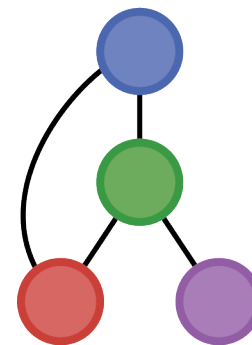


# Automatic Generation of JuMP.jl Constraints from ModelingToolkit.jl Models

Dimitri Alston, Joseph Choi, Pengfei Xu, Robert Gottlieb

Matthew Stuber, P&W Associate Professor in  
Advanced Systems Engineering

November 18<sup>th</sup>, 2025



Process Systems and  
Operations Research  
Laboratory

# Motivation

## Dynamic Optimization

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{calc} = x_{A,i} + \frac{2}{21} x_{B,i} + \frac{2}{21} x_{D,i}$$

$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

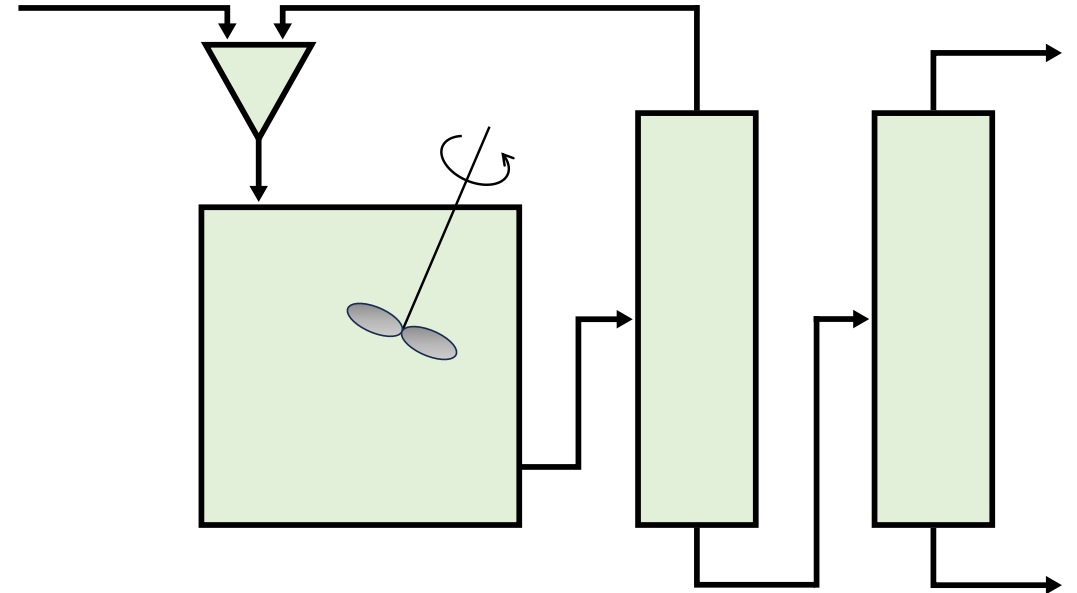
$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left( \frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

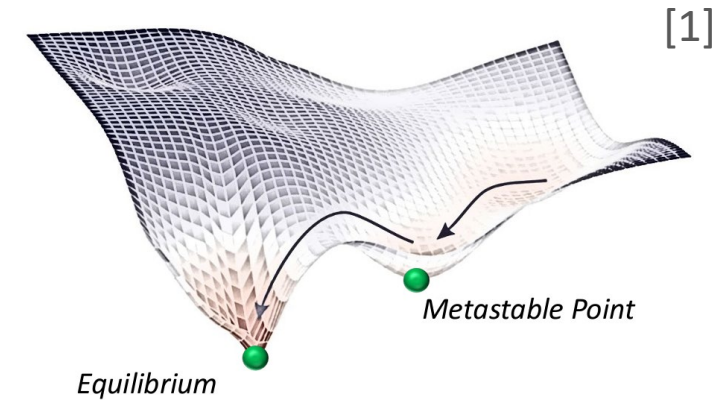
$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

## Process Flow Sheets



# Deterministic Global Optimization

- Nonconvex problems arise in many applications
  - Thermodynamic stability
  - Kinetic parameter estimation
  - Advanced control systems
  - Design under uncertainty
  - Etc.



$$\min_{\mathbf{p} \in P} \phi(\mathbf{x}(\mathbf{p}, t_f), \mathbf{p})$$

$$\text{s.t. } \dot{\mathbf{x}}(\mathbf{p}, t) = \mathbf{f}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}, t) = \mathbf{0} \quad \forall t \in I = [t_0, t_f]$$

$$\mathbf{x}(\mathbf{p}, t_0) = \mathbf{x}_0(\mathbf{p})$$

$$\mathbf{g}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}) \leq \mathbf{0}$$

$$P = \{\mathbf{p} \in \mathbb{R}^m : \mathbf{p}^L \leq \mathbf{p} \leq \mathbf{p}^U\}$$

[1] Grajcarova, L. Simulations of structural phase transitions in crystals using ab initio metadynamics. INIS-IAEA. (2013).

# Kinetic Parameter Estimation

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

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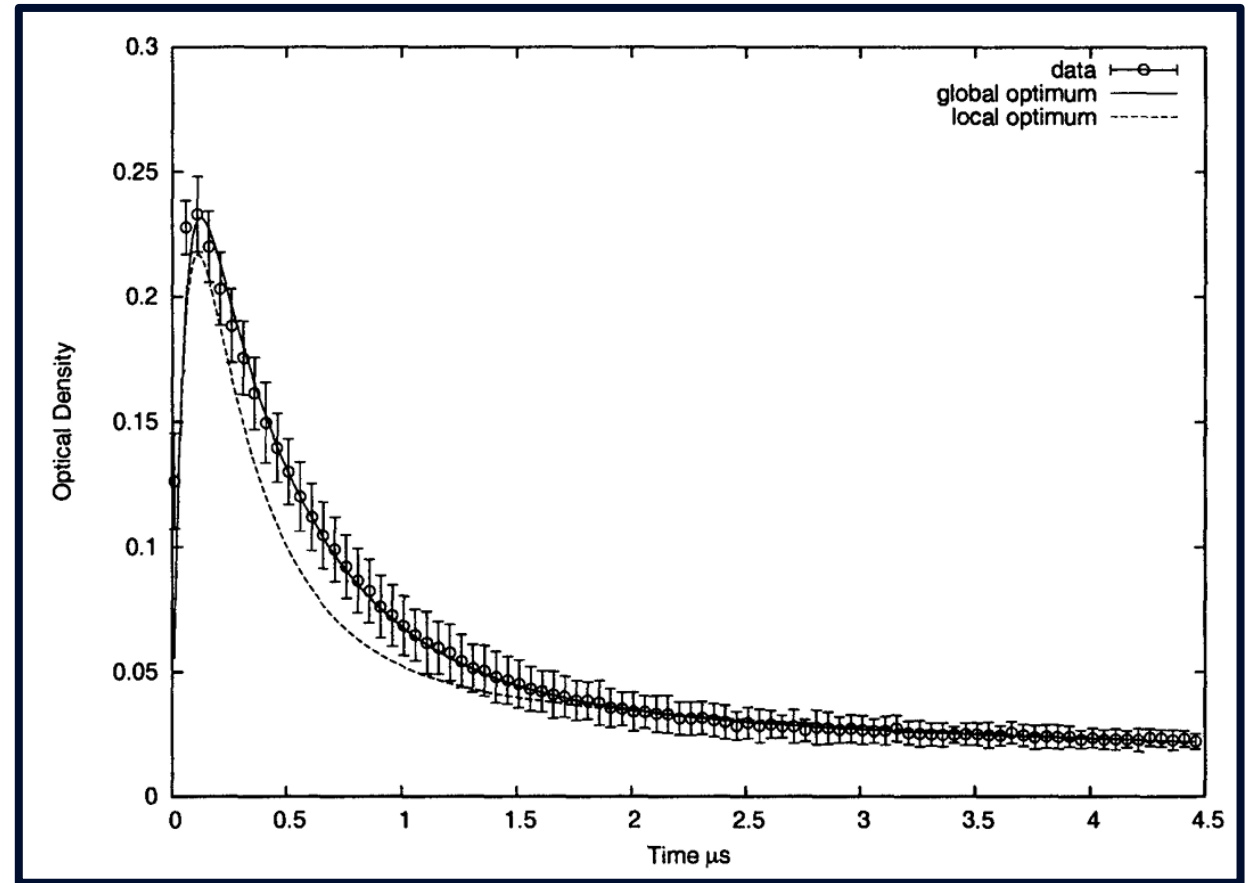
$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left( \frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

