Polynomial pole placement - part 2

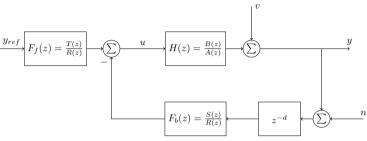
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Goal of today's lecture

Understand the design procedure of polynomial pole placement

Two-degree-of-freedom controller



$$Y(z) = \frac{F_f(z)H(z)}{1 + z^{-d}F_b(z)H(z)}Y_{ref}(z) + \underbrace{\frac{S_s(z)}{1}}_{1 + z^{-d}F_b(z)H(z)}V(z) - \underbrace{\frac{z^{-d}F_b(z)H(z)}{1 + z^{-d}F_b(z)H(z)}}_{I + z^{-d}F_b(z)H(z)}N(z)$$

Evidently $S_s(z) + T_s(z) = 1$ Conclusion: One must find a balance between disturbance rejection and noise attenuation.

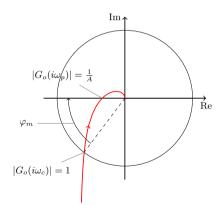


The sensitivity function

$$S_s(z) = \frac{1}{1 + z^{-d}F_b(z)H(z)} = \frac{1}{1 + G_o(z)} = \frac{1}{G_o(z) - (-1)}$$

$$|S_s(e^{i\omega h})| = |S_s(i\omega)| = \frac{1}{|G_o(i\omega) - (-1)|}$$

The magnitude of the sensitivity function is inverse proportional to the distance of the Nyquist curve to the critical point -1



The design procedure

The design procedure

Given plant model $H(z) = \frac{B(z)}{A(z)}$ and specifications on the desired closed-loop poles $A_{cl}(z)$

1. Find polynomials R(z) and S(z) with $n_R \ge n_S$ such that

$$A(z)R(z)z^d + B(z)S(z) = A_{cl}(z)$$

2. Factor the closed-loop polynomial as $A_{cl}(z) = A_c(z)A_o(z)$, where $n_{A_o} \leq n_R$. Choose

$$T(z)=t_0A_o(z),$$

where $t_0 = \frac{A_c(1)}{B(1)}$.

The control law is then

$$R(q)u(k) = T(q)u_c(k) - S(q)y(k).$$

The closed-loop response to the command signal is given by

$$A_c(q)y(k) = t_0B(q)u_c(k).$$



Determining the order of the controller

With Diophantine equation

$$A(z)R(z)z^d + B(z)S(z) = A_{cl}(z) \qquad (*)$$

and feedback controller

$$F_b(z) = \frac{S(z)}{R(z)} = \frac{s_0 z^n + s_1 z^{n-1} + \dots + s_n}{z^n + r_1 z^{n-1} + \dots + r_n}$$

How should we choose the order of the controller? Note:

- ▶ the controller has $n + n + 1 = 2 \deg R + 1$ unknown parameters
- ▶ the LHS of (*) has degree deg $(A(z)R(z)z^d + B(z)S(z)) = \deg A + \deg R + d$
- ► The diophantine gives as many (nontrivial) equations as the degree of the polynomials on each side when we set the coefficients equal.
 - \Rightarrow Choose deg R so that $2 \deg R + 1 = \deg A + \deg R + d$



Determining the order of the controller - Exercise

With the plant model

$$H(z) = \frac{B(z)}{A(z)} = \frac{b}{z+a}$$

and d = 0 (no delay), what is the appropriate degree of the controller

$$F_b(z) = \frac{S(z)}{R(z)} = \frac{s_0 z^n + s_1 z^{n-1} + \dots + s_n}{z^n + r_1 z^{n-1} + \dots + r_n}$$

so that all parameters can be determined from the diophantine equation

$$A(z)R(z) + B(z)S(z) = A_c(z)A_o(z)?$$

1.
$$n = 0$$
 2. $n = 1$

3.
$$n = 2$$
 4. $n = 3$

Determining the order of the controller - Exercise - Solution

With the plant model

$$H(z) = \frac{B(z)}{A(z)} = \frac{b}{z+a}$$

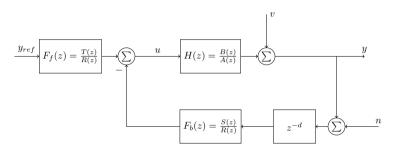
and d = 0 (no delay), what is the appropriate degree of the controller

$$F_b(z) = \frac{S(z)}{R(z)} = \frac{s_0 z^n + s_1 z^{n-1} + \dots + s_n}{z^n + r_1 z^{n-1} + \dots + r_n}$$

so that all parameters can be determined from the diophantine equation

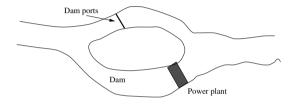
$$A(z)R(z) + B(z)S(z) = A_c(z)A_o(z)$$
?
1. $n = 0$ 2.
3. 4.

