

FLUID MECHANICS

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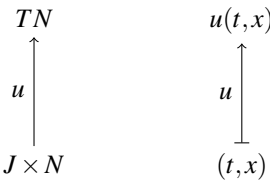
ABSTRACT. Everything about Fluid Mechanics

CONTENTS

Part 1. On Landau and Lifshitz’s Fluid Mechanics	1
1. Ideal Fluids	1
The energy flux	3
So-called momentum flux	4
Drag force in potential flow past a body	4
2. Viscous Fluids	4
3. Navier-Stokes Equations	4
3.1. Material Derivative	5
4. Energy transport and Energy dissipation	5
Part 2. Notes on Sabersky	6
5. Shear: shear stress	6
6. Compressible Fluids-One-Dimensional Flow	7
6.1. thermodynamic Preliminaries	7
6.2. The Energy Equation	7
6.3. Normal Shock Waves	7
Part 3. Fluid Mechanics (revisited)	8
7. Conservation	8
References	9

Part 1. On Landau and Lifshitz’s Fluid Mechanics

[1]



cf. Section 11.2 “Geometric setting of ideal continuum motion” of Holm, Schmah, Stoics [9]

Definition 1. Let spacetime manifold M admit a time-foliation $M = \mathbb{R} \times N$, where N represents spatial points. Let domain $\mathscr{D} \subseteq N$ represent positions of material particles of system in its **reference configuration**. Coordinate function (a^i) on \mathscr{D} represent **particle labels**.

- **configuration** $\mathrel{\mathop:}=$ diffeomorphism $g : \mathscr{D} \rightarrow \mathscr{D}$, $g \in \text{Diff}(\mathscr{D})$ space of diffeomorphisms from \mathscr{D} to \mathscr{D}
- **fluid motion** $g_t \equiv g(t) \in \text{Diff}(\mathscr{D})$

Chapter 1 of Landau and Lifshitz (1987) [1].
Use the **Eulerian** or spatial velocity, the velocity at time t of the particle currently in position \mathbf{x} [9] which is a time-dependent velocity field:
Let N be the spatial manifold, with spacetime manifold $M = \mathbb{R} \times N$, $\dim N = n$

Date: 17 juillet 2015.
1991 Mathematics Subject Classification. Fluid Mechanics.
Key words and phrases. Fluid Mechanics.
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Definition 2.

$$(1) \quad \begin{aligned} x &: \mathcal{D} \times \mathbb{R} \rightarrow \mathcal{D} \\ x(a, t) &:= g_t(a) = g(t) \cdot a \in \mathcal{D} \end{aligned}$$

describes path in \mathcal{D} by a particle labeled $a \in \mathcal{D}$

Definition 3. Lagrangian or material velocity - keep particle labels a fixed.

$$(2) \quad U(a, t) := \frac{\partial}{\partial t} g_t \cdot a = \frac{\partial}{\partial t} x(a, t)$$

$U(a, t)$ is velocity of particle with label a at time t .

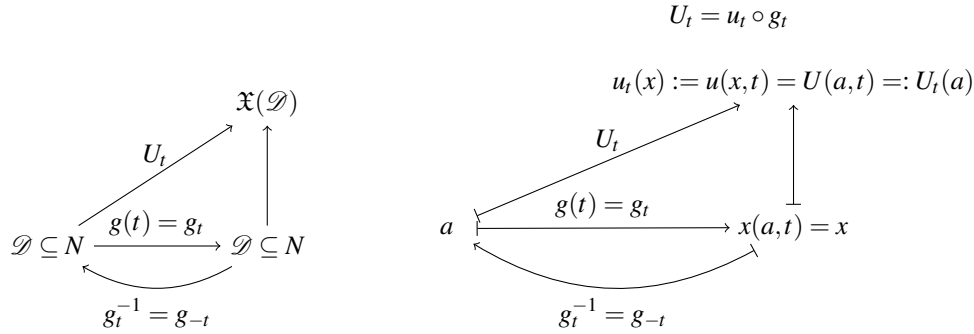
Eulerian or spatial velocity u
if $x = x(a, t) = g_t(a)$

$$(3) \quad u(x, t) := U(a, t) = U(g_t^{-1}(x), t)$$

$u(x, t)$ is velocity at time t of particle currently in position x

Now $u \implies u_t \in \mathfrak{X}(\mathcal{D})$

$$\begin{aligned} u_t(x) &:= u(x, t) \\ U_t(a) &:= U(a, t) \text{ though this isn't really a vector field.} \end{aligned}$$



Definition 4. Given path $g(t) \in \text{Diff}(\mathcal{D})$,

$$\begin{aligned} \text{Lagrangian velocity field } U_t &: \mathcal{D} \rightarrow \mathfrak{X}(\mathcal{D}) \\ U_t &\equiv \dot{g}(t) \equiv \frac{\partial g(t)}{\partial t} \end{aligned}$$

$$\dot{g}(t) \cdot a := \dot{g}(t)(a) = U_t(a) = \frac{\partial g_t}{\partial t} \cdot a$$

$$\begin{array}{ccc} g: \mathbb{R} \rightarrow \text{Diff}(\mathcal{D}) & & \text{Diff}(\mathcal{D}) \\ g(t) \in \text{Diff}(\mathcal{D}) & & \downarrow \frac{\partial}{\partial t} \\ \dot{g}(t) \equiv \frac{\partial g(t)}{\partial t} \equiv U_t & & T_g \text{Diff}(\mathcal{D}) \end{array}$$

$$\begin{array}{ccc} a \in \mathcal{D} & \xrightarrow{\dot{g}(t) \equiv \frac{\partial g(t)}{\partial t} \equiv U_t} & U_t(a) \in T_{g_t(a)} \mathcal{D} \\ & \searrow g(t) = g_t & \uparrow u_t \\ & & g(t) \cdot a = x(a, t) \in \mathcal{D} \end{array}$$

Thus

$$U_t = u_t \circ g_t$$

$$(4) \quad \begin{aligned} T_g \text{Diff}(\mathcal{D}) &= \{u \circ g | u \in \mathfrak{X}(\mathcal{D})\} = \\ &= \{ \text{smooth } U: \mathcal{D} \rightarrow T\mathcal{D} | U(a) \in T_{g(a)} \mathcal{D} \quad \forall a \in \mathcal{D} \} \end{aligned}$$

Theorem 1 ((Tangent lift of right translation)). *Let $\varphi \in \text{Diff}(\mathcal{D})$*

Let R_φ be right translation map

$$R_\varphi: \text{Diff}(\mathcal{D}) \rightarrow \text{Diff}(\mathcal{D})$$

$$R_\varphi: g \mapsto g \circ \varphi$$

tangent life of R_φ is map $TR_\varphi: T\text{Diff}(\mathcal{D}) \rightarrow T\text{Diff}(\mathcal{D})$

$$(5) \quad TR_\varphi(U) = TR_\varphi \left(\frac{d}{dt} \Big|_{t_0} g_t \right) := \frac{d}{dt} \Big|_{t_0} (g_t \circ \varphi) = U \circ \varphi$$

since $\forall a \in \mathcal{D}$

$$(6) \quad \frac{d}{dt} \Big|_{t_0} (g_t \circ \varphi)(a) = \frac{d}{dt} \Big|_{t_0} (g_t \circ \varphi(a)) = \left(\frac{d}{dt} \Big|_{t_0} g_t \right) \cdot \varphi(a) = U \circ \varphi(a)$$

$U\varphi \equiv TR_\varphi(U)$

Eulerian velocity corresponding to flow $g(t)$ is $u_t = \dot{g}(t)g^{-1}(t)$

$$\begin{array}{ccccc} T\text{Diff}(\mathcal{D}) & \xrightarrow{TR_\varphi} & T\text{Diff}(\mathcal{D}) & & \frac{d}{dt} \Big|_{t_0} g_t = U \xrightarrow{TR_\varphi} U \circ \varphi = \frac{d}{dt} \Big|_{t_0} (g_t \circ \varphi) \\ \uparrow & & \uparrow & & \uparrow \\ \text{Diff}(\mathcal{D}) & \xrightarrow{R_\varphi} & \text{Diff}(\mathcal{D}) & & \frac{d}{dt} \Big|_{t_0} g_t \xrightarrow{R_\varphi} g \circ \varphi \end{array}$$

cf. Section 5.2 “Abstract Lie groups and Lie algebras” of Holm, Schmah, Stoics [9]

The mass of fluid in some volume $V_0 \subset N$ is $\int_{V_0} \rho \text{vol}^n$, where ρ is fluid density, $\rho \in C^\infty(N)$.