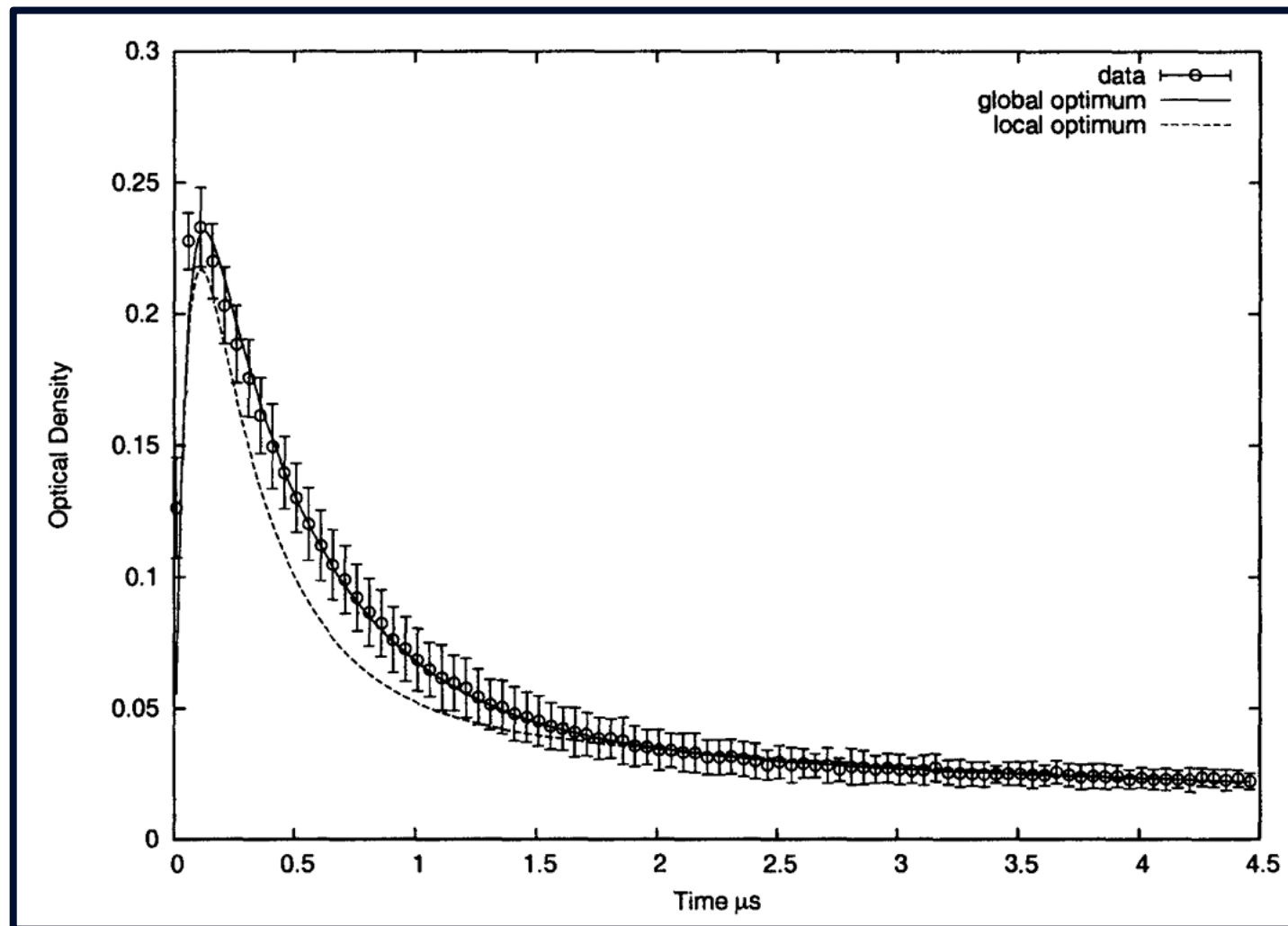
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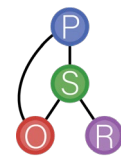


[2] Taylor, J.W., et al. Direct measurement of the fast, reversible addition of oxygen to cyclohexadienyl radicals in nonpolar solvents, The Journal of Physical Chemistry A. 108, 7193-7203 (2004).

# Kinetic Parameter Estimation



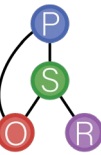
[2] Taylor, J.W., et al. Direct measurement of the fast, reversible addition of oxygen to cyclohexadienyl radicals in nonpolar solvents, *The Journal of Physical Chemistry A*. 108, 7193-7203 (2004).



# EAGO.jl

## Easy Advanced Global Optimization

- Open-source deterministic global solver for nonconvex MINLPs
  - Semi-infinite programs (SIPs)
  - Dynamic optimization
  - User-defined functions
- Uses branch-and-bound (B&B) to guarantee global optimality or infeasibility
- Applies McCormick-based relaxations for convex lower-bounding problems
- Designed in conjunction with JuMP



# Recent Advances in EAGO.jl

## Easy Advanced Global Optimization

- Improved bilinear relaxations<sup>[4]</sup>
- Optimization of ANNs<sup>[5]</sup>
- Custom implementation of PDLP on GPUs



[4] Wilhelm, M.E. and Stuber, M.D. Improved Convex and Concave Relaxations of Composite Bilinear Forms. Journal of Optimization Theory and Applications. 197, 174-204 (2023).

[5] Wang, C., Wilhelm, M.E., and Stuber, M.D. Semi-Infinite Optimization with Hybrid Models. Industrial & Engineering Chemistry Research. 61, 5239-5254 (2022).



# Recent

## Easy Advances

- Improved
- Optimization
- Custom in



eago



All

Images

Videos

News

Maps

Search Assist

Duck.ai



Protected



New Zealand

Safe search: moderate

Any time

eago.co.nz  
eago.co.nz

...

