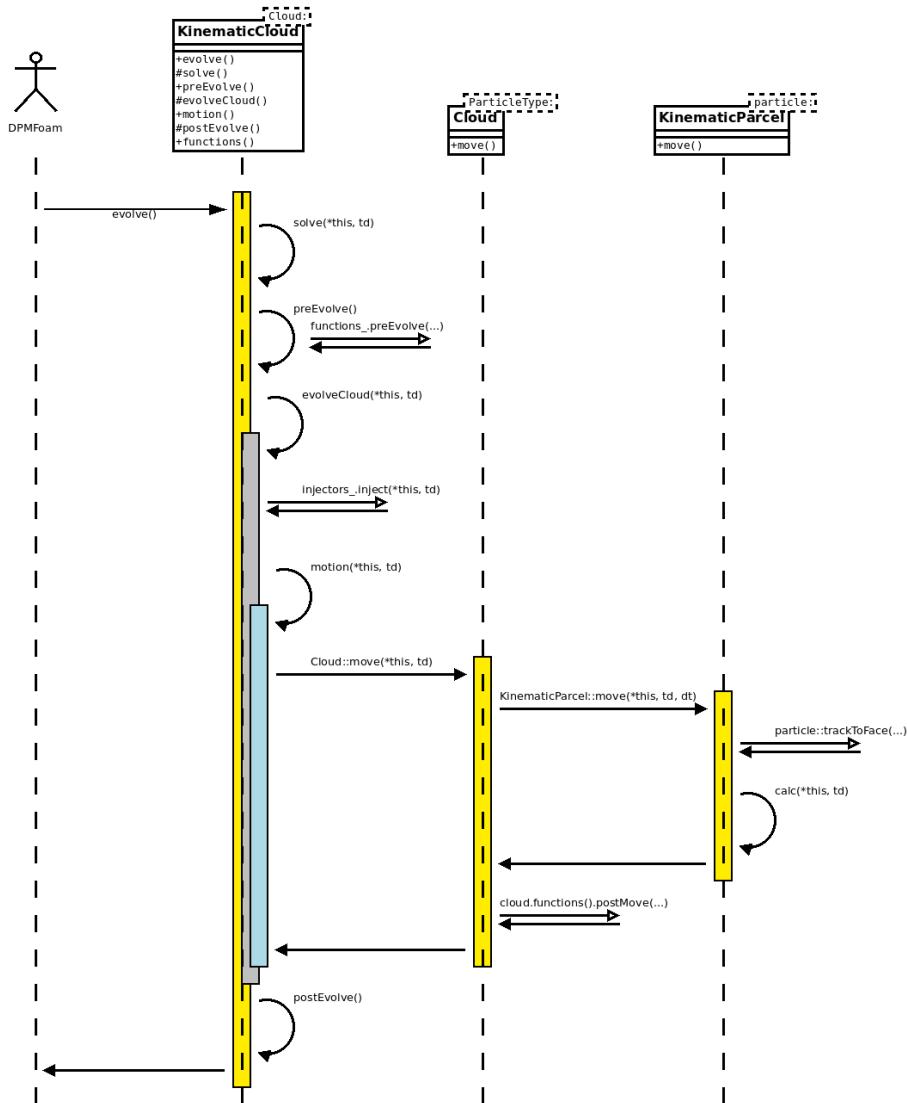


Figure 149: A simplified sequence diagram of a call to `evolve()` from `DPMFoam`.

The sequence shown in Figure 149 is more important to the developer than to the user. Cloud function objects do offer methods that are evaluated at various stages over this sequence. The names of the methods are quite telling: `preEvolve()`, `postEvolve()`, etc., with these it is important for the developer to understand the sequence of events.

47.6 Run-time post-processing

The cloud class offers function object to perform some run-time post-processing. These can be found at `$FOAM_SRC/lagrangian/intermediate/submodels/CloudFunctionObjects`. Among the cloud function objects are ones for counting particles crossing a certain patch or computing the volume fraction field of the lagrangian particles. See Section 47.8.2 for a more detailed discussion on cloud function objects.

47.7 Times of Use

47.7.1 Not so telling error messages

Out of domain

As OpenFOAM's Lagrangian particle framework keeps track of the cells in which a particle is located, a Lagrangian solver needs to determine the cell label of each particle's initial position. OpenFOAM's particle tracking algorithm is described among other resources in [45, 42, 49].

When a particle is placed outside the domain, i.e. the position in the `positions` file is outside the domain, OpenFOAM is unable to find a cell label for this very particle. Note that failing to find a cell which contains the particle's location may happen also for other reasons than placing it outside the domain. As the error message in Listing 326 suggests, this might also happen through a combination of insufficient write precision and domain decomposition or reconstruction. However, plainly putting them outside the domain is also a possibility, especially, when a script is used to create the initial particle distribution.

```
--> FOAM FATAL ERROR:

cell, tetFace and tetPt search failure at position (0.0026 0.0026 0.4502)
for requested cell 0
If this is a restart or reconstruction/decomposition etc. it is likely that the write
precision is not sufficient.
Either increase 'writePrecision' or set 'writeFormat' to 'binary'

From function void Foam::particle::initCellFacePt()
in file /home/user/OpenFOAM/OpenFOAM-2.3.x/src/lagrangian/basic/lnInclude/particleI.H at
line 758.

FOAM aborting
```

Listing 326: Error message issued by OpenFOAM when a Lagrangian simulation is started with particle positions defined outside of the domain; `checkMesh` reports for this case an *Overall domain bounding box (0 0 0) (0.15 0.15 0.45)*; Note the position (Line 3) at which the search failure occurs

47.8 Sub models

47.8.1 Injection models

There are a number of models to insert Lagrangian particles or parcels into the simulation domain.

Common controls inherited from base classes

The injection models have a number of base classes which determine common behaviour and provide common data. Common control parameters are the *start of injection* (SOI), and the mass to be injected (`massTotal`).

ManualInjection

The `manualInjection` model is probably the simplest model. The user needs to provide the to-be-injected particle mass and the injection positions. All parcels are introduced at SOI.

CellZoneInjection

The `cellZoneInjection` model works similar to the manual injection model. The locations at which parcels are injected, however, are determined using a user-provided `cellSet`. The actual injection locations are randomly distributed across the `cellSet`. The number of inserted parcels is determined by the volume of the `cellSet` and the user-specified target parcel number density. All parcels are introduced at once at SOI.

FieldActivatedInjection

The `fieldActivatedInjection` model is also related to the manual injection model. In addition to the user-provided injection locations, a scalar factor and the names of a threshold field and a referenceField have to be

specified. Parcels are injected only at locations at which the following relation holds:

$$\text{factor} * \text{referenceField}[celli] \geq \text{thresholdField}[celli] \quad (92)$$

Parcel injection is controlled by the injector positions read from the positions file. All positions, which fulfil the condition above are valid injector positions. Furthermore, the number of parcels per injector (`parcelsPerInjector`) has to be specified. Each injector injects `parcelsPerInjector` parcels which account for a `parcelsPerInjector`-th of `massTotal`. Parcels are injected from SOI onwards until `massTotal` is reached.

PatchInjection

The `patchInjection` model introduces parcels at a patch rather than within a volume like the models discussed above. This injection model implements a classical inflow condition for Lagrangian particles. The injection position on the patch is chosen randomly. Parcels are injected from SOI until `massTotal` is reached.

47.8.2 CloudFunctionObjects

`CloudFunctionObject` are, similar to the standard `functionObjects` for fields, function objects for Lagrangian clouds. The main purpose of OpenFOAM's cloud function objects – judging by the implemented ones at the time of writing – is post-processing. However, cloud function objects can also be used to actively influence the Lagrangian particles.

PatchPostProcessing

This cloud function object can be used to accumulate data from all particles leaving the domain through a specified patch. Thus, e.g. a residence time distribution (RTD) can be generated using this data.

FacePostProcessing

This cloud function object serves a similar purpose as the `PatchPostProcessing` cloud function object, only this one acts on face sets.

VoidFraction

This cloud function object can be used to create the volume fraction field associated with the particles. Thus, the name `VoidFraction` can be misleading.

If we take a look at the code, we clearly see that the volume fraction of the particles is computed. In Listing 327, we see the two methods of this cloud function object which are responsible for computing the result. The field `theta` is initialized to zero, this is not shown in the listing. In the method `postMove()`, which is called for each parcel after it has moved within the current timestep, the particle's volume is added to the field `theta`. In the method `postEvolve()`, which is called after evolving the Lagrangian cloud for the current time step has been completed, the field `theta` is divided by the mesh's volume, i.e. a field in which the value of a cell is that cell's volume.

Thus, as in each cell the volume of the particles is accumulated and subsequently divided by the volume of the cell, we end up with the volume fraction of the particles.

```

1 template<class CloudType> void Foam::VoidFraction<CloudType>::postMove
2 {
3     // ...
4 }
5 {
6     volScalarField& theta = thetaPtr_();
7     theta[celli] += dt*p.nParticle()*p.volume();
8 }
9
10 template<class CloudType> void Foam::VoidFraction<CloudType>::postEvolve()
11 {
12     volScalarField& theta = thetaPtr_();
13     const fvMesh& mesh = this->owner().mesh();
14     theta.primitiveFieldRef() /= mesh.time().deltaTValue()*mesh.V();
15     CloudFunctionObject<CloudType>::postEvolve();

```

Listing 327: Two methods of `VoidFraction.C`

ParticleCollector

The ParticleCollector cloud function object can be used to count particles traversing an arbitrary surface defined by a set of polygons or the area enclosed by concentric circles. The data accumulated by this cloud function object involves the accumulated particle mass and the mass flow rate passing through the surface.

Optionally, counted particles can be removed from the simulation.

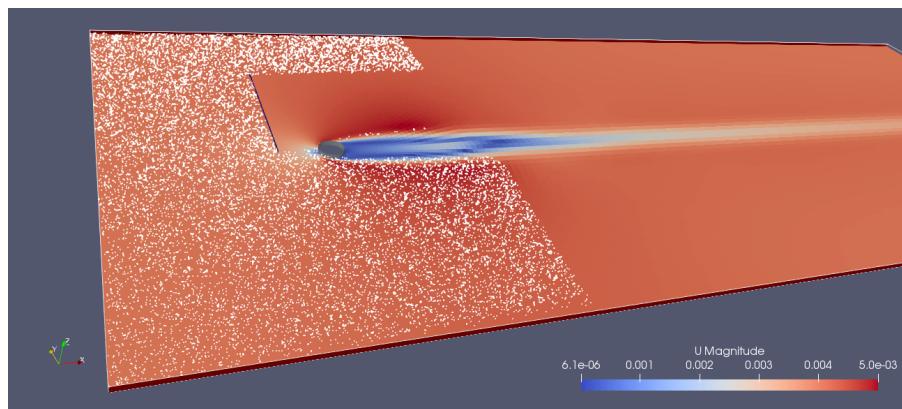


Figure 150: A set of polygons has been defined to count and remove traversing particles. In this case of a cylinder in laminar cross-flow, particles are inserted through the inlet patch. The ParticleCollector cloud function object was set to remove all counted particles, which is clearly visible in this snapshot.

48 Porosity

48.1 Overview

Porosity in simulation fluid flow can take many forms, from quite simplistic to elaborate.

48.2 porosityModels

The porosityModels compute a contribution to the momentum equation which should account for the additional pressure loss due to the porous region.

Note that these porosity models are used to model the effect of matter that is otherwise not present in the simulation. If we would fully include this matter into our simulation, we would end up with an two-phase Euler-Euler simulation featuring one static phase¹⁷².

48.2.1 fixedCoeff

In the header file of the *fixedCoeff* model, we can find the following definition of the model's contribution to the momentum equation. The additional resistance is split into a linear term, with α as the associated coefficient, and a quadratic term, with β as the corresponding coefficient. The physical units of those coefficients are 1/s respectively 1/m.

$$\mathbf{S} = -\rho_{\text{ref}} (\alpha + \beta \|\mathbf{U}\|) \mathbf{U} \quad (93)$$

48.2.2 powerLaw

The *powerLaw* model defines the contribution to the momentum equation as follows:

$$\mathbf{S} = -\rho_{\text{ref}} C_0 \|\mathbf{U}\|^{C_1-1} \mathbf{U} \quad (94)$$

48.2.3 DarcyForchheimer

The DarcyForchheimer model computes the resistance contribution of the porous region as follows:

$$\mathbf{S} = - \left(\mu D + \frac{\rho \|\mathbf{U}\|}{2} F \right) \mathbf{U} \quad (95)$$

The model coefficients D and F have the physical units of 1/m² respectively 1/m.

48.2.4 solidification

The solidification porosity model allows to compute a temperature dependent contribution to the momentum equation.

$$\mathbf{S} = -\alpha \rho D(T) \mathbf{U} \quad (96)$$

The drag coefficient $D(T)$ is a user-defined function of temperature. This allows the transition from no resistance when the fluid is liquid to a very high resistance when the fluid has solidified.

48.3 Porosity in single-phase simulations

One of the defining hallmark of a single phase simulation is the existence of only one single phase: the fluid. Hence, the phase that in reality constitutes the porous phase is by definition absent from the simulation. However, certain aspects of the porous phase can be accounted for using modelling.

¹⁷²A stationary phase model for reactingMultiphaseEulerFoam was released in 2018, which may serve to more accurately model the solid phase of a packed bed reactor. See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/e352828514abe029065d8032ec78516c980a7a2d>.

48.3.1 Pressure-loss

The presence of a porous zone or region in a flow will create an additional pressure loss. This can be accounted for by using a model of the `explicitPorositySource` family of models. See Section 48.2 for a discussion on these models.

One example of something that causes “only” pressure loss and requires no further modelling might be a mesh screen on an air intake which is intended to avoid the ingress of foreign objects.

48.3.2 Presence

Porous material not only causes an additional pressure drop, it also takes up space that would otherwise be available for the fluid. If we imagine a porous zone within a pipe fully occupying the cross-section, by virtue of mass conservation, the fluid must flow faster through the porous region than it does up- or downstream of it.

This is relevant if we want to compute the transport of species. If we neglect the volumetric effect of the solid material, we may underestimate the time it takes for the transported species to traverse the simulation domain.

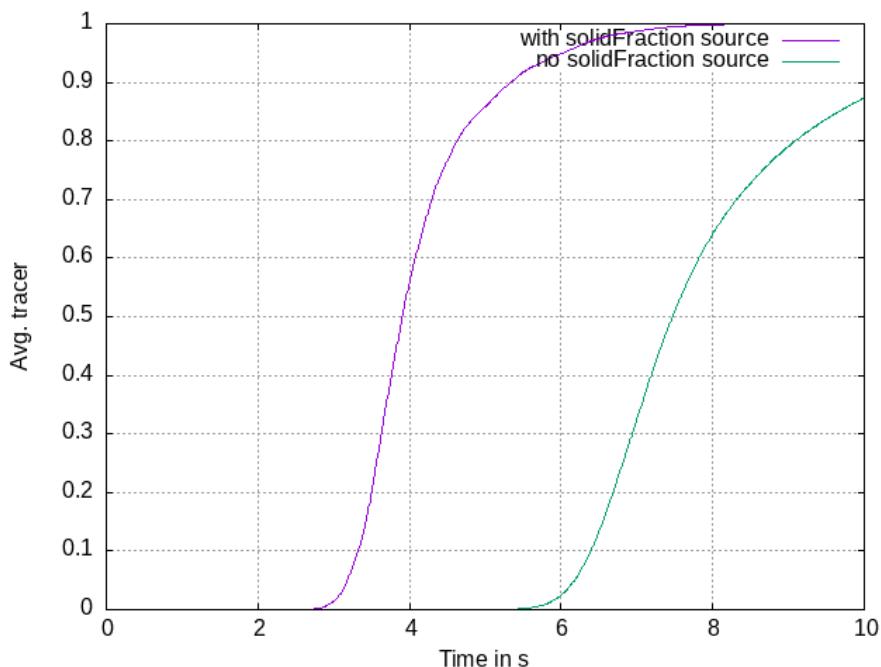


Figure 151: The average concentration of a passive tracer at the outlet. Accounting for the presence of a solid taking up a significant fraction of the volume, strongly affects the transport of a tracer. In both cases the mass flow was the same.

The `volumeFractionSource` model is used in the `fvModels` file to account for the presence of porous material in the fluid domain. The header file of this model summarizes this model’s intention and working principle as follows:

This fvModel adds transport terms into the equations to account for the presence of a constant volume fraction. The volume fraction is read from `constant/alpha.<volumePhase>`, where `<volumePhase>` is given as a parameter to the fvModel. Both advective and diffusive terms are added, and the resulting solution is time-accurate. The flux and velocity are treated as superficial.

This can be used to represent the effect of porous media that are caused purely by the reduction in volume of the fluid phase; i.e., additional blockage, and changes to transport and diffusion rates. It does not represent losses or transfers with the porous media. That requires separate sub-modelling.

48.3.3 Thermal inertia

A solid material present in a fluid flow not only causes pressure loss, it also might affect heat transfer. Here, we only have a very simplistic modelling choice: solidEquilibriumEnergySource.

This model assumes the solid porous matter to be in thermal equilibrium with the fluid. Hence, this model is only applicable if thermal inertia of the solid is not too large compared to the fluid. Otherwise, the heat transfer between fluid and os

Part V

Solver

49 Solution Algorithms

The solution of the Navier-Stokes equations require solving the coupled equations of velocity and pressure fields. There are several solution algorithms that try to decouple the equations and compute the velocity and pressure separately. In order to decouple the computation of velocity and pressure, a predictor-corrector strategy is followed. This approach is referred to in literature on numerical methods as *segregated solution*.

The alternative to solving for velocity and pressure in a segregated fashion is to solve for the fully coupled – also referred to as block coupled – equation system. In general, the momentum equation yields three equations for the three velocity components and the pressure equation, which is derived from the continuity equation, yields an equation for pressure. Instead of solving each of the four discretized equations individually, the fully coupled set of equations could also be solved for. This translates a possible improvement in converge rate, however, it also encompasses a much larger memory requirement and an altered convergence behaviour.

This section will deal with the segregated solution methods, as they are the most commonly used. In the last sub-section we will briefly discuss coupled methods.

49.1 SIMPLE

Figure 152 shows the flow chart of the SIMPLE algorithm. The SIMPLE algorithm predicts the velocity and then corrects both the pressure and the velocity. This is repeated until a convergence criteria is reached. The labels in Figure 152 are related to the terminology used in the source code of the `simpleFoam` solver. The solution procedure can be described as follows

1. Check if convergence is reached – `simple.loop()`
2. Predict the velocities using the momentum predictor– `UEqn.H`
3. Correct the pressure and the velocities– `pEqn.H`
4. Solve the transport equations for the turbulence model¹⁷³– `turbulence->correct()`
5. Go back to step 1

In OpenFOAM the SIMPLE algorithm is used for steady-state solvers.

49.1.1 Predictor

The predictor of `simpleFoam` is a momentum predictor.

```
1 // Momentum predictor
2 tmp<fvVectorMatrix> UEqn
3 (
4     fvm::div(phi, U)
5     + turbulence->divDevReff(U)
6     ==
7     sources(U)
8 );
9
10 UEqn().relax();
11
12 sources.constrain(UEqn());
13
14 solve(UEqn() == -fvc::grad(p));
```

Listing 328: Predictor in `UEqn.H` of `simpleFoam`

¹⁷³In case of a laminar simulation an empty function is called. Turbulence is modelled in OpenFOAM in a very generic way. Therefore, a laminar simulation uses the `laminar` turbulence model.

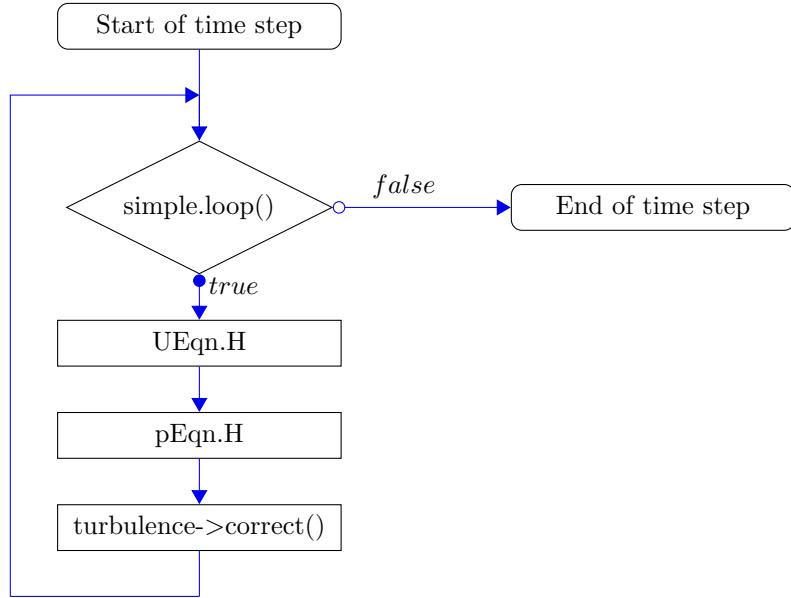


Figure 152: Flow chart of the SIMPLE algorithm

49.1.2 Corrector

The corrector is used to correct the pressure field by using the predicted velocity. This corrected pressure is used to correct the velocities by solving the continuity equation.

The non-orthogonal pressure corrector loop is necessary only for non-orthogonal meshes [52].

```

p.boundaryField().updateCoeffs();

volScalarField rAU(1.0/UEqn().A());
U = rAU*UEqn().H();
UEqn.clear();

phi = fvc::interpolate(U, "interpolate(HbyA)") & mesh.Sf();
adjustPhi(phi, U, p);

// Non-orthogonal pressure corrector loop
while (simple.correctNonOrthogonal())
{
    fvScalarMatrix pEqn
    (
        fvm::laplacian(rAU, p) == fvc::div(phi)
    );
    pEqn.setReference(pRefCell, pRefValue);

    pEqn.solve();

    if (simple.finalNonOrthogonalIter())
    {
        phi -= pEqn.flux();
    }
}

#include "continuityErrs.H"

// Explicitly relax pressure for momentum corrector
p.relax();

// Momentum corrector
U -= rAU*fvc::grad(p);
U.correctBoundaryConditions();
sources.correct(U);

```

Listing 329: Corrector in *pEqn.H* of *simpleFoam*

49.2 PISO

The PISO algorithm also follows the predictor-corrector strategy. Figure 153 shows the flow chart of the PISO algorithm. The velocity is predicted using the momentum predictor. Then, the pressure and the velocity is corrected until a predefined number of iterations is reached. Afterwards, the transport equations of the turbulence model are solved.

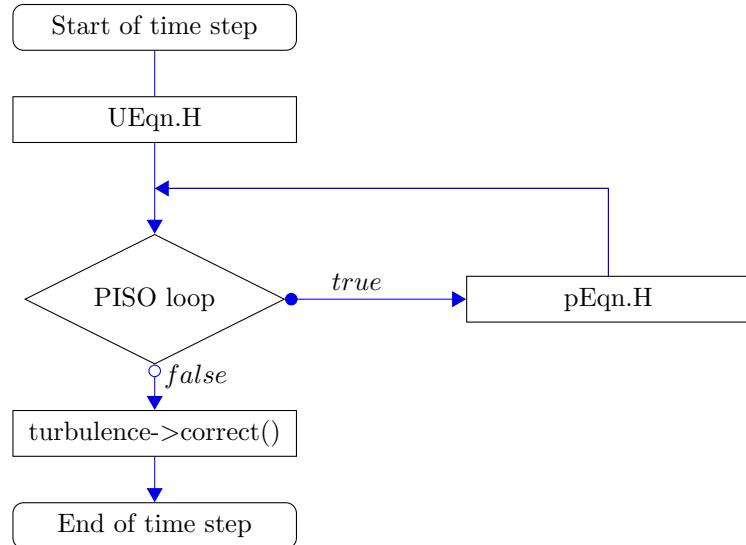


Figure 153: Flow chart of the PISO algorithm

49.3 PIMPLE

The PIMPLE algorithm, which is a combination of the SIMPLE and PISO algorithms, is discussed further in Sections 52 and 52.2.

49.4 Block-coupled solution

The block-coupled approach is something completely different than the aforementioned segregated algorithms. In block-coupled solutions all equations (three equations for velocity and one for pressure) are solved at the same time. This requires the construction of a fully coupled, discretised equation system for all four variables. Thus, block-coupled solvers have a much larger memory footprint than sequential solvers.

49.4.1 Block-coupled solvers

The foam-extend project <https://foam-extend.sourceforge.io/>, at the time of writing, distributes two solvers using the block-coupled solution approach.

blockCoupledScalarTransportFoam

This solver is derived from the standard *scalarTransportFoam* solver and solves the transport of two coupled passive scalars.

$$\nabla \cdot (\mathbf{u}T) + \nabla \cdot (D_T \nabla T) = \alpha (T_s - T) \quad (97)$$

$$\nabla \cdot (D_{Ts} \nabla T_s) = \alpha (T - T_s) \quad (98)$$

pUCoupledFoam

This solver is a steady state solver for incompressible, turbulent single phase flow. This solver solves for velocity and pressure simultaneously.

50 Solver modelling

This section covers topics which are common to the discussed solvers, yet details of these topics vary from solver to solver.

50.1 Flux field `phi`

Both incompressible and compressible solvers use a flux field named `phi`. This is a face flux which is defined at the cell faces. In the case of an incompressible solver, it is computed by the inner product of the flow velocity (interpolated to the face centres) and the face normal vector. The dimension of `phi` is cubic metres per second.

In the case of a compressible solver, `phi` is computed using the product of density and flow velocity as the first operand of the inner vector product. The code in Listing 330 clearly reflects this definition. The dimension of `phi` in compressible solver is consequently kilograms per second.

```
1 surfaceScalarField phi
2 (
3     IOobject
4     (
5         "phi",
6         runTime.name(),
7         mesh,
8         IOobject::READ_IF_PRESENT,
9         IOobject::AUTO_WRITE
10    ),
11    linearInterpolate(rho*U) & mesh.Sf()
12 );
```

Listing 330: Computing the compressible face-flux field `phi` in the file `compressibleCreatePhi.H` from OpenFOAM's source code.

50.1.1 Computing mass flows in post-processing

Thus, if we want to compute mass flows in (run-time) post-processing, we need to take of the fact whether we are running an incompressible or a compressible solver in the proper definition of the corresponding function-object.

In both cases, we simply need to sum up `phi` over a patch or a face zone. However, in the case of an incompressible solver we need to specify a weight field or a scale factor to account for the fluid density. Otherwise, our function-object would compute the volumetric flow rate rather than the mass flow rate.

50.2 Pressure

50.2.1 Compressibility

Most, if not all, solvers of OpenFOAM use a pressure field on some form. One key difference of how the pressure field is used is whether one is using an incompressible or a compressible solver. In the case of an incompressible solver, the pressure is a pressure divided by density, which is reflected in the physical unit the pressure field uses in incompressible cases¹⁷⁴. This is also discussed in Section 9.4.

50.2.2 Hydrostatics

Another variation in the use of the pressure field are solvers that account for hydrostatic pressure. These solvers, e.g. multiphase solvers, often use two pressure fields: the static pressure `p` and a modified pressure `p_rgh`.

$$p_{rgh} = p - \rho(\mathbf{g} \cdot \mathbf{h}) \quad (99)$$

¹⁷⁴The “official” book on OpenFOAM refers to this modified pressure as *kinematic pressure*, see <https://doc.cfd.direct/notes/cfd-general-principles/pressure>.

The governing equations of various solvers are reformulated to contain `p_rgh` rather than `p`, which benefits the numerical solution. There is little official documentation on this approach¹⁷⁵, however, in one comment in OpenFOAM's bug tracker¹⁷⁶, Henry Weller states:

I derived and implemented the `p_rgh` formulation to avoid numerical issues associated with the interaction of large gradients of the buoyancy force with mesh irregularity.

In the case when a solver uses both pressure fields, one of them, generally `p_rgh`, gets specific boundary conditions, whereas the other one features only `calculated` boundary conditions. Otherwise, one might violate Eq. (99) at the boundary.

¹⁷⁵The documentation of OpenCFD discusses this topic a little, see <https://www.openfoam.com/documentation/guides/latest/doc/guide-applications-solvers-variable-transform-p-rgh.html>.

¹⁷⁶See <https://bugs.openfoam.org/view.php?id=1170>

51 Solver modules

With the release of OpenFOAM-11, modular solvers were introduced¹⁷⁷. These solver modules replace the traditional solvers, and they are aimed to make maintaining OpenFOAM easier for the developers of OpenFOAM. Since the first release of OpenFOAM, a solver was its own program/executable. Other models concerning fluid flow, e.g., turbulence, has been relegated to shared libraries. This reduced code duplication, since not every incompressible single-phase solver needed to implement its own turbulence model. Instead, it was used via the library. Note, that certain exceptions to this general statement existed over the course of OpenFOAM development, e.g., some multiphase solvers did indeed implement their own special formulation of the turbulence model. Over the years, however, this was being eliminated.

Modular solvers follow a similar approach. Instead of every solver implementing more or less the same equations, there is now a common solver module. Thus, solvers themselves are now libraries instead of executables. One example mentioned by the developers highlighting the advantage of this new development, is that the same fluid flow solver module can now be used for pure flow cases as well as the fluid flow portion of a conjugate heat transfer (CHT) problem. This strongly reduces the number of solvers in OpenFOAM and greatly improves the maintainability of OpenFOAM.

Like other big revisions of OpenFOAM's source code with the aim to improve maintainability, this revision has led to a more generalized code, which simplifies the code base from a software development perspective. However, the beginner might find the revision to have led to less readily readable code. With solvers being distinct applications, we can find the most top-level code in one place. With the solver modules, however, this code is hidden in the class hierarchy of the solver modules.

51.1 General use

With the classical solvers being transferred into libraries, we now call the executable `foamRun` when we want to conduct a simulation. The choice of solver is now relegated to a setting in `controlDict`. Listing 331 shows how this is done. There is a new keyword: `solver`, which takes the name of the solver module, which is to be used.

```
application      foamRun;
solver          fluid;
```

Listing 331: Selecting the appropriate solver module in `controlDict`.

The example shown in Listing 331 is analogous to calling `rhoPimpleFoam`¹⁷⁸ from the command line and/or using `rhoPimpleFoam` as the value for the `application` keyword.

51.1.1 `foamRun` - one application to run them all

Now, that individual solvers are libraries, we have only one application to call: `foamRun`. Since all solvers in OpenFOAM were constructed in a similar fashion, it seems, in hindsight, somewhat inevitable that this commonality got abstracted away. Thus, code duplication was reduced in the source code of OpenFOAM. As an exercise to the reader, we suggest comparing the source code of similar solvers from a pre-modules version of OpenFOAM, e.g., compare the top-level source code of `pisoFoam` and `pimpleFoam`. Similarities will be obvious, similarities which in a programming oriented frame can be regarded as code duplication. Another such exercise, would be to compare a solver which has a variant with and without mesh motion, e.g., `pimpleFoam` and `pimpleDyMFoam` in some older release.

Listing 332 shows the run-time loop of the `foamRun` application. This shows the basic structure most, if not all, solvers in OpenFOAM followed. Here, `foamRun` defines the structure and calls the appropriate methods of the solver module in their respective order.

```
1 Info << nl << "Starting time loop\n" << endl;
2
3 while (pimple.run(runTime))
4 {
5     // Update PIMPLE outer-loop parameters if changed
6     pimple.read();
```

¹⁷⁷See <https://openfoam.org/release/11/> and <https://cfd.direct/openfoam/free-software/modular-solvers/>.

¹⁷⁸Or one of the other solvers superseded by the fluid solver module.

```

7     solver.preSolve();
8
9
10    // Adjust the time-step according to the solver maxDeltaT
11    adjustDeltaT(runTime, solver);
12
13    runTime++;
14
15    Info<< "Time = " << runTime.userTimeName() << nl << endl;
16
17    // PIMPLE corrector loop
18    while (pimple.loop())
19    {
20        solver.moveMesh();
21        solver.motionCorrector();
22        solver fvModels().correct();
23        solver.prePredictor();
24        solver.momentumPredictor();
25        solver.thermophysicalPredictor();
26        solver.pressureCorrector();
27        solver.postCorrector();
28    }
29
30    solver.postSolve();
31
32    runTime.write();
33
34    Info<< "ExecutionTime = " << runTime.elapsedCpuTime() << " s"
35    << " ClockTime = " << runTime.elapsedClockTime() << " s"
36    << nl << endl;
37
38
39    Info<< "End\n" << endl;
40
41    return 0;

```

Listing 332: The main part of the source code of `foamRun`: the run-time loop.

51.2 Class hierarchy

Figure 154 shows some part of the class hierarchy of the solver modules. We see, that all modules derive from the abstract base class `solver`, which in turn is derived from `regIOobject` (not shown).

From `solver`, the classes `fluidSolver` and `solid` are derived. The `solid` solver module is the module responsible for solving the energy transport in the solid regions of conjugate heat transfer (CHT) cases. Hence, this module has references to a solid thermophysical model and a reference to the temperature field.

`fluidSolver` is described in the header file as the class which provides Courant number time-step control. From `fluidSolver`, the first concrete solver modules are derived, e.g.: `incompressibleFluid`. This module is described in the header file as follows:

Solver module for steady or transient turbulent flow of incompressible isothermal fluids with optional mesh motion and change.

Uses the flexible PIMPLE (PISO-SIMPLE) solution for time-resolved and pseudo-transient and steady simulations.

Optional fvModels and fvConstraints are provided to enhance the simulation in many ways including adding various sources, constraining or limiting the solution.

Another concrete module derived from `fluidSolver` is `isothermalFluid`, which in turn acts as the base class for the compressible solver modules `fluid` and `multicomponentFluid`.

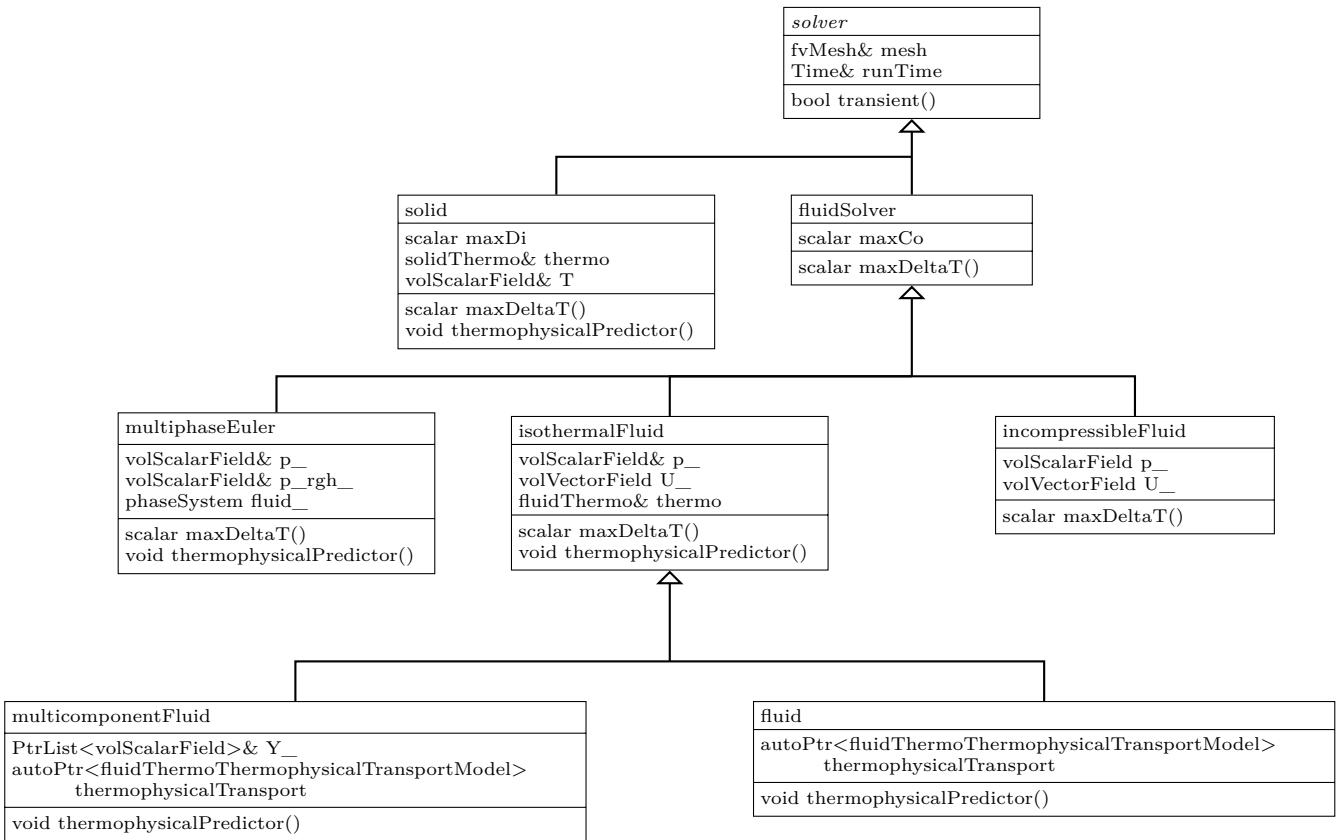


Figure 154: A selected part of the class hierarchy of the solver modules.

Figure 154 is relatively sparse on the data members and methods of the shown classes. The figure also contains only a selection of classes for the sake of brevity.

We see that the **solver** module provides references to the basic classes **fvMesh** and **Time**. It also implements the distinction between a steady and transient solution.

The **fluidSolver** module has data members and methods relating to Courant number based time step control, which is common to all transient solvers. Hence, this is located high in the class hierarchy's inheritance tree.

The first concrete modules **incompressibleFluid** and **isothermalFluid** have flow related data members such as the pressure and velocity fields among others. One noticeable difference between **incompressibleFluid** and **isothermalFluid** is that the former holds the pressure field itself, while the latter holds a reference to the pressure field. This is because in the case of the **isothermalFluid** module, the pressure field is provided by the **fluidThermo** model. Hence, a reference is sufficient. In the case of the **incompressibleFluid** module, there is no **fluidThermo** model, thus it needs to hold the pressure field itself. Note, that **incompressibleFluid** also implements a **thermophysicalPredictor()** method (not shown), which is a trivial empty method. This is because with incompressible fluids there is no thermo-physics going on.

The two modules **fluid** and **multicomponentFluid** both feature a pointer to a **thermophysicalTransport** model as well as a **thermophysicalPredictor()** method. These are a result of dropping the assumption of the fluid being isothermal.

The **multicomponentFluid** module, has a pointer list for species volume fraction fields, since **multicomponentFluid** adds the functionality of multicomponent fluids with optional chemical reactions.

From this brief discussion of the inheritance relations and some of the classes, we see that the further down the inheritance tree we go, the more complex the solver modules are. Common functionality can be found higher up the inheritance tree, where it might be shared between multiple modules.

51.3 Case study: incompressible flow

The simplest useful solvers of OpenFOAM are those for incompressible flow: **simpleFoam** for steady-state simulations as well as **pisoFoam** and **pimpleFoam** for transient simulations. These three solvers are superseded

by the *incompressibleFluid* solver module.

51.3.1 Steady-state or transient

The distinction between solving for a steady state or a transient solution is now relegated to the selection of the temporal discretisation in the file **fvSchemes**. There, selecting `steadyState` is akin to calling `simpleFoam`, whereas selecting a transient scheme is akin to calling `pisoFoam` or `pimpleFoam`.

```
1 ddtSchemes
2 {
3     default      Euler; // or any other transient scheme if we used pisoFoam or pimpleFoam
4     default      steadyState; // if we used simpleFoam in earlier versions
5 }
```

Listing 333: Selecting the appropriate solver module in **controlDict**.

51.3.2 SIMPLE, PISO or PIMPLE

The formulation of the PIMPLE algorithm is such, that it is a combination of the PISO and SIMPLE algorithm¹⁷⁹. Hence, we can view the SIMPLE and the PISO algorithms as special cases of a general PIMPLE algorithm. Thus, SIMPLE and PISO can be obtained by selecting appropriate parameters in the control dictionary of PIMPLE.

If we compare the source code of `pisoFoam` and `pimpleFoam`, we will find remarkable similarity which sometimes almost borders on duplication. Hence, in hindsight, consolidation of solvers into overarching solvers and then into solver modules seems a quite natural development.

Thus, the choice between using the SIMPLE, PISO or PIMPLE algorithm is reduced to making an appropriate selection in the relevant dictionaries. This is even alluded to by the solver itself. If we run a simulation using the PIMPLE algorithm with only one iteration for the outer correction loop, then we will see an info-message like the following:

```
PIMPLE: Operating solver in transient mode with 1 outer corrector
PIMPLE: Operating solver in PISO mode
```

Hence, we are safe to assume, that with OpenFOAM, PISO is a special case of PIMPLE.

SIMPLE vs. PISO/PIMPLE

Looking through the tutorials of OpenFOAM-12, the author has made an observation. Steady-state cases have a SIMPLE dictionary in **fvSolution** for solution control, whereas transient cases have a PIMPLE dictionary in **fvSolution**.

Listing 334 shows two commands and the resulting output. First, we use `find` to find all **fvSchemes** files, which we in turn pass on to `grep` to look for the temporal discretisation, which we inspect for the word `steadyState`. Note, that this is done only for the tutorial cases of the *incompressibleFluid* module.

The second command is a similar search for the word SIMPLE in all **fvSolution** files. This is, again, done via the use of `find` and `grep`. Note, that the results for both commands are the same cases. Hence, we confirm the earlier statement that steady-state cases have a SIMPLE dictionary for solution control.

```
user@host:~/OpenFOAM/OpenFOAM-12/tutorials/incompressibleFluid$ find . -name fvSchemes | xargs
    grep ddtSchemes -A2 | grep steadyState
./pipeCyclic/system/fvSchemes-    default      steadyState;
./mixerVessel2DMRF/system/fvSchemes-  default      steadyState;
./ductSecondaryFlow/system/fvSchemes- default      steadyState;
./drivaerFastback/system/fvSchemes- // For transient, replace steadyState, e.g. with Euler
./pitzDailySteady/system/fvSchemes-  default      steadyState;
./motorBike/motorBike/system/fvSchemes- default      steadyState;
./mixerSRF/system/fvSchemes-    default      steadyState;
./T3A/system/fvSchemes-    default      steadyState;
./windAroundBuildings/system/fvSchemes- default      steadyState;
```

¹⁷⁹See https://www.tfd.chalmers.se/~hani/kurser/OS_CFD_2022/lectureNotes/PIMPLE.pdf

```

./airFoil2D/system/fvSchemes- default steadyState;
./turbineSiting/system/fvSchemes- default steadyState;
./motorBikeSteady/system/fvSchemes- default steadyState;
./rotorDisk/system/fvSchemes- default steadyState;
./wingMotion/wingMotion2D_steady/system/fvSchemes- default steadyState;
./roomResidenceTime/system/fvSchemes- default steadyState;
./pitzDailySteadyExperimentalInlet/system/fvSchemes- default steadyState;
user@host:~/OpenFOAM/OpenFOAM-12/tutorials/incompressibleFluid$ find . -name fvSolution |
  xargs grep SIMPLE
./pipeCyclic/system/fvSolution:SIMPLE
./mixerVessel2DMRFLystem/fvSolution:SIMPLE
./ductSecondaryFlow/system/fvSolution:SIMPLE
./drivaerFastback/system/fvSolution:SIMPLE
./pitzDailySteady/system/fvSolution:SIMPLE
./motorBike/motorBike/system/fvSolution:SIMPLE
./T3A/system/fvSolution:SIMPLE
./windAroundBuildings/system/fvSolution:SIMPLE
./airFoil2D/system/fvSolution:SIMPLE
./turbineSiting/system/fvSolution:SIMPLE
./motorBikeSteady/system/fvSolution:SIMPLE
./rotorDisk/system/fvSolution:SIMPLE
./wingMotion/wingMotion2D_steady/system/fvSolution:SIMPLE
./roomResidenceTime/system/fvSolution:SIMPLE
./pitzDailySteadyExperimentalInlet/system/fvSolution:SIMPLE

```

Listing 334: Inspecting the incompressible tutorial cases: checking for steady-state cases and the presence of a SIMPLE dictionary.

51.3.3 Case study: *pitzDaily*

If one has multiple versions of OpenFOAM present on one's system, we can study the differences between certain tutorial cases. Figure 155 shows the only difference in the *pitzDaily* tutorial case directly attributable to the introduction of the solver modules: the **solver** keyword, which was already discussed and shown in Listing 331.

All other differences between the files of the *pitzDaily* tutorial case between OpenFOAM-6 and OpenFOAM-12 are due to other changes over time: first and foremost, the version number in the file header. We see in Figure 155 that the data file header, i.e., the bit following the **FoamFile** descriptor has lost its I/O format version number¹⁸⁰. Furthermore, the banner at the top of each file contains the respective OpenFOAM version number.

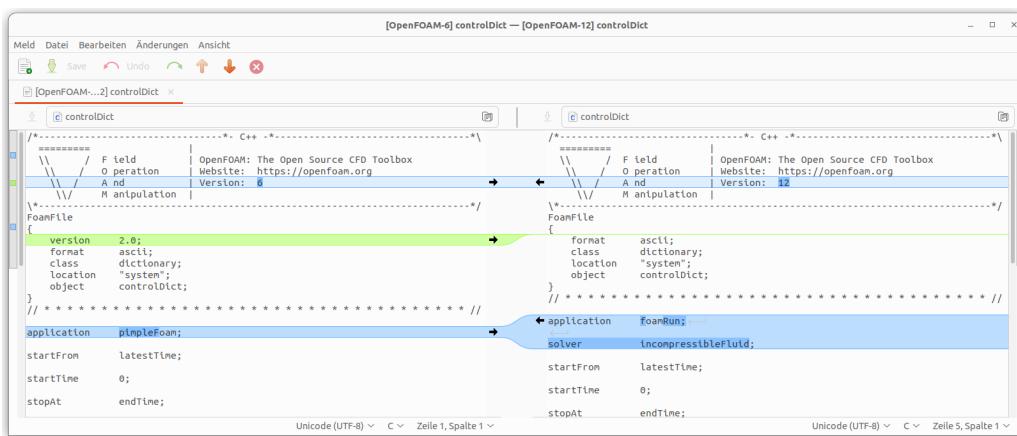


Figure 155: The differences of **controlDict** of the *pitzDaily* tutorial from OpenFOAM-6 and OpenFOAM-12.

Thus, from the user perspective, only very little has changed due to the introduction of the solver modules. We now simply call a different executable and we have an additional setting in **controlDict**: the **solver** keyword-value pair.

¹⁸⁰This version number was made optional with the development of OpenFOAM-9, i.e., OpenFOAM-9 is the first point release for which this version number is optional. See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/01494463d068d66ab94efc4984a1148f2b4652cb>.

52 pimpleFoam

pimpleFoam is a transient incompressible solver using the PIMPLE algorithm, which is a combination of PISO and SIMPLE. The solver is described in the file `pimpleFoam.C` as follows:

```
Large time-step transient solver for incompressible, flow using the PIMPLE
(merged PISO-SIMPLE) algorithm.
```

Turbulence modelling is generic, i.e. laminar, RAS or LES may be selected.

52.1 Governing equations

52.1.1 Continuity equation

The general continuity equation reads as follows:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad (100)$$

we now assume incompressible fluids: $\rho = \text{const}$

$$\nabla \cdot \mathbf{u} = 0 \quad (101)$$

or in alternative notation

$$\text{div}(\mathbf{u}) = 0 \quad (102)$$

$$\frac{\partial u_i}{\partial x_i} = 0 \quad (103)$$

52.1.2 Momentum equation

Departing from the Navier-Stokes equations, the momentum equation of *pimpleFoam* are derived.

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \nabla(\rho \mathbf{u} \mathbf{u}) + \nabla \cdot \tau = -\nabla p + \mathbf{g} \quad (104)$$

because we assume a constant density we can divide by ρ

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u} \mathbf{u}) + \frac{1}{\rho} \nabla \cdot \tau = -\frac{\nabla p}{\rho} + \frac{\mathbf{g}}{\rho} \quad (105)$$

The last term is defined a general source term

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u} \mathbf{u}) + \frac{1}{\rho} \nabla \cdot \tau = -\frac{\nabla p}{\rho} + \mathbf{Q} \quad (106)$$

the shear stresses and the pressure are denoted by new symbols: $\frac{\tau}{\rho} = \mathbf{R}^{eff}$ und $\frac{p}{\rho} = p$

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u} \mathbf{u}) + \nabla \cdot \mathbf{R}^{eff} = -\nabla p + \mathbf{Q} \quad (107)$$

The Boussinesq hypothesis allows us to add the Reynolds stresses to the shear stresses. This stress tensor – containing shear as well as Reynolds stresses – is denoted \mathbf{R}^{eff} , the effective stress tensor. Both RAS as well as LES turbulence models are based on the Boussinesq hypothesis.

$$\mathbf{R}^{eff} = -\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) \quad (108)$$

$$R_{ij}^{eff} = -\nu^{eff} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \quad (109)$$

The trace of τ fulfills the continuity equation for incompressible fluids

$$\text{tr}(\mathbf{R}^{eff}) = R_{ii}^{eff} = -2\nu^{eff} \left(\frac{\partial u_i}{\partial x_i} \right) = 0 \quad (110)$$

$$\frac{\partial u_i}{\partial x_i} = \nabla \cdot \mathbf{u} = 0 \quad (111)$$

Therefore, we can replace \mathbf{R}^{eff} with the deviatoric part of \mathbf{R}^{eff}

$$\mathbf{R}^{eff} = \underbrace{\text{dev}(\mathbf{R}^{eff})}_{\text{deviatoric part}} + \underbrace{\frac{1}{3} \text{tr}(\mathbf{R}^{eff}) \mathbf{I}}_{\text{hydrostatic part}} \quad (112)$$

$$\text{dev}(\mathbf{R}^{eff}) = \mathbf{R}^{eff} - \frac{1}{3} \underbrace{\text{tr}(\mathbf{R}^{eff}) \mathbf{I}}_{=0} \quad (113)$$

Therefore, the momentum equation can be rewritten

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \underbrace{\nabla \cdot (\text{dev}(\mathbf{R}^{eff}))}_{=\text{div}(\text{dev}(\mathbf{R}^{eff}))} = -\nabla p + \mathbf{Q} \quad (114)$$

Finally, we use Eq. (108)

$$\mathbf{R}^{eff} = -\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) \quad (108)$$

to gain

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \nabla \cdot (\text{dev}(-\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T))) = -\nabla p + \mathbf{Q} \quad (115)$$

52.1.3 Implementation

The momentum equation is implemented in the file `UEqn.H`. The first two terms of Eq. (115) can easily be identified in the source code in Listing 335.

The first term is the local derivative of the momentum – due to the incompressibility of the fluid, the density was eliminated – can be found in line 5 of Listing 335. Here, the instruction in the source code reads very much the same as the mathematical notation.

$$\frac{\partial \mathbf{u}}{\partial t} \quad \Leftrightarrow \quad \text{fvm}::ddt(U)$$

The second term of Eq. (115) is the convective transport of momentum. The use of the identifier `phi` should not lead to confusion. In order to read the equations from the source code, `phi` can be replaced with `U` without changing the meaning of the equations. The reason why `phi` is used in the source code lies in the solution procedure. See Section 75 for a detailed discussion about `phi`.

$$\underbrace{\nabla(\mathbf{u}\mathbf{u})}_{\text{div}(\mathbf{u}\mathbf{u})} \quad \Leftrightarrow \quad \text{fvm}::div(phi, U)$$

The third term of Eq. (115) is the diffusive momentum transport term. Diffusive momentum transport is caused by the laminar viscosity as well as turbulence. Therefore, the turbulence model handles this term. See line 7 of Listing 335.

$$\underbrace{\nabla \cdot (\text{dev}(\mathbf{R}^{eff}))}_{=\text{div}(\text{dev}(\mathbf{R}^{eff}))} \quad \Leftrightarrow \quad \text{turbulence->divDevReff}(U)$$

The terms on the *rhs* of Eq. (115) are the pressure gradient and the source term.

$$\begin{aligned} \underbrace{-\nabla p}_{=-\text{grad } p} &\Leftrightarrow -\text{fvc::grad}(p) \\ \mathbf{Q} &\Leftrightarrow \text{sources}(\mathbf{U}) \end{aligned}$$

```

1 // Solve the Momentum equation
2
3 tmp<fvVectorMatrix> UEqn
4 (
5   fvm::ddt(U)
6   + fvm::div(phi, U)
7   + turbulence->divDevReff(U)
8 );
9
10 UEqn().relax();
11
12 sources.constrain(UEqn());
13
14 volScalarField rAU(1.0/UEqn().A());
15
16 if (pimple.momentumPredictor())
17 {
18   solve(UEqn() == -fvc::grad(p) + sources(U));
19 }
```

Listing 335: The file *UEqn.H* of *pimpleFoam*

52.2 The PIMPLE Algorithm – or, what's under the hood?

This Section deals with the way *pimpleFoam* and *twoPhaseEulerFoam*, which also uses the PIMPLE algorithm, work. Therefore, we examine the implementation of *pimpleFoam*. Listing 336 shows the main loop of *pimpleFoam*.

The first instruction is the loop over all time steps. Then there are some operations – the three `#include` instructions – concerning time step control. After incrementing the time step (Line 7), the PIMPLE loop comes (from Line 10 onwards).

Inside this loop, first the momentum equation is solved (Line 12), then the pressure correction loop is entered (Line 17).

At the end of the PIMPLE loop the turbulent equations¹⁸¹ – if there are any present¹⁸² – are solved (Line 22). At the end of each time step the data is written.

```

1 while (runTime.run())
2 {
3   #include "readTimeControls.H"
4   #include "CourantNo.H"
5   #include "setDeltaT.H"
6
7   runTime++;
8
9   // --- Pressure-velocity PIMPLE corrector loop
10  while (pimple.loop())
11  {
12    #include "UEqn.H"
13
14    // --- Pressure corrector loop
15    while (pimple.correct())
16    {
17      #include "pEqn.H"
18    }
19 }
```

¹⁸¹In case of a $k-\epsilon$ model, there are two transport equations to be solved. Other turbulence models require the solution of less or none transport equation.

¹⁸²In case of a laminar simulation, no operation is carried out.

```

20   if (pimple.turbCorr())
21   {
22     turbulence->correct();
23   }
24 }
25
26 runTime.write();
27 }
```

Listing 336: The main loop of *pimpleFoam*

Figure 156 shows the flow chart of the PIMPLE algorithm. This algorithm is executed every time step. If the PIMPLE loop is entered only once, then the algorithm is essentially the same as the PISO algorithm. Listing 343 draws this conclusion from the code itself.

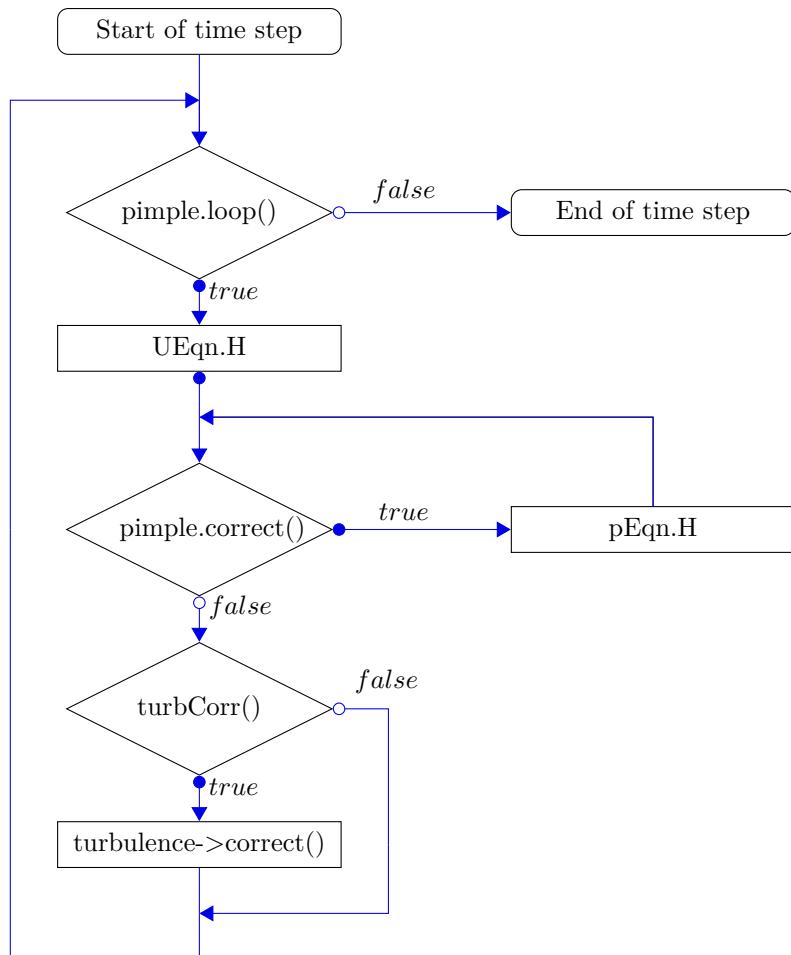


Figure 156: Flow chart of the PIMPLE algorithm

52.2.1 `readTimeControls.H`

In line 3 of Listing 336 the file `readTimeControls.H` is included to the source code using the `#include` preprocessor macro. This is a very common way to give the code of OpenFOAM structure and order. Code which is used repeatedly is outsourced into a separate file. This file is then included with the `#include` macro. Thus, code duplication is prevented. The file `readTimeControls.H` might be included into every solver that is able to use variable time steps. If this code was not outsourced into a separate file, this code would be found in every variable time step solver. Maintaining this code, would be tiresome and prone to errors.

Listing 500 shows the contents of `readTimeControls.H`. The first instruction reads from `controlDict` the `adjustTimeStep` parameter. If there is no entry matching the name of the parameter ("`adjustTimeStep`"), then

```

1 const bool adjustTimeStep =
2   runTime.controlDict().lookupOrDefault("adjustTimeStep", false);
3 scalar maxCo =
4   runTime.controlDict().lookupOrDefault<scalar>("maxCo", 1.0);
5 scalar maxDeltaT =
6   runTime.controlDict().lookupOrDefault<scalar>("maxDeltaT", GREAT);

```

Listing 337: The content of `readTimeControls.H`

a default value is used. So, omitting the parameter `adjustTimeStep` in `controlDict` will result in a simulation with a fixed time step.

This is a very straight forward example of determining the behaviour of a solver using only the source code. In this case the names of the source file as well as variable and function names are rather self explaining. In other cases one has to dig deeply into the code to learn about what a certain command does.

52.2.2 pimpleControl

Examining the files `pimpleControl.H` and `pimpleControl.C` will generate some knowledge of the inner life of `pimpleFoam`.

Solution controls

Listings 338 and 339 show parts of `pimpleControl.H` and `pimpleControl.C`. Listing 338 shows the declaration of protected¹⁸³ data in `pimpleControl.H`.

```

1 // Protected data
2   // Solution controls
3     // Maximum number of PIMPLE correctors
4     label nCorrPIMPLE_;
5
6     // Maximum number of PISO correctors
7     label nCorrPISO_;
8
9     // Current PISO corrector
10    label corrPISO_;
11
12    // Flag to indicate whether to only solve turbulence on final iter
13    bool turbOnFinalIterOnly_;
14
15    // Converged flag
16    bool converged_;

```

Listing 338: Protected data in `pimpleControl.H`

```

1 void Foam::pimpleControl::read()
2 {
3   solutionControl::read(false);
4
5   // Read solution controls
6   const dictionary& pimpleDict = dict();
7
8   nCorrPIMPLE_ = pimpleDict.lookupOrDefault<label>("nOuterCorrectors", 1);
9
10  nCorrPISO_ = pimpleDict.lookupOrDefault<label>("nCorrectors", 1);
11
12  turbOnFinalIterOnly_ = pimpleDict.lookupOrDefault<Switch>("turbOnFinalIterOnly", true);
13 }

```

Listing 339: Read solution controls in `pimpleControl.C`

¹⁸³Most programming languages provide *access specifiers* to specify the visibility of variables. The keyword `protected` means, that the variables can be accessed only inside the class `pimpleControl` and all classes inherited from `pimpleControl`.

Reading the code we can see which keyword in the PIMPLE dictionary – it is a part of the `fvSolution` dictionary (see Section 11.5) – is connected to which variable in the code. Three of the protected variables of Listing 338 are assigned in Listing 339. One of them has the same name in both the code and the dictionary. The other two have different names.

Pitfall: no sanity checks

The two variables `nCorrPimple` and `nCorrPiso` control the solution algorithm. If the corresponding entry in the PIMPLE dictionary in `fvSolution` is missing, then default values are used, see Section 68.3 for details behind the method `lookupOrDefault()`. However, the user can provide any number in `fvSolution` as long as it is legal¹⁸⁴. Thus, a zero or negative number is a legal entry from the source codes point of view. With respect to the solution algorithm a zero or negative entry makes no sense at all.

The connection between keywords and the algorithm

The keyword `nOuterCorrectors` translates – with the help of Listing 339 to the variable `nCorrPIMPLE_`. This variable controls how often the PIMPLE loop is traversed. Listing 340 shows parts of the definition of the function `loop()` of the class `pimpleControl`. The return value of this function decides whether the PIMPLE loop is entered or not. In line 5 of Listing 340 an internal counter is incremented – the `++` operator of C++ adds 1 to the variable the operator is applied to. Afterwards, the internal counter is compared to the value of `nCorrPIMPLE_`. If this internal counter is then equal to the sum of `nCorrPIMPLE_ + 1`, then the function `loop()` returns `false`.

The internal counter is initialised to the value of 0. Listing 341 shows the constructor of the class `solutionControl`. The class `pimpleControl` is derived from `solutionControl`. So, every instance of `pimpleControl` has an internal counter `corr_` inherited from `solutionControl`. Line 9 of Listing 341 shows how the counter `corr_` is initialised to zero.

```

1  bool Foam::pimpleControl::loop()
2  {
3      read();
4
5      corr_++;
6
7      /* code removed for the sake of brevity */
8
9      if (corr_ == nCorrPIMPLE_ + 1)
10     {
11         if ((!residualControl_.empty()) && (nCorrPIMPLE_ != 1))
12         {
13             Info<< algorithmName_ << ": not converged within "
14                 << nCorrPIMPLE_ << " iterations" << endl;
15         }
16
17         corr_ = 0;
18         mesh_.data::remove("finalIteration");
19         return false;
20     }
21
22     /* code continues */

```

Listing 340: Some content of `pimpleControl.C`

```

1  Foam::solutionControl::solutionControl(fvMesh& mesh, const word& algorithmName)
2  :
3  mesh_(mesh),
4  residualControl_(),
5  algorithmName_(algorithmName),
6  nNonOrthCorr_(0),
7  momentumPredictor_(true),
8  transonic_(false),
9  corr_(0),
10 corrNonOrtho_(0)
11 {}

```

¹⁸⁴See Section 68.4.2 for details on the `label` datatype.

Listing 341: The constructor of the class `solutionControl` in `solutionControl.C`

The keyword `nCorrectors` translates – with the help of Listing 339 to the variable `nCorrPISO_`. This variable controls how often the PISO loop – or the corrector loop – is traversed. Listing 338 shows, that there are two variables related to the PISO loop, `nCorrPISO_` and `corrPISO_`. The first variable is the limit and the second is the counter.

`nCorrPISO_` is read from the `fvSolution` dictionary by the use of the `nCorrectors` keyword. This number tells the solver, how many times the corrector loop should be traversed. The corrector loop is a feature of the PISO algorithm. Hence, the maximum number of corrector loop iterations is called `nCorrPISO_`.

The variable `corrPISO_` is declared in the constructor of the class `pimpleControl`, see Listing 343. There the variable is initialised to zero.

Listing 342 shows the definition of the function `correct()` of the class `pimpleControl`. The return value of this function controls if the corrector loop is entered. In line 3 the counter `corrPISO_` is incremented every time this function is called. In line 10 the value of the counter is compared to the maximum number of corrector loop iterations.

```
1 inline bool Foam::pimpleControl::correct()
2 {
3     corrPISO_++;
4
5     if (debug)
6     {
7         Info<< algorithmName_ << " correct: corrPISO = " << corrPISO_ << endl;
8     }
9
10    if (corrPISO_ <= nCorrPISO_)
11    {
12        return true;
13    }
14    else
15    {
16        corrPISO_ = 0;
17        return false;
18    }
19 }
```

Listing 342: The inline function `correct()` in `pimpleControlI.H`

PIMPLE or PISO algorithm

Listing 343 shows parts of the code of the constructor of the class `pimpleControl`. At first some data fields are set to initial values. Then the `read()` function is called, this function is shown in Listing 339. After reading the solution controls the variable `nCorrPIMPLE_` is tested. If this value is equal to one, then the solution algorithm equates the PISO algorithm. In this case an according message is printed to the Terminal.

```
1 Foam::pimpleControl::pimpleControl fvMesh& mesh) :
2     solutionControl(mesh, "PIMPLE"),
3     nCorrPIMPLE_(0),
4     nCorrPISO_(0),
5     corrPISO_(0),
6     turbOnFinalIterOnly_(true),
7     converged_(false)
8 {
9     read();
10
11    if (nCorrPIMPLE_ > 1)
12    {
13        /* code removed for shortness of listing */
14    }
15    else
16    {
17        Info<< nl << algorithmName_ << ": Operating solver in PISO mode" << nl << endl;
18    }
}
```

Listing 343: Constructor of `pimpleControl` in `pimpleControl.C`

52.2.3 Residual control of the outer PIMPLE-loop

The keyword `nOuterCorrectors` controls the number of outer-loop iterations used for each time step by the PIMPLE algorithm. In addition to the fixed number `nOuterCorrectors`, the number of outer-loop iterations can also be controlled by the residuals of the actual solution. If this residual-control is used, then `nOuterCorrectors` sets the upper limit for outer-loop iterations, if the specified tolerance for the residuals is met with less iterations, then the outer-loop is considered converged.

A note on OpenFOAM-6

With OpenFOAM-6¹⁸⁵ the residual-control framework of the PIMPLE solution control class was reorganized, making it consistent with the SIMPLE solution control class. With this changes, `residualControl` acts on the simulation as a whole, whereas the new `outerCorrectorResidualControl` manages the outer-loop of the PIMPLE algorithm.

```
PIMPLE
{
    // ...

    outerCorrectorResidualControl
    {
        p_rgh
        {
            relTol      0;
            tolerance   0.0001;
        }
    }
}
```

Listing 344: *outerCorrectorResidualControl*

¹⁸⁵<https://github.com/OpenFOAM/OpenFOAM-dev/commit/4c8122783aedaa7dadf0486163a98350e625db32#diff-13b1708e0fc8512ad44fa3edd4175459>

53 rhoPimpleFoam

53.1 General remarks

rhoPimpleFoam is a compressible, single-phase solver.

53.2 Solution algorithm

rhoPimpleFoam uses, as the name indicates, the PIMPLE algorithm.

53.3 Governing equations

53.3.1 Density

The solver *rhoPimpleFoam* is a pressure-based solver, which solves for the velocity and the pressure field. The alternative would be a density-based solver, which solves for velocity and density. However, density-based solvers are quite rare in OpenFOAM, as the only solver known to the author is rhoCentralFoam.

For the density there are two options: either compute the density from the continuity equation; or compute it from the pressure via the thermodynamic model, i.e. the equation of state. These two options are controlled by the keyword **SIMPLERho** in the PIMPLE dictionary of the file **fvSolution**.

Solving the continuity equation

In Listing 345 the continuity equation is shown. This equation is solved, when the keyword **SIMPLERho** is set to false.

```
1 {  
2     fvScalarMatrix rhoEqn  
3     (  
4         fvm::ddt(rho)  
5         + fvc::div(phi)  
6         ==  
7         fvOptions(rho)  
8     );  
9  
10    fvOptions.constrain(rhoEqn);  
11  
12    rhoEqn.solve();  
13  
14    fvOptions.correct(rho);  
15 }
```

Listing 345: The continuity equation in the file **rhoEqn.H**

Computing the density via the equation of state

The other option to compute the density is to compute it via the equation of state. This option is used when the keyword **SIMPLERho** is set to true.

Below, the equation of state for a perfect gas is shown.

$$\rho = \frac{p}{RT} \tag{116}$$

In the example of a perfect gas, using the equation of state has the advantage that the density is computed from the pressure and the temperature, which have already been computed.

This option was described in the relevant commit message¹⁸⁶ as follows:

With this option the density is updated from thermodynamics rather than continuity after the pressure equation which is better behaved if pressure is relaxed and/or solved to a loose relative tolerance.

¹⁸⁶<https://github.com/OpenFOAM/OpenFOAM-dev/commit/79ff91350ef6092b2dd864029a6023bec2b66b50>

54 twoPhaseEulerFoam

This section is valid for OpenFOAM-2.0 til OpenFOAM-2.2.

54.1 General remarks

twoPhaseEulerFoam is a solver for two-phase problems. According to the CFD-Online Forum (<http://www.cfd-online.com/Forums/openfoam/>) this solver as well as *bubbleFoam* is based on the PhD thesis of Henrik Rusche [56]. In the course of an update of OpenFOAM-2.1.x in July 2012 the solution algorithm of the continuity equation was changed.

54.1.1 Turbulence

twoPhaseEulerFoam can only use the k- ϵ turbulence model. This model is so to say hardcoded and can only be turned on or off.

54.1.2 Kinetic theory

twoPhaseEulerFoam can make use of the kinetic theory for granular simulations, e.g. air flowing through a bed of small particles. This model can also be turned on or off.

In the following sections kinetic theory is ignored for the reason of keeping listings and explanations short.

54.2 Solver algorithm

twoPhaseEulerFoam is based on the PIMPLE algorithm. However, there are some modifications necessary for solving two-phase problems. Listing 346 shows the main part of this solver. The first two lines inside the main loop (*pimple.loop()*) differ from *pimpleFoam*. These lines deal with the two-phase continuity equation and the inter-phase momentum exchange coefficients.

Next, in line 6, comes the momentum predictor. It contains the momentum equations for both phases and solves them subsequently, thus the filename *UEqns.H*.

After the predictor comes the corrector. The corrector is in fact a corrector loop. Inside this loop (*pimple.correct()*) the correction of pressure and velocity is computed. Inside the corrector loop (line 15) there is also a conditional second call of the continuity equation. The condition consists of two boolean statements. The first is a boolean variable, which is set in a dictionary by the user. The second is generated by the solution control.

