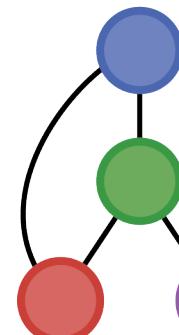


Automatic Generation of JuMP.jl Constraints from ModelingToolkit.jl Models

Dimitri Alston, Joseph Choi, Pengfei Xu, Robert Gottlieb

Matthew Stuber, P&W Associate Professor in
Advanced Systems Engineering

November 18th, 2025



Process Systems and
Operations Research
Laboratory

Motivation

Dynamic Optimization

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{calc} = x_{A,i} + \frac{2}{21}x_{B,i} + \frac{2}{21}x_{D,i}$$

$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

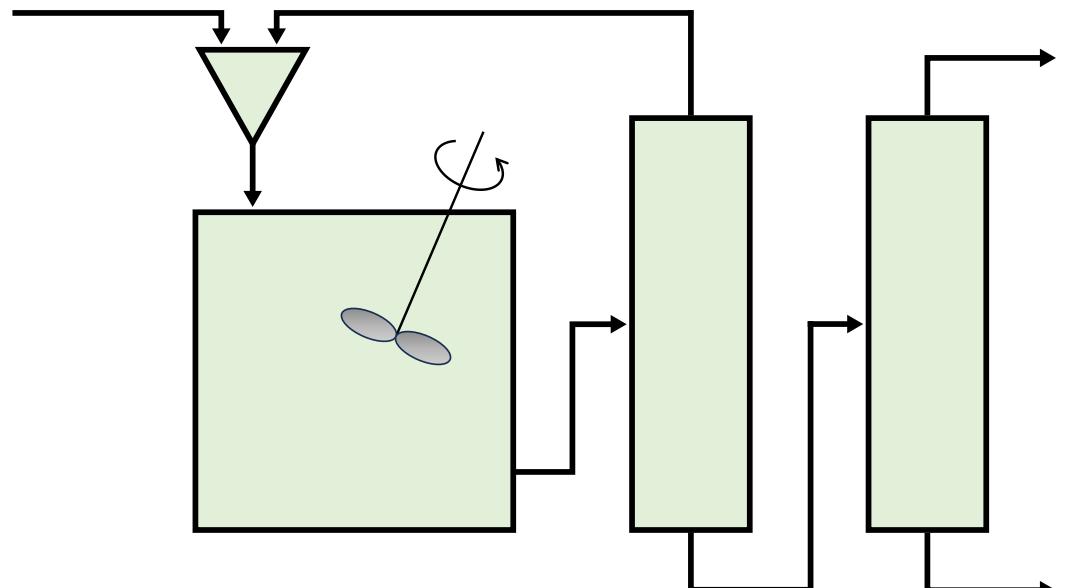
$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

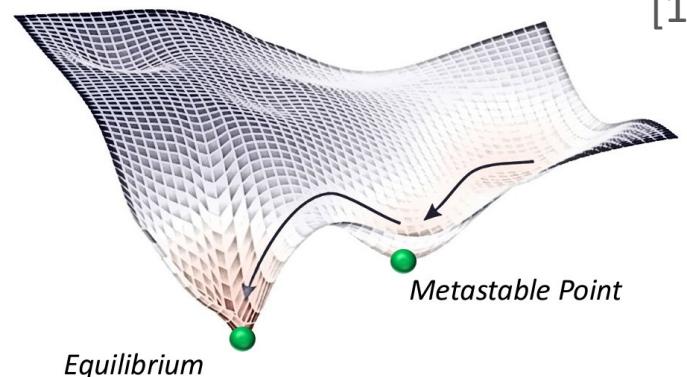
$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

Process Flow Sheets



Deterministic Global Optimization

- Nonconvex problems arise in many applications
 - Thermodynamic stability
 - Kinetic parameter estimation
 - Advanced control systems
 - Design under uncertainty
 - Etc.



$$\min_{\mathbf{p} \in P} \phi(\mathbf{x}(\mathbf{p}, t_f), \mathbf{p})$$

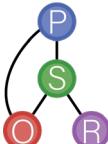
$$\text{s.t. } \dot{\mathbf{x}}(\mathbf{p}, t) = \mathbf{f}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}, t) = \mathbf{0} \quad \forall t \in I = [t_0, t_f]$$

$$\mathbf{x}(\mathbf{p}, t_0) = \mathbf{x}_0(\mathbf{p})$$

$$\mathbf{g}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}) \leq \mathbf{0}$$

$$P = \{\mathbf{p} \in \mathbb{R}^m : \mathbf{p}^L \leq \mathbf{p} \leq \mathbf{p}^U\}$$

[1] Grajcarova, L. Simulations of structural phase transitions in crystals using ab initio metadynamics. INIS-IAEA. (2013).



Kinetic Parameter Estimation

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{calc} = x_{A,i} + \frac{2}{21}x_{B,i} + \frac{2}{21}x_{D,i}$$

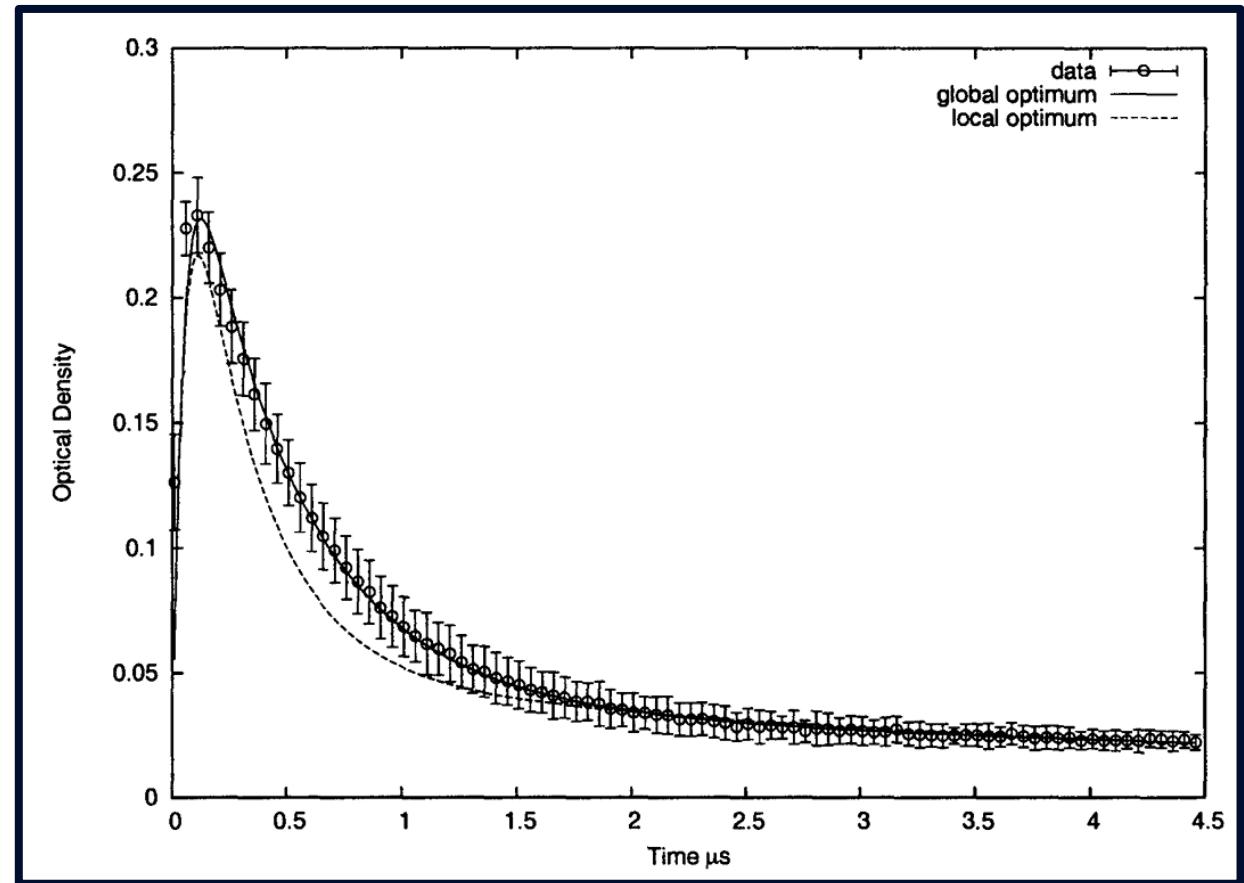
$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