The total mass of fluid flowing out of volume V_0 is

$$\begin{aligned} \frac{d}{dt} \int_{V_0} \rho \text{vol}^n &= \int_{V_0} \mathcal{L}_{\frac{\partial}{\partial t} + \mathbf{u}}(\rho \text{vol}^n) = \int_{V_0} \frac{\partial}{\partial t} \rho \text{vol}^n + \int_{V_0} \mathcal{L}_{\mathbf{u}} \rho \text{vol}^n \\ \int_{V_0} \mathcal{L}_{\mathbf{u}} \rho \text{vol}^n &= \int_{V_0} di_{\mathbf{u}} \rho \text{vol}^n + i_{\mathbf{u}} d\rho \text{vol}^n = \int_{V_0} di_{\mathbf{u}} \rho \text{vol}^n + 0 = \int_{V_0} di_{\mathbf{u}} \rho \text{vol}^n = \int_{\partial V_0} i_{\mathbf{u}} \rho \text{vol}^n \end{aligned}$$

Now

$$\begin{aligned} i_u \text{vol}^n &= i_u \frac{\sqrt{g}}{n!} \varepsilon_{i_1 \dots i_n} dx^{i_1} \wedge \dots \wedge dx^{i_n} \\ i_u dx^{i_1} \wedge \dots \wedge dx^{i_n} &= u^{i_1} dx^{i_2} \wedge \dots \wedge dx^{i_n} - dx^{i_1} \wedge u^{i_2} dx^{i_3} \wedge \dots \wedge dx^{i_n} + \dots + (-1)^{n+1} dx^{i_1} \wedge \dots \wedge dx^{i_{n-1}} u^{i_n} = \varepsilon_{j_1 \dots j_n}^{i_1 \dots i_n} u^{j_1} dx^{j_2} \wedge \dots \wedge dx^{j_n} \\ &\implies i_u \text{vol}^n = \frac{\sqrt{g}}{(n-1)!} \varepsilon_{j_1 \dots j_n} u^{j_1} dx^{j_2} \wedge \dots \wedge dx^{j_n} \end{aligned}$$

If $\sqrt{g} = 1, n = 2$,

$$i_u \text{vol}^2 = (u^1 dx^2 - u^2 dx^1) = u \cdot n_1 dx^2 + u \cdot n_2 dx^1 = u \cdot ndS$$

with $n_1 = e_1$ and $n_2 = -e_2$.

Now

$$\begin{aligned} di_u \rho \text{vol}^n &= \\ &= \frac{\partial(\sqrt{g} \rho u^{j_1})}{\partial x^k} \frac{\varepsilon_{j_1 \dots j_n}}{(n-1)!} dx^k \wedge dx^{j_2} \wedge \dots \wedge dx^{j_n} = \frac{\partial(\sqrt{g} \rho u^k)}{\partial x^k} \frac{\varepsilon_{j_1 \dots j_n}}{n!} dx^{j_1} \wedge \dots \wedge dx^{j_n} = \frac{1}{\sqrt{g}} \frac{\partial(\sqrt{g} \rho u^k)}{\partial x^k} \text{vol}^n = \\ &= \frac{\partial(\rho u^k)}{\partial x^k} \text{vol}^n + \rho u^k \frac{\partial \ln \sqrt{g}}{\partial x^k} \text{vol}^n = \text{div}(\rho u) \text{vol}^n + \rho u^k \frac{\partial \ln \sqrt{g}}{\partial x^k} \text{vol}^n \end{aligned}$$

Now if $\sqrt{g} = 1$, then

$$\frac{d}{dt} \int_{V_0} \rho \text{vol}^n = \int_{V_0} \frac{\partial \rho}{\partial t} \text{vol}^n + \int_{V_0} di_u \rho \text{vol}^n = \int_{V_0} \frac{\partial \rho}{\partial t} \text{vol}^n + \int_{V_0} \text{div}(\rho u) \text{vol}^n \implies \frac{\partial \rho}{\partial t} + \text{div}(\rho u) = 0$$

which is the so-called mass continuity equation. $j = \rho u$ is the mass flux density.

cf. Sec.1.2. Euler's equation [1],

The Cauchy-stress tensor T is a symmetric (0,2) tensor, so that $T \in \Gamma(T^*M \otimes T^*M)$.

Let the normal field n be normal to the surface of V_0 .

Let's do this:

$$T \xrightarrow{(n, -)} T(n, -) \in T^*M = \Omega^1(M) \xrightarrow{*} *T(n, -) \in \Omega^{m-1}(M)$$

So applying the Hodge operator,

$$pg_{ij} n^i dx^j \mapsto \frac{\sqrt{g}}{(n-1)!} pg_{ij} n^i \varepsilon_{j_2 \dots j_n}^j dx^{j_2} \wedge \dots \wedge dx^{j_n} = pi_n \text{vol}^n$$

$$- \int *T(n, -)$$

The force on V_0 due to the Cauchy-stress tensor is

$$\int_{\partial V_0} *T(n, -)$$

Taking, for the special case of the perfect fluid, $T = -pg$, then

$$- \int_{\partial V_0} pi_n \text{vol}^n = - \int_{V_0} d(pi_n \text{vol}^n) = - \int \text{div}(pn) \text{vol}^n = - \int \text{grad} p \text{vol}^n$$

using Stoke's law.

EY : 20150720 come to think about it, we should probably treat T as $T_{ij} dx^i \otimes dx^j$ and only do stuff on dx^i to retain $\otimes dx^j$ to get a direction out, a 1-formed valued $m-1$ form, $\dim M = m$

This is probably the correct way to think about it:

Given the Cauchy stress tensor $T = T^{ij} e_i \otimes e_j$, which is a (2,0)-rank tensor, T is a section of the $TM \otimes TM$ bundle, i.e. $\Gamma(TM \otimes TM)$, so that $T \in \Gamma(TM \otimes TM)$.

We want to do this:

$$\Gamma(TM \otimes TM) \xrightarrow{(\sharp, -)} \Omega^1(M, TM) \xrightarrow{(*, -)} \Omega^{n-1}(M, TM)$$

$$T = T^{ij} e_i \otimes e_j = T^{ij} e_j \otimes e_i \xrightarrow{(\sharp, -)} T_j^i e^j \otimes e_i \xrightarrow{(*, -)} T_{j \frac{\sqrt{g}}{(n-1)!}}^i \varepsilon_{j_2 \dots j_n}^j dx^{j_2} \wedge \dots \wedge dx^{j_n} \otimes e_i = T_j^i dS^j \otimes e_i$$

Thus, the force on V_0 due to the Cauchy-stress tensor is

$$\int_{\partial V_0} T_j^i dS^j \otimes e_i$$

and so for the case of $T = -pg$,

$$- \int_{\partial V_0} pg^i_j dS^j \otimes e_i$$

For the time rate of change of momentum, see my other pdf entitled ‘‘Aspects of Geometry in Propulsion.’’ There, we find the rate of change of momentum

$$\int_{V_0} \rho \left(\frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} \right) \text{vol}^n \otimes e_i$$

Euler's equation is then

$$(7) \quad \rho \left(\frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} \right) = - \frac{\partial \rho}{\partial x^j} g^{ij}$$

The energy flux.

Review of Thermodynamics. Let Σ be the manifold of equilibrium (and non-equilibrium) states of the system.

Proposition 1 (First Law: Energy Conservation).

$$(8) \quad dU = Q - dW = Q - p dV$$

with $U, p, V \in C^\infty(\Sigma)$, and $dU, Q, dW, dV \in \Omega^1(\Sigma)$, and where U is internal energy, p is pressure, V is the volume of the system.

Proposition 2 (Second Law).

$$(9) \quad Q = T dS$$

where $Q, dS \in \Omega^1(\Sigma)$, and $S \in C^\infty(\Sigma)$ and with

$$(10) \quad dS \geq 0$$

describing irreversibility.

Definition 5 (Enthalpy).

$$(11) \quad H = U + pV$$

where H is the **enthalpy**, $H \in C^\infty(\Sigma)$.

Now, for M being the molar mass, and defining per unit mass quantities as we go,

$$\begin{aligned} dH &= dU + V dp + p dV = Q + V dp = T dS + V dp \\ \xrightarrow{1/M} \frac{dH}{M} &= dh = T \frac{dS}{M} + \frac{V}{M} dp = T ds + \frac{dp}{\rho} \end{aligned}$$

where $\rho = M/V$.

Now the total energy in a fluid occupying region V_0 is

$$\int_{V_0} \left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n$$

where $\int_{V_0} \frac{1}{2} \rho v^2 \text{vol}^n$ is the total kinetic energy of fluid and ε internal energy per unit mass.