### Eago Sanitary - New Zealand

As one of the leading bathroom product and sanitary ware manufacturers in China, **EAGO's** series range from intelligent steam shower houses and shower enclosures, through to massage bathtubs, common acrylic bathtubs, water closets, and glass, acrylic and ceramic washbasins.

#### Home

Welcome To Eago NZ As one of the leading bathroom product and sanitary...

#### Company Profile

In January, 2004, Jin Jie Co., Ltd. moved its production to the new factory and...

#### Spa Baths

EAGO has a wide range of showers to cater for the widest tastes from...

#### Products

Eago Sanitary - New Zealand - Products

store.eagolighting.co.nz  
<https://store.eagolighting.co.nz> > store > default > customer-login

...

### EAGO Lighting - Welcome

Fill in the contact form to leave a message 46C Parkway Drive, Rosedale, Auckland 0632  
[sales@eagolighting.co.nz](mailto:sales@eagolighting.co.nz) +64 9 948 6128

Eagousa.com  
<https://eagousa.com> > toilets.html

...

### EAGO Toilets

**EAGO R-359SEAT** Replacement Soft Closing Toilet Seat for TB359 MSRP: \$160.00 Add to Compare  
**EAGO TB353** One Piece Dual High Efficiency Low Flush Eco-Friendly Toilet MSRP: \$740.00 Add to Compare  
**EAGO R-353LID** Replacement Ceramic Toilet Lid for TB353 MSRP: \$60.00 Add to Compare...



23).

[4] Wilhelm, M.E. and Stuber, M.D.

[5] Wang, C., Wilhelm, M.E., and St





# Should you use JuMP?

## When should you not use JuMP?

JuMP supports a broad range of optimization classes. However, there are still some that it doesn't support, or that are better supported by other software packages.

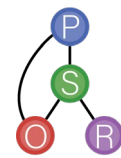
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Packages in Julia compose well. It's common for people to pick two unrelated packages and use them in conjunction to create novel behavior. JuMP isn't one of those packages.

If you want to **optimize an ordinary differential equation** from [DifferentialEquations.jl](#) or tune a neural network from [Flux.jl](#), consider using other packages such as:

- [Optim.jl](#)
- [Optimization.jl](#)
- [NLPMODELS.jl](#)
- [Nonconvex.jl](#)

[6] [https://jump.dev/JuMP.jl/stable/should\\_i\\_use/#When-should-you-not-use-JuMP?](https://jump.dev/JuMP.jl/stable/should_i_use/#When-should-you-not-use-JuMP?)



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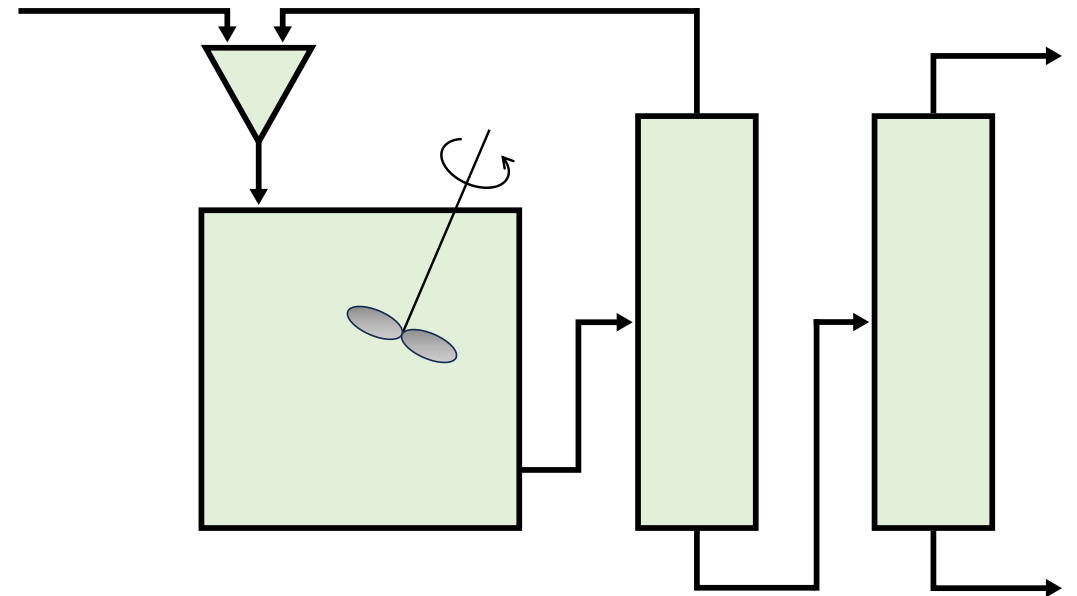
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$$\frac{dx_T}{dt} = -k_1 x_T x_F$$