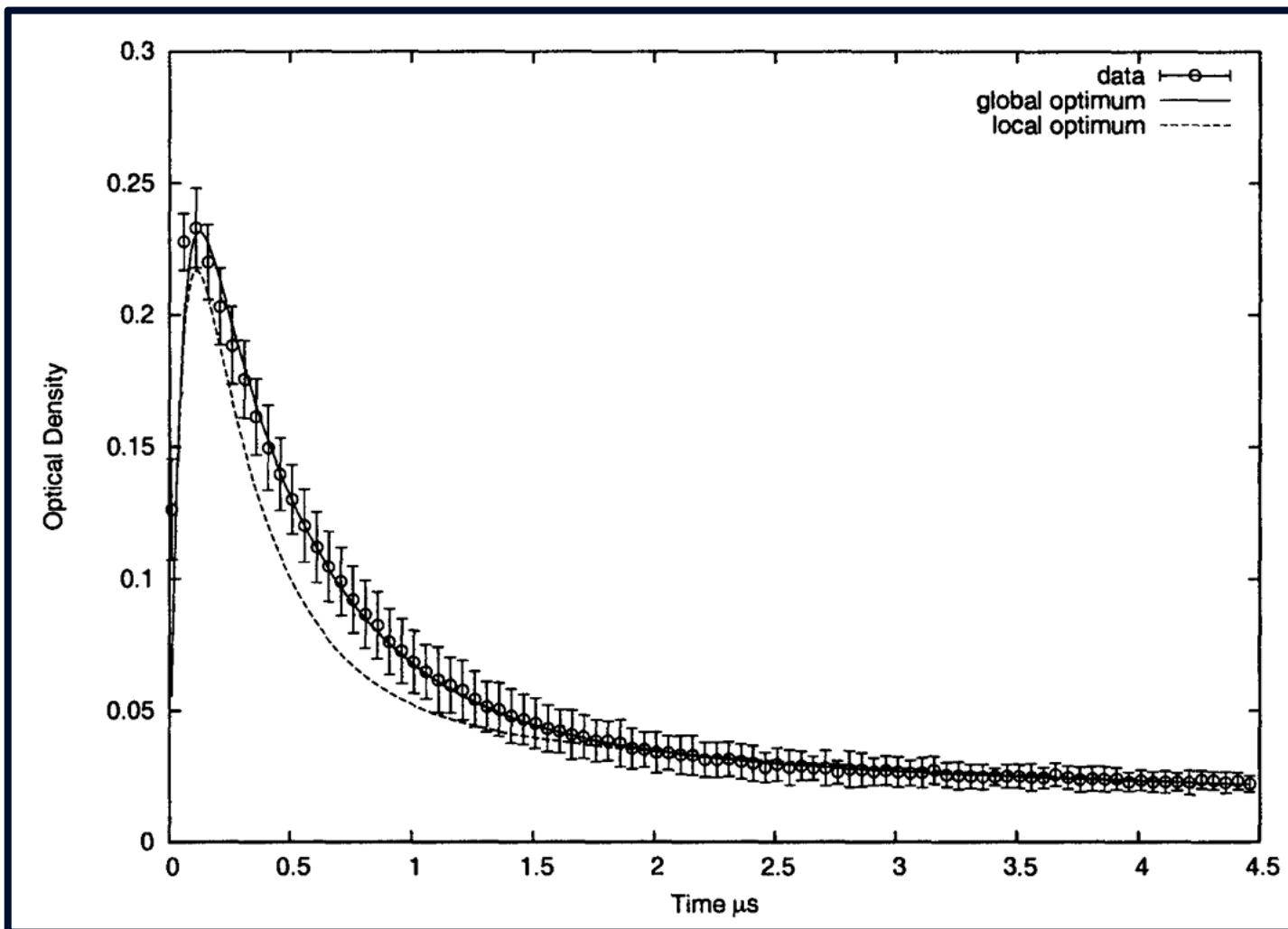
$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$



[2] Taylor, J.W., et al. Direct measurement of the fast, reversible addition of oxygen to cyclohexadienyl radicals in nonpolar solvents, The Journal of Physical Chemistry A. 108, 7193-7203 (2004).

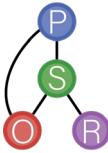


Kinetic Parameter Estimation



[2] Taylor, J.W., et al. Direct measurement of the fast, reversible addition of oxygen to cyclohexadienyl radicals in nonpolar solvents, *The Journal of Physical Chemistry A*. 108, 7193-7203 (2004).

JuMP-dev 2025



EAGO.jl

Easy Advanced Global Optimization

- Open-source deterministic global solver for nonconvex MINLPs
 - Semi-infinite programs (SIPs)
 - Dynamic optimization
 - User-defined functions
- Uses branch-and-bound (B&B) to guarantee global optimality or infeasibility
- Applies McCormick-based relaxations for convex lower-bounding problems
- Designed in conjunction with JuMP



Recent Advances in EAGO.jl

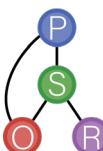
Easy Advanced Global Optimization

- Improved bilinear relaxations^[4]
- Optimization of ANNs^[5]
- Custom implementation of PDLP on GPUs



[4] Wilhelm, M.E. and Stuber, M.D. Improved Convex and Concave Relaxations of Composite Bilinear Forms. *Journal of Optimization Theory and Applications*. 197, 174-204 (2023).

[5] Wang, C., Wilhelm, M.E., and Stuber, M.D. Semi-Infinite Optimization with Hybrid Models. *Industrial & Engineering Chemistry Research*. 61, 5239-5254 (2022).



Recent

Easy Advanced

- Improved
- Optimization
- Custom in



eago



All Images Videos News Maps

Search Assist

Duck.ai



Protected

New Zealand

Safe search: moderate

Any time

eago.co.nz
eago.co.nz



Eago Sanitary - New Zealand

As one of the leading bathroom product and sanitary ware manufacturers in China, EAGO's series range from intelligent steam shower houses and shower enclosures, through to massage bathtubs, common acrylic bathtubs, water closets, and glass, acrylic and ceramic washbasins.

Home

Welcome To Eago NZ As one of the leading bathroom product and sanitary...

Company Profile

In January, 2004, Jin Jie Co., Ltd. moved its production to the new factory and...

Spa Baths

EAGO has a wide range of showers to cater for the widest tastes from...

