

No.4: Uncertainty quantification in an oil plume model.

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Introduction

Uncertainties

Flow rates: **5,000** barrels/day (first released report); **50,000-70,000** barrels/day (McNutt et al. 2012)

Gas to oil ratio (GOR): **1600** $\text{ft}^3/\text{barrel}$, **2470** $\text{ft}^3/\text{barrel}$, **3000** $\text{ft}^3/\text{barrel}$ (Valentine et al. 2010; Reddy et al. 2012)

Other parameters: Oil droplet/gas bubble initial distribution, entrainment coefficients, etc.

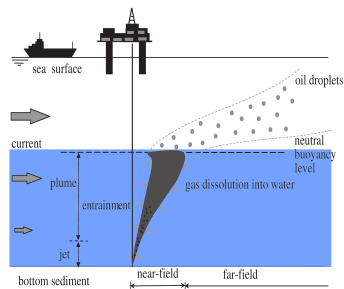


Figure : Modified from Li Zheng et al. 2003

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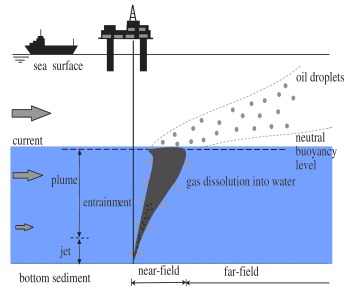
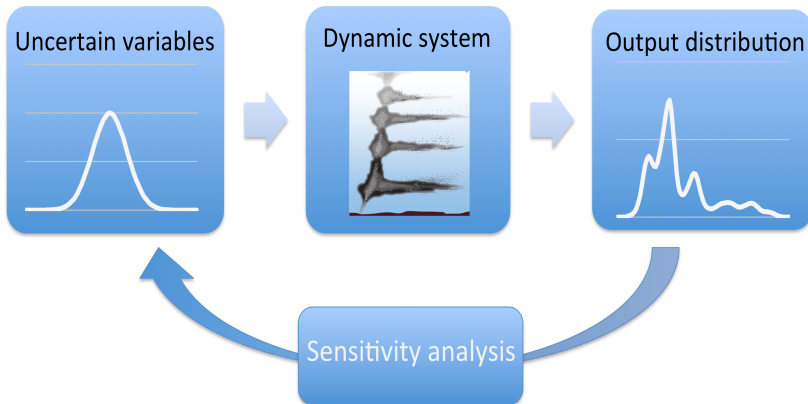


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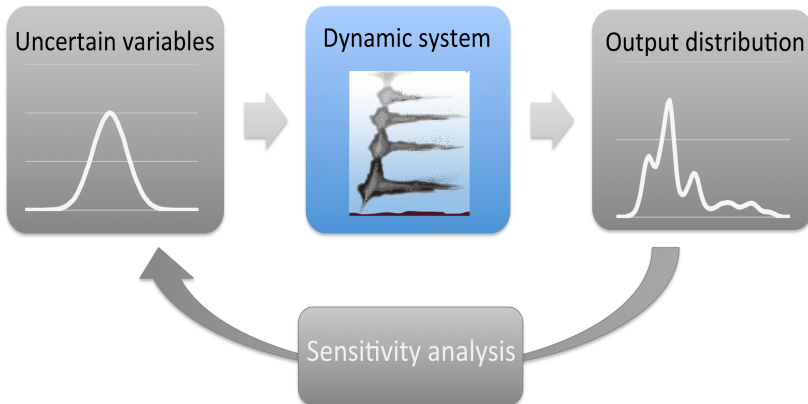
Goal

Assess how uncertainties of inputs of an oil plume model manifest in its outputs.

Uncertainty propagation



Uncertainty propagation: model & methods



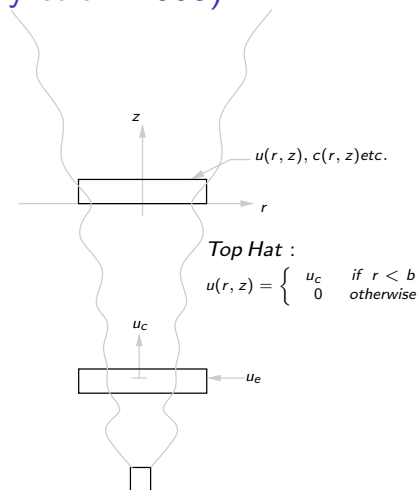
Integral plume model (Socolofsky et al. 2008)

Self similarity assumption

$$Q(z) = 2\pi \int_0^\infty u(r, z) r dr = \pi b^2(z) u(z)$$

$$M(z) = 2\pi \int_0^\infty u^2(r, z) r dr = \pi b^2 u^2$$

Variables have similar lateral profiles at different plume heights.



