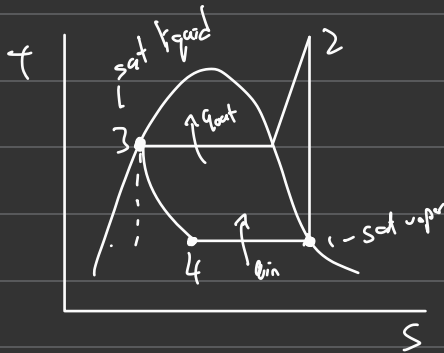
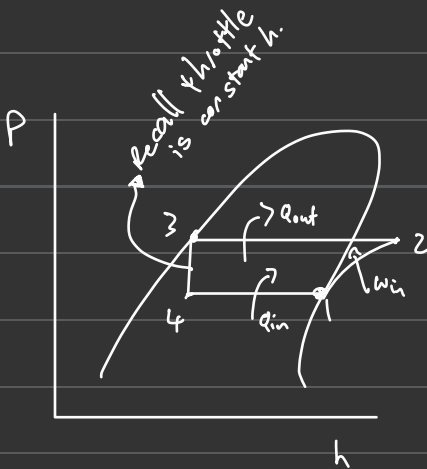


The Carnot refrigerator cannot be implemented practically. So:

Ideal Vapor-compression Ref. cycle:



- 1-2 isentropic compression
- 2-3 Constant  $p$  heat rejection - condenser  $T_{\text{room}}$
- 3-4 Throttling in exp. device
- 4-1 Constant  $p$  heat absorption - evaporator load heat



$$COP_R = \frac{q_L}{w_{net,in}} = \frac{h_1 - h_4}{h_2 - h_1}$$

$h_1 = h_g @ P$   
 $h_3 = h_f @ P$

$$COP_{HP} = \frac{q_H}{w_{net,in}} = \frac{h_2 - h_3}{h_2 - h_1}$$

steady flow

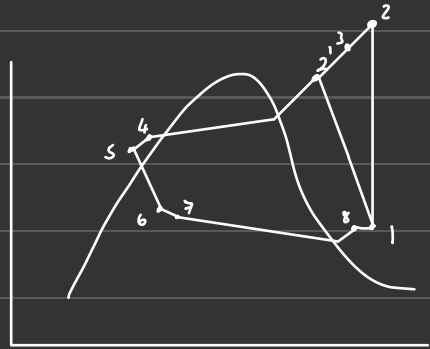
Do not use  $T$  here as this is not Carnot.

1 ton?

## Real Vapor-compressor refs.

Due to irreversibilities,

- fluid friction
- heat transfer v. surroundings



1. non-isentropic compression
2. superheated vapor at evap. exit
3. subcooled liq. at condenser exit
4. Pressure drops in condenser and evap.

## Dual stage refs. cycle.

$$P_i = \sqrt{P_L P_H} \quad \text{optimal intermediate P.}$$