Products

Eago Sanitary - New Zealand - Products

store.eagolighting.co.nz

<https://store.eagolighting.co.nz> > store > default > customer-login



EAGO Lighting - Welcome

Fill in the contact form to leave a message 46C Parkway Drive, Rosedale, Auckland 0632
sales@eagolighting.co.nz +64 9 948 6128

Eagousa.com

<https://eagousa.com> > toilets.html



EAGO Toilets

EAGO R-359SEAT Replacement Soft Closing Toilet Seat for TB359 MSRP: \$160.00 Add to Compare

EAGO TB353 One Piece Dual High Efficiency Low Flush Eco-Friendly Toilet MSRP: \$740.00 Add to Compare

Compare EAGO R-353LID Replacement Ceramic Toilet Lid for TB353 MSRP: \$60.00 Add to Compare...

[4] Wilhelm, M.E. and Stuber, M.D.

[5] Wang, C., Wilhelm, M.E., and St

23).



Should you use JuMP?

When should you not use JuMP?

JuMP supports a broad range of optimization classes. However, there are still some that it doesn't support, or that are better supported by other software packages.

You want to optimize a complicated Julia function

Packages in Julia compose well. It's common for people to pick two unrelated packages and use them in conjunction to create novel behavior. JuMP isn't one of those packages.

If you want to [optimize an ordinary differential equation](#) from [DifferentialEquations.jl](#) or tune a neural network from [Flux.jl](#), consider using other packages such as:

- [Optim.jl](#)
- [Optimization.jl](#)
- [NLPModels.jl](#)
- [Nonconvex.jl](#)

[6] https://jump.dev/JuMP.jl/stable/should_i_use/#When-should-you-not-use-JuMP?



Motivation

Dynamic Optimization

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{\text{act}} - I_i^{\text{ref}})^2$$

$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{\text{act}} = x_{A,i} + \frac{2}{21}x_{B,i} + \frac{2}{21}x_{D,i}$$

$$\frac{dx_A}{dt} = k_1 x_E x_T - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_4 x_A^2$$

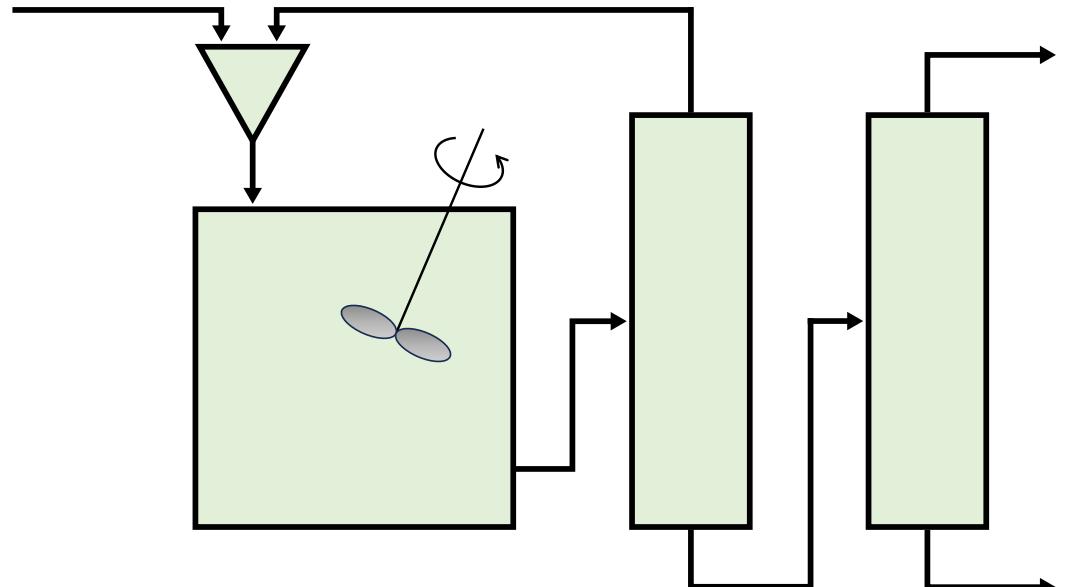
$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{2f}}{K_2} + k_5 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_E}{dt} = -k_1 x_E x_T$$