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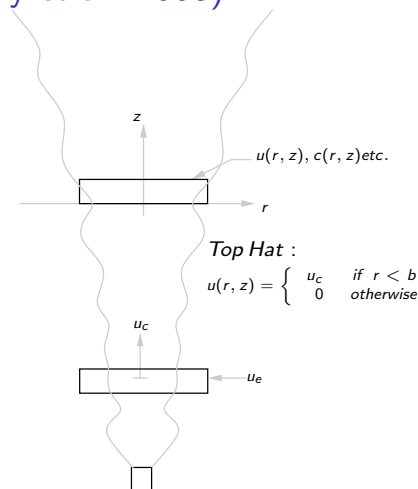
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Entrainment hypothesis

$$u_e = \alpha u_c$$

The entrainment velocity u_e is proportional to the central velocity u_c .



Integral plume model (Socolofsky et al. 2008)

Model descriptions

- Stratification dominated (*DWH*, Camilli et al. 2010, Socolofsky et al. 2011)
- Double-plume approach

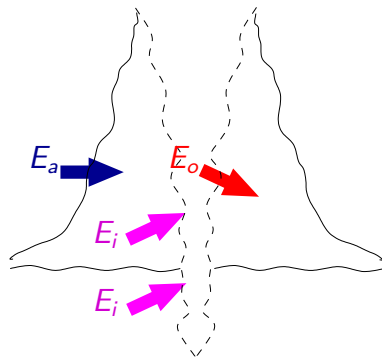


Figure : Entrainment processes using double-plume approach

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Primary processes

- Buoyancy force
- Turbulent entrainment
- Buoyant detrainment
- Dissolution of the gas bubbles

(Crounse et al. 2007)

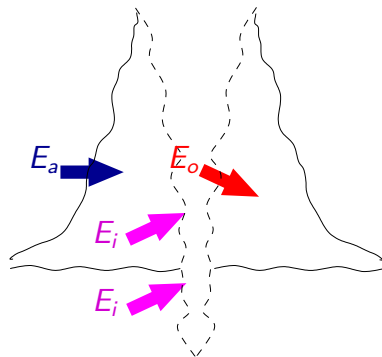
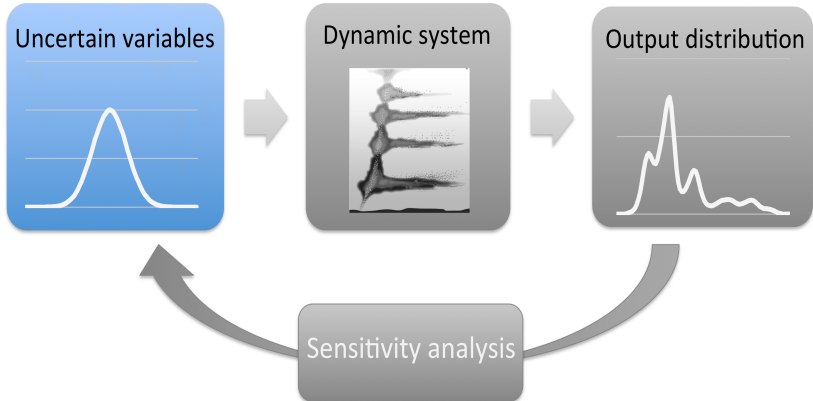


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Uncertainty propagation: uncertain variables



Uncertainty parameters

Parameter	Distribution	Random variable
Entrainment coefficient	$U(0.06, 0.116)$	$\xi_1 \sim U(-1, 1)$
Entrainment ratio	$U(0.4, 0.6)$	$\xi_2 \sim U(-1, 1)$
Gas-to-oil ratio	$U(1600, 3000)$	$\xi_3 \sim U(-1, 1)$
95th percentile of the droplet/bubble size (D_{95})	$U(7, 10)$	$\xi_4 \sim U(-1, 1)$
Droplet distribution spreading ratio	$U(1.8, 4)$	$\xi_5 \sim U(-1, 1)$

Quantities of interest

Trap height, peel height and mass flux of different gas bubble sizes.

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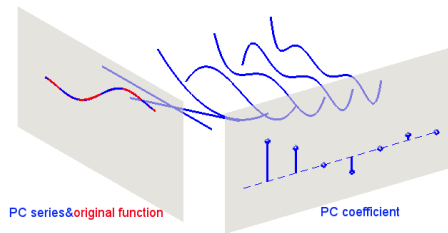
Uncertainty propagation

Monte-Carlo method requires over tens of thousands of simulations, how to speed up?