Two-degree-of-freedom controller, the importance of the observer poles

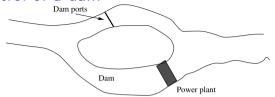


$$Y(z) = \frac{t_0 B(z) z^d}{A_c(z)} Y_{ref}(z) + \frac{A(z) R(z) z^d}{A_c(z) A_o(z)} V(z) - \frac{S(z) B(z)}{A_c(z) A_o(z)} N(z)$$

Conclusiones 1) There is a partial separation between designing for reference tracking and designing for perturbance rejection. 2) The observer poles (the roots of $A_o(z)$) can be used to determine a balance between disturbance rejection and noise attenuation.

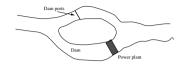


Objective Design a control system to maintain the water level under influence of disturbances.



Amount of water in dam:
$$x(t) = x_0 + y(t)$$

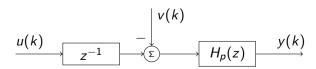
Flow through dam ports: $f(t) = f_0 - u(t)$
Uncontrolled flows out: $d(t) = f_p(t) - f_i(t) = d_0 + v(t)$
Dynamics: $\frac{d}{dt}x(t) = \frac{d}{dt}y(t)$
 $= -f(t) - d(t) = -f_0 - d_0 + u(t) - v(t)$



Discrete-time process dynamics

Deviation in the level of water y(k) = y(k-1) - v(k-1) + u(k-2)

Deviation in the non-controlled flows

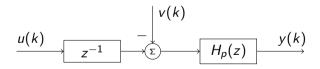


The process dynamics

Deviation in the level of water

$$y(k) = y(k-1) - v(k-1) + u(k-2)$$

Deviation in the non-controlled flows



Activity What is the transfer function from u(k) to y(k)?

1:
$$H(z) = \frac{z}{z-1}$$
 2: $H(z) = \frac{1}{z-1}$ 3: $H(z) = \frac{1}{z(z-1)}$

Given process $H(z) = \frac{B(z)}{A(z)} = \frac{1}{z(z-1)}$ and desired poles in z = 0.9.

1. The Diophantine equation $A(z)R(z)z^d + B(z)S(z) = A_{cl}(z)$

$$z(z-1)R(z) + S(z) = A_{cl}(z)$$

The order of the controller is

$$\deg R = \deg A + d - 1 = 2 - 1 = 1, \quad \Rightarrow \quad F_b(z) = \frac{S(z)}{R(z)} = \frac{s_0 z + s_1}{z + r_1}$$

2. Resulting Diophantine equation

$$z(z-1)(z+r_1)+s_0z+s_1=A_{cl}(z)$$

The degree of $A_{cl}(z)$ is 3. Choose $A_o(z) = z$, (deg $A_o = \deg R$)

$$A_{cl}(z) = A_o(z)A_c(z) = z(z - 0.9)^2$$



3. From the Diophantine equation

$$z(z-1)(z+r_1) + s_0z + s_1 = z(z-0.9)^2$$
$$z^3 + (r_1-1)z^2 - r_1z + s_0z + s_1 = z^3 - 1.8z^2 + 0.81z$$

we obtain the equations

$$\begin{cases} z^2 : & r_1 - 1 = -1.8 \\ z^1 : & -r_1 + s_0 = 0.81 \\ z^0 : & s_1 = 0 \end{cases} \Rightarrow \begin{cases} r_1 = -0.8 \\ s_0 = 0.01 \\ s_1 = 0 \end{cases}$$
$$F_b(z) = \frac{0.01z}{z_0 - 0.8}$$

4. We have $A_o(z) = z$, so

$$T(z) = t_0 A_o(z) = t_0 z$$
 $G_c(z) = rac{T(z)B(z)}{A_o(z)A_c(z)} = rac{t_0 B(z)}{A_c(z)}, \quad ext{queremos } G_c(1) = 1$
 $t_0 = rac{A_c(1)}{B(1)} = rac{(1-0.9)^2}{1} = 0.01$

Control law

$$R(q)u(kh) = T(q)u_c(kh) - S(q)y(kh)$$

$$(q - 0.8)u(kh) = 0.01 q u_c(kh) - 0.01 q y(kh)$$

$$u(kh + h) = 0.8u(kh) + 0.01u_c(kh + h) - 0.01y(kh + h)$$