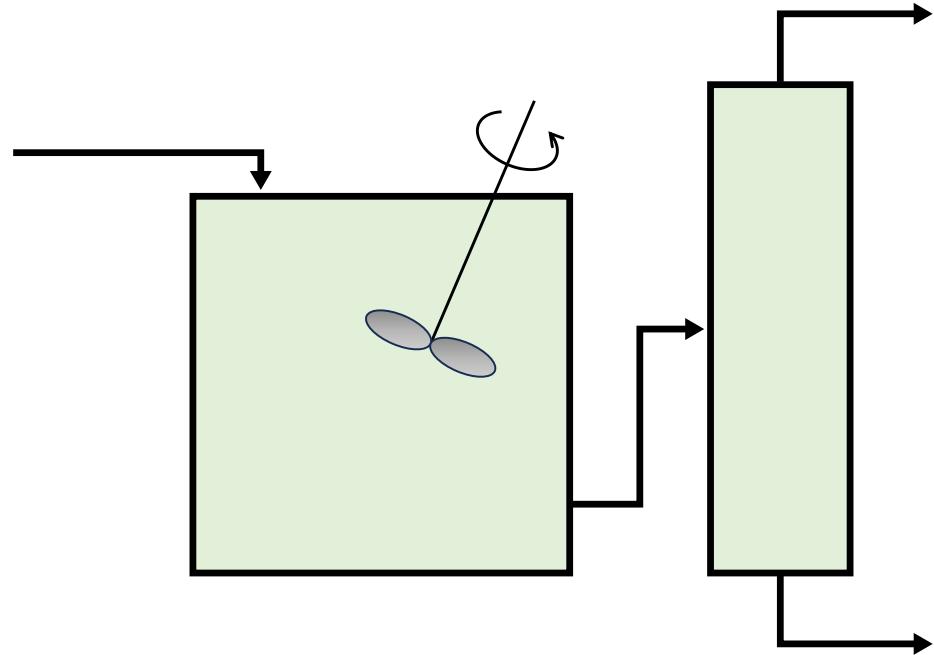
$$\frac{dx_T}{dt} = -k_7 x_E x_T$$

Process Flow Sheets



Causal vs Acausal Modeling

Causal/Sequential-Modular



Acausal/Equation-Oriented

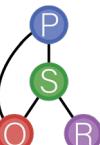
$$y_{2,A} + y_{2,B} + y_{2,C} = 1$$

$$y_{2,B}F = y_{1,B} + Vr_B$$

$$y_{2,C}F = y_{1,C} + Vr_C$$

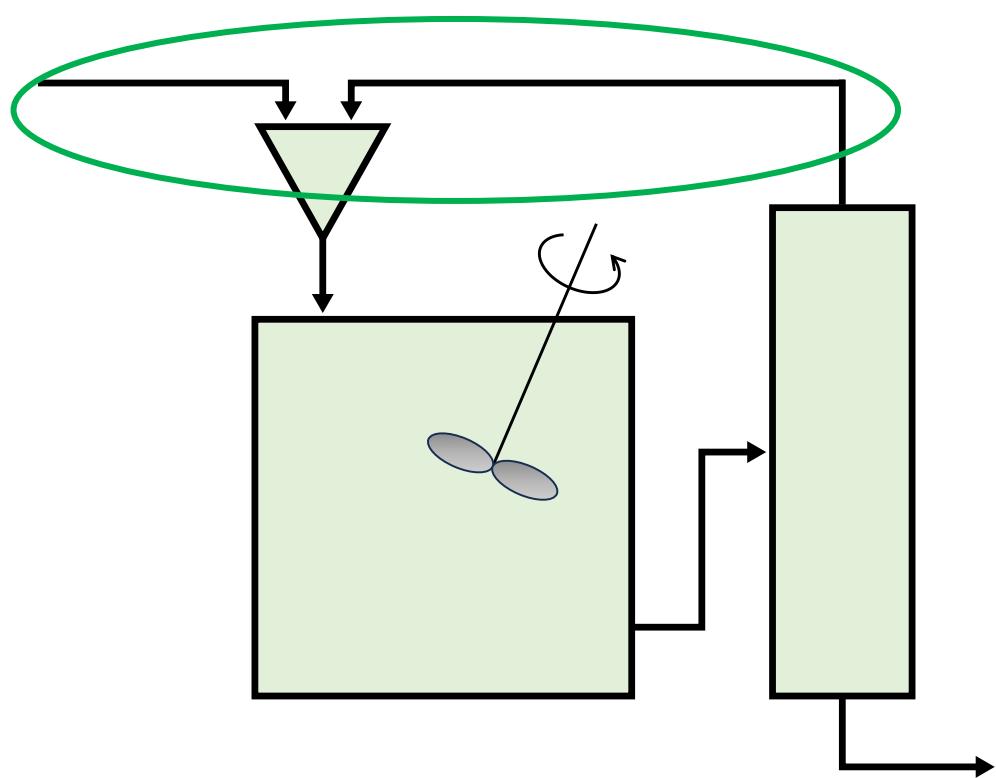
$$y_{3,A} = y_{1,A} - Vr_A$$

$$y_{4,B} + y_{4,C} = y_{2,B} + y_{2,C}$$



Causal vs Acausal Modeling

Causal/Sequential-Modular



Acausal/Equation-Oriented

$$y_{3,A} + y_{3,B} + y_{3,C} = 1$$

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$$y_{3,C}F = y_{2,C} + Vr_C$$

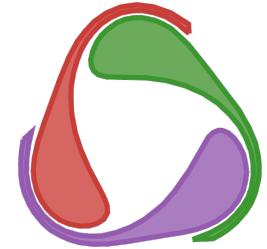
$$y_{4,A} = y_{2,A} - Vr_A$$

$$y_{5,B} + y_{5,C} = y_{3,B} + y_{3,C}$$

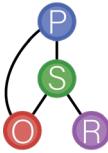
$$y_{2,A} = y_{1,A} + y_{4,A}$$

ModelingToolkit.jl

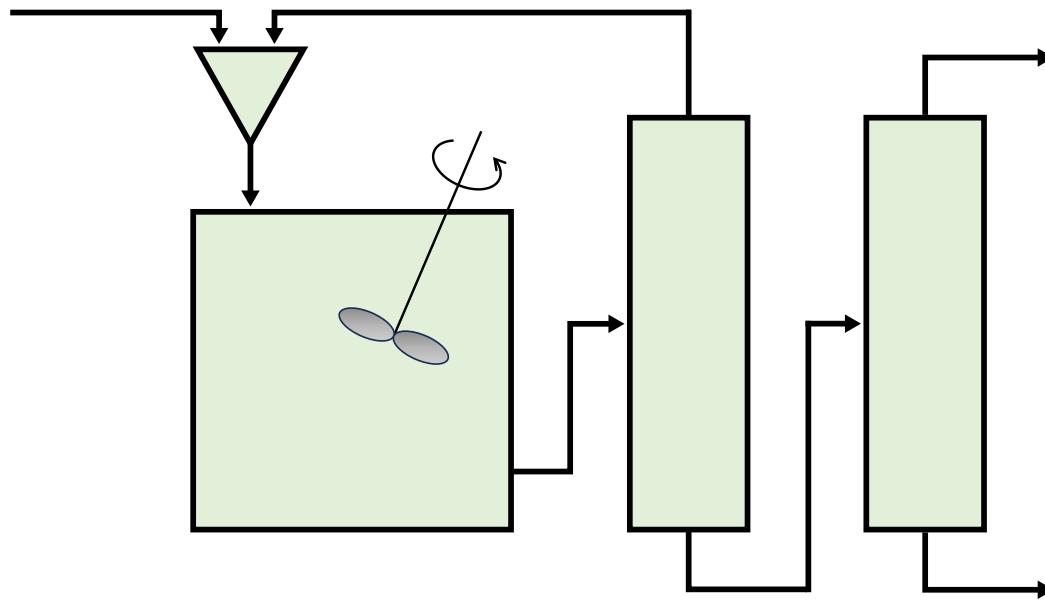
- Open-source, acausal modeling framework in Julia
- Supports a broad range of system types
 - ODEs, SDEs, PDEs
 - Nonlinear systems
 - Optimization problems
- Automatically composes, transforms, and reduces models
 - Dimensionality reduction through algebraic simplification



[8] Ma, Y. et al. Modelingtoolkit: A composable graph transformation system for equation-based modeling. arXiv preprint arXiv:2103.05244 (2021).



Componentized Model



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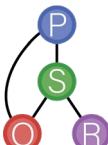
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[6] https://jump.dev/JuMP.jl/stable/should_i_use/#When-should-you-not-use-JuMP?



Optimization.jl

Modeling Optimization Problems

ModelingToolkit.jl is not only useful for generating initial value problems (`ODEProblem`). The package can also build optimization systems.

 Note

The high level `@mtkmodel` macro used in the [getting started tutorial](#) is not yet compatible with `OptimizationSystem`. We thus [have to use a lower level interface to define optimization systems](#). For an introduction to this interface, read the [programmatically generating Systems](#) tutorial.

[9] <https://docs.sciml.ai/ModelingToolkit/stable/tutorials/optimization/>



Optimization in Julia

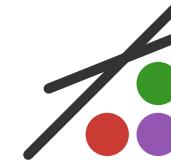
SciML



[10]

- 25+ libraries, 100+ solvers
- No deterministic global optimization support

JuMP

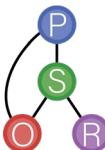


[11]

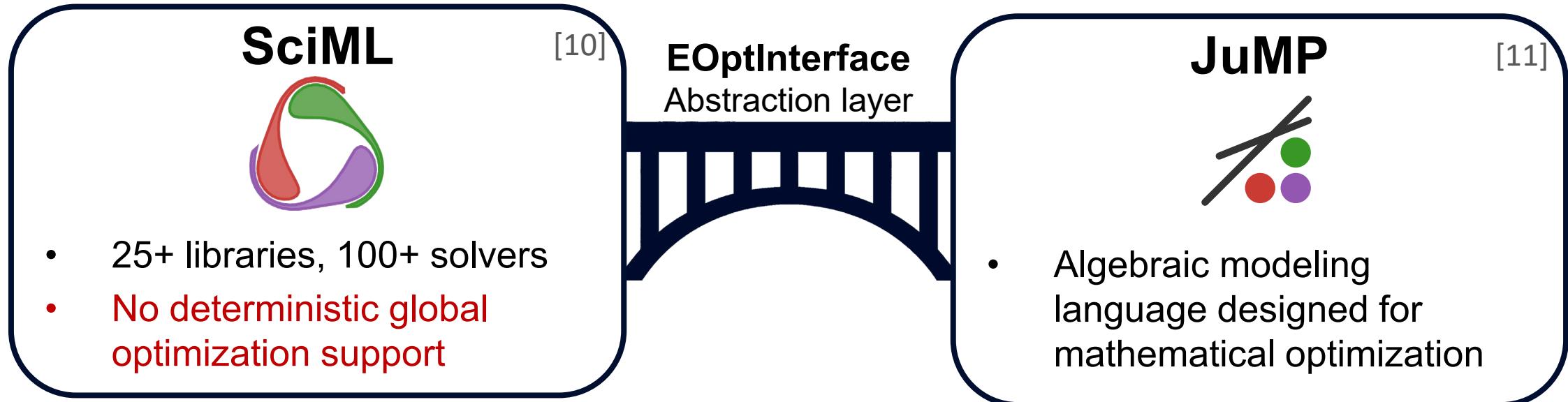
- Algebraic modeling language designed for mathematical optimization

[10] Dixit, V.K. and Rackauckas C. Optimization.jl: A Unified Optimization Package. (2023).