$$\frac{dx_F}{dt} = -k_1 x_T x_F$$

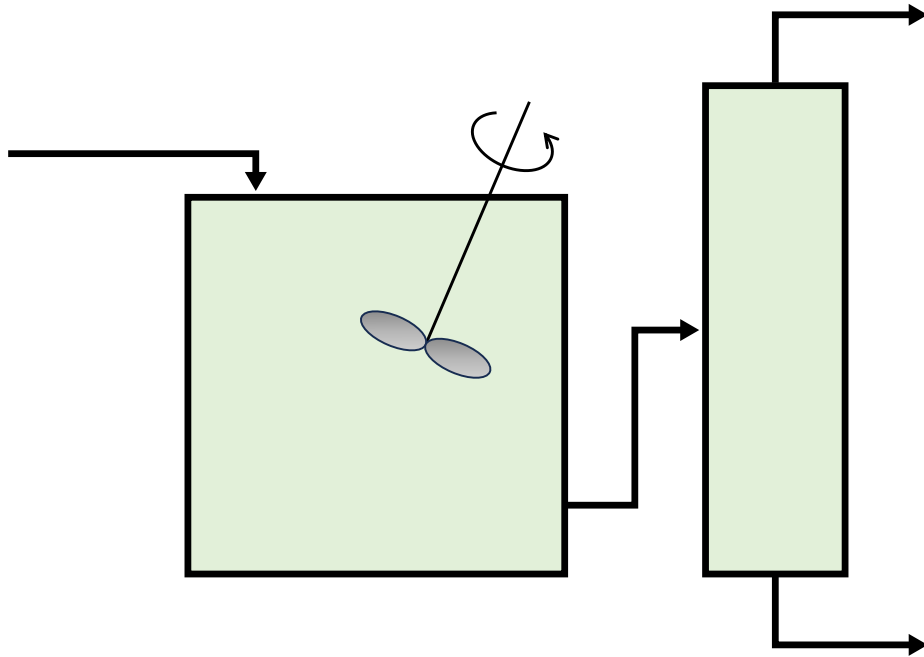
## Process Flow Sheets



# Causal vs Acausal Modeling

**Causal/Sequential-Modular**

**Acausal/Equation-Oriented**



$$y_{2,A} + y_{2,B} + y_{2,C} = 1$$

$$y_{2,B}F = y_{1,B} + Vr_B$$

$$y_{2,C}F = y_{1,C} + Vr_C$$

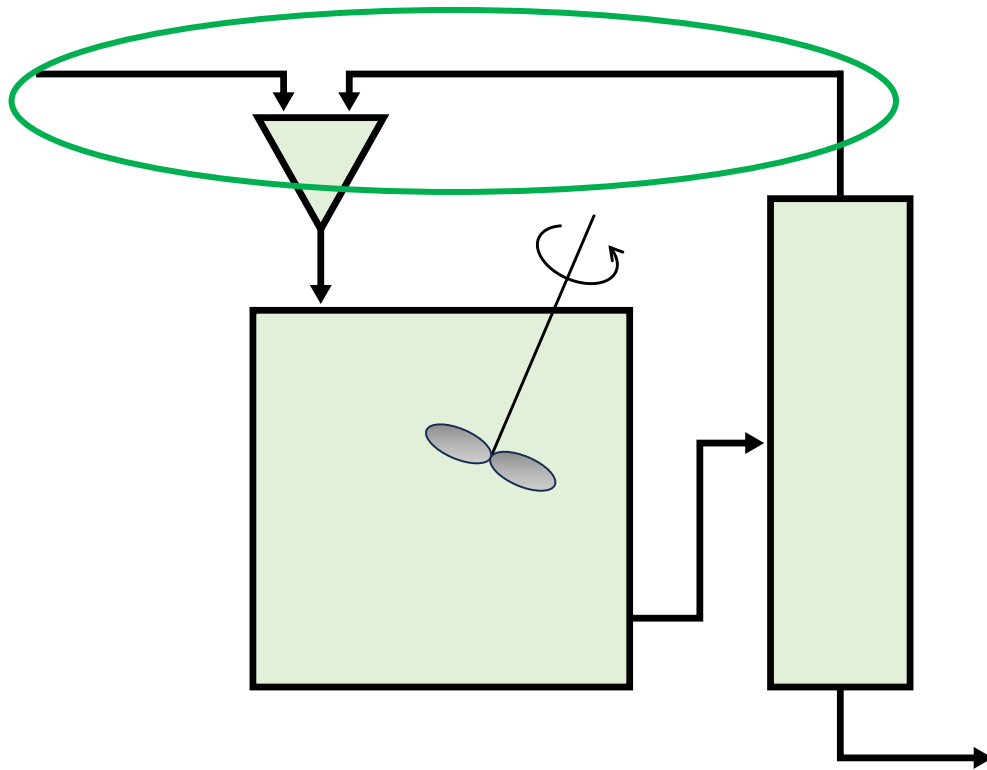
$$y_{3,A} = y_{1,A} - Vr_A$$

$$y_{4,B} + y_{4,C} = y_{2,B} + y_{2,C}$$

# Causal vs Acausal Modeling

## Causal/Sequential-Modular

## Acausal/Equation-Oriented



$$y_{3,A} + y_{3,B} + y_{3,C} = 1$$

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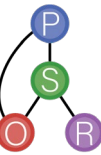
$$y_{4,A} = y_{2,A} - Vr_A$$

$$y_{5,B} + y_{5,C} = y_{3,B} + y_{3,C}$$

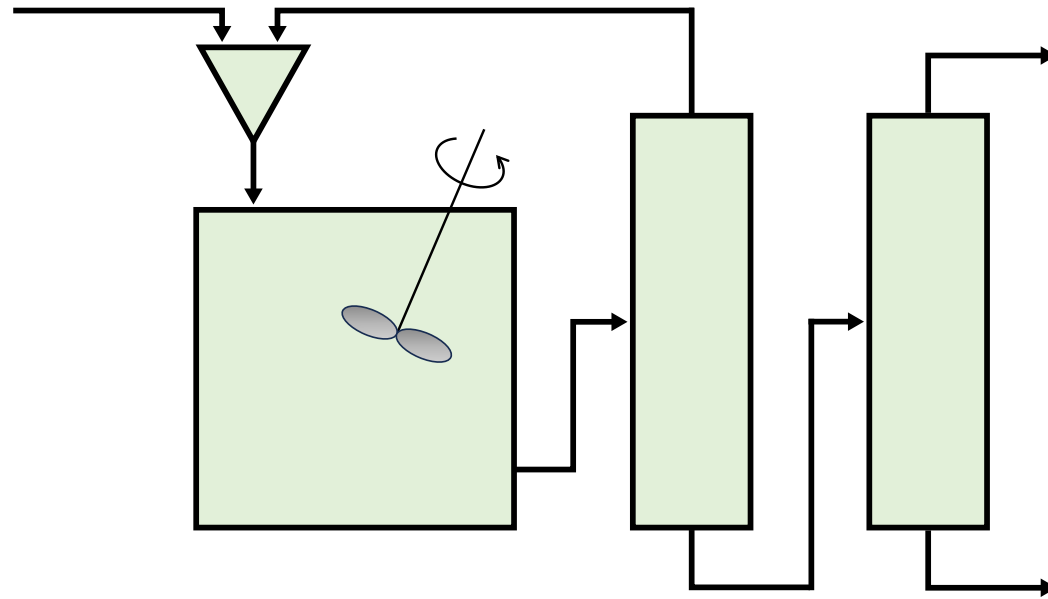
$$y_{2,A} = y_{1,A} + y_{4,A}$$

# ModelingToolkit.jl

- Open-source, acausal modeling framework in Julia
- Supports a broad range of system types
  - ODEs, SDEs, PDEs
  - Nonlinear systems
  - Optimization problems
- Automatically composes, transforms, and reduces models
  - Dimensionality reduction through algebraic simplification



# Componentized Model



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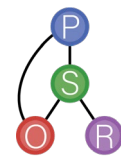
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# Optimization.jl

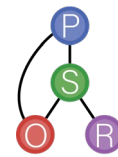
## Modeling Optimization Problems

ModelingToolkit.jl is not only useful for generating initial value problems (`ODEProblem`). The package can also build optimization systems.

### ! Note

The high level `@mtkmodel` macro used in the [getting started tutorial](#) is not yet compatible with `OptimizationSystem`. We thus **have to use a lower level interface to define optimization systems**. For an introduction to this interface, read the [programmatically generating Systems tutorial](#).

[9] <https://docs.sciml.ai/ModelingToolkit/stable/tutorials/optimization/>





# Optimization in Julia

## SciML

[10]



- 25+ libraries, 100+ solvers
- No deterministic global optimization support

## JuMP

[11]



- Algebraic modeling language designed for mathematical optimization

[10] Dixit, V.K. and Rackauckas C. Optimization.jl: A Unified Optimization Package. (2023).

[11] Lubin, M., Dowson, O., Garcia, J.D. et al. JuMP 1.0: recent improvements to a modeling language for mathematical optimization. *Math. Prog. Comp.* 15, 581–589 (2023).