After the corrector loop the total time derivatives of the velocities are calculated. Finally, the turbulent transport equations are solved. In this case it is the k- ϵ model that is called explicitly (line 23).

```
1 // --- Pressure-velocity PIMPLE corrector loop
2 while (pimple.loop())
3 {
4     #include "alphaEqn.H"
5     #include "liftDragCoeffs.H"
6     #include "UEqns.H"
7
8     // --- Pressure corrector loop
9     while (pimple.correct())
10    {
11        #include "pEqn.H"
12
13        if (correctAlpha && !pimple.finalIter())
14        {
15            #include "alphaEqn.H"
16        }
17    }
18
19    #include "DDtU.H"
20
21    if (pimple.turbCorr())
22    {
23        #include "kEpsilon.H"
```

24 }
25 }

Listing 346: The main loop of *twoPhaseEulerFoam*

Figure 157 shows the flow chart of all operations that are performed during one time step.

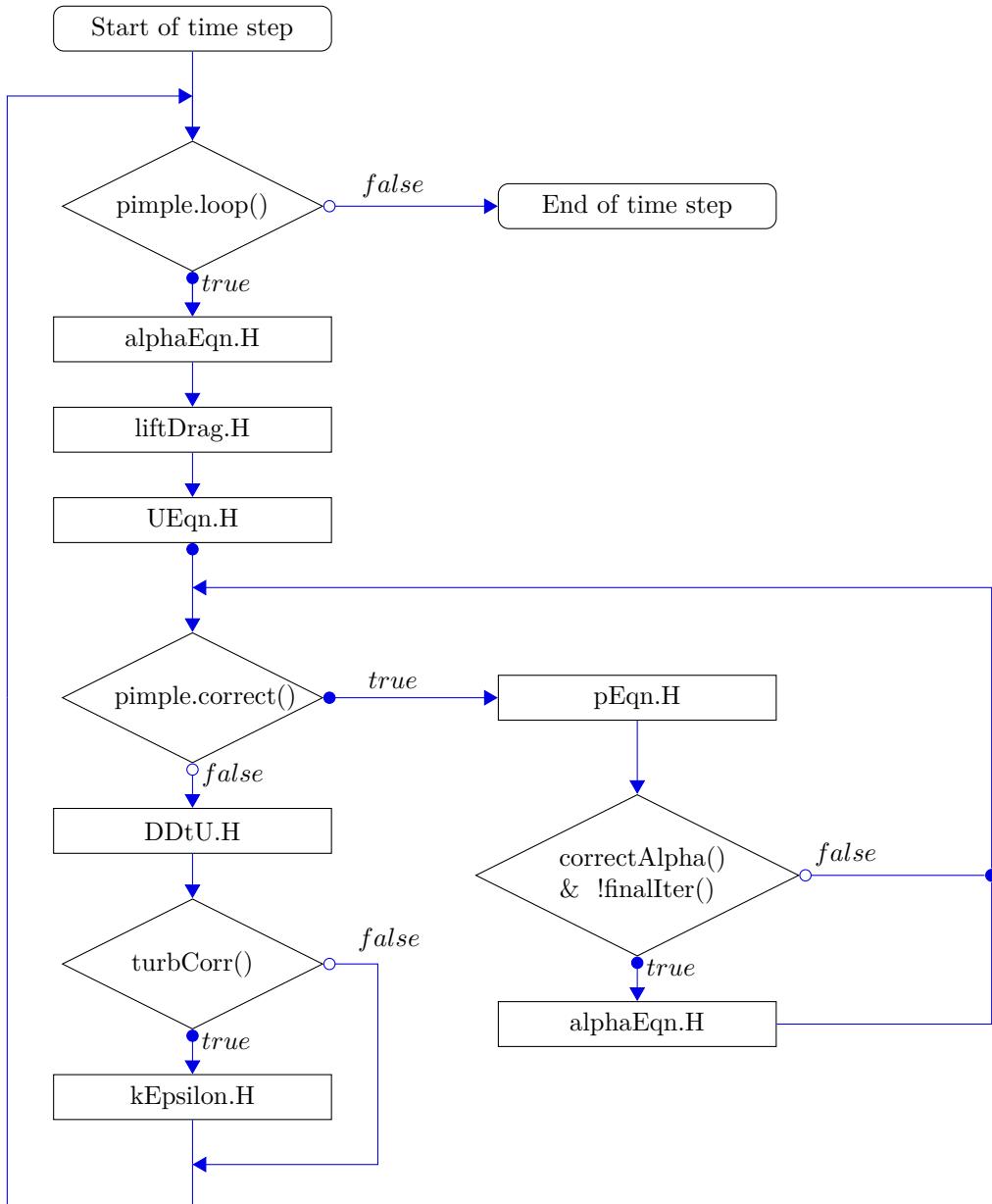


Figure 157: Flow chart of the main loop of *twoPhaseEulerFoam*

54.2.1 Continuity

The continuity equation is implemented in the file `alphaEqn.H`.

Second call

In line 15 of Listing 346 the continuity equation is called again inside an `if`-statement. The condition depends on two boolean expressions.

The first, `correctAlpha`, is controlled by the `fvSolution` dictionary. Assigning a value to this keyword – the keyword has the same name as the boolean variable in the source code – is mandatory. The reading operation of this keyword from the dictionary can be found in the source file `readTwoPhaseEulerFoamControls.H` and is shown in Listing 347.

Three keywords are looked up from the `fvSolution` dictionary. All of them are related to the solving algorithm for the continuity equation. Those entries are read from the dictionary by invoking the function `lookup()`. See Section 68.3 for a detailed discussion about looking up keywords from dictionaries.

```

1 #include "readTimeControls.H"
2
3 int nAlphaCorr(readInt(pimple.dict().lookup("nAlphaCorr")));
4 int nAlphaSubCycles(readInt(pimple.dict().lookup("nAlphaSubCycles")));
5 Switch correctAlpha(pimple.dict().lookup("correctAlpha"));

```

Listing 347: The content of `readTwoPhaseEulerFoamControls.H`

The second boolean expression controlling the second call in line 15 of Listing 346 is controlled by the number of iterations of the PIMPLE loop. See Section 52.2 for a discussion about the PIMPLE algorithm.

The expression `pimple.finalIter()` is `true` when the last iteration of the PIMPLE algorithm is entered. Therefore, the expression `!pimple.finalIter()` is `true` if, and only if, the value of `nOuterCorrectors` or `nCorrPIMPLE_` is greater than one. Because only then, there is more than one PIMPLE iteration and only then, there is an iteration other than the final one.

If the PIMPLE loop is traversed only once, then `alphaEqn.H` is not entered a second time.

The file `alphaEqn.H`

The examination of the file `alphaEqn.H` results in the flow chart in Figure 158. The corrector loop is traversed a specified number of times. This number is set by the keyword `nAlphaCorr` of the `fvSolution` dictionary. The corrector loop is a simple `for` loop.

Inside the corrector loop is a sub-cycle loop. Inside this loop the continuity equation is solved. After the sub-cycle the volume fraction of the continuous phase is updated. The sub-cycle loop is also traversed a specified number of times. This number is set by the keyword `nAlphaSubCycles` of the `fvSolution` dictionary.

When the corrector loop is not entered anymore, the mixture density is updated.

54.3 Momentum exchange between the phases

54.3.1 Drag

The solver `twoPhaseEulerFoam` offers a number of drag models. In the sources of `twoPhaseEulerFoam` there are this models

- Ergun
- Gabilaro
- GidaspowErgunWenYu
- GidaspowSchillerNaumann
- SchillerNaumann
- SyamlalOBrien
- WenYu

The equations behind this models can be found in [27] or [65].

Drag is considered in the governing equations by the use of the so-called drag-function K . This drag-function is either computed directly, or it is computed by the use of the drag coefficient C_d . The drag force is the product of the drag-function and the relative velocity between the phases \mathbf{U}_r [27].

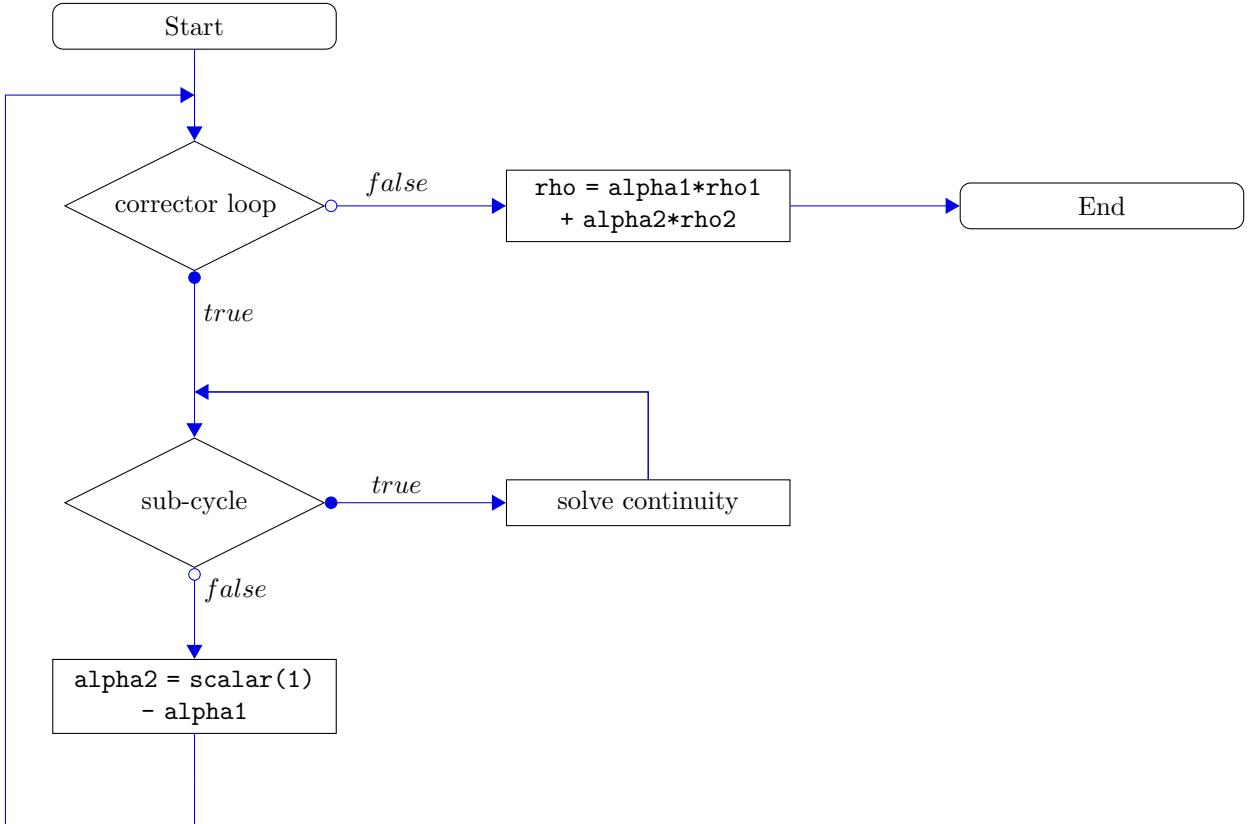


Figure 158: Flow chart of the operations in `alphaEqn.H`

Schiller-Naumann drag

We use the Schiller-Naumann drag model as an example to demonstrate how OpenFOAM calculates the drag force. This drag model utilizes a drag coefficient that is a function of the Reynolds number.

$$C_d = \begin{cases} \frac{24}{Re} (1 + 0.15 Re^{0.687}) & \text{if } Re \leq 1000 \\ 0.44 & \text{if } Re > 1000 \end{cases} \quad (117)$$

$$K = \frac{3}{4} C_d \rho_B \frac{U_r}{d_A} \quad (118)$$

The drag coefficient is dimensionless, whereas the product of the drag-function K and the relative velocity has the dimension of a force density.

$$\begin{aligned} [K] &= [C_d] \cdot [\rho_B] \cdot \left[\frac{U_r}{d_A} \right] = 1 \cdot \frac{\text{kg}}{\text{m}^3} \cdot \frac{\text{m}}{\text{s}} \frac{1}{\text{m}} = \frac{\text{kg}}{\text{m}^3 \text{s}} \\ [K \cdot U_r] &= \frac{\text{kg}}{\text{m}^3 \text{s}} \cdot \frac{\text{m}}{\text{s}} = \frac{\text{kgm}}{\text{s}^2} \cdot \frac{1}{\text{m}^3} = \frac{\text{N}}{\text{m}^3} \end{aligned}$$

Listing 348 shows, how the drag-function is computed by the Schiller-Naumann drag model.

```
Foam::tmp<Foam::volScalarField> Foam::SchillerNaumann::K
(
    const volScalarField& Ur
) const
{
    volScalarField Re(max(Ur*phasea_.d()/phaseb_.nu(), scalar(1.0e-3)));
    volScalarField Cds
    (

```

```

    neg(Re - 1000)*(24.0*(1.0 + 0.15*pow(Re, 0.687))/Re)
    + pos(Re - 1000)*0.44
};

return 0.75*Cds*phaseb_.rho()*Ur/phasea_.d();
}

```

Listing 348: Calculation of the drag-function in the file `SchillerNaumann.H`

The drag force contributes to the momentum balance. Probably for numerical reasons, one part of the drag is considered in the momentum equation and the other part is considered in the pressure equation.

54.3.2 Lift

The lift model of `twoPhaseEulerFoam` is described in [56]. The lift model computes the lift force on a rigid sphere in shear flow. The force density is calculated from the relative velocity between the phases and the vorticity of the mixture.

$$\frac{F_L}{V_B} = C_L \rho_c |\mathbf{U}_r \times (\nabla \times \mathbf{U}_c)| \quad (119)$$

mit

$$\begin{aligned} \mathbf{U}_r &= \mathbf{U}_A - \mathbf{U}_B \\ \mathbf{U}_c &= \underbrace{\alpha \mathbf{U}_A + (1 - \alpha) \mathbf{U}_B}_{=\beta} \\ \rho_c &= \alpha \rho_A + \beta \rho_B \end{aligned}$$

The lift force is computed in the file `liftDragCoeffs.H`. The vector field `liftCoeff` contains the lift force density.

```
volVectorField liftCoeff(Cl*(beta*rhob + alpha*rhoa)*(Ur ^ fvc::curl(U)));
```

Listing 349: Berechnung Auftriebskraft; `liftDragCoeffs.H`

The dimensions of the field `liftCoeff` is the dimension of a force density.

$$[liftCoeff] = [C_L] \cdot [\rho_c] \cdot [\mathbf{U}_r \times (\nabla \times \mathbf{U}_c)] = 1 \cdot \frac{\text{kg}}{\text{m}^3} \cdot \frac{\text{m}}{\text{s}} \frac{1}{\text{m}} \frac{\text{m}}{\text{s}} = \frac{\text{kgm}}{\text{s}^2} \cdot \frac{1}{\text{m}^3} = \frac{\text{N}}{\text{m}^3}$$

54.3.3 Virtual mass

The virtual mass – an accelerating bubble needs not only to accelerate its own mass, it also needs to accelerate some of the displaced fluid – is considered in the momentum equation.

$$M_{A,VM} = \beta \frac{\rho_B}{\rho_A} C_{VM} \left(\frac{\mathbf{D}_B \mathbf{U}_B}{\mathbf{D}t} - \frac{\mathbf{D}_A \mathbf{U}_A}{\mathbf{D}t} \right) \quad (120)$$

In the source code, the momentum exchange term due to virtual mass is split into two parts. One part is included in the `rhs` of the momentum equation, the other is considered in the `lhs`. This separation is probably for numerical reasons.

```
UaEqn =
(
  scalar(1) + Cvm*rhob*beta/rhoa *
  (
    fvm::ddt(Ua)
    + fvm::div(phi_a, Ua, "div(phi_a,Ua)")
    - fvm::Sp(fvc::div(phi_a), Ua)
  )
)
```

```
+ /* other terms */
==  
/* other terms */
- beta/rhoa*(liftCoeff - Cvm*rhob*DDtUb)  
);
```

Listing 350: Terms including virtual mass in the file UEqns.H

54.4 Kinetic Theory

For the simulation of dense gas-solid particulate flows the particulate phase can be modelled using the kinetic theory model.

55 *twoPhaseEulerFoam-2.3*

This section is valid for OpenFOAM-2.3.

With the release of OpenFOAM-2.3 the two-phase Eulerian solver *twoPhaseEulerFoam* has seen some major changes. See the release notes for further details: <http://www.openfoam.org/version2.3.0/multiphase.php>.

55.1 Physics

The most important change in *twoPhaseEulerFoam* from version $\leq 2.2.x$ to 2.3 is that the solver is based on a completely different set of physical models. In version 2.3 phases are modelled using OpenFOAM's thermo-physical models. The phases are considered compressible, therefore all simplifications when considering a phase incompressible do not hold anymore.

55.1.1 Pressure

In *twoPhaseEulerFoam-2.3* the pressure is now a real physical pressure. In an incompressible simulation the absolute value of the pressure has no meaning, only pressure differences count. In a compressible model, the absolute value of the pressure has an effect, e.g. when using the **isothermalDiameter** diameter model to determine the diameter of the dispersed phase elements.

Thus, when migrating a simulation case from OpenFOAM-2.2 or lower to 2.3, check the pressure initial condition and the boundary conditions.

55.1.2 Temperature

As the new version of the solver uses thermo-physical models for the phases, the user is required to specify not only the thermo-physical properties of the phases, the user also has to provide initial and boundary conditions for the temperature of both phases. Thus, two additional fields are present – or need to be present – in the time directories, e.g. **T.air** and **T.water**.

55.2 Naming scheme

The overhaul of *twoPhaseEulerFoam* in version 2.3 aims for reuseability and generality of the solver code itself as well as of the case data. A general distinction of data concerning a single phase and data concerning the whole simulation case can be made.

Case data is named as usual (e.g. **fvSchemes**, **controlDict**, **g**, etc.). Data related to a specific phase is now stored in files with a filename that consists of two parts. The naming scheme follows the well known **FILENAME.EXTENSION** naming scheme. In this case **FILENAME** denotes the type of information and **EXTENSION** denotes the phase itself. This naming scheme is much more general than other naming schemes that are/were used in OpenFOAM (cf. **U1**, **U2** vs. **Uwater**, **Uair** vs. **U.air**, **U.water**).

Listing 351 shows the contents of the **0** and *constant* folders of the bubble column tutorial case. There we see the **FILENAME.EXTENSION** naming scheme applied. As each phase has a velocity and a temperature, we see two files for velocity and temperature. The volume fraction is an exception, as there are only two phase considered, the volume fraction of water is easily calculated, i.e. **alpha.water = 1.0 - alpha.air**. As the pressure is share by all phases, the pressure file has no file-extension. In the *constant* folder there is also data that applies to one phase and data that applies to the simulation case. The files **g** and **phaseProperties** have no extensions because they contain no information specific to one phase. The thermophysical properties of the phases air and water are stored in the appropriate files.

The naming scheme that was introduced with *twoPhaseEulerFoam-2.3* is fit to create a material data library. The way the phases or the phase data is organized within the solver is now independent of the way the phase data is organized within the case.

```
user@host:~/OpenFOAM/OpenFOAM-2.3.x/tutorials/multiphase/twoPhaseEulerFoam/RAS/bubbleColumn$  
ls 0 -1  
alpha.air  
alpha.air.org  
epsilon.air  
epsilon.water  
k.air
```

```

k.water
nut.air
nut.water
p
T.air
Theta
T.water
U.air
U.water
user@host:~/OpenFOAM/OpenFOAM-2.3.x/tutorials/multiphase/twoPhaseEulerFoam/RAS/bubbleColumn$ 
    ls constant -1
g
phaseProperties
polyMesh
thermophysicalProperties.air
thermophysicalProperties.water
turbulenceProperties.air
turbulenceProperties.water

```

Listing 351: Content of the *0* and *constant* folders of the bubble column tutorial case of *twoPhaseEulerFoam* in OpenFOAM-2.3.x

55.3 Solver capabilities

Not only the naming scheme is more general in version 2.3, also the solver itself is more generalized.

Compressibility all phases are treated as compressible. In the file **thermophysicalProperties** the behaviour of a phase can be specified.

Energy equation *twoPhaseEulerFoam* solves an energy equation for all phases. This can not be turned off.

Phase interaction has been extended. A great number of models specific for gas-liquid systems have been included.

Turbulence Turbulence is treated in a more general way. A number of turbulence models can be used in contrast to earlier versions of *twoPhaseEulerFoam* that had *kEpsilon* hard-coded.

55.4 Turbulence models

twoPhaseEulerFoam-2.3 uses a whole new class of turbulence models. As the governing equations of *twoPhaseEulerFoam* – namely the momentum equation – aren't phase intensive anymore, also the governing equations of the turbulence model are formulated in their general multi-phase form¹⁸⁷.

This limits the choice of turbulence models to a small number of multi-phase turbulence models. Listings 352 and 353 show the list of available turbulence models at the time of writing (May 2014).

```

Valid RASModel types:

6
(
LaheyKEpsilon
continuousGasKEpsilon
kEpsilon
kineticTheory
mixtureKEpsilon
phasePressure
)

```

Listing 352: Valid RAS turbulence models of *twoPhaseEulerFoam*.

```

Valid LESModel types:

5
(
NicenoKEqn

```

¹⁸⁷ <http://www.openfoam.org/version2.3.0/multiphase.php>

```

Smagorinsky
SmagorinskyZhang
continuousGasKEqn
kEqn
)

```

Listing 353: Valid LES turbulence models of *twoPhaseEulerFoam*.

55.4.1 Naming scheme

One feature of the multi-phase turbulence model framework is that the additional turbulent viscosity is now named `nut`, regardless of whether a RAS or an LES model is used. This is possible, since both additional viscosities stem from the application of the Boussinesq-hypothesis.

In single-phase simulations an LES turbulence model works with the field `nuSgs`, whereas a RAS model uses `nut`. See textbooks on CFD for the theory behind RAS and LES turbulence models and the origin and meaning of ν_t and ν_{sgs} [37]. Sections 73 and 74 cover the incompressible $k - \epsilon$ model respectively some basics on LES turbulence models.

55.4.2 kEpsilon

Listing 354 shows the governing equations of the compressible multi-phase formulation of the $k - \epsilon$ model. The governing equations are largely equivalent to the compressible formulation of the single-phase $k - \epsilon$ model. The formulation deviates from the compressible single-phase formulation in two aspects. First, the convective term is corrected with the continuity error, see Lines 5 and 18. Furthermore, there is an additional source term on the RHS, see Lines 11 and 24.

```

1   tmp<fvScalarMatrix> epsEqn
2   (
3       fvm::ddt(alpha, rho, epsilon_)
4       + fvm::div(alphaRhoPhi, epsilon_)
5       - fvm::Sp(fvc::ddt(alpha, rho) + fvc::div(alphaRhoPhi), epsilon_)
6       - fvm::laplacian(alpha*rho*DepsilonEff(), epsilon_)
7   ==
8       C1_*alpha*rho*G*epsilon_/k_
9       - fvm::SuSp(((2.0/3.0)*C1_ + C3_)*alpha*rho*divU, epsilon_)
10      - fvm::Sp(C2_*alpha*rho*epsilon_/k_, epsilon_)
11      + epsilonSource()
12  );
13
14  tmp<fvScalarMatrix> kEqn
15  (
16      fvm::ddt(alpha, rho, k_)
17      + fvm::div(alphaRhoPhi, k_)
18      - fvm::Sp(fvc::ddt(alpha, rho) + fvc::div(alphaRhoPhi), k_)
19      - fvm::laplacian(alpha*rho*DkEff(), k_)
20  ==
21      alpha*rho*G
22      - fvm::SuSp((2.0/3.0)*alpha*rho*divU, k_)
23      - fvm::Sp(alpha*rho*epsilon_/k_, k_)
24      + kSource()
25  );

```

Listing 354: Governing equations of the `kEpsilon` turbulence model.

55.4.3 LaheyKEpsilon

The `LaheyKEpsilon` turbulence model is a derivation of the standard `kEpsilon` turbulence model, see Listing 355. The `LaheyKEpsilon` turbulence model is an extension of the standard $k - \epsilon$ model to account for the effect of the dispersed phase on the turbulence of the continuous phase. This effect is referred to as *bubble induced turbulence* (BIT).

There are essentially two ways to account for BIT. One follows the idea of Sato and Sekoguchi [57], there an additional viscosity models the effect of the increased turbulence caused by the wakes of the bubbles. The

other approach is based on the work of Pfleger and Becker [53]. They included additional source terms in the transport equations for k and ϵ .

The Lahey model uses with its standard coefficients both approaches.

```

1 template<class BasicTurbulenceModel>
2 class LaheyKEpsilon
3 :
4     public kEpsilon<BasicTurbulenceModel>
5 {
6     /* class definition */
7 }
```

Listing 355: The first lines of the `LaheyKEpsilon` turbulence model definition.

Pitfall: the other phase

When using the `LaheyKEpsilon` model for one phase phase, the other phase is not allowed to be modelled as laminar. Listing 356 shows the method `phaseTransferCoefficient()` of the `LaheyKEpsilon` turbulence model. In Line 13 of Listing 356 we find the function call `gasTurbulence.k()` in the denominator. If `laminar` is chosen as turbulence model for the other phase, then the method `k()` of the `laminar` turbulence model is called. Listing 357 shows the definition of this method. We easily see, that the zero return value will cause problems in the `phaseTransferCoeff()` method of the `LaheyKEpsilon` turbulence model.

```

1 template<class BasicTurbulenceModel>
2 tmp<volScalarField>
3 LaheyKEpsilon<BasicTurbulenceModel>::phaseTransferCoeff() const
4 {
5     const volVectorField& U = this->U_;
6     const alphaField& alpha = this->alpha_;
7     const rhoField& rho = this->rho_;
8     const turbulenceModel& gasTurbulence = this->gasTurbulence();
9     return
10    (
11        max(alphaInversion_ - alpha, scalar(0))
12        *rho
13        *min(gasTurbulence.epsilon()/gasTurbulence.k(), 1.0/U.time().deltaT())
14    );
15 }
```

Listing 356: The method `phaseTransferCoeff()` of the `LaheyKEpsilon` turbulence model.

```

1 template<class BasicTurbulenceModel>
2 Foam::tmp<Foam::volScalarField>
3 Foam::laminar<BasicTurbulenceModel>::k() const
4 {
5     return tmp<volScalarField>
6     (
7         new volScalarField
8         (
9             IOobject
10            (
11                IOobject::groupName("k", this->U_.group()),
12                this->runTime_.timeName(),
13                this->mesh_,
14                IOobject::NO_READ,
15                IOobject::NO_WRITE
16            ),
17            this->mesh_,
18            dimensionedScalar("k", sqr(this->U_.dimensions()), 0.0)
19        )
20    );
21 }
```

Listing 357: The method `k()` of the `laminar` turbulence model.

Pitfall: the dispersed phase

It is not possible to assign the `LaheyKEpsilon` turbulence model to the dispersed phase, either to the dispersed phase alone or to both phases. In any case the attempt to do so results in a segmentation fault when first using the turbulence model at the initialisation of the simulation case. The reason for this is not entirely known to the author.

55.4.4 `mixtureKEpsilon`

Usage

The $k - \epsilon$ model is computed for the mixture, i.e. the transport equations are solved for using the mixture properties. Thus, the solution variables are named `km` and `epsilonM`, see Listing 358.

```
DILUPBiCG: Solving for epsilonM, Initial residual = 0.0114325, Final residual = 2.79117e-09,
No Iterations 2
DILUPBiCG: Solving for km, Initial residual = 0.0078252, Final residual = 6.13173e-09, No
Iterations 2
```

Listing 358: Solver output of `twoPhaseEulerFoam` using the `mixtureKEpsilon` turbulence model.

In order to use the mixture $k - \epsilon$ model, it needs to be specified in both `turbulenceProperties` files. Listing 359 shows the resulting error message when `mixtureKEpsilon` is specified for only one of the phases. As the turbulence model for the mixture applies to both phases, it needs to be specified for both phases.

```
--> FOAM FATAL ERROR:
```

```
lookup of turbulenceProperties.water from objectRegistry region0 successful
but it is not a mixtureKEpsilon, it is a LaheyKEpsilon

From function objectRegistry::lookupObject<Type>(const word&) const
in file /home/user/OpenFOAM/OpenFOAM-2.3.x/src/OpenFOAM/lnInclude/objectRegistryTemplates.
C at line 181.
```

```
FOAM aborting
```

Listing 359: Solver output of `twoPhaseEulerFoam` when the `mixtureKEpsilon` turbulence model is specified for only one of the two phases.

Theory

The governing equations of the mixture $k - \epsilon$ model can be found in the sources at `\$FOAM_SRC/TurbulenceModels/phaseCompressible/RAS/mixtureKEpsilon` and in [12]. The biggest difference between the equations stated in [12] and the code of `mixtureKEpsilon` can be found in the Lines 5 and 18 of Listing 360. There, the continuity equation of the mixture appears on the left of the governing equations. This minor difference between the formulation of the equation can be resolved in two steps. First, we take a look on the first two terms of the governing equations in [12] (local derivative and convective term), see Eqns. (121) to (124).

$$\frac{\partial \rho_m \epsilon_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m \epsilon_m) + \dots \quad (121)$$

$$\rho_m \frac{\partial \epsilon_m}{\partial t} + \epsilon_m \frac{\partial \rho_m}{\partial t} + \epsilon_m \nabla \cdot (\rho_m \mathbf{u}_m) + \rho_m \mathbf{u}_m \cdot \nabla \epsilon_m + \dots \quad (122)$$

$$\rho_m \frac{\partial \epsilon_m}{\partial t} + \underbrace{\epsilon_m \left(\frac{\partial \rho_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m) \right)}_{=0} + \rho_m \mathbf{u}_m \cdot \nabla \epsilon_m + \dots \quad (123)$$

$$\rho_m \frac{\partial \epsilon_m}{\partial t} + \rho_m \mathbf{u}_m \cdot \nabla \epsilon_m + \dots \quad (124)$$

In order to derive equations equivalent to the code implemented in OpenFOAM, we begin with Eq. (124) and use the product rule of differentiation, cf. Eqns. (121) and (122).

$$\rho_m \frac{\partial \epsilon_m}{\partial t} + \rho_m \mathbf{u}_m \cdot \nabla \epsilon_m + \dots \quad (124)$$

$$\frac{\partial \rho_m \epsilon_m}{\partial t} - \epsilon_m \frac{\partial \rho_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m \epsilon_m) - \epsilon_m \nabla \cdot (\rho_m \mathbf{u}_m) + \dots \quad (125)$$

$$\frac{\partial \rho_m \epsilon_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m \epsilon_m) - \epsilon_m \left(\frac{\partial \rho_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m) \right) + \dots \quad (126)$$

Eq (126) is now equivalent to the first terms of the ϵ equation of Listing 360. The exact reason why this formulation was chosen is unknown to the author, a probable reason might be a better numerical behaviour.

```

1   tmp<fvScalarMatrix> epsEqn
2   (
3       fvm::ddt(rhom, epsilonm)
4       + fvm::div(phim, epsilonm)
5       - fvm::Sp(fvc::ddt(rhom) + fvc::div(phim), epsilonm)
6       - fvm::laplacian(DepsilonEff(rhom*nutm), epsilonm)
7     ==
8       C1_*rhom*Gm*epsilonnm/km
9       - fvm::SuSp((2.0/3.0)*C1_)*rhom*divUm, epsilonm)
10      - fvm::Sp(C2_*rhom*epsilonnm/km, epsilonm)
11      + epsilonSource()
12  );
13
14 tmp<fvScalarMatrix> kmEqn
15 (
16     fvm::ddt(rhom, km)
17     + fvm::div(phim, km)
18     - fvm::Sp(fvc::ddt(rhom) + fvc::div(phim), km)
19     - fvm::laplacian(DkEff(rhom*nutm), km)
20 ==
21     rhom*Gm
22     - fvm::SuSp((2.0/3.0)*rhom*divUm, km)
23     - fvm::Sp(rhom*epsilonnm/km, km)
24     + kSource()
25 );

```

Listing 360: Governing equations of the `mixtureKEpsilon` turbulence model.

The basic relations between the turbulent quantities of the mixture and the turbulence quantities of the individual phases are based on the turbulence response coefficient C_t , which is the ratio between the r.m.s. values of the velocity fluctuations of the dispersed and the continuous phase [12].

$$C_t = \frac{U'_d}{U'_c} \quad (127)$$

with this coefficient, we can now express the following relations, which we can find in the file `mixtureKEpsilon.C`

$$\rho_m = \alpha_c \rho_c + \alpha_d \rho_d \quad (128)$$

$$C_c^2 = \frac{\rho_m}{\alpha_c \rho_c + C_t^2 \alpha_d \rho_d} \quad (129)$$

$$k_c = C_c^2 k_m \quad (130)$$

$$k_d = C - t^2 k_c \quad (131)$$

$$\epsilon_c = C_c^2 \epsilon_m \quad (132)$$

$$\epsilon_d = C_t^2 \epsilon_c \quad (133)$$

$$\nu_t = C_\mu \frac{k_m^2}{\epsilon_m} \quad (134)$$

$$\nu_{c,eff} = \nu_c + \nu_t \quad (135)$$

$$\nu_{d,eff} = \nu_d + C_t^2 \frac{\nu_c}{\nu_d} \nu_t \quad (136)$$

What remains to clarify is how the turbulence response coefficient C_t is determined. OpenFOAM implements the model proposed by Issa [36] and validated by Hill [28] [56, 12]. Furthermore, the turbulence response coefficient is modified to account for the influence of the dispersed phase's volume fraction α_d , see e.g. [56, 12].

$$C_{t,0} = \frac{3 + \beta}{1 + \beta + 2\rho_d/\rho_c} \quad (137)$$

$$\beta = \frac{2A_d L_e^2}{\rho_c \nu_c Re_t} \quad (138)$$

$$Re_t = \frac{U'_c L_e}{\nu_c} \quad (139)$$

$$L_e = C_\mu \frac{k_c^{3/2}}{\epsilon_c} \quad (140)$$

$$U'_c = \sqrt{\frac{2k_c}{3}} \quad (141)$$

$$C_t(\alpha_d) = 1 + (C_{t,0} - 1)e^{-f(\alpha_d)} \quad (142)$$

$$f(\alpha_d) = 180\alpha_d - 4.71 \cdot 10^3\alpha_d^2 + 4.26 \cdot 10^4\alpha_d^3 \quad (143)$$

55.4.5 SmagorinskyZhang LES

The SmagorinskyZhang turbulence model is a zero equation LES turbulence model. This turbulence model corrects the turbulent viscosity by a contribution due to bubble induced turbulence (BIT) [71]. As there is no use of turbulent quantities of the other phase, there is no limitation in turbulence model choice for the other phase.

55.4.6 NicenoKEqn LES

The NicenoKEqn turbulence model is an LES model which solves a transport equation for the unresolved turbulent kinetic energy k_{SGS} . Similar to the model of Lahey, the model of Niceno is able to account for effects of bubble induced turbulence. This is done through an additional viscosity and/or an additional source term in the transport equation for the turbulent kinetic energy.

Similar to the Lahey model, the Niceno model accesses turbulent quantities of the other phase, for this reason it is not possible to model the other phase as a laminar phase. As we can see in Line 13 of Listing 361, the Niceno model takes the square root of the gas phase's turbulent kinetic energy, when computing the phase transfer coefficient. The method `k()` of the laminar turbulence models returns zero for the turbulent kinetic energy. This triggers a floating point exception (FPE).

```

1 template<class BasicTurbulenceModel>
2 tmp<volScalarField>
3 NicenoKEqn<BasicTurbulenceModel>::phaseTransferCoeff() const
4 {
5     const volVectorField& U = this->U_;
6     const alphaField& alpha = this->alpha_;
7     const rhoField& rho = this->rho_;
8     const turbulenceModel& gasTurbulence = this->gasTurbulence();
9     return
10    (
11        max(alphaInversion_ - alpha, scalar(0))
12        *rho
13        *min(this->Ce_*sqrt(gasTurbulence.k())/(this->delta(), 1.0/U.time().deltaT())
14    );
15 }
```

Listing 361: The method `phaseTransferCoeff()` of the Niceno turbulence model.

55.4.7 Pitfall: phase inversion

Phase inversion is the situation when the volume fraction of the continuous phase vanishes in some regions. As almost all terms of the governing equations are weighted with the volume fraction `alpha`, a vanishing volume fraction can lead to serious numerical problems.

Solution via model choice

The following example demonstrates the problems which may be faced when dealing with phase inversion. An air-water bubble column is modelled including some of the air above the water surface. Figure 159 shows the air volume fraction within the bubble column.

When `mixtureKEpsilon` is selected as turbulence model, the volume fraction is not included in the governing equation, so phase inversion poses no big problem, see Listing 360 or Eq. (126).

When `kEpsilon` is selected for the liquid phase, the volume fraction in the governing equations is the volume fraction of the liquid phase. This volume fraction vanishes above the water surface. Thus, in parts of the domain the solution of the governing equations faces numerical problems. The governing equations can still be solved in this case, but preconditioning the resulting matrix equation fails. Preconditioning is a step that is intended to improve the iterative solution of the resulting matrix equation. In the case of the `kEpsilon` turbulence model for the liquid phase, the only way to avoid crashing the simulation is to use a CG-solver with no preconditioning. The GAMG-solver and the smooth solver fail completely.

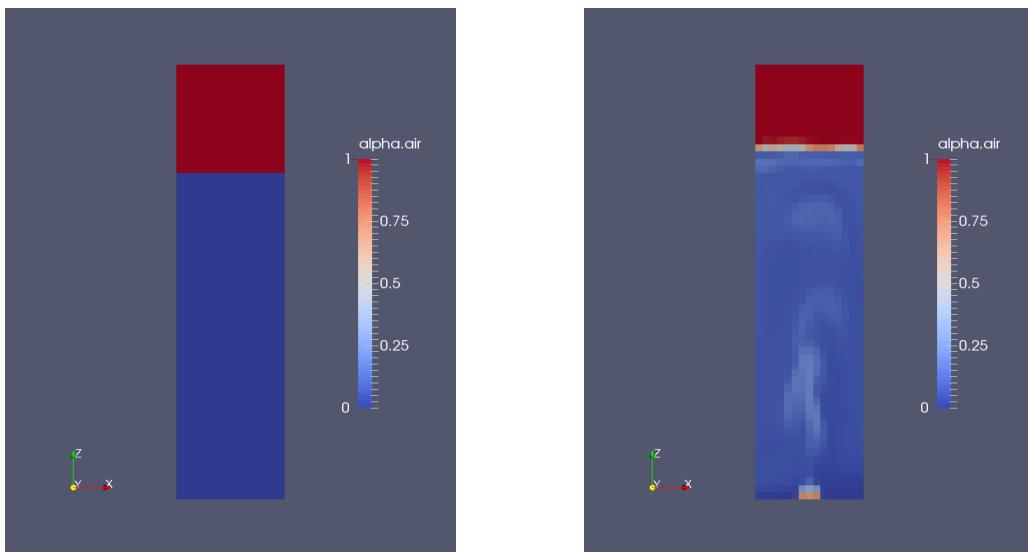


Figure 159: Air volume fraction of the bubble column. Initial field (left) and solution at $t = 10$ s (right).

Table 9 lists possible model choices for two-phase simulations including phase-inversion.

Liquid	Gas	constraints / remarks
<code>kEpsilon</code>	laminar	solver: PBiCG, preconditioner: <code>none</code>
<code>mixtureKEpsilon</code>	<code>mixtureKEpsilon</code>	
<code>Lahey</code>	<code>continuousKEqn</code>	
<code>SmagorinskyZhang</code>	laminar	no issue, since SmagorinskyZhang is a zero-equation model
<code>Niceno</code>	laminar	solver: PBiCG, preconditioner: <code>none</code>
<code>Niceno</code>	<code>continuousKEqn</code>	

Table 9: Turbulence model combinations for phase-inversion cases.

Solution via phaseLimitStabilization

With OpenFOAM-6¹⁸⁸ an fvOption source was introduced to specifically, numerically stabilize transport equations when the phase fraction falls below a certain threshold. This source adds an implicit source term to a transport equation for all cells in which the phase fraction falls below a certain limit. This fvOption is further discussed in Section 46.3.2.

¹⁸⁸<https://openfoam.org/release/6/>

In our example, we can use the `phaseLimitStabilization` fvOption to stabilize the transport equations for the turbulence fields. This way, we can also eliminate, or alleviate, the problems caused by phase inversion, as in all regions with a vanishing phase fraction, the `phaseLimitStabilization` source prevents the transport equations from becoming ill-posed.

55.5 Energy equation

In OpenFOAM-2.3 the `twoPhaseEulerFoam` solver incorporates the functionality of *compressibleTwoPhaseEulerFoam*¹⁸⁹. Accounting for compressibility necessitates the solution of the energy equation. The solving of the energy equation requires the specification of additional discretisation schemes and a solver in `fvSchemes` and `fvSolution`. Depending on the simulation parameters the energy equation is solved in terms of the enthalpy `h` or internal energy `e`.

The energy equation is formulated in a generic form in terms of `he`. The actual decision to solve for `h` or `e` is made at run-time after the thermophysical properties of the two phases have been read.

Besides the internal energy or enthalpy the energy equation involves also the kinetic energy `K`, which is in fact a specific kinetic energy. Listing 362 shows how this kinetic energy is computed. This source code translates into the following mathematical relation.

$$K_i = \frac{1}{2} |U_i|^2 \quad (144)$$

```
Info << "Creating field kinetic energy K\n" << endl;
volScalarField K1(IOobject::groupName("K", phase1.name()), 0.5*magSqr(U1));
volScalarField K2(IOobject::groupName("K", phase2.name()), 0.5*magSqr(U2));
```

Listing 362: Definition of the kinetic energy field in the file `createFields.H` of `twoPhaseEulerFoam`.

The solution of the energy equation can not be deactivated. Even if thermophysical parameters are chosen to represent incompressible phases, the energy equation will be solved each time step.

55.5.1 Governing equations

Listing 363 shows the energy equation for one phase. In Line 3 we see the local derivative and the convection term of the generic internal energy/ enthalpy `he`. In Line 5 is the local derivative and the convection term of the specific kinetic energy `K`.

In the Lines 4 and 6 we see a correction for the continuity error. See Section 71.3 for a detailed discussion.

From Lines 8 to 10 we see the term regarding the mechanical work done. Here we see a conditional expression depending whether the equation is solved for internal energy or enthalpy. All other terms in the equation are formulated generically. Besides the use of the abstract `he`, which is internal energy or enthalpy, the use of the variable `Cpv` is also a characteristic of this generic formulation. This variable stands for either the heat capacity at constant pressure or the heat capacity at constant volume.

Lines 12 to 17 contain the diffusive heat flux. Line 19 represents the heat flux between the two phases. Line 22 contains possible heat sources.

Lines 20 and 21 can be considered a numerical trick. If we ignore the `fvm::Sp()` for a while and add the terms of the two lines, we see that they add up to zero. Adding zero is mathematically allowed. If we do not ignore the `fvm::Sp()`, we need to find out, what is happening. `fvm::Sp()` is an implicit source term, i.e. the contribution of this term goes into the system matrix of the resulting linear equation system. An implicit source term not only contributes to the system matrix, these terms go into the diagonal entries of the system matrix. When solving linear equation systems iteratively, it is preferable to work on a *diagonally dominant* system matrix [37]. Exactly, this is achieved by the Lines 20 and 21. The term in Line 21 adds to the diagonal of the system matrix, whereas the term of Line 20 adds to the right hand side of the ensuing linear equation system. As both sides of the equation have been equally treated, nothing was done wrong mathematically. However, as *diagonal dominance* is numerically a good thing, the convergence behaviour was probably improved.

```
1   fvScalarMatrix he1Eqn
2   (
3       fvm::ddt(alpha1, rho1, he1) + fvm::div(alphaRhoPhi1, he1)
```

¹⁸⁹<http://www.openfoam.org/version2.3.0/multiphase.php>

```

4   - fvm::Sp(contErr1, he1)
5   + fvc::ddt(alpha1, rho1, K1) + fvc::div(alphaRhoPhi1, K1)
6   - contErr1*K1
7   +
8     he1.name() == thermo1.phasePropertyName("e")
9     ? fvc::ddt(alpha1)*p + fvc::div(alphaPhi1, p)
10    : -alpha1*dpt
11  )
12  - fvm::laplacian
13  (
14    fvc::interpolate(alpha1)
15    *fvc::interpolate(thermo1.alphaEff(phase1.turbulence().mut())),
16    he1
17  )
18 ==
19   heatTransferCoeff*(thermo2.T() - thermo1.T())
20   + heatTransferCoeff*he1/Cpv1
21   - fvm::Sp(heatTransferCoeff/Cpv1, he1)
22   + fvOptions(alpha1, rho1, he1)
23 );

```

Listing 363: Energy equation in the file `EEqns.H` of *twoPhaseEulerFoam*.

55.6 Momentum equation

Due to the changes on the modelling side and some restructuring, the momentum equation has a different form compared to previous versions of this solver.

The most general form of the momentum conservation equation for two-phase flow is as follows¹⁹⁰

$$\frac{\partial \alpha_q \rho_q \mathbf{u}_q}{\partial t} + \nabla \cdot (\alpha_q \rho_q \mathbf{u}_q \mathbf{u}_q) - \nabla \cdot \boldsymbol{\tau}_q = \sum_i \mathbf{F}_{q,i} + \sum_i K_{pq,i} (\mathbf{u}_p - \mathbf{u}_q) \quad (145)$$

with

$$\begin{aligned} K_{pq,i} &= -K_{qp,i} \\ K_{qq,i} &= 0 \end{aligned}$$

55.6.1 Units

Now we shall take a short look on the units of this equation. Each term of the equation has to have the same unit. We take the local derivative to determine the unit of all terms in this equation.

$$\left[\frac{\partial \alpha_q \rho_q \mathbf{u}_q}{\partial t} \right] = \frac{1 \text{ kg}}{\text{s m}^3 \text{ s}} = \frac{1}{\text{m}^3} \underbrace{\frac{\text{kg m}}{\text{s}^2}}_{\text{N}} = \frac{\text{N}}{\text{m}^3} \quad (146)$$

We see that all terms of the momentum equation have the unit of a force density. On the RHS of the momentum equation we have two kinds of source terms.

The first kind of source terms – \mathbf{F}_i – can be referred to as body forces, e.g. the gravitational force. This is consistent with our observation, that this terms have the unit of a force density.

$$[\mathbf{F}_i] \stackrel{!}{=} \frac{\text{N}}{\text{m}^3} = \frac{\text{kg}}{\text{m}^2 \text{ s}^2} \quad (147)$$

The second kind of source terms – $K_{pq,i} (\mathbf{u}_p - \mathbf{u}_q)$ – are phase interaction terms. This terms are the product of a coefficient $K_{pq,i}$ with the relative velocity $\mathbf{u}_R = \mathbf{u}_p - \mathbf{u}_q$. Such a phase interaction term might be due to drag. Now we determine the unit of the interphase momentum exchange coefficient $K_{pq,i}$.

$$[K_{pq,i} (\mathbf{u}_p - \mathbf{u}_q)] \stackrel{!}{=} \frac{\text{N}}{\text{m}^3} = \frac{1 \text{ kg}}{\text{s m}^3 \text{ s}} \quad (148)$$

$$[K_{pq,i}] = \frac{\text{kg}}{\text{m}^3 \text{ s}} \quad (149)$$

¹⁹⁰The phase q is the considered phase and phase p denotes the other phase.

55.6.2 Implemented equations

Listing 364 shows one of the momentum conservation equations. On Line 3 we see the local derivative and the convective term. The origin of the term in Line 4 is explained in 71.3. On Line 5 we see a term stemming from the MRF approach. On Line 6 is the momentum diffusion.

On the RHS there are a number of force terms. Although, they are named `*Force`, they are in fact force density terms. On Line 8 we see a part of the drag force. The force due to gravity and the other part of the drag are considered in the pressure equation [56].

```

1     U1Eqn =
2     (
3         fvm::ddt(alpha1, rho1, U1) + fvm::div(alphaRhoPhi1, U1)
4         - fvm::Sp(contErr1, U1)
5         + mrfZones(alpha1*rho1 + virtualMassCoeff, U1)
6         + phase1.turbulence().divDevRhoReff(U1)
7     ==
8         - liftForce
9         - wallLubricationForce
10        - turbulentDispersionForce
11        - virtualMassCoeff
12        *(
13            fvm::ddt(U1)
14            + fvm::div(phi1, U1)
15            - fvm::Sp(fvc::div(phi1), U1)
16            - DDtU2
17        )
18        + fvOptions(alpha1, rho1, U1)
19    );
20    U1Eqn.relax();
21    U1Eqn += fvm::Sp(dragCoeff, U1);
22    fvOptions.constrain(U1Eqn);

```

Listing 364: The code of the momentum conservation equation of phase 1 of `twoPhaseEulerFoam` in `UEqns.H`

The interfacial momentum exchange terms are computed prior to the construction of the momentum equation. Listing 365 shows the relevant lines of the file `UEqns.H`. We see that the momentum exchange terms are provided by some methods. We know that the variable `fluid` is of the type `twoPhaseSystem`. Thus, the methods called to compute the momentum exchange terms are methods of the class `twoPhaseSystem`, see Section 42.2.1.

```

1 volScalarField dragCoeff(fluid.dragCoeff());
2
3 volScalarField virtualMassCoeff(fluid.virtualMassCoeff());
4 volVectorField liftForce(fluid.liftForce());
5 volVectorField wallLubricationForce(fluid.wallLubricationForce());
6 volVectorField turbulentDispersionForce(fluid.turbulentDispersionForce());

```

Listing 365: The definition of the interfacial momentum exchange force terms of the momentum conservation equations of `twoPhaseEulerFoam` in `UEqns.H`

55.7 Interfacial interaction

55.7.1 Blending

The interfacial momentum exchange models need to work over the whole range of flow situations. These range from $\alpha_1 = 0$ to $\alpha_1 = 1$. In order to well-posedness of the governing equations special care needs to be taken for the case of phase inversion.

There are three options for blending available: none, linear and hyperbolic.

```

// create x

if (model_.valid())
{
    x() += model_->K()(f1() - f2());
}

```

```

}

if (model1In2_.valid())
{
    x() += model1In2_->K()(1 - f1);
}

if (model2In1_.valid())
{
    x() += model2In1_->K()*f2;
}

// other code

return x;

```

Listing 366: The application of blending; part of the method K() in BlendedInterfacialModel.C

No Blending

The blending model `none`, which is defined in the files `noBlending.H` and `noBlending.C`, is quite instructive. This blending model, which is essentially a non-model, returns the blending factors `f1` and `f2` as it is demanded by the base class of all blending models.

As there is no blending with the `none` blending model, the user needs to specify which phase is the continuous phase. In `twoPhaseEulerFoam-2.3` there is no implicit assumption on which phase is the dispersed and which is continuous. Listing 367 shows how the `none` blending model is selected. There we also see the explicit specification of the continuous phase.

```

blending
{
    default
    {
        type      none;
        continuousPhase water;
    }
}

```

Listing 367: Choosing not to use blending as the blending method

Now, we have a look on the blending factors returned by the `none` model. Listing 368 shows the definition of the methods `f1()` and `f2()`. These methods return a newly created temporary scalar field (`volScalarField`) that is in turn created from a constant expression.

In the case of `f1()`, the constant expression is `phase2.name() != continuousPhase__` which returns a boolean value. In the case of `f2()` the corresponding expression is `phase1.name() == continuousPhase__`, which also returns a boolean value. Here, we enter the realm of implicit type conversions¹⁹¹. Implicit type conversions are part of the language's standard. Thus, if we look up the working draft of the C++11standard, we find the following sentence in the section on *Integral promotions*:

A prvalue of type `bool` can be converted to a prvalue of type `int`, with `false` becoming zero and `true` becoming one.

Thus, we find that the blending factors returned by `none` are of the values zero or one, which is the set of values we would expect in this case. If the boolean expressions yield the correct factors can be tried out with a simple *pen-and-paper test*. Choose a continuous phase (i.e. `phase2` is the continuous phase) and evaluate all expressions (i.e. determine the values of `f1` and `f2`, and apply these values on the expressions found in Listing 366.).

```

Foam::tmp<Foam::volScalarField> Foam::blendingMethods::noBlending::f1
(
    const phaseModel& phase1, const phaseModel& phase2
) const
{
    const fvMesh& mesh(phase1.mesh());

```

¹⁹¹See e.g. http://en.cppreference.com/w/cpp/language/implicit_cast

```

    return
    tmp<volScalarField>
    (
        new volScalarField
        (
            IOobject( /* arguments removed */ ),
            mesh,
            dimensionedScalar
            (
                "f",
                dimless,
                phase2.name() != continuousPhase_
            )
        );
    }
Foam::tmp<Foam::volScalarField> Foam::blendingMethods::noBlending::f2
(
    const phaseModel& phase1, const phaseModel& phase2
) const
{
    const fvMesh& mesh(phase1.mesh());

    return
    tmp<volScalarField>
    (
        new volScalarField
        (
            IOobject( /* arguments removed */ ),
            mesh,
            dimensionedScalar
            (
                "f",
                dimless,
                phase1.name() == continuousPhase_
            )
        );
}

```

Listing 368: Computing the blending factors. The arguments of the constructor of the `IOobject` class have been removed to save space.

Linear

As we saw from the `none` model, the blending factors `f1` and `f2` have two extreme values, i.e. zero and one. The model name `linear` suggests that this models yields a linear variation between these two limiting values.

The `linear` blending model has two model parameters, shown in Listing 369. These represent the limits up to which a phase can be considered to be fully dispersed, i.e. a clear distinction between dispersed phase and continuous phase is possible. The second parameter is the limit up to which the phases can be considered partly dispersed. These two limits are necessary, as the solver is intended to handle phase inversion, i.e. situations in which one phase is the dispersed phase in only parts of the domain.

The definition of the blending factor `f1` is shown in Listing 370. We limit the discussion on `f1`, as the other blending factor is defined analogously. The interested reader is encouraged to analyse `f2`. The code of Listing 370 can be translated into equation (150).

$$f_1(\alpha) = \begin{cases} 1 & \text{if } \alpha \leq \text{maxFullyDispersedAlpha} \\ \frac{\alpha - \text{maxFullyDispersedAlpha}}{\text{maxPartlyDispersedAlpha} - \text{maxFullyDispersedAlpha}} & \text{if } \alpha \leq \text{maxPartlyDispersedAlpha} \\ 0 & \text{if } \alpha > \text{maxPartlyDispersedAlpha} \end{cases} \quad (150)$$

```
//- Maximum fraction of phases which can be considered fully dispersed
HashTable<dimensionedScalar, word, word::hash>
maxFullyDispersedAlpha_;
```

```

//-- Maximum fraction of phases which can be considered partly dispersed
HashTable<dimensionedScalar, word, word::hash>
    maxPartlyDispersedAlpha_;

```

Listing 369: Model parameters of the linear blending model; declaration in the file `linear.H`

```

Foam::tmp<Foam::volScalarField> Foam::blendingMethods::linear::f1
(
    const phaseModel& phase1, const phaseModel& phase2
) const
{
    const dimensionedScalar
        maxFullAlpha(maxFullyDispersedAlpha_[phase1.name()]);
    const dimensionedScalar
        maxPartAlpha(maxPartlyDispersedAlpha_[phase1.name()]);

    return
        min
        (
            max
            (
                (phase1 - maxFullAlpha)
                /(maxPartAlpha - maxFullAlpha + SMALL),
                scalar(0.0)
            ),
            scalar(1.0)
        );
}

```

Listing 370: Computing the linear blending factor `f1` in the file `linear.C`

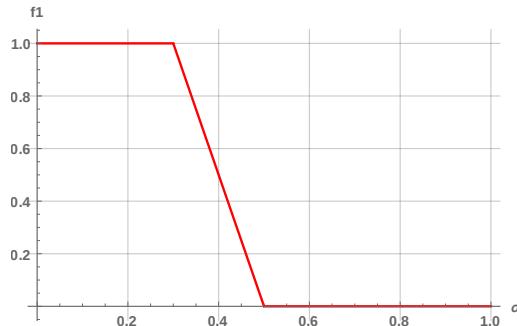


Figure 160: The value of `f1` over α ; model parameters are set to `maxFullAlpha` = 0.3 and `maxPartAlpha` = 0.5; these settings are taken from the *bubble column tutorial* case of *twoPhaseEulerFoam*.

Hyperbolic

The `hyperbolic` blending model offers a continuous function for the blending factor for the whole range of the dispersed phase's volume fraction, see Figure 161. Again, we analyse only the definition of `f1` and leave the reader the opportunity to follow the argument made, with the definition of `f2`.

The `hyperbolic` blending model needs in total three model parameters. The parameter `transitionAlphaScale` controls how steep the transition between 0 and 1 is. The other two parameters are `maxDispersedAlpha` for each phase. At this parameter the blending function (151) has the value $1/2$.

$$f_1(\alpha) = \frac{1}{2} \left(1 + \tanh \left(\frac{4(\alpha - \text{maxDispersedAlpha})}{\text{transitionAlphaScale}} \right) \right) \quad (151)$$

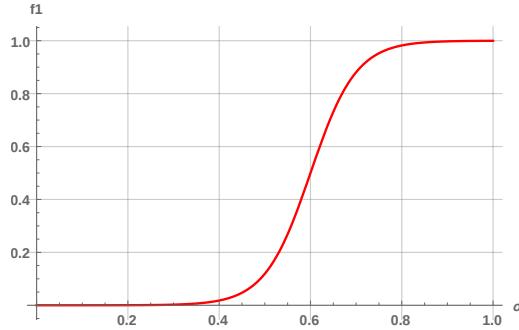


Figure 161: The value of f_1 over α ; model parameters are set to `maxDispersedAlpha = 0.6` and `transitionAlphaScale = 0.4`;

55.8 Interfacial momentum exchange

55.8.1 Drag

Units

From viewing the governing equations we saw, that the drag term consists of a coefficient and the relative velocity between the phases.

$$\mathbf{F}_{drag} = K_{pq,drag} (\mathbf{u}_p - \mathbf{u}_q) \quad (152)$$

We find the same structure in the terms of the implemented equations. The Listing below shows one part of the drag term – as the drag term consists of the coefficient and a velocity difference, we can split the term up into two contributing parts.

```
U1Eqn += fvm::Sp(dragCoeff, U1);
```

As we know from our considerations about the units of the terms of the momentum equation, the drag force contribution in general needs to have the unit of a force density. Thus, we determined the unit of the coefficient, see Eqn. (149).

$$[\text{dragCoeff}] = \frac{\text{kg}}{\text{m}^3 \text{s}} \quad (153)$$

By having a close look on the base class for the drag models, we can check the unit of the coefficient. The base class of the drag model has a static data member that carries the information about the unit of the provided coefficient. In fact, all interfacial momentum exchange models have such a member. In the header file of the base class for the drag models, a constant static member¹⁹² `dimK` is declared.

```
//- Coefficient dimensions
static const dimensionSet dimK;
```

In the implementation file, the static data member is initialised to the appropriate value. In Section 9 we reviewed OpenFOAM's feature to provide physical units. There we can see, that the order of units in a `dimensionSet` is [kg m s K mol].

```
const Foam::dimensionSet Foam::dragModel::dimK(1, -3, -1, 0, 0);
```

Thus, we see, that the drag force coefficient has indeed the unit we derived from our earlier considerations.

¹⁹²A static data member of a class exists only once for all instances of this class, i.e. regardless of how many actual objects of this class exist, the data member exists only once. This makes perfect sense for common properties such as the unit of the coefficient, which is the same for all drag models.

Returning the output

Other than the drag models of prior versions of *twoPhaseEulerFoam* (version 2.2 and below), the drag models in *twoPhaseEulerFoam-2.3* return the product of drag coefficient C_D and the Reynolds number Re . Consequently, the method returning the output of the individual drag models is named `CdRe()`.

The drag model itself, i.e. the base class returns the drag force coefficient K . This drag force coefficient is provided by the method `K()` which is a method of the base class `dragModel`. The base class also has a pure virtual method named `CdRe()`. Pure virtual means that derived classes need to implement this method and that we are unable to create an instance of the base class itself. We only can create instances of one of the derived classes. As a derived class must implement all pure virtual methods, we are guaranteed that these methods actually exist. The Listings 371 and 372 show the relevant parts of code of the class `dragModel`. The method `K()` calls the method `CdRe()`, see Line 5 of Listing 372.

```

1 // - Drag coefficient
2     virtual tmp<volScalarField> CdRe() const = 0;
3
4 // - The drag function K used in the momentum equation
5 //     ddt(alpha1*rho1*U1) + ... = ... K*(U1-U2)
6 //     ddt(alpha2*rho2*U2) + ... = ... K*(U2-U1)
7     virtual tmp<volScalarField> K() const;

```

Listing 371: The declaration of the methods `K()` and `CdRe()` in `dragModel.H`

```

1 Foam::tmp<Foam::volScalarField> Foam::dragModel::K() const
2 {
3     return
4         0.75
5     *CdRe()
6     *max(pair_.dispersed(), residualAlpha_)
7     *swarmCorrection_->Cs()
8     *pair_.continuous().rho_()
9     *pair_.continuous().nu_()
10    /sqr(pair_.dispersed().d());
11 }

```

Listing 372: The definition of the method `K()` in `dragModel.C`

If we translate Listing 372 into math we yield

$$K = \frac{3}{4} C_D Re \alpha C_S \frac{\rho_C \nu_C}{d_B^2} \quad (154)$$

Now, we insert the definition of the bubble Reynolds number

$$K = \frac{3}{4} C_D \frac{d_B U_R}{\nu_C} \alpha C_S \frac{\rho_C \nu_C}{d_B^2} \quad (155)$$

$$K = \frac{3}{4} \alpha C_S C_D \frac{\rho_C}{d_B} U_R \quad (156)$$

If we now take a look on the units

$$[K] = \left[\frac{\rho_C}{d_B} U_R \right] = \frac{\text{kg}}{\text{m}^3} \frac{1}{\text{m}} \frac{\text{m}}{\text{s}} = \frac{\text{kg}}{\text{m}^3 \text{s}} \quad (157)$$

Again, we find the proper physical unit for the drag force coefficient.

Here we show the definition of the method `CdRe()` from the class `SchillerNaumann` as an example since the Schiller Naumann drag model is well known.

```

1 Foam::tmp<Foam::volScalarField> Foam::dragModels::SchillerNaumann::CdRe() const
2 {
3     volScalarField Re(pair_.Re());
4
5     return

```

```

6     neg(Re - 1000)*24.0*(1.0 + 0.15*pow(Re, 0.687))
7     + pos(Re - 1000)*0.44*max(Re, residualRe_);
8 }

```

Listing 373: The relevant lines of code in `SchillerNaumann.C`

Swarm correction

The drag models offer swarm correction of the drag force, since it is observed that swarms of bubbles behave different from single bubbles. At the time of writing (September 2014) there are two choices.

noSwarm This model simply returns unity when `swarmCorrection_->Cs()` is called.

TomiyamaSwarm This model computes the swarm correction factor according to [63].

The Tomiyama swarm correction factor depends on the bubble volume fraction α and a model parameter l .

$$C_{S,Tomiyama} = (1 - \alpha)^{3-2l} \quad (158)$$

Both swarm correction models are derived from an abstract base class `swarmCorrection`. Thus the framework is ready for future extension of model choice.

55.8.2 Lift

The lift force on a dispersed phase element (DPE) is defined as

$$\mathbf{F}_L = C_L \alpha \rho_C (\mathbf{U}_R \times (\nabla \times \mathbf{U})) \quad (159)$$

with

C_L	lift force coefficient
α	volume fraction of the dispersed phase
ρ_C	density of the continuous phase
\mathbf{U}_R	relative velocity between the phases
\mathbf{U}	mixture velocity

Units

In contrast to the drag model, the lift model provides the actual force term for the governing equations. The base class of the lift models declares a static constant data member `dimF` for storing the unit of the force term computed by the list model.

```
//- Force dimensions
static const dimensionSet dimF;
```

In the implementation file `liftModel.C` the static data member is initialized and it has indeed the unit of a force density. Note: the order of units in a `dimensionSet` is [kg m s K mol].

$$[\mathbf{F}_i] = \frac{\text{N}}{\text{m}^3} = \frac{\text{kg}}{\text{m}^2 \text{s}^2} \quad (147)$$

```
const Foam::dimensionSet Foam::liftModel::dimF(1, -2, -2, 0, 0);
```

Returning the output

The general computation of the lift force is done – similar to the drag models – within the method `F()` of the base class. The base class calls the method `C1()` of the concrete lift model for the lift force coefficient. This is similar to the method `K()` of the drag model base class calling the method `CdRe()` of the concrete drag model classes.

The method `F()` of the base class returns the force density field due to the lift force.

```

1  //-- Lift coefficient
2  virtual tmp<volScalarField> C1() const = 0;
3
4  //-- Lift force
5  virtual tmp<volVectorField> F() const;
```

Listing 374: The declaration of the methods `F()` and `C1()` in `liftModel.H`

```

1 Foam::tmp<Foam::volVectorField> Foam::liftModel::F() const
2 {
3     return
4         C1()
5         *pair_.dispersed()
6         *pair_.continuous().rho()
7         *
8         pair_.Ur() ^ fvc::curl(pair_.continuous().U())
9     );
10 }
```

Listing 375: The definition of the method `F()` in `liftModel.H`

The actual lift force coefficient is provided by the concrete lift force model. Again, analogue to the drag model classes, the base class for the lift models declares the pure virtual method `C1()`. This means, every lift model derived from the base class has to implement `C1()` and we are not able to create an instance of the base class itself. Thus, the existence of the method `C1()` is guaranteed. The implementation of `C1()` is the remaining degree of freedom for the individual lift force models.

There are several choices available to the user:

noLift this model returns a zero field when either `F()` or `C1()` is called. This class overwrites the method `F()` which is inherited from the base class with its own implementation. Thus, when `F()` is called, the implementation of the class `noLift` is called, i.e. `noLift::F()`. All other lift force models do not implement `F()`, thus, `liftModel::F()` is called.

constantCoefficient this model is the easiest implementation of a lift force model. The constant lift force coefficient C_L is provided by the user. `C1()` simply returns this value in the form of the appropriate data type, i.e. the coefficient provided by the user is a dimensionless number (declared as `const dimensionedScalar C1_;`), however, the method `C1()` returns a `volScalarField`.

lift force model X there are several models available that compute the lift force coefficient from flow properties.

55.8.3 Virtual mass

The class structure for the virtual mass models follow the example of the drag and lift models. There is an abstract base class providing a method `F()` for the force term F_{VM} due to virtual mass. The force term due to virtual mass if defined as

$$F_{VM} = C_{VM} \alpha \rho_C \quad (160)$$

with

C_{VM}	virtual mass coefficient
α	volume fraction of the dispersed phase
ρ_C	density of the continuous phase

The derived classes provide the virtual mass coefficient C_{VM} via the method `Cvm()`. The user has the choice between:

noVirtualMass this class returns zero when `F()` is called. This model overwrites the method `F()` with its own implementation returning a zero field. All other classes make use of the base classes implementation of `F()` which all derived classes inherited. The method `Cvm()` also returns a zero field.

```
Foam::tmp<Foam::volScalarField>
Foam::virtualMassModels::noVirtualMass::K() const
{
    return Cvm()*dimensionedScalar("zero", dimDensity, 0);
}
```

constantVirtualMassCoefficient this class computes the contribution due to virtual mass based on a constant virtual mass coefficient C_{VM} which is provided by the user.

Lamb this model computes the virtual mass coefficient C_{VM} depending on the aspect ratio of the dispersed phase elements. With the help of aspect ratio models a particle shape different from spheres and even shape variation can be modelled within some limits.

55.8.4 Aspect ratio models

When dealing with non-spherical bubbles or particles, the shape has to be considered in the interfacial momentum exchange models. One way of dealing with this situation is to formulate those models to incorporate the aspect ratio of the dispersed phase elements.

Here, the aspect ratio models come into play. These compute the aspect ratio of the dispersed phase elements depending on material and possibly flow properties. However, the influence of shape can also be considered using other approaches.

The aspect ratio is used in the `TomiyamaAnalytic` drag model and the `Lamb` virtual mass model. The interested reader can find this out by invoking the following commands.

```
cd $FOAM_APP/solvers/multiphase/twoPhaseEulerFoam/interfacialModels
find -name *.C | xargs grep 'pair_.E()'
```

The second command is a combination of a `find` command and a `grep` command. `find` finds all files with the file extension `.C` and `grep` searches this files for the pattern `pair_.E()`. This pattern is the function call which returns the aspect ratio E of a phase pair.

55.8.5 Wall lubrication

The wall lubrication force pushes bubbles away from the walls. The class structure is similar to the aforementioned models. There is an abstract base class and derived classes implementing a specific model. The base class declares the pure virtual method `F()` which returns the force term due to wall lubrication. The derived class have to implement this method.

There is a derived class named `noWallLubrication` which simply implements the method `F()` in way to return a zero field. There are also three models computing the wall lubrication force.

55.8.6 Turbulent dispersion

Turbulent dispersion describes the effect of turbulent motion of the liquid phase on the gas phase. The models are also derived from an abstract base class. There is a class named `noTurbulentDispersion` which returns a zero field for the force term and there are a number of classes implementing individual models. The base class declares the method `F()` as a pure virtual method. This means there is no generic formulation as in the case of the drag or lift models.

constantTurbulentDispersionCoefficient

The constant coefficient model implements the following model for the force due to turbulent dispersion.

$$\mathbf{F}_{TD} = C_{TD}\alpha\rho_C k_C \nabla\alpha \quad (161)$$

with

C_{TD}	turbulent dispersion coefficient
α	volume fraction of the dispersed phase
ρ_C	density of the continuous phase
k_C	kinetic turbulent energy of the continuous phase

Burns

The Burns model implements the following model for the force due to turbulent dispersion.

$$\mathbf{F}_{TD} = K_{Drag} \frac{\nu_{C,t}}{\sigma} \nabla\alpha \left(1 + \frac{\alpha}{1 - \alpha} \right) \quad (162)$$

with

K_{Drag}	drag force coefficient due to drag
α	volume fraction of the dispersed phase
$\nu_{C,t}$	turbulent viscosity of the continuous phase
σ	surface tension

Note that K_{drag} is not evaluated by calling method `K()` of the class `dragModel`. Listing 376 shows the actual code that computes the force term of the Burns model.