[11] Lubin, M., Dowson, O., Garcia, J.D. et al. JuMP 1.0: recent improvements to a modeling language for mathematical optimization. *Math. Prog. Comp.* 15, 581–589 (2023).



Optimization in Julia



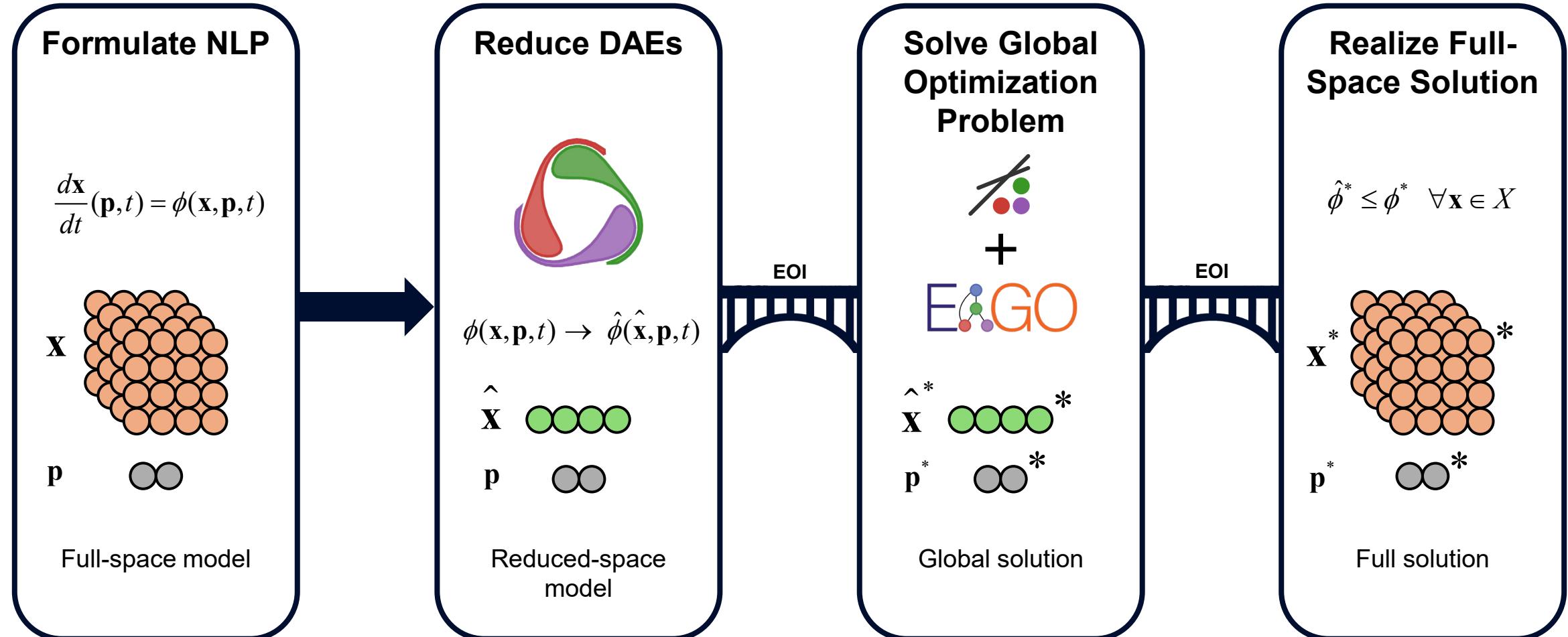
[10] Dixit, V.K. and Rackauckas C. Optimization.jl: A Unified Optimization Package. (2023).

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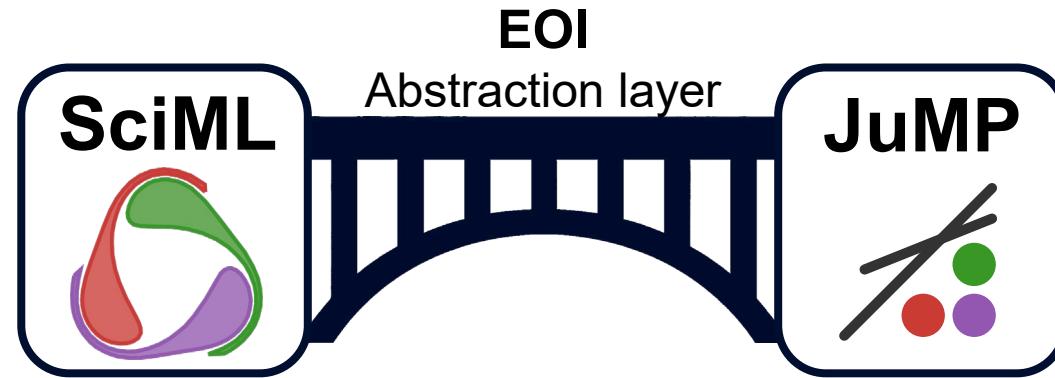
EOptInterface.jl

Equation-oriented Optimization Interface (EOI)



EOptInterface Features

- Automatically generate JuMP constraints from ModelingToolkit models
- Display decision variables
- Detect and directly transcribe ODEs
- Calculate full-space solutions



Case Studies

- 1) Dynamic Kinetic Parameter Estimation
- 2) Steady-State Process Flow Sheet
- 3) Nonlinear Model Predictive Control (NMPC)



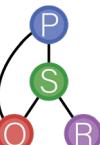
Dynamic Kinetic Parameter Estimation

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$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$
$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$
$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$
$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

[12] Mitsos, A., Chachuat, B., and Barton, P.I. McCormick-based relaxations of algorithms. *SIAM Journal on Optimization*, SIAM. 20:2, 573-601 (2009).



Dynamic Kinetic Parameter Estimation

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$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

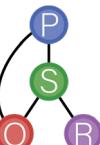
$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

```
@mtkmodel KineticParameterEstimation begin
    @parameters begin
        T = 273.0
        K_2 = 46.0*exp(6500.0/T - 18.0)
        K_3 = 2.0*K_2
        k_1 = 53.0
        k_1s = k_1*1e-6
        k_5 = 1.2e-3
        c_02 = 2e-3

        k_2f
        k_3f
        k_4
    end
    @variables begin
        x_A(t) = 0.0
        x_B(t) = 0.0
        x_D(t) = 0.0
        x_Y(t) = 0.4
        x_Z(t) = 140.0
        I(t)
    end
    @equations begin
        D(x_A) ~ k_1*x_Z*x_Y - c_02*(k_2f + k_3f)*x_A + k_2f/K_2*x_D + k_3f/K_3*x_B - k_5*x_A^2
        D(x_B) ~ c_02*k_3f*x_A - (k_3f/K_3 + k_4)*x_B
        D(x_D) ~ c_02*k_2f*x_A - k_2f/K_2*x_D
        D(x_Y) ~ -k_1s*x_Z*x_Y
        D(x_Z) ~ -k_1*x_Z*x_Y
        I ~ x_A + 2/21*x_B + 2/21*x_D
    end
end
```

[12] Mitsos, A., Chachuat, B., and Barton, P.I. McCormick-based relaxations of algorithms. *SIAM Journal on Optimization*, SIAM. 20:2, 573-601 (2009).