The time rate of change of the energy is

$$\begin{aligned} \frac{d}{dt} \int_{V_0} \left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n &= \int_{V_0} \mathcal{L}_{\frac{\partial}{\partial t} + v} \left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n = \int_{V_0} \frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n + \mathcal{L}_v \left(\left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n \right) = \\ &= \int_{V_0} \frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n + di_v \left(\left(\frac{1}{2} \rho v^2 + \rho \varepsilon \right) \text{vol}^n \right) \end{aligned}$$

So-called momentum flux. Sec. 1.7 of Landau and Lifshitz [1].

Let the total momentum of a fluid in volume $V_0 \subset N$, V_0 a submanifold of spatial manifold N , with $\dim V_0 = \dim N = n$ be P :

$$P = \int_{V_0} \rho \text{vol}^n u^i \otimes e_i \in \mathfrak{X}(M)$$

with

$$\rho \text{vol}^n u^i \otimes e_i \in \Omega^n(M; TM)$$

Now

$$\dot{P} := \frac{d}{dt} P = \int_{V_0} \mathcal{L}_{\frac{\partial}{\partial t} + u} (\rho \text{vol}^n u^i \otimes e_i)$$

which can be shown (see Yeung (2015) “Aspects of Geometry in Propulsion”) to be

$$\dot{P} = \int_{V_0} \frac{\partial(\rho u^i)}{\partial t} \text{vol}^n \otimes e_i + \int_{\partial V_0} \rho u^i i_u \text{vol}^n \otimes e_i$$

Now

$$\rho u^i i_u \text{vol}^n = \rho u^i \frac{\sqrt{g}}{(n-1)!} \varepsilon_{ki_2 \dots i_n} u^k dx^{i_2} \wedge \dots \wedge dx^{i_n} = \rho u^i u^k \frac{\sqrt{g}}{(n-1)!} \varepsilon_{ki_2 \dots i_n} dx^{i_2} \wedge \dots \wedge dx^{i_n} = \rho u^i u^k dS_k$$

So starting from equating the time rate of change of momentum \dot{P} with the external forces on it, $\int_{\partial V_0} T_j^i dS^j \otimes e_i$, then, for the special case of the perfect fluid, $T = -pg$

$$\dot{P} = \int_{\partial V_0} T_j^i dS^j$$

$$\implies \int_{V_0} \frac{\partial \rho u^i}{\partial t} \text{vol}^n \otimes e_i + \int_{\partial V_0} \rho u^i u^k dS_k \otimes e_i = - \int_{\partial V_0} pg^{ij} dS_j \otimes e_i$$

Now move the boundary term on the left hand side, $\int_{\partial V_0} \rho u^i u^j dS_j \otimes e_i$ over to the right hand side:

$$\int_{V_0} \frac{\partial \rho u^i}{\partial t} \text{vol}^n \otimes e_i = - \int_{\partial V_0} \rho u^i u^k dS_k \otimes e_i - \int_{\partial V_0} pg^{ij} dS_j \otimes e_i = - \int_{\partial V_0} (\rho u^i u^j + pg^{ij}) dS_j \otimes e_i$$

Then the momentum flux tensor $\Pi \in \Gamma(TM \otimes TM)$, in this case, takes the form

$$\Pi^{ij} = \rho u^i u^j + pg^{ij}$$

Drag force in potential flow past a body. Sec. 1.11 of Landau and Lifshitz [1].

The dictionary: for $v = v^i \frac{\partial}{\partial x^i} \in \mathfrak{X}(M)$,

$$v^\flat = v_i dx^i = g_{ij} v^j dx^i \in \Omega^1(M)$$

$$*v^\flat = \frac{\sqrt{g}}{(n-1)!} v_i \varepsilon_{j_2 \dots j_n}^i dx^{j_2} \wedge \dots \wedge dx^{j_n}$$

$$d * v^\flat = \frac{\partial}{\partial x^k} (\sqrt{g} v_i) \frac{\varepsilon_{j_2 \dots j_n}^i}{(n-1)!} dx^k \wedge dx^{j_2} \wedge \dots \wedge dx^{j_n} = \text{div}(v) \text{vol}^n + \frac{\partial \ln \sqrt{g}}{\partial x^i} v^i \text{vol}^n$$

$$dv^\flat = \frac{\partial v_j}{\partial x^j} dx^i \wedge dx^j$$

$$*dv^\flat = \frac{\partial v_j}{\partial x^i} \frac{\sqrt{g}}{(n-2)!} \varepsilon_{k_3 \dots k_n}^{ij} dx^{k_3} \wedge \dots \wedge dx^{k_n}$$

if $\sqrt{g} = 1$, $n = 3$,

$$(*dv^\flat)^\sharp = \text{curl}(v)$$

If $dv^\flat = 0$, then $v^\flat = d\phi$ (i.e. v^\flat is an exact form).

2. VISCOUS FLUIDS

Chapter 2 of Landau and Lifshitz [1]

Introduce a viscous stress tensor $\sigma' \in \Gamma(TM \otimes TM)$. Then do the following transformations:

$$\sigma' \xrightarrow{(\sharp, -)} (\sigma')^i_j e^j \otimes e_i \xrightarrow{(*, -)} (\sigma')^{ij} dS_j \otimes e_i$$

So the external force on the fluid in region V_0 is

$$\int_{\partial V_0} (T^{ij} + (\sigma')^{ij}) dS_j \otimes e_i$$

$$c_2 \circ c_1$$

$$\begin{array}{ccccc} \rho & \xrightarrow{c_1} & \sigma & \xrightarrow{g} & \tau \\ \downarrow F & & \downarrow F & & \downarrow F \\ F(\rho) & \xrightarrow{F(c_1)} & F(\sigma) & \xrightarrow{F(c_2)} & F(\tau) \\ & \searrow & & \nearrow & \\ & F(c_2 \circ c_1) = F(c_2) \circ F(c_1) & & & \end{array}$$

3. NAVIER-STOKES EQUATIONS

I am following closely Chorin and Marsden, Sec. 1.3 “The Navier-Stokes Equations”, Ch. 1 The Equations of Motion [6].

“On the left hand side,”

$$\begin{aligned} \frac{d}{dt} \int_{B(t)} \rho u \text{vol}^n &=: \frac{d}{dt} P := \frac{d}{dt} \int_{B(t)} m \otimes u = \int_{B(t)} (\mathcal{L}_{\frac{\partial}{\partial t} + u} m) \otimes u + \int_{B(t)} m \otimes \mathcal{L}_{\frac{\partial}{\partial t} + u} u = \\ &= 0 + \int_{B(t)} m \otimes \left(\frac{\partial u}{\partial t} + u^i \frac{\partial u^j}{\partial x^i} \frac{\partial}{\partial x^j} \right) = \int_{B(t)} m \otimes \left(\left(\frac{\partial u^j}{\partial t} + u^i \frac{\partial u^j}{\partial x^i} \right) \frac{\partial}{\partial x^j} \right) \end{aligned}$$

assuming mass conservation $\mathcal{L}_{\frac{\partial}{\partial t} + u} m = 0$.

“On the right hand side” are the physical forces on the fluid. Consider first only the forces on its surface $\partial B(t)$:

$$\int T^{ij} dS_j \otimes \frac{\partial}{\partial x^i}$$

with T being the stress tensor. For the case of a fluid,

$$T = -gp + \sigma \in \Gamma(\otimes^2 TM)$$

where σ is usually called the *viscous stress tensor*.

For deformation tensor E , σ can appear in two forms for its constitutive relation with E (this constitutive relation is assumed to be linear, E and σ are symmetric rank-2 tensors, due to angular momentum conservation, and fluid is assumed to be isotropic),

$$\sigma = \lambda(\text{tr} E)1 + 2\mu E$$

$$\sigma = 2\mu(E - \frac{1}{d} \text{tr}(E)1) + \eta \text{tr}(E)1 \in \Gamma(\otimes^2 TM)$$

with μ being the 1st. coefficient of viscosity

$$\eta = \lambda + \frac{2}{d} \mu \text{ being the 2nd. coefficient of viscosity.}$$

Now if we took the exterior derivative d of each of the following:

$$-g^{ij} p dS_j = -pg^{ij} \frac{\sqrt{g}}{(n-1)!} \varepsilon_{ji_2 \dots i_n} dx^{i_2} \wedge \dots \wedge dx^{i_n} \xrightarrow{d} -\frac{1}{\sqrt{g}} \frac{\partial (pg^{ik} \sqrt{g})}{\partial x^k} \text{vol}^n$$

