4-4.1 Integrating Processes: Level Process

Consider the process tank shown in Fig. 4-4.1. An input stream enters the tank freely, whereas the output stream depends on the speed of the pump. The pump speed is regulated by the signal m(t), %.

The relation between the output flow and the signal is given by:

$$\tau_{p} \frac{df_{o}(t)}{dt} + f_{o}(t) = K_{p} m(t)$$

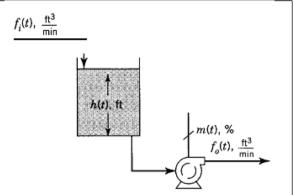


Figure 4-4.1 Process tank with pump manipulating outlet flow.

An unsteady-state mass balance around the tank provides the first equation needed:

$$\rho f_i(t) - \rho f_o(t) = \rho A \frac{dh(t)}{dt}$$

Only two equations are required to model this simple process.

Following the usual procedure, we obtain

$$\rho \overline{f_i} - \rho \overline{f_o} = \rho A \frac{d\overline{h}}{dt} = 0$$

Restando:

$$\rho f_{i}(t) - \rho f_{o}(t) - (\rho \overline{f}_{i} - \rho \overline{f}_{o}) =$$

$$\rho A \frac{dh(t)}{dt} - \rho A \frac{d\overline{h}}{dt}$$

$$\rho f_{i}(t) - \rho f_{o}(t) - \rho \overline{f}_{i} + \rho \overline{f}_{o} =$$

$$\rho A \frac{d[h(t) - \overline{h}]}{dt}$$

$$F_{i}(s) - F_{o}(s) = \rho AsH(s)$$

$$\frac{F_{i}(s) - F_{o}(s)}{As} = H(s)$$

$$H(s) = \frac{1}{As} [F_i(s) - F_o(s)]$$

where the deviation variables are

$$H(t) = h(t) - \overline{h}$$

$$F_i(t) = f_i(t) - \overline{f_i}$$

$$F_o(t) = f_o(t) - \overline{f_o}$$

$$\tau_{n} s F_{n}(s) + F_{n}(s) = K_{n} M(s)$$

$$\frac{F_o(s)(\tau_p s + 1)}{K_p} = M(s)$$

$$F_{o}(s) = \frac{K_{p}}{\left(\tau_{p}s + 1\right)}M(s)$$

where the new deviation variable is

$$M(t) = m(t) - \overline{m}$$

Sustituyendo:

$$H(s) = \frac{1}{As} \left[F_i(s) - \frac{K_p}{(\tau_p s + 1)} M(s) \right]$$

By superposition we can obtein transfer funtions desires:

$$\frac{H(s)}{F_i(s)} = \frac{1}{As}$$

$$\frac{H(s)}{M(s)} = -\frac{K_p}{As(\tau_p s + 1)}$$

S term in denominator indicates the "integrating" nature of the process

Let us develop the response of the system to a change of -B% in the signal m(t). That is,

$$m(t) = -Bu(t)$$

$$M(s) = -B\frac{1}{s}$$

$$H(s) = \frac{1}{As} \left[F_i(s) - \frac{K_p}{(\tau_p s + 1)} \left(-B\frac{1}{s} \right) \right]$$

$$H(s) = \frac{1}{As} \left[F_i(s) + \frac{BK_p}{s(\tau_p s + 1)} \right]$$

$$H(s) = \left[\frac{1}{As} F_i(s) + \frac{1}{As} \frac{BK_p}{s(\tau_p s + 1)} \right]$$

$$H(s) = \frac{1}{As} F_i(s) + \frac{BK_p}{As^2(\tau_p s + 1)}$$

$$\frac{f_i(t), \frac{\mathrm{ft}^3}{\mathrm{min}}}{h(t), \mathrm{ft}}$$

Figure 4-4.1 Process tank with pump manipulating outlet flow.

Principles and Practice of Automatic Process Control