# Optimization in Julia

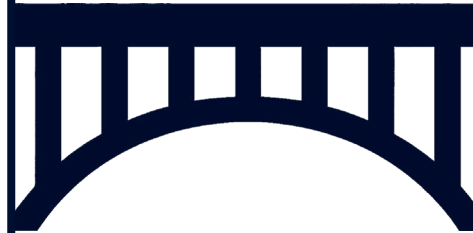
**SciML**

[10]



- 25+ libraries, 100+ solvers
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**EOptInterface**  
Abstraction layer



**JuMP**

[11]



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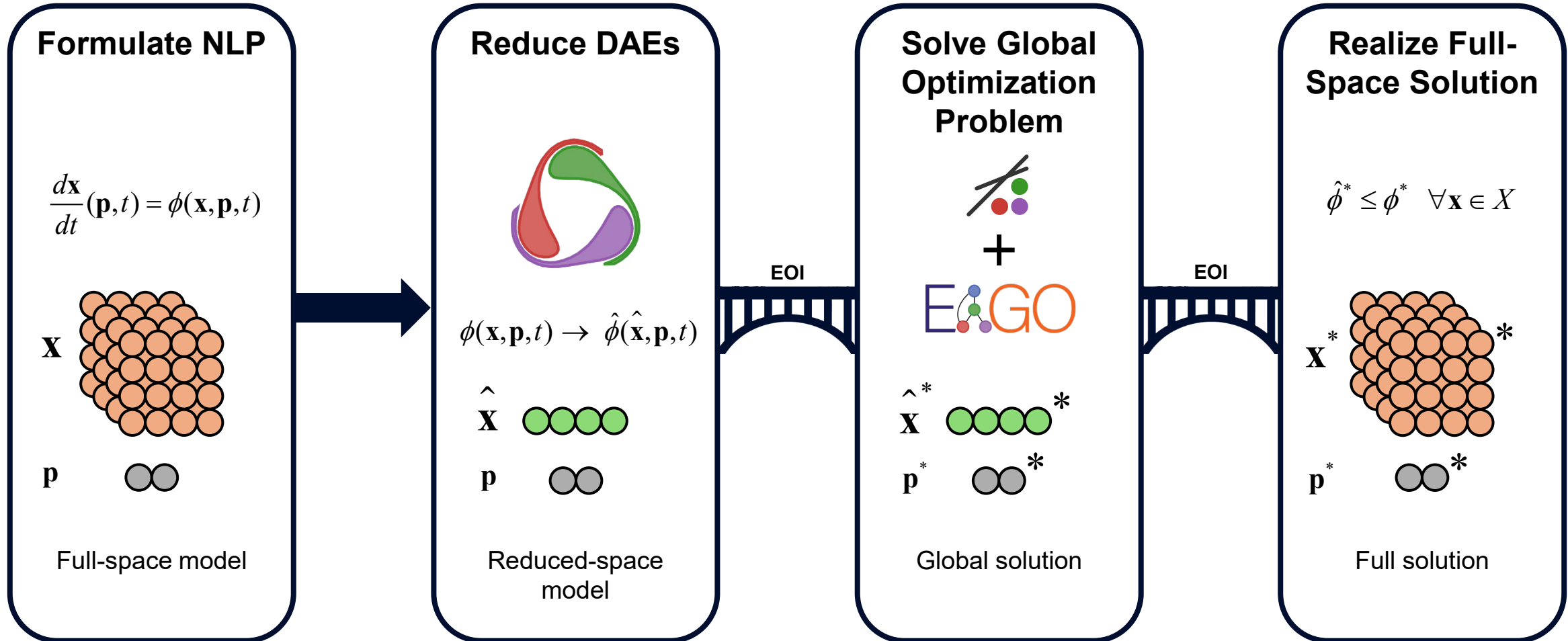
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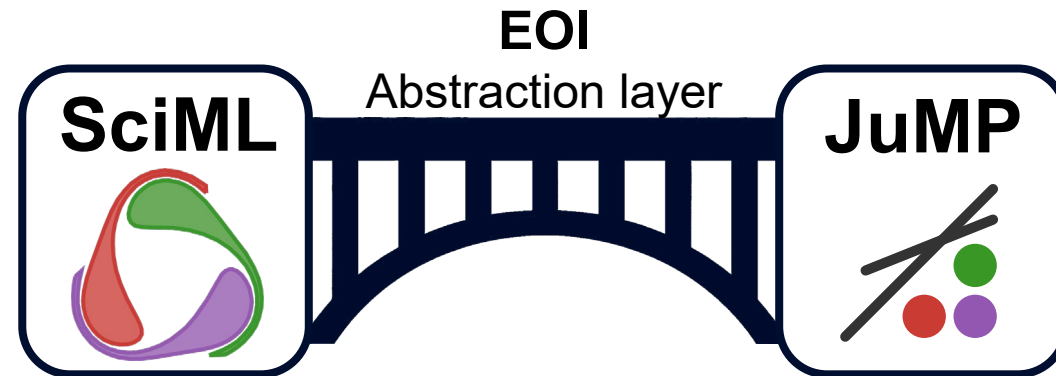
# EOptInterface.jl

Equation-oriented Optimization Interface (EOI)



# EOptInterface Features

- Automatically generate JuMP constraints from ModelingToolkit models
- Display decision variables
- Detect and directly transcribe ODEs
- Calculate full-space solutions



# Case Studies

- 1) Dynamic Kinetic Parameter Estimation
- 2) Steady-State Process Flow Sheet
- 3) Nonlinear Model Predictive Control (NMPC)

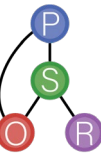


# Dynamic Kinetic Parameter Estimation

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$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$\begin{aligned} I_i^{calc} &= x_{A,i} + \frac{2}{21} x_{B,i} + \frac{2}{21} x_{D,i} \\ \frac{dx_A}{dt} &= k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2 \\ \frac{dx_B}{dt} &= c_{O_2} k_{3f} x_A - \left( \frac{k_{3f}}{K_3} + k_4 \right) x_B \\ \frac{dx_D}{dt} &= c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D \\ \frac{dx_Y}{dt} &= -k_{1s} x_Z x_Y \\ \frac{dx_Z}{dt} &= -k_1 x_Z x_Y \end{aligned}$$



# Dynamic Kinetic Parameter Estimation

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

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$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

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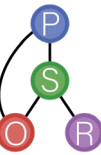
$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

```
@mtkmodel KineticParameterEstimation begin
  @parameters begin
    T = 273.0
    K_2 = 46.0*exp(6500.0/T - 18.0)
    K_3 = 2.0*K_2
    k_1 = 53.0
    k_1s = k_1*1e-6
    k_5 = 1.2e-3
    c_O2 = 2e-3

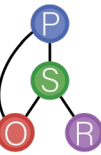
    k_2f
    k_3f
    k_4
  end
  @variables begin
    x_A(t) = 0.0
    x_B(t) = 0.0
    x_D(t) = 0.0
    x_Y(t) = 0.4
    x_Z(t) = 140.0
    I(t)
  end
  @equations begin
    D(x_A) ~ k_1*x_Z*x_Y - c_O2*(k_2f + k_3f)*x_A + k_2f/K_2*x_D + k_3f/K_3*x_B - k_5*x_A^2
    D(x_B) ~ c_O2*k_3f*x_A - (k_3f/K_3 + k_4)*x_B
    D(x_D) ~ c_O2*k_2f*x_A - k_2f/K_2*x_D
    D(x_Y) ~ -k_1s*x_Z*x_Y
    D(x_Z) ~ -k_1*x_Z*x_Y
    I ~ x_A + 2/21*x_B + 2/21*x_D
  end
end
```