Consider $E = \frac{1}{2} \left(g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j} + \frac{\partial g_{ij}}{\partial x^k} u^k \right) dx^i \otimes dx^j \in \Gamma(\otimes^2 T^*M)$, then

$$\begin{aligned} E^\sharp &= \frac{1}{2} \left(g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j} + \frac{\partial g_{ij}}{\partial x^k} u^k \right) g^{il} \frac{\partial}{\partial x^l} \otimes g^{jm} \frac{\partial}{\partial x^m} = \frac{1}{2} \left(g^{il} \frac{\partial u^m}{\partial x^i} + g^{jm} \frac{\partial u^l}{\partial x^j} + g^{il} g^{jm} \frac{\partial g_{ij}}{\partial x^k} u^k \right) \frac{\partial}{\partial x^l} \otimes \frac{\partial}{\partial x^m} \\ &\implies \frac{\partial (E^\sharp)^{ij}}{\partial x^j} = \\ &= \frac{1}{2} \left(\frac{\partial g^{ki}}{\partial x^j} \frac{\partial u^j}{\partial x^k} + g^{ki} \frac{\partial^2 u^j}{\partial x^j \partial x^k} + \frac{\partial g^{kj}}{\partial x^j} \frac{\partial u^i}{\partial x^k} + g^{kj} \frac{\partial^2 u^i}{\partial x^j \partial x^k} + \frac{\partial}{\partial x^j} (g^{li} g^{mj}) \frac{\partial g_{lm}}{\partial x^k} u^k + g^{li} g^{mj} \frac{\partial^2 g_{lm}}{\partial x^j \partial x^k} u^k + g^{li} g^{mj} \frac{\partial g_{lm}}{\partial x^k} \frac{\partial u^k}{\partial x^j} \right) \end{aligned}$$

If $g^{ij} = \delta^{ij}$ (i.e. Cartesian coordinates)

$$\begin{aligned} (E^\sharp)^{ij} &= \frac{1}{2} \left(\frac{\partial u^j}{\partial x^i} + \frac{\partial u^i}{\partial x^j} \right) \\ \implies \text{tr}(E^\sharp) &= \frac{\partial u^i}{\partial x^i} \end{aligned}$$

$$\frac{\partial (E^\sharp)^{ij}}{\partial x^j} = \frac{1}{2} \left(\frac{\partial^2 u^j}{\partial x^j \partial x^i} + \frac{\partial^2 u^i}{\partial x^j \partial x^j} \right) := \frac{1}{2} \left(\frac{\partial}{\partial x^i} (\text{div} u) + \Delta u^i \right)$$

So then, if λ, μ don't depend on position, for

$$\begin{aligned} \sigma^{ij} dS_j &= \lambda (\text{tr} E) \delta^{ij} + 2\mu E^{ij} \xrightarrow{d} \left(\frac{\partial (\lambda (\text{tr} E) \delta^{ij} \sqrt{g})}{\partial x^j} + 2 \frac{\partial (\mu E^{ij} \sqrt{g})}{\partial x^j} \right) \text{vol}^n \frac{1}{\sqrt{g}} = \\ &= \left(\lambda \frac{\partial (\text{tr} E \sqrt{g})}{\partial x^i} + 2\mu \frac{\partial E^{ij} \sqrt{g}}{\partial x^j} \right) \text{vol}^n \frac{1}{\sqrt{g}} \end{aligned}$$

then with $g^{ij} = \delta^{ij}$,

$$d\sigma^{ij} dS_j = \left(\lambda \frac{\partial}{\partial x^i} \text{div} u + \mu \left(\frac{\partial}{\partial x^i} (\text{div} u) + \Delta u^i \right) \right) \text{vol}^n$$

Thus, we reproduce, in Cartesian coordinates, the *Navier-Stokes equations* for *compressible, viscous* fluid flow:

$$(12) \quad \boxed{\rho \left(\frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} \right) = -\frac{\partial p}{\partial x^i} + (\lambda + \mu) \frac{\partial}{\partial x^i} \text{div} u + \mu \Delta u^i}$$

The case of *incompressible homogeneous* flow is when $\rho = \rho_0$, a constant, and $\text{div} u = 0$ (i.e. “no volume expansion”), so that the Navier-Stokes equations for incompressible flow is

$$\rho_0 \left(\frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} \right) = -\frac{\partial p}{\partial x^i} + \mu \Delta u^i$$

Set L characteristic length

U characteristic velocity

Then

$$\begin{aligned} (u')^i &= \frac{u^i}{U} & \frac{\partial u^i}{\partial t} &= \frac{U}{L/U} \frac{\partial (u')^i}{\partial t'} = \frac{U^2}{L} \frac{\partial (u')^i}{\partial t'} \\ (x')^j &= \frac{x^j}{L} & \frac{\partial u^i}{\partial x^j} &= \frac{U}{L} \frac{\partial (u')^i}{\partial (x')^j} \\ t' &= \frac{t}{L/U} & \frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} &= \frac{U^2}{L} \frac{\partial (u')^i}{\partial t'} + U (u')^j \frac{U}{L} \frac{\partial (u')^i}{\partial (x')^j} = \frac{U^2}{L} \left(\frac{\partial (u')^i}{\partial t'} + (u')^j \frac{\partial (u')^i}{\partial (x')^j} \right) \end{aligned}$$

$$\begin{aligned} \text{div} u &= \frac{L}{U} \text{div} u' & -\frac{\partial p}{\partial x^i} &= \frac{-1}{L} \frac{\partial p}{\partial (x')^i} \xrightarrow{\cdot \frac{L}{\rho U^2}} -\frac{1}{\rho U^2} \frac{\partial p}{\partial (x')^i} \\ \Delta (u')^i &= \frac{L^2}{U} \Delta u^i & (\lambda + \mu) \frac{\partial}{\partial x^i} \text{div} u &= (\lambda + \mu) \frac{U}{L^2} \frac{\partial}{\partial (x')^i} \text{div} u' \xrightarrow{\cdot \frac{L}{\rho U^2}} (\lambda + \mu) \frac{1}{\rho L U} \frac{\partial}{\partial (x')^i} \text{div} u' \\ & & \mu \Delta u^i &= \mu \frac{U}{L^2} \Delta (u')^i \xrightarrow{\cdot \frac{L}{\rho U^2}} \frac{\mu L}{\rho U^2} \Delta u^i = \frac{\mu}{\rho L U} \Delta (u')^i \end{aligned}$$

Define $R := \frac{\rho L U}{\mu}$, the **Reynolds number**. R is a dimensionless quantity. $\frac{(\lambda + \mu)}{\rho L U}$ is a dimensionless quantity.

Bhatia, Norgard, Pascucci, Bremer have an insightful survey on the so-called Helmholtz-Hodge decomposition and expands upon it and what's out there already in the literature [7].

Let domain be the smooth submanifold $\mathcal{D} \subset N$, N is the spatial manifold. $\text{dima} = \dim N = n$; spacetime manifold $M = \mathbb{R} \times N$.

$a = (a^i) \in \mathcal{D}$ is a particle label.

It'd be instructive to compare expressions between Chorin and Marsden [6] and Landau and Lifshitz [1]:

$$\begin{aligned} \sigma &= 2\mu (E - \frac{1}{d} \text{tr}(E) 1) + \eta \text{tr}(E) 1 \in \Gamma(\otimes^2 TM) \\ E &= \frac{1}{2} (g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j} + \frac{\partial g_{ij}}{\partial x^k} u^k) dx^i \otimes dx^j \in \Gamma(\otimes^2 T^*M) \\ E^\sharp &= \frac{1}{2} \left(\frac{\partial u^j}{\partial x^i} + \frac{\partial u^i}{\partial x^j} \right) \frac{\partial}{\partial x^i} \otimes \frac{\partial x^j}{\in} \Gamma(\otimes^2 TM) \\ \text{tr} E^\sharp &= \frac{\partial u^i}{\partial x^i} \\ \mu &\equiv \text{1st. coefficient of viscosity} \\ \eta &= \lambda + \frac{2}{d} \mu \equiv \text{2nd. viscosity} \\ \rho \left(\frac{\partial u^i}{\partial t} + u^j \frac{\partial u^i}{\partial x^j} \right) &= -\frac{\partial p}{\partial x^i} + (\lambda + \mu) \frac{\partial}{\partial x^i} \text{div} u + \mu \Delta u^i = \\ &= -\frac{\partial p}{\partial x^i} + \mu \Delta u^i + \left(\eta + (1 - \frac{2}{d}) \mu \right) \frac{\partial}{\partial x^i} \text{div} u \\ &\iff \sigma'_{ik} = \eta \left(\frac{\partial v_i}{\partial x_k} + \frac{\partial v_k}{\partial x_i} - \frac{2}{3} \delta_{ik} \frac{\partial v_l}{\partial x_l} \right) + \eta \delta_{ik} \frac{\partial v_l}{\partial x_l} \\ &\iff \rho \left[\frac{\partial v}{\partial t} + (v \cdot \text{grad}) v \right] = -\text{grad} p + \eta \Delta v + \left(\zeta + \frac{\eta}{3} \right) \text{grad div} v \end{aligned}$$

3.1. Material Derivative. Consider $u^j \frac{\partial u^i}{\partial x^j}$ or $(u \cdot \text{grad})u$. Landau and Lifshitz on pp. 48, Sec. 15 has a useful table of the Equations of Motion in Curvilinear Coordinates [1]. Recall the metric g for cylindrical and spherical coordinates, for $g \in \otimes^2 T^*M$ and $g^{-1} \in \otimes^2 TM$

$$\begin{aligned} g &= dr^2 + r^2 d\phi^2 + dz^2 & g &= d\rho^2 + \rho^2 d\theta^2 + \rho^2 \sin \theta d\phi^2 \\ g^{-1} &= \left(\frac{\partial}{\partial r} \right)^2 + \frac{1}{r^2} \left(\frac{\partial}{\partial \phi} \right)^2 + \left(\frac{\partial}{\partial z} \right)^2 & g^{-1} &= \left(\frac{\partial}{\partial \rho} \right)^2 + \frac{1}{\rho^2} \left(\frac{\partial}{\partial \theta} \right)^2 + \frac{1}{\rho^2 \sin \theta} \left(\frac{\partial}{\partial \phi} \right)^2 \end{aligned}$$

4. ENERGY TRANSPORT AND ENERGY DISSIPATION

Chorin and Marsden, pp. 10 [6].