The reason for computing the drag force coefficient K “by hand” rather than calling `dragModel::K()` might be the run-time. By not calling `K()` we can save one virtual function call¹⁹³. The operations to compute K have to be done anyway, so there is a net saving of one virtual function call.

```

1  Foam::tmp<Foam::volVectorField>
2  Foam::turbulentDispersionModels::Burns::F() const
3  {
4      const fvMesh& mesh(pair_.phase1().mesh());
5      const dragModel&
6          drag
7          (
8              mesh.lookupObject<dragModel>
9              (
10                  IOobject::groupName(dragModel::typeName, pair_.name())
11              )
12          );
13
14      return
15      - 0.75
16      *drag.CdRe()
17      *pair_.dispersed()
18      *pair_.continuous().nu()
19      *pair_.continuous().turbulence().nut()
20      /(
21          sigma_
22          *sqr(pair_.dispersed().d())
23      )
24      *pair_.continuous().rho()
25      *fvc::grad(pair_.continuous())
26      *(1.0 + pair_.dispersed()/max(pair_.continuous(), residualAlpha_));
27 }
```

Listing 376: The definition of the method `F()` in the file `Burns.C`

¹⁹³Virtual function calls are considered to be more expensive in terms of run-time than direct function calls, since the correct function to call has to be determined at run-time [25].

Gosman

The Gosman model implements the following model for the force due to turbulent dispersion.

$$\mathbf{F}_{TD} = K_{Drag} \frac{\nu_{C,t}}{\sigma} \nabla \alpha \quad (163)$$

55.9 MRF method - avoiding errors

The MRF method can be used to simulate stirred vessels. By the time of writing, this is the only way to do so with the Eulerian multiphase solvers, since none of the Eulerian solvers has dynamic mesh capability. The basics behind the MRF method are discussed in Section 77.

55.9.1 Inlet boundaries and MRF zones

The MRF method corrects the velocities at the boundaries within the MRF zone. Thus, if a gas inlet BC is placed within the MRF zone, the simulation takes an unintended route. In Figure 162 we see the outcome of a gas inlet boundary placed within an MRF zone. Note, the tangential alignment of the velocity vectors on the right image. The initial inlet definition (visible on the left image) is overridden by the MRF's constraint.

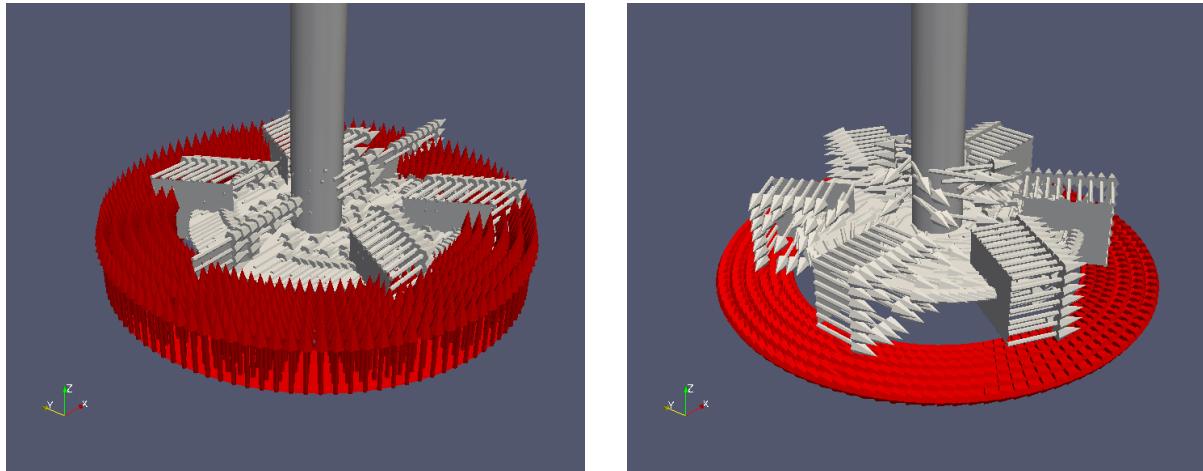


Figure 162: Velocity vectors of the gaseous phase at the inlet boundary (red vectors) in an aerated stirred tank. That the gas inlet boundary lies within the MRF zone. On the left, we see the initial condition and on the right we see the boundary condition after the constraints by the MRF method have been applied.

56 reactingTwoPhaseEulerFoam

With the release of OpenFOAM-3.0.0¹⁹⁴ in 2015 the solvers *reactingTwoPhaseEulerFoam* and *reactingMultiphaseEulerFoam* were introduced. These solvers feature expanded modelling capabilities compared to the ancestors *twoPhaseEulerFoam* and *multiphaseEulerFoam*. These two solvers are one of the results of a collaboration of companies from the chemical and process industries, and the makers of OpenFOAM¹⁹⁵.

reactingTwoPhaseEulerFoam and *reactingMultiphaseEulerFoam* form the reactingEulerFoam family of Euler-Euler solvers. These two solvers use a largely common code base for underlying models, such as phase-models, interfacial momentum-transfer models and interfacial composition models. Many of the developments that went into the evolution of the *twoPhaseEulerFoam* solver from OpenFOAM-2.2 and earlier to OpenFOAM-2.3 have been continued and led to a further generalization of the code base.

Since both solvers derive from a largely common code base, this section mostly applies to both *reactingTwoPhaseEulerFoam* and *reactingMultiphaseEulerFoam*.

56.1 Solver basics

This solver uses the PIMPLE algorithm for solving the governing equations for the two-phase flow.

56.2 Phase modelling

The code base of the phase modelling library is a good example of the principles of encapsulation, abstraction and generic programming at work.

56.2.1 Phase model classes

There is a number of phase-model template classes, each implementing a different aspect of multi-phase modelling, e.g. momentum-transfer, heat-transfer, etc.. Thus, for a specific model a number of these templates has to be nested in a similar fashion as Lagrangian particle models are constructed by plugging template classes into each other.

The class templates, which provide modelling of a certain aspect, can also have an opposite twin-implementation. This allows to construct phase models which either include a certain aspect, or not, by selecting a certain set of templates at compile-time. One example for such a twin-implementation is the aspect of reactions. A phase can either be a reacting one, or an inert one. Thus, there are two template classes dealing with reactions: the templates *InertPhaseModel* and *ReactingPhaseModel*. The name of the template class is quite suggestive to as how each class implements this aspect.

phaseModel

This is the base class for all phase models, and it defines the behaviour of a phase. This class is itself derived from the class *volScalarField*. Thus, the phase model is its own volume fraction field. This class holds very little data, apart from the phase's index, its name and a pointer to the phase's diameter model.

However, this class defines a large number of abstract methods, which the various template classes need to implement.

MovingPhaseModel

This class template provides the functionality and the data for a moving phase, i.e. it holds the velocity field and the flux fields. This class also provides a momentum equation for the phase. This class also holds a pointer to the turbulence model.

```
1 template<class BasePhaseModel>
2 Foam::tmp<Foam::fvVectorMatrix>
3 Foam::MovingPhaseModel<BasePhaseModel>::UEqn()
4 {
5     const volScalarField& alpha = *this;
6     const volScalarField& rho = this->thermo().rho();
7 }
```

¹⁹⁴<https://openfoam.org/release/3-0-0/>

¹⁹⁵<https://openfoam.org/chemical-process-engineering/>

```

8     return
9     (
10        fvm::ddt(alpha, rho, U_)
11        + fvm::div(alphaPhi_, U_)
12        + fvm::SuSp(- this->continuityError(), U_)
13        + this->fluid().MRF().DDt(alpha*rho, U_)
14        + turbulence_->divDevRhoReff(U_)
15    );
16 }

```

Listing 377: Constructing the momentum equation of a moving phase in the class `MovingPhaseModel`

The momentum equation provided by this class template bears a striking resemblance to the momentum equation of a compressible solver. If we compare the Listings 377 and 378, we recognize the four of the five terms from Listing 377 as the RHS of the momentum equation of Listing 378. The only difference is, that the terms of the multi-phase momentum equation contain the volume fraction field `alpha`, which takes a uniform value of 1 in the single-phase solver.

```

1 tmp<fvVectorMatrix> tUEqn
2 (
3     fvm::ddt(rho, U)
4     + fvm::div(phi, U)
5     + MRF.DDt(rho, U)
6     + turbulence->divDevRhoReff(U)
7     ==
8     fvOptions(rho, U)
9 );

```

Listing 378: Constructing the momentum equation of a compressible, single-phase solver, on the example of `rhoPimpleFoam`

As the list of options is read and created by the solver, the phase model is oblivious to the presence of any options. Thus, there are no calls to the `fvOptions` framework within the phase models. This is a task for the solver to deal with options from the `fvOptions` framework.

AnisothermalPhaseModel

This class template provides the data and the methods necessary to implement energy transfer, i.e. an energy equation.

IsothermalPhaseModel

This class is the counterpart of the `AnisothermalPhaseModel`, it implements all abstract methods associated with the transport of thermal energy in a trivial manner.

MultiComponentPhaseModel

This template class provides the data and methods associated with species transport within a phase, e.g. the gas phase consisting of several gases.

PurePhaseModel

This template class is used for phases that consist of a single species. Thus there is no need to solve species transport equations. Hence, this class template implements all abstract methods defined in the base class `phaseModel` in a trivial manner, e.g. it returns an empty list of mass fractions when the method `phaseModel::Y()` is called, which is intended to return the species mass fractions.

InertPhaseModel

This template class is used for non-reactive phases, and it implements all methods dealing with reactions in a trivial way. Thus, it returns zero for the heat release rate and the mass transfer rate.

ReactingPhaseModel

This template class is used for reactive phases. Thus, the heat release rate and the mass transfer rate are computed by the underlying reaction model and returned.

56.2.2 Phase system classes

56.2.3 Solution

Phase transport

Solving the transport equation for a phase is handled by the concrete phase system class, e.g. by `twoPhaseSystem` in the case of `reactingTwoPhaseEulerFoam`. This is implemented by the method `solve()` of the phase system class.

Momentum, energy and species transport

Solving the momentum, energy and species transport equations is handled by the solvers itself. The phase models and the phase system models provide the transport equations and transfer terms.

In Listing 379 we see a snippet of `reactingTwoPhaseEulerFoam`'s source code, which deals with the construction of the momentum equation for one phase. This is also an example of the interaction of phase models and phase system models. The LHS of the momentum equation is provided by the phase model, note the call to `phase1.UEqn()`. This call is actually implemented in the template `MovingPhaseModel`, which we see in Listing 377. This template class provides the local derivative, the convective term, a phase-conservation correction, a correction from the MRF framework and the momentum diffusion term.

The RHS of the momentum equation in Listing 379 is a momentum transfer term and a contribution from the `fvOptions` framework. The momentum transfer term is provided by the phase system model.

```
1 U1Eqn =
2 (
3     phase1.UEqn()
4     ==
5     *momentumTransfer[phase1.name()]
6     + fvOptions(alpha1, rho1, U1)
7 );
8 U1Eqn.relax();
9 fvOptions.constrain(U1Eqn);
10 fvOptions.correct(U1);
```

Listing 379: Constructing the momentum equation of the first phase in `reactingTwoPhaseEulerFoam`

56.3 Turbulence modelling

`reactingTwoPhaseEulerFoam` supports per-phase turbulence modelling, which also allows to treat a phase as laminar, as laminar modelling can be seen as a special case of turbulence modelling. By setting both phases to `mixtureKEpsilon`, a turbulence model for the mixture can be solved, with this specific model being the only option. Thus, all modelling strategies discussed in Section 42.3.1 are available with this solver.

56.4 Interfacial momentum exchange

57 multiphaseEulerFoam

`multiphaseEulerFoam` is an Eulerian solver for n phases. This solver differs in some points from the solver `twoPhaseEulerFoam`.

57.1 Fields

The naming scheme of the fields differs from other multiphase solvers. `multiphaseEulerFoam` directly uses names (e.g. Uair, Uwater, Uoil, etc.).

57.1.1 `alphas`

A specialty of `multiphaseEulerFoam` is the field `alphas`. This field does not represent the volume fraction of a certain phase and is therefore not bounded by 0 and 1. This field is used to represent all phases in a single scalar field. `alphas` is computed by summing up the products of phase index and phase fraction.

$$\text{alphas} = \sum_{i=0}^{n-1} i * \alpha_i \quad (164)$$

Because `alphas` is computed quantity, the file `alphas` can be missing in the `0`-directory.

57.2 Momentum exchange

The parameters for the momentum exchange, e.g. the drag model, need to be specified pair-wise.

57.2.1 `drag`

```
drag
(
    (air water)
    {
        type blended;

        air
        {
            type SchillerNaumann;
            residualPhaseFraction 0;
            residualSlip 0;
        }

        water
        {
            type SchillerNaumann;
            residualPhaseFraction 0;
            residualSlip 0;
        }

        residualPhaseFraction 1e-2;
        residualSlip 1e-2;
    }
)

/* further definitions */
```

Listing 380: Pair-wise definition of the drag model in the file `transportProperties`

57.2.2 `virtual mass`

The coefficients for considering virtual mass must also be specified pair-wise. Listing 381 shows how the coefficients for virtual mass are specified in the `damBreak` tutorial.

```
virtualMass
(
    (air water)      0.5
    (air oil)        0.5
    (air mercury)   0.5
    (water oil)      0.5
    (water mercury) 0.5
    (oil mercury)   0.5
);
```

Listing 381: Pair-wise definition of Coefficients for virtual mass in the file `transportProperties`

57.2.3 `lift force`

Currently (OpenFOAM 2.1.1) there is no lift model in `multiphaseEulerFoam`.

58 *driftFluxFoam*

`driftFluxFoam` is a solver of OpenFOAM to simulate e.g. settling of disperse particles in a liquid. `driftFluxFoam` is the successor of `settlingFoam`, which has been discontinued with the release of OpenFOAM-2.3.1¹⁹⁶. `settlingFoam` was used by Brennan [14] in his thesis, which contains a lot of information on deriving the drift flux model from the Eulerian two-fluid model equations. The header of `driftFluxFoam` describes this solver as follows:

Solver for 2 incompressible fluids using the mixture approach with the drift-flux approximation for relative motion of the phases.

Used for simulating the settling of the dispersed phase and other similar separation problems.

`driftFluxFoam` complies with the generic solver design of OpenFOAM, thus this solver can use all available turbulence models. It also can use the MRF method and the *fvOptions* framework.

58.1 Governing equations

The governing equations for the mixture are derived from the two-fluid model [14, 33].

58.1.1 Mixture continuity equation

The mixture continuity equation can be easily derived by adding the continuity equations of the two phases:

$$\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) = 0 \quad (165)$$

with the constitutive relations

$$\rho_m = \alpha_1 \rho_1 + \alpha_2 \rho_2 \quad (166)$$

$$\rho_m \mathbf{u}_m = \alpha_1 \rho_1 \mathbf{u}_1 + \alpha_2 \rho_2 \mathbf{u}_2 \quad (167)$$

we gain

$$\frac{\partial \rho_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m) = 0 \quad (168)$$

58.1.2 Mixture momentum equation

Derivation from literature

The derivation of the mixture momentum equation is analogous to the derivation of the mixture continuity equation. Therefore, we skip the general derivation and refer the interested reader to the appropriate literature [14, 33]. In this section, we want to focus on the derivation of the specific equations implemented in `driftFluxFoam`.

We start from the derivation given in the appendix of Brennan [14]:

$$\frac{\partial \rho_m \mathbf{u}_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}_m \mathbf{u}_m) = -\nabla p_m + \nabla \cdot \left(\boldsymbol{\tau} + \boldsymbol{\tau}_t - \sum \alpha_k \rho_k \mathbf{u}_{km} \mathbf{u}_{km} \right) + \rho_m \mathbf{g} + \mathbf{M}_k \quad (169)$$

we pay special attention to the diffusion stress $\sum \alpha_k \rho_k \mathbf{u}_{km} \mathbf{u}_{km}$, which represents momentum diffusion due to the relative motion between the phases.

$$\sum \alpha_k \rho_k \mathbf{u}_{km} \mathbf{u}_{km} = \alpha_1 \rho_1 \mathbf{u}_{1m} \mathbf{u}_{1m} + \alpha_2 \rho_2 \mathbf{u}_{2m} \mathbf{u}_{2m} \quad (170)$$

For convenience we introduce the symbol $\boldsymbol{\tau}_{dm}$ for the diffusion stress

$$\boldsymbol{\tau}_{dm} = \sum \alpha_k \rho_k \mathbf{u}_{km} \mathbf{u}_{km} \quad (171)$$

¹⁹⁶<http://www.openfoam.org/version2.3.1/>

with \mathbf{u}_{km} , the velocity of the phase k relative to the mixture's centre of mass; \mathbf{u}_{km} is also referred to as *diffusion velocity* of the phase k

$$\mathbf{u}_{km} = \mathbf{u}_k - \mathbf{u}_m \quad (172)$$

Ishii and Hibiki [33] states a relation between the diffusion velocities of the two phases:

$$\alpha_1 \rho_1 \mathbf{u}_{1m} + \alpha_2 \rho_2 \mathbf{u}_{2m} = \mathbf{0} \quad (173)$$

Thus, we can eliminate \mathbf{u}_{1m} from the diffusion stress τ_{dm}

$$\tau_{dm} = \alpha_1 \rho_1 \left(\frac{\alpha_2 \rho_2}{\alpha_1 \rho_1} \right)^2 \mathbf{u}_{2m}^2 + \alpha_2 \rho_2 \mathbf{u}_{2m}^2 \quad (174)$$

$$\tau_{dm} = \alpha_2 \rho_2 \mathbf{u}_{2m}^2 \left(\frac{\alpha_2 \rho_2}{\alpha_1 \rho_1} + 1 \right) \quad (175)$$

$$\tau_{dm} = \alpha_2 \rho_2 \mathbf{u}_{2m}^2 \left(\frac{\alpha_2 \rho_2 + \alpha_1 \rho_1}{\alpha_1 \rho_1} \right) \quad (176)$$

$$\tau_{dm} = \alpha_2 \rho_2 \mathbf{u}_{2m}^2 \left(\frac{\rho_m}{\alpha_1 \rho_1} \right) \quad (177)$$

$$\tau_{dm} = \rho_m \frac{\alpha_2}{\alpha_1} \frac{\rho_2}{\rho_1} \mathbf{u}_{2m}^2 \quad (178)$$

Implementation

From the source code in Listing 382 we see the diffusion stress an the fourth term on the LHS of the momentum equation.

```

1 fvVectorMatrix UEqn
2 (
3     fvm::ddt(rho, U)
4     + fvm::div(rhoPhi, U)
5     + MRF.DDt(rho, U)
6     + fvc::div(UdmModel.tauDm())
7     + turbulence->divDevRhoReff(U)
8 ===
9     fvOptions(rho, U)
10 );

```

Listing 382: The momentum equation of `driftFluxFoam`

Next, we take a look at the implementation of the diffusion stress.

```

1 tmp<volSymmTensorField> Foam::relativeVelocityModel::tauDm() const
2 {
3     volScalarField betac(alphac_*rhoc_);
4     volScalarField betad(alphad_*rhod_);
5
6     // Calculate the relative velocity of the continuous phase w.r.t the mean
7     volVectorField Ucm(betad*Udm_/betac);
8
9     return tmp<volSymmTensorField>
10    (
11        new volSymmTensorField
12        (
13            "tauDm",
14            betad*sqr(Udm_) + betac*sqr(Ucm)
15        )
16    );
17 }

```

Listing 383: The diffusion stress of `driftFluxFoam` computed by the `relativeVelocityModel`

And now, we translate the source code into some math:

$$\tau_{bm} = \beta_d \mathbf{u}_{dm}^2 + \beta_c \mathbf{u}_{cm}^2 \quad (179)$$

with

$$\beta_d = \alpha_d \rho_d \quad (180)$$

$$\beta_c = \alpha_c \rho_c \quad (181)$$

$$\mathbf{u}_{cm} = \frac{\beta_d}{\beta_c} \mathbf{u}_{dm} \quad (182)$$

we gain

$$\tau_{bm} = \beta_d \mathbf{u}_{dm}^2 + \beta_c \left(\frac{\beta_d}{\beta_c} \right)^2 \mathbf{u}_{dm}^2 \quad (183)$$

$$\tau_{bm} = \beta_d \mathbf{u}_{dm}^2 \left(1 + \frac{\beta_d}{\beta_c} \right) \quad (184)$$

$$\tau_{bm} = \alpha_d \rho_d \mathbf{u}_{dm}^2 \left(1 + \frac{\alpha_d \rho_d}{\alpha_c \rho_c} \right) \quad (185)$$

$$\tau_{bm} = \alpha_d \rho_d \mathbf{u}_{dm}^2 \left(\frac{\alpha_c \rho_c + \alpha_d \rho_d}{\alpha_c \rho_c} \right) \quad (186)$$

$$\tau_{bm} = \alpha_d \rho_d \mathbf{u}_{dm}^2 \frac{\rho_m}{\alpha_c \rho_c} \quad (187)$$

$$\tau_{bm} = \rho_m \frac{\alpha_d \rho_d}{\alpha_c \rho_c} \mathbf{u}_{dm}^2 \quad (188)$$

We notice, that (188) derived from the source code, equals (178), derived from literature with phase 2 being the disperse phase d .

Relative velocity

The diffusion velocity \mathbf{u}_{dm} and the drift velocity \mathbf{u}_{dj} are linked by a constitutive relation:

$$\mathbf{u}_{dm} = \frac{\rho_1}{\rho_m} \mathbf{u}_{dj} \quad (189)$$

We find this relation also in the source code in Listings 388 and 389. Ishii and Hibiki [33] state, that in the case of dispersed two-phase flow the drag correlation should be expressed in terms of the drift velocity \mathbf{u}_{dj} .

The relative velocity models provide a method that returns \mathbf{u}_{dm} , however, in the source code of the Listings 388 and 389 we find relation (189) translated into C++. There, the expression for \mathbf{u}_{dm} consists of the density ratio and a relation for the drift velocity, which links the terminal velocity of a single particle and the volume fraction of the disperse phase.

58.2 incompressibleTwoPhaseInteractingMixture

The class `incompressibleTwoPhaseInteractingMixture` serves as the transport model for `driftFluxFoam`. This class holds all the information of the two phases and provides the mixture quantities. `driftFluxFoam` solves the momentum and pressure equations for the mixture. Thus, this solver is in between a single-phase solver and a full two-fluid solver such as `twoPhaseEulerFoam`.

Via this transport model, the mixture quantities propagate to the turbulence model, since the turbulence model receives a transport model class as template parameter at construction. This is one example for the versatility of the new, templated turbulence modelling framework. The precursor `settlingFoam` had a hard-coded $k - \epsilon$ turbulence model. Also the viscosity model was kind of hard-coded.

58.3 Mixture viscosity models

Settling equipment is often operated with solids concentrations at which the presence of the solid particles affect fluid properties. Besides using the mixture density, a mixture viscosity also has to be used.

58.3.1 mixtureViscosityModel

The class `mixtureViscosityModel` is the abstract base class for the actual viscosity models. This class serves a similar purpose as the base class for the single-phase viscosity models `viscosityModel` located in `$FOAM_SRC/transportModels/incompressible/viscosityModels/viscosityModel`. These two base classes are rather similar and there are only slight differences in their implementations.

58.3.2 slurry

The `slurry` mixture viscosity model is a correction for the Newtonian viscosity with reference to Thomas [62].

$$\mu = \mu_c (1 + 2.5\alpha_d + 10.05\alpha_d^2 + 0.00273 e^{16.6\alpha}) \quad (190)$$

The source code computing the mixture viscosity is a direct translation of the math above into C++.

```
1 Foam::tmp<Foam::volScalarField>
2 Foam::mixtureViscosityModels::slurry::mu(const volScalarField& muc) const
3 {
4     return
5     (
6         muc*(1.0 + 2.5*alpha_ + 10.05*sqr(alpha_) + 0.00273*exp(16.6*alpha_))
7     );
8 }
```

Listing 384: The calculation of the mixture viscosity by the `slurry` mixture viscosity model.

58.3.3 plastic

The plastic viscosity model is based on a generic viscosity model (191) for liquids exhibiting plastic behaviour.

$$\tau = aC^b \alpha \quad (191)$$

The `plastic` model implemented in `driftFluxFoam` translates to:

$$\mu = \min [\mu_c + k * (10^{n\alpha} - 1), \mu_{max}] \quad (192)$$

Listing 385 shows the source code computing the mixture viscosity. The `-1` in the second term ensures, that we retain the laminar viscosity of the continuous phase in the case the dispersed volume fraction vanishes, since anything to the power of zero equals one.

```
1 Foam::tmp<Foam::volScalarField>
2 Foam::mixtureViscosityModels::plastic::mu(const volScalarField& muc) const
3 {
4     return min
5     (
6         muc
7         + plasticViscosityCoeff_
8         *(
9             pow
10            (
11                scalar(10),
12                plasticViscosityExponent_*alpha_
13            ) - scalar(1)
14        ),
15        muMax_
16    );
17 }
```

Listing 385: The calculation of the mixture viscosity by the `plastic` mixture viscosity model.

58.3.4 BinghamPlastic

`BinghamPlastic` is a Bingham plastic model.

58.4 Relative velocity models - hindered settling

In this section we use the symbol v for the velocity to follow the notation of Brennan [14] as well as the source code of OpenFOAM.

58.4.1 The base class

The base class holds the data common to the derived models. The base class holds the private field `Udm_` for the diffusion velocity \mathbf{u}_{dm} and declares an abstract method `correct()`. The method `correct()` is used by the derived classes to compute the diffusion velocity `Udm_`.

The method `Udm()` of the base class simply returns `Udm_`, and the method `tauDm()` returns the diffusion stress computed from the diffusion velocity.

The diffusion velocity

The class for the relative velocity model holds a vector field for the diffusion velocity. The internal field values are determined from the actual model in use, however, the boundary conditions are taken over from the mixture velocity field.

This, we can read from the source code of the base class. In Listing 386 we see the initializer responsible for the diffusion velocity.

```
1 Udm_
2 (
3     IOobject
4     (
5         "Udm",
6         alphac_.time().timeName(),
7         alphac_.mesh(),
8         IOobject::NO_READ,
9         IOobject::AUTO_WRITE
10    ),
11    alphac_.mesh(),
12    dimensionedVector("Udm", dimVelocity, vector::zero),
13    mixture.U().boundaryField().types()
14 )
```

Listing 386: The initializer entry for `Udm_` in the constructor of the `relativeVelocityModel` class.

For the interpretation of Listing 386 we need to dig out the appropriate constructor of the class `GeometricField`¹⁹⁷. In Listing 387 we see that the constructor receives five arguments, of which the last has a default value. If we pass only four arguments, the fifth will be determined from the default value.

```
1 // Constructor given IOobject, mesh, dimensioned<Type> and patch types.
2 GeometricField
3 (
4     const IOobject&,
5     const Mesh&,
6     const dimensioned<Type>&,
7     const wordList& wantedPatchTypes,
8     const wordList& actualPatchTypes = wordList()
9 );
```

Listing 387: The signature of the constructor called by the code in Listing 386.

If we compare the arguments of the constructor call of Listing 386 and the signature in Listing 387, we see that the first argument passed is clearly an `IOobject`. The second argument is a reference to the mesh itself, which is obvious from the call to `alphac_.mesh()` in Listing 386.

The third argument determines the type of the field as well as the initial value. The template parameter `Type` determines whether the field is a scalar, a vector or a tensor field. As a `dimensionedVector` is passed in Listing 386, `Type` evaluates to `vector`¹⁹⁸.

¹⁹⁷Bear in mind, that `volVectorField` and others are specialisations of the templated class `GeometricField`.

¹⁹⁸Bear in mind, that `dimensionedVector` is a specialisation of the templated class `dimensioned<Type>` and `dimensionedVector` is a shorthand for `dimensioned<vector>`.

The fourth argument is a list of patch types, since we passed only one dimensioned value as the third argument, there has been no information passed on the boundary conditions of the field up to now. By passing the list of boundary types of the mixture velocity field (`mixture.U()`), the boundary conditions of the field `Udm_` are specified.

As there is no fifth argument passed in Listing 386, the return value of the call `wordList()` is used.

58.4.2 simple

The model named `simple` is similar to the model used by Brennan [14] with attribution to Dahl [19]. This model is very similar to the Vesilind [67] model (194), Brennan [14] explains the change of the base from the Euler number e to the base 10 with a closer fit to experimental data gathered by Dahl [19].

$$v_s = v_0 10^{-k\alpha} \quad (193)$$

The implementation of the `simple` model is more or less a direct translation from math (193) to C++. In the exponent the maximum of the dispersed volume fraction and zero is taken to avoid numerical trouble from negative values of the volume fraction. Reversing the sign in an exponent is never a good idea in numerical simulation.

```

1 void Foam::relativeVelocityModels::simple::correct()
2 {
3     Udm_ = (rhoc_/rho_)*V0_*pow(scalar(10), -a_*max(alphad_, scalar(0)));
4 }
```

Listing 388: The calculation of the dispersed diffusion velocity `Udm_` by the `simple` relative velocity model.

58.4.3 general

The model referred to as `general` is most probably based on the model of Takács [61], there is no reference to any literature in the header file. The Takács [61] model (195) is a so-called double-exponential model based on the model of Vesilind [67], see (194) [30, 14].

$$v_s = v_0 e^{-nX} \quad (194)$$

$$v_s = v_0 (e^{-r_h X} - e^{-r_p X}) \quad (195)$$

with

v_s	settling velocity	
v_0	maximum settling velocity	
n	model parameter	(196)
r_h	settling parameter for hindered settling	
r_p	settling parameter for low solids concentration	
X	suspended solids concentration	

The implementation .

```

1 void Foam::relativeVelocityModels::general::correct()
2 {
3     Udm_ =
4         (rhoc_/rho_)
5         *V0_
6         *(
7             exp(-a_*max(alphad_ - residualAlpha_, scalar(0)))
8             - exp(-a1_*max(alphad_ - residualAlpha_, scalar(0)))
9         );
10 }
```

Listing 389: The calculation of the dispersed diffusion velocity `Udm_` by the `general` relative velocity model.

58.5 settlingFoam

Here we take a closer look on `settlingFoam` (of OpenFOAM-2.2.x), which is the predecessor of `driftFluxFoam`. By comparing the implementations of these two solvers we can observe the transition of the OpenFOAM source code base to a more encapsulated approach.

58.5.1 Mixture viscosity

`settlingFoam` was/is restricted to the plastic or Bingham viscosity models. Listing 390 shows the code of `settlingFoam`, which computes the mixture viscosity. This code is located in a source file, which is included into the body of the PIMPLE loop of the solver.

Thus, for this solver, the treatment of mixture viscosity is not encapsulated. The viscosity models are not located in separate files and the code of the solver itself contains all the knowledge of the viscosity models. Extending the solver with one or more mixture viscosity models would entail building an extended `if`-cascade within the file `correctViscosity.H`.

```
1  {
2      /* compute plastic viscosity */
3      mul = muc +
4          plasticViscosity
5          (
6              /* code removed for brevity */
7          );
8
9      if (BinghamPlastic)
10     {
11         volScalarField tauy = yieldStress
12         (
13             /* see yieldStress.H */
14         );
15         mul =
16             /* compute contribution of yield stress */
17             + mul;
18     }
19
20     mul = min(mul, muMax);
21 }
```

Listing 390: The calculation of the mixture viscosity in the file `correctViscosity.H` of `settlingFoam` of OpenFOAM-2.2.x. Comments added by the author.

58.5.2 Relative velocity models

`settlingFoam` of OpenFOAM-2.2.x offers the same choice of relative velocity models as `driftFluxFoam` at the time of writing. However, implementation-wise we note, that model selection is, again, done in an `if`-statement cascade.

```
1  if (VdjModel == "general")
2  {
3      Vdj = V0*
4      (
5          exp(-a*max(alpha - alphaMin, scalar(0)))
6          - exp(-a1*max(alpha - alphaMin, scalar(0)))
7      );
8  }
9  else if (VdjModel == "simple")
10 {
11     Vdj = V0*pow(10.0, -a*alpha);
12 }
13 else
14 {
15     FatalErrorIn(args.executable())
16         << "Unknown VdjModel : " << VdjModel
17         << abort(FatalError);
18 }
```

```
19  
20 Vdj.correctBoundaryConditions();
```

Listing 391: The calculation of the relative velocity in the file `calcVdj.H` of `settlingFoam` of OpenFOAM-2.2.x.

58.5.3 Turbulence

Turbulence in `settlingFoam` was/is implemented in a similar fashion as in `twoPhaseEulerFoam` of that time. Both solvers feature a hard-coded $k - \epsilon$ turbulence model, which is adapted to the solvers needs.

Part VI

Postprocessing

There are two principal possibilities for post processing in OpenFOAM. First, there are tools that are executed after a simulation has finished. These tools work on the written data of the solution. *sample* and *paraView* are two examples for such tools.

Besides that, there is *run-time post processing*. Run-time post processing performs certain operations on the solution data as it is generated. Consequently, run-time post processing allows for a much finer time resolution. The functions objects – e.g. for calculating forces or force coefficients – are an example for run-time post processing. The big disadvantage of this method is, that the user has to know the intended post processing steps before starting a simulation. See <http://www.openfoam.com/features/runtime-postprocessing.php> for more information about run-time post processing.

59 *functions*

A function objects - in general - are objects, which are used in a similar manner as a function. This main benefit of function objects is that they can have a permanent state. This state can be used to store data between “calls” of the function object. A very illustrative example is OpenFOAM’s function object *fieldAverage*, which computes the temporal average of fields. This function object needs to update itself with every time step computed and the current time-averaged fields need to be preserved between “calls” of *fieldAverage*.

Function objects usually serve one specific purpose, e.g. compute the time average of a field quantity. Thus, there is a large, ever growing number of function objects available in OpenFOAM. Some of which are listed below to give an impression of the wide range of tasks currently covered by OpenFOAM’s function objects:

fieldAverage compute the temporal average of field quantities

the fieldValue family compute the spatial average (or other operations) of field quantities

forces compute the forces on a body (surface)

forceCoeffs compute force coefficients, e.g. for drag, lift and torque

sampledSet save the field values of a certain region, e.g. along a line

probes save field values at certain points

streamLine compute streamlines

scalarTransport solve a passive scalar transport equation

codedFunctionObject implement your own function object in a not-entirely-from-scratch framework

The list above is only a small selection of available functions. Check out OpenFOAM’s sources for a complete overview on available function objects¹⁹⁹.

59.1 Stay up to date

Run-time post-processing with function objects is a feature of OpenFOAM which is very much in the realm of application and daily use, in contrast to the inner workings of the mesh class. Thus, function objects receive much attention from the developers in form addition of new function objects, extending the features of existing function objects or reorganizing and renaming existing function objects.

The first two points (addition and extension) are clearly for the benefit of the users, whereas the latter one (reorganisation) most probably benefits the developers in reducing code duplication or easing maintenance. Reorganisation might go hand in hand with renaming of function objects²⁰⁰. In such a case you might need to modify the function object definitions of your cases when migrating them to a newer²⁰¹ version.

Apart from all the other benefits of using the latest version of OpenFOAM, especially when it comes to function objects, you might be able to save yourself from developing a function object for your needs, if a newer version of OpenFOAM already contains a function object implementing the functionality you need.

59.2 Definition

Function objects are defined in the file **controlDict**. There, a function dictionary is created which contains all necessary informations. Listing 392 shows the basic structure of such a definition.

Every function has a name. This name is stated at the place of the NAME placeholder in Listing 392. This name is also the name of the folder OpenFOAM creates in the case directory. There, all data generated by the function object is stored.

¹⁹⁹New users might hate this statement, but *the documentation is in the code*.

²⁰⁰As an illustrative example, the function object for processing field values within a cell set has changed its name from *cellSource* (OpenFOAM-3.0) over *volRegion* (OpenFOAM-4.0) to *volFieldValue* (OpenFOAM-5.0). This has been done, most probably, to keep the naming scheme consistent with the underlying class names or make the name descriptive of its task. However, as in many aspects of life in general, there is no unique, best way to do things. In this case, the function object’s name can describe *what it is* or *what it does*. Both ways are equally valid and there might even be more aspects to choose from.

²⁰¹The same is the case for migrating cases to older versions, however, using the current version should be the norm.

Each function object also has a type. This type needs to be specified at the place of the TYPE placeholder. The type needs to be from the list of the available functions. To find out, which functions are available, the *banana-trick*²⁰² can be used. Listing 393 shows the error message that is caused by the banana-trick.

The placeholder LIBRARY marks the place where the name of the library needs to be entered. A function object is not a program that is executable on its own. It is merely a library that is used by other programs. In our case, the function objects are called by the solvers. Therefore, the function objects are not compiled into executables. The compiler creates libraries when the function objects are compiled. These libraries contain the functions in a machine readable form.

The keyword `enabled` is optional. With this keyword function objects can be excluded from execution.

```
functions
{
    NAME
    {
        type          TYPE;
        functionObjectLibs ("LIBRARY");
        enabled      true;
        /*
            Definition
        */
    }
}
```

Listing 392: Definition of function objects in the file `controlDict`

```
--> FOAM FATAL ERROR:
Unknown function type banana

Valid functions are :

13
(
cellSource
faceSource
fieldAverage
fieldCoordinateSystemTransform
fieldMinMax
nearWallFields
patchProbes
probes
readFields
sets
streamLine
surfaceInterpolateFields
surfaces
)
```

Listing 393: Output of the *banana-trick*; applied to the keyword `type`

59.3 Control

All function objects are related more or less directly to the base class `functionObject`, which is defined in the file `$FOAM_SRC/OpenFOAM/db/functionObjects/functionObject/functionObject.H`. This class defines the smallest common behaviour of all function objects. Thus, it may pay off to study this class, as all we learn from it applies to all function objects.

59.3.1 Time control

The stages of function objects

Some OpenFOAM function objects might have some internal state which needs to be updated, whereas others might have no need for an internal state. Simple function object, which write selected data to disk might fall

²⁰²If OpenFOAM expects a keyword from a limited set of allowed keywords, stating an invalid keyword usually causes OpenFOAM to print the list of allowed entries.

under the latter category, e.g. the function object `surfaceRegion` from the `fieldValue` family of function objects simply writes the data from specified patches to disk. This is done only at write time.

On the other hand, function objects might need to compute data from the solution data and thus need an internal state, e.g. the `fieldAverage` function object needs to continuously update its internal fields for the temporal averages, even if it writes them less frequently to disk.

Thus, the operational stages of a function object are divided in `execute` (for updating its internal state) and `write` (for writing data, and computing to-be-written-data, which is not an internal state).

Execution & write control

The attributes of function objects for when-to-write are `writeControl` and `writeInterval`, in older versions of OpenFOAM these were `outputControl` and `outputInterval`. These control when and how often the data from the function object is written to disk.

A similar pair of controls (`executeControl` and `executeInterval`) exists for controlling when the function object is executed, i.e. its internal state is updated.

Note, that while can use the setting `writeInterval adjustableRunTime`; for the write interval of the `functionObject`, we need to ensure that the same setting is made for the simulation in general. If the simulation uses the setting `writeInterval runTime`; then the setting of the `functionObject` is over-ruled.

Enablement

The `enabled` flag controls whether the function object is enabled. This takes a boolean value and control whether to execute the function object or not. This might be useful for testing or debugging simulation cases. This flag allows you to define function objects and stop them from being used without deleting them from `controlDict`. A rather brute-force alternative to this flag, from the case file editing perspective, would be to comment the function object definition. However, changing the flag from `on` to `off` and vice-versa requires less characters changed than commenting and uncommenting²⁰³.

The pair `timeStart` and `timeEnd` control when to begin using a function object and when to stop. These controls are optional and are in most cases omitted. The default behaviour, when these controls are omitted, is to execute function objects from the start of the simulation and to execute them until the simulation finishes. In fact, the default values are a negative, ridiculously large number²⁰⁴ for `timeStart` and a ridiculously large number for `timeEnd`. Thus, no reasonable simulation will start before the default value of `timeStart` or run any longer than the default value of `timeEnd`. This way, there is no need for conditional statements, a simple comparison against the current time suffices.

59.3.2 Region control

The `region` keyword controls to which mesh region the function object applies. This can be omitted in all cases with only one mesh region, as stating the mesh region is superfluous. However, there are cases in OpenFOAM with more than one mesh region, such as conjugated heat transfer simulations. In this case we have one mesh (region) for the fluid region and one mesh (region) for the solid parts of our domain to solve for heat transfer. In this case we can use a function object to log the average temperature of both the fluid and the solid regions. Thus, we specify two function objects to evaluate the volumetric average temperature, however, we need to specify the region for which the function objects are to be executed.

The (abstract)²⁰⁵ base class responsible for selecting a mesh region to operate on is `regionFunctionObject`. A number of function objects are derived more or less directly from `regionFunctionObject`. Among these are function objects of the `fieldValues` family as well as `fieldMinMax` and `fieldAverage`.

59.4 probes

The function `probes` saves the values of certain field quantities at specific points in space. Listing 394 shows an example of the definition of a `probes` function object.

²⁰³Admittedly, with the use of multi line comments (`/* no comment */`), the amount of changed characters is four, compared to one or two when using the `enabled` flag. Potential savings are minuscule.

²⁰⁴The source code of the `scalar` class defines a static variable `VGREAT`, which is close to the maximum representable floating point number. `VGREAT` and similar static variables are frequently used for initialisation of variables.

²⁰⁵The class `regionFunctionObject` inherits two pure virtual methods from its base class `functionObjectTexttt` which it does not implement. Thus, `regionFunctionObject` is an abstract class.

This function object is of the type `probes`. The name of the function object is `probes1`. The data generated by this function is stored in the directory `probes1`. This directory contains a sub-directory. The name of this sub-directory corresponds to the time at which the simulation is started. This prevents files from being overwritten in case a simulation is continued at some point in time.

Figure 163 shows the directory tree after a simulation ended. There, the folder `probes1` contains a sub-directory named `0`. This is the time the simulation started. The `0` folder contains the files `p` and `U`.

The keywords `outputControl` and `outputInterval` are optional. They control – as their names suggest – the way the data is written to the hard drive.

`fields` contains the names of the fields that are of interest. `probeLocations` contains a set of points. The data of a specified field is computed for this locations and written to a file. The name of this file is the fields of interest. Listing 394 will result in two files. The file `p` contains the values of the pressure for all locations, the file `U` will contain the values of the velocity at all locations.

The function `probes` is contained in the file `libsampling.so`. This information can be gained from the tutorials. See Section 78.3 for more information about how to search the tutorials for specific information.

```

functions
{
    probes1
    {
        type          probes;
        functionObjectLibs ("libsampling.so");
        enabled       true;
        outputControl timeStep;
        outputInterval 1;

        fields
        (
            p
            U
        );

        probeLocations
        (
            ( 0.0254 0.0253 0 )
            ( 0.0508 0.0253 0 )
        );
    }
}

```

Listing 394: The definition of `probes` in the file `controlDict`

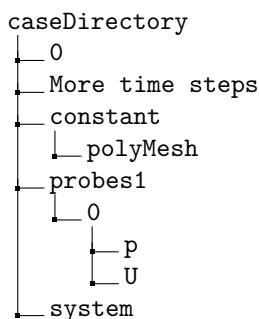


Figure 163: A part of the directory tree after the simulation ended

59.4.1 Pitfalls

Probe location outside the domain

If the probe location is outside of the domain OpenFOAM will issue a warning message and continue with the simulation.

```
--> FOAM Warning :  
From function findElements::findElements(const fvMesh&)  
in file probes/probes.C at line 102  
Did not find location (0.075 0 0.48) in any cell. Skipping location.
```

Listing 395: probe location outside of the domain

Unknown or non-existent field

If the probes dictionary contains fields that are not present to be probed, then no warning or error message will be issued. OpenFOAM simply continues computation. If the dictionary contains no valid fields to be probed, then the probe function will not be executed. Consequently no folder for storing the data will be created.

Using probes with moving mesh

When we use probes, OpenFOAM searches the mesh for the cells containing the specified probe locations. More specifically, it determines the cell indices of the cells containing the probe locations. Thus, OpenFOAM can easily obtain the cell value of the probed field. In essence a field in OpenFOAM is a list of values, and the cell index is used to navigate the list.

However, when we use moving meshes, the cell index related to a certain point in space may change over time, e.g. when probing a point within a rotating mesh region. Consequently, everytime the mesh is updated, we need to ensure that the cell indices of the probed are updated as well.

In OpenFOAM probes have a boolean flag (`fixedLocations`) controlling this updating of the cell indices. By default, this flag is set to true, meaning that no updating is required. Below, in Listing 396, we see the description of this flag from the header file `probes.C`.

```
//- Fixed locations, default = yes  
// Note: set to false for moving mesh calations where locations  
//       should move with the mesh  
bool fixedLocations_;
```

Listing 396: Description of the `fixedLocations` boolean flag in `probes.H`

When using moving meshes, add the `fixedLocations` flag to your `probesDict`, as shown in Listing 397 below.

```
fields  
(  
    ...  
)  
  
probeLocations  
(  
    ...  
)  
  
// add this for cases using moving meshes  
fixedLocations      false;
```

Listing 397: Add the `fixedLocations` flag to the `probesDict` when using probes with moving meshes

59.5 *fieldAverage*

fieldAverage computes time-averaged fields. Listing `lst:fieldAverageControlDict` shows an example of how this function is set up.

```
functions  
{  
    fieldAverage1  
    {  
        type          fieldAverage;
```

```

functionObjectLibs ("libfieldFunctionObjects.so");
enabled      true;
outputControl outputTime;
fields
(
    Ua
    {
        mean      on;
        prime2Mean off;
        base      time;
    }
);
}
}

```

Listing 398: Definition of a *fieldAverage* function object in the file `controlDict`

The *fieldAverage* function object can be provided with a averaging window size and name to compute a sliding average. In this case, the resulting averaged field bears the window name as a file name suffix besides the field name and the suffix `Mean`. With this feature, multiple averages of a field can be computed. Listing 399 shows two averages of the field `U.water`.

If no window is specified, *fieldAverage* computes the average from the start time of the function object. The resulting field bears the name of the to-be-averaged field and the suffix `Mean`. If a window size and a window name is specified, the resulting field's name is extended with the window name.

```
U.water  U.waterMean  U.waterMean_w1
```

Listing 399: Multiple averages of the field `U.water`

59.6 *faceSource*

59.6.1 Average over a plane

faceSource extracts data from surfaces (faces). Listing 400 shows how the average of a field quantity over a cutting plane is set up.

```

functions
{
    faceObj1
    {
        type      faceSource;
        functionObjectLibs ("libfieldFunctionObjects.so");
        enabled    true;
        outputControl outputTime;

        // Output to log&file (true) or to file only
        log       true;

        // Output field values as well
        valueOutput false;

        // Type of source: patch/faceZone/sampledSurface
        source      sampledSurface;

        sampledSurfaceDict
        {
            // Sampling on triSurface
            type      cuttingPlane;
            planeType pointAndNormal;
            pointAndNormalDict
            {
                basePoint ( 0 0 0.3 );
                normalVector ( 0 0 1 );
            }
            interpolate true;
        }
    }
}

```

```

// Operation: areaAverage/sum/weightedAverage ...
operation      areaAverage;
fields
(
    alpha
);
}

```

Listing 400: Definition of a *faceSource* function object in the file `controlDict`

59.6.2 Compute volumetric flow over a boundary

Listing 401 shows the definition of a function object that is used to compute the volumetric flow over a boundary face. The key points for this are the definition of a weight field and the use of the summation operation. The weight field is automatically applied to the processed field, there is no need to specifically an operation such as *weightedSum*. If no weight field is defined, no weight field is used.

```

functions
{
    faceIn
    {
        type          faceSource;
        functionObjectLibs ("libfieldFunctionObjects.so");
        enabled        true;
        outputControl  timeStep;
        log           true;
        valueOutput    false;
        source         patch;
        sourceName     spargerInlet;
        surfaceFormat  raw;
        operation      sum;
        weightField    alpha1;

        fields
        (
            phi1
        );
    }
}

```

Listing 401: Definition of a *faceSource* function object in the file `controlDict`

59.6.3 Pitfall: `valueOutput`

The option `valueOutput` writes the field values on the sampled surface to disk. This can lead to massive disk space usage when setting `outputControl` to `timeStep`. In this case the field values are written for every time step. The option `valueOutput` should be disabled unless it is really needed.

Figure 164 shows the contents of the `postProcessing` folder after two time steps have been written to disk. For each sampled field the field values on the sampled patch are written to disk in files in the `surface` folder.

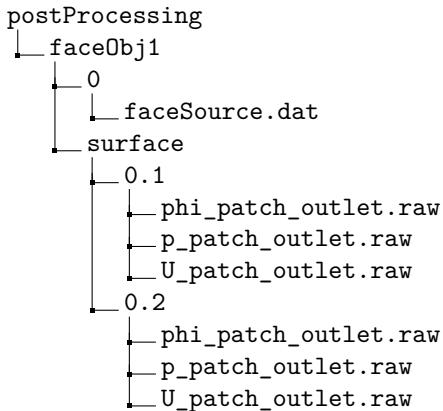


Figure 164: The content of the `postProcessing` folder

59.7 `cellSource`

The `cellSource` function object acts on all cells of the mesh or on the cells of a `cellZone`.

Listing 402 shows the definition of a `cellSource` function object. In this case, a part of the domain is contained in the `cellZone left`. The function object calculates the volume-average value of the volume fraction of air. The keyword `valueOutput` is set to the value `false` and marked as evil by the comment for reasons explained in Section 59.6.3.

```

1 functions
2 {
3     airContent_left
4     {
5         type          cellSource;
6         functionObjectLibs ("libfieldFunctionObjects.so");
7         enabled        true;
8         outputControl timeStep;
9         log           true;
10        valueOutput   false; // evil
11        source        cellZone;
12        sourceName    left;
13        operation     volAverage;
14
15        fields
16        (
17            alpha.air
18        );
19    }
20}

```

Listing 402: A usage example of the `cellSource` function object

59.8 `readFields`

If we want to post-process a case, which we computed with a custom solver that created custom fields, and the post-processing involves these custom fields, it is very likely that OpenFOAM will complain of those fields not being present in the database when we run our post-processing function objects. That's when `readFields` comes into play.

The description in the header files reads:

Reads fields from the time directories and adds them to the mesh database for further post-processing.

This function object serves the purpose to read specified fields, and add those to the database. Thus, adding this function object to our post-processing function objects allows us to post-process any custom fields with OpenFOAM's standard function objects.

59.9 writeObjects

If we want to post-process fields, that are not written by default, then we can tell OpenFOAM to write specified fields to disk. The description of the header file for this function object states:

Allows specification of different writing frequency of objects registered to the database.

59.10 Execute C++ code as functionObject

OpenFOAM makes it possible to execute C++ code as a functionObject²⁰⁶. This feature is disabled by default. To activate it a flag has to be changed. This is done for a single user in `~/.OpenFOAM/$WM_PROJECT_VERSION/controlDict` or system wide in `$WM_PROJECT_DIR/etc/controlDict`. In one of these files the flag shown in Listing 403 has to be set to one. It can be, that the first of these files does not exist, i.e. there are no user specific settings. The question of precedence (User setting over system wide setting) has not been pursued by the author.

Listing 404 shows an example of this feature. The field quantities U_1 , U_2 and p are read in and some calculated values are printed to the Terminal.

```
// Allow case-supplied C++ code (#codeStream, codedFixedValue)
allowSystemOperations 1;
```

Listing 403: Allow case-supplied C++ code

```
1 extraInfo
2 {
3     type          coded;
4     functionObjectLibs ("libutilityFunctionObjects.so");
5     redirectType   average;
6     code
7     #{
8         const volVectorField& U1 = mesh().lookupObject<volVectorField>("U1");
9         const volVectorField& U2 = mesh().lookupObject<volVectorField>("U2");
10        Info << "max U1 = " << max(mag(U1)).value() << ", U2 = " << max(mag(U2)).value() << endl;
11        const volScalarField& p = mesh().lookupObject<volScalarField>("p");
12        Info << "p min/max = " << min(p).value() << ", " << max(p).value() << endl;
13    #};
14 }
```

Listing 404: Define a *functionObject* using C++

When the solver is invoked, the so called coded functionObject is compiled on the fly. Listing 405 shows a portion of the solver output. Between the entry into the time loop and the first calculations, the code is read from controlDict and pasted into a template of a coded functionObject.

```
Starting time loop
```

```
Using dynamicCode for functionObject extraInfo at line 69 in "/home/user/OpenFOAM/user-2.1.x/
run/twoPhaseEulerFoam/bubbleColumn/system/controlDict::functions::extraInfo"
Creating new library in "dynamicCode/average/platforms/linux64GccDPOpt/lib/
libaverage_731fed868edc5a1d75988808649ac874cf00e044.so"
Invoking "wmake -s libso /home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bubbleColumn/
dynamicCode/average"
wmakeLnInclude: linking include files to ./lnInclude
Making dependency list for source file functionObjectTemplate.C
Making dependency list for source file FilterFunctionObjectTemplate.C
'/home/user/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/bubbleColumn/dynamicCode/average/...
platforms/linux64GccDPOpt/lib/libaverage_731fed868edc5a1d75988808649ac874cf00e044.so' is
up to date.
Courant Number mean: 1.68517e-05 max: 0.00363
Max Ur Courant Number = 0.00363
Time = 0.001

MULES: Solving for alpha1
```

Listing 405: On the fly compilation of C++ coded functionObjects

²⁰⁶The release notes of OpenFOAM-2.0.0 suggest that this feature was introduced with version 2.0.0. See <http://www.openfoam.org/version2.0.0/>

OpenFOAM creates a directory named `dynamicCode` in the case directory. There, all files related to the coded functionObject can be found, source files as well as binaries. Figure 165 shows the directory tree after OpenFOAM compiled the coded functionObject.

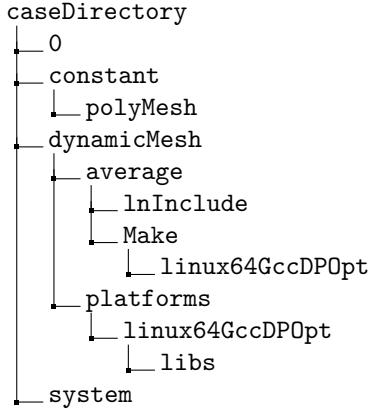


Figure 165: Directory tree after compilation of a coded functionObject

59.11 wallHeatFlux

The `wallHeatFlux` function object can be used to determine the wall heat flux. By default, `wallHeatFlux` computes the wall heat flux for all patches of the type `wall`. Alternatively a list of patches can be passed to the function object using the `patches` keyword.

Determining the physical units

In Line 7 of Listing 406, we see that the wall heat flux field is initialized with the physical unit kilogram per cubic second. In Line 17, we see that the wall heat flux is computed from the product of the thermal diffusivity for the enthalpy and the gradient of the `he`-field²⁰⁷.

$$[\text{wallHeatFlux}] = [\alpha] \cdot [he.\text{snGrad}()] \quad (197)$$

$$[\text{wallHeatFlux}] = \frac{\text{kg}}{\text{m s}} \cdot \frac{\text{J}}{\text{kg m}} = \frac{1}{\text{m s}} \cdot \frac{\text{Ws}}{\text{m}} = \frac{\text{W}}{\text{m}^2} \quad (198)$$

The equations above, demonstrate the how to derive the physical unit of the resulting wall heat flux computed by this function object. Indeed, the result is Watt per square meter. Note, that the `alpha`-field is the thermal diffusivity of the enthalphy²⁰⁸.

```

1 tmp<volScalarField> twallHeatFlux
2 (
3     volScalarField::New
4     (
5         type(),
6         mesh_,
7         dimensionedScalar(dimMass/pow3(dimTime), 0)
8     )
9 );
10
11 /* some code removed for brevity */
12
13 forAll(wallHeatFluxBf, patchi)
14 {
15     if (!wallHeatFluxBf[patchi].coupled())

```

²⁰⁷With compressible solvers, the user can choose to either solve the energy for the specific enthalpy `h` or the specific internal energy `e`. The `he`-field is a convenient placeholder for either one. Note that the specific enthalpy and the specific internal energy both have the physical unit of Joule per kilogram.

²⁰⁸You can find the definition of `alpha` in the files `basicThermo.H` and `basicThermo.C`

```

16     {
17         wallHeatFluxBf[patchi] = alphaBf[patchi]*heBf[patchi].snGrad();
18     }
19 }
```

Listing 406: The computation of the wall heat flux in `wallHeatFlux.C`

The `wallHeatFlux` function object, not only computes the wall heat flux as a field, it also prints the extrema and the integral-value per patch to the Terminal, and also writes those values into a data file. The integral value is of course the amount of energy transferred per-patch in terms of Watts.

59.12 Execute *functions* after a simulation has finished

59.12.1 execFlowFunctionObjects

`execFlowFunctionObjects` is a post-processing tool of OpenFOAM. This tool allows the user to execute function objects after a simulation is finished. Normally, function objects are executed during the simulation. However, in some cases it is useful to apply a function to the data set of a already completed simulation, e.g. for testing the function.

Defining function objects in a separate file

Listing 407 shows a file which contains only the definition of a function object. For the sake of clarity, this file is named `functionDict`. Defining functions in a separate file reflects the division of labor in some way. The file `controlDict` is controlling the solver, whereas the file `functionDict` defines the function objects. The file `functionDict` can be included into the file `controlDict` by an `#include` statement. See Section 11.3.5 for examples.

```

FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    location     "system";
    object       functionDict;
}
// * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * //

functions
{
    probes1
    {
        type probes;
        functionObjectLibs ("libsampling.so");
        dictionary probesDict;
    }
}

```

Listing 407: Define functions in a separate dictionary. The file `functionDict`

Run *execFlowFunctionObjects*

execFlowFunctionObjects has to be told, that the functions are defined in a separate file. By default, the tool reads the file **controlDict**. By using the parameter **-dict** the user can specify an alternative file containing the function dictionary.

```
execFlowFunctionObjects -noFlow -dict functionDict
```

Listing 408: Invocation of *execFlowFunctionObjects*

60 *sample*

sample is a simple post processor. This tool is controlled by the file `sampleDict`. *sample* extracts data from the solution of a specific region. *sample* can extract data from the following geometric regions:

- from one or several points in space
- along a line
- on a face

sample is usually executed after a simulation has finished.

60.1 Usage

The simplest way to use *sample* is to call the command `sample`. In this case *sample* looks for a file named `sampleDict` located in the `system` directory. With the `-dict` an alternative file with a different name can be specified. However, this file has to reside in the `system` directory.

By default *sample* operates on all time steps. The option `-latestTime` can be used to sample only the latest solution data. The option `-time` can be used to specify a certain time or a time range to operate on.

Specifying a limited number of time steps to perform sampling on significantly reduces the time needed for this operation. The disk space used by the data generated by *sample* is usually in the order of up to a few megabytes. Therefore saving hard disk space is not an issue when using *sample*.

60.2 *sampleDict*

The file `sampleDict` controls what and where data is to be sampled.

60.2.1 Output format

There are 6 possible output formats (`csv`, `gnuplot`, `jplot`, `raw`, `vtk`, `xmgr`). The difference between the listed formats is the way how the data is organised inside the file.

sample creates one file for scalar quantities and one for vector quantities. The names of the data files are built from the names of the sampled fields, the output format and the name of the geometric set. E.g. `lineXuniform_Ua_Ub.csv`, this file contains the velocity fields `Ua` and `Ub` along the line `lineXuniform`. The data format of the sampled data is comma seperated values (`csv`).

60.2.2 Fields

The fields that are to be sampled are listed in the list `fields`.

Invalid entries are ignored, without any warning message. In the example of Listing 409 the list of fields contains the name `banana`. However, there is no field named `banana`, so *sample* will simply ignore this entry – *sample* will not issue any warning or error message. Thus, a typo in the `sampleDict` is not that easy to find. *sample* reports no warning but the intended field is not sampled. Always double check the entries in the `fields` sub-dictionary for typos, especially when sampling fields with composite names, e.g. `U2Mean` or `U2Prime2Mean`.

```
// Fields to sample.
fields
(
    alpha
    banana
    Ua
    Ub
);
```

Listing 409: Fields to sample in the file `sampleDict`

60.2.3 Geometric regions

The geometric regions on which *sample* can operate are

sets A set can contain one or several points or a line. Along a line, points can be distributed in an equidistant fashion.

surfaces A surface can be defined in several ways. Possible are, among others, cutting planes or iso-surfaces.

60.2.4 Pitfalls

Missing keywords

If the keywords *sets* and *surfaces* are missing in *sampleDict*, *sample* will run without producing any error messages or any data. If in Listing 410 the word *banana* would be replaced by *sets* and *orange* by *surfaces*, *sample* would work as expected. If *sample* is called with a *sampleDict* like in Listing 410, *sample* produces no data and issues no warning.

```
setFormat raw;

surfaceFormat vtk;

formatOptions
{
    ensight
    {
        format ascii;
    }
}

interpolationScheme cellPoint;

fields
(
    p
    U
);

banana
(
    lineX1
    {
        type      uniform;
        axis      distance;
        start    (0.0015    0.5027 0.05);
        end      (0.0995    0.5027 0.05);
        nPoints  20;
    }
);

orange
();
```

Listing 410: Not working example of *sampleDict*

Faulty line definition

If the data along a line is to be sampled and the definition of the line is erroneous so that the line is outside the domain, *sample* will issue a warning message. Listing 411 shows an example of such a warning message. However, *sample* will not report an error and it will finish its run. So, when the output of *sample* is not checked, this might go unnoticed.

```
--> FOAM Warning :
  From function sampledSets::combineSampledSets(..)
  in file sampledSet/sampledSets/sampledSets.C at line 102
```

```
Sample set lineX0 has zero points.
```

Listing 411: Warning message of *sample* due to a faulty line definition

Insufficient write precision

In the OpenFOAM tutorials, the majority of cases use a write precision of 6 digits, which should be sufficient in most cases. However, in certain instances, a greater number of digits may be required.

When we are sampling the pressure field, it depends on whether we are using an incompressible or a compressible solver, for the 6 digits of write precision to be adequate or not. An incompressible solver uses a pressure field, which is divided by the fluid density. Furthermore, for incompressible solvers, the absolute value of the pressure is irrelevant. Thus, many cases use 0 as their reference or ambient pressure, e.g. at an outlet. With compressible solver, on the other hand, we use the pressure field and the absolute value of the pressure is relevant. Thus, the pressure field has, in many cases, the ambient pressure is 100000 Pa. This is where the write precision comes into the picture. In Listing 412 we see the result of sampling the pressure of a compressible case, when using a write precision of 6 digits. The reference pressure of 100000 Pa nearly drowns-out all information on the pressure variation in this case, as the 6 digits are nearly completely used-up to represent the ambient pressure. The little variations within the solution domain can not be fully resolved due to a lack of digits.

```
x,p  
0,100001  
0.00055,100001  
0.0011,100001  
0.00165,100001  
0.0022,100001  
0.00275,100001  
...
```

Listing 412: Sampling the pressure field of a compressible case with a write precision of 6 digits.

Even worse is the result when using only 5 digits. In this case, see Listing 413, OpenFOAM switches to scientific notation, and is only able to represent the ambient pressure. The small variation of pressure is now completely lost.

```
x,p  
0,1e+05  
0.00055,1e+05  
0.0011,1e+05  
0.00165,1e+05  
0.0022,1e+05  
0.00275,1e+05  
...
```

Listing 413: Sampling the pressure field of a compressible case with a write precision of 5 digits.

Using a sufficient number of digits ensures that the pressure variation within the solution domain can be sampled and processed further.

```
x,p  
0,100001.1161  
0.00055,100001.116  
0.0011,100001.1153  
0.00165,100001.1145  
0.0022,100001.1134  
0.00275,100001.1123  
...
```

Listing 414: Sampling the pressure field of a compressible case with a write precision of 10 digits.

Choosing a sufficient number of digits seems like really obvious solution. So, when do we run into the problem of sampling data with an insufficient number of digits? When we run a simulation using the binary write format for the field data. In this case, the pressure field is written to disk in binary format, with maximum precision. However, the sampled data will always be written to disk in ascii format. This is when we run into

the troubles discussed in this section. When we simply do not care about the number of digits, because we feel save by using the binary format.

60.3 Update OpenFOAM-4

The post processing utility *sample* and others have been superseded by the tool `postProcess`, which bundles post processing tasks. Fortunately, not all is lost. All utilities that are superceded by `postProcess` issue a warning message about them being obsolete now. However, this message contains very helpful information on how to proceed. In the case of *sample*, existing `sampleDicts` can be used further with little modification.

```
sample has been superceded by the postProcess utility:  
postProcess -func sample  
  
To re-use existing 'sampleDict' files simply add the following entries:  
  type sets;  
  libs ("libsampling.so");  
and run  
  postProcess -func sampleDict
```

Listing 415: Warning message in OpenFOAM-4 when trying to use *sample*

61 ParaView

ParaView is a graphical post-processor. This program is called by invoking the command `paraFoam`. `paraFoam` is a script that calls *ParaView* with additional OpenFOAM libraries.

61.1 Reader's choice

Post-processing OpenFOAM cases offers the choice between two variants, i.e. we can choose between the native OpenFOAM-reader of ParaView, and OpenFOAM's reader module. In general, both readers are equivalent, yet there are some differences between those two.

For this document, OpenFOAM's reader is generally used, unless when explicitly mentioning the native reader.

61.1.1 OpenFOAM's reader

OpenFOAM's reader is used when we launch ParaView using the `paraFoam` command. `paraFoam` is actually a script, which launches ParaView with the appropriate libraries.

From observation, we see that when we run the `paraFoam` command, a file gets created named `CASE_NAME.OpenFOAM`. When ParaView is closed again, this file is automatically removed. The important bit of this file, which we refer to as the case-file, is the file extension. The file itself is an empty file.

Thus, in order to use ParaView with OpenFOAM's reader module, we can simply create a file with the `*.OpenFOAM` file extension²⁰⁹, open ParaView and open this file using the `File > Open` menu.

The OpenFOAM reader module pre-dates the native reader and supports only serial or reconstructed cases. The OpenFOAM reader is considered to support all of OpenFOAM's features²¹⁰.

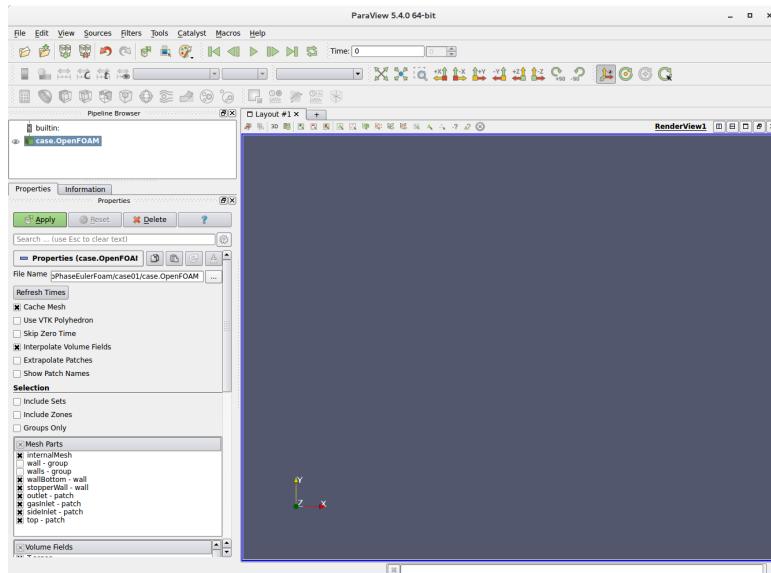


Figure 166: Launching ParaView with OpenFOAM's reader for OpenFOAM cases.

61.1.2 Native reader

If we launch ParaView, we can't simply use the `File > Open` menu to open an OpenFOAM case. Thus, in order to open an OpenFOAM case, we need to create a case-file with a `*.foam` file extension. This file can then be opened using the `File > Open` menu, which causes ParaView to use its native reader for OpenFOAM cases.

²⁰⁹E.g. using the command: `touch foo.OpenFOAM`

²¹⁰<https://www.openfoam.com/documentation/user-guide/paraview.php>

Decomposed cases

One major advantage of the native reader is, that it is fully parallelized. Thus, we can post-process decomposed cases without prior reconstruction of the case. Thus, we can avoid the duplication of data when post-processing an ongoing case. Figure 167 shows a screenshot, when opening a case-file for the native reader. In the properties panel on the left, there is a drop-down menu, which shows the setting *Reconstructed Case* in Figure 167. This setting can be changed to *Decomposed Case*, in order to read the parallelized case data.

The native ParaView reader is considered to potentially encounter problems with complex dictionary input.

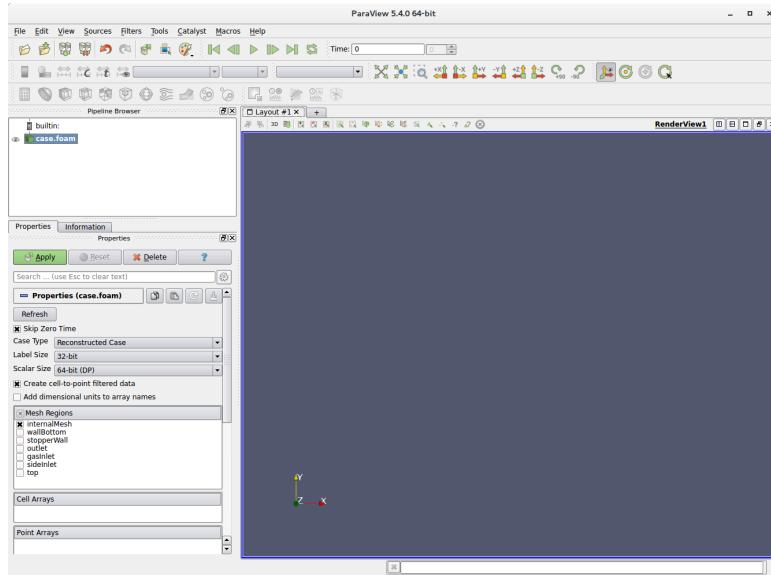


Figure 167: Launching ParaView with its native reader for OpenFOAM cases.