# Dynamic Kinetic Parameter Estimation

- EOptInterface

```
if integrator == "Explicit Euler"  
    @constraint(model, [j in 1:V, i in 1:(N-1)], xs[j,i+1] == xs[j,i] + t_step*dx[j](xs[:,i]..., ps...))  
elseif integrator == "Implicit Euler"  
    @constraint(model, [j in 1:V, i in 1:(N-1)], xs[j,i+1] == xs[j,i] + t_step*dx[j](xs[:,i+1]..., ps...))
```





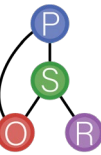
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    @constraint(model, [j in 1:V, i in 1:(N-1)], xs[j,i+1] == xs[j,i] + t_step*dx[j](xs[:,i+1]..., ps...))
```

- InfiniteOpt

```
problem = JuMPDynamicOptProblem(system, [u0_map; p_map], (t_start, t_end); dt = 0.001)  
solution = solve(problem, JuMPCollocation(Ipopt.Optimizer, constructRK4()))  
  
problem = InfiniteOptDynamicOptProblem(system, [u0_map; p_map], t_span; steps = 100)  
solution = solve(problem, InfiniteOptCollocation(Ipopt.Optimizer))
```



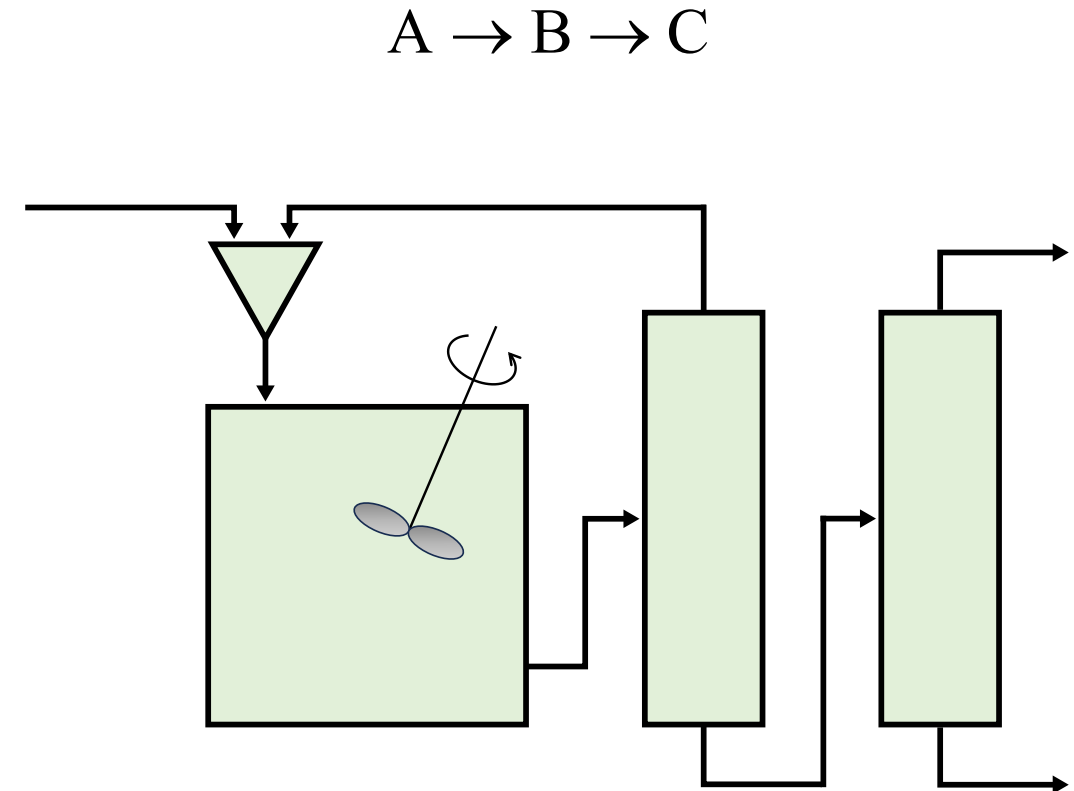
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- 2) Steady-State Process Flow Sheet
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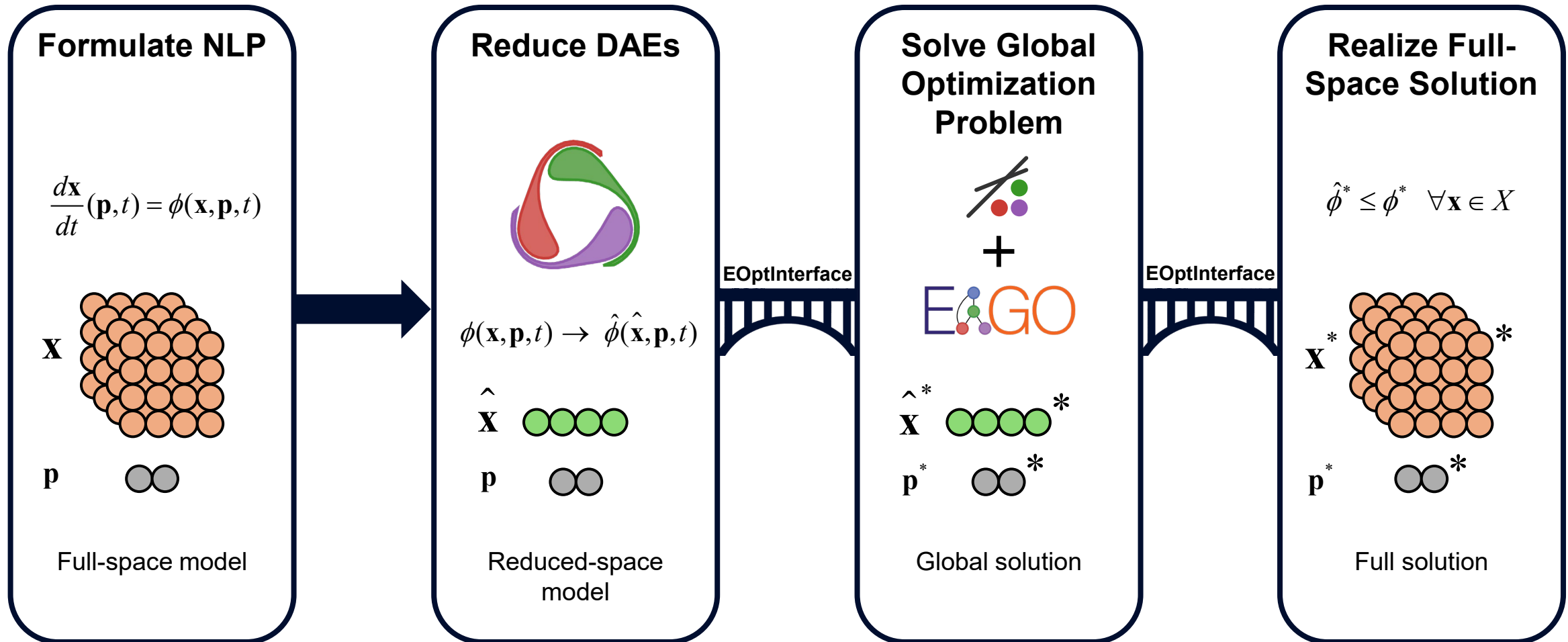