Definition 6. Fluid is *incompressible* if $\frac{d}{dt} \int \text{vol}^n = 0$

Now

$$\begin{aligned} \frac{d}{dt} \int \text{vol}^n &= \int \mathcal{L}_{\frac{\partial}{\partial t} + u} \text{vol}^n = \int \frac{\partial}{\partial t} \text{vol}^n + \mathcal{L}_u \text{vol}^n = \int 0 + di_u \text{vol}^n + i_u d\text{vol}^n = \int d \frac{\sqrt{g}}{n} \varepsilon_{i_1 i_2 \dots i_n} u^{i_1} dx^{i_2} \wedge \dots \wedge dx^{i_n} + 0 = \\ &= \int \frac{1}{\sqrt{g}} \frac{\partial (\sqrt{g} u^k)}{\partial x^k} \text{vol}^n \end{aligned}$$

If $\frac{d}{dt} \int \text{vol}^n = 0$ i.e. fluid is incompressible, $\text{div} u := \frac{1}{\sqrt{g}} \frac{\partial (\sqrt{g} u^k)}{\partial x^k} = 0$

Let

$$E_{\text{KE}} := \frac{1}{2} \int_{B(t)} \rho |u|^2 \text{vol}^n$$

Then

$$\frac{d}{dt} E_{\text{KE}} = \frac{d}{dt} \left[\frac{1}{2} \int_{B(t)} \rho |u|^2 \text{vol}^n \right] = \frac{1}{2} \int_{B(t)} \mathcal{L}_{\frac{\partial}{\partial t} + u} (m |u|^2) = \frac{1}{2} \int_{B(t)} (\mathcal{L}_{\frac{\partial}{\partial t} + u} m) |u|^2 + m \mathcal{L}_{\frac{\partial}{\partial t} + u} |u|^2 = \frac{1}{2} \int_{B(t)} 0 + m \mathcal{L}_{\frac{\partial}{\partial t} + u} |u|^2$$

Now

$$\frac{\partial}{\partial t} |u|^2 = u^i \frac{\partial}{\partial t} (g_{ij} u^j) + u_i \frac{\partial u^i}{\partial t}$$

If g_{ij} is time-independent,

$$\frac{\partial}{\partial t} |u|^2 = 2u_i \frac{\partial u^i}{\partial t}$$

Also,

$$\begin{aligned} \mathcal{L}_u |u|^2 &= u^k \frac{\partial}{\partial x^k} (g_{ij} u^j u^i) = 2u^k u_i \frac{\partial u^i}{\partial x^k} + u^k u^j u^i \frac{\partial g_{ij}}{\partial x^k} = 2u_i (u^k \frac{\partial u^i}{\partial x^k} + \frac{1}{2} u^l \frac{\partial g_{jk}}{\partial x^l} u^j g^{ik}) = \\ &= 2u_i \left(u^k \frac{\partial u^i}{\partial x^k} + \Gamma_{jk}^i u^j u^k \right) = 2u \cdot \nabla_u u \end{aligned}$$

and all (I claim; I worked it out) that was required was that g be metric-compatible, i.e. $\nabla g = 0$.

Thus,

$$\frac{d}{dt} E_{\text{KE}} = \int_{B(t)} m u_i \left(\frac{\partial u^i}{\partial t} + \nabla_u u^i \right)$$

Consider the “right hand side” (RHS), the work done on the fluid system by the stresses on the surface boundary, $T \in \Gamma(\otimes^2 T^* M)$, and body forces per mass, b . I propose that this work takes this form:

$$(13) \quad \int_{\partial B} u_i T^{ij} dS_j + \int_B m b^i u_i \equiv \int_{\partial B} T(u, dS) + \int_B m \langle u, b \rangle$$

Now

$$\begin{aligned} \int_{\partial B} u_i T^{ij} dS_j &= \int_B \frac{1}{\sqrt{g}} \frac{\partial (u_i T^{ij} \sqrt{g})}{\partial x^j} \text{vol}^n \equiv \int_B \text{div}(u_i T^{ij}) \text{vol}^n = \int_B \left(u_i \frac{\partial T^{ij}}{\partial x^j} + T^{ij} \frac{1}{\sqrt{g}} \frac{\partial (u_i \sqrt{g})}{\partial x^j} \right) \text{vol}^n \equiv \\ &\equiv \int_B \left(u_i \frac{\partial T^{ij}}{\partial x^j} + T^{ij} \text{div} u_i \right) \text{vol}^n \end{aligned}$$

Suppose $T^{ij} = -p g^{ij}$. Then

$$\begin{aligned} \int_B \text{div}(u_i T^{ij}) \text{vol}^n &\equiv \int_B \frac{-1}{\sqrt{g}} \frac{\partial (u_i p g^{ij} \sqrt{g})}{\partial x^j} \text{vol}^n = - \int_B \frac{1}{\sqrt{g}} \frac{\partial (u^j p \sqrt{g})}{\partial x^j} \text{vol}^n = - \int_B \left(u^j \frac{\partial p}{\partial x^j} + \frac{p}{\sqrt{g}} \frac{\partial (u^j \sqrt{g})}{\partial x^j} \right) \text{vol}^n = \\ &= - \int_B \left(u^j \frac{\partial p}{\partial x^j} + p \text{div} u \right) \text{vol}^n \end{aligned}$$

For $T^{ij} = -p g^{ij}$, this result is the most general case. If the fluid is incompressible, then $\text{div} u = 0$, so the contribution to the work done on the fluid is $-\int_B u^j \frac{\partial p}{\partial x^j} \text{vol}^n$.

Thus, energy conservation, for an incompressible fluid is

$$\rho u_i \left(\frac{\partial u^i}{\partial t} + \nabla_u u^i \right) = -u^j \frac{\partial p}{\partial x^j} + \rho u_i b^i$$

Part 2. Notes on Sabersky

5. SHEAR: SHEAR STRESS

cf. Chapter 1 Introduction

In Appendix A Forms in Continuum Mechanics, Subsection A.g. Some Typical Computations Using Forms, Frankel (2004) [3] defines the so-called **rate of deformation** tensor, which Frankel describes as measuring how the flow deforms the physical system in consideration.

Consider curve $\gamma: \mathbb{R} \rightarrow N$ and generating velocity vector field $u = \dot{\gamma} \in \mathfrak{X}(N)$.

$$\gamma(t) \in N$$

Now $\gamma(0) = x(0)$ and so we recall the idea of ψ_t , a local 1-parameter group $(\psi_t)_{t \in I \subset \mathbb{R}}$ of local diffeomorphisms s.t. $\psi_t(x(0)) = x(t) \in N$.

$$\gamma(t) = x(t)$$

Now recall the definition of the Lie derivative of a tensor (e.g. Def. 2.2.6 on pp. 58, Chapter 2 Lie Groups and Vector Bundles of Jost (2011) [4]:

$$\mathcal{L}_u g := \frac{d}{dt} (\psi_t^* g)|_{t=0} = \lim_{t \rightarrow 0} \frac{\psi_t^* g' - g}{t} = \lim_{t \rightarrow 0} \frac{\left(g'_{ij} \frac{\partial x^i}{\partial a^k} \frac{\partial x^k}{\partial a^l} - g_{kl} \right)}{t} da^k \otimes da^l$$

If $\mathcal{L}_u g = 0$, then metric g doesn’t change along integral curves of u , so u generates cont. 1-parameter family of symmetries ψ_t for g .¹

Otherwise, $\mathcal{L}_u g \neq 0$.