Polynomial Chaos Expansion (PCE)

Polynomial chaos (Wiener 1938)

$y(\xi) \approx y_P = \sum_{k=0}^P \hat{y}_k \psi_k(\xi)$ is a spectral type expansion in the **uncertain** variables ξ . Once the coefficients \hat{y}_k are determined, the series can be analyzed for probabilistic and approximation information.

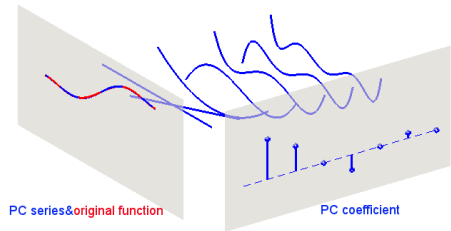


PC series with Legendre polynomials

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PC series with Legendre polynomials

Determine the coefficients

Non-intrusive Galerkin projection (integrals) in ξ -space:

$$\hat{y}_k = \frac{\langle y(\xi), \psi_k(\xi) \rangle}{\langle \psi_k^2(\xi) \rangle} \approx \frac{\sum_{q=1}^Q y(\xi_q) \psi_k(\xi_q) \mathbf{w}_q}{\langle \psi_k^2(\xi) \rangle}$$

Gaussian Process Regression (GPR)

Gaussian Process Regression

$$\mathcal{M}(x) \approx \mathcal{M}^{(\mathcal{GP})}(x) = \beta^T \cdot f(x) + \mathcal{GP}(0, k(x, x'; \theta))$$

$\mathcal{GP}(0, k(x, x'; \theta))$ is a zero mean Gaussian process, $\beta^T \cdot f(x)$ is the mean value of the Gaussian process, β is a set of coefficients and $f(x)$ is a set of basis functions for the mean function.

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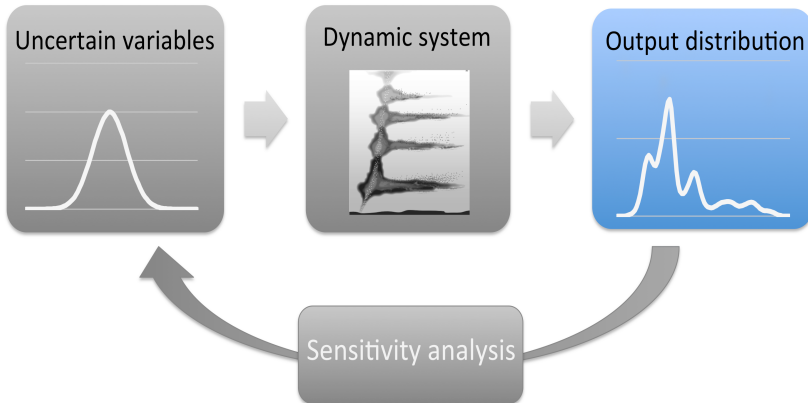
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Determine the GPR emulator

The hyper-parameters, θ , in the covariance function $k(x, x'; \theta)$ and the β need to be estimated from a training set via maximum likelihood method.

Uncertainty propagation: output statistics



Probability density function (PDF) comparison

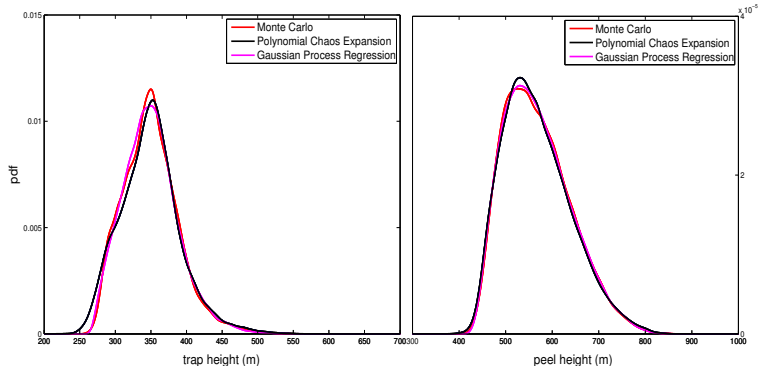


Figure : Monte-Carlo method needs 50,000 model simulations (about 30,000 CPU hours). Emulator-type methods need less than 1,000 model simulations, which decrease computation time by a factor of **50**.