# Steady-State Process Flow Sheet

- Minimize total annualized costs
- Design variables:
  - Feed flowrate
  - Reactor volume



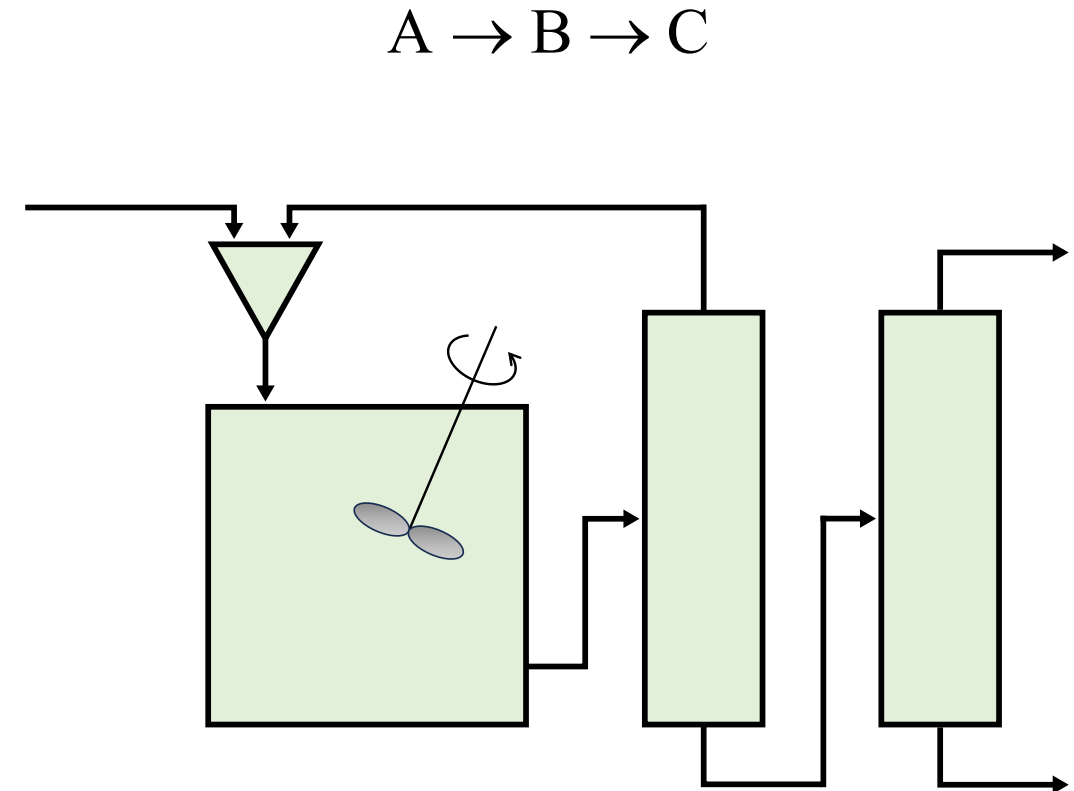
# EOI Workflow



# Steady-State Process Flow Sheet

- Minimize total annualized costs
- Design variables:
  - Feed flowrate
  - Reactor volume

Model	Number of variables	Solve Time (s)
Full-space	50	202.0
Reduced-space	6	3.441

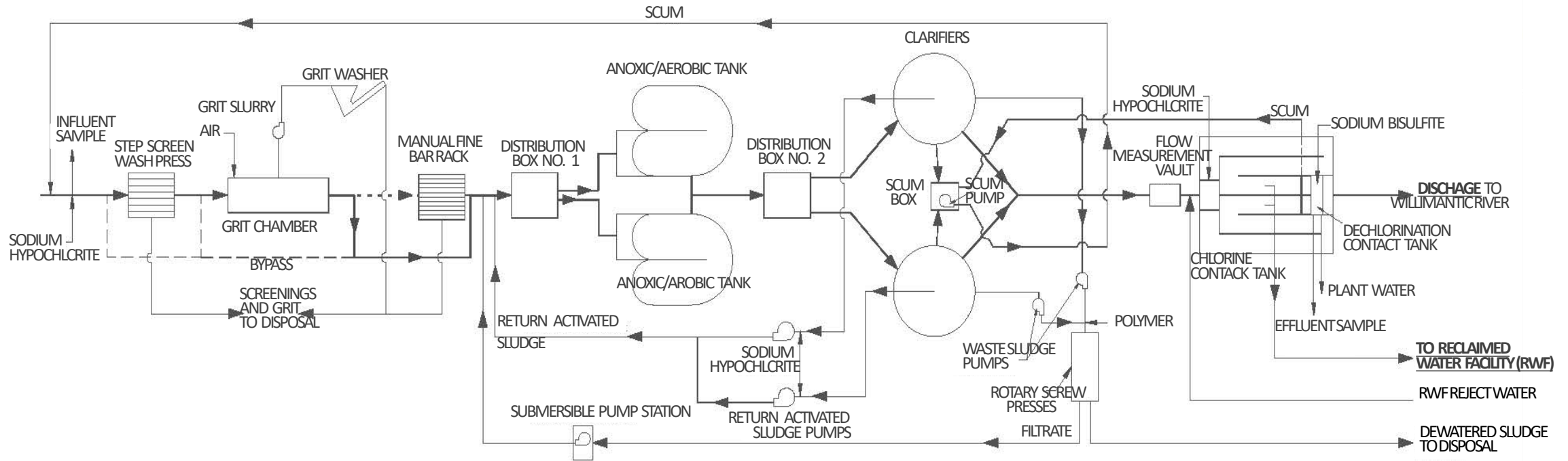


# Case Studies

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  - Exploit dimensionality reduction from ModelingToolkit for optimization
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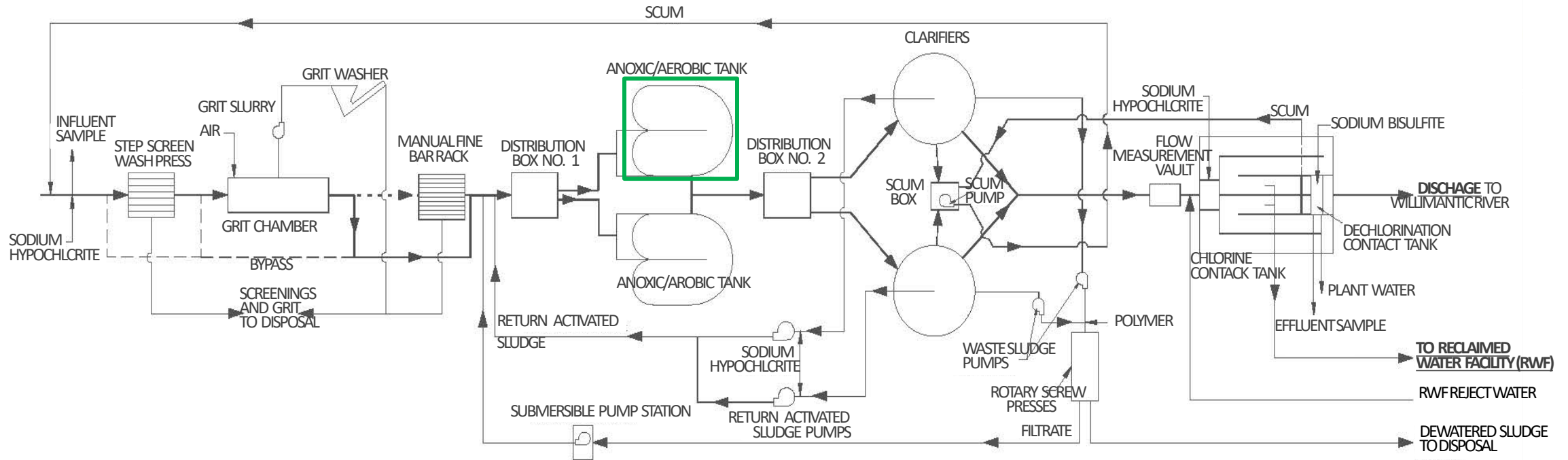


# Nonlinear Model Predictive Control



UConn Water Resource Recovery Facility

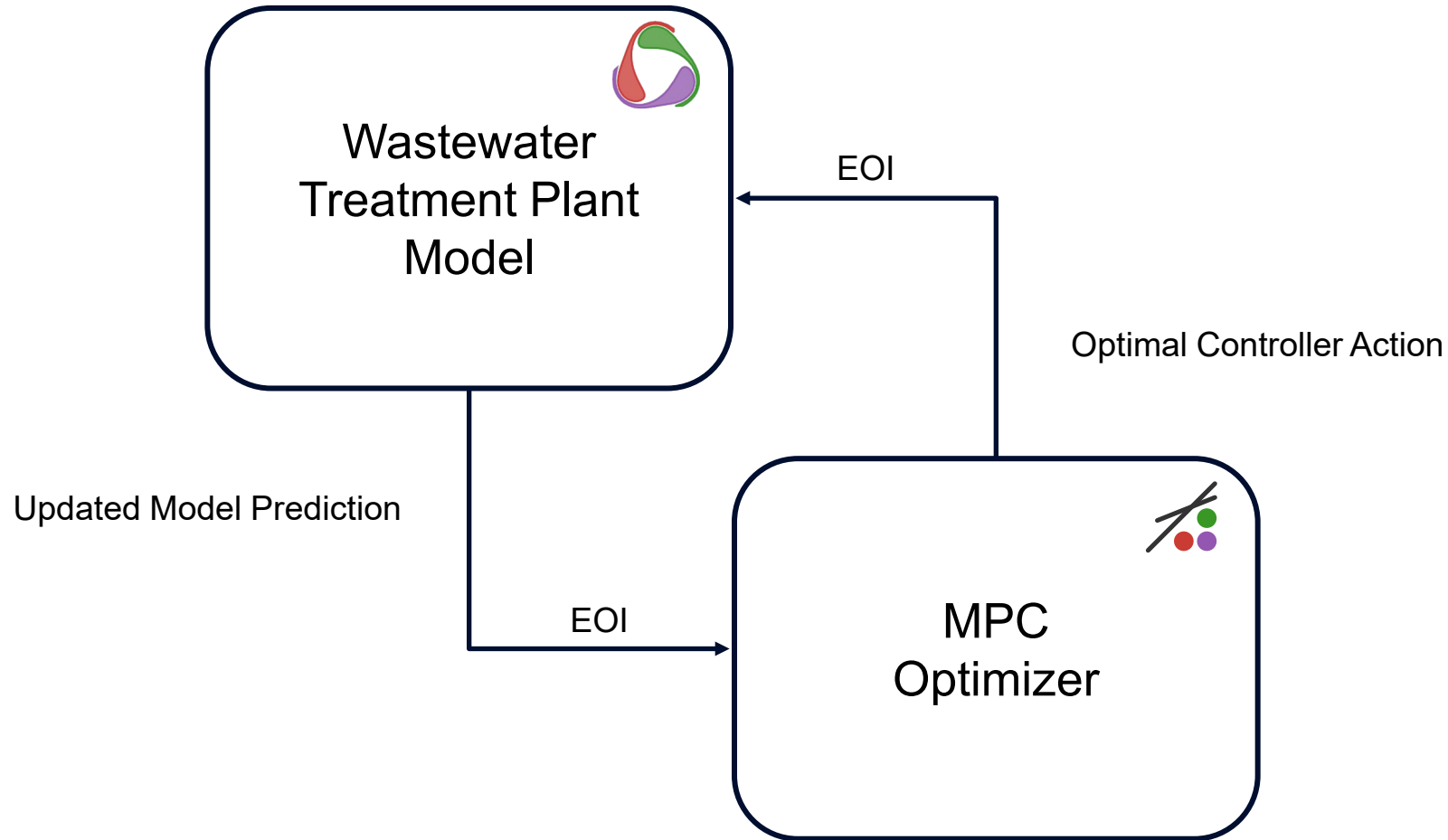
# Nonlinear Model Predictive Control



UConn Water Resource Recovery Facility



# Nonlinear Model Predictive Control



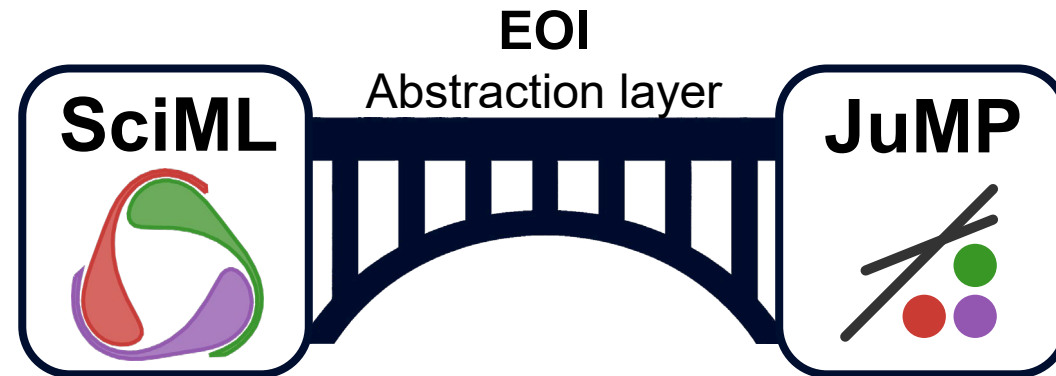
# Case Studies

- 1) Dynamic Kinetic Parameter Estimation
  - Direct transcription of ODEs
- 2) Steady-State Process Flow Sheet
  - Exploit dimensionality reduction from ModelingToolkit for optimization
- 3) Nonlinear Model Predictive Control (NMPC)
  - Fully integrated real-time closed-loop NMPC



# Conclusion

- **EOptInterface.jl**
  - Seamlessly integrates modeling and simulation with formal optimization
  - Contains multiple discretization methods for ODEs
  - You can use your favorite solver in JuMP



- **Future Work**
  - EAGODynamicOptimizer.jl

# Acknowledgements

Members of the Process Systems and Operations Research Laboratory at the University of Connecticut (<https://www.psor.uconn.edu>)

**UConn**  
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Process Systems and  
Operations Research  
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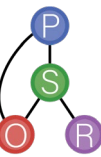
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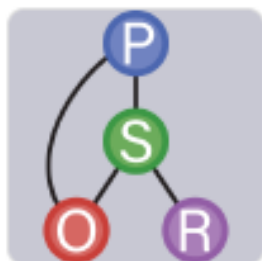
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# Questions?



## Process Systems and Operations Research Laboratory

The PSOR Laboratory at UConn develops numerical analysis methods and software for process systems engineering applications.

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