Multi-region cases

Another neat feature of the native reader is that it recognizes multi-region cases. Thus, by simply opening a `*.foam` file, the reader automatically reads-in the individual regions of the case. See Figure 168 for an example.

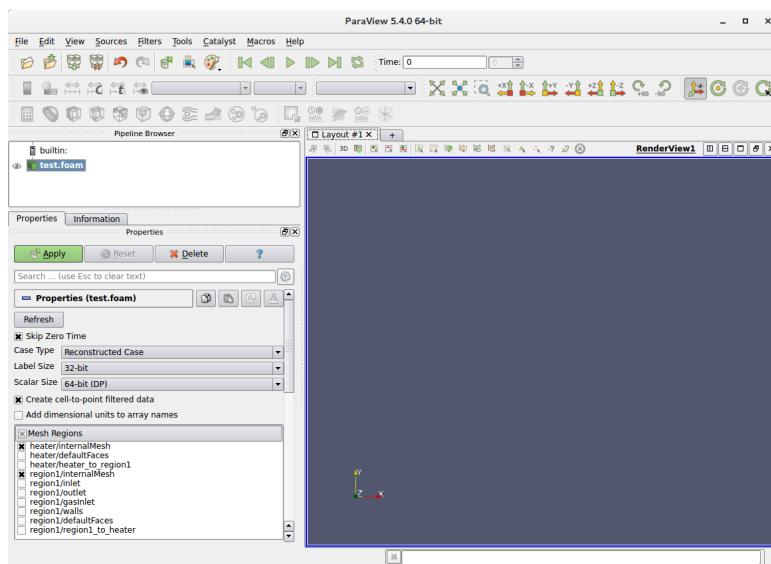


Figure 168: Using ParaView with its native reader to read a multi-region OpenFOAM case.

Pitfall: decomposed multi-region cases with constant/polyMesh still being present

One instance, the native reader struggles is when the mesh of a multi-region case has been created from a single-region mesh, and the initial mesh is still around. When such a case is decomposed, then the native reader will encounter the initial single-region mesh and the individual region-meshes in the `constant` directory, however, in the `processor*` directories, only the region-meshes are present.

In Listing 169 shows the directories of a case that triggers the problem described above. The mesh of this case has been created by subsequent execution of `blockMesh`, `topoSet` and `splitMeshRegions`; which created the initial mesh, created cellZones and split the mesh into regions according to the cellZones. Since there is no way to decompose both the initial mesh and the region-meshes, which would by the way make no sense at all, we need to remove the initial mesh in `constant/polyMesh` for the native reader to work properly.

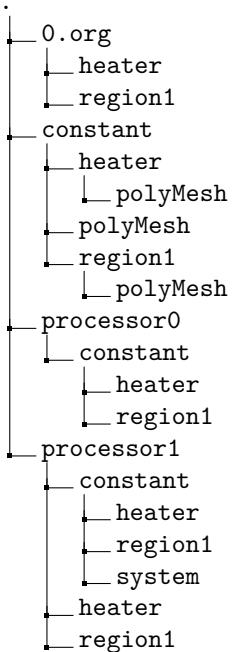


Figure 169: The case directories of a decomposed, multi-region case with the initial mesh still present. This directory tree was generated by calling the following command from the case directory: `tree -L 3 -d`

61.2 View the mesh

Besides viewing and post-processing simulation results, *ParaView* can be used to view only the mesh. E.g. when refining a mesh it is important to check neighbouring blocks for the transition of mesh fineness.

When no fields are selected, *paraView* only reads the mesh information. Therefore, it is possible to view the mesh without the rest of the case properly set up. After the `Apply` button has been pressed and *paraView* has read all the data, the user has to choose from the representation drop-down menu in the toolbar the option `Surface with edges`.

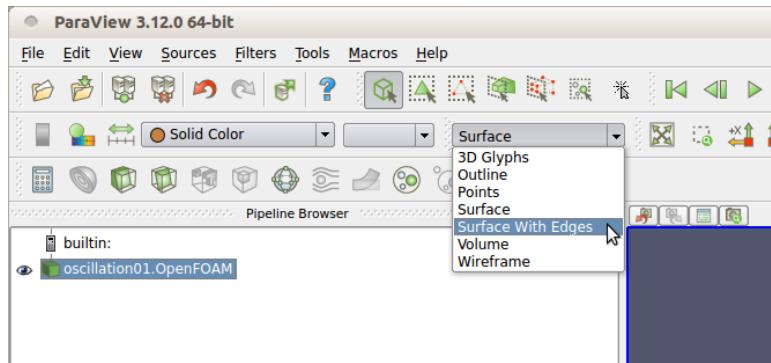


Figure 170: Select the proper representation to view the mesh

61.2.1 Sort-of-pitfall: cell shape representation

When examining meshes, we would like to get the cell shapes correctly represented. However, there seems to be an issue with ParaView's ability to display various cell shapes. Figure 171 shows an example in which the cell shape is not represented correctly. By default, ParaView seems to decompose polyhedrals into hexahedra, tetrahedra and other simple shapes.

Thus, the image shown in Figure 171 wrongly suggests a mesh consisting of mainly hexahedra, and many cells being distorted.

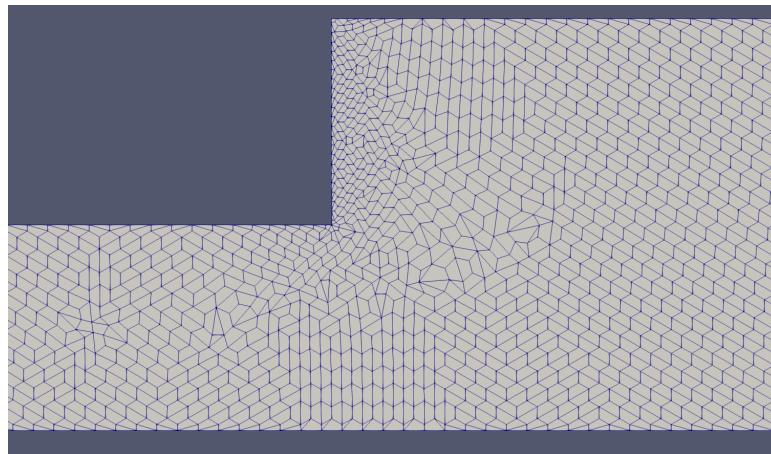


Figure 171: Viewing a polyhedral mesh with ParaView's standard settings.

If we want to correctly display the mesh, we need to check the box labelled *Use VTK Polyhedron* in the properties panel. In Figure 166, this is the second box from the top. If we check this box, and read the case, or check this box and refresh ParaView's state by clicking on the **Apply** button, the displayed mesh changes to the representation shown in Figure 172. Now we can clearly see the polyhedral cell shapes.

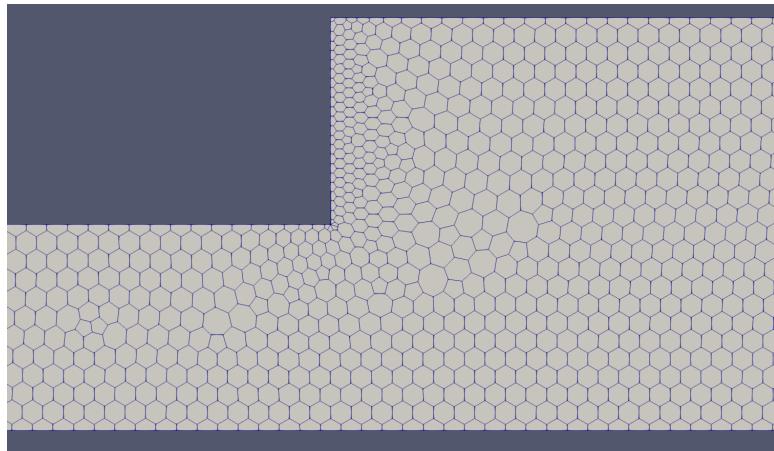


Figure 172: Viewing a polyhedral mesh with adjusted settings.

The native reader

It is the author's assumption that the underlying cause of this representation issue has its origins in ParaView itself, because the native reader of ParaView lacks a comparable option to adjust cell shape representation. Viewing the mesh with the native reader yields the result shown in Figure 173, which is a comparable representation as in Figure 171. In both cases, the polyhedra are decomposed into hexahedra and other simple shapes, yet the decomposition differs a little.

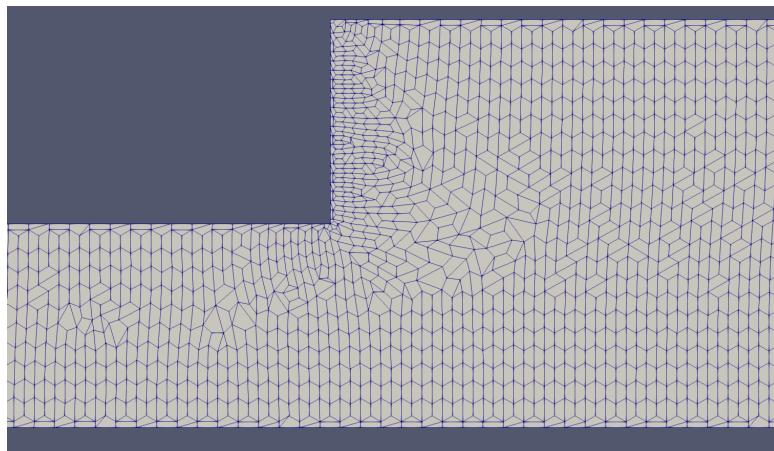


Figure 173: Viewing a polyhedral mesh with ParaView's native OpenFOAM reader.

61.2.2 Pitfall: default field selection

If a user works on the refinement of the mesh and the definition of boundary conditions has not been made, then calling *ParaView* can crash because of its default selection of the pressure field. After pressing the **Apply** button *ParaView* tries to read in all selected fields. In case of a faulty definition of the boundary fields, this ends in the termination of the program. Listing 416 shows a corresponding error message.

```
--> FOAM FATAL IO ERROR:
keyword bottom is undefined in dictionary "/home/user/OpenFOAM/user-2.1.x/run/icoFoam/case01
/0/p::boundaryField"

file: /home/user/OpenFOAM/user-2.1.x/run/icoFoam/case01/0/p::boundaryField from line 25 to
line 35.

From function dictionary::subDict(const word& keyword) const
in file db/dictionary/dictionary.C at line 461.
```

Listing 416: Reading error due missing boundary field definition

61.3 Saving animations

61.3.1 Save as animation - video format

The straight-forward way to save animations in ParaView is to save a view as an animation in the form of a video file. Simply choose **File > Save Animation ...** from the menu, and select a video format²¹¹ when ParaView asks for a file name.

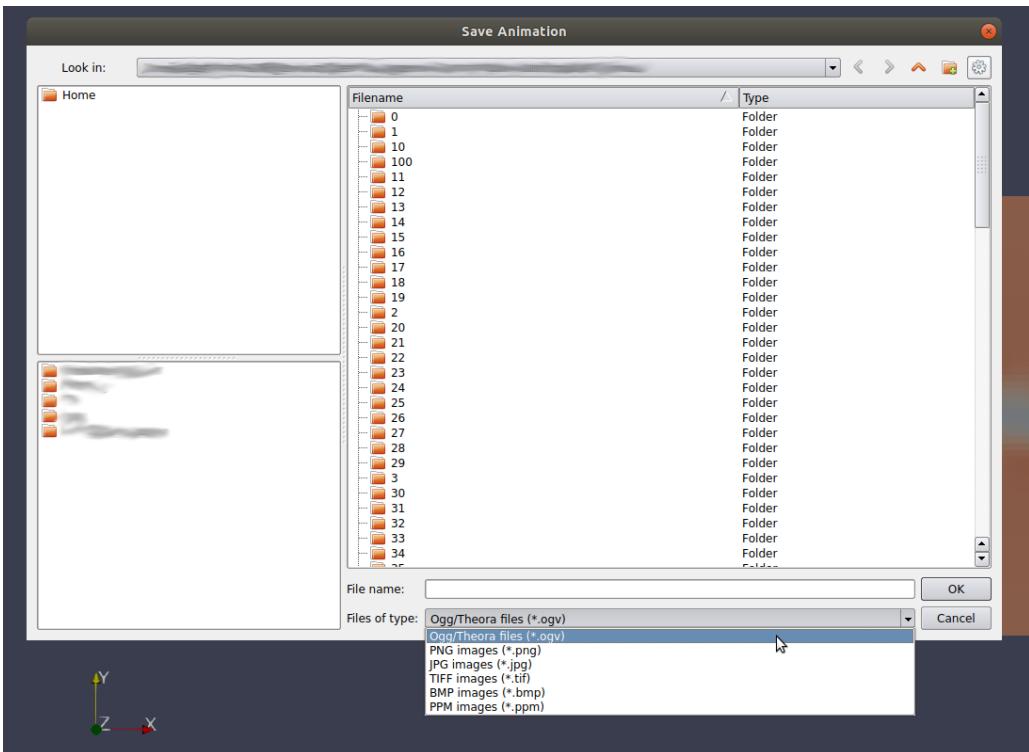


Figure 174: Selecting the file name for the animation.

61.3.2 Save as animation - individual images

Saving a view from ParaView in the form of a video file may sometimes yield unsatisfactory results, e.g. dropping individual frames. Hence, we might want an option to create an animation with more control over the animation-making process.

For this, we save the animation from ParaView as a sequence of individual images, which will be automatically numbered sequentially by ParaView. From these images, we can then create an animation using a video encoding software of our choice.

Using FFmpeg

In this example we use FFmpeg, which is a widely available, open source multimedia library. See <https://en.wikipedia.org/wiki/FFmpeg> and <https://ffmpeg.org> for more information. Listing 417 shows an example of how an animation can be created from the individual images saved by ParaView. Here, we assume that we saved our view under the file name `velField.png`, ParaView then automatically inserts sequential

²¹¹ParaView appears to support only the OGV format, at least with the tested versions 5.4.0 and 5.6.0. For the OGV format, see e.g. <https://en.wikipedia.org/wiki/Theora> or <https://www.theora.org>.

numbering. In the call to FFmpeg, we specify a frame rate in frames per second using the `-r` command line argument.

With the command line argument `-i` we specify the input for our animation. Here, we use the file name we used earlier to save the individual frames, however, we account for the sequential numbering by inserting a place-holder, i.e. `%04d`, which stands for a zero-padded integer with a fixed width of 4 characters. FFmpeg will insert sequential numbers starting from 0.

If we wanted to start our animation from a frame other than the one named `velField.0000.png`, we can provide an alternative starting number with the command line argument `-start_number`.

The last argument of the command in Listing 417 is the name of the resulting video file.

```
# change to the directory containing the individual images
user@host:~$ ls
velField.0000.png  velField.0012.png  velField.0024.png  velField.0036.png  velField.0048.png
... # output deleted for clarity
user@host:~$ ffmpeg -r 1 -start_number 19 -i velField.%04d.png velocityField.ogv
```

Listing 417: Creating an animation from individual images.

61.4 Case manipulation using ParaView

ParaView offers some tools to manipulate case data, here we shall discuss some of them along with potential use-cases. This discussion is neither exhaustive nor complete.

61.4.1 Create a tet-mesh and export as VTK

Tetrahedralize filter

The *Tetrahedralize* filter of ParaView creates a tetrahedralisation of the current mesh, which may consist of any cell types. The result is an all-tet mesh.

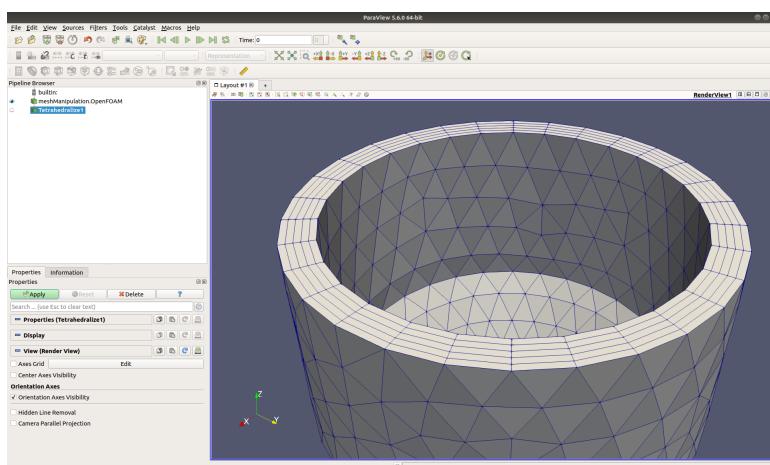


Figure 175: The Tetrahedralize filter of ParaView takes no user input.

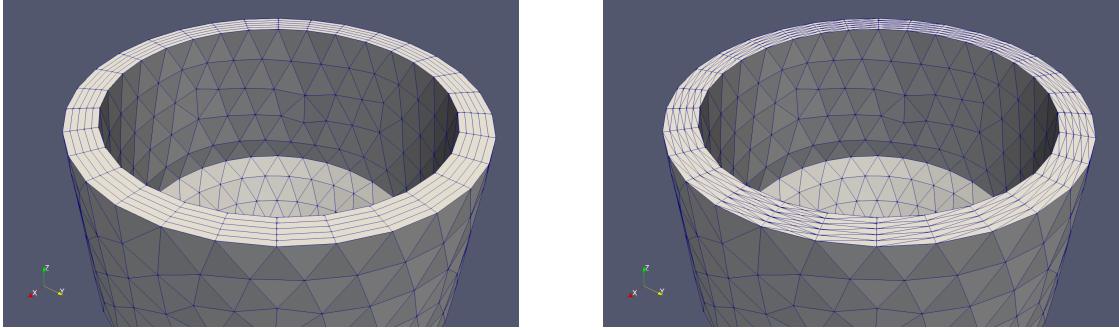


Figure 176: *Left:* an extruded mesh created from an STL surface mesh. *Right:* the mesh after tetrahedralisation.

Export VTK

Exporting the tetrahedralized mesh in the VTK format can simply be done in ParaView by selecting the **Tetrahedralize** item in the Model Tree and using the *Save Data* command of the File menu, i.e. select **File** → **Save Data** in the menu bar of ParaView. The subsequent dialogue will ask for a format and a file name.

After we have provided a file name and selected the VTK format, we are asked in a subsequent step whether to write time steps; whether to write the file in ASCII or binary format; and whether to compress the exported files.

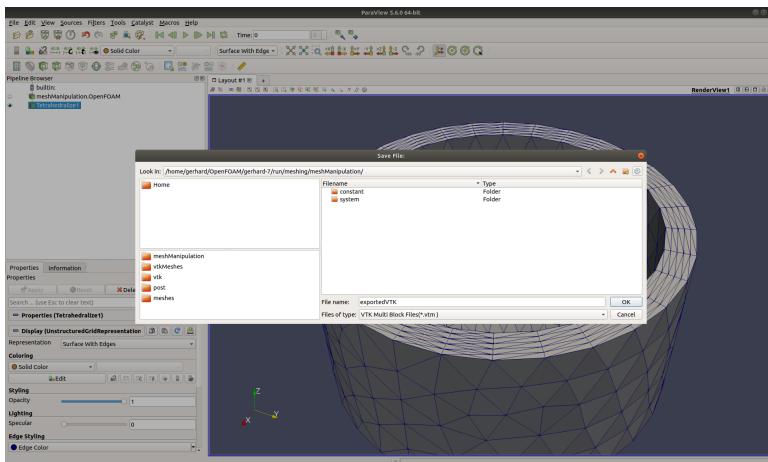


Figure 177: Exporting data from ParaView using the *Save Data* command from the *File* menu.

ParaView will export a couple of files from the tetrahedralized mesh. A VTK Multi Block File is written to the case directory, which is basically a manifest of the other exported files. These files are written into an export-folder, which has the same name as the Multi Block File with the exception of the file extension. Within this folder, the other files are written, which contain the volume mesh as well as the patches. In the example shown in Listing 418 the file `exportedVTK_0_0.vtu` contains the volume mesh, and the other files contain a patch each.

```
user@host:~/OpenFOAM/user-7/run/meshing/meshManipulation$ cat exportedVTK.vtm
<VTKFile type="vtkMultiBlockDataSet" version="1.0" byte_order="LittleEndian" header_type="UInt64">
<vtkMultiBlockDataSet>
<Block index="0" name="unzoned">
<DataSet index="0" name="internalMesh" file="exportedVTK/exportedVTK_0_0.vtu"/>
</Block>
<Block index="1" name="patches">
<DataSet index="0" name="sides" file="exportedVTK/exportedVTK_1_0.vtu"/>
<DataSet index="1" name="originalPatch" file="exportedVTK/exportedVTK_2_0.vtu"/>
<DataSet index="2" name="otherSide" file="exportedVTK/exportedVTK_3_0.vtu"/>
</Block>
</vtkMultiBlockDataSet>
```

```

<FieldData>
  <dataArray type="Float64" Name="TimeValue" NumberOfTuples="1" format="ascii" RangeMin="0"
  RangeMax="0">
    0
  </dataArray>
</FieldData>
</VTKFile>
user@host:~/OpenFOAM/user-7/run/meshing/meshManipulation$ ls exportedVTK
exportedVTK_0_0.vtu  exportedVTK_1_0.vtu  exportedVTK_2_0.vtu  exportedVTK_3_0.vtu
user@host:~/OpenFOAM/user-7/run/meshing/meshManipulation$

```

Listing 418: The content of the VTK Multi Block File viewed in the Terminal; and the files written into the export-folder.

Legacy VTK

If we wanted to use the Legacy VTK format for our exported mesh, we need to open the exported file containing the internal mesh with ParaView again. In our case, we need to open the file `exportedVTK_0_0.vtu` from the export folder. This data is then again exported using the *Save Data* command from the *File* menu. Now that we are dealing with pure VTK data, we can select to write the data in the Legacy VTK format.

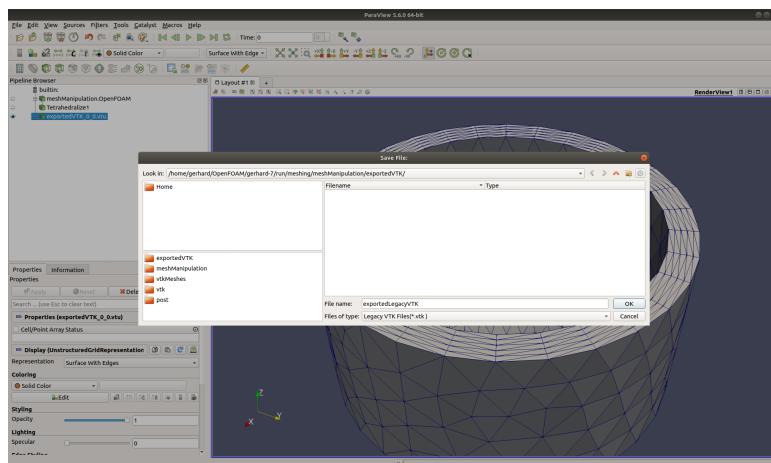


Figure 178: Export data from ParaView in the Legacy VTK format.

All roads lead to FOAM

With the big number of tools included with OpenFOAM and also the surrounding bits and pieces of software, you should not be surprised to learn that there is also an alternative way to achieve a tetrahedralisation of an OpenFOAM mesh using completely different tools. See Section 30.10 for an alternative approach.

62 postProcess

With OpenFOAM-4.0 the function object framework was rewritten. In the course of this rewrite a `postProcess` utility was introduced and a `postProcess` option was added to most of the solvers²¹². The `postProcess` utility also supersedes certain post-processing utilities, e.g. `sample`.

62.1 Usage

62.1.1 Pre-configured function objects

There are a number of pre-configured function objects, which are ready to use with `postProcess`. These can be found in `$FOAM_ETC/caseDicts/postProcessing`. They can also be listed using the `-list` option of `postProcess`.

```
user@host:~$ postProcess -list
```

Listing 419: Determine the extrema by magnitude of a velocity field

62.1.2 Passing parameters

Listing 420 shows how to determine the minimum and maximum magnitude of a velocity field.

```
user@host:~$ postProcess -fields '(U.water)' -func "minMaxMagnitude(U.water)"
```

Listing 420: Determine the extrema by magnitude of a velocity field

Listing 421 shows how to process two velocity fields at once, we simply pass the names of the fields in a comma-separated list.

```
user@host:~$ postProcess -fields '(U.air U.water)' -func "minMaxMagnitude(U.air,U.water)"
```

Listing 421: Determine the extrema by magnitude of two velocity fields

In Listing 422 we process a single velocity field and pass additional parameters to the function object. In this case, we do not want to know the location of the minimum and maximum velocity magnitude.

```
user@host:~$ postProcess -fields '(U.air)' -func "minMaxMagnitude(U.air,location=off)"
```

Listing 422: Determine the extrema by magnitude of a velocity field with no location

After running our function objects, we see that data was written into the `postProcessing` directory. We note that the folder names correspond to the argument passed via the `-func` option.

```
user@host:~$ ls postProcessing
minMaxMagnitude(U.air,location=off) minMaxMagnitude(U.air,U.water)
```

Listing 423: The contents of the `postProcessing` directory after running two function objects from the above listings

62.1.3 Post-processing decomposed cases

We can run `postProcess` in parallel in the same way we run a solver in parallel. This allows us to post-process a case, which has not been reconstructed.

```
mpirun -np 4 postProcess -parallel
```

Listing 424: Run `postProcess` in parallel, i.e. post-process a decomposed case.

²¹²Counting the solvers with `find $FOAM_SOLVERS -name 'files' | xargs grep 'EXE' | wc` yielded a number of 82 solvers, of which 73 included the `postProcess.H` header file, which provided the `postProcess` option. The second number was determined with the following command: `find $FOAM_SOLVERS -name '*.C' | xargs grep '\#include[[:space:]]\\"postProcess.H\\"' | wc`.

63 gnuplot

gnuplot is a command-line driven graphing utility for many platforms²¹³. gnuplot can be used to plot data generated by OpenFOAM's various run-time post-processing tools, e.g., function objects.

Listing 425 shows a dummy script, which demonstrates most of the basic features we might need. gnuplot, when plotting data from ASCII files, works in a column-based manner, with the individual columns in a file representing individual data points while the rows represent the points in time.

See <http://www.gnuplot.info/demo/> for large selection of demo plots.

63.1 Usage example

63.1.1 gnuplot input script

Listing 426 shows an example of a file, we might want to print some data from. Each line, contains the time in the first column, an averaged scalar in the second column and an averaged vector in the following columns.

The first half of the gnuplot script in Listing 426 deals with general settings. Then, we see a `plot` command followed by arguments, which specify from what data source, which columns, how to plot the data and how to label the resulting graph. The first argument is simply the path of the data file containing the data we would like to plot. The second argument is indicated by the keyword `using` followed by two numbers separated by a colon. These two numbers specify which columns of the data file to use for the plot. The first entry specifies the x-values and the second entry specifies the y-value. The third argument indicated by the keyword `with` specifies the plot style and the final argument indicated by the keyword `title` is used to provide a label, which is used to create a legend for the plot.

Listing 426 shows that the `plot` command can span over multiple lines to improve readability. This is done by indicating a line-break using the back-slash \ character. gnuplot will read on, when it encounters a back-slash at the end of a line.

In Listing 426, we provide the `plot` command with two elements to plot. Each element in this example is from a different file, however, they will be plotted into the same plot.

At the beginning of the input script, we set the terminal to png, thus creating a graphics file in the PNG format. The last two lines, set the terminal to X11 and repeat the plot. This causes gnuplot to create a plot window and show the plot in the graphical user interface of our operating system. Thus, we create the plot twice, first as an image file and then as a plot window. This is done mainly for convenience, alternatively we could simply create the plot as an image and then open the image using an image viewer.

```
1 set terminal png
2 set output "generatedValues.png"
3
4 set xlabel "Time [s]"
5 set ylabel "Various values"
6
7 set key top right
8 set grid
9
10 # this is a comment
11 set yrang [-0.1:1.1];
12
13 plot \
14     "postProcessing/patchAverage01/0/surfaceFieldValue.dat" using 1:5 \
15         with lines title "value_1", \
16     "postProcessing/patchAverage02/0/surfaceFieldValue.dat" using 1:2 \
17         with lines title "value_2"
18
19 set terminal x11
20 replot
```

Listing 425: Plot data generated by a function object.

²¹³See <http://gnuplot.info/>

63.1.2 The data file

The gnuplot script shown in Listing 425 can deal with lightly formatted output as shown in Listing 426. The heading comments, indicated by the # character, pose no problem for gnuplot to identify the data. Similarly, the parentheses indicating the velocity data do not interfere.

```
user@host:~/OpenFOAM/user-12/run/pimpleFoam/testCase$ head postProcessing/patchAverage01/0/
    surfaceFieldValue.dat
# Selection type : patch inlet
# Faces : 16
# Area : 4.000000e-04
# Time      areaAverage(s)  areaAverage(U)
0           1.000000e+00  (0.000000e+00 0.000000e+00 2.000000e+00)
0.000119617 1.000000e+00  (0.000000e+00 0.000000e+00 2.000000e+00)
0.000262608 1.000000e+00  (0.000000e+00 0.000000e+00 2.000000e+00)
0.000433211 1.000000e+00  (0.000000e+00 0.000000e+00 2.000000e+00)
...
...
```

Listing 426: Lightly formatted data generated by a function object.

63.1.3 Command line execution

Listing 427 shows how gnuplot is executed from the command line. We pass two options, first we tell gnuplot to persist, i.e., the plot window(s) remain open after gnuplot has finished. The second option is used to pass an input script. By design, gnuplot is an interactive command-line program. However, using input scripts is more convenient for our purposes.

```
user@host:~/OpenFOAM/user-12/run/pimpleFoam/testCase$ gnuplot -p -c plotValues.gp
```

Listing 427: Running *gnuplot* in our case directory. The *-p* command line options (*p* for *persist*) lets the plot window remain opened after gnuplot has finished. The *-c* command line argument is used to pass an input script to gnuplot.

Part VII

External Tools

Besides *paraView*, there are a number of other useful tools, which do not come from the OpenFOAM Foundation. This section will cover such tools.

64 *pyFoam*

pyFoam is a collection of useful Python²¹⁴ scripts. These scripts are mostly written to serve one specific task. Further information can be found at http://openfoamwiki.net/index.php/Contrib_PyFoam.

64.1 Installation

The installation of *pyFoam* is described at http://openfoamwiki.net/index.php/Contrib_PyFoam#Installation. The major prerequisite for the use of *pyFoam* is, that a Python interpreter is installed. To check if a Python interpreter is installed on the system, simply type `python --version` in the Terminal. If a version number is displayed, like Python 2.7.3, then Python is installed. Otherwise, the operating system would display an error message, stating that the command `python` can not be found.

Further information about Python are found at <http://python.org/> and <http://docs.python.org/>.

64.2 *pyFoamPlotRunner*

The script *pyFoamPlotRunner* starts a simulation and plots the residuals like Fluent would do.

```
user@host:~/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/columnCase$ pyFoamPlotRunner.py  
twoPhaseEulerFoam
```

Listing 428: Calling *pyFoamPlotRunner*

64.2.1 Plotting options

Listing 429 shows the plotting options offered by *pyFoam*.

```
What to plot  
-----  
Predefined quantities that the program looks for and plots  
  
--no-default          Switch off the default plots (linear, continuity and  
                      bound)  
--no-linear            Don't plot the linear solver convergence  
--no-continuity        Don't plot the continuity info  
--no-bound             Don't plot the bounding of variables  
--with-iterations      Plot the number of iterations of the linear solver  
--with-courant          Plot the courant-numbers of the flow  
--with-execution        Plot the execution time of each time-step  
--with-deltat           'Plot the timestep-size time-step  
--with-all              Switch all possible plots on
```

Listing 429: Plotting flags of the *pyFoamPlot** utilities

64.3 *pyFoamPlotWatcher*

The script *pyFoamPlotWatcher* is intended to visualize solution data (e.g. residuals, time steps, Courant number, etc.) after the simulation has finished. This requires that the solver output is written into a file, see Section 12.1.1. *pyFoamPlotWatcher* does essentially the same job as *pyFoamPlotRunner* with the difference that the former tool is for finished simulations and the latter monitors a running simulation. So the description of the features of *pyFoamPlotWatcher* holds also true for *pyFoamPlotRunner*.

```
user@host:~/OpenFOAM/user-2.1.x/run/twoPhaseEulerFoam/columnCase$ pyFoamPlotWatcher.py LOGFILE
```

Listing 430: Calling *pyFoamPlotWatcher*

By default *pyFoamPlotWatcher* plots the curves of the residuals, continuity information and bounded variables. With options several other curves can be plotted (e.g. time step, iterations, Courant number, etc.). With regular expressions user specified data can be extracted from the log file.

²¹⁴Python is an interpreted programming language.

Listing 431 shows the invocation of *pyFoamPlotWatcher* to plot additionally to the default selection also the Courant number. The processing of the solver output stored in the file `LOGFILE` is limited with the option `--end` with a specific value – 0.1 s in this case. There is also a `--start` option. The plot created by the command in Listing 431 is shown in Figure 179.

```
pyFoamPlotWatcher.py LOGFILE --end=0.1 --with-courant
```

Listing 431: Calling *pyFoamPlotWatcher* with some options

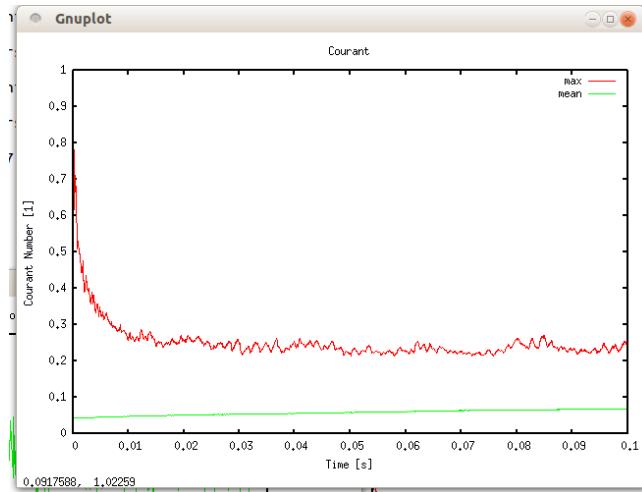


Figure 179: The Courant number plotted with *pyFoamPlotWatcher*.

64.3.1 Custom regular expressions

With regular expressions *pyFoamPlotWatcher* can extract arbitrary data from the solver output. This section elaborates this feature by the example of plotting the Courant number based on the relative velocity of a two-phase solver.

General information

pyFoamPlotWatcher has no option to display the history of the Courant number based on `Ur`, the relative velocity between the phases. Listing 432 shows some lines of the solver output of the two-phase solver *twoPhaseEulerFoam*. The line in red displays the Courant number based on the relative velocity `Ur`. The line above the red colored line displays the Courant number based on the mixture velocity, see Section 68.6.4 and 68.6.4 for information on the definition of the Courant number and the Courant number of the two-phase solver *twoPhaseEulerFoam*.

```
DILUPBiCG: Solving for k, Initial residual = 0.000824921, Final residual = 1.47595e-06, No
Iterations 2
ExecutionTime = 70870.7 s ClockTime = 71186 s

Calculating averages

Courant Number mean: 0.103485 max: 0.422517
Max Ur Courant Number = 0.448791
deltaT = 0.00380929
Time = 72.5848

MULES: Solving for alpha1
MULES: Solving for alpha1
```

Listing 432: Some lines of the solver output of *twoPhaseEulerFoam*

Extracting the information

To extract the information from the log file we need to create a file containing the regular expression.

```
{"expr":"Max Ur Courant Number = (%f%)","name":"UrCoNum"}
```

Listing 433: The file `customRegexp`

If `pyFoamPlotWatcher` finds a file named `customRegexp` in the case directory, this file will be processed automatically. If the file containing the regular expression has another name or is located in another place the option `--regexp-file=REG_EXP_FILE` can be used to specify the path to that file.

Listing 433 contains comma separated entries ("expr" and "name"). The values are separated by a colon from the name of the entries (e.g. "name": "UrCoNum"). The first entry contains the regular expression to extract the data. The second provides the name of the extracted data, but this entry can be omitted.

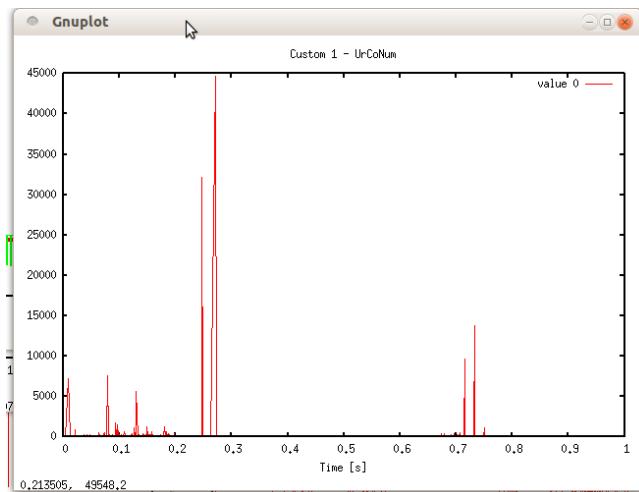


Figure 180: The Courant number based on the relative velocity plotted with `pyFoamPlotWatcher`

The absurdly high value of the Courant number indicates that the simulation did not go well. The need for plotting the Courant number based on `Ur` emanated from a trouble-shooting episode. Thus this section was written to preserve the gained knowledge.

64.3.2 Custom regular expression revisited

The plotting utilities of `pyFoam` (`pyFoamPlotRunner` and `pyFoamPlotWatcher`) accept custom regular expressions also in a different format than the format of Listing 433. This new format was introduced with version 0.5.3. See http://openfoamwiki.net/index.php/Contrib_PyFoam#Plotting_with_customRegexp_files for further information. The new format looks resembles an OpenFOAM dictionary.

Listing 434 shows an example of the solver output that will be post-processed. The goal is to draw curves of the quantities of the red line. Listing 435 shows the corresponding regular expression. The plotting utilities of `pyFoam` offer the `--dump-custom-regexp` option to generate the custom regular expression in the new format from the old format. Listing 436 is the result of this operation.

```
DILUPBiCG: Solving for beta, Initial residual = 0.000307666, Final residual = 7.36162e-08, No
Iterations 2
DILUPBiCG: Solving for T, Initial residual = 0.000514273, Final residual = 2.57279e-07, No
Iterations 1
Concentration = 0.0509085 Min T = 0.00498731 Max T = 0.218343
Bubble load = 0.00623198 Min beta = 0 Max beta = 0.0677904
Time = 19.96
```

Listing 434: Some lines of the solver output to post-process

```
{"expr":"Concentration = (%f%) Min T = (%f%) Max T = (%f%)","name":"Concentration","titles":["avg","min","max"]}
```

Listing 435: The custom regular expression in the odl format

```
Custom01
{
    accumulation first;
    enabled yes;
    expr "Concentration = (%f%) Min T = (%f%) Max T = (%f%)";
    name Custom01_Concentration;
    persist no;
    raisit no;
    theTitle "Custom 1 - Concentration";
    titles
    (
        avg
        min
        max
    );
    type regular;
    with lines;
    xlabel "Time [s]";
}
```

Listing 436: The custom regular expression in the new format

64.3.3 Special treatment of certain characters

Note that the solver output we processed so far contained no parentheses. The parentheses are interpreted by the regular expression. In order to deal with parentheses in the solver output they need to be escaped properly. The same is true for brackets. So the following example is also valid, when brackets are contained in the solver output that is to be processed with regular expressions.

Listing 437 shows some lines of solver output of twoPhaseEulerFoam. The line marked in red contains parentheses. In order to post-process these lines with regular expressions these parentheses need to be escaped in the regular expression. Listing 438 shows the corresponding regular expression. Note the escaped parentheses marked in red.

```
Time = 19.9957

MULES: Solving for alpha1
MULES: Solving for alpha1
Dispersed phase volume fraction = 0.0168317 Min(alpha1) = 3.92503e-87 Max(alpha1) = 0.2
GAMG: Solving for p, Initial residual = 9.46269e-05, Final residual = 1.65711e-06, No
       Iterations 1
time step continuity errors : sum local = 2.08826e-05, global = 4.51574e-08, cumulative =
-0.0334048
```

Listing 437: Some lines of the solver output of *twoPhaseEulerFoam*

```
{"expr":"Dispersed phase volume fraction = (%f%) Min\\(alpha1\\) = (%f%) Max\\(alpha1\\) = (%f%)",
  "name":"Volume fraction","titles":["avg","min","max"]}
```

Listing 438: The regular expression to extract the information about the volume fraction

Not only the parentheses have a special meaning in regular expressions. An internet search²¹⁵ or detailed knowledge on regular expressions will yield the knowledge which characters have to be escaped.

64.3.4 Ignoring stuff

Listing 438 extracts three numbers from the line marked in Listing 437. Using this regular expression plots all three curves. If we are interested in only the first number – the average volume fraction – we replace the second and third (%f%) with a .+ to ignore the second and third number. In this special case this seems an overkill

²¹⁵E.g. <http://stackoverflow.com/questions/399078/what-special-characters-must-be-escaped-in-regular-expressions>

– we could also delete parts of the expression since we are only interested in the first number – but if we are interested in the first and the third number, then we need to ignore the second number.

64.3.5 Producing images

The Figures 179 and 180 are screenshots of the images plotted by *pyFoamPlotWatcher*. However, there is the option `--hardcoded` that tells the *pyFoam* plot utilities to save the plots on the disk. By default a PNG image is produced but with the option `--format-of-hardcopy=HARDCOPYFORMAT` other formats can be chosen.

Figure 181 shows the plot produced by the regular expression of Listing 438.

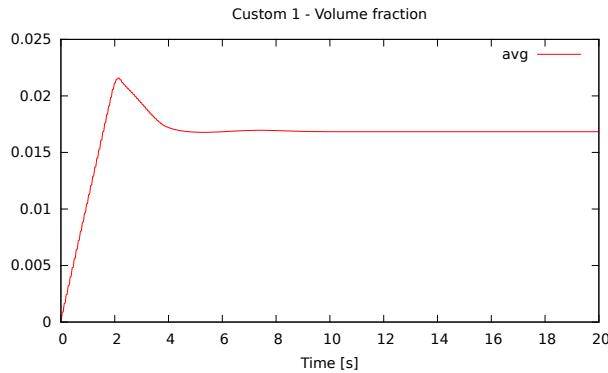


Figure 181: The average volume fraction plotted with *pyFoamPlotWatcher* and a custom regular expression

64.3.6 Writing data

Producing images is often not enough for post-processing. The option `--write-files` causes *pyFoam* to write the extracted data to the hard drive. Thus the extracted data can be processed by other programs.

64.3.7 Case analysis

The option `--with-all` generate a number of plots that can be helpful to examine the performance of simulation case. See Listing 429 for an explanation of the available plots.

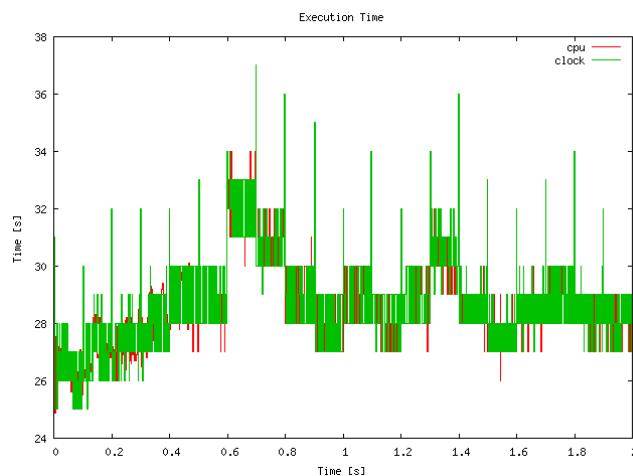


Figure 182: The execution time plotted over time with *pyFoamPlotWatcher*. The occasional writing of the data to harddisk are clearly visible as spikes in the execution time.

64.4 *pyFoamClearCase*

As the name implies, *pyFoamClearCase* cleans the case directory. This script deletes all time directories save the *0* directory. By the use of command line options, a finer control of the actions of *pyFoamClearCase* is possible. Some of these options are:

- keep-last** keep the last time step
- keep-regular** keep all time steps
- after=T** delete all time steps for $t > T$
- remove-processor** delete the *processor** directories

The script is invoked by typing its name in the Terminal. Listing 439 shows how this script is executed. The options cause *pyFoamClearCase* to keep the last time directory and to remove all *processor** folders.

```
pyFoamClearCase.py . --keep-last --remove-processor
```

Listing 439: Calling *pyFoamClearCase*

Note the file ending *.py* after the name of the script. This ending indicates, that the script is written in Python. It also indicates, that *pyFoamClearCase* is an executable script rather than a program on its own.

64.5 *pyFoamCloneCase*

This script is used to copy a case. By default the *0*, the *constant* and the *system* directory are copied. Additionally, there are various command line arguments to control the operation of the script, e.g. copy also the latest time step or the *processor** directories.

64.6 *pyFoamDecompose*

This script is used to decompose the computational domain. Other than the tool *decomposePar*, this script does not need an existing *decomposeParDict*. This script receives command line arguments, generates the *decomposeParDict* and calls *decomposePar*.

In Listing 440 the script is called with two arguments. The first argument is the path to the case directory. In this case the dot refers to the current directory. The second argument is the number of sub-domains. From this arguments, *pyFoamDecompose* creates a *decomposeParDict*. The first argument is necessary to tell the script where to save the newly created file. The second argument is the most fundamental information for domain decomposition – the number of sub-domains.

There is a large number of additional arguments which allow to exert more control over the way the domain is decomposed.

```
pyFoamDecompose.py . 4
```

Listing 440: Invocation of *pyFoamDecompose*

Listing 441 contains the *decomposeParDict* created by the command of Listing 440.

```
// * * * * * * * * * //
FoamFile
{
    version 0.5;
    format ascii;
    root "ROOT";
    case "CASE";
    class dictionary;
    object nix;
}
method scotch;
numberOfSubdomains 4;
scotchCoeffs
```

```
{  
}
```

Listing 441: The file `decomposeParDict` generated by `pyFoamDecompose decomposeParDict`

The output of `pyFoamDecompose` is stored in the file `Decomposer.logfile`.

64.7 `pyFoamDisplayBlockMesh`

If there is a problem with mesh topology and one isn't able to find the error in the `blockMeshDict`, this tool can be of great help. `pyFoamDisplayBlockMesh` does exactly what the name of the tool suggests. It reads `blockMeshDict` and displays the topology of the mesh. One might think, that that's exactly what is described in Section 17.6.2 (display the blocks with `paraView`). However, if the definition of the mesh is erroneous, `blockMesh` will not create a mesh and `paraView` is therefore not able to display the blocks.

`pyFoamDisplayBlockMesh` is a tool that allows the user to visualise a faulty mesh. This is of great help to find e.g. an error in the block definition, especially when there are more than one blocks. In Figure 183 a screenshot of the GUI of this tool is shown. In the main panel the vertices and the edges are displayed. With the two sliders below single blocks as well as patches can be marked and coloured. The local axes of a single block are displayed as tubes labelled with the corresponding names of the axes.

The blocks shown in Figure 183 have a faulty definition, so `blockMesh` produces an error message instead of creating a mesh. With the help of this tool, the cause for the error is easily found. The marked block should be in the right part of the geometry, so vertex number 5 should not be part of this block.

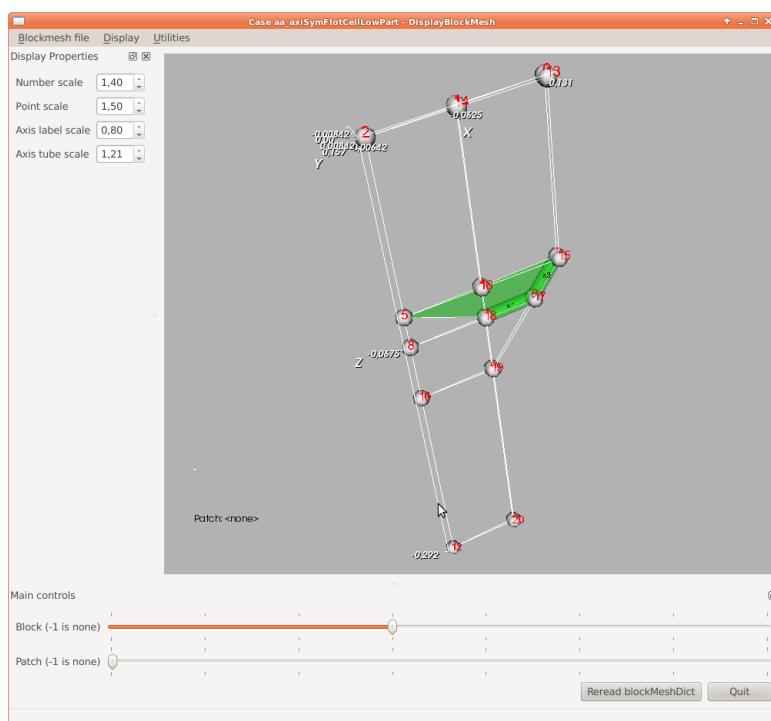


Figure 183: Screenshot of `pyFoamDisplayBlockMesh`

Right of the main panel the output of the standard meshing utilities `blockMesh` and `checkMesh` can be displayed (not shown in the picture). These utilities can be executed from the menu of this tool. Moreover, the `blockMeshDict` can be edited with this tool.

64.8 `pyFoamCaseReport`

The tool `pyFoamCaseReport` generates a summary of the simulation case. The amount of information displayed can be controlled by command line flags. Listing 442 shows how to create a full summary of a case. However, the full information lies within the dictionaries of the case. This tool provides only selected information.

```
pyFoamCaseReport.py --full-report .
```

Listing 442: Create a summary of the case with *pyFoamCaseReport*

65 *swak4foam*

The name *swak4foam* comes from *SWiss Army Knife for Foam*. *swak4foam* evolved from a collection of tools like *groovyBC*, *funkySetFields* and *simpleFunctionObjects*. The documentation of *swak4foam* is located at <http://openfoamwiki.net/index.php/Contrib/swak4Foam>.

65.1 Installation

To install *swak4foam* one needs to download the source code and compile them. The source code of *swak4foam* is managed by the use of a *subversion*²¹⁶ repository. Listing 443 shows how the source code is downloaded by subversion. The first command changes the working directory of the terminal to `~/OpenFOAM`. The second command creates a directory named `swak4foam`. The third command changes the working directory of the terminal to the newly created folder and the last commands actually downloads the source code to the current directory.

```
cd ~/OpenFOAM
mkdir swak4foam
cd swak4foam
svn checkout https://openfoam-extend.svn.sourceforge.net/svnroot/openfoam-extend/trunk/
  Breeder_2.0/libraries/swak4Foam/
```

Listing 443: Installation of *swak4foam*

After downloading, the sources need to be compiled by calling `Allwmake`.

65.2 *simpleSwakFunctionObjects*

simpleSwakFunctionObjects is an extension of *simpleFunctionObjects*. The functions of this library are used to post process data and extend functionality of OpenFOAM.

65.2.1 Extrema of a field quantity

If only the extrema of a field quantity are of interest, the tools of OpenFOAM (*probes*, *sample*) are of little use. One way of solving this problem could be, to modify the solver to write the extrema to the standard output. In Listing 444 some line of the standard output of *twoPhaseEulerFoam* are shown. This solver prints the mean value as well as the extrema of the volume fraction of the dispersed phase. The corresponding lines of source code can serve as a blueprint for a solver modification.

However, if the user is not inclined to modify and compile OpenFOAM solvers, *simpleSwakFunctionObjects* provide the solution.

```
DILUPBiCG: Solving for alpha, Initial residual = 3.48391e-05, Final residual = 2.94111e-12,
  No Iterations 2
Dispersed phase volume fraction = 0.00824276  Min(alpha) = -1.66816e-19  Max(alpha) = 0.6
DILUPBiCG: Solving for alpha, Initial residual = 3.71563e-07, Final residual = 8.16115e-14,
  No Iterations 2
Dispersed phase volume fraction = 0.00824276  Min(alpha) = -3.31819e-19  Max(alpha) = 0.6
```

Listing 444: Solver-Ausgabe von *twoPhaseEulerFoam*

swakExpression

The function to do the job is called *swakExpression*. This function is part of the library *libsimpleSwakFunctionObjects*. Listing 445 shows how this function is set up as a function object in the file `controlDict`. In this example the minimal value of the field `alpha` is saved. Notice the statement in last line of the Listing. This statement tells the solver to use the specified library. This library contains the function `swakExpression`. See Section 11.3.3 for further information about using external libraries.

²¹⁶*subversion*, abbreviated SVN, is a version control software to manage software projects.

```

functions
{
    minAlpha
    {
        type swakExpression;
        verbose true;
        accumulations ( min );
        valueType internalField;
        expression "min(alpha)";
    }
}

libs ("libsimpleSwakFunctionObjects.so");

```

Listing 445: Definition of the function *swakExpression* in the file **controlDict**

Keywords

This section explains the most important keywords of Listing 445.

type specifies the type the function object

verbose a switch that controls whether the generated data is to be printed on the solver output or not. The data is written into a file anyway.

accumulations allowed entries: {**min**,**max**,**average**,**sum**}. Quote from the CFD-Online Forum²¹⁷: *accumulations is only needed if you need "a single number" to print to the screen. For instance if you use a swakExpression-FO to print the maximum and minimum of your field to the screen.*

valueType defines the type of the geometric region on which the function is applied. Allowed entries: {**internalField** **cellSet** **faceZone** **patch** **faceSet** **set** **surface** **cellZone**}

expression defines the quantity that is sought for. This can be a simple statement or a formula computing a quantity.

²¹⁷ <http://www.cfd-online.com/Forums/openfoam/103504-swak4foam-calculating-velocity-transformations.html>

66 *blockMeshDG*

blockMeshDG is a modification of the meshing tool *blockMesh* to allow for double grading. Double grading means, that the ratio between the discretisation length of the middle and the ends of an edge is prescribed. This tool was developed by some users of OpenFOAM and is was published in the CFD-Online OpenFOAM Forum (<http://www.cfd-online.com/Forums/openfoam/70798-blockmesh-double-grading.html>). There is also a page in the OpenFOAM Wiki (http://openfoamwiki.net/index.php/Contrib_blockMeshDG).

Notice

This topic is outdated, as *blockMesh* of standard OpenFOAM already includes a feature for the discussed purpose. This was introduced with OpenFOAM-3.0²¹⁸.

66.1 Installation

The downloaded source code is ready for compilation after unpacking. All necessary entries have already been made to prevent the new utility to collide with the standard utilities of OpenFOAM. The make script creates an executable named *blockMeshDG*.

66.2 Usage

To discern between normal grading and double grading, the expansion ratio needs to be negative for double grading²¹⁹. A positive entry causes normal grading to be applied just like it is the case with the standard utility.

66.3 Pitfalls

66.3.1 Uneven number of cells

blockMeshDG obviously has a problem with an uneven number of cells. Figure 184 shows the resulting mesh, when 15 cells are used for the double graded edge. In this case, although the mesh is of bad quality, *checkMesh* reports no error. However, the output of *checkMesh* contains some indications that something is not alright.

Listing 446 shows some lines of the output of *checkMesh*. The very high aspect ratio is an indicator that something is wrong with the mesh. Also the fact that the minimum and maximum values of face area or cell volume differ by up to three orders of magnitude should lead to the same conclusion. Unfortunately, *checkMesh* issues not even a warning message.

Checking geometry...

```
Max aspect ratio = 81 OK.
Minimum face area = 3.8395e-08. Maximum face area = 1.68746e-05. Face area magnitudes OK.
Min volume = 9.59875e-11. Max volume = 4.21864e-08. Total volume = 4.92214e-05. Cell
volumes OK.
Mesh non-orthogonality Max: 42.2304 average: 11.7938
Non-orthogonality check OK.
Min/max edge length = 3.079e-05 0.00508035 OK.
```

Listing 446: Some output of *checkMesh*

So far, the only solution to this problem is to use an even number of cells.

²¹⁸<https://openfoam.org/release/3-0-0/>

²¹⁹A negative entry unequal to unity causes *blockMesh* to crash with a floating point exception. Therefore, using negative entries for double grading does not alter the standard behaviour.

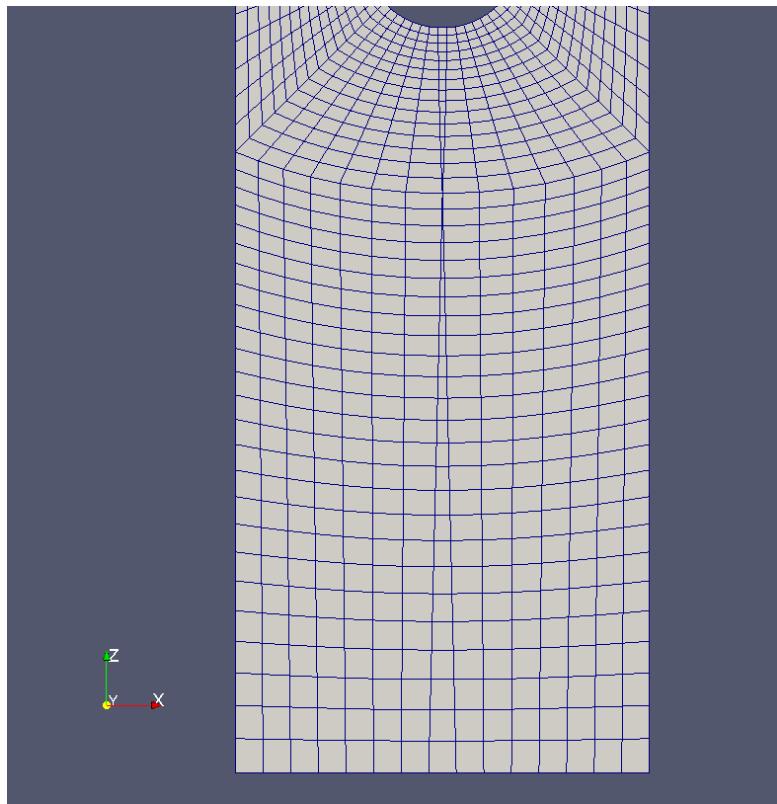


Figure 184: Double grading problem

Part VIII

Source Code & Programming

67 Understanding some C and C++

In this Section some features of the C++ programming language are discussed.

67.1 Definition vs. Declaration

In C and C++ there is the distinction between the declaration and the definition of a variable. Briefly explained, declaring a variable only tells the compiler that the variable exists and has a certain type. The declaration does not specify what the variable actually is.

A definition also tells the compiler what exactly a variable is. This does not necessarily mean that the variable is assigned a value.

Further information on that matter can be found in [59, 39] or http://www.cprogramming.com/declare_vs_define.html.

67.1.1 A classy example

In Listing 447 we define the class `phaseInterface`, i.e. we tell the compiler what the class looks like (data members, methods, etc.). Within the class `phaseInterface` we want to use the class `phaseModel`. This class already exists and is defined elsewhere, so there is no need for us to repeatedly define the class `phaseModel`. Creating our own definition of `phaseModel` would be useless and stupid.

To be able to use the existing class `phaseModel` we need to introduce this class to the compiler. In Line 4 of Listing 447 we do exactly this. We tell the compiler, that there is a class named `phaseModel`, that is all the information needed by now. This is sometimes referred to as *forward declaration*.

When we compile our class we need to make sure that we include the definition of `phaseModel`, e.g. via linking to the library in which `phaseModel` is defined.

```
1 namespace Foam
2 {
3
4     class phaseModel;
5
6     class phaseInterface
7     {
8         // lots of C++ code
9     };
10
11 }
```

Listing 447: Declaration and definition of classes

67.2 Namespaces

Namespaces are a feature of C++ to support a logical structure within the program. The basic idea behind namespaces put in simple words is *to keep things (variables and functions) visible where they need to be visible*. Like any other method of keeping things neat and tidy you could also survive without namespaces. However, to loosely quote Prof. Jasak, one of the founders of OpenFOAM: *OpenFOAM is an example of how to make proper use of C++*. Therefore, we have a closer look on namespaces in OpenFOAM.

General information about the concept of namespaces can be found here:

- <http://www.cplusplus.com/doc/tutorial/namespaces/>
- <http://www.cprogramming.com/tutorial/namespaces.html>
- <http://www.learncpp.com/cpp-tutorial/711-namespaces/>

Some OpenFOAM specific aspects related to namespaces are discussed in Section 68.2.

67.3 const correctness

The `const` keyword has several uses and using `const` has some implications.

67.3.1 Constant variables

This is the most easy part. Any variable can be declared constant by using the `const` keyword. This can precede the datatype or the variable name. Both lines in Listing 448 are correct statements.

```
const int limit = 5;
int const answer = 42;
```

Listing 448: Constant variables

67.3.2 Constants and pointers

Pointing to a constant

A pointer can be used to point to a constant variable. The pointer itself is not constant and therefore changeable. However, the keyword `const` has to be used when declaring a pointer pointing to a constant variable. However, a pointer pointing to a constant can also point to a non-constant variable.

```
int const constVar1 = 42;
const int constVar2 = 13;
int variable = 11;

const int* pointer = &constVar1;

std::cout << "The pointer points to " << *pointer << std::endl;

// change the pointer
pointer = &constVar2;

std::cout << "The pointer points to " << *pointer << std::endl;

// point to a non-constant
pointer = &variable;

std::cout << "The pointer points to " << *pointer << std::endl;
```

Listing 449: Pointing to constant variables

```
The pointer points to 42
The pointer points to 13
The pointer points to 11
```

Listing 450: Output of Listing 449

A constant pointer

A pointer can be constant regardless of the variable it points to. So, the address stored in the pointer can not be changed, the pointer will always point to the same variable. However, the variable itself can be altered. Listing 451 shows an example.

```
int variable = 11;

int* const constPointer1 = &variable;

std::cout << "The constant pointer points to " << *constPointer1 << std::endl;

variable = 79;

std::cout << "The constant pointer points to " << *constPointer1 << std::endl;
```

Listing 451: Using constant pointers

```
The constant pointer points to 11
The constant pointer points to 79
```

Listing 452: Output of Listing 451

A constant pointer to a constant

It is also possible to create a constant pointer pointing to a constant variable.

However, the last line of Listing 453 seems a bit unlogical but it isn't. To get the meaning of this line correctly, we need to read the left hand side of the assignment from right to left. First of all `constpointer4` is the name of the new variable. Secondly, `int* const` tells the compiler that the new variable is a constant pointer to an integer. This means, that the pointer itself – the location it points to – can not be changed. The last statement `const` at the very beginning of the line, means, that the variable the pointer points to can not be changed. However, `variable` is not a constant, so it can be altered anyway. The last line of Listing 453 does not change the nature of the variable `variable`, but it restricts the pointer to read-only operations. So, `variable` can be changed, but not using `constPointer4`.

```
int const constVar1 = 42;
int variable = 11;

const int* const constPointer2 = &constVar1;
const int* const constPointer4 = &variable;
```

Listing 453: A constant pointer to a constant

67.4 Function inlining

Motivation

Functions that carry out only a small number of operations are not very efficient, because the function call might take more time than the execution of all the operations. Especially if such a function is often called, the performance of the program suffers. However, writing functions is a good way to keep the code tidy.

On the one hand, functions enable the programmer to separate code in a logical way. Code that is written for a specific task is outsourced into a function with a hopefully meaningful name. This improved readability and maintainability of the code.

On the other hand is writing functions a proper way to avoid code redundancy. Tasks that are carried out repeatedly are best put into a function. Therefore, the code has to be written only once and the function can be used wherever it is necessary.

The `inline` statement

The solution for this conflict is function inlining. The `inline` statement allows the compiler to replace the function call with the function body, i.e. the operations performed by the function. This enables the programmer to keep the code tidy without the disadvantage of wasting time for time consuming function calls.

Listing 454 shows the definition of an inline function. The function body contains only two logical operations. The `inline` statement precedes the data type of the return value. So, writing inline functions is not different than writing ordinary functions.

```
inline bool Foam::pimpleControl::finalIter() const
{
    return converged_ || (corr_ == nCorrPIMPLE_);
```

Listing 454: The definition of an inline function

The use of the `inline` statement does not guarantee that the compiler replaces the function call. This depends on the compiler and the compiler settings.

OpenFOAM specifics

The OpenFOAM Code Style Guide (<http://www.openfoam.org/contrib/code-style.php>) demands from programmers to separate the definition of inline and non-inline functions.

Use inline functions where appropriate in a separate *classNameI.H* file.

Listing 455 shows the contents of the folder `pimpleControl`. Dividing the code of a program or a module into *.C and the *.H file is the common way to separate declarations from the rest of the program. The *.dep file is generated by the compiler during compilation. The fourth file in the folder is a second header file as demanded by the Code Style Guide. Listing 454 is a part of `pimpleControlI.H`.

```
pimpleControl.C  pimpleControl.dep  pimpleControl.H  pimpleControlI.H
```

Listing 455: Content of the folder `pimpleControl`

67.5 Constructor (de)construction

In object oriented programming (OOP) everything is an object. All objects are created by a constructor and if necessary destroyed by a destructor.

67.5.1 General syntax

The constructor is a method of a class like any other function or method²²⁰. However, the constructor is bound to comply some rules.

- The constructor always has the same name as its class
- The constructor has no return value

Listing 456 shows a simple class describing a point in a two-dimensional domain. This class has two constructors. The first constructor receives no arguments and initializes the member variables with zero. The second constructor receives two integer variables as arguments and uses these variables to initialize the member variables `xPos` and `yPos`.

Writing two or more constructors is possible because C++ supports function overloading. This means there can be several functions with the same name differing in the input arguments.

```
1  class Point
2  {
3      int xPos;
4      int yPos;
5
6      public:
7          Point()
8          {
9              /* constructor code */
10             xPos = 0;
11             yPos = 0;
12         }
13         Point(int x, int y)
14         {
15             xPos = x;
16             yPos = y;
17         }
18     };
```

Listing 456: A class for a 2D point

²²⁰The terms function and method are used interchangeably. However, the method indicates the use of object oriented programming. The term function is also used in procedural programming and does not automatically indicate the use of OOP.

Listing 457 demonstrates how to create new variables of the type `Point`. The first line creates a variable of the type `Point`. Because no arguments are passed in this line, the first constructor of Listing 456 is called by the compiler.

The second line creates also a point. The numbers inside the parenthesis are passed to the constructor. Therefore the second constructor of Listing 456 is called and the member variables are initialised based on the arguments.

```
1 Point p1;
2 Point p2(3, 8);
```

Listing 457: Using the class for a 2D point

67.5.2 Copy-Constructor

The copy constructor is used to create a copy of an object. The C++ compiler will create a default copy constructor if the programmer does not write one. However, the default copy constructor has restrictions regarding the handling of complex classes.

```
1 Point::Point(Point & p)
2 {
3     /* copy constructor code */
4     xPos = p.xPos;
5     yPos = p.yPos;
6 }
```

Listing 458: The copy constructor for the 2D point class

Hiding the copy constructor

A copy constructor can be hidden. Therefore, no copying is allowed. To do so, the copy constructor must be defined using a `private` modifier.

Listing 459 shows a simple example of a copy constructor that is declared as `private`. This means the copy constructor can only be called from within the class itself, i.e. only within the class `Point`.

Listing 460 shows an example from within the source code of OpenFOAM. There, the copy constructor of the class `turbulenceModel` is hidden by declaring it `private`.

```
1 class Point
2 {
3     private:
4     Point(Point & p);
5 };
```

Listing 459: Hiding the copy constructor

```
1 class turbulenceModel
2 :
3     public regIOobject
4 {
5     private:
6     // Private Member Functions
7
8     //-- Disallow default bitwise copy construct
9     turbulenceModel(const turbulenceModel&);
10
11    /* code continues */
```

Listing 460: Hiding the copy constructor

67.5.3 Initialisation list

A class in C++ can have member variables of any type. Complex classes may need some kind of initialisation to ensure all variables have a defined state. When an instance of a class is created by the constructor, the initialisation list contains all statements to initialise member variables of the class.

Listing 461 shows a simple example of a constructor with an initialisation list. Listing 576 in Section 73.2.2 shows an usage example of an initialisation list in the OpenFOAM sources.

```
1  class Rectangle
2  {
3      Point topLeft;
4      Point bottomRight;
5
6      public:
7          Rectangle()
8          {
9              topLeft = Point();
10             bottomRight = Point();
11         }
12
13     Rectangle(Point a, Point b)
14     :
15         topLeft(a),
16         bottomRight(b)
17     {
18         /* constructor code */
19     }
20 }
```

Listing 461: A constructor with an initialisation list

67.6 Object orientation

67.6.1 Abstract classes

See Section 68.10 for a discussion about the implementation of the generic turbulence models in OpenFOAM. This generic turbulence modelling makes heavy use of abstract classes and inheritance.

67.7 Templates

OpenFOAM makes heavy²²¹, clever use of templates. Templates are a language feature of C++ that allow for generic programming. An illustrative example for the use of templates in programming is the implementation of container classes, e.g. linked lists. Without the use templates, the multiplicity of possible container contents would force us to implement a vast number of specialized classes, e.g. `nodeList`, `faceList` and `cellList` for lists of nodes, faces and cells.

Such a problem could be solved by the use of multiple inheritance. This way, we would need to implement one base class for a list. The specialized classes would then inherit from the base list class and from the class of the intended content. This solution, however, has several disadvantages [5]. As complexity grows, the path via multiple inheritance is doomed to become a problem in its own, instead of alleviating or solving the original problem.

Templates offer us a way to tell a class: use the type T, which can be any type the compiler allows. Thus, we create one templated container class. Later, when we need to create lists of nodes, faces and cells, we tell the compiler to substitute T for the concrete types. The compiler then generates the appropriate code. Checks done by the compiler ensure, that specializing a valid templated class produces little to no surprises.

Listing 462 shows the use of templates. We first implement a generic list. Later, we specialize this list for the types of nodes, faces and cells. The `typedef` instruction allows us to define a convenient name. Once these names are defined, we may even stop being aware that we are using a templated class.