Then u is *not* a Killing vector. ψ_t are not symmetric diffeomorphisms (i.e. isometries).

Let’s compute $\mathcal{L}_u g$.

Calin and Chang (2005) [5] does a great job in calculating out *explicitly* with *explicit* calculation steps in all their proofs of theorems, lemmas, claims. For instance, in Chapter 5 Conservation Theorems, Section 5.3 The Energy-momentum tensor, Subsection 5.3.4 Divergence of the energy-momentum tensor, pp. 83, Lemma 5.33 of Calin and Chang (2005) [5], it gives the explicit calculation of $\mathcal{L}_u g$, exactly what we need:

$$\begin{aligned} \mathcal{L}_u g &= (\mathcal{L}_u g_{ij} dx^i) \otimes dx^j + g_{ij} dx^i \otimes \mathcal{L}_u dx^j = (i_u d(g_{ij} dx^i) + d(g_{ij} u^i)) \otimes dx^j + g_{ij} dx^i \otimes du^j = \\ &= (i_u \left(\frac{\partial g_{ij}}{\partial x^k} dx^k \wedge dx^i \right) + \frac{\partial (g_{ij} u^i)}{\partial x^k} dx^k) \otimes dx^j + g_{ij} dx^i \otimes \frac{\partial u^j}{\partial x^k} dx^k = \\ &= \left(u^k \frac{\partial g_{ij}}{\partial x^k} dx^i - u^i \frac{\partial g_{ij}}{\partial x^k} dx^k + u^i \frac{\partial g_{ij}}{\partial x^k} dx^k + g_{ij} \frac{\partial u^i}{\partial x^k} dx^k \right) dx^j + g_{ij} \frac{\partial u^j}{\partial x^k} dx^i \otimes dx^k = \left(u^k \frac{\partial g_{ij}}{\partial x^k} + g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j} \right) dx^i \otimes dx^j \end{aligned}$$

This calculation is completely equivalent to using, besides the product rule on symmetric tensors, the \mathbb{K} -linearity property of \mathcal{L} ,

$$(14) \quad \mathcal{L}_u g = (\mathcal{L}_u g_{ij}) dx^i \otimes dx^j + g_{ij} ((\mathcal{L}_u dx^i \otimes dx^j) + dx^i \otimes \mathcal{L}_u dx^j) = (u^k \frac{\partial g_{ij}}{\partial x^k} + g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j}) dx^i \otimes dx^j$$

Now, by theorem, for any smooth manifold, $\exists!$ Levi-Civita connection that’s torsion-free (which can always be constructed to be torsion-free) and metric-compatible (which has to be defined, but otherwise, we’ve got not enough structure). Then on any coordinate chart, since by requiring metric compatibility, then $\nabla g = 0$, so

$$\begin{aligned} \nabla g = 0 &\implies \\ \frac{\partial g_{ij}}{\partial x^k} - g_{lj} \Gamma_{ik}^l - g_{il} \Gamma_{jk}^l &= \frac{\partial g_{ij}}{\partial x^k} - g_{lj} \Gamma_{ki}^l - g_{il} \Gamma_{kj}^l = 0 \end{aligned}$$

using torsion free ∇ (so $\Gamma_{ki}^l = \Gamma_{ik}^l$ i.e. index symmetry) property.

Then from our expression for $\mathcal{L}_u g$, Eq. 14,

$$\begin{aligned} u^k \frac{\partial g_{ij}}{\partial x^k} + g_{kj} \frac{\partial u^k}{\partial x^i} + g_{ik} \frac{\partial u^k}{\partial x^j} &= u^k \frac{\partial g_{ij}}{\partial x^k} + g_{kj} ((\nabla_i u)^k - \Gamma_{ji}^k u^j) + g_{ik} ((\nabla_j u)^k - \Gamma_{ij}^k u^i) = \\ &= \underbrace{u^k \frac{\partial g_{ij}}{\partial x^k} - g_{kj} \Gamma_{ji}^k u^j - g_{ik} \Gamma_{ij}^k u^i}_{=\nabla_u g = \nabla g(u) = 0} + g_{kj} (\nabla_i u)^k + g_{ik} (\nabla_j u)^k \end{aligned}$$

¹Fionn Fitzmaurice. “Differential Geometry.” <https://www.maths.tcd.ie/~fionn/dg/dg.pdf>

Thus,

$$(15) \quad \boxed{\mathcal{L}_u g = (g_{kj}(\nabla_i u)^k + g_{ik}(\nabla_j u)^k) dx^i \otimes dx^j}$$

for the Levi-Civita connection on any metric manifold (N, g) .

Note that wikipedia calls this the “strain rate” tensor in its “Viscous stress tensor” article.

The viscous stress tensor, ε_{ij} or $\varepsilon = \varepsilon_{ij} dx^i \otimes dx^j \in \Gamma(\otimes^2 T^*M)$, then is related, for the case of Newtonian fluids, to $\mathcal{L}_u g$ in the following manner:

$$\varepsilon_{ij} = \mu_{ij}{}^{kl} (\frac{1}{2} \mathcal{L}_u g)_{kl} \text{ or } \varepsilon = (\mu_{ij} (\frac{1}{2} \mathcal{L}_u g)) dx^i \otimes dx^j = \mu (\frac{1}{2} \mathcal{L}_u g)$$

where $\otimes^2 T^*M \xrightarrow{\mu} \otimes^2 T^*M$.

Examples, i.e. specific cases.

Suppose u is all in $\frac{\partial}{\partial x}$ direction (1 direction).

$$u = u^x \frac{\partial}{\partial x} \equiv u \frac{\partial}{\partial x}$$

$$g_{kj}(\nabla_i u)^k = g_{kj} \left(\frac{\partial u^k}{\partial x^i} + \Gamma^k_{ji} u^j \right) = g_{xj} \left(\frac{\partial u}{\partial x^i} \right) + g_{kj} \Gamma^k_{xi} u$$

$$\begin{aligned} \mathcal{L}_u g &= (g_{kj}(\nabla_i u)^k + g_{ik}(\nabla_j u)^k) dx^i \otimes dx^j = (g_{xj} \left(\frac{\partial u}{\partial x^i} \right) + g_{kj} \Gamma^k_{xi} u + g_{xi} \left(\frac{\partial u}{\partial x^j} \right) + g - ki \Gamma^k_{xj} u) dx^i \otimes dx^j = \\ &= 2 \left(g_{xj} \left(\frac{\partial u}{\partial x^i} \right) + g_{ki} \Gamma^k_{xj} u \right) dx^i \otimes dx^j \end{aligned}$$

if $u = u(y)$, $\Gamma^k_{xj} = 0$, $g = 1$

$$\mathcal{L}_u g = 2 \left(\frac{\partial u}{\partial y} \right) dy \otimes dx$$

$$\mu \left(\frac{1}{2} \mathcal{L}_u g \right) \left(\frac{\partial}{\partial y} \right) = \mu \frac{\partial u}{\partial y} dx \mapsto \mu \frac{\partial u}{\partial y} = \tau_x = \tau$$

6. COMPRESSIBLE FLUIDS-ONE-DIMENSIONAL FLOW

6.1. thermodynamic Preliminaries.

6.2. The Energy Equation. Since

$$h_0 = h_1 + \frac{u_1^2}{2}$$

then

$$\frac{C_p}{MN} \tau_0 = \frac{C_p \tau_1}{MN} + \frac{u_1^2}{2} = \frac{C_p \tau_2}{MN} + \frac{u_2^2}{2} \text{ or } \tau_0 = \tau + \frac{u^2}{2 \frac{C_p}{MN}}$$

Now the speed of sound at a particular point along the flow, 1, is

$$a_1 = \sqrt{\gamma R T_1} = \sqrt{\gamma \frac{\tau_1}{M}}$$

and so

$$\implies \tau_0 = \tau + \frac{\mathfrak{M}^2 \gamma \tau}{2 \frac{C_p}{M}} = \tau \left(1 + \frac{\mathfrak{M}^2 (\gamma - 1)}{2} \right)$$

If $\mathfrak{M} = 1$, when $\tau_1 = \tau^*$,

$$\tau_0 = \tau^* \left(1 + \frac{\gamma - 1}{2} \right) = \tau^* \left(\frac{\gamma + 1}{2} \right) \text{ or } \tau^* = \frac{2 \tau_0}{\gamma + 1}$$

$$(16) \quad a^* = \sqrt{\gamma R T^*} = \sqrt{\gamma \frac{\tau^*}{M}} = \sqrt{\frac{2 \gamma \tau_0}{M(\gamma + 1)}} = \left(\frac{2 \gamma R T_0}{\gamma + 1} \right)^{1/2} \implies u^* \equiv a^* = \left(\frac{2 \gamma R T_0}{\gamma + 1} \right)^{1/2} = \sqrt{\frac{2 \gamma \tau_0}{M(\gamma + 1)}}$$