Dynamic Kinetic Parameter Estimation

- EOptInterface

```
if integrator == "Explicit Euler"
    @constraint(model, [j in 1:V, i in 1:(N-1)], xs[j,i+1] == xs[j,i] + t_step*dx[j](xs[:,i]..., ps...))
elseif integrator == "Implicit Euler"
    @constraint(model, [j in 1:V, i in 1:(N-1)], xs[j,i+1] == xs[j,i] + t_step*dx[j](xs[:,i+1]..., ps...))
```



Dynamic Kinetic Parameter Estimation

- EOptInterface

```
if integrator == "Explicit Euler"
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```

- InfiniteOpt

```
problem = JuMPDynamicOptProblem(system, [u0_map; p_map], (t_start, t_end); dt = 0.001)
solution = solve(problem, JuMPCollocation(Iopt.Optimizer, constructRK4()))

problem = InfiniteOptDynamicOptProblem(system, [u0_map; p_map], t_span; steps = 100)
solution = solve(problem, InfiniteOptCollocation(Iopt.Optimizer))
```



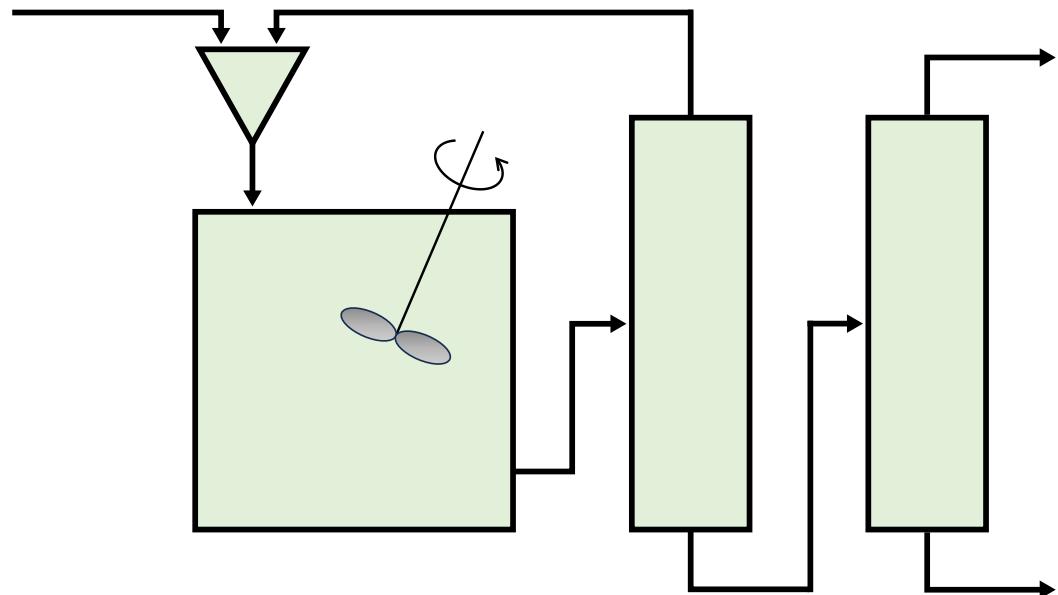
Case Studies

- 1) Dynamic Kinetic Parameter Estimation
 - Direct transcription of ODEs
- 2) Steady-State Process Flow Sheet
- 3) Nonlinear Model Predictive Control (NMPC)



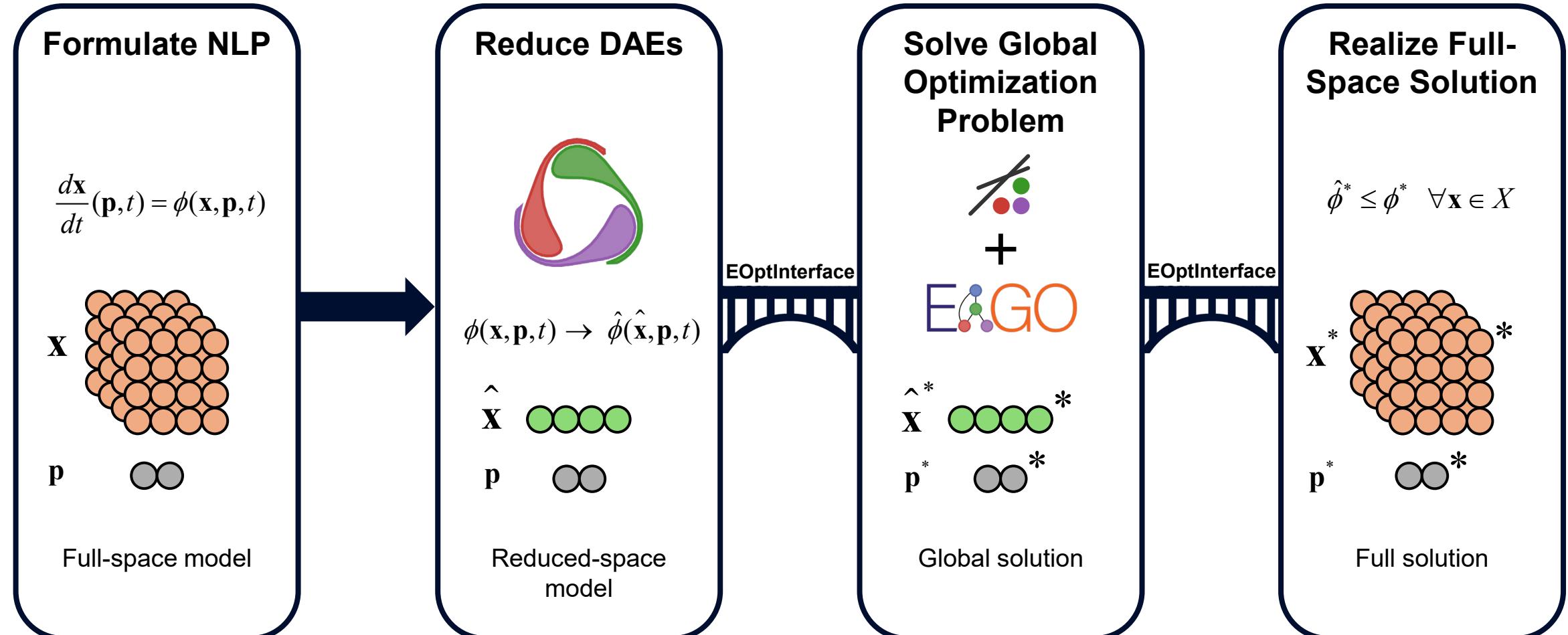
Steady-State Process Flow Sheet