Fluorescence

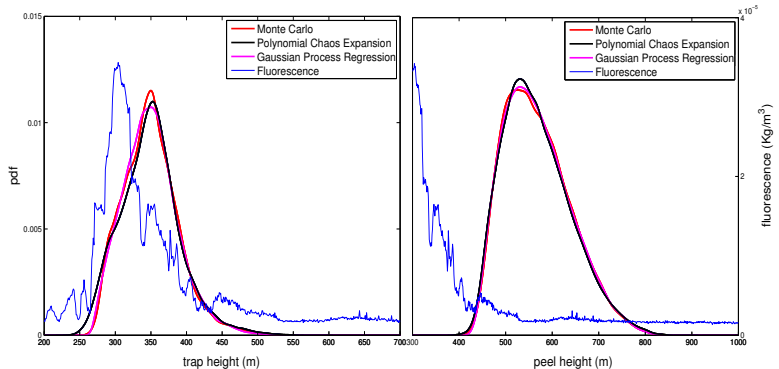


Figure : Fluorescence intensity (a proxy for oil concentration) in blue from the R/V Brooks McCall on May 30, 2010 (Socolofsky 2011).

Gas bubble distribution

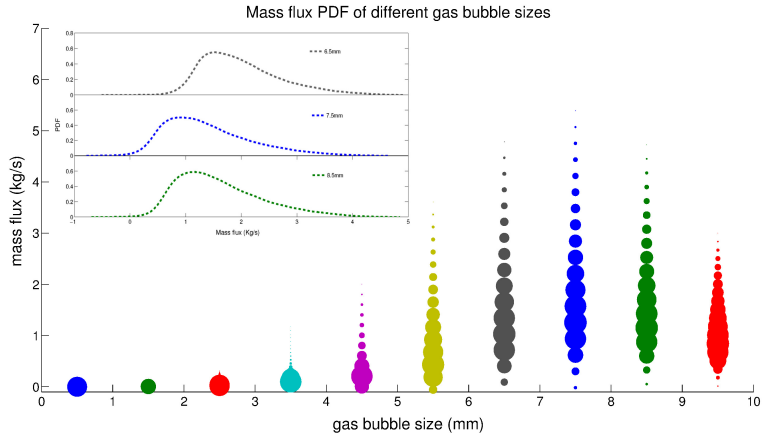
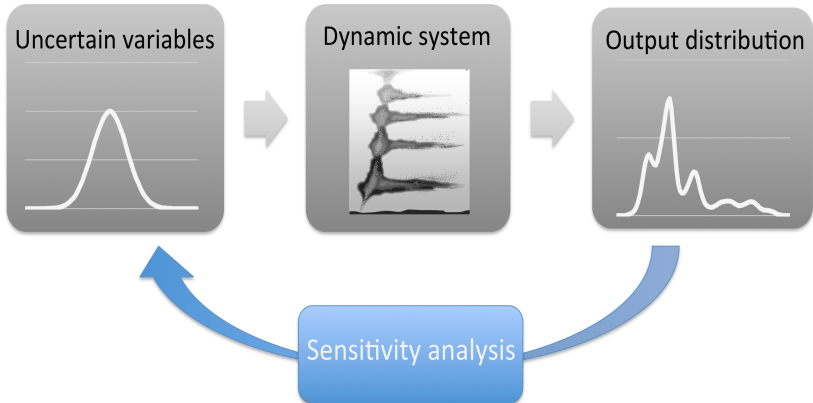


Figure : Mass flux PDF at the trap height for different gas bubble sizes.

Input for Lagrangian model - prediction with uncertainty

Uncertainty propagation: Global sensitivity analysis



Sensitivity index

Global sensitivity analysis aims to quantify the contribution of different random input variables to the model variability.

$$\text{Sensitivity index} = \frac{\text{Variance of } \xi_i}{\text{Total Variance}}$$

Parameter	Distribution	Sensitivity index
Entrainment coefficient	$U(0.06, 0.116)$	0.4191
Entrainment ratio	$U(0.4, 0.6)$	0.4394
Gas-to-oil ratio	$U(1600, 3000)$	0.1280
95th percentile of the droplet/bubble size (D_{95})	$U(7, 10)$	0.0699
Droplet distribution spreading ratio	$U(1.8, 4)$	0.0801

Table : Total sensitivity indices associated with different random variables

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Summary & future work

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- Propagating uncertainties through the plume model provides **statistical characteristics** of quantities of interest.
- The emulator-type methods **agree** very well with the Monte-Carlo set in the plume model.
- Sensitivity analysis points out the **key** parameter in the model

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Future work

- Expand the input uncertain space to include **additional** sources of uncertainties.
- Identify observational data to perform an **inverse** uncertainty propagation and to **correct** input uncertainties

Thank you !