²²¹The command `find $FOAM_SRC -name '*.[CH]' | xargs grep 'template' | wc` yields – at the time of writing – 24646 occurrences of the word `template` in `$FOAM_SRC`. This makes 12323 occurrences within the source code itself – remember the presence and the use of the `lnInclude` directories.

```

template <class T>
class list
{
    // define a list of type T
}

typedef list<node> nodeList;
typedef list<face> faceList;
typedef list<cell> cellList;

```

Listing 462: Templated lists

OpenFOAM follows a similar strategy, who would guess from the top-level code, that `volScalarField` is in fact a templated class with three template parameters, see Listing [reflist:volScalarField](#). Besides being a more convenient name²²² we also save a lot of typing effort due to the shorter name²²³. The use of type definitions – `typedef` statements – is not mere convenience. Using the full specialisation of `GeometricField` instead of `volScalarField` translates to *hardcoding*. If the developers of OpenFOAM, at some point, decide to base `volScalarField` on the class `smartScalar` instead of `scalar`, only one line of code needs to be changed instead of thousands. Thus, the use of `typedefs` strongly supports code readability and maintainability [5].

```

typedef GeometricField<scalar, fvPatchField, volMesh> volScalarField;

```

Listing 463: The `typedef` defining `volScalarField`

67.7.1 Use of templates by OpenFOAM

Since this document is not a book on any specific topic, certain topics are addressed in a manner ranging from structured to completely random. Templates have already been discussed in a number of sections, mostly describing the use of templates on specific code examples. Since, there is no fun and varying benefit in restructuring a large document, we will give pointers to other sections in which templates are discussed:

We discuss the use of templates in Section [39.1](#) where we compare the implementation of turbulence modelling in OpenFOAM. There is a non-templated implementation, which was superseded by a templated one starting from the release of OpenFOAM-2.3.0.

We discuss the use of templates in Section [47](#) where we take a look at the implementation of Lagrangian particle tracking with a little excursion to the topic of linked lists.

The use of templates is also discussed in Section [68.3.2](#) at the example of keyword lookup from dictionary files.

67.7.2 Do not fear the template

The syntax for templated code is different from the syntax encountered in non-templated code. Here we will discuss some features of templated code, which may seem mysterious to the novice.

Template template parameter

In the introduction of this section, we stated, that the template parameter `T` is a placeholder for a concrete type. However, the template parameter may itself be a templated class. A templated template parameter is referred to as *template template parameter*. We could avoid using template template parameters, however, they help us to avoid code duplication and lead to safer code [5].

The library implementing Lagrangian particle tracking is a very illustrative example of nested templates, i.e. templated classes being used as template parameters. Furthermore, we observe deriving a class from its template parameter. Check out Section [47](#).

²²²`volScalarField` field carries roughly the same essential information as `GeometricField<scalar, fvPatchField, volMesh>`.

²²³We count 15 versus 46 characters. At the time of writing, with the command `find $FOAM_SRC -name '*.[CH]' | xargs grep 'volScalarField' | wc` we count 8752 occurrences of `volScalarField` in the source code of OpenFOAM-dev at the time of writing. This leads to an estimated 4376 occurrences in the code itself.

68 Under the hood of OpenFOAM

This section contains short code examples that in some way explain the behaviour of OpenFOAM in certain situations. All examples in this section are motivated by other parts of this manual. In some cases the source code of some applications is examined somewhere else.

68.1 Solver algorithms

See Sections 49, 52 and 54 in Part V.

68.2 Namespaces

68.2.1 Constants

Physics is full of constants. Therefore it would be nice to have a central location in which physical or mathematical constants are defined. OpenFOAM provides constants within the namespace `Foam::constant`. There the pre-defined constants are divided into the groups, such as

- electromagnetic
 - `mu0` - the magnetic permeability of vacuum
 - `epsilon0` - the electrical permittivity of vacuum
- physicoChemical
 - `R` - the universal gas constant
- mathematical
 - `pi` - π
 - `e` - the Euler number

In Listing 464 it is demonstrated how to access the constant `pi` within the source code. Listing 465 shows all the mathematical constants defined in OpenFOAM-2.2.x. From a computational performance point of view it makes perfect sense to pre-define often used constants such as two `pi`. Also note that instead of diving `pi` by 2.0 it is multiplied with 0.5. Mathematically these operations are equivalent, however, in terms of computational cost the floating point multiplication is to be preferred over the floating point division as it is much faster [1].

Also note that OpenFOAM does not define `e` and π on its own, it rather uses the constants provided by the system library. See e.g. http://www.gnu.org/software/libc/manual/html_node/Mathematical-Constants.html for the mathematical constants provided by the GNU C library (glibc). Thus `e` and `pi` are defined by accessing `M_E` and `M_PI`.

Further note that the constants are declared with the `const` specifier, which is the only sane way to define constants in C and C++.

```
1 scalar foo = constant::mathematical::pi;
```

Listing 464: A useless code example demonstrating the access to π with OpenFOAM's source code

```
1 const scalar e(M_E);
2 const scalar pi(M_PI);
3 const scalar twoPi(2*pi);
4 const scalar piByTwo(0.5*pi);
```

Listing 465: The mathematical constants provided by `mathematicalConstants.H`

In the FOAM-extend the access to e.g. the mathematical constants works the same way. Only the namespace is named `mathematicalConstants` instead of `constant::mathematical`. This is due to the fact that FOAM-extend is largely based on OpenFOAM-1.6.

68.3 Keyword lookup from dictionary

There are generally two kinds of keywords in a dictionary. There are mandatory keywords and optional ones.

68.3.1 Mandatory keywords

When a mandatory keyword is not found in a dictionary, OpenFOAM issues an error message and terminates.

Listing 466 shows the reading operation for three mandatory keywords. The function `lookup()` can be examined further in Listing 467.

```
1 #include "readTimeControls.H"
2
3 int nAlphaCorr(readInt(pimple.dict().lookup("nAlphaCorr")));
4 int nAlphaSubCycles(readInt(pimple.dict().lookup("nAlphaSubCycles")));
5 Switch correctAlpha(pimple.dict().lookup("correctAlpha"));
```

Listing 466: The content of `readTwoPhaseEulerFoamControls.H`

The code

Line 32 in Listing 467 shows, that the function `lookup()` simply calls value of `lookupEntry()`. This method also calls another method (`lookupEntryPtr()`) and does the error handling. The error handling routine clearly shows, that OpenFOAM will terminate in case the keyword wasn't found (see line 19).

```
1 const Foam::entry& Foam::dictionary::lookupEntry
2 (
3     const word& keyword,
4     bool recursive,
5     bool patternMatch
6 ) const
7 {
8     const entry* entryPtr = lookupEntryPtr(keyword, recursive, patternMatch);
9
10    if (entryPtr == NULL)
11    {
12        FatalIOErrorIn
13        (
14            "dictionary::lookupEntry(const word&, bool, bool) const",
15            *this
16        )
17        << "keyword " << keyword << " is undefined in dictionary "
18        << name()
19        << exit(FatalIOError);
20    }
21
22    return *entryPtr;
23 }
24
25 Foam::ITstream& Foam::dictionary::lookup
26 (
27     const word& keyword,
28     bool recursive,
29     bool patternMatch
30 ) const
31 {
32     return lookupEntry(keyword, recursive, patternMatch).stream();
33 }
```

Listing 467: Some content of `dictionary.C`

68.3.2 Optional keywords

A method that is used to read an optional keyword from a dictionary is usually provided with a default value. This default value is used in the case that the keyword is non-existent in the dictionary.

Listing 468 shows the reading operation for three optional keywords. The read function is called with two arguments. The first is the keyword and the second is the default value. If the function `lookupOrDefault()` finds no entry, then the default value is returned.

```

1 const bool adjustTimeStep =
2     runTime.controlDict().lookupOrDefault("adjustTimeStep", false);
3 scalar maxCo =
4     runTime.controlDict().lookupOrDefault<scalar>("maxCo", 1.0);
5 scalar maxDeltaT =
6     runTime.controlDict().lookupOrDefault<scalar>("maxDeltaT", GREAT);

```

Listing 468: The content of `readTimeControls.H`

The code

Listing 469 shows the definition of the function `lookupOrDefault()`. This function also calls another function to lookup the keyword – actually it looks for the value assigned to the specified keyword in the dictionary – and enters a conditional branch. In case the keyword was found, the corresponding value is returned (line 14). If the keyword was not found, then the default value is returned (line 18).

In Listing 469 the function is defined with four input arguments. However, in Listing 468 this function is called with only two arguments.

The solution for this contradiction can be found in the file `dictionary.H`, where this function is declared. This declaration can also be found in Listing 470. There, in lines 6 and 7, default values for two arguments are specified. Therefore, the function can be called with only two arguments – with the two arguments that have no default value²²⁴. If the function is called with all its arguments, the passed argument overrides the default value.

When declaring a function that uses default values for its arguments, the arguments without default value must precede the arguments that have a default value. Otherwise, there could be ambiguity.

```

1 template<class T>
2 T Foam::dictionary::lookupOrDefault
3 (
4     const word& keyword,
5     const T& deflt,
6     bool recursive,
7     bool patternMatch
8 ) const
9 {
10     const entry* entryPtr = lookupEntryPtr(keyword, recursive, patternMatch);
11
12     if (entryPtr)
13     {
14         return pTraits<T>(entryPtr->stream());
15     }
16     else
17     {
18         return deflt;
19     }
20 }

```

Listing 469: Some content of `dictionaryTemplates.C`

```

1 template<class T>
2 T lookupOrDefault
3 (
4     const word&,
5     const T&,
6     bool recursive=false,
7     bool patternMatch=true
8 ) const;

```

Listing 470: Some content of `dictionary.H`

²²⁴The function could also be called with three arguments, then the default value of the third argument would be overridden and the fourth argument would have its default value.

68.3.3 Superseding mandatory keywords

In some cases, a base class might demand the presence of a keyword, which some derived classes make use of and others do not. This creates the situation that a keyword-value pair must be specified, which, depending on the user's choice, has an effect or not.

However, as the keyword is demanded by the base class, it remains mandatory, regardless of the derived class' behaviour. A derived class can not alter the behaviour of its base class. Thus, in some edge cases a keyword-value pair has to be provided even though it does nothing.

The decision of how to distribute the necessary data among the base class and its derived classes may not always be as straight forward. Apart from the two obvious limiting cases: data needed only by one specific derived class, and data needed by all derived classes; the decision of what data to put where is up to the software designers.

If a sufficient number of derived classes are very similar to each other, then an intermediate base class might be warranted. With an intermediate base class, data common to all classes derived from the intermediate base class can be handed over to the intermediate base class. However, the class hierarchy of a certain model can not always exactly reflect the inner logic of data usage of that model family.

In Figure 185 we see such an example of an intermediate base class. The data members shown in the class diagram are read by their respective classes as mandatory entries. The base class `InjectionModel` reads the scalar `massTotal`, which is used to determine how many particles to inject. However, some derived injection models allow for a direct specification of the number of particles, thus rendering the mandatory value for `massTotal` moot. In these cases, the injection model issues a warning message informing the user that `massTotal` has no effect.

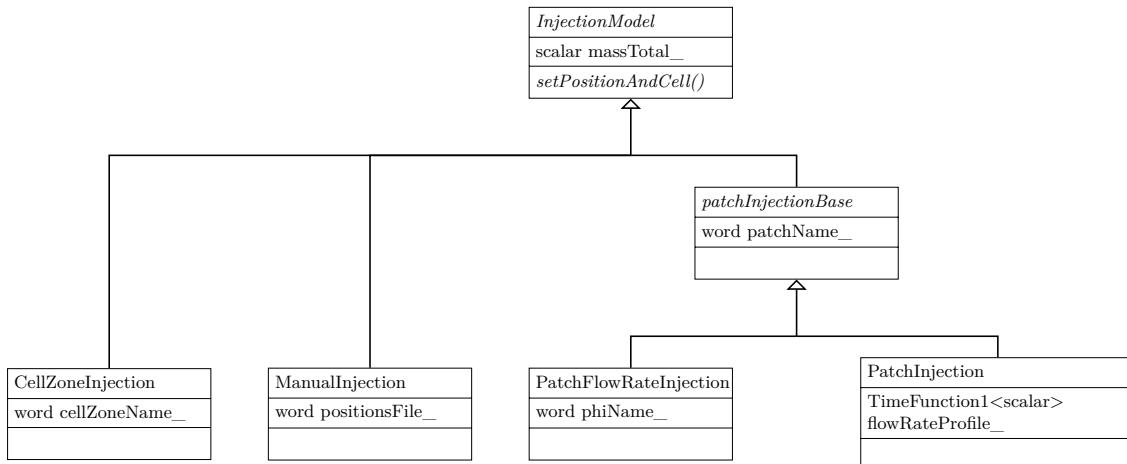


Figure 185: Class hierarchy of some injection models for Lagrangian particles. An intermediate base class is used to reduce code duplication from closely related, yet different injection models.

68.4 OpenFOAM specific datatypes

68.4.1 The `Switch` datatype

A lot of settings in dictionaries are switches to activate or deactivate a feature. Listing 471 shows the part of the source code defining all valid values. Inside the source code a switch can only be true or false, as the class `Switch` is used as a boolean data type. However, in the dictionaries a switch can have more values – provided they denote a decision. Human languages usually have more ways of answering a yes-no question, this may be the motivation for allowing this range of values for switches.

```

1 // NB: values chosen such that bitwise '&' 0x1 yields the bool value
2 // INVALID is also evaluates to false, but don't rely on that
3 const char* Foam::Switch::names[Foam::Switch::INVALID+1] =
4 {
5     "false", "true",
6     "off",   "on",
  
```

```

7   "no",      "yes",
8   "n",       "y",
9   "f",       "t",
10  "none",    "true", // is there a reasonable counterpart to "none"?
11  "invalid"
12 };
```

Listing 471: Some content of `Switch.C`

Listing 472 shows an example of how the `Switch` datatype can be used in the code. This example reads from the `transportProperties` dictionary. If no valid entry named `testSwitch` is present, then the value of the switch is set to `false`. Notice the second argument of the method `lookupOrDefault()`, it reads `Switch(false)`. This means, that a new object of the type `Switch` is created with the boolean value `false` being passed to the constructor of the class `Switch`. This new object of type `Switch` is then used – if necessary – as default value for the switch named `testSwitch`.

```
1 Switch testSwitch(transportProperties.lookupOrDefault<Switch>("testSwitch", Switch(false)));
```

Listing 472: Usage example of the `Switch` datatype

68.4.2 The `label` datatype

When examining the solution algorithms, like in Section 52.2, counters can be found. OpenFOAM uses a datatype called `label` for such counters, e.g. see Listing 338.

The following applies to versions prior to OpenFOAM-3.0

The most obvious datatype for a counter would be the integer datatype `int`. Listing 473 contains some lines of the file `label.H`, where this datatype is defined. Depending on system or compilation parameters, `label` is of the type `int`, `long` or `long long`²²⁵.

Listing 473 shows the definition of `label` in case `int` is used as the underlying datatype.

```

1 namespace Foam
2 {
3     typedef int label;
4
5     static const label labelMin = INT_MIN;
6     static const label labelMax = INT_MAX;
7
8     inline label readLabel(Istream& is)
9     {
10         return readInt(is);
11     }
12
13 } // End namespace Foam
```

Listing 473: Some content of `label.H`

The following applies to versions from OpenFOAM-3.0 onwards

OpenFOAM offers, at the time of writing, essentially two choices for the size of the `label` datatype: 32 or 64 bit. This, essentially boils down to the decision of whether to use `int32_t` or `int64_t`. Since, the data types `int`, `long` and `long long` only guarantee a minimum size²²⁶, the fixed-width integers²²⁷ `int32_t` or `int64_t` are used as a base for the `label` data type.

The label size can be selected prior to compilation with the compiler option `WM_LABEL_SIZE`, which can take the value of 32 or 64. From the compiler option and some pre-processor macros the integer type is constructed.

²²⁵In C as well as in C++ the domain of `long` is greater or equal than the domain of `int`. `long long` was defined in the C99 standard of C and was later introduced to the C++11 standard. The domain of `long long` is again larger or equal than the domain of `long`. The type `long long` uses at least 64 bit. So it is on 64 bit systems the largest possible datatype. The datatype `long` can use – depending on the compiler – 32 or 64 bit. The type `long long` guarantees the use of 64 bit.

²²⁶See <http://en.cppreference.com/w/cpp/language/types>

²²⁷See <http://en.cppreference.com/w/cpp/types/integer>

```

1 #define INT_ADD_SIZE(x,s,y) x ## s ## y
2 #define INT_ADD_DEF_SIZE(x,s,y) INT_ADD_SIZE(x,s,y)
3 #define INT_SIZE(x,y) INT_ADD_DEF_SIZE(x,WM_LABEL_SIZE,y)
4
5 #if WM_LABEL_SIZE != 32 && WM_LABEL_SIZE != 64
6     #error "label.H: WM_LABEL_SIZE must be set to either 32 or 64"
7 #endif
8
9 namespace Foam
10 {
11
12 typedef INT_SIZE(int, _t) label;
13 /* code removed for brevity */
14
15 }

```

Listing 474: Some content of `label.H`

In Listing 474, we see some helper macros, and a sanity check. The sanity check throws an error if the `label` size is not 32 or 64. The last line of Listing 474 is the actual `typedef` for the `label` data type²²⁸. The macro `INT_SIZE` is used via several helper macros and the compiler option `WM_LABEL_SIZE` to construct a fixed-width integer data type `int32_t` or `int64_t`. The `##` operator in the `INT_ADD_SIZE` macro is used to concatenate the macro's arguments²²⁹.

68.4.3 The `scalar` datatype

Similar, to the integer data type, there is an OpenFOAM-specific floating-point data type, the `scalar`. A `scalar` is depending on the compiler settings either a float or a double. In 2018²³⁰ an extended precision double was added as another option.

The basic floating-point data type `float` is 32 bits wide²³¹, i.e. its binary representation takes up 32 bits. The `double` type uses twice the number of bits, hence the name `double`. Using either `float` or `double` for computing is often referred to as using single or double precision.

OpenFOAM follows this convention by naming the corresponding compiler option `WM_PRECISION_OPTION`. This can have the value `SP` or `DP`, for single precision or double precision. The latest addition²³², long double²³³, can be chosen by the value `LP`.

Using fixed-width data types, integers as well as floating-point types, makes the application more portable, e.g. binary result files computed by one computer can be opened and processed on a different computer, provided that both OpenFOAM installations are based on the same data type size, e.g. 32 bit integers and double precision floating-points.

Listing 475 shows the definition of the type `floatScalar`, which refers to the standard data type `float`. Analogously, there is also a type `doubleFloat`, which refers to the standard data type `double`. By introducing the type `scalar`, OpenFOAM's source code is independent of the floating-point type which is actually used. The types `floatScalar` and `doubleScalar` are intermediaries to aid the selection by the user prior to compilation.

The types `floatScalar` and `doubleScalar` are mainly used by low-level code tasked with input and output (I/O). No applications (solvers and utilities) and no high-level libraries, e.g. turbulence, use these data types. All high-level code is abstracted from the actual floating-point data type.

```

1 namespace Foam
2 {
3
4     typedef float floatScalar;
5
6     /* code removed for brevity */

```

Listing 475: Some content of `floatScalar.H`

²²⁸See <https://en.wikipedia.org/wiki/Typedef>

²²⁹See https://en.wikibooks.org/wiki/C_Programming/Preprocessor_directives_and_macros

²³⁰See <https://github.com/OpenFOAM/OpenFOAM-dev/commit/d82cc36c5af97e799a82fadf455e06d192ae1e65>

²³¹See https://en.wikipedia.org/wiki/IEEE_754

²³²See footnote 230

²³³See https://en.wikipedia.org/wiki/Long_double

Listing 476 shows the relevant lines of the file `scalar.H` which defines the type `scalar` based on the evaluation of `WM_SP` or `WM_DP`. Depending on whether `WM_SP` or `WM_DP` has been defined, the type `scalar` refers to `floatScalar` or `doubleScalar`.

```

1 #if defined(WM_SP)
2
3 // Define scalar as a float
4 namespace Foam
5 {
6     typedef floatScalar scalar;
7     /* code removed for brevity */
8 }
9
10 #elif defined(WM_DP)
11
12 // Define scalar as a double
13 namespace Foam
14 {
15     typedef doubleScalar scalar;
16     /* code removed for brevity */
17 }
18
19 #endif

```

Listing 476: Some content of `scalar.H`

68.4.4 The `tmp<>` datatype

There is a special class for all temporary data. Because there is no memory management in C++ the programmer has to delete unused variables. The author assumes that the `tmp` class for all kinds of temporary data is meant to distinguish temporary variables from other variables.

The `tmp` class uses a technique called generic programming.

68.4.5 The `IOobject` datatype

The class `IOobject` handles the behaviour of all kinds of data structures. Although, there are no variables of the type `IOobject`, understanding some parts of this class will help to understand certain aspects of OpenFOAM.

Listings 477 and 478 show some examples from the sources of the solver *twoPhaseEulerFoam*. There, the class `IOobject` is used in the creation of fields as well as the creation of dictionary objects.

In Listing 477 two `volScalarField` variables are created. The constructor of the class `volScalarField` receives two arguments. In both cases the first argument is an `IOobject`.

Let us read the arguments of the `IOobject` constructor call. The first argument is the name of the `IOobject`. The two last arguments are the read and write flags.

In the case of the fields `alpha1` and `alpha2` the read and write flags are different. The field `alpha1` is read at the start of the application. The write flag causes the field `alpha1` to be written to disk, whenever the data is written. The field `alpha2` on the contrary is not written to disk and the application also does not try to read it.

The name of the `IOobject` is also the name which the application uses as file name. Therefore the field `alpha1` will be written to disk in a file named `alpha1`. Also when the application tries to read `alpha1`, it tries to read from the file `alpha1`.

```

1 volScalarField alpha1
2 (
3     IOobject
4     (
5         "alpha1",
6         runTime.timeName(),
7         mesh,
8         IOobject::MUST_READ,
9         IOobject::AUTO_WRITE
10    ),
11    mesh
12 );

```

```

13
14 volScalarField alpha2
15 (
16     IOobject
17     (
18         "alpha2",
19         runTime.timeName(),
20         mesh,
21         IOobject::NO_READ,
22         IOobject::NO_WRITE
23     ),
24     scalar(1) - alpha1
25 );

```

Listing 477: Definition of volume fraction fields in `createFields.H`

Listing 478 shows the definition of an `IOdictionary`. The constructor of the class `IOdictionary` receives also an `IOobject` as argument. Again, the name of the `IOobject` is also the name of the file the application tries to read when reading in the dictionary. Notice also the read flag. This flag causes the application to check if the file has been modified during run-time. If this is the case, the file will be read again.

```

1 IOdictionary ppProperties
2 (
3     IOobject
4     (
5         "ppProperties",
6         runTime.constant(),
7         mesh,
8         IOobject::MUST_READ_IF_MODIFIED,
9         IOobject::NO_WRITE
10    )
11 );

```

Listing 478: Definition of a dictionary in `readPPProperties.H`

Read & write flags

In the constructor so called read and write flags are provided as arguments, see e.g. Lines 8 and 9 of Listing 478.

Listing 479 shows the available read/write flags. The flag `MUST_READ_IF_MODIFIED` was introduced with OpenFOAM-2.0.0²³⁴. The available read flags offer quite some flexibility.

```

1 // - Enumeration defining the valid states of an IOobject
2 enum objectState
3 {
4     GOOD,
5     BAD
6 };
7
8 // - Enumeration defining the read options
9 enum readOption
10 {
11     MUST_READ,
12     MUST_READ_IF_MODIFIED,
13     READ_IF_PRESENT,
14     NO_READ
15 };
16
17 // - Enumeration defining the write options
18 enum writeOption
19 {
20     AUTO_WRITE = 0,
21     NO_WRITE = 1
22 };

```

Listing 479: Definition of the object states and read/write flags of `IOobject` in `IOobject.H`

²³⁴<http://www.openfoam.org/version2.0.0/runtime-control.php>

Pitfall: Solving for a NO_READ field

The author stumbled across an interesting error during modifying a solver. This falls into the category copy & paste error. However, the author wishes to share the experience.

If we like to extend an existing solver with a scalar transport equation, we need to create the field we want to solve for, in our case a `volScalarField`. There are plenty of files from which we can copy the relevant code. Listing 480 shows an example. The name of the field was changed as was the write flag. Since we want to create colourful images, the write flags needs to be set to `AUTO_WRITE`. However, no care was taken of the read flag.

```
1  volScalarField T
2  (
3      IOobject
4      (
5          "T",
6          runTime.timeName(),
7          mesh,
8          IOobject::NO_READ,
9          IOobject::AUTO_WRITE
10     ),
11     mesh,
12     dimensionedScalar("zero", dimensionSet(0, 0, 0, 0, 0), 0.0)
13 );
```

Listing 480: Creating a field with an `IOobject::NO_READ` read flag.

After we created out field `T`, and composed the transport equation for this field (`TEqn`), we want to solve this transport equation. However, the call `TEqn.solve()` yields some unexpected outcome. Listing 481 shows the error message issued by OpenFOAM.

```
--> FOAM FATAL ERROR:

valueInternalCoeffs cannot be called for a calculatedFvPatchField

on patch inlet of field T in file "/home/user/OpenFOAM/user-2.3.x/run/foo/case/0/T"
You are probably trying to solve for a field with a default boundary condition.

From function calculatedFvPatchField<Type>::valueInternalCoeffs(const tmp<scalarField>&)
const
in file fields/fvPatchFields/basic/calculated/calculatedFvPatchField.C at line 154.

FOAM exiting
```

Listing 481: Error message of OpenFOAM caused by trying to solve for a no-read field.

At first, the message seems counter-intuitive, since we checked the boundary conditions in the file `T` over and over. Also changing the boundary conditions does not produce a different outcome.

The error message says, we wanted to solve for a field with default boundary conditions. This is perfectly true, however, we need to find out why. Since, we created the field with a `NO_READ` flag, no boundary conditions were provided. Thus, OpenFOAM assigns default boundary conditions. This is also the case if we leave patches in the `boundaryField` dictionary of the files that are read from disk.

Continued Problems

Changing the read flag in Listing 480 alone does not solve the problem. Changing the read flag from `NO_READ` to `MUST_READ` yields the same error message as in Listing 481.

The reason for this are the arguments of the constructor call in Listing 480. If a field is to be read from disk, we must not pass a value (Line 12 in Listing 480).

For our modified solver to work, we need to remove the argument passed in Line 12 in Listing 480. The developers of OpenFOAM have foreseen this case, thus OpenFOAM issues a warning message, when a value is passed to a constructor with a `MUST_READ` or `MUST_READ_IF_MODIFIED` read flag, see Listing 482.

```
--> FOAM Warning :
From function GeometricField<Type, PatchField, GeoMesh>::readIfPresent()
```

```

in file /home/user/OpenFOAM/OpenFOAM-2.3.x/src/OpenFOAM/lnInclude/GeometricField.C at line
 108
read option IOobject::MUST_READ or MUST_READ_IF_MODIFIED suggests that
a read constructor for field T would be more appropriate.

```

Listing 482: Warning message of OpenFOAM caused by inappropriate constructor arguments concerning read flags and initial values.

Renaming an **IOobject**

When constructing a field from components, as it is done in Listings 477 or 480 in this section, we explicitly provide a name for the **IOobject**, which is in turn used for the registry and the file name when writing the field to disk.

Listing 483 shows a coded functionObject which computes the Mach number for the gas phase. This code is quite simple, we lookup the fields for (gas) velocity, pressure and (gas) density, and compute the Mach number using the same formula we found in the already existing **MachNo** functionObject.

```

1 computeMachNoGas
2 {
3     libs ("libutilityFunctionObjects.so");
4     type coded;
5
6     codeWrite
7     #{
8         // Lookup
9         const volVectorField& Ugas = mesh().lookupObject<volVectorField>("U.gas");
10        const volScalarField& p = mesh().lookupObject<volScalarField>("p");
11        const volScalarField& rhoGas = mesh().lookupObject<volScalarField>("rho.gas");
12
13        // Compute
14        volScalarField MachNoGas(mag(Ugas)/sqrt(p*rhoGas));
15
16        // Write
17        MachNoGas.write();
18    #};
19 }

```

Listing 483: Computing a gas-phase Mach number using a coded functionObject.

Listing 484 shows the output of the code in Listing 483 as it appears on disk. There, the name of the file containing our computed Mach number was constructed by OpenFOAM from the expression we used in Line 14.

```

user@host:~/OpenFOAM/user-12/run/multiphaseEuler/testCase$ ls 0.1/
alpha.gas   alphaRhPhi.gas   alpha.solids   alphat.gas
k.gas   '(mag(U.gas)|sqrt((p*rho.gas)))'   nut.gas   omega.gas   p
phi   phi.gas   p_rgh   T.gas   T.solids   U.gas   uniform

```

Listing 484: The contents of a solved-for time step with the computed gas-phase Mach number. Note the unusual file name.

While this constructed name makes it relatively easy to identify the field, it is not very practical. Thus, a nicer name would be preferable. This is where Listing 485 has a solution.

First, we create our Mach number field as a non-constant field. And then, we call the **rename()** function, which is a method of the **IOobject** class. Line 15 shows the call of the **rename()** function, which takes the new name as its sole argument. Since, we are modifying the properties of the field, it can not be a **const** type. The field will then be written to disk with this new name, which makes handling much easier²³⁵.

```

1 computeMachNoGas
2 {
3     libs ("libutilityFunctionObjects.so");
4     type coded;

```

²³⁵We invite the reader to imagine the amount of escape characters that would be needed, if we wanted to perform any operation on this file in a Linux Terminal using its constructed name.

```

5   codeWrite
6   #{
7     // Lookup
8     const volVectorField& Ugas = mesh().lookupObject<volVectorField>("U_gas");
9     const volScalarField& p = mesh().lookupObject<volScalarField>("p");
10    const volScalarField& rhoGas = mesh().lookupObject<volScalarField>("rho_gas");
11
12    // Compute
13    volScalarField MachNoGas(mag(Ugas)/sqrt(p*rhoGas));
14    MachNoGas.rename("MachNoGas");
15
16    // Write
17    MachNoGas.write();
18  #};
19 }

```

Listing 485: Computing a gas-phase Mach number and assigning a proper name.

68.4.6 Random stuff

OpenFOAM features a random number generator (RNG). The generated numbers within the sequence itself – depending on the quality of the algorithm – are close to being random. Random number generators on computers are also referred to as pseudo-random number generators as they are generally deterministic. Otherwise, nobody would be able to write code for such random number generators.

The randomness enters the scene in the form of the initial state of the random number generator, also known as seed. Choosing a non-constant seed value is key to obtain good random numbers. Using a constant seed value – using the same value each time the application is run – leads to an ever-recurring random number sequence, i.e. for the same initial conditions the RNG generates the same sequence of numbers.

The good, the bad and the ugly – in reverse order

The worst thing to do is to use a constant value for seeding the RNG. In Listing 486 we use zero als seed value. This value is equal every time we run the application. Thus, it comes as no surprise, when the random numbers we print to the Terminal are always the same, i.e. we print the same sequence of 20 numbers between one and a hundred every time we run the application containing the code of Listing 486.

```

1 // random stuff
2 #include "Random.H"
3 Random ranGen(0);
4
5 for (int j = 0; j < 20; j++)
6 {
7   Info << ranGen.integer(1, 100) << endl;
8 }

```

Listing 486: A simple test for random numbers; the ugly.

In order to obtain different sequences, we need to choose a better seed value. In fact, we need to choose a seed value that is different every time we run our application. The time would be a perfect example for such a seed value. However, we need to make errors in order to learn something. In the sources, we came across the method `osRandomInteger()`. This sounds great, use a random number to seed a random number generator. On a second thought, this sounds more of a chicken-egg problems, but let's continue.

So we implement the code of Listing 487, which is simply a different seed value. However, when we run the code, we find out, that we obtain the same sequences over and over, just as in the previous case.

Digging into the code, we find out, that `osRandomInteger()` uses the random number generator provided by POSIX. However, there seems to be no proper seeding of the POSIX random number generator.

```

1 // random stuff
2 #include "Random.H"
3 Random ranGen(osRandomInteger());
4
5 for (int j = 0; j < 20; j++)

```

```

6  {
7     Info << ranGen.integer(1, 100) << endl;
8 }
```

Listing 487: A simple test for random numbers, the bad.

As mentioned above, the time is the perfect seed value. However, since we are now at the good solution, we need something other than time. In Listing 488, we use the PID of the application as the seed value for the RNG. The PID is unlikely to be equal when the application is run several times. In fact, the kernel of the OS assigns the PIDs sequentially from a range of integer numbers, e.g. on the authors Linux machine the PID of a process is in the range between 1 and 32768. If the end of the number range is reached, the kernel starts all over, skipping numbers which are still in use. Furthermore, the PID is guaranteed to be different, when running an application in parallel, i.e. all the sub-processes have a unique PID.

```

1 // random stuff
2 #include "Random.H"
3 Random ranGen(pid());
4
5 for (int j = 0; j < 20; j++)
6 {
7     Info << ranGen.integer(1, 100) << endl;
8 }
```

Listing 488: A simple test for random numbers; the good.

The even better

As already mentioned, using the time gives us a different seed value every time, the application is run. The method `getTime()` returns the number of seconds that have passed since January, 1st 1970. The code of Listing 489 now yields different number sequences every time we run the application. Also, PID-reuse is also not an issue anymore, since, whenever a PID gets reused, the time is certainly different. As we use the time to seed the RNG, the year 2038 problem²³⁶ is a non-issue to us, since we are only interested in unique values rather than correct representation of time.

```

1 // random stuff
2 #include "Random.H"
3 #include "clock.H"
4 Random ranGen(clock::getTime());
5
6 for (int j = 0; j < 20; j++)
7 {
8     Info << ranGen.integer(1, 100) << endl;
9 }
```

Listing 489: A simple test for random numbers; the even better.

The perfect

The solution above is nearly perfect, the only issue left is running in parallel. This might seem a non-issue when we just want to implement random numbers for an application we only will use in serial. However, the trick is rather easy.

We use the current time as seed value and add the PID. This will ensure, that when multiple processes are spawned at the same time, when starting a parallel run, each process has its unique seed value thanks to the contribution of the PID.

```

1 // random stuff
2 #include "Random.H"
3 #include "clock.H"
4 Random ranGen(clock::getTime()+pid());
```

²³⁶https://en.wikipedia.org/wiki/Year_2038_problem

```

6 for (int j = 0; j < 20; j++)
7 {
8     Info << ranGen.integer(1, 100) << endl;
9 }
```

Listing 490: A simple test for random numbers; the perfect.

68.5 OpenFOAM specific macros for convenient programming

68.5.1 For-loops

... for lists

The `UList` class defines some macros for looping over the contents of the list. We frequently encounter for loops using statements such as `forAll`, `forAllIter` or `forAllConstIter`. These statements, however, are not part of the C or C++ programming language, they are macros provided by the `UList` class.

In Listing 491 we see the definition of the `forAll` macro.

```

1 #define forAll(list, i) \
2     for (Foam::label i=0; i<(list).size(); i++)
```

Listing 491: The definition of the `forAll` macro in `UList.H`

When the `forAll` macro is in use, a for-loop might look as the example in Listing 492.

```

1 forAll(someList, i)
2 {
3     // list body
4 }
```

Listing 492: Using the `forAll` macro to traverse a list.

The code in Listing 492 is, at compile time, expanded into the code shown in Listing 493.

```

1 for (Foam::label i=0; i<(someList).size(); i++)
2 {
3     // list body
4 }
```

Listing 493: Expanding the `forAll` macro. This is what the C++ pre-processor does with Listing 492.

... for containers

For container data types, which have an associated iterator data type, there are the `forAllIter` and `forAllConstIter` macros. The concept of the container is an abstraction to encompass sequenced containers (lists) and associative containers (hash table). The concept of the iterator is used to decouple the access to elements of the container from the internal organisation of the container²³⁷.

Below, in Listing 494 we see the definition of the `forAllIter` macro, which uses an iterator to traverse the container, note the usage of the methods `begin()` and `end()`, as well as to access the individual element, access is shown by example in Listing 495.

```

1 #define forAllIter(Container,container,iter) \
2     for \
3     ( \
4         Container::iterator iter = (container).begin(); \
5         iter != (container).end(); \
6         ++iter \
7     )
```

Listing 494: The definition of the `forAllIter` macro in `UList.H`

²³⁷https://en.wikipedia.org/wiki/Iterator_pattern

In the example below, in Listing 495, a cloud of Lagrangian particles is traversed, and each particle can be accessed via the iterator. This piece of code, respectively the developer working on this code, is completely oblivious of the underlying data structure which the Lagrangian cloud class uses.

By using the iterator for traversing the cloud, and accessing its elements, the developers of OpenFOAM could change the cloud's internal way of storing the data without breaking the higher-level code.

```
1 forAllIter(Cloud<solidParticle>, c, iter)
2 {
3     solidParticle& p = iter();
4
5     // ...
6 }
```

Listing 495: Using the *forAllIter* macro to access all particles in a Lagrangian particle cloud.

... for everything else

At the time of writing, OpenFOAM-5 is the current release, such for-loop macros are only defined for the class **UList**. Thus, the macro can only be used on data types derived from **UList**.

If our for-loop is not about traversing a list, or any container data type derived from **UList**, then we need to write the for-loop in the traditional fashion.

68.6 Time management

68.6.1 Time stepping

Transient solvers solve the governing equations each time step at least once. Depending on the solution algorithm there are several inner iterations (iterations within a time step) during one outer iteration.

pimpleFoam

Listing 496 shows the beginning of the main loop of *pimpleFoam*. After the three **include** instructions, the **runTime** object is incremented. This means, the current time step is incremented to the next time step.

```
1 /* code removed for the sake of brevity */
2
3 Info<< "\nStarting time loop\n" << endl;
4
5 while (runTime.run())
6 {
7     #include "readTimeControls.H"
8     #include "CourantNo.H"
9     #include "setDeltaT.H"
10
11    runTime++;
12
13    Info<< "Time = " << runTime.timeName() << nl << endl;
14
15    /* code continues */
```

Listing 496: The beginning of the main loop of *pimpleFoam* in *pimpleFoam.C*

pisoFoam

Listing 497 shows the beginning of the main loop of *pisoFoam*.

```
1 /* code removed for the sake of brevity */
2
3 Info<< "\nStarting time loop\n" << endl;
4
5 while (runTime.loop())
6 {
```

```

7   Info<< "Time = " << runTime.timeName() << nl << endl;
8
9 #include "readPISOControls.H"
10 #include "CourantNo.H"
11
12 // Pressure-velocity PISO corrector
13 {
14 /* code continues */

```

Listing 497: The beginning of the main loop of *pisoFoam* in **pisoFoam.C**

There, there is no incrementation of any `runTime` object. The explanation for this, lies in the condition of the `while` statement. In *pisoFoam*, the `while` statement is controlled by the return value of the function call `runTime.loop()`. Whereas, in *pimpleFoam*, the `while` statement is controlled by the return value of the function call `runTime.run()`.

Let's have a closer look on `runTime.loop()`. Listing 498 shows, that the function `loop()` calls the function `run()` and then increments the `runTime` object by calling `operator++()`.

The `++` operator of the `Time` class

Listing 499 shows the first lines of the definition of the `++` operator of the `Time` class. The last instruction of Listing 499 set the time value to the current time value plus the time step.

```

1 bool Foam::Time::loop()
2 {
3     bool running = run();
4
5     if (running)
6     {
7         operator++();
8     }
9
10    return running;
11 }

```

Listing 498: The definition of the function `loop()` in **Time.C**

```

1 Foam::Time& Foam::Time::operator++()
2 {
3     deltaT0_ = deltaTSave_;
4     deltaTSave_ = deltaT_;
5
6     // Save old time name
7     const word oldTimeName = dimensionedScalar::name();
8
9     setTime(value() + deltaT_, timeIndex_ + 1);
10
11 /* code removed for the sake of brevity */

```

Listing 499: The definition of the operator `++` in **Time.C**

68.6.2 Setting the new time step

Transient simulations can be run with fixed and variable time steps. In a simulation with fixed time step the time step is constant. The value of the time step must be set before the simulation is started. The time step influences the accuracy and stability of the simulation. The value of the time step determines the time scales that can be resolved in the simulation. Via the Courant-Friedrichs-Lowy (CFL) criterion the time step is linked to the stability of the time integration method.

Most transient OpenFOAM solvers offer the possibility of transient simulations with variable time steps. The user then provides the limits for the determination of the time steps. The most obvious limit is the maximum time step `maxDeltaT`. This is the upper limit for the value of each new time step. This is the parameter for the user to determine the time scale to be resolved.

The second limit for determining the time steps is the maximum Courant number. This parameters purpose is to maintain stability of the numerical solution.

Listing 500 shows the code that reads the time controls. The first instruction reads the entry in `controlDict` specifying whether to use variable time steps or not. This code is rather self-explanatory. If there is not entry in `controlDict` then a fixed time step is used. The other two instructions read values for the maximum Courant number and the maximum time step. The default value for the maximum Courant number is 1.0, which is the limit for the explicit Euler time integration method.

```

1 const bool adjustTimeStep =
2     runTime.controlDict().lookupOrDefault("adjustTimeStep", false);
3 scalar maxCo =
4     runTime.controlDict().lookupOrDefault<scalar>("maxCo", 1.0);
5 scalar maxDeltaT =
6     runTime.controlDict().lookupOrDefault<scalar>("maxDeltaT", GREAT);
```

Listing 500: The content of the file `readTimeControls.H`

Determining the new time step

The value of the new time step has to obey both limit mentioned above, the maximum time step and the maximum Courant number. In order to prevent oscillations the increase of the time step is damped. Listing 501 shows how the time step is computed each time step.

```

1 if (adjustTimeStep)
2 {
3     scalar maxDeltaTFact = maxCo/(CoNum + SMALL);
4     scalar deltaTFact = min(min(maxDeltaTFact, 1.0 + 0.1*maxDeltaTFact), 1.2);
5
6     runTime.setDeltaT
7     (
8         min
9         (
10             deltaTFact*runTime.deltaTValue(),
11             maxDeltaT
12         )
13     );
14
15     Info << "deltaT = " << runTime.deltaTValue() << endl;
16 }
```

Listing 501: The content of the file `setDeltaT.H`

Let us have a look on what the code is actually doing.

$$\text{maxDeltaTFact} = \frac{\text{maxCo}}{\text{Co} + \text{SMALL}} \quad (199)$$

$$\text{deltaTFact} = \min(\min(\text{maxDeltaTFact}, 1.0 + 0.1 * \text{maxDeltaTFact}), 1.2) \quad (200)$$

The scalar `maxDeltaTFact` (Line 3 in Listing 501 and Eq. (199)) is the relation between the maximum Courant number and the current Courant number (see Section 68.6.4 on how the Courant number is determined). The role of the constant `SMALL` is to prevent division by zero, which would cause the solver to crash.

The scalar `deltaTFact` is computed from `maxDeltaTFact`. This line of code (Line 4 and Eq. (200)) implements the damping, i.e. the rate of increase of the time step is limited. The nested use of two `min()` functions determines the minimum of three values. The most obvious of these three values is the last argument. If this value is the smallest, then the next time step is 20 % larger than the last one.

Eq. (200) shows the minimum of the first two arguments in a mathematical way. Figure 186 shows the three arguments of Eq. (200). We use the symbol x for the scalar `maxDeltaTFact`. In Figure 186 the values for x are greater than one. Eq. (202) elaborates why this is the case. x is the ratio of the maximum Courant number Co_{max} and the current Courant number Co . As the current Courant number is always smaller than the maximum Courant number we replace Co with fCo_{max} , with $f < 1$. After cancelling Co_{max} the inverse of f remains. Thus x is always greater than one.

$$\min(x, 1 + 0.1x) = \begin{cases} x & x < \frac{10}{9} \\ 1 + 0.1x & x > \frac{10}{9} \end{cases} \quad (201)$$

$$x = \frac{Co_{max}}{Co} = \frac{Co_{max}}{\frac{f Co_{max}}{<1}} = \frac{1}{f} \quad (202)$$

$$\Rightarrow x > 1 \quad (203)$$

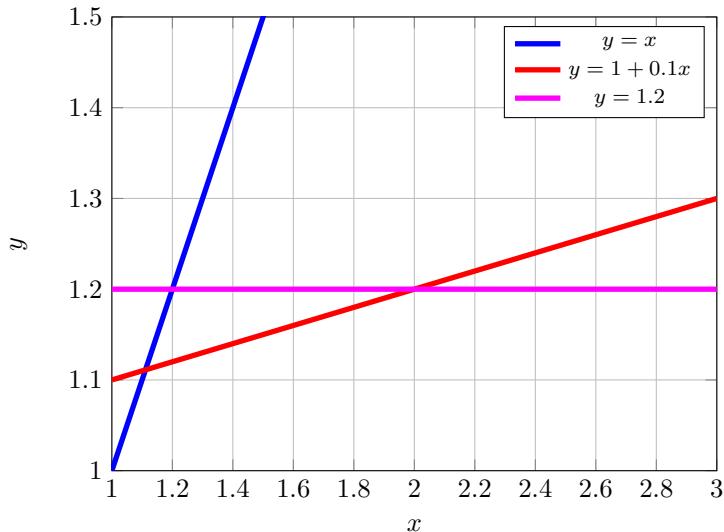


Figure 186: The three arguments of Eq. (200) plotted over x

The argument of the function `setDeltaT()` contains the abidance of the first limit, the maximum time step. There the minimum of the newly calculated and the maximum time step is passed on.

68.6.3 A note on the passing of time

In this section we will take a closer look at the implementation of the `Time` class.

Class design

A quick glance at the file `Time.H` reveals some very interesting information on the nature of time, or more precisely, the nature of the `Time` class. Listing 502 shows us, that the class `Time` class inherits from five base classes²³⁸.

```
class Time
:
    public clock,
    public cpuTime,
    public TimePaths,
    public objectRegistry,
    public TimeState
{
    /* class definition */
}
```

Listing 502: The information on inheritance of the `Time` class; an extract of `Time.H`.

²³⁸Literarily spoken, the `Time` class is not only Dr. Jekyll and Mr. Hyde, it is also Citizen Kane, Mrs. Robinson and the Tambourine Man.

The TimeState class

From Listing 502 we see that `Time` is a `TimeState` due to inheritance. In Listing 503 we see the information on inheritance of the `timeState` class. There we see, that `TimeState` is a `dimensionedScalar`.

```
class TimeState
{
    public dimensionedScalar
{
    /* class definition */
}
```

Listing 503: The information on inheritance of the `TimeState` class; an extract of `TimeState.H`.

Distinguishing between time steps

The fact that `Time` is a `TimeState` which in turn is a `dimensionedScalar` helps to understand the Lines 6, 13 and 21 of Listing 504. There, the `name()` method of the `dimensionedScalar` name space is called.

```
1 Foam::Time& Foam::Time::operator++()
2 {
3     // some code removed for brevity
4
5     // Save old time name
6     const word oldTimeName = dimensionedScalar::name();
7
8     setTime(value() + deltaT_, timeIndex_ + 1);
9
10    // some code removed for brevity
11
12    // Check that new time representation differs from old one
13    if (dimensionedScalar::name() == oldTimeName)
14    {
15        int oldPrecision = precision_;
16        do
17        {
18            precision_++;
19            setTime(value(), timeIndex());
20        }
21        while (precision_ < 100 && dimensionedScalar::name() == oldTimeName);
22
23        WarningIn("Time::operator++()")
24            << "Increased the timePrecision from " << oldPrecision
25            << " to " << precision_
26            << " to distinguish between timeNames at time " << value()
27            << endl;
28
29        if (precision_ == 100 && precision_ != oldPrecision)
30        {
31            // Reached limit.
32            WarningIn("Time::operator++()")
33                << "Current time name " << dimensionedScalar::name()
34                << " is the old as the previous one " << oldTimeName
35                << endl
36                << "      This might result in overwriting old results."
37                << endl;
38    }
39    // some code removed for brevity
40 }
```

Listing 504: The increment operator (`++`) of the `Time` class; an extract of `Time.C`.

From Line 23 to 27 of Listing 504 we see the code which generates the warning message we saw in Listing 48 in Section 11.3.2.

In Lines 21 and 29 we find the hard-coded limit for the time precision. If the time precision reaches a value of 100, then it is no more increased.

Naming the time with precision

In Section 11.3.2 we saw that the value of the `timePrecision` can be a source of error. We will now elaborate on the actual causes of this error.

Listing 505 shows the definition of the method `timeName(const scalar)`. This method is used to create a properly formatted time name²³⁹ from a given scalar representing the time. In this method the time precision comes into play in the form of the data member `precision_`, which is a static data field of the `Time` class with a protected visibility. In this method the time value with high precision is converted to a string representation (the time name) with limited precision²⁴⁰.

```
1 // - Return time name of given scalar time
2 Foam::word Foam::Time::timeName(const scalar t)
3 {
4     std::ostringstream buf;
5     buf.setf(ios_base::fmtflags(format_), ios_base::floatfield);
6     buf.precision(precision_);
7     buf << t;
8     return buf.str();
9 }
```

Listing 505: The method `timeName(const scalar)` of the class `Time`; an extract of `Time.C`. Note, that the descriptive comment is taken from the header file `Time.H`.

When the time is advanced, e.g. using the increment operator of the `Time` class, the method `setTime()` is called. Listing 506 shows the definition of this method. The new time value is passed to this method. In the second instruction we see how the time name is updated to the new value²⁴¹.

```
1 void Foam::Time::setTime(const scalar newTime, const label newIndex)
2 {
3     value() = newTime;
4     dimensionedScalar::name() = timeName(timeToUserTime(newTime));
5     timeIndex_ = newIndex;
6 }
```

Listing 506: The method `setTime()` of the class `Time`; an extract of `Time.C`.

The method `setTime()` gets called e.g. by the operator `*` of the `Time` class, see Line 8 of Listing 504. There, the time index is increased by one. From the header file of the `TimeState` class, we see, that the time index is of the data type `label`, which is essentially an integer data type. Thus, we see, that the time index is a consecutive number counting the time steps.

68.6.4 The Courant number

The Courant number Co is the ratio of the time step Δt and the characteristic convection time scale $u/\Delta x$. Eq. (204) shows the definition of the Courant number. However in a practical CFD code the Courant number will be computed in a slightly different way. Eq. (205) shows how Eq. (204) is expanded with A/A to gain a formulation featuring the flux and the volume of the control volume instead of the velocity and the discretisation length. Eq. (206) shows the extension of Eq. (205) for a one-dimensional finite volume formulation. The mean of the fluxes of the faces E and W defines the convective time scale. This definition seems obvious in some way in the one-dimensional case. For two or three-dimensional cases the choice of how to define the characteristic flux seems not straight forward.

²³⁹The data type of the return value of this method is `word`, which is a string data type of OpenFOAM. Thus, the time name is a string representation of the time. It is important to note, that the string representation of the time is different than the actual value of the time.

²⁴⁰It is this method which creates the time name 0.102 from the time value 0.1023, when precision is set to three digits, as it is the case in the example described in Section 11.3.2.

²⁴¹The call of `timeToUserTime()` can be ignored. This method simply returns the passed value. This method has a non-trivial implementation in the `engineTime` class, which keeps track of time in terms of engine RPM and crank-shaft angle. `engineTime` is derived from `Time`.

$$Co = \frac{u\Delta t}{\Delta x} \quad (204)$$

$$Co = \frac{u\Delta t}{\Delta x} = \frac{u\Delta t}{\Delta x} \frac{A}{A} = \frac{\phi\Delta t}{\Delta V} \quad (205)$$

$$Co = \frac{\frac{|\phi_E| - |\phi_W|}{2} \Delta t}{\Delta V} = \frac{1}{2} \frac{(|\phi_E| - |\phi_W|) \Delta t}{\Delta V} \quad (206)$$

The Courant number in OpenFOAM

In OpenFOAM the Courant number is computed for all cells. In fact OpenFOAM computes a maximum Courant number, i.e. the largest Courant number of all cells, and a mean Courant number, i.e. the mean Courant number of all cells.

Listing 507 shows the code responsible for computing the Courant number. Line 8 of Listing 507 translates to Eq. (207). `sumPhi` is a scalar field containing the sum of the magnitudes of all face fluxes of every cell, i.e. for each cell the magnitude of the face fluxes are summed up. Eq. (207) holds for every cell.

Eq. (208) is the mathematical representation of line 11. There the maximum value of the ratio between the values of `sumPhi` and the cell volume is determined. Both variables `sumPhi` and `mesh.V()` contain values for every cell. Therefore the `gMax()` function returns the maximum value.

Eq. (209) represents line 14.

```

1  scalar CoNum = 0.0;
2  scalar meanCoNum = 0.0;
3
4  if (mesh.nInternalFaces())
5  {
6      scalarField sumPhi
7      (
8          fvc::surfaceSum(mag(phi))().internalField()
9      );
10
11     CoNum = 0.5*gMax(sumPhi/mesh.V().field())*runTime.deltaTime();
12
13     meanCoNum =
14         0.5*(gSum(sumPhi)/gSum(mesh.V().field()))*runTime.deltaTime();
15 }
16
17 Info<< "Courant Number mean: " << meanCoNum
18     << " max: " << CoNum << endl;
```

Listing 507: The content of the file `CourantNo.H`

$$\text{sumPhi} = \sum_{f_i} |\phi_{f_i}| \quad (207)$$

$$\text{CoNum} = \frac{1}{2} \max_{\text{all cells}} \left(\frac{\text{sumPhi}}{V_{cell}} \right) \Delta t \quad (208)$$

$$\text{meanCoNum} = \frac{1}{2} \frac{\sum \text{sumPhi}}{\sum V_{cell}} \Delta t \quad (209)$$

Discussion

The way to compute the Courant number in a three dimensional case is not straight forward as mentioned above. This section reflects the authors way of understanding. So there is no guarantee of validity. The factor of $1/2$ and the summation of ϕ_{f_i} is explained by the author as follows.

We base our reflections on a two dimensional control volume. Eq. (211) shows the summation written in the long form. This equation is then rearranged to yield Eq. (212). In Eq. (212) the summation is reduced to two terms. These terms are the arithmetic mean of the face flux in the principal directions $N - S$ and $W - E$. This summation is then identified as the L_1 norm of the mean face fluxes in the principal directions.

The reason for choosing the L_1 norm is not self-evident. In any case is the L_1 norm computationally cheaper than the Euklidian or L_2 norm. However, the use of the L_1 norm seems justified since it measures the distance

covered by a movement, see http://en.wikipedia.org/wiki/Taxicab_geometry.

$$Co = \frac{1}{2} \frac{\sum_{f_i} |\phi_{f_i}|}{V_{cell}} \Delta t \quad (210)$$

$$Co = \frac{1}{2} \frac{|\phi_N| + |\phi_E| + |\phi_S| + |\phi_W|}{V_{cell}} \Delta t \quad (211)$$

$$Co = \frac{\frac{|\phi_N| + |\phi_S|}{2} + \frac{|\phi_E| + |\phi_W|}{2}}{V_{cell}} \Delta t \quad (212)$$

$$Co = \frac{\overline{|\phi|}^{NS} + \overline{|\phi|}^{WE}}{V_{cell}} \Delta t \quad (213)$$

$$Co = \frac{\|\overline{|\phi|}^{\mathbf{x}_i}\|_1}{V_{cell}} \Delta t \quad (214)$$

We introduce the following symbols

$$\frac{1}{2} \sum_{f_i} |\phi_{f_i}| = \|\overline{|\phi|}^{\mathbf{x}_i}\|_1 = \|\Phi\|_1 \quad (215)$$

$$Co = \frac{\|\Phi\|_1}{V_{cell}} \Delta t \quad (216)$$

The way the mean Courant number is computed seems incorrect at the first glance but it isn't.

$$Co = \frac{\|\Phi\|_1}{V_{cell}} \Delta t \quad (216)$$

The mean value of the quantity x is defined as follows

$$\bar{x} = \frac{1}{N} \sum_{i=1}^N x_i \quad (217)$$

Next we write the mean value of the Courant number. An unmarked summation is a summation over all cells.

$$\overline{Co} = \frac{1}{N} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \Delta t \quad (218)$$

$$\overline{Co} = \frac{1}{N} \underbrace{\sum V_{cell}}_{=1} \underbrace{\sum \|\Phi\|_1}_{=1} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \Delta t \quad (219)$$

$$\overline{Co} = \frac{\sum \|\Phi\|_1}{\sum V_{cell}} \underbrace{\frac{1}{N} \sum V_{cell}}_X \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \Delta t \quad (220)$$

Eq. (220) now resembles Eq. (209). Now we concentrate on the term X which is the only difference between Eqns. (220) and (209).

$$X = \frac{1}{N} \frac{\sum V_{cell}}{\sum \|\Phi\|_1} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \quad (221)$$

$$X = \underbrace{\frac{\sum V_{cell}}{N}}_{=\overline{V_{cell}}} \frac{1}{\sum \|\Phi\|_1} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \quad (222)$$

$$X = \frac{\overline{V_{cell}}}{\sum \|\Phi\|_1} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \quad (223)$$

$$X = \frac{1}{\sum \|\Phi\|_1} \sum \left(\frac{\|\Phi\|_1}{\frac{V_{cell}}{\overline{V_{cell}}}} \right) \quad (224)$$

We assume $\frac{V_{cell}}{\bar{V}_{cell}} \approx 1$

$$X = \frac{1}{\sum \|\Phi\|_1} \sum \left(\frac{\|\Phi\|_1}{1} \right) \quad (225)$$

$$X = \frac{\sum \|\Phi\|_1}{\sum \|\Phi\|_1} = 1 \quad (226)$$

Thus we have shown that the way the mean Courant number `meanCoNum` is computed is actually the mean Courant number \bar{Co} . However, this attempt of a proof is based on some assumptions.

First, the way the author explains the meaning of the summation of the face fluxes relies on hexahedral cells. The argument made seems not to be applicable on tetrahedral cells. Secondly, the assumption $\frac{V_{cell}}{\bar{V}_{cell}} \approx 1$ is valid for homogeneous grids. For a uniform grid this assumption would be ideally fulfilled. If the volume of the largest and smallest cells differs a lot this assumption is not justified.

Some thoughts on the computational costs

Why the formula for the mean Courant number is rearranged from

$$\bar{Co} = \frac{1}{N} \sum \left(\frac{\|\Phi\|_1}{V_{cell}} \right) \Delta t \quad (227)$$

to

$$\bar{Co} = \frac{\sum \|\Phi\|_1}{\sum V_{cell}} \Delta t \quad (228)$$

is unknown to the author.

It is the opinion of the author that this is made for reasons of computational cost. Two times the summation over all values of a field plus one division is computationally cheaper than an elementwise division of two fields and one subsequent summation over all elements of the resulting field.

This would be the case if the division operation takes more time than the summation operation which is very likely the case. Depending on the system the floating point division operation can take several times longer than a floating point multiplication.

In the first case n times one division and one addition needs to be made, with n the number of field values. In the second case $2n$ times additions and one division is to be made.

$$T_1 = n(T_d + T_s) \quad T_2 = 2nT_s + T_d \quad (229)$$

We introduce the factor δ , that is the ratio between T_d and T_s .

$$T_1 = n(\delta T_s + T_s) \quad T_2 = 2nT_s + \delta T_s \quad (230)$$

$$T_1 = nT_s(1 + \delta) \quad T_2 = T_s(2n + \delta) \quad (231)$$

$$\frac{T_1}{T_s} = n(1 + \delta) \quad \frac{T_2}{T_s} = (2n + \delta) \quad (232)$$

Next we assume that n is very large

$$\frac{T_1}{T_s} = n(1 + \delta) \quad \frac{T_2}{T_s} \approx 2n \quad (233)$$

So the first formula takes $1 + \delta$ operations, whereas the second formula takes approximately $2n$ operations. If δ is larger than one, the second formula will take less time for computation. A δ smaller than one is highly unlikely or even impossible as the addition is a very simple operation. Remember, δ is the ratio between the time a division takes and the time an addition takes. The actual ratio vary according to the system architecture, the compiler and the implementation, e.g. [1] reports a factor of 5 to 6 for single and double precision floating point division. This argument does not consider the memory usage of the operations involved, it only focuses on the number of floating point operations.

Because the Courant number is computed after every time step the time needed to calculate the Courant number has an impact on the simulation time.

68.6.5 The two-phase Courant number

In a two-phase simulation there are several choices of how to compute the Courant number. In total, there are 4 velocity fields (U_1 , U_2 , U and U_r). These are the velocities of the phases 1 and 2 as well as the mixture and relative velocities. The solver *twoPhaseEulerFoam* computes the Courant number for the mixture and the relative velocities.

Listing 508 shows the content of the file *CourantNos.H* which is part of the source code of this solver. Line 1 computes the mixture Courant number by including the file *CourantNo.H*. This is the file described in Section 68.6.4. As this code operates on the field *phi*, which happens to be the flux of the mixture, the mixture Courant number is computed.

The next lines compute the Courant number based on the relative phase flux. At line 11 the maximum of this two Courant numbers is determined and stored into the variable *CoNum*.

CoNum is the Courant number used by the time stepping mechanism. So the variable time steps of the *twoPhaseEulerFoam* solver are based on the maximum of the mixture and relative velocity Courant number.

```
1 #include "CourantNo.H"
2
3 {
4     scalar UrCoNum = 0.5*gMax
5     (
6         fvc::surfaceSum(mag(phi1 - phi2))().internalField()/mesh.V().field()
7     )*runTime.deltaTValue();
8
9     Info<< "Max Ur Courant Number = " << UrCoNum << endl;
10
11    CoNum = max(CoNum, UrCoNum);
12 }
```

Listing 508: The content of the file *CourantNos.H*

68.7 The registry

At some point in our study of OpenFOAM's sources, its documentation or the internet we all came across words like *registered objects* or similar expressions. This section tries to cast some light on this topic, or at least present the thoughts and findings of the author. This section is closely related to Section 68.8.

68.7.1 The classes involved

Here is an extract of the descriptions found in the header files of the respective classes.

IObject *IObject* defines the attributes of an object for which implicit *objectRegistry* management is supported, and provides the infrastructure for performing stream I/O.

regIObject *regIObject* is an abstract class derived from *IObject* to handle automatic object registration with the *objectRegistry*.

objectRegistry registry of *regIObjects*

In Figure 187 a detail of the class hierarchy surrounding the class *regIObject* is shown.

IObject

This class provides the basic facilities for I/O. In Section 68.4.5 the practical or typical use of this class is shown.

regIObject

This class is an abstract class as the description in the header mentions. In Figure 187 the name of the pure virtual method which makes this class an abstract class is shown in an italic font. This means all classes derived from *regIObject* must implement this pure virtual method. This also means, that we can not create an object of the type *regIObject* directly. Thus, in all of OpenFOAM's sources we find a constructor call for the class *regIObject* only in the initializer list of classes derived from *regIObject*.

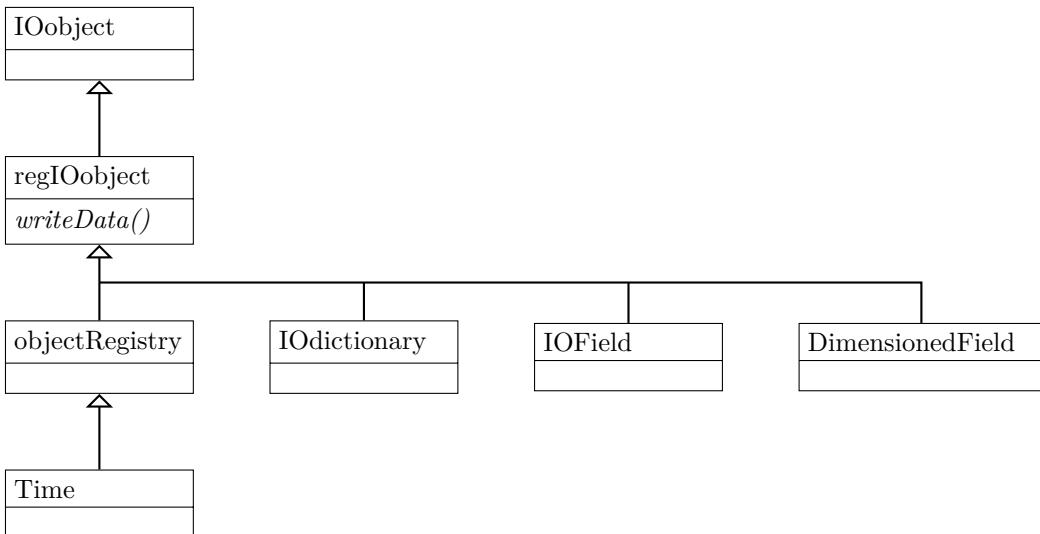


Figure 187: A partial view of the class hierarchy involving `regIOobject`; note that this diagram is complete only for the classes `IOobject` and `regIOobject` – meaning `IOobject` is not derived from any other class and `regIOobject` is derived from only `IOobject`; the other classes have more base classes than shown in this diagram.

objectRegistry

The `objectRegistry` is eponymous to this section. In fact there is not the one registry in OpenFOAM, there are several. Among others, the classes `Time`, `cloud`, and `polyMesh` are derived from `objectRegistry`. Figure 188 shows the classes from which `objectRegistry` is derived.

objectRegistries: space and time

In OpenFOAM there is usually only one object of the type `Time`, usually named `runTime`. There are no solvers to the knowledge of the author, which use more than one instance of the class `Time`. As most solvers also feature only one mesh, the separation between `Time` and `polyMesh` as being a registry seems to be overdone.

However, there are solvers which feature several meshes, e.g. the conjugate heat transfer solvers. In the simplest configuration there is one mesh for the solid part of the domain and one mesh for the fluid part of the domain. However, the solver `chtMultiRegionFoam` supports an arbitrary number of fluid and solid domains. In this case the temperature field `T` of the solid region i needs to be registered with the appropriate registry, namely the mesh of the solid region i . Since the fluid in the fluid region also has a temperature, there will also be a temperature field `T` registered to the appropriate fluid mesh. Thus, the separation of the object registries, i.e. mesh(es) and time, saves us from a potential name clash, as we have two temperature fields `T`. Thus, the mesh(es) are registered with the object registry `runTime`, whereas fields are registered with the appropriate mesh.

An OpenFOAM solver has a number of object registries in use, the most prominent are the `runTime` and the `mesh` objects. For fields it is important to know that they belong to a mesh, since the entity `field` is a mere list of values. Only the connection to the mesh gives the field an actual meaning, i.e. the entry at position i in the list is the cell centre value of cell i . Furthermore, the field also needs a connection to the actual time state of the simulation, otherwise there would be no meaningful way to define or calculate a temporal derivative.

68.7.2 Using the registry

Of what use could a possible object registry be? Well, ask the code.

In Section 78.3 we showed a way to search files for a certain pattern. Now we search all files with the file extension `.C` for the pattern `lookupObject` and count the hits²⁴². Listing 509 shows the command we can use. First we use `find` to look for all files with the specified pattern for the file name. The result is then piped to

²⁴²The method `lookupObject()` can be used to ask the registry for a registered object. The usefulness will be explained in the subsequent paragraphs.

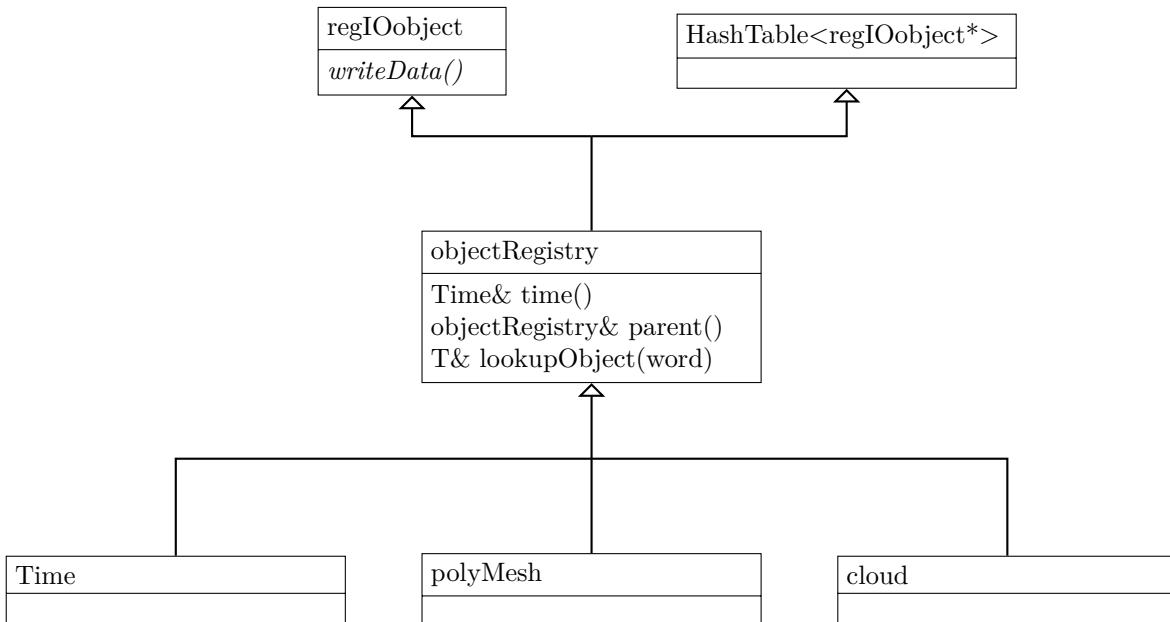


Figure 188: The base classes of the class `objectRegistry`; this class is derived from `regIOobject` and a `HashTable`; note that the template parameter of the `HashTable` is a pointer to `regIOobject`; thus `objectRegistry` is an `regIOobject` as well as a `HashTable` of `regIOobject` pointers – this is C++’s template madness and inheritance wizardry in action.

`grep` which searches the files for the specified pattern. Lastly, the result of `grep` is piped to `wc`, which counts lines, words and bytes. Thus the first number returned by this sequence of commands tells us the number of hits. The actual number of hits is approximately half the displayed number, since in the process of building OpenFOAM from sources, symbolic links are created within the `lnInclude` folders²⁴³.

```
find $FOAM_SRC -name '*.C' | xargs grep 'lookupObject' | wc
```

Listing 509: Find and scan files with file extension .C for the pattern `lookupObject` and count the hits

The command of Listing 509 results in 1068 hits in the author’s OpenFOAM-2.3.x installation at the time of writing. 537 of these hits come from symbolic links of `lnInclude` directories. This means that `lookupObject()` gets used a lot. So what is `lookupObject()` good for?

Need to know vs. want to know

One principle of *encapsulation* or *information hiding* is a fundamental principle of object-oriented programming²⁴⁴. The general idea is to hide the actual implementation of something behind a publicly accessible interface. Thus, the inner workings of a class may change without affecting its use. The iterator concept is a good example of the benefits of information hiding. Typical container classes implement a feature called iterators that are used to iterate over all elements of the container. By using the public interface of the iterator, the actual container behind may be any kind of data structure (a linked list, a vector, a hash table, etc.).

Besides providing and using interfaces for accessing the data of a class it is also a common and good practice to restrict the scope of data, e.g. temporary data being local to the class or method where it is actually used. Thus, in the design of the classes we implement we limit the data contained within and/or passed to the class to the necessary minimum, i.e. the viscosity law used in a solver does not need to know about the solver we used to solve the discretized equation system. However, there might arise the need to access data, which the original designers of a certain family of classes did not anticipate.

²⁴³The `lnInclude` folders collect links to all files of a certain library, thus when compiling a solver that uses this library we need to include only the `lnInclude` folder and not the whole directory tree of the library’s sources. This minimizes the number of entries in the `Make/options` files.

²⁴⁴Information hiding and encapsulation are often used synonymously, however, strictly spoken they are not exactly the same.

Namespaces & scopes

Another aspect are namespaces and variable scopes within our source codes. A variable is visible in the namespace and scope it is declared. If we look at the top level code of a solver, e.g. `twoPhaseEulerFoam`, we see a lot of `#include` statements and the `main()` method of the program. Although, we find no direct statement involving the namespace, in the file `fvCFD.H` a statement is hidden which causes the compiler to use the namespace `Foam`. This is the reason why we can later e.g. in `createFields.H` use typenames such as `volScalarField` which are defined in the namespace `Foam`. Otherwise we would need to explicitly specify the namespace as well, e.g. `Foam::volScalarField`. Thus, all objects created by a solver such as `mesh`, `runTime`, etc. are visible in the namespace `Foam`.

Models however, have their own namespaces. Listing 510 shows an example of such a model with its own namespace. Within the namespace `Foam` a new namespace `diameterModels` is created. Within this namespace the class `isothermal` is defined. Thus the classes implementing diameter models do not pollute the `Foam` namespace.

Although, the `diameterModels` namespace is a subset of the `Foam` namespace and everything declared within `Foam` is also visible within `Foam::diameterModels`, the diameter models are compiled with other models into a shared library. Thus, when these files are compiled, the compiler knows nothing of the objects in the namespace `Foam` created in e.g. `createFields.H`.

```
namespace Foam
{
namespace diameterModels
{

class isothermal
:
public diameterModel
{
// code removed
}
```

Listing 510: The class definition of the `isothermal` class, derived from the class `diameterModel` in `isothermalDiameter.H`

Looking up stuff

Listing 511 shows the definition of the method `d()` of the class `isothermal`. For the reasons explained above `isothermal.C` and `createFields.H` being in different compilation units, we can not access the pressure field `p` directly from within the method body, even though `p` is part of the namespace `Foam`. However, other diameter models do not need to access the pressure field, e.g. `constant` which implements a constant diameter.

```
Foam::tmp<Foam::volScalarField> Foam::diameterModels::isothermal::d() const
{
    const volScalarField& p = phase_.U().db().lookupObject<volScalarField>
    (
        "p"
    );

    return d0_*pow(p0_/p, 1.0/3.0);
}
```

Listing 511: The definition of the method `d()` of the class `diameterModel` in `isothermalDiameter.C`

The example above shows the value of the lookup mechanism. Since some sub-models operate on some fields, it is easy to get a reference to the mesh from the field, as it is done in `phase_.U().db()`. `phase_` is a member of the base class of the diameter models²⁴⁵. The call `phase_.U()` returns a reference to the velocity field of the phase in question. As the velocity field is registered with the mesh otherwise we wouldn't know which velocity value belongs to a certain cell we get a reference to the mesh by calling `db()`, which is a method of the class `IObject`. This handy mechanism saves us from polluting sub-models with references to the mesh, the time, to fields we might need at some point or some derived classes might need in special cases.

²⁴⁵It is a convention of OpenFOAM's developers to append an underscore character (`_`) to the names of the data members of a class in order to make them easily distinguishable from method parameters.

Thus the `lookupObject()` method provides a tool for us to get references to fields which at compile-time may not be declared and thus usable. Remember, the pressure field is declared in the solver's `createFields.H` file, which is in a different compilation unit as the library we are compiling our diameter model for. If the code of the diameter model and the solver would be in the same compilation unit (the solver's executable) we would not need the lookup mechanism. However, since the developers of OpenFOAM aim for modularity, placing everything into a single compilation unit is against the design principles of modularity and reusability.

The `lookupObject()` method is templated since we can register anything with the mesh, in fact anything that is derived from `regIOobject`, since an `objectRegistry` is a `HashTable` of `regIOobject` pointers. Thus, at compile-time the method and the compiler do not know exactly which data types it is going to handle. This is where templates come into play. The templated method is implemented once for the template parameter, and when we use the method, we simply replace the template parameter with the actual type, as in `lookupObject<volScalarField>("p")`. The compiler then does the rest of the work and generates the appropriate code. We could resolve this issue without templates by using function overloading at the price of massive code duplication and poor maintainability.

68.7.3 Printing the registry

If you are curious you can add the following lines of code to a test utility of yours to check what is registered with the `mesh` and the `runTime` object registry. Note that `mesh` and `runTime` must be accessible from the place you put the code into. Also the names of the objects might differ in some cases.

```
Info << "mesh.names() " << mesh.names() << nl << endl;
Info << "runTime.names() " << runTime.names() << endl;
```

Listing 512: Printing the contents of the object registries `mesh` and `runTime` to Terminal

68.8 I/O - input & output

Some aspects of I/O were already covered in Sections 68.4.5 and 68.3. However as this collection of stuff is fragmented by design or by the lack of such we cover the topic of I/O in a more general manner.

68.8.1 Output to Terminal - OpenFOAM's very own `printf()`

In programming we have often the need to print stuff to the Terminal, e.g. for `printf()` debugging²⁴⁶. With C++ general I/O was implemented on the basis of I/O streams. C++'s I/O streams provide a type-safe and uniform way to implement I/O for both built-in and user-defined types [59]. See Listings 513 and 514 for the use of C's `printf()` function and C++'s streams.

```
#include <stdio.h>

int main(int argc, char** argv)
{
    printf("Hello, World!\n");
    return 0;
}
```

Listing 513: The *Hello World!* example of C.

```
#include <iostream>

int main()
{
    std::cout << "Hello World!" << std::endl;
    return 0;
}
```

Listing 514: The *Hello World!* example of C++.

²⁴⁶Named after C's ubiquitous `printf()` function, see <http://stackoverflow.com/a/189570/2055536>

OpenFOAM implements its own stream library. The generic stream library of OpenFOAM is based on the class `Iostream`. The description of this class in its header file sheds some light on the reasons for doing so:

An `Iostream` is an abstract base class for all input/output systems; be they streams, files, token lists etc.

The basic operations are construct, close, read token, read primitive and read binary block. In addition version control and line number counting is incorporated. Usually one would use the read primitive member functions, but if one were reading a stream on unknown data sequence one can read token by token, and then analyse.

OpenFOAM handles all kinds of communication in terms of streams, among others: Terminal I/O with the user, file I/O and inter-process communication for parallel processing. The *Hello World!* example for the OpenFOAM world in Listing 515 looks very similar to the example of C++.

```
#include "Istream.H"

using namespace Foam;

int main(int argc, char *argv[])
{
    Info << "Hello OpenFOAM!" << endl;

    return 0;
}
```

Listing 515: The *Hello World!* example written in OpenFOAM.

Conditional (debug) output

`printf()` debugging is a very handy, low-level technique to trouble-shoot pieces of code. In the case of actual debugging, we will remove all lines of code printing to the Terminal once we are done debugging. However, we might want to create software, which may be either talkative or silent²⁴⁷. In this case we need conditional `Info` statements.

Listing 516 shows a *Hello World!* example with conditional output. This listing is quite lengthy, since we decided not to use simple boolean to control the conditional output. Instead we opted for a real case scenario, in which the verbosity is controlled by a command line option. This, however, entailed some more lines of code to deal with command line parameters.

```
#include "argList.H"

bool verbose(false);

using namespace Foam;

int main(int argc, char *argv[])
{
    argList::addNote
    (
        "This is a \"Hello World!\" program for the OpenFOAM world."
    );

    argList::noBanner();
    argList::noParallel();

    argList::removeOption("noFunctionObjects");
    argList::removeOption("case");

    argList::addBoolOption
    (
        "verbose",
        "control the chatty-ness of me"
    );
    Foam::argList args(argc, argv);
```

²⁴⁷Have you ever come across `-v` or `--verbose` command line switches when using UNIX or LINUX computers?

```

if (args.optionFound("verbose"))
{
    verbose = true;
}

Info << "Hello OpenFOAM!" << endl;

if (verbose) Info << "... and hello to all other non-OpenFOAM worlds!" << endl;

return 0;
}

```

Listing 516: The *Hello World!* example written in OpenFOAM with conditional chattiness.

In addition to the boolean command line switch, we added a note informing the user about the executable. This note gets displayed, when the usage message is shown by invoking the executable with the command line option `-help`. OpenFOAM adds a number of command line parameters by default, thus we remove some of them (the ones that make no sense for a *Hello World!* program, such as the parallel option).

The second to last line of code is the one that actually controls the conditional output. This is done by a good old `if` statement.

In the source code of the function objects of OpenFOAM-2.3.x we observed another possibility to define conditional output. There, we can pass an argument to `Info`. With OpenFOAM-2.4.x and higher versions this does not compile anymore. Listing 517

```

// OpenFOAM-2.3.x
Info(log_) << "    Including porosity effects" << endl;

// OpenFOAM-2.4.x and higher
if (log_) Info << "    Including porosity effects" << endl;

```

Listing 517: Implementing conditional output, controlled by the `Switch log_`, in different OpenFOAM versions. This example is taken from the `force` function object. See the file `force.C`.

A variant of the conditional `Info(log_)` statement was reinstated in May 2016²⁴⁸, with the `Log` macro, which is defined as follows:

```

// - Report write to Foam::Info if the local log switch is true
#define Log \
    if (log) Info

```

Listing 518: The definition of the `Log` macro, originally for conditional output of function objects. See the file `messageStream.H`.

68.8.2 The registry and the I/O or the truth behind `runTime.write()`

Registering fields with the `runTime` object registry also makes our lives easier when we want to write the current state of the simulation to disk. In a great number of solvers, possibly in all of them, we find an instruction like `runTime.write()` within the main loop of the `main` method. This call to the method `write()` causes fields to be written to disk. As every solver writes a different set of fields to disk, we may ask ourselves how the solver or OpenFOAM knows which fields to write when we call the `write()` method of the `runTime` object? Here, the registry nature of the `Time` class comes into play. Since we register all our fields, which we eventually want to read or write, with the `runTime` object, the `runTime` object has a list of objects (`regIOobjects` in fact) which are to (or might) be written²⁴⁹. In fact, since `objectRegistry` is derived from the type `HashTable`, an object registry *is a* list of objects which are to (or might) be written²⁵⁰. The call of the `write` method of the `Time` class causes `Time` to iterate over its self (`runTime` *is a* list of `regIOobjects` by inheritance²⁵¹) and call the `write()` method of every single item within the list. The method `write()` is defined in the `regIOobject` class.

²⁴⁸<https://github.com/OpenFOAM/OpenFOAM-dev/commit/48e58170392e5ef60538cfef28dd70c70a62e17b>

²⁴⁹depending on the write flags of the `IObject` part of the type. See Section 68.4.5 for a discussion on the read and write flags of the `IObject` class.

²⁵⁰A hash table is not really a list, however, we can iterate over a hash table the same way we can iterate over a list. The description in the header file of the `HashTable` class describes the class as being *An STL-conforming hash table*.

²⁵¹think around the family tree, e.g. in Figure 188

```

1  bool Foam::Time::writeObject
2  (
3      IOstream::streamFormat fmt,
4      IOstream::versionNumber ver,
5      IOstream::compressionType cmp
6  ) const
7  {
8      if (outputTime())
9      {
10         // some code removed
11
12         timeDict.regIOobject::writeObject(fmt, ver, cmp);
13         bool writeOK = objectRegistry::writeObject(fmt, ver, cmp);
14
15         // further code removed

```

Listing 520: Parts of the method `writeObject()` of the class `Time` in `TimeIO.C`

The closer look into the sources is revealing if we take some of C++'s rules into consideration. Listing 519 shows us the method that is called when we call `write()` on `runTime`, bear in mind that `Time` is derived in second generation from `regIOobject` via the class `objectRegistry`. The listing shows a call of the method `writeObject()`.

```

bool Foam::regIOobject::write() const
{
    return writeObject
    (
        time().writeFormat(),
        IOstream::currentVersion,
        time().writeCompression()
    );
}

```

Listing 519: The method `write()` of the class `regIOobject` in `regIOobjectWrite.C`

If we search the sources of `Time` and all its base classes we find out that `Time`, `regIOobject` and `objectRegistry` all define a method called `writeObject()`²⁵². All of these three methods share the same signature²⁵³, i.e. they receive the same function arguments. Since the call of `writeObject()` is not further specified for a certain namespace, it is the method `writeObject()` of the class `Time`, which is called when we call `runTime.write()` as `runTime` is of the type `Time`.

In Listing 520 we see a portion of the definition of the method `writeObject()` of the class `Time`. There we also see calls explicitly to the methods `writeObject()` of the classes `regIOobject` and `objectRegistry`.

Thus, the method `writeObject()` of all three classes (`Time`, `regIOobject` and `objectRegistry`) are called when `runTime.write()` is called. It is worth noticing that the call of `regIOobject::writeObject()` is invoked on the `timeDict` object. The definition of this object is part of the removed code prior to the call. A look into the source code reveals, that `timeDict` is an `IOdictionary` which is a class also derived from `regIOobject`, see Figure 187. The call of `timeDict.writeObject()` is the piece of code which creates the `uniform` folders within the time step directories²⁵⁴.

The method `writeObject()` of the class `objectRegistry` does the actual iteration over all elements within the registry. Listing 521 shows the actual iteration over the hash table of `regIOobject` pointers. For each element `writeObject()` is called if the write flag is not set to `NO_WRITE`. Now the method `writeObject()` of the class `regIOobject` is called, since the iteration is over `regIOobject` pointers. This call on Line 16 of Listing 521 causes a registered field to be written to disk.

```

1  bool Foam::objectRegistry::writeObject

```

²⁵²The arguments of the function are dropped in the text for the sake of brevity. In fact there is no method named `writeObject()` with an empty parameter list. This can be checked via these commands: `find $FOAM_SRC -name '*.[CH]' | xargs grep 'writeObject()'`

²⁵³The function signature consists of the name of the function and its parameters.

²⁵⁴In case you ever wondered where these come from.

```

2  (
3      IOstream::streamFormat fmt,
4      IOstream::versionNumber ver,
5      IOstream::compressionType cmp
6  ) const
7  {
8      bool ok = true;
9
10     forAllConstIter(HashTable<regIOobject*>, *this, iter)
11     {
12         // code removed handling debug output
13
14         if (iter()->writeOpt() != NO_WRITE)
15         {
16             ok = iter()->writeObject(fmt, ver, cmp) && ok;
17         }
18     }
19
20     return ok;
21 }
```

Listing 521: Parts of the method `writeObject()` of the class `objectRegistry` in `objectRegistry.C`

In conclusion we have learned by digging the source code of OpenFOAM the magical inner workings of the call `runTime.write()`. First the `Time` class writes its state to disk into the `uniform` folder and then the `objectRegistry` part of the `runTime` object writes all registered fields. It was already mentioned in Section 68.6 that the class `Time` has a multiply divided personality. And some of those even bring along an ancestry. This highlights the need to have a certain understanding of C++ in order to be able to deduce what's going on from the sources of OpenFOAM as OpenFOAM makes very heavy use of C++'s language features such as multiple inheritance, polymorphism and templates. In the context of programming paradigms involved, OpenFOAM makes use of (among others): *object-orientation* and *generic programming*.

68.9 Making an argument – passing arguments

In Listing 516 of Section 68.8 command line arguments were used to influence an application's behaviour. In Section 11.1 different means of exerting control over an application are discussed. There, the point was made that command line arguments are the lowest level of control over an application. Command line arguments need to be specified each time an application is run. Only default values for optional arguments are permanent.

This section discusses some points about command line arguments.

68.9.1 The order of things

If we study applications, which make use of their own command line arguments, we see that there is certain order of things. Listing 522 shows a minimal example of how to define command line arguments.

First, the static method `addBoolOption` method is called to add our own command line argument. Then, the file `setRootCase.H` is included. Listing 523 shows the contents of this file. We see that a variable of the type `Foam::argList` is created and all command line arguments²⁵⁵ are passed to the constructor of `Foam::argList`. The constructor of `Foam::argList` only performs checks on the validity of the already defined options. In fact no further options can be added after the call to the constructor of `Foam::argList`. Once the constructor has been called, an object named `args` exists, which can be used to lookup options and extract information.

```

argList::addBoolOption
(
    "verbose",
    "be more talkative"
);

#include "setRootCase.H"

const bool verbose = args.optionFound("verbose");
```

²⁵⁵In C++ `argc` is the number of command line arguments, and `argv` is the actual command line arguments. `argc` and `argv` are passed from the Terminal to the `main()` method of the application, see `main()`'s method signature: `int main(int argc, char *argv[])`

Listing 522: The order of things in the source code for defining command line arguments

```
Foam::argList args(argc, argv);
if (!args.checkRootCase())
{
    Foam::FatalError.exit();
}
```

Listing 523: The content of the file `setRootCase.H`

68.9.2 Dealing with SPAAAACE!

Having a space in an argument's name is not really a good idea, since the Terminal generally interprets a space as the end of an argument. In common UNIX/Linux tools multi-word arguments are generally separated with hyphens, e.g. `--auto-compress`. In the OpenFOAM universe, we see the use of camel case²⁵⁶, e.g. `-noFunctionObjects` to deal with multi-word argument names.

However, if we really want to have spaces within our argument's name, OpenFOAM allows us to do so. Listing 524 demonstrates how to define an argument named `search point`.

```
argList::addOption
(
    "search point",
    "vector",
    "find the cell containing the specified coords at <vector> - eg, '(1 0 0)'"
)

/* no comment */

vector v;
if (args.optionReadIfPresent("search point", v))
{
    Info<< "Searching cell at point: " << v << endl;
}
```

Listing 524: Reading a point's coordinates from a command line argument

Using an argument with a space in it, requires taking special care, as shown in Listing 525. Quotes are used to prevent the Terminal from interpreting the space within the argument's name as the end of the argument's name.

Listing 526 shows the danger of defining arguments with spaces. In this case the quotes were not used, just as we are used to.

```
findCellByPointCoords -'search point' '(-0.993389 -1.90411 12.4942)'
```

Listing 525: Passing a point's coordinate to an application; note the quotes around the argument's name

```
user@host:~$ findCellByPointCoords -search point '(-0.993389 -1.90411 12.4942)'
```

...

```
--> FOAM FATAL ERROR:
Wrong number of arguments, expected 0 found 2
Invalid option: -search

FOAM exiting
```

Listing 526: Passing a point's coordinate to an application; omitting the quotes around the argument's name leads to a misinterpretation

²⁵⁶https://en.wikipedia.org/wiki/Camel_case

68.10 Turbulence models

In Section 39.3 it is stated that the user can choose between three options.

1. A laminar simulation
2. Using a RAS turbulence model
3. Using a LES turbulence model

This statement is reflected in the relationship between the classes implementing the turbulence models in OpenFOAM. Object oriented programming allows the programmer to translate relationships directly from human language to source code. Two statements can be made about turbulence models

1. All RAS turbulence models are turbulence models, but not all turbulence models are RAS turbulence models.
2. A RAS turbulence model is not the same as an LES turbulence model, however, both are turbulence models.

Both statements are reflected by the class diagram of the turbulence models. On the top is the abstract class `turbulenceModel`. This abstract class, provides the framework for all derived turbulence classes. Also, all functionality common to all possible turbulence classes can be defined in this class. All derived classes will then inherit this functionality.

Each turbulence model is derived from this abstract base class. Each turbulence class will implement specific functionality individually.

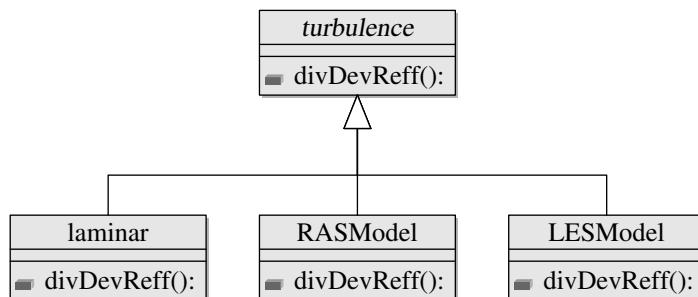


Figure 189: Graphic representation of inheritance of the turbulence model classes.

68.10.1 The abstract base class `turbulenceModel`

The base class `turbulenceModel` is an abstract class²⁵⁷. It contains several pure-virtual functions. To be able to call these functions, these functions must be overridden by the classes that are derived from the base class. A pure-virtual class can not be called. Listing 527 shows the declaration of pure-virtual or abstract methods. The = 0 indicates that a method is abstract.

```
//- Return the turbulence viscosity
virtual tmp<volScalarField> nut() const = 0;

//- Return the effective viscosity
virtual tmp<volScalarField> nuEff() const = 0;
```

Listing 527: Declaration of the virtual methods in `turbulenceModel.H`

The base class contains not only virtual functions. It also contains functions that are the same for all derived classes. Consequently, these functions are implemented by the base class. Listing 528 shows the implementation of the function `nu()`. This function is used to access the laminar or molecular viscosity. The laminar viscosity

²⁵⁷A class that contains one or more abstract methods is called an abstract class. If a class contains only abstract methods, then it is sometimes called a pure-abstract class.

is a property of the fluid itself and has nothing to do with turbulence. However, the turbulence models need to access the laminar viscosity.

```
//- Return the laminar viscosity
inline tmp<volScalarField> nu() const
{
    return transportModel_.nu();
}
```

Listing 528: Implementation of `nu()` in `turbulenceModel.H`

Every class derived from an abstract class must at least override the abstract methods. The non-abstract methods of the base class – like `nu()` from Listing 528 – can be used by the derived classes. No matter if a RAS or a LES turbulence model is used, the laminar viscosity will always be the same.

68.10.2 The class `RASModel`

The class `RASModel` is derived from the abstract class `turbulenceModel`. The class `RASModel` itself is the base class for all RAS turbulence models. It is also an abstract class because it does not override all abstract methods inherited from `turbulenceModel`.

However, the class `RASModel` implements all methods that are common to all RAS turbulence models. Listing 529 shows the implementation of the method `nuEff()` in the class `RASModel`.

```
//- Return the effective viscosity
virtual tmp<volScalarField> nuEff() const
{
    return tmp<volScalarField>
    (
        new volScalarField("nuEff", nut() + nu())
    );
}
```

Listing 529: Implementation of `nuEff()` in `RASModel.H`

The effective viscosity `nuEff` is calculated from the laminar viscosity, which is a property of the fluid, and the turbulent viscosity. The turbulent viscosity is a property of the turbulence model. The function `nu()` in Listing 529 is implemented in the class `turbulenceModel`, see Listing 528. The function `nut()` is not implemented by the class `RASModel`. Therefore, this method must be implemented by the classes derived from `RASModel`.

68.10.3 RAS turbulence models

All RAS turbulence models are derived from the class `RASModel`. Each derived class must implement all remaining abstract methods. Figure 190 shows a simplified class diagram – there is a number of RAS turbulence models available in OpenFOAM.

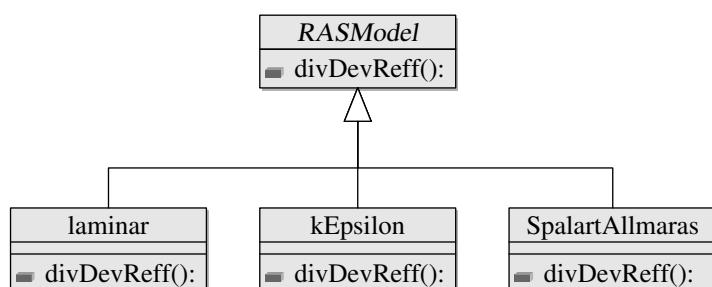


Figure 190: Inheritance of RAS turbulence models

68.10.4 The class `kEpsilon`

The class `kEpsilon` is derived from `RASModel`.

```
class kEpsilon
:
public RASModel
{
/* class definition */
}
```

Listing 530: Class definition of `kEpsilon` in `kEpsilon.H`

The function `nut()` has to be implemented by `kEpsilon`. Listing 531 shows how the function `nut()` is implemented. This function simply returns the class member `nut_`.

```
//- Return the turbulence viscosity
virtual tmp<volScalarField> nut() const
{
    return nut_;
}
```

Listing 531: Implementation of `nut()` in `kEpsilon.H`

The way how `nut_` is calculated differs between the RAS turbulence models. See Listing 574 in Section 73.2.2.

68.11 Debugging mechanism

OpenFOAM brings along a handy debugging mechanism. This mechanism can be used when creating additional model libraries. The OpenFOAM wiki features a section explaining the built-in debug mechanism²⁵⁸.

The global debug flags – controlling the behaviour of the debugging system-wide – are specified in `\$FOAM_SRC/.../etc/controlDict`. From OpenFOAM-2.2.0 onwards the global debug flags can be overridden by stating the debug flags of choice in the case's `controlDict`²⁵⁹.

As this debugging mechanism relies on internal variables no re-compiling is involved when using this kind of debugging mechanism. This kind of debugging is sometimes referred to as *printf debugging*²⁶⁰.

By default all debug switches are initialised with a zero value, therefore the debug feature for the specific class is disabled. However, when the solver sets up the case, the global and local entries are checked. Listing 532 shows the entry in the `controlDict` to override debug switches. Listing 533 shows the solver output informing us of the local settings in `controlDict`.

```
DebugSwitches
{
    DefaultStability      0;
    YoonLuttrellAttachment 1;
}
```

Listing 532: Specifying debug switches in the case's `controlDict`

```
Overriding DebugSwitches according to controlDict
DefaultStability 0;
YoonLuttrellAttachment 1;
```

Listing 533: Solver output when specifying debug switches in the case's `controlDict`

²⁵⁸http://openfoamwiki.net/index.php/HowTo_debugging#Getting_builtin_feedback_from_OpenFOAM

²⁵⁹<http://www.openfoam.org/version2.0/runtime-control.php>

²⁶⁰See <http://oopweb.com/CPP/Documents/DebugCPP/Volume/techniques.html> or <http://en.wikipedia.org/wiki/Debugging#Techniques>

68.11.1 Using the debugging mechanism

If the debugging mechanism is enabled for a class²⁶¹, Listing 534 shows how to actually use it. The code is amazingly simple. The magic behind the scenes provides a variable named `debug`. We simply use this variable in an `if` statement.

```
// print debug information
if (debug)
{
    // debug action
}
```

Listing 534: Using the debug mechanism in a class.

68.11.2 Use case: Write intermediate fields

Listing 535 shows the definition of a method named `Ea`. For debugging purposes we want to write intermediate fields to disk. In Line 7 of Listing 535 we compute a Reynolds number and store it in `ReB`. This is used to generate the return value of the method. In normal operation only the return value is of interest. When debugging also intermediate results may be of interest. The field `ReB` is by default not written to disk and ceases to exist when the scope leaves the method, i.e. when the method reaches its end the variable `ReB` is automatically deleted²⁶².

Note the arguments passed in Line 7. The first is the name of the field. We could omit this argument, however, when we write the variable `ReB` to disk the first argument determines the file name. If this argument was omitted, then an automatically generated name – based on the way the field was generated – would be used. In this very case the file written would be named `max((mag((U1-U2))*d)|nu),0.001`. We easily recognize the formula of Line 7. A file name containing special characters (non-alphanumeric characters) is generally not advisable²⁶³.

In Line 14 we manually call the `write()` method. This method is available to all registered input/output objects²⁶⁴. As we construct the local variable `ReB` from the registered i/o object `Ur` we can safely assume that `ReB` will also be of this type.

```
1 Foam::tmp<Foam::volScalarField> Foam::YoonLuttrellAttachment::Ea
2 (
3     const volScalarField& Ur, const dimensionedScalar& dP
4 ) const
5 {
6     // do stuff
7     volScalarField ReB("ReB", max( Ur*dP/phase2_.nu(), scalar(1.0e-3) ));
8
9     // debug instructions
10    if (debug)
11    {
12        if (Ur.time().outputTime())
13        {
14            ReB.write();
15        }
16    }
17
18    // do more stuff
19 }
```

Listing 535: Manually writing intermediate fields for debugging.

²⁶¹See Section 68.12 on the background of the debugging mechanism.

²⁶²This behaviour is subsumed under the term *automatic variable*. See e.g. http://en.cppreference.com/w/cpp/language/storage_duration

²⁶³See e.g. http://www.teamdrive.com/Invalid_characters_in_file_and_folder_names.html

²⁶⁴See http://openfoamwiki.net/index.php/OpenFOAM_guide/Input_and_Output_operations_using_dictionaries_and_the_IObject_class and http://openfoamwiki.net/index.php/OpenFOAM_guide/objectRegistry

68.12 A glance behind the run-time selection and debugging magic

OpenFOAM offers some amazing features. E.g. at compile-time of a fluid solver nobody knows which turbulence model will be used with the solver. In fact it can be none at all or any of the available. The same is true for drag models and the two-phase Eulerian solver with the exception that you can not use no drag law.

The entire wisdom behind the run-time selection mechanism, however, is more complex than what is presented in this section. Here, we focus on the macros we can find in the source files of the `SchillerNaumann` drag model class. We know, this drag model is derived from the base class `dragModel`. For the run-time selection mechanism to work, the base class also needs to do some preparations. See http://openfoamwiki.net/index.php/OpenFOAM_guide/runTimeSelection_mechanism for a discussion on the run-time selection mechanism. This section hopefully sheds some light into some of the inner workings of the run-time selection mechanism.

We shall now have a look behind the magic powers of OpenFOAM using the SchillerNaumann drag model as an example. The Listings 536 and 537 (Lines 10 and 3) show the two harmlessly looking lines of code enabling all the magic.

```
1 namespace Foam
2 {
3     class SchillerNaumann
4     :
5         public dragModel
6     {
7
8     public:
9         // Runtime type information
10        TypeName("SchillerNaumann");
11    }
12 }
```

Listing 536: The relevant lines of code in `SchillerNaumann.H`

```
1 namespace Foam
2 {
3     defineTypeNameAndDebug(SchillerNaumann, 0);
4 }
```

Listing 537: The relevant lines of code in `SchillerNaumann.C`

68.12.1 Part 1 - `TypeName`

First we will examine Line 10 of Listing 536.

```
TypeName("SchillerNaumann");
```

What looks like a function call is actually a preprocessor macro²⁶⁵ with parameters²⁶⁶. The macro `TypeName` is defined in the file `typeInfo.H`. Listing 538 shows its definition.

A `\#define` macro consists of at least two parts. First comes the identifier, then comes the optional parameter list in parentheses and at least the replacement token list until the end of the line²⁶⁷. As the macro is expanded by the preprocessor, the identifier (in this case `TypeName`) is replaced with the replacement tokens (all instructions after the parameter list). A macro can not cover more than one line, however, by using the backslash (\) the current line is continued with the next line²⁶⁸.

```
1 // Declare a ClassName() with extra virtual type info
2 #define TypeName(TypeNameString) \
3     ClassName(TypeNameString); \
4     virtual const word& type() const { return typeName; }
```

Listing 538: The macro definition in `typeInfo.H`

²⁶⁵http://en.wikipedia.org/wiki/C_preprocessor

²⁶⁶See e.g. <http://www.cplusplus.com/doc/tutorial/preprocessor/>

²⁶⁷<https://gcc.gnu.org/onlinedocs/cpp/The-preprocessing-language.html>

²⁶⁸<https://gcc.gnu.org/onlinedocs/cpp/The-preprocessing-language.html#The-preprocessing-language>

Thus, the line `TypeName("SchillerNaumann");` expands to.

```
ClassName("SchillerNaumann");
virtual const word& type() const { return typeName; }
```

The second line is a function definition. As this function definition is made by the macro, this function is defined for every class where the `TypeName` macro is stated in the class definition. This demonstrates one of the major reasons for using preprocessor macros – the ability to write recurring pieces of code just once.

The first line of the above listing is itself a macro. Listing 539 shows the macro definitions that are necessary to expand the `ClassName` macro.

```
1 //-- Add typeName information from argument \a TypeNameString to a class.
2 // Also declares debug information.
3 #define ClassName(TypeNameString) \
4     ClassNameNoDebug(TypeNameString); \
5     static int debug \
6
7 //-- Add typeName information from argument \a TypeNameString to a class.
8 // Without debug information
9 #define ClassNameNoDebug(TypeNameString) \
10    static const char* typeName_() { return TypeNameString; } \
11    static const ::Foam::word typeName
```

Listing 539: Two macro definitions in `className.H`

Thus, we further expand the `TypeName("SchillerNaumann")` macro.

```
static const char* typeName_() { return "SchillerNaumann"; } \
static const ::Foam::word typeName
static int debug
virtual const word& type() const { return typeName; }
```

As the `TypeName("SchillerNaumann")` macro was put into the class definition of the `verb+SchillerNaumann+` class, the macro added two function definitions (first and last line), one of which is a static method, and two static variables (the two center line).

Static elements of class (variables or methods) are elements that exist only once for all instances of a class²⁶⁹. In the case of a two-phase Eulerian solver two instances of the `SchillerNaumann` class might exist – in the case this model was specified for both phases. No matter which of the two instances of the class call the method `typeName()` it is always the same function called. In this case – returning the name of the class – the use of a static method makes perfect sense and is the only sensible way to implement this task.

The `TypeName("SchillerNaumann")` macro is used to create a method that returns the name of the class and a method that return the name of the type. Obviously, the class name and the type name were not considered equivalent when designing OpenFOAM²⁷⁰. The variables created by the `TypeName("SchillerNaumann")` macro are a static variable containing the type name and a static variable named `debug`. This `debug` variable controls the debug mechanism covered in Section 68.11.

68.12.2 Part 2 - `defineTypeNameAndDebug`

Now we will examine Line 3 of Listing 537 which is repeated just below.

```
defineTypeNameAndDebug(SchillerNaumann, 0);
```

The `defineTypeNameAndDebug` macro is defined the file `className.H`.

```
1 //-- Define the typeName and debug information
2 #define defineTypeNameAndDebug(Type, DebugSwitch) \
3     defineTypeName(Type); \
4     defineDebugSwitch(Type, DebugSwitch)
```

Listing 540: A macro definition in `className.H`

²⁶⁹http://www.tutorialspoint.com/cplusplus/cpp_static_members.htm

²⁷⁰See Section 68.12.3 for an example when class name and type name are different.

Thus our macro expands to two macros.

```
defineTypeName(SchillerNaumann);
defineDebugSwitch(SchillerNaumann, 0);
```

Listing 541 shows the macro definitions necessary to expand the above two macros.

```
1 //-- Define the typeName, with alternative lookup as \a Name
2 #define defineTypeNameWithName(Type, Name) \
3     const ::Foam::word Type::typeName(Name)
4
5 //-- Define the typeName
6 #define defineTypeName(Type) \
7     defineTypeNameWithName(Type, Type::typeName_())
8
9 //-- Define the debug information, lookup as \a Name
10 #define defineDebugSwitchWithName(Type, Name, DebugSwitch) \
11     int Type::debug(::Foam::debug::debugSwitch(Name, DebugSwitch))
12
13 //-- Define the debug information
14 #define defineDebugSwitch(Type, DebugSwitch) \
15     defineDebugSwitchWithName(Type, Type::typeName_(), DebugSwitch); \
16     registerDebugSwitchWithName(Type, Type, Type::typeName_())
```

Listing 541: Four macro definitions in `debugName.H`

Thus, our macros expand to:

```
const ::Foam::word SchillerNaumann::typeName(SchillerNaumann::typeName_());
int SchillerNaumann::debug(::Foam::debug::debugSwitch(SchillerNaumann, 0));
registerDebugSwitchWithName(SchillerNaumann, SchillerNaumann, SchillerNaumann::typeName_());
```

The first line of the expansion of the macro `defineTypeNameAndDebug(SchillerNaumann, 0)` assigns the return value of the function `typeName_()` to the static variable `typeName`. This has the effect that the class name and the type name have an equal value. However, the way this framework is set up allows for different names.

The second line assigns the return value of the function call `::Foam::debug::debugSwitch(SchillerNaumann, 0)` to the static variable `SchillerNaumann::debug`. The reason why the value is not directly used to assign the value to the static variable is that the called method adds the debug switch to a dictionary, see Listing 542.

The last line of the macro expansion invokes another macro. Listing 543 shows the macro definition of `registerDebugSwitchWithName`.

```
1 int Foam::debug::debugSwitch(const char* name, const int defaultValue)
2 {
3     return debugSwitches().lookupOrAddDefault
4     (
5         name, defaultValue, false, false
6     );
7 }
```

Listing 542: Adding the debug switch to the dictionary in `debug.C`

```
1 //-- Define the debug information, lookup as \a Name
2 #define registerDebugSwitchWithName(Type, Tag, Name) \
3     class add##Tag##ToDebug \
4     : \
5         public ::Foam::simpleRegIOobject \
6     { \
7     public: \
8         add##Tag##ToDebug(const char* name) \
9             : \
10             ::Foam::simpleRegIOobject(Foam::debug::addDebugObject, name) \
11         {} \
12         virtual ~add##Tag##ToDebug() \
13     {}
```

```

14     virtual void readData(Foam::Istream& is)
15     {
16         Type::debug = readLabel(is);
17     }
18     virtual void writeData(Foam::Ostream& os) const
19     {
20         os << Type::debug;
21     }
22 };
23 add##Tag##ToDebug add##Tag##ToDebug_(Name)

```

Listing 543: Definition of the `registerDebugSwitchWithMacro` macro in `debugName.H`

68.12.3 A walk in the park: demonstrate some of this magic

In the above sections we took a look behind two very powerful pre-processor macros. So, what is this all for?

The turbulence models are very prominent examples for the usefulness of the run-time selection mechanism. At compile-time – the time we or the OpenFOAM developers compile a solver – nobody knows, what exact turbulence model we want to use for our simulation. Thus, we need to decide at run-time – at the time the solver reads all the case information – which turbulence model to use. In order to save us from writing a solver for each turbulence model, solvers can be written in a generic way. I.e. at the time we compile the solver nobody, not even the compiler, cares about the actual turbulence model. The base class `turbulenceModel` tells the compiler and the solver how a turbulence model works, that is all we need to know at compile time.

However, at run-time we need to decide which turbulence model to use. Fortunately, OpenFOAM takes care of that and we do not need to bother. In some cases, however, we would like to know which turbulence model is currently used. We could achieve this by either reading the case data²⁷¹ or by making use of the run-time magic.

Listing 544 shows three lines of code. The intention behind this line is to print the return values of the methods `typeName_()` and `type()`. These two methods were provided by the two macros dissected in Sections 68.12.1 and 68.12.2.

```

1 Info << "Happy printf() debugging:" << endl;
2 Info << turbulence->typeName_() << endl;
3 Info << turbulence->type() << endl;

```

Listing 544: Applying some of the magic, the source code.

Listing 545 shows the results of the three lines of code of Listing 544. The code in Listing 544 presumes that turbulence modelling is used in its generic form, as it is the case in e.g. `pimpleFoam`. In this example the variable `turbulence` is of the type `autoPtr<incompressible::turbulenceModel> turbulence`.

From the output we see, that the variable `turbulence` is indeed of type `turbulenceModel`. However, as the class `turbulenceModel` is an abstract base class, no solver will ever actually use `turbulenceModel` itself²⁷². In this case, the solver used the `kOmega` turbulence model. Thus, the method `type()` returns the name of the actual turbulence model. Here we also see the sense behind the distinction between the class name and the type name as discussed some paragraphs above. In the example of a concrete class those are the same. For a base class, however, this distinction makes perfect sense.

```

1 Happy printf() debugging:
2 turbulenceModel
3 kOmega

```

Listing 545: Applying some of the magic, the output.

²⁷¹This would mean re-programming existing functionality. The case data related to turbulence modelling was already read by the constructor of the turbulence model. Manually reading this information again would result in some kind of code duplication. The more elegant way to solve this problem is to access the information already gathered.

²⁷²See Section 68.10 for information about how turbulence models are organized in OpenFOAM.

68.13 Notes on running OpenFOAM in parallel

OpenFOAM is perfectly capable of running on multiple processors, however, even as OpenFOAM hides some or most of the technical issues arising from running in parallel from the programmer by its very intelligent design, there are still some things we need to consider and pitfalls we may stumble into.

First of all, let us take a moment and thank the universe, that OpenFOAM does so much on its own, in the background, when it comes to parallel running²⁷³. If you restrict yourself to OpenFOAM's high-level data structures, as any sensible human being should, then you get *running in parallel* basically for free. You would not want to get into the details of how Lagrangian particles traverse sub-domains, or how to compute the gradient of a field at the very boundary of a sub-domain.

This section is devoted to topics which offer us mere mortals the chance to nevertheless mess up despite all the magic OpenFOAM brings to the table. Other topics, such as printing to Terminal²⁷⁴, are presented out of curiosity, as in *how to do X?*

68.13.1 Printing to Terminal

When running an application in parallel, we might want for each one of the parallel processes being able to print to the Terminal, or we might want that only the master process can print to the Terminal. OpenFOAM allows you to do both.

Hush! The master is printing

If you want only the master to print to the Terminal, all is well. Just continue to use the `Info` statement we are all familiar with.

```
1 // this should be printed only once
2 Info << "Hello OpenFOAM World!" << endl;
```

Listing 546: Printing to the Terminal using the `Info` statement.

The output of Listing 546 is shown in Listing 548, which is the result of a parallel run with 4 processes²⁷⁵.

Parallel print, the choir of processes

If we want all of the parallel processes to have their say, respectively print to Terminal, we can use the `Pout` statement. This statement allows each running process to print to the Terminal.

```
1 // this should be printed only once
2 Info << "Hello OpenFOAM World!" << endl;
3
4 // this should be printed once for each running process
5 Pout << "... this is process " << pid() << " speaking!" << endl;
```

Listing 547: Printing to the Terminal using the `Pout` statement.

The `Pout` statement prepends the output message with the processor number, which starts counting from 0, and 0 being the master process. Note in Listing 548 that the order in which the individual processes print to the Terminal is not fixed.

```
1 Hello OpenFOAM World!
2 [1] ... this is process 2315 speaking!
3 [2] ... this is process 2316 speaking!
4 [0] ... this is process 2314 speaking!
5 [3] ... this is process 2317 speaking!
6 Finalising parallel run
```

Listing 548: Resulting output of Listing 547.

²⁷³If you think otherwise, or are curious, see <http://mpitutorial.com/tutorials/> as a starting point for getting into the nitty-gritty of implementing parallel communication using MPI.

²⁷⁴It would require a bit of (evil) creativity on the part of the user to mess up something as simple as printing to Terminal.

²⁷⁵... if the author is to be believed.

68.13.2 Condensing values (sums, extrema)

If we want to sum up all the values of a field, or if we want to determine the extrema (minimum and maximum), we most probably want to perform these operations globally, i.e. across all our sub-domains in a parallel run.

What needs to be done, is to perform the operation, e.g. summing up, within the sub-domain, communicating the result (e.g. all processes report to the master), and continuing the operation (the master determines the final result).

As OpenFOAM's developer designed the code base to be most friendly to the user, there are statements named `gSum`, `gMin`, `gMax` and others, which do exactly that.

```
1 // correct in serial, however, not so in parallel
2 Info<< "Sum of field U : " << sum(mag(X)*mesh.V()) << endl;
3
4 // correct summing-up
5 Info<< "Sum of field U : " << gSum(mag(X)*mesh.V()) << endl;
```

Listing 549: Computing and printing the total amount of field `X` to the Terminal.

If we were to sum up `mesh.V()`, which is a scalar field made-up of the cell's volumes, we get the total volume of the domain, when we use `gSum(mesh.V())`. If we used `sum(mesh.V())`, then we would get roughly the total domain's volume divided by the number of processes. This is roughly an N -th of the domain's volume, as decomposition does not always yield sub-domains with a size exactly one N -th of the global domain, e.g. when having an even number of cells and dividing into three parts.

68.14 Math-like syntax in OpenFOAM

OpenFOAM is designed in a way, for its top-level code to resemble mathematical notation, or to quote the original paper [68]:

The intention is to develop a C++ class library that makes it possible to implement complicated mathematical and physical models as high-level mathematical expressions. This is facilitated by making the high levels of the code resemble as closely as possible standard vector and tensor notation.

68.14.1 Pitfalls

Operator precedence: use caution with vector products

In mathematics certain operations are evaluated with priority over others²⁷⁶. The same holds true for most programming languages. The general rules of operator precedence²⁷⁷ in C++ closely follow the rules known from mathematics.

However, as OpenFOAM extends the rudimentary mathematical capabilities of standard C++ with concepts such as vectors and tensors, the question of operator precedence becomes interesting. Since, there are no vector products in C++ and completely new operators can not be defined, some existing operators have to be overloaded to implement the vector products. Furthermore, the operator precedence of existing operators can not be altered.

As it turns out, the bitwise AND (`&`) and bitwise XOR (`^`) have been overloaded to implement the inner and outer vector product. An unfortunate side-effect of using these operators is, that the inner and outer vector product have a lower precedence than the basic operators such as addition, subtraction and multiplication. This is because the bitwise AND and bitwise XOR operators have a quite low precedence.

To the unsuspecting user, it may come as a surprise when the following formula results in a compilation error:

$$\mathbf{a} \cdot \mathbf{b} - c$$

As mentioned above, the unexpected operator precedence leads to:

$$\mathbf{a} \cdot (\mathbf{b} - c)$$

²⁷⁶https://en.wikipedia.org/wiki/Order_of_operations

²⁷⁷https://en.cppreference.com/w/cpp/language/operator_precedence

Trying to compile the formula from above, translated into OpenFOAM source code:

```
1 const vector a(1.0, 2.0, 3.0);
2 const vector b(0.0, 42.0, 666.0);
3 const scalar c(0.815);
4
5 vector d( a & b - c);
```

Listing 550: This simple vector operation leads to a compiler error.

leads to a compiler error. Among the potentially plentiful lines of compiler warning and error messages, the line below is the relevant one. It informs us of our intent to subtract a scalar from a vector, which is undefined.

```
error: no match for 'operator-' (operand types are 'const vector {aka const Foam::Vector<
double>}' and 'const scalar {aka const double}'')
```

Listing 551: The compiler error message

Thus, users are advised to use plenty of parentheses to avoid such problems. The issue with operator precedence is well explained by Hrv Jasak in a forum post²⁷⁸:

That's because operator& and operator^ are really binary C++ operators in C++ and the language does not allow you to define your own operators or change operator precedence.

We have chosen to re-use the operators for nice syntax - makes the code look nice. Therefore, all I can recommend is lots of brackets in vector/tensor products.

The same also applies to the double inner product, which takes two tensors of at least 2nd order. This operator is implemented by overloading the logical AND (&&) operator, which has an even lower precedence than the bitwise binary operators.

²⁷⁸<https://www.cfd-online.com/Forums/openfoam/61023-operator-precedence.html>

69 General remarks on OpenFOAM programming

This section covers some general advice for users who want to implement their own models and solvers or modify existing ones.

69.1 Preparatory tasks

69.1.1 Create user specific directories

In order to be able to distinguish between the standard solvers and models from the solvers and models created by the user, some new directories have to be created. Not only do we need to keep our models and applications apart from the models and applications of the standard OpenFOAM installation, we also need to keep our models and applications from those of other users. Thus, every user will get his or her own user directory. The name of this user directory follows OpenFOAM's naming convention which combines the user name and the version number of OpenFOAM, i.e. `user-4.0`. Thus, we can also keep our own stuff for OpenFOAM-X separate from the stuff for OpenFOAM-Y.

In this, we follow the organisational scheme of OpenFOAM's standard solvers and models, of which the source code resides in `$WM_PROJECT_DIR/applications/solvers` and `$WM_PROJECT_DIR/OpenFOAM-2.1.x/src`. Therefore, we need to create some folders to place our sources in: `$WM_PROJECT_USER_DIR/applications/solvers` and `$WM_PROJECT_USER_DIR/src`. Listing 552 lists the necessary commands. Open a Terminal and type the commands of the Listing to do the job.

```
cd $WM_PROJECT_USER_DIR
mkdir -p applications/solvers
mkdir src
```

Listing 552: Create the proper directories for a user's solvers and models

Note the use of the variable `$WM_PROJECT_USER_DIR`, which resolves to your OpenFOAM installation's user directory, which also contains the run-directory (`$FOAM_RUN`).

Apart from the aspect of keeping good order, there's also another considerations: permissions. On our own workstation, with OpenFOAM being installed in the user's `home` directory, we have no problem putting our own source files into OpenFOAM's source code and extend the existing code base. However, on shared system, with OpenFOAM being installed system-wide, we may have no write permissions for the folders in which OpenFOAM's source code resides.

Thus, in order to not pick up bad working habits, it is strongly advised to follow procedures on our own workstation which can be directly transferred to shared machines.

69.2 Start from existing code

69.2.1 Copy the sources

If you want to create a new model or solver, it is generally recommended to base it on the model or solver from OpenFOAM's standard installation, which comes closest to your intended set of features.

69.2.2 Change compilation settings

Before proceeding any further certain compilation settings have to be changed from the settings of OpenFOAM's standard code base.

Change the executable's or library's name

The executable's or library's name is determined by a setting in the file `Make/files` of the source code of the respective solver or model. For a solver the name of the executable is determined by the setting `EXE`. Listing 554 shows how the name of the executable for the solver `pimpleFoam` is defined.

```
EXE = $(FOAM_APPBIN)/pimpleFoam
```

Listing 553: Setting the name of `pimpleFoam`'s executable in the file `Make/files` of `pimpleFoam`'s source code²⁷⁹

Analogously, defining the name of the shared library²⁸⁰ is done by the setting `LIB` in the file `Make/files` of the library's source code.

```
LIB = $(FOAM_LIBBIN)/liblagrangian
```

Listing 554: Setting the name of the shared object of the Lagrangian particle library in the file `Make/files` of Lagrangian library source code

The settings for `EXE` and `LIB` are full file paths. Thus, next to the assignment (the `=` symbol) we find a directory, the path name separator (the `/` symbol) and the actual name of the executable or shared library.

Change the executable's or library's location

Avoiding mixing up user created solvers and models from the ones provided by OpenFOAM's standard installation involves apart from changing the file name of the executable or shared object also the path the executable or shared object resides in. This is specified, as already shown above, in the file `Make/files`.

For user created solvers and models, users are advised to change the path specifier to `FOAM_USER_APPBIN` or `FOAM_USER_LIBBIN` respectively. Thus, user generated solvers and libraries are also spatially separated²⁸¹ from standard solvers and libraries.

If you use a system-wide OpenFOAM installation, then you most probably have only read access to the `FOAM_APPBIN` and `FOAM_LIBBIN` directories. Thus, trying to compile your solver or model will fail, even when there are no errors. In this case, the resulting error message might contain some hint about missing permissions.

Check `Make/files`

After adjusting the compilation settings, check and re-check the file `Make/files`. Listing 555 shows the vital entries of the file highlighted. In the listing, the source file has the same name as the executable. Furthermore, the executable will be located in the user's application directory.

```
myApplication.C  
EXE = $(FOAM_USER_APPBIN)/myApplication
```

Listing 555: The content of `Make/files`

The file `Make/files` controls what is compiled and where the resulting executable will be stored. Thus, getting `Make/files` right will save yourself from breaking something else, i.e. the model or application you base your new model or application on. On the other hand, the file `Make/options` controls what is needed to successfully compile the model or application. Getting `Make/options` wrong initially will do no harm.

Check `Make/options`

The file `Make/options` tells the compiler where to find additional source files, and it tells the linker²⁸² where to find additional libraries. The file `Make/options` only needs to be edited, if you use existing models, or source files from other directories. This, however, is often the case.

The content of the file `Make/options` is divided in two parts. First, there are the paths for compiler to look for source files to include. The second part is a list of libraries for the linker to link the current model or application with.

²⁷⁹The executable does not necessarily have to have the same name as the source file. However, different names can lead to confusion and make code maintenance harder. Therefore, it is strongly recommended to use consistent names, i.e. to name the source file `SOLVER.C` and the executable `SOLVER`.

²⁸⁰The main purpose of dividing code into applications and libraries is to allow for multiple unconnected applications using certain implemented behaviour (the libraries). Thus, libraries are shared by an arbitrary number of applications. Hence, libraries are compiled into files which are referred as *shared objects* or *shared libraries*. The names of these files are appended by the filename extension `.so`, i.e. `libraryName.so`.

²⁸¹by residing in different directories

²⁸²Compilation of C or C++ code is usually done in two steps. First all files are compiled and then the object files generated by the compiler are linked together to form the executable.

```

EXE_INC = \
-I$(LIB_SRC)/meshTools/lnInclude \
-I$(LIB_SRC)/finiteVolume/lnInclude

LIB_LIBS = \
-lmeshTools

```

Listing 556: Content of `Make/options`

Initial compilation

Once the existing sources have been copied and, most importantly, the compilation settings have been changed, we can run an initial compilation. Although, at this point, nothing in the source code has changed, running an initial compilation is recommended to check whether we have got the compilation settings right.

For applications simply execute `wmake`, for shared libraries the compiler gets an additional parameter: `wmake libso`. After the compilation the compiled binary should show up in `FOAM_USER_APPBIN` or `FOAM_USER_LIBBIN` respectively.

69.3 Create the source code from scratch

The steps discussed above may not be needed by certain users. OpenFOAM provides some macros to create the basic source-code-skeleton for, among others, new applications, boundary conditions or functions objects. In the case of creating a new application from scratch, the user simply calls the macro `foamNewApp` and provides the desired application name. The executable's path will automatically be set to `FOAM_USER_APPBIN`. New function objects or boundary conditions will automatically be compiled into `FOAM_USER_LIBBIN`.

69.4 Using a user-created libraries

Distinguishing between solvers and libraries is a good thing, since we can create and reuse certain models. If we want our application to use a model of ourself, we need to tell the compiler and the linker where to find our (already compiled) model.

In Listing 557 we see the necessary entries for the file `Make/options` for an application which is to use a user-created library with the very creative name *myLibrary*. The green line in Line 4 of the listing tells the compiler where to find the source code of the library *myLibrary*.

After the compilation stage finished successfully, the compiled application needs to be linked to the compiled library, i.e. shared object. This is shown in the Lines 8 and 9 of the Listing. The red line defines an additional directory in which to look for shared objects. As good style dictates us to compile our own libraries into `FOAM_USER_LIBBIN`, the additional directory for the linker is `FOAM_USER_LIBBIN`.

The blue line, Line 9 of the Listing, then tells the linker the name of the shared object of *myLibrary*.

```

EXE_INC = \
-I$(LIB_SRC)/meshTools/lnInclude \
-I$(LIB_SRC)/finiteVolume/lnInclude \
-I$(MY_LIB_SRC_PATH)/myLibrary/lnInclude

LIB_LIBS = \
-lmeshTools \
-L$(FOAM_USER_LIBBIN) \
-lmyLibrary

```

Listing 557: Content of `Make/options` of an application using a user-created library

69.5 Pitfalls

Modifying existing models or creating new ones bears the potential for many bugs and errors. This section tries to discuss some of them, which either occur regularly or may be difficult to track down. Such a list can never be complete and it is clearly biased towards the errors made and encountered by the author. These errors are not necessarily restricted to OpenFOAM, moreover, modifying OpenFOAM involves programming and programming involves bugs and errors. Enjoy reading.

69.5.1 Segfault due to modified library and failing to update the solver

Libraries are reusable parts of code, which are independent of the solver(s) using them. However, this independence may create problems if we modify the library and fail to recompile the solver(s) that are using said library, even if said solver(s) have not been touched. The problem that might occur is a segmentation fault (*segfault* in short) at construction of the modified objects. Unfortunately, a segfault does not produce very telling error messages, see Listing 558. Note that we assume that compilation of the library finished successfully.

```
#0  Foam::error::printStack(Foam::Ostream&) at ?:?:?
#1  Foam::sigSegv::sigHandler(int) at ?:?:?
#2  ? in "/lib/x86_64-linux-gnu/libc.so.6"
#3  ? in "/lib/x86_64-linux-gnu/libc.so.6" Segmentation fault (Core dumped)
```

Listing 558: A segmentation fault

The reason for this behaviour, the solver violently fails at start-up due to a segmentation fault, is that our modifications to the library changed its memory layout. As we did not recompile the solver, the solver had no means to learn about the changed memory layout. Thus, at solver start-up, the solver reserves an incorrect amount of memory for the objects of the library. At construction of these objects, this mismatch causes the segmentation fault.

Recompiling the solver, which has not been touched seems at first counter-intuitive. However, when the memory layout of the library changed, the solver will reserve memory according to the old memory layout. Recompiling the solver will simply update memory allocation.

The tricky bit of this error, is that it does not always occur. If we change a library and our changes do not alter the memory layout, all is well. No error will occur. This opens the possibility of *modifying the library and running the solver using that library* to sometimes work and sometimes cause this error.

Further reading

<https://stackoverflow.com/questions/2346806/what-is-a-segmentation-fault>
https://en.wikipedia.org/wiki/Segmentation_fault

69.5.2 (Failing to) Tell the solver to use a library

Modifying an existing library, or creating your own from scratch, results in a new shared object file in the `FOAM_USER_LIBBIN` directory. However, if you want your solver to make use of this library, you need to tell the solver to do so. *Models in FOAM_USER_LIBBIN are not loaded by an application by default!*

This is done via the `libs` list entry in `controlDict`, see Section 11.3.3. Failing to do so results in a very odd situation. The model compiles without error; the solver, if you are using your own, also compiles without error²⁸³; the case setup seems without error²⁸⁴; and yet the case does not run, when you try to make use of your own model. In this situation, the seemingly correct case setup yields the same result as the *banana test* (see Section 11.2.1), since OpenFOAM is unable to find the correct model associated with the name we provided in the case files.

69.6 Tips

Check and double-check that you compile to the user-directories

Always make sure, that you compile your applications to `FOAM_USER_APPBIN` and your libraries to `FOAM_USER_LIBBIN`. The reason for this, and the way how to ensure this, are discussed in 69.2.2.

When modifying a library, also recompile the solver(s) using the library

This mean a seemingly extraneous step²⁸⁵, however, it might prevent weird behaviour. One reason for recompiling the solver using a recently modified library was discussed above in Section 69.5.1.

Furthermore, especially when templates are involved, e.g. you modify a templated class, it is vital to compile the library which provided the templated model and the solver that uses the templated model. Templates need special attention, care and love, do not neglect them.

²⁸³If the library compilation had failed, the linker would throw an error, if you tried to compile a solver using that library.

²⁸⁴i.e. the case runs, when you use only standard OpenFOAM features.

²⁸⁵In some cases it is sufficient only to compile the library, e.g. when fixing a type in an `Info` message.

Use Allwclean or wclean liberally

Clean-up your temporary build-files for good measure by running wclean. Especially when templated classes are involved, clearing build-files might be essential.

Also, if you update the underlying OpenFOAM version, recompiling your custom libraries and solvers will also require cleaning of the build-files. If the underlying OpenFOAM installation, then the dependency list, i.e. the `*.dep` file present in the `Make` directory of your code, may contain the file-names of files which might have ceased to exist.

69.7 Case study: extending an existing model library

Since the points discussed so far have been quite general, we shall walk through the process of extending an existing model library by another additional model. This shall serve as a demonstration of the pertinent points of this topic.

Porting the JouleHeating fvOption model to OpenFOAM-7

OpenCFD/ESI released a fvOptions model for Joule heating with version 17.06 of OpenFOAM²⁸⁶. Joule heating is the process of heating a conductor via the passage of electrical current. This is usually relevant for solid bodies, which are heated and in turn transfer heat to other solid bodies in contact as well as the surrounding fluids.

A simulation project which involved the electrical heating of a metal sample in a test chamber and the subsequent establishment of a thermally driven flow in said test chamber made it necessary to port the Joule heating fvOptions model to OpenFOAM-7, which was the OpenFOAM installation in use on our computational systems.

Since the involved code bases are compatible, this is basically a textbook case of extending OpenFOAM-7 with a non-user created additional model. Copy&pasting source code from OpenFOAM-17.06 and adjusting compilation settings can hardly be considered model development. However, with this example we can perfectly illustrate the workflow involved in extending an existing model library. Since fvOptions also exist in OpenFOAM-7, we are basically only adding the Joule heating model.

69.7.1 Setting up our model's source tree

First, we create a proper model source tree. Listing 191 shows the directory listing with all files in place. The `Allwclean` and `Allwmake` scripts are optional in this case. If we had more libraries in `/OpenFOAM/user-7/src/` they might be of use, e.g., following an update of the underlying source code of OpenFOAM, which necessitates a re-compilation of all of our models.

We have created the model source tree in this case by copying the whole fvOptions source tree of OpenFOAM-17.06 into our own user-specific model source folder²⁸⁷ followed by deleting everything that's not related to Joule heating. After deleting the unrelated files and folders, only the content listed in Listing 191 remains, except the `Allwclean` and `Allwmake` scripts which were created by us.

²⁸⁶<https://www.openfoam.com/news/main-news/openfoam-v1706>

²⁸⁷Translated into a Linux command, this amounts to the following:

```
cp -r /home/user/OpenFOAM/OpenFOAM-v1706/src/fvOptions /home/user/OpenFOAM/user-7/src/myFvOptions
```

```

user@host:~/OpenFOAM/user-7/src/myFvOptions$ tree
.
├── Allwclean
├── Allwmake
├── Make
│   ├── files
│   └── options
└── sources
    └── derived
        └── jouleHeatingSource
            ├── jouleHeatingSource.C
            ├── jouleHeatingSource.H
            └── jouleHeatingSourceTemplates.C

```

Figure 191: The model source tree of our new model for OpenFOAM-7.

A slight tangent: what if we do not delete the unrelated files?

If we left all the original source files in place and only adjusted the compilation settings, we would end up with a source tree that can be compiled without any problems. However, there would be trouble later on.

In this case, we would create duplicates of all models that are present in both fvOptions libraries, the one of OpenFOAM-17.06 (which we copied over to our model source folder) and the one of OpenFOAM-7 (which is the version we are working on, and for which we want to compile our new model). One such model common to both versions of OpenFOAM is `semiImplicitSource`.

If we now create a case which uses our new model library, i.e., `myFvOptions`, then OpenFOAM would encounter pairs of classes having the same name coming from two different libraries. There would be a class called `semiImplicitSource` from the original `libfvOptions` library of OpenFOAM-7 and there would also be a class called `semiImplicitSource` from our own `libmyFvOptions` library.

Listing 559 shows a shortened snippet of warning message which is the result of having duplicate models in our own model library.

```

... output removed for clarity

Creating finite volume options from "system/fvOptions"

Selecting finite volume options type jouleHeatingSource
Duplicate entry semiImplicitSource in runtime selection table fvOptions
#0 /home/user/OpenFOAM/OpenFOAM-7/platforms/linux64GccDPInt32Opt/lib/libOpenFOAM.so(
    _ZN4Foam5error14safePrintStackERSo+0x49) [0x75218fa0a3c9]
#1 /home/user/OpenFOAM/OpenFOAM-7/platforms/linux64GccDPInt32Opt/lib/libfvOptions.so(+0x57203)
) [0x75218e2f2203]
#2 /lib64/ld-linux-x86-64.so.2(+0x647e) [0x75219394647e]

... output removed for clarity

Duplicate entry semiImplicitSource in runtime selection table fvOptions
#0 /home/user/OpenFOAM/OpenFOAM-7/platforms/linux64GccDPInt32Opt/lib/libOpenFOAM.so(
    _ZN4Foam5error14safePrintStackERSo+0x49) [0x75218fa0a3c9]
#1 /home/user/OpenFOAM/OpenFOAM-7/platforms/linux64GccDPInt32Opt/lib/libfvOptions.so(+0x57203)
) [0x75218e2f2203]
#2 /lib64/ld-linux-x86-64.so.2(+0x647e) [0x75219394647e]

... output removed for clarity

```

Listing 559: The warning message of OpenFOAM when it encounters duplicate classes in a case using a library which duplicates already existing models.

While this does not immediately kill our case, OpenFOAM filling screens and screens with warning message is not a sign that instills confidence into our ways of doing things.

A tangent to the tangent: what if we really want to duplicate stuff? Temporarily.

Sometimes, duplication is our entry point into developing a model of our own. If an existing model is close to our intended goals, it is a valid approach to first duplicate the existing model we want to work from, and then modify the duplicate to implement our intended purpose.

Here, we would copy the existing model in question and clean-up if necessary. Then, we need to adjust the compilation settings. Finally, to take care of the duplication issue, we need to change class names.

We will discuss this using a concrete example. Consider we want to use the functionObject `MachNo` as the starting point for a functionObject of our own `myNonDimNum`. First, we start by copying the relevant source code from the existing OpenFOAM sources and clean-up our copy. Then, we need to rename the source files of our copy from `MachNo` to `myNonDimNum`, as well as replace all occurrences of `MachNo` in those files with `myNonDimNum`. Listing 560 shows the relevant Linux commands, so that we don't need to do all this replacing manually, which would be error prone.

We start from the cleaned-up copy of the existing source code, thus only `MachNo` and `Make` are present in our own `myFunctionObjects` library. First, we rename the `MachNo` folder using `mv`. Then, we rename all files contained in the newly renamed folder using `rename`.²⁸⁸ Finally, we replace all occurrences of `MachNo` in those files by `myNonDimNum` using `sed`. The fact that `rename` and `sed` use the same syntax for the renaming/replacing is very convenient.

```
user@host:~/OpenFOAM/user-9/src/myFunctionObjects$ ls
MachNo  Make
user@host:~/OpenFOAM/user-9/src/myFunctionObjects$ mv MachNo myNonDimNum
user@host:~/OpenFOAM/user-9/src/myFunctionObjects$ rename 's/MachNo/myNonDimNum/g' myNonDimNum
/*
user@host:~/OpenFOAM/user-9/src/myFunctionObjects$ sed -i 's/MachNo/myNonDimNum/g' myNonDimNum
/*
```

Listing 560: Avoiding the duplication issue when duplicating an existing model.

If we now compile our `myFunctionObjects` library, we create a functional duplicate of `MachNo` but without any duplication issues as mentioned above. Though our new functionObject essentially still does the same as `MachNo`, it has a new different name that is not present in the standard `functionObjects` of OpenFOAM.

Once, we have made sure our copy compiles and can be used in a case without any errors; we have assured ourselves to have a valid working base. Thus, we can start making modifications to our functionObject.

69.7.2 Adjusting the compilation settings

Next, we need to adjust the settings for the compiler. Since the files in the `Make` folder are still copies of the original OpenFOAM-17.06 source code, we need to adjust them as well. Similar to the source tree, we need to delete everything unrelated within these files. Listing 561 shows the remaining contents of `Make/files`.

The last line of Listing 561 specifies the full path of the resulting binary file. Here, we have replaced `FOAM_LIBBIN` with `FOAM_USER_LIBBIN`, and we have chosen a new name: `libmyFvOptions` instead of `libfvOptions`. The presence of the variable `derivedSources` is a remnant of the original `Make/files` file. We could have eliminated its use, since this is clearly not needed when only compiling one file.

```
user@host:~/OpenFOAM/user-7/src/myFvOptions$ cat Make/files
derivedSources=sources/derived
$(derivedSources)/jouleHeatingSource/jouleHeatingSource.C

LIB = $(FOAM_USER_LIBBIN)/libmyFvOptions
```

Listing 561: Adjusting the `Make/files` files.

Listing 562 shows the contents of `Make/options`. This file contains the parameters for source code inclusion and linkage by the compiler. The original parameters can stay in place. Even if some of them are superfluous for our specific model we like to compile, they will not cause any issues.

To this file we need to add information. Line 3 has been added by us. Here we supply the compiler the original location of the `fvOptions` library to search for included files. In this case, this might not be strictly necessary since we do not include any other source files of the `fvOptions` library. However, if we want to compile

²⁸⁸`rename` is usually not pre-installed on most Linux's, but can easily be installed using the package management.

a file which is derived from the base class of the respective model family we want to extend, then we need to add the path to the original model library to the include settings. Otherwise, the compile would not be able to find the sources for the base class.

In Line 18, we add the original model library to the linker settings. This is also very likely superfluous in our case, but there might be situations in which this would be required.

```
user@host:~/OpenFOAM/user-7/src/myFvOptions$ cat Make/options
EXE_INC = \
-I$(LIB_SRC)/fvOptions/lnInclude \
-I$(LIB_SRC)/finiteVolume/lnInclude \
-I$(LIB_SRC)/meshTools/lnInclude \
-I$(LIB_SRC)/sampling/lnInclude \
-I$(LIB_SRC)/transportModels \
-I$(LIB_SRC)/transportModels/compressible/lnInclude \
-I$(LIB_SRC)/transportModels/incompressible/lnInclude \
-I$(LIB_SRC)/thermophysicalModels/basic/lnInclude \
-I$(LIB_SRC)/thermophysicalModels/specie/lnInclude \
-I$(LIB_SRC)/thermophysicalModels/solidThermo/lnInclude \
-I$(LIB_SRC)/TurbulenceModels/turbulenceModels/lnInclude \
-I$(LIB_SRC)/TurbulenceModels/compressible/lnInclude \
-I$(LIB_SRC)/TurbulenceModels/incompressible/lnInclude

LIB_LIBS = \
-lfvOptions \
-lfiniteVolume \
-lmeshTools \
-lsampling \
-lfluidThermophysicalModels \
-lsolidThermo \
-lturbulenceModels \
-lincompressibleTurbulenceModels \
-lcompressibleTurbulenceModels
```

Listing 562: Adjusting the `Make/options` files.

69.7.3 Compile the model library

Now that we have created a model source tree for our model²⁸⁹, we can compile our model. Since the compilation settings have also been adjusted accordingly, we end up with a binary library located in `FOAM_USER_LIBBIN`.

69.7.4 Using the model library

Once the library compiles without any error, we can use it in an OpenFOAM case. Listing 564 shows the entry we need to add to the file `controlDict`. This is a list of names, we assign to the parameter `libs`. Thus, the space between `libs` and the opening parenthesis is important.

```
1 libs      ("libmyFvOptions.so");
```

Listing 563: Telling OpenFOAM to use an additional library for this case in the `controlDict`.