- Minimize total annualized costs
- Design variables:
 - Feed flowrate
 - Reactor volume



[13] Kokossis, A. and Floudas, C.A. Synthesis of isothermal reactor-separator-recycle systems. *Chemical Engineering Science*. 46, 1361-1383 (1991).

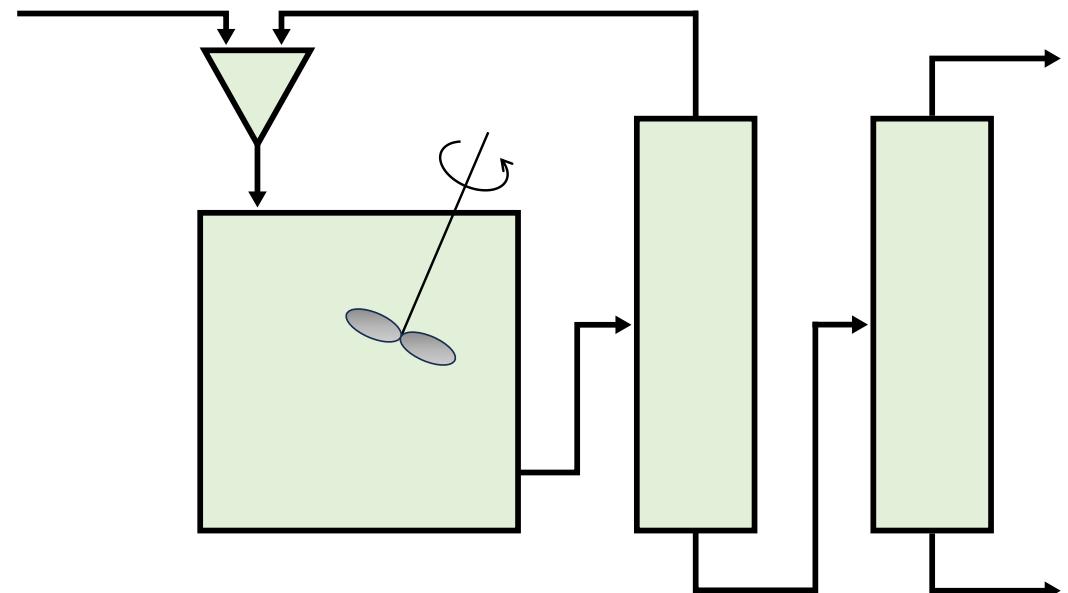
EOI Workflow



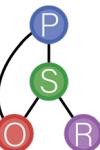
Steady-State Process Flow Sheet

- Minimize total annualized costs
- Design variables:
 - Feed flowrate
 - Reactor volume

Model	Number of variables	Solve Time (s)
Full-space	50	202.0
Reduced-space	6	3.441

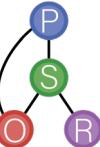


[13] Kokossis, A. and Floudas, C.A. Synthesis of isothermal reactor-separator-recycle systems. *Chemical Engineering Science*. 46, 1361-1383 (1991).

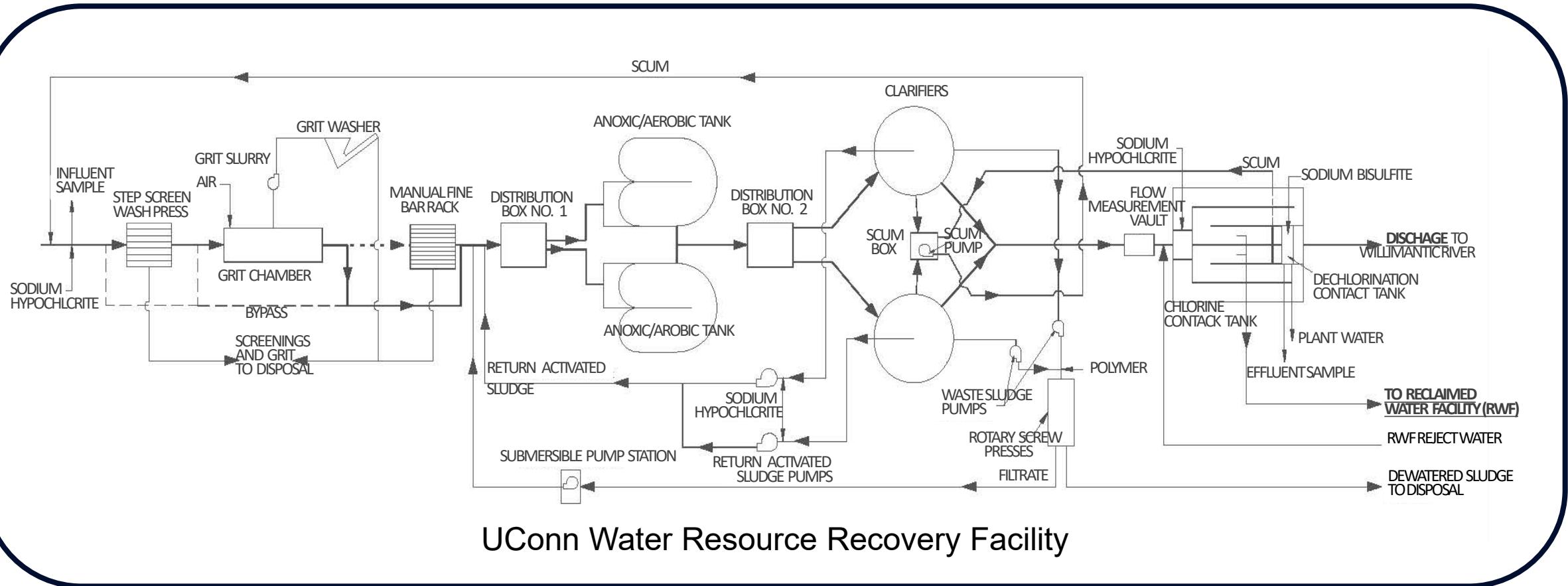


Case Studies

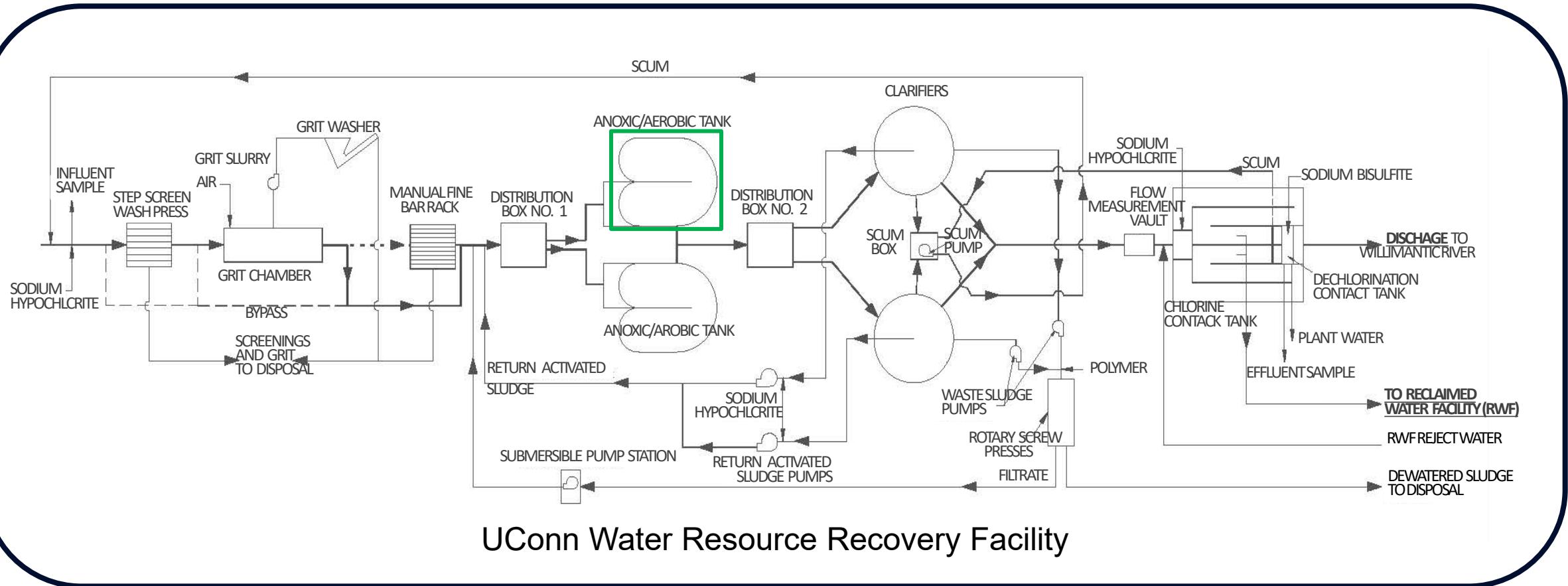
- 1) Dynamic Kinetic Parameter Estimation
 - Direct transcription of ODEs
- 2) Steady-State Process Flow Sheet
 - Exploit dimensionality reduction from ModelingToolkit for optimization
- 3) Nonlinear Model Predictive Control (NMPC)



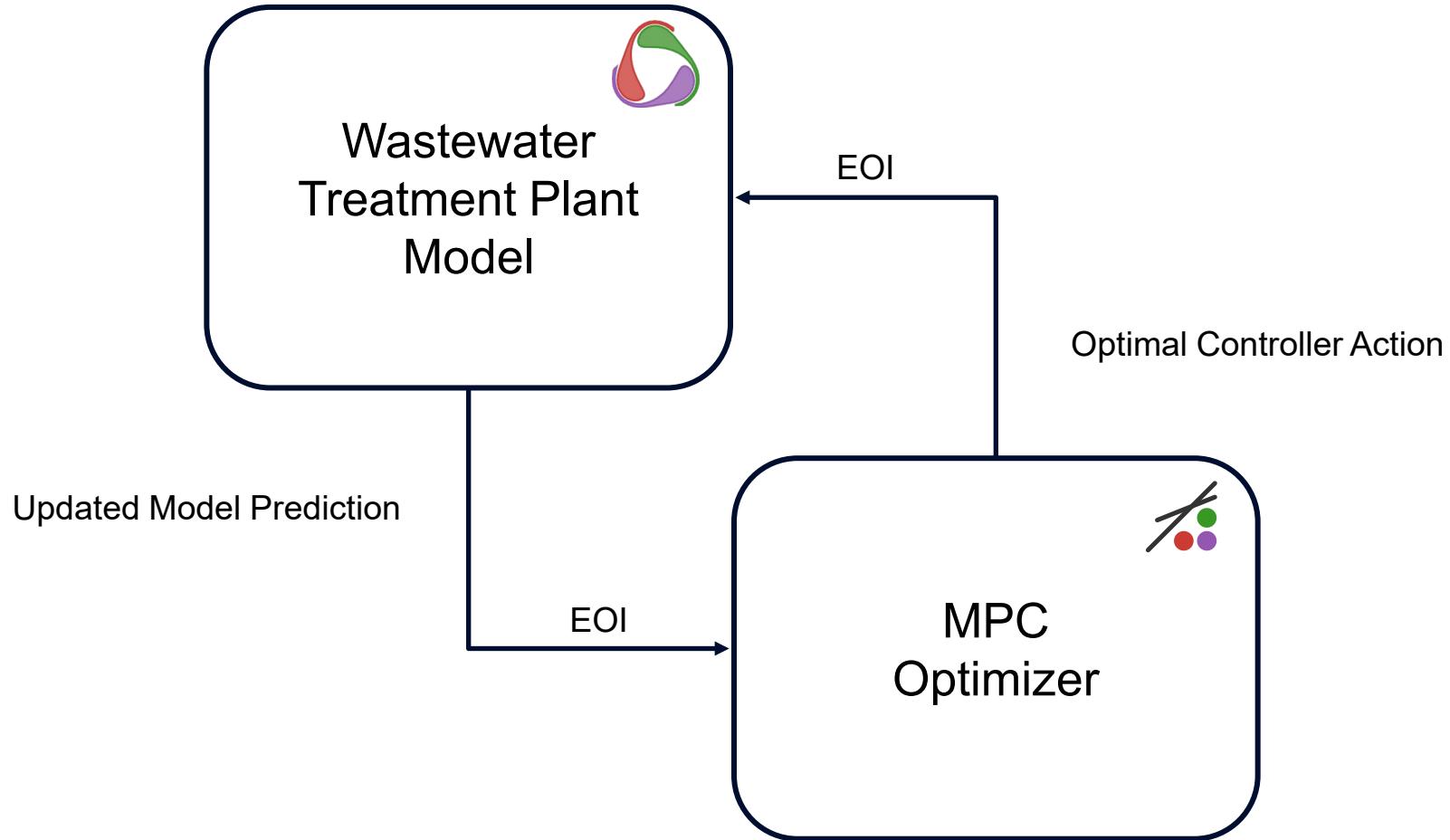
Nonlinear Model Predictive Control