If $u > u^*$,

$$\begin{aligned} \mathfrak{M} &:= \frac{u}{a} = \frac{u}{\sqrt{\gamma \frac{\tau}{M}}} > \sqrt{\frac{2 \tau_0}{\tau(\gamma + 1)}} = \sqrt{\frac{2}{\gamma + 1} \left(1 + \frac{\mathfrak{M}^2 (\gamma - 1)}{2} \right)} \\ \implies \mathfrak{M}^2 &> \frac{2}{\gamma + 1} + \mathfrak{M}^2 \frac{(\gamma - 1)}{\gamma + 1} \text{ or } \mathfrak{M}^2 \left(\frac{2}{\gamma + 1} \right) > \frac{2}{\gamma + 1} \\ &\implies \mathfrak{M} > 1 \end{aligned}$$

So if $u > u^*$, then $\mathfrak{M} > 1$. Likewise,

if $u < u^*$, then $\mathfrak{M} < 1$

Thus, the name $u^* \equiv a^*$ *critical velocity*

6.3. Normal Shock Waves. Use moving reference frame in which shock is stationary, and resulting steady.

Continuity:

$$\rho_1 v_1 A = \rho_2 v_2 A \implies \rho_1 v_1 = \rho_2 v_2$$

momentum equation: using

$$\Pi^{ij} = \rho u^i u^j + p g^{ij}$$

then

$$\rho_1 v_1^2 + p_1 = \rho_2 v_2^2 + p_2$$

energy equation:

$$h_0 = h_1 + \frac{v_1^2}{2} = h_2 + \frac{v_2^2}{2} \text{ or } \frac{C_p \tau_1}{MN} + \frac{v_1^2}{2} = \frac{C_p \tau_2}{MN} + \frac{v_2^2}{2} \implies \frac{C_p R T_1}{N} + \frac{v_1^2}{2} = \frac{C_p R}{N} T_0$$

Also, note that I end up using this heat capacity *for the ideal gas* relation all the time in (rocket) propulsion:

$$C_p = \gamma C_v = \frac{\gamma N}{\gamma - 1} \text{ since } C_p = C_v + N \text{ or } \gamma = 1 + N/C_v$$

With mass continuity, momentum conservation, and the energy equation (Bernoulli invariant), then, using Python’s sympy to do the algebra, detailed in file fluid.py

```
# mass conservation
massconsEq = Eq(rho_1*u_1, rho_2*u_2)

# momentum flux conservation
momconsEq = Eq(rho_1*u_1**2+p_1, rho_2*u_2**2+p_2)

# energy equation or Bernoulli invariant
Bernoulli_invariant_1to2_Eq = Eq( C_p*R*T_1/N + u_1**2/2, C_p*R*T_2/N + u_2**2/2)

# stagnation enthalpy relation
stagh1Eq = Eq( C_p*R*T_0/N , C_p*R*T_1/N + u_1**2/2)
stagh2Eq = Eq( C_p*R*T_0/N , C_p*R*T_2/N + u_2**2/2)

# ideal gas law
ideal_gas1Eq = Eq(p_1, rho_1*R*T_1)
ideal_gas2Eq = Eq(p_2, rho_2*R*T_2)

# This reproduces Eq. (9.26) of Sabersky, Acosta, Hauptmann, Gates pp. 357, Sec. 9.6., Normal Shock Waves !!!
(momconsEq.subs(p_1, ideal_gas1Eq.rhs).subs(p_2, ideal_gas2Eq.rhs).subs(rho_2, solve(massconsEq, rho_2)[0])/rho_1).simplify()
# R*T_1 - R*T_2*u_1/u_2 + u_1**2 - u_1*u_2

# This reproduces Eq. (9.27) of Sabersky, Acosta, Hauptmann, Gates pp. 357, Sec. 9.6., Normal Shock
# Waves, where stagnation temperature relation was substituted into momentum and continuity equation
PrandtlEq1d = momconsEq.subs(p_1, ideal_gas1Eq.rhs).subs(p_2, ideal_gas2Eq.rhs).
subs(rho_2, solve(massconsEq, rho_2)[0]).subs(T_1, solve(stagh1Eq, T_1)[0]).subs(T_2, solve(stagh2Eq, T_2)[0])

PrandtlEq1d = PrandtlEq1d.subs(C_p, gamma*N/(gamma-1) )

solve(PrandtlEq1d, u_1**2)[0]
# (2*R*T_0*gamma*u_1 - 2*R*T_0*gamma*u_2 + gamma*u_1*u_2**2 + u_1*u_2**2)/(u_2*(gamma + 1))
# Thus, writing this out on paper, we get the desired result, Prandtl’s equation (9.28) on pp. 357 of
# Sabersky, Acosta, Hauptmann, Gates
```

and thus

$$u_1 u_2 = \frac{2RT_0 \gamma}{\gamma + 1} = (a^*)^2$$

for, the critical velocity was derived from only the energy equation (or Bernoulli invariant) and Mach *definition*, and was shown, explicitly, that if the velocity u at a point is greater than this critical velocity $u^* \equiv a^*$, then the flow is supersonic (cf. Eq. **16**):

$$u^* \equiv a^* = \left(\frac{2\gamma RT_0}{\gamma + 1} \right)^{1/2} = \sqrt{\frac{2\gamma \tau_0}{M(\gamma + 1)}}$$

So if $u_1 > a^*$, then $u_2 < a^*$, and so approaching flow is supersonic and downstream flow is subsonic.

Second law of thermodynamics forbids the other way.

Note that

$$u_1 u_2 = \frac{2RT_0 \gamma}{\gamma + 1} \text{ or } \mathfrak{M}_1 \mathfrak{M}_2 = \frac{2}{\gamma + 1} \frac{T_0}{\sqrt{T_1 T_2}}$$

(9.16) from Sabersky,

$$(17) \quad \boxed{\mathfrak{M}_2^2 = \frac{\mathfrak{M}_1^2(\gamma - 1) + 2}{2\gamma \mathfrak{M}_1^2 - \gamma + 1}}$$

Although preceding results obtained for constant-area duct, they're valid in gradually varying duct

shock region very thin; order of a few molecular mean free path lengths; area change across the shock is then usually negligible

for practical purposes

Preceding, viscosity effects near wall ignored; since velocity must still be 0 at wall, supersonic flow must revert to subsonic in near-wall region.[2]

Now recall that for $U = U(\tau, V)$ (in general, $U = U(\tau)$ for perfect ideal gas),

$$\tau d\sigma = dU + p dV = \left(\frac{\partial U}{\partial \tau} \right)_V d\tau + \left(\frac{\partial U}{\partial V} \right)_\tau dV + p dV = C_V d\tau + \left(\left(\frac{\partial U}{\partial V} \right)_\tau + p \right) dV$$

If $U = U(\tau)$,

$$\begin{aligned} \tau d\sigma &= C_V d\tau + p dV \text{ or } d\sigma = \frac{C_V}{\tau} d\tau + \frac{p}{\tau} dV = \frac{C_V}{\tau} d\tau + \frac{N}{V} dV \\ \implies \int_\gamma d\sigma &= \sigma_2 - \sigma_1 = C_V \ln \left(\frac{\tau_2}{\tau_1} \right) + N \ln \frac{V_2}{V_1} = C_V \ln \left(\frac{\tau_2}{\tau_1} \right) + N \ln \left(\frac{\rho_1}{\rho_2} \right) \end{aligned}$$

From momentum conservation, and ideal gas law and Mach definition,

$$\rho_1 u_1^2 + p_1 = \rho_2 u_2^2 + p_2 \text{ or } p_1 - p_2 = \rho_2 u_2^2 - \rho_1 u_1^2 = \frac{p_2}{RT_2} u_2^2 - \frac{p_1}{RT_1} u_1^2 = \gamma (p_2 \mathfrak{M}_2^2 - p_1 \mathfrak{M}_1^2) \text{ or } \frac{p_1}{p_2} = \frac{1 + \gamma \mathfrak{M}_2^2}{1 + \gamma \mathfrak{M}_1^2}$$

For real shocks, $\mathfrak{M}_1 > \mathfrak{M}_2$, so $p_1 < p_2$

Now

$$\begin{aligned} \frac{\rho_1}{\rho_2} &= \frac{p_1 T_2}{p_2 T_1} \\ \frac{T_1}{T_2} &= \frac{1 + \frac{\gamma-1}{2} \mathfrak{M}_2^2}{1 + \frac{\gamma-1}{2} \mathfrak{M}_1^2} \\ \frac{\rho_1}{\rho_2} &= \frac{(1 + \gamma \mathfrak{M}_2^2)}{(1 + \gamma \mathfrak{M}_1^2)} \frac{(1 + \frac{\gamma-1}{2} \mathfrak{M}_2^2)}{(1 + \frac{\gamma-1}{2} \mathfrak{M}_1^2)} \end{aligned}$$