With `controlDict` taken care of, we can then use the newly created model in our case. For this example, we can specify an `fvOption` of the type `jouleHeatingSource`.

```
1 /*----- C++ -----*/
2 | ====== |
3 | \ \ /   F ield      | OpenFOAM: The Open Source CFD Toolbox
4 | \ \ /   O peration   | Version: v1906
5 | \ \ /   A nd        | Web: www.OpenFOAM.com
6 | \ \ /   M anipulation |
7 */
8 FoamFile
9 {
10     version    2.0;
```

²⁸⁹In our special case by copying an existing source code from elsewhere, and subsequent cleaning up.

```

11     format      ascii;
12     class       dictionary;
13     location    "system";
14     object      fvOptions;
15 }
16 // * * * * *
17
18 heating
19 {
20     type          jouleHeatingSource;
21     active        true;
22
23     ... output removed for clarity
24 }
25 // ****

```

Listing 564: Using our newly created fvOption in fvOptions.

Without adding our own model library to `controlDict`, as shown in Listing 564, this would trigger an involuntary *banana test*, i.e., OpenFOAM would not recognize `jouleHeatingSource`, throw an error and list all possible valid options.

70 wmake - the build system of OpenFOAM

OpenFOAM's build system `wmake` has been developed along the lines of `make`²⁹⁰.

70.1 Supporting multiple versions of OpenFOAM

Supporting multiple versions of OpenFOAM requires additional effort and care when internals of OpenFOAM are modified between the versions. Here caution is warranted. Simple changes to internals can be accommodated with relatively little effort, however, there is a point at which one needs to decide whether to drop support of older versions if the changes become too big.

However, if there is only a minor difference, the extra effort should be manageable. In this section we discuss how to accommodate such minor changes to OpenFOAM's internals.

The brute-force method of supporting multiple versions of OpenFOAM would be to maintain a code base for each version of OpenFOAM. However, the reason why this is a bad idea lies in the verb of the prior sentence: maintain. Duplicating all our code for each new version of OpenFOAM is the recipe for a maintenance nightmare. Thus, we ideally would like to maintain a single code base for all versions of OpenFOAM we would like to support²⁹¹. All special, version-dependent treatment of the code will undoubtedly add to the code and increase complexity, however, the benefit of having only one code base is thought to outweigh the added complexity.

In this discussion, we assume that our code is compatible with OpenFOAM-8 and OpenFOAM-9, lesser versions or other variants are not supported. The code snippets shown here are taken from a solver created and maintained by the author, however, only snippets are used to demonstrate the points of the discussion.

70.1.1 options file

Listing 565 shows several things going on. First, we pass the version number of OpenFOAM as a compiler option. This allows us to abort compilation if the version does not match the supported ones, and to make the distinction between versions in the source code itself. Then, we define include paths and library names which depend on the version of OpenFOAM.

In Line 1 of Listing 565, we create a variable within the `options` file. This variable is then passed added to `PFLAGS` in the form of a compiler option in Line 2.

In Line 5, we see how to check the OpenFOAM version to ensure compilation does only occur for supported versions of OpenFOAM. We use a sequence of `if` conditions with empty branches when the OpenFOAM version matches the supported versions, in the branch for all other versions, i.e., the unsupported ones, an error is thrown²⁹² and compilation terminates.

From Line 12 onwards, we see an `if` condition. Following this `if` condition, we specify version-dependent include directories. In Line 13, we see an `info` statement, which can be used for trouble-shooting and to indicate to the user which branch of the `if` clause is being taken.

From Line 22 onwards, the `EXE_INC` entry of the options file is built by combining the compiler options of `PFLAGS`, the version-dependent include directories of `COND_INC` and the remaining include directories which are common to all supported versions. A similar strategy is used for specifying the libraries with `EXE_LIB`.

```
1 FOAM_VERSION_MAJOR := $(WM_PROJECT_VERSION)
2 PFLAGS += -DFOAM_VERSION=$(FOAM_VERSION_MAJOR)
3
4
5 ifeq ($(FOAM_VERSION_MAJOR),9)
6 else ifeq ($(FOAM_VERSION_MAJOR),8)
7 else
8     $(error OpenFOAM-7 and older is not supported)
9 endif
10
11
12 ifeq ($(FOAM_VERSION_MAJOR),9)
13     $(info This branch)
14     COND_INC = \
15         -I$(LIB_SRC)/transportModels/lnInclude \
```

²⁹⁰See [https://en.wikipedia.org/wiki/Make_\(software\)](https://en.wikipedia.org/wiki/Make_(software))

²⁹¹Note the restriction to *all versions we would like to support*. Supporting all versions of OpenFOAM is out of the question for all but the most basic or simple models/solvers/tools.

²⁹²See https://www.gnu.org/software/make/manual/html_node/Make-Control-Functions.html

```

16      -I$(LIB_SRC)/dynamicFvMesh/lnInclude
17 else
18     COND_INC = \
19       -I$(LIB_SRC)/sampling/lnInclude
20 endif
21
22 EXE_INC = \
23   $(PFLAGS) \
24   $(COND_INC) \
25   -I$(LIB_SRC)/finiteVolume/lnInclude \
26   -I$(LIB_SRC)/meshTools/lnInclude
27
28
29 ifeq ($(FOAM_VERSION_MAJOR),9)
30   COND_LIB = \
31     -lfvModels \
32     -lfvConstraints
33 else
34   COND_LIB = \
35     -lfvOptions
36 endif
37
38 EXE_LIBS = \
39   $(COND_LIB) \
40   -lfiniteVolume \
41   -lmeshTools

```

Listing 565: An `options` file with conditional include paths and library names.

70.1.2 Source code

Once the files of the build system are in order, we can turn to the source code itself. Here, we also might need to adjust the code depending on the actual version of OpenFOAM. In the Listing below, we include a version-dependent header-file²⁹³. From Line 2 of Listing 566 onwards, the relevant `include` statements are within an `if` statement, ensuring the proper header-file gets included at compilation.

```

1 // conditional include due to changes in OpenFOAM
2 #if FOAM_VERSION == 9
3   #include "phaseDynamicMomentumTransportModel.H"
4 #elif FOAM_VERSION == 8
5   #include "phaseCompressibleMomentumTransportModel.H"
6 #endif

```

Listing 566: A conditional `include` statement in a source file.

Note, that the `if` statement in Listing 566 uses the variable that was passed as a compiler argument in Line 2 of Listing 565.

²⁹³Between OpenFOAM-8 and OpenFOAM-9 multi-phase Eulerian turbulence modelling was re-organized.

Part IX

Theory

This section covers more detailed topics and tries to look *under the hood* of OpenFOAM from a non-programming view.

71 Discretization

Discretization is largely, if not entirely, governed by the settings made in the file `fvSchemes`. Listing 567 shows such an `fvSchemes` file from one of the standard tutorials. We can observe, without going into specifics, that we are allowed to specify discretization schemes on a per-term/per-equation basis, as done in the `divSchemes` or a default discretization scheme for all terms/equations. This allows, as shown in Listing 567, the momentum equation to use a different convective discretization scheme than the equations related to turbulence modelling.

In contrast, the temporal discretization is set by specifying a default discretization scheme, which is then applied to all equations that feature a temporal derivative.

Listing 567: The `fvSchemes` file of the `pitzDaily` tutorial case of OpenFOAM-10.

Choosing different convective schemes is quite common in the tutorials of OpenFOAM, whereas other discretization schemes are often handled by defaults. OpenFOAM allows the user to do this for all terms, however, one would be hard pressed to think of a situation, in which different temporal discretization makes sense for different equations in a simulation.

71.1 Temporal discretization

71.2 Spatial discretization

The purpose of spatial discretization schemes is to compute the face values of fields whose values are stored at the cell centre. The face values are then used e.g. for computing the spatial derivatives.

71.2.1 upwind scheme

An upwind scheme determines the face value of a quantity simply by choosing the cell centered value of the cell that is located upwind of the face in question.

71.2.2 linearUpwind scheme

The `linearUpwind` scheme is equivalent to FLUENTs *Second-Order Upwind Scheme*.

71.2.3 QUICK scheme

The FLUENT Theory Guide [9] states:

For quadrilateral and hexahedral meshes, where unique upstream and downstream faces and cells can be identified, ANSYS FLUENT also provides the QUICK scheme for computing a higher-order value of the convected variable at a face.

71.2.4 MUSCL scheme

71.3 Continuity error correction

In the governing equations of some solvers in OpenFOAM – e.g. in `twoPhaseEulerFoam` of OpenFOAM-2.3.x – we find a special correction for the continuity error.

71.3.1 Conserving the form

Before we start our considerations, we take a closer look on the *conservation* and *nonconservation* form of a transport equation. First, we recall the definition of the substantial derivative:

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + (\mathbf{u} \cdot \nabla) \quad (234)$$

For example applied to an arbitrary scalar K

$$\frac{DK}{Dt} = \frac{\partial K}{\partial t} + \mathbf{u} \cdot \nabla K \quad (235)$$

Continuity equation

As a first example we look up the differential form of the continuity equation.

$$\text{conservation form:} \quad \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad (236)$$

$$\text{nonconservation form:} \quad \frac{D\rho}{Dt} + \rho \nabla \cdot \mathbf{u} = 0 \quad (237)$$

Both forms are equivalent to each other, since we can express one equation easily by the other one with the help of some simple mathematical operations.

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad (238)$$

$$\frac{\partial \rho}{\partial t} + \nabla \rho \cdot \mathbf{u} + \rho \nabla \cdot \mathbf{u} = 0 \quad (239)$$

$$\underbrace{\frac{\partial \rho}{\partial t}}_{\frac{D\rho}{Dt}} + \mathbf{u} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{u} = 0 \quad (240)$$

Transport equation

For the next example we use the right hand side of the transport equation of enthalpy in a multiphase problem. This example is motivated by the energy equation of *twoPhaseEulerFoam* in OpenFOAM-2.3.x. We could also have used the momentum equation, however, we want to avoid confusion by the repeated occurrence of the velocity.

We look up the energy equation for multiphase flows from a textbook or other resources [9, 6]. For the sake of brevity, we state only the left hand side of the equation. The equation we looked up (Eqn. (241)) happens to be formulated in the *conservation* form. We now rearrange the equation in order to gain the *nonconservation* form.

$$\frac{\partial \alpha_k \rho_k h_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k h_k) = RHS \quad (241)$$

by partial derivation of the LHS, we gain

$$\frac{\partial \alpha_k \rho_k}{\partial t} h_k + \alpha_k \rho_k \frac{\partial h_k}{\partial t} + h_k \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) + \alpha_k \rho_k \mathbf{u}_k \cdot \nabla h_k = RHS \quad (242)$$

$$\underbrace{h_k \left(\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) \right)}_I + \underbrace{\alpha_k \rho_k \left(\frac{\partial h_k}{\partial t} + \mathbf{u}_k \cdot \nabla h_k \right)}_{II} = RHS \quad (243)$$

We now pay attention to the term marked by I, we recognize the phase-continuity equation which equals zero. The term marked with II is the substantial derivative of h_k . Thus we gain with Eqn. (244), the *nonconservation* form of the energy equation.

$$\alpha_k \rho_k \left(\frac{\partial h_k}{\partial t} + \mathbf{u}_k \cdot \nabla h_k \right) = RHS \quad (244)$$

$$\alpha_k \rho_k \frac{D h_k}{D t} = RHS \quad (245)$$

All the operations we applied to get from Eqn. (241) to (244) applied only to the left hand side. Thus, the distinction in *conservation* and *nonconservation* form applies only to the left hand side of the equation.

71.3.2 Continuity error

In theory and in the mathematical sense the *conservation* and *nonconservation* forms are equivalent. However, in we do not solve the s we gain from physics, but the linear equation system stemming from discretizing those PDEs. The resulting linear equation system we solve is not necessarily a direct representation of our initial PDEs. The difference between the (exact) solution of the system of algebraic equations and the (unknown) solution of the mathematical model (the PDEs) is generally referred to as *discretisation error* [38].

We now use Eqns. (241) and (244) to some rearrangement.

$$\frac{\partial \alpha_k \rho_k h_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k h_k) = \alpha_k \rho_k \left(\frac{\partial h_k}{\partial t} + \mathbf{u}_k \cdot \nabla h_k \right) + h_k \left(\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) \right) \quad (246)$$

$$\frac{\partial \alpha_k \rho_k h_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k h_k) - h_k \left(\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) \right) = \alpha_k \rho_k \left(\frac{\partial h_k}{\partial t} + \mathbf{u}_k \cdot \nabla h_k \right) \quad (247)$$

We now want to solve the energy equation. For this we choose the *nonconservative* form (244).

$$\alpha_k \rho_k \left(\frac{\partial h_k}{\partial t} + \mathbf{u}_k \cdot \nabla h_k \right) = RHS \quad (244)$$

Using Eq. (247), we could also write

$$\frac{\partial \alpha_k \rho_k h_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k h_k) - h_k \underbrace{\left(\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) \right)}_{contErr1} = RHS \quad (248)$$

Mathematically, Eqns. (244) and (248) are equivalent. However, when we now discretize both equations in order to solve them numerically, the left hand sides of Eqns. (244) and (248) might actually be different, as the discretised phase continuity equation might not equal zero.

We now take a break from math and take a look into the source code of *twoPhaseEulerFoam-2.3.x*. In Listing 569 we see the first terms of the energy equation of one phase. For a discussion on the full energy equations see Section 55.5.

In Lines 3 and 4 of Listing 569 we see the left hand side of Eqn. (248).

```

1   fvScalarMatrix he1Eqn
2   (
3       fvm::ddt(alpha1, rho1, he1) + fvm::div(alphaRhoPhi1, he1)
4       - fvm::Sp(contErr1, he1)
5       /* other stuff*/
6   );

```

Listing 568: The first terms of the energy equation in the file `EEqns.H` of *twoPhaseEulerFoam*.

```

1   volScalarField contErr1
2   (
3       fvc::ddt(alpha1, rho1) + fvc::div(alphaRhoPhi1)
4       - (fvOptions(alpha1, rho1)&rho1)
5   );

```

Listing 569: The definition of the continuity error in the file `twoPhaseEulerFoam.C`.

We can create more resemblance if we repeat Eqn. (248) and name some of the terms. In Listing 569 the definition of the continuity error differs slightly from Eqn. (248). This is due to the fact, that the solver considers phase sources, see Line 4 of Listing 569.

$$\underbrace{\frac{\partial \alpha_k \rho_k h_k}{\partial t}}_{fvm::ddt(alpha1, rho1, he1)} + \underbrace{\nabla \cdot (\alpha_k \rho_k \mathbf{u}_k h_k)}_{fvm::div(alphaRhoPhi1, he1)} - h_k \underbrace{\left(\frac{\partial \alpha_k \rho_k}{\partial t} + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k) \right)}_{contErr1} = RHS \quad (248)$$

72 Momentum diffusion in an incompressible fluid

72.1 Governing equations

In Section 52.1 we discussed the governing equations of a solver for incompressible fluids.

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \underbrace{\nabla \cdot (\text{dev}(\mathbf{R}^{eff}))}_{=\text{div}(\text{dev}(\mathbf{R}^{eff}))} = -\nabla p + \mathbf{Q} \quad (114)$$

$$\mathbf{R}^{eff} = -\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) \quad (108)$$

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \nabla \cdot (\text{dev}(-\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T))) = -\nabla p + \mathbf{Q} \quad (115)$$

The momentum diffusion term is handled by the turbulence model.

$$\underbrace{\nabla \cdot (\text{dev}(\mathbf{R}^{eff}))}_{=\text{div}(\text{dev}(\mathbf{R}^{eff}))} \Leftrightarrow \text{turbulence-} \rightarrow \text{divDevReff}(\mathbf{U})$$

72.2 Implementation

All turbulence model of OpenFOAM are based on a generic turbulence model class. Figure 189 in Section 68.10 shows a class diagram. There, it is shown, that all RAS turbulence model classes as well as all LES turbulence model classes are derived from the same base class. A lot of solvers of OpenFOAM allow the user to choose between laminar simulation as well as RAS or LES turbulence modelling. Therefore, by the time of writting the source code, nobody could have known, which turbulence exactly will handle the momentum diffusion term.

To overcome such problems, modern programming languages support a technique called polymorphism. In the source code the instruction `turbulence->divDevReff(U)` is called to compute the diffusive term. This instruction means, that the method `divDevReff()` of the object `turbulence` is called.

```

1 // Solve the Momentum equation
2
3 tmp<fvVectorMatrix> UEqn
4 (
5   fvm::ddt(U)
6   + fvm::div(phi, U)
7   + turbulence->divDevReff(U)
8 );
9
10 UEqn().relax();
11
12 sources.constrain(UEqn());
13
14 volScalarField rAU(1.0/UEqn().A());
15
16 if (pimple.momentumPredictor())
17 {
18   solve(UEqn() == -fvc::grad(p) + sources(U));
19 }
```

Listing 570: The file `UEqn.H` of `pimpleFoam`

The source code of the file `createFields.H` tells us, that the object `turbulence` is of the data type `turbulenceModel`.

```

1 singlePhaseTransportModel laminarTransport(U, phi);
2
3 autoPtr<incompressible::turbulenceModel> turbulence
4 (
5   incompressible::turbulenceModel::New(U, phi, laminarTransport)
6 );
```

Listing 571: The file `createFields.H` of `pimpleFoam`

By the time of compilation, it is guaranteed that the object `turbulence` is of the data type `turbulenceModel`. However, `turbulence` will never actually be of the data type `turbulenceModel`. It will be of a data type derived from `turbulenceModel`. The decision which exact method `divDevReff()` has to be called, will be made at run-time based on the actual type of `turbulence`.

Listing 572 shows the declaration of the virtual method `divDevReff()`. See Section 68.10 for a discussion on virtual methods. Listing 573 shows how this method is actually implemented by the standard $k-\epsilon$ turbulence models of OpenFOAM.

```
//- Return the source term for the momentum equation
virtual tmp<fvVectorMatrix> divDevReff(volVectorField& U) const = 0;
```

Listing 572: Declaration of the virtual Method `divDevReff` in `turbulenceModel.H`

```
tmp<fvVectorMatrix> kEpsilon::divDevReff(volVectorField& U) const
{
    return
    (
        - fvm::laplacian(nuEff(), U)
        - fvc::div(nuEff()*dev(T(fvc::grad(U))))
    );
}
```

Listing 573: Implementation of the virtual Method `divDevReff` in `kEpsilon.H`

The calculation of `divDevReff()` is equivalent to Eq. (115).

$$\begin{aligned} \text{divDevReff} &= \nabla \cdot (\text{dev}(-\nu(\nabla \mathbf{U} + (\nabla \mathbf{U})^T))) \\ &= \underbrace{-\nabla \cdot (\nu(\nabla \mathbf{U}))}_{\text{laplacian}(nu,U)} - \underbrace{\nabla \cdot (\nu(\nabla \mathbf{U})^T)}_{\text{div}(nu*\text{dev}(T(\text{grad}(U))))} \end{aligned}$$

The momentum diffusion term is most probably split into two parts for numerical reasons.

73 The incompressible k- ϵ turbulence model

73.1 The k- ϵ turbulence model in literature

The governing equations for the k- ϵ model for a single phase are taken from Wilcox [69].

Eddy viscosity

$$\mu_T = \rho C_\mu \frac{k^2}{\epsilon} \quad (249)$$

Turbulent kinetic energy

$$\rho \frac{\partial k}{\partial t} + \rho U_j \frac{\partial k}{\partial x_j} = \tau_{ij} \frac{\partial U_i}{\partial x_j} - \rho \epsilon + \frac{\partial}{\partial x_j} \left[(\mu + \frac{\mu_T}{\sigma_k}) \frac{\partial k}{\partial x_j} \right] \quad (250)$$

Dissipation Rate

$$\rho \frac{\partial \epsilon}{\partial t} + \rho U_j \frac{\partial \epsilon}{\partial x_j} = C_{\epsilon 1} \frac{\epsilon}{k} \tau_{ij} \frac{\partial U_i}{\partial x_j} - C_{\epsilon 2} \rho \frac{\epsilon^2}{k} + \frac{\partial}{\partial x_j} \left[(\mu + \frac{\mu_T}{\sigma_\epsilon}) \frac{\partial \epsilon}{\partial x_j} \right] \quad (251)$$

Closure coefficients

$$C_{\epsilon 1} = 1.44, \quad C_{\epsilon 2} = 1.92, \quad C_\mu = 0.09, \quad \sigma_k = 1.0, \quad \sigma_\epsilon = 1.3 \quad (252)$$

The transport equations for k and ϵ are reorganized to follow the basic structure

$$\text{local derivative} + \text{convection} + \text{diffusion} = \text{source \& sink terms}$$

Turbulent kinetic energy

$$\rho \frac{\partial k}{\partial t} + \rho U_j \frac{\partial k}{\partial x_j} - \frac{\partial}{\partial x_j} \underbrace{\left[\underbrace{(\mu + \frac{\mu_T}{\sigma_k})}_{D_k} \frac{\partial k}{\partial x_j} \right]}_G = \underbrace{\tau_{ij} \frac{\partial U_i}{\partial x_j}}_G - \rho \epsilon \quad (253)$$

Dissipation Rate

$$\rho \frac{\partial \epsilon}{\partial t} + \rho U_j \frac{\partial \epsilon}{\partial x_j} - \frac{\partial}{\partial x_j} \underbrace{\left[\underbrace{(\mu + \frac{\mu_T}{\sigma_\epsilon})}_{D_\epsilon} \frac{\partial \epsilon}{\partial x_j} \right]}_G = C_{\epsilon 1} \frac{\epsilon}{k} \underbrace{\tau_{ij} \frac{\partial U_i}{\partial x_j}}_G - C_{\epsilon 2} \rho \frac{\epsilon^2}{k} \quad (254)$$

Diffusivity constants

$$D_k = \mu + \frac{\mu_T}{\sigma_k} \quad (255)$$

$$D_\epsilon = \mu + \frac{\mu_T}{\sigma_\epsilon} \quad (256)$$

The constant expressions in the diffusive terms are combined into the diffusivity constants D_k and D_ϵ . The first term on the right hand side of the turbulent kinetic energy equation is the production of turbulent kinetic energy G .

73.2 The k- ϵ turbulence model in OpenFOAM

73.2.1 Governing equations

The governing equations of the k- ϵ model of OpenFOAM are basically the same equations as in Section 73.1. The vector notation is used in this section because the syntax OpenFOAM uses strongly resembles the vector notation. However, there are some modifications to the equations.

First, the transport equations for k and ϵ are divided by the density ρ . Therefore, all terms containing viscosity contain the kinematic viscosity ν instead of the dynamic viscosity μ .

Secondly, the standard $k-\epsilon$ model of OpenFOAM has eliminated the model constant σ_k . Since the value of this constant is one, this constant has been eliminated. This does not change the behaviour of the model. However, if the user tries to change this model constant, nothing actually happens. See Section 39.4.2 for a discussion and an example.

Finally, the convection term is converted into two term by the product rule of differentiation. See Eqn. (258).

Eddy viscosity, see Listing 574

$$\begin{aligned}\mu_T &= \rho \nu_T \\ \nu_T &= C_\mu \frac{k^2}{\epsilon}\end{aligned}\quad (257)$$

Turbulent kinetic energy, see Listing 575

$$\begin{aligned}U_j \frac{\partial k}{\partial x_j} &= \mathbf{U} \cdot \frac{\partial k}{\partial \mathbf{x}} = \mathbf{U} \cdot \nabla k \\ \mathbf{U} \cdot \frac{\partial k}{\partial \mathbf{x}} &= \nabla \cdot (\mathbf{U}k) - (\nabla \cdot \mathbf{U})k\end{aligned}\quad (258)$$

$$\frac{\partial k}{\partial t} + \nabla \cdot (\mathbf{U}k) - (\nabla \cdot \mathbf{U})k - \nabla \cdot (D_k \nabla k) = G - \epsilon \quad (259)$$

Dissipation Rate

$$\frac{\partial \epsilon}{\partial t} + \nabla \cdot (\mathbf{U}\epsilon) - (\nabla \cdot \mathbf{U})\epsilon - \nabla \cdot (D_\epsilon \nabla \epsilon) = C_1 G \frac{1}{k} - C_2 \frac{\epsilon^2}{k} \quad (260)$$

Diffusivity constants - Note that σ_k has been eliminated from the equations

$$D_k = \text{DkEff} = \nu + \nu_T \quad (261)$$

$$D_\epsilon = \text{DepsiEff} = \nu + \frac{\nu_T}{\sigma_\epsilon} \quad (262)$$

Closure coefficients - default values

$$C_1 = 1.44, \quad C_2 = 1.92, \quad C_\mu = 0.09, \quad \sigma_\epsilon = 1.3 \quad (263)$$

The default values of the model constants can be found in the constructor of the respective turbulence model class.

73.2.2 The source code

Listing 574 shows the calculation of the eddy viscosity. A (too) short glimpse on the code may lead to confusion, as the function `sqr()` meaning taking a variable to the power of two looks similar to `sqrt()`, which is the square root.

Listing 575 shows the transport equation for the turbulent viscosity. The last term on the right hand side is expanded.

$$\epsilon = \underbrace{\frac{\epsilon}{k} k}_{\text{fvm::Sp(epsilon/k, k)}} \quad (264)$$

```
nut_ = Cmu_*sqr(k_)/epsilon_;
```

Listing 574: Calculation of the eddy viscosity

```

tmp<fvScalarMatrix> kEqn
(
    fvm::ddt(k_)
    + fvm::div(phi_, k_)
    - fvm::Sp(fvc::div(phi_), k_)
    - fvm::laplacian(DkEff(), k_)

==

G
- fvm::Sp(epsilon_/k_, k_)

);

```

Listing 575: Transport equation for the turbulent kinetic energy

Constructor

Listing 576 shows the first lines of the constructor of the `kEpsilon` class. The constructor receives five arguments. After the colon (in line 9), the initialisation list follows. This list contains also the default values of the model constants. See Section 67.5 for details about constructors in C++. In line 18 the default value of the model constant C_μ is defined.

```

1 kEpsilon::kEpsilon
2 (
3     const volVectorField& U,
4     const surfaceScalarField& phi,
5     transportModel& transport,
6     const word& turbulenceModelName,
7     const word& modelName
8 )
9 :
10 RASModel(modelName, U, phi, transport, turbulenceModelName),
11
12 Cmu_
13 (
14     dimensioned<scalar>::lookupOrAddToDict
15     (
16         "Cmu",
17         coeffDict_,
18         0.09
19     )
20 ),
21 /* code continues */

```

Listing 576: The constructor of the `kEpsilon` class

73.3 The $k-\epsilon$ turbulence model in *bubbleFoam* and *twoPhaseEulerFoam*

The $k-\epsilon$ turbulence model is hardcoded in *bubbleFoam* and *twoPhaseEulerFoam*. This means, that these solvers do not use the generic turbulence modelling other than most OpenFOAM solvers.

The question of turbulence modelling in dispersed two-phase flows is not fully answered yet. There are several strategies:

Per phase The turbulence is modelled for both phases individually.

Mixture The turbulence is modelled based on mixture quantities.

Liquid phase Turbulence is modelled based in the quantites of the liquid phase. The turbulence of the dispersed phase is either neglected or considered by a model constant.

73.3.1 Governing equations

The $k-\epsilon$ turbulence model of *bubbleFoam* and *twoPhaseEulerFoam* is in some aspects different than the standard $k-\epsilon$ turbulence model of OpenFOAM.

1. The diffusivity constants are calculated from the effective viscosity. Compare Eqns. (255, 256) and (270, 271)

2. The model constants σ_k and σ_ϵ are replaced by their reciprocal values.
3. Other than in the standard $k-\epsilon$ model, the model constant σ_k is not dropped. By defining a value for the constant $\alpha_{1,k} = 1/\sigma_k$, a value for σ_k is assigned.

Turbulence modelling in *bubbleFoam* and *twoPhaseEulerFoam* is based on the liquid quantities. Turbulence of the gas phase is considered by the use of the model constant C_t . This constant connects the turbulent viscosity of the liquid and the gas phase. By setting this constant to zero, turbulence is ignored in the gas phase.

Eddy viscosity

$$\nu_{2,T} = C_\mu \frac{k^2}{\epsilon} \quad (265)$$

$$\nu_{2,eff} = \nu_2 + \nu_{2,T} \quad (266)$$

$$\nu_{1,eff} = \nu_1 + C_t^2 \nu_{2,T} \quad (267)$$

Turbulent kinetic energy, see Listing 575

$$\frac{\partial k}{\partial t} + \nabla \cdot (\mathbf{U}_2 k) - (\nabla \cdot \mathbf{U}_2) k - \nabla \cdot (\alpha_{1,k} \nu_{2,eff} \nabla k) = G - \epsilon \quad (268)$$

Dissipation Rate

$$\frac{\partial \epsilon}{\partial t} + \nabla \cdot (\mathbf{U}_2 \epsilon) - (\nabla \cdot \mathbf{U}_2) \epsilon - \nabla \cdot (\alpha_{1,\epsilon} \nu_{2,eff} \nabla \epsilon) = C_1 G \frac{1}{k} - C_2 \frac{\epsilon^2}{k} \quad (269)$$

Diffusivity constants - Note the different definition

$$\alpha_{1,k} = \frac{1}{\sigma_k}$$

$$\alpha_{1,\epsilon} = \frac{1}{\sigma_\epsilon}$$

$$D_k = \alpha_{1,k} \nu_{2,eff} = \frac{\nu_{2,eff}}{\sigma_k} \quad (270)$$

$$D_\epsilon = \alpha_{1,\epsilon} \nu_{2,eff} = \frac{\nu_{2,eff}}{\sigma_\epsilon} \quad (271)$$

Closure coefficients - default values

$$C_1 = 1.44, \quad C_2 = 1.92, \quad C_\mu = 0.09, \quad \alpha_{1,k} = 1, \quad \alpha_{1,\epsilon} = 0.76923 \quad (272)$$

73.3.2 Source code

The transport equations of *bubbleFoam* and *twoPhaseEulerFoam* reside in the file *kEpsilon.H*. Listing 577 shows the most important lines of *kEpsilon.H*.

```

1 tmp<volTensorField> tgradU2 = fvc::grad(U2);
2 volScalarField G(2*nut2*(tgradU2() && dev(symm(tgradU2()))));
3
4 // Dissipation equation
5 fvScalarMatrix epsEqn
6 (
7     fvm::ddt(epsilon)
8     + fvm::div(phi2, epsilon)
9     - fvm::Sp(fvc::div(phi2), epsilon)
10    - fvm::laplacian
11    (
12        alpha1Eps*nuEff2, epsilon,
13        "laplacian(DepsilonEff, epsilon)"
14    )
15    ==
16    C1*G*epsilon/k

```

```

17     - fvm::Sp(C2*epsilon/k, epsilon)
18 );
19
20 // Turbulent kinetic energy equation
21 fvScalarMatrix kEqn
22 (
23     fvm::ddt(k)
24     + fvm::div(phi2, k)
25     - fvm::Sp(fvc::div(phi2), k)
26     - fvm::laplacian
27     (
28         alpha1k*nuEff2, k,
29         "laplacian(DkEff, k)"
30     )
31     ==
32     G
33     - fvm::Sp(epsilon/k, k)
34 );
35
36 // Re-calculate turbulence viscosity
37 nut2 = Cmu*sqr(k)/epsilon;

```

Listing 577: The turbulent transport equations of the `bubbleFoam` and `twoPhaseEulerFoam` solver

73.4 Modelling the production of turbulent kinetic energy

When comparing the turbulent equations from literature and the sources, the definition of the production of turbulent kinetic energy shows great differences.

73.4.1 Definitions from literature and source files

The production of turbulent kinetic energy seems to be differently defined.

Thesis of H. Rusche [56] - the basis of *bubbleFoam* and *twoPhaseEulerFoam*

$$P_b = 2\nu_{2,eff} (\nabla \mathbf{U}_b \cdot \operatorname{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T)) \quad (273)$$

Source code - `kEpsilon.H` of *bubbleFoam* - See Line 2 Listing 577

$$G = 2\nu_T (\nabla \mathbf{U}_2 : \operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2))) \quad (274)$$

Source code - standard k- ϵ model, `kEpsilon.C`

$$G = 2\nu_T |\operatorname{sym}(\nabla \mathbf{U})|^2 \quad (275)$$

Ferzinger Peric [37]

$$P = \mu_T \nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \quad (276)$$

Wilcox [69]

$$G = \mu_T \nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) - \frac{2}{3} \rho k \mathbf{I} : \nabla \mathbf{U} \quad (277)$$

Some definitions use the dynamic viscosity and some others use the kinematic viscosity. For incompressible fluids, this is no major difference between the definitions.

73.4.2 Different use of viscosity

Eq. (273) is the only definition that makes use of the [56] effective viscosity instead of the turbulent viscosity. The reason for this is not explained.

However, the FLUENT Theory Guide [9] states that the effective viscosity is used to calculate the production term when high-Reynolds number versions of the k- ϵ model are used. It is not further specified what is meant with high-Reynolds number versions of the k- ϵ model.

73.4.3 Notation

The definitions in Section 73.4.1 are written in vector notation. However, there seems to be a minor flaw in Eq. (273). There

$$P_b = 2\nu_{2,eff} (\nabla \mathbf{U}_b \cdot \operatorname{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T)) \quad (273)$$

The dot can not denote an inner product. The result only has the correct dimension, if the dot denotes a contraction. Therefore, the equation should read

$$P_b = 2\nu_{2,eff} (\nabla \mathbf{U}_b : \operatorname{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T)) \quad (278)$$

73.4.4 Definitions from literature

The definition of the production term in Eq. (276) and (277) differ only in the last term.

$$G = \mu_T \nabla \mathbf{U} : (\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T) - \frac{2}{3} \rho k \mathbf{I} : \nabla \mathbf{U} \quad (277)$$

Using the following identities, the contraction can be replaced by an inner product

$$\mathbf{I} : \nabla \mathbf{U} = \operatorname{tr}(\nabla \mathbf{U}) = \nabla \cdot \mathbf{U} \quad (279)$$

For incompressible fluids the divergence of the velocity must be zero due to the continuity equation

$$\nabla \cdot \mathbf{U} = 0 \quad (280)$$

$$G = \mu_T \nabla \mathbf{U} : (\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T) - \underbrace{\frac{2}{3} \rho k \mathbf{I} : \nabla \mathbf{U}}_{=0} \quad (281)$$

Therefore, Eqns. (276) and (277) are identical if the fluid is incompressible. We now can examine the differences of the definitions of the production term, using Eq. (276) as reference equation.

73.4.5 Definitions of Rusche and *bubbleFoam*

The solvers *bubbleFoam* and *twoPhaseEulerFoam* are based on the thesis of H. Rusche [56]. However, the production term is defined differently. Compare Eq. (273) and (274).

$$P_b = 2\nu_{2,eff} (\nabla \mathbf{U}_b : \operatorname{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T)) \quad (273)$$

$$G = 2\nu_T (\nabla \mathbf{U}_2 : \operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2))) \quad (274)$$

We ignore the different symbols for the velocity of the continuous phase

$$\mathbf{U}_2 = \mathbf{U}_b \quad (282)$$

The second operator of the contraction is different in both equations. We ask, if the following equation holds

$$\nabla \mathbf{U}_2 : \operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2)) \stackrel{?}{=} \nabla \mathbf{U}_b : \operatorname{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T) \quad (283)$$

With the following identities the question is easily answered

$$\operatorname{dev}(\mathbf{T}) = \mathbf{T} - \frac{1}{3} \operatorname{tr}(\mathbf{T}) \quad (284)$$

$$\operatorname{sym}(\mathbf{T}) = \frac{1}{2} (\mathbf{T} + (\mathbf{T})^T) \quad (285)$$

$$\operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2)) = \operatorname{dev}\left(\frac{1}{2} (\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T)\right) \quad (286)$$

$$\operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2)) = \frac{1}{2} \operatorname{dev}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T) \quad (287)$$

$$\operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2)) = \underbrace{\frac{1}{2} \left((\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T) - \frac{1}{3} \operatorname{tr}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T) \right)}_{=\operatorname{dev}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T)} \quad (288)$$

$$\operatorname{dev}(\operatorname{sym}(\nabla \mathbf{U}_2)) = \frac{1}{2} \operatorname{dev}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T) \quad (289)$$

This leads to the answer

$$\nabla \mathbf{U}_2 : \text{dev}(\text{sym}(\nabla \mathbf{U}_2)) = \frac{1}{2} \nabla \mathbf{U}_b : \text{dev}(\nabla \mathbf{U}_b + (\nabla \mathbf{U}_b)^T) \quad (290)$$

The definition of the production term in the source code differs in two ways from the definition in the source code

1. The use of different viscosities, see Eqns. (273) and (274).
2. A factor of 2, compare Eqns. (283) and (290)

The reason for this differences is not clear. H. Rusche refers to an article which is not available to the author.

73.4.6 Definitions of Ferzinger and *bubbleFoam*

We now compare the definitions of Ferzinger and *bubbleFoam*. The definition of Ferzinger is – like the equations in most other book about turbulence – for single-phase systems. However, *bubbleFoam* is a two-phase solver. The question of considering turbulence in two-phase systems is not answered yet. *bubbleFoam* considers turbulence for the continuous phase by the use of a turbulence model. The turbulence of the disperse phase is linked to the continuous phase. Therefore, turbulence model equations of *bubbleFoam* are quite similar to single-phase turbulence equations.

$$G = 2\nu_T (\nabla \mathbf{U}_2 : \text{dev}(\text{sym}(\nabla \mathbf{U}_2))) \quad (274)$$

$$P = \mu_T \nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \quad (276)$$

We ignore the different viscosities and ask ourselves

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \stackrel{?}{=} 2 (\nabla \mathbf{U}_2 : \text{dev}(\text{sym}(\nabla \mathbf{U}_2))) \quad (291)$$

Inserting Eq. (289) gives

$$\begin{aligned} \nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) &= 2 (\nabla \mathbf{U}_2 : \underbrace{\text{dev}(\text{sym}(\nabla \mathbf{U}_2))}_{=\frac{1}{2} \text{dev}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T)}) \end{aligned} \quad (292)$$

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U}_2 : \text{dev}(\nabla \mathbf{U}_2 + (\nabla \mathbf{U}_2)^T) \quad (293)$$

Now we insert Eq. (284) into the *rhs* of Eq. (293)

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U} : \left(\text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) + \frac{1}{3} \text{tr}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \right) \quad (294)$$

Using the following identities and Eq. (279)

$$\text{tr}(\mathbf{A} + \mathbf{B}) = \text{tr}(\mathbf{A}) + \text{tr}(\mathbf{B}) \quad (295)$$

$$\text{tr}(\mathbf{A}^T) = \text{tr}(\mathbf{A}) \quad (296)$$

$$\mathbf{I} : \nabla \mathbf{U} = \text{tr}(\nabla \mathbf{U}) = \nabla \cdot \mathbf{U} \quad (297)$$

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U} : \left(\text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) + \frac{2}{3} (\nabla \cdot \mathbf{U}) \right) \quad (297)$$

The second term of the *rhs* vanishes according to the continuity equation for an incompressible fluid

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U} : \left(\text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) + \frac{2}{3} \underbrace{(\nabla \cdot \mathbf{U})}_{\nabla \cdot \mathbf{U}=0} \right) \quad (298)$$

Eq. (299) now resembles Eq. (293). Therefore, we proofed that the definition of *bubbleFoam* is equivalent to the definition of Ferzinger

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U} : \text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \quad (299)$$

73.4.7 Definition of standard k- ϵ of OpenFOAM

We now compare the definition of the production term of the standard k- ϵ model implemented in OpenFOAM with the definition found in [37].

Source code - standard k- ϵ model, `kEpsilon.C`

$$G = 2\nu_T |\text{sym}(\nabla \mathbf{U})|^2 \quad (275)$$

Ferzinger Peric [37]

$$P = \nu_T \nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \quad (276)$$

Starting from Eq. (276), we will use Eq. (299) and Eq. (289)

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = \nabla \mathbf{U} : \text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) \quad (299)$$

$$\text{dev}(\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = 2 \text{ dev}(\text{sym}(\nabla \mathbf{U})) \quad (289)$$

to gain

$$\nabla \mathbf{U} : (\nabla \mathbf{U} + (\nabla \mathbf{U})^T) = 2 \nabla \mathbf{U} : \text{dev}(\text{sym}(\nabla \mathbf{U})) \quad (300)$$

We use definition (301) to change Eq. (275)

$$|\text{sym}(\nabla \mathbf{U})|^2 = \text{sym}(\nabla \mathbf{U}) : \text{sym}(\nabla \mathbf{U}) \quad (301)$$

Now we pose the question

$$\text{sym}(\nabla \mathbf{U}) : \text{sym}(\nabla \mathbf{U}) \stackrel{?}{=} \nabla \mathbf{U} : \text{dev}(\text{sym}(\nabla \mathbf{U})) \quad (302)$$

The *lhs* of Eq. (302) corresponds to Eq. (275). The *rhs* of Eq. (302) was derived from Eq. (276). Now, we use some identities

$$\text{dev}(\mathbf{T}) = \mathbf{T} - \frac{1}{3} \text{tr}(\mathbf{T}) \quad (284)$$

$$\text{tr}(\text{sym}(\mathbf{T})) = \text{tr}(\mathbf{T}) \quad (303)$$

to reformulate the *rhs* of Eq. (302)

$$\nabla \mathbf{U} : \text{dev}(\text{sym}(\nabla \mathbf{U})) = \nabla \mathbf{U} : \left(\text{sym}(\nabla \mathbf{U}) - \frac{1}{3} \text{tr}(\nabla \mathbf{U}) \right) \quad (304)$$

As we now concentrate on incompressible single-phase problems, we can eliminate the second term of the *rhs* of Eq. (304) by the use of Eq. (279)

$$\mathbf{I} : \nabla \mathbf{U} = \text{tr}(\nabla \mathbf{U}) = \nabla \cdot \mathbf{U} = 0 \quad (279)$$

We now have

$$\nabla \mathbf{U} : \text{dev}(\text{sym}(\nabla \mathbf{U})) = \nabla \mathbf{U} : \text{sym}(\nabla \mathbf{U}) \quad (305)$$

The following equation remains, which is easily proofed by some tensor calculus

$$\text{sym}(\nabla \mathbf{U}) : \text{sym}(\nabla \mathbf{U}) = \nabla \mathbf{U} : \text{sym}(\nabla \mathbf{U}) \quad (306)$$

Every tensor can be decomposed into a symmetric and a skew part

$$\mathbf{T} = \text{sym}(\mathbf{T}) + \text{skew}(\mathbf{T}) \quad (307)$$

$$\text{sym}(\mathbf{T}) = \frac{1}{2} (\mathbf{T} + \mathbf{T}^T) \quad (308)$$

$$\text{skew}(\mathbf{T}) = \frac{1}{2} (\mathbf{T} - \mathbf{T}^T) \quad (309)$$

Therefore, we can write

$$\mathbf{T} : \text{sym}(\mathbf{T}) = \text{sym}(\mathbf{T}) : \text{sym}(\mathbf{T}) + \text{skew}(\mathbf{T}) : \text{sym}(\mathbf{T}) \quad (310)$$

The following properties of skew tensors let the second contraction vanish

$$\underbrace{\text{skew}(\mathbf{T})}_{a_{ij}} : \underbrace{\text{sym}(\mathbf{T})}_{s_{ij}} \quad (311)$$

$$a_{ii} = 0 \quad (312)$$

$$a_{ij} = -a_{ji} \quad (313)$$

$$\text{skew}(\mathbf{T}) : \text{sym}(\mathbf{T}) = a_{ij}s_{ij} = 0 \quad (314)$$

Finally, we obtain

$$\mathbf{T} : \text{sym}(\mathbf{T}) = \text{sym}(\mathbf{T}) : \text{sym}(\mathbf{T}) \quad (315)$$

Therefore, we proofed that the definition of the standard k- ϵ model is equivalent to the definition of Ferzinger.

74 Some theory behind the scenes of LES

74.1 LES model hierarchy

The large eddy simulation is based on the spatial filtering of the governing equations. Similar to the Reynolds-averaged modelling strategy (filtering with respect to time), the large eddy modelling strategy requires some closure models. In principle, the velocity is decomposed into a grid-scale and a sub-grid scale portion. The grid-scale portion is resolved by the governing equations. The sub-grid scale portion – or the influence of the sub-grid scale portion on the resolved velocity – needs to be modelled.

Similar to the RANS approach, the closure terms appear in the stress terms of the momentum equations. There are several modelling strategies to close the equations. The class hierarchy of the LES models of OpenFOAM reflects the different approaches. Figure 192 shows the first layer of the class hierarchy of the LES models in OpenFOAM. First layer means that a class derived from the abstract class `LESModel` may be an abstract class itself and therefore be the base for other classes²⁹⁴²⁹⁵.

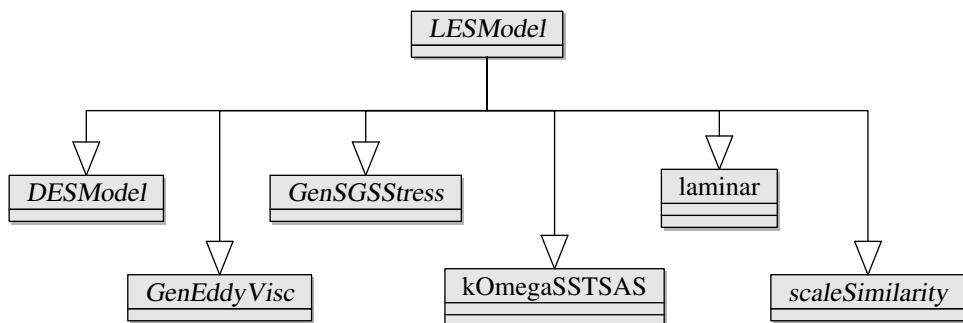


Figure 192: First layer of the class hierarchy of the LES models of OpenFOAM

The classification according to Figure 192 is not the only possible way to divide all existing LES models into categories.

74.2 Eddy viscosity models

One of the most common approaches of closing the governing equations when using an LES turbulence modelling strategy are eddy viscosity models. Like the RANS turbulence models, the eddy viscosity models make use of the Boussinesq hypothesis. The contribution of the sub-grid scale terms is modelled by an additional viscosity. The effective viscosity is the sum of the laminar viscosity and the sub-grid viscosity.

$$\nu_{eff} = \nu + \nu_{SGS} \quad (316)$$

74.2.1 Class hierarchy

The base class for all eddy viscosity models is `GenEddyVisc`. Figure 193 shows the class hierarchy with focus on `GenEddyVisc`.

74.2.2 Classification

The eddy viscosity models can be divided further based on the way the sub-grid viscosity is computed and the complexity of the model.

²⁹⁴In a class diagram a class with an italic written name is an abstract class. A class with an upright written name is an actual class.

²⁹⁵This shows the great advantage of object oriented programming. The class hierarchy of the code reflects the relation between the objects in reality, e.g. every eddy viscosity model is an LES model, but not every LES model is an eddy viscosity model.

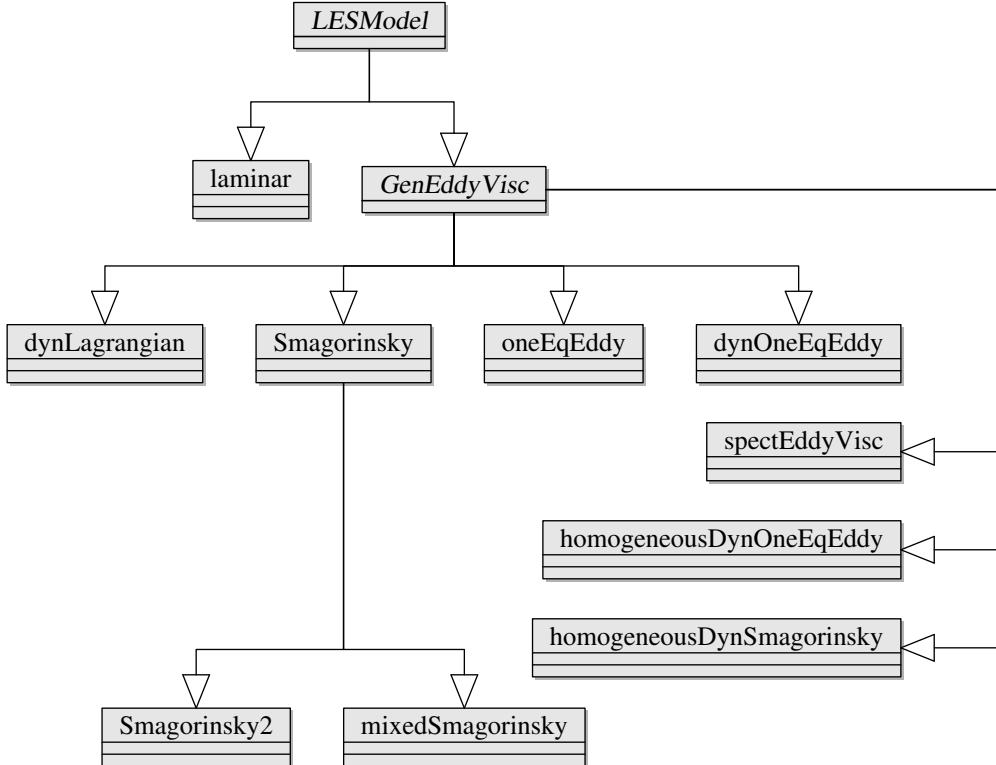


Figure 193: Class hierarchy of the eddy viscosity models in OpenFOAM

	constant coefficient	dynamic coefficient
algebraic model	Smagorinsky Smagorinsky2	homogeneousDynSmagorinsky spectEddyVisc
one equation model	oneEqEddy	dynOneEqEddy homogeneousDynOneEqEddy dynLagrangian

Table 10: Comparison of the eddy viscosity models of OpenFOAM

74.2.3 Eddy viscosity

For dimensional reasons, the eddy viscosity must be a product of a length and a velocity scale [26]. Eq. (318) shows the generic equation for the sub-grid viscosity. An additional model constant is the third term in the product. The way the model constant is computed as well as the choice for the length and velocity scales is determined by the model.

$$[\nu_{SGS}] = \frac{m^2}{s} = \frac{m}{s} \cdot m \quad (317)$$

$$\nu_{SGS} = C_{SGS} l_{SGS} q_{SGS} \quad (318)$$

A choice that is common to a number of eddy viscosity models in OpenFOAM is to choose the filter width as the length scale and the square root of the sub-grid kinetic energy as the velocity scale. Algebraic models usually calculate the sub-grid kinetic energy from known quantities, e.g. based on the velocity gradient. One equation models typically solve a transport equation for the sub-grid scale kinetic energy.

$$l_{SGS} = \Delta \quad (319)$$

$$[l_{SGS}] = \text{m} \quad (320)$$

$$q_{SGS} = \sqrt{k_{SGS}} \quad (321)$$

$$[q_{SGS}] = \sqrt{\frac{\text{m}^2}{\text{s}^2}} = \frac{\text{m}}{\text{s}} \quad (322)$$

74.2.4 The Smagorinsky LES model

The Smagorinsky eddy viscosity is one of the simplest LES models. From Table 10 we see that this is an algebraic model with a constant model coefficient. This model was published 1963 [58].

Eq. (323) shows the definition of the sub-grid scale viscosity according to the Samgorinsky model as it can be found in literature [26].

$$\nu_{SGS} = (C_S \Delta)^2 |\mathbf{S}| \quad (323)$$

with

$$\begin{aligned} \mathbf{S} &= \text{sym}(\nabla \mathbf{u}) = \text{sym}(\text{grad}(\mathbf{u})) \\ |\mathbf{T}| &= \sqrt{\mathbf{T} : \mathbf{T}} \end{aligned}$$

Some rearrangement of Eq. (323) is necessary to match the form of Definition (318) and (321). Eqns. (324) to (326) show the necessary steps to match the generic definition of ν_{SGS} .

$$\nu_{SGS} = C_S^2 \underbrace{\Delta}_{l_{SGS}} \underbrace{\Delta \sqrt{\mathbf{S} : \mathbf{S}}}_{q_{SGS}} \quad (324)$$

$$q_{SGS} = \sqrt{k_{SGS}} = \Delta \sqrt{\mathbf{S} : \mathbf{S}} \quad (325)$$

$$\Rightarrow k_{SGS} = \Delta^2 \mathbf{S} : \mathbf{S} \quad (326)$$

Implementation

The implementation in the source code differs a little from the equations above.

```

1 void Smagorinsky::updateSubGridScaleFields(const volTensorField& gradU)
2 {
3     nuSgs_ = ck_*delta()*sqrt(k(gradU));
4     nuSgs_.correctBoundaryConditions();
5 }
```

Listing 578: The function `updateSubGridScaleFields()` in the file `Smagorinsky.C`

```

1 tmp<volScalarField> k(const tmp<volTensorField>& gradU) const
2 {
3     return (2.0*ck_/ce_)*sqr(delta())*magSqr(dev(symm(gradU)));
4 }
```

Listing 579: The function `k()` in the file `Smagorinsky.H`

Listing 578 shows the implementation of how the sub-grid viscosity is computed by the Smagorinsky model in OpenFOAM. Listing 579 shows how the model calculates the sub-grid kinetic energy.

$$\nu_{SGS} = ck \Delta \sqrt{k} \quad (327)$$

$$k = 2 \frac{ck}{ce} \Delta^2 |\text{dev } \mathbf{S}|^2 \quad (328)$$

with

$$\mathbf{S} = \text{sym grad}(\mathbf{u}) \quad (329)$$

it follows

$$\nu_{SGS} = ck\Delta \sqrt{2\frac{ck}{ce}\Delta^2|\text{dev } \mathbf{S}|^2} \quad (330)$$

$$\nu_{SGS} = ck\sqrt{2\frac{ck}{ce}\Delta^2|\text{dev } \mathbf{S}|} \quad (331)$$

the comparison with Eq. 323 shows

$$\nu_{SGS} = (C_S\Delta)^2|\mathbf{S}| \quad (323)$$

$$\Rightarrow C_S^2 = ck\sqrt{2\frac{ck}{ce}} \quad (332)$$

Eq. (332) shows how the Smagorinsky constant can be calculated from the model constants. The Smagorinsky constant is often stated in publications using or investigating the Smagorinsky model, because it is the only degree of freedom of the Smagorinsky model.

In OpenFOAM the Smagorinsky model has two model constants. *ce* is inherited from the class `GenEddyVisc`. This constant is used in the definition of the sub-grid dissipation rate. The default value of *ce* is 1.048 and is defined in the constructor of the class `GenEddyVisc` in the file `GenEddyVisc.C`.

Therefore, the model constant *ck* is the only degree of freedom of the Smagorinsky model of OpenFOAM. The default value of *ck* is 0.094. This results in a default value for *C_S* of 0.1995 ≈ 0.2. The value of *C_S* varies in literature depending on the publication from 0.07 to 0.33 [11, 47].

```

1 // - Return sub-grid disipation rate
2 virtual tmp<volScalarField> epsilon() const
3 {
4     return tmp<volScalarField>
5     (
6         new volScalarField
7         (
8             IOobject
9             (
10                "epsilon",
11                runTime_.timeName(),
12                mesh_,
13                IOobject::NO_READ,
14                IOobject::NO_WRITE
15            ),
16            ce_*k()*sqrt(k())/delta()
17        )
18    );
19 }
```

Listing 580: The function `epsilon()` in the file `GenEddyVisc.H`

74.2.5 The `oneEqEddy` LES model

The `oneEqEddy` model is one of the standard LES models of OpenFOAM. This model is an one equation eddy viscosity model with a constant model coefficient. Eq. 333 shows how the sub-grid viscosity is calculated by the `oneEqEddy` model. The constant *ck* has a default value of 0.094.

$$\nu_{SGS} = ck\Delta\sqrt{k_{SGS}} \quad (333)$$

The transport equation for k_{SGS}

As this model is an one equation model, it introduces an additional equation to the set of equations. This additional equation is a transport equation for the sub-grid kinetic energy k_{SGS} . k_{SGS} is the kinetic energy of

the unresolved portion of the velocity. Thus, k_{SGS} is called sub-grid kinetic energy.

$$\frac{\partial k_{SGS}}{\partial t} + \nabla \cdot (k_{SGS} \mathbf{u}) - \nabla \cdot (D_k \nabla k_{SGS}) = G - \epsilon_{SGS} \quad (334)$$

with

$$\begin{aligned} D_k &= \nu + \nu_{SGS} \\ G &= \nu_{SGS} |\text{sym}(\nabla \mathbf{u})|^2 \\ \epsilon_{SGS} &= ce \frac{\sqrt{k_{SGS}}}{\Delta} k_{SGS} \end{aligned}$$

Eq. 334 is similar to the transport equation for k of the $k-\epsilon$ model. Also the definition of the sub-grid viscosity is similar to the definition of the turbulent viscosity of the $k-\epsilon$ model. This is not very obvious. Therefore, we shall explore this matter further.

$$\nu_{SGS} = ck \Delta \sqrt{k_{SGS}} \quad (333)$$

$$\nu_{SGS} = ck \frac{ce}{ce} \frac{k_{SGS}}{k_{SGS}} \frac{\sqrt{k_{SGS}}}{\sqrt{k_{SGS}}} \Delta \sqrt{k_{SGS}} \quad (335)$$

$$\nu_{SGS} = ck ce \frac{k_{SGS} \sqrt{k_{SGS}} \sqrt{k_{SGS}}}{ce \frac{k_{SGS} \sqrt{k_{SGS}}}{\Delta}} \quad (336)$$

$$\nu_{SGS} = ck ce \frac{k_{SGS}^2}{\epsilon_{SGS}} \quad (337)$$

Eq. 337 is similar to Eq. 257 – the definition of the turbulent viscosity of the $k-\epsilon$ model

$$\nu_T = C_\mu \frac{k^2}{\epsilon} \quad (257)$$

The product of ck and ce when using their default values gives $ck \cdot ce = 0.0985$ which is approximately the default value of C_μ of the $k-\epsilon$ model, which is $C_\mu = 0.09$.

75 The use of phi

75.1 The question

The governing equations of the solvers of OpenFOAM are written in a special notation that makes it easy to compare the source codes with equations from a fluid dynamics textbook. In Section 52.1 the governing equations of the solver *pimpleFoam* are examined. There, the terms of Eq. 115 are compared with the source code, see Listing 335. Here, we repeat the comparison of how the convective term is written in the sources and how this term is expressed mathematically.

$$\underbrace{\nabla(\mathbf{u}\mathbf{u})}_{\text{div}(\mathbf{u}\mathbf{u})} \Leftrightarrow \text{fvm}::\text{div}(\phi, \mathbf{U})$$

We now examine how *phi* is defined and how we can find *phi* in the math.

75.2 Implementation

75.2.1 The origin of fields

One way to learn more about *phi* is to look for its definition in the source code of OpenFOAM.

Listing 581 shows the first lines of the *main* function of the solver *pimpleFoam*. The *main* function of any C or C++ program is entered, when this program is executed. So, the instructions of Listing 581 are the first instructions that are executed, when the solver is called.

In line 6 of Listing 581 the file *createFields.H* is included. This file contains instructions that create the data structures of all fields that are necessary for the solver (e.g. the pressure or the velocity field).

```
1 int main(int argc, char *argv[])
2 {
3     #include "setRootCase.H"
4     #include "createTime.H"
5     #include "createMesh.H"
6     #include "createFields.H"
7     #include "initContinuityErrs.H"
8
9     /* the rest of the solver */
```

Listing 581: The first few line of the *main* function of *pimpleFoam* in *pimpleFoam.C*

The file *createFields.H* contains the content of Listing 582. There, the velocity field *U* is created. In line 15 the file *createPhi.H* is included. There, the field *phi* is created.

```
1 Info<< "Reading field U\n" << endl;
2 volVectorField U
3 (
4     IOobject
5     (
6         "U",
7         runTime.timeName(),
8         mesh,
9         IOobject::MUST_READ,
10        IOobject::AUTO_WRITE
11    ),
12    mesh
13 );
14
15 #include "createPhi.H"
```

Listing 582: The creation of *U* and *phi* in the file *createFields.H*

75.2.2 How phi is defined

Listing 583 shows the content of the file `createPhi.H`. From this Listing we see the data type of `phi`, it is `surfaceScalarField`. This tells us, that `phi` is a scalar, that is defined on the faces of the control volumes (cells) of the mesh.

Line 13 tells us how `phi` is defined. There, we find out, that `phi` is the inner product of the velocity – we forgot for the moment about the function `linearInterpolate` – and the face surface area vector. In Listing 584 we see the declaration of the function `Sf()`. In Listing 585 we see, that the variable `mesh` of Listing 583 is of the type `fvMesh`.

```

1 Info<< "Reading/calculating face flux field phi\n" << endl;
2
3 surfaceScalarField phi
4 (
5     IOobject
6     (
7         "phi",
8         runTime.timeName(),
9         mesh,
10        IOobject::READ_IF_PRESENT,
11        IOobject::AUTO_WRITE
12    ),
13    linearInterpolate(U) & mesh.Sf()
14 );

```

Listing 583: The creation of `phi` in the file `createPhi.H`

```

1 // - Return cell face area vectors
2 const surfaceVectorField& Sf() const;

```

Listing 584: The declaration of the method `Sf()` of the class `fvMesh` in the file `fvMesh.H`

```

1 Foam::Info
2   << "Create mesh for time = "
3   << runTime.timeName() << Foam::nl << Foam::endl;
4
5 Foam::fvMesh mesh
6 (
7     Foam::IOobject
8     (
9         Foam::fvMesh::defaultRegion,
10        runTime.timeName(),
11        runTime,
12        Foam::IOobject::MUST_READ
13    )
14 );

```

Listing 585: The creation of the mesh in the file `createMesh.H`

75.3 The math

Now, let us examine the origin of `phi` from the mathematical point of view. We start with the governing equations of a solver for incompressible fluids. Therefore, Eq. 115 is repeated below.

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \nabla \cdot \text{dev}(-\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)) = -\nabla p + \mathbf{Q} \quad (115)$$

This equation is written in differential form and is valid everywhere in the fluid. In order to use the finite volume method, we need the governing equations in the integral form. Integrating Eq. (115) over a control volume yields:

$$\int_V \frac{\partial \mathbf{u}}{\partial t} + \nabla(\mathbf{u}\mathbf{u}) + \nabla \cdot \text{dev}(-\nu^{eff} (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)) dV = \int_V -\nabla p + \mathbf{Q} dV \quad (338)$$

Now we will have a closer look on the second term of Eq. (338). That is the convective term we already saw at the beginning of this section.

Using Gauss' theorem, we replace the integration over the volume of our control volume with the integration over the surface of the control volume.

$$\int_V \nabla(\mathbf{u}\mathbf{u}) dV = \oint_{\partial V} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S} \quad (339)$$

Because our control volume is a polyhedron (in most cases a hexahedron or a tetrahedron), the surface integral reduces to a sum of intergrals over the faces S_f of the polyhedron.

$$\oint_{\partial V} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S} = \sum_f \int_{S_f} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S}_f \quad (340)$$

$$\|\mathbf{S}_f\| = S_f \quad (341)$$

With \mathbf{S}_f being the surface normal vector of the face f . The norm of this vector is equal to the area of the face f . We denote with the subscript f the mean face-value of a quantity.

$$\sum_f \int_{S_f} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S}_f = \sum_f (\mathbf{u}\mathbf{u})_f \cdot \mathbf{S}_f \quad (342)$$

$$(\mathbf{u}\mathbf{u})_f = \frac{1}{S_f} \int_{S_f} (\mathbf{u}\mathbf{u}) d\mathbf{S}_f \quad (343)$$

$$(\mathbf{u}\mathbf{u})_f \approx (\mathbf{u}_f \mathbf{u}_f) \quad (344)$$

$$\sum_f (\mathbf{u}\mathbf{u})_f \cdot \mathbf{S}_f \approx \sum_f (\mathbf{u}_f \mathbf{u}_f) \cdot \mathbf{S}_f \quad (345)$$

Eq. (345) contains the fundamental assumption or approximation of the finite volume method. It is assumed, that the mean face-value of the product of the velocities is (approximately) equal to the product of the mean face-values of the velocity, see Eq. (344). In general, the operations averaging and multiplication are not commutative.

We are now nearly finished. The *rhs* of Eq. (345) contains all ingredients we need for *phi*. A surface area vector, a velocity and an inner vector product. See Listing 583. However, this ingredients are not in the order we need. Therefore, there is need for some more math to do.

A general rule of tensor calculus states:

$$\mathbf{a} \otimes \mathbf{b} \cdot \mathbf{c} = \mathbf{a}(\mathbf{b} \cdot \mathbf{c}) \quad (346)$$

In this document, we omit the symbol \otimes for the sake of brevity.

$$\mathbf{a} \otimes \mathbf{b} \cdot \mathbf{c} = (\mathbf{a}\mathbf{b}) \cdot \mathbf{c} \quad (347)$$

Eq. (347) looks like the *rhs* of Eq. (345).

$$(\mathbf{u}_f \mathbf{u}_f) \cdot \mathbf{S}_f = \mathbf{u}_f \underbrace{(\mathbf{u}_f \cdot \mathbf{S}_f)}_{= \phi_f} \quad (348)$$

$$\mathbf{u}_f (\mathbf{u}_f \cdot \mathbf{S}_f) = \mathbf{u}_f \phi_f \quad (349)$$

75.4 Summary

Now, after having dug deep into the sources and after having done some math, we can summarize all thoughts so far. We want to understand this equivalency.

$$\underbrace{\nabla(\mathbf{u}\mathbf{u})}_{\text{div}(\mathbf{u}\mathbf{u})} \Leftrightarrow \text{fvm}::\text{div}(\text{phi}, \text{U})$$

The math tells us the following identities.

$$\int_V \nabla(\mathbf{u}\mathbf{u}) dV = \oint_{\partial V} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S} \quad (350)$$

$$\oint_{\partial V} (\mathbf{u}\mathbf{u}) \cdot d\mathbf{S} = \sum_f (\mathbf{u}\mathbf{u})_f \cdot \mathbf{S}_f \quad (351)$$

$$\sum_f (\mathbf{u}\mathbf{u})_f \cdot \mathbf{S}_f \approx \sum_f (\mathbf{u}_f \mathbf{u}_f) \cdot \mathbf{S}_f \quad (352)$$

$$\sum_f (\mathbf{u}_f \mathbf{u}_f) \cdot \mathbf{S}_f = \sum_f \mathbf{u}_f (\mathbf{u}_f \cdot \mathbf{S}_f) \quad (353)$$

$$\sum_f \mathbf{u}_f (\mathbf{u}_f \cdot \mathbf{S}_f) = \sum_f \mathbf{u}_f \phi_f \quad (354)$$

We have shown, that the integral formulation of the convective term can be reformulated to incorporate ϕ and \mathbf{u} instead of $\mathbf{u}\mathbf{u}$.

76 Derivation of the IATE diameter model

In this section we cover the derivation of OpenFOAM's IATE diameter model from [35].

76.1 Number density transport equation

We start with the transport equation for the bubble number density distribution $f = f(V, \mathbf{x}, t)$, e.g. from [35]. For sake of readability in most cases we refer to $f(V, \mathbf{x}, t)$ simply as f .

The first term of Eqn. (355) is the local rate of change of the bubble number density distribution. The second term represents convective transport. The third term represents the rate of change due to change of bubble volume. On the right hand side of the equation are source terms due to bubble interactions S_j and phase change S_{ph} .

$$\frac{\partial f}{\partial t} + \nabla \cdot (f\mathbf{u}) + \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) = \sum_j S_j + S_{ph} \quad (355)$$

The equation for the bubble number density distribution is much too detailed for most flow studies [41]. Thus, we derive a transport equation for the area concentration a_i . The area concentration is a moment of the bubble number density distribution. Besides the area concentration we can define further quantities based on the moments of the number density distribution.

Eqn. (356) lists the general definition of the i -th moment m_i of the probability density function $f(x)$.

$$m_i = \int_a^b f(x)x^i dx \quad (356)$$

We now define some moments of the bubble number density distribution.

$$\text{Total number of bubbles per unit volume} \quad n(x, t) = \int_{V_{min}}^{V_{max}} f(V, \mathbf{x}, t) dV \quad (357)$$

$$\text{Volume fraction of bubbles} \quad \alpha(x, t) = \int_{V_{min}}^{V_{max}} f(V, \mathbf{x}, t) V dV \quad (358)$$

$$\text{Area concentration of bubbles} \quad a_i(x, t) = \int_{V_{min}}^{V_{max}} f(V, \mathbf{x}, t) A_i(V) dV \quad (359)$$

76.2 Interfacial area transport equation

76.2.1 Deriving the governing equations

We will use Eqn. (359) to derive a transport equation for the area concentration from Eqn. (355). First we multiply Eqn. (355) by the average interfacial area $A_i(V)$ of bubbles with the volume V .

$$A_i \frac{\partial f}{\partial t} + A_i \nabla \cdot (f\mathbf{u}) + A_i \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) = A_i \left(\sum_j S_j + S_{ph} \right) \quad (360)$$

Then, we integrate Eqn. (360) over all bubble sizes

$$\int_{V_{min}}^{V_{max}} \left[A_i \frac{\partial f}{\partial t} + A_i \nabla \cdot (f\mathbf{u}) + A_i \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) \right] dV = \int_{V_{min}}^{V_{max}} A_i \left(\sum_j S_j + S_{ph} \right) dV \quad (361)$$

Now we will take a closer look on the single terms of Eqn. (361). For the first term, we simply apply Leibnitz rule. Here it is important to note, that A_i is constant in space and time. With Eqn. (359), we gain the local

derivative of the interfacial area concentration a_i .

$$\int_{V_{min}}^{V_{max}} A_i \frac{\partial f}{\partial t} dV = \frac{\partial}{\partial t} \int_{V_{min}}^{V_{max}} A_i f dV \quad (362)$$

$$\int_{V_{min}}^{V_{max}} A_i \frac{\partial f}{\partial t} dV = \frac{\partial}{\partial t} a_i \quad (363)$$

The convective term of Eqn. (361) can be treated in a similar fashion. If the velocity is independent of the bubble size, we can put the \mathbf{u} in front of the integral over all bubble sizes. Thus, we gain the convective term for the interfacial area concentration.

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \int_{V_{min}}^{V_{max}} \nabla \cdot (A_i f \mathbf{u}) dV \quad (364)$$

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \nabla \cdot \left(\mathbf{u} \int_{V_{min}}^{V_{max}} A_i f dV \right) \quad (365)$$

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \nabla \cdot (\mathbf{u} a_i) \quad (366)$$

If the velocity is not independent of the bubble size we can follow a similar strategy to derive a convective term which is formulated in terms of the interfacial area concentration.

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \int_{V_{min}}^{V_{max}} \nabla \cdot \left(\frac{a_i}{a_i} A_i f \mathbf{u} \right) dV \quad (367)$$

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \nabla \cdot \left(a_i \frac{\int_{V_{min}}^{V_{max}} A_i f \mathbf{u} dV}{a_i} \right) \quad (368)$$

$$\int_{V_{min}}^{V_{max}} A_i \nabla \cdot (f \mathbf{u}) dV = \nabla \cdot (a_i \mathbf{u}_i) \quad (369)$$

With the average local bubble velocity weighted by the bubble number \mathbf{u}_i [20]

$$\mathbf{u}_i = \frac{\int_{V_{min}}^{V_{max}} A_i f \mathbf{u} dV}{\int_{V_{min}}^{V_{max}} A_i f dV} \quad (370)$$

The third term of Eqn. (361) needs more special treatment. In Section 76.5.1 we show the proof for (371). This term relates to the gas expansion.

$$\int_{V_{min}}^{V_{max}} A_i \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) dV = -\frac{2}{3} \frac{\dot{\alpha}}{\alpha} a_i \quad (371)$$

The RHS of Eqn. 361 contains the terms due to bubble-bubble interaction and due to phase change.

$$\int_{V_{min}}^{V_{max}} \left[A_i \frac{\partial f}{\partial t} + A_i \nabla \cdot (f \mathbf{u}) + A_i \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) \right] dV = \int_{V_{min}}^{V_{max}} A_i \left(\sum_j S_j + S_{ph} \right) dV \quad (361)$$

There are two approaches to model the source terms due to bubble interaction [43]. One can solve the integral equation for these source terms (372) or solve algebraic equations using mean parameters (373).

The latter approach assumes monosized bubble, i.e. a bubble breaks up into two equalsized daughter bubbles [43]. In this approach each bubble interaction results in a change of interfacial area $\Delta A_i = \frac{1}{3} A_i$.

$$\int_{V_{min}}^{V_{max}} A_i \sum_j S_j dV = \Phi_j \quad (372)$$

$$\Phi_j = S_j \Delta A_i \quad (373)$$

with the interfacial area A_i

$$A_i = \frac{a_i}{n} \quad (374)$$

and bubble number density n , $\Psi = \frac{1}{36\pi}$ for spherical bubbles

$$n = \Psi \frac{a_i^3}{\alpha^2} \quad (375)$$

$$\Phi_j = \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{a_i} \right)^2 S_j \quad (376)$$

The phase change term can be modelled directly, but within the framework of this manual we will not consider phase change. Thus we gained a transport equation for the interfacial area concentration a_i .

$$\frac{\partial a_i}{\partial t} + \nabla \cdot (\mathbf{u} a_i) = \frac{2}{3} \frac{\dot{\alpha}}{\alpha} a_i + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{a_i} \right)^2 S_j \quad (377)$$

76.3 Interfacial curvature transport equation

76.3.1 Basic definitions

The IATE diameter model solves a transport equation for the interfacial curvature `kappai_`.

Solves for the interfacial curvature per unit volume of the phase rather than interfacial area per unit volume to avoid stability issues relating to the consistency requirements between the phase fraction and interfacial area per unit volume.

Class description in `IATE.H`

By looking into the sources, we find the following relations

$$a_i = \alpha \kappa \quad (378)$$

$$d_{sm} = \frac{6}{\kappa} \quad (379)$$

Thus, the Sauter mean diameter d_{sm} equals

$$d_{sm} = \frac{6\alpha}{a_i} \quad (380)$$

Which corresponds with the definition given in literature [33, 34].

$$d_{sm} = \frac{6\alpha}{a_i} \quad (381)$$

Listing 586 and 587 show the relevant source code of the IATE diameter model. This source code is the basis for Eqns. (378) and (379).

```

1 // - Return the interfacial area
2 tmp<volScalarField> a() const
3 {
4     return phase_*kappai_;
5 }
```

Listing 586: Definition of the method `a()` of the IATE diameter model class in the file `IATE.H`.

```

1 Foam::tmp<Foam::volScalarField> Foam::diameterModels::IATE::dsm() const
2 {
3     return max(6/max(kappai_, 6/dMax_), dMin_);
4 }
```

Listing 587: Definition of the method `dsm()` of the IATE diameter model class in the file `IATE.C`.

The definition of `kappai_` as the interfacial curvature seems a bit counter-intuitive, as the curvature of a sphere is the inverse of its radius.

76.3.2 Derivation of the governing equations

We will now derive the governing equations for the interfacial curvature κ from the equations for the interfacial area concentration a_i which we derived from the transport equations for the bubble size distribution.

Here we will make no further assumptions, as we are simply rearranging the equations. We start from the transport equation for the interfacial area concentration a_i and OpenFOAM's definition of a_i .

$$\frac{\partial a_i}{\partial t} + \nabla \cdot (\mathbf{u} a_i) = \frac{2}{3} \frac{\dot{\alpha}}{\alpha} a_i + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{a_i} \right)^2 S_j \quad (377)$$

$$a_i = \alpha \kappa \quad (378)$$

Inserting (378) into (377) yields

$$\frac{\partial \alpha \kappa}{\partial t} + \nabla \cdot (\mathbf{u} \alpha \kappa) = \frac{2}{3} \frac{\dot{\alpha}}{\alpha} \alpha \kappa + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{\alpha \kappa} \right)^2 S_j \quad (382)$$

Next, we apply partial derivation of all terms containing κ

$$\alpha \frac{\partial \kappa}{\partial t} + \kappa \frac{\partial \alpha}{\partial t} + \kappa \nabla \cdot (\mathbf{u} \alpha) + \alpha \mathbf{u} \cdot \nabla \kappa = \frac{2}{3} \dot{\alpha} \kappa + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{1}{\kappa} \right)^2 S_j \quad (383)$$

$$\kappa \underbrace{\left[\frac{\partial \alpha}{\partial t} + \nabla \cdot (\mathbf{u} \alpha) \right]}_{\dot{\alpha}} + \alpha \left[\frac{\partial \kappa}{\partial t} + \mathbf{u} \cdot \nabla \kappa \right] = \frac{2}{3} \dot{\alpha} \kappa + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{1}{\kappa} \right)^2 S_j \quad (384)$$

$$\alpha \left[\frac{\partial \kappa}{\partial t} + \mathbf{u} \cdot \nabla \kappa \right] = -\frac{1}{3} \dot{\alpha} \kappa + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{1}{\kappa} \right)^2 S_j \quad (385)$$

$$\frac{\partial \kappa}{\partial t} + \mathbf{u} \cdot \nabla \kappa = -\frac{1}{3} \dot{\alpha} \frac{\kappa}{\alpha} + \sum_j \frac{1}{3} \frac{1}{\Psi} \frac{1}{\alpha} \left(\frac{1}{\kappa} \right)^2 S_j \quad (386)$$

With $\frac{1}{\kappa} = \frac{\alpha}{a_i}$

$$\underbrace{\frac{\partial \kappa}{\partial t} + \nabla \cdot (\kappa \mathbf{u})}_{I} - \underbrace{\kappa \nabla \cdot \mathbf{u}}_{II} = -\frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa + \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{a_i} \right)^2 \sum_j \frac{S_j}{\alpha} \quad (387)$$

The form of Eqn. (387) is chosen to match the equations given in [35]. The second term of the RHS has exactly the same form as the equivalent terms in [35].

76.3.3 Implemented equations

Thus, we have derived a transport equation for κ . However, we still need to check the equations that are implemented in OpenFOAM. Therefore, we take a look at the source code.

In Listing 588 we see the main code for the transport equation. In Line 4 we see the terms marked with I of Eqn. (387). In Line 5 term II of Eqn. (387) is implemented.

```

1 // Construct the interfacial curvature equation
2 fvScalarMatrix kappaiEqn
3 (
4     fvm::ddt(kappai_) + fvm::div(phase_.phi(), kappai_)
5     - fvm::Sp(fvc::div(phase_.phi()), kappai_)
6     ==
7     - fvm::SuSp(R, kappai_)
8 //+ Rph() // Omit the nucleation/condensation term
9 );

```

Listing 588: Construction of the transport equation in the file IATE.C.

The right hand side of the equation in Listing 588 combines all term of the RHS of Eqn. (387) into the term `fvm::SuSp(R, kappai_)`. The method `fvm::SuSp()` implements a source term for a matrix equation. The arguments translate to `R * kappai_`.

The first term on the RHS of Eqn. (387) is due to the change of bubble volume (dilatation effect). The code in Listing 589 translates to Eqn. (388).

```

1 // Initialise the accumulated source term to the dilatation effect
2 volScalarField R
3 (
4     (
5         (1.0/3.0)
6         /max
7         (
8             fvc::average(phase_ + phase_.oldTime()),
9             residualAlpha_
10            )
11        )
12     *(fvc::ddt(phase_) + fvc::div(phase_.alphaPhi()))
13 );

```

Listing 589: The first term of the RHS of Eqn. (387) of the transport equation in the file `IATE.C`.

$$R = \frac{1}{3} \frac{\frac{\partial \alpha}{\partial t} + \nabla \cdot (\alpha \mathbf{u})}{\alpha} \quad (388)$$

The method call `fvm::SuSp(R, kappai_)` multiplies `R` with `kappai_`. Thus we recognize the first term of the RHS of Eq. (387).

$$\text{Eqn. (387)} \quad III = -\frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa \quad (389)$$

$$\text{OpenFOAM} \quad III = -R\kappa \quad (390)$$

$$R = \frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa \quad (391)$$

$$III = -\frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa \quad (392)$$

The other source terms related to the models for bubble-bubble interaction are added to `R`. Listing 590 shows the loop over all sources, note the minus sign.

```

1 // Accumulate the run-time selectable sources
2 forAll(sources_, j)
3 {
4     R -= sources_[j].R();
5 }

```

Listing 590: The second term of the RMS of Eqn. (387) of the transport equation in the file `IATE.C`.

For the interaction models the minus of Listing 590 cancels the minus of Listing 588.

76.4 Interaction models

OpenFOAM provides a base class for all models related to bubble-bubble interaction. There are several interaction mechanisms implemented.

1. Breakage due to impact of turbulent eddies (TI - *turbulent impact*)
2. Coalescence through random collision driven by turbulent eddies (RC - *random collision*)
3. Coalescence due to acceleration of the following bubble in the wake of preceding bubble (WE - *wake entrainment*)

The base class is named `IATEsource` and it defines a pure virtual function named `R()`. This means that every derived class has to provide its implementation of `R()`. Besides `R()`, the base class provides a number of helper methods that are used in the derived classes, e.g. bubble Reynolds number `Re()` or the Weber number `We()`.

76.4.1 Turbulent impact - TI

In [34, 35] the source term due to turbulent impact is stated as:

$$n = \Psi \frac{a_i^3}{\alpha^2} \quad (393)$$

$$u_t = \sqrt{2k} \quad (394)$$

$$R_{TI} = C_{TI} \left(\frac{n u_t}{D_b} \right) \exp \left(-\frac{We_{cr}}{We} \right) \sqrt{1 - \frac{We_{cr}}{We}} \quad \text{where } We_{cr} > We \quad (395)$$

The Weber number We can be seen as the ratio of inertia forces and surface tension forces and is defined as:

$$We = \frac{\rho u^2 d}{\sigma} \quad (396)$$

with

ρ	density
u	characteristic velocity
d	characteristic length scale
σ	surface tension

The Weber number is provided by the class `IATESource` as the base class for all interaction models. See Section 76.4.4 for implementation details.

The critical Weber number We_{cr} and the model constant C_{TI} must be provided by the user in the appropriate dictionary.

76.4.2 Random collision - RC

In [34, 35] the source term due to random collision is stated as:

$$u_t = \sqrt{2k} \quad (397)$$

$$R_{RC} = C_{RC} \left[\frac{n^2 u_t D_b^2}{\alpha_{max}^{1/3} (\alpha_{max}^{1/3} - \alpha^{1/3})} \right] \left[1 - \exp \left(-C \frac{\alpha_{max}^{1/3} \alpha^{1/3}}{\alpha_{max}^{1/3} - \alpha^{1/3}} \right) \right] \quad (398)$$

The model constants C_{RC} , C and α_{max} need to be provided by the user.

76.4.3 Wake entrainment - WE

In [34, 35] the source term due to wake entrainment is stated as:

$$R_{WE} = C_{WE} C_D^{1/3} n^2 D_b^2 u_r \quad (399)$$

The model constant C_{WE} needs to be provided by the user.

76.4.4 Implementation details of the `IATESource` class

Weber number

The Weber number is implemented in the class `IATESource`, see Listing 591. This definition makes use the method `Ur()`, which is also provided by `IATESource`.

```

1  Foam::tmp<Foam::volScalarField> Foam::diameterModels::IATESource::We()
2  const
3  {
4      return otherPhase().rho()*sqr(Ur())*phase().d()/fluid().sigma();
5 }
```

Listing 591: The definition of the Weber number We in `IATESource.C`

Relative velocity

The relative velocity between the bubbles and the surrounding fluid is given by [32, 40]. Compare Eqn. (400) and Listing 592.

$$u_r = \sqrt{2} \left[\frac{\sigma g \Delta \rho}{\rho_L^2} \right]^{1/4} (1 - \alpha)^{1.75} \quad (400)$$

```

1  Foam::tmp<Foam::volScalarField> Foam::diameterModels::IATEsource::Ur() const
2  {
3      const uniformDimensionedVectorField& g =
4          phase().U().db().lookupObject<uniformDimensionedVectorField>("g");
5
6      return
7          sqrt(2.0)
8          *pow025
9          (
10             fluid().sigma()*mag(g)
11             *(otherPhase().rho() - phase().rho())
12             /sqr(otherPhase().rho())
13         )
14         *pow(max(1 - phase(), scalar(0)), 1.75);
15 }
```

Listing 592: The definition of the relative velocity between bubbles and surrounding liquid in `IATEsource.C`

The IATE implicitly applies only to bubbly systems, i.e. gas-liquid systems. If the IATE model is applied to the denser phase, then Line 11 of Listing 592 leads to a floating-point exception (FPE). If `phase` refers to the liquid phase, then Line 11 evaluates to a negative number. Raising a negative number to a non-integer power is not possible within the domain of the real numbers. Thus, OpenFOAM will issue an error message due to a floating-point exception.

Comparing the formulations

Here we take a closer look on the implementation of the source terms. Listing 593 shows the method `R()` of the `IATEsource` class.

```

1  Foam::tmp<Foam::volScalarField>
2  Foam::diameterModels::IATESources::turbulentBreakUp::R() const
3  {
4      tmp<volScalarField> tR
5      (
6          new volScalarField
7          (
8              IOobject
9              (
10                 "R",
11                 iate_.phase().U().time().timeName(),
12                 iate_.phase().mesh()
13             ),
14             iate_.phase().U().mesh(),
15             dimensionedScalar("R", dimless/dimTime, 0)
16         )
17     );
18
19     volScalarField R = tR();
20     scalar Cti = Cti_.value();
21     scalar WeCr = WeCr_.value();
22     volScalarField Ut(this->Ut());
23     volScalarField We(this->We());
24     const volScalarField& d(iate_.d());
25
26     forAll(R, celli)
27     {
28         if (We[celli] > WeCr)
29         {
```

```

30     R[celli] =
31         (1.0/3.0)
32         *Cti/d[celli]
33         *Ut[celli]
34         *sqrt(1 - WeCr/We[celli])
35         *exp(-WeCr/We[celli]);
36     }
37 }
38
39     return tR;
40 }

```

Listing 593: The definition of the method `R()` in `turbulentBreakUp.C`

Listing 593 translates to the following mathematical expression:

$$R_{TI} = \frac{1}{3} \frac{C_{TI}}{d_{sm}} u_t \sqrt{1 - \frac{We_{cr}}{We}} \exp\left(-\frac{We_{cr}}{We}\right) \quad \text{where } We > We_{cr} \quad (401)$$

Comparing Eqns. (395) and (401) reveals some differences in formulation. This is due to the fact, that Eq. (395) is a source term for the transport equation for the interfacial area concentration a_i and Eq. (401) is a source term for the transport equation for the interfacial curvature κ .

In the derivation of the curvature equation from the area concentration equation we divided by the volume fraction. Otherwise, only rearrangement and variable substitution was performed.

For this term we now have a look on the RHS of the equations for a_i and κ and compare the implementation of OpenFOAM with the equations stated in literature.

We begin with repeating the equations for a_i and κ . The interaction source term S_j can be found in this form in [35].

$$\frac{\partial a_i}{\partial t} + \nabla \cdot (\mathbf{u} a_i) = \frac{2}{3} \frac{\dot{\alpha}}{\alpha} a_i + \sum_j \frac{1}{3} \frac{1}{\Psi} \left(\frac{\alpha}{a_i}\right)^2 S_j \quad (377)$$

$$\frac{\partial \kappa}{\partial t} + \nabla (\kappa \mathbf{u}) - \kappa \nabla \cdot \mathbf{u} = -\frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa + \underbrace{\frac{1}{3\Psi} \left(\frac{\alpha}{a_i}\right)^2 \sum_j \frac{S_j}{\alpha}}_{IV} \quad (387)$$

The interaction model source terms in the curvature equation of OpenFOAM takes the following form:

$$\frac{\partial \kappa}{\partial t} + \nabla (\kappa \mathbf{u}) - \kappa \nabla \cdot \mathbf{u} = -\frac{1}{3} \frac{\dot{\alpha}}{\alpha} \kappa + \underbrace{\sum_j R_j \kappa}_{IV} \quad (402)$$

We now compare the terms marked with IV of Eqns. (387) and (402). As these terms must be equal, we can form the following equation.

$$\frac{1}{3\Psi} \left(\frac{\alpha}{a_i}\right)^2 \sum_j \frac{S_j}{\alpha} = \sum_j R_j \kappa \quad (403)$$

We now demand, that the summands need to be equal, and we focus on the term for turbulent break-up (TI)

$$\underbrace{\frac{1}{3\Psi} \left(\frac{\alpha}{a_i}\right)^2 \frac{1}{\alpha} C_{TI} \left(\frac{n u_t}{D_b}\right) \exp\left(-\frac{We_{cr}}{We}\right)}_{S_j} \sqrt{1 - \frac{We_{cr}}{We}} = \underbrace{\frac{1}{3} \frac{C_{TI}}{d_{sm}} u_t \sqrt{1 - \frac{We_{cr}}{We}} \exp\left(-\frac{We_{cr}}{We}\right)}_{R_j} \kappa \quad (404)$$

Next, we cancel all common symbols and expressions, note the different symbols for the bubble diameter ($D_b = d_{sm}$)

$$\frac{1}{\Psi} \left(\frac{\alpha}{a_i}\right)^2 \frac{1}{\alpha} n = \kappa \quad (405)$$

We now insert the definition of n , see Eq. (393)

$$\frac{1}{\Psi} \left(\frac{\alpha}{a_i} \right)^2 \frac{1}{\alpha} \Psi \frac{a_i^3}{\alpha^2} = \kappa \quad (406)$$

$$\frac{a_i}{\alpha} = \kappa \quad (407)$$

We now end up with an equation that is fulfilled, when we look at the definition of κ , see Eqn. (378)

$$a_i = \alpha \kappa \quad (378)$$

Thus, we have demonstrated on the example of the source term for turbulent break-up of bubbles, that the implementation of OpenFOAM follows exactly the model published in [35].

76.5 Appendix

76.5.1 The proof for Eqn. (371)

We use the following symbols.

$$x = V \quad (408)$$

$$f(x) = f(V, \mathbf{x}, t) \quad (409)$$

$$g(x) = A_i(V) \quad (410)$$

$$a = V_{min} \quad (411)$$

$$b = V_{max} \quad (412)$$

Thus, the LHS of Eqn. (371) becomes

$$\int_{V_{min}}^{V_{max}} A_i \frac{\partial}{\partial V} \left(f \frac{dV}{dt} \right) dV = \int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx \quad (413)$$

Now, we apply partial integration

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = \left[f(x) \frac{dx}{dt} g(x) \right]_a^b - \int_a^b \frac{\partial g(x)}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx \quad (414)$$

As $f(x)$ is a probability density distribution it has the following properties

$$f(a) = f(b) = 0 \quad (415)$$

Thus, the first term of the RHS of Eqn. (414) vanishes

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \int_a^b \frac{\partial g(x)}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx \quad (416)$$

We now take a closer look on the relation between the average interfacial area of a bubble A_i and the volume of a bubble V .

$$A_i = d^2 \pi \quad (417)$$

$$V = \frac{d^3 \pi}{6} \quad (418)$$

$$\Rightarrow d = \sqrt[3]{\frac{6V}{\pi}} \quad (419)$$

$$A_i = \left(\frac{6V}{\pi} \right)^{2/3} \pi \quad (420)$$

Returning to our simplified notation for this proof

$$g(x) = \left(\frac{6x}{\pi}\right)^{2/3} \pi \quad (421)$$

For Eqn. (416) we also need the derivative of $g(x)$

$$\frac{\partial g(x)}{\partial x} = \frac{2}{3} \left(\frac{6}{\pi}\right)^{2/3} (x)^{-1/3} \pi \quad (422)$$

$$\frac{\partial g(x)}{\partial x} = \frac{2}{3} \left(\frac{6}{\pi}\right)^{2/3} \frac{x^{2/3}}{x} \pi \quad (423)$$

$$\frac{\partial g(x)}{\partial x} = \frac{2}{3} \frac{1}{x} \left(\frac{6x}{\pi}\right)^{2/3} \pi \quad (424)$$

$$\frac{\partial g(x)}{\partial x} = \frac{2}{3} \frac{g(x)}{x} \quad (425)$$

We now insert Eqn. (416) into Eqn. (416).

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \int_a^b \frac{2}{3} \frac{g(x)}{x} \left(f(x) \frac{dx}{dt} \right) dx \quad (426)$$

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \frac{2}{3} \int_a^b \frac{\dot{x}}{x} f(x) g(x) dx \quad (427)$$

Next, we take a closer look on the term $\frac{\dot{x}}{x}$. Since x is the volume of the bubbles V , we can relate V to the void fraction or gas phase volume fraction α . For any control volume V_{CV} we can state, that the volume of the bubbles V is equal to the volume fraction times the control volume. Here we neglect mass transfer by evaporation, see [34] for a derivation considering evaporation.

$$V = \alpha V_{CV} \quad (428)$$

$$\dot{V} = \dot{\alpha} V_{CV} \quad (429)$$

$$\frac{\dot{V}}{V} = \frac{\dot{\alpha} V_{CV}}{\alpha V_{CV}} = \frac{\dot{\alpha}}{\alpha} \quad (430)$$

$$\frac{\dot{x}}{x} = \frac{\dot{\alpha}}{\alpha} \quad (431)$$

We further assume that the rate of change of volume is independent of the volume itself [34, 40].

$$\frac{\dot{V}}{V} \neq f(V) \quad (432)$$

By using relation (427) and (431) on Eqn. (427), we gain

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \frac{2}{3} \frac{\dot{\alpha}}{\alpha} \int_a^b f(x) g(x) dx \quad (433)$$

or by using the other notation, Eqns. (408)-(408)

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \frac{2}{3} \frac{\dot{\alpha}}{\alpha} \int_{V_{min}}^{V_{max}} f A_i dV \quad (434)$$

$$\int_a^b g(x) \frac{\partial}{\partial x} \left(f(x) \frac{dx}{dt} \right) dx = - \frac{2}{3} \frac{\dot{\alpha}}{\alpha} a_i \quad (435)$$

And by using (359) on (434) we have proofed (371).

77 Derivation of the governing equations for the MRF approach

77.1 Preliminary observations

In order to use the MRF approach the mesh has to be divided into different regions. As the MRF approach in OpenFOAM covers only rotating reference frames²⁹⁶ only rotation can be imposed on a region. A region for which a non-zero rotation is specified has to be axi-symmetric with respect to the rotational axis. Furthermore, older versions of OpenFOAM²⁹⁷ only support steady rotation, i.e. the angular velocity ω is constant.

77.1.1 Pitfalls

Axi-symmetric region for MRF rotation

As stated above, the MRF region for applying reference frame rotations has to be axi-symmetric. However, OpenFOAM performs no checks to test whether this is the case. Thus, on a region axi-symmetric with respect to the z -axis, may very well be used to prescribe a reference frame rotation around the x -axis. The results will be blatantly wrong, and the solver might crash. However, if you are unlucky enough, the solver will not crash and compute woefully wrong results, wasting time and computational resources.



Always check whether the `axis` of the `MRFProperties` coincides with the symmetry axis of your MRF zone. Furthermore, make sure that `origin` of the `MRFProperties` lies on the symmetry axis of the MRF zone.

77.2 Mass conservation equation

The mass conservation equation for incompressible flows

$$\nabla \cdot \mathbf{u} = 0 \quad (436)$$

is valid in all inertial frames of reference. An inertial frame of reference is either fixed in space and time or moving with a constant translational velocity.

Due to the constraints listed in the previous section we consider only rotating reference frames in the MRF method. To translate a vector from its representation in the inertial frame of reference to the rotating frame of reference a rotation matrix \mathbf{Q} is used. A rotation matrix has the property that the inverse is also the transposed.

$$_R\mathbf{u} = \mathbf{Q}\mathbf{u} \quad (437)$$

$$\mathbf{u} = \mathbf{Q}^T _R\mathbf{u} \quad (438)$$

$$\mathbf{Q}^{-1} = \mathbf{Q}^T \quad (439)$$

The index R before the symbol \mathbf{u} denotes that the vector $_R\mathbf{u}$ is given in the rotating frame of reference. If there is no index before the symbol the vector is given in the inertial coordinate system. The index R is put before the symbol to prevent the vector $_R\mathbf{u}$ to be mistaken as a relative velocity.

Beginning with the mass conservation equation in the inertial coordinate system we derive the mass conservation in the rotating coordinate system.

$$\nabla \cdot \mathbf{u} = 0 \quad (440)$$

$$\nabla \cdot \left(\underbrace{\mathbf{Q}^T \mathbf{Q}}_{=I} \mathbf{u} \right) = 0 \quad (441)$$

$$\nabla \cdot (\mathbf{Q}^T _R\mathbf{u}) = 0 \quad (442)$$

²⁹⁶E.g. in Fluent it is possible to prescribe frame motion with unsteady translational and rotational speeds [9]. This leads essentially to more additional terms in the governing equations. OpenFOAM, however, limits the frame motion to steady rotation.

²⁹⁷Prior to OpenFOAM-3.0, see Section 77.4.2.

We use the relation $\nabla \cdot (\mathbf{A} \cdot \mathbf{a}) = (\nabla \cdot \mathbf{A}) \cdot \mathbf{a} + \mathbf{A} : (\nabla \mathbf{a})$ and the note that the rotation matrix is constant in space.

$$\nabla \cdot (\mathbf{Q}^T {}_R \mathbf{u}) = \underbrace{(\nabla \cdot \mathbf{Q}^T)}_{=0} \cdot {}_R \mathbf{u} + \mathbf{Q}^T : (\nabla {}_R \mathbf{u}) \quad (443)$$

$$\nabla \cdot (\mathbf{Q}^T {}_R \mathbf{u}) = \mathbf{Q}^T : (\nabla {}_R \mathbf{u}) \quad (444)$$

$$\mathbf{Q}^T : (\nabla {}_R \mathbf{u}) = 0 \quad (445)$$

Next we multiply the equation from the left with the rotation matrix.

$$\mathbf{Q} \mathbf{Q}^T : (\nabla {}_R \mathbf{u}) = 0 \quad (446)$$

$$\mathbf{I} : (\nabla {}_R \mathbf{u}) = 0 \quad (447)$$

We remember that the contraction of the unit tensor and a velocity gradient is equal to the divergence of the velocity.

$$\mathbf{I} : (\nabla {}_R \mathbf{u}) = \nabla \cdot {}_R \mathbf{u} \quad (448)$$

$$\nabla \cdot {}_R \mathbf{u} = 0 \quad (449)$$

Thus, we showed that the mass conservation equation with the velocity expressed in the rotating coordinate system has the same formulation as the mass conservation equation in inertial coordinates.

77.3 Momentum conservation equation

When we use a rotating coordinate system, we can decompose the flow velocity in two components. The first is due to the rotation of the frame of reference and the second is the relative motion between the particle or fluid parcel under consideration and the rotating reference frame.

$$\mathbf{u} = \boldsymbol{\omega} \times \mathbf{r} + \mathbf{u}_R \quad (450)$$

Eq. (450) can also be written in this form using the spin tensor $\boldsymbol{\Omega}$

$$\mathbf{u} = \boldsymbol{\Omega} \mathbf{r} + \mathbf{u}_R \quad (451)$$

The spin tensor is a skew-symmetric tensor that contains the components of $\boldsymbol{\omega}$, the angular velocity vector.

$$\boldsymbol{\Omega} = \begin{pmatrix} 0 & -\omega_z & \omega_y \\ \omega_z & 0 & -\omega_x \\ -\omega_y & \omega_x & 0 \end{pmatrix} \quad (452)$$

We now derive the momentum equation for the velocity for the rotating zone starting from the momentum conservation equation for incompressible Newtonian fluids.

$$\frac{\partial \mathbf{u}}{\partial t} + (\nabla \mathbf{u}) \cdot \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (453)$$

The terms on the LHS are the total time derivate of \mathbf{u} . Thus, we can write

$$\frac{d\mathbf{u}}{dt} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (454)$$

With Eq. (450) we yield

$$\frac{d}{dt} (\boldsymbol{\Omega} \mathbf{r} + \mathbf{u}_R) = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (455)$$

We consider only steady rotation; thus, the temporal derivative of the spin vanishes

$$\frac{d\mathbf{u}_R}{dt} + \underbrace{\frac{d\boldsymbol{\Omega}}{dt}}_{=0} \mathbf{r} + \boldsymbol{\Omega} \frac{d\mathbf{r}}{dt} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (456)$$

$$\frac{d\mathbf{u}_R}{dt} + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (457)$$

We now evaluate the total time derivative of \mathbf{u}_R

$$\frac{\partial \mathbf{u}_R}{\partial t} + \underbrace{\frac{\partial \mathbf{u}_R}{\partial \mathbf{x}}}_{=\nabla \mathbf{u}_R} \underbrace{\frac{d\mathbf{x}}{dt}}_{=\mathbf{u}} + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (458)$$

$$\frac{\partial \mathbf{u}_R}{\partial t} + (\nabla \mathbf{u}_R) \cdot \mathbf{u} + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (459)$$

Now we insert \mathbf{u}_R from Eq. (450) into the local derivative

$$\frac{\partial}{\partial t} (\mathbf{u} - \boldsymbol{\Omega} \mathbf{r}) + (\nabla \mathbf{u}_R) \cdot \mathbf{u} + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (460)$$

As the velocity component due to the steady rotation of the reference frame is constant, the term $\frac{\partial}{\partial t} (\boldsymbol{\Omega} \mathbf{r})$ will vanish

$$\frac{\partial \mathbf{u}}{\partial t} + (\nabla \mathbf{u}_R) \cdot \mathbf{u} + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (461)$$

The second term on the LHS can be rewritten using the following identity

$$\nabla(\mathbf{a}\mathbf{b}) = (\nabla \cdot \mathbf{b})\mathbf{a} + (\nabla \mathbf{a}) \cdot \mathbf{b} \quad (462)$$

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot (\mathbf{u}_R \mathbf{u}) + \boldsymbol{\Omega} \mathbf{u} = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) \quad (463)$$

Thus, we derived the governing equation for the absolute velocity using flux relative to the local frame of reference.

The contribution from the rotation of the domain is limited to two terms in the governing equation. The LHS of Eq. (464) contains the relative velocity in the second term. The RHS of Eq. (464) contains the Coriolis force in the last term.

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot (\mathbf{u}_R \mathbf{u}) = -\frac{\nabla p}{\rho} + \nabla \cdot (\nu \nabla \mathbf{u}) - \boldsymbol{\Omega} \mathbf{u} \quad (464)$$

Eq. (464) corresponds to the momentum equation in absolute velocity formulation that can be found in the Fluent Theory Manual [9]. Another resource for the MRF approach in OpenFOAM is Nilsson 48.

77.4 Notes on the implementation of the MRF Approach

Adding Coriolis forces in the cells of the moving zone is not the only operation necessary for the MRF approach. The boundary conditions of the rotor have to be adjusted. As the rotor is moving the fluid velocity at the rotor walls is not zero. The velocity at the walls has to equal the solid body rotational velocity of the rotor.

77.4.1 OpenFOAM-2.*

In OpenFOAM-2.2.x the MRF method is part of the *fvOptions* mechanism²⁹⁸. This is a general mechanism that allows for run-time selectable physics. The *fvOptions* framework is a generalization for the source terms in the momentum equation. Via this framework the MRF approach can be selected along with momentum (e.g. wind turbine rotors), porosity (i.e. for modelling porous zones) and energy sources (e.g. for regions with heat transfer).

To provide this flexibility the *fvOptions* framework is implemented using an abstract class to define the behaviour of the general source. Derived class implement the actual physics, e.g. the MRF method. Thus the class `MRFSource` is derived from `option`.

The constructor of the class `MRFSource` calls the method `initialise()`. This method is defined in the class `MRFSource` and calls the method `correctBoundaryVelocity` of the class `MRFZone`. In the method `correctBoundaryVelocity` the velocity values of boundaries within an MRF-zone are set to the solid body rotational velocity. Otherwise the no-slip boundary condition would enforce a zero absolute velocity which would be clearly wrong.

²⁹⁸See <http://www.openfoam.org/version2.2.0/fvOptions.php>

In Listing 594 we see the prescription of the solid body velocity for all faces that lie within the MRF-zone. On these faces the solid body velocity is prescribed.

$$\mathbf{u}_{rot} = \boldsymbol{\omega} \times (\mathbf{r}_{face} - \mathbf{r}_{origin}) \quad (465)$$

```

1 void Foam::MRFZone::correctBoundaryVelocity(volVectorField& U) const
2 {
3     const vector Omega = this->Omega();
4     // Included patches
5     forAll(includedFaces_, patchi)
6     {
7         const vectorField& patchC = mesh_.Cf().boundaryField()[patchi];
8         vectorField pfld(U.boundaryField()[patchi]);
9         forAll(includedFaces_[patchi], i)
10        {
11            label patchFacei = includedFaces_[patchi][i];
12            pfld[patchFacei] = (Omega ^ (patchC[patchFacei] - origin_));
13        }
14        U.boundaryField()[patchi] == pfld;
15    }
16 }
```

Listing 594: The method `correctBoundaryVelocity` in the file `MRFZone.C`

Capabilities and limitations of the MRF approach

The MRF method in OpenFOAM deals only with rotations other than FLUENT, which is also capable of accounting for translational movement [9]. In both CFD softwares the velocity of the moving reference frame needs to be constant. This means OpenFOAM is capable of dealing with rotating reference frames that move with a constant angular velocity.

The boundary of the zone, in which the rotation of the frame of reference is active, must be oriented in a way, so that the velocity component of the reference frame's velocity normal to the boundary is zero. This means for a rotating frame of reference the zone in which this movement is acting needs to be a cylinder²⁹⁹ with its axis parallel to the axis of rotation of the reference frame.

The FLUENT theory manual says that the MRF method is strictly speaking only valid for steady state cases [9]. However, FLUENT offers this method for unsteady simulations too [9].

The sliding mesh technique gives more accurate results than the MRF method especially when it comes to transient simulations. However, the main advantage of the MRF method is its low impact on computational cost, compared to moving mesh techniques.

77.4.2 OpenFOAM-3.*

With OpenFOAM-3.0.0³⁰⁰ the MRF method was taken out from the `fvOptions` framework. The developers of OpenFOAM give the following reason for this mode:

fvOptions does not have the appropriate structure to support MRF as it is based on option selection by user-specified fields whereas MRF MUST be applied to all velocity fields in the particular solver. A consequence of the particular design choices in fvOptions made it difficult to support MRF for multiphase and it is easier to support frame-related and field related options separately.

Currently the MRF functionality provided supports only rotations but the structure will be generalized to support other frame motions including linear acceleration, SRF rotation and 6DoF which will be run-time selectable.

As noted in the cited message above, the MRF framework was also generalized. Thus, rotating reference frames are not limited to steady rotations anymore. Listing 595 shows how this change allows to spin-up reference frame rotation. This might improve numerical behaviour in the initial stages of the simulation.

²⁹⁹In fact the zone can be any volume defined by any surface of revolution of the rotational axis of the reference frame. However, the cylinder is the easiest and most convenient choice.

³⁰⁰<http://www.openfoam.org/version3.0.0/>

```
MRF1
{
    cellZone      rotor;

    active        yes;

    nonRotatingPatches ();

    origin        (0 0 0);
    axis          (0 0 1);

    omega         table
                  2(
                      (0   0.01)
                      (0.5 104.72)
                  );
}
```

Listing 595: Passing a table as angular velocity to the MRF framework.

Part X

Appendix

78 Useful Linux commands

78.1 Getting help

78.1.1 Display -help

Virtually all Linux commands display a summary of the programs purpose and usage. To display this message the command has to be invoked with one of those parameters: `-h`, `-help`, `--help`. If the wrong parameter is used the help message is displayed anyway or an error message naming the correct parameter to display the usage information, see Listing 596.

```
user@host:~$ ls -help
ls: invalid option -- e
Try 'ls --help' for more information.
user@host:~$
```

Listing 596: Displaying the help message

Apparently all of the tools and solvers of OpenFOAM³⁰¹ display such help messages. New Linux and OpenFOAM users are strongly encouraged to study the help messages to deepen their understanding and insight.

78.1.2 man pages

Many Linux commands have an additional, more detailed documentation³⁰². This is written in the *man* pages (*man* is short for manual). To display the *man* pages of a certain command, simply put the name of the command or program behind the command `man`. Listing 597 shows how to display the *man* pages of the Linux command `cp`.

```
man cp
```

Listing 597: Displaying the *man* pages

The *man* pages cover general commands of Linux, system call, library function of the C standard library and much more. On some systems the *man* pages are only partially or not at all installed by default.

78.2 Finding files

78.2.1 Searching files system wide

Searching for a file on the whole file system can be done by `locate`. Listing 598 shows the result of the search for the source file of `icoFoam`.

```
user@host:~/OpenFOAM/user-2.1.x/run/icoTurb$ locate icoFoam.C
/home/user/OpenFOAM/OpenFOAM-2.0.x/applications/solvers/incompressible/icoFoam/icoFoam.C
/home/user/OpenFOAM/OpenFOAM-2.1.x/applications/solvers/incompressible/icoFoam/icoFoam.C
```

Listing 598: Looking for *icoFoam.C*

78.2.2 In a certain directory

To find a file in a certain directory and its sub-directories `find` can be used. Listing 599 shows the command to search the file `LESProperties` in the OpenFOAM tutorials.

³⁰¹No exception is known to the author.

³⁰²As an example: the *man* pages of `gcc` are longer than 10000 lines.

```
find $FOAM_TUTORIALS -name LESProperties
```

Listing 599: Search *LESProperties* in the tutorials

78.3 Find files and scan them

How do I define probes? I have seen this already, but where?

To answer this question one has to find all files in which *probes* can be defined – the *controlDict* in this case. Additionally, all of the files returned by the search have to be scanned for the definition of *probes*. As an OpenFOAM case consists of a number of text files, it is easy to scan these files for certain keywords. So, the answer to the question above is: find all *controlDicts* and scan them for the word *probe*.

Instead of performing this task manually, a single one-liner in the Terminal does the magic. Listing 600 shows how all files named *controlDict* in the tutorials are located and scanned for the word *probes*.

```
find $FOAM_TUTORIALS -name controlDict | xargs grep 'probes' -sl
```

Listing 600: Find and scan files

find looks for respectively finds all files with the name passed with the option **-name** in the specified folder and its folders. *xargs* executes the passed command line. The output of *find* is passed to *grep* as input by a pipe. *grep* then scans all files for the word *probes*.

git it done the other way

If OpenFOAM is installed from a *git* source code repository, we can also use *git* to search for patterns. Here, all (tracked) files are searched for the provided pattern. The reason for using *git*, is that *git* tracks file content in a very efficient way. Thus searching is generally faster, especially if we scan a lot of files. E.g. if we want to know where in the sources **VGREAT** is defined.

In the case of the example above, we would need to go to the tutorials directory and then tell *git* to search for the pattern “*probes*”. This causes an overall search, which is not limited to *controlDicts*. In fact, we find also some clean-up scripts.

```
cd $FOAM_TUTORIALS  
git grep probes
```

Listing 601: Scan files using *git grep*

78.4 Scan a log file

grep can scan a text file for a certain pattern. In this example we want to scan the solver output for a certain pattern. The solver *twoPhaseEulerFoam* displays after every time step the minimum and maximum value of the volume fraction α . For α to be physically meaningful, its value has to be of the range $0 \leq \alpha \leq 1$.

In this example a simulation crashed and the main suspicion is, that there were values of α greater than one. Listing 602 shows two lines of solver output. The first line has a maximum value of one. In some cases, when regions evolve where the continuous phase vanishes, e.g. above a water surface, this value is perfectly reasonable. The second line comprises a maximum value of α greater than unity. This value is unphysical, because a phase can not occupy a certain amount of space – a cell – to more than 100%.

Due to the fact that simulations often do not crash immediately the log file containing the solver output is hundreds of thousands of lines long. To look for maximum values of α greater than unity manually is not an option. We need an one-liner that does that automatically for us. That's where *grep* comes in.

```
Dispersed phase volume fraction = 0.194351 Min(alpha) = 7.52826e-42 Max(alpha) = 1  
Dispersed phase volume fraction = 0.060562 Min(alpha) = 2.30261e-52 Max(alpha) = 1.00003
```

Listing 602: Example: solver output regarding volume fraction

Listing 603 shows how the user can scan the log file for the appropriate pattern. grep expects as first argument the pattern to look for. The second argument is optional, it specifies the file from which to read. If no file was specified, grep would read from standard input. The option `-c` makes grep display only the number of number of matches. Otherwise, grep would display all lines in which a match was found. In a situation in which the number of hits could reach hundreds or thousands, displaying all lines with a match could be unwise.

The first command in Listing 603 would detect a match for both lines of Listings 602. So this pattern '`Max(alpha) = 1`' is not useful to find out whether α exceeded unity or not.

The second command in Listing 603 will only detect lines in which α is larger than unity. So, of the two lines of Listings 602, only the second one would result in a match.

```
grep 'Max(alpha) = 1' foamRun.log -c
grep 'Max(alpha) = 1.' foamRun.log -c
```

Listing 603: Scan the log using *grep*

78.5 Running in scripts

78.5.1 Starting a batch of jobs

To use the computing power of a computing cluster it is a good idea to let the cluster do the work in batches. To be able to do this, this section explains how to use a script to run a number of simulations sequentially. So, the cluster can calculate a great number of cases without the need for the user to start each job separately. This would be unacceptable when simulating overnights.

The script in Listing 604 starts two parallel simulations including domain decomposition and reconstruction. The script assumes to start from a directory which contains all two cases. The first group of commands changes into a subdirectory of the current directory (`cd './fullColumn_fineV01'`). The next commands perform all tasks of a parallel simulation. Then the script changes to the second case (`cd '../fullColumn_fineV02'`).

This is a very basic script. It contains no checks if a simulation has terminated prematurely or any other useful features.

```
#!/bin/bash
# fine 01

echo 'fine01'
cd './fullColumn_fineV01'

echo 'decomposing'
decomposePar > foamDecompose.log

mpirun -np 2 twoPhaseEulerFoam -parallel > foamRun.log

echo 'reconstructing'
reconstructPar > foamReconstruct.log

# fine 02
echo 'fine02'
cd '../fullColumn_fineV02'

echo 'decomposing'
decomposePar > foamDecompose.log

mpirun -np 2 twoPhaseEulerFoam -parallel > foamRun.log

echo 'reconstructing'
reconstructPar > foamReconstruct.log
```

Listing 604: Using a shell script to start several simulations.

78.5.2 Terminating a running script

There may be need to stop a script from any further execution without terminating the currently running simulation. This example assumes that a script with name `runCalculations` is to be terminated. First the PID

of *runCalculations* has to be known. In Section 12.3.2 explains this bit in detail. Listing 604 shows how to look for the PID. The command in Listing 604 outputs two lines. The first line comes from the running script and the second line stems from the running parallel calculation. This is because all running processes matching the pattern `run` were searched for. Therefore, also the running instance of `mpirun` was found.

```
user@host:~$ ps -el | grep run
0 S 8553 14913 14517 0 80 0 - 2687 wait pts/11 00:00:00 runCalculations
0 S 8553 14917 14913 0 80 0 - 2687 wait pts/11 00:00:00 mpirun
user@host:~$
```

Listing 605: Search for PIDs using *ps* and *grep*

Terminate the script

If the script was terminated using `kill`, then the simulation would continue unaffected. Listing 606 shows how the script is terminated and `mpirun` continues to be running.

```
user@host:~$ ps -e | grep run
14913 pts/11 00:00:00 runCalculations
14917 pts/11 00:00:00 mpirun
user@host:~$ kill -KILL 14913
user@host:~$ ps -e | grep run
14917 pts/11 00:00:00 mpirun
```

Listing 606: Use *kill* to stop a shell script.

Terminate the script and the simulation

To terminate both the script and the simulation – in this example – the running simulation has to be terminated also. Terminating only the running simulation only, will cause the script to execute the next command. So, first the script and then the simulation need to be terminated.

78.6 diff

`diff` is a command line tool that analyses two files and prints a summary of the differences of those files. Further information on `diff` can be found in the man-pages or the help-message.

78.6.1 Meld

Meld is a graphical front-end to `diff`. This allows for a side-by-side comparison of both files under investigation. Parts of the file that differ are highlighted by colors. For more information about *Meld* see <http://meldmerge.org/>.

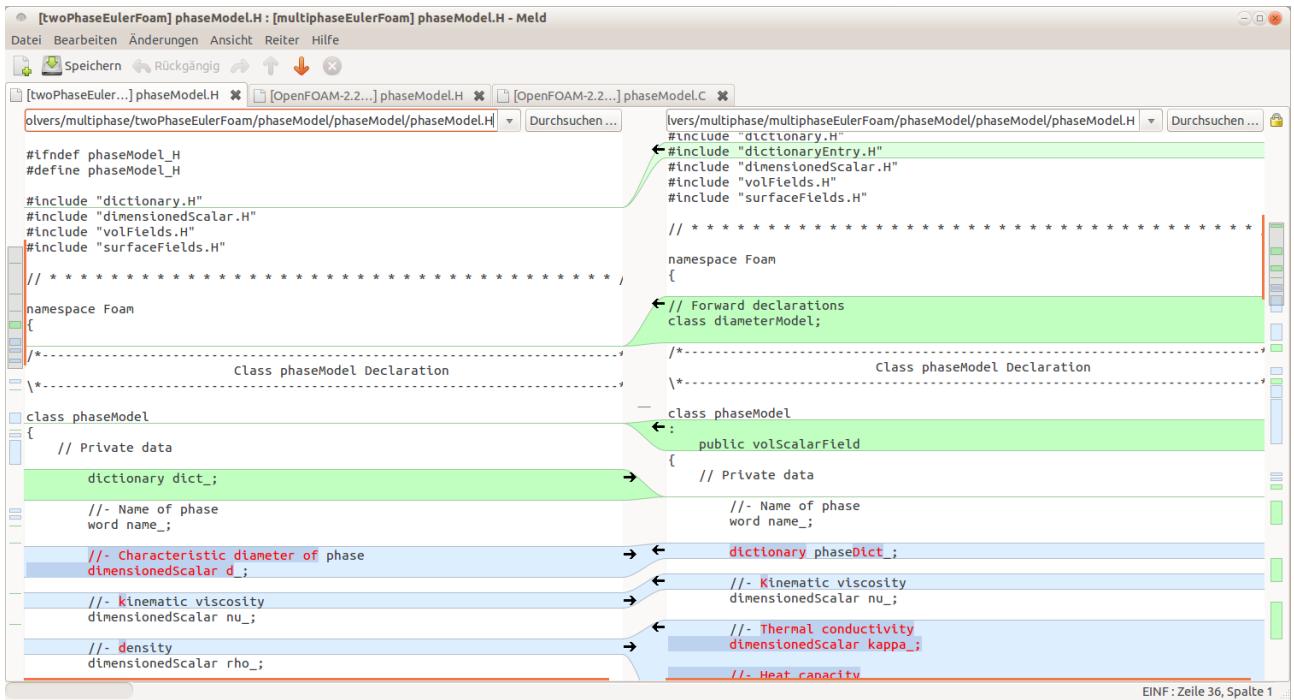


Figure 194: A screenshot of *Meld*

78.7 Case setup

There are a lot of tasks when setting up a case. Even though we might use a tutorial case as a starting point, a lot of tedious work might lie ahead of us. Computers are better at certain tasks than we humans [[Citation needed](#)].

Thus, we might be better off automating boring tasks. The pyFoam library is a good collection of useful stuff. However, certains tasks are done by mere one-liners in Linux. This is what this section is about.

78.7.1 Renaming files

The current mult-phase solvers use a naming scheme in which the name of the phase determines the file's extension. Thus, the thermophysical properties of the phase air are stored in the file `thermophysicalProperties.air`. This causes in certain cases the need to rename a number of files, because we use argon as gaseous phase and we want to comply with the naming scheme. The dirty hack would be to just exchange the properties of air with those of argon without changing the naming of the phase.

In Linux there are many ways to perform this sort of task. For mere text substitution a solution based on regular expressions is the way to go. Listing 607 shows how the command `rename` is used to rename all files containing a certain text.

```
rename 's/air/argon/g' ./*
```

Listing 607: Change the extension of all files having the extension `air` to `argon`.

78.8 Miscellaneous

This section contains references to useful scripts or commands explained elsewhere in this document.

Terminate a background process

See Section [12.3.2](#).

Delete the *processor** directories

If one or several simulations have been conducted on a computing cluster, it makes sense so reconstruct the domain on the cluster. Otherwise the workstation of the user would be blocked for the time needed to complete reconstruction. After reconstructing the domain the *processor** directories still contain all the time step data. If the *processor** folders are deleted on the cluster, the user can afterwards copy the whole case directory to the workstation without transmitting the solution data twice.

See Section [12.5.2](#) for how to deal with *processor** directories.

Redirect output

Redirecting the output of a program is explained in Section [12.1.1](#).

79 Archive data

Parametric studies generate a great deal of data. After the post-processing is done all files could be compressed to save disk space. On Linux systems the *tar* archiving utility may be the agent of choice. The name *tar* comes from *tape archive*, which is pretty descriptive in terms of the origins of this archiving program. A *tar* archive is a single file which contains all archived files and folders. This step alone is only a reorganisation of the data, fit for the usage of sequential data storage devices like magnetic tapes.

In a second step the tar archive needs to be compressed. For this task there are many possible choices. Linux systems usually provide programs like gzip, bzip2 or xz. The distinction between archiving and compressing is probably for historical as well as practical reasons. There is also one paradigm of the UNIX philosophy (*Make each program do one thing well*) which supports the segregation in archiving and compression. The compression programs usually differ in the utilised compression algorithms. There is one rule of thumb stating: The more data is to be compressed, the longer compression takes.

Table 11 lists the achieved compression of a parametric studies with 21 cases totalling in 50 GB of data. The data was written in ascii format. Compressing the data resulted in a 70+ % reduction of used disk space. If space consuming cases are to archived, slow algorithms that result in good compression rates should be preferred.

	used disk space	reduction
21 cases uncompressed	50 GB	
compressed: *.tar.bz2	13.7 GB	36.3 GB - 72.6 %

Table 11: Comparison of disk space reduction

Archive log files

In this example log files are archived. In this case the same algorithm achieves an even greater reduction of disk space usage. This example shows that the achieved compression rate strongly depends on the input data.

	used disk space	reduction
16 log files uncompressed	2.0 GB	
compressed: *.tar.bz2	154.7 MB	1.85 GB - 92.3 %

Table 12: Comparison of disk space reduction

Yet another compression comparison

When archiving OpenFOAM cases, the mesh generation may be very convoluted or time consuming. So it might be preferable to archive the mesh generation separately from the actual case. Thus, for the actual case we might want to include the final mesh and do not bother with mesh creation.

This section compares how three compression tools perform on a Linux system when compressing a mesh. The mesh in question was created by *blockMesh* and certain files are in binary format.

Listing 608 shows the actual command that were used to compress the mesh.

```
tar -cv polyMesh | gzip --best > polyMesh.tar.gz
tar -cv polyMesh | bzip2 --best > polyMesh.tar.bz
tar -cv polyMesh | lzma -9 > polyMesh.tar.xz
```

Listing 608: Compressing the mesh with various tools; note the setting for maximum compression

Listing 609 shows the sizes of the original mesh and its compressed forms. The used compression algorithms differ considerably. Compression was performed with the setting for best compression, the time it took for each tool to compress the mesh was not recorded. However, the stronger the compression the more time it takes to compress. Since for archiving purposes disk space is the limiting factor, we chose maximum compression.

```
user@host:~$ du -sh polyMesh*
23M polyMesh
5,3M polyMesh.tar.bz
6,2M polyMesh.tar.gz
2,6M polyMesh.tar.xz
```

Listing 609: Comparing the disk usage of a mesh and its various compressions

From the comparison in Listing 609 we see that the LZMA compression algorithm achieves the best compression, followed by BZIP2 and GZIP. All three compression algorithms are widely available in the UNIX world in the form of open source implementations.

The effects of renumbering and/or writing binary

When playing around with various ways to archive an existing mesh, something quite interesting has been observed: the archive file-size differs whether the mesh had been renumbered or not. Note that this comparison only deals with archiving the mesh, no solution data (i.e. fields) have been archived alongside the mesh.

In Table 13 we compare the resulting file size of an archive of a reasonable complex, all-hex mesh with 147262 cells. The required disk space of the mesh itself only differs between writing in ascii or binary format. Renumbering the mesh does not have an effect, which is not surprising, since renumbering does not add or remove information. Thus, the required disk space of the mesh should not change due to renumbering.

When it comes to archiving the mesh, however, renumbering certainly has an effect on the resulting file size of the archive. Compressing the *as-is*³⁰³ mesh yields only a slightly smaller archive, when the mesh was written in binary format to disk. The big surprise, however, is when we compare the resulting archive file size for the renumbered mesh. In both cases, ascii and binary, the compressed, renumbered mesh results in a larger archive file size than the compressed, *as-is* mesh.

The mesh	ascii	binary	The archive	ascii	binary
as-is	22M	16M	as-is	1,7M	1,6M
renumbered	22M	16M	renumbered	2,5M	2,0M

Table 13: Comparing the resulting file size of the mesh archive file for various conditions/treatments. All file or folder sizes were determined with the Linux command `du -sh FILE`. The mesh was compressed using the LZMA algorithm at maximum compression: `tar -cv constant/polyMesh | lzma -9 > polyMesh.tar.xz`.

We can draw two conclusions from this comparison. The most obvious is, that writing data in binary format is always favourable over writing in ascii format, especially for uncompressed data. Writing in ascii should only be used for trouble-shooting. In production, binary is definitely the format of choice. Writing in binary not only saves disk space in storage, it also provides the maximum read/write precision, since all relevant bits of each numerical value are stored. In contrast, writing in ascii format only writes a finite number of significant bits.

The second conclusion we can draw from the comparison above, is not to store the renumbered mesh. Even if renumbering would/does³⁰⁴ not increase archive file size, renumbering is an operation we can easily perform prior to our simulation. The time it takes to renumber the mesh is negligible compared to the overall simulation time. Thus, we advise to archive meshes in an un-renumbered state. This, in addition to potential savings on storage, gives future users the choice whether to run the simulation on a renumbered mesh or not. On an already renumbered mesh it is impossible to determine the benefits of renumbering the mesh with respect to simulation time or convergence. An operation which can always be performed at demand does not need to be archived.

³⁰³We denote the state of the mesh after mesh-creation by the term *as-is* in order to distinguish it from the renumbered state. Mesh creation consists of a call to *blockMesh*, extruding a patch and finally removing parts of the mesh with *subsetMesh*. After these steps, any sets of points, faces or cells are deleted. Also zones of any kind have not been defined. Thus, *as-is* denotes the final, minimal mesh.

³⁰⁴One case of renumbering causing larger archive file sizes does not necessarily mean that this will always cause this effect.

References

- [1] Intel 64 and IA-32 Architectures Optimization Reference Manual.
- [2] Viscosity of gases. In David R. Lide, editor, *CRC Handbook of Chemistry and Physics*. CRC Press, 2005.
- [3] The International System of Units, 2006. URL www.bipm.org/en/si/si_brochure.
- [4] The International System of Units (SI), 2008. URL <http://physics.nist.gov/Pubs/SP330/sp330.pdf>.
- [5] A. Alexandrescu. *Modern C++ Design: Generic Programming and Design Patterns Applied*. Addison Wesley, 2001.
- [6] J. D. Anderson. *Computational Fluid Dynamics*. McGraw-Hill International Editions, 1995.
- [7] E. D. C. Andrade. A theory of the viscosity of liquids. - Part I. *The London, Edinburgh, and Dublin Philosophical Magazine and Journal of Science*, 17(113):698–732, 1934.
- [8] E. D. C. Andrade. A theory of the viscosity of liquids. - Part II. *The London, Edinburgh, and Dublin Philosophical Magazine and Journal of Science*, 17(112):497–511, 1934.
- [9] Inc. ANSYS. *FLUENT Theory Guide*, 14.5 edition, 2012.
- [10] ANSYS, Inc. *ANSYS CFX-Solver Theory Guide*, 14.0 edition, November 2011.
- [11] N. G. Deen B. Niceno, M. T. Dhotre. One-equation sub-grid scale (sgs) modelling for euler-euler large eddy simulation (eeles) of dispersed bubbly flow. *Chemical Engineering Science*, 63:3923–3931, 2008.
- [12] A. Behzadi, R. I. Issa, and H. Rusche. Modelling of dispersed bubble and droplet flow at high phase fractions. *Chemical Engineering Science*, 59:759–770, 2004.
- [13] J. Boussinesq. Théorie de l’Écoulement tourbillant. *Mem. Présentés par Divers Savants Acad. Sci. Inst. Fr.*, 23:46–50, 1877.
- [14] Daniel Brennan. *The Numerical Simulation of Two-Phase Flows in Settling Tanks*. PhD thesis, Imperial College of Science, Technology & Medicine, 2001.
- [15] A. Burcat and B. Ruscic. Third millennium ideal gas and condensed phase thermochemical database for combustion and updates from active thermochemical tables. Technical report, Argonne National Laboratory, 2005.
- [16] N. Böcker, M. Grahl, A. Tota, P. Häussinger, P. Leitgeb, and B. Schmücker. *Ullmann’s Encyclopedia of Industrial Chemistry*, chapter Nitrogen. Wiley-VCH Verlag GmbH & Co. KGaA, 2013.
- [17] Yunus A. Çengel. *Heat Transfer - a practical approach*. McGraw-Hill, second edition, 2003.
- [18] S. Chapman and T. G. Cowling. *Mathematical theory of non-uniform gases*. Cambridge University Press, 1952.
- [19] C. P. Dahl. *Numerical modelling of flow and settling in secondary settling tanks*. PhD thesis, Aalborg University, Denmark, 1993.
- [20] J.-M. Delhaye. Some issues related to the modeling of interfacial areas in gas-liquid flows I. the conceptual issues. *Comptes Rendus de l’Académie des Sciences - Series {IIB} - Mechanics*, 329(5):397–410, 2001.
- [21] M. T. Dhotre and J. B. Joshi. CFD simulation of heat transfer in turbulent pipe flow. *Industrial & Engineering Chemistry Research*, 43:2816–2829, 2004.
- [22] Eric S. Raymond. *The Art of UNIX Programming*. Addison-Wesley, 2003.
- [23] A. Eucken. Über die temperaturabhängigkeit der wärmeleitfähigkeit einiger gase. *Physikalische Zeitschrift*, 12(24):1101–1107, 1911.
- [24] A. Eucken. Über das wärmeleitvermögen, die spezifische wärme und die innere reibung der gase. *Physikalische Zeitschrift*, 14(8):324–331, 1913.

- [25] Agner Fog. Optimizing software in c++. Technical report, Technical University of Denmark, 2014.
- [26] J. Fröhlich. *Large Eddy Simulationen turbulenter Strömungen*. Teubner, 2006.
- [27] E. Peirano & A.-E. Almstedt H. Enwald. Eulerian two-phase flow theory applied to fluidization. *Int. J. Multiphase Flow*, 22:21–66, 1996.
- [28] David P. Hill. *The computer simulation of dispersed two-phase flows*. PhD thesis, Imperial College of Science, Technology and Medicine, 1998.
- [29] C. L. Hogan and R. B. Sawyer. The thermal conductivity of mmetal at high temperature. *Journal of Applied Physics*, 23(2):177–180, 1952.
- [30] B. Holenda, I. Pásztor, Á. Kárpáti, and Á Rédey. Comparison of one-dimensional secondary settling tank models. Technical report, European Water Association (EWA), 2006.
- [31] J. R. Howell, R. Siegel, and Mengüç. *Thermal Radiation Heat Transfer*. CRC Press, fifth edition, 2010.
- [32] M. Ishii. One-dimensional drift-flux-model and constitutive equations for relative motion between pphase in various two-phase flow regimes. Technical report, Argonne National Laboratory, 1977.
- [33] M. Ishii and T. Hibiki. *Thermo-Fluid Dynamics of Two-Phase Flow*. Springer, 2nd edition, 2011.
- [34] M. Ishii, S. Kim, and J. Uhle. Interfacial area transport equation: model development and benchmark experiments. *International Journal of Heat and Mass Transfer*, 45:3111–3123, 2002.
- [35] M. Ishii, S. Kim, and J. Kelly. Development of interfacial area transport equation. *Nuclear Engineering and Technology*, 37(6):525–536, 2005.
- [36] R. I. Issa. A simple model for c_t . Private Communications, 1992. see Hill [28].
- [37] M. Peric J. H. Ferzinger. *Computational Methods for Fluid Dynamics*. Springer, 2002.
- [38] Hrvoje Jasak. *Error Analysis and Estimation for the Finite Volume Method with Applications to Fluid Flows*. PhD thesis, Imperial College of Science, Technology & Medicine, 1996.
- [39] Brian W. Kernighan and Dennis M. Ritchie. *The C Programming Language*. Prentice Hall, Inc., 2nd edition, 1988.
- [40] S. Kim, X. Sun, M. Ishii, S. G. Beus, and F. Lincoln. Interfacial area transport and evaluation of source and sink terms for confined air-water bubbly flow. *Nuclear Engineering and Design*, 219:61–75, 2002.
- [41] G. Kocamustafaogullari and M. Ishii. Foundation of the interfacial area transport equation and its closure relations. *Int. J. Heat Mass Transfer*, 38(3):481–493, 1995.
- [42] Fabian Peng Kärrholm. *Numerical Modelling of Diesel Spray Injection, Turbulence Interaction and Combustion*. PhD thesis, Chalmers University of Technology, Göteborg, Sweden, 2008.
- [43] Y. Liu, T. Hibiki, and M. Ishii. Modeling of interfacial area transport in two-phase flows. In *Advances in Multiphase Flow and Heat Transfer*, volume 4, chapter 1, pages 3–27. Bentham Science Publishers, 2012.
- [44] Alejandro López. Lpt for erosion modeling in openfoam – differences between solidparticle and kinematicparcel, and how to add erosion modeling. Technical report, Chalmers University of Technology, 2014. URL http://www.tfd.chalmers.se/~hani/kurser/OS_CFD_2013/AlejandroLopez/LPT_for_erosionModelling_report.pdf.
- [45] G. B. Macpherson, N. Nordin, and H. G. Weller. Particle tracking in unstructured, arbitrary polyhedral meshes for use in cfd and molecular dynamics. *Communications in Numerical Methods in Engineering*, 25: 263–273, 2009.
- [46] Holger Marschall. *Towards the Numerical Simulation of Multi-Scale Two-Phase Flows*. PhD thesis, Technische Universität München, 2011.
- [47] M. Milelli. *A numerical analysis of confined turbulent bubble plumes*. PhD thesis, Swiss Federal Institute of Technology Zurich, 2002.

- [48] Hakan Nilsson. Turbomachinery training at ofw8. Technical report, Chalmers University of Technology, Gothenburg, Sweden, 2013.
- [49] Niklas Nordin. *Complex Chemistry Modeling of Diesel Spray Combustion*. PhD thesis, Chalmers University of Technology, 2009.
- [50] International Union of Pure and Applied Chemistry. Iupac compendium of chemical terminology – the gold book, 2014. URL <http://goldbook.iupac.org/>.
- [51] *OpenFOAM - Programmer's Guide*. OpenFOAM Foundation, 2.1.0 edition, 2011.
- [52] *OpenFOAM - User Guide*. OpenFOAM Foundation, 2.1.0 edition, 2011.
- [53] D. Pfleger and S. Becker. Modelling and simulation of the dynamic flow behaviour in a bubble column. *Chemical Engineering Science*, 56:1737–1747, 2001.
- [54] B. E. Poling, J. M. Prausnitz, and J. P. O'Connell. *The Properties of Gases and Liquids*. McGraw-Hill, fifth edition edition, 2000.
- [55] S. P. Pope. *Turbulent Flows*. Cambridge University Press, 2000.
- [56] Henrik Rusche. *Computational Fluid Dynamics of dispersed two-phase flows at high phase fractions*. PhD thesis, Imperial College of Science, Technology & Medicine, 2002.
- [57] Y. Sato and K. Sekoguchi. Liquid velocity distribution in two-phase flow. *International Journal of Multiphase Flow*, 2:79–95, 1975.
- [58] J. Smagorinsky. General circulation experiments with the primitive equations; i. the basic experiment. *Monthly Weather Review*, 91:99, 1963.
- [59] Bjarne Stroustrup. *The C++ Programming language*. Addison-Wesley, 4th edition, 2013.
- [60] William Sutherland. Lii. the viscosity of gases and molecular force. *The London, Edinburgh, and Dublin Philosophical Magazine and Journal of Science*, 36(223):507–531, 1893.
- [61] Imre Takács. *Experiments in Activated Sludge Modelling*. PhD thesis, Ghent University, Belgium, 2008.
- [62] D. G. Thomas. Transport characteristics of suspension: VIII. a note on the viscosity of Newtonian suspensions of uniform spherical particles. *Journal of Colloid Science*, 1965.
- [63] A. Tomiyama, I. Kataoka, T. Fukuda, and T. Sakaguchi. Drag coefficients of bubbles. 2nd report. drag coefficient for a swarm of bubbles and its applicability to transient flow. *Nippon Kikai Gakkai Ronbunshu*, 61(588):2810–2817, 1995.
- [64] VDI-Gesellschaft Verfahrenstechnik und Chemieingenieurwesen (GVC). Thermophyscial properties. In *VDI Heat Atlas*. Springer, 2010.
- [65] Berend van Wachem. *Derivation, implementation and validation of computer simulation models for gas-solid fluidized beds*. PhD thesis, Delft University of Technology, 2000.
- [66] H. K. Versteeg and W. Malalasekera. *An introduction to computational fluid dynamics – the finite volume method*. Longman Scientific & Technical, 1995.
- [67] A. Vesilind. Design of prototype thickeners from batch settling tests. *Water Sewage Works*, 115(5):302–307, 1968.
- [68] H. G. Weller, G. Tabor, H. Jasak, and C. Fureby. A tensorial approach to computational continuum mechanics using object-oriented techniques. *Computers in Physics*, 12:620–631, 1998.
- [69] David C. Wilcox. *Turbulence Modelling for CFD*. DCW Industries, Inc., 1994.
- [70] M. L. Williams, R. F. Landel, and J. D. Ferry. The temperature dependence of relaxation mechanisms in amorphous polymers and other glass-forming liquids. *Journal of the American Chemical society*, 77(14):3701–3707, 1955.
- [71] D. Zhang, N. G. Deen, and J. A. M. Kuipers. Numerical simulation of the dynamic flow behaviour in a bubble column: A study of closures for turbulence and interface forces. *Chemical Engineering Science*, 61:7593–7608, 2006.

Nomenclature

ACMI	Arbitrary Coupled Mesh Interface	LZMA	Lempel-Ziv-Markov chain algorithm
AMI	Arbitrary Mesh Interface	MPI	message passing interface
ASCII	American Standard Code for Information Interchange	MRF	multiple reference frame
BC	boundary condition	OO	object-oriented
BIT	Bubble induced turbulence	OOD	object-oriented design
CAD	computer aided design	OOP	object oriented programming
CFD	Computational fluid dynamics	OS	operating system
CG	Conjugate gradient	PDE	Partial differential equation
DO	discrete ordinates	Perl	An interpreted programming language
DPE	Dispersed phase element	PID	process identifier
EDF	Électricité de France	PIMPLE	An algorithm based on PISO and SIMPLE algorithm
FIFO	A data structure following the "First In, First Out" principle	PISO	Pressure Implicit with Split Operator
FPE	Floating-point exception	POSIX	Portable Operating System Interface
FVM	Finite volume method	RAS	Reynolds averaged simulation
GAMG	Geometric algebraic multi-grid	RHS	Right hand side
GCC	GNU compiler collection	RNG	random number generator
gcc	GNU compiler collection	RTD	residence time distribution
GNU	GNU is not Unix	SAT	Standard ACIS Text
GUI	graphical user interface	SI	Le Système Internationale d'Unités
I/O	input and output	SIMPLE	Semi-Implicit Method for Pressure-Linked Equations
IATE	Interfacial area transport equation	SOI	start of injection
IGES	Initial Graphics Exchange Specification	STL	Surface Tesselation Language
IT	Information technology	UNIX	an operating system; ancestor of many modern operating systems, e.g. all kinds of Linux, Mac OS X.
LES	Large eddy simulation	VOF	Volume of fluid
LPT	Lagrangian Particle Tracking		