Nonlinear Model Predictive Control



Nonlinear Model Predictive Control



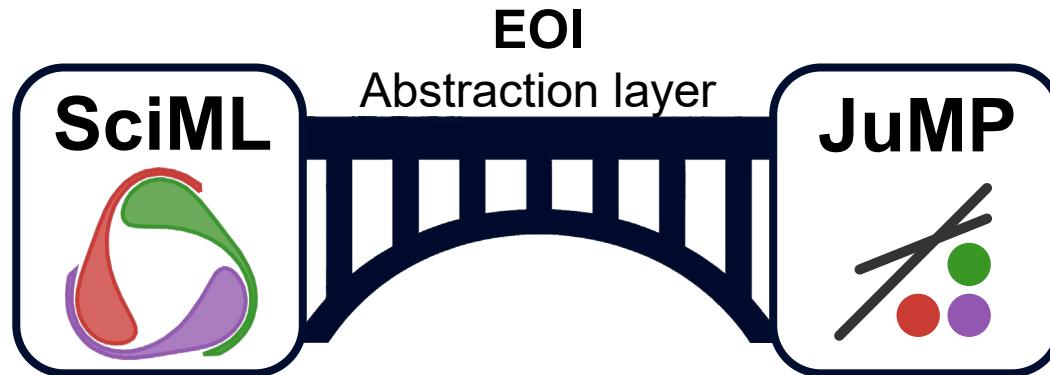
Case Studies

- 1) Dynamic Kinetic Parameter Estimation
 - Direct transcription of ODEs
- 2) Steady-State Process Flow Sheet
 - Exploit dimensionality reduction from ModelingToolkit for optimization
- 3) Nonlinear Model Predictive Control (NMPC)
 - Fully integrated real-time closed-loop NMPC



Conclusion

- **EOptInterface.jl**
 - Seamlessly integrates modeling and simulation with formal optimization
 - Contains multiple discretization methods for ODEs
 - You can use your favorite solver in JuMP



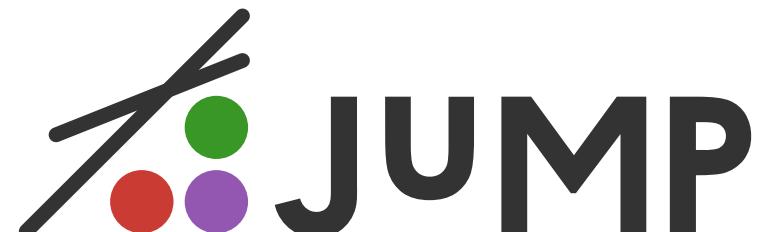
- **Future Work**
 - EAGODynamicOptimizer.jl

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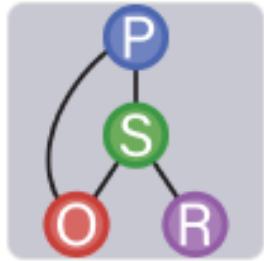
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Questions?



Process Systems and Operations Research Laboratory

The PSOR Laboratory at UConn develops numerical analysis methods and software for process systems engineering applications.

22 followers

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