Shock waves are highly irreversible, since very large velocity and temperature gradients occur through shock itself; hence frictional, or dissipative effects must be present.[2]

$$\sigma_2 - \sigma_1 = \frac{N}{\gamma - 1} \ln \left[\frac{1 + \frac{\gamma-1}{2} \mathfrak{M}_1^2}{1 + \frac{\gamma-1}{2} \mathfrak{M}_2^2} \right] + N \ln \left[\frac{1 + \gamma \mathfrak{M}_2^2}{1 + \gamma \mathfrak{M}_1^2} \frac{(1 + \frac{\gamma-1}{2} \mathfrak{M}_2^2)}{(1 + \frac{\gamma-1}{2} \mathfrak{M}_1^2)} \right]$$

From Sabersky (9.29),(9.16),(9.31) [2]

$$\implies s_2 - s_1 = \frac{R\gamma}{\gamma - 1} \ln \left[\frac{2}{(\gamma + 1) \mathfrak{M}_1^2} + \frac{\gamma - 1}{\gamma + 1} \right] + \frac{R}{\gamma - 1} \ln \left[\frac{2\gamma \mathfrak{M}_1^2}{\gamma + 1} - \frac{\gamma - 1}{\gamma + 1} \right]$$

Part 3. Fluid Mechanics (revisited)

7. CONSERVATION

$$(18) \quad \frac{\partial \rho}{\partial t} + \nabla \cdot \mathbf{j} = 0$$

$$\frac{d}{dt} m \equiv \dot{m} = \frac{d}{dt} \int \rho \text{vol}^n = \int \left(\frac{\partial \rho}{\partial t} + \mathcal{L}_u \rho \right) \text{vol}^n = \int \left(\frac{\partial \rho}{\partial t} + (\mathbf{d}i_u + i_u \mathbf{d}) \rho \right) \text{vol}^n = \int \frac{\partial \rho}{\partial t} + \mathbf{d}i_u \rho \text{vol}^n$$

Now

$$\begin{aligned} \text{vol}^n &= \frac{\sqrt{g}}{n!} \varepsilon_{i_1 \dots i_n} dx^{i_1} \wedge \dots \wedge dx^{i_n} \\ i_{\mathbf{u}} \text{vol}^n &= \frac{\sqrt{g}}{(n-1)!} \varepsilon_{i_1 \dots i_n} u^{i_1} dx^{i_2} \wedge \dots \wedge dx^{i_n} \\ &\xrightarrow{\mathbf{d}} \frac{\varepsilon_{i_1 \dots i_n}}{(n-1)!} \frac{\partial(\sqrt{g} u^{i_1} \rho)}{\partial x^j} dx^j \wedge dx^{i_2} \wedge \dots \wedge dx^{i_n} = \frac{1}{\sqrt{g}} \frac{\partial(\sqrt{g} u^j \rho)}{\partial x^j} \text{vol}^n \\ &\implies \frac{\partial \rho}{\partial t} + \text{div } j = 0 \text{ or } \frac{\partial \rho}{\partial t} + \frac{1}{\sqrt{g}} \frac{\partial(\sqrt{g} u^j \rho)}{\partial x^j} = 0 \end{aligned}$$

As a sanity check, consider a change of coordinates from cylindrical to Cartesian coordinates.

Consider $g = g_{ij} dx^i \otimes dx^j \in T^*M \otimes T^*M \equiv \otimes^2 T^*M$.

For smooth (embedding or diffeomorphism) $F : N \rightarrow M$,

$$\text{in our particular case, } F(r, \phi, z) = (x, y, z) = \begin{pmatrix} r \cos \phi \\ r \sin \phi \\ z \end{pmatrix}$$

Now the pullback is $F^*g \in \otimes^2 T^*N$

$$\begin{aligned} F^*g(X, Y) &= g(F_*X, F_*Y) = g \left(\frac{\partial y^j}{\partial x^i} X^i \frac{\partial}{\partial y^j}, \frac{\partial y^k}{\partial x^l} Y^l \frac{\partial}{\partial y^k} \right) = \frac{\partial y^j}{\partial x^i} \frac{\partial y^k}{\partial x^l} X^i Y^l g \left(\frac{\partial}{\partial y^j}, \frac{\partial}{\partial y^k} \right) = \frac{\partial y^j}{\partial x^i} \frac{\partial y^k}{\partial x^l} X^i Y^l g_{jk} \\ &\implies (F^*g)_{ij} = \frac{\partial y^l}{\partial x^i} \frac{\partial y^m}{\partial x^j} g_{lm} \end{aligned}$$

If $g_{jk} = \delta_{jk}$ (usual Euclidean metric),

$$(F^*g)_{ij} = \frac{\partial y^k}{\partial x^i} \frac{\partial y^k}{\partial x^j} = \left(\frac{\partial y^i}{\partial x^k} \right)^T \frac{\partial y^k}{\partial x^j} = (D_x y)^T D_x y$$

(F^*g) is simply the Jacobian^T · Jacobian.

For cylindrical coordinates,

$$\begin{aligned} D_x y &= \begin{bmatrix} c\phi & -rs\phi & \\ s\phi & rc\phi & \\ & & 1 \end{bmatrix} \\ \implies F^*g &= \begin{bmatrix} c\phi & s\phi & \\ -rs\phi & rc\phi & \\ & & 1 \end{bmatrix} \begin{bmatrix} c\phi & -rs\phi & \\ s\phi & rc\phi & \\ & & 1 \end{bmatrix} = \begin{bmatrix} 1 & & \\ & r^2 & \\ & & 1 \end{bmatrix} \\ \sqrt{\det(F^*g)} &= \sqrt{r^2} = r \end{aligned}$$

So

$$\text{div } j = \frac{1}{r} \frac{\partial(r u^r \rho)}{\partial r} + \frac{1}{r} \frac{\partial(r u^\phi \rho)}{\partial \phi} + \frac{1}{r} \frac{\partial(r u^z \rho)}{\partial z} = \frac{1}{r} \frac{\partial(r u^r \rho)}{\partial r} + \frac{\partial(u^\phi \rho)}{\partial \phi} + \frac{\partial(u^z \rho)}{\partial z}$$

REFERENCES

- [1] L. D. Landau, E.M. Lifshitz, **Fluid Mechanics**, Second Edition: Volume 6 (Course of Theoretical Physics S) Butterworth-Heinemann, 1987, ISBN-13: 978-0750627672
- [2] Rolf H. Sabersky, Allen J. Acosta, Edward G. Hauptmann, E.M. Gates. **Fluid Flow: A First Course in Fluid Mechanics** (4th Edition). Prentice Hall. (August 22, 1998). ISBN-13: 978-0135763728
- [3] T. Frankel, **The Geometry of Physics**, Cambridge University Press, Second Edition, 2004.
- [4] Jürgen Jost. **Riemannian Geometry and Geometric Analysis (Universitext)**. 6th ed. 2011 Edition. Springer; 6th ed. 2011 edition (August 9, 2011). ISBN-13: 978-3642212970
- [5] Ovidiu Calin, Der-Chen Chang. **Geometric Mechanics on Riemannian Manifolds: Applications to Partial Differential Equations** (Applied and Numerical Harmonic Analysis). Birkhäuser. 2005. ISBN-13: 978-0817643546
- [6] Alexandre J. Chorin, Jerrold E. Marsden. **A Mathematical Introduction to Fluid Mechanics** (Texts in Applied Mathematics), Springer; 3rd edition, 2000. ISBN-13: 978-0387979182
- [7] Harsh Bhatia, Gregory Norgard, Valerio Pascucci, Peer-Timo Bremer. “The Helmholtz-Hodge DecompositionA Survey,” IEEE Transactions on Visualization and Computer Graphics, Vol. 19, 2013
- [8] John Lee, **Introduction to Smooth Manifolds** (Graduate Texts in Mathematics, Vol. 218), 2nd edition, Springer, 2012, ISBN-13: 978-1441999818
- [9] Darryl D. Holm, Tanya Schmäh, Cristina Stoica, **Geometric Mechanics and Symmetry: From Finite to Infinite Dimensions** (Oxford Texts in Applied and Engineering Mathematics) 2009, ISBN-13: 978-0199212903 ISBN-10: 0199212902
- [10] Tsutomu Kambe, **Geometrical Theory of Dynamical Systems and Fluid Flows**, Advanced Series in Nonlinear Dynamics: Volume 23, 2009, <http://www.worldscientific.com/worldscibooks/10.1142/7418> ISBN: 978-981-4282-24-6 (